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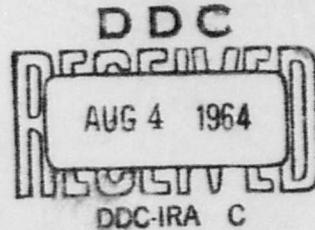
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ARGON-OXYGEN-NITROGEN THREE COMPONENT SYSTEM EXPERIMENTAL VAPOR-LIQUID EQUILIBRIUM DATA

TECHNICAL DOCUMENTARY REPORT NO. APL TDR 64-64
APRIL 1964

AF Aero Propulsion Laboratory
Research and Technology Division
Air Force Systems Command
Wright-Patterson Air Force Base, Ohio

PROJECT NO. 3048, TASK NO. 30193



(Prepared under Contract No. AF 33(657)-8742
by Air Products and Chemicals, Inc., Research and
Development Department, Allentown, Pa.; G. M. Wilson,
P. M. Silverberg, and M. G. Zellner, authors)

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FOREWORD

This report summarizes all work done under contract to the Air Force for the experimental determination of vapor-liquid equilibrium in argon, oxygen, and nitrogen mixtures from July 15, 1962 to April 8, 1964.

The following persons were contributing authors on this subject:

L. Israel - literature search and many useful computer programs.

A. Jambhekar - mixture virial coefficients.

C. J. Sterner - former director of the vapor-liquid laboratory.

P. Fennema - improved chromatographic analysis.

This report is dedicated to that hardy band of technicians who ran the equipment two shifts for a seemingly endless ten months. Our thanks go to E. Frederick, R. Gotthardt, J. Wallace, C. Worman, and especially to H. Donat whose perserverance, unfailing precision, and mechanical ability helped pull us over many rough spots.

ABSTRACT

This Final Technical Documentary Report presents the results from July 15, 1962 to April 15, 1964 as covered by the contract for the experimental determination of vapor-liquid equilibrium data in argon, oxygen, and nitrogen mixtures. The experimental apparatus and procedures are described. The experimental data at 26, 23, 20, 18, 16, 14, 12, 10, 8, 6, 4, 2 and 1 atmosphere levels are presented. A correlation of our experimental data is made. Plots and tables of equilibrium constants, relative volatilities and activity coefficients are presented. Experimental and calculated results are compared and a comparison of the data to the literature is made. Analytical enthalpy data is presented.

The correlation reproduces the experimental data with an error less than 2.5%; being worst at 20 atmospheres and best at 6 atmospheres.

This Technical Documentary Report has been reviewed and is approved.

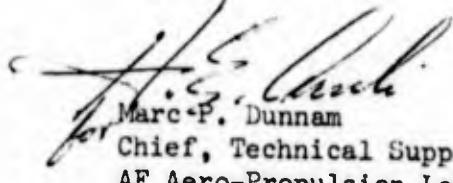

Marc P. Dunnam
Chief, Technical Support Division
AF Aero-Propulsion Laboratory

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I. INTRODUCTION

This project, under contract with the U. S. Air Force, was undertaken to measure and correlate vapor-liquid equilibrium data in binary and ternary mixtures of oxygen, nitrogen, and argon. This project was undertaken because much of the existing data are reported only for low pressures and few data have been obtained in the ternary system. The measurements of this project establish the vapor-liquid equilibrium properties of the oxygen-nitrogen-argon system over a wide range of pressures and over the entire range of binary and ternary compositions. One thousand nine hundred and sixty two data points were measured and this system may well be one of the most thoroughly studied ternary systems to date.

The project effort was divided into three parts as follows:

1. A literature search for existing data.
2. The measurement of vapor-liquid equilibrium data at the following combinations of pressures and compositions. The actual compositions measured are in only approximate agreement with the listed compositions and, therefore, more than one run was sometimes made in a given concentration region.

<u>Pressure, Atm</u>	<u>Mole Ratio</u>	<u>Mole Fraction Argon</u>
	$N_2/(N_2 + O_2)$	
1	0	0
2	0.10	0.01
4	0.20	0.02
6	0.40	0.03
8	0.60	0.04
10	0.80	0.05
12	0.90	0.07
14	0.97	0.10
16	1.00	0.20
18	-----	0.40
20	-----	0.60
23	-----	0.80
26	-----	0.90

3. The thermodynamic correlation of the equilibrium data and the analytical determination of enthalpy data.

This report summarizes:

1. The results of the literature search.
2. A bibliography of existing vapor-liquid equilibrium, enthalpy, and related data of the oxygen-nitrogen-argon system.
3. A description of the experimental apparatus.
4. Tables of the experimental data.
5. A thermodynamic correlation of the data.
6. Tables and figures of derived vapor-liquid equilibrium and enthalpy data.

The experimental data are accurate to within $\pm 0.5\%$ in the pressure and $\pm 1\%$ in the relative volatility. By smoothing the data it is possible to obtain equilibria accurate to $\pm 0.5\%$ in the relative volatility. The thermodynamic correlation of the data is not quite as accurate as the experimental data due to a weakness in the correlation method at temperatures above the critical temperature of nitrogen and at pressures near the critical point of a mixture. The largest difference between the correlation and the experimental data appears to be at 20 atmospheres where the calculated pressure and relative volatilities deviate 2.5% from the experimental data. This accuracy is satisfactory for most process design calculations, but it may be desirable on occasion to interpolate directly from the experimental data.

II. LITERATURE SEARCH

A literature search was made to obtain all existing data relating to vapor-liquid equilibrium and enthalpy of the oxygen-nitrogen-argon system. The search included the following sources of information.

1. Chemical Abstracts (January 1957 - December 1962).
2. Chemical Titles (January 1961 - May 1963).
3. Armed Services Technical Information Agency (ASTIA) - A complete search of the ASTIA collection was obtained (to September 1963).
4. Cryogenic Data Center - NBS Cryogenic Engineering Laboratory, Boulder, Colorado - Two searches to January 1963 and to October 1963.
5. Existing bibliographies on the subject:
 - a. "The Compendium", Johnson, V. J. (ed.), WADD Tech. Rept. 60-56, (1961).
 - b. E. F. Yendall and Olzewski, W. J., "Saturation Properties of Oxygen-Nitrogen Mixtures", ASD Technical Rept. 61-536, Sept. 1961.
 - c. Ju Chin Chu, et al, Vapor Liquid Equilibrium Data, J. W. Edwards Co., Ann Arbor, Michigan, 1956.
 - d. E. Hala, et al, Vapor-Liquid Equilibrium, Pergamon, New York, 1958.
 - e. G. A. Cook, ed., Argon, Helium, and the Rare Gases, Vol. II, Interscience, New York, 1961.
 - f. J. Timmermans, Physico-Chemical Constants of Binary Systems, Interscience, New York, 1960.

A bibliography of the data is given in the Appendix according to the following categories:

- A. Vapor-Liquid Equilibrium Data Nitrogen-Oxygen System
- B. Vapor-Liquid Equilibrium Data Nitrogen-Argon System
- C. Vapor-Liquid Equilibrium Data Argon-Oxygen System

- D. Vapor-Liquid Equilibrium Data Nitrogen-Oxygen-Argon Ternary System
- E. Enthalpy Data
- F. Pressure-Volume-Temperature Data for Gaseous Mixtures of N₂-O₂-Ar (including air) used in checking the virial coefficients
- G. Vapor Pressure Data
- H. Miscellaneous References

From this search it is concluded that few vapor-liquid equilibrium data exist in three principal areas, namely:

- 1. Few data exist for the nitrogen-argon binary system.
- 2. Few data exist above pressures of 5 to 10 atmospheres.
- 3. Few data exist for the argon-oxygen-nitrogen ternary system.

From the search for enthalpy data it is concluded that:

- 1. Heat of mixing data for the binaries of the oxygen-nitrogen-argon system are reported only at low temperatures.
- 2. Latent heat data are reported in terms of correlations based principally on vapor pressure data. Except for argon the data appear to be satisfactory, but in the case of argon there appears to be little experimental data to back up the correlated data.

III. EXPERIMENTAL APPARATUS AND PROCEDURE

A. Recirculation System

A schematic flow diagram of the equilibrium apparatus⁽¹⁾ is presented in Figure 1. The elements which make up the complete apparatus consist of: equilibrium cell, recirculation pump, closed recirculation loop, constant-temperature bath, system pressure gauge, cell thermocouple, liquid sampling line, gas sampling coil, system volume regulator, charging manifold, vacuum pump and numerous subsidiary equipment such as valves, gauges, etc. A photograph of the apparatus is presented in Figure 2 showing the cell barricade, pressure gauges, volume regulator and temperature controller.

The recirculation method is one of the standard laboratory techniques for obtaining accurate vapor-liquid equilibrium data at temperatures below ambient. With this method, a cell partly full of liquid and of appreciable volume is maintained at a constant operating temperature. The vapor inside the cell is drawn out of the top of the cell, warmed to ambient temperature, passed through a pump which increases the pressure of the vapor slightly, cooled back to the cell temperature and introduced to the bottom of the cell. The recirculated vapor bubbles through the liquid to the vapor space and continues the cycle through the system. As the vapor bubbles through the liquid, the liquid is agitated and the liquid and vapor approach equilibrium. When equilibrium is achieved, portions of the vapor and of the liquid are withdrawn from the system and analyzed for chemical compositions.

In this apparatus, the vapors warm to ambient temperature in exposed tubing, recirculate by use of an electromagnetic pump⁽²⁾ and cool to cell temperature in a coil of tubing which is immersed in the constant-temperature bath.

B. Equilibrium Cell

A schematic diagram of the equilibrium cell is shown on Figure 3. The equilibrium cell is a vertical cylindrical tube made of laminated glass which is sealed at both ends by Teflon gaskets supported by end flanges. The end flanges are connected to each other by tie-rods outside of the cell. The glass tube, which is usable at pressures up to 800 psia and temperatures to -340°F, is 3/8 in. ID, 11/16 in. OD and 3-1/2 in. long with squared-off ends ground flat and fire-polished. The liquid sampling line and the three-element thermocouple both enter the equilibrium cell at the top through the 1/4 in. OD vapor outlet line. The recirculated vapor enters the cell through small holes in a distributor plate which caps the inlet line. Inside the cell the flow of bubbles from the vapor inlet is broken up by a series of horizontal screens. Near the top of the cell, a plug of fiberglass prevents carryover of entrained liquid.

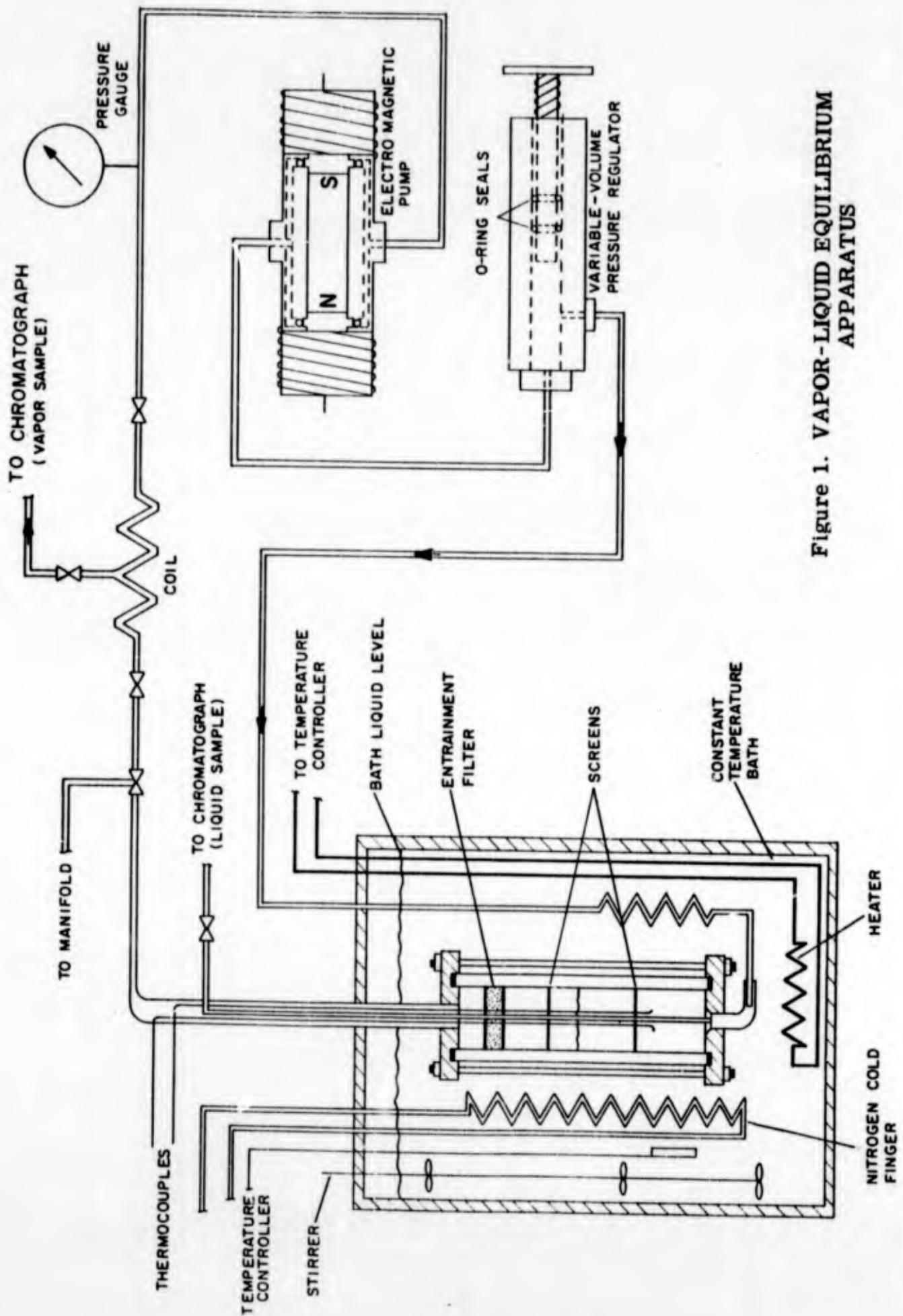


Figure 1. VAPOR-LIQUID EQUILIBRIUM APPARATUS

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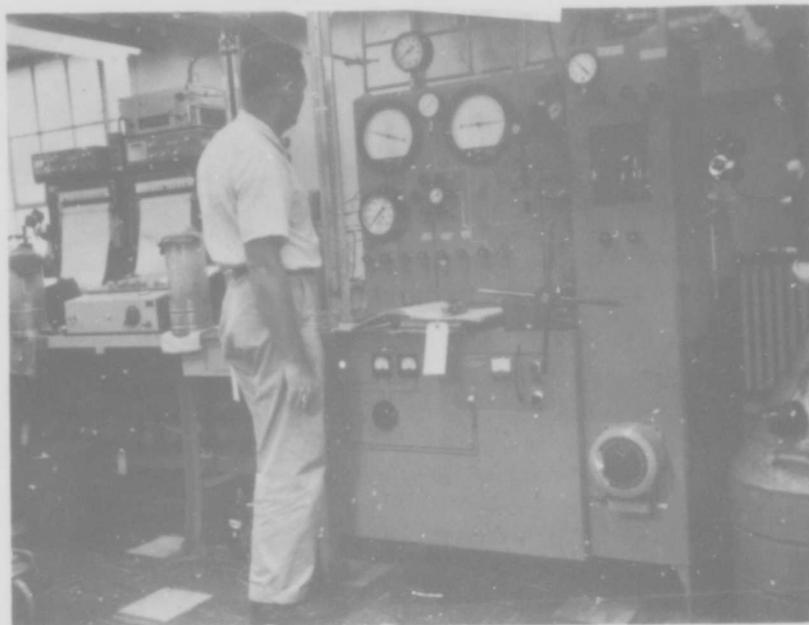


FIGURE 2. FRONT VIEW OF EQUILIBRIUM APPARATUS

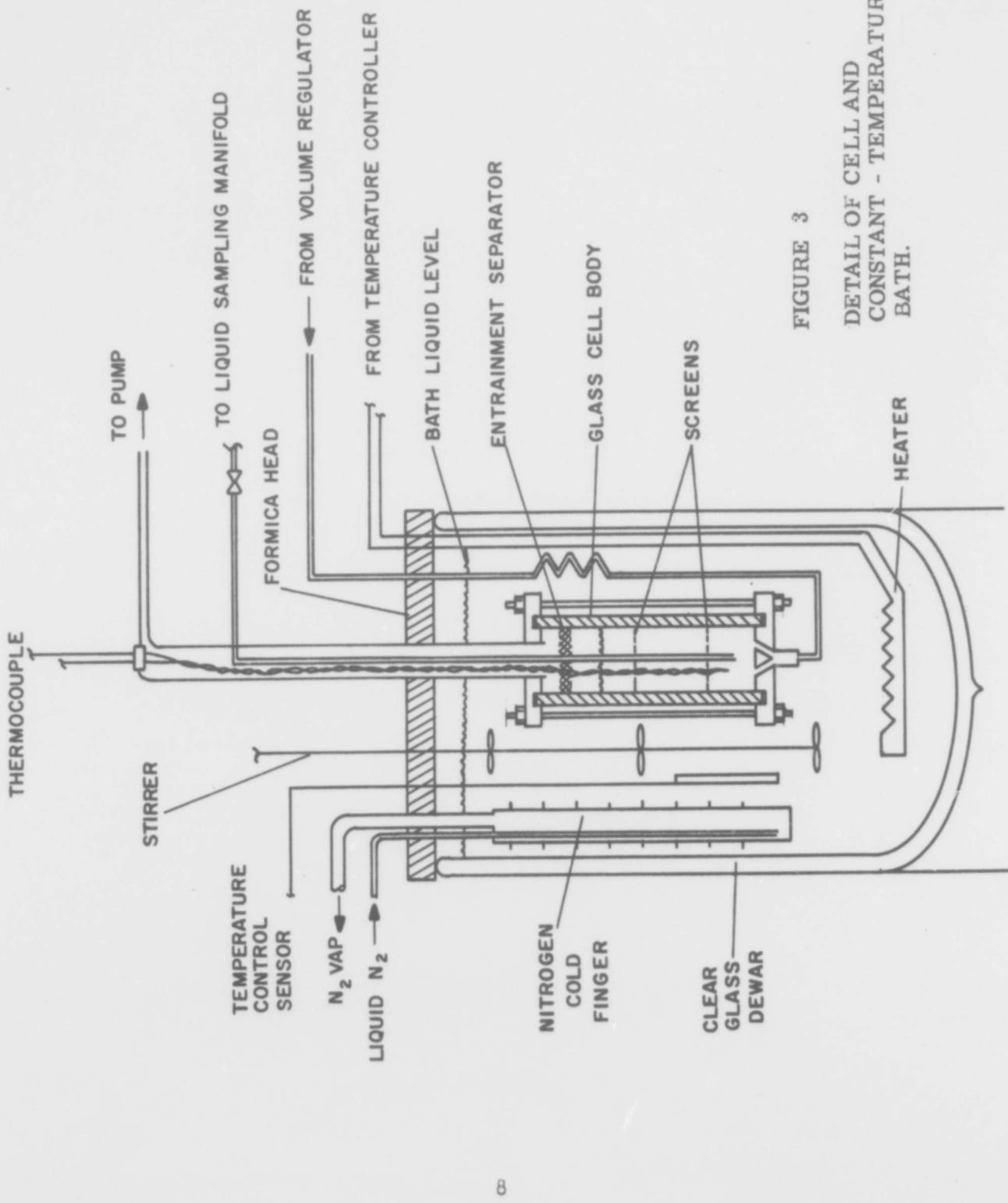


FIGURE 3

DETAIL OF CELL AND
CONSTANT - TEMPERATURE
BATH.

The equilibrium cell is immersed in a constant-temperature liquid bath which is contained in a clear glass dewar vessel. The dewar is supported on a pedestal within a steel barricade which is open top and bottom. The equilibrium cell is illuminated and may be viewed while operating through the clear dewar and a safety glass window in the barricade. A photograph of the cell and bath are shown in Figure 4.

C. Constant-Temperature Bath

The constant-temperature bath in which the equilibrium cell is immersed may be any of one of several fluids, depending on the operating temperature. From the highest temperature covered down to -301°F , Freon-13* was used. Liquid argon was used down to -308°F . Liquid nitrogen was used down to -320°F .

The temperature of the bath liquid is controlled to within $\pm 0.01^{\circ}\text{F}$ by use of a proportional electronic controller. The bath is cooled by liquid nitrogen which flows into a "cold finger" at a constant rate and evaporates. The temperature of the bath is adjusted to operating conditions by passing an electrical current through a resistance heating element immersed in the bath. The heating current is regulated by the controller which receives temperature information from a platinum resistance thermometer which is immersed in the bath. The bath liquid is kept agitated by a motor-driven stirrer. Two additional thermocouples in the bath are used to determine the bath temperature and to check on the controller action.

D. Operating Procedure

Routine operation of the equilibrium apparatus begins with the cell at room temperature and the entire system under vacuum. Precooled bath liquid is added to the dewar vessel and the cell is cooled down to the operating temperature. Measured quantities of the component gases are introduced to the system, one component at a time, generally starting with nitrogen. The quantities of gas added are calculated beforehand and measured by pressure changes in a volume-calibrated manifold. Before any component is allowed to enter the manifold, the manifold is evacuated and purged with the appropriate gas. The recirculation pump is turned on while the components are being introduced and continues to operate until it is time to sample. When all components have been added to the system, slight adjustments of the pressure and liquid volume are made by adding small additional quantities of the appropriate component. After the desired liquid volume has formed and the pressure is established at the proper level, the apparatus is permitted to operate at constant temperature and pressure for approximately one half hour before taking samples. The sampling procedures are described under "E. Sampling Systems".

*E.I. DuPont de Nemours Inc. registered trademark.

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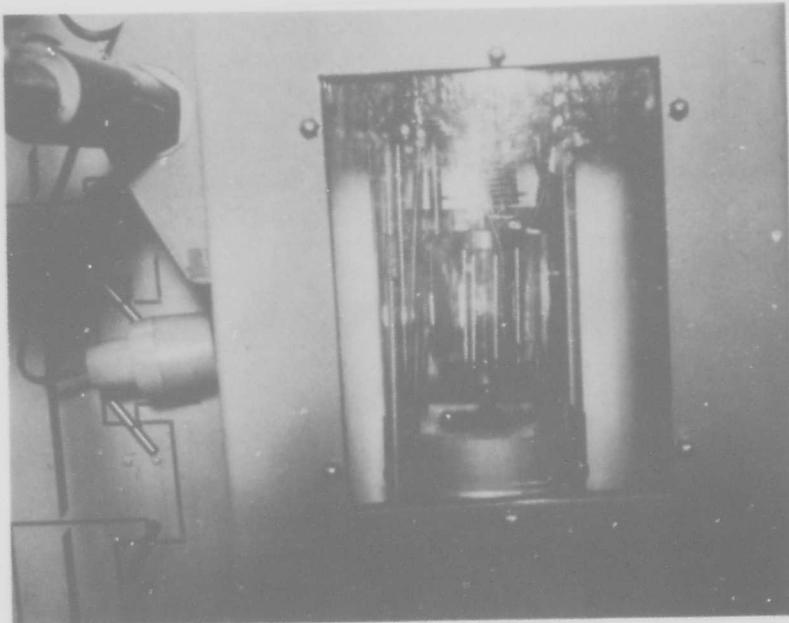


FIGURE 4. CLOSE-UP OF THE EQUILIBRIUM CELL AND
CONSTANT TEMPERATURE BATH.

The cell is the long cylinder upright in the center of the dewar.

Normally, after the samples have been taken, the pressure is released from the system, the bath liquid is recovered from dewar and the cell is allowed to warm to room temperature. The system is then evacuated and allowed to remain under vacuum overnight to be ready for operation the next day. Since more than one run is made per day, it was not necessary to allow the cell to warm up between runs on a particular day, but only at the last run.

E. Sampling Systems

After one-half hour of operation, the recirculating pump is stopped and the system pressure is recorded. At this time, a large proportion of the vapor in the system remains in the vapor sampling coil which is part of the recirculation loop. Valves at the end of this sampling coil are closed to isolate the coil from the rest of the system. When these valves are closed, gas samples can be removed at anytime from the coil through the gas sampling valve without being affected by the liquid sampling procedure.

After the vapor sample has been trapped in the vapor coil, the liquid in the cell is sampled by withdrawing a portion of it through the liquid sampling line. The liquid sampling line extends into the equilibrium cell through the vapor outlet to a point just above the vapor distributor plate. The holes in the distributor plate are so arranged that the bubbles of vapor rise clear of the end of the sampling line as they pass up through the liquid. The liquid sampling line, which is a 1/16 in. OD tube with the dead volume reduced to capillary dimensions by insertion of a 20 ga. wire, leads to the liquid sampling valve, which in turn leads to the liquid sampling manifold.

The procedure for taking liquid samples is quite critical and has a considerable effect on the accuracy of the final data. As the liquid sample passes up through the sampling line to the sampling valve, it is warmed from its saturation temperature to a temperature well in the superheat region. The liquid totally vaporizes in a short section of the sampling line, resulting in a fractionation effect in that section of the line. As liquid continues to flow, the fractionation region of the sampling line tends to accumulate the less volatile components, finally reaching approximate equilibrium with the flowing sample stream. It is necessary to throw away the first portion of sample which passes through the sampling valve and to make sure that the flow rate of sample is maintained constant during the sample period. The flow rate is maintained constant by making only one setting of the sampling valve and allowing the vapor to expand through the valve to a pressure which is less than half of the system pressure. Also, while the liquid sample is being withdrawn from the cell, the pressure in the system is maintained by screwing in on the system volume regulator.

Both liquid and vapor samples are finally collected in 75 cc. sample cylinders which are equipped with a pressure gauge at one end and a shut-off valve at the other end. Sample cylinders and manifold are normally purged with sample gas and then evacuated before being filled with the sample.

F. Pressure Measurement

The pressure in the equilibrium system is measured by a temperature-compensated Bourdon-tube gauge which has been calibrated by the manufacturer (Heise) and checked with a dead-weight gauge. The low-pressure gauge which was used for measuring pressures at 20 atmospheres and below can be read directly to the nearest 0.1 psi with a hysteresis error of ± 0.005 psi. The high-pressure gauge which was used for pressures above 20 atmospheres can be read directly to the nearest 0.3 psi with a hysteresis error of ± 0.1 psi.

The pressure gauges used in this experimental program have been tested with an Ashcroft Portable Dead-Weight Tester. The results of this calibration are shown in Figures 5 and 6. As can be seen on the graphs, the 500 psia gauge, Heise H16100, shows no deviation up to 220 psia and deviates only 0.1 psi above 220 psia. The 300 psia gauge, Heise H31596, shows a slight drift with increasing pressure, but the error is never larger than 0.1%. This gauge is considered satisfactory without a correction to the readings.

G. Temperature Measurement

The temperature of the equilibrium liquid is measured by a three-element copper-constantan thermocouple which is immersed in the liquid inside the cell. Melting ice is used as the warm end reference junction. Seven separate calibrations have been made of the thermocouple by measurement of the vapor pressure of oxygen. We initially calibrated against the vapor pressures of argon, oxygen and nitrogen but systematic deviations became evident. Oxygen was used as the standard because its normal boiling point is an International Standard Temperature and in this way our calibration was guaranteed to pass through this point.

All seven calibrations covered the temperature range -220°F to -300°F . One calibration extended warmer and one calibration extended colder. The data for all seven calibrations was fitted by least squares to a polynomial of millivolts vs. temperature. Figure 7 shows the deviation of the measured versus calculated millivolts with a dashed line drawn to indicate the millivolt deviation equivalent to 0.1°F . As can be seen, almost all points are within 0.1°F of the calibration equation.

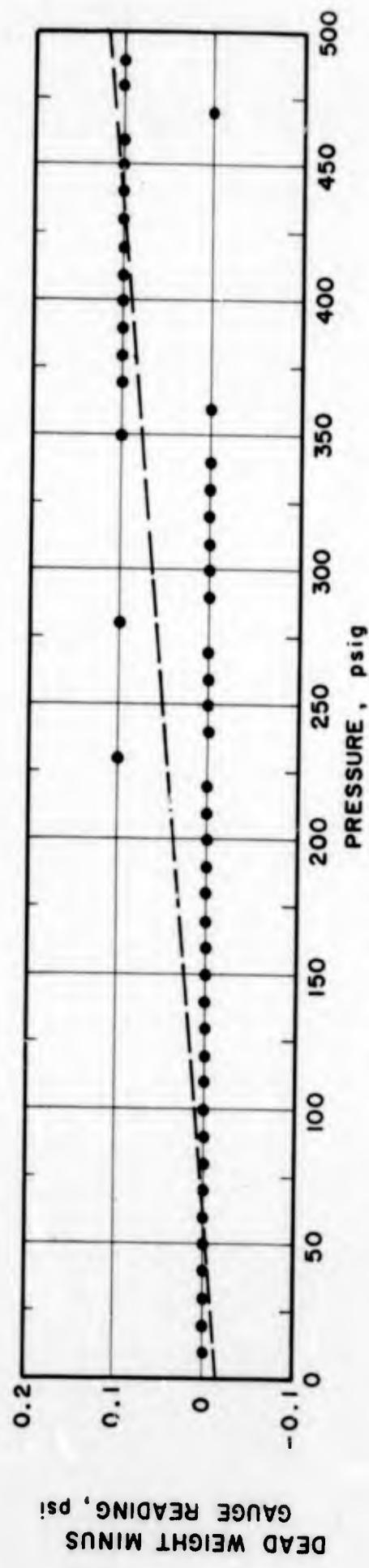


Figure 5. Dead Weight Test of 500 psi Heise Gauge.

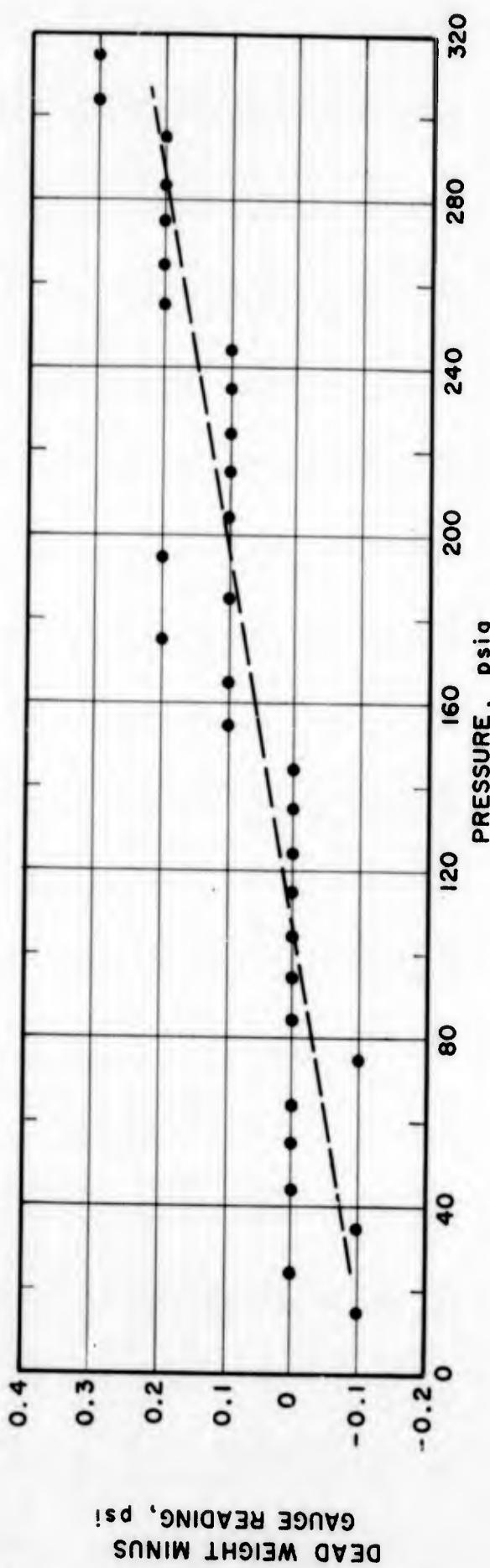


Figure 6. Dead Weight Test of 300 psi Heise Gauge.

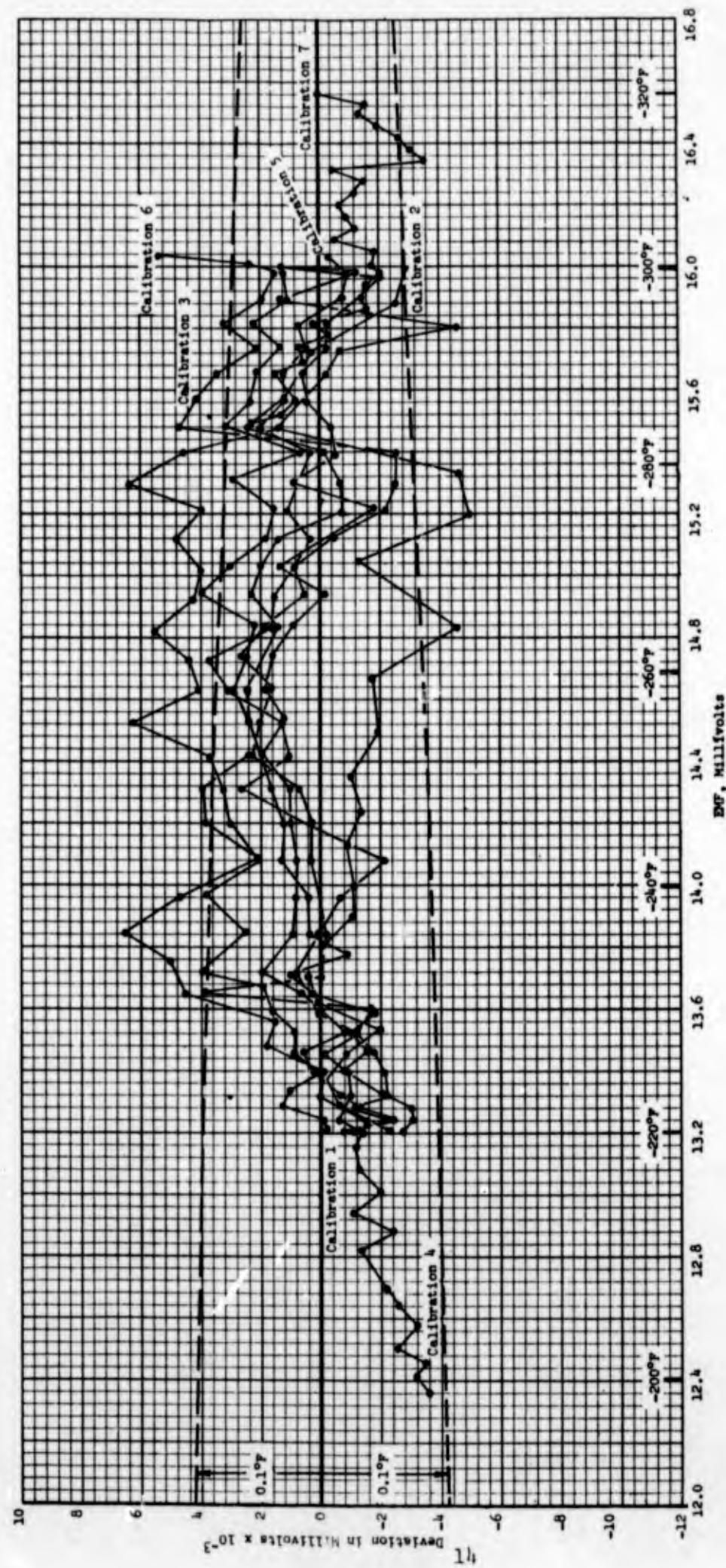


Figure 7. Thermocouple Calibration.

H. Time of Equilibration

Five runs were made to determine equilibration time of the experimental apparatus with mixtures of nitrogen and argon in the cell. Measurements were made of the following variables after adding an incremental sample of either argon or nitrogen:

1. Temperature - every five seconds
2. Pressure - every five seconds
3. Liquid level - every second on movie film
4. Composition - continuously by means of a Gow-Mac Thermal Conductivity Cell installed in parallel to the vapor recirculation line.

The conditions of the runs are given in Table 1 and the results of Run A, which can be considered typical, are shown in Figure 8 . This figure indicates that all the properties change at the same time and the same way. In this case, there was a sharp rise right after the argon was added, a rapid fall-off, a slow recovery with overshoot and a settling to steady-state values. By the time six minutes had elapsed, the transient had settled out. In the measurement of vapor-liquid equilibria, thirty minutes were allowed for equilibration, so equilibrium errors are negligible and contribute a smaller error than reading the pressure and temperature.

TABLE 1
EQUILIBRATION TEST RESULTS

<u>Run</u>	<u>Temperature of F</u>	<u>Initial Pressure Psia</u>	<u>Final Pressure Psia</u>	<u>Time to Equilibrate</u>	<u>% N₂ in Vapor</u>	<u>% Ar in Vapor</u>	<u>Material Added</u>
A	-255	175.6	174.0	4-1/2 min.	51.04	48.96	Argon
B	-247	293.8	290.3	4-1/2 min.	83.73	16.27	Argon
C	-228	294.1	293.7	4-1/2 min.	10.40	89.60	Argon
D	-279	58.8	60.8	5 min.	34.02	65.98	Nitrogen
E	-294	58.8	57.5	4 min.	94.21	5.79	Argon

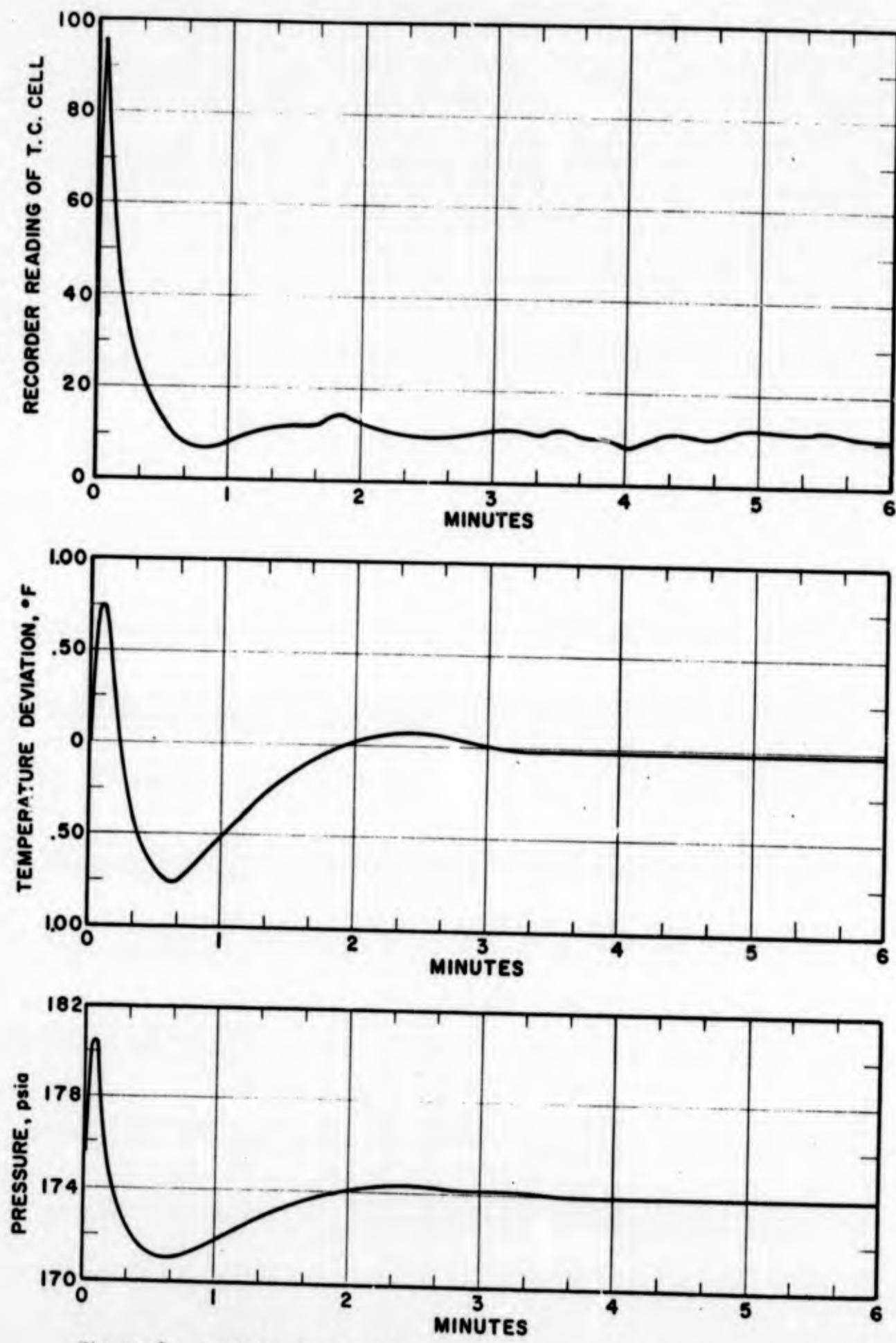


Figure 8. Equilibration Test Run on Vapor-Liquid Apparatus.

IV. ANALYTICAL METHODS

The best analytical method for analyzing the argon-oxygen-nitrogen mixtures was judged to be gas chromatography. Other techniques which were considered included: paramagnetic and electrolytic methods for oxygen, titanium sponge technique for argon, and mass spectrometry for argon, oxygen and nitrogen. These techniques were found to have limitations of accuracy and speed which make them inferior to gas chromatography.

A. Analyses to Run 264

For the first 150 experimental points a technique was used described in the first quarterly report(3). With this technique, the flow of carrier gas and sample was split, passed through two separate columns and recombined to pass through the same detector. One column was a five-foot length of 28-32 mesh molecular sieve 5A at 105°F and the other column was a six-foot length of 30-70 mesh molecular sieve 5A at -110°F. The first column was used to separate the nitrogen from the argon plus oxygen and the second column was used to separate the oxygen from the argon. In order to get proper separation of the argon it was necessary to provide a retention time of about 12.5 minutes for the oxygen. The maximum deviation with any particular sample was about 1.5% of the resulting analysis.

Between runs 150 and 264 a dual-chromatograph system was used for analysis. One chromatograph determined oxygen and nitrogen and the other chromatograph determined argon. The columns in each chromatograph were identical (6 ft 5A molecular sieves at 30°C), but one chromatograph used argon as the carrier gas and the other used oxygen as the carrier. In this way, the only separation required in either column was between the nitrogen and the other two gases. The chromatograph using argon carrier gas would only register the oxygen part of the argon + oxygen peak and in the chromatograph using oxygen carrier gas, only the argon part of the argon + oxygen peak would register. Frequent calibration standards were required to assure internal consistency of the data. There was an improvement in accuracy over the preceding method.

B. Analyses After Run 264

Beginning with run 264 a new method was adopted whereby all three components of an oxygen-nitrogen-argon mixture can be separated on a single chromatographic column. By this method it is possible to calculate the relative proportions of each component from the relative peak size. This has several advantages over the previous methods where a knowledge of the absolute peak size was required. This new method is less sensitive to drift in operating detector current and column

variations since it is only the variation during the period of elution of the peaks which affect the analysis. With the absolute method, any variation in current or column conditions from the time a standard calibration is run until the unknown sample is run will affect the analysis.

By this new method, the components are separated at liquid oxygen temperature on a chromatographic column containing tetrafluoromethane (Freon 14)*as a solvent on firebrick. The separation is made in the order of the boiling points of the gases with nitrogen emerging first from the column. A sample chromatogram of a mixture containing 77.40% nitrogen, 10.13% argon and 12.47% oxygen is shown in Figure 9 . Each of the component peaks is clearly separated from the other peaks. It is possible to obtain duplicate analyses of a mixture which agree within 0.3%. Tests with a standard blend, however, show variations of as much as 1% between analyses on separate days. This presumably is due to some interference between the peaks.

The separation is performed on a 15' x 1/4" column with a flow rate of approximately 230 cc/minute of helium. The ratio of Freon 14 to firebrick is about 1 to 3 by weight. The column is made up by first packing the column with the firebrick, then charging the column with a mixture of Freon 14 and helium at room temperature to a pressure high enough to put the required amount of Freon 14 in the column. This usually requires charging to a pressure between 900 and 1100 psig. Subsequent to pressurization with the Freon 14-helium mixture the column is submerged in boiling liquid oxygen whereupon the Freon 14 condenses as the immobile chromatographic solvent on the firebrick. This column is then used in the conventional manner to separate the components of the oxygen-nitrogen-argon mixtures. The sample size is 5 cc fed in at either 760 or 900 mm Hg (10 cc flooded the column). A sample normally fully separates in fourteen minutes.

Starting with run 1530, the method was modified. It was discovered that a mixture of 30% ethane, 60% tetrafluoromethane, and 10% helium solved the problem of the tailing of nitrogen into the argon peak. The argon retention time increased slightly bringing it closer to the oxygen peak. The charging pressure of the column was reduced to between 500 and 700 psig and the flow rate increased to 300 cc/minute. Analysis time was reduced by this improvement to nine minutes.

A specially built electronic integrator records the response of the thermal conductivity cell. The basic chromatograph is a Beckman GC-2 with two 5 cc sample loops. The column described above is external to the chromatograph box in a dewar of liquid oxygen. The integrator has

*E. I. Dupont de Nemours Inc. registered trademark.

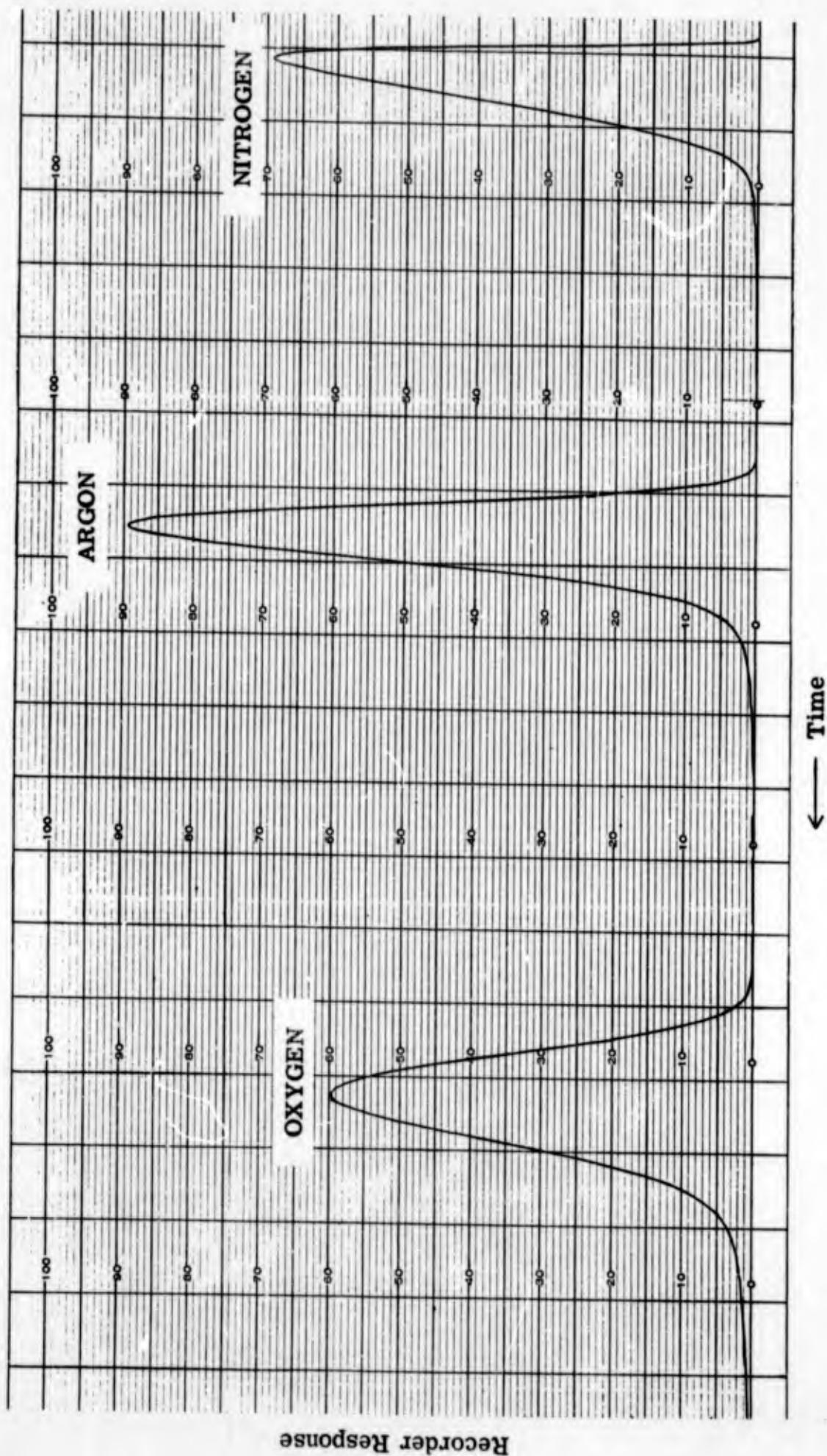


Figure 9. Sample Chromatogram.

four components:

- (1) Hewlett-Packard 5532A Electronic Counter for display
- (2) Dymec Model 2210 Voltage to Frequency Converter
- (3) Sola Type CVH-1 Harmonic-Neutralized Constant Voltage Transformer
- (4) Sanborn 860-1500-PA Amplifier

Also the output of the thermal conductivity cell is recorded as peaks by a Brown Electronik Recorder with variable sensitivity and span. This recorder is electrically isolated from the integrator. Photographs of the chromatograph are shown in Figures 10 and 11.

The thermal conductivity detector was calibrated in December 1962 and November 1963 over a wide range of sample size and operating conditions to insure accurate analysis of the mixtures. It was found that a two-fold variation in flow rate affects the analysis only 0.3%. A change in the filament current to 2/3 the operating value only affected the analysis by 1%. During actual operation these variables would be expected to vary over only a fraction of these changes. In order to determine the effect of sample size, standard blends of oxygen, nitrogen, and argon were used to determine the response of the detector relative to a 2 cc sample of oxygen. The results of this calibration are shown in Figure 12, in which the relative response, q , is the inverse of the thermal conductivity cell response. The triangles represent points taken in 1963 and the circles represent the points taken in 1962. The lines drawn on the graph are the calibrations used in all calculations. It can be seen that for the two calibrations the response of oxygen and the response of nitrogen agree. The response of argon differs by 2% for small samples. This difference in the case of argon probably represents a variation in the standards rather than a variation in the cell response. This is indicated by the results in Table 2 which lists analyses of two mixtures which were routinely analyzed daily to determine whether the column was good or needed rebuilding. The special mix ran out at the end of August and synthetic air was first used on April 18, 1963. It is evident from examination of Table 2 that while there was scatter in the daily analyses, there was no systematic trend in the analyses with time.

Compositions were calculated using the relative responses lines shown in Figure 12. The mole fraction of a component is given in terms of peak area and relative response as

$$x_i = \frac{A_i q_i}{A_1 q_1 + A_2 q_2 + A_3 q_3} \quad (1)$$

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Figure 10. Photograph of Gas Chromatograph.

The column is submerged in the steel dewar in the background. The Beckman GC2-A is shown in the near background. The sample bomb and sample feed system are above the operator's hand. The manometer is behind the recorder. On top of the recorder are the Electronic Counter and the Voltage to Frequency Converter. Not shown are the transformer and amplifier.

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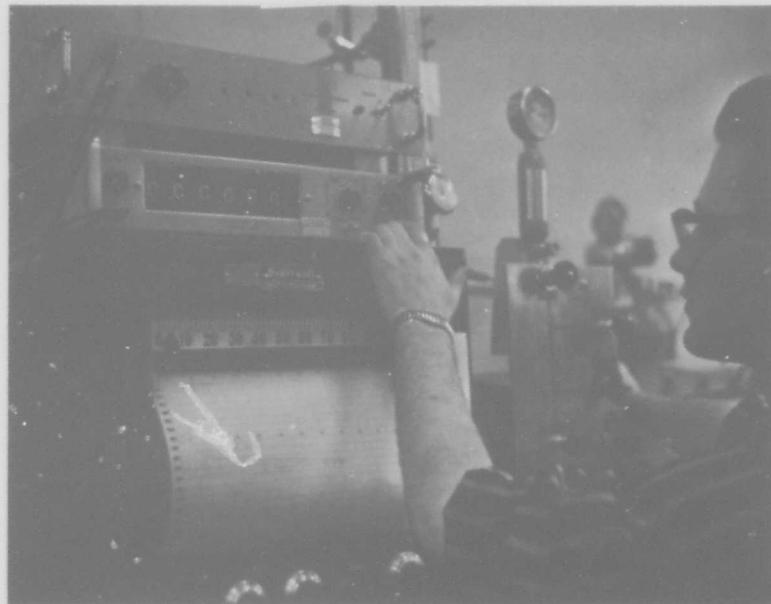


Figure 11. Close-up of Electronic Components of the Chromatograph.

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○ DEC., 1962

△ NOV., 1963

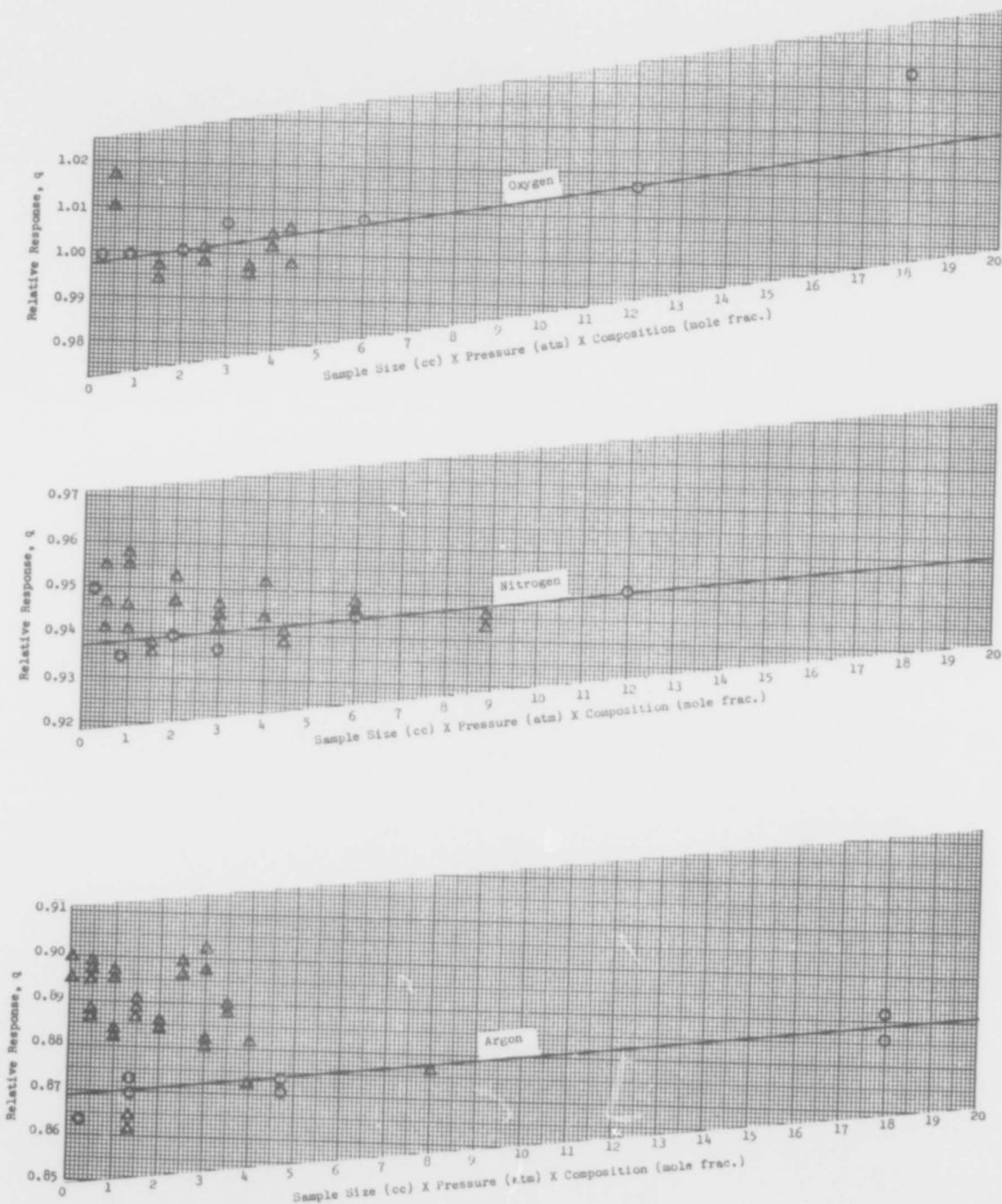


Figure 12. Chromatograph Calibration Curves.

TABLE 2
 SAMPLE LONG-TERM ANALYSES

Synthetic Air				Special Mix			
Date	N ₂	Ar	O ₂	Date	N ₂	Ar	O ₂
4-18-63	77.594	0.891	21.513	1-8-63	47.035	3.771	49.195
4-29-63	77.556	0.836	21.607	1-23-63	46.602	3.835	49.563
5-13-63	78.028	0.920	21.051	3-19-63	46.844	3.805	49.350
6-3-63	77.772	0.912	21.315	4-4-63	46.692	3.754	49.555
6-13-63	77.571	0.874	21.553	4-16-63	47.028	3.678	49.295
7-4-63	77.663	0.838	21.497	4-29-63	46.683	3.764	49.552
7-18-63	77.674	0.775	21.569	5-13-63	46.648	3.800	49.550
8-1-63	77.936	0.531	21.531	6-3-63	46.925	3.783	49.291
8-16-63	77.107	0.874	22.018	6-24-63	46.861	3.755	49.383
8-29-63	77.467	0.793	21.739	7-11-63	48.841	3.630	49.527
9-17-63	77.600	0.853	21.546	7-29-63	49.074	3.533	47.394
9-30-63	77.859	0.837	21.302	8-16-63	48.377	3.533	48.089
10-4-63	78.544	0.837	20.617	8-29-63	46.974	3.726	49.299
10-21-63	77.508	0.897	21.593				

V. EXPERIMENTAL DATA

The tables to follow list the entire experimental data taken during this project. There are listed a total of 1962 points, although there are 1965 listed run numbers; the missing numbers are runs where a mishap such as a lost sample occurred. The data range from one to twenty-six atmospheres and from 139°R to 250°R. Tables 3 through 16 are arranged according to pressure level and the run numbers represent only the chronology of measurement. All runs have been included whether they were used in the correlation or discarded for badness of fit.

The component gases used for these measurements are APCI produced with typical analyses as follows:

Oxygen: 99.70% O₂, 0.30% Ar
Nitrogen: 99.997% N₂, 0.003% Ar
Argon: 99.996% Ar, 0.002% N₂, 0.002% O₂

A typical run had the following history. One hour elapsed from the time of introduction of the first gas into the equilibrium apparatus until the samples were taken. The samples were stored approximately six hours as analytical inventory and then one hour elapsed during analysis. The raw area data was sent to the computer the next morning and the calculated compositions returned in the afternoon one day later.

Modifications in procedure took place throughout the duration of the program. The first run was made Aug. 13, 1962 and the last run was made October 17, 1963. The following progressive modifications took place during the program.

Run 151: Changed to dual chromatograph system for analysis

Run 264: Changed to relative response, Freon column chromatograph for analysis

Run 609: Finished initial contract

Run 610: Started extension to contract. The 500 psia pressure gauge was installed on the equilibrium apparatus in place of the 300 psia gauge.

Run 936: The 500 psia pressure gauge was removed from the equilibrium apparatus and the 300 psia gauge re-installed.



Runs 1361-1683, 1689-1965: Detachable sample loops used on equilibrium apparatus. All other runs used sample bombs

Run 1530: Mixed solvent Freon-Ethane replaced Freon in the column of the chromatograph

Run 1965: Last run.

TABLE 3
EXPERIMENTAL DATA AT 1 ATM.

RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION			VAPOR MOL FRACTION			RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION			VAPOR MOL FRACTION			
		N2	AR	O2	N2	AR	O2			N2	AR	O2	N2	AR	O2	
1576	158.9	.0755	•••	•••	.9245	•••	•••	1611	155.9	•0758	•5913	•3329	•2055	•5522	•2423	
1577	155.9	.1554	•••	•••	.8446	•4239	•••	1612	155.9	•0653	•7274	•2074	•1825	•6592	•1583	
1578	150.9	.3115	•••	•••	.6885	.6571	•••	1613	155.9	•0585	•8213	•1202	•1625	•7463	•0912	
1579	155.9	.0462	•••	•••	.9538	•••	•••	1614	152.9	•2371	•0361	•7268	•5597	•0316	•4087	
1580	152.9	.1411	•••	•••	.8589	•••	•••	1615	152.9	•2378	•0639	•6983	•5465	•0564	•3971	
1581	162.4	•••	•••	•••	.0299	.9701	•••	1616	152.9	•2274	•0872	•6854	•5346	•0759	•3894	
1582	162.2	•••	•••	•••	.0506	.9494	•••	1617	152.9	•2107	•1264	•6549	•5142	•1102	•3757	
1583	162.1	•••	•••	•••	.0647	.9353	•••	1618	152.9	•2117	•2134	•5749	•4922	•1792	•3286	
1584	161.8	•••	•••	•••	.0726	.9274	•••	1619	152.9	•1899	•3600	•4501	•4403	•2955	•2642	
1585	161.5	•••	•••	•••	.0985	.9015	•••	1620	152.9	•1769	•4923	•3308	•4075	•3950	•1974	
1586	161.2	•••	•••	•••	.1249	.8751	•••	1621	152.9	•1614	•6344	•2042	•3736	•4996	•1266	
1587	160.4	•••	•••	•••	.2343	.7657	•••	1622	152.9	•1491	•7455	•1054	•3573	•5752	•0675	
1588	158.9	•••	•••	•••	.5054	.4946	•••	1623	150.9	•3151	•0141	•6708	•6573	•0112	•3315	
1589	158.4	•••	•••	•••	.6682	.3318	•••	1624	150.9	•3156	•0266	•6558	•6527	•0220	•3253	
1590	157.9	•••	•••	•••	.8403	.1597	•••	1625	150.9	•3055	•0423	•6522	•6404	•0330	•3267	
1591	157.4	•••	•••	•••	.9541	.0459	•••	1626	150.9	•3035	•0499	•6466	•6369	•0377	•3255	
1592	158.9	•••	•••	•••	.0743	.0192	.9156	1627	150.9	•312	•0613	•6375	•6357	•0477	•3165	
1593	158.9	•••	•••	•••	.0629	.0231	.9140	2175	•0310	•7516	•1628	•150.9	•6080	•6087	•6252	
1594	158.9	•••	•••	•••	.0629	.0335	.9036	2116	•0434	•7450	•1629	•150.9	•3006	•1274	•5720	
1595	158.9	•••	•••	•••	.0604	.0448	.8948	2045	•0592	•7363	•1630	•150.9	•2969	•2138	•4693	
1596	158.9	•••	•••	•••	.0591	.0559	.0850	1977	•0724	•7299	•1631	•150.9	•2852	•3181	•3967	
1597	158.9	•••	•••	•••	.0549	.0812	.8639	1821	•1036	•7143	•1632	•150.9	•2545	•4878	•2578	
1598	158.9	•••	•••	•••	.0574	.1087	.8339	1621	•1414	•6965	•1633	•150.9	•2407	•6712	•6881	
1599	158.9	•••	•••	•••	.0411	.1632	.7957	1310	•2062	•6628	•1634	•148.9	•3881	•0692	•5427	
1600	158.9	•••	•••	•••	.0239	.2824	.6937	0792	•3374	•5834	•1635	•148.9	•3826	•1667	•4507	
1601	155.9	•••	•••	•••	.1496	.0165	.8339	0839	•1821	•1036	•7143	•1636	•148.9	•3661	•2559	•4878
1602	155.9	•••	•••	•••	.1451	.0266	.8282	4091	•0284	•5624	•1637	•148.9	•3611	•3675	•2715	•6455
1603	155.9	•••	•••	•••	.1475	.0347	.8178	4075	•0374	•5552	•1638	•148.9	•3363	•5470	•1167	•6094
1604	155.9	•••	•••	•••	.1432	.0478	.8090	4024	•0501	•5475	•1639	•148.9	•3131	•6869	•5790	•4239
1605	155.9	•••	•••	•••	.1442	.0607	.7951	4092	•0628	•5280	•1640	•145.0	•5523	•4477	•4210	•2049
1606	155.9	•••	•••	•••	.1381	.0846	.7773	3871	•0887	•5242	•1641	•143.0	•6514	•1486	•2162	•1693
1607	155.9	•••	•••	•••	.1354	.1155	.7491	3603	•1487	•4910	•1642	•143.0	•7307	•2693	•9147	•0494
1608	155.9	•••	•••	•••	.1249	.1894	.6857	3331	•1909	•4760	•1643	•146.9	•4961	•5039	•8050	•1950
1609	155.9	•••	•••	•••	.1030	.3263	.5707	2785	•3213	•4003	•1644	•141.5	•8710	•1290	•9627	•0373
1610	155.9	•••	•••	•••	.0883	.4522	.4595	2397	•4355	•3247	•1645	•140.0	•9860	•0140	•9962	•0036

TABLE 3
EXPERIMENTAL DATA AT 1 ATM. (continued)

RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION N2 AR 02	VAPOR MOL FRACTION N2 AR 02	RUN NO.	TEMP. DEG.R	Liquid MOL FRACTION N2 AR 02	VAPOR MOL FRACTION N2 AR 02
1646	141.5	.8457	.1543	1682	140.0	.9766	.0102
1647	141.0	.8790	.1210	1683	140.0	.9779	.0132
1648	140.4	.9373	.0627	1923	162.5	.0162	.0059
1649	140.2	.9623	.0377	1924	160.4	.0088	.9912
1650	140.0	.9822	.0178	1925	158.9	.2559	.7441
1651	139.7	.9928	.0072	1926	158.9	.0789	.9057
1652	146.9	.4775	.0150	1927	157.4	.0154	.9917
1653	146.9	.4825	.0217	1928	155.9	.1397	.0026
1654	146.9	.4840	.0354	1929	155.9	.0612	.9783
1655	146.9	.4800	.0485	1930	155.9	.1297	.3901
1656	146.9	.4879	.0673	1931	155.9	.0578	.3595
1657	146.9	.4694	.0924	1932	155.9	.0432	.0059
1658	146.9	.4789	.1308	1933	150.9	.2924	.0563
1659	146.9	.4743	.2292	1942	150.9	.4874	.0236
1660	146.9	.4489	.3809	1943	146.9	.4958	.0641
1661	146.9	.4344	.5184	1944	146.9	.4529	.1244
1662	145.0	.6166	.0392	1945	145.0	.5769	.1584
1663	145.0	.6106	.0873	1946	145.0	.5936	.0395
1664	145.0	.5916	.1818	1947	145.0	.6075	.0418
1665	145.0	.5823	.2789	1948	145.0	.5867	.2465
1666	143.0	.7478	.0112	1949	143.0	.7464	.0207
1667	143.0	.7522	.0250	1950	143.0	.7571	.0203
1668	143.0	.7584	.0337	1951	143.0	.7150	.0215
1669	143.0	.7524	.0502	1952	143.0	.7077	.0214
1670	143.0	.7528	.0744	1953	141.5	.9612	.0124
1671	143.0	.7464	.0921	1954	141.5	.8647	.0124
1672	143.0	.7313	.1314	1955	141.5	.8504	.0124
1673	143.0	.7203	.2422	1956	141.5	.8664	.0124
1674	141.5	.8569	.0226	1957	141.5	.8562	.0124
1675	141.5	.8573	.0744	1958	140.8	.9001	.0124
1676	141.5	.8578	.0395	1959	140.1	.9622	.0124
1677	141.5	.8515	.0499	1960	140.2	.9549	.0124
1678	141.5	.8544	.0615	1961	140.3	.9523	.0124
1679	141.5	.8502	.0875	1962	129.9	.9845	.0124
1680	141.5	.8616	.1097	1963	140.0	.9838	.0124
1681	140.0	.9788	.0080	1964	140.0	.9844	.0124
				1965	140.0	.9778	.0019
						.0044	.0019
						.0022	.0019
						.0132	.0019
						.9934	.0019
						.0085	.0019
						.0151	.0019
						.9924	.0019
						.0057	.0019

TABLE I
EXPERIMENTAL DATA AT 2 ATM.

RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION			VAPOR MOL FRACTION			RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION			VAPOR MOL FRACTION		
		N ₂	AR	O ₂	N ₂	AR	O ₂			N ₂	AR	O ₂	N ₂	AR	O ₂
1466	171.9	.0721	***	***	.9279	.2160	***	1500	168.9	.1258	.1657	.7085	.3082	.1703	.5215
1467	168.9	.1470	***	***	.8530	.3769	***	1501	168.9	.1058	.2999	.5944	.2589	.2997	.4414
1468	162.9	.3437	***	***	.6563	.6407	***	1502	168.9	.0845	.4310	.4845	.2239	.4141	.3620
1469	158.9	.5139	***	***	.4861	.7823	***	1503	168.9	.0725	.5494	.3781	.1775	.5296	.2928
1470	160.9	.3406	.6594	***	.5779	.4221	***	1504	168.9	.0623	.6623	.2754	.1506	.6330	.2164
1471	165.9	.1371	.8629	***	.3001	.6999	***	1505	168.9	.0484	.7692	.1824	.1205	.7307	.1487
1472	167.9	.0708	.9292	***	.1762	.8238	***	1506	165.9	.2297	.0280	.7423	.5029	.0258	.4713
1473	175.1	***	***	***	.0464	.9536	***	1507	165.9	.2228	.0672	.7100	.4845	.0616	.4538
1474	175.3	***	***	***	.0195	.9805	***	1508	165.9	.2160	.1350	.6490	.4619	.1202	.4179
1475	175.0	***	***	***	.0524	.9476	***	1509	165.9	.2012	.2539	.5450	.4280	.2190	.3531
1476	174.8	***	***	***	.0690	.9310	***	1510	165.9	.1812	.4112	.4076	.3848	.3475	.2677
1477	174.7	***	***	***	.0808	.9192	***	1511	165.9	.1646	.5671	.2683	.3518	.4692	.1790
1478	174.5	***	***	***	.0962	.9038	***	1512	165.9	.1461	.7326	.1213	.3194	.5955	.0851
1479	174.3	***	***	***	.1180	.8820	***	1513	165.9	.1390	.8357	.0253	.3044	.6784	.0173
1480	173.4	***	***	***	.2357	.7643	***	1514	162.9	.3364	.0131	.6506	.6306	.0129	.3565
1481	171.9	***	***	***	.5059	.4941	***	1515	162.9	.3317	.0286	.6397	.6273	.0225	.3502
1482	171.4	***	***	***	.5902	.4098	***	1516	162.9	.3331	.0402	.6267	.6262	.0315	.3403
1483	170.6	***	***	***	.7881	.2119	***	1517	162.9	.3288	.0531	.6181	.6228	.0411	.3361
1484	170.3	***	***	***	.9722	.0278	***	1518	162.9	.3324	.0666	.6010	.6225	.0515	.3260
1485	171.9	***	***	***	.0719	.0094	***	1519	162.9	.3240	.0965	.5795	.6245	.0701	.3054
1486	171.9	***	***	***	.0717	.0167	***	1520	162.9	.3220	.1370	.5410	.5970	.1048	.2982
1487	171.9	***	***	***	.0699	.0332	***	1521	162.9	.3146	.2092	.4761	.5787	.1577	.2636
1488	171.9	***	***	***	.0658	.0507	***	1522	162.9	.2930	.3768	.3302	.5382	.2757	.1661
1489	168.9	.1393	***	***	.0652	.0619	***	1523	162.9	.2740	.5469	.1792	.5058	.3903	.1039
1490	168.9	.1370	***	***	.0565	.0880	***	1524	162.9	.2601	.6540	.0859	.4860	.4610	.0530
1491	171.9	***	***	***	.1505	.1286	***	1525	160.9	.4083	.0573	.5343	.6986	.0388	.2626
1492	171.9	***	***	***	.0282	.2552	***	1526	160.9	.4062	.0949	.4986	.6882	.0653	.2465
1493	168.9	.1318	***	***	.0581	.0581	***	1527	160.9	.3932	.1777	.4290	.6643	.1206	.2150
1494	168.9	.1323	***	***	.0880	.0880	***	1528	160.9	.3766	.3155	.3078	.6311	.2144	.1545
1495	168.9	.1323	***	***	.1318	.0880	***	1529	160.9	.3595	.4856	.1549	.6029	.3140	.0831
1496	168.9	.1323	***	***	.1318	.0880	***	1530	158.9	.5052	.0127	.4822	.7761	.0778	.2161
1497	168.9	.1323	***	***	.0563	.0563	***	1531	158.9	.5088	.0255	.4658	.7757	.0132	.2081
1498	168.9	.1323	***	***	.0880	.7802	***	1532	158.9	.5039	.0404	.4556	.7711	.0256	.2033
1499	168.9	.1323	***	***	.1318	.0880	***	1533	158.9	.5052	.0595	.4353	.7653	.0382	.1966

TABLE 4
EXPERIMENTAL DATA AT 2 ATM. (continued)

RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION N2 AR 02	VAPOR MOL FRACTION N2 AR 02	RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION N2 AR 02	VAPOR MOL FRACTION N2 AR 02
1534	158.9	.5070	.0721	.4209	.7633	.0450	.1917
1535	158.9	.5024	.0979	.3997	.7578	.0618	.1804
1536	158.9	.4960	.1387	.3653	.7494	.0869	.1637
1537	158.9	.4978	.2360	.2662	.7285	.1419	.1296
1538	158.9	.4725	.3439	.1836	.7088	.2066	.0846
1539	158.9	.4560	.4730	.0710	.6680	.2780	.0340
1540	156.9	.6172	.9377	.3451	.8374	.0212	.1415
1541	156.9	.6072	.1204	.2724	.8204	.0675	.1122
1542	156.9	.6061	.1386	.2553	.9173	.0779	.1048
1543	156.9	.6027	.1926	.2047	.3116	.1055	.0829
1544	156.9	.5723	.3893	.0384	.7753	.2084	.1898
1545	154.9	.7392	.0133	.2474	.9013	.0072	.0915
1546	154.9	.7376	.0279	.2346	.8976	.0144	.0880
1547	154.9	.7343	.0416	.2239	.8952	.0211	.0837
1548	154.9	.7318	.0541	.2142	.8922	.0270	.0808
1549	154.9	.7273	.0693	.2035	.8888	.0359	.0753
1550	154.9	.7220	.0992	.1786	.8805	.0507	.0686
1551	154.9	.7246	.1281	.1473	.8768	.0659	.0573
1552	154.9	.7038	.2521	.0441	.8560	.1266	.0174
1553	152.9	.8681	.0164	.1155	.9519	.0082	.0399
1554	152.9	.8756	.0249	.0995	.9525	.0123	.0352
1555	152.9	.8732	.0380	.0889	.9532	.0167	.0302
1556	152.9	.8722	.0465	.0813	.9531	.0199	.0270
1557	152.9	.8633	.0465	.0828	.9483	.0245	.0273
1558	152.9	.8654	.0724	.0622	.9447	.0339	.0215
1559	152.9	.8895	.0952	.0453	.9409	.0432	.0159
1560	151.9	.9460	.0071	.0469	.9810	.0032	.0158
1561	151.9	.9409	.0207	.0385	.9790	.0087	.0122
1562	151.9	.7349	.0339	.0313	.9767	.0144	.0089
1563	151.9	.9343	.0424	.0233	.9740	.0192	.0069
1564	154.9	.74012599	.90440956
1565	152.9	.87441256	.95650435
1566	151.9	.94490551	.98150185
1567	151.2	.9949	.005199740026
1568	151.4	.9810	.019099190081
							.0070
							.9972
							.0028

TABLE 5
EXPERIMENTAL DATA AT 4 ATM.

RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION			VAPOR MOL FRACTION			RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION			VAPOR MOL FRACTION		
		N2	AR	02	N2	AR	02			N2	AR	02	N2	AR	02
1361	182.8	.0702	.9298	••••	.1547	.8453	••••	1394	186.8	.0717	.0609	.8674	.1783	.0721	.7496
1362	180.8	.1320	.8663	••••	.2703	.7297	••••	1395	186.8	.0679	.0781	.8540	.1672	.0905	.7422
1363	174.8	.3667	.6313	••••	.5732	.4268	••••	1396	186.8	.0639	.1128	.8233	.1543	.1302	.7155
1364	171.9	.5277	.4723	••••	.7130	.2870	••••	1397	186.8	.0547	.1363	.8090	.1360	.1442	.7042
1365	168.4	.7372	.2626	••••	.8583	.1417	••••	1398	186.8	.0474	.1859	.7668	.1162	.1598	.6688
1366	166.9	.8444	.1556	••••	.9214	.0786	••••	1399	186.8	.0252	.3400	.6348	.0615	.3413	.5572
1367	165.9	.9181	.0819	••••	.9614	.0386	••••	1400	183.8	.1581	.0139	.8281	.3473	.0148	.6380
1368	165.6	.9373	.0627	••••	.9706	.0292	••••	1401	183.8	.1524	.0274	.8022	.3422	.0296	.6282
1369	165.4	.9529	.0471	••••	.9778	.0222	••••	1402	183.8	.1490	.0435	.8076	.3320	.0454	.6226
1370	165.3	.9632	.0368	••••	.9826	.0172	••••	1403	183.8	.1492	.0589	.7919	.3286	.0610	.6103
1371	165.1	.9775	.0225	••••	.9902	.0098	••••	1404	183.8	.1444	.0767	.7789	.3186	.0903	.6011
1372	165.0	.9872	.0128	••••	.9941	.0059	••••	1405	183.8	.1403	.1073	.7524	.3108	.1133	.5759
1373	186.8	.0860	••••	••••	.9140	.2081	••••	7919	183.8	.1315	.1320	.7366	.2935	.1379	.5686
1374	183.8	.1591	••••	••••	.8409	.3527	••••	6473	183.8	.1243	.1982	.6775	.2683	.2019	.5298
1375	177.8	.3454	••••	••••	.6546	.6008	••••	3992	183.8	.0937	.4245	.4818	.2014	.4176	.3810
1376	171.9	.5987	••••	••••	.4013	.8070	••••	1930	183.8	.0738	.5904	.3358	.1592	.5649	.2720
1377	168.4	.7788	••••	••••	.2212	.9065	••••	0935	183.8	.0552	.7561	.1887	.1207	.7216	.1577
1378	166.9	.8697	••••	••••	.1303	.9485	••••	1303	183.8	.0454	.9092	.0454	.1007	.8658	.0385
1379	165.4	.9620	••••	••••	.0380	.9861	••••	0139	183.8	.0246	.7255	.4821	.0255	.4924	.4924
1380	190.6	••••	••••	••••	.0252	.9748	••••	.0346	.9654	1413	.2334	.0689	.6977	.4625	.0633
1381	190.4	••••	••••	••••	.0514	.9466	••••	.0677	.9323	1414	.2262	.1275	.6463	.4410	.5457
1382	190.3	••••	••••	••••	.0446	.9554	••••	.0605	.9395	1415	.2021	.2884	.5095	.3889	.2475
1383	190.2	••••	••••	••••	.0471	.9529	••••	.0640	.9360	1416	.1738	.3127	.5136	.3345	.4451
1384	190.1	••••	••••	••••	.0519	.9481	••••	.0656	.9344	1417	.1579	.0464	.1957	.3087	.2204
1385	189.8	••••	••••	••••	.0804	.9196	••••	.1077	.8923	1418	.1447	.7674	.0879	.2880	.6488
1386	188.8	••••	••••	••••	.1947	.8053	••••	.2444	.7556	1419	.1415	.8257	.0328	.2784	.6971
1387	187.3	••••	••••	••••	.4232	.5768	••••	.4807	.5193	1420	.177.8	.3435	.0091	.6473	.6006
1388	186.3	••••	••••	••••	.6296	.3704	••••	.6616	.3384	1421	.177.8	.3423	.0211	.6366	.3920
1389	185.8	••••	••••	••••	.7869	.2131	••••	.8077	.1923	1422	.177.8	.3407	.0387	.5966	.0167
1390	185.4	••••	••••	••••	.9313	.0687	••••	.9399	.0631	1423	.177.8	.3380	.0472	.6206	.3867
1391	186.8	.0812	••••	••••	.0154	.9033	••••	.1988	.0182	1424	.177.8	.3305	.0867	.5889	.0315
1392	186.8	.0765	••••	••••	.0316	.8920	••••	.1878	.0378	1425	.177.8	.3200	.1328	.5472	.3779
1393	186.8	.0748	••••	••••	.0478	.8774	••••	.1869	.0563	1426	.177.8	.3152	.1763	.5085	.3369

TABLE 5
EXPERIMENTAL DATA AT 4 ATM. (continued)

RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION			VAPOR MOL FRACTION N2 AR 02	RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION			VAPOR MOL FRACTION N2 AR 02
		N2	AR	02				N2	AR	02	
1427	177.8	.3092	.2168	.4740	.5384	.1731	.2885	1460	166.9	.8683	.0667
1428	177.8	.2841	.4007	.3153	.4925	.3097	.1978	1461	166.9	.8583	.0650
1429	177.8	.3054	.5906	.1040	.4502	.4755	.0743	1462	166.9	.8557	.0626
1430	174.8	.4548	.0319	.5132	.6996	.0234	.2771	1463	165.4	.9614	.0120
1431	174.8	.4474	.0906	.4621	.6842	.0649	.2509	1464	165.4	.9625	.0226
1432	174.8	.4374	.1559	.4068	.6664	.1108	.2229	1465	165.4	.9634	.0148
1433	174.8	.4171	.2735	.3094	.6416	.1913	.1670	1869	190.6	.0187	.0179
1434	174.8	.3981	.4444	.1574	.6991	.3026	.0833	1870	190.6	.0110	.0110
1435	174.8	.3890	.5421	.0689	.5966	.3629	.6405	1871	190.1	.0291	.0291
1436	171.9	.5999	.0114	.3887	.8025	.0114	.0114	1872	189.3	.0558	.0442
1437	171.9	.5913	.0251	.3837	.8001	.0149	.0149	1873	185.4	.8583	.0147
1438	171.9	.5940	.0341	.3718	.8029	.0214	.1757	1874	183.8	.9506	.0494
1439	171.9	.5931	.0512	.3557	.7973	.0321	.1706	1875	180.8	.0339	.0291
1440	171.9	.5932	.0618	.3451	.7938	.0388	.1674	1876	180.8	.1991	.0242
1441	171.9	.5898	.0880	.3222	.7893	.0552	.1555	1877	177.8	.2954	.0558
1442	171.9	.5868	.1162	.2970	.7828	.0735	.1438	1878	177.8	.5055	.0442
1443	171.9	.5664	.2279	.2057	.7585	.1404	.1011	1879	177.8	.3369	.0422
1444	171.9	.5505	.3554	.0951	.7406	.2140	.0454	1880	176.8	.3831	.0242
1445	169.9	.6897	.0641	.2461	.8494	.0433	.1074	1881	174.8	.0937	.0172
1446	169.9	.6811	.1252	.1936	.8420	.0721	.0859	1882	171.9	.4248	.0147
1447	169.9	.6678	.2317	.1005	.8234	.1315	.0451	1883	171.9	.3354	.0148
1448	168.4	.7814	.0118	.2068	.9048	.0062	.0890	1884	171.9	.5055	.0558
1449	168.4	.7764	.0259	.1977	.9046	.0128	.0826	1885	169.9	.7618	.0448
1450	168.4	.7744	.0406	.1850	.8999	.0209	.0792	1886	168.4	.7552	.0448
1451	168.4	.7694	.0565	.1741	.8945	.0310	.0738	1887	168.4	.5907	.0448
1452	168.4	.7686	.0645	.1669	.8952	.0352	.0696	1888	166.9	.5785	.0558
1453	168.4	.7668	.0929	.1403	.8898	.0503	.0599	1889	166.9	.6380	.0448
1454	168.4	.7614	.1346	.1040	.8826	.0725	.0449	1890	166.9	.8492	.0448
1455	168.4	.7446	.2051	.0463	.8705	.1095	.0200	1891	165.4	.7741	.0427
1456	166.9	.8655	.0126	.1219	.9453	.0066	.0461	1892	165.4	.9552	.0155
1457	166.9	.8676	.0255	.1067	.9454	.0126	.0421	1893	165.4	.9547	.0106
1458	166.9	.8681	.0344	.0975	.9447	.0169	.0394	1894	165.4	.9535	.0132
1459	166.9	.8667	.0467	.0646	.9411	.0244	.0344	1895	165.1	.9780	.0174
										.9872	.0126

TABLE 6
EXPERIMENTAL DATA AT 6 ATM.

RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION			VAPOR MOL FRACTION			RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION			VAPOR MOL FRACTION						
		N2	AR	O2	N2	AR	O2			N2	AR	O2	N2	AR	O2				
453	197.8	.0721	•	•	.9279	•	•	492	186.8	.3645	•	•	.4545	•	.5705	•	.1430	•	.2865
454	195.8	.1213	•	•	.8787	•	•	493	182.8	.5443	•	•	.4110	•	.7464	•	.0253	•	.2282
455	191.8	.2285	•	•	.7715	•	•	494	192.8	.5410	•	•	.4035	•	.7405	•	.0377	•	.2217
456	187.8	.3548	•	•	.6452	•	•	495	182.8	.5387	•	•	.3988	•	.7410	•	.0484	•	.2106
457	183.8	.5069	•	•	.4931	•	•	496	182.8	.5354	•	•	.0936	•	.7308	•	.0550	•	.2042
458	179.8	.6890	•	•	.3110	•	•	497	182.8	.5276	•	•	.1321	•	.7362	•	.0930	•	.1708
459	176.8	.8413	•	•	.1587	•	•	498	182.8	.5153	•	•	.1867	•	.7076	•	.1292	•	.1632
460	174.8	.9513	•	•	.0487	•	•	499	179.8	.6770	•	•	.0355	•	.8351	•	.0222	•	.1427
461	200.8	•	•	•	.0274	•	•	500	179.8	.6730	•	•	.0574	•	.8296	•	.0358	•	.1346
462	200.5	•	•	•	.0550	•	•	501	179.8	.6710	•	•	.0755	•	.8398	•	.0433	•	.1169
463	200.2	•	•	•	.0488	•	•	502	179.6	.6679	•	•	.0953	•	.8236	•	.0591	•	.1173
464	199.9	•	•	•	.0602	•	•	503	179.8	.6630	•	•	.1332	•	.8038	•	.0831	•	.1020
465	174.8	.9373	•	•	.0627	•	•	504	179.8	.6536	•	•	.1906	•	.8404	•	.0957	•	.0639
466	175.3	.9035	•	•	.0965	•	•	505	177.8	.7714	•	•	.0626	•	.8849	•	.0367	•	.0785
467	175.8	.8728	•	•	.1272	•	•	506	177.8	.7714	•	•	.0995	•	.8814	•	.0560	•	.0606
468	176.3	.8395	•	•	.1605	•	•	507	177.8	.7655	•	•	.1372	•	.8750	•	.0797	•	.0454
469	198.8	.6441	•	•	.0307	•	•	508	177.8	.7566	•	•	.1975	•	.8451	•	.1139	•	.0210
470	198.8	.0408	•	•	.0474	•	•	509	175.8	.8903	•	•	.0240	•	.9500	•	.0125	•	.0376
471	198.8	.0251	•	•	.0623	•	•	510	175.8	.8651	•	•	.0511	•	.9466	•	.0274	•	.0259
472	198.8	.0354	•	•	.0794	•	•	511	175.6	.8796	•	•	.0637	•	.9407	•	.0407	•	.0235
473	198.8	.0247	•	•	.0247	•	•	512	175.8	.8823	•	•	.0670	•	.9534	•	.0800	•	.0376
474	198.8	.0100	•	•	.1561	•	•	513	175.8	.8782	•	•	.0972	•	.9364	•	.0455	•	.0168
475	194.8	.1400	•	•	.0319	•	•	514	175.8	.8742	•	•	.1140	•	.9325	•	.0527	•	.0109
476	194.8	.1371	•	•	.0486	•	•	515	175.8	.9461	•	•	.0383	•	.9407	•	.0407	•	.0235
477	194.8	.1334	•	•	.0676	•	•	516	174.8	.6517	•	•	.0748	•	.9760	•	.0175	•	.0065
478	194.8	.1317	•	•	.0441	•	•	517	174.8	.6422	•	•	.0074	•	.9749	•	.0498	•	.0214
479	194.8	.1242	•	•	.7669	•	•	518	174.8	.6422	•	•	.0440	•	.9038	•	.0038	•	.0214
480	194.8	.1154	•	•	.1130	•	•	519	174.8	.6239	•	•	.0191	•	.9359	•	.0245	•	.0234
481	190.8	.2531	•	•	.0327	•	•	520	174.8	.5843	•	•	.0366	•	.8996	•	.0875	•	.0727
482	190.8	.2294	•	•	.7790	•	•	521	174.8	.6239	•	•	.0635	•	.9038	•	.0118	•	.0357
483	190.8	.2483	•	•	.0529	•	•	522	174.8	.6239	•	•	.0635	•	.9038	•	.0118	•	.0357
484	190.8	.2477	•	•	.0683	•	•	523	174.8	.6239	•	•	.0635	•	.9038	•	.0118	•	.0357
485	190.8	.2441	•	•	.0834	•	•	524	174.8	.6239	•	•	.0635	•	.9038	•	.0118	•	.0357
486	190.8	.2398	•	•	.1232	•	•	525	174.8	.6239	•	•	.0635	•	.9038	•	.0118	•	.0357
487	186.8	.3858	•	•	.0529	•	•	526	174.8	.6239	•	•	.0635	•	.9038	•	.0118	•	.0357
488	186.8	.3641	•	•	.0683	•	•	527	174.8	.6239	•	•	.0635	•	.9038	•	.0118	•	.0357
489	186.8	.3725	•	•	.0899	•	•	528	174.8	.6239	•	•	.0635	•	.9038	•	.0118	•	.0357
490	186.8	.3773	•	•	.0699	•	•	529	174.8	.6239	•	•	.0635	•	.9038	•	.0118	•	.0357
491	186.8	.3725	•	•	.1243	•	•	530	174.8	.6239	•	•	.0635	•	.9038	•	.0118	•	.0357

TABLE 6
EXPERIMENTAL DATA AT 6 ATM. (continued)

RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION N2 AR 02	VAPOR MOL FRACTION N2 AR 02	RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION N2 AR 02	VAPOR MOL FRACTION N2 AR 02
1304	190.8	.1452	.8548	1343	184.8	.3940	.4997
1305	184.8	.3758	.6242	1344	182.8	.5392	.0093
1306	179.8	.6219	.3781	1345	182.8	.5397	.4515
1307	177.8	.7409	.2591	1346	182.8	.4301	.0067
1308	174.6	.9522	.0478	1347	182.8	.4302	.7502
1309	174.4	.9610	.0390	1348	182.8	.4302	.7436
1310	174.3	.9701	.0299	1349	179.8	.6809	.0210
1311	174.2	.9802	.0198	1350	179.8	.6809	.0210
1312	174.1	.9918	.0082	1351	179.8	.6788	.0210
1313	201.0	1352	179.8	.6649	.0255
1314	200.9	1353	179.8	.6649	.0255
1315	200.7	1354	179.8	.6454	.0255
1316	198.8	1355	179.8	.6454	.0255
1317	197.8	1356	177.8	.7922	.0195
1318	196.8	1357	177.8	.7922	.0195
1319	196.4	1358	177.8	.8365	.0198
1320	196.1	1359	177.8	.8365	.0198
1321	198.8	.0464	.0120	1360	175.8	.8992	.0198
1322	194.8	.1446	.0118	1361	175.8	.8992	.0198
1323	194.8	.1371	.0524	1362	175.8	.8992	.0198
1324	194.8	.1168	.1409	1363	175.8	.8992	.0198
1325	194.8	.0854	.3512	1364	175.8	.8992	.0198
1326	194.8	.0618	.5288	1365	175.8	.8992	.0198
1327	194.8	.0469	.4094	1366	175.8	.8992	.0198
1328	194.8	.0377	.6631	1367	175.8	.8992	.0198
1329	190.8	.2539	.0170	1368	175.8	.8992	.0198
1330	190.8	.2444	.0603	1369	175.8	.8992	.0198
1331	190.8	.1435	.8454	1370	175.8	.8992	.0198
1332	190.8	.1336	.3655	1371	175.8	.8992	.0198
1333	190.8	.1337	.4486	1372	175.8	.8992	.0198
1334	190.8	.1338	.4238	1373	175.8	.8992	.0198
1335	190.8	.1339	.2668	1374	175.8	.8992	.0198
1336	186.8	.1340	.4486	1375	175.8	.8992	.0198
1337	186.8	.1341	.4397	1376	175.8	.8992	.0198
1338	186.8	.1342	.4238	1377	175.8	.8992	.0198
1339	186.8	.1339	.2668	1378	175.8	.8992	.0198
1340	184.8	.1340	.4486	1379	175.8	.8992	.0198
1341	184.8	.1341	.4397	1380	175.8	.8992	.0198
1342	184.8	.1342	.4238	1381	175.8	.8992	.0198

TABLE 7
EXPERIMENTAL DATA AT 8 ATM.

RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION				VAPOR MOL FRACTION				LIQUID MOL FRACTION				VAPOR MOL FRACTION			
		N2	AR	O2		N2	AR	O2		N2	AR	O2		N2	AR	O2	
389	206.8	.0512	•	•	•	.9488	•	1.127	•	.8873	425	195.8	•	.3450	•	0.669	•
390	202.8	.1495	•	•	•	.8505	•	2.931	•	.7069	426	195.8	•	.3412	•	0.872	•
391	197.8	.2940	•	•	•	.7060	-	4.939	•	.5061	427	195.8	•	.3368	•	1.212	•
392	193.8	.4290	•	•	•	.5710	•	6.371	•	.3629	428	195.8	•	.3265	•	1.740	•
393	189.8	.5830	•	•	•	.4170	•	7.638	•	.2362	429	191.8	•	.4940	•	3.352	•
394	186.8	.7138	•	•	•	.2862	•	8.507	•	.1493	430	191.8	•	.4900	•	0.590	•
395	184.8	.8085	•	•	•	.1915	•	9.051	•	.0949	431	191.8	•	.4926	•	0.451	•
396	182.8	.9125	•	•	•	.0875	•	9.586	•	.0414	432	191.8	•	.4878	•	0.436	•
397	209.0	•	•	•	•	.0116	•	9.984	•	.0151	433	191.8	•	.4815	•	1.308	•
398	208.7	•	•	•	•	.0381	•	9.619	•	.0493	434	191.8	•	.4714	•	1.197	•
399	208.4	•	•	•	•	.0673	•	9.327	•	.0854	435	187.8	•	.6665	•	0.382	•
400	208.1	•	•	•	•	.0985	•	9.015	•	.1231	436	187.8	•	.6616	•	0.552	•
401	181.8	.9620	•	•	•	.0380	•	•	•	.9790	0210	•	•	437	187.8	.6600	•
402	182.3	.9306	•	•	•	.0694	•	•	•	.9606	0394	•	•	438	187.8	.6551	•
403	182.8	.8985	•	•	•	.1015	•	•	•	.9425	0575	•	•	439	187.8	.6507	•
404	183.3	.8647	•	•	•	.1353	•	•	•	.9218	0782	•	•	440	187.8	.6408	•
405	205.8	.0690	•	•	•	.0316	•	.8994	•	.1456	0384	•	•	441	185.8	.7624	•
406	205.8	.0657	•	•	•	.0467	•	.8877	•	.1385	0543	•	•	442	185.8	.7532	•
407	205.8	.0625	•	•	•	.0636	•	.8739	•	.1318	0743	•	•	443	185.8	.7482	•
408	205.8	.0592	•	•	•	.0764	•	.8644	•	.1236	0896	•	•	444	185.8	.7444	•
409	205.8	.0525	•	•	•	.1071	•	.8404	•	.1105	1.240	•	•	445	185.8	.7317	•
410	205.8	.0444	•	•	•	.1535	•	.8021	•	.0933	1.759	•	•	446	185.8	.7157	•
411	201.8	.1699	•	•	•	.0329	•	.9792	•	.3202	0344	•	•	447	183.8	.8513	•
412	201.8	.1678	•	•	•	.0485	•	.7838	•	.3166	0505	•	•	448	183.8	.7415	•
413	201.8	.1635	•	•	•	.0677	•	.7687	•	.3068	0690	•	•	449	183.8	.7317	•
414	201.8	.1606	•	•	•	.0873	•	.7560	•	.0933	1.759	•	•	450	183.8	.8567	•
415	201.8	.1545	•	•	•	.1160	•	.7295	•	.2898	0132	•	•	451	182.8	.8552	•
416	201.8	.1461	•	•	•	.1673	•	.6866	•	.2273	0171	•	•	452	182.8	.8513	•
417	197.8	.2670	•	•	•	.0336	•	.6795	•	.4816	0304	•	•	453	182.8	.9027	•
418	197.8	.2853	•	•	•	.0531	•	.6616	•	.4779	0488	•	•	454	182.8	.0700	•
419	197.8	.2829	•	•	•	.0703	•	.6468	•	.4728	0620	•	•	455	182.8	.8425	•
420	197.8	.2797	•	•	•	.0859	•	.6345	•	.4672	0785	•	•	456	182.8	.8484	•
421	197.8	.2749	•	•	•	.1214	•	.6037	•	.4572	1.091	•	•	457	182.8	.8513	•
422	197.8	.2656	•	•	•	.1761	•	.5583	•	.4402	1.577	•	•	458	182.8	.8567	•
423	195.8	.3559	•	•	•	.0343	•	.6148	•	.5541	0296	•	•	459	182.8	.6647	•
424	195.8	.3487	•	•	•	.0514	•	.5999	•	.0429	4067	•	•	460	182.8	.0203	•

TABLE 7
EXPERIMENTAL DATA AT 8 ATM. (continued)

RUN NO.	TEMP. DEG. R.	LIQUID MOL FRACTION			VAPOR MOL FRACTION			LIQUID MOL FRACTION			VAPOR MOL FRACTION		
		N2	AR	O2	N2	AR	O2	N2	AR	O2	N2	AR	O2
592	185.8	.7534	.0354	.2113	.8713	.0212	.1075	1279	195.8	.3411	.0417	.6173	.5485
593	183.8	.8564	.0207	.1229	.9273	.0123	.0604	1280	195.8	.3143	.2450	.4407	.4933
594	182.8	.9033	.0201	.0766	.9542	.0112	.0346	1281	195.8	.2997	.3660	.3344	.4710
595	182.8	.9044	.0457	.0499	.9491	.0269	.0239	1282	195.8	.2740	.5207	.2054	.2978
1246	181.8	.9645	.0355	.0355	.9834	.0166	.0166	1283	195.8	.2585	.6835	.0580	.4346
1247	199.8	.1126	.88742062	.7938	1284	191.8	.4970	.0086	.4944	.4130
1248	197.8	.1775	.82253043	.6957	1285	191.8	.4926	.0517	.4557	.6947
1249	191.8	.4142	.58585816	.4184	1286	191.8	.4462	.3391	.2147	.6850
1250	187.8	.6073	.39277481	.2519	1287	191.8	.4224	.5123	.0653	.6202
1251	184.8	.7771	.22299679	.1321	1288	189.8	.5739	.0373	.3889	.5912
1252	182.0	.9446	.05349708	.0292	1289	189.8	.5669	.0828	.3503	.7521
1253	181.6	.9691	.03099835	.0165	1290	189.8	.5621	.1163	.3217	.7357
1254	181.4	.9835	.01659915	.0085	1291	189.8	.5426	.2457	.2117	.7340
1255	181.2	.9965	.00359982	.0018	1292	189.8	.5223	.3915	.0862	.6826
1256	209.00089	.99120106	.9894	1293	187.8	.6227	.3095	.0678	.7633
1257	208.80260	.97400313	.9697	1294	187.8	.6094	.3581	.0325	.7529
1258	208.40709	.92910877	.9123	1295	185.8	.7578	.0059	.2363	.8790
1259	207.32000	.80002391	.7609	1296	185.8	.7597	.0266	.2137	.8743
1260	205.84186	.58144628	.5372	1297	185.8	.7517	.0702	.1781	.8669
1261	204.86224	.37766524	.3476	1298	185.8	.7256	.2362	.0382	.8368
1262	204.08511	.14898610	.1390	1299	182.8	.9085	.0139	.0776	.9588
1263	205.8	.0707	.0113	.9180	.1503	.0139	.8357	1300	182.8	.9042	.0596	.0362	.9497
1264	205.8	.0257	.2503	.7240	.0539	.2821	.6640	1301	181.8	.9644	.0080	.0277	.9835
1265	201.8	.1728	.0128	.8145	.3274	.0132	.6594	1302	182.8	.9609	.0170	.0222	.9810
1266	201.8	.1044	.4105	.4851	.1950	.4027	.4023	1303	181.8	.9582	.3117	.0102	.9785
1267	201.8	.0613	.5967	.3220	.5127	.5760	.2713	1827	209.00110	.9890
1268	201.8	.0679	.7204	.2118	.6889	.1790	.1790	1928	208.80302	.9698
1269	201.8	.0567	.8326	.1087	.1122	.7915	.0962	1829	197.8	.2801	.0685	.0396	.9602
1270	201.8	.0545	.8906	.0548	.1027	.8498	.0475	1830	195.8	.3500	.0454	.6514	.4706
1271	199.8	.1795	.3013	.5202	.3148	.2832	.4020	1831	203.89248	.5525	.4092
1272	199.8	.1560	.4659	.3780	.2744	.4284	.2972	1832	185.8	.7611	.0118	.0271	.8782
1273	199.8	.1362	.6018	.2619	.2447	.5460	.2093	1833	183.8	.8432	.1271	.0298	.9121
1274	199.8	.1215	.7635	.1151	.2213	.6847	.0940	1834	182.8	.9144	.0155	.0087	.0738
1275	197.8	.2154	.4646	.3200	.3615	.4007	.2378	1835	181.8	.9653	.0124	.0222	.9591
1276	197.8	.1972	.6106	.1923	.3343	.5191	.1466	1836	181.8	.9582	.0418	.0064	.0841
1277	197.8	.1641	.7775	.0382	.3102	.6603	.0295	1837	181.2	.9957	.00439977
													.0023

TABLE 8
EXPERIMENTAL DATA AT 10 ATM.

RUN NO.	TEMP. DEG.R.	LIQUID MOL FRACTION		VAPOR MOL FRACTION		RUN NO.	TEMP. DEG.R.	LIQUID MOL FRACTION		VAPOR MOL FRACTION	
		N2	AR	N2	AR			N2	AR	N2	AR
325	212.8	.0706	•	.9294	•	1439	•	.8561	365	197.8	•
326	209.8	.1463	•	.8537	•	2719	•	.7281	366	197.8	•
327	205.8	.2587	•	.7413	•	4329	•	.5671	367	197.8	•
328	201.8	.3844	•	.6156	•	5767	•	.4233	368	197.8	•
329	197.8	.5284	•	.4716	•	7067	•	.2933	369	197.8	•
330	193.8	.6881	•	.3119	•	8249	•	.1751	370	197.8	•
331	190.8	.8243	•	.1757	•	9077	•	.0923	371	193.8	•
332	188.8	.9203	•	.0797	•	9606	•	.0394	372	193.8	•
333	215.8	•	•	.0076	•	9924	•	.0099	373	193.8	•
334	215.5	•	•	.0352	•	9646	•	.0445	374	193.8	•
335	215.2	•	•	.0681	•	9319	•	.0833	375	193.8	•
336	214.9	•	•	.1024	•	8976	•	.1240	376	193.8	•
337	187.7	.9666	•	.0334	•	9810	•	.6190	377	191.8	•
338	188.2	.9384	•	.0614	•	9640	•	.3600	378	191.8	•
339	188.8	.9090	•	.0910	•	9460	•	.0540	379	191.8	•
340	189.3	.8801	•	.1199	•	9282	•	.0718	380	191.8	•
341	212.8	.0652	•	.0278	•	9070	•	.1306	381	189.8	•
342	212.8	.0611	•	.0457	•	.9936	•	.1218	382	189.8	•
343	212.8	.0567	•	.0596	•	.9836	•	.1154	383	189.8	•
344	212.8	.0536	•	.0779	•	.9686	•	.1079	384	189.8	•
345	212.8	.0470	•	.1085	•	.8446	•	.0947	385	189.8	•
346	212.8	.0395	•	.1524	•	.8081	•	.0791	386	189.8	•
347	208.8	.1662	•	.0330	•	.8009	•	.3027	387	188.8	•
348	208.8	.1621	•	.0496	•	.7883	•	.2971	388	188.8	•
349	208.8	.1592	•	.0653	•	.7755	•	.2992	389	188.8	•
350	208.8	.1566	•	.0814	•	.7620	•	.2847	390	188.8	•
351	208.8	.1524	•	.1131	•	.7346	•	.2741	391	160.9	•
352	208.8	.1430	•	.1430	•	.7090	•	.2580	392	1519	•
353	204.8	.0320	•	.2895	•	.6876	•	.4575	393	1501	•
354	204.8	.0297	•	.2797	•	.6493	•	.4575	394	1526	•
355	204.8	.0276	•	.2758	•	.6035	•	.4597	395	1597	•
356	204.8	.0271	•	.2714	•	.5616	•	.6471	396	1519	•
357	204.8	.0269	•	.2698	•	.5120	•	.4419	397	1510	•
358	204.8	.0259	•	.2595	•	.4874	•	.4355	398	1525	•
359	204.8	.0254	•	.2556	•	.4874	•	.4173	399	1516	•
360	204.8	.0246	•	.2516	•	.4933	•	.4173	400	1517	•
361	204.8	.0240	•	.2474	•	.5016	•	.4173	401	1518	•
362	200.8	.0402	•	.0681	•	.1141	•	.6161	402	1525	•
363	200.8	.0393	•	.1234	•	.4531	•	.5741	403	1519	•
364	200.8	.0365	•	.1770	•	.4373	•	.5611	404	1517	•

TABLE 8
EXPERIMENTAL DATA AT 10 ATM. (continued)

RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION			VAPOR MOL FRACTION			RUN NO.	TEMP. REG.R	LIQUID MOL FRACTION			VAPOR MOL FRACTION		
		N2	AR	O2	N2	AR	O2			N2	AR	O2	N2	AR	O2
1192	197.8	.4502	.54985035	.3965	1233	195.8	.5945	.0607	.3448	.7537	.0434	.2029
1193	193.8	.6400	.36007632	.2368	1234	195.8	.5862	.1151	.2988	.7403	.5816	.1761
1194	190.8	.0015	.19858780	.1220	1235	195.8	.5754	.1983	.2263	.7288	.1377	.1335
1195	188.2	.9529	.04719728	.0272	1236	195.8	.5438	.3528	.1033	.6963	.2416	.0622
1196	188.0	.9657	.03439800	.0200	1237	193.8	.6847	.0094	.3059	.8209	.0075	.1716
1197	187.5	.9948	.00529983	.0017	1238	193.8	.6349	.3232	.0418	.7592	.2172	.0236
1198	215.60488	.95120654	.9346	1239	191.8	.7736	.0123	.2141	.8738	.0078	.1165
1199	215.40683	.93170855	.9145	1240	191.8	.7717	.0223	.2061	.8774	.0130	.1096
1200	215.30723	.92770894	.9106	1241	191.8	.7705	.0372	.1922	.8737	.0228	.1036
1201	213.82500	.75002866	.7134	1242	188.8	.9273	.0074	.0654	.9621	.0044	.0336
1202	212.34866	.51345226	.4774	1243	188.8	.9286	.0202	.0512	.9626	.0116	.0258
1203	211.37065	.29347254	.2746	1244	188.8	.9272	.0399	.0329	.9611	.0228	.0161
1204	210.69671	.03299681	.0319	1245	188.8	.9242	.0463	.0295	.9589	.0264	.0147
1205	212.8	.0297	.0139	.9573	.1394	.0133	.6473	1800	215.70153	.98470195	.9805
1206	212.8	.0623	.0232	.9146	.1305	.0288	.8407	1801	215.60279	.97210350	.9650
1207	212.8	.0179	.2537	.7285	.0363	.2861	.6777	1802	211.07560	.24407721	.2279
1208	208.8	.1617	.0251	.8132	.3009	.0268	.6723	1803	210.69094	.09069143	.0857
1209	208.8	.1574	.0409	.8017	.2884	.0431	.6685	1804	212.8	.0676	.0144	.9180	.1357	.0167	.8476
1210	208.8	.1281	.1969	.6751	.2357	.1981	.5663	1805	212.8	.0643	.0286	.9071	.1292	.0327	.8381
1211	208.8	.1058	.3869	.5134	.1885	.3776	.4339	1806	208.8	.1683	.0115	.8202	.3073	.0118	.6809
1212	208.8	.0793	.5763	.3425	.1416	.5635	.2949	1807	208.8	.1659	.0253	.8089	.3013	.0255	.6732
1213	208.8	.0625	.7524	.1652	.1128	.7235	.1638	1808	204.8	.2634	.1119	.6246	.4302	.1023	.4674
1214	208.8	.0508	.9123	.0370	.0935	.8744	.0322	1809	212.8	.0672	.0100	.9228	.1355	.0113	.8532
1215	204.8	.2811	.0274	.6915	.4585	.0253	.5161	1810	204.8	.1893	.6308	.1800	.3082	.5510	.1407
1216	204.8	.2745	.0671	.6584	.4475	.0615	.4910	1811	200.8	.3992	.0743	.5265	.5841	.0519	.3540
1217	204.8	.2430	.2485	.5085	.3938	.2236	.3825	1812	200.8	.3964	.0999	.5037	.5782	.0824	.3394
1218	204.8	.2100	.4539	.3362	.3420	.4003	.2577	1813	197.8	.5210	.0104	.4687	.7001	.0078	.2921
1219	204.8	.1939	.6274	.1787	.3089	.5503	.1408	1814	195.8	.5936	.0229	.3834	.7588	.0166	.2246
1220	204.8	.1613	.7375	.0811	.2979	.6362	.0659	1815	195.8	.5691	.1958	.2351	.7189	.1384	.1427
1221	202.8	.2963	.3051	.3986	.4520	.2627	.2853	1816	193.8	.6843	.0137	.3020	.8199	.0094	.1707
1222	202.8	.2644	.5489	.1867	.4063	.4562	.1375	1817	193.8	.6382	.3279	.0339	.7645	.2166	.0189
1223	202.8	.3267	.0971	.0463	.3825	.5829	.0346	1818	191.8	.7775	.0138	.2087	.8794	.0091	.1115
1224	200.8	.4077	.0109	.5814	.5980	.0089	.3931	1819	191.8	.7757	.0138	.2087	.8794	.0091	.1115
1225	200.8	.4020	.0353	.5627	.5899	.0290	.3811	1820	191.8	.7776	.0160	.2064	.1979	.0167	.1063
1226	200.8	.3433	.4331	.2236	.5013	.3432	.1555	1821	191.8	.7735	.0374	.1891	.8807	.0101	.1092
1227	200.8	.3267	.5761	.0971	.4790	.4526	.0693	1822	191.8	.7500	.1960	.0540	.8481	.0238	.1004
1228	197.8	.5163	.0263	.4574	.6931	.0198	.2872	1823	190.8	.82121788	.90780922
1229	197.8	.5092	.0500	.4406	.5627	.0275	.3075	1824	187.6	.98260174	.99230077
1230	197.8	.4729	.3089	.2182	.6337	.2275	.1388	1825	187.5	.9839	.01619917	.0083	.0319
1231	197.8	.4624	.3994	.1382	.6188	.2918	.0893	1826	188.8	.9213	.0165	.0622	.9591	.0090	.0319

TABLE 9
EXPERIMENTAL DATA AT 12 ATM.

RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION			VAPOR MOL FRACTION			RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION			VAPOR MOL FRACTION		
		N2	AR	O2	N2	AR	O2			N2	AR	O2	N2	AR	O2
258	216.7	.11938017	.2185	...	295	206.8	.4015	.0376	.5610	.5758	.0319	.3923
259	212.8	.22477753	.3643	...	296	206.8	.3987	.0571	.5442	.5739	.0479	.3783
260	208.8	.34216579	.5214	...	297	206.8	.3965	.0748	.5287	.5670	.0637	.3693
261	204.8	.46025198	.6496	...	298	206.8	.3926	.0923	.5151	.5615	.0776	.3609
262	200.8	.62613739	.7712	...	299	206.8	.3843	.1320	.4837	.5514	.1104	.3382
263	197.8	.75242476	.8592	...	300	206.8	.3749	.1886	.4365	.5374	.1558	.3068
264	195.8	.84121556	.9107	...	301	202.8	.5453	.0390	.4156	.7048	.0300	.2652
265	194.8	.88481152	.9385	...	302	202.8	.5406	.0583	.4011	.7017	.0447	.2536
266	221.4	.01589842	303	202.8	.5377	.0803	.3821	.6962	.0610	.2428
267	221.10444	.5556	...	304	202.8	.5363	.0987	.3650	.6894	.0756	.2350
268	220.80787	.9213	...	305	202.8	.5307	.1392	.3302	.6840	.1044	.2116
269	220.51102	.8896	...	306	202.8	.5204	.2120	.2677	.6701	.1584	.1715
270	194.8	.86881312	.9180	...	307	199.8	.6663	.0379	.2958	.7960	.0270	.1770
271	195.3	.84181582	.8998	...	308	199.8	.6620	.0603	.2777	.7915	.0426	.1659
272	195.8	.81351665	309	199.8	.6583	.0852	.2565	.7860	.0603	.1537
273	196.3	.76582142	310	199.8	.6560	.1063	.2377	.7825	.0755	.1419
274	218.7	.05910313	.997	...	311	199.8	.6476	.1456	.2068	.7748	.1013	.1240
275	218.7	.05400499	.8961	...	312	199.8	.6382	.2193	.1425	.7603	.1534	.0863
276	218.7	.04930675	.8833	...	313	198.8	.7024	.0614	.2362	.8193	.0423	.1385
277	218.7	.04360927	.8637	...	314	198.8	.6954	.1093	.1953	.8098	.0749	.1154
278	193.3	.95280472	315	198.8	.6885	.1510	.1604	.8020	.1031	.0950
279	193.8	.92280772	316	198.8	.6789	.2164	.1048	.7904	.1476	.0621
280	218.7	.04111223	.8365	...	317	196.8	.7936	.0377	.1687	.8804	.0245	.0951
281	218.7	.03071684	.8009	...	318	196.8	.7899	.0575	.1526	.8767	.0376	.0856
282	194.3	.89811019	319	196.8	.7867	.0749	.1384	.8732	.0674	.0494
283	214.8	.16120366	.8032	...	320	196.8	.7828	.0974	.1198	.8663	.0642	.0675
284	214.8	.15640531	.7905	...	321	196.8	.7764	.1333	.0903	.8622	.0971	.0507
285	214.8	.15240698	.7779	...	322	196.8	.7656	.1836	.0506	.8533	.1183	.0284
286	214.8	.14740879	.7648	...	323	195.8	.8333	.0564	.1103	.9015	.0371	.0614
287	214.8	.14621303	.7295	...	324	195.8	.8270	.0934	.0797	.6959	.0597	.0444
288	214.8	.12871835	.6878	...	325	195.8	.6629	.0226	.3145	.7992	.0172	.1836
289	210.8	.03376962	.4338	...	326	198.8	.7069	.0190	.2741	.8266	.0126	.1609
290	210.8	.26700545	.6785	...	327	198.8	.5228	.567	.7021	.0435	.2544	.8231
291	210.8	.26270490	.6663	...	328	196.8	.5152	.651	.7930	.0203	.1470	.0300
292	210.8	.25920842	.6567	...	329	195.8	.5057	.788	.8402	.0159	.1439	.0123
293	210.8	.25141205	.6282	...	330	195.8	.570	.1140	.4830	.8363	.1245	.9068
294	210.8	.24711810	.5720	...	331	195.8	.570	.1672	.3906	.1135	.9661	...
													.0339	.9799	...

TABLE 9
EXPERIMENTAL DATA AT 12 ATM. (continued)

RUN NO.	TEMP. DEG.R.	Liquid MOL FRACTION N2 AR 02	VAPOR MOL FRACTION N2 AR 02	RUN NO.	TEMP. DEG.R.	Liquid MOL FRACTION N2 AR 02	VAPOR MOL FRACTION N2 AR 02
1136	212.8	.1072	.8928	1174	199.8	.6227	.3280
1137	210.8	.1699	.8301	1175	198.8	.6730	.2711
1138	204.8	.3896	.6104	1176	196.8	.8044	.0061
1139	199.8	.6152	.3848	1177	196.8	.7998	.0188
1140	193.0	.9778	.0222	1178	196.8	.7973	.0340
1141	221.50198	1179	195.8	.8308	.1209
1142	221.20554	1179	195.8	.8083	.0483
1143	221.00726	1180	194.3	.9237	.0075
1144	219.82094	1181	194.3	.9223	.0184
1145	218.73670	1182	194.3	.9233	.0224
1146	217.75377	1183	194.3	.9182	.0370
1147	216.85439	1184	194.3	.9158	.0484
1148	216.49159	1185	194.3	.9138	.0667
1149	218.70665	1186	193.3	.9684	.0069
1150	218.76622	1187	193.3	.9676	.0143
1151	214.81639	1188	193.3	.9662	.0233
1152	214.81554	1189	194.3	.9273	.0424
1153	214.81643	1190	194.3	.9121	.0103
1154	214.81026	1191	194.3	.9184	.0116
1155	214.80787	1192	194.3	.9205	.0116
1156	214.80662	1193	194.3	.9233	.0153
1157	214.80581	1194	194.3	.9224	.0272
1158	214.80511	1195	194.3	.9182	.0227
1159	210.82265	1196	194.3	.9538	.0235
1160	210.83393	1197	194.3	.9512	.0293
1161	210.84317	1198	194.3	.9493	.0293
1162	210.81940	1199	194.3	.9485	.0293
1163	210.81617	1200	194.3	.9477	.0293
1164	206.84075	1201	194.3	.9469	.0293
1165	206.84035	1202	194.3	.9461	.0293
1166	206.83570	1203	194.3	.9453	.0293
1167	206.83414	1204	194.3	.9445	.0293
1168	206.83203	1205	194.3	.9437	.0293
1169	202.84970	1206	194.3	.9429	.0293
1170	202.84835	1207	194.3	.9421	.0293
1171	199.86670	1208	194.3	.9413	.0293
1172	199.86635	1209	194.3	.9405	.0293
1173	199.85642	1210	194.3	.9397	.0293

TABLE 10
EXPERIMENTAL DATA AT 14 ATM.

RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION			VAPOR MOL FRACTION			RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION			VAPOR MOL FRACTION		
		N2	AR	O2	N2	AR	O2			N2	AR	O2	N2	AR	O2
194	223.7	• 0.603	• • •	• 0.307	• 1.308	• • •	• 0.692	235	204.8	• 0.682	• 279.3	• 7761	• 0.507	• 1732	
195	219.7	• 1.716	• • •	• 0.254	• 0.293	• • •	• 0.707	236	204.8	• 0.643	• 2582	• 7713	• 0.593	• 1594	
196	216.7	• 0.246	• • •	• 0.744	• 0.405	• • •	• 0.594	237	204.8	• 0.642	• 1179	• 2395	• 7658	• 0.651	• 1491
197	211.5	• 0.405	• • •	• 0.594	• 0.572	• • •	• 0.427	238	204.8	• 0.642	• 1406	• 2169	• 7627	• 1.023	• 1350
198	207.3	• 0.506	• • •	• 0.440	• 0.703	• • •	• 0.296	239	204.8	• 0.629	• 2082	• 1619	• 7520	• 1.479	• 1001
199	203.8	• 0.702	• • •	• 0.297	• 0.198	• • •	• 1.802	240	202.8	• 0.739	• 0.040	• 2205	• 8419	• 0.282	• 1299
200	200.8	• 0.827	• • •	• 1.726	• 0.017	• • •	• 0.983	241	202.8	• 0.735	• 0.671	• 1978	• 8303	• 0.470	• 1227
201	198.8	• 0.914	• • •	• 0.851	• 0.953	• • •	• 0.463	242	202.8	• 0.727	• 0.857	• 1873	• 8275	• 0.595	• 1130
202	226.5	• • •	• 0.215	• 0.785	• • •	• 0.263	• 9737	243	202.8	• 0.725	• 1.035	• 1711	• 8249	• 0.723	• 1028
203	226.2	• • •	• 0.452	• 0.954	• • •	• 0.523	• 0.447	244	202.8	• 0.715	• 1.482	• 1359	• 8168	• 1.021	• 0.811
204	225.9	• • •	• 0.620	• 0.915	• • •	• 0.983	• 0.917	245	202.8	• 0.707	• 1.964	• 0.961	• 8081	• 1.344	• 0.575
205	225.6	• • •	• 0.902	• 0.996	• • •	• 1.268	• 0.673	246	201.8	• 0.721	• 0.651	• 1627	• 8594	• 0.452	• 0.954
206	197.8	• 0.958	• 0.412	• • •	• 0.974	• • •	• 0.260	• 247	201.8	• 0.765	• 1.066	• 1279	• 8544	• 0.722	• 0.734
207	198.3	• 0.931	• 0.682	• • •	• 0.956	• • •	• 0.435	• 248	201.8	• 0.760	• 1.554	• 0.845	• 8463	• 1.044	• 0.493
208	198.8	• 0.898	• 1.002	• • •	• 0.935	• • •	• 0.645	• 249	201.8	• 0.748	• 2039	• 0.475	• 8374	• 1.351	• 0.275
209	199.3	• 0.757	• 1.243	• • •	• 0.920	• • •	• 0.796	• 250	199.8	• 0.865	• 0.438	• 912	• 9204	• 0.285	• 0.510
210	224.7	• 0.422	• 0.169	• 0.941	• 0.821	• 0.198	• 0.898	251	199.8	• 0.860	• 0.713	• 685	• 9145	• 0.475	• 0.380
211	224.7	• 0.391	• 0.269	• 0.934	• 0.766	• 0.320	• 0.891	252	199.8	• 0.856	• 0.962	• 0.473	• 9088	• 0.623	• 0.286
212	224.7	• 0.357	• 0.384	• 0.925	• 0.697	• 0.452	• 0.851	253	199.8	• 0.953	• 1.146	• 0.321	• 9069	• 0.750	• 0.181
213	224.7	• 0.329	• 0.514	• 0.641	• 0.641	• 0.603	• 0.675	254	199.8	• 0.851	• 1.292	• 0.198	• 9057	• 0.533	• 0.111
214	224.7	• 0.273	• 0.760	• 0.959	• 0.533	• 0.897	• 0.857	255	199.8	• 0.869	• 0.251	• 1057	• 9251	• 0.164	• 0.596
215	224.7	• 0.173	• 1.209	• 0.618	• 0.353	• 1.342	• 0.305	256	198.8	• 0.911	• 0.510	• 0.376	• 9442	• 0.332	• 0.226
216	219.7	• 1.672	• 0.917	• 0.931	• 0.294	• 0.259	• 0.235	257	198.8	• 0.904	• 0.772	• 0.186	• 9410	• 0.485	• 0.105
217	219.7	• 1.644	• 0.306	• 0.630	• 0.326	• 0.321	• 0.685	258	199.8	• 0.851	• 1.292	• 0.198	• 8810	• 1.407	• 0.593
218	219.7	• 1.613	• 0.647	• 0.791	• 0.735	• 0.493	• 0.677	259	203.8	• 0.704	• 0.411	• 0.251	• 8188	• 0.285	• 1812
219	219.7	• 1.562	• 0.607	• 0.795	• 0.270	• 0.633	• 0.666	260	202.8	• 0.736	• 0.639	• 0.995	• 8345	• 0.458	• 1.197
220	219.7	• 1.509	• 0.976	• 0.751	• 0.256	• 1.006	• 0.643	261	201.8	• 0.773	• 0.623	• 1.605	• 8631	• 0.413	• 0.951
221	219.7	• 1.420	• 1.531	• 0.704	• 0.240	• 1.530	• 0.409	262	199.8	• 0.871	• 0.405	• 0.693	• 9234	• 0.269	• 0.497
222	214.8	• 3.098	• 0.230	• 4.663	• 4.661	• 0.219	• 5.171	263	200.8	• 0.309	• 0.98	• 1.902	• 8897	• 0.269	• 1.103
223	214.8	• 3.104	• 0.368	• 4.527	• 4.511	• 0.346	• 5.043	264	197.8	• 0.969	• 0.307	• 9835	• 0.307	• 0.165	• 0.165
224	214.8	• 3.060	• 0.490	• 4.430	• 4.430	• 0.396	• 5.009	265	217.7	• 1.041	• 0.959	• 0.1713	• 8287	• 0.1713	• 0.165
225	214.8	• 3.031	• 0.671	• 6.296	• 4.499	• 0.624	• 4.977	266	214.8	• 2014	• 7.986	• 0.3079	• 6921	• 0.251	• 0.251
226	214.8	• 2.976	• 1.151	• 5.944	• 4.355	• 1.037	• 4.508	267	209.8	• 3.666	• 6.134	• 0.5224	• 4776	• 0.248	• 0.248
227	214.8	• 2.779	• 1.691	• 5.530	• 4.172	• 1.546	• 4.282	268	204.8	• 6.032	• 3.968	• 0.7230	• 2770	• 0.158	• 0.158
228	209.8	• 4.715	• 0.242	• 5.053	• 6.339	• 0.200	• 3.460	269	201.8	• 7.552	• 2.448	• 0.8367	• 1.633	• 0.091	• 0.091
229	209.8	• 4.641	• 0.443	• 4.699	• 6.263	• 0.364	• 3.373	270	198.0	• 0.957	• 0.423	• 0.3079	• 9749	• 0.251	• 0.251
230	209.5	• 4.676	• 1.512	• 5.944	• 4.562	• 0.621	• 4.662	271	197.7	• 9.752	• 0.248	• 0.248	• 9846	• 0.154	• 0.154
231	209.8	• 4.573	• 1.667	• 4.354	• 4.172	• 0.674	• 3.012	272	197.5	• 9.842	• 0.158	• 0.158	• 9909	• 0.091	• 0.091
232	209.6	• 4.442	• 1.505	• 4.014	• 4.014	• 0.600	• 1.218	273	197.4	• 9.890	• 0.110	• 0.110	• 9939	• 0.061	• 0.061
233	209.6	• 4.362	• 2.252	• 3.366	• 5.954	• 1.804	• 2.341	274	226.6	• 0.039	• 0.962	• 0.0382	• 9818	• 0.1A2	• 0.1A2
234	204.8	• 0.655	• 0.430	• 3.012	• 0.705	• 0.316	• 1.879	275	226.4	• 0.039	• 0.962	• 0.0382	• 9818	• 0.4P0	• 0.4P0

TABLE 10
EXPERIMENTAL DATA AT 14 ATM. (continued)

RUN NO.	TEMP. DEG.R.	LIQUID MOL FRACTION		VAPOR MOL FRACTION		RUN NO.	TEMP. DEG.R.	LIQUID MOL FRACTION		VAPOR MOL FRACTION		
		N2	AR	02	N2	AR	02	N2	AR	02	N2	AR
1076	226.3	••••	•0499	•9501	••••	•0608	•9392	1117	207.8	•4931	•3793	•1276
1077	225.5	••••	•1330	•8670	••••	•1581	•8419	1118	207.8	•4829	•4651	•6267
1078	224.7	••••	•2356	•7644	••••	•2650	•7350	1119	204.8	•6684	•0111	•6148
1079	223.2	••••	•4624	•5376	••••	•4925	•5075	1120	204.8	•6659	•0233	•3496
1080	222.2	••••	•6800	•3200	••••	•6989	•3011	1121	204.8	•6633	•0393	•0520
1081	221.6	••••	•8804	•1196	••••	•8847	•1153	1122	204.8	•6208	•3073	•7917
1082	221.4	••••	•9653	•0347	••••	•9678	•0322	1123	201.8	•7926	•0119	•0159
1083	224.7	•0449	•0168	•9363	•0843	•0195	•8962	1124	201.8	•7934	•0227	•7915
1084	219.7	•1703	•0209	•8096	•2858	•0198	•6945	1125	201.8	•7896	•0380	•0255
1085	219.7	•1594	•0730	•7676	•2684	•0718	•6598	1126	201.8	•7875	•0526	•0252
1086	219.7	•1529	•0997	•7474	•2578	•1014	•6408	1127	201.8	•7866	•0618	•2187
1087	219.7	•1295	•2491	•6214	•2171	•2488	•5341	1128	198.8	•9592	•0076	•0159
1088	219.7	•0967	•4596	•4437	•1599	•4529	•3872	1129	198.8	•9260	•0207	•0253
1089	219.7	•0746	•6313	•2941	•1253	•6141	•2606	1130	198.8	•9232	•0262	•0156
1090	219.7	•0608	•7251	•1642	•1036	•7483	•1481	1131	198.8	•9266	•0389	•9591
1091	219.7	•0559	•8547	•0894	•0946	•8234	•0820	1132	197.8	•9766	•0062	•0248
1092	217.7	•2291	•0198	•7511	•3566	•0200	•6133	1133	197.8	•9725	•0139	•0249
1093	217.7	•2127	•0979	•6894	•3393	•0952	•5656	1134	197.8	•9664	•0255	•0161
1094	217.7	•1870	•2461	•5667	•2961	•2373	•4666	1135	226.2	••••	•0504	•0213
1095	217.7	•1563	•4359	•4078	•2489	•4123	•3388	1136	221.4	••••	•9496	•032
1096	217.7	•1283	•6746	•1971	•2054	•6240	•1706	1137	224.7	•1225	•0136	•0077
1097	217.7	•1093	•8810	•0097	•1783	•6133	•0084	1138	219.7	•1664	•0085	•0047
1098	214.8	•3146	•0175	•6679	•4743	•0165	•5093	1139	219.7	•1440	•0181	•0194
1099	214.8	•3063	•0530	•6407	•4616	•0489	•1760	1140	214.8	•2580	•0492	•4512
1100	214.8	•3011	•0898	•6091	•4507	•0809	•4685	1141	211.8	•3986	•0477	•5537
1101	214.8	•2699	•2737	•4564	•4014	•2436	•3550	1142	204.8	•6563	•0237	•8252
1102	214.8	•2469	•4283	•3248	•3567	•3778	•2555	1143	201.8	•7464	•2536	•8218
1103	214.8	•2127	•6567	•1246	•3301	•5704	•0995	1144	199.8	•8590	•1034	•7915
1104	214.8	•2135	•7334	•0531	•3217	•6352	•0432	1145	198.8	•9192	•0089	•0194
1105	211.8	•4064	•0473	•5463	•5681	•0386	•3933	1146	198.8	•9171	•0231	•0149
1106	211.8	•3939	•1114	•4948	•5473	•0942	•3585	1147	198.8	•9162	•0303	•0193
1107	211.8	•3854	•1701	•4445	•5351	•1438	•3211	1148	198.8	•9156	•0445	•0194
1108	211.8	•3462	•4446	•2092	•4779	•3662	•1559	1149	198.8	•9117	•0549	•0216
1109	211.8	•3242	•5921	•0836	•4557	•4914	•0529	1150	197.8	•9673	•0077	•0216
1110	209.8	•4608	•0130	•5062	•6410	•0107	•3484	1151	197.8	•9659	•0158	•0099
1111	209.8	•4750	•0313	•4938	•6353	•0250	•3397	1152	197.8	•9650	•0248	•0285
1112	209.8	•4696	•0614	•4700	•4265	•0496	•3238	1153	198.0	•9507	•0493	•0055
1113	209.8	•4297	•3123	•2580	•5723	•2487	•1790	1154	198.7	•9662	•0338	•0139
1114	209.8	•4002	•5358	•0640	•5374	•4178	•0448	1155	197.5	•9791	•0209	•0130
1115	207.8	•5382	•0951	•3568	•6831	•0738	•2431	1156	197.4	•9851	•0149	•0088
1116	207.8	•5190	•2138	•2683	•6582	•1624	•1794	1157	197.7	•9632	•0368	•0232

TABLE 11
EXPERIMENTAL DATA AT 16 ATM.

RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION				VAPOR MOL FRACTION N2 AR 02	RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION				VAPOR MOL FRACTION N2 AR 02
		N2	AR	02	N2				N2	AR	02	N2	
130	227.7	.9570	•	•	•	.9130	171	209.8	.6352	•	0328	.3320	•
131	224.7	.1585	•	•	•	.8412	172	209.8	.6290	•	0500	.1209	•
132	220.7	.2741	•	•	•	.7259	173	209.8	.6275	•	0777	.2948	•
133	216.7	.3981	•	•	•	.6019	174	209.8	.6233	•	1166	.2601	•
134	211.8	.5444	•	•	•	.4556	175	209.8	.5075	•	1773	.2152	•
135	207.8	.7174	•	•	•	.2826	176	206.8	.7593	•	0206	.2201	•
136	204.8	.8501	•	•	•	.1499	177	206.8	.7542	•	0345	.2113	•
137	202.8	.9292	•	•	•	.0706	178	206.8	.7515	•	0565	.1920	•
138	231.2	•	•	•	•	.0125	179	206.8	.7487	•	0750	.1763	•
139	230.9	•	•	•	•	.0412	180	206.8	.7435	•	1114	.1452	•
140	230.6	•	•	•	•	.0744	181	206.8	.7277	•	1631	.1092	•
141	230.3	•	•	•	•	.1043	182	205.8	.7915	•	0433	.1652	•
142	201.8	.9725	•	•	•	.0272	183	205.6	.7845	•	0653	.1503	•
143	202.3	.9424	•	•	•	.0576	184	205.8	.7823	•	0952	.1225	•
144	202.8	.9153	•	•	•	.0847	185	205.8	.7680	•	1576	.0743	•
145	203.3	.8658	•	•	•	.1142	186	203.8	.8830	•	0232	.0938	•
146	229.7	.8348	•	•	•	.0123	187	203.8	.8764	•	0395	.0840	•
147	229.7	.0315	•	•	•	.0238	188	203.8	.8731	•	0581	.0688	•
148	229.7	.0262	•	•	•	.0343	189	203.8	.8735	•	0616	.0649	•
149	229.7	.0271	•	•	•	.0407	190	203.8	.8648	•	1166	.0186	•
150	229.7	.3232	•	•	•	.0678	191	203.8	.8643	•	1232	.0125	•
151	229.7	.6124	•	•	•	.1249	192	202.8	.9208	•	0400	.9208	•
152	224.7	.1614	•	•	•	.0156	193	202.8	.9183	•	0637	.0180	•
153	224.7	.1576	•	•	•	.0289	194	202.8	.9162	•	1762	.0637	•
154	224.7	.1563	•	•	•	.0367	195	202.8	.9135	•	0304	.7079	•
155	224.7	.1525	•	•	•	.0467	196	202.8	.9090	•	0463	.9043	•
156	224.7	.1452	•	•	•	.0790	197	202.8	.8954	•	0435	.8711	•
157	224.7	.1337	•	•	•	.1375	198	202.8	.8937	•	0397	.9113	•
158	219.7	.3548	•	•	•	.0178	199	202.8	.8904	•	0276	.9154	•
159	219.7	.3814	•	•	•	.0304	200	202.8	.8854	•	0141	.9284	•
160	219.7	.2974	•	•	•	.0478	201	202.8	.8837	•	0276	.9154	•
161	219.7	.2941	•	•	•	.0557	202	202.8	.8822	•	0141	.9284	•
162	219.7	.2651	•	•	•	.1130	203	202.8	.8808	•	0141	.9284	•
163	219.7	.2747	•	•	•	.1553	204	202.8	.8808	•	0143	.9284	•
164	214.8	.4557	•	•	•	.0215	205	202.8	.6083	•	0180	.3737	•
165	214.8	.4576	•	•	•	.0316	206	202.8	.6049	•	0293	.4293	•
166	214.8	.4524	•	•	•	.0458	207	202.8	.6026	•	0393	.3580	•
167	214.8	.4507	•	•	•	.0607	208	202.8	.6019	•	0523	.4135	•
168	214.8	.4419	•	•	•	.1003	209	202.8	.5880	•	0834	.3286	•
169	214.8	.4278	•	•	•	.1684	210	202.8	.5718	•	1006	.2884	•
170	209.8	.6389	•	•	•	.0194	211	202.0	.7644	•	0146	.3417	•

TABLE II
EXPERIMENTAL DATA AT 16 ATM. (continued)

RUN NO.	TEMP. DEG. K	LIQUID MOL FRACTION N2 AR O2	VAPOR MOL FRACTION N2 AR O2	RUN NO.	TEMP. DEG. R	LIQUID MOL FRACTION N2 AR O2	VAPOR MOL FRACTION N2 AR O2
1000	201.6	.49552	.01448	1049	211.8	.5058	.0648
1000	226.09302	1050	209.8	.6467	.3262
1010	226.30698	1051	209.8	.0124	.0093
1010	226.78058	1052	209.8	.6392	.2210
1011	227.76902	1053	209.8	.1502	.0375
1012	227.73098	1054	209.8	.6166	.2009
1013	229.25264	1055	209.8	.4974	.1249
1014	230.82391	1056	206.8	.5026	.0731
1014	230.87619	1057	206.8	.4926	.0731
1015	231.00573	1058	206.8	.2686	.1212
1015	231.09427	1059	206.8	.7314	.1389
1016	231.10407	1060	206.8	.0690	.0061
1016	231.19593	1061	206.8	.0410	.0061
1017	224.70349	1062	203.8	.9657	.0096
1017	224.70377	1063	203.8	.0393	.2255
1018	224.72601	1064	203.8	.2561	.0299
1018	224.76110	1065	203.8	.1795	.0299
1019	224.74502	1066	203.8	.4137	.0418
1019	224.74680	1067	203.8	.0478	.0418
1020	224.75589	1068	202.8	.3719	.0321
1021	224.70521	1069	201.8	.7344	.0321
1022	224.70390	1070	201.8	.2146	.0170
1022	224.78716	1071	201.8	.0894	.0170
1023	224.79564	1072	201.8	.0090	.0170
1024	221.722265	1073	201.8	.0741	.0170
1025	221.72152	1074	201.8	.6376	.0170
1026	221.72006	1075	201.8	.1867	.0170
1027	221.76510	1076	201.8	.2015	.0170
1028	221.71475	1077	201.8	.6760	.0170
1029	219.73018	1078	201.8	.0222	.0170
1030	219.726A7	1079	201.8	.0949	.0170
1031	219.775A9	1080	201.8	.2502	.0170
1032	219.71519	1081	201.8	.8183	.0170
1033	219.73018	1082	201.8	.0498	.0170
1034	219.72001	1083	201.8	.6075	.0170
1035	219.71863	1084	201.8	.1834	.0170
1036	216.77352	1085	201.8	.0767	.0170
1037	216.73644	1086	201.8	.1322	.0170
1038	216.74672	1087	201.8	.4984	.0170
1039	216.73417	1088	201.8	.2001	.0170
1040	216.71863	1089	201.8	.7645	.0170
1041	214.83005	1090	201.8	.6581	.0170
1042	214.84672	1091	201.8	.0114	.0170
1043	214.84477	1092	201.8	.0914	.0170
1044	214.84259	1093	201.8	.3140	.0170
1045	214.83783	1094	201.8	.4681	.0170
1046	211.85556	1095	201.8	.0865	.0170
1047	211.85306	1096	201.8	.2475	.0170
1048	211.85174	1097	201.8	.3409	.0170
						.1417	.1402
						.2611	.2245
						.0966	.1866
						.2611	.206.8
						.1417	.1402

TABLE 12
EXPERIMENTAL DATA AT 18 ATM.

RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION		VAPOR MOL FRACTION		RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION		VAPOR MOL FRACTION		
		N2	AR	02	N2	AR	02	N2	AR	02	N2	AR
56	231.8	.08739127	.14278573	109	214.8	.5674	.1665	.2662
67	227.8	.19598041	.30436957	110	209.8	.7935	.0189	.1875
68	224.7	.27847216	.41685832	111	209.8	.7874	.0341	.1786
69	220.7	.40235977	.54004600	112	209.8	.7851	.0539	.1610
70	216.7	.53204680	.66553345	113	209.8	.7810	.0733	.1457
71	211.8	.71202880	.81761824	114	209.8	.7754	.1114	.1133
72	208.8	.84511549	.89661034	115	209.8	.7623	.1844	.0533
73	206.8	.92830717	.95760424	116	207.8	.8780	.0177	.1043
74	235.20372	.96280435	117	207.8	.8736	.0310	.0954
75	234.90682	.93160805	118	207.8	.8745	.0486	.0768
76	234.61035	.89651202	119	207.8	.8670	.0662	.0668
77	234.31340	.86601553	120	207.8	.8598	.0905	.0496
78	205.3	.988601149922	121	207.8	.8587	.1217	.0196
79	205.8	.969303979737	122	206.8	.9213	.0305	.0482
80	206.3	.934106599563	123	206.8	.9143	.0471	.0386
81	206.8	.904009609348	124	206.8	.9159	.0603	.0238
82	233.7	.03450240	.94140593	125	206.8	.9067	.0811	.0123
83	233.70292	.04759233	126	205.8	.9671	.0127	.0202
84	233.70238	.06219141	127	205.8	.9696	.0045	.0258
85	233.70172	.10758752	128	205.8	.9670	.0136	.0194
86	229.7	.1410168	.84312270	129	205.8	.9617	.0323	.0060
87	229.7	.13030221	.84762206	130	205.8	.96529148
88	229.71350	.03568294	131	205.8	.7357235
89	229.71307	.04558238	132	205.8	.72704096
90	229.71182	.07298089	133	205.8	.84262730
91	229.71195	.11937702	134	205.8	.5371574
92	224.71195	.11937093	135	205.8	.5369616
93	224.72754	.01534066	136	205.8	.2353304
94	224.72656	.02457098	137	205.8	.5372247
95	224.727183951	138	205.8	.5817541
96	224.72754	.01534066	139	205.8	.57312247
97	224.72626	.09406434	140	205.8	.5638542
98	219.74279	.13936128	141	205.8	.4914542
99	219.74205	.01825613	142	205.8	.42394285
100	219.74316	.02685416	143	205.8	.5634285
101	219.74276	.04305294	144	205.8	.5634285
102	219.74218	.05575225	145	205.8	.5644075
103	219.74218	.08994883	146	205.8	.5754040
104	214.85917	.01803902	147	205.8	.58736857
105	214.85882	.02693849	148	205.8	.5864040
106	214.85906	.04233670	149	205.8	.58734040
107	214.85806	.06013593	150	205.8	.58734040
108	214.85797	.09743229	151	205.8	.58734040

TABLE 12
EXPERIMENTAL DATA AT 18 ATM. (continued)

RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION N2 AR 02	VAPOR MOL FRACTION N2 AR 02	RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION N2 AR 02	VAPOR MOL FRACTION N2 AR 02
943	205.6	.9748	.0252	986	214.8	.6009	.0127
944	205.5	.9797	.0203	987	214.8	.5568	.3236
945	235.40181	988	212.8	.6834	.0119
946	235.30265	989	212.8	.6763	.0542
947	235.00558	990	212.8	.6678	.0966
948	233.72039	991	212.8	.6553	.1555
949	232.43892	992	212.8	.6420	.2815
950	231.45770	993	209.8	.8003	.0124
951	230.58189	994	209.8	.7974	.0425
952	230.39064	995	209.8	.7730	.0279
953	229.71372	996	207.8	.8863	.0106
954	229.71066	997	207.8	.8817	.0404
955	229.70839	998	206.8	.9308	.0057
956	229.70618	999	206.8	.9278	.0160
957	229.70421	995	209.8	.1992	.0279
958	229.70266	996	207.8	.8863	.0073
959	226.72119	997	207.8	.8817	.0779
960	226.71301	998	206.8	.9308	.0124
961	226.71676	999	206.8	.9278	.0124
962	226.73178	995	209.8	.1992	.0279
963	226.71283	996	207.8	.8863	.0073
964	226.71109	997	207.8	.8817	.0779
965	224.71056	998	206.8	.9308	.0124
966	224.78531	999	206.8	.9278	.0124
967	224.72730	995	209.8	.1992	.0279
968	224.70442	996	207.8	.8863	.0073
969	224.72633	997	207.8	.8817	.0779
970	224.70904	998	206.8	.9308	.0124
971	224.72403	999	206.8	.9278	.0124
972	221.73547	995	209.8	.1992	.0279
973	221.73361	996	207.8	.8863	.0073
974	221.73200	997	207.8	.8817	.0779
975	221.72848	998	206.8	.9308	.0124
976	221.72706	999	206.8	.9278	.0124
977	219.74342	995	209.8	.1992	.0279
978	219.73958	996	207.8	.8863	.0073
979	219.73200	997	207.8	.8817	.0779
980	219.73771	998	206.8	.9308	.0124
981	216.73478	999	206.8	.9278	.0124
982	216.75315	995	209.8	.1992	.0279
983	216.75193	996	207.8	.8863	.0073
984	216.74931	997	207.8	.8817	.0779
985	216.74902	998	206.8	.9308	.0124
986	216.74721	999	206.8	.9278	.0124

TABLE 13
EXPERIMENTAL DATA AT 20 ATM.

RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION				RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION				VAPOR MOL FRACTION N2 AR 02
		N2	AR	02	N2			N2	AR	02	N2	AR
1	232.5	.17498251	.27247276	42	214.8	.7389	.0444	.2167
2	223.7	.42325768	.56334367	43	214.8	.7353	.0647	.2000
3	214.1	.77152285	.85041496	44	214.8	.7315	.0763	.1923
4	211.0	.89871013	.93680622	45	214.8	.7234	.1231	.1270
5	235.6	.09409060	.15538447	46	214.8	.7184	.1789	.1009
6	227.6	.31446856	.43315659	47	212.8	.8161	.0644	.1027
7	221.7	.48035197	.61643836	48	212.8	.8123	.0449	.1429
8	212.8	.82221778	.88111189	49	212.8	.8177	.0171	.1652
9	239.50980	.99200102	50	212.8	.8115	.0711	.1174
10	239.40161	.98390197	51	212.8	.8023	.1073	.0904
11	239.20449	.95510519	52	212.8	.8023	.0942	.8646
12	238.90581	.94190633	53	212.8	.7960	.1451	.8592
13	209.8	.991300879367	54	211.8	.8608	.0253	.1139
14	209.3	.962803729943	55	211.8	.8552	.0539	.0909
15	209.8	.936406369734	56	211.8	.8492	.0942	.0566
16	210.3	.909509049557	57	211.8	.8466	.1243	.0290
17	234.7	.10670211	.87229356	58	210.8	.9045	.0103	.0371
18	234.7	.10450307	.86491800	59	210.8	.9012	.0237	.0720
19	234.7	.10840341	.95751727	60	210.8	.8979	.0380	.0171
20	234.7	.10340594	.43731680	61	210.8	.8988	.0448	.0364
21	234.7	.11700102	.87271865	62	210.8	.8989	.0575	.0189
22	234.7	.11630175	.86620113	63	210.8	.8947	.0901	.0064
23	229.7	.25910090	.73158662	64	209.8	.9438	.0254	.0527
24	229.7	.26570151	.71923751	65	209.8	.9445	.0453	.0373
25	229.7	.25150231	.72543754	66	209.8	.9445	.0453	.0281
26	229.7	.24820326	.71923689	67	209.8	.78040401
27	229.7	.24560476	.70663610	68	209.8	.94810281
28	229.7	.23371037	.66263704	69	209.8	.9445	.0453	.0373
29	224.7	.38930247	.58605203	70	214.1	.78040437
30	224.7	.38240370	.58065184	71	221.7	.49810153
31	224.7	.37330581	.56865094	72	217.7	.63940639
32	224.7	.37110863	.54265018	73	209.8	.9467	.0360	.0160
33	224.7	.36441326	.50294974	74	212.8	.8216	.0777	.0281
34	224.7	.34752330	.41954677	75	214.8	.7427	.0804	.1445
35	219.7	.54860371	.41436318	76	219.7	.5686	.0183	.0368
36	219.7	.55250371	.41046287	77	229.7	.4397	.0254	.0160
37	219.7	.54670589	.39445018	78	219.7	.4215	.0641	.0373
38	219.7	.52440990	.37664974	79	214.8	.3862	.0235	.0194
39	219.7	.51321530	.33386436	80	211.8	.2052	.0116	.1235
40	219.7	.50422283	.26756247	81	212.8	.2702	.0116	.8194
41	214.8	.74110255	.23340189	82	212.8	.1537	.0576	.0162

TABLE 13
EXPERIMENTAL DATA AT 20 ATM. (continued)

RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION N2 AR 02	VAPOR MOL FRACTION N2 AR 02	RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION N2 AR 02	VAPOR MOL FRACTION N2 AR 02
834	208.7	.9951	.0049	876	221.7	.4510	.2474
835	209.0	.9792	.0208	877	221.7	.4420	.3213
836	209.4	.9599	.0401	878	221.7	.4154	.4958
837	212.8	.7936	.2064	879	219.7	.5591	.0132
838	217.7	.5707	.4293	880	219.7	.5575	.0472
839	229.7	.1290	.8710	881	219.7	.5508	.0786
840	231.7	.0671	.9329	882	219.7	.5029	.3706
841	209.3	.2697	.0303	883	217.7	.6227	.0770
842	219.7	.5615	.4385	884	217.7	.6126	.1353
843	239.2	..	.0249	885	217.7	.5891	.2892
844	238.8	..	.0629	886	214.8	.7420	.0138
845	238.5	..	.0932	887	214.8	.7443	.0301
846	237.9	..	.1605	888	214.8	.7409	.0591
847	236.6	..	.3363	889	214.8	.7059	.2679
848	235.6	..	.5025	890	209.3	.9674	.0192
849	234.7	..	.7127	891	209.3	.9673	.0211
850	234.3	..	.8401	892	209.3	.9634	.0305
851	234.7	.0908	.1164	893	1684	.238.9	..
852	234.7	.0493	.3344	894	1685	.234.7	..
853	234.7	.0309	.4557	895	1686	.234.7	..
854	234.7	.0147	.5585	896	1687	.231.7	..
855	234.7	.0011	.6968	897	1688	.231.7	..
856	231.7	.1634	.1482	898	1689	.229.7	..
857	231.7	.1227	.3945	899	1690	.229.7	..
858	231.7	.0917	.6179	900	1691	.229.7	..
859	231.7	.0710	.8409	901	1692	.229.7	..
860	231.7	.0714	.8533	902	1693	.227.7	..
861	229.7	.1940	.2720	903	1694	.227.6	..
862	229.7	.1720	.4257	904	1695	.224.7	..
863	229.7	.1496	.5926	905	1696	.221.7	..
864	229.7	.1426	.6973	906	1697	.224.7	..
865	227.7	.2822	.1229	907	1698	.224.7	..
866	227.7	.2675	.2022	908	1699	.219.7	..
867	227.7	.2454	.4023	909	1700	.212.8	..
868	227.7	.2156	.5622	910	1701	.212.8	..
869	227.7	.1971	.7460	911	1702	.211.8	..
870	224.7	.3918	.5303	912	1703	.210.8	..
871	224.7	.3831	.4104	913	1704	.210.8	..
872	224.7	.3207	.4632	914	1705	.209.3	..
873	224.7	.3015	.6175	915	1706	.209.3	..
874	221.7	.4767	.0835	916	1859	.238.9	..
875	221.7	.4650	.1525	917	1865	.2843	..

TABLE 1b
EXPERIMENTAL DATA AT 23 ATM.

RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION			VAPOR MOL FRACTION N2 AR 02	RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION			VAPOR MOL FRACTION N2 AR 02
		N2	AR	02				N2	AR	02	
724	240.2	.11125	.	.	.8675	1742	240.2	.8258	.	.	.0281
725	236.7	.02048	.	.	.7952	.3004	240.2	.6996	.757	.1054	.1640
726	229.7	.04082	.	.	.5918	.5301	240.2	.4699	.758	.1033	.0450
727	223.7	.5871	.	.	.4129	.	240.2	.	.1005	.0583	.8517
728	218.2	.8068	.	.	.1932	.6956	240.2	.3044	.759	.0925	.1555
729	215.3	.9233	.	.	.0767	.8656	240.2	.1344	.760	.0841	.0122
730	213.8	.9607	.	.	.0193	.9506	240.2	.0494	.761	.0653	.6957
731	236.7	.0767	.	.	.9233	.9877	240.2	.0123	.762	.0303	.2390
732	232.7	.2043	.	.	.7957	.1140	240.2	.9860	.763	.4482	.5215
733	226.7	.4147	.	.	.5853	.2814	240.2	.7186	.764	.0059	.6265
734	220.7	.6574	.	.	.3426	.5160	236.7	.4840	.765	.2063	.3666
735	216.7	.8409	.	.	.1591	.7367	236.7	.2633	.766	.1992	.0070
736	215.3	.9108	.	.	.0892	.8836	236.7	.1164	.767	.1959	.0077
737	214.5	.9488	.	.	.0512	.9349	236.7	.0651	.768	.1934	.0077
738	214.1	.9662	.	.	.0339	.9635	236.7	.0365	.769	.1875	.0077
739	213.9	.9728	.	.	.0272	.9765	236.7	.0235	.770	.1875	.0077
740	213.7	.9621	.	.	.0179	.9801	236.7	.0199	.771	.1875	.0077
741	213.5	.9942	.	.	.0059	.9871	236.7	.0129	.772	.1875	.0077
742	244.7	0.0134	0.0866	0.0050	236.7	0.0157	0.9843	0.0235	0.0235
743	244.6	0.0233	0.9767	0.0269	236.7	0.0269	0.9731	0.0199	0.0199
744	244.5	0.0331	0.9669	0.0378	236.7	0.0331	0.9622	0.0199	0.0199
745	244.4	0.0407	0.9593	0.0467	236.7	0.0407	0.9533	0.0199	0.0199
746	244.2	0.0611	0.9389	0.0611	236.7	0.0718	0.9282	0.0269	0.0269
747	243.9	0.0948	0.9052	0.0948	236.7	0.1084	0.8916	0.0331	0.0331
748	243.4	0.1528	0.8472	0.1528	236.7	0.1709	0.8291	0.0407	0.0407
749	242.3	0.2852	0.7148	0.2852	236.7	0.3092	0.6908	0.0467	0.0467
750	241.3	0.4386	0.5614	0.4386	236.7	0.4621	0.5379	0.0661	0.0661
751	240.2	0.6679	0.3321	0.6679	236.7	0.6809	0.3191	0.0884	0.0884
752	239.8	0.8177	0.1623	0.8177	236.7	0.8229	0.1771	0.1072	0.1072
753	240.2	0.1134	0.0078	0.1753	0.0078	0.1134	229.7	0.1753	0.0103	0.0144	0.0144
754	240.2	0.1141	0.0141	0.1732	0.0141	0.1141	229.7	0.1732	0.0120	0.0144	0.0144
755	240.2	0.1071	0.0223	0.8706	0.0223	0.1071	229.7	0.8706	0.0241	0.0241	0.0241

TABLE 14
EXPERIMENTAL DATA AT 23 ATM. (continued)

RUN NO.	LIQUID MOL FRACTION			VAPOR MOL FRACTION			TEMP. DEG. R.	RUN NO.	LIQUID MOL FRACTION			VAPOR MOL FRACTION		
	N2	AR	O2	N2	AR	O2			N2	AR	O2	N2	AR	O2
726	229.7	.3955	.0684	.5361	.5174	.0614	4212	820	218.2	.7919	.1018	.1063	.8512	.0767
729	229.7	.3655	.0973	.5142	.5053	.0870	4077	821	218.2	.7798	.1898	.0304	.8351	.1440
790	229.7	.3865	.1250	.4886	.5013	.1103	3885	822	216.7	.8622	.0273	.1105	.9054	.0201
791	229.7	.3742	.1770	.4488	.4842	.1563	3594	823	216.7	.8503	.1216	.0280	.8909	.0919
792	229.7	.3541	.3147	.3312	.4574	.2756	2670	824	216.7	.8550	.0743	.0708	.8954	.0559
793	229.7	.3277	.4964	.1759	.4258	.4325	1417	825	215.3	.9255	.0076	.0669	.9492	.0054
794	226.7	.5041	.0184	.4775	.6175	.0162	3663	826	215.3	.9242	.0226	.0532	.9466	.0168
795	226.7	.4953	.0501	.4547	.6096	.0437	3467	827	215.3	.9223	.0347	.0431	.9462	.0243
796	226.7	.4699	.0822	.4279	.6057	.0705	3239	828	215.3	.9184	.0467	.0349	.9429	.0336
797	226.7	.4794	.1392	.3813	.5899	.1164	2936	829	215.3	.9187	.0604	.0210	.9414	.0438
798	226.7	.4666	.2455	.2679	.5718	.2114	2169	830	215.3	.9158	.0767	.0075	.9390	.0562
799	226.7	.4479	.3526	.1995	.5494	.2978	1528	831	213.8	.9827	.0058	.0115	.9901	.0031
800	223.7	.6066	.0106	.3828	.7104	.0091	2805	832	213.8	.9830	.0103	.0067	.9884	.0075
801	223.7	.6035	.0246	.3719	.7102	.0204	2695	833	213.8	.9831	.0137	.0032	.9881	.0098
802	223.7	.6005	.0362	.3633	.7048	.0297	2655	918	213.5	.9946	.0023	.0023	.9963	.0016
803	223.7	.6003	.0519	.3476	.7035	.0423	2542	919	215.3	.9212	.0377	.0411	.9447	.0273
804	223.7	.5982	.0652	.3367	.7008	.0530	2462	920	216.7	.8591	.0757	.0653	.8977	.0572
805	223.7	.5940	.0932	.3129	.6935	.0762	2303	921	218.2	.8063	.0080	.1857	.8670	.0064
806	223.7	.5882	.1185	.2932	.6882	.0967	2151	922	220.7	.7170	.0235	.2595	.7940	.0185
807	223.7	.5731	.2137	.2131	.6699	.1739	1562	923	220.7	.6765	.2474	.0761	.7548	.1925
808	223.7	.5478	.3766	.0756	.6409	.3008	0583	924	223.7	.6025	.0258	.3717	.7094	.0209
809	223.7	.7121	.0193	.2687	.7978	.0140	1882	925	223.7	.6105	.0000	.3895	.7142	.0000
810	220.7	.7031	.0593	.2376	.7855	.0459	1686	926	226.7	.4305	.4799	.0896	.5317	.3999
811	220.7	.7006	.093A	.2056	.7815	.0737	1449	927	229.7	.3160	.6183	.0656	.4111	.5354
812	220.7	.6824	.1904	.1272	.7658	.1481	0861	928	229.7	.3092	.6908	.0422	.4022	.5978
813	220.7	.6693	.2913	.0394	.7472	.2253	0275	929	232.7	.2113	.7446	.0442	.2896	.6725
814	218.2	.8080	.0092	.1826	.8663	.0082	1255	930	236.7	.2018	.0268	.7714	.2951	.0268
815	218.2	.8068	.0209	.1723	.8616	.0158	1226	931	239.6	.0000	.9093	.0907	.9122	.0878
816	218.2	.8055	.0330	.1615	.8613	.0260	1127	932	240.2	.1138	.0080	.8782	.1757	.0083
817	218.2	.8033	.0448	.1518	.8613	.0340	1047	933	240.2	.1093	.0389	.8517	.1641	.0431
818	218.2	.8030	.0540	.1430	.8610	.0408	0982	934	240.2	.0297	.4579	.5124	.4712	.4832
819	218.2	.7971	.0743	.1266	.8552	.0571	0877	935	240.2	.0090	.3578	.6332	.6492	.3396

TABLE 15
EXPERIMENTAL DATA AT 26 ATM.

RUN No.	TEMP. DEG.R	LIQUID MOL FRACTION				VAPOR MOL FRACTION N2 AR 02	RUN No.	TEMP. DEG.R	LIQUID MOL FRACTION				VAPOR MOL FRACTION N2 AR 02
		N2	AR	02	N2				N2	AR	02	N2	
610	245.1	.1071	***	***	.8929	.1659	646	242.7	.0502	.8991	.0507	.0730	.8773 .0498
611	240.7	.2319	***	***	.7681	.3236	647	240.7	.2281	.0049	.7670	.3203	.0051 .6746
612	234.7	.4057	***	***	.5943	.5152	648	240.7	.2290	.0077	.7633	.3190	.0082 .6728
613	226.7	.5976	***	***	.4024	.6942	649	240.7	.2256	.0116	.7626	.3148	.0120 .6732
614	222.7	.8094	***	***	.1906	.6626	650	240.7	.2268	.0173	.7560	.3133	.0178 .6689
615	219.7	.9250	***	***	.0750	.9464	651	240.7	.2189	.0271	.7539	.3125	.0277 .6598
616	216.2	.9790	***	***	.0210	.9868	652	240.7	.2214	.0310	.7477	.3093	.0307 .6600
617	241.7	.1055	***	***	.1481	.8519	653	240.7	.2137	.0608	.7256	.2994	.0608 .6398
618	237.7	.2004	***	***	.2700	.7300	654	240.7	.1901	.1587	.6512	.2693	.1560 .5747
619	231.7	.4090	***	***	.5920	.4973	655	240.7	.1512	.3826	.4662	.2132	.3709 .4160
620	225.7	.6378	***	***	.3622	.7109	656	240.7	.1194	.6170	.2636	.1722	.5885 .2393
621	221.2	.8373	***	***	.1627	.8753	657	240.7	.1072	.7296	.1632	.1549	.6969 .1482
622	219.2	.9311	***	***	.0690	.9471	658	240.7	.0963	.8469	.0568	.1409	.8055 .0536
623	218.6	.9494	***	***	.0506	.9612	659	237.7	.3134	.0044	.6822	.4187	.0043 .5770
624	218.4	.9654	***	***	.0346	.9736	660	237.7	.3115	.0131	.6754	.4159	.0122 .5719
625	218.2	.9739	***	***	.0261	.9806	661	237.7	.3123	.0164	.6712	.4150	.0156 .5694
626	218.1	.9864	***	***	.0136	.9896	662	237.7	.3101	.0252	.6647	.4111	.0238 .5652
627	217.8	.9950	***	***	.0050	.9966	663	237.7	.3085	.0432	.6493	.4095	.0409 .5496
628	244.4	***	***	***	.9300	.0700	664	237.7	.3034	.0644	.6321	.4024	.0619 .5356
630	244.5	***	***	***	.8530	.1470	665	237.7	.2971	.0920	.6109	.3949	.0869 .5182
631	244.6	***	***	***	.8067	.1933	666	237.7	.2813	.2021	.5166	.3707	.1916 .4375
632	244.7	***	***	***	.7719	.2281	667	237.7	.2569	.3154	.4277	.3435	.2927 .3638
633	244.9	***	***	***	.7087	.2913	668	237.7	.2261	.5436	.2303	.3015	.4991 .1994
634	245.2	***	***	***	.6510	.3481	669	237.7	.2032	.7612	.0357	.2725	.6964 .0311
635	245.6	***	***	***	.5594	.4406	670	234.7	.3880	.0743	.5377	.4936	.0687 .4377
636	246.0	***	***	***	.4805	.5195	671	234.7	.3765	.1626	.4609	.4277	.1484 .3671
637	246.7	***	***	***	.3591	.6409	672	234.7	.3433	.3138	.3429	.4378	.2808 .2814
638	248.1	***	***	***	.1702	.8296	673	234.7	.3211	.5075	.1714	.4085	.4491 .1424
640	249.9	***	***	***	.0728	.9280	674	234.7	.3134	.5817	.1049	.3987	.5133 .0880
641	242.7	.1535	***	***	.0661	.7806	675	234.7	.3075	.6407	.0518	.3921	.5642 .0437
642	242.7	.1351	***	***	.2041	.6608	676	231.7	.4964	.0100	.4936	.6039	.0087 .3875
643	242.7	.9965	***	***	.4374	.4661	677	231.7	.4966	.0147	.4886	.6039	.0127 .3834
644	242.7	.8873	***	***	.5017	.4111	678	231.7	.4966	.0259	.4775	.6020	.0229 .3751
645	242.7	.6571	***	***	.1527	.0025	679	231.7	.0000	.0000	.0000	.5988	.0322 .3690

TABLE. 15
EXPERIMENTAL DATA AT 26 ATM. (continued)

RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION N2 AR. 02	VAPOR MOL FRACTION N2 AR. 02	RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION N2 AR. 02	VAPOR MOL FRACTION N2 AR. 02
681	231.7	.4934	.3424	697	219.2	.9397	.0216
691	231.7	.4874	.4642	715	219.2	.9393	.0204
692	231.7	.4813	.4443	716	219.2	.9393	.0226
693	231.7	.4650	.4253	717	219.2	.9367	.0406
694	231.7	.4271	.4067	718	219.2	.9334	.0513
695	231.7	.4119	.5352	719	219.2	.9332	.0552
696	228.7	.5945	.0265	720	218.2	.9799	.0085
697	228.7	.5884	.0465	721	218.2	.9780	.0167
698	228.7	.5875	.0624	722	231.7	.4934	.0329
699	228.7	.5749	.1455	723	247.2
700	228.7	.5580	.2422	893	249.6
701	225.7	.5335	.3975	894	249.4
702	225.7	.7014	.0103	895	249.2
703	225.7	.6996	.0209	896	248.8
704	225.7	.6981	.0283	897	245.2	.1094	.0190
705	225.7	.6963	.0393	898	245.2	.1008	.0611
706	225.7	.6936	.0465	899	245.2	.0849	.1341
707	225.7	.6929	.0615	900	245.2	.0744	.1846
708	225.7	.6894	.0909	901	245.2	.0516	.3086
709	225.7	.6700	.1924	902	242.7	.1369	.6369
710	222.7	.6547	.0397	903	242.7	.0251	.0247
711	222.7	.8652	.0123	904	240.7	.2312	.0098
712	221.2	.8642	.0235	905	240.7	.2277	.0237
713	220.2	.8561	.0491	906	240.7	.2208	.0575
714	219.2	.9416	.0077	907	237.7	.2155	.6597
715	221.2	.8563	.1418	908	234.7	.3766	.1479
716	221.2	.8019	.0563	909	231.7	.4913	.0488
717	222.7	.7967	.0655	910	225.7	.6978	.0463
718	220.2	.8650	.1360	911	225.7	.6649	.2567
719	221.2	.8561	.0491	912	221.2	.8649	.0318
720	221.2	.8563	.1360	913	221.2	.8634	.0401
721	221.2	.8564	.1360	914	219.2	.9330	.0464
722	220.2	.9014	.0211	915	218.2	.9794
723	221.2	.8517	.0931	916	218.2	.9751	.0184
724	220.2	.8982	.0365	917	217.8	.9949	.0051
725	220.2	.8902	.0915	918	217.8
726	219.2	.9416	.0077	919	217.8	.9960	.0040

TABLE 16
EXPERIMENTAL DATA AT MIXED PRESSURE LEVELS

<u>Run No.</u>	<u>Press. Atm.</u>	<u>Temp. Deg. R</u>	<u>Liquid Mol Fraction</u>			<u>Vapor Mol Fraction</u>		
			<u>N₂</u>	<u>Ar</u>	<u>O₂</u>	<u>N₂</u>	<u>Ar</u>	<u>O₂</u>
50	19.5	212.8	.7875	.0869	.1256	.8562	.0623	.0815
1914	1.03	163.0	.0039	-----	.9961	.0166	-----	.9834
1915	1.05	162.5	.0130	-----	.9870	.0491	-----	.9509
1916	0.97	162.0	.0035	-----	.9965	.0144	-----	.9856
1917	0.99	162.0	.0066	-----	.9934	.0248	-----	.9752
1918	0.98	161.3	.0179	-----	.9821	.0677	-----	.9323
1919	0.99	160.3	.0364	-----	.9636	.1313	-----	.8687
1920	0.97	160.0	.0385	-----	.9615	.1404	-----	.8596
1921	1.05	159.8	.0746	-----	.9254	.2397	-----	.7603
1922	1.01	159.0	.0833	-----	.9167	.2627	-----	.7373

VI. CORRELATION OF EXPERIMENTAL DATA

A. Thermodynamic Equations

The problem of correlation of vapor-liquid equilibrium data at high pressures is more complicated than at low pressures since the effect of pressure on the free energy of the liquid and also the effect of deviations from ideality in the vapor must be taken into account. A derivation of the equilibrium equations which take these effects into account follows.

The effect of pressure upon the free energy of a component in the liquid is given by the relation

$$dG_i = \bar{V}_i dp \quad (2)$$

and the effect of nonideality in the vapor is accounted for by means of the fugacity coefficient defined as

$$\phi_i = \frac{f_i}{p y_i} \quad (3)$$

The activity coefficient of component i in the liquid is now defined as

$$\ln \gamma_i = \ln \frac{f_i}{f_i^* x_i} = \left[\frac{\partial(G^E/RT)}{\partial n_i} \right]_{T,p,n_j} \quad (4)$$

The derivation of the equilibrium equations involves a seven-step process:

1. The component is taken as a vapor from a standard pressure at which the vapor behaves ideally to the vapor pressure p_i^o .

$$\frac{\Delta G^I}{RT} = \ln p_i^o + \ln \phi_i^o \quad (5)$$

2. The vapor is condensed at the pressure p_i^o to liquid.

$$\frac{\Delta G^{II}}{RT} = 0 \quad (6)$$

3. The liquid is taken from the pressure p_i^o to the pressure of mixing p_m .

$$\frac{\Delta G_{III}}{RT} = \int_{p_i^o}^{p_m} \frac{v_i^o}{RT} dp \quad (7)$$

4. The component is mixed at the pressure p_m .

$$\frac{\Delta G_{IV}}{RT} = \ln x_i \gamma_i \quad (8)$$

5. The mixture is taken from the pressure p_m to the total vapor pressure of the mixture.

$$\frac{\Delta G_V}{RT} = \int_{p_m}^p \frac{\bar{V}_i}{RT} dp \quad (9)$$

6. The component in the liquid mixture is in equilibrium with the vapor at the pressure p and composition y_i .

$$\frac{\Delta G_{VI}}{RT} = 0 \quad (10)$$

7. The vapor is taken from the pressure p and composition y to a standard pressure at which the vapor behaves ideally, and then is separated into the various components.

$$\frac{\Delta G_{VII}}{RT} = \ln p y_i - \ln \phi_i \quad (11)$$

Now since the free energy is a property of state and independent of the route by which the state is obtained, the sum of all these changes should add to zero since the initial and final states are the same. Thus the following relation for equilibrium is obtained.

$$\sum \frac{\Delta G}{RT} = \ln p_i^o \phi_i^o + \int_{p_i^o}^{p_m} \frac{v_i^o}{RT} dp + \ln x_i \gamma_i + \int_{p_m}^p \frac{\bar{V}_i}{RT} dp - \ln p y_i \phi_i = 0 \quad (12)$$

If this equation is solved for p_{y_i} , the following is obtained:

$$\ln p_{y_i} = \ln \frac{p_i^o \phi_i^o x_i \gamma_i}{\phi_i} + \int_{p_i^o}^{p_m} \frac{v_i^o}{RT} dp + \int_{p_m}^p \frac{\bar{V}_i}{RT} dp \quad (13)$$

For the correlation of the nitrogen-argon-oxygen vapor liquid data there were insufficient partial molar volume data to use this equation as it stands, and it was necessary to simplify it. Thus it was assumed that the partial molar volume of a component in solution is equivalent to the liquid molar volume of that component and that the liquid volume is independent of pressure. With these assumptions, the equilibrium relation simplifies to the following equation which is the one used in correlating the nitrogen-argon-oxygen data.

$$p_{y_i} = \left[\frac{p_i^o x_i \gamma_i \phi_i^o}{\phi_i} \right] e^{\frac{v_i^o (p - p_i^o)}{RT}} \quad (14)$$

These assumptions regarding the molar volume are partly justified by the fact that the correction is usually small amounting to less than 20% in most cases and any errors which are made in this correction can be partially compensated for with other parameters. However, in the neighborhood of the critical point this correction is undoubtedly larger and deviates significantly from the simplifying assumptions made here. Therefore it is improbable that this simplified equation will be applicable in the neighborhood of the critical point.

In the calculation of equilibria it is helpful to bear in mind that according to the phase rule, $F = c - P + 2$; c variables must be specified (since $P = 2$) before the equilibrium point can be calculated. Thus one might specify the liquid composition and the temperature (the liquid composition involves $c - 1$ variables since $\sum_i x_i = 1$) or perhaps the mole fraction of one component in the liquid, the temperature and the pressure. If it is necessary to calculate not only the equilibrium point but also the number of moles in each phase, one more variable must be specified since the phase rule includes only intensive variables. Thus for example, one might specify an overall composition of the two-phase system, the pressure and the temperature.

The ease of numerical calculation varies depending upon which variables are specified; however even in the simplest cases iterative type calculations are necessary. This iteration is necessary since the functions ϕ_i , γ_i and $e^{Vi(p-p_i)/RT}$ are not specified in terms of any one set of variables. For this reason the task of manual calculation would be prohibitive and calculations were done on a GE-225 computer.

B. Liquid Molar Volume

The liquid molar volume of the three components were determined by a least squares fit of existing data to the equation

$$V = a + b x + c x^2 + d x^3 + e x^4 + f x^5 \quad (15)$$

Table 17 lists the constants obtained and the literature source for the data. Above the critical temperature of nitrogen the molar volume of nitrogen represents an extrapolation of the data from below the critical temperature. Data close to the critical point were not fitted.

TABLE 17
LIQUID MOLAR VOLUME CORRELATION CONSTANTS

Component	a	b	c	d	e	f	Lit. Ref.
Nitrogen	- 0.7	147.1	-264.1	227.08	- 92.29	14.649	(4)
Argon	-98.7	451.5	-610.2	393.62	-122.11	14.803	(4)
Oxygen	-34.0	178.6	-221.5	139.05	.. 43.09	5.341	(5)

C. Vapor Pressure of Pure Components

Vapor pressure data for oxygen were taken from the literature. These data were used for the calibration of the three junction thermocouple of the equilibrium cell. Vapor pressure data for nitrogen and argon were measured in the cell based upon the temperature scale obtained from the oxygen data. Initially, it was attempted to calibrate the thermocouple from literature data on all three components, but calculated temperatures disagreed by as much as 0.2°R ; therefore, only the data for oxygen were used in the calibration. If the oxygen temperature scale is in error by 0.2°R , then our temperature scale is in error by 0.2°R , but the ratio of vapor pressures will be more nearly correct than as calculated from the literature data.

Our value for the boiling point of oxygen is 162.36°R compared to the accepted value of 162.34°R ⁽⁶⁾.

The vapor pressure data were fitted to the Riedel equation⁽⁷⁾.

$$\ln p_i^{\circ} = A - \frac{B}{T} + C \ln T + DT^6 \quad (16)$$

The constants obtained by a least squares fit to the data are summarized in Table 18 and deviation plots of the data are given in Figures 13, 14, and 15. The agreement with the data is generally within $\pm 0.3\%$ although there are some deviations as high as 1% from the correlated curves.

The vapor pressure of nitrogen calculated above the nitrogen critical temperature represents an extrapolation of the data from below the critical temperature.

TABLE 18

CONSTANTS FOR PURE COMPONENT VAPOR PRESSURES

Component	A	B	C	D	Data Source
Nitrogen	25.2115	1598.96	-2.24519	1.5445×10^{-15}	This Work
Argon	18.7043	1621.12	-1.12969	0.4132×10^{-15}	This Work
Oxygen	21.6017	1781.43	-1.56188	0.4032×10^{-15}	8,9,10,11,12

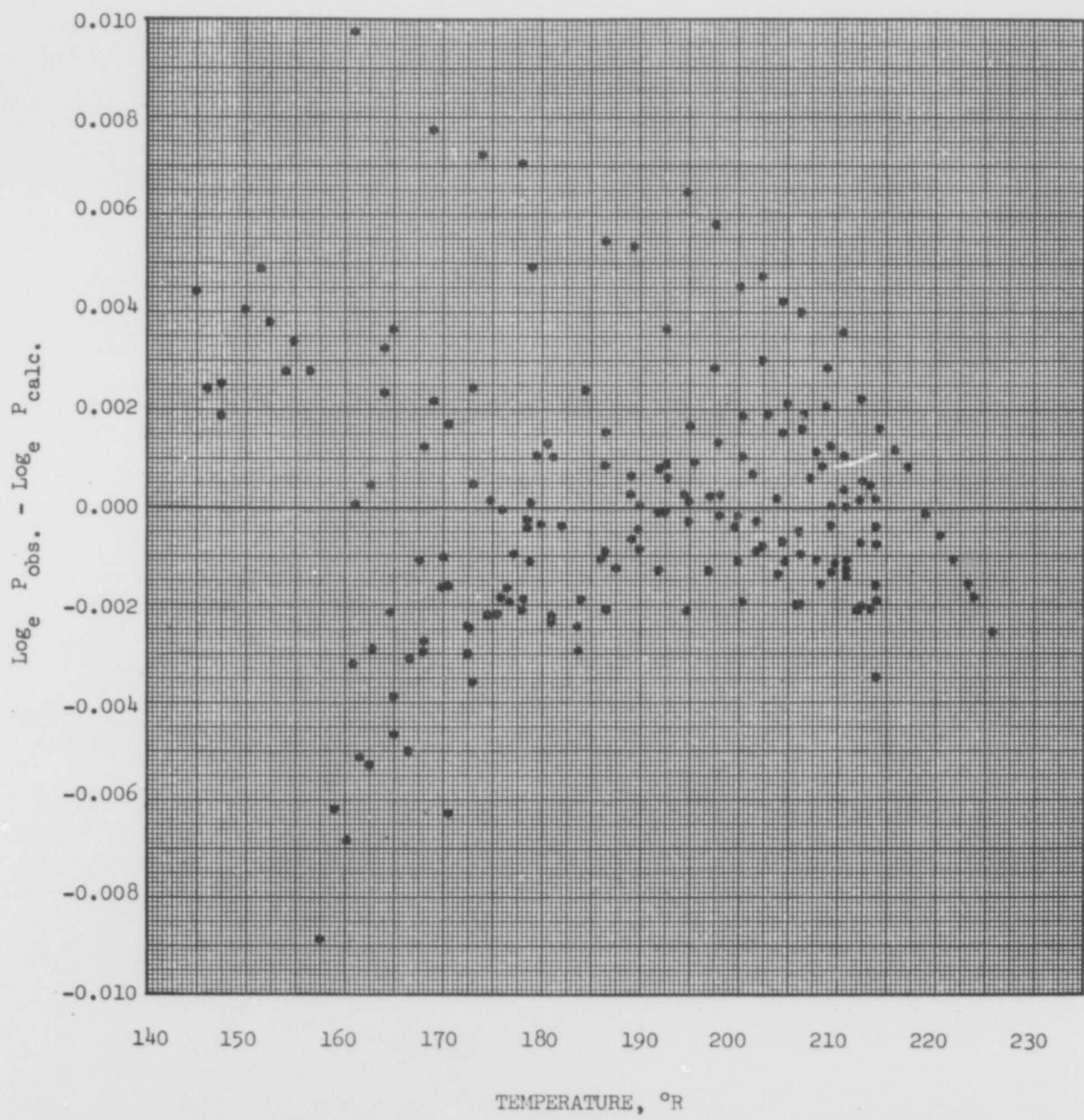


Figure 13. Deviation of APCI Nitrogen Vapor Pressure Data from Riedel Equation.

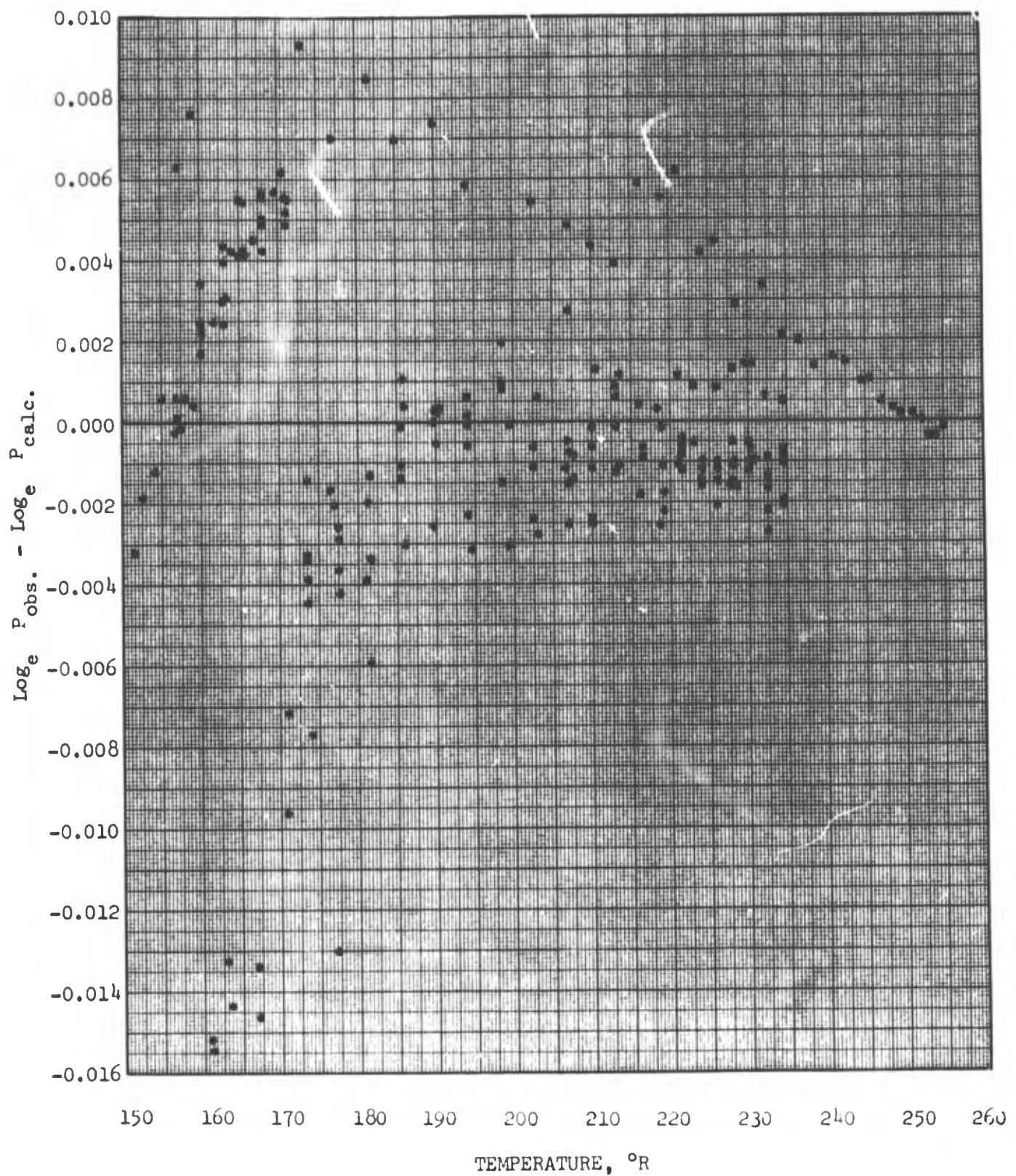


Figure 14. Deviation of APCI Argon Vapor Pressure Data from Riedel Equation.

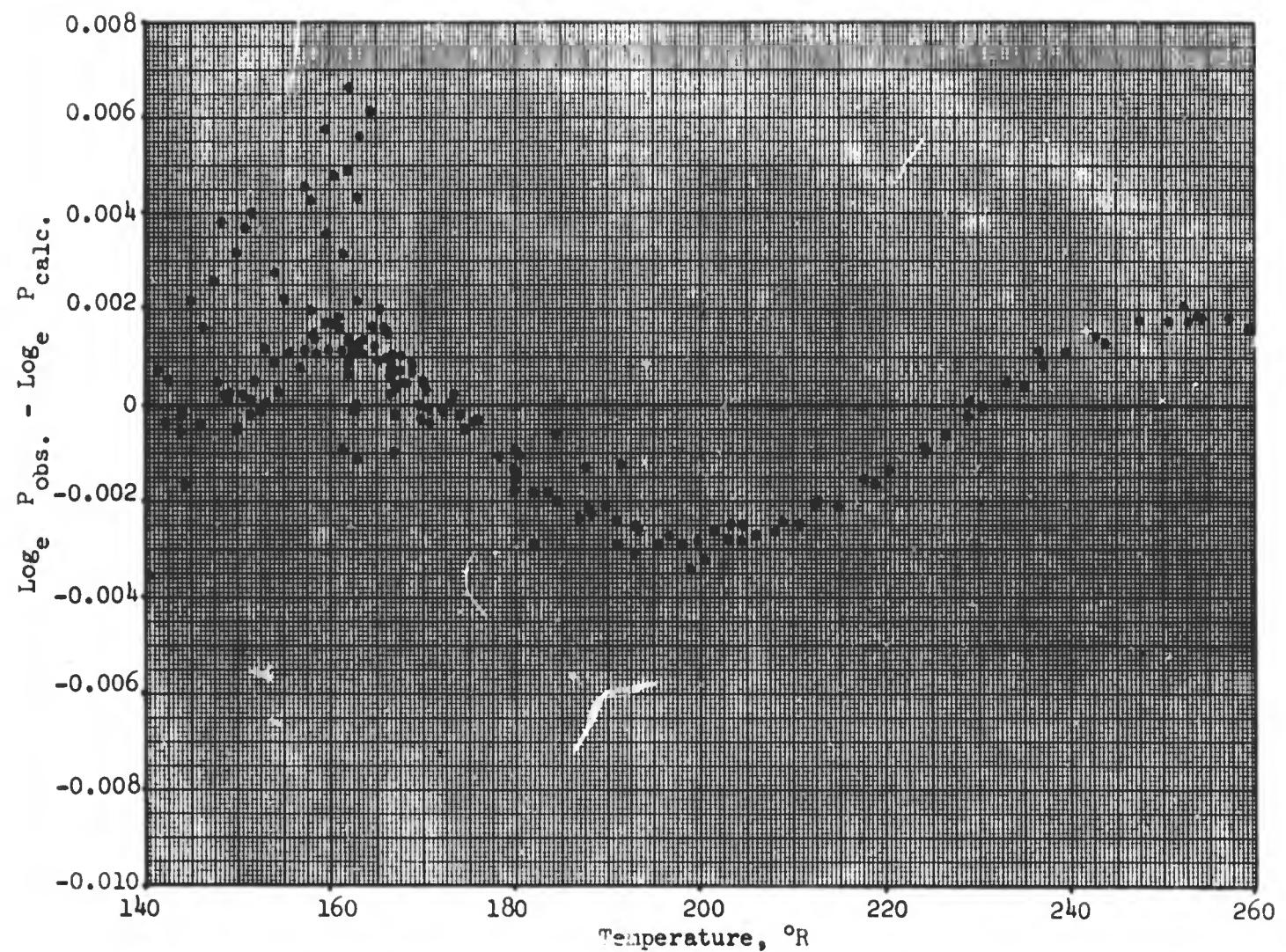


Figure 15. Deviation of Literature Oxygen Vapor Pressure Data from Riedel Equation.

A comparison of vapor pressure data from the literature for nitrogen^(5,8,13,14,15) and argon^(5,16,17) is given in Figures 16 and 17. The data for nitrogen deviate systematically about 0.7% from the calculated curve; the vapor pressures from the literature being too high. The data for argon are in good agreement with the correlation at high temperatures but at low temperatures the disagreement is of the order of 1%. These differences were part of the source of difficulty in correlating the data when the equilibrium cell thermocouple was calibrated from these data. This inconsistency then led to the calibration of the thermocouple from the vapor pressure of oxygen alone.

D. Fugacity Coefficient

The fugacity coefficient in the vapor phase is calculated from the virial equation of state terminating with the third virial coefficient

$$\frac{PV}{RT} = Z = 1 + \frac{B}{V} + \frac{C}{V^2} \quad (17)$$

The equation for the fugacity coefficient is as follows:

$$\ln \phi_i = \frac{2}{V} \sum_{j=1}^n y_j B_{ij} + \frac{3}{2V^2} \sum_{j=1}^n \sum_{k=1}^n y_j y_k C_{ijk} - \ln Z \quad (18)$$

The cross coefficients B_{ij} and C_{ijk} are calculated by methods similar to those presented by Pitzer⁽¹⁸⁾ and by Prausnitz⁽¹⁹⁾. The values of the second and third coefficients are given in Tables 19 and 20.

The calculated coefficients for the pure components are in good agreement with literature data^(20,30) as is indicated in Figures 18, 19, and 20. The third virial coefficient deviates more than does the second; however, an error of 0.1 ($\text{ft}^3/\text{lb-mole}$)² in the third virial coefficient produces a maximum error of only about 0.2% in the calculated fugacity coefficient.

The virial equation terminated at the third virial coefficient deviates negligibly from experimental P-V-T data at densities up to one half the critical density as shown in Figures 21, 22, and 23. At the experimental pressures of measurement the density of the vapor was always less than one half the critical density.

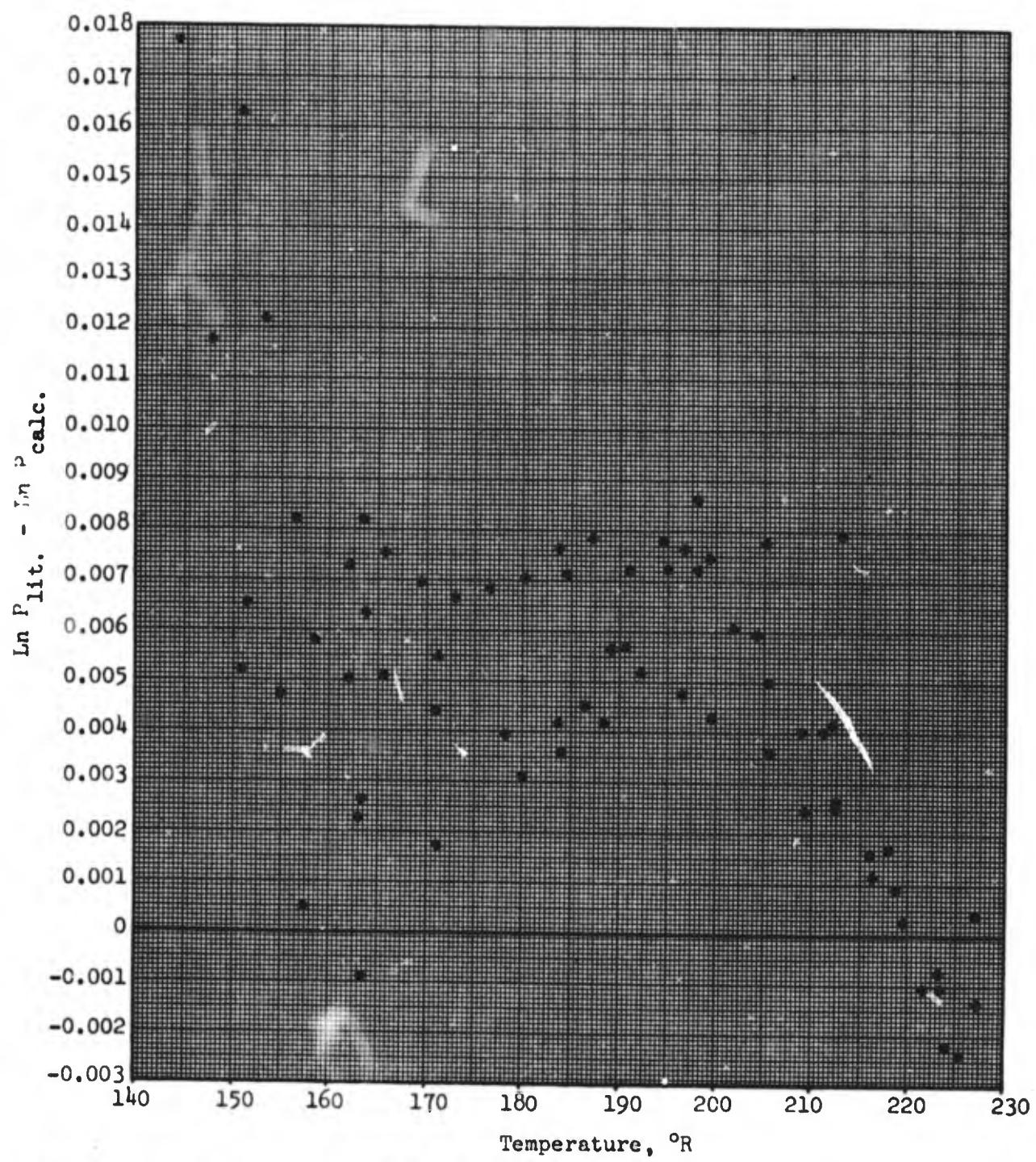


Figure 16. Deviation of Literature Vapor Pressure from APCI Correlation for Nitrogen.

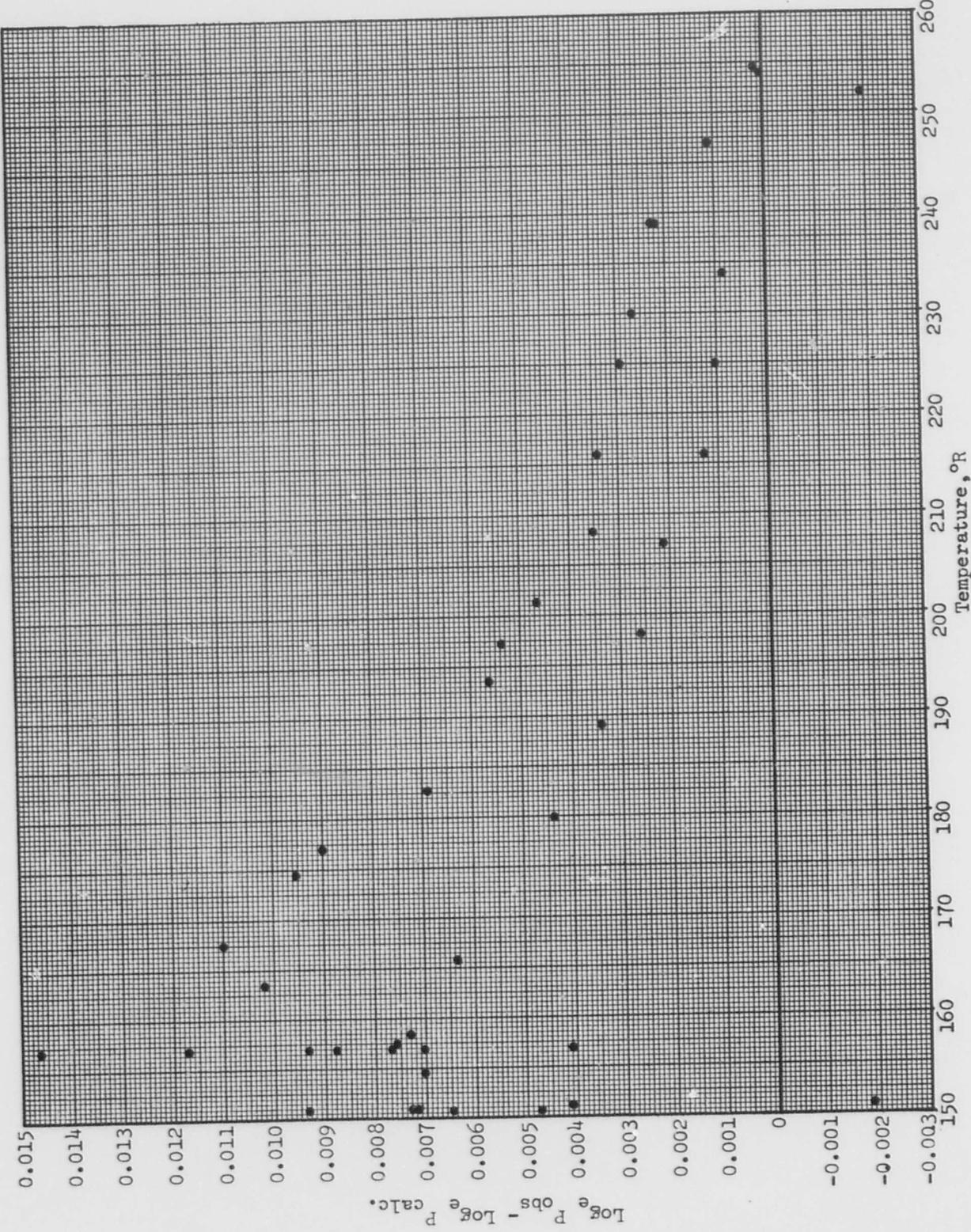


Figure 17. Deviation of Literature Vapor Pressure from APCI correlation for Argon.

TABLE 19

SECOND VIRIAL COEFFICIENTS USED IN CALCULATIONS
 Cubic Feet/Pound Mole

Nitrogen = 1, Argon = 2, Oxygen = 3

<u>T, °R</u>	<u>-B₁₁</u>	<u>-B₁₂</u>	<u>-B₁₃</u>	<u>-B₂₂</u>	<u>-B₂₃</u>	<u>-B₃₃</u>
130	4.886	5.063	5.340	5.150	5.484	6.054
140	4.226	4.398	4.595	4.527	4.748	5.154
150	3.703	3.868	4.015	4.014	4.168	4.475
160	3.277	3.435	3.549	3.587	3.699	3.941
170	2.922	3.074	3.165	3.226	3.311	3.508
180	2.623	2.769	2.843	2.918	2.983	3.149
190	2.366	2.507	2.568	2.653	2.704	2.845
200	2.144	2.281	2.331	2.423	2.463	2.585
210	1.951	2.083	2.125	2.221	2.253	2.360
220	1.780	1.909	1.945	2.043	2.069	2.163
230	1.629	1.754	1.784	1.885	1.906	1.990
240	1.494	1.616	1.642	1.744	1.760	1.835
250	1.373	1.493	1.514	1.617	1.630	1.697
260	1.264	1.381	1.400	1.503	1.512	1.574

TABLE 20
 THIRD VIRIAL COEFFICIENTS USED IN CALCULATIONS (Cubic Feet/Pound Mole)²
 Nitrogen = 1, Argon = 2, Oxygen = 3

<u>T, °R</u>	<u>C₁₁₁</u>	<u>C₁₁₂</u>	<u>C₁₁₃</u>	<u>C₁₂₂</u>	<u>C₁₂₃</u>	<u>C₁₃₃</u>	<u>C₂₂₂</u>	<u>C₂₂₃</u>	<u>C₂₃₃</u>	<u>C₃₃₃</u>
130	-1.024	-2.175	-2.371	-3.662	-3.927	-4.205	-5.581	-5.933	-6.303	-6.692
140	0.035	-0.685	-0.799	-1.614	-1.770	-1.935	-2.809	-3.020	-3.241	-3.474
150	0.578	0.110	0.043	-0.492	-0.566	-0.685	-1.264	-1.393	-1.529	-1.672
160	0.850	0.533	0.495	0.130	0.073	0.013	-0.386	-0.466	-0.551	-0.640
170	0.974	0.753	0.731	0.473	0.439	0.403	0.117	0.067	0.015	-0.041
180	1.018	0.858	0.847	0.657	0.638	0.617	0.405	0.374	0.342	0.307
190	1.019	0.898	0.894	0.750	0.740	0.728	0.566	0.547	0.527	0.506
200	0.995	0.902	0.902	0.789	0.785	0.779	0.651	0.640	0.629	0.616
210	0.960	0.885	0.888	0.797	0.796	0.795	0.690	0.684	0.679	0.672
220	0.919	0.857	0.862	0.786	0.788	0.789	0.701	0.699	0.697	0.695
230	0.877	0.824	0.830	0.765	0.768	0.771	0.695	0.696	0.697	0.697
240	0.835	0.789	0.795	0.738	0.743	0.747	0.680	0.683	0.685	0.687
250	0.795	0.754	0.760	0.709	0.714	0.719	0.660	0.663	0.667	0.670
260	0.757	0.719	0.726	0.679	0.685	0.691	0.636	0.641	0.645	0.649

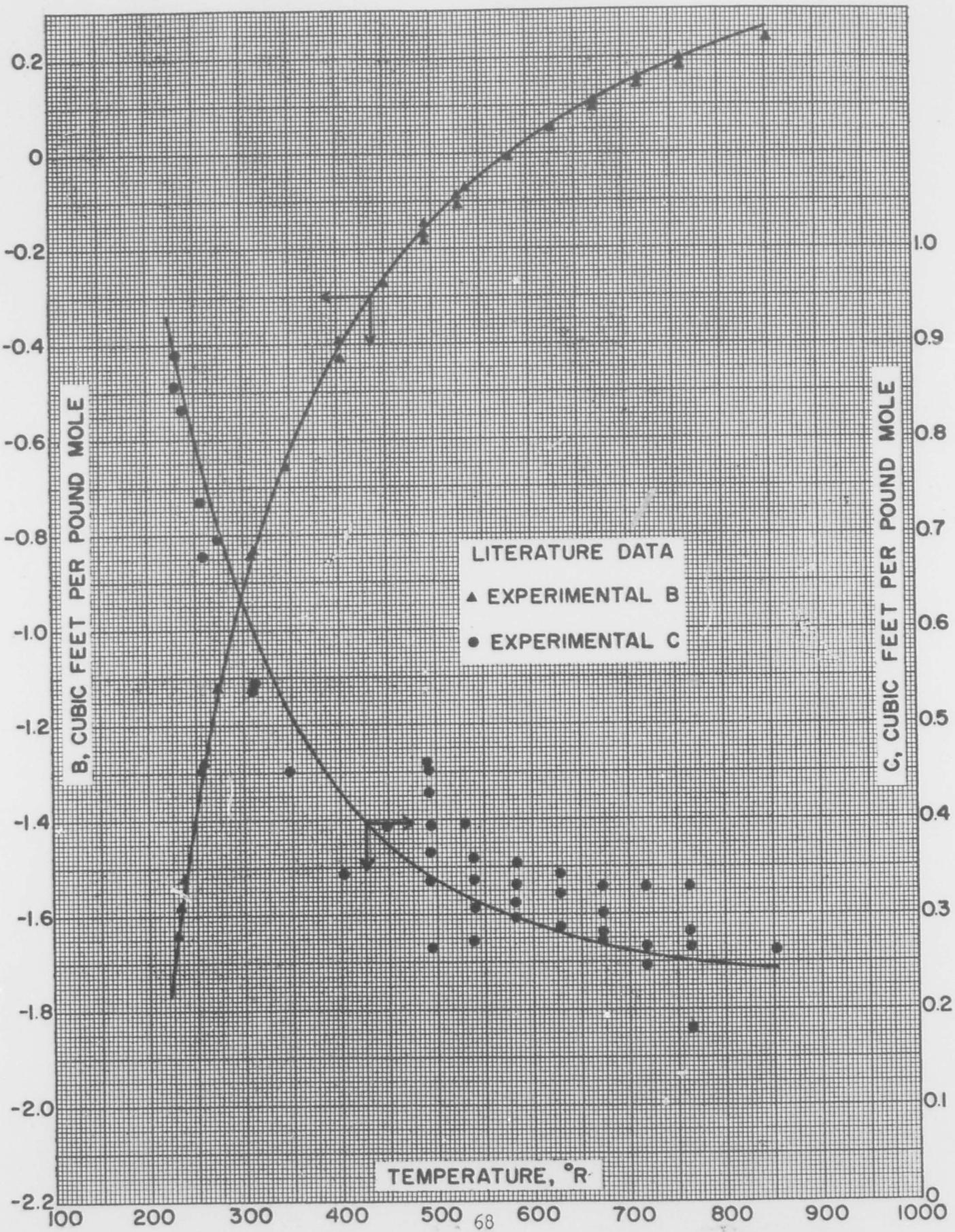


Figure 18. Calculated Second and Third Virial Coefficients, B and C, for Nitrogen.

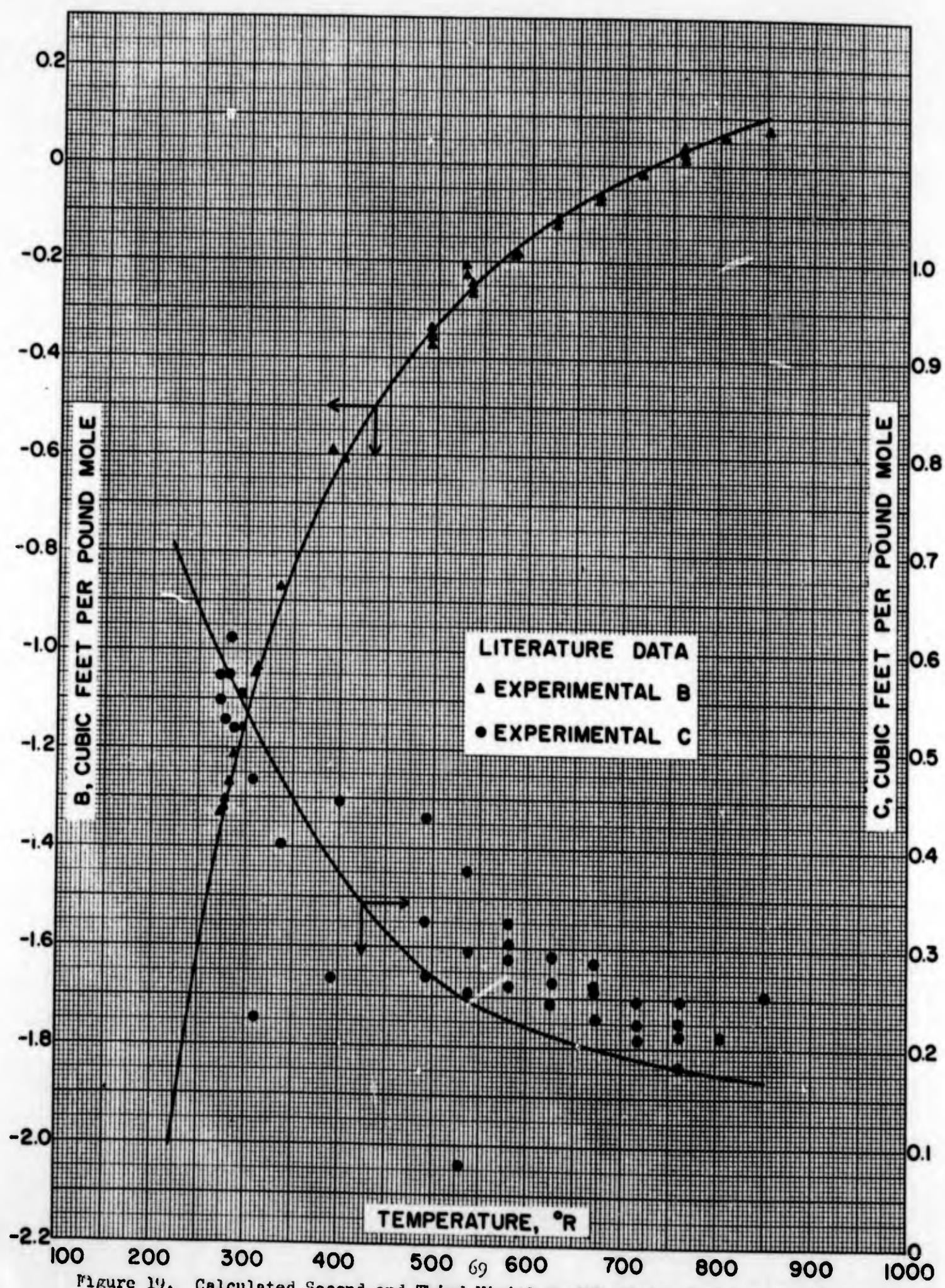


Figure 19. Calculated Second and Third Virial Coefficients, B and C, for Argon.

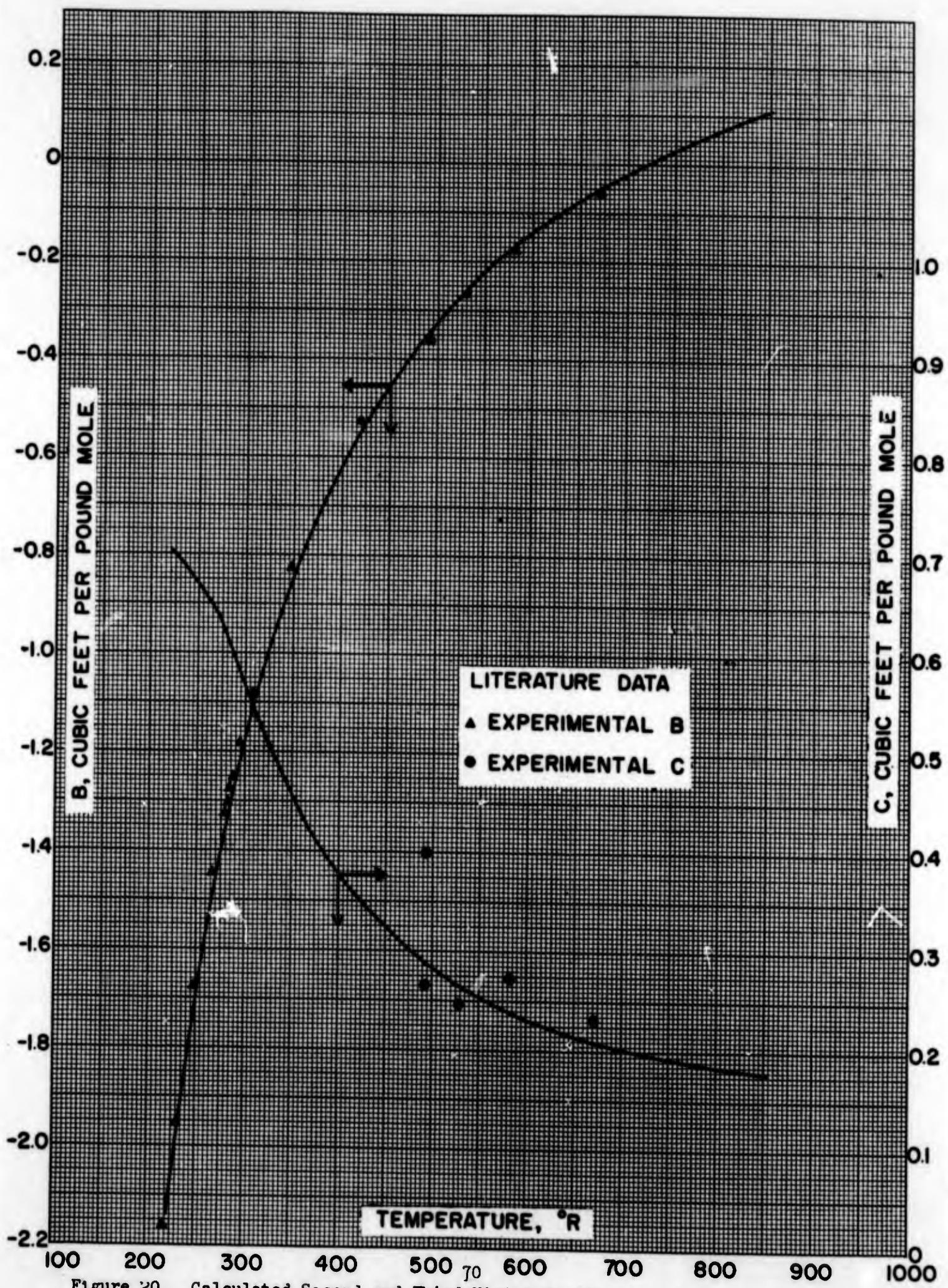


Figure 20. Calculated Second and Third Virial Coefficient, B and C , for Oxygen.

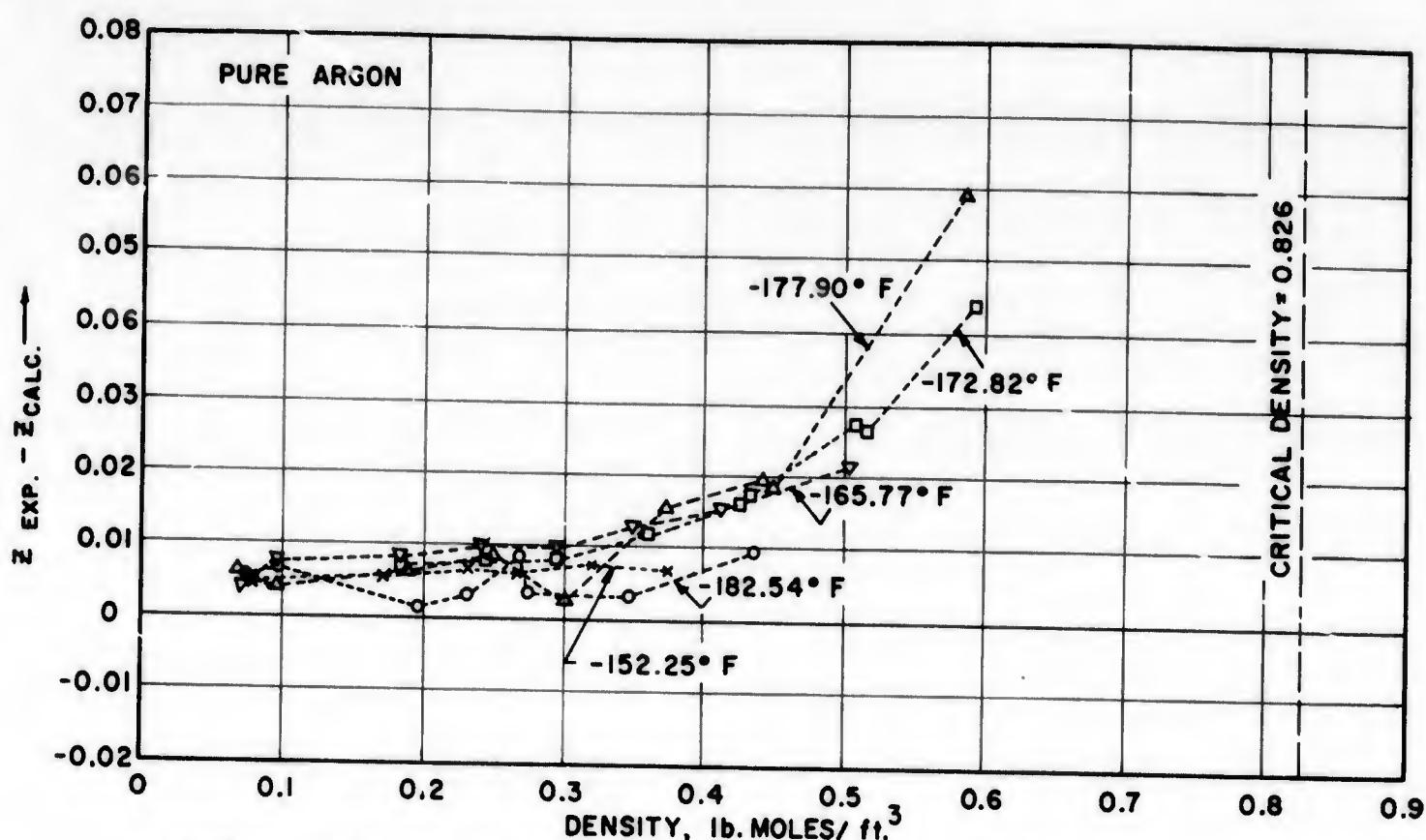


Figure 21. Comparison of Calculated and Experimental Compressibility Data, Argon.

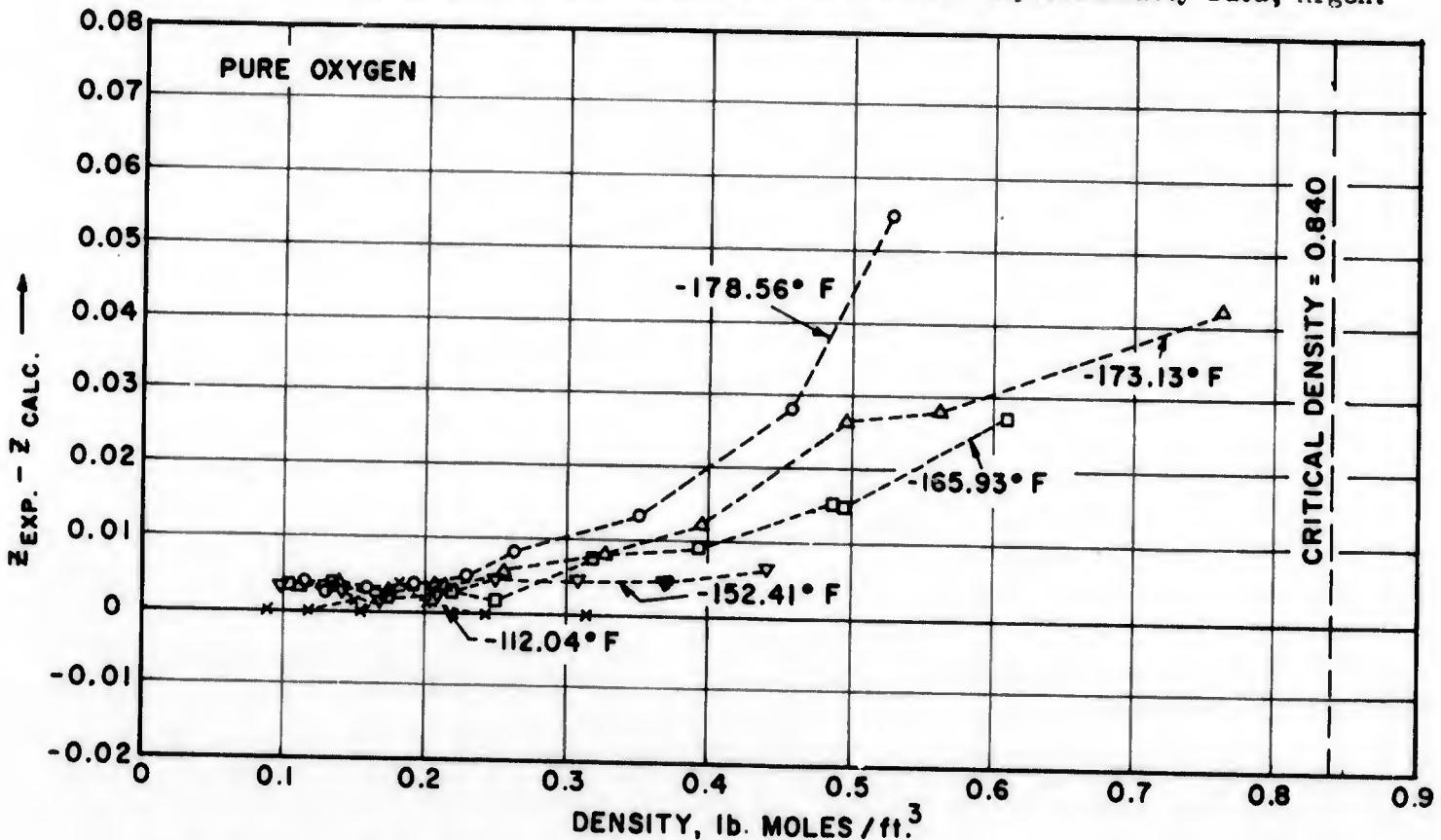


Figure 22. Comparison of Calculated and Experimental Compressibility Data, Oxygen.

Knobler and co-workers⁽³¹⁾ have measured the cross coefficients of argon-oxygen, oxygen-nitrogen, and nitrogen-argon at 90°K. These data are shown in Figure 2⁴ plotted along with the calculated curves. No other cross coefficient data were found.

Keunnen, Virscholle and Van Urk⁽³²⁾ have measured the compressibility of two oxygen-nitrogen mixtures and Penning⁽³³⁾ has made measurements on air. Deviations in compressibility are shown plotted in Figures 25 and 26 where the difference is small as in the case of the pure components.

In view of these comparisons it is felt that the virial equation and the virial coefficients are within the experimental range of accuracy of existing P-V-T data and holds for mixtures as well as for pure components. The deviation in compressibility factor is of the order of 0.005 which probably corresponds to the uncertainty in the fugacity coefficient.

E. Activity Coefficient Equation

The liquid activity coefficient data calculated from the experimental data were correlated by means of the Van Laar equation. In a binary mixture it may be written as

$$\ln \gamma_1 = S_1 \left[\frac{S_2 x_2}{S_1 x_1 + S_2 x_2} \right]^2 A_{12} \quad (19)$$

or in a multicomponent mixture as

$$\ln \gamma_i = S_i \left[\sum_{j=1}^n \varrho_j A_{ij} - \frac{1}{2} \sum_{j=1}^n \sum_{k=1}^n \varrho_j \varrho_k A_{jk} \right] \quad (20)$$

$$\text{where } \varrho_j = \frac{\sum_{k=1}^n S_k x_k}{n}$$

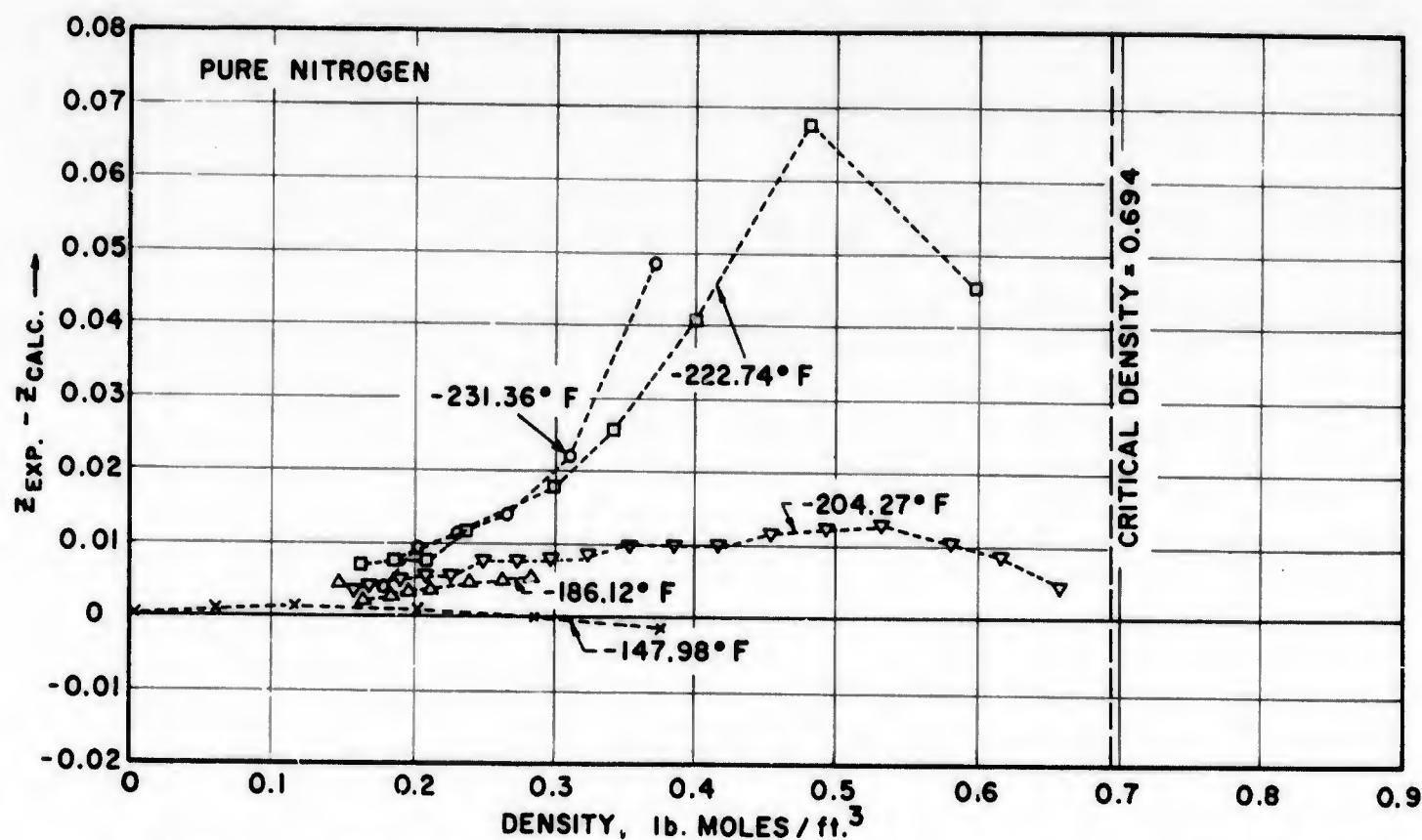


Figure 23. Comparison of Calculated and Experimental Compressibility Data, Nitrogen.

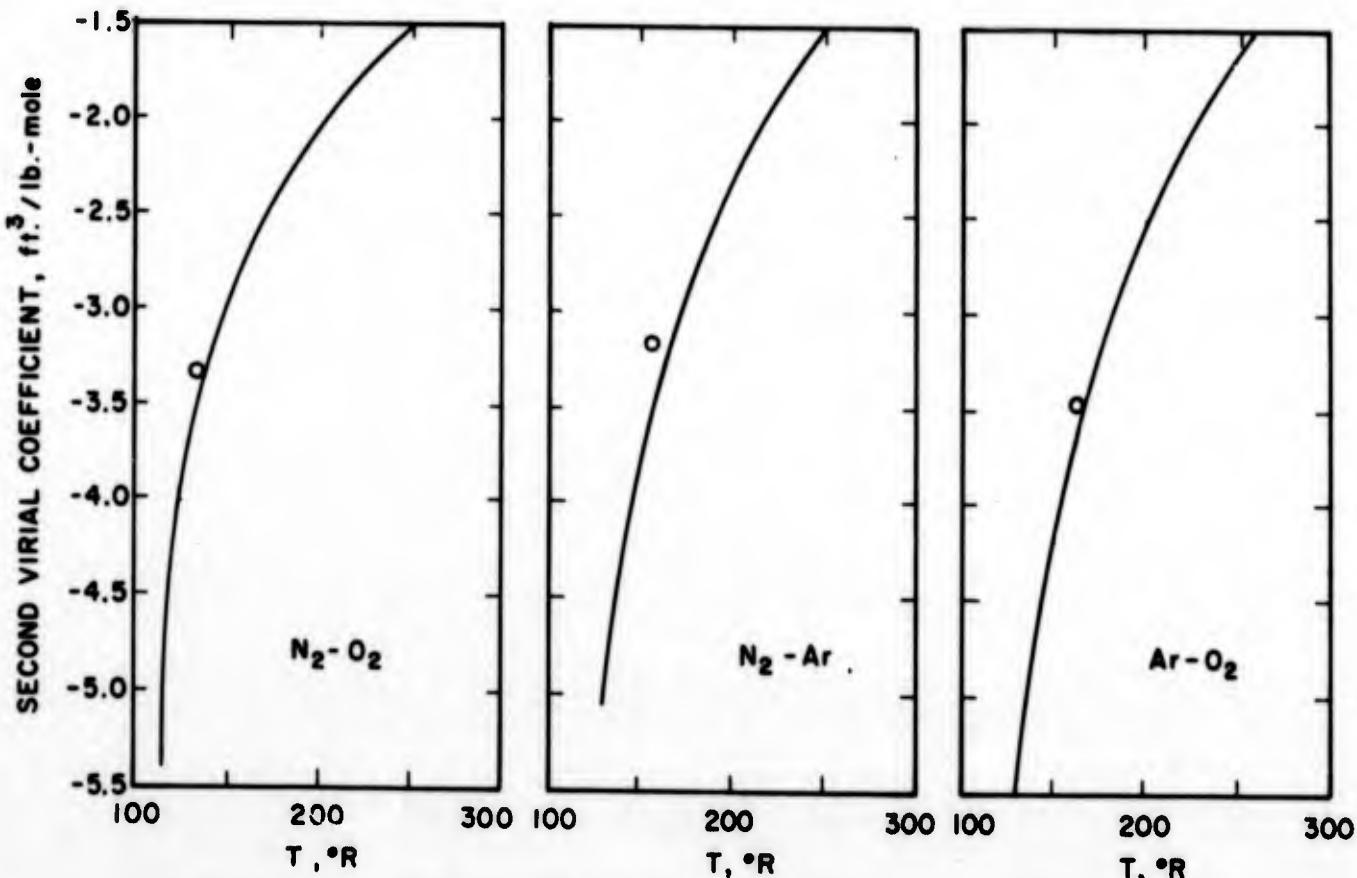


Figure 24. Comparison of Calculated and Experimental Cross Coefficients.

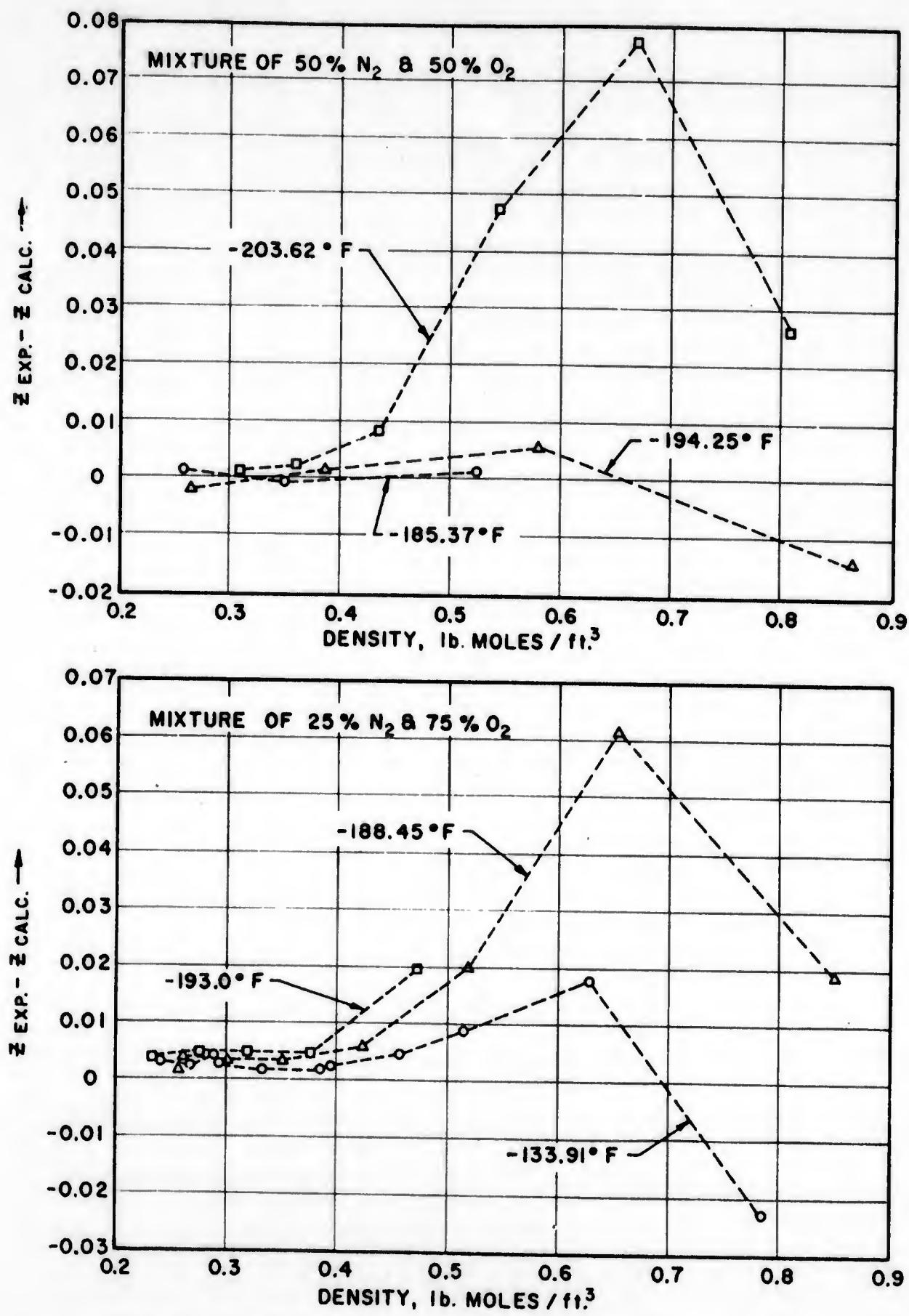


Figure 25. Comparison of Calculated and Experimental Compressibility Data, Nitrogen-Oxygen Mixture.

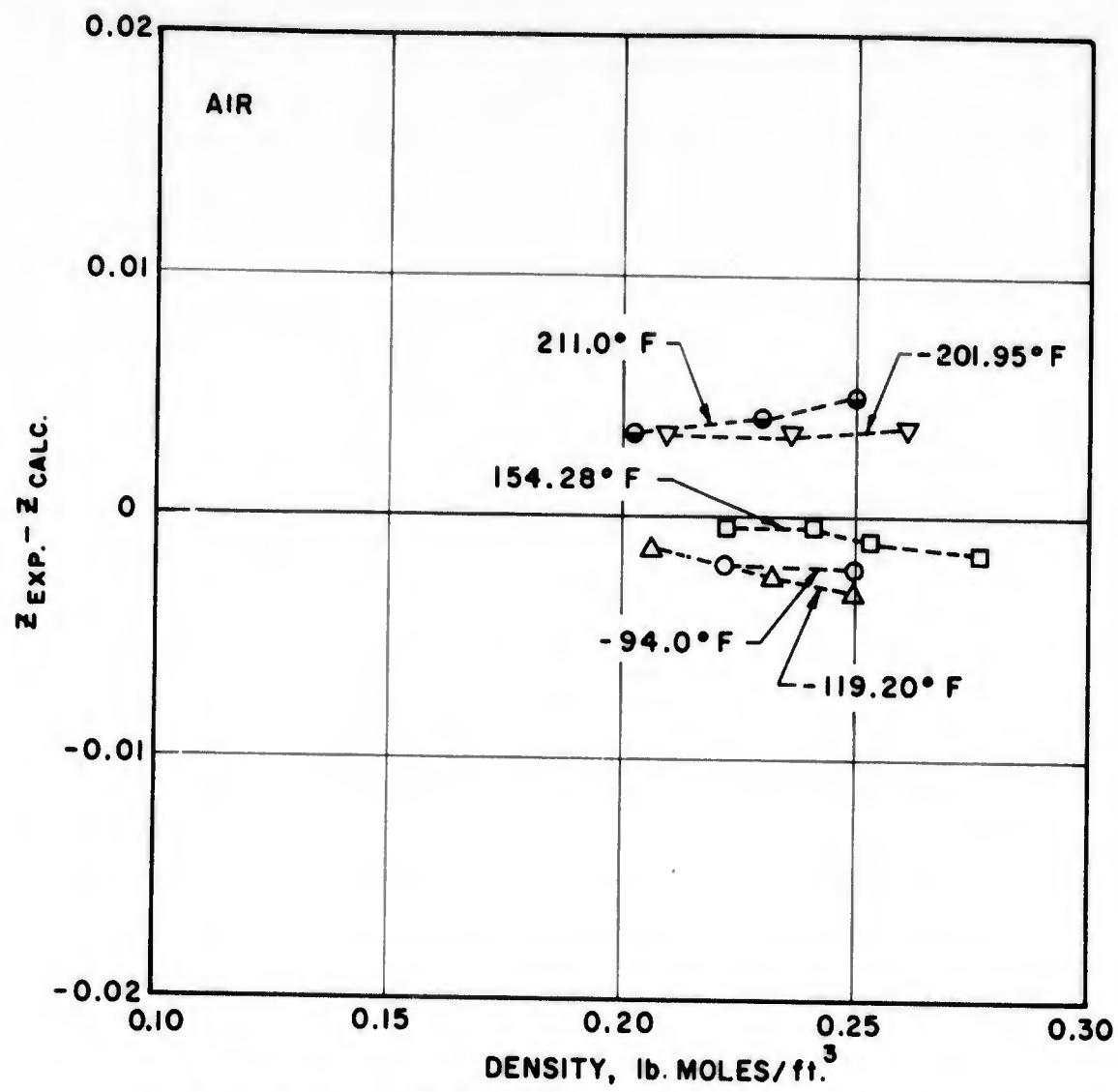


Figure 26. Comparison of Calculated and Experimental Compressibility Data, Air.

The interaction coefficients A_{ij} were assumed to be temperature dependent according to the relation

$$A_{ij} = a_{ij} + b_{ij}/T$$

(21)

The constants in the Van Laar equation were determined by a least squares fit to the entire set of vapor-liquid equilibrium data. The constants obtained are given in Table 21. A discussion of the correlation and comparisons with data are given in the following section.

TABLE 21
VAN LAAR CONSTANTS FOR NITROGEN-ARGON-OXYGEN
ACTIVITY COEFFICIENTS IN THE LIQUID PHASE

Component	Van Laar Volume	a_{ij}			b_{ij}		
		N_2	Ar	O_2	N_2	Ar	O_2
Nitrogen	1.00	0	-.1515	-.0669	0	51.8	43.9
Argon	1.00	-.1515	0	-.0837	51.8	0	40.7
Oxygen	1.00	-.0669	-.0837	0	43.9	40.7	0

VII. COMPARISON OF CORRELATION TO DATA

The experimental vapor-liquid equilibrium data were fitted by the method of least squares to the constants in the logarithm of the activity coefficient of each component. By this method a single vapor-liquid equilibrium point provided two activity coefficient points in a binary mixture and three points in a ternary mixture. With 1962 equilibrium points this produced 5344 activity coefficient points, requiring considerable running time on the computer each time a least squares analysis was made. Each experimental point was weighted equally because equal weight seems as logical for this set of data as other methods of weighting. If the Gibbs free energy of mixing had been fitted, it would have been more logical to weight the data differently because data at low concentrations of a component would not receive sufficient weight.

A summary of the various least square analysis runs made on the computer is given in Table 22, where the curve-fit number is in the chronological order of the analysis made. Runs 1, 2, 3, and 4 show that it makes little difference in the RMS error whether the three binaries are assumed to be symmetrical or unsymmetrical in the activity coefficient. Runs 5 and 6 are equivalent to Runs 4 and 1 respectively, except that points deviating more than three times the RMS error were deleted. The percentage of points deleted was five times the theoretical number of 0.3% based on a random error distribution, and the RMS error was reduced approximately 50%--38 times the theoretical value of 1.3%--justifying the deletion of the points. Runs 5 and 6 show that it makes little difference in the RMS error whether the constants a_{ij} are set to zero or not; the error only increasing from .0235 to .0261. Because of this insensitivity, the constants b_{ij} have been fixed consistent with heat of mixing data from the literature and the coefficients a_{ij} have been adjusted to fit the activity coefficient data. Runs 7 and 8 correspond to this restriction, however, it was found that there was a systematic bias in the correlation due to errors in the vapor pressures of the pure components.

This bias is shown in Table 23 where there were 1517 nitrogen points in Run 8 with positive deviation compared with only 229 points with negative deviation. An examination of the data showed that the correlation could be improved if the vapor pressures of the pure components were adjusted slightly. An adjustment of the data was made by the use of vapor pressure data measured under the present project in place of data reported in the literature as described in Section III-G. The results of the adjustment are shown as the difference between Runs 8 and 10 in Tables 22 and 23. The RMS error dropped slightly and the number of positive and negative deviations became more nearly the same.

TABLE 22

CONSTANTS AND ROOT MEAN SQUARE ERROR OF VARIOUS CURVE-FITS

Constant	Curve-Fit Number								
	1	2	3	4	5	6	7	8	9
s_{N_2}	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0
s_{Ar}	1.0	.9743*	.9743	1.0	1.0	1.0	1.0	1.0	1.0
s_{O_2}	1.0	.9469*	.9469	1.0	1.0	1.0	1.0	1.0	1.0
a_{N_2-Ar}	0.0	0.0	.0696*	.0698*	.1237*	0.0	-.1415*	-.1397*	-.1555*
b_{N_2-Ar}	24.54*	24.54	11.61*	11.16*	1.01*	24.60*	51.8	51.8	51.8
$a_{N_2-O_2}$	0.0	0.0	.1849*	.1818*	.2191*	0.0	-.0432*	-.0439*	-.0653*
$b_{N_2-O_2}$	34.81*	34.81	-.60*	0.0*	-7.74*	34.51*	43.9	43.9	43.9
a_{Ar-O_2}	0.0	0.0	-.1096*	-.1046*	-.0984*	0.0	-.0864*	-.0893*	-.0808*
b_{Ar-O_2}	23.31*	23.31	46.45*	44.47*	42.64*	22.78*	40.7	40.7	40.7
RMS Error	.0456	.0455	.0444	.0445	.0235	.0261	.0466	.0284	.0431
Points Deleted	0	0	0	0	87	86	0	81	0
									92

#Coefficient Varied in That Run

TABLE 23

 SUMMARY OF POSITIVE AND NEGATIVE
 DEVIATIONS OF EXPERIMENTAL POINTS FROM CORRELATION

Run No.	Nitrogen		Argon		Oxygen	
	Plus	Minus	Plus	Minus	Plus	Minus
8	1517	229	829	935	533	1201
10	1135	614	1024	733	570	1176

Run 10 has been adopted as the final correlation although there still remain systematic deviations in the data as shown in Figures 27 to 31. The various regions designated in these figures correspond to the following:

Region I, nitrogen mole fraction greater than 0.5

Region II, argon mole fraction greater than 0.5

Region III, oxygen mole fraction greater than 0.5

Region IV, mole fraction of all three components less than 0.5.

These figures indicate systematic deviations at low temperatures; a relatively even distribution at between 170 and 180°R; systematic deviations between 190 and 210°R; a relatively even distribution between 220 and 230°R; and systematic deviations above 230°R. This pattern exists somewhat independent of the region examined, but is most predominant in Regions II, III, and IV.

A comparison of calculated vs. measured activity coefficients in each of the binaries are presented in Figures 32 to 45. The data were divided into approximately 20°R intervals and plotted on separate graphs. The solid lines represent the calculated activity coefficient at the two extremes of temperature. In this comparison the same systematic deviation is observed as in Figures 27 to 31 for the nitrogen-oxygen and nitrogen-argon system, the largest systematic error being approximately 2.5% in the nitrogen-argon system. The oxygen-argon system seems to show no systematic deviations.

A comparison of calculated and measured equilibria in the binary and ternary systems is given in Figures 46 to 82 which show tie lines in a ternary phase diagram at constant temperature and pressure. The figures are ordered

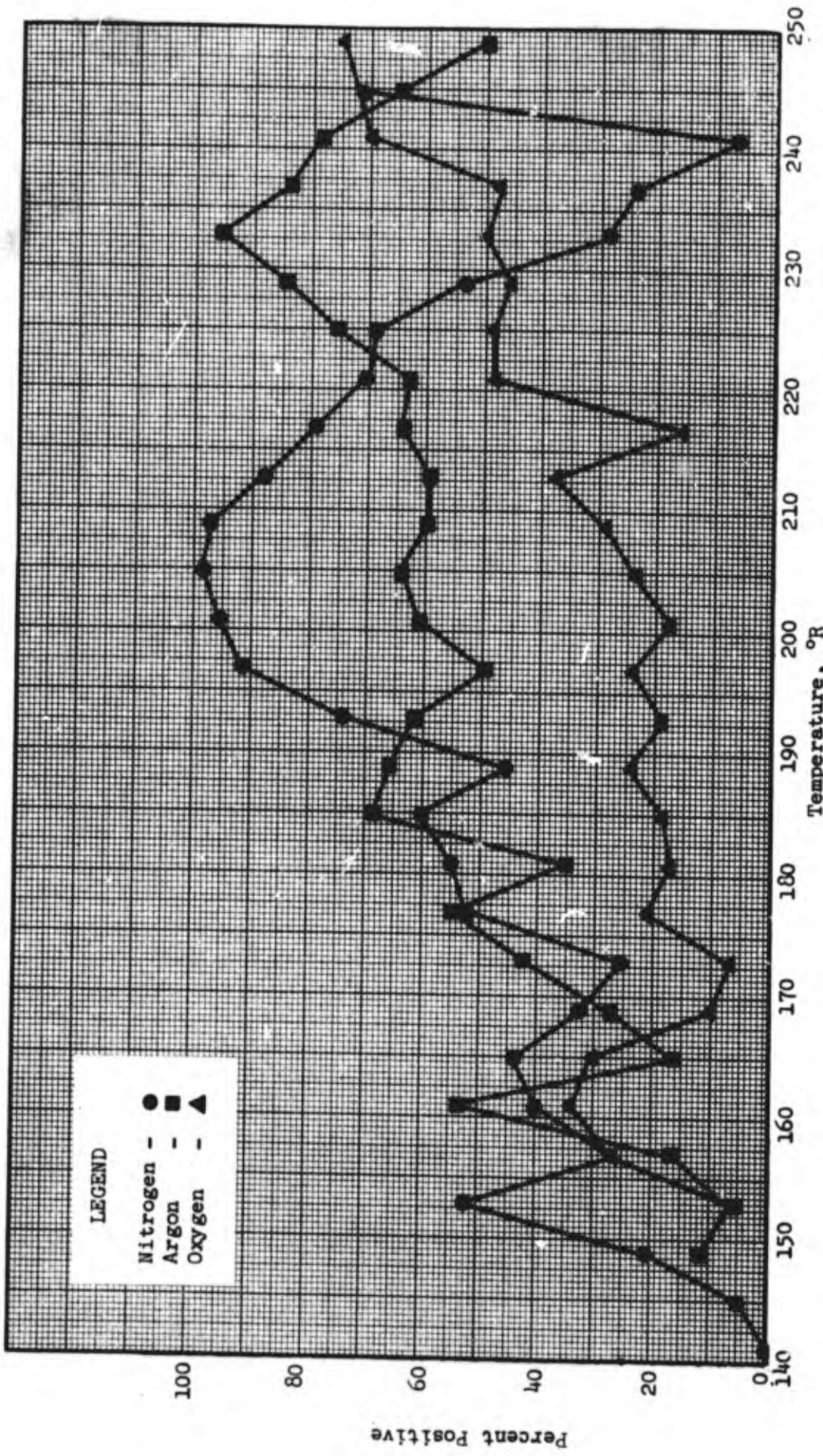


Figure 27. Summary of Bias of Points in Region I.

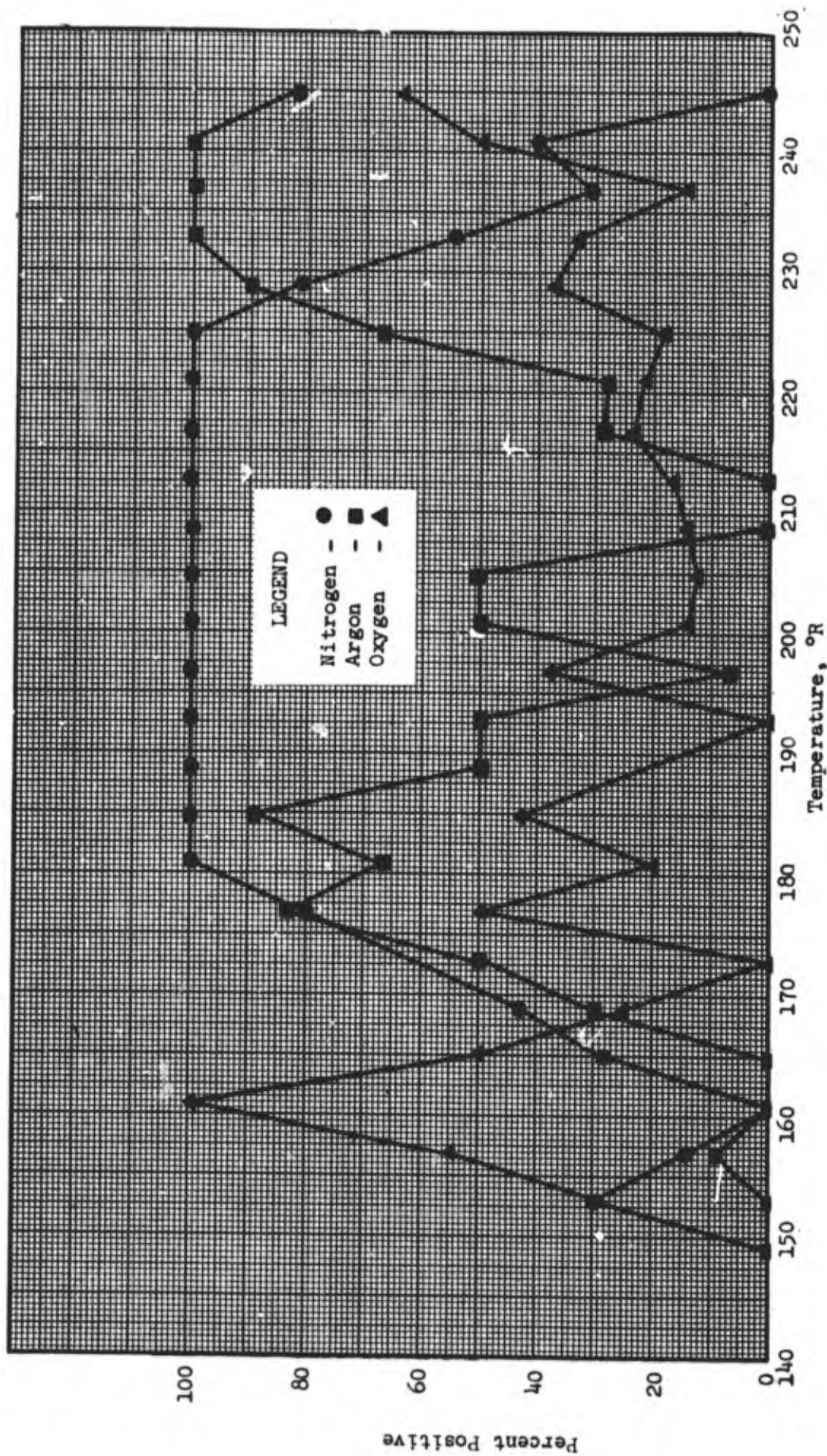


Figure 28. Summary of Bias of Points in Region II.

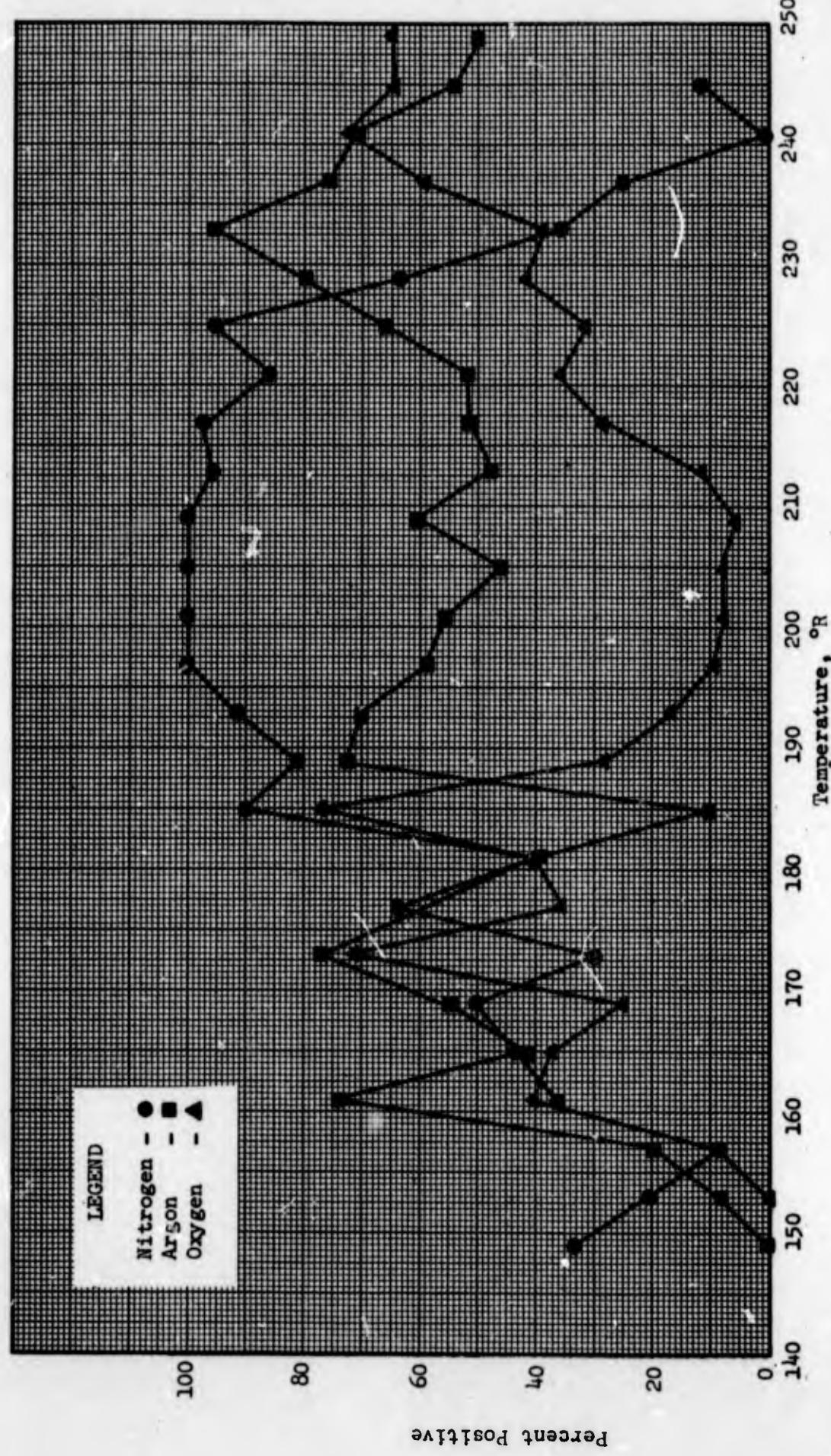


Figure 29. Summary of Bias of Points in Region III.

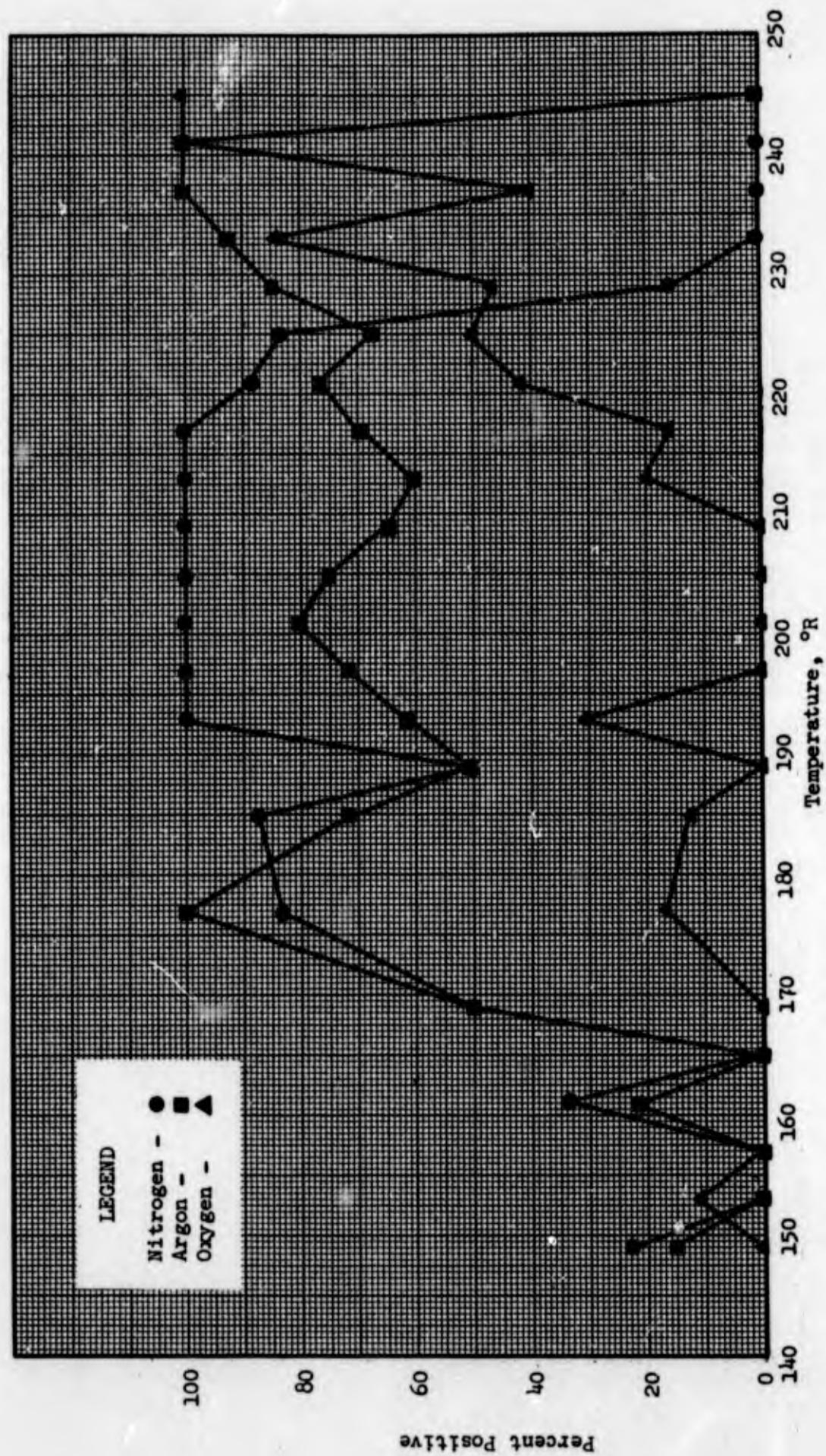


Figure 30. Summary of Bias of Points in Region IV.

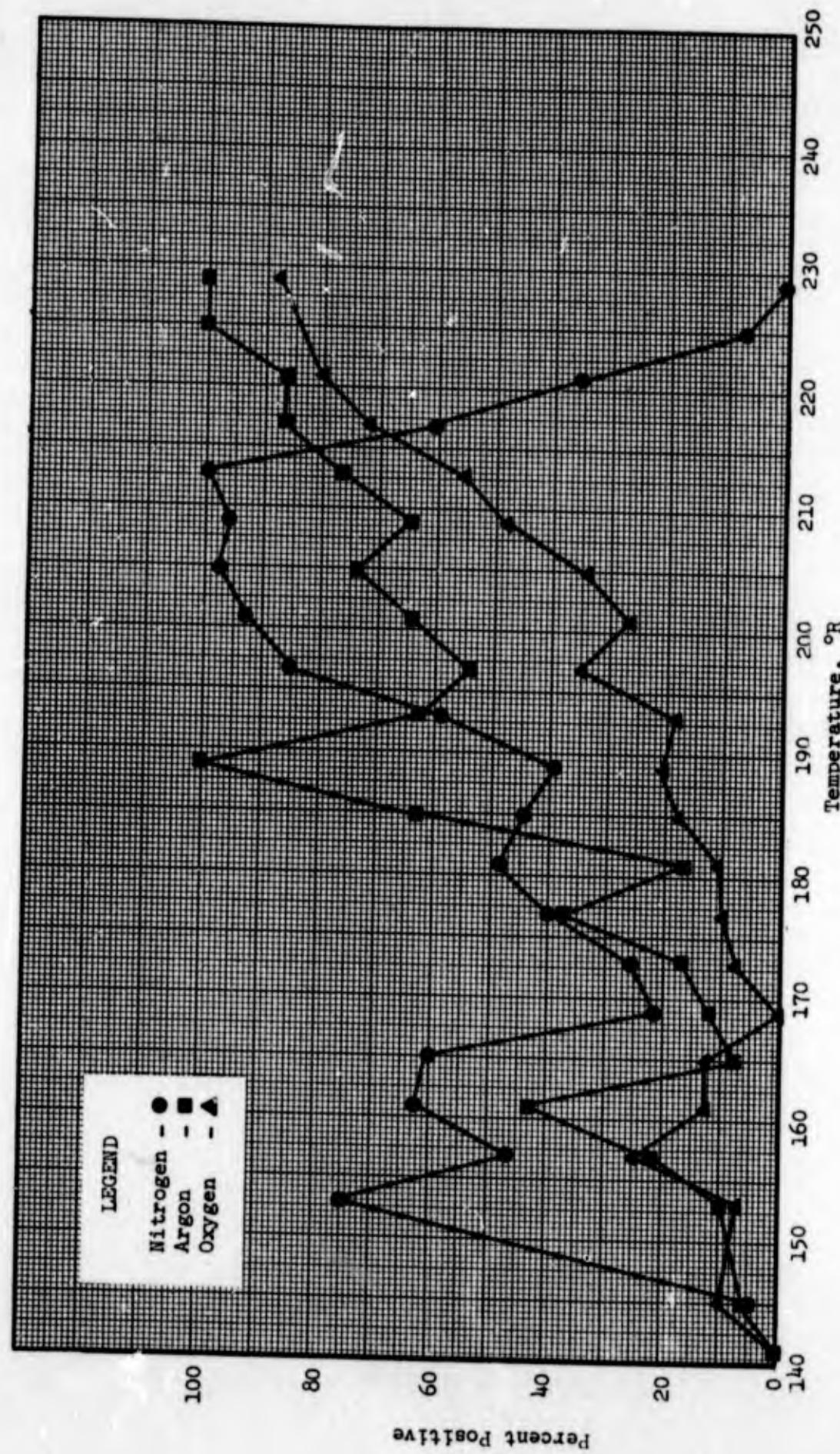


Figure 31. Summary of Bias of Points in all Regions.

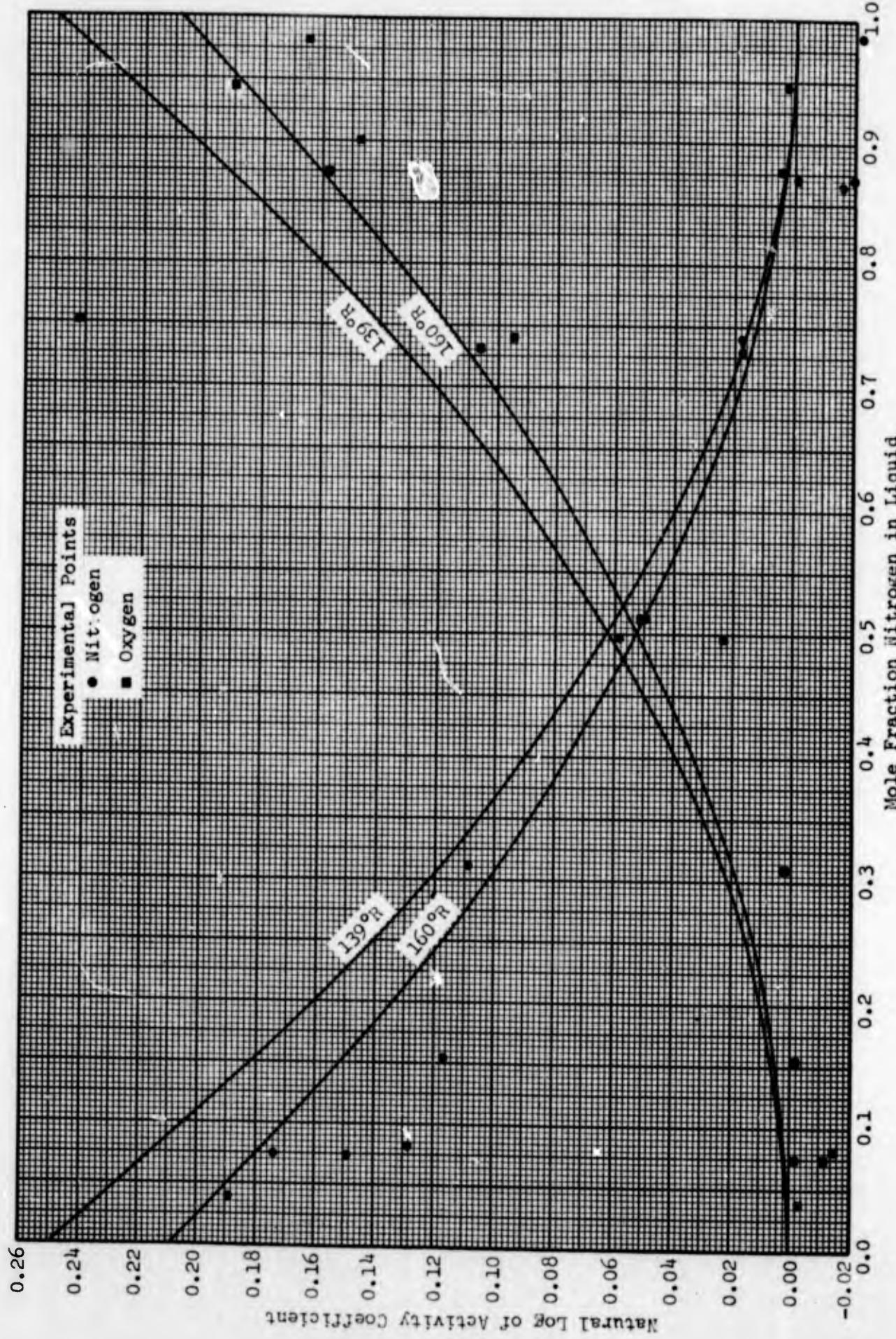


Figure 32. Activity Coefficients in the Nitrogen-Oxygen binary System,
Calculated vs. Experimental.

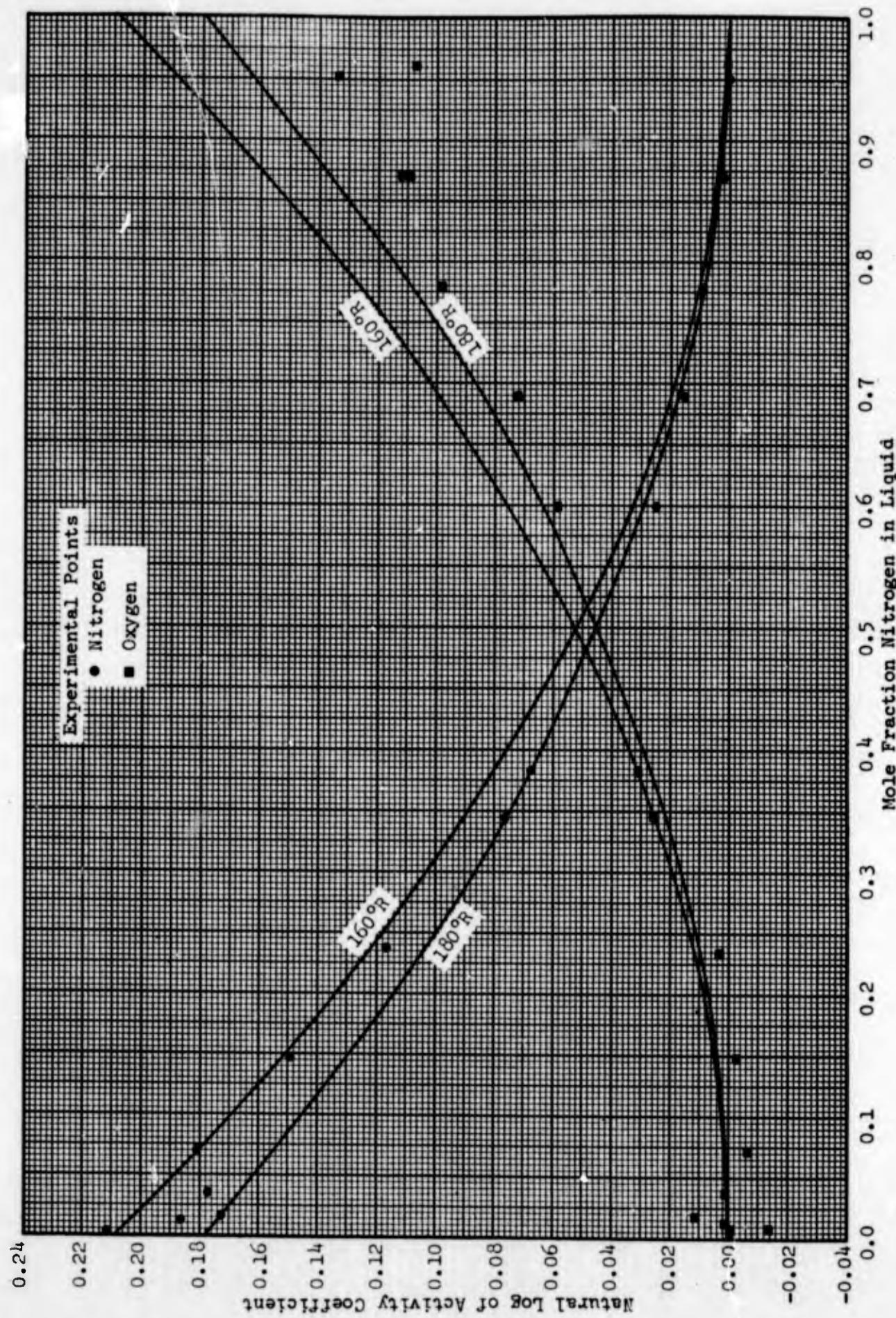


Figure 33. Activity Coefficients in the Nitrogen-Oxygen Binary System, Calculated vs. Experimental.

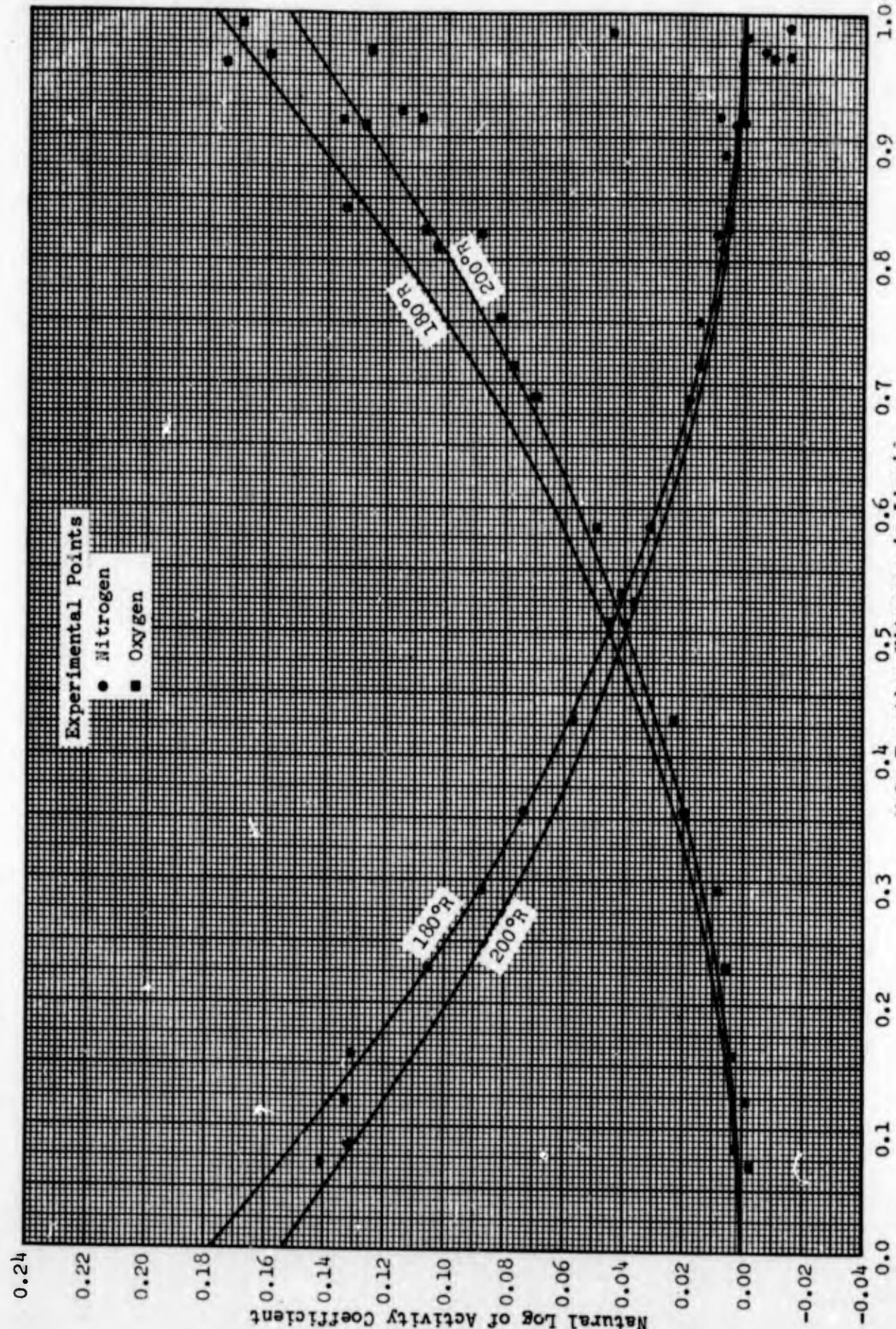


Figure 34. Activity Coefficients in the Nitrogen-Oxygen Binary System, Calculated vs. Experimental.

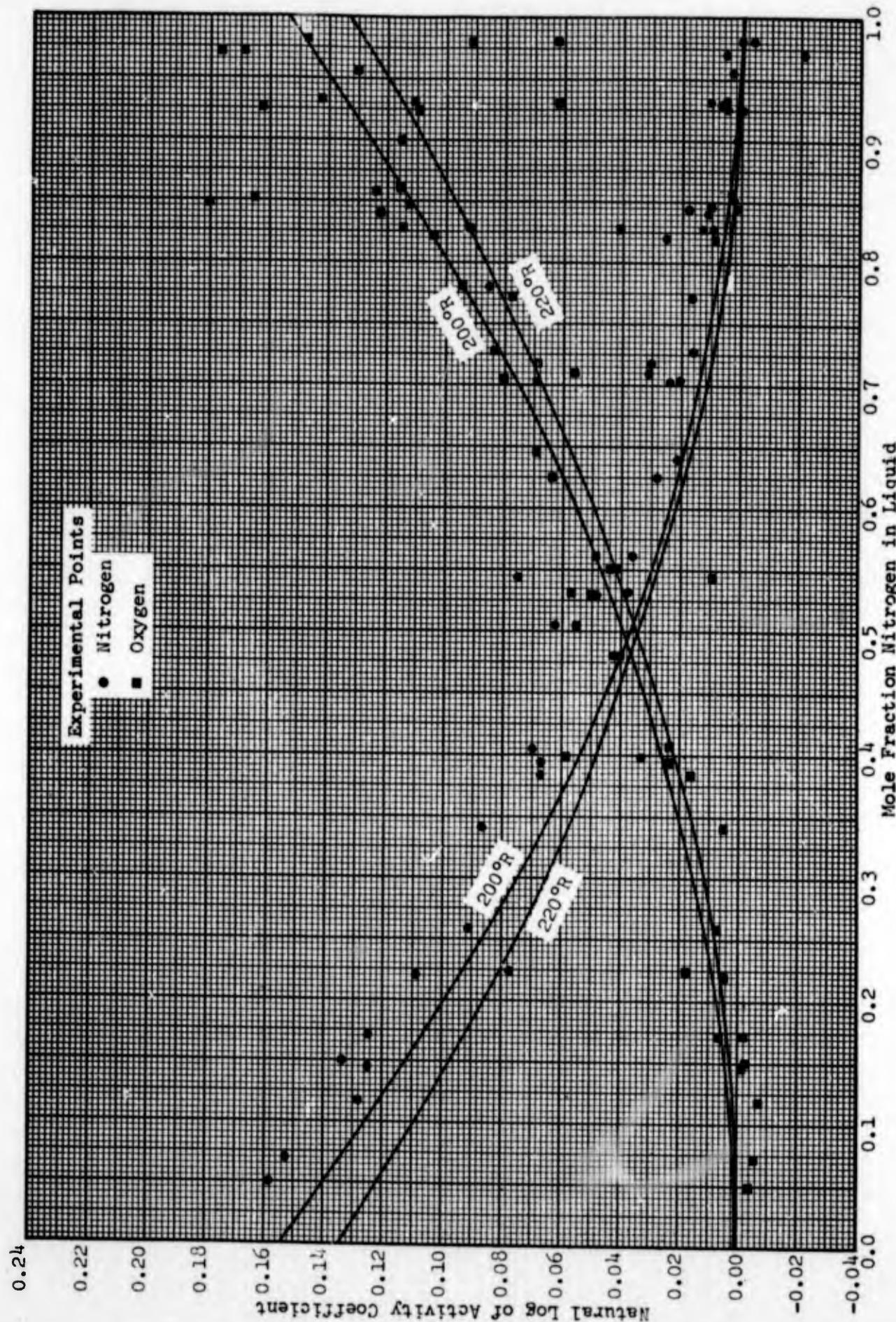


Figure 35. Activity Coefficients in the Nitrogen-Oxygen Binary System,
Calculated vs. Experimental.

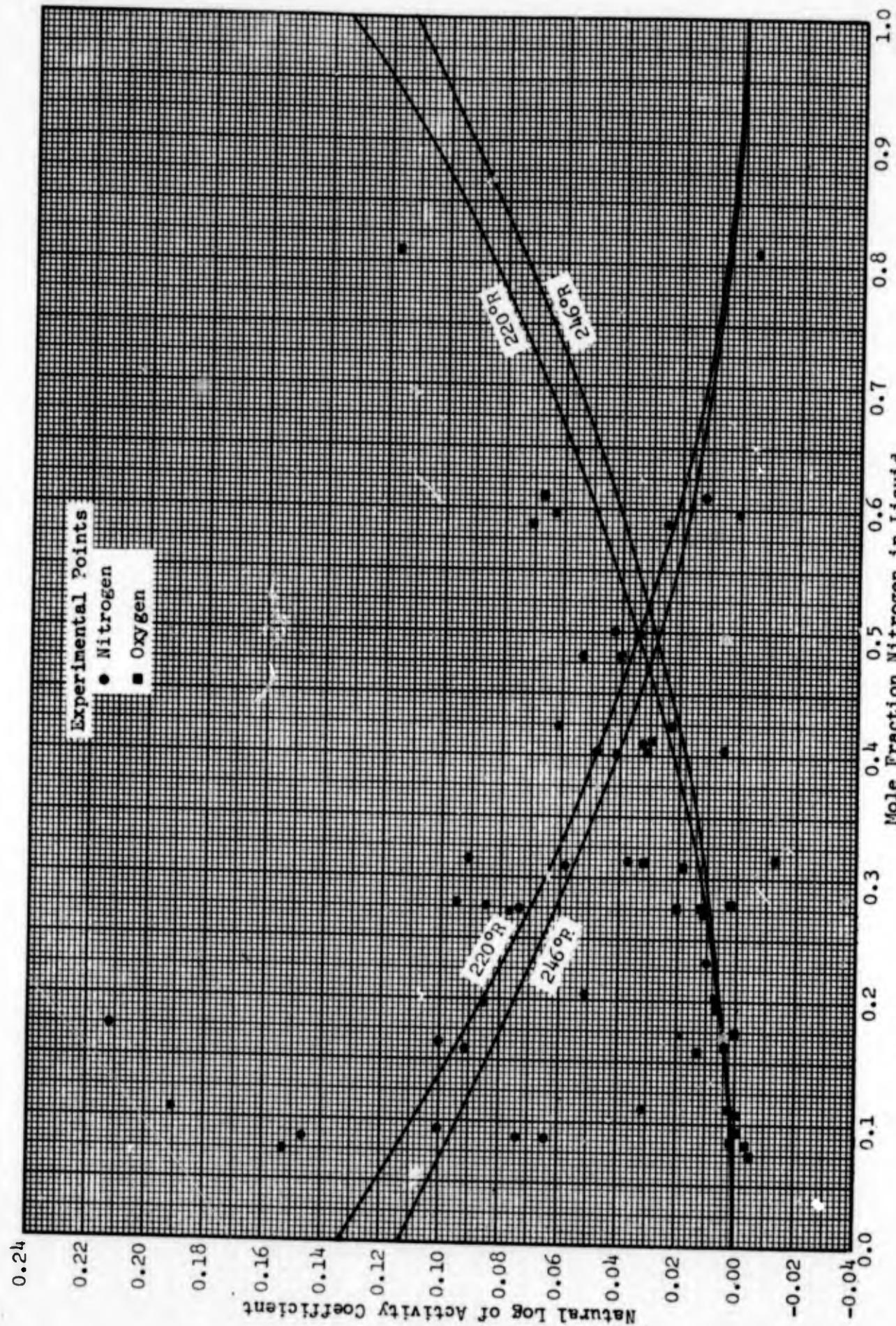


Figure 36. Activity Coefficients in the Nitrogen-Oxygen Binary System.
Calculated vs. Experimental.

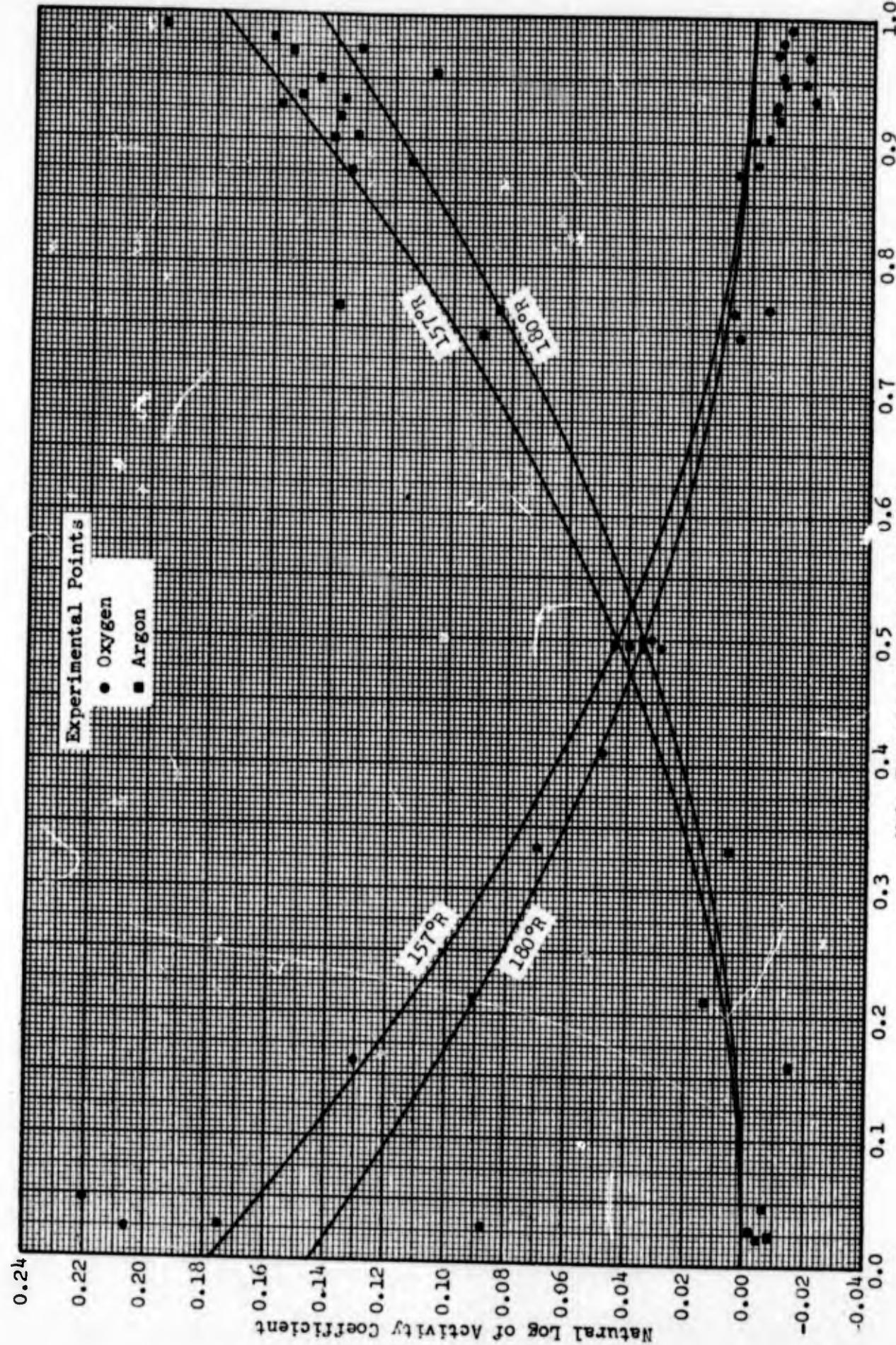


Figure 37. Activity Coefficients in the Oxygen-Argon Binary System, Calculated vs. Experimental.

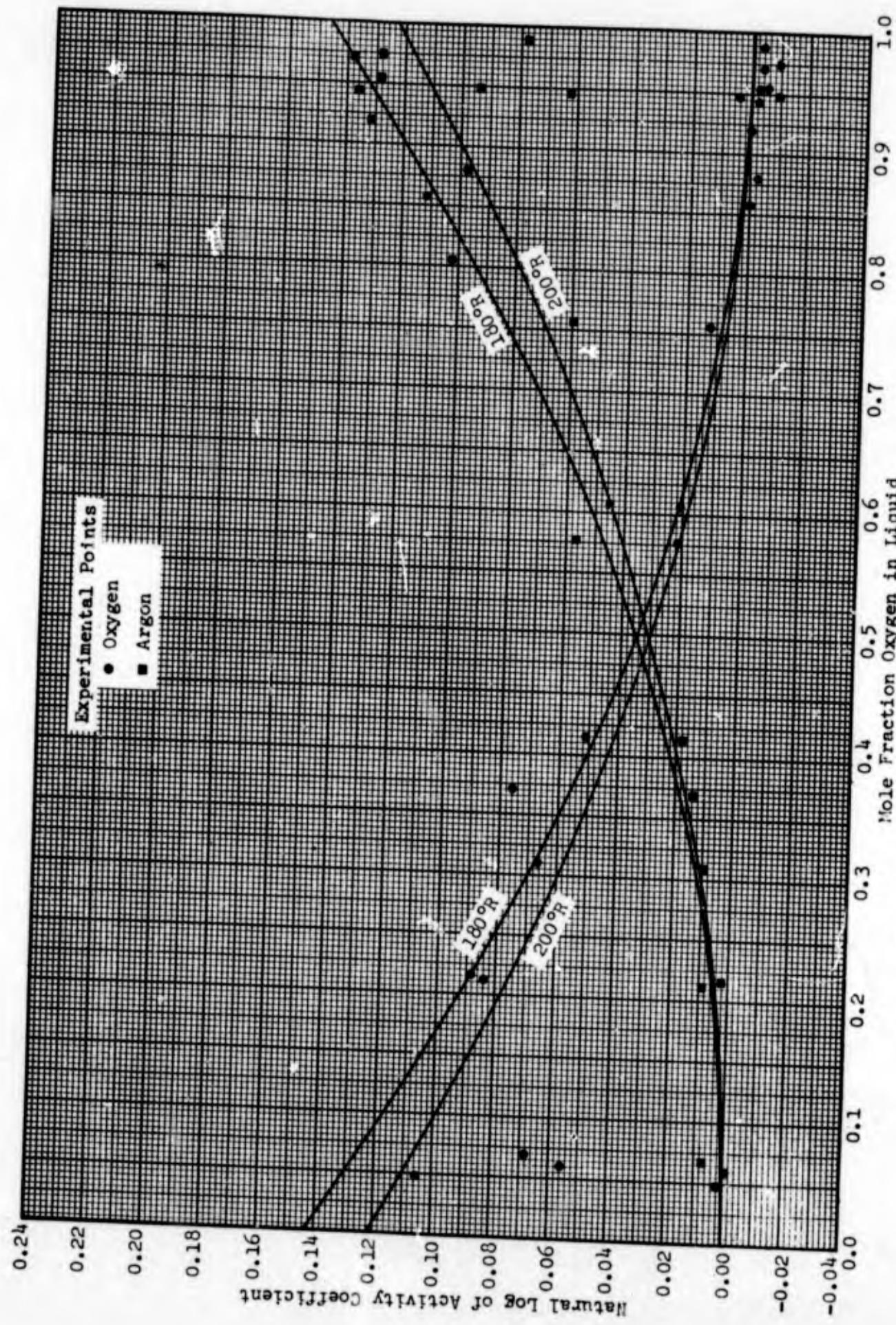


Figure 38. Activity Coefficients in the Oxygen-Argon Binary System, Calculated vs. Experimental.

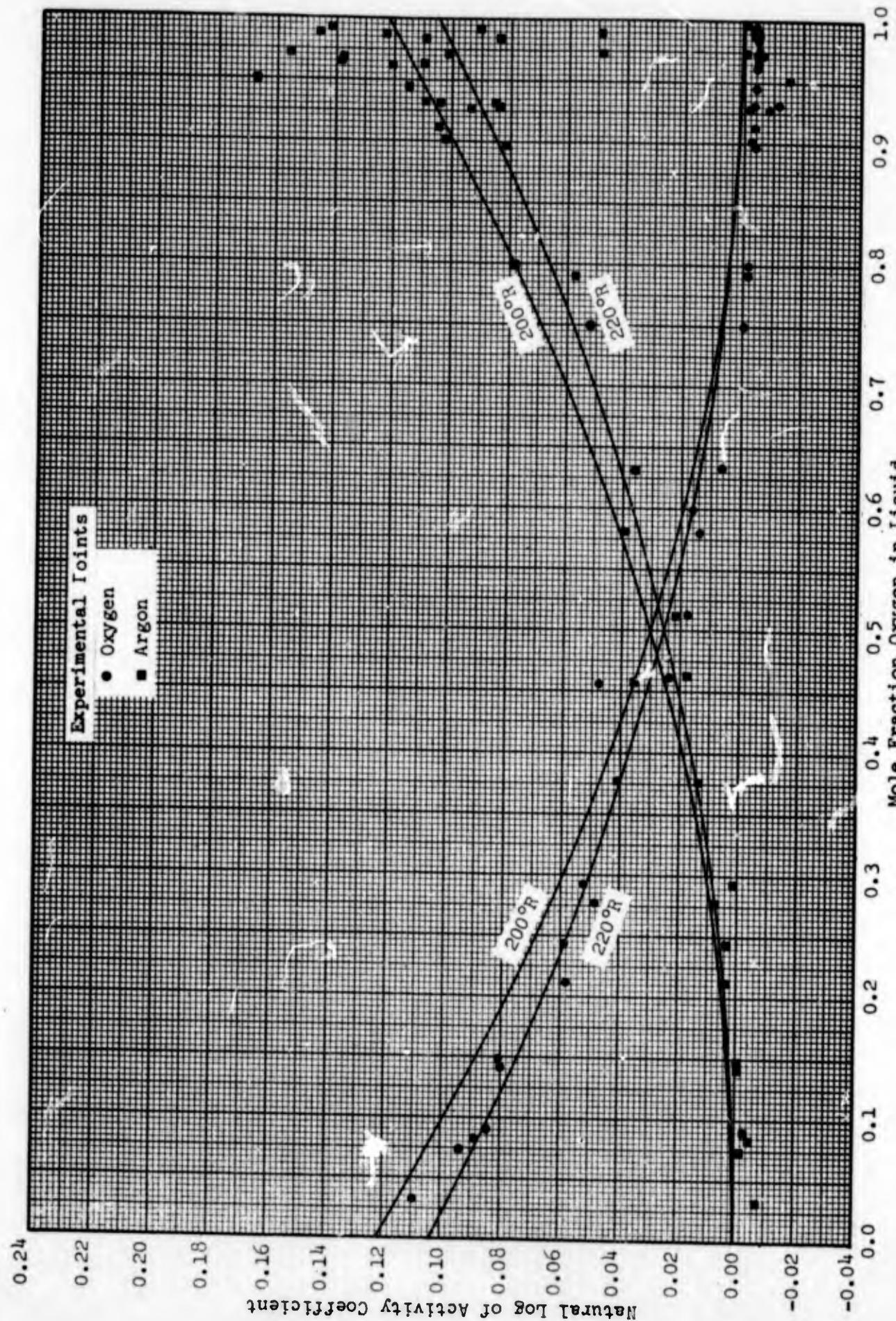


Figure 39. Activity Coefficients in the Oxygen-Argon Binary System, Calculated vs. Experimental.

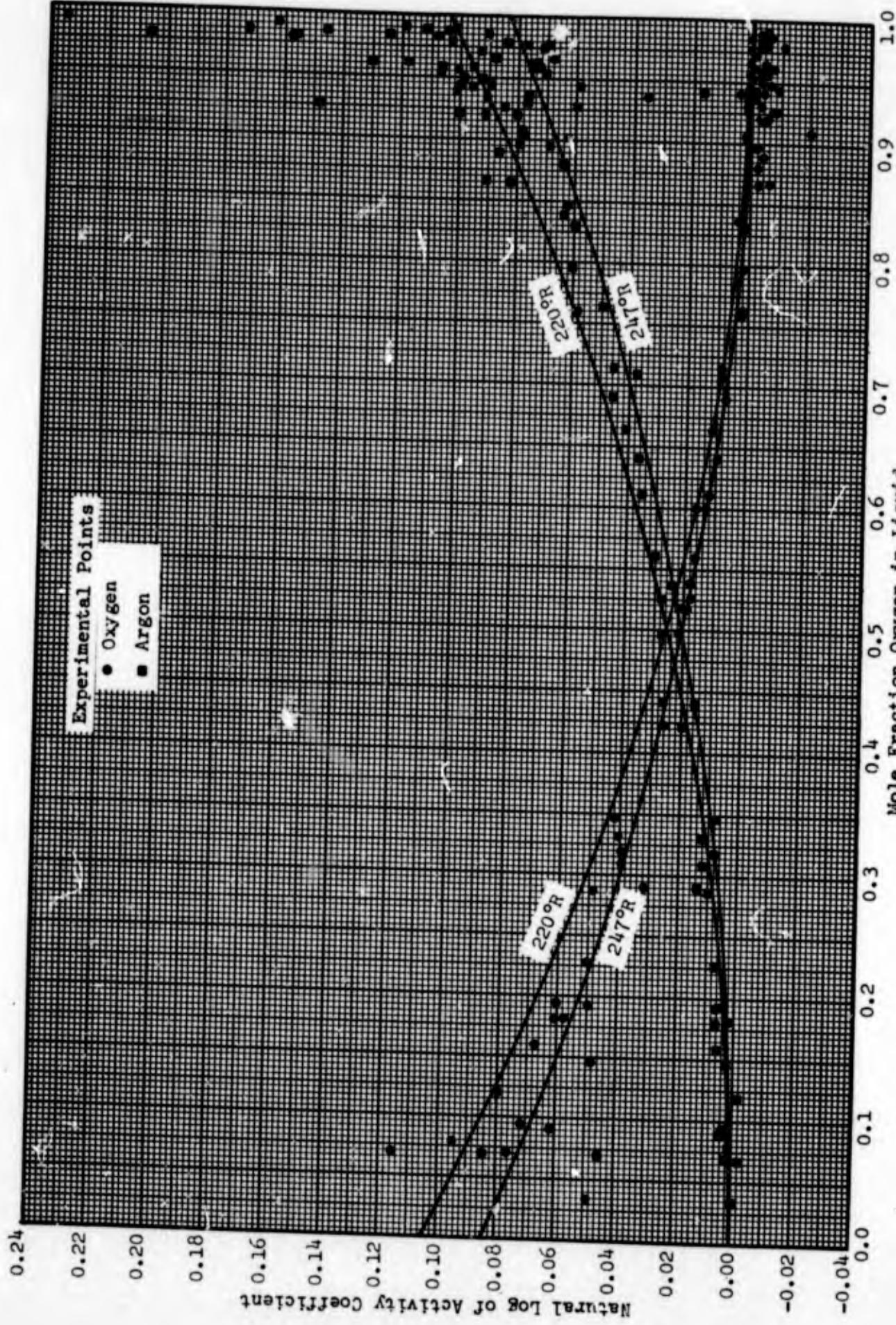


Figure 40. Activity Coefficients in the Oxygen-Argon Binary System,
Calculated vs. Experimental.

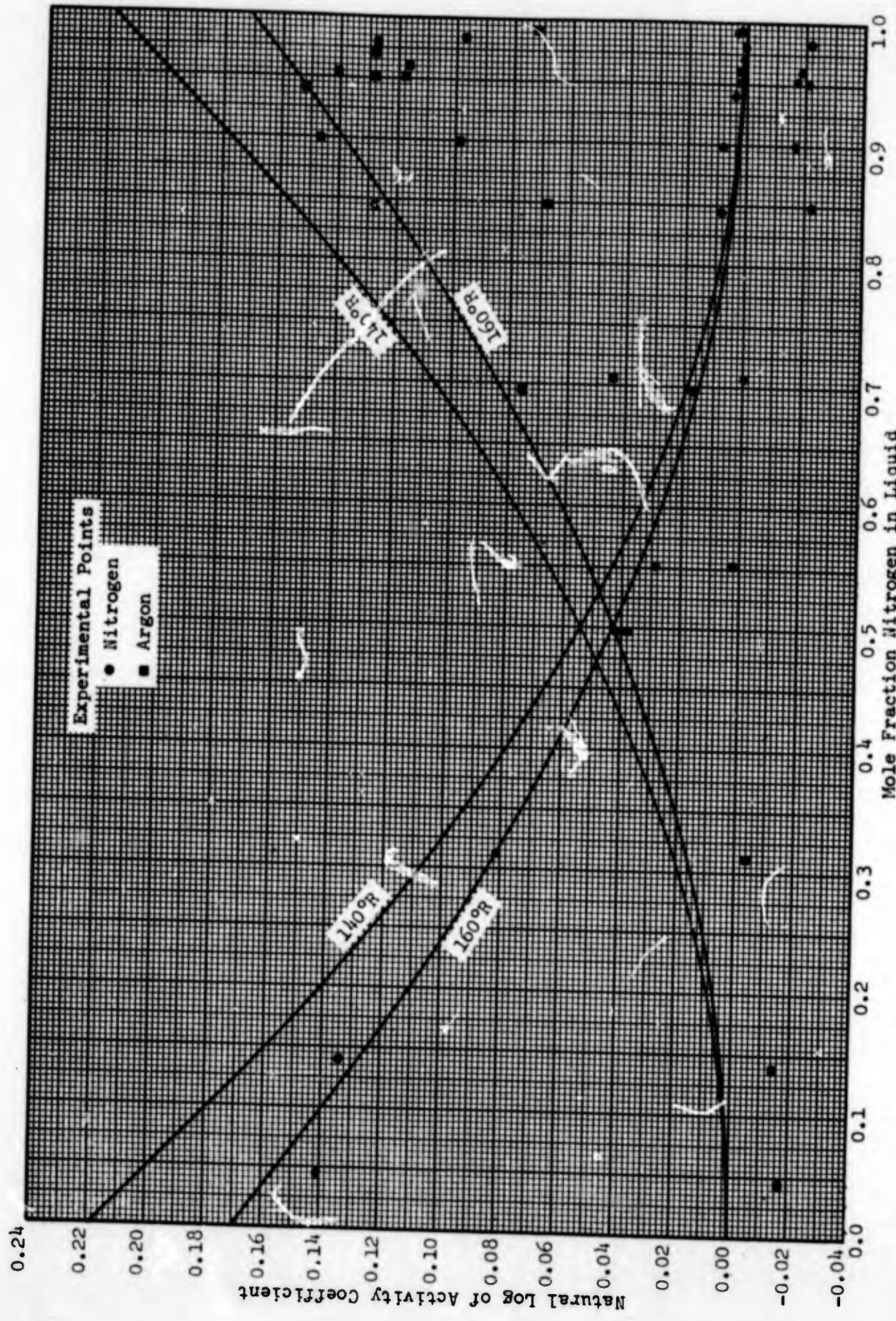


Figure 41. Activity Coefficients in the Nitrogen-Argon binary System, Calculated vs. Experimental.

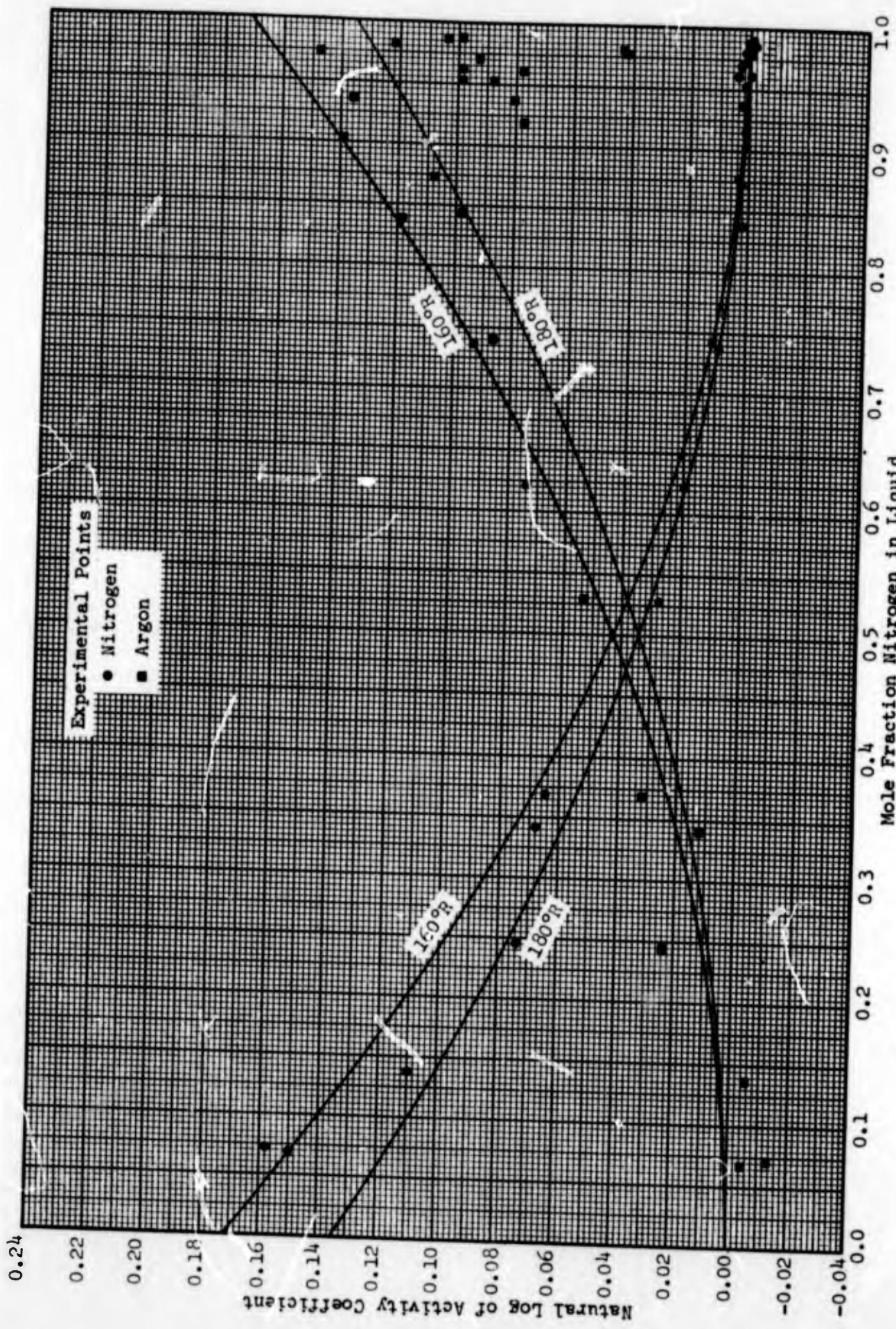


Figure 42. Activity Coefficients in the Nitrogen-Argon Binary System, Calculated vs. Experimental.

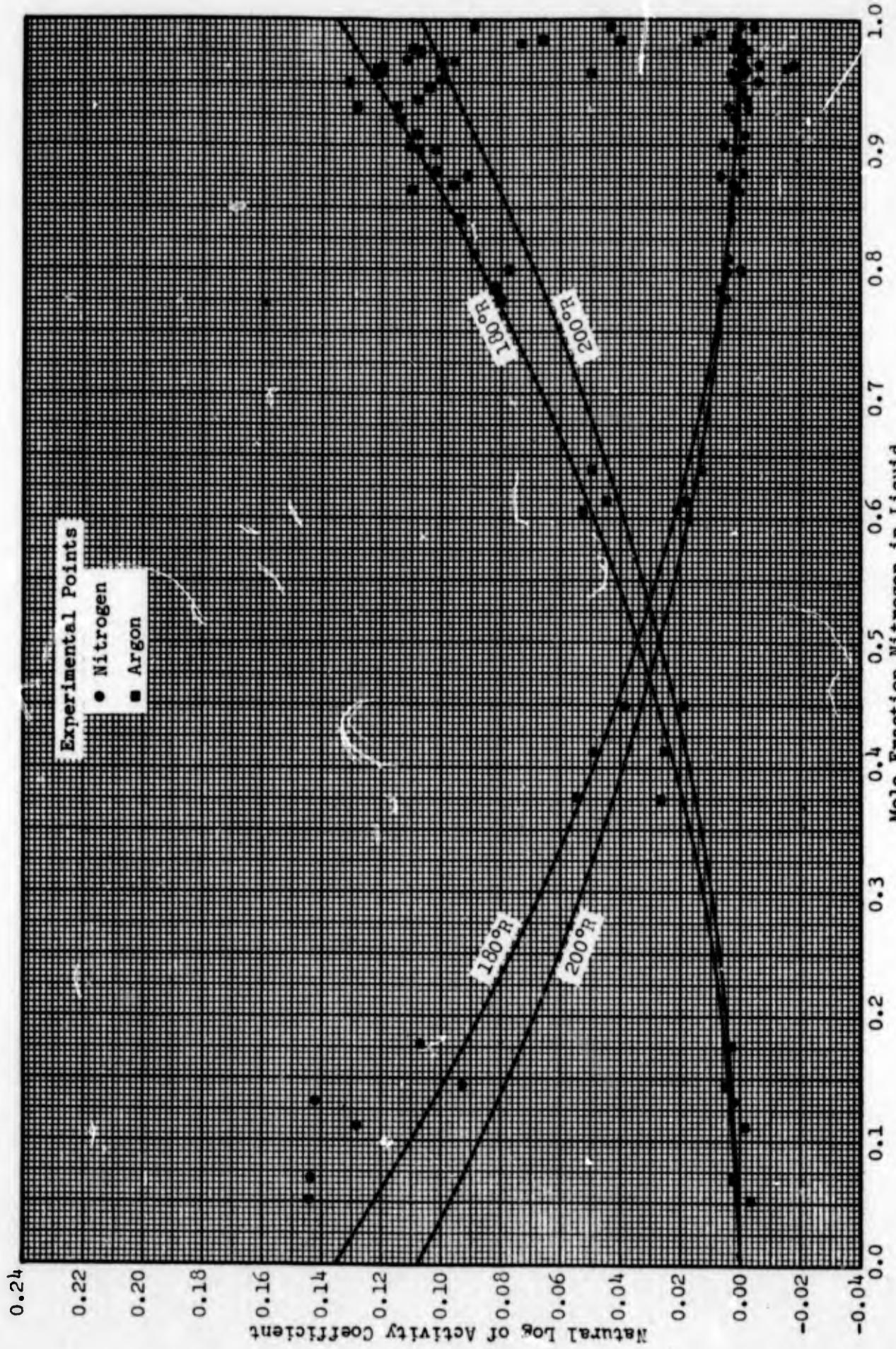


Figure 4.3. Activity Coefficients in the Nitrogen-Argon Binary System, Calculated vs. Experimental.

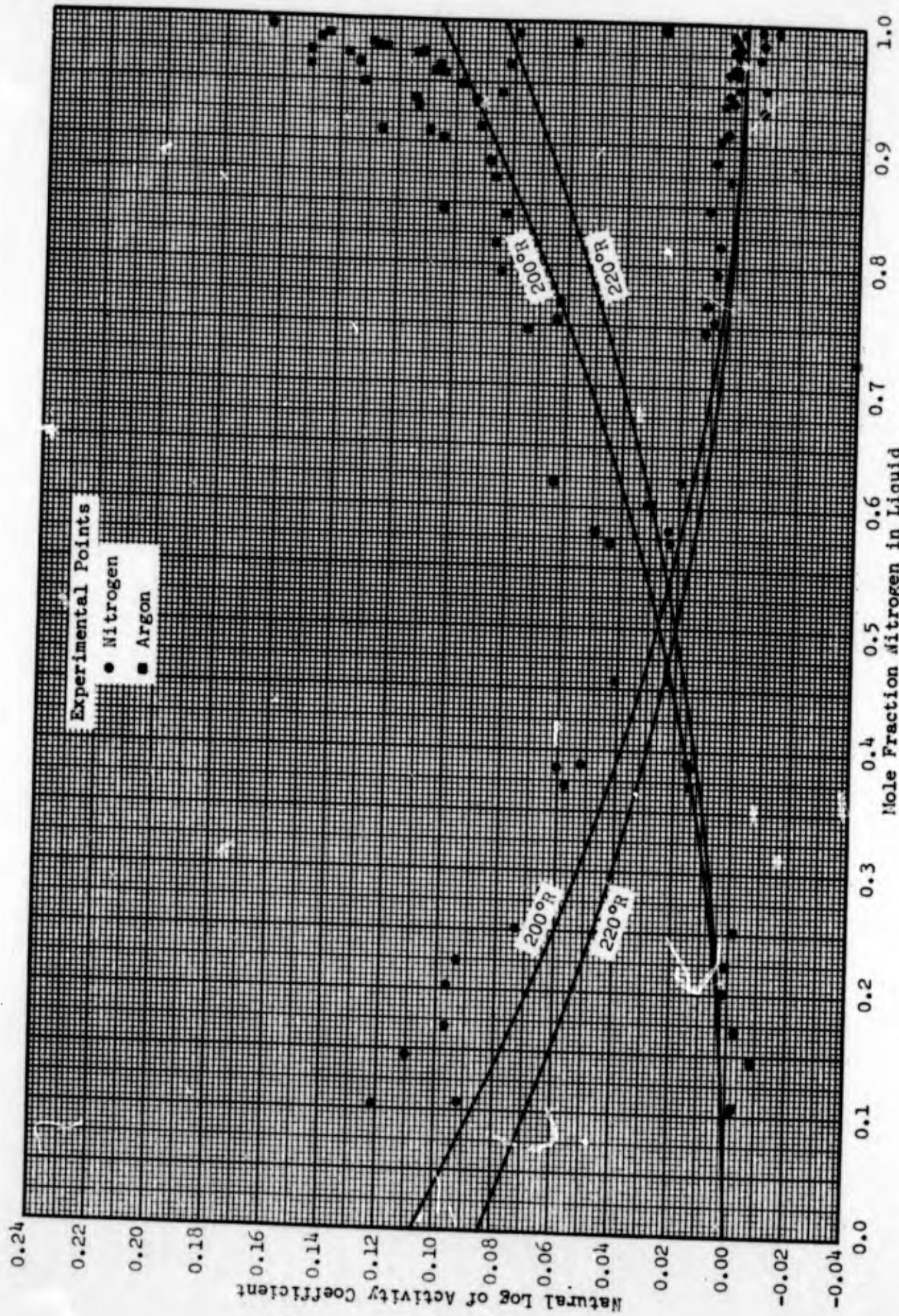


Figure 44. Activity Coefficients in the Nitrogen-Argon Binary System, Calculated vs. Experimental.

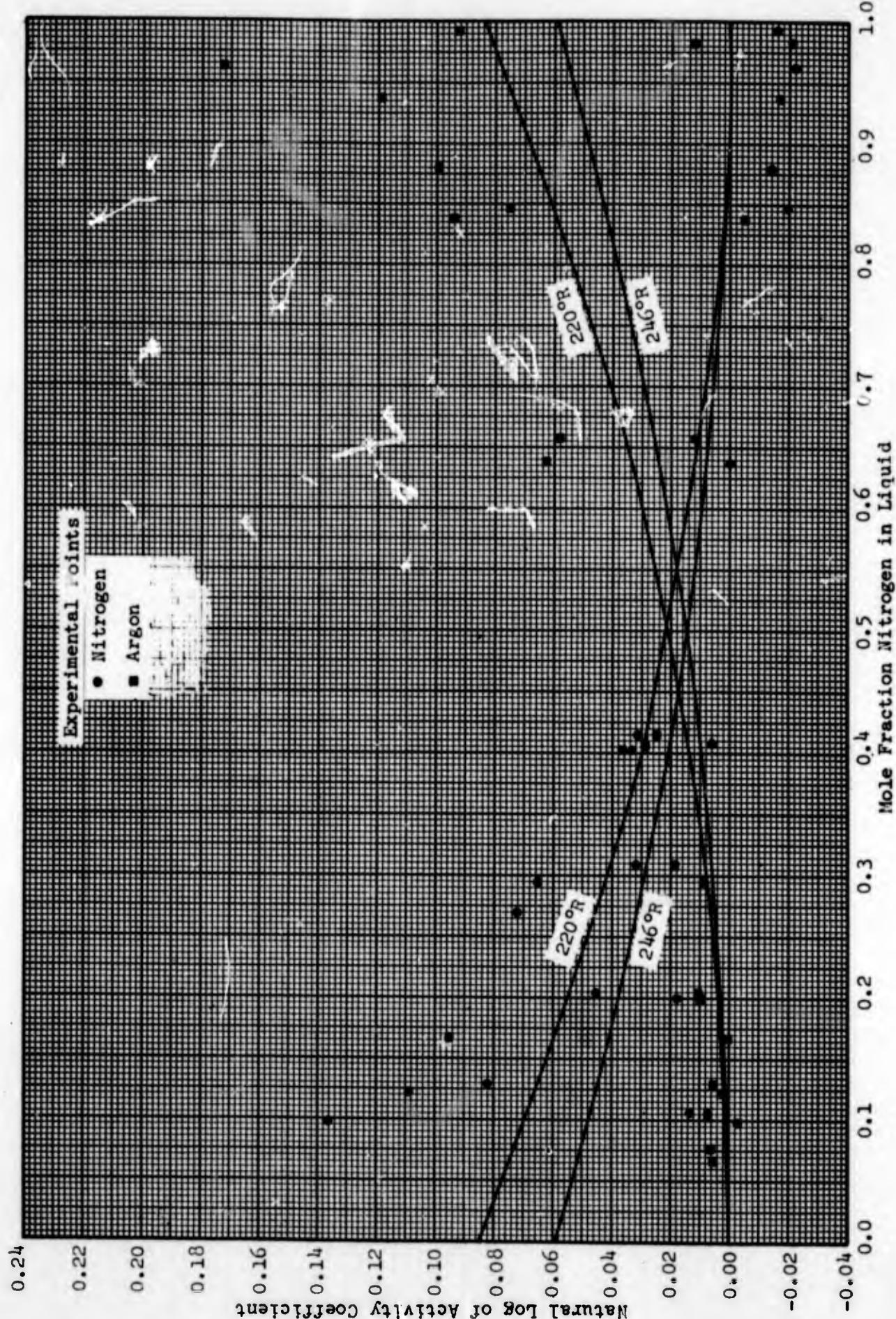


Figure 45. Activity Coefficients in the Nitrogen-Argon Binary System, Calculated vs. Experimental.

according to increasing pressure. The liquid phase corresponds to tie line points on the left and the vapor phase corresponds to tie line points on the right, and lines have been drawn connecting all points in both phases. These data show systematic deviations consistent with the deviations in activity coefficients. The largest error occurs at 20 atm where the difference corresponds to an error of 2.5% in the calculation of the pressure.

From an examination of the differences between calculated and measured data it is concluded that the correlation represents the data with a difference less than 2.5% in relative volatility and pressure in most regions. The largest difference is probably about 2.5%. The experimental data scatter less than this with an accuracy of about $\pm 0.5\%$ in the pressure and $\pm 1\%$ in the relative volatility.

A comparison of the correlation with literature data can probably be best made in terms of comparisons with the Latimer⁽³⁴⁾ correlation, since it represents a good summary of existing data. This comparison is given in Figures 83 to 85 for each of the binary systems. In the nitrogen-oxygen system the difference varies up to about 2% depending on the composition and pressure. In the nitrogen-argon system the difference varies up to 10% at 20 atm, and in the argon-oxygen system the difference varies up to about 5%.

Factors which influence this correlation are:

1. The properties of "liquid" nitrogen above the critical temperature of nitrogen.
2. The partial molar volume of the components at pressures approaching the critical pressure of a mixture.
3. The assumption of a separate free energy expression for the vapor phase and the liquid phase.

These factors are inherent problems in the correlation of data by means of activity coefficients based upon the pure liquid component as the standard state. The systematic errors observed with this correlation probably are due to the uncertainty of these factors.

An alternate but more difficult approach would be to correlate the data in terms of an equation of state applicable to both the vapor and the liquid phases. This method would eliminate the need for a pure liquid reference state. The partial molar volume could be calculated from the equation of state, and the free energy equation would be continuous in going from vapor to liquid.

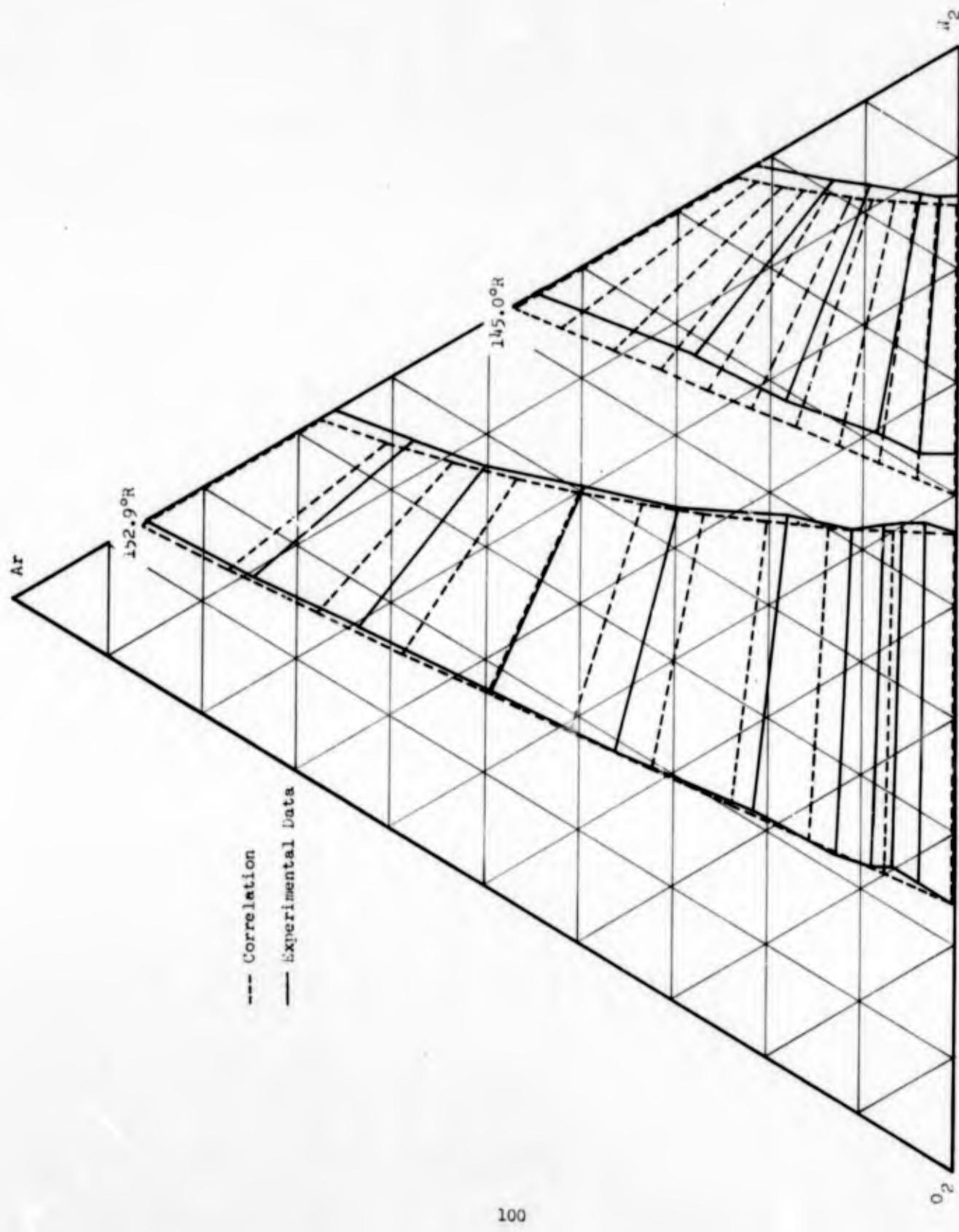


Figure 46. Comparison of Experimental Data and the Correlation, 1 Atmosphere.

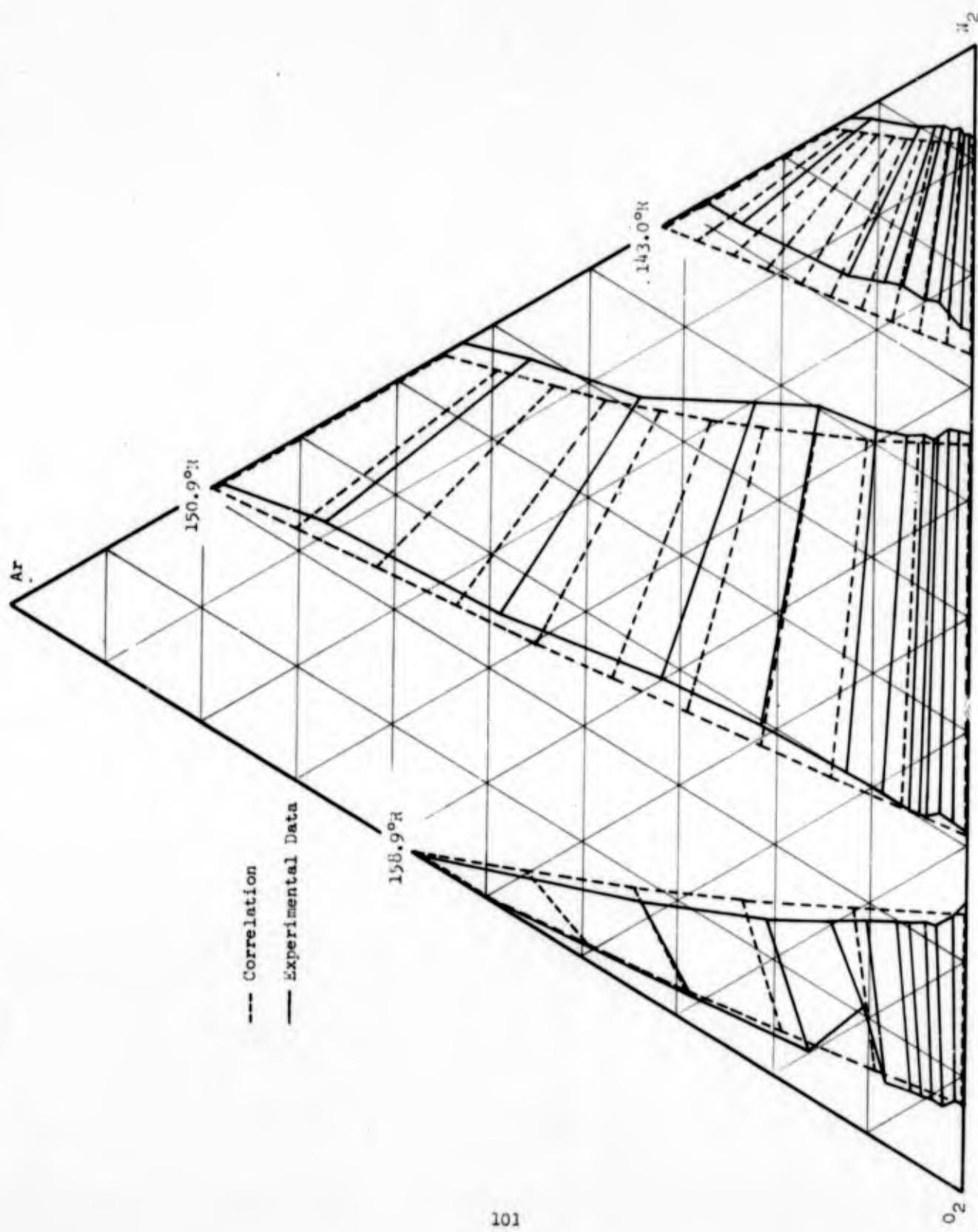


Figure 47. Comparison of Experimental Data and the Correlation, 1 Atmosphere.

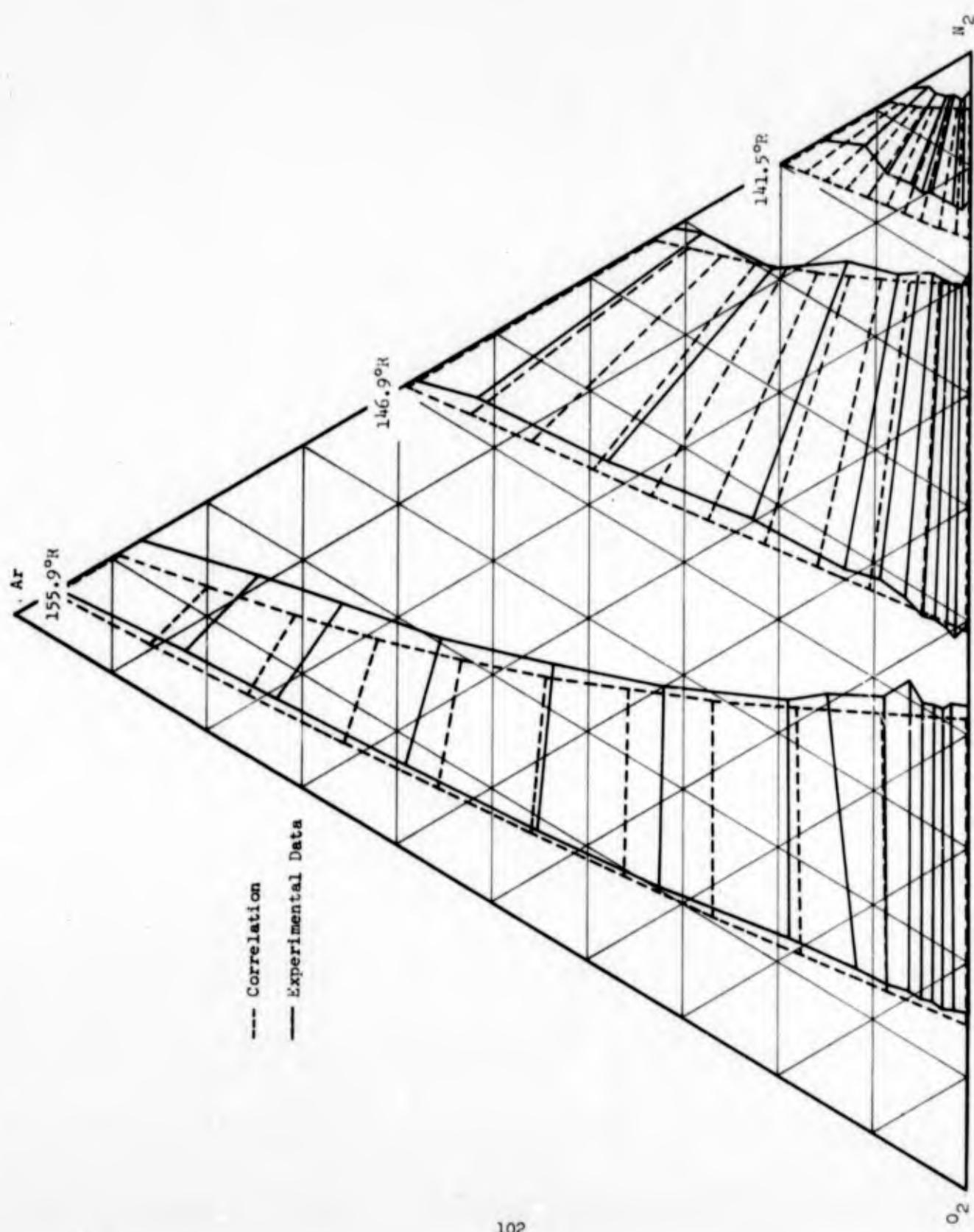


Figure 48. Comparison of Experimental Data and the Correlation, 1 Atmosphere.

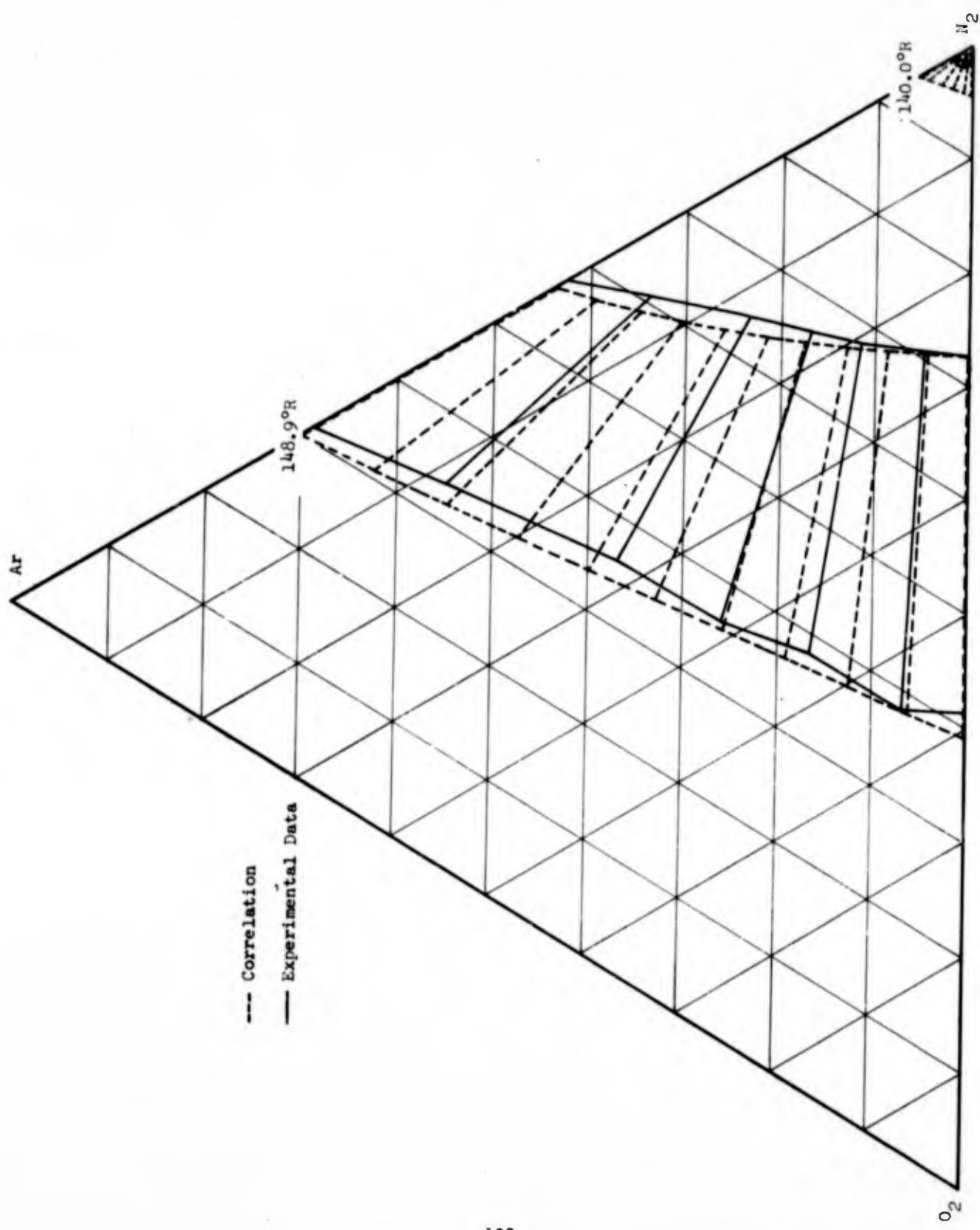


Figure 49. Comparison of Experimental Data and the Correlation, 1 Atmosphere.

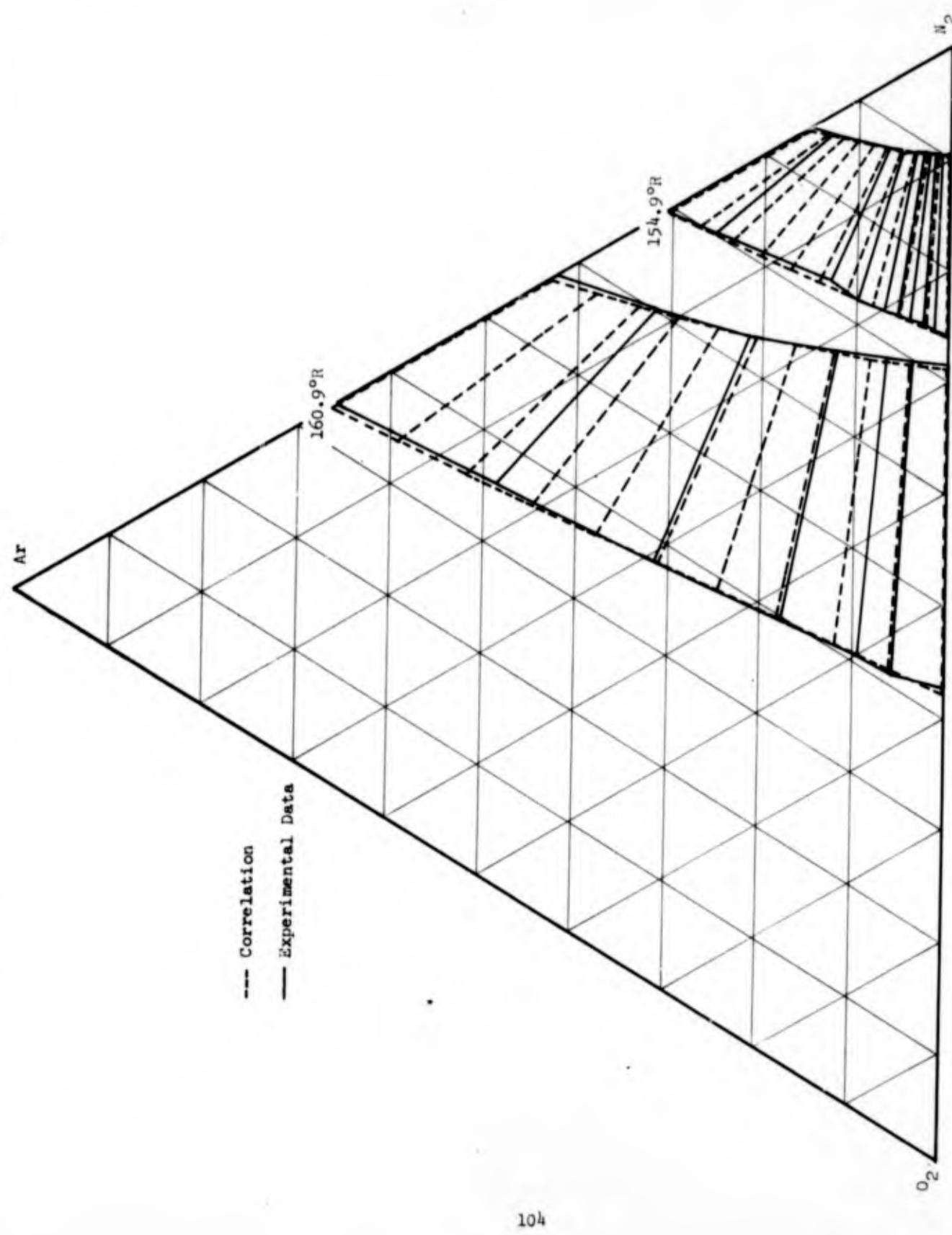


Figure 50. Comparison of Experimental Data and the Correlation, 2 Atmospheres.

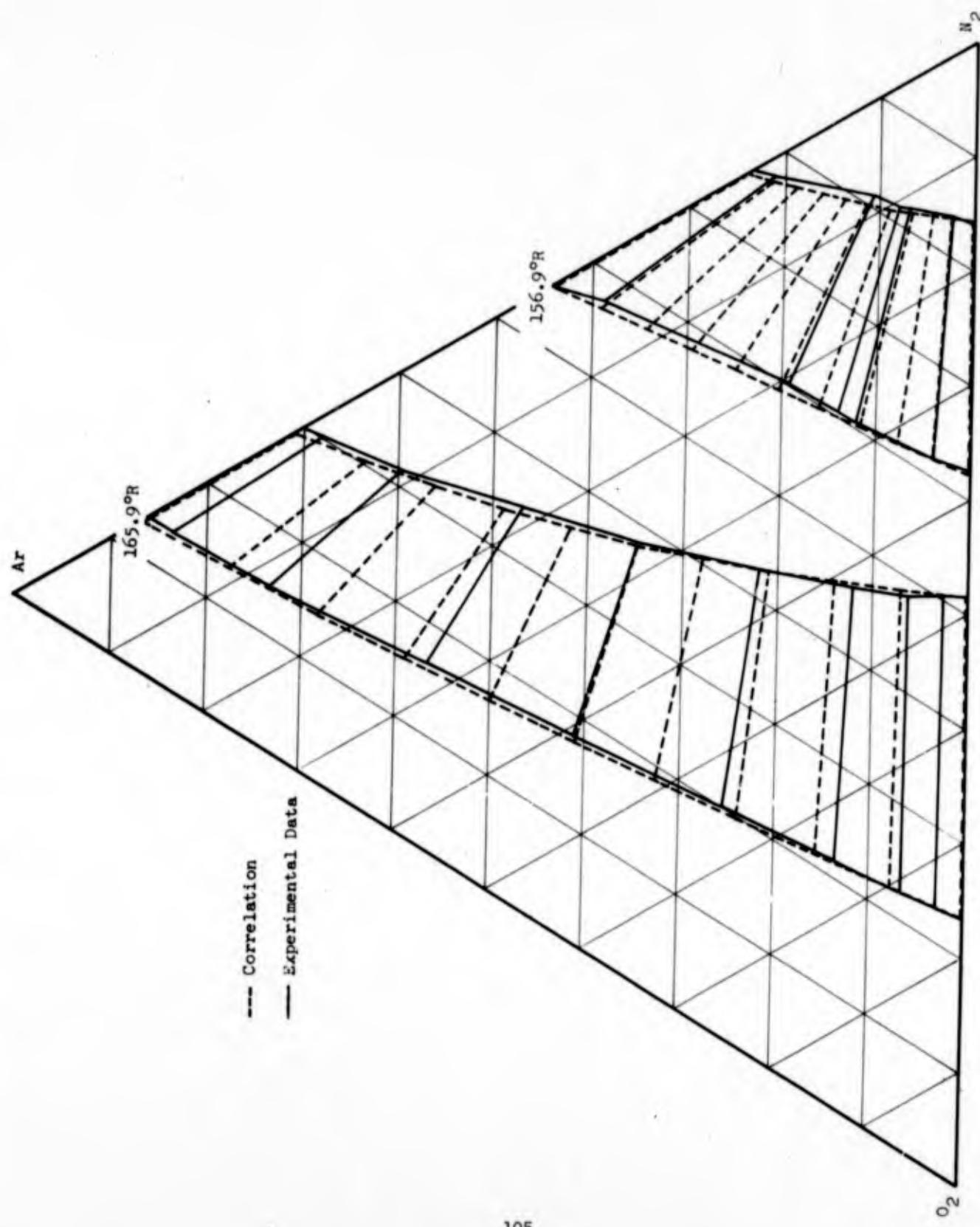


Figure 51. Comparison of Experimental Data and the Correlation, 2 Atmospheres.

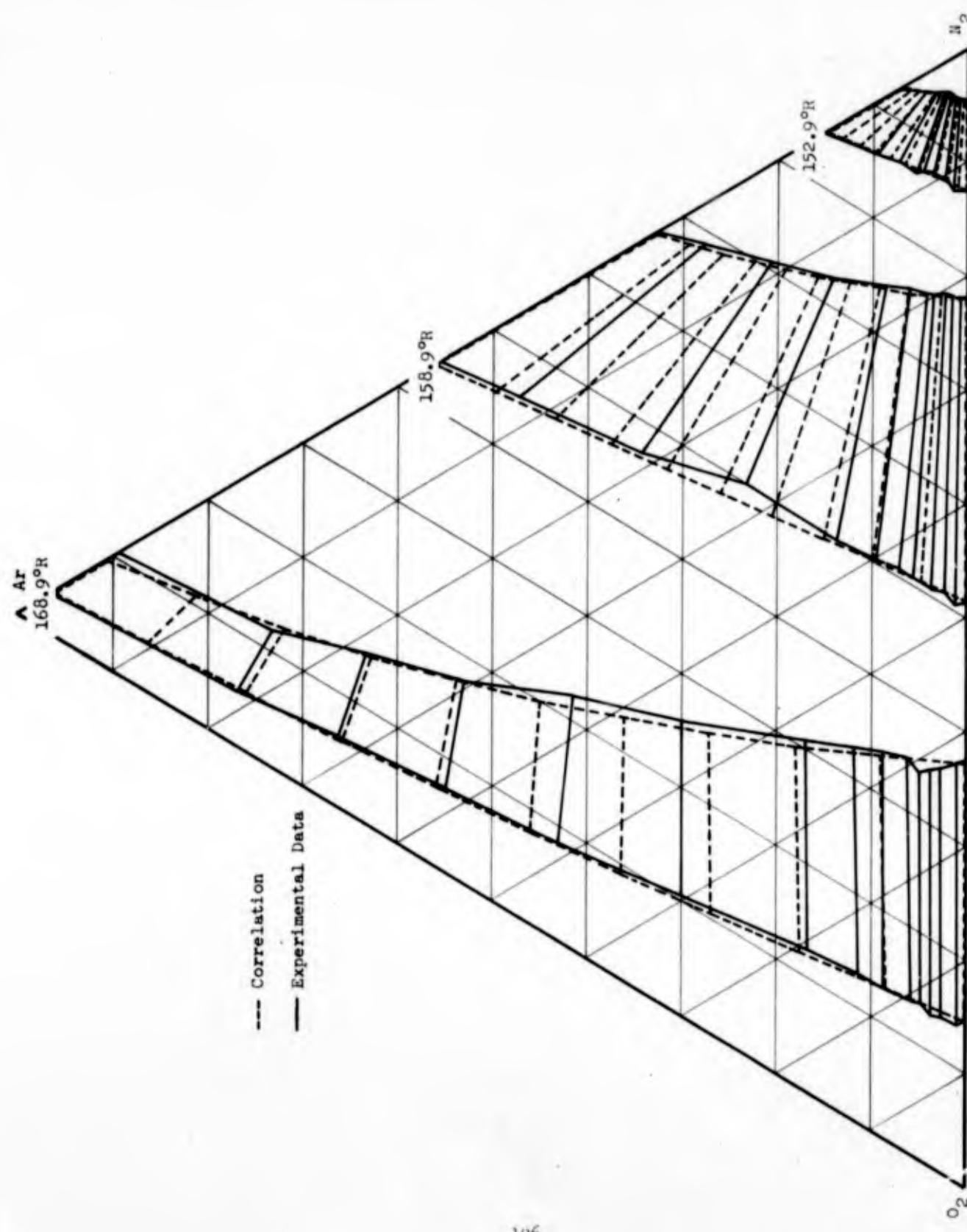


Figure 52. Comparison of Experimental Data and the Correlation, 2 Atmospheres.

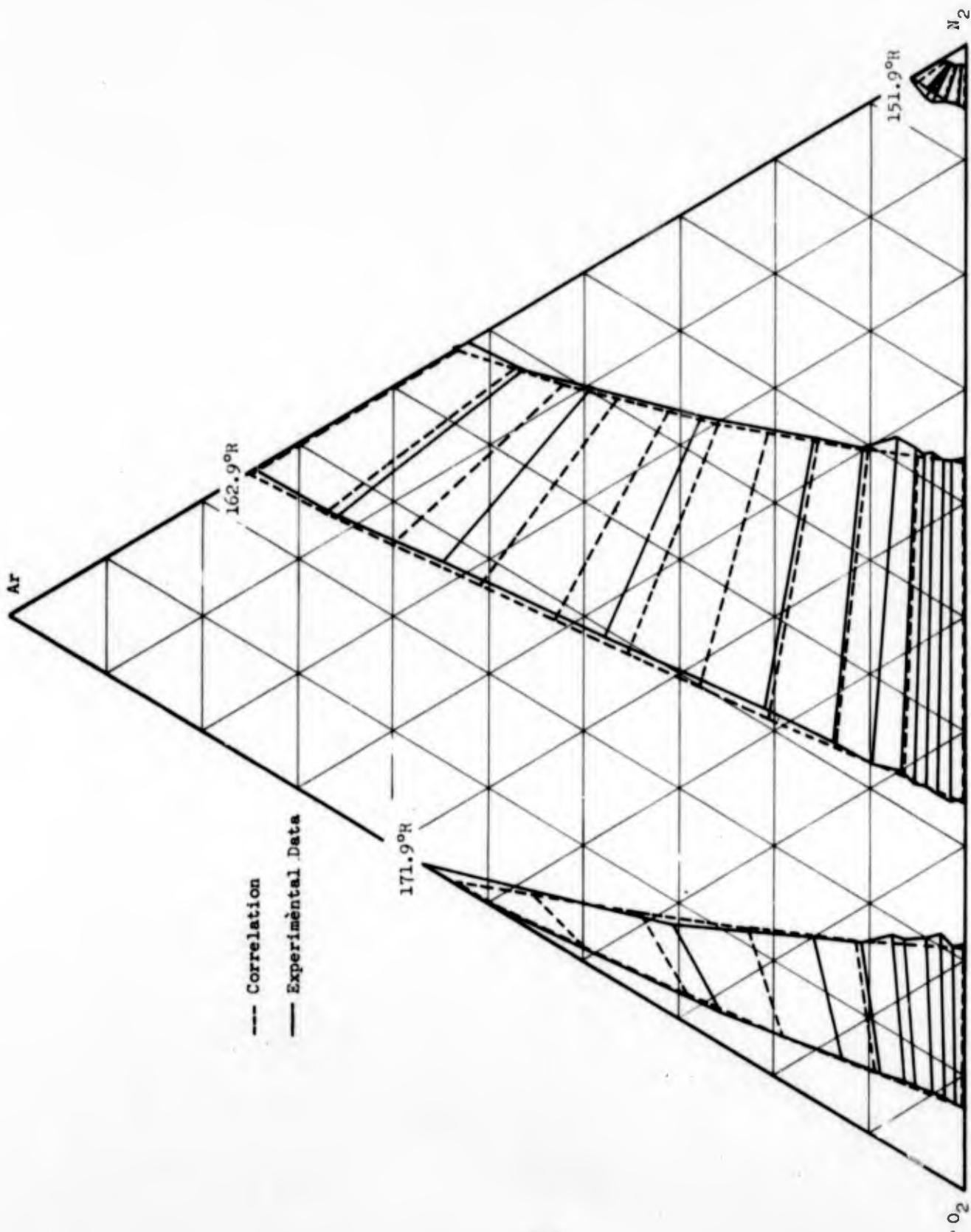


Figure 53. Comparison of Experimental Data and the Correlation, 2 Atmospheres.

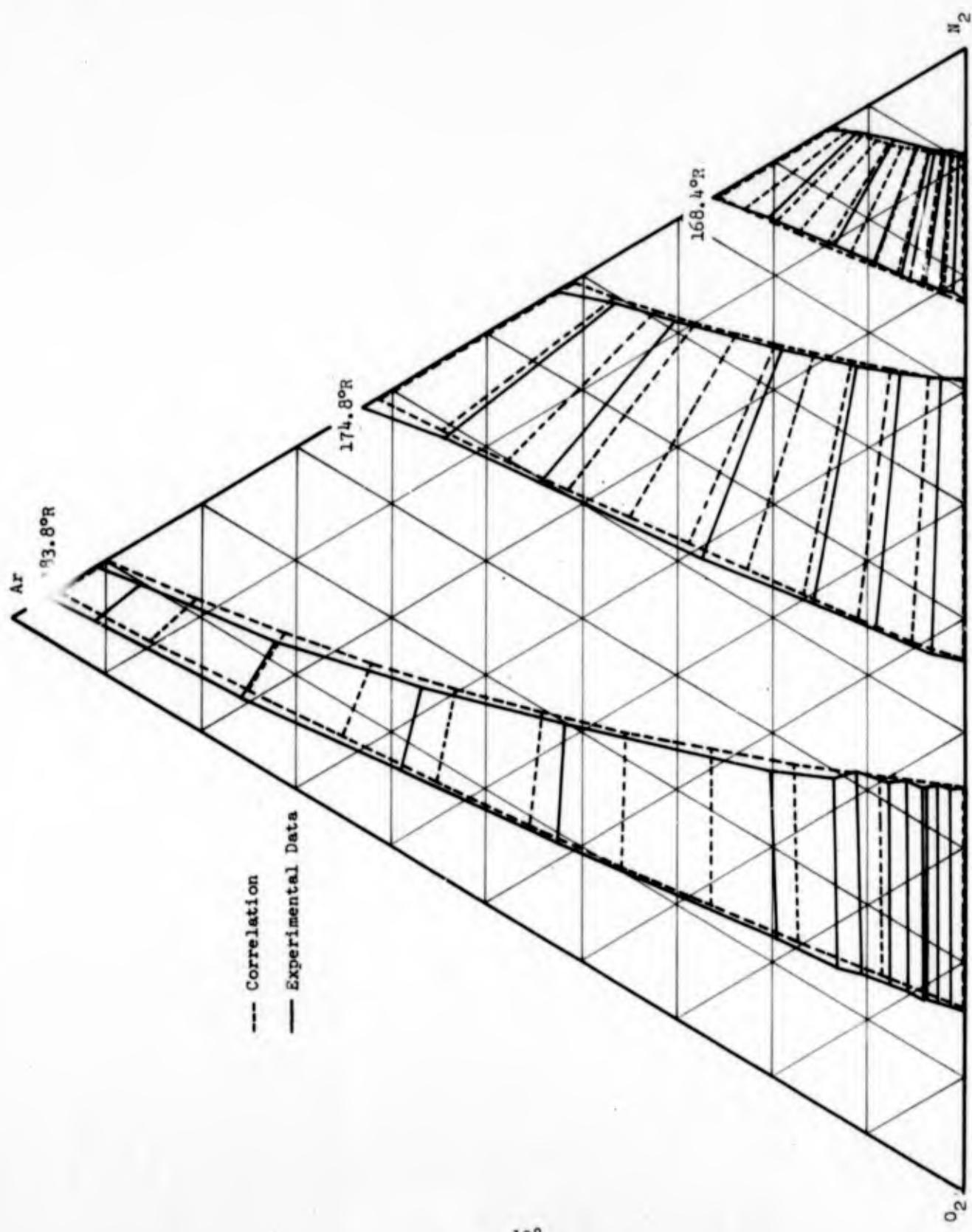


Figure 54. Comparison of Experimental Data and the Correlation, 4 Atmospheres.

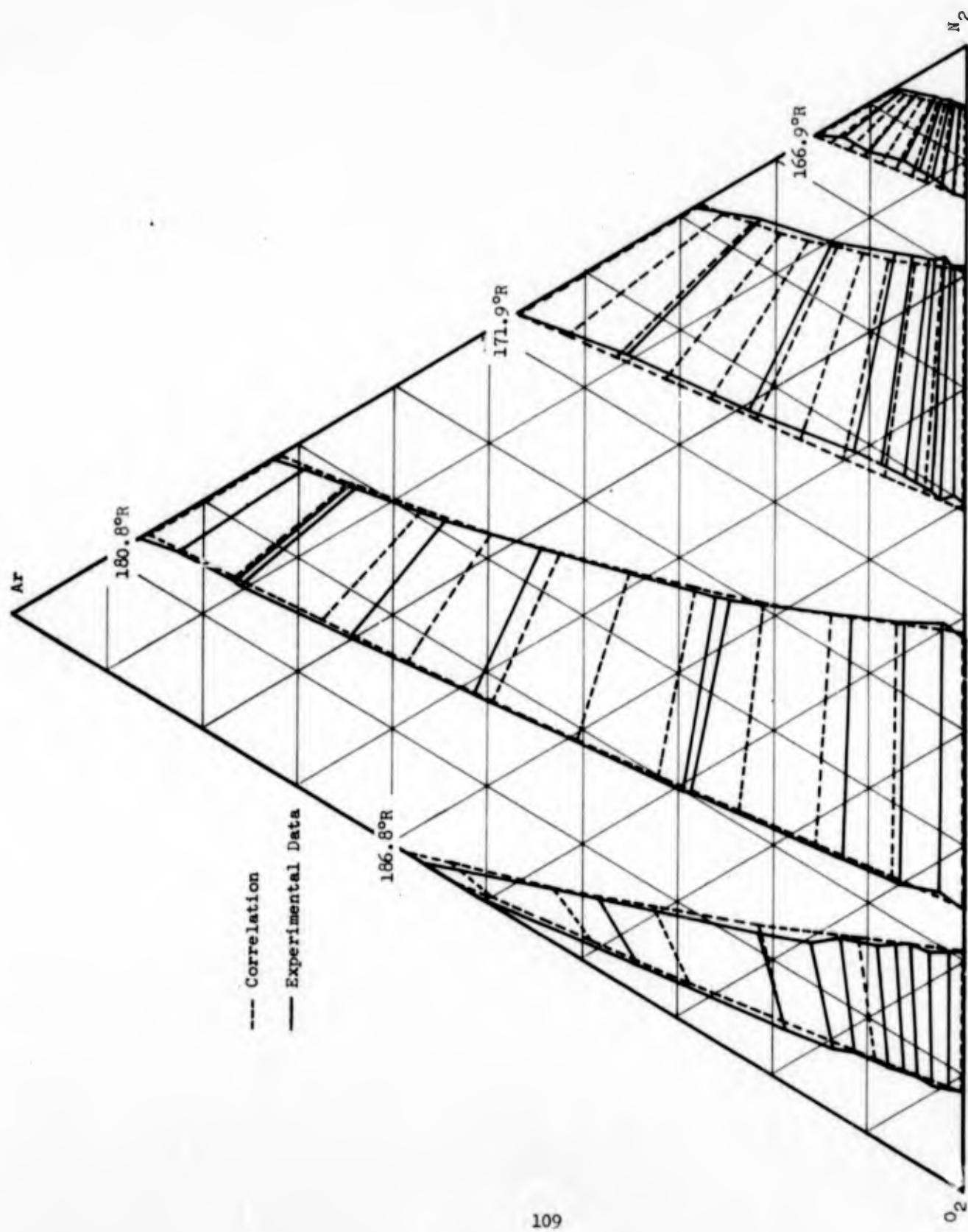


Figure 55. Comparison of Experimental Data and the Correlation, 4 Atmospheres.

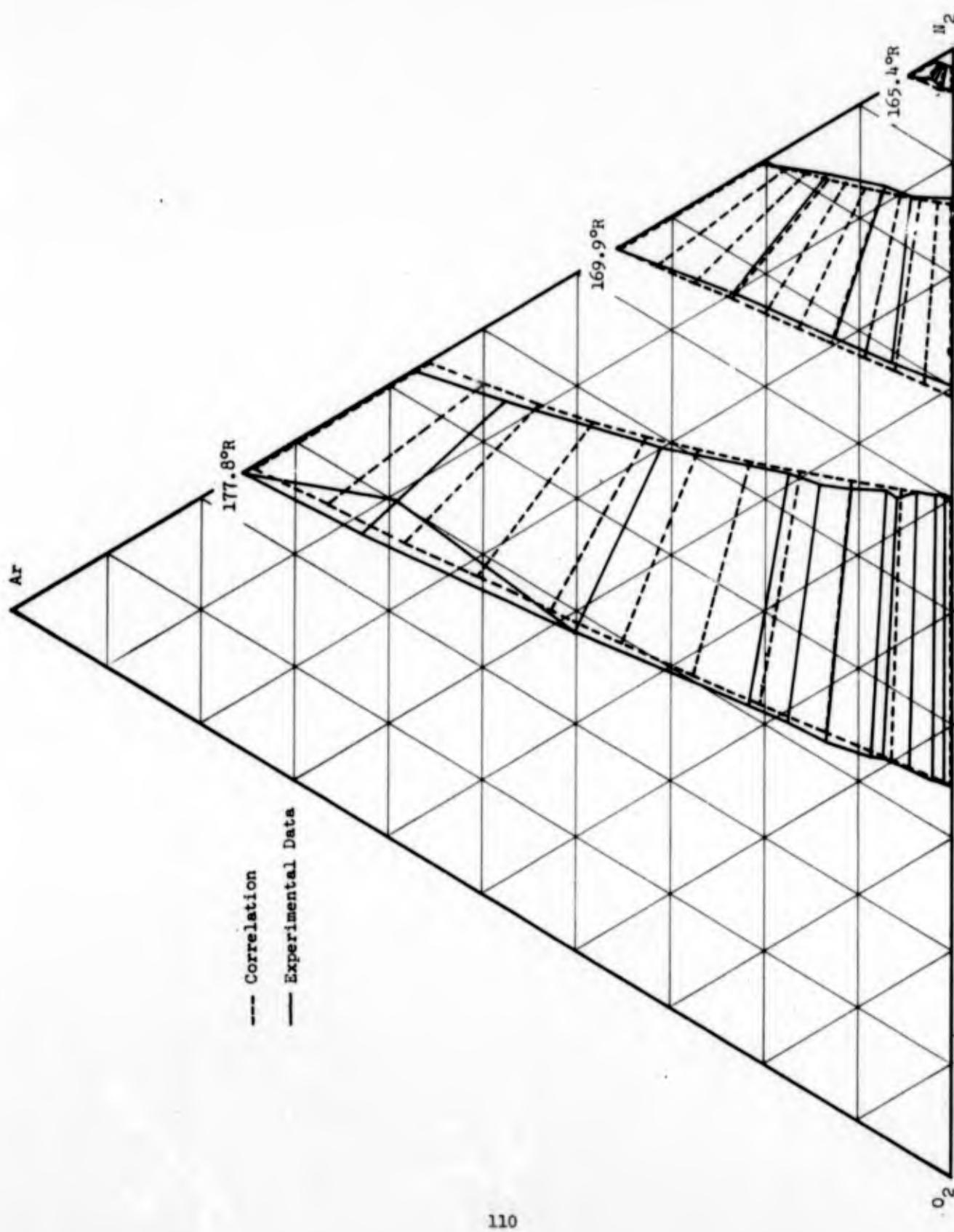


Figure 56. Comparison of Experimental Data and the Correlation, 4 Atmospheres.

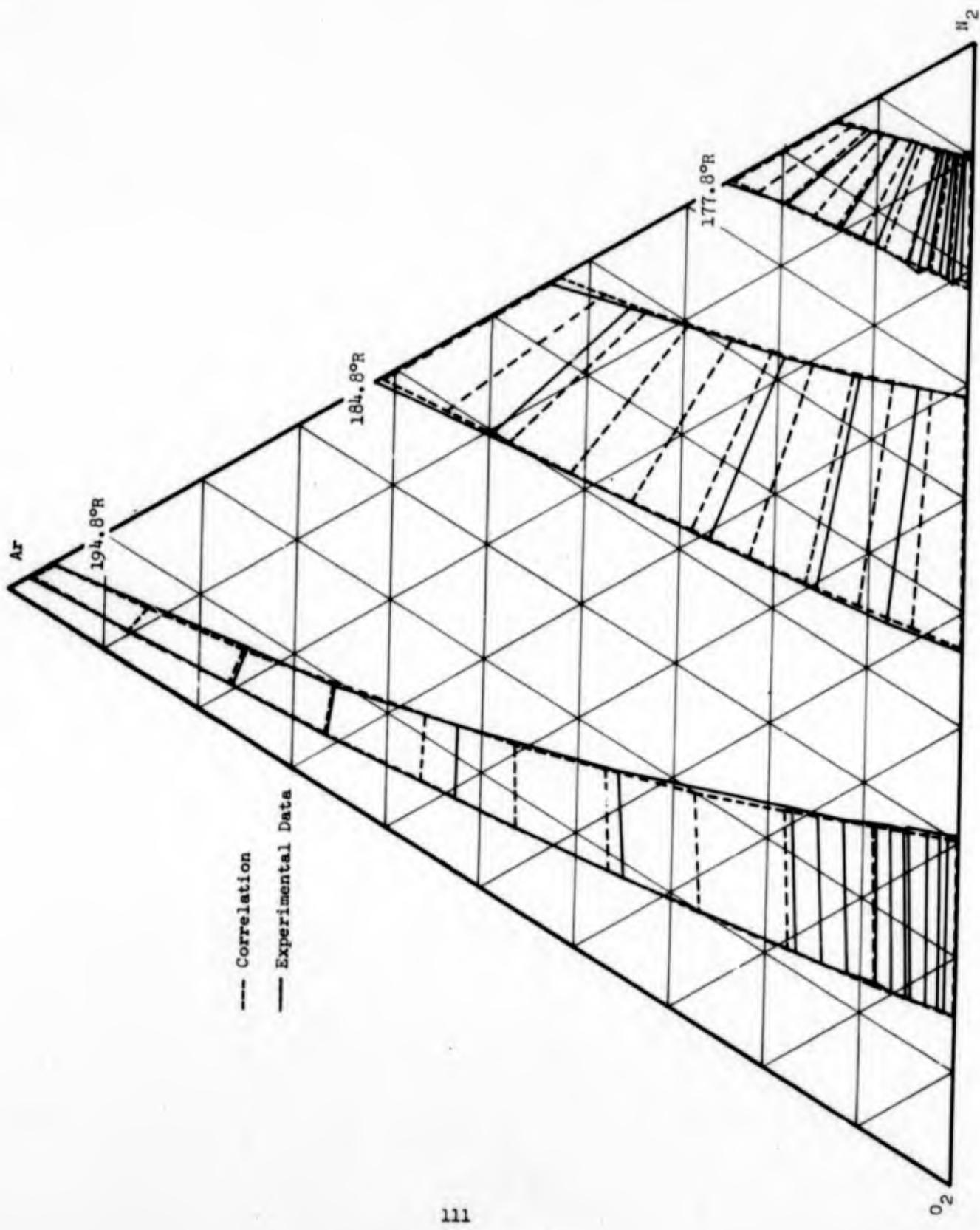


Figure 57. Comparison of Experimental Data and the Correlation, 6 Atmospheres.

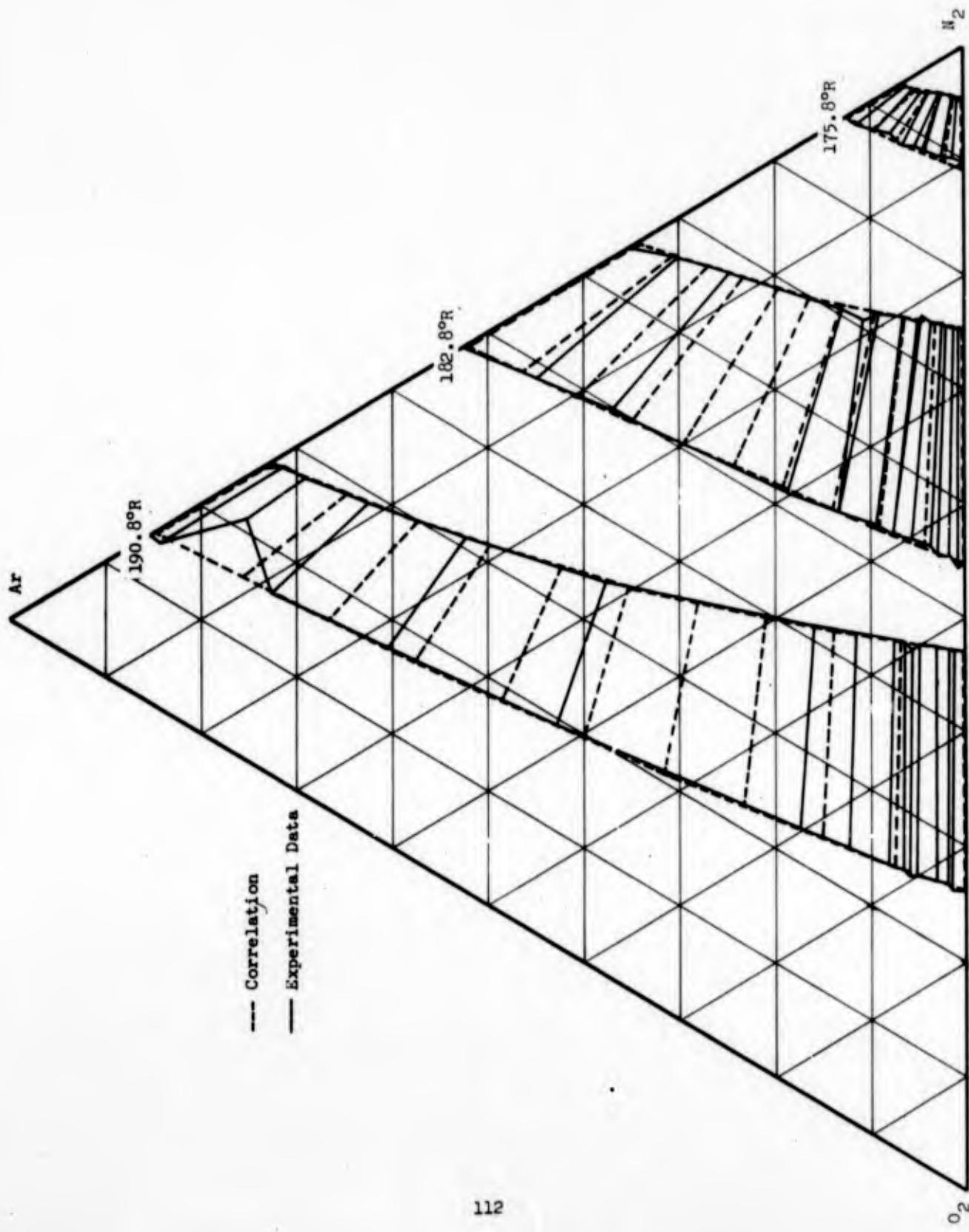


Figure 58. Comparison of Experimental Data and the Correlation, 6 Atmospheres.

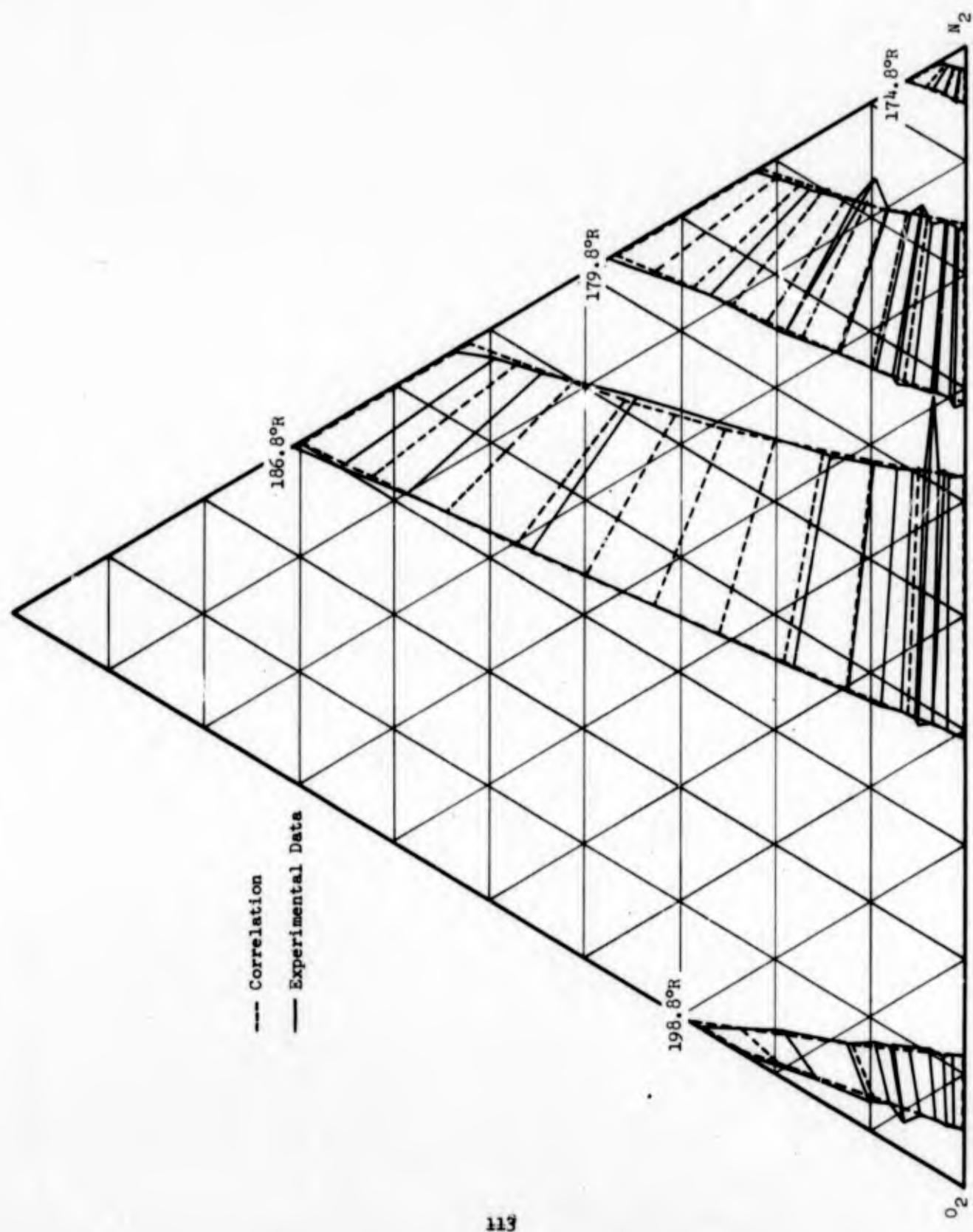


Figure 59. Comparison of Experimental Data and the Correlation, 6 Atmospheres.

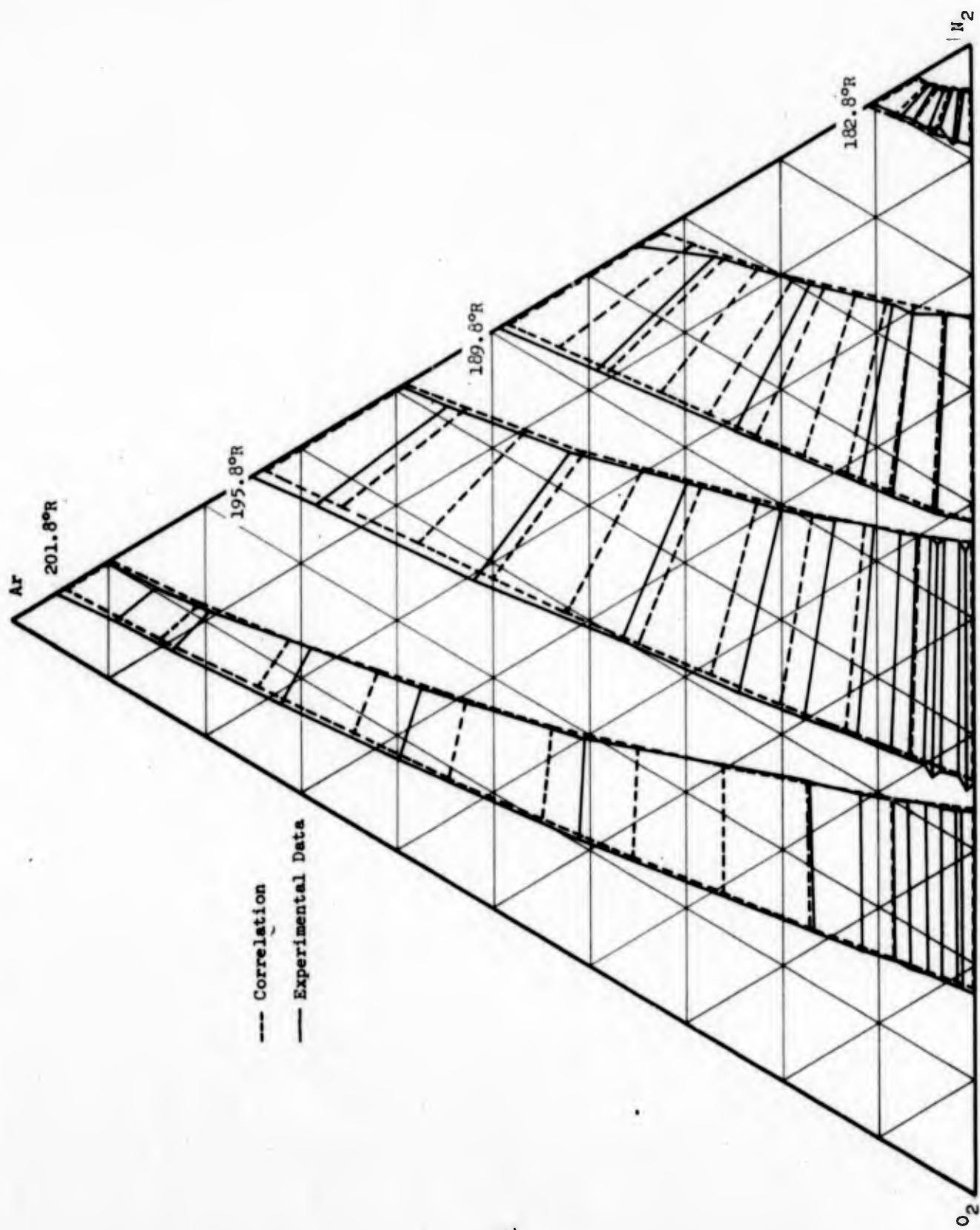


Figure 60. Comparison of Experimental Data and the Correlation, 8 Atmospheres.

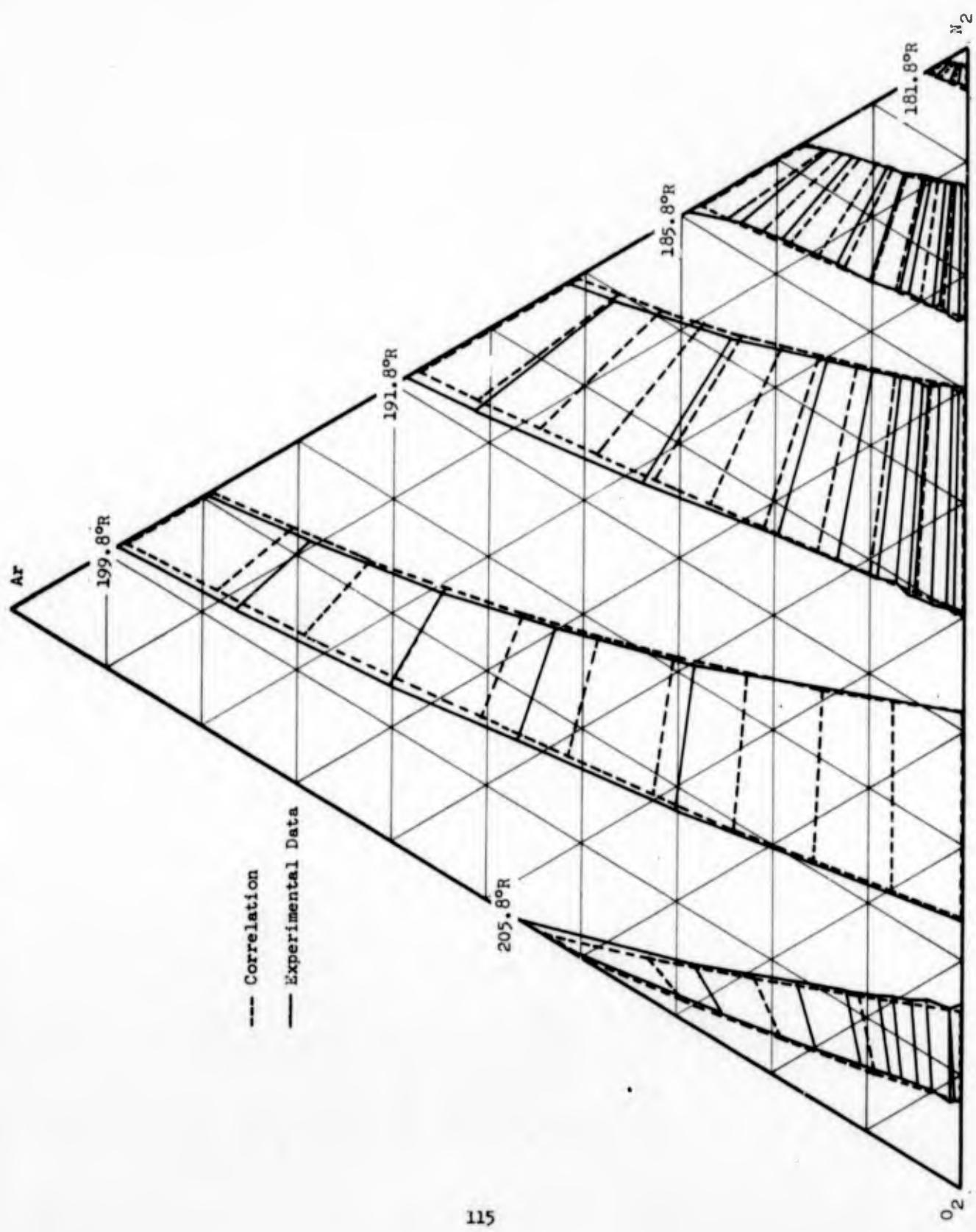


Figure 61. Comparison of Experimental Data and the Correlation, 8 Atmospheres.

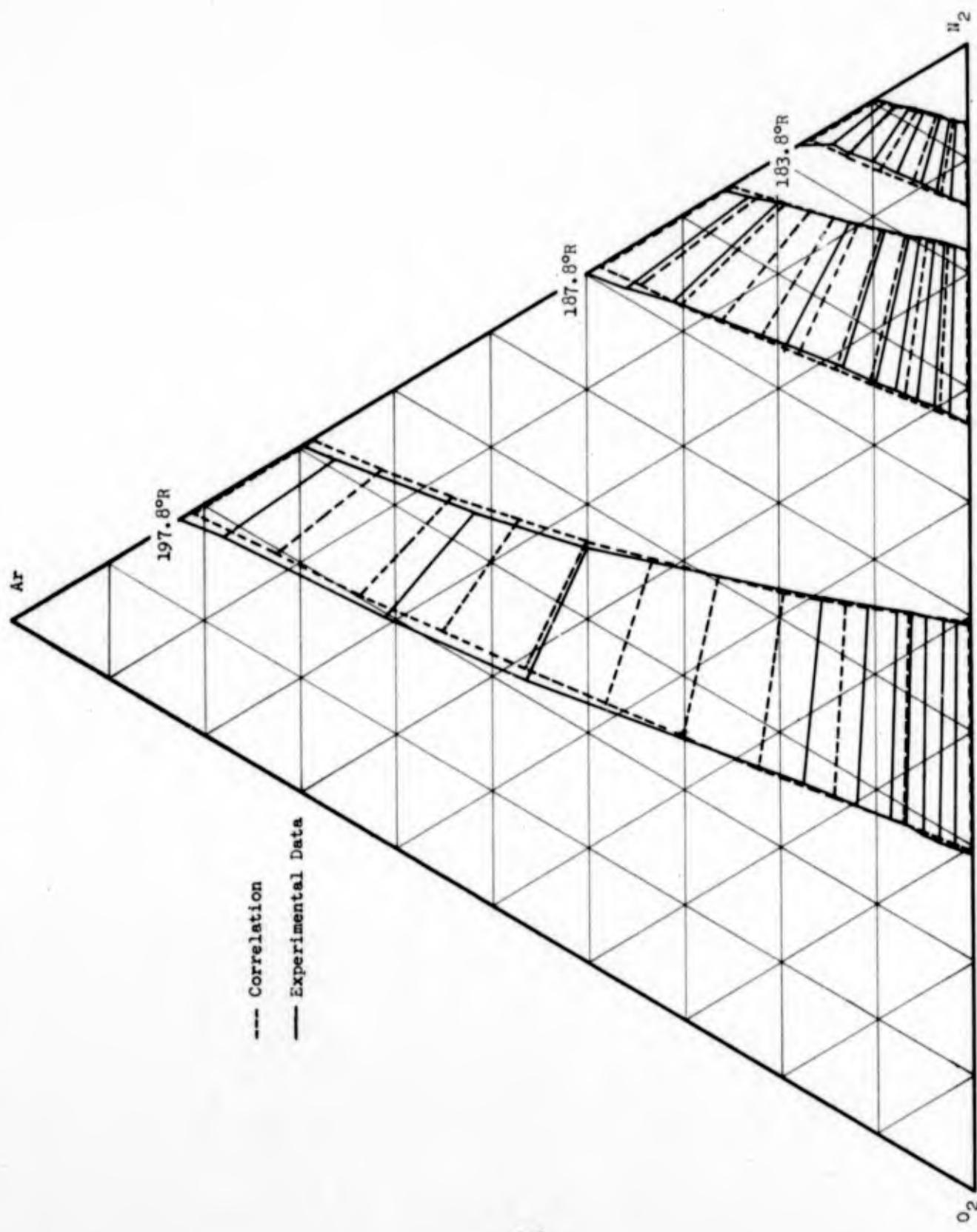


Figure 62. Comparison of Experimental Data and the Correlation, 8 Atmospheres.

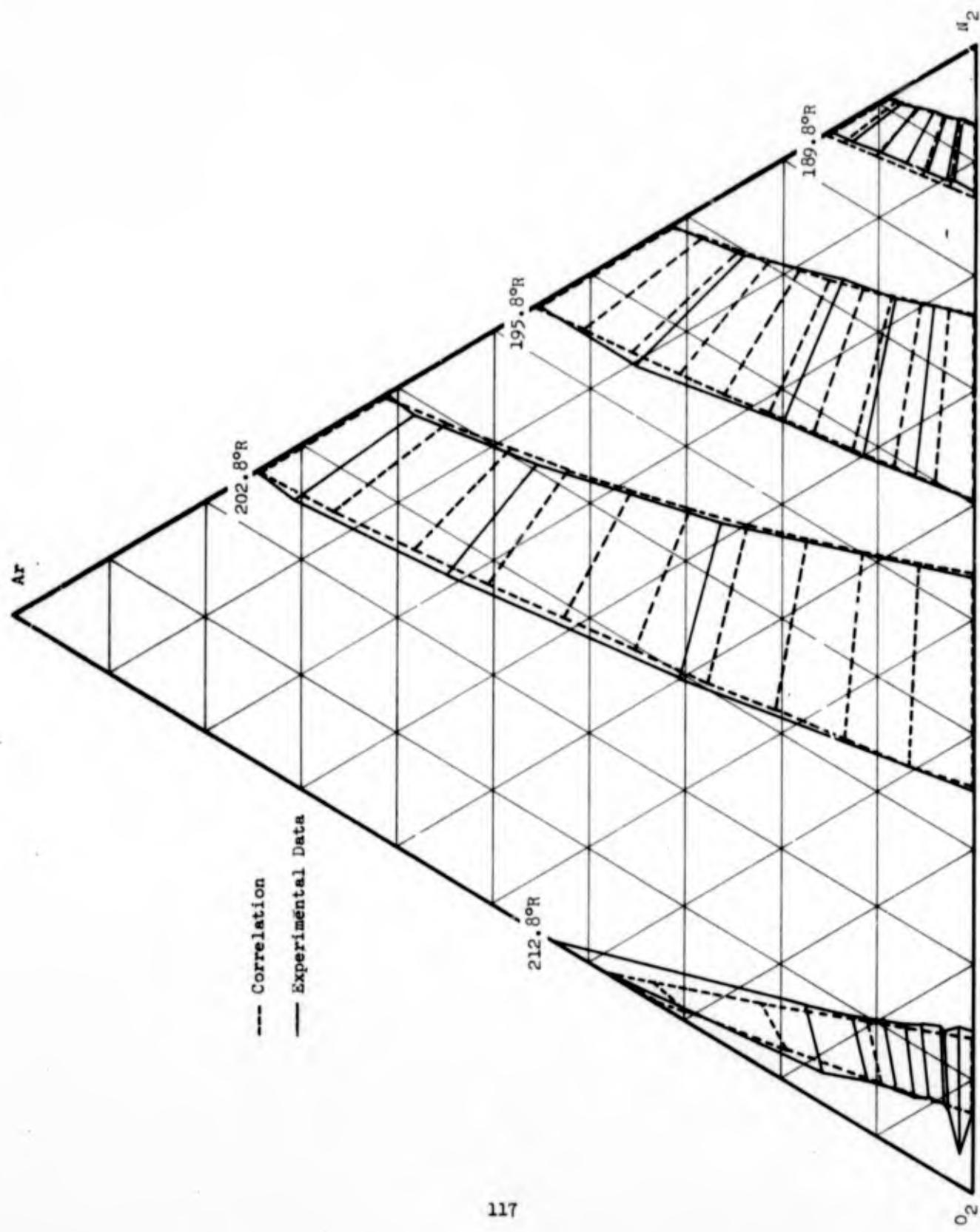


Figure 63. Comparison of Experimental Data and the Correlation, 10 Atmospheres.

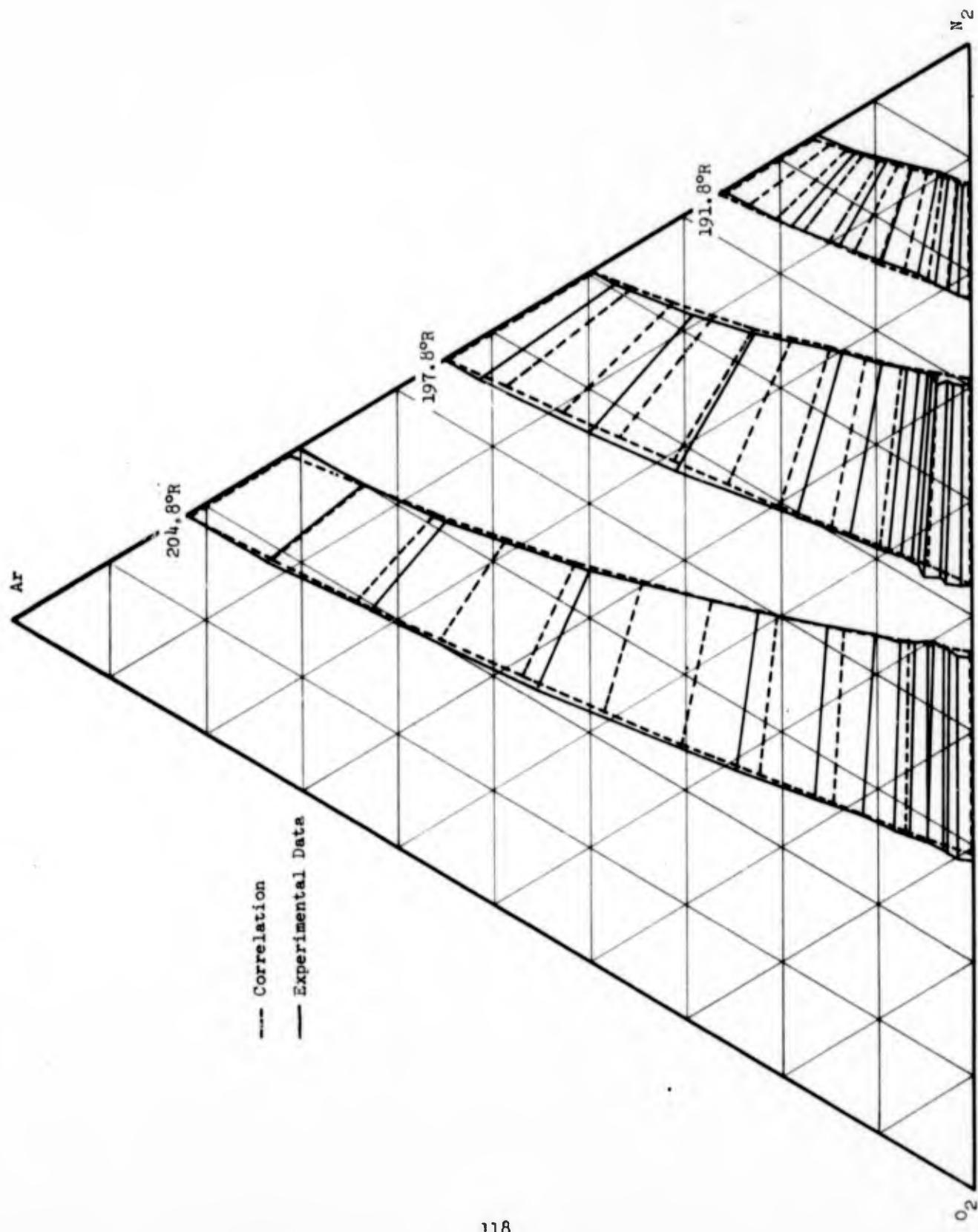


Figure 64. Comparison of Experimental Data and the Correlation, 10 Atmospheres.

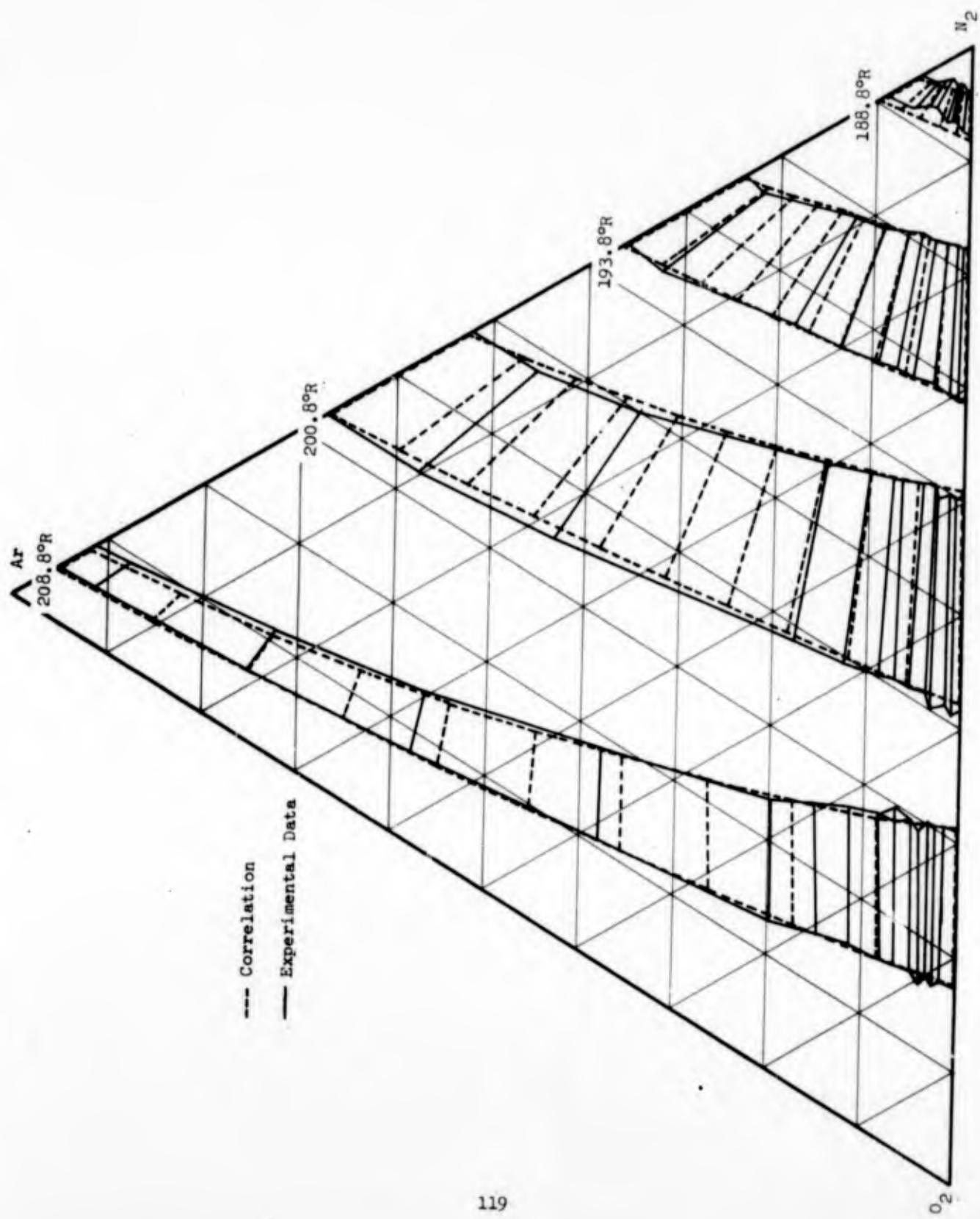


Figure 65. Comparison of Experimental Data and the Correlation, 10 Atmospheres.

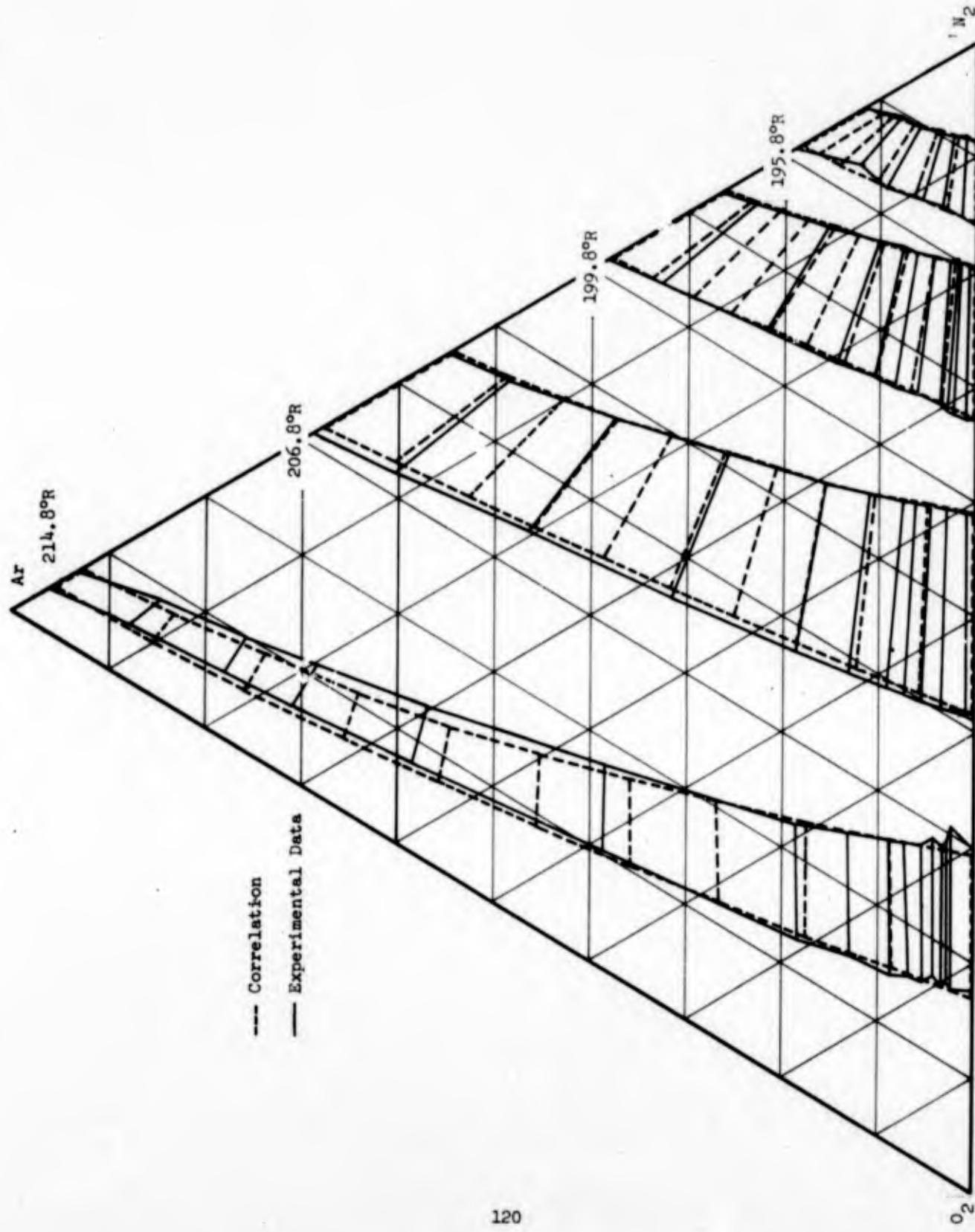


Figure 66. Comparison of Experimental Data and the Correlation, 12 Atmospheres.

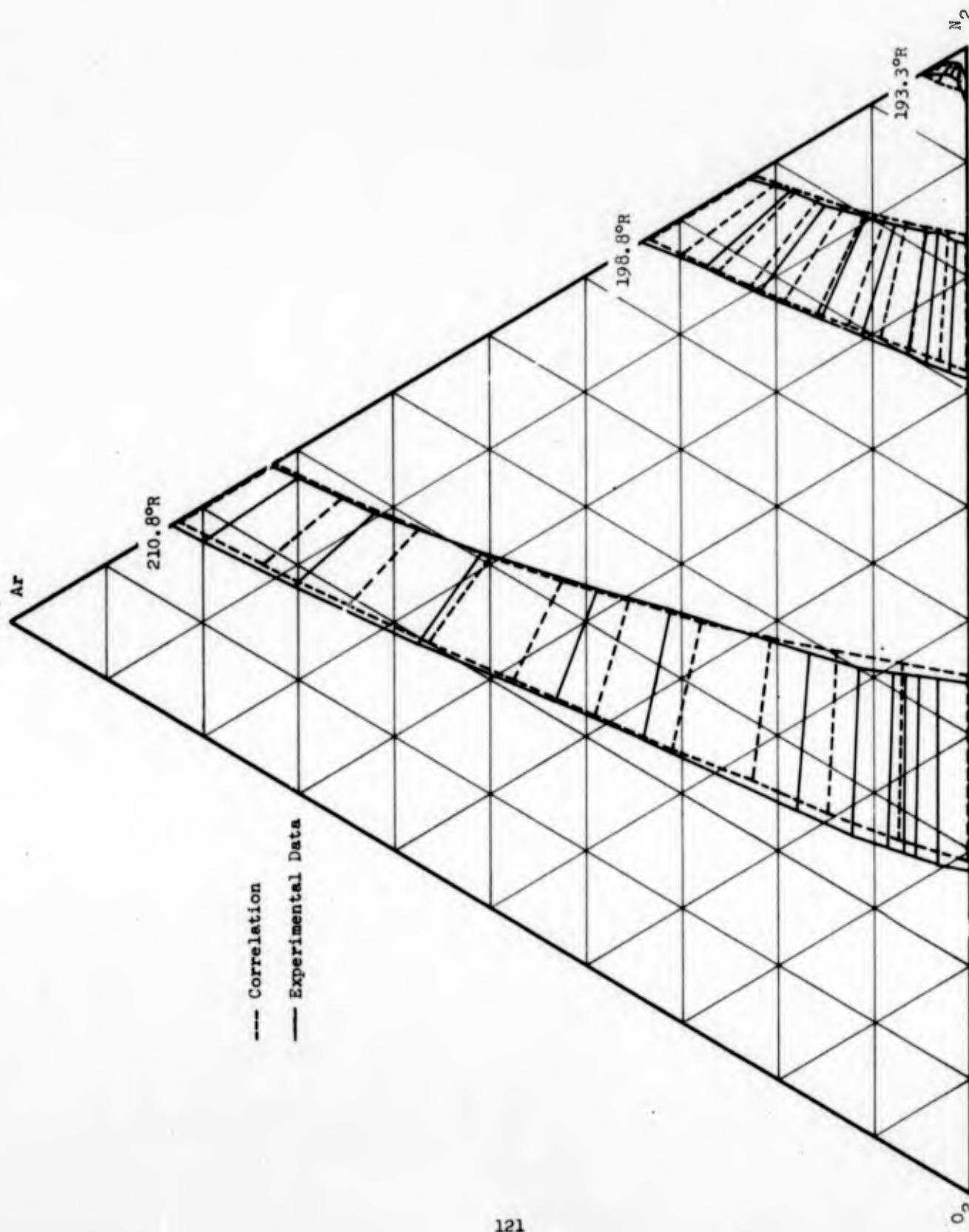


Figure 67. Comparison of Experimental Data and the Correlation, 12 Atmospheres.

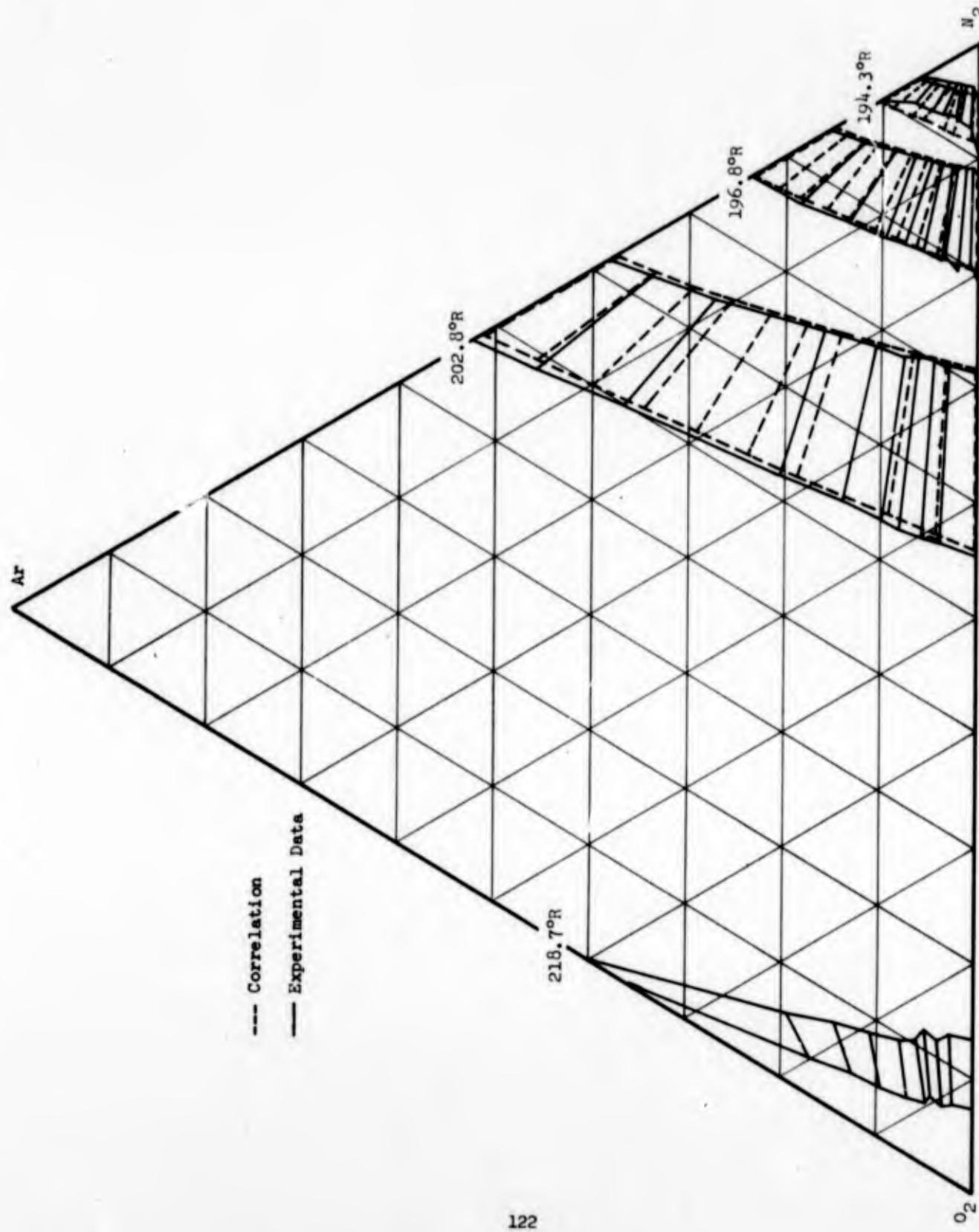


Figure 68. Comparison of Experimental Data and the Correlation, 12 Atmospheres.

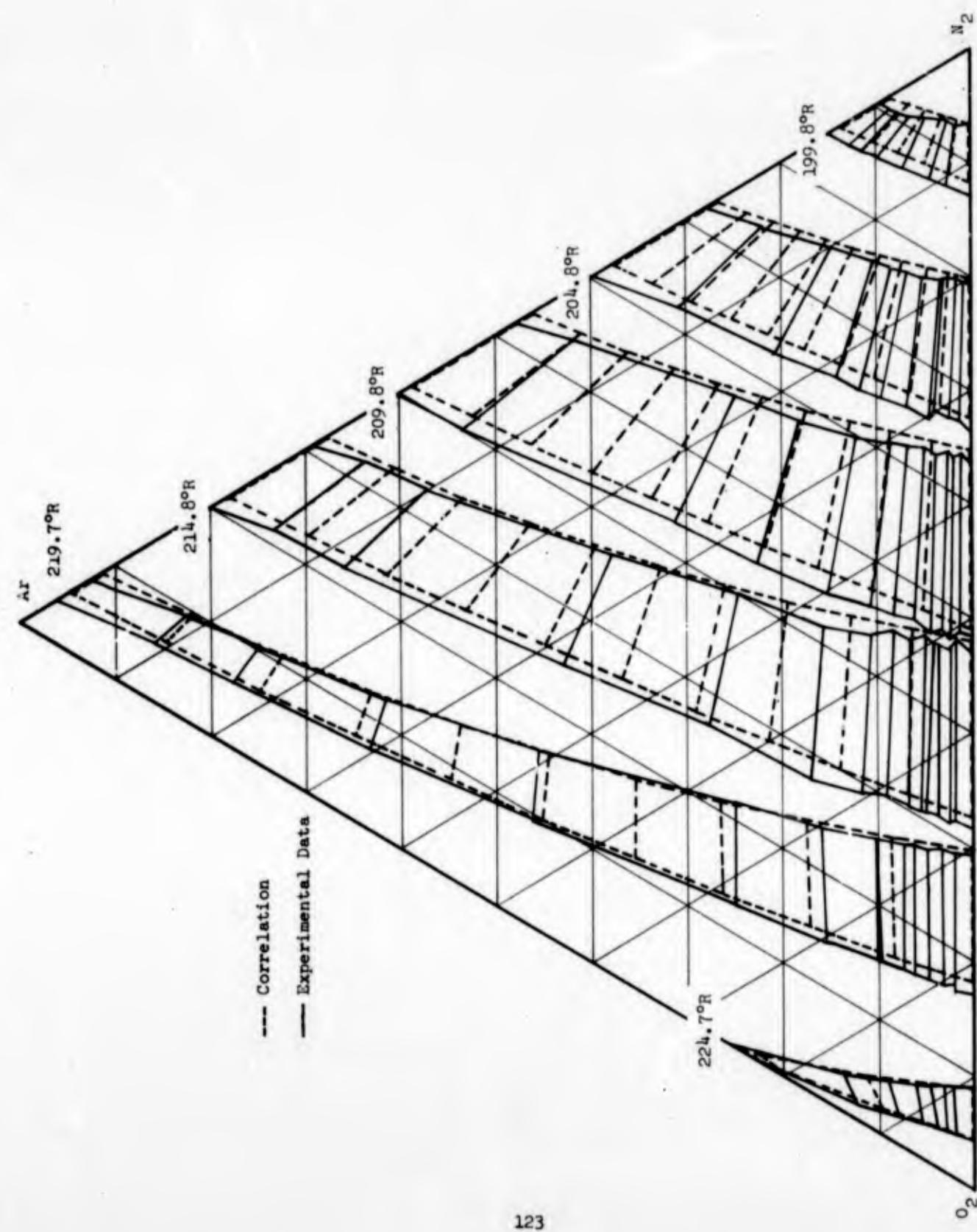


Figure 69. Comparison of Experimental Data and the Correlation, 14 Atmospheres.

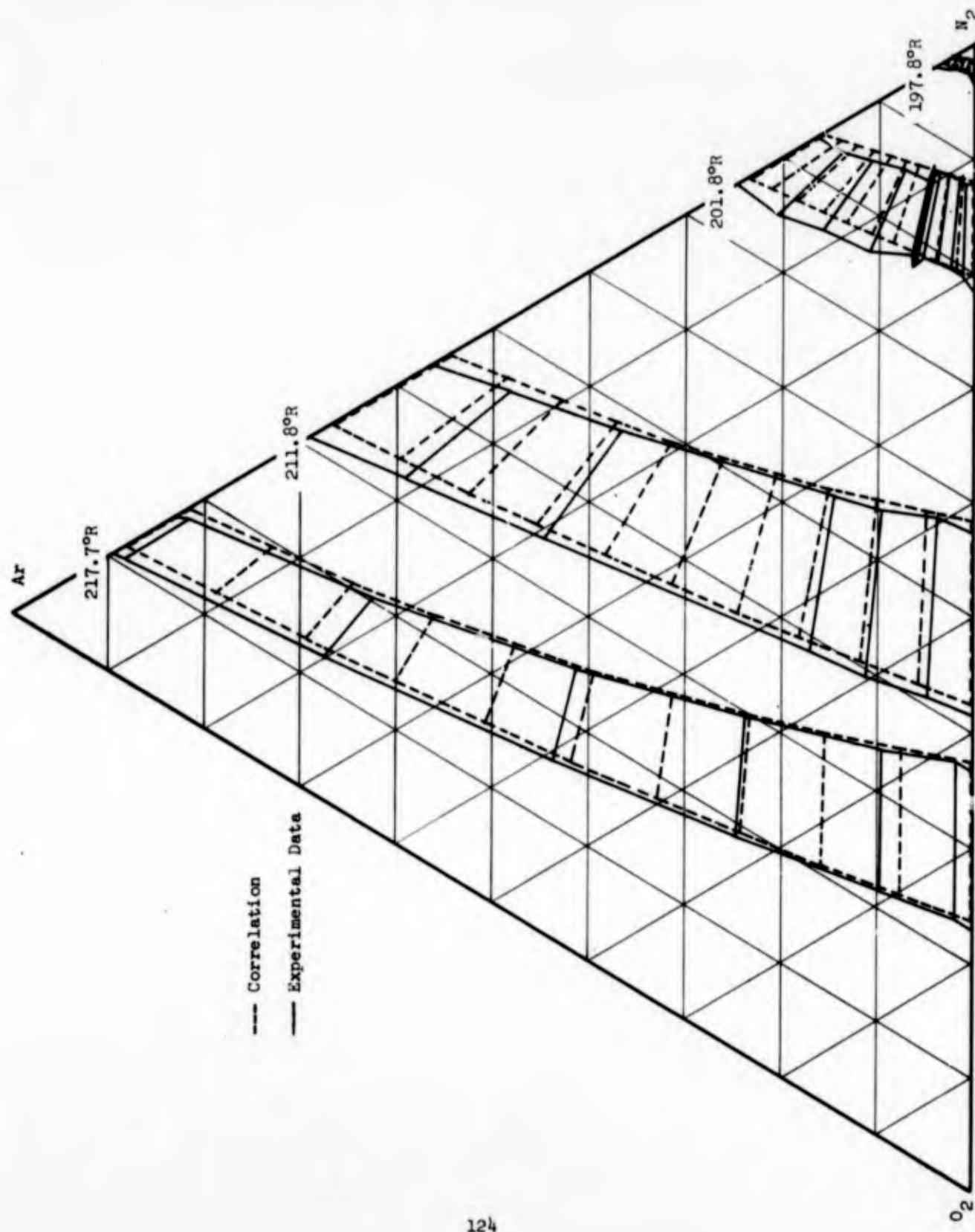


Figure 70. Comparison of Experimental Data and the Correlation, 14 Atmospheres.

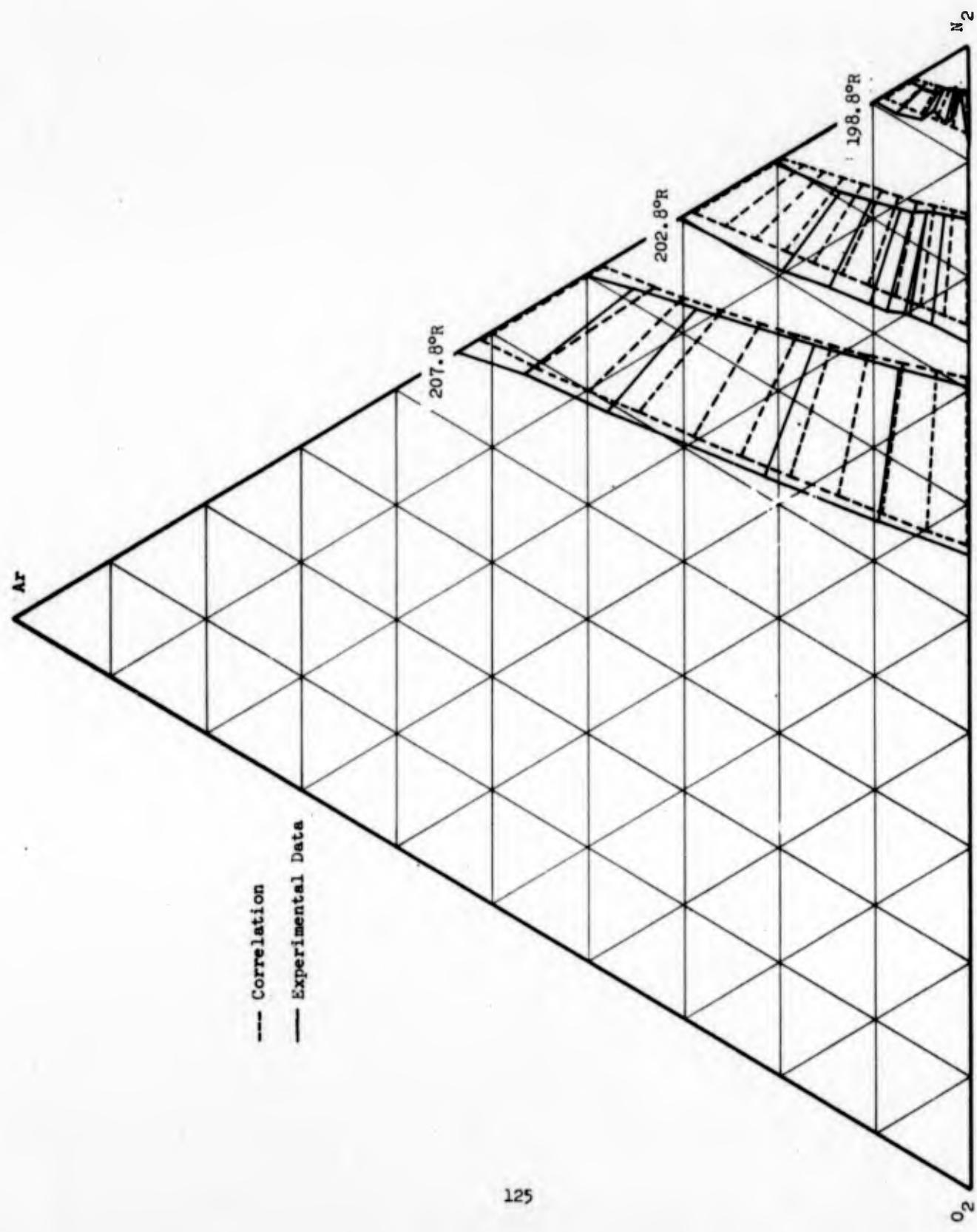


Figure 71. Comparison of Experimental Data and the Correlation, $14 \text{ Ar}-\text{N}_2$.

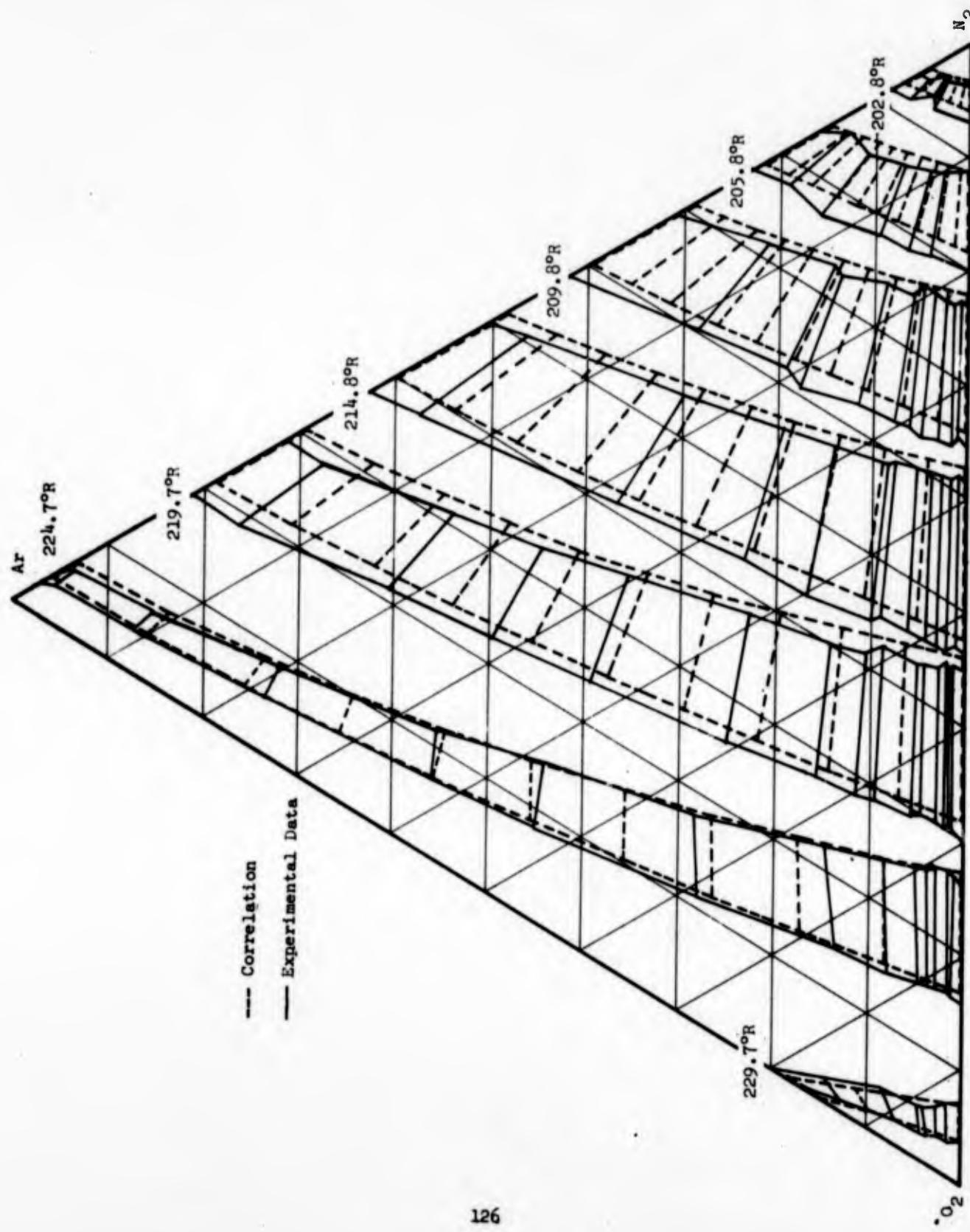


Figure 72. Comparison of Experimental Data and the Correlation, 16 Atmospheres.

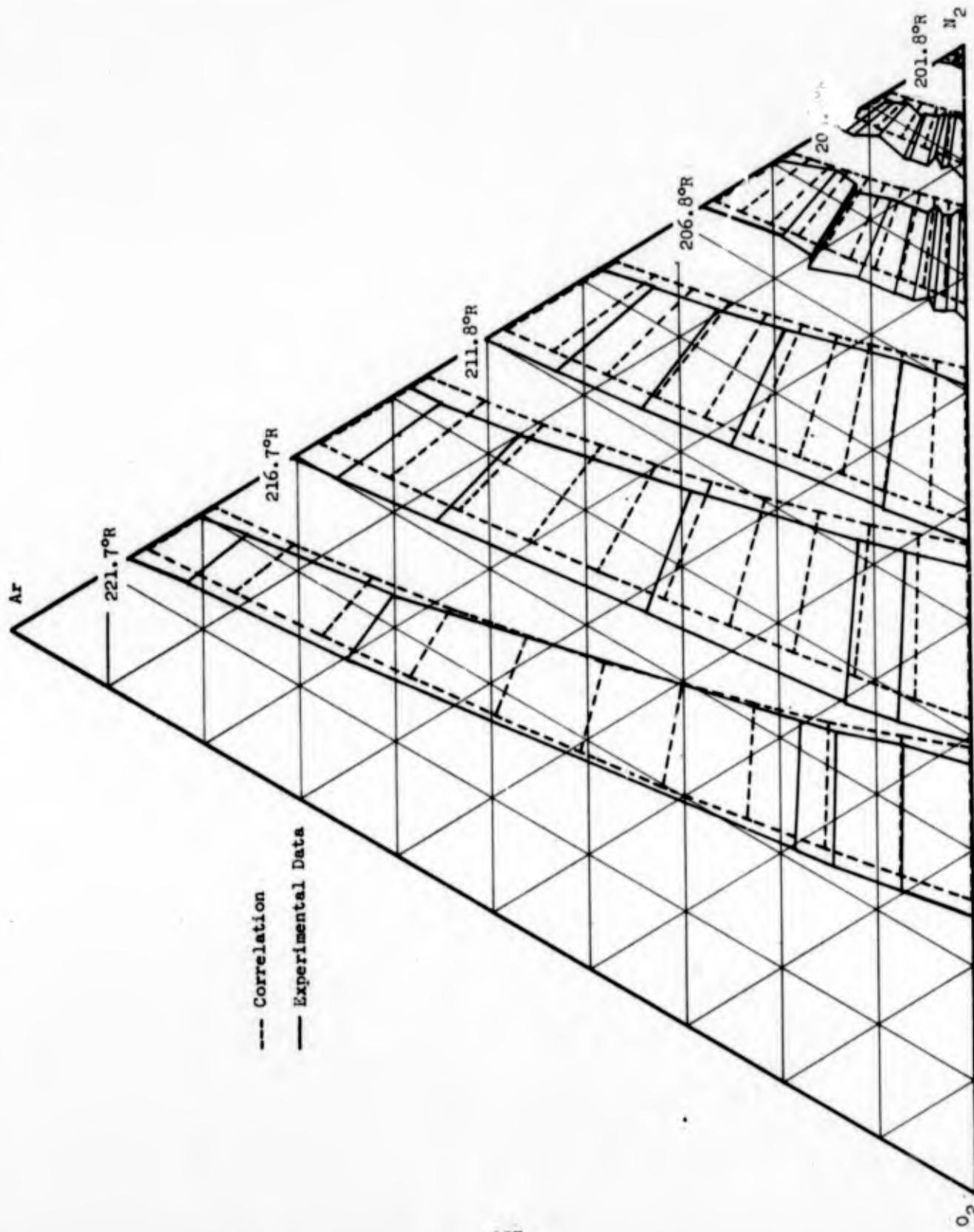


Figure 73. Comparison of Experimental Data and the Correlation, 16 Atmospheres.

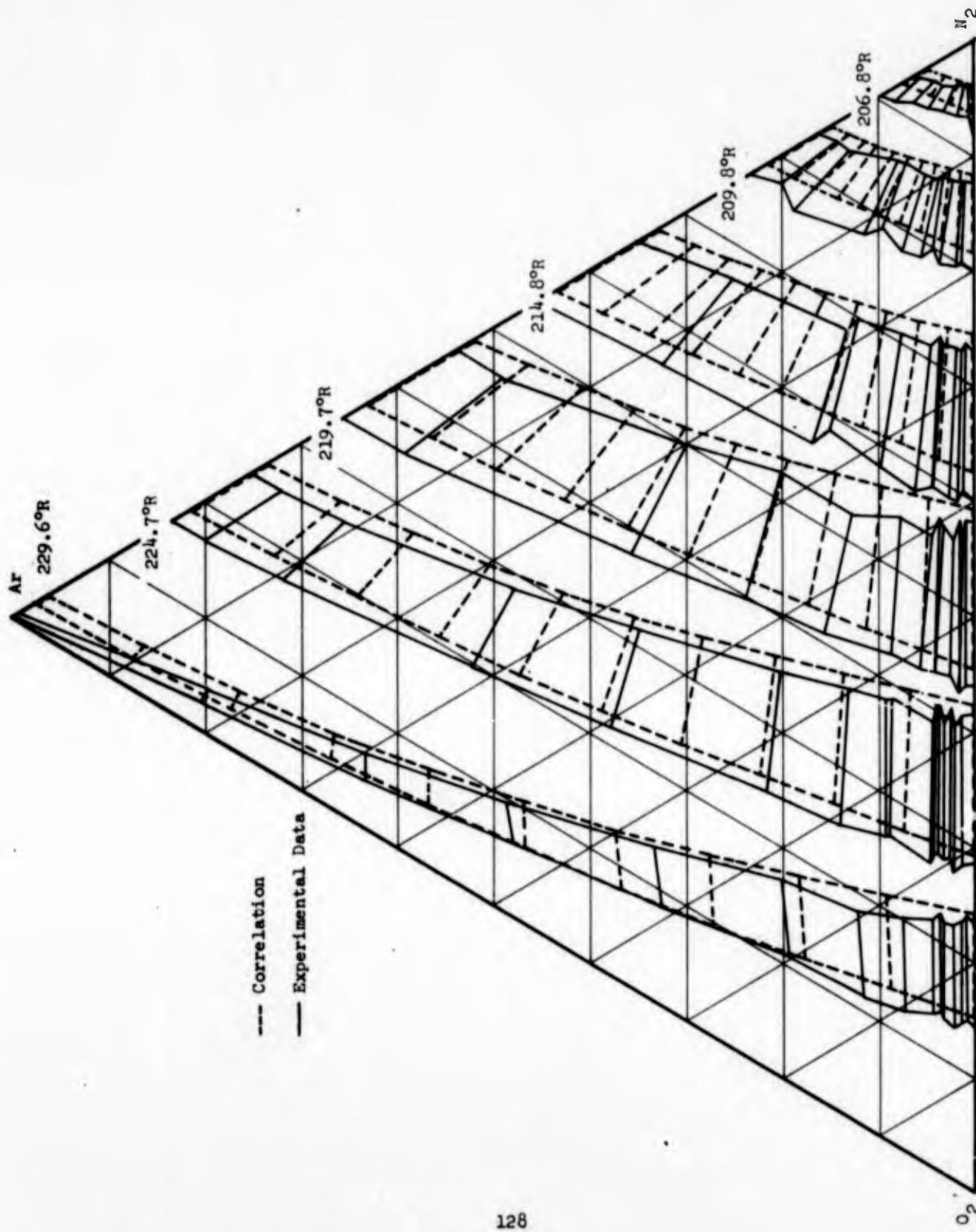


Figure 74. Comparison of Experimental Data and the Correlation, 18 Atmospheres.

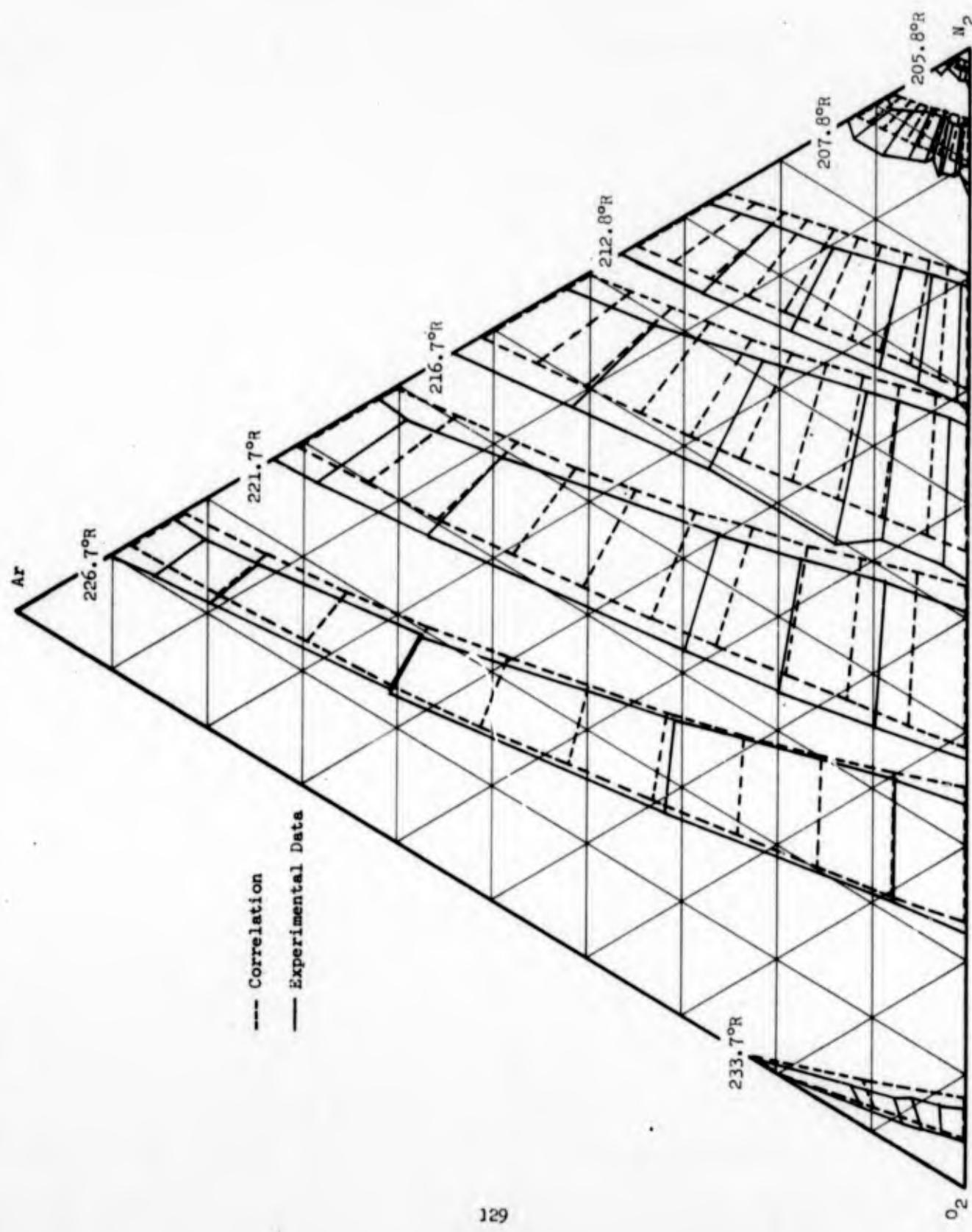


Figure 75. Comparison of Experimental Data and the Correlation, 18 Atmospheres.

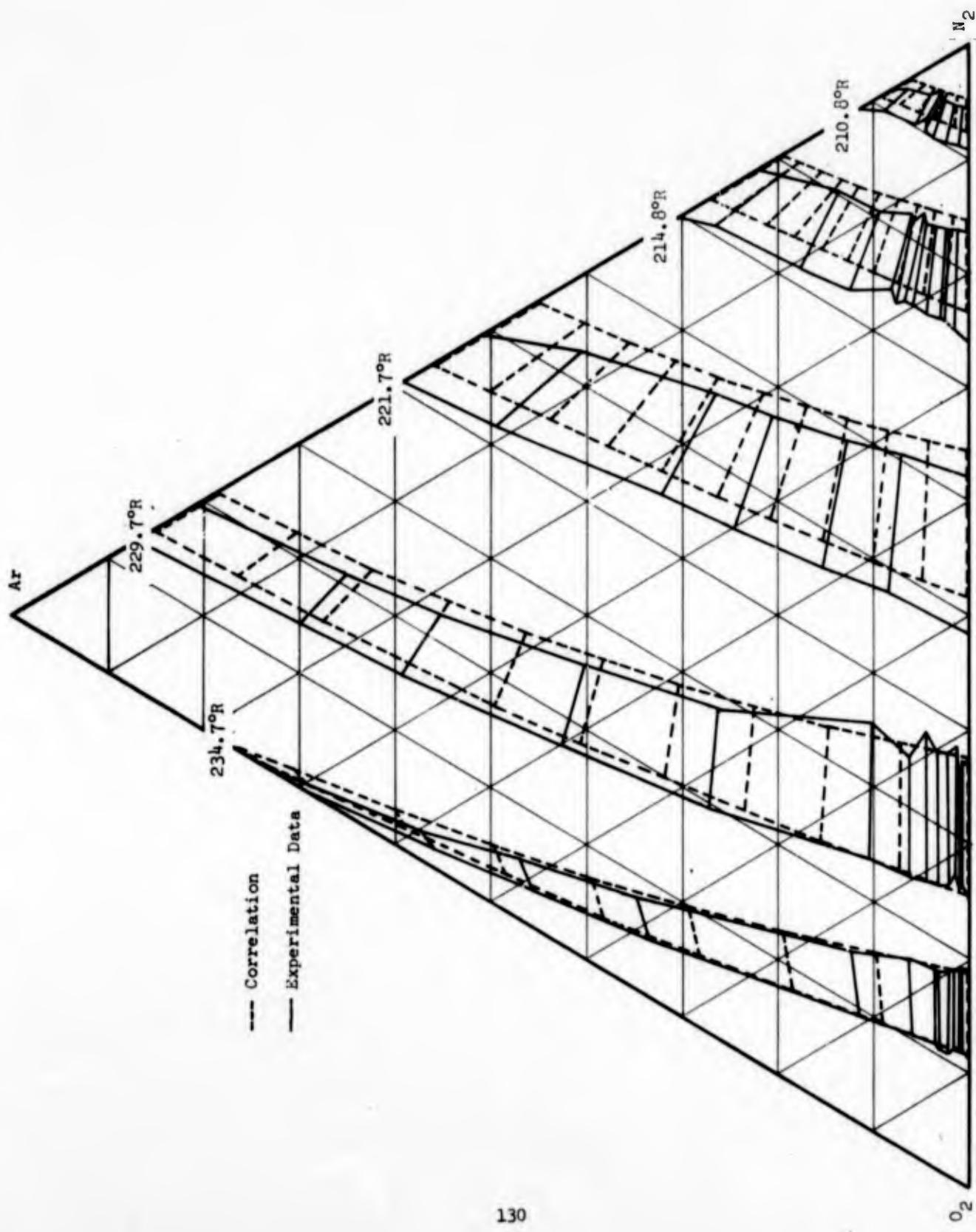


Figure 76. Comparison of Experimental Data and the Correlation, 20 Atmospheres.

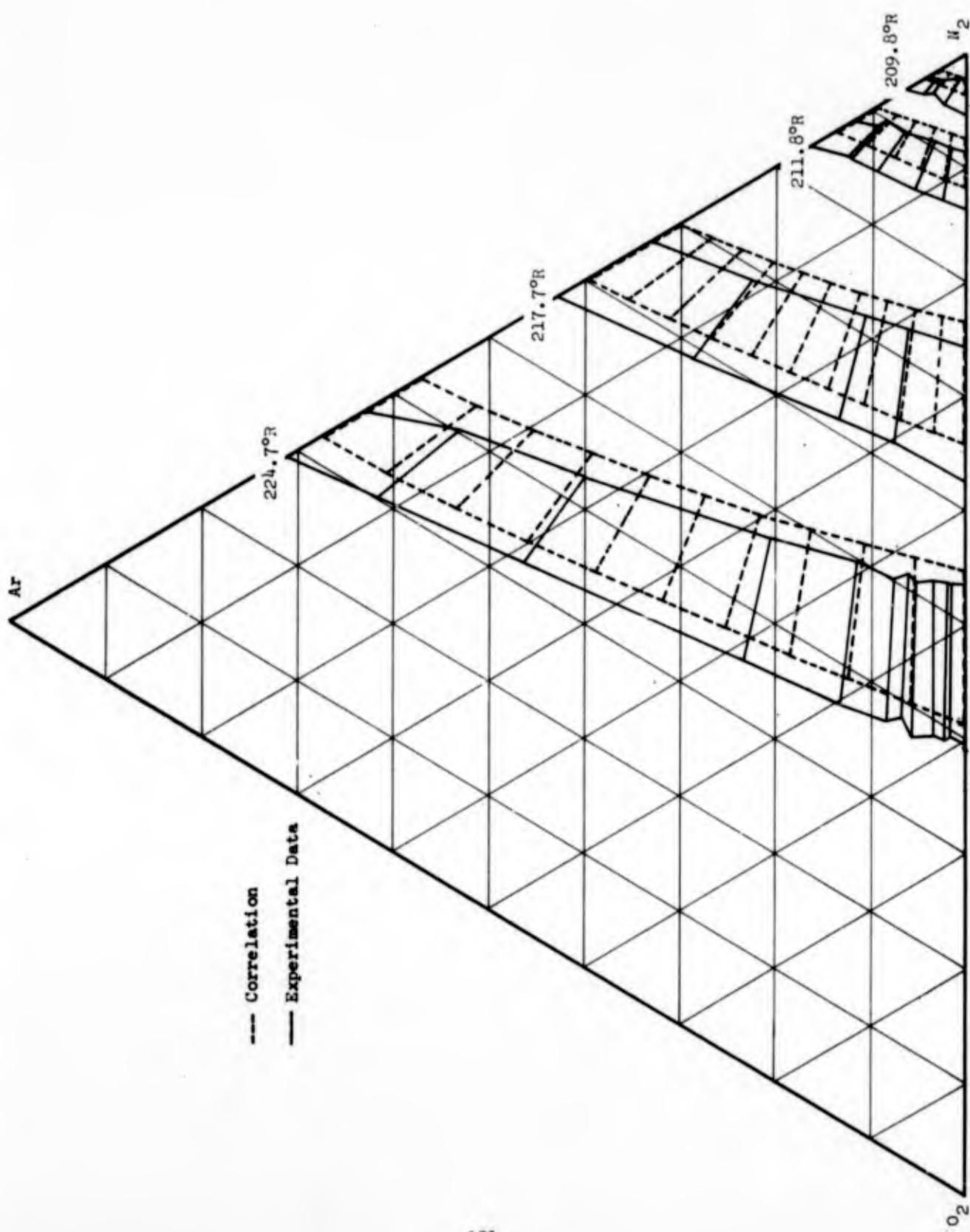


Figure 77. Comparison of Experimental Data and the Correlation, 20 Atmospheres.

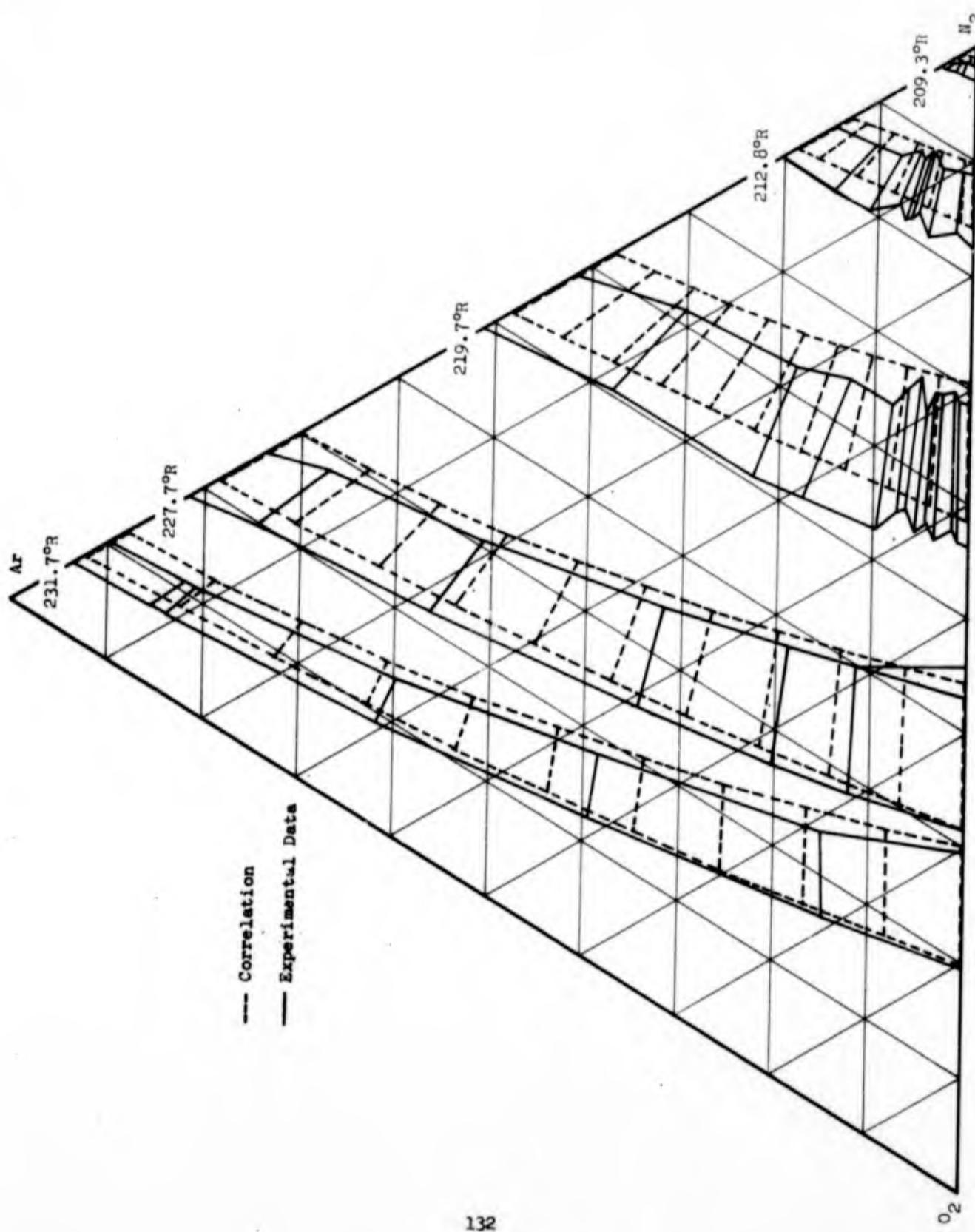


Figure 78. Comparison of Experimental Data and the Correlation, 20 Atmospheres.

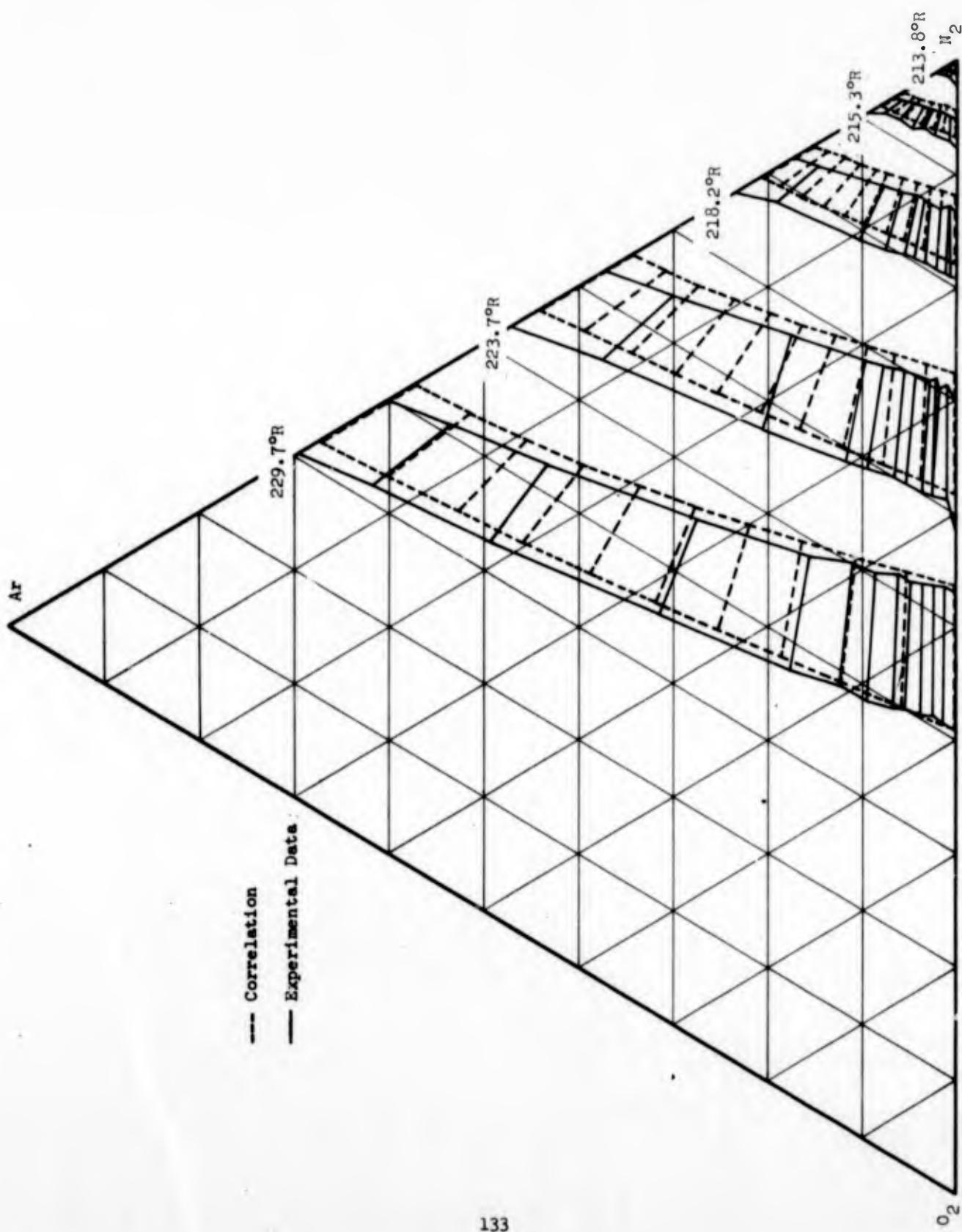


Figure 79. Comparison of Experimental Data and the Correlation, 23 Atmospheres.

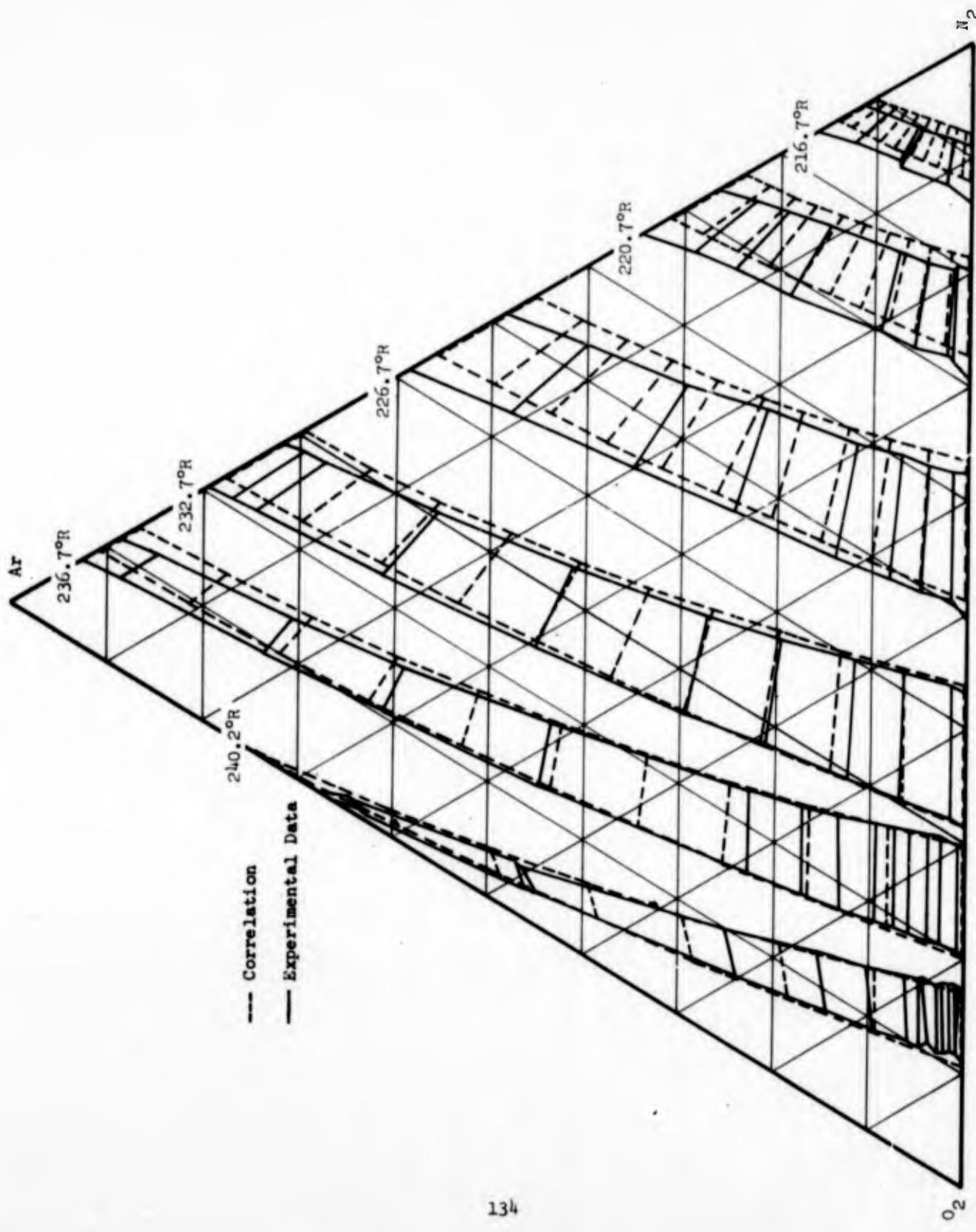


Figure 80. Comparison of Experimental Data and the Correlation, 23 Atmospheres.

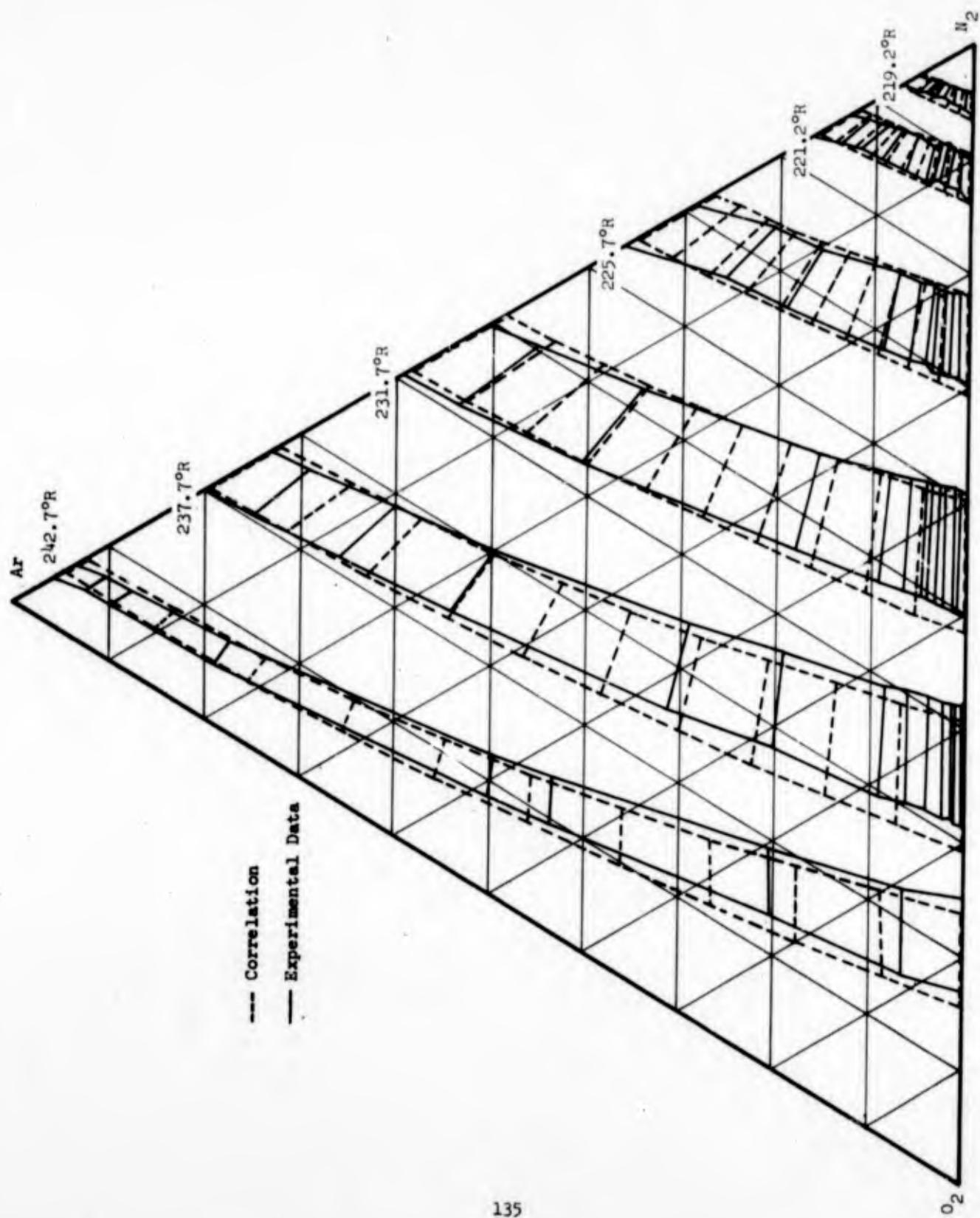


Figure 81. Comparison of Experimental Data and the Correlation, 26 Atmospheres.

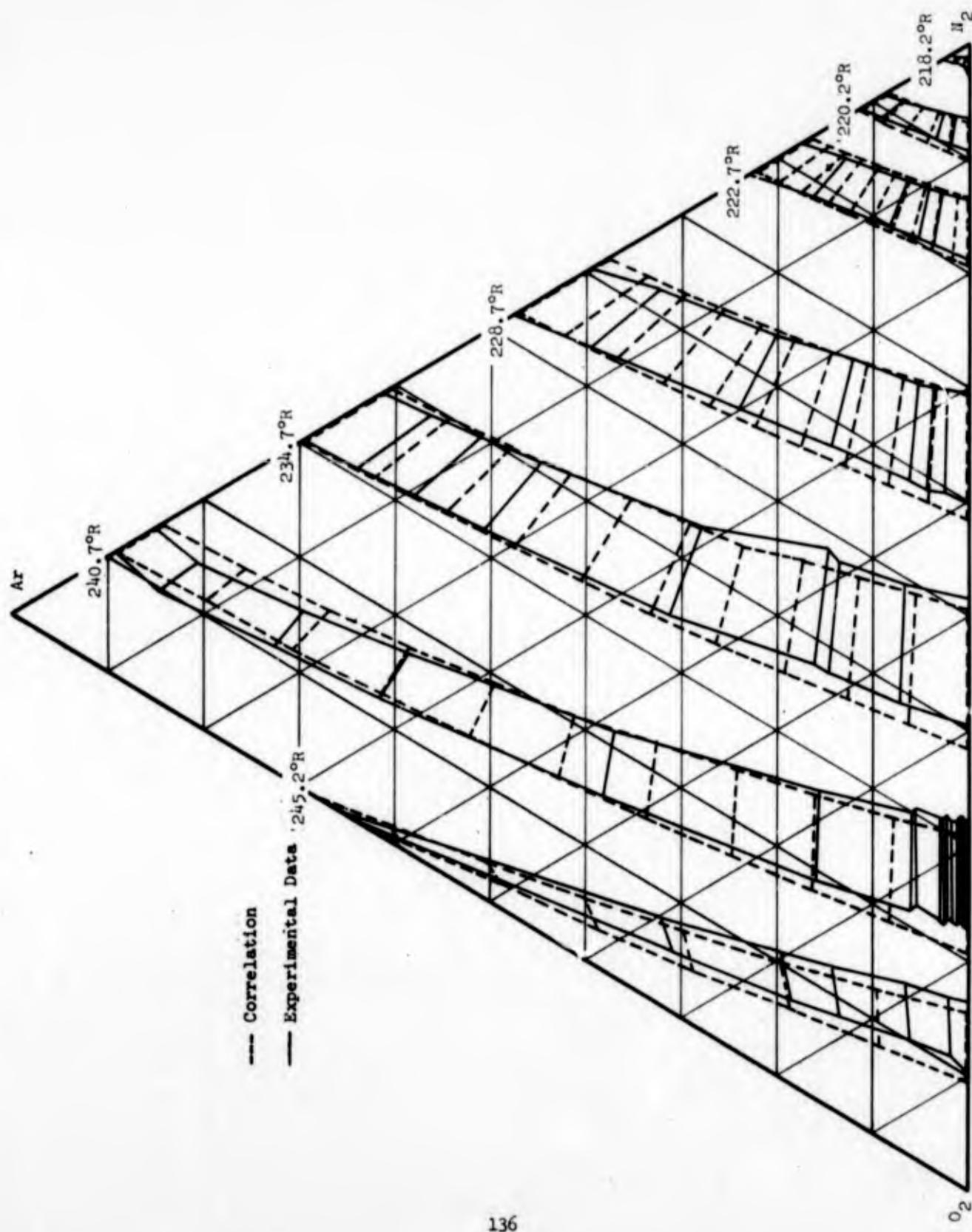


Figure 82. Comparison of Experimental Data and the Correlation, 26 Atmospheres.

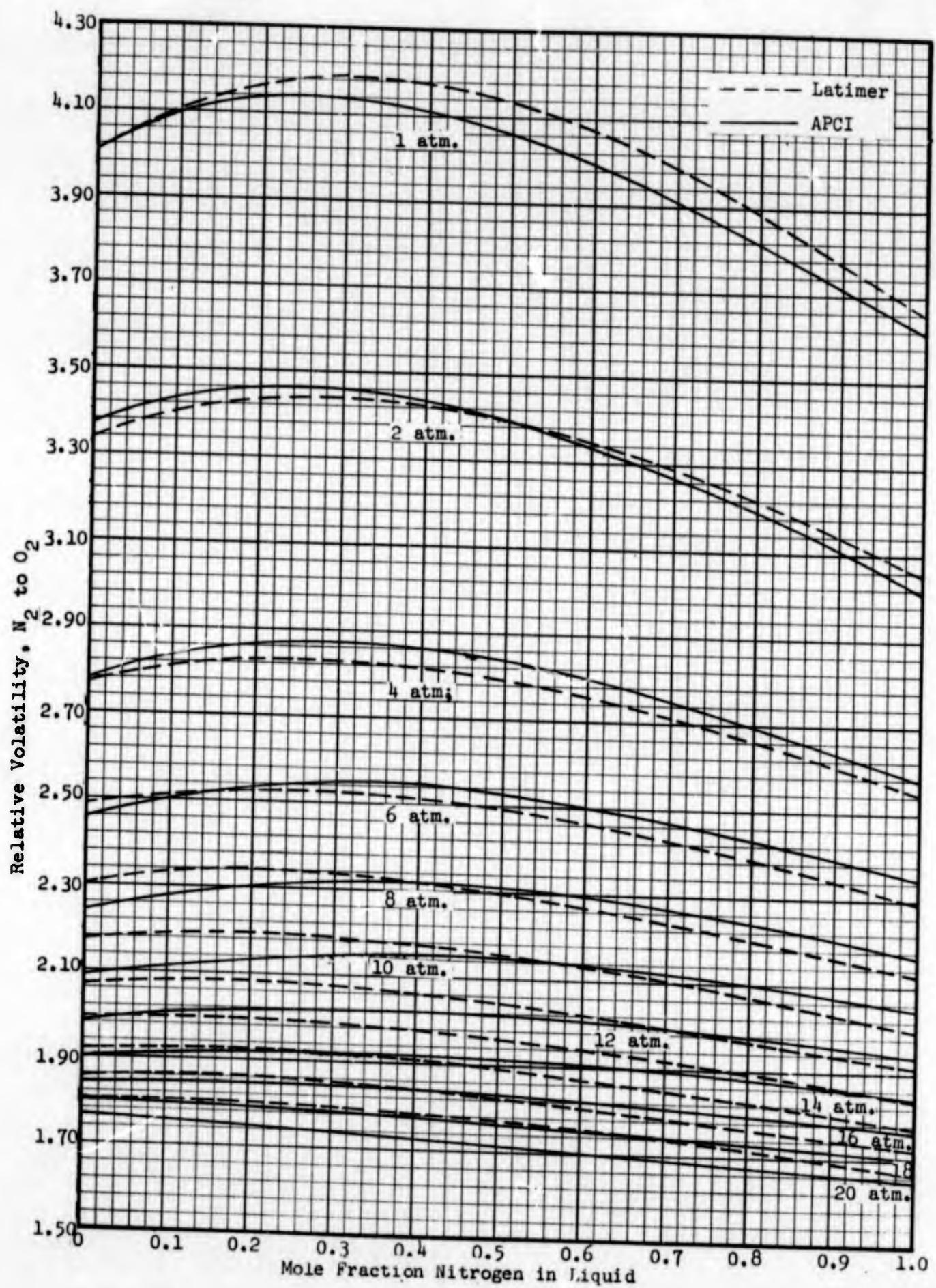


Figure 83. Comparison of APCI Correlation to Latimer Correlation for Nitrogen-Oxygen System.

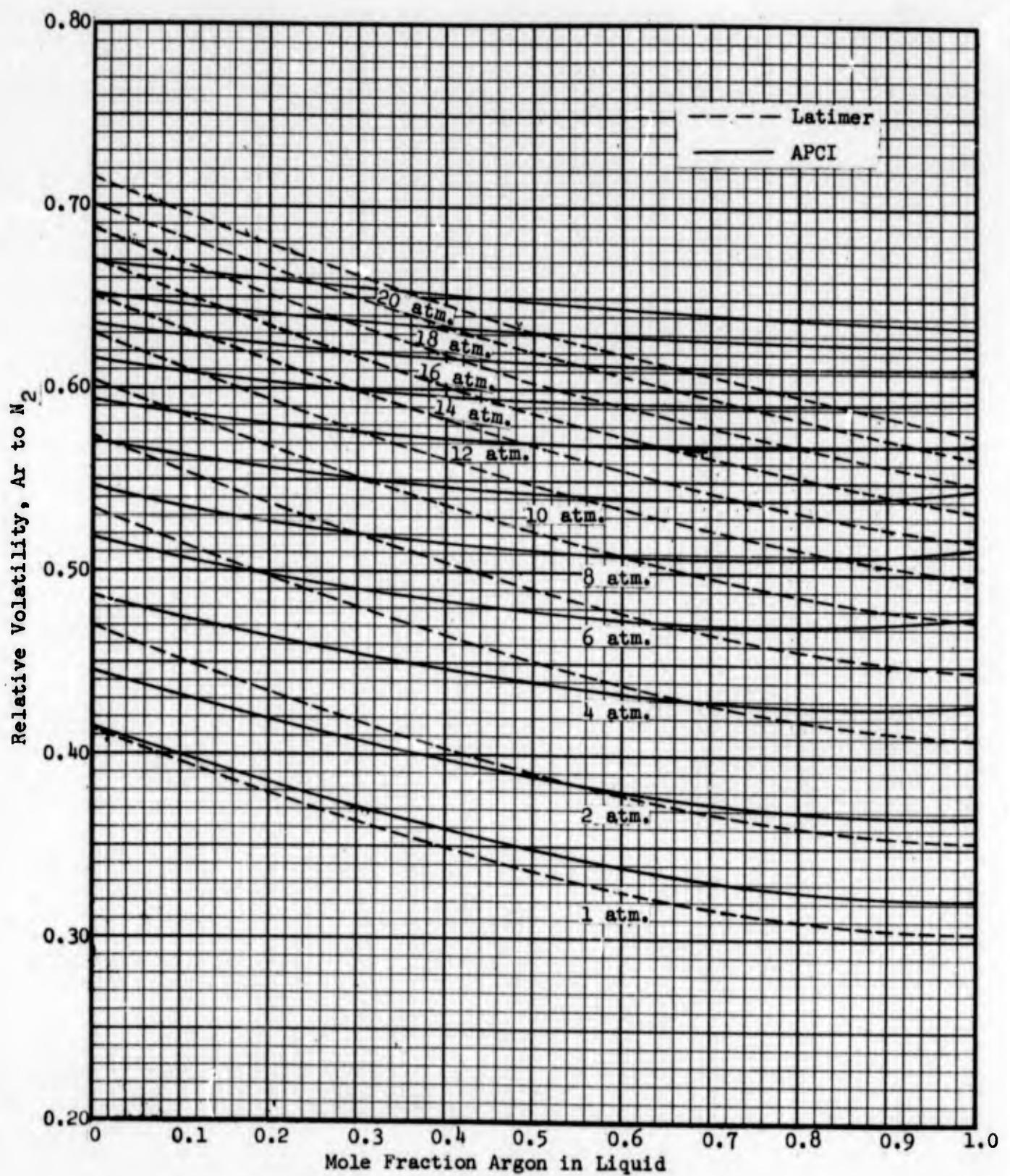


Figure 84. Comparison of APCI Correlation to Latimer Correlation for Argon-Nitrogen System.

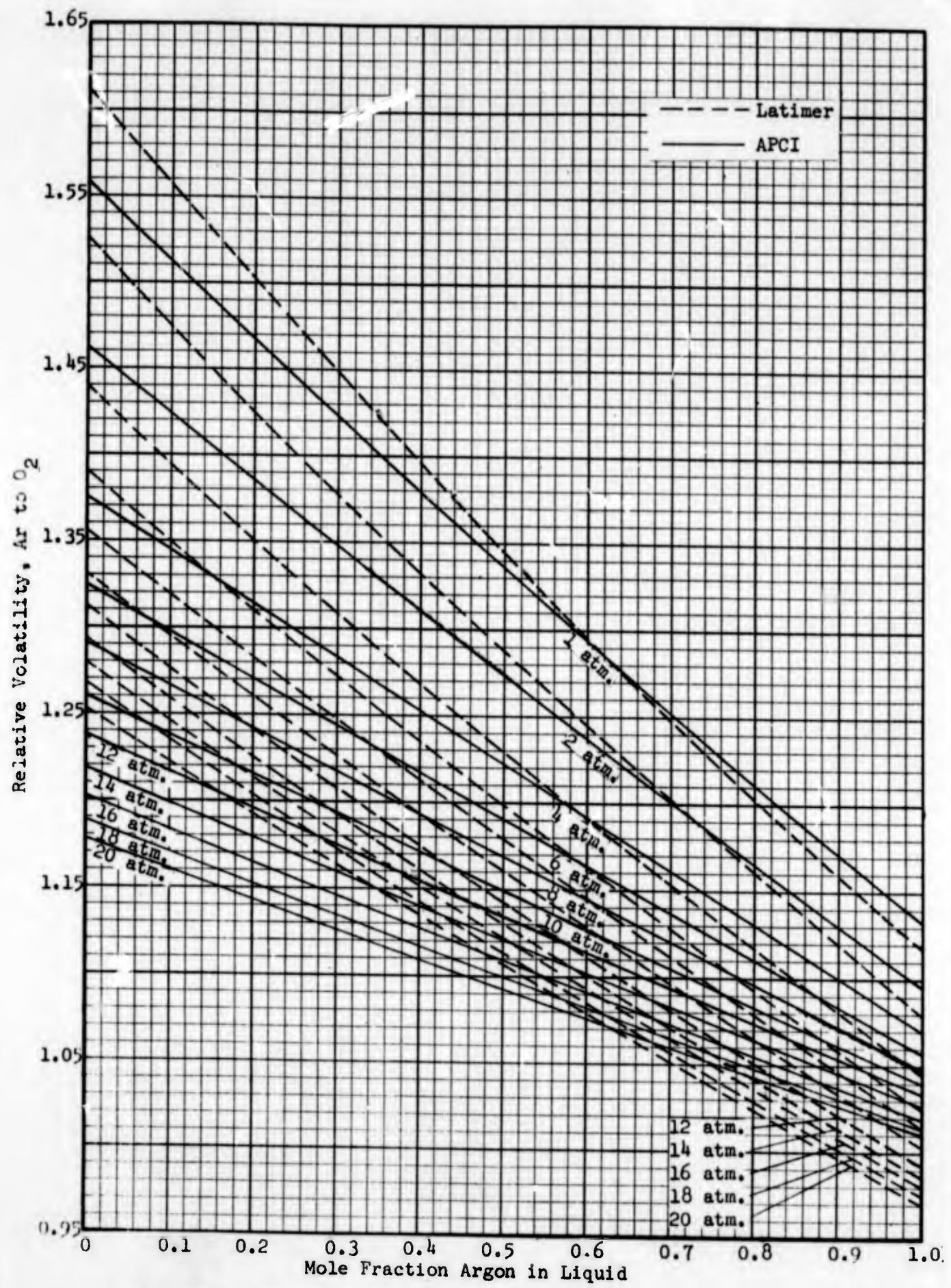


Figure 85. Comparison of APCI Correlation to Latimer Correlation for Argon-Oxygen System.

VIII. ENTHALPY CORRELATION

Enthalpy data obtained from the literature were correlated for computer usage in calculating the enthalpy of the vapor and enthalpy of the liquid according to the equations

$$H_{\text{vap.}} = \sum_i x_i H_i^* + \sum_i x_i (Hg_i - H_i^*) \quad (22)$$

$$\begin{aligned} H_{\text{liq.}} = & \sum_i x_i H_i^* + \sum_i x_i (Hg_i^{\circ} - H_i^*) - \sum_i x_i \Delta H_{vi}^{\circ} \\ & + \sum_i x_i V_i^{\circ} (p - p_i^{\circ}) + \sum_i x_i \Delta \bar{H}_m \end{aligned} \quad (23)$$

Reported below are the correlations to the data with referencing and commentary about accuracy.

A. Heat of Mixing

1. Argon-Oxygen - The data of Pool and co-workers⁽³⁵⁾ at 84°K appear more consistent than that of Knobler and co-workers⁽³⁶⁾ at 86°K. Pool's least squares fit of the data converted to BTU/lb-mole is:

$$H_m = x_{O_2} x_{Ar} [103 + 13.5 (x_{O_2} - x_{Ar})] \quad (24)$$

2. Nitrogen-Argon - The only data found were that of Pool and co-workers⁽³⁵⁾ at 84°K. Their least squares fit converted to BTU/lb-mole is:

$$H_m = x_{Ar} x_{N_2} [86.9 - 23.2 (x_{Ar} - x_{N_2})] \quad (25)$$

3. Nitrogen-Oxygen - The only data found were that of Knobler, van Heijningen and Beenakker⁽³⁶⁾ at 77°K. Weighting the points at oxygen mole fraction of 0.14 half as heavily as the rest, a method of averages curve fit gives within 10% accuracy:

$$H_m = x_{N_2} x_{O_2} [82.8 + 29 (x_{O_2} - x_{N_2})] \text{ BTU/lb-mole.} \quad (26)$$

For a heat of mixing of the form $H_m = x_1 x_2 [A + B (x_1 - x_2)]$, the partial molal heat of mixing is:

$$\Delta \overline{H}_m = x_2^2 [A + B (3x_1 - x_2)] \quad (27)$$

$$\Delta \overline{H}_m = x_1^2 [A + B (x_1 - 3x_2)] \quad (28)$$

B. Ideal Gas Heat Capacity 140-250°R

1. Argon - from Nat. Bur. Stds. (37): $C_p^\circ = 4.9647 \text{ BTU/mole } ^\circ\text{R}$ (29)

2. Oxygen - tabulation by Wooley (38): $C_p^\circ = 6.9558 \text{ BTU/mole } ^\circ\text{R}$ (30)

3. Nitrogen - from Goff and Gratch (39). Least squares curve fit:
 $C_p^\circ = 6.950571 + 0.27735687 \times 10^{-5}T + 0.3438922 \times 10^{-8}T^2$.
 Sum of squares error = 1×10^{-9} . (31)

C. Latent Heat

1. Nitrogen - The correlation is a least squares curve fit of the data from Mage, Jones, Katz, and Roebuck (40) and of Strobridge (41) $\Delta H_{v_i}^\circ$ in BTU/lb-mole, T in $^\circ\text{R}$.

$$\ln \Delta H_{v_i}^\circ = 6.36376 + 0.121474 \ln (226.91 - T) + 0.0880106 [\ln (226.91 - T)]^2 - 0.00987388 [\ln (226.91 - T)]^3 \quad (32)$$

$$\text{Root mean square error} = 8.1 \text{ BTU/lb-mole}$$

$$\text{A simpler fit is: } \ln \Delta H_{v_i}^\circ = 6.19701 + 0.354836 \ln (226.91 - T) \quad (33)$$

$$\text{Root mean square error} = 22 \text{ BTU/lb-mole}$$

2. Argon - The correlation is a least squares curve fit of the data of Flubacher, Leadbetter, and Morrison (42) and of Din (4). $\Delta H_{v_i}^\circ$ in BTU/lb-mole, T in $^\circ\text{R}$

$$\ln \Delta H_{v_i}^\circ = 7.35231 - 0.733687 \ln (271.30 - T) + 0.331584 [\ln (271.30 - T)]^2 - 0.0317968 [\ln (271.30 - T)]^3 \quad (34)$$

$$\text{Root mean square error} = 2.8 \text{ BTU/lb-mole}$$

$$\text{A simpler fit is: } \ln \Delta H_{v_i}^\circ = 6.20952 + 0.366142 \ln (271.30 - T) \quad (35)$$

$$\text{Root mean square error} = 27.6 \text{ BTU/lb-mole}$$

3. Oxygen - The correlation is a least squares fit synthesized from the data given by Fukurawa and McCoskey⁽⁴³⁾, Alikhanov⁽⁴⁴⁾, Claitor and Crawford⁽⁴⁵⁾ and the graphical data of Wilbers⁽⁴⁶⁾.

ΔH_{vi}° in BTU/lb-mole, T in °R

$$\ln \Delta H_{vi}^{\circ} = 5.61017 + 0.733877 \ln (278.60-T) - 0.0572340 [\ln (278.60-T)]^2 + 0.0016562 [\ln (278.60-T)]^3 \quad (36)$$

Root mean square error = 6.9 BTU/lb-mole

$$\text{A simple fit is: } \ln \Delta H_{vi}^{\circ} = 6.16014 + 0.384736 \ln (278.60-T) \quad (37)$$

Root mean square error = 77 BTU/lb-mole

- D. Enthalpy of the Real Gas - The commonly used symbol $(H-H^*)_T$ represents the effect of pressure at constant temperature on the enthalpy of a real gas. This quantity can be computed from the virial equation of state terminating with the third virial coefficient.

$$\frac{PV}{RT} = Z = 1 + \frac{B}{V} + \frac{C}{V^2} \quad (38)$$

Since B and C are functions of temperature only, the following equation is derived:

$$\frac{(H_{gi}-H_i^*)_T}{RT} = \left[\frac{1}{V} (B-T \frac{dB}{dT}) + \frac{1}{V^2} (C - \frac{1}{2} T \frac{dC}{dT}) \right] \quad (39)$$

The coefficients for argon, oxygen, and nitrogen are given in Section VID.

E. Saturated Pure Component Heat Capacity

1. Argon Liquid - from WADD Compendium⁽⁵⁾

$$C_p = 0.22 + 0.00468 \frac{T}{(151-T)^{1/2}} \quad (40)$$

C_p units cal/gm-°K, T in °K

2. Oxygen Liquid - insufficient data to correlate.

3. Nitrogen Liquid - Correlation of Strobridge⁽⁴¹⁾

$$C_s = \frac{6.24688186T}{(126.26-T)^2} + 39.39006895 + 0.6821295539T - 0.01052432772T^2 + 0.00006001046981T^3 \quad (41)$$

C_s units joule/gm-mole °K, T in °K

4. Argon Vapor - from Din⁽⁴⁾

$$C_s = 325.63362 - 8.8669510T + 0.08828184T^2 - 0.00031196544T^3 \quad (42)$$

C_s units joule/gm-mole °K, T in °K

5. Oxygen Vapor - from Claitor and Crawford⁽⁴⁵⁾

$$C_s = -468.26228 - 2.6649068T + 0.010328679T^2 + 9.0958184 \times 10^{-5}T^3 + 1.4860065 \times 10^{-7}T^4 \quad (43)$$

C_s units BTU/lb-mole °F, T in °F

6. Nitrogen Vapor - from Strobridge⁽⁴¹⁾

$$C_s = 48.332643 - 0.7791322T - 0.0065282424T^2 + 1.7403752 \times 10^{-4}T^3 - 7.9049655 \times 10^{-7}T^4 \quad (44)$$

C_s units joule/gm °K, T in °K

Enthalpy data presented in the Appendix were calculated for the vapor from the virial equation of state and the ideal gas heat capacities; the reference state is the ideal gas at 0°R. The liquid enthalpy was calculated from a curve fit of liquid enthalpy data for the pure components calculated from the latent heat of vaporization and the enthalpy of the vapor. The

following are the analytical equations obtained for the saturated liquid enthalpy of nitrogen, argon, and oxygen; temperature in °R.

Nitrogen:

$$H_{liq.} = - 9774 + 158.74T - 1.2087T^2 + 4.3451 \times 10^{-3}T^3 - 5.589 \times 10^{-6}T^4 \quad (45)$$

Argon:

$$H_{liq.} = - 3634 + 12.71T - 2.976 \times 10^{-2}T^2 + 6.08 \times 10^{-5}T^3 + 1.418 \times 10^{-7}T^4 \quad (46)$$

Oxygen:

$$H_{liq.} = - 882 - 56.32T + 0.58608T^2 - 2.2058 \times 10^{-3}T^3 + 3.131 \times 10^{-6}T^4 \quad (47)$$

Based upon the scatter in the experimental enthalpy data, these equations are estimated to be correct within ± 20 BTU/lb-mole. Because of this large uncertainty no correction was made for the effect of the heat of mixing and the effect of pressure on the enthalpy of the liquid. The enthalpy was calculated simply as

$$H_{liq.} = \sum_i x_i H_{liq. i} \quad (48)$$

The correction for the heat of mixing varies up to 25 BTU/lb-mole and the correction for the effect of pressure on the enthalpy is only significant at the higher pressures where it varies up to 40 BTU/lb-mole. A check on the thermodynamic consistency of the data was made by comparison of calculated values of the saturated heat capacity with experimental data by means of the following equation neglecting the second term.

$$C_{sat.} = \left(\frac{\partial H}{\partial T} \right)_{sat.} - v \left(\frac{\partial P}{\partial T} \right)_{sat.} \quad (49)$$

The comparison of the data is given in Table 24.

At low temperatures the calculated and experimental heat capacities are in good agreement for nitrogen and oxygen, and somewhat poorer agreement for argon. The largest deviations of about 10% occur at high temperatures where the effect of pressure on the enthalpy may begin to be significant. The agreement is considered good enough that the calculated heat capacities given in the appendix are based upon a temperature differentiation of the enthalpy equations.

TABLE 24

COMPARISON OF CALCULATED AND EXPERIMENTAL
SATURATED LIQUID HEAT CAPACITIES, BTU/lb-MOLE-°R

Temperature °F	Nitrogen		Argon		Oxygen	
	Exp. (41)	Calc.	Exp. (5)	Calc.	Exp. (47)	Calc.
-320	12.8	12.4
-310	13.9	14.0	10.7	9.8	12.9	12.9
-300	14.2	14.1	10.9	10.2	13.0	13.1
-290	14.6	14.6	11.2	10.6	13.2
-280	15.1	15.5	11.5	11.2	13.3
-270	15.8	16.6	11.7	11.9	13.4
-260	16.9	17.8	12.0	12.6	13.6
-250	18.9	18.9	12.2	13.5	14.0
-240	13.1	14.4	14.6
-230	14.6	15.5	15.6

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APPENDIX I
GRAPHICAL PRESENTATION OF CORRELATIONA. K-Values Vs. Pressure

The 36 graphs to follow present the K-values defined as:

$$K_i = \frac{y_i}{x_i} \quad (50)$$

of the three components as a function of pressure along selected isotherms. Envelopes defining the binary compositions are drawn as dashed lines.

The graphs are grouped in order of component: nitrogen, argon, oxygen. Inside each group they are ordered with respect to increasing mole fraction nitrogen in the liquid.

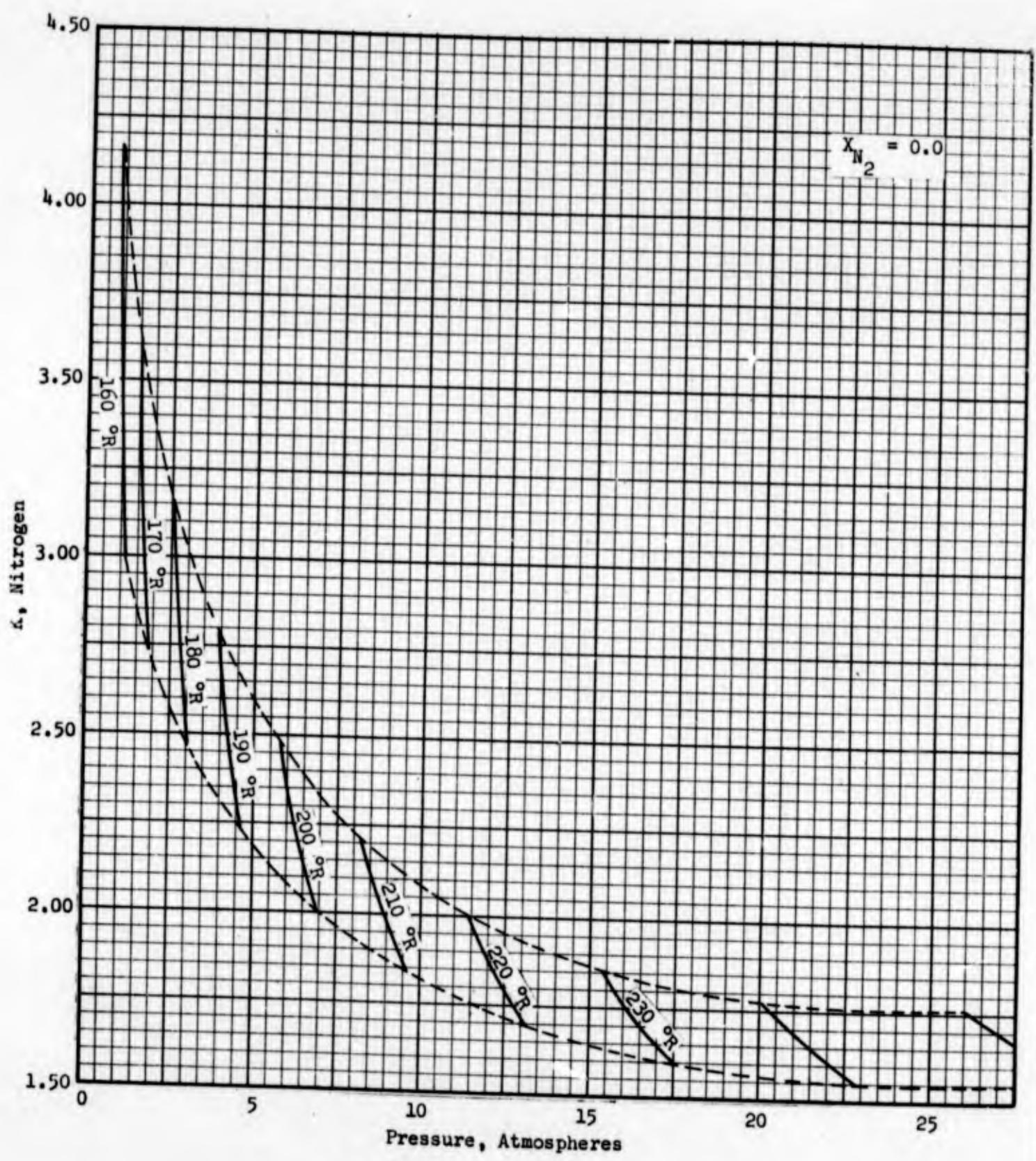


Figure 86. K-Values of Nitrogen,

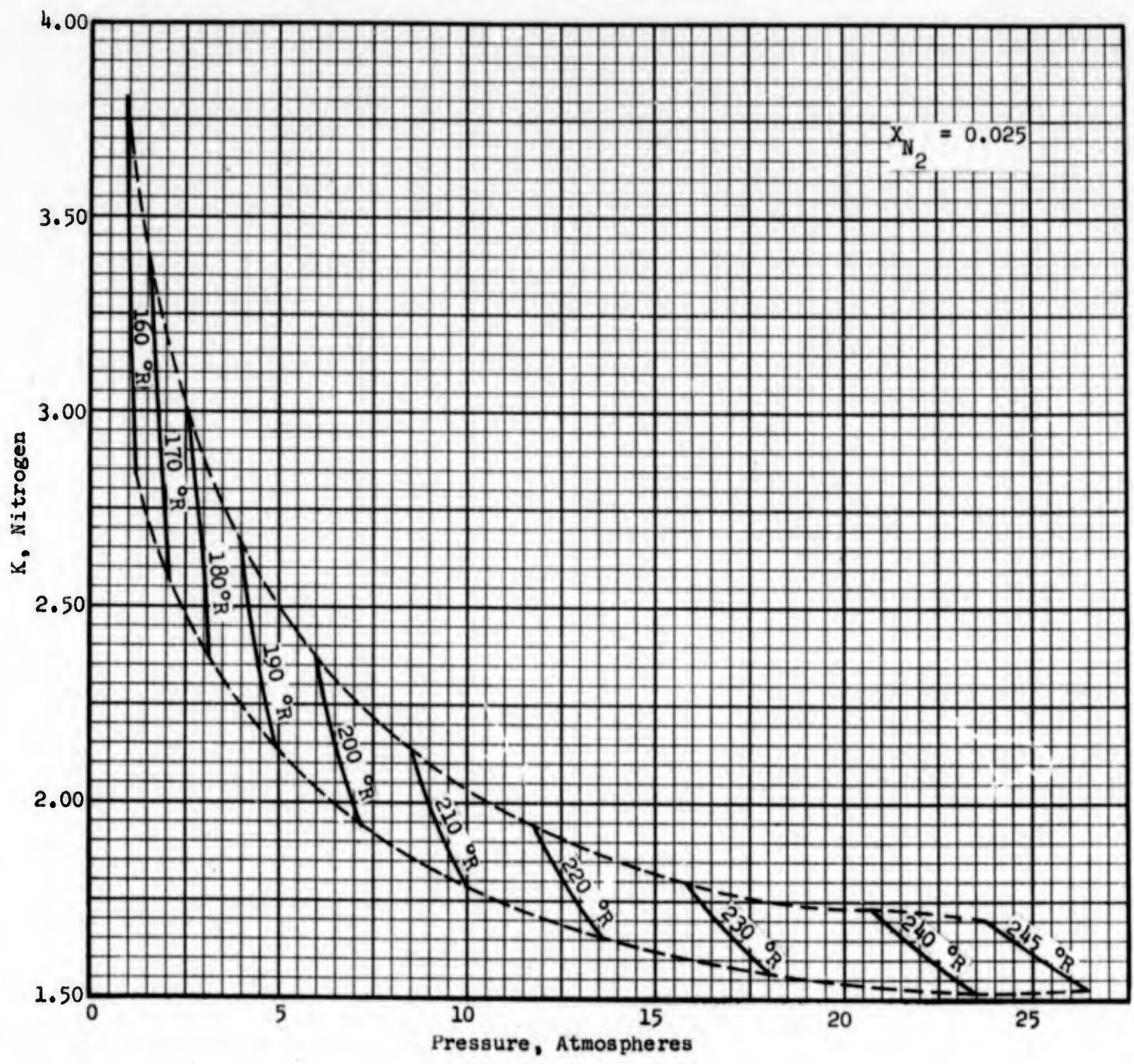


Figure 87. K-Values of Nitrogen.

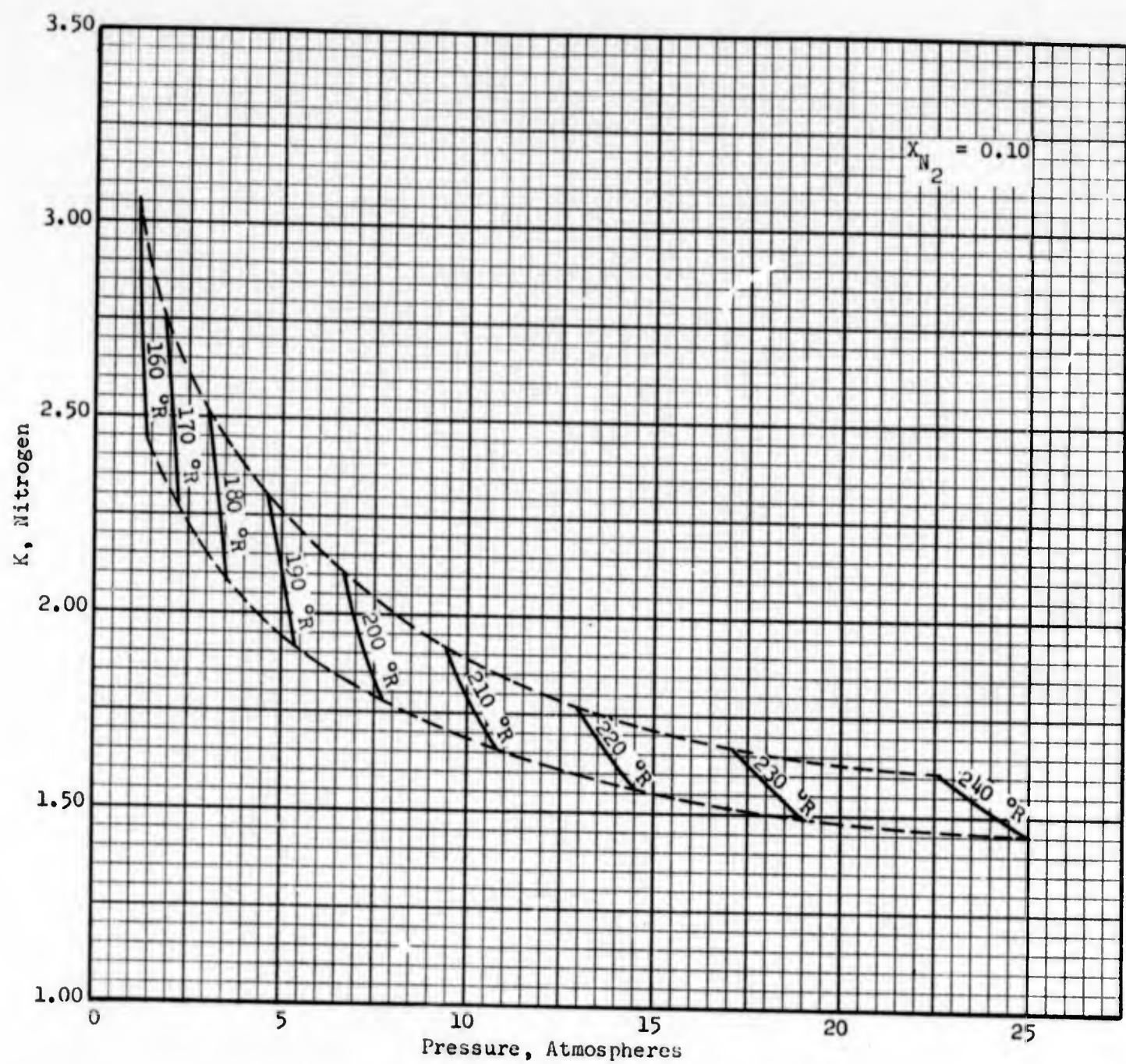


Figure 88. K-Values of Nitrogen.

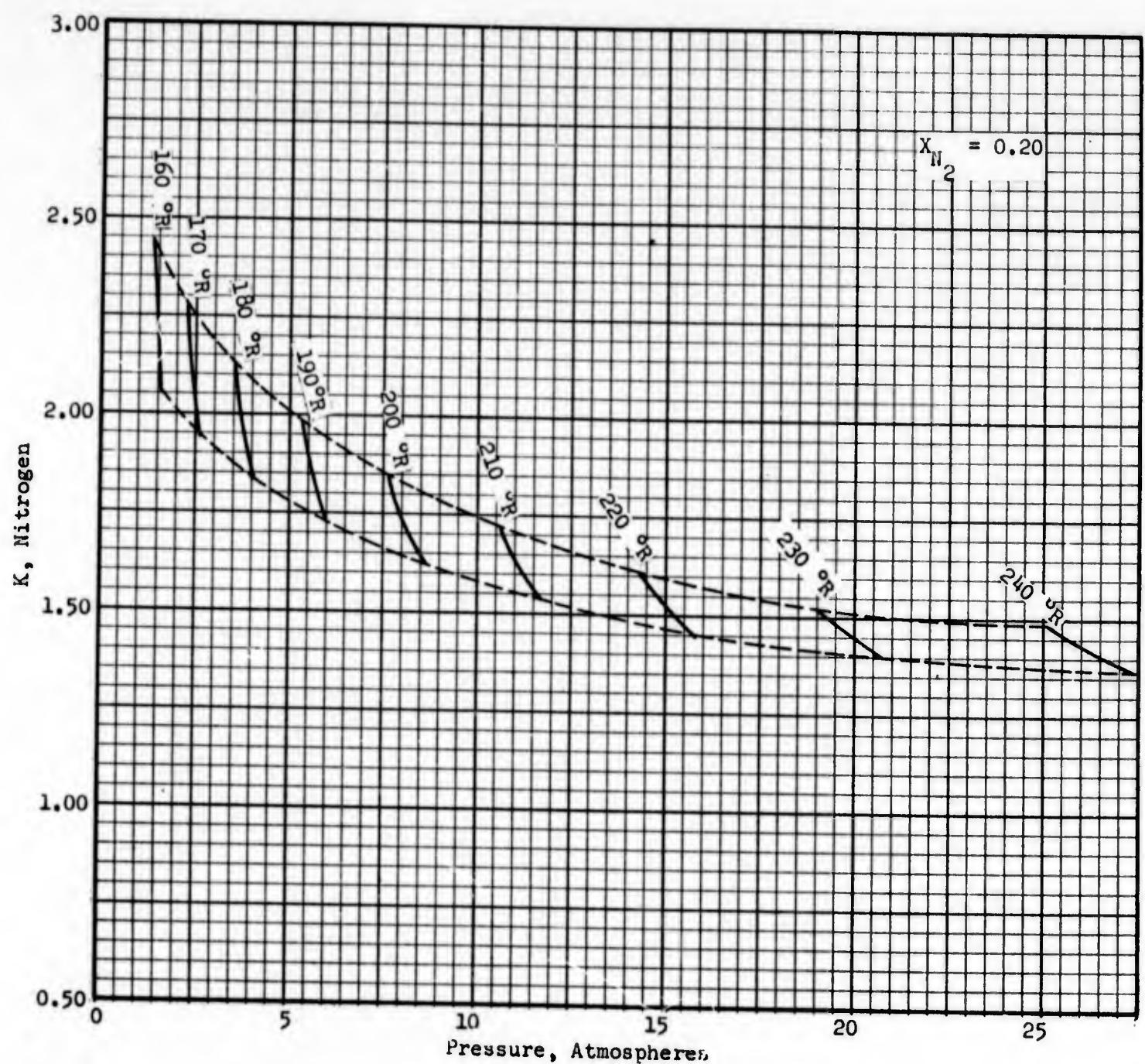


Figure 89. K-Values of Nitrogen.

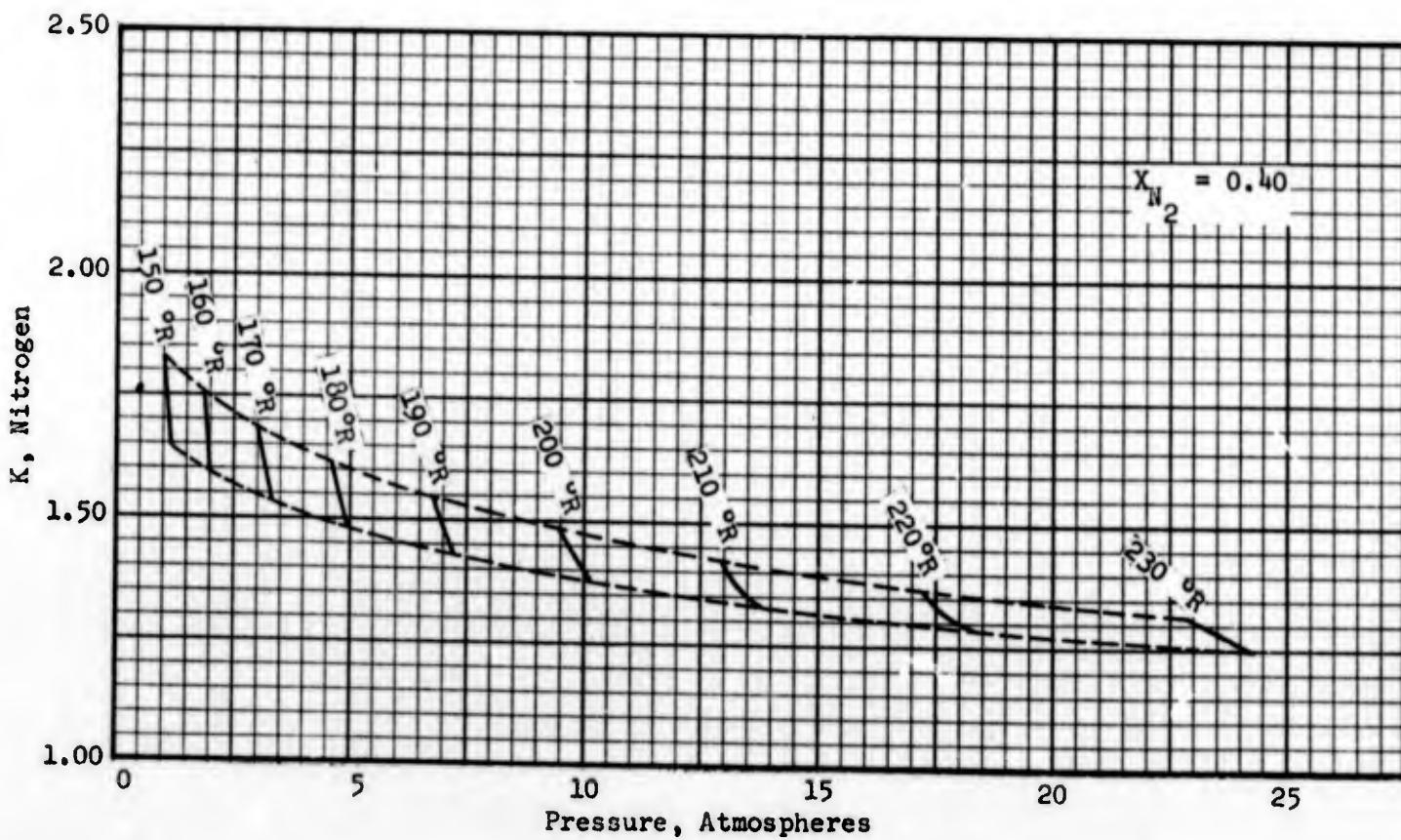
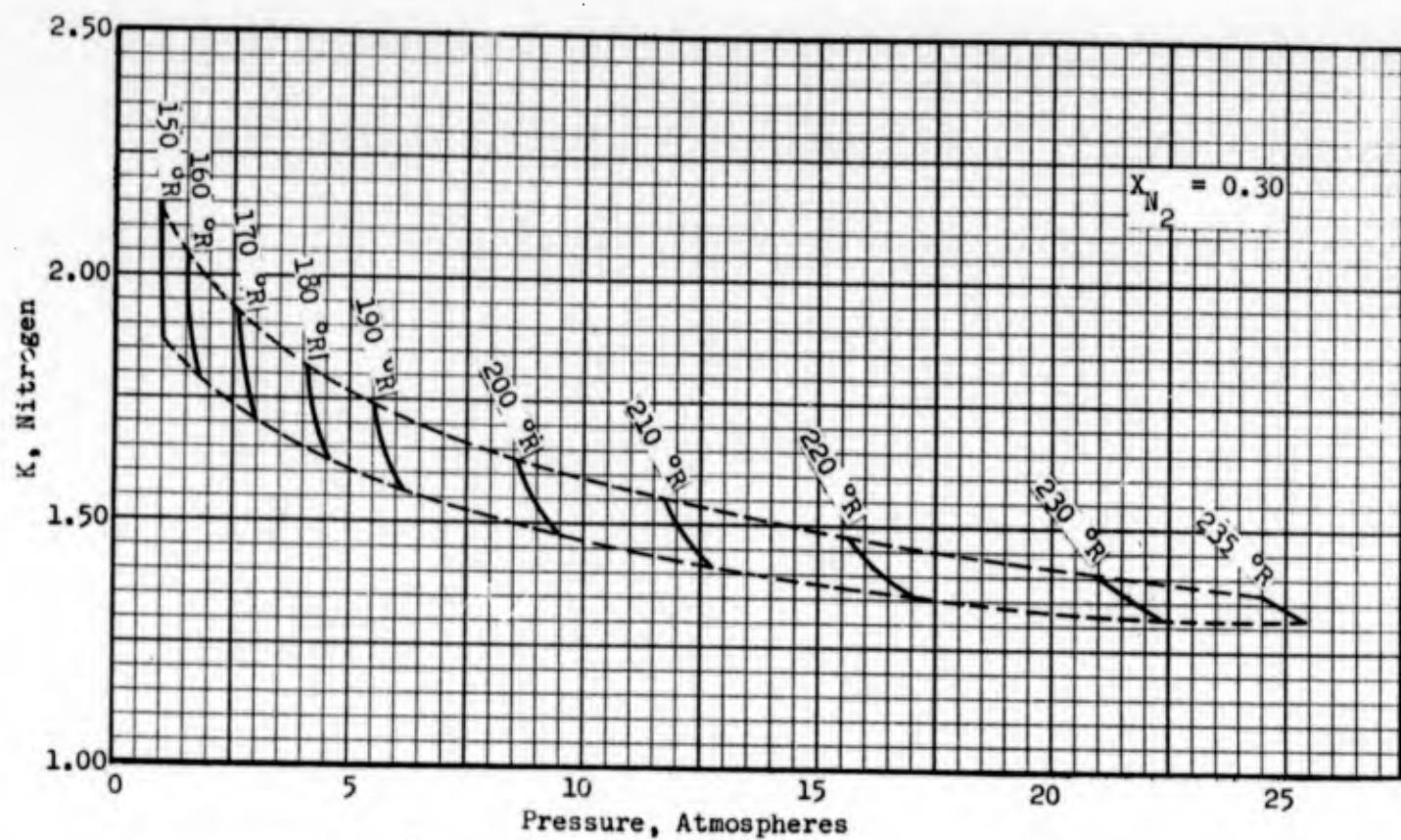


Figure 90. K-Values of Nitrogen.

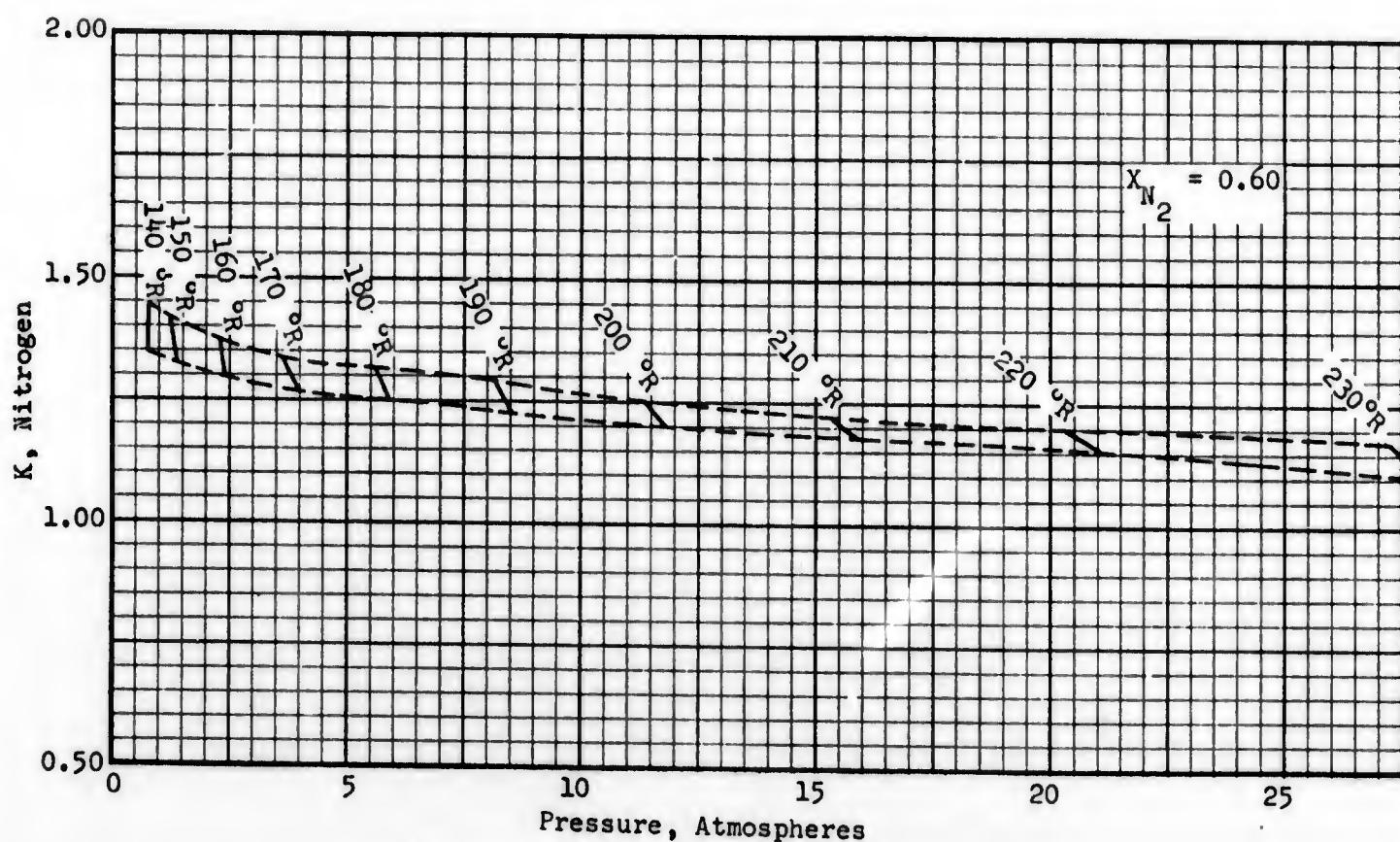
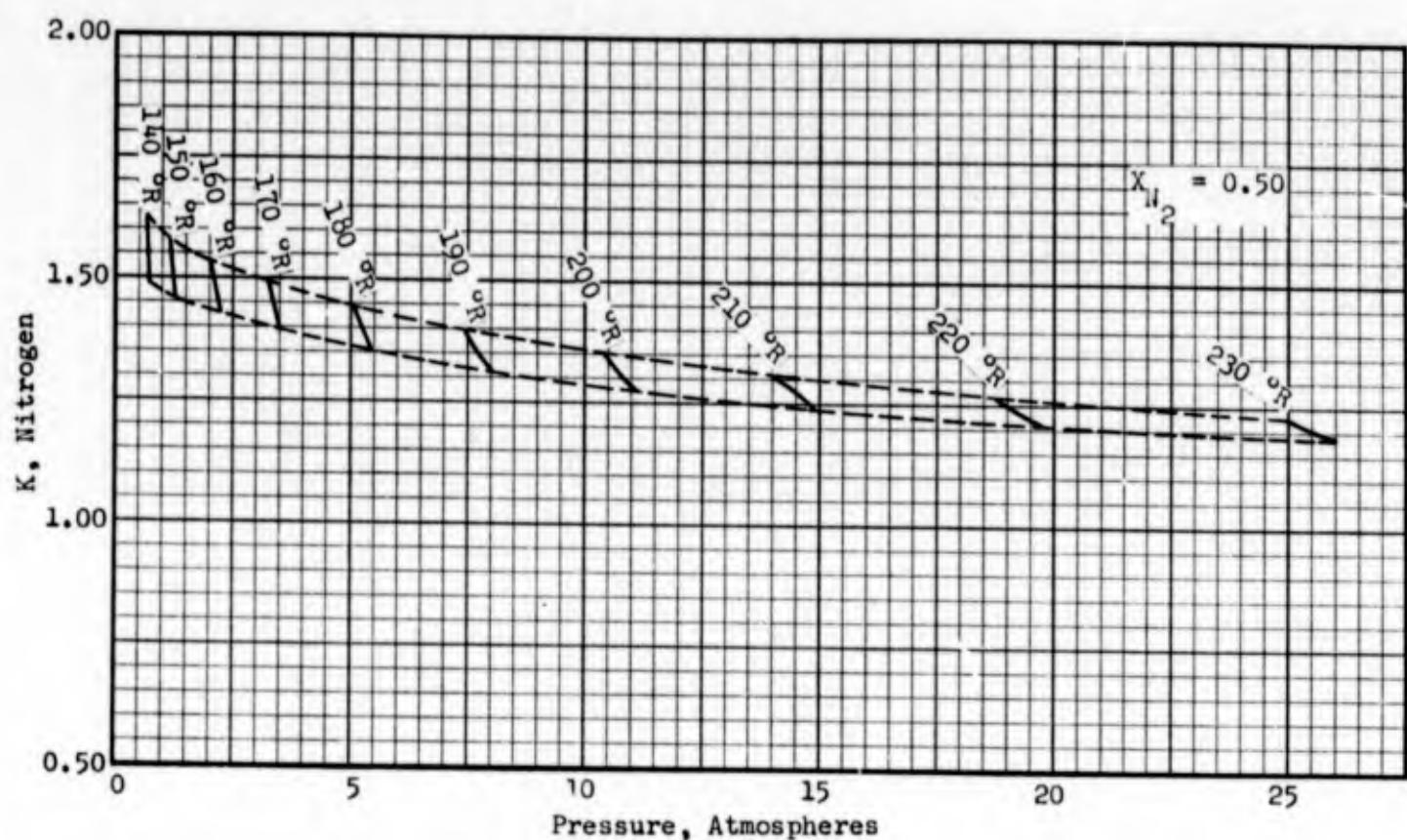


Figure 91. K-Values of Nitrogen.

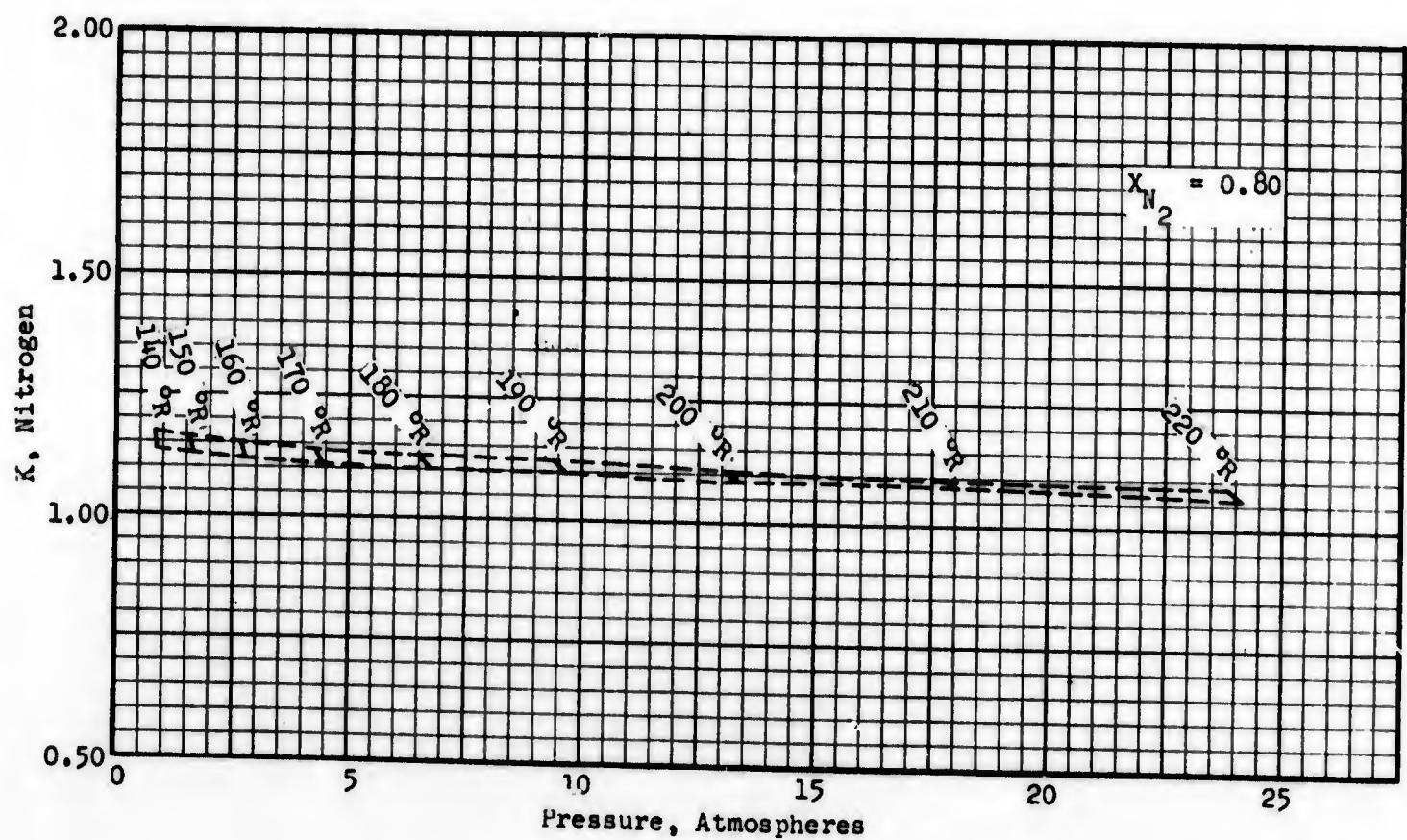
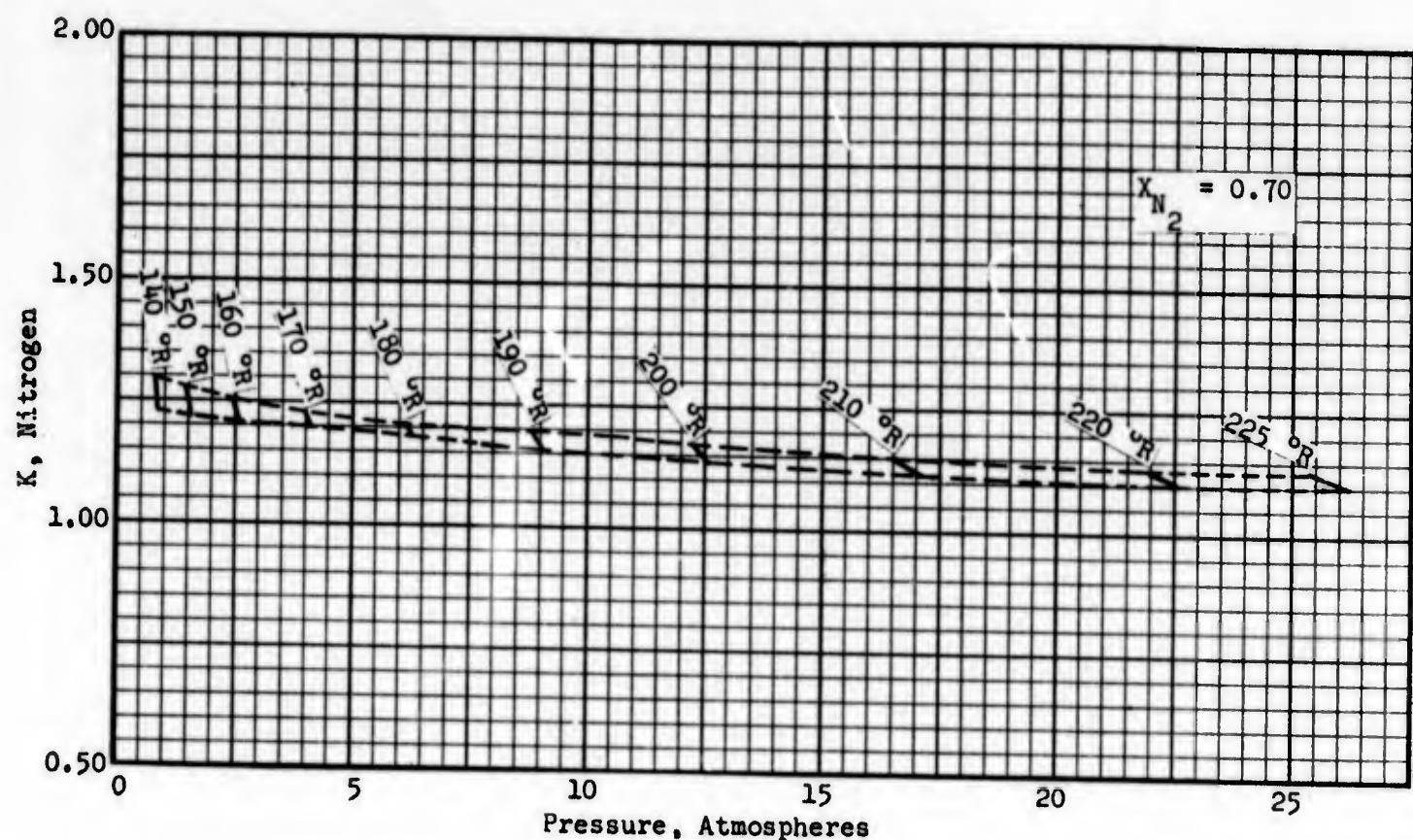


Figure 92. K-Values of Nitrogen.

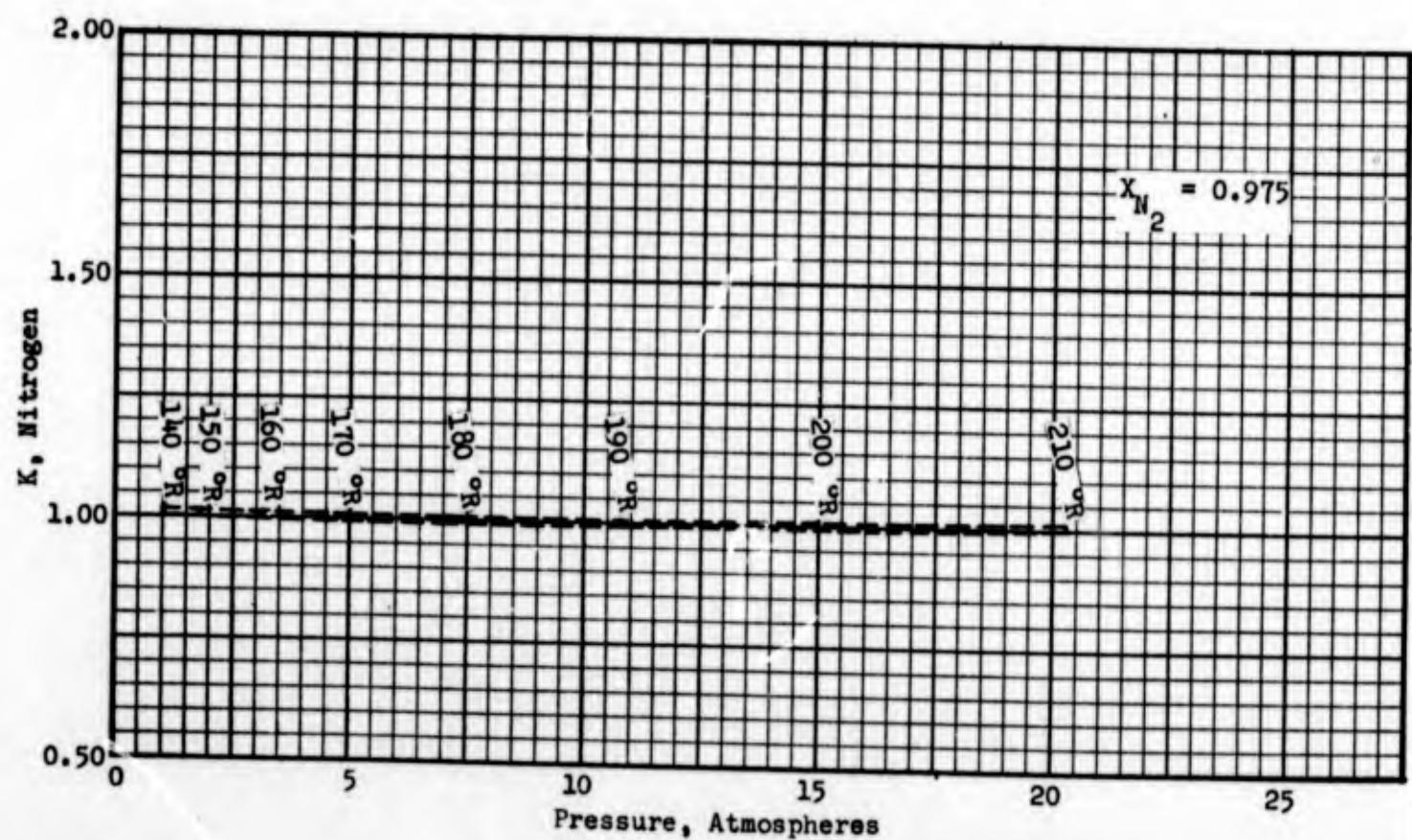
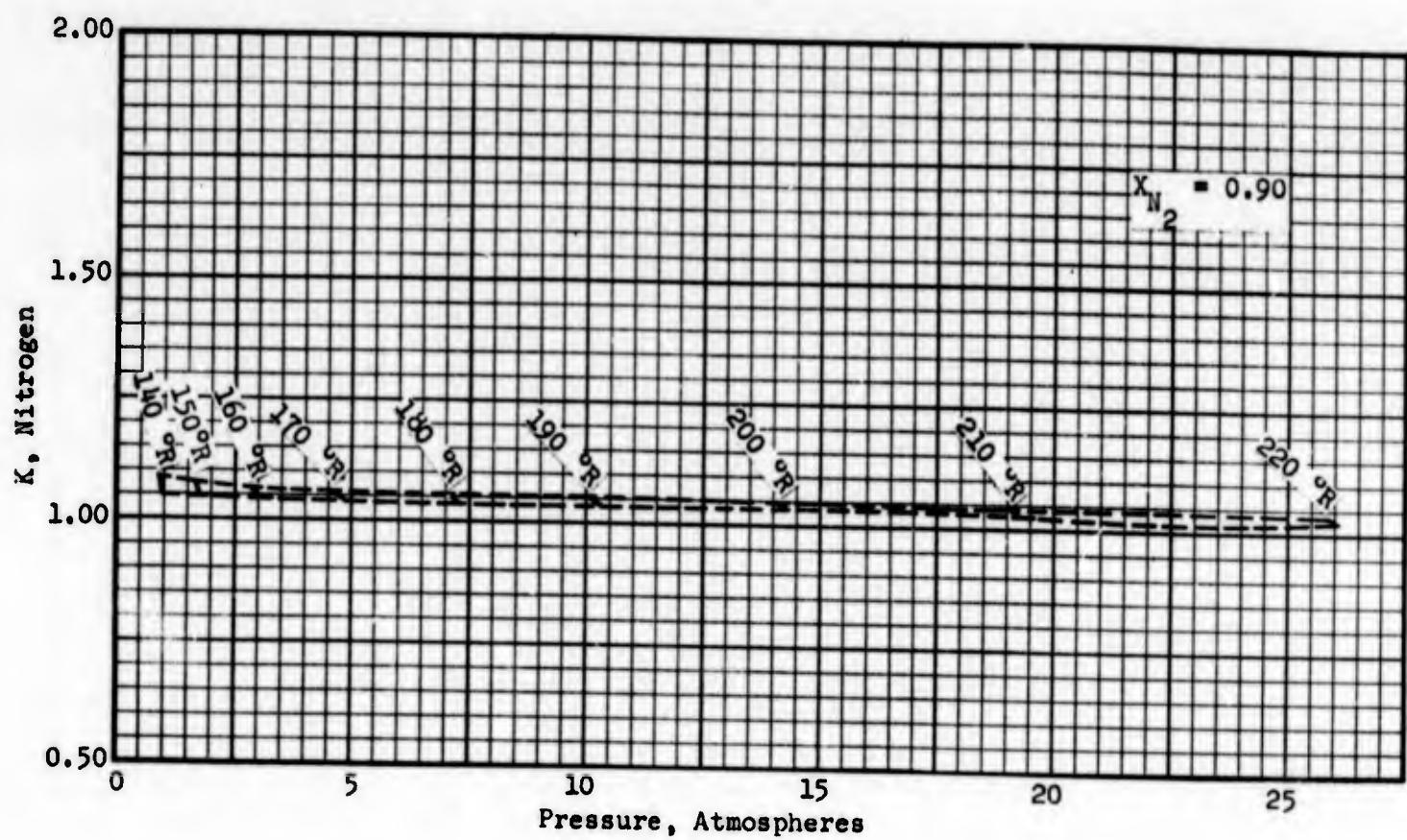


Figure 93. K-Values of Nitrogen.

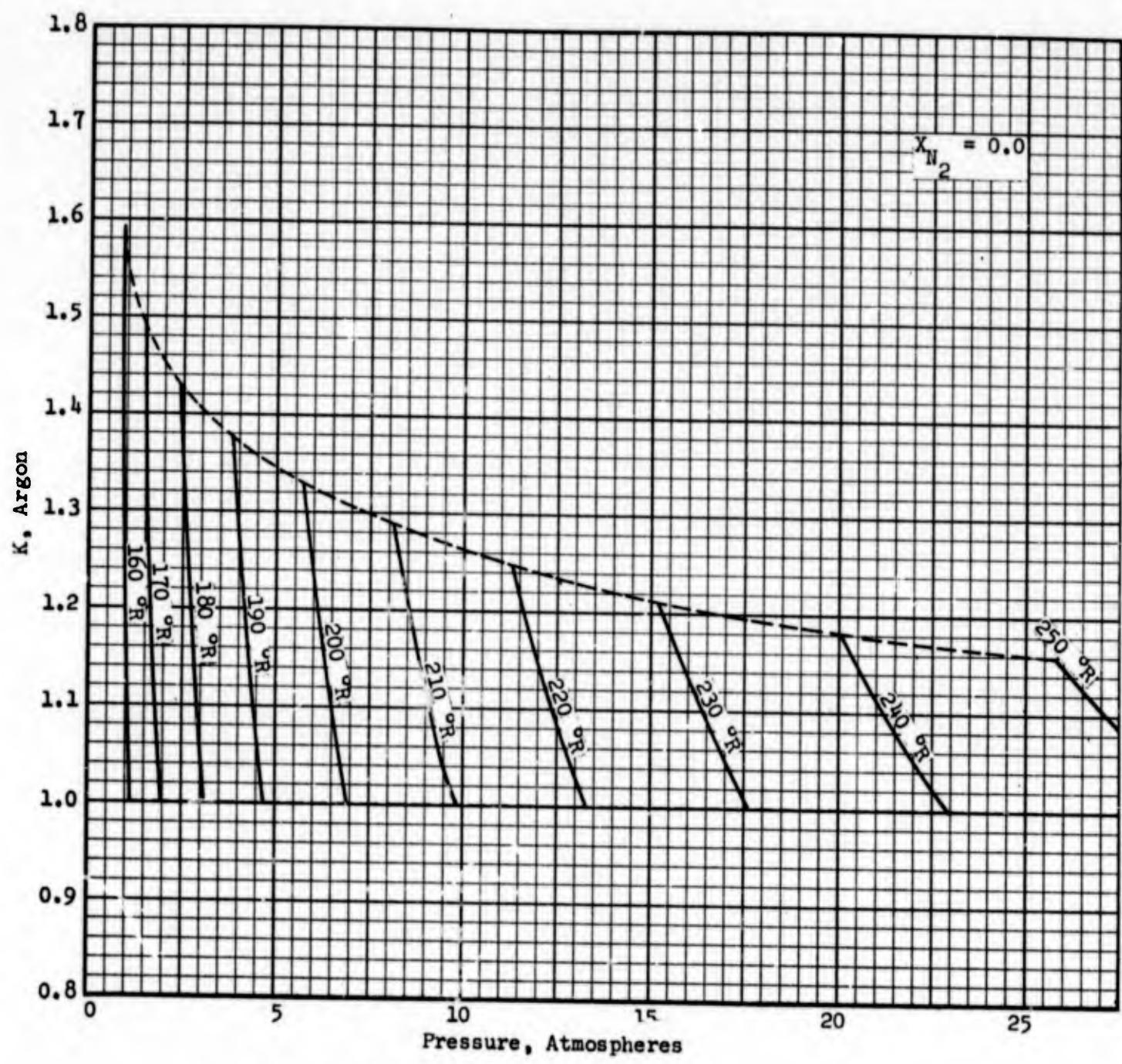


Figure 94. K-Values of Argon.

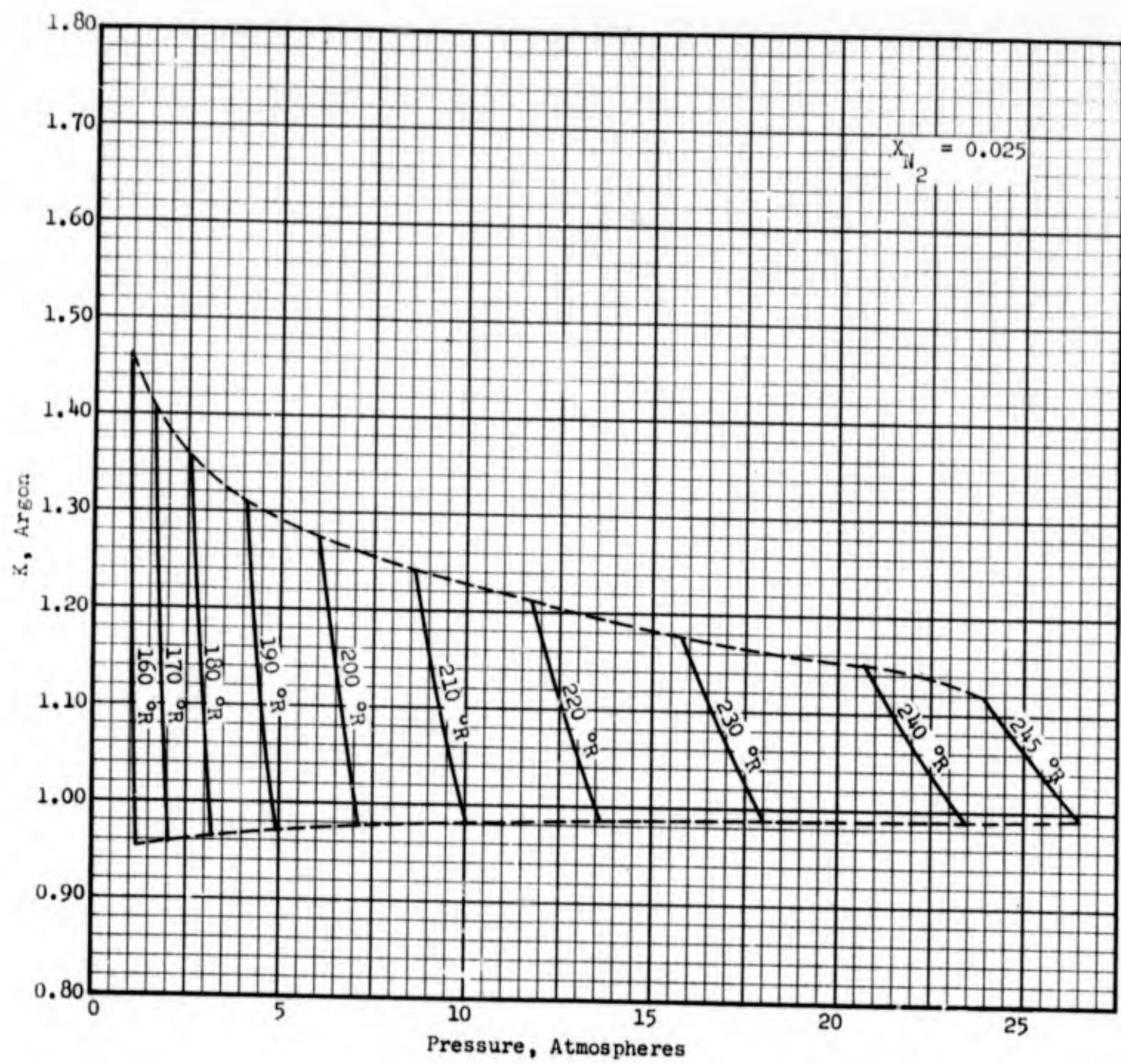


Figure 95. K-Values of Argon

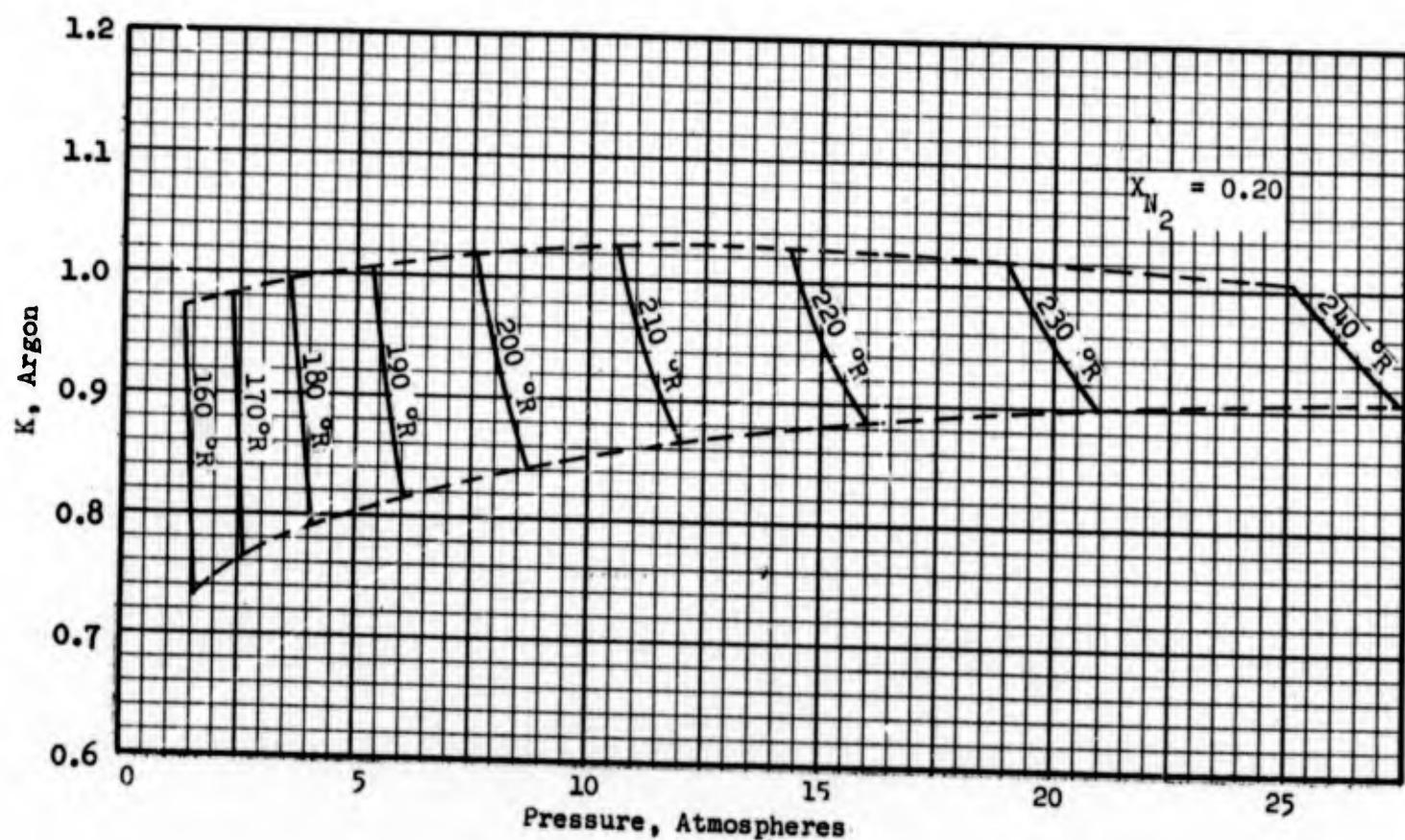
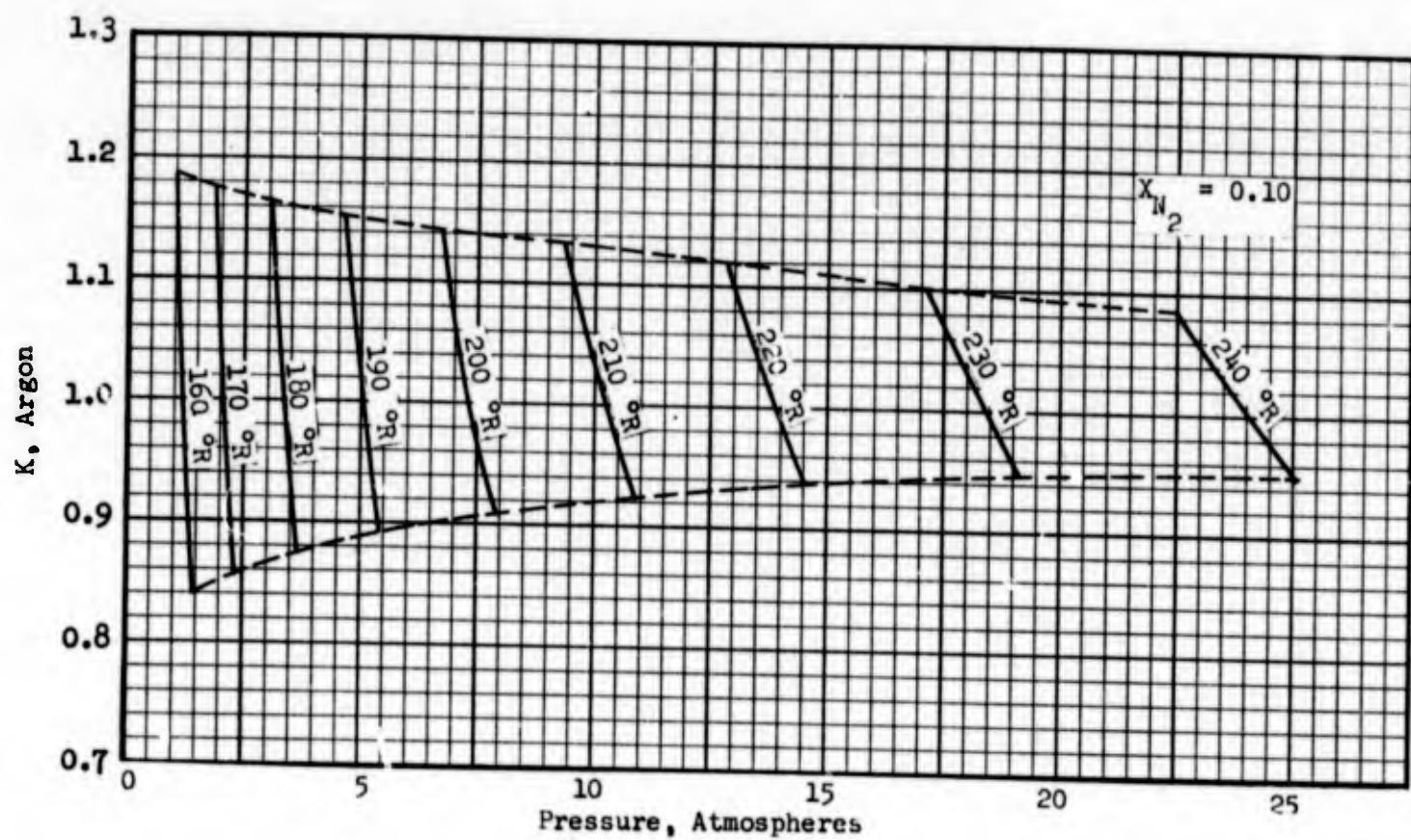


Figure 96. K-Values of Argon.

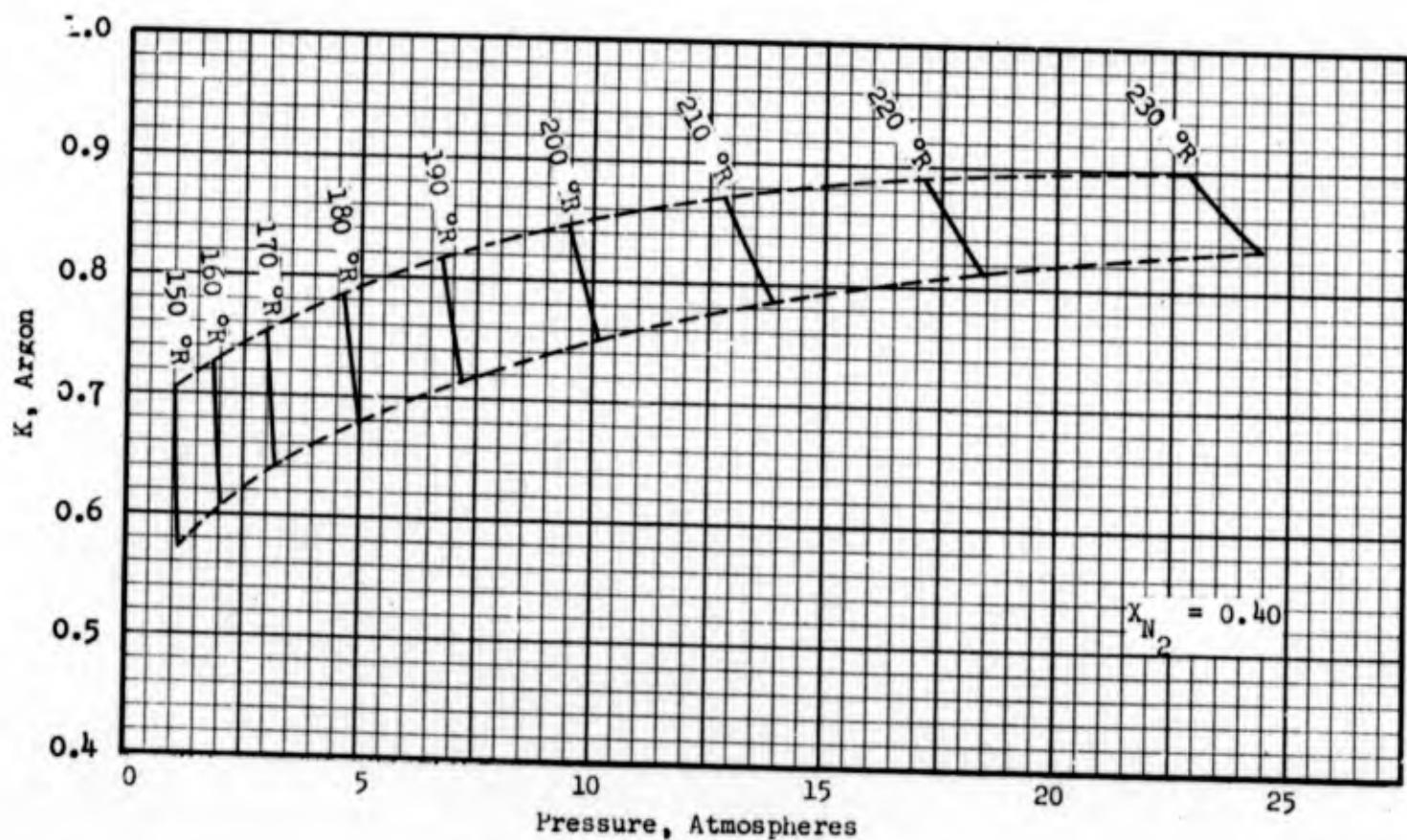
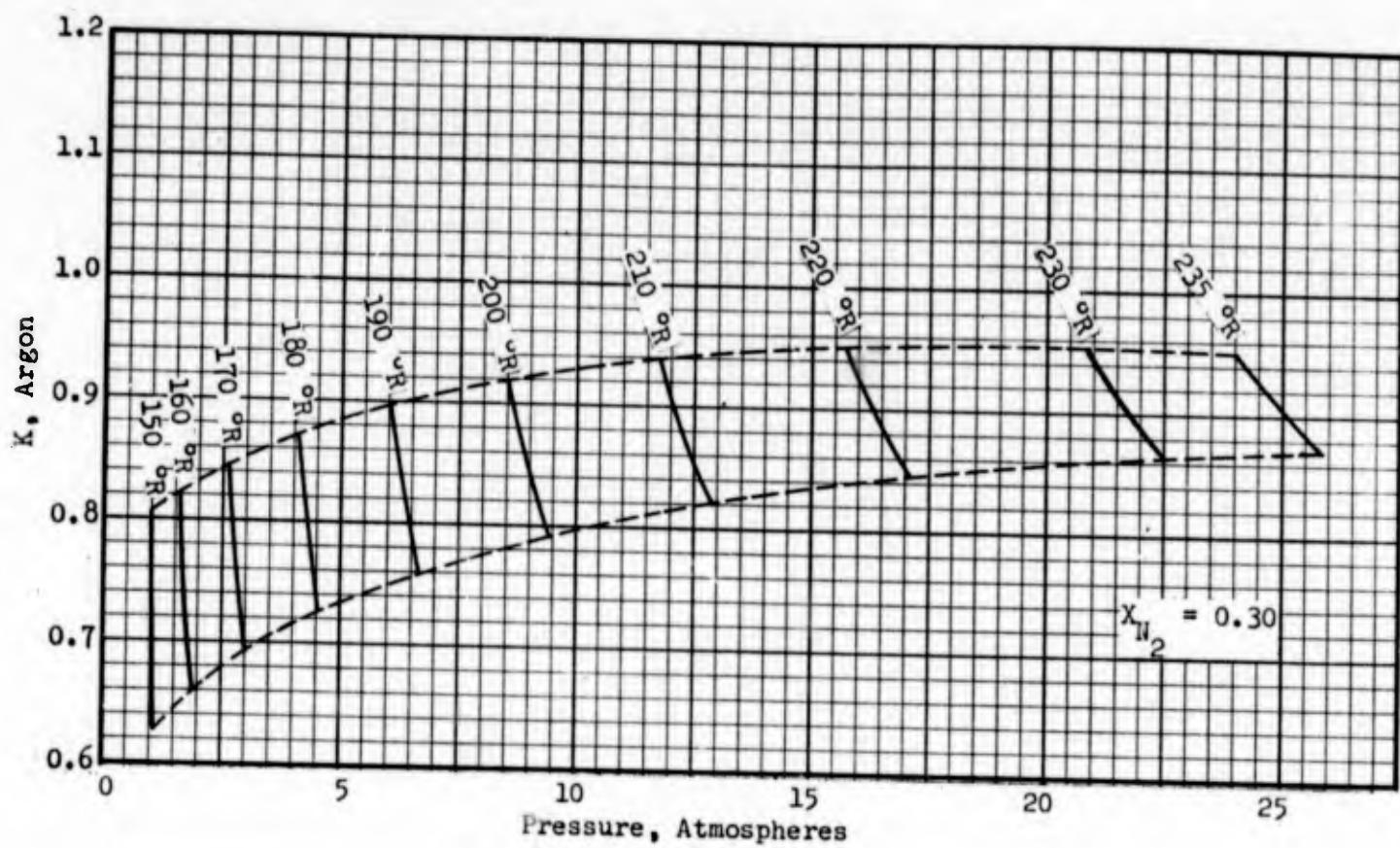


Figure 97. K-Values of Argon.

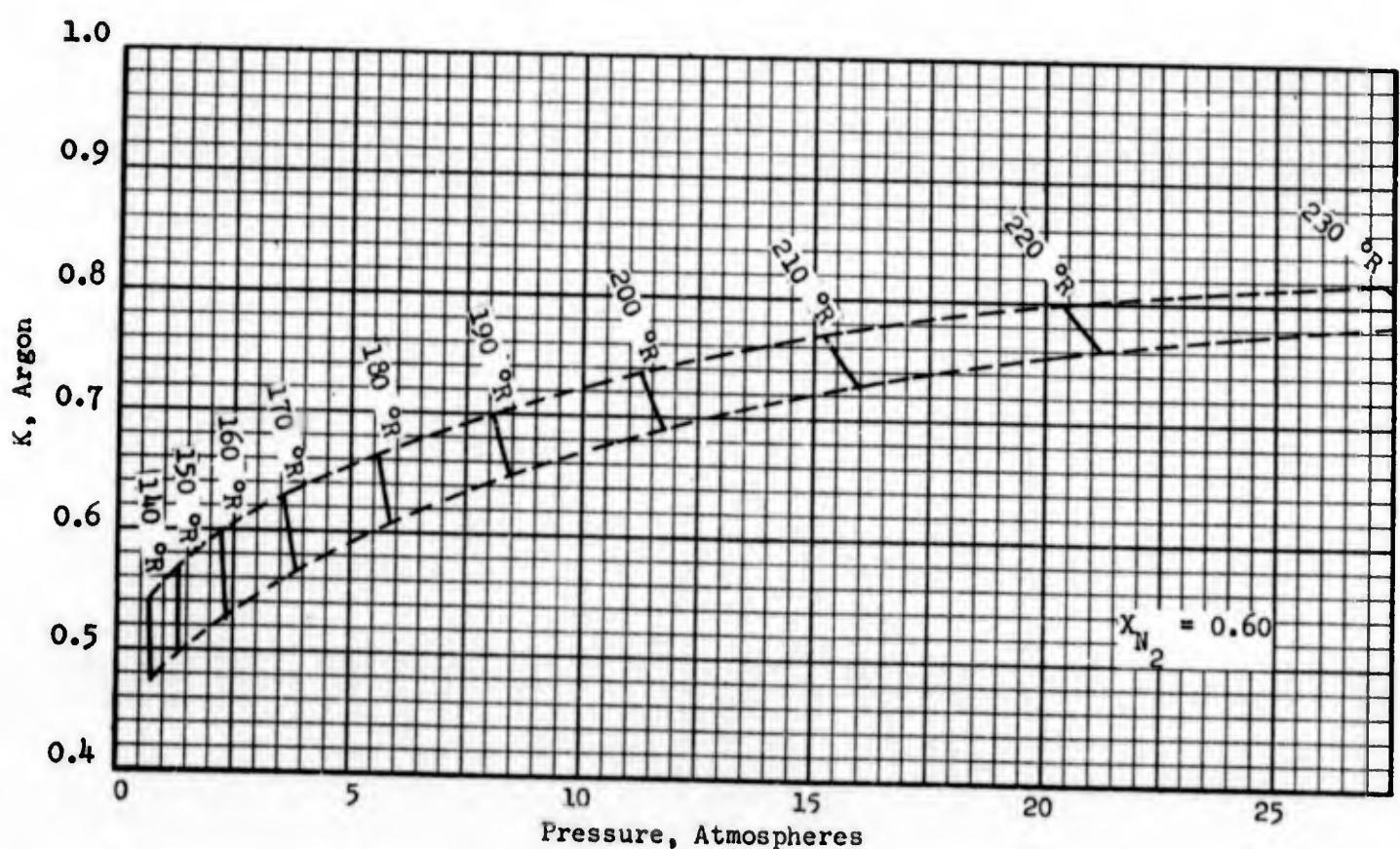
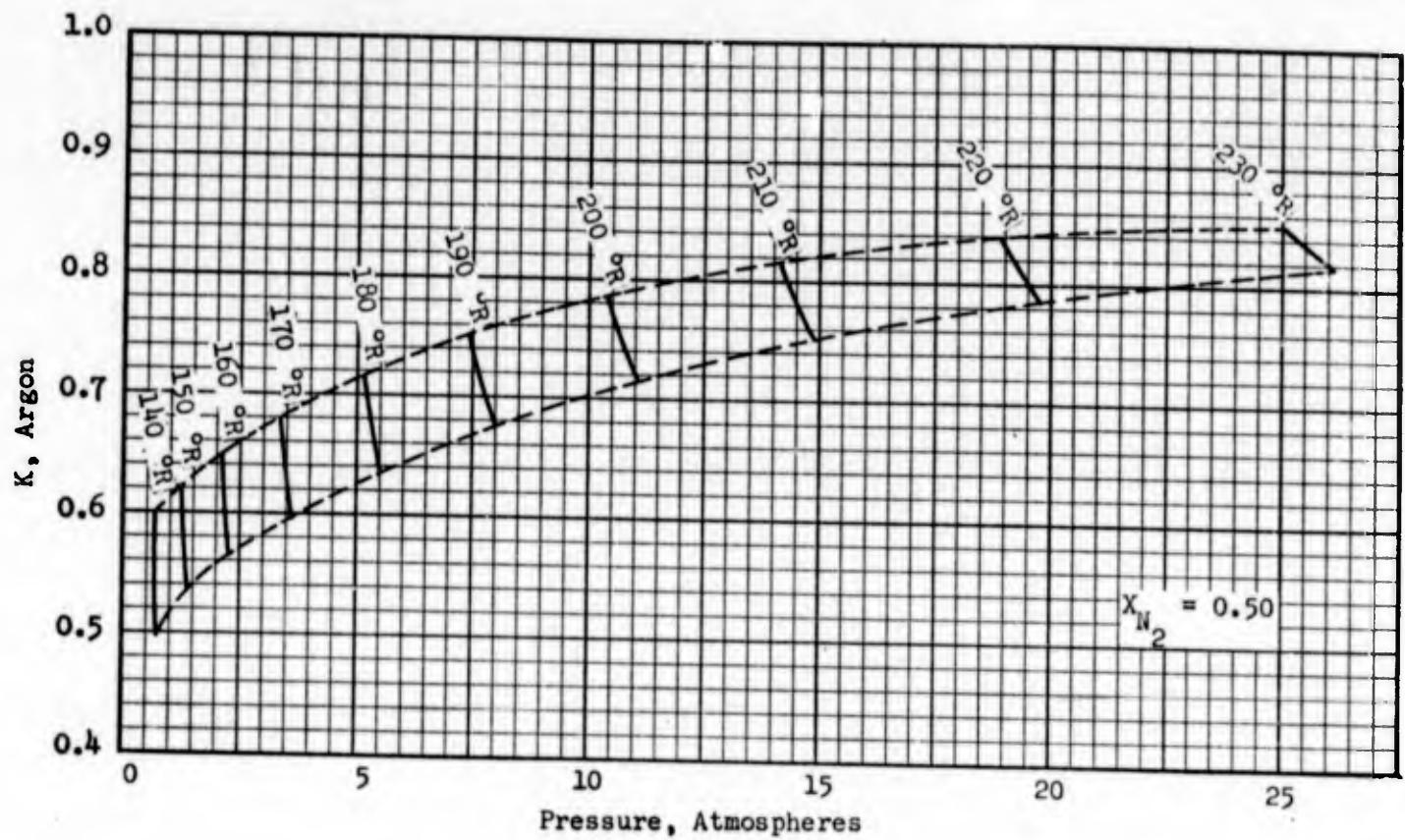


Figure 98. K-Values of Argon.

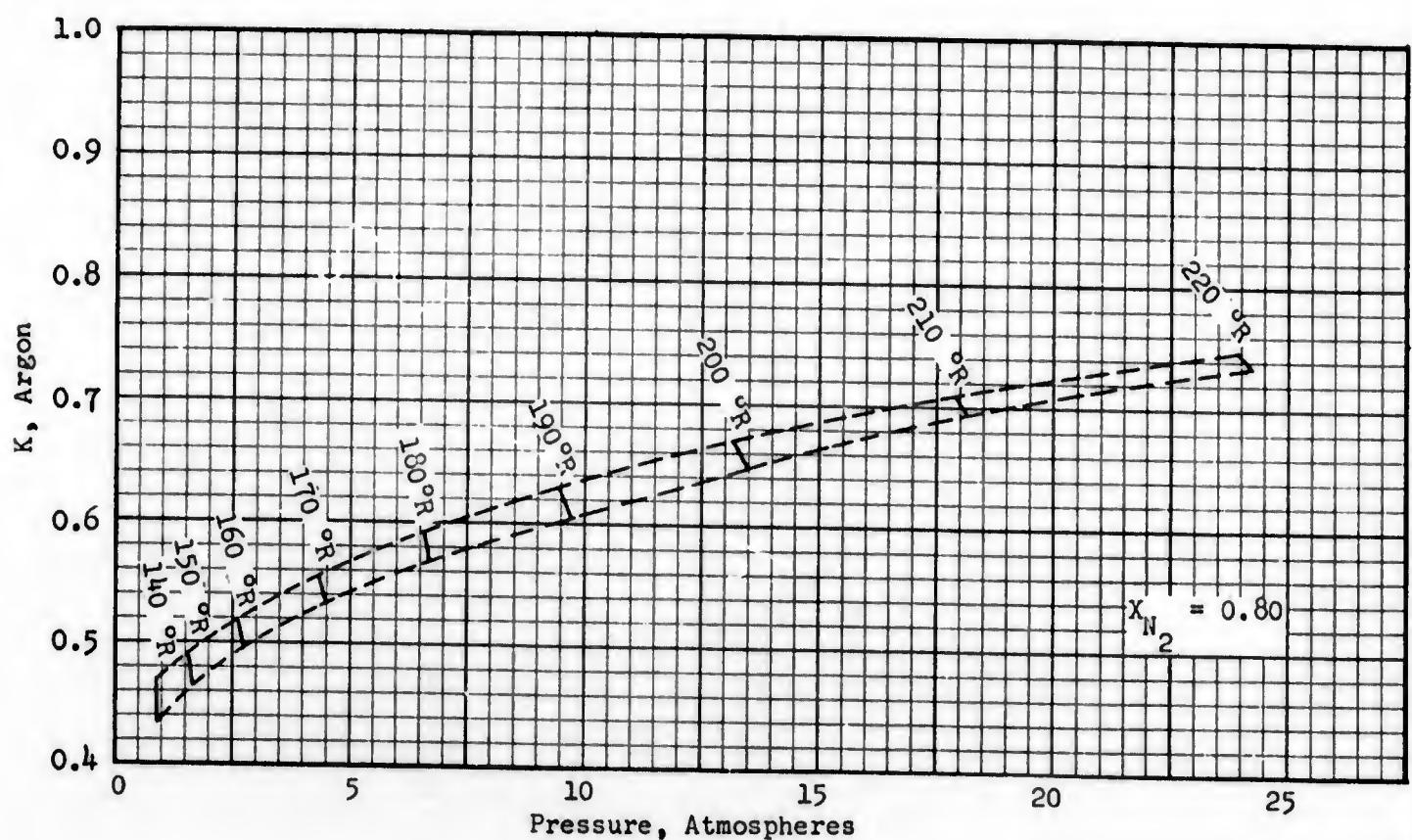
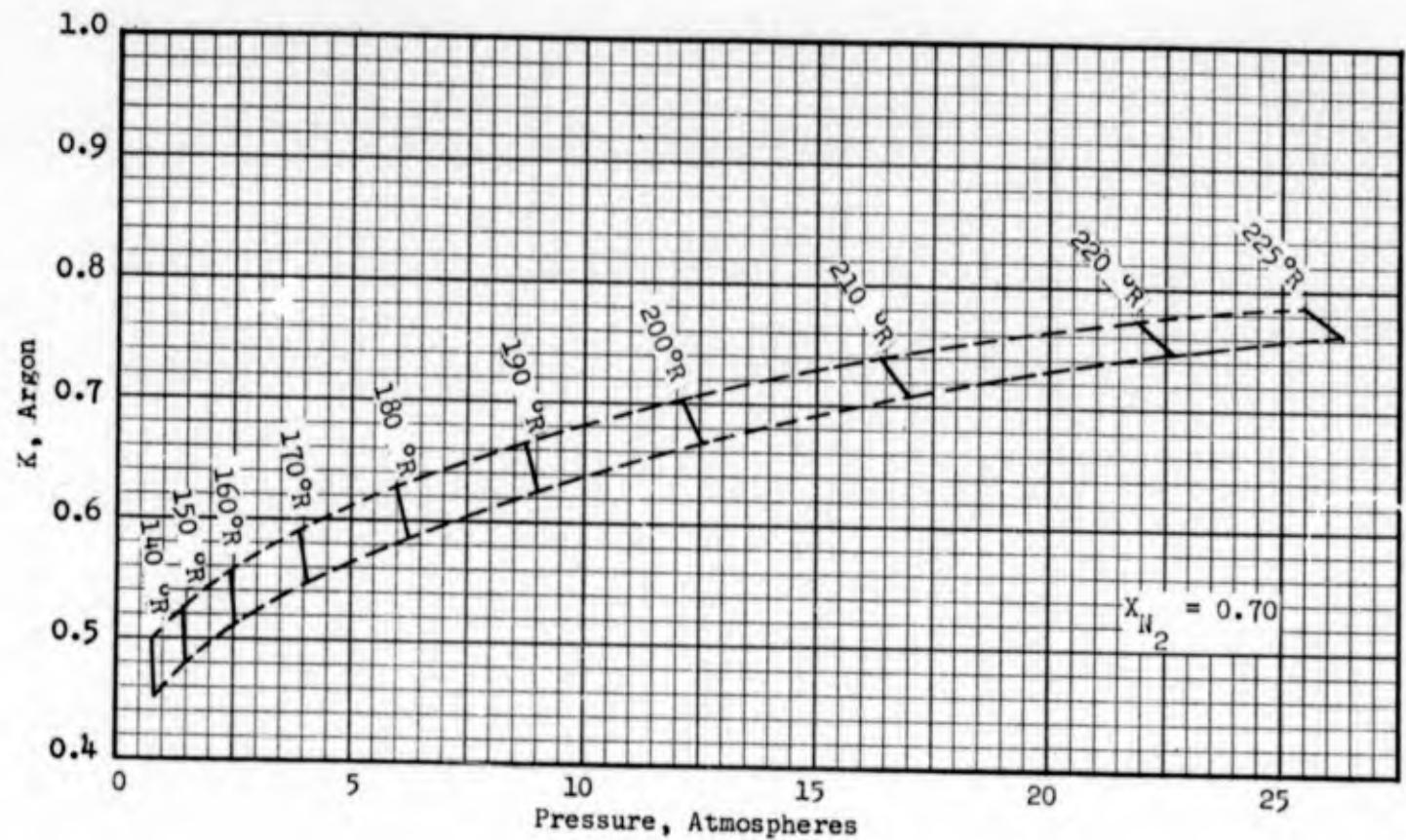


Figure 99. K-Values of Argon.

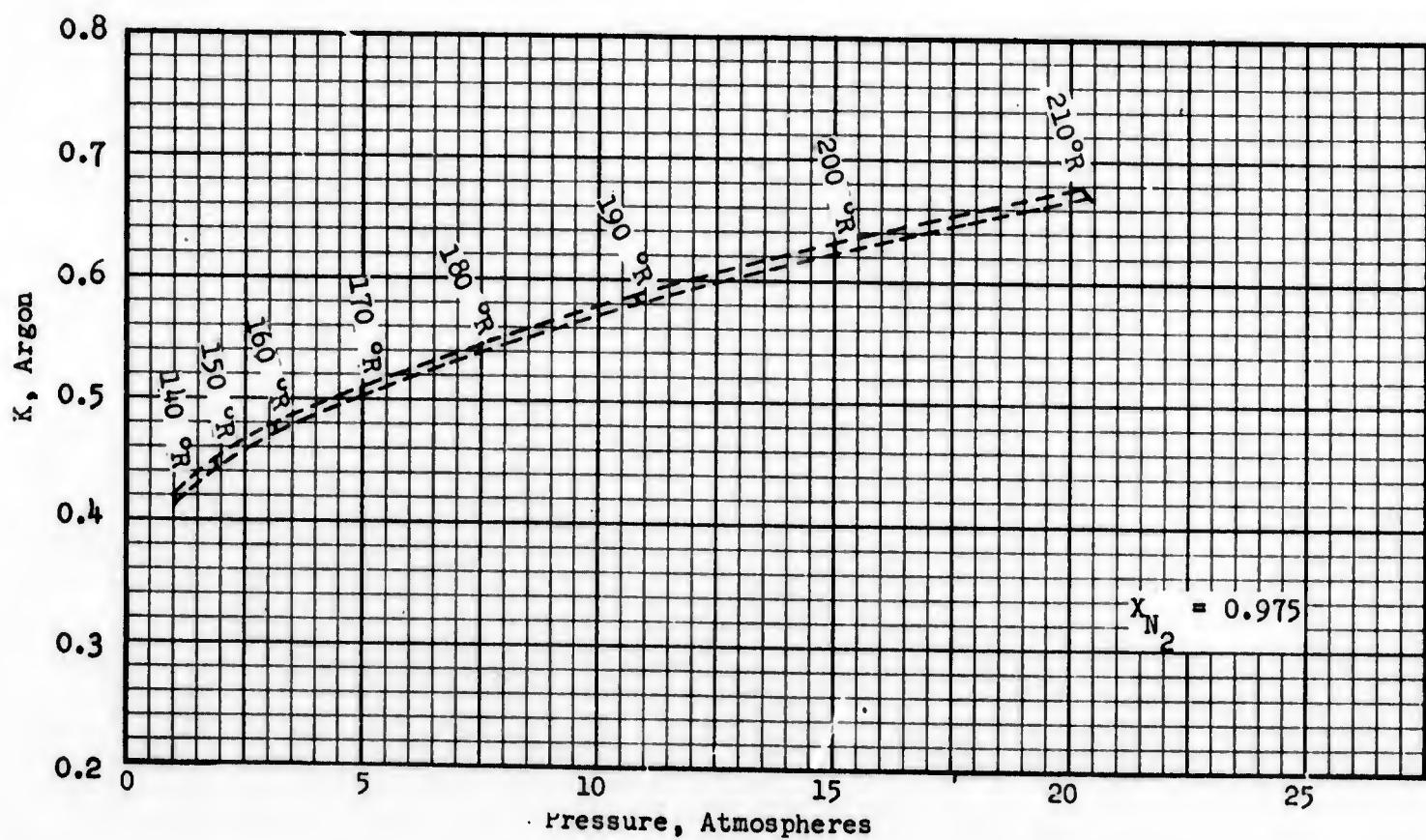
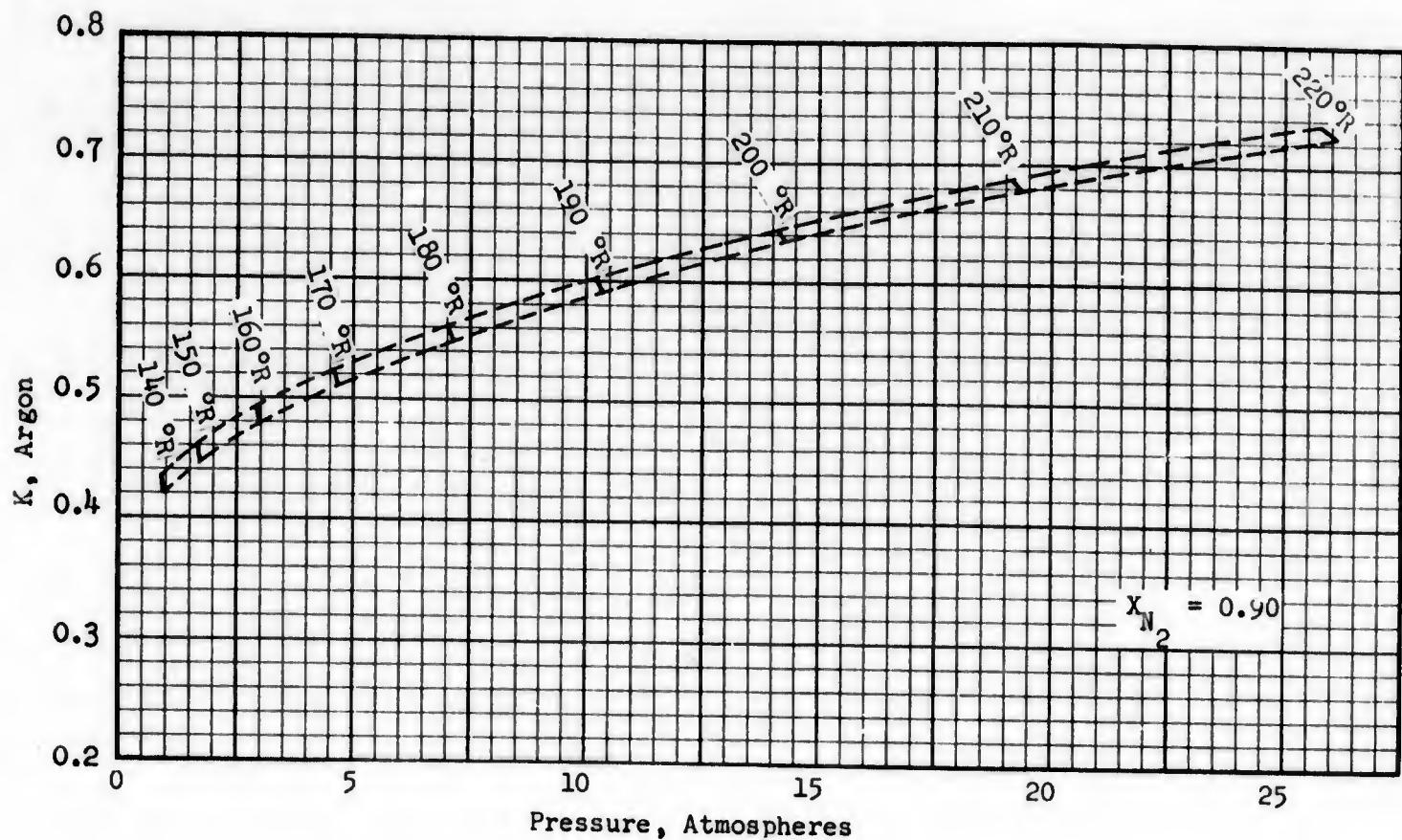


Figure 100. K-Values of Argon.

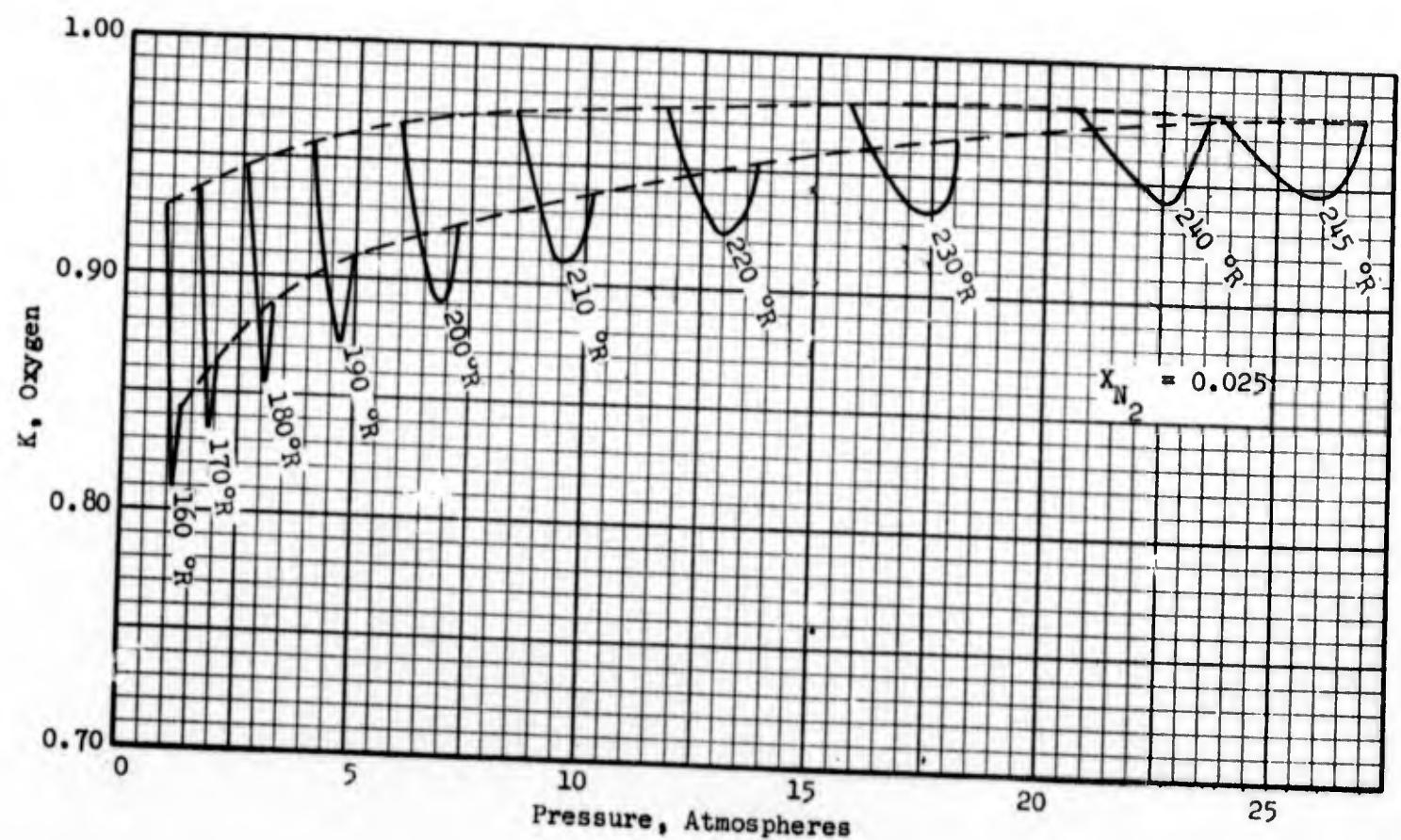
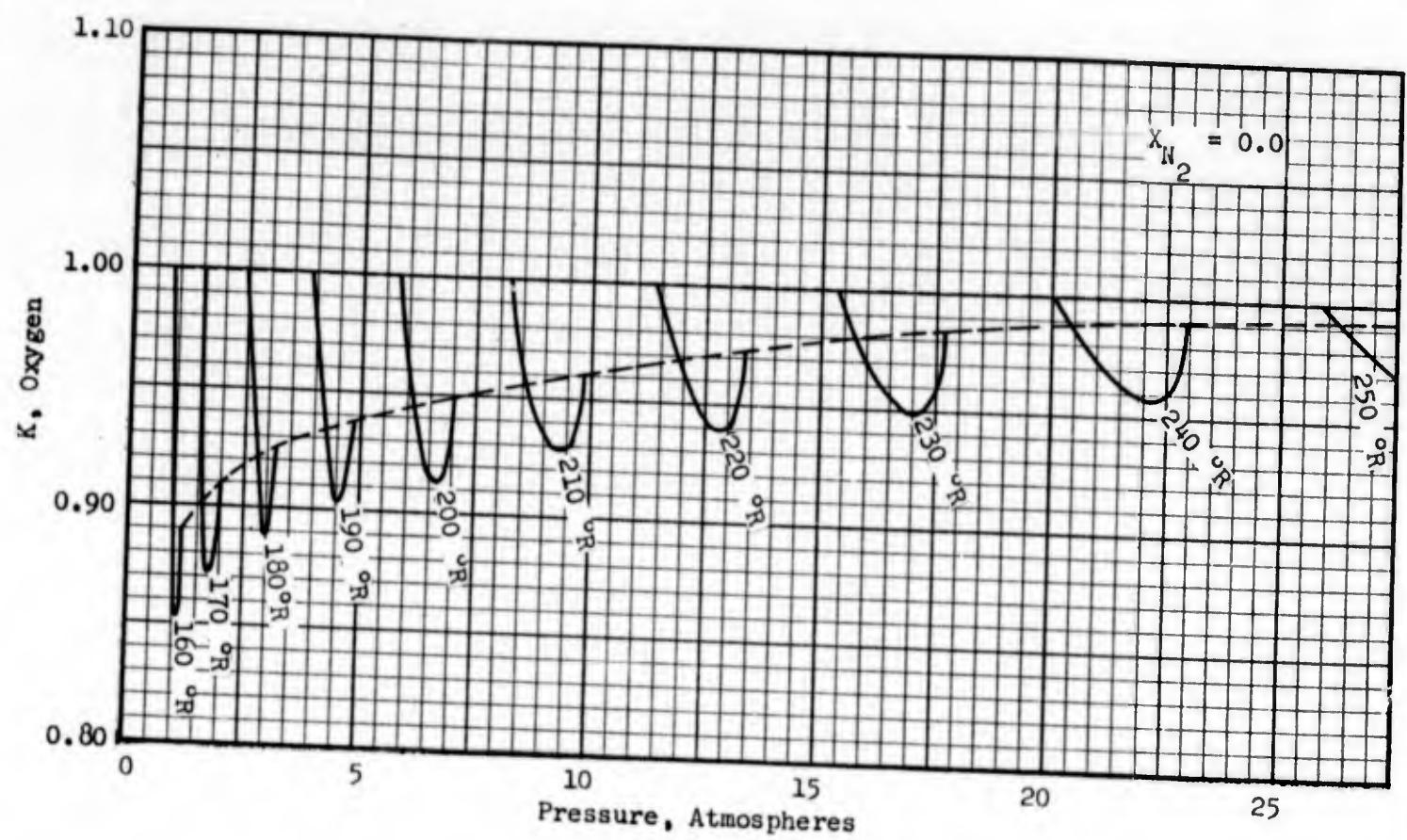


Figure 101. K-Values of Oxygen.

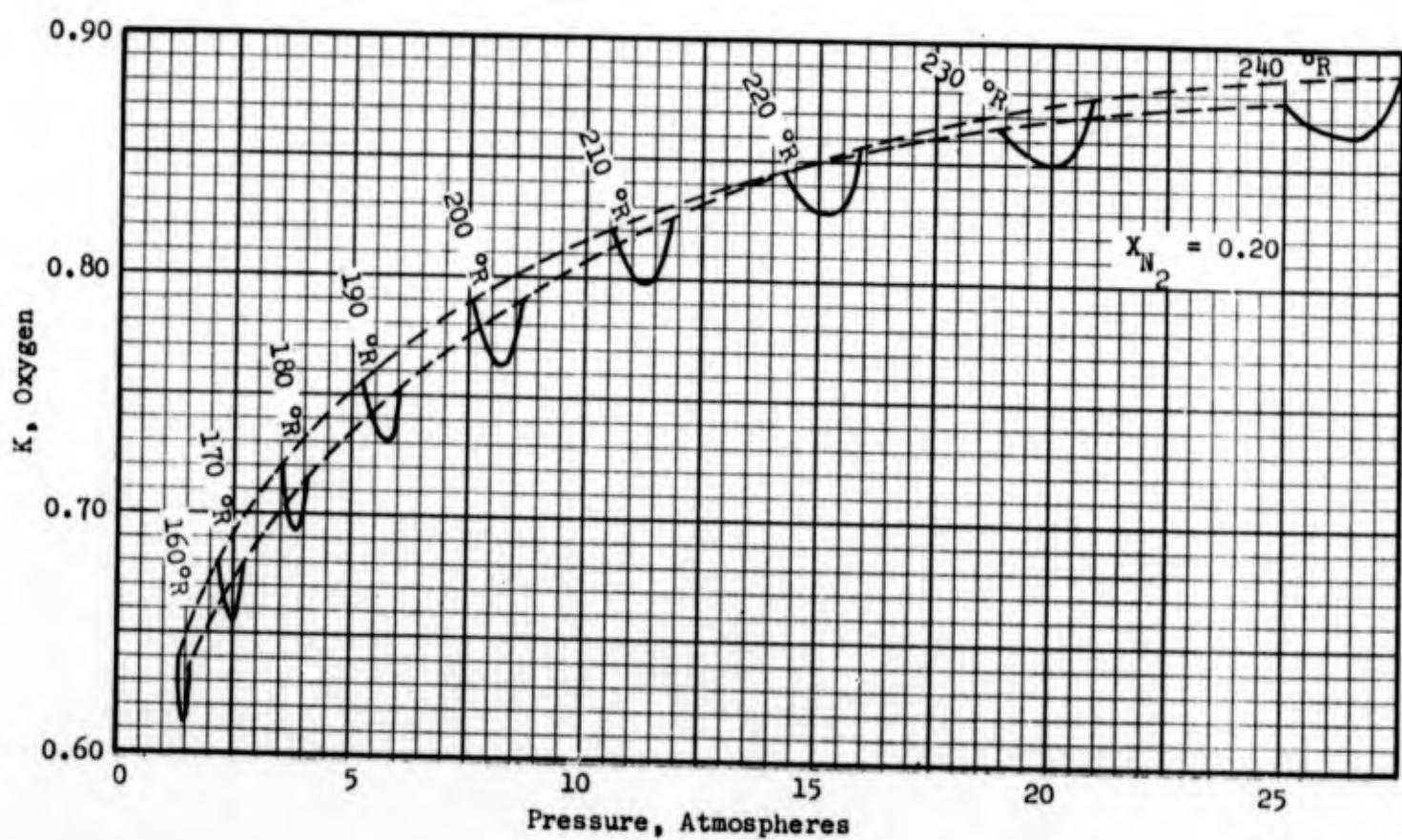
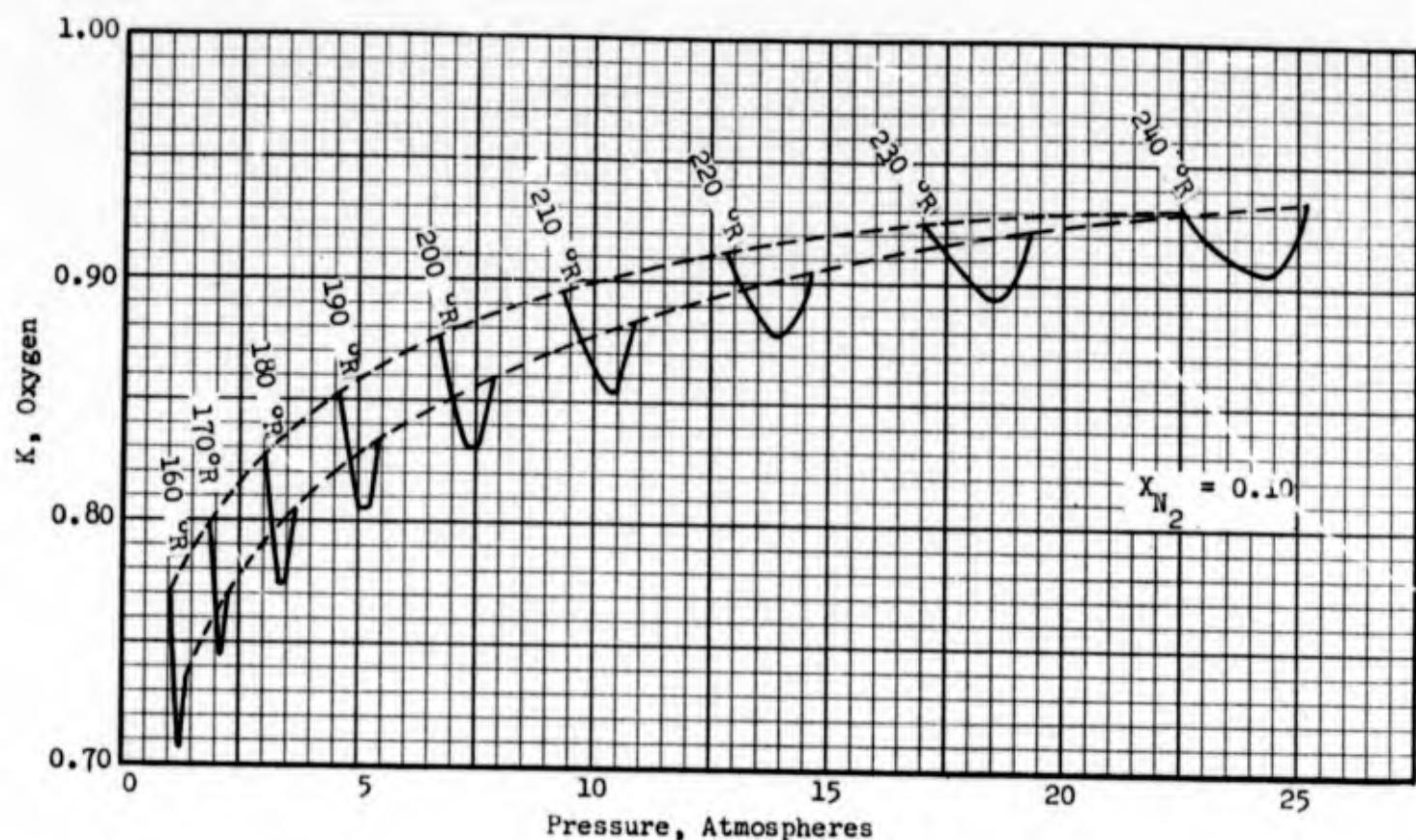


Figure 102. K-Values of Oxygen.

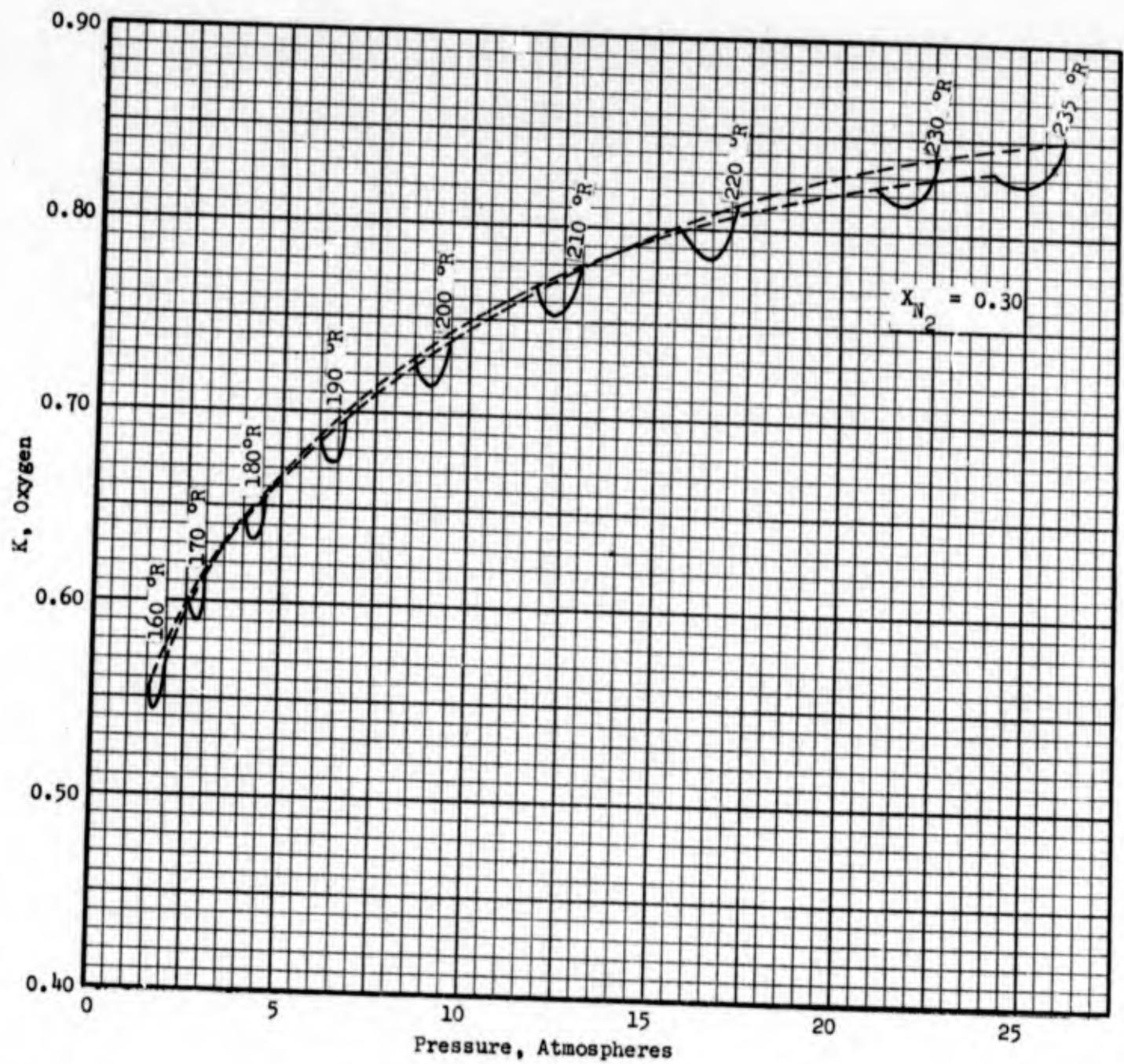


Figure 103. K-Values of Oxygen.

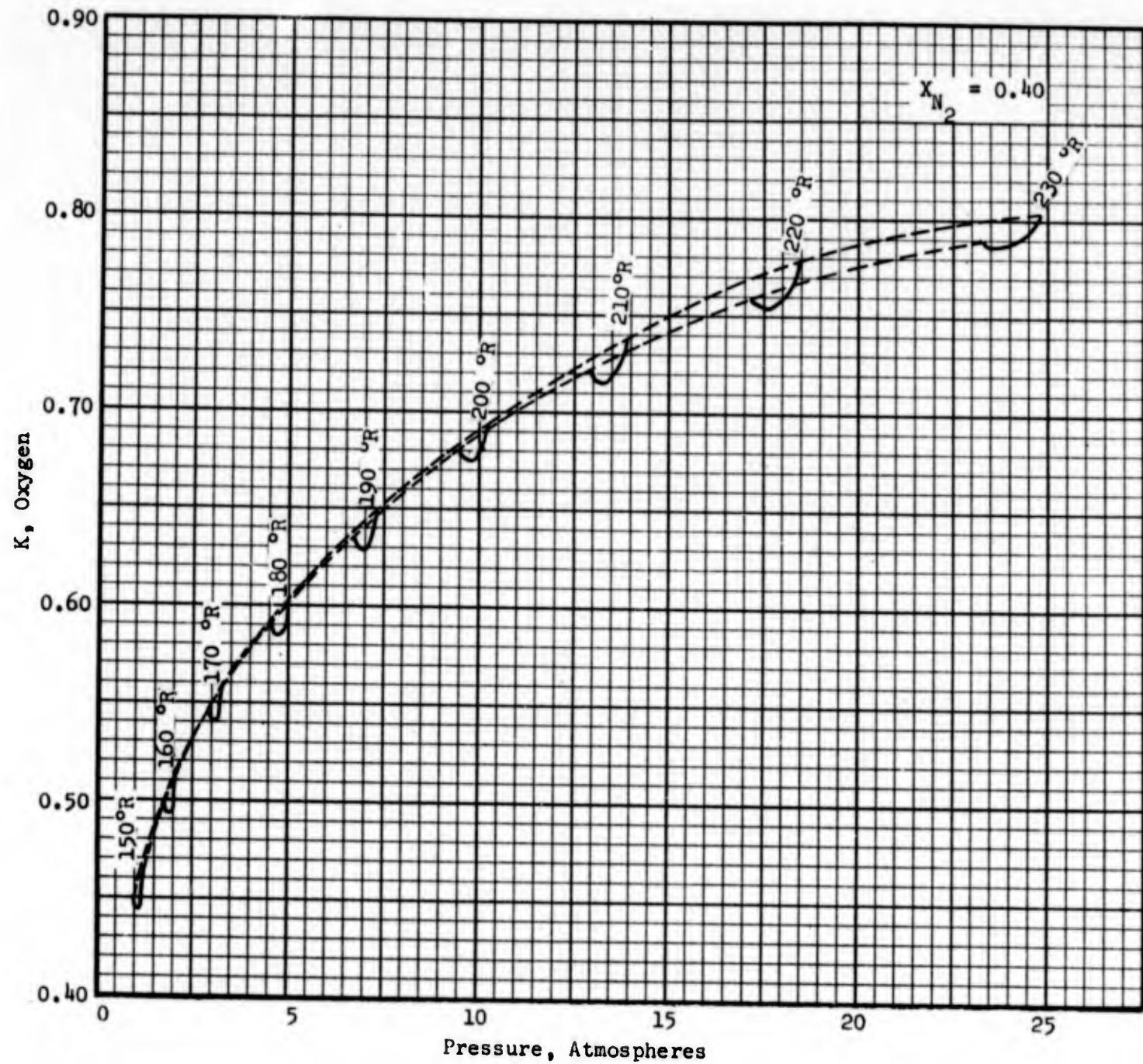


Figure 104. K-Values of Oxygen.

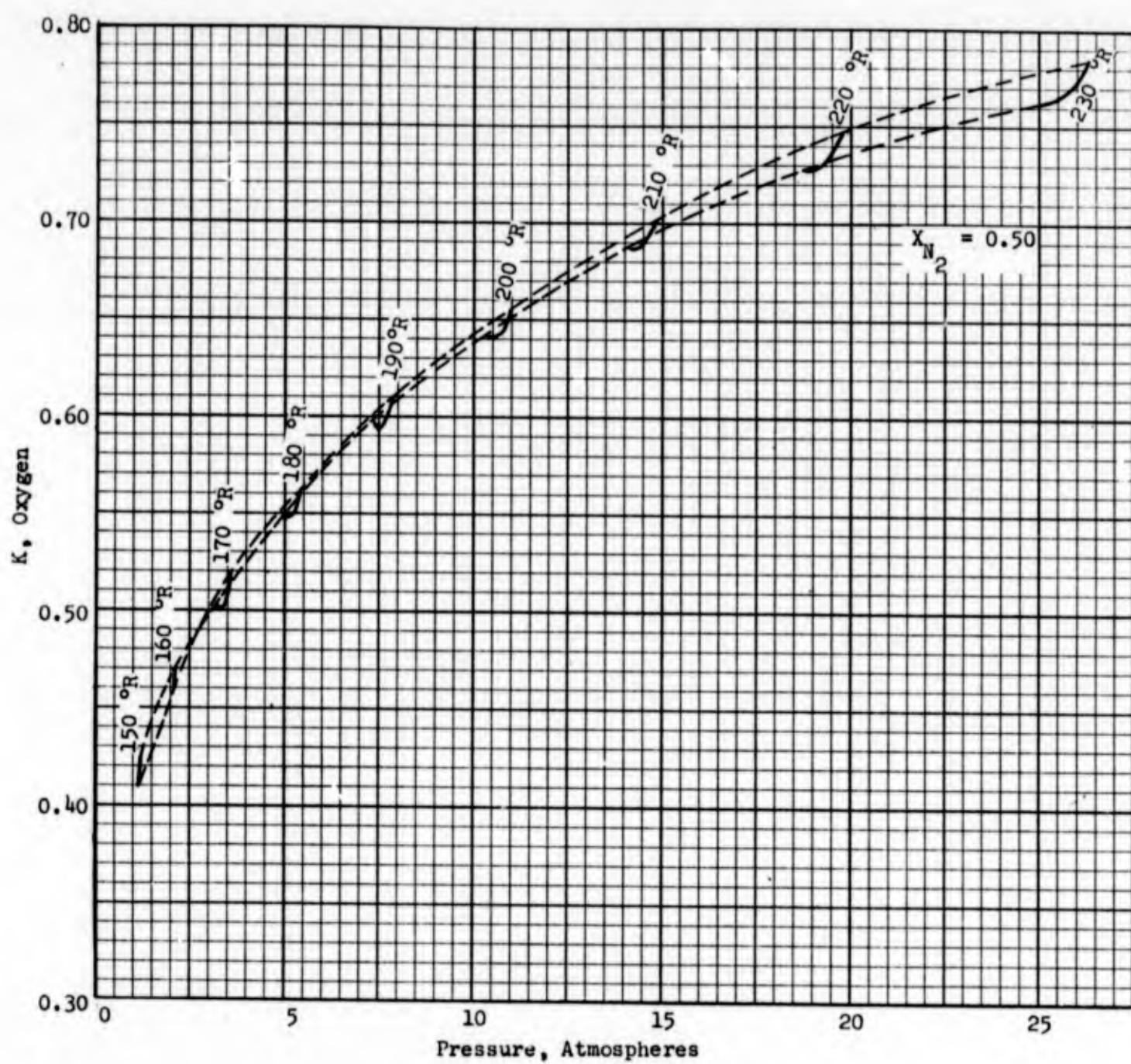


Figure 105. K-Values of Oxygen

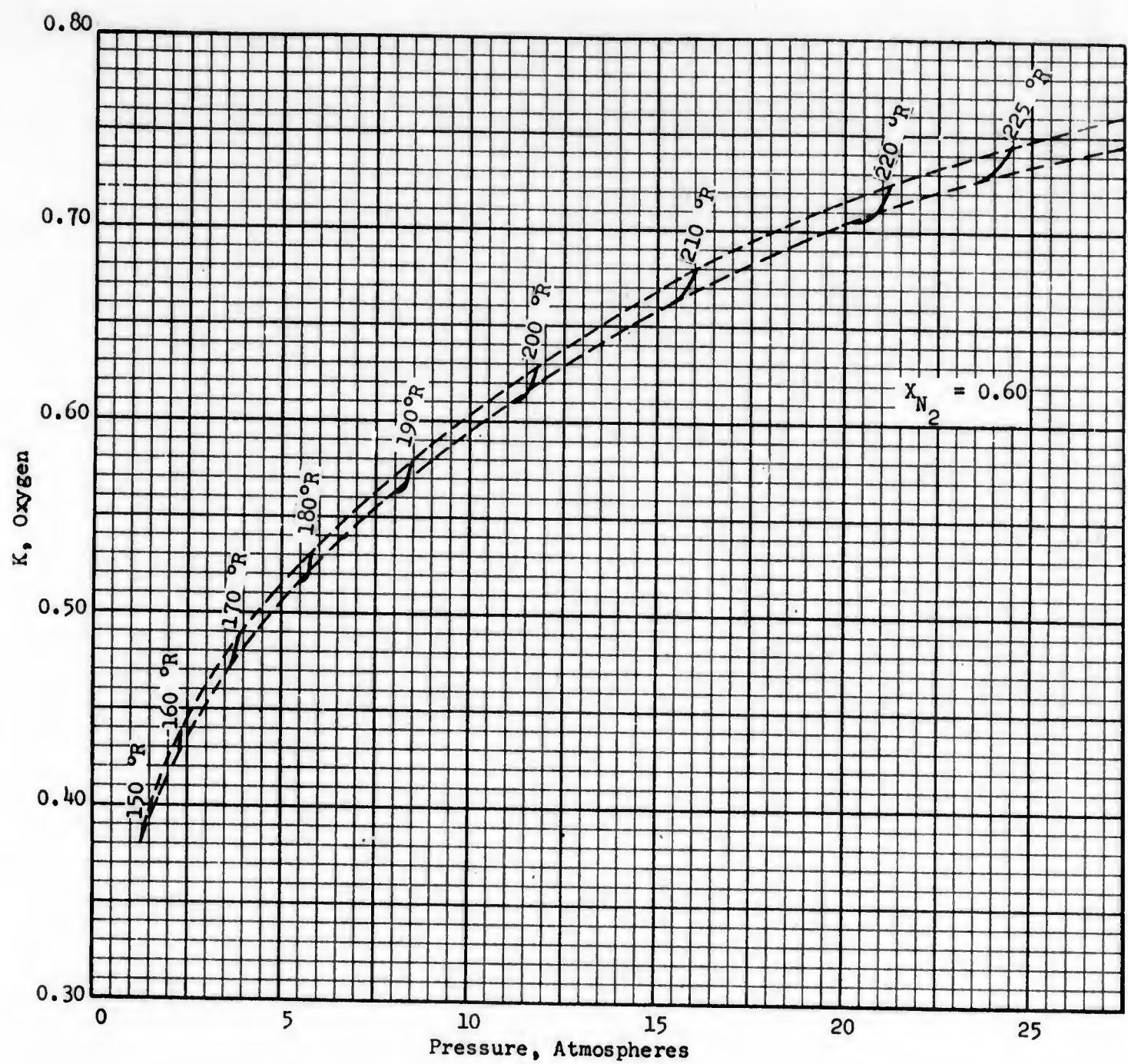


Figure 106. K-Values of Oxygen

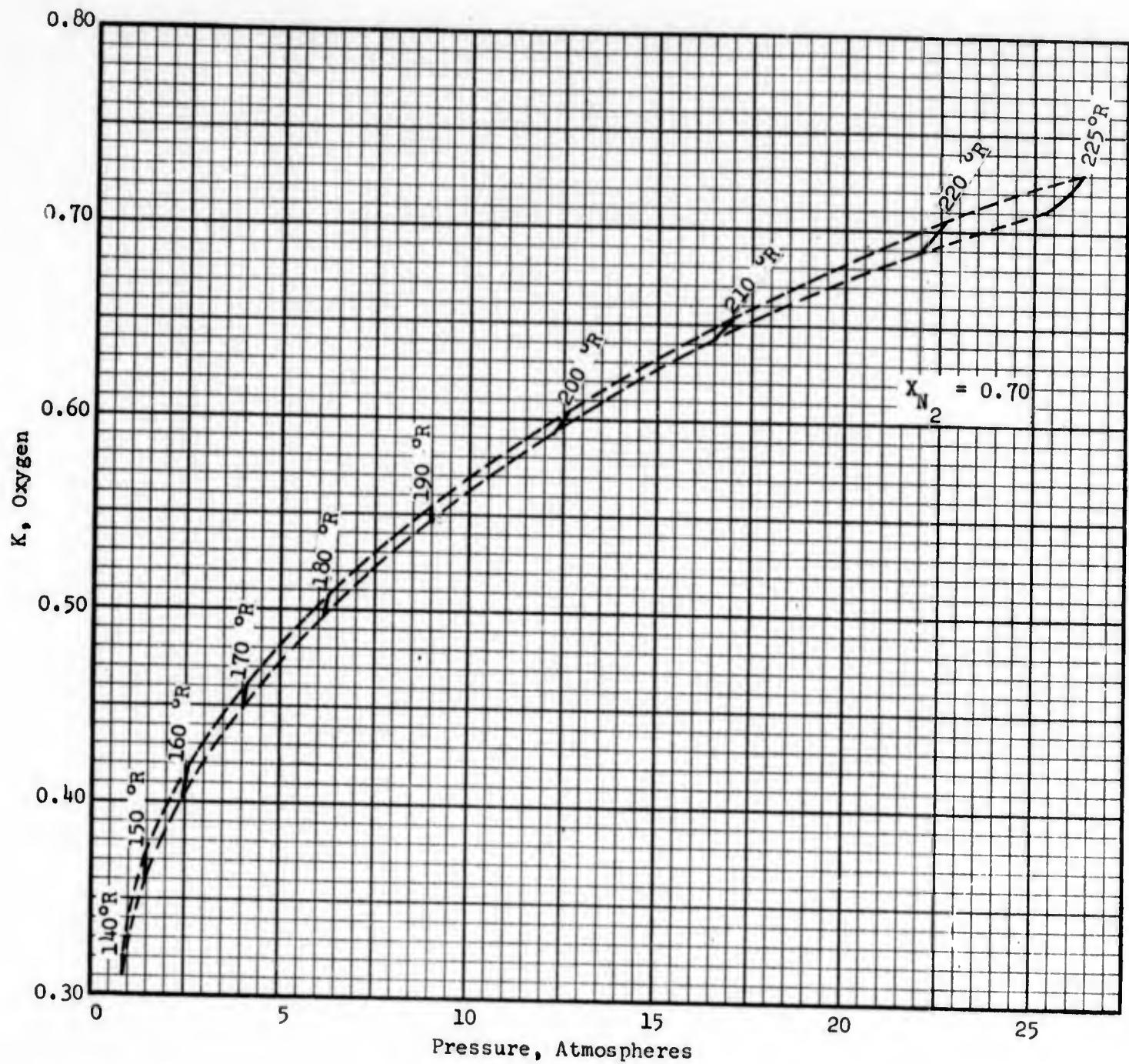


Figure 107. K-Values of Oxygen.

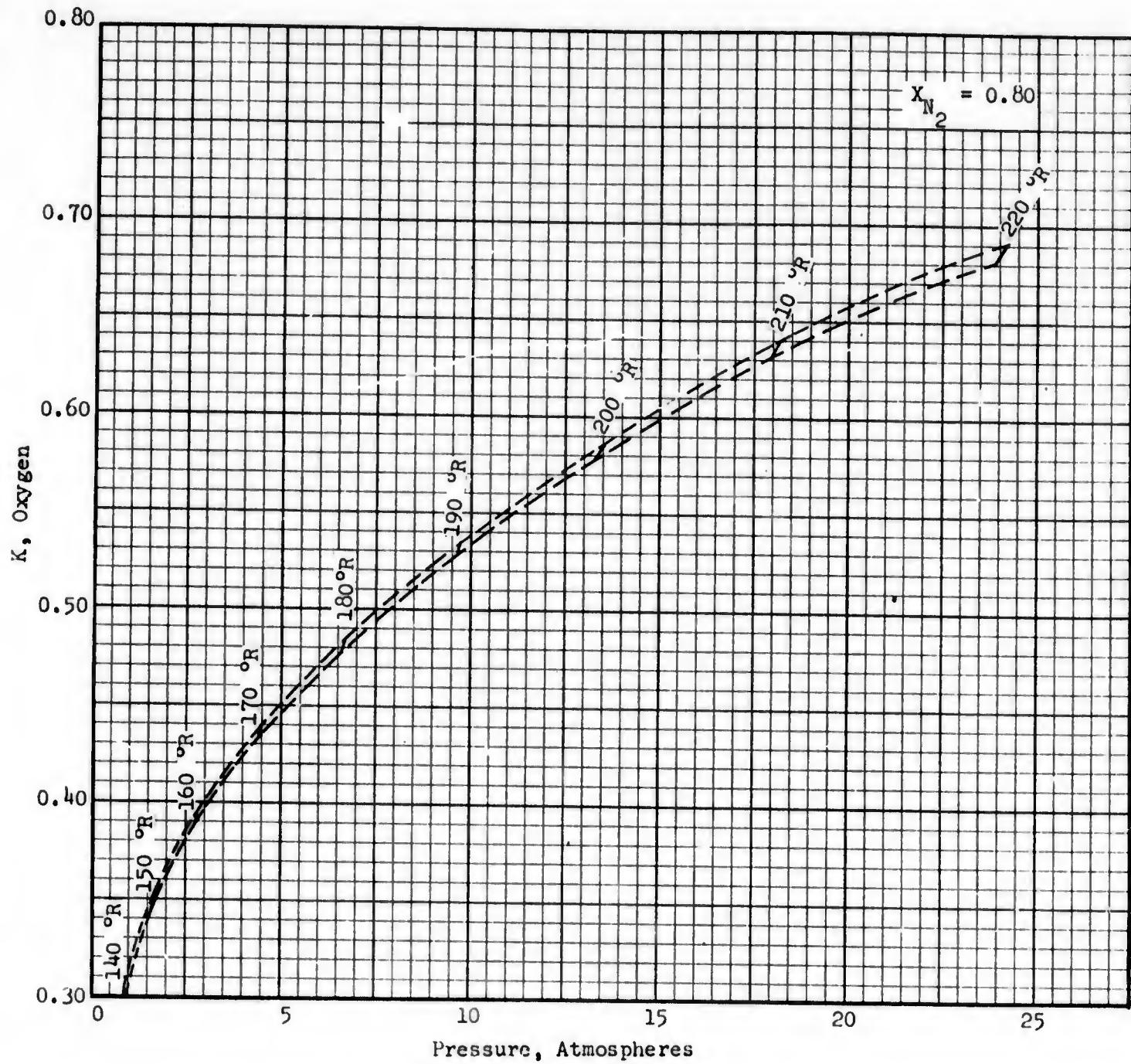


Figure 108. K-Values of Oxygen.

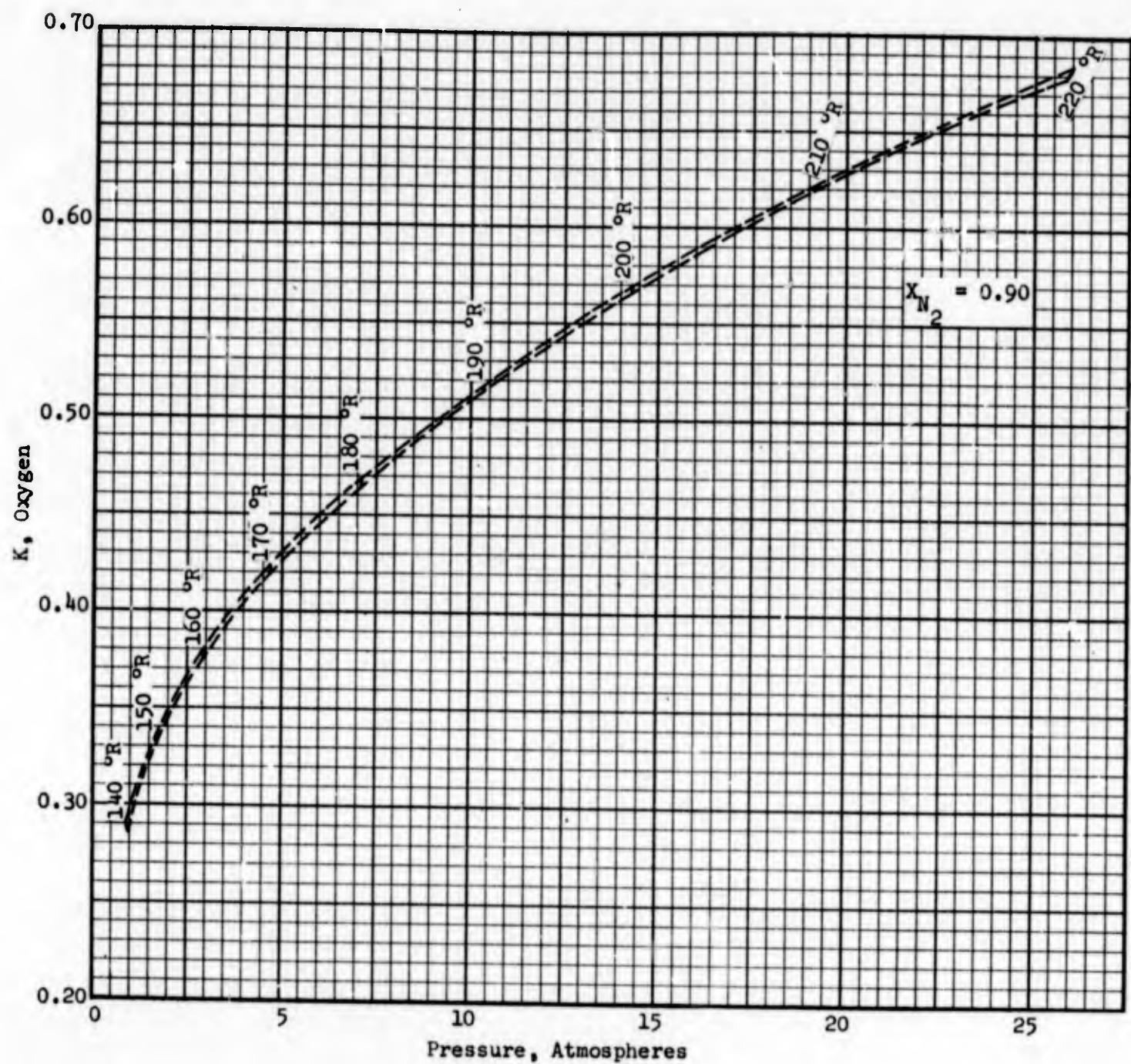


Figure 109. K-Values of Oxygen.

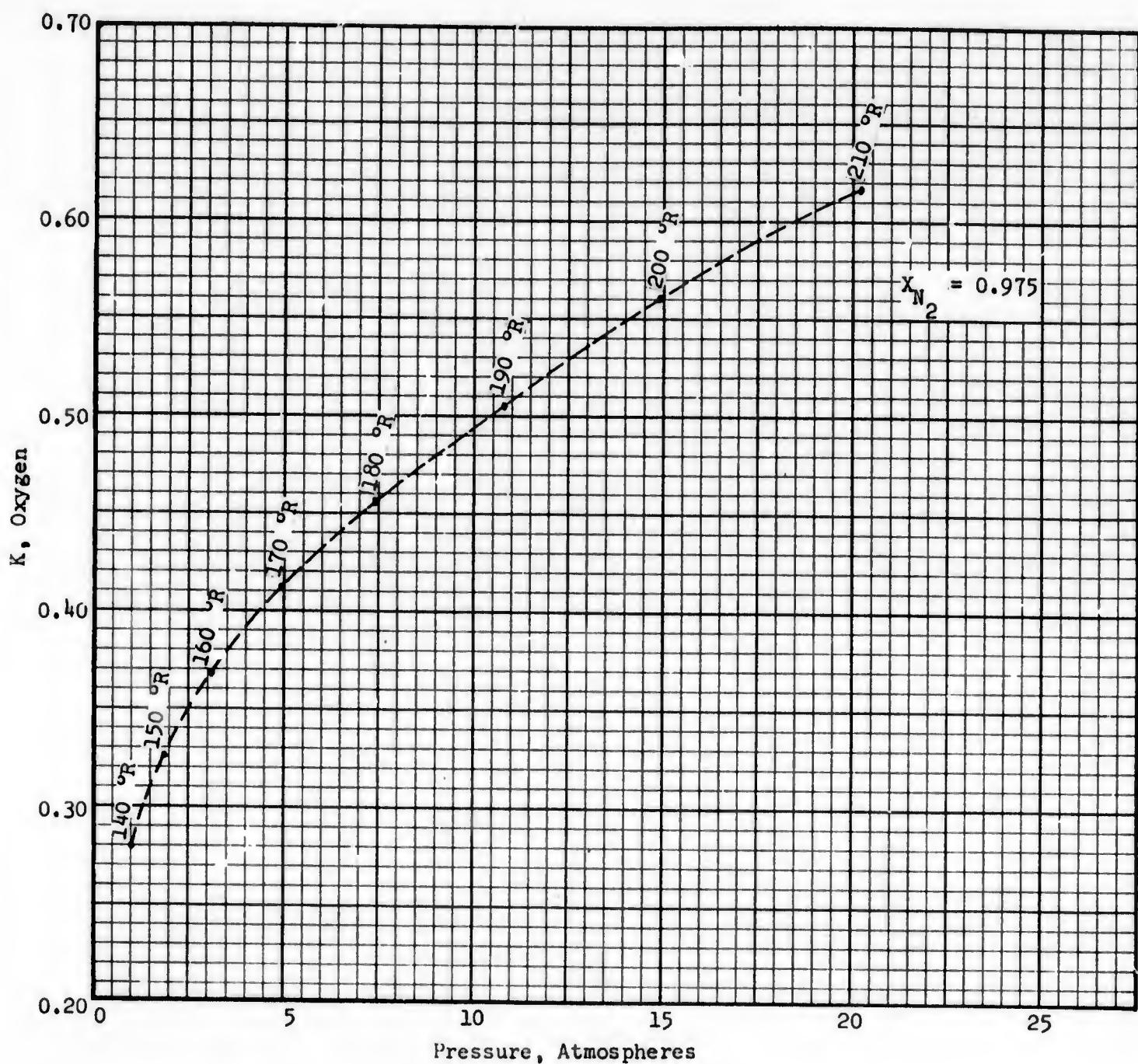


Figure 110. K-Values of Oxygen.

B. Relative Volatility of Argon to Nitrogen in Ternary System

The 12 graphs to follow present the relative volatility of argon to nitrogen defined

$$\alpha_{Ar-N_2} = \frac{y_{Ar}}{x_{Ar}} \cdot \frac{x_{N_2}}{y_{N_2}} \quad (51)$$

as a function of mole fraction argon in the liquid along selected isobars. The graphs are arranged in order of increasing mole percent nitrogen in the liquid.

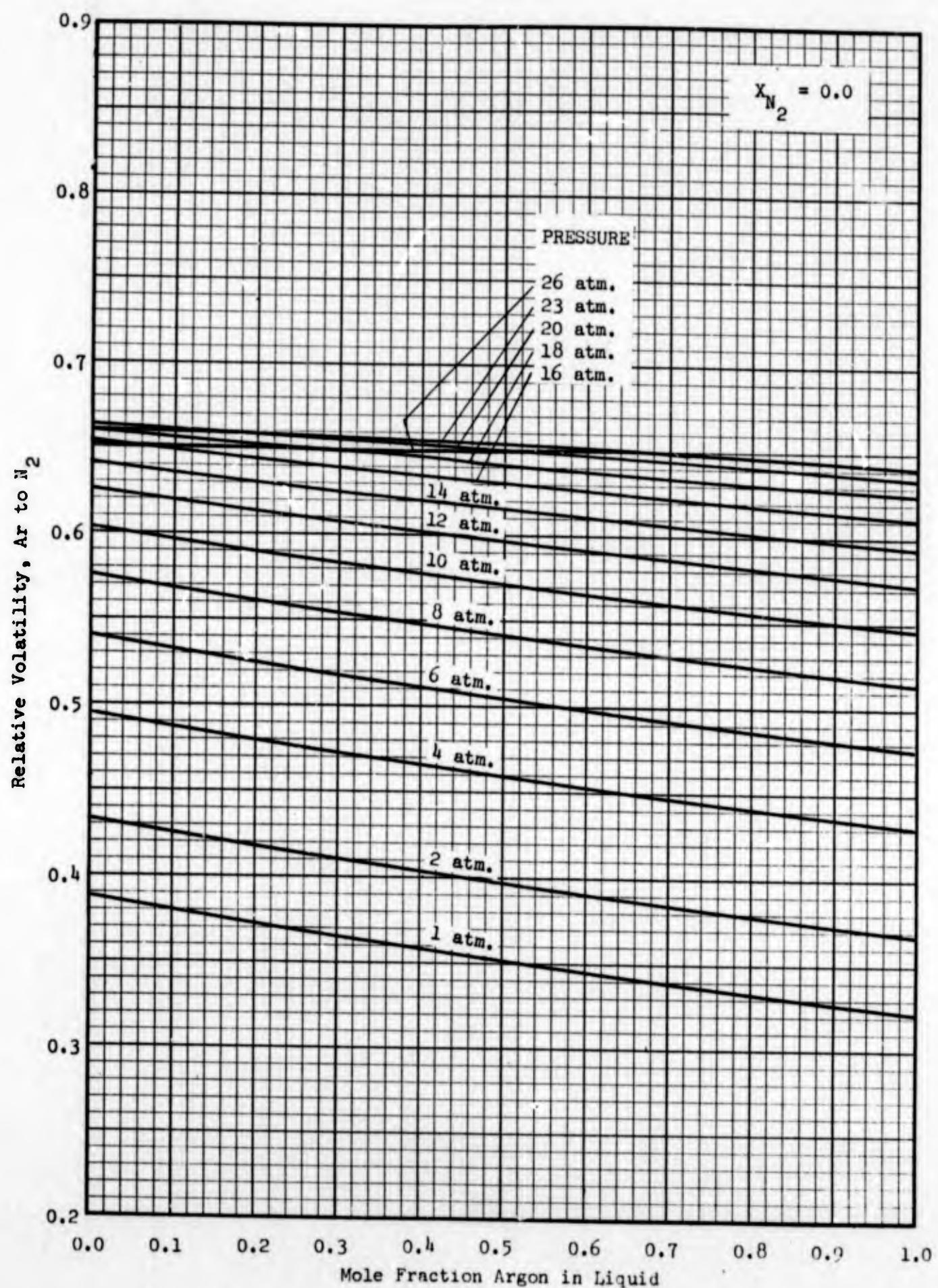


Figure III. Relative Volatility of Argon to Nitrogen.

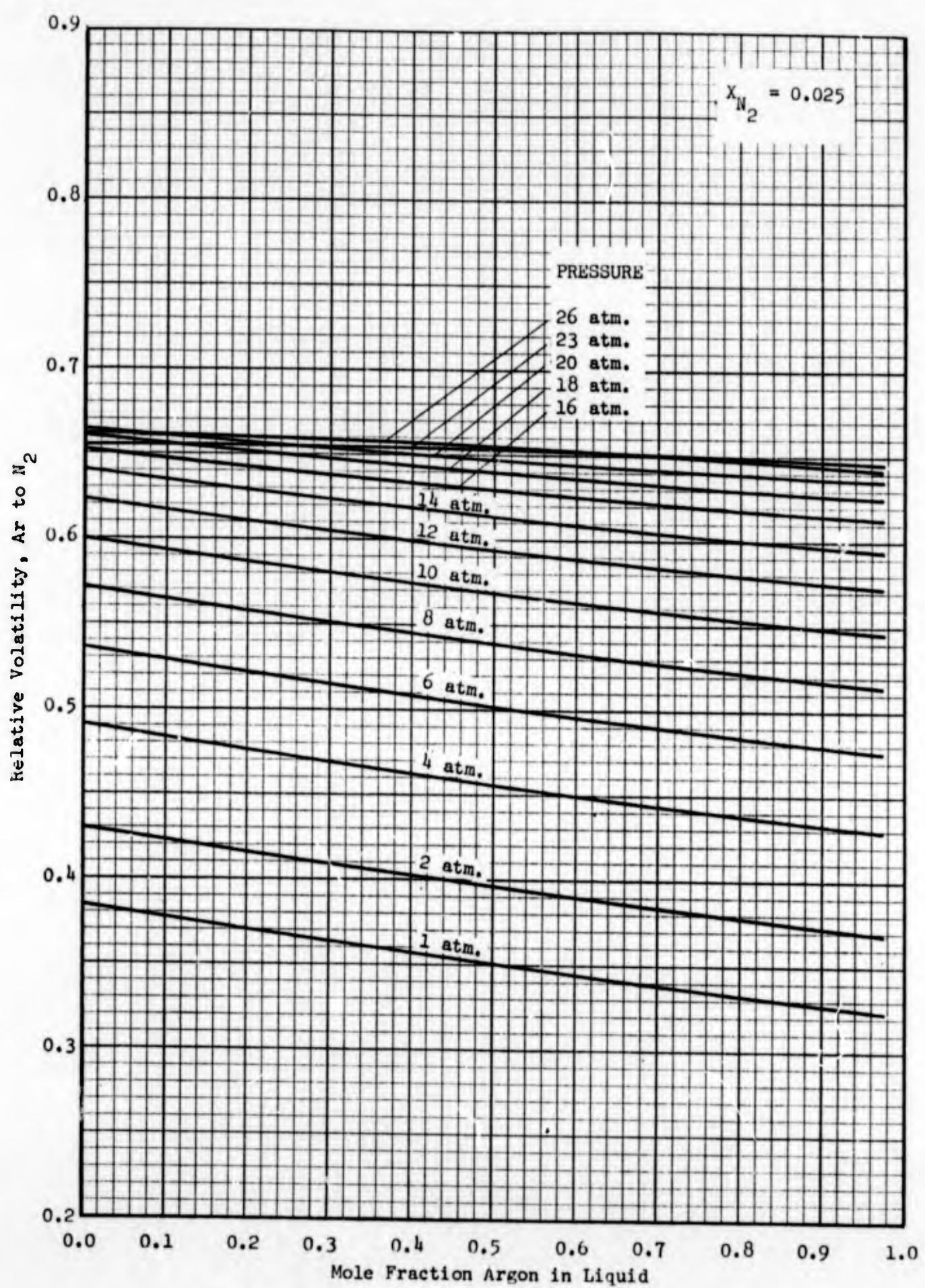


Figure 112. Relative Volatility of Argon to Nitrogen.

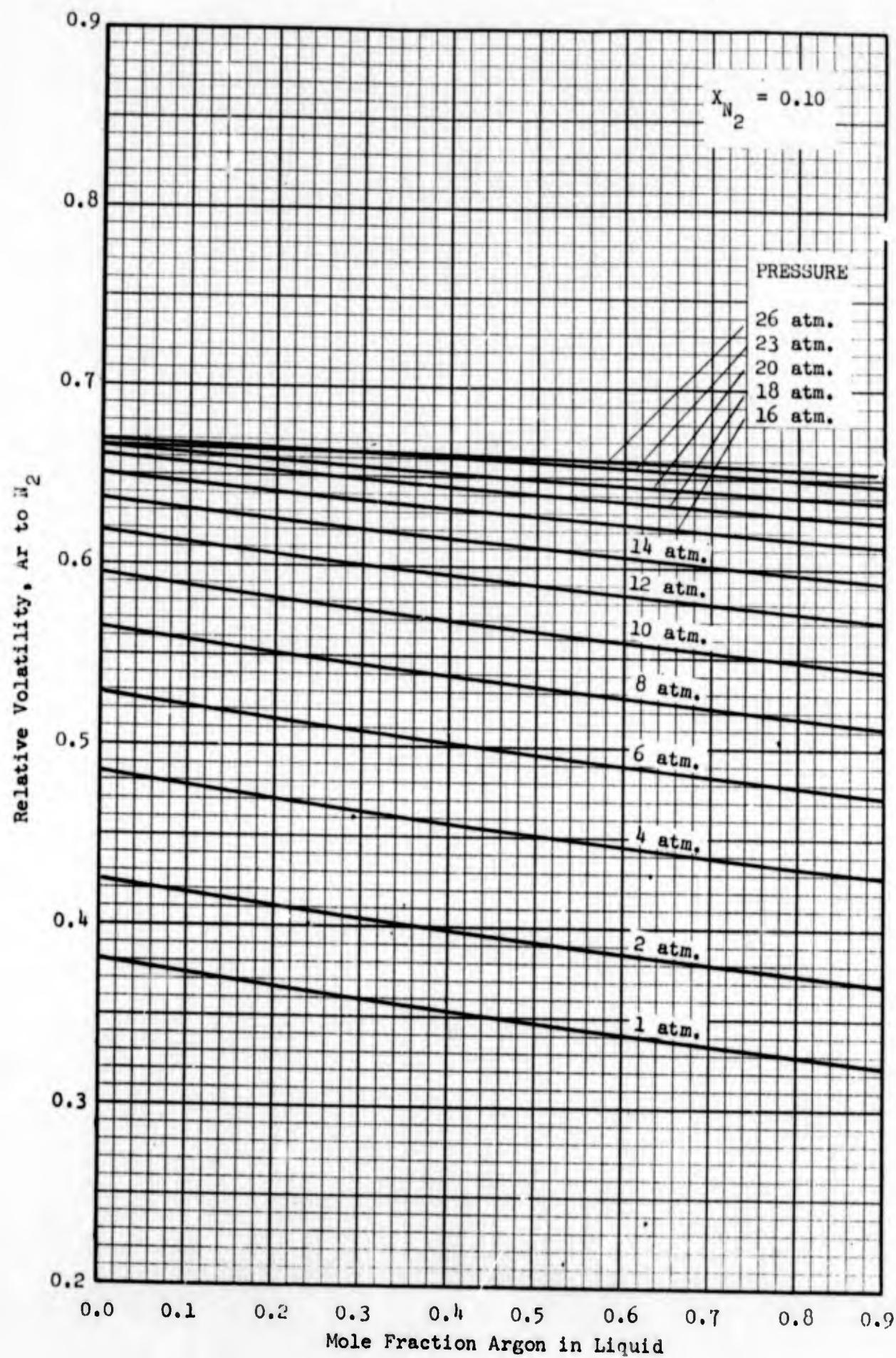


Figure 113. Relative Volatility of Argon to Nitrogen.

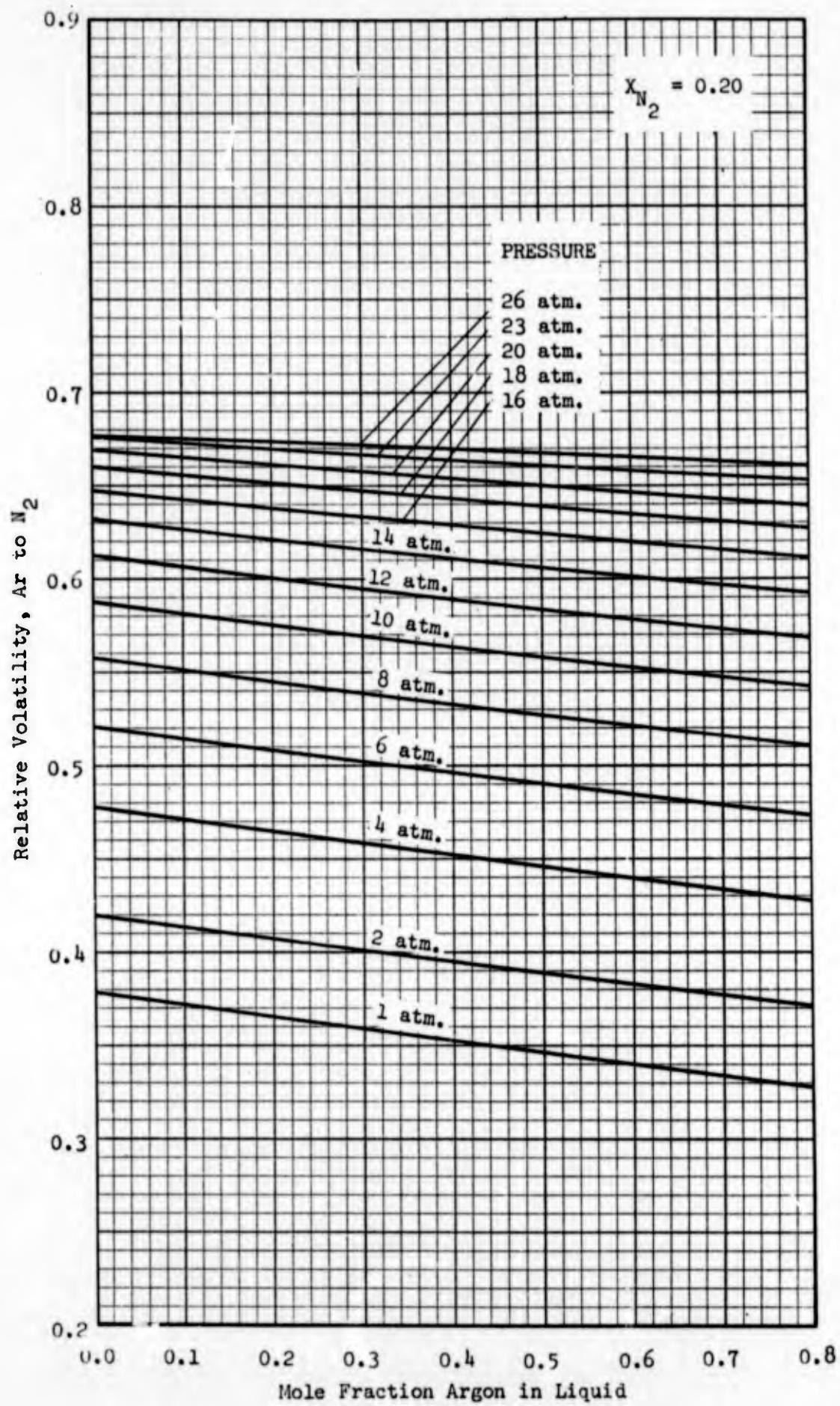


Figure 114. Relative Volatility of Argon to Nitrogen.

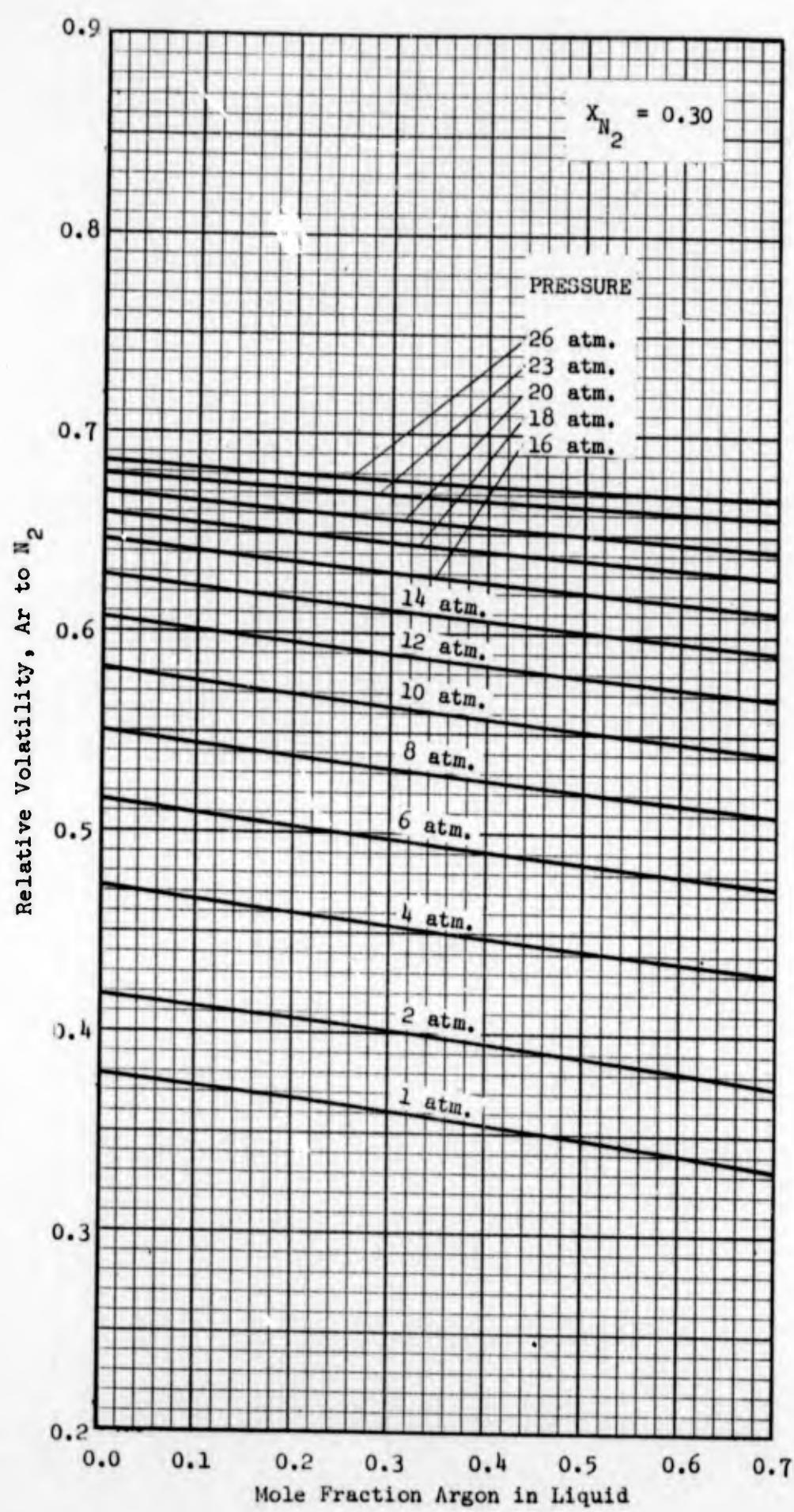


Figure 115. Relative Volatility of Argon to Nitrogen.

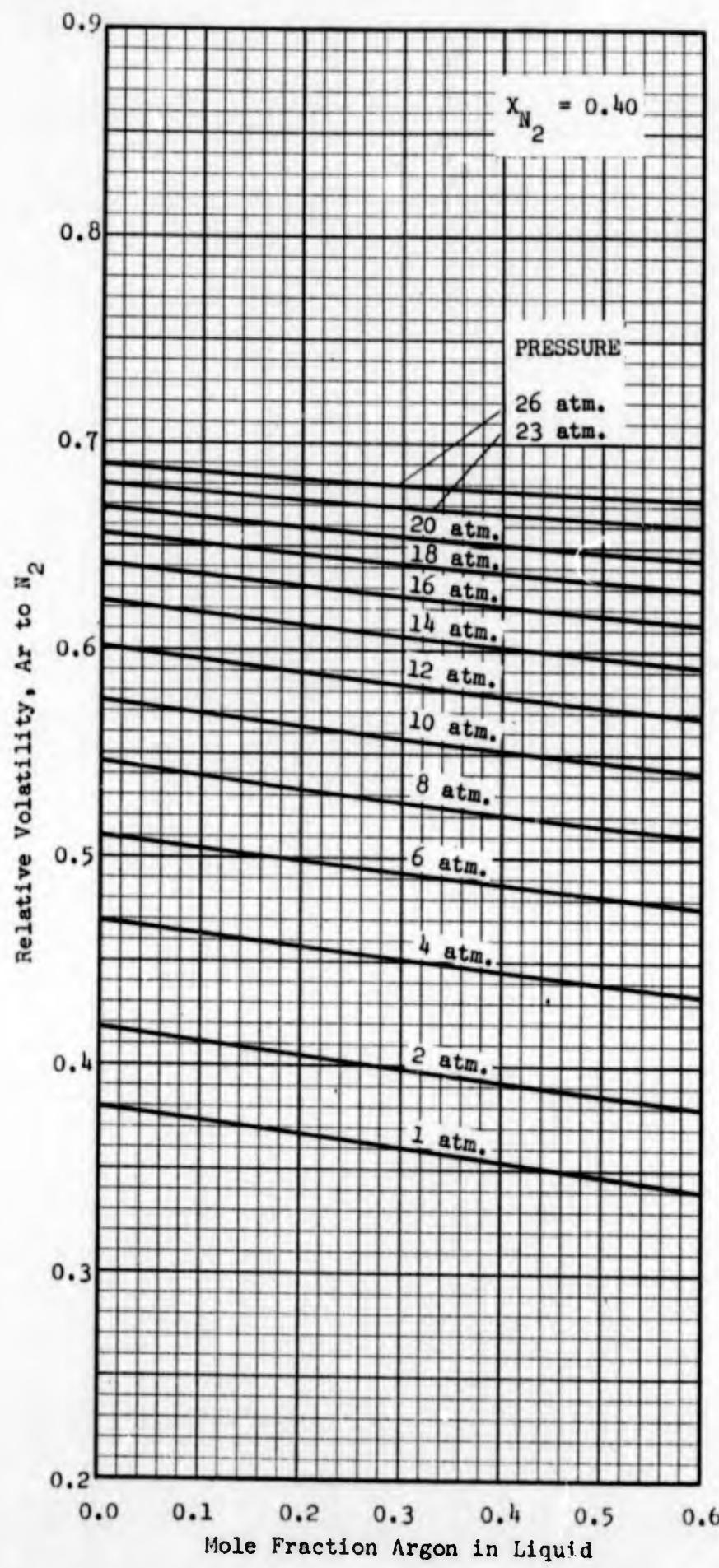


Figure 116. Relative Volatility of Argon to Nitrogen.

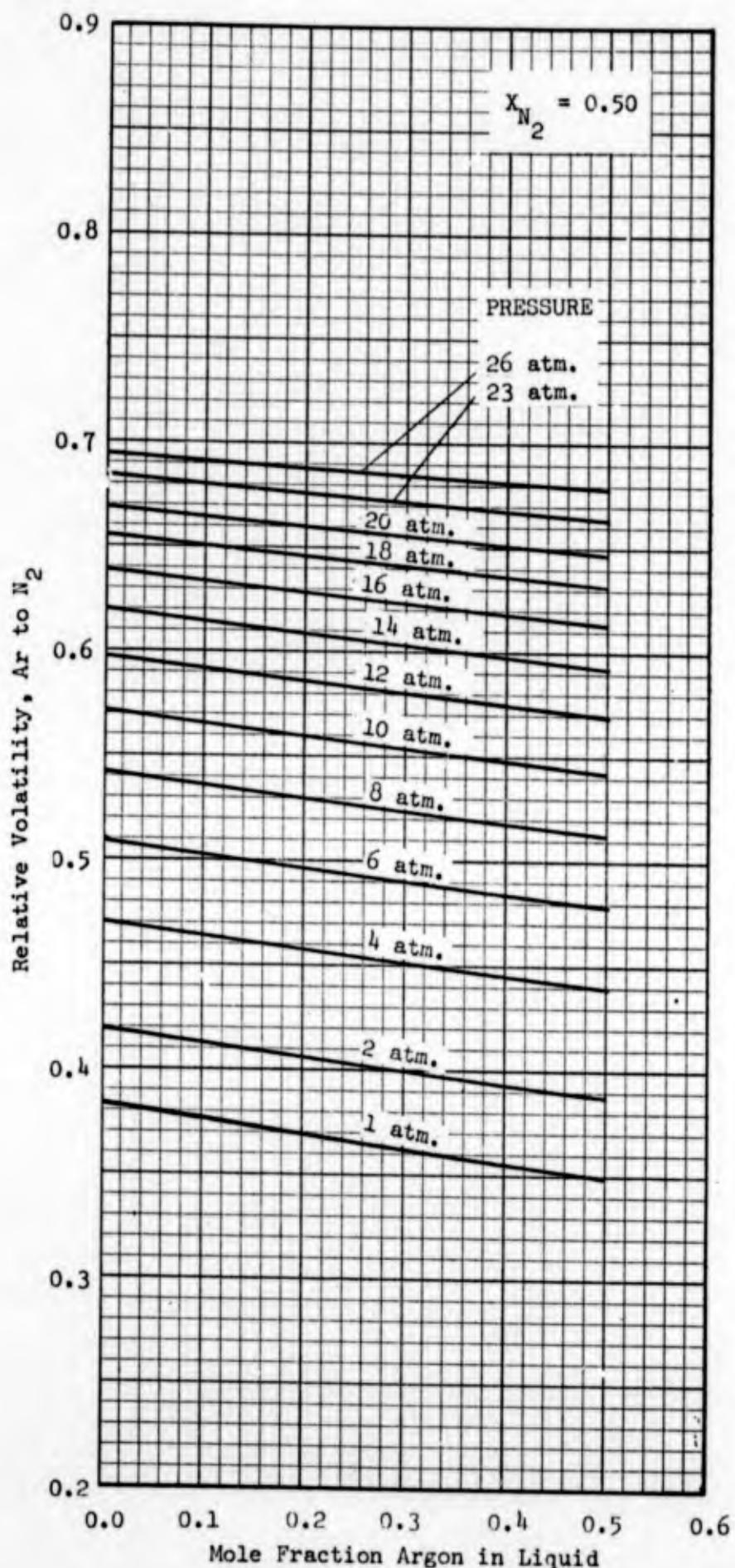


Figure 117. Relative Volatility of Argon to Nitrogen.

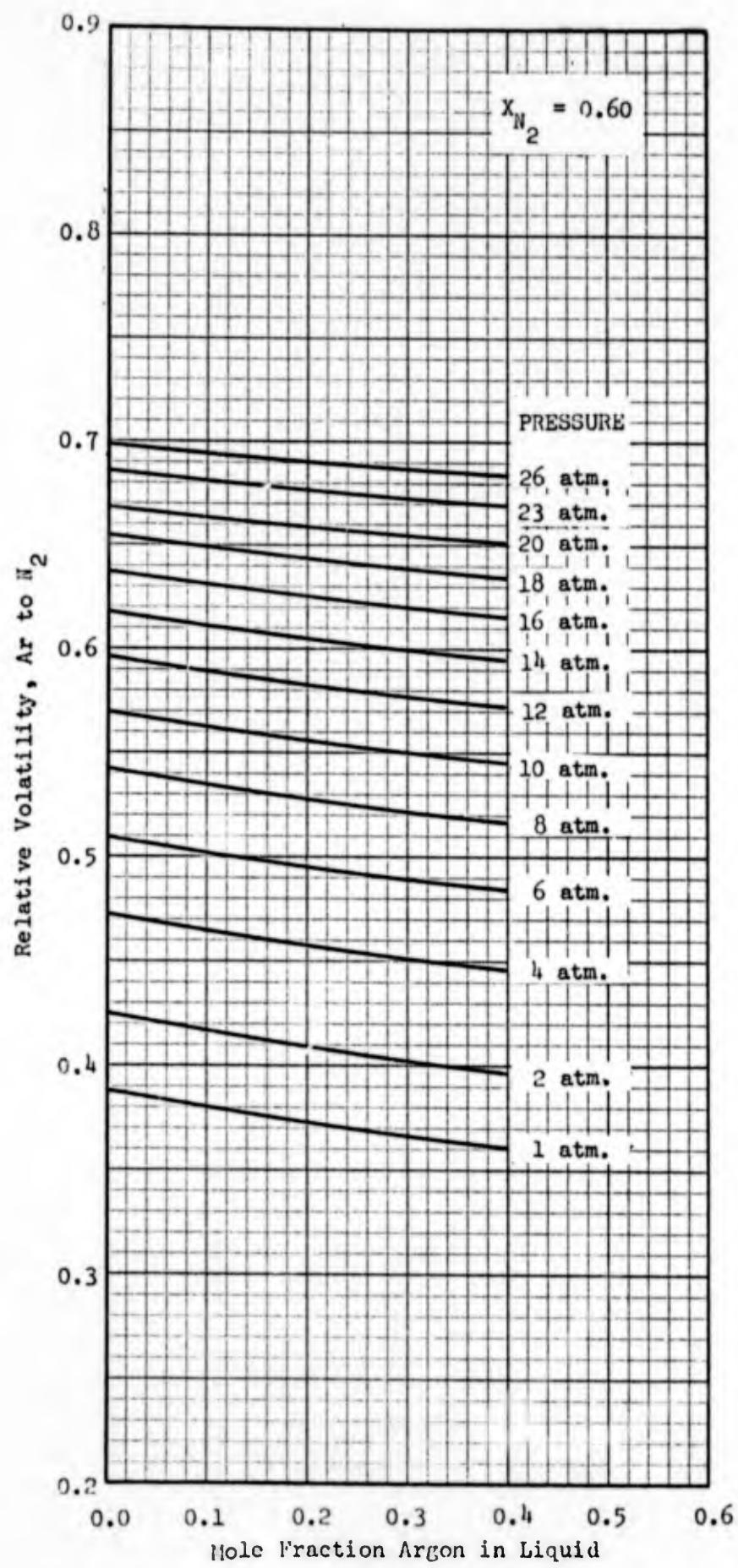


Figure 118. Relative Volatility of Argon to Nitrogen.

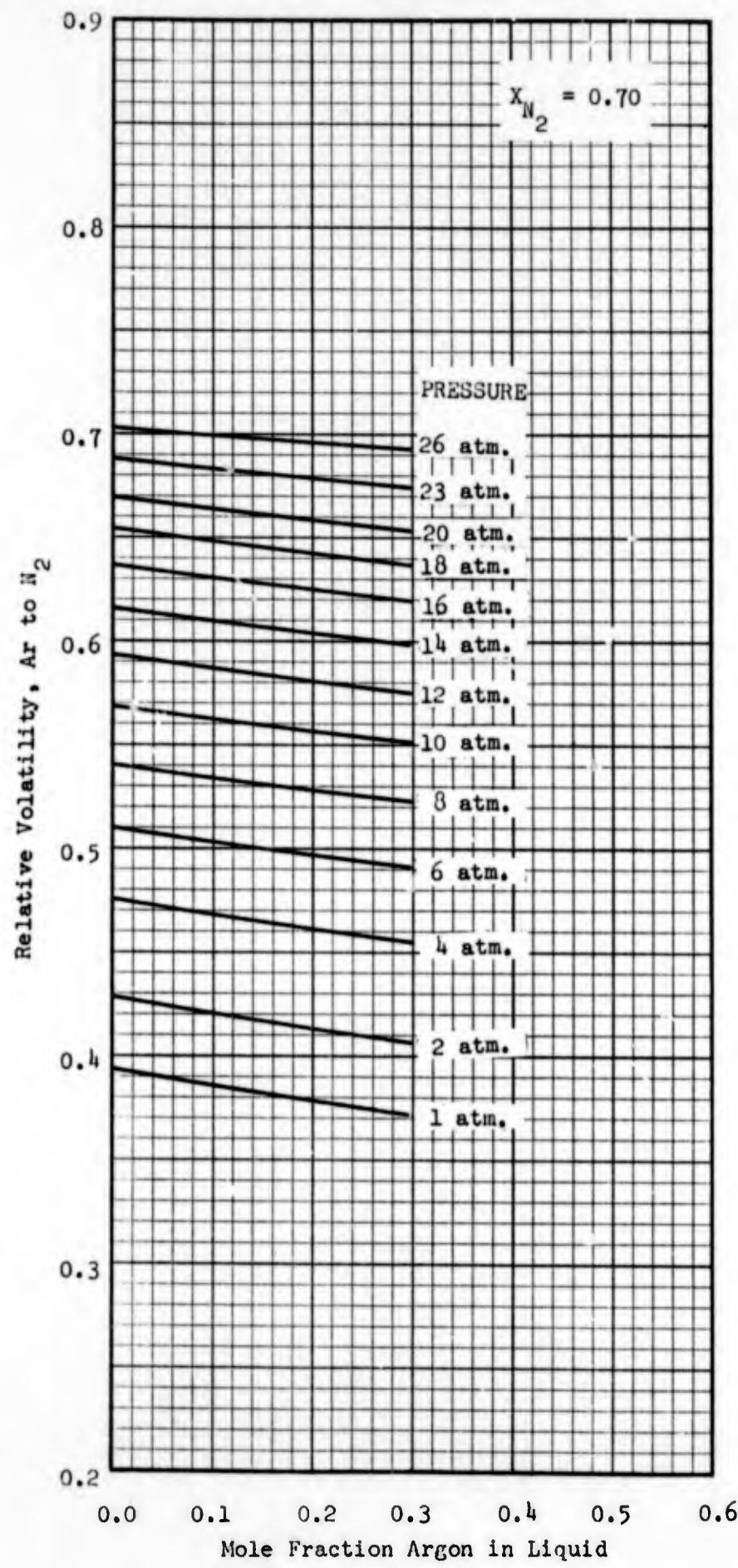


Figure 119. Relative Volatility of Argon to Nitrogen.

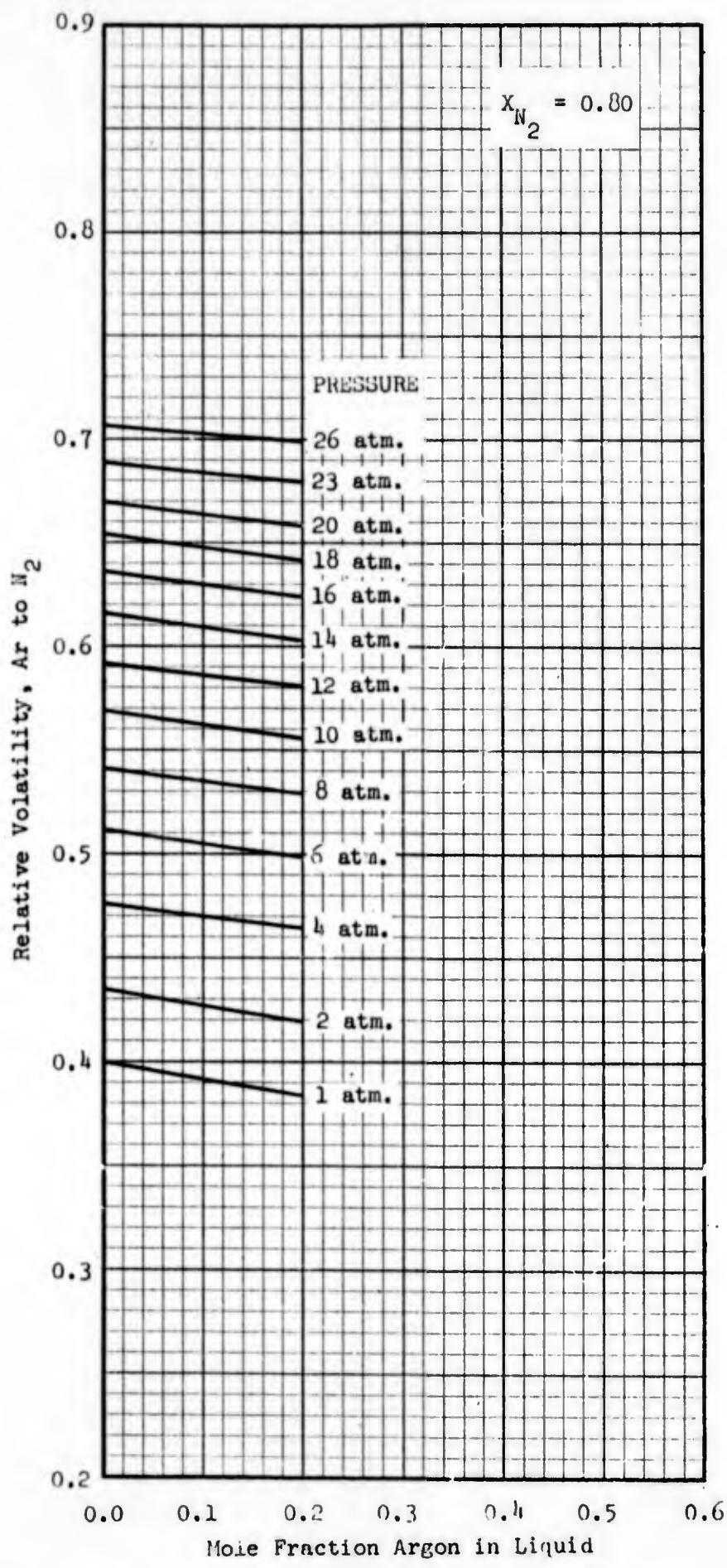


Figure 120. Relative Volatility of Argon to Nitrogen.

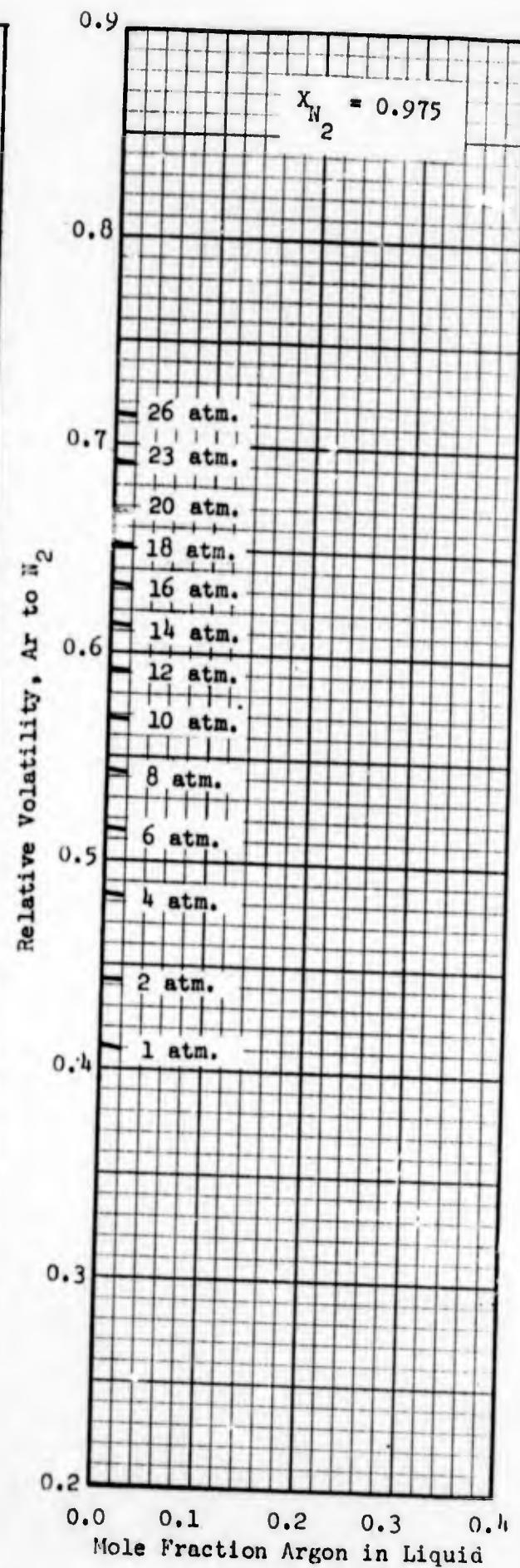
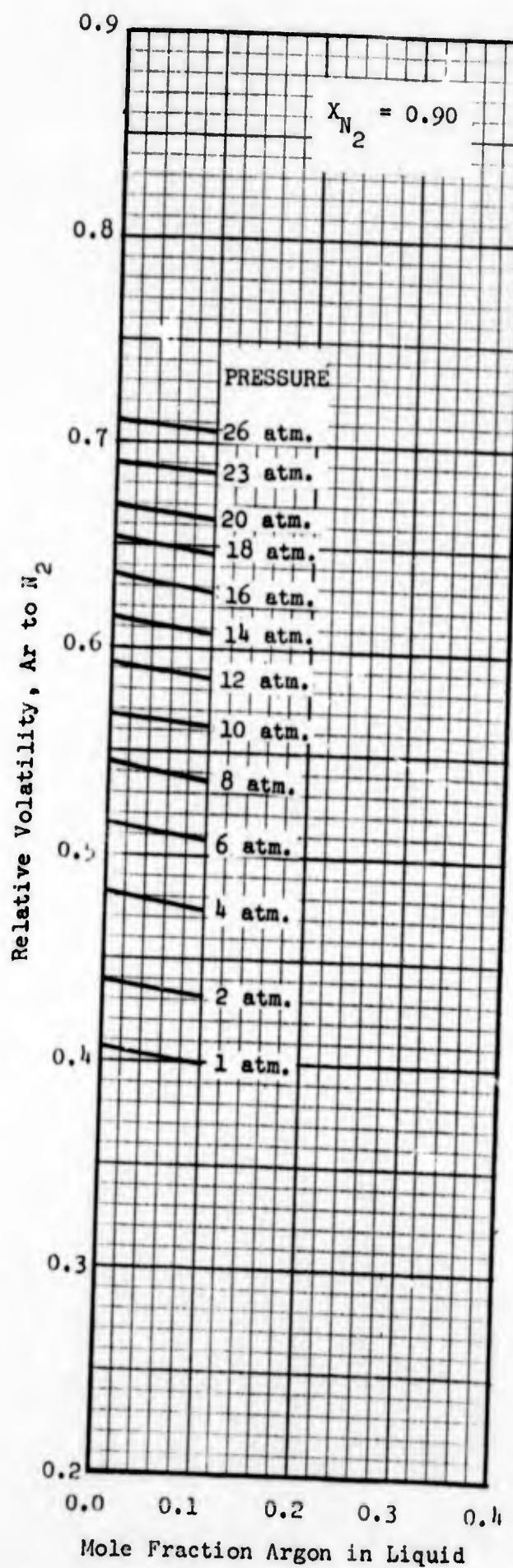


Figure 121. Relative Volatility of Argon to Nitrogen.

C. Relative Volatility of Argon to Oxygen
in Ternary System

The 12 graphs to follow present the relative volatility of argon to oxygen defined

$$\alpha_{\text{Ar}-\text{O}_2} = \frac{y_{\text{Ar}}}{x_{\text{Ar}}} \cdot \frac{x_{\text{O}_2}}{y_{\text{O}_2}} \quad (52)$$

as a function of mole fraction argon in the liquid along selected isobars. The graphs are arranged in order of increasing mole percent nitrogen in the liquid.

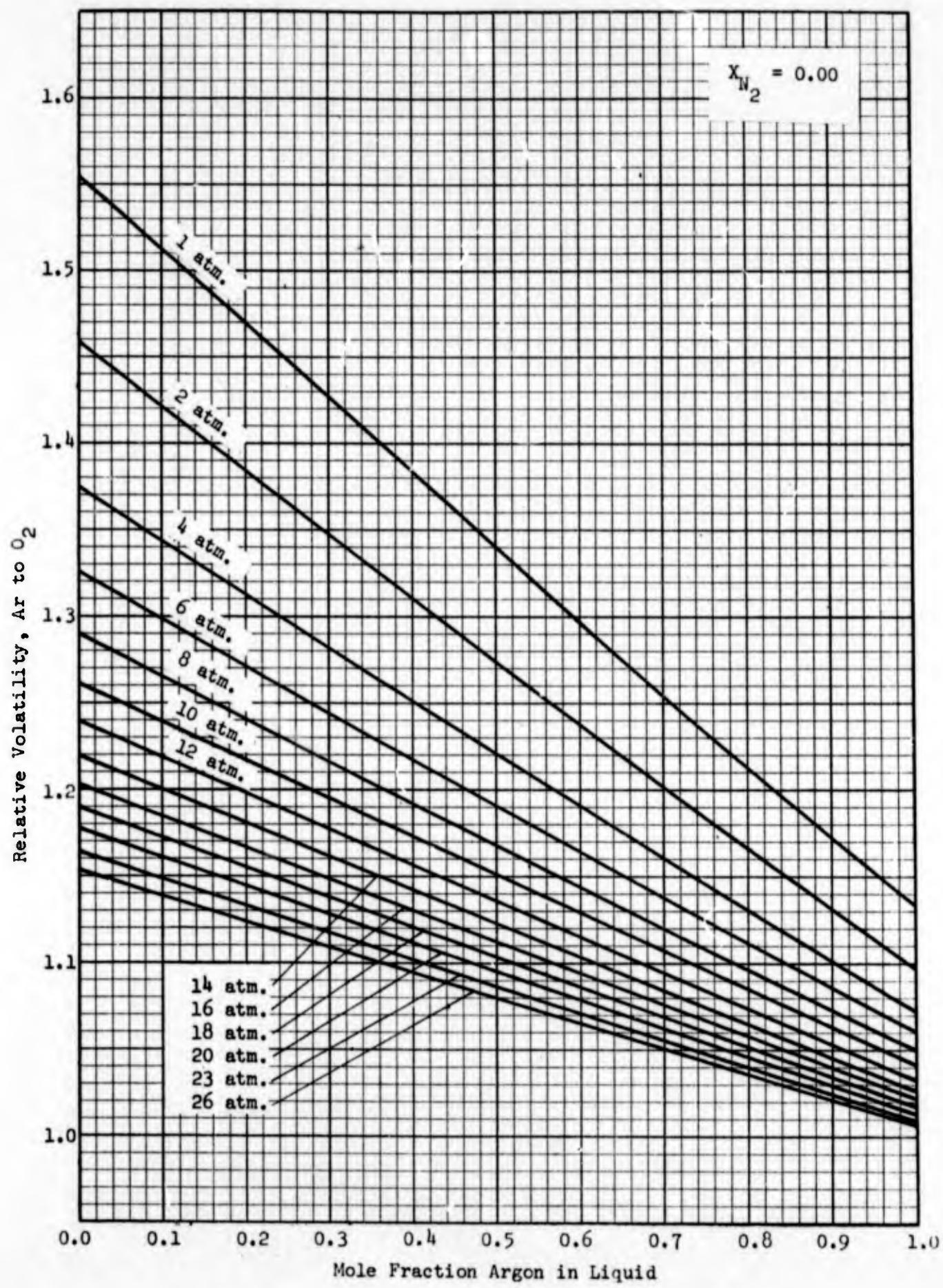


Figure 122. Relative Volatility of Argon to Oxygen.

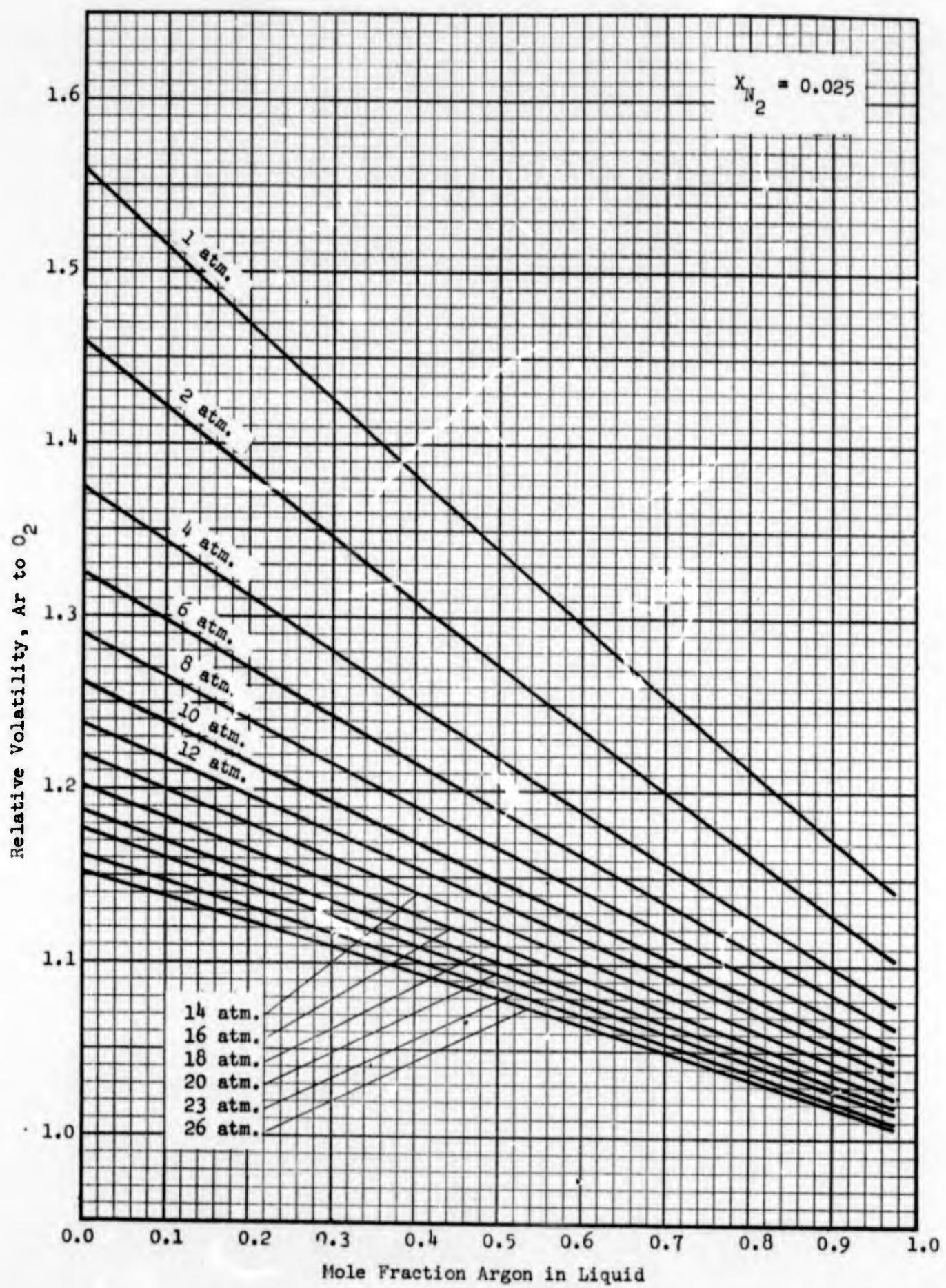


Figure 123. Relative Volatility of Argon to Oxygen.

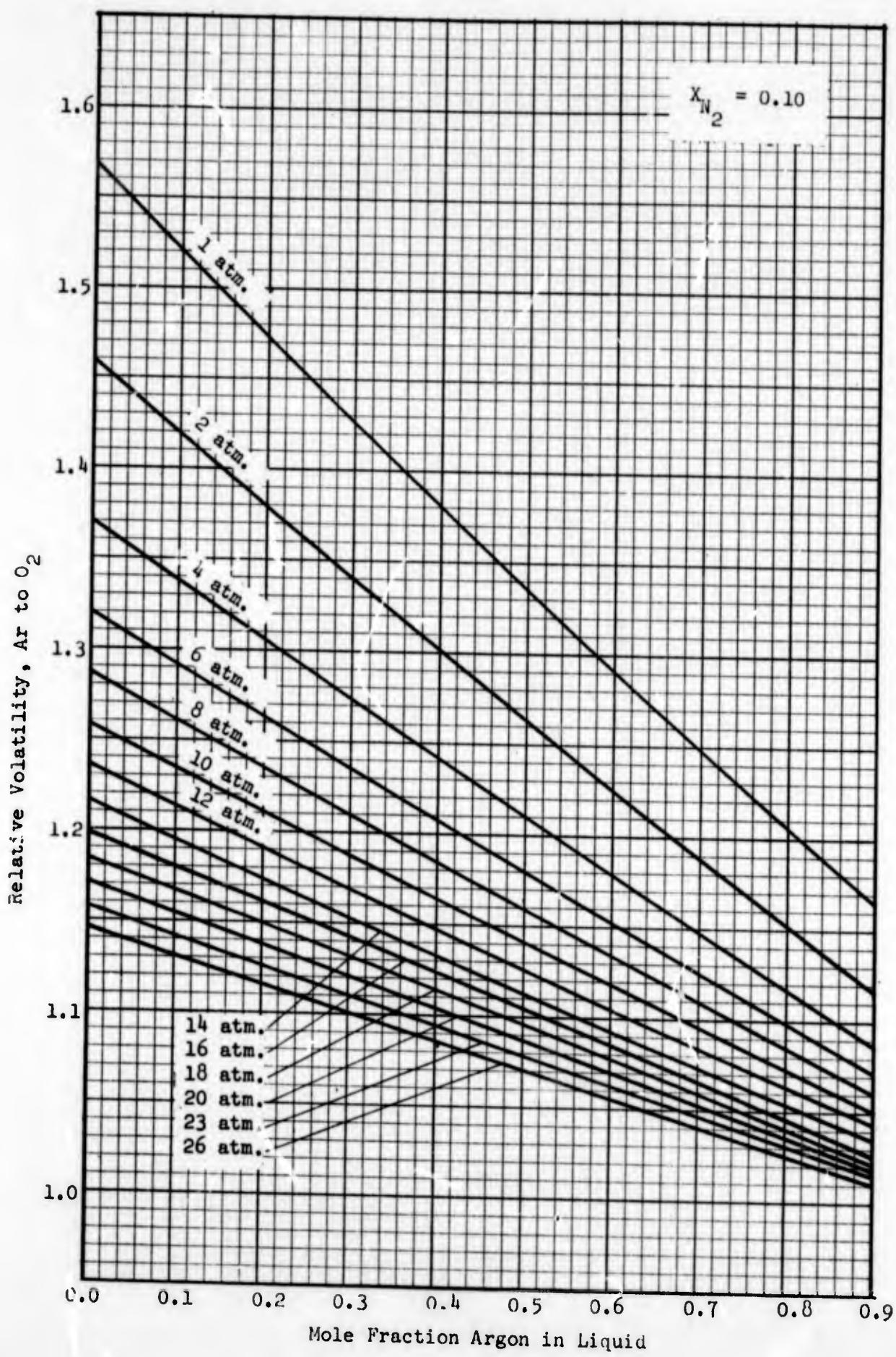


Figure 124. Relative Volatility of Argon to Oxygen.

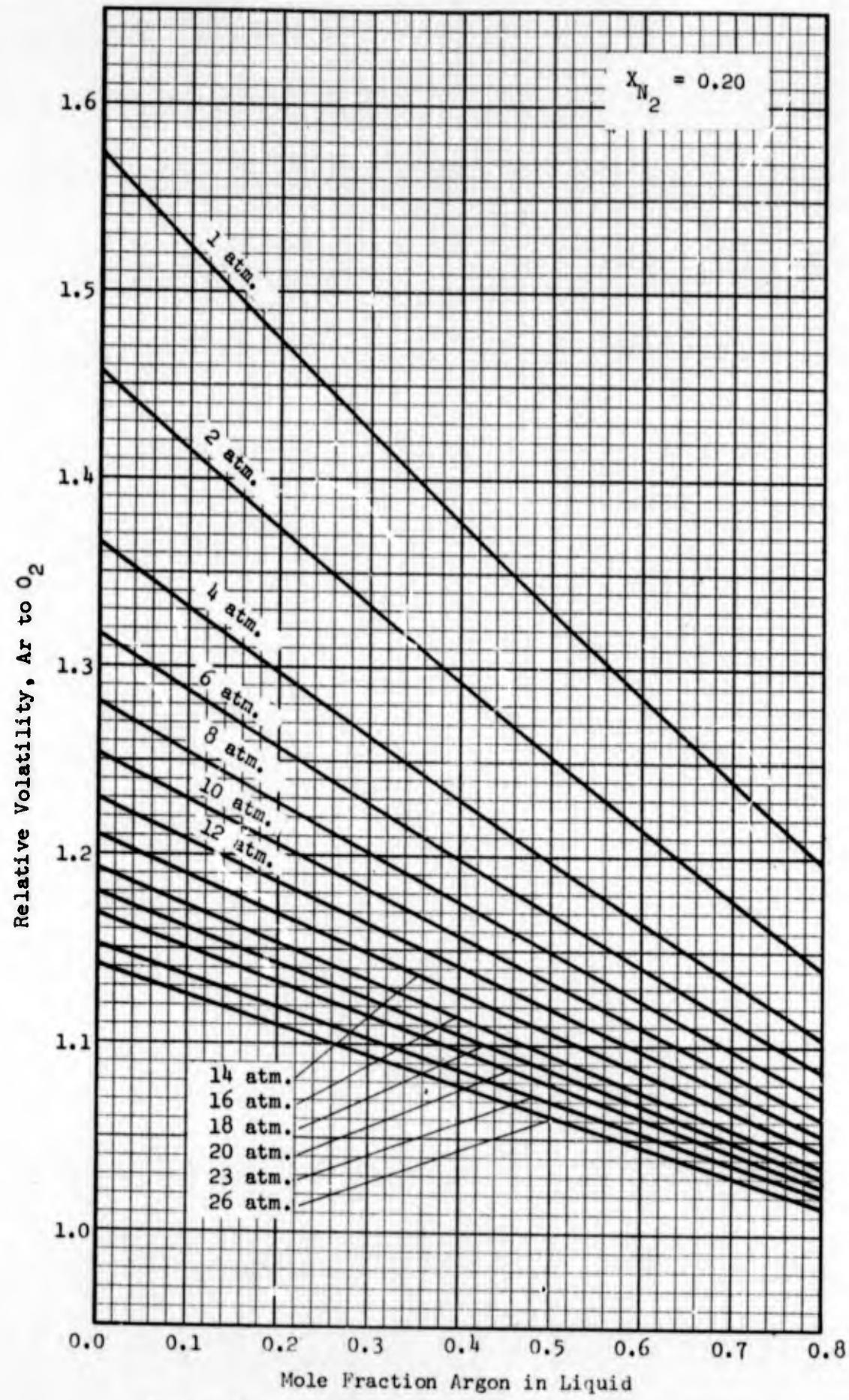


Figure 125. Relative Volatility of Argon to Oxygen.

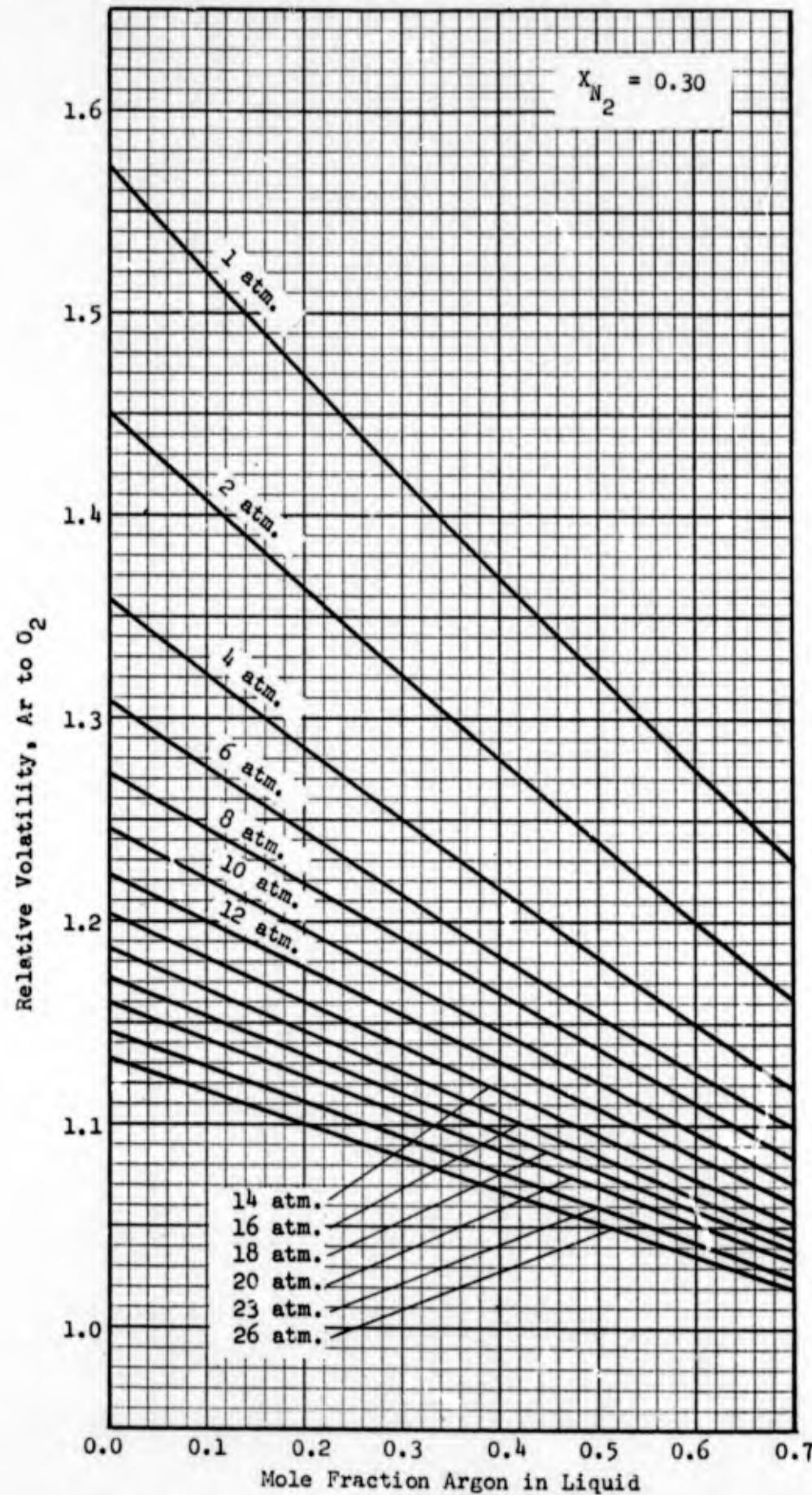


Figure 126. Relative Volatility of Argon to Oxygen.

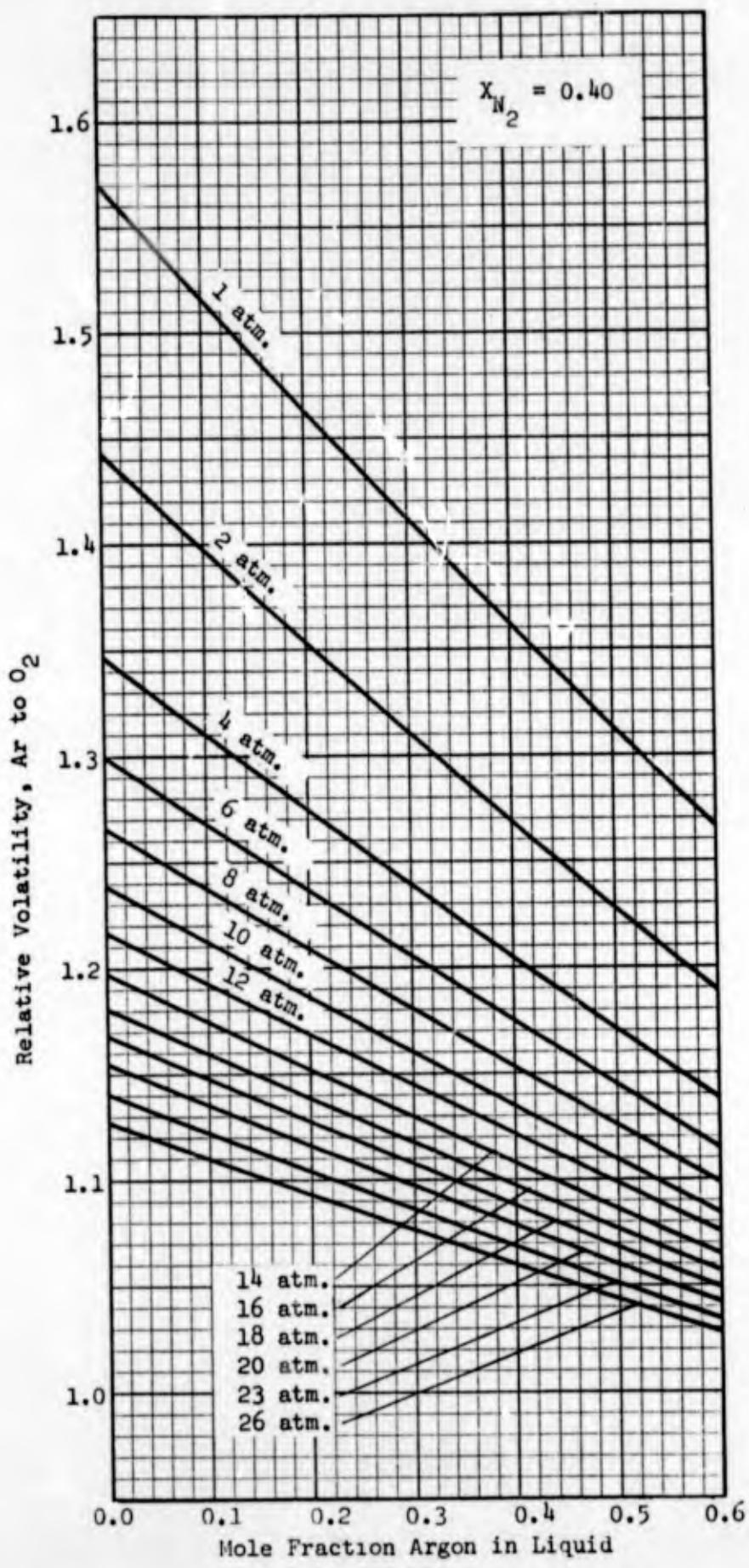


Figure 127. Relative Volatility of Argon to Oxygen.

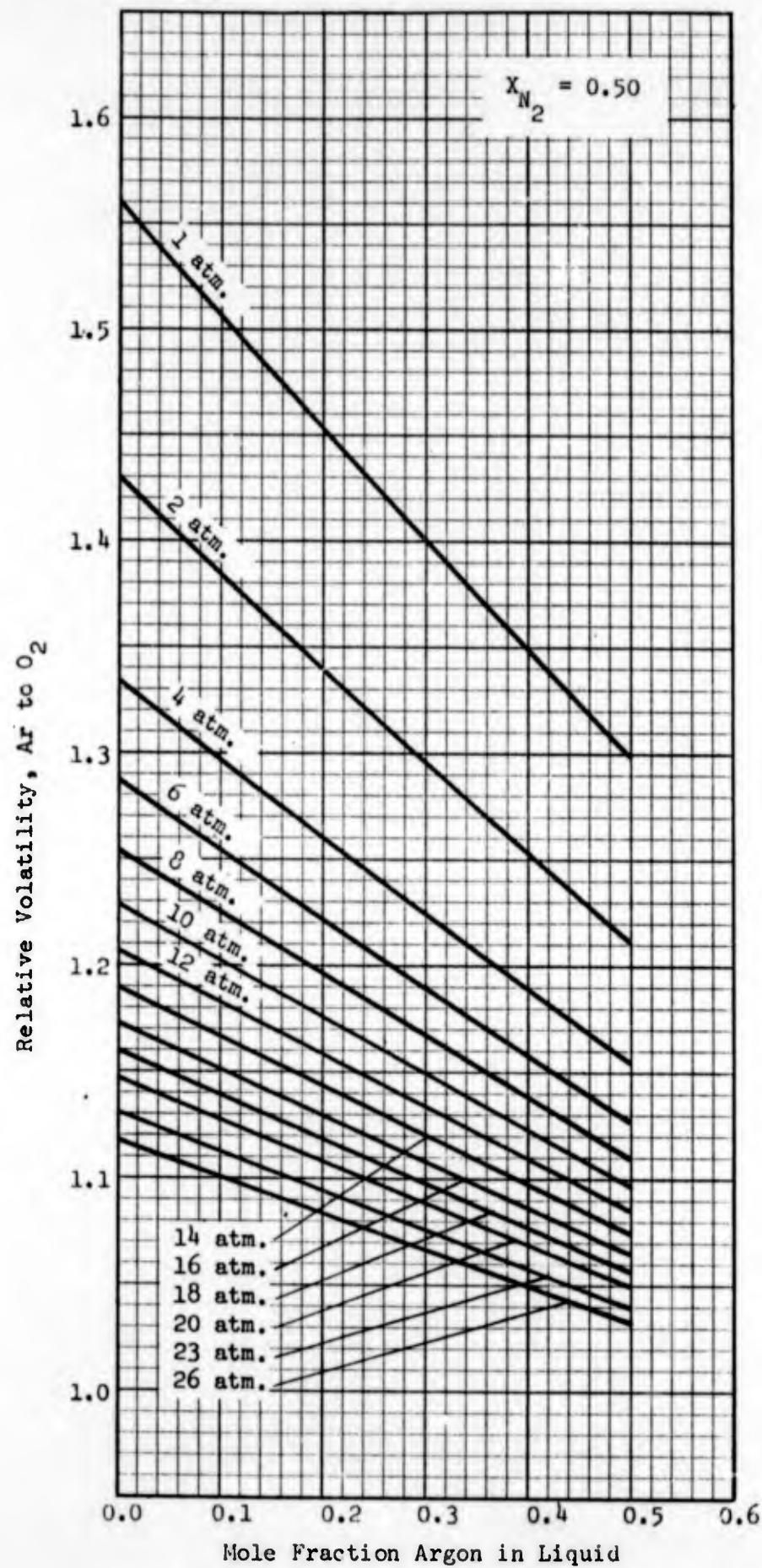


Figure 128. Relative Volatility of Argon to Oxygen.

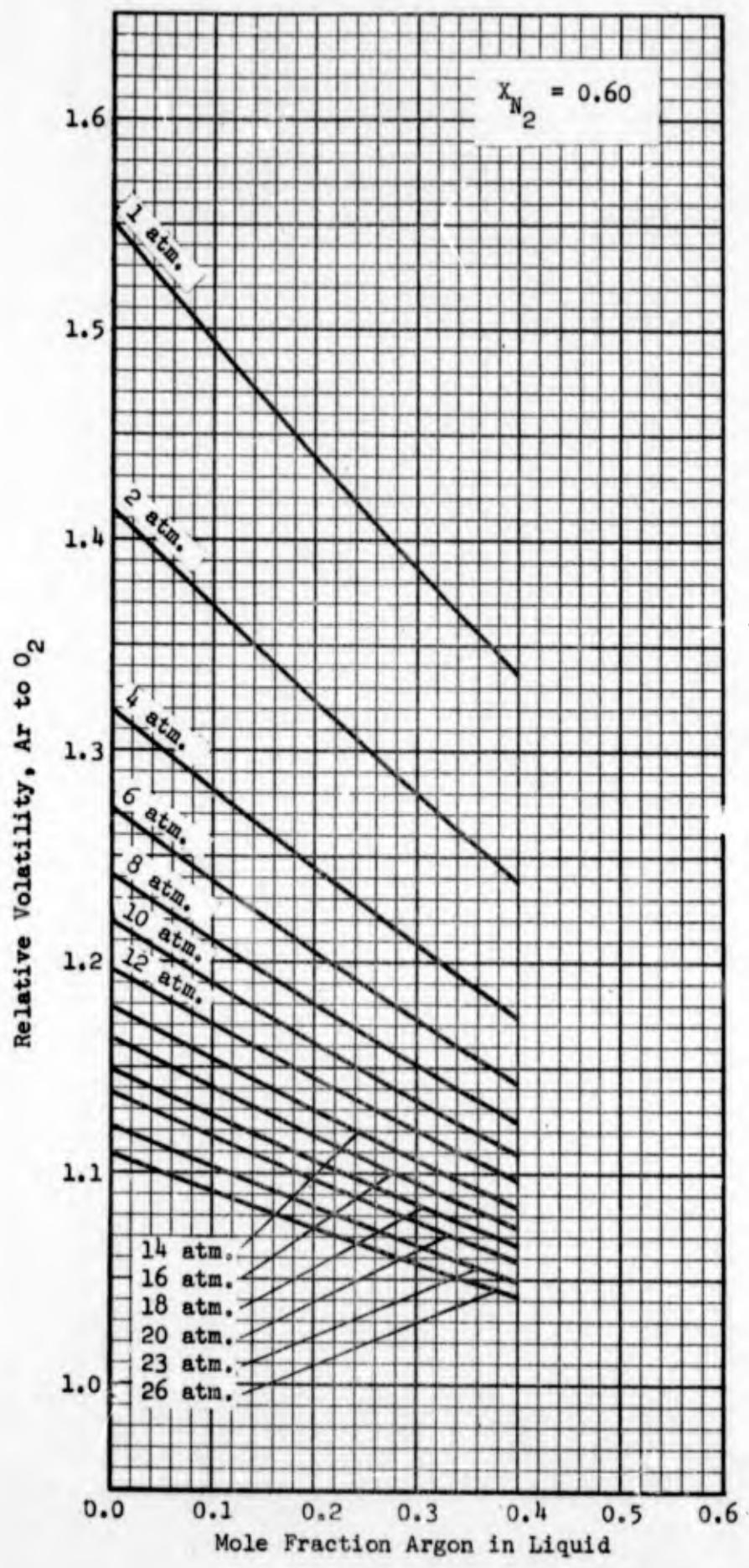


Figure 129. Relative Volatility of Argon to Oxygen.

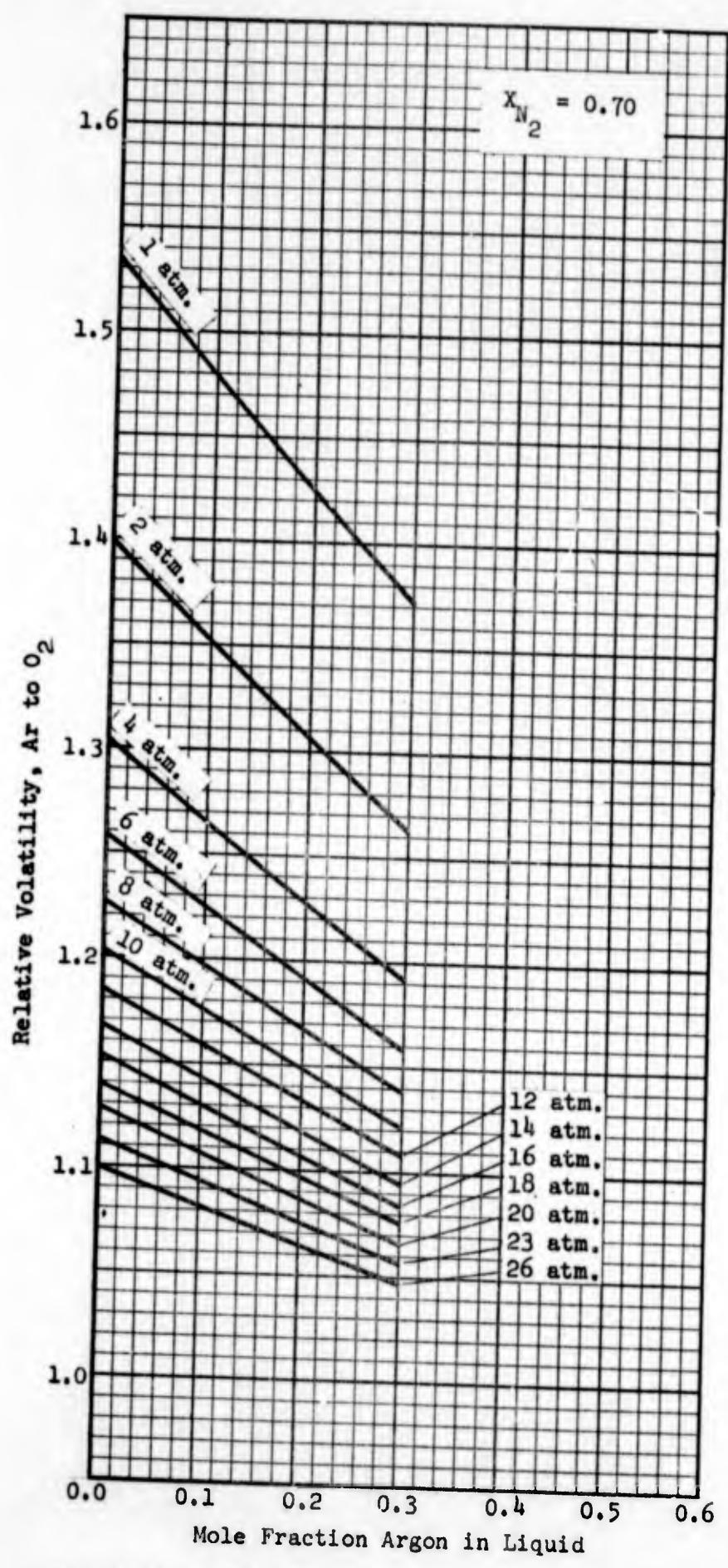


Figure 130. Relative Volatility of Argon to Oxygen.

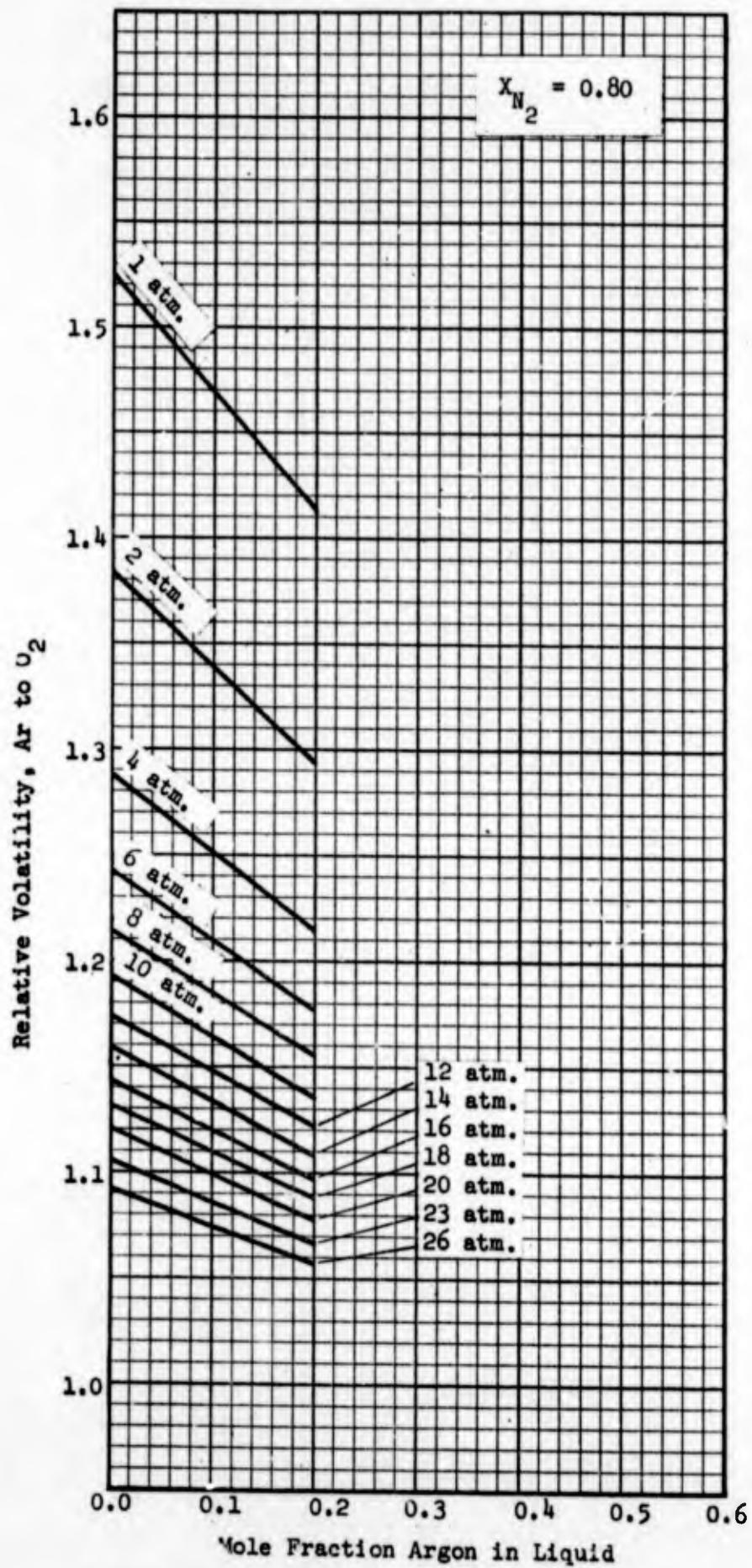


Figure 131. Relative Volatility of Argon to Oxygen.

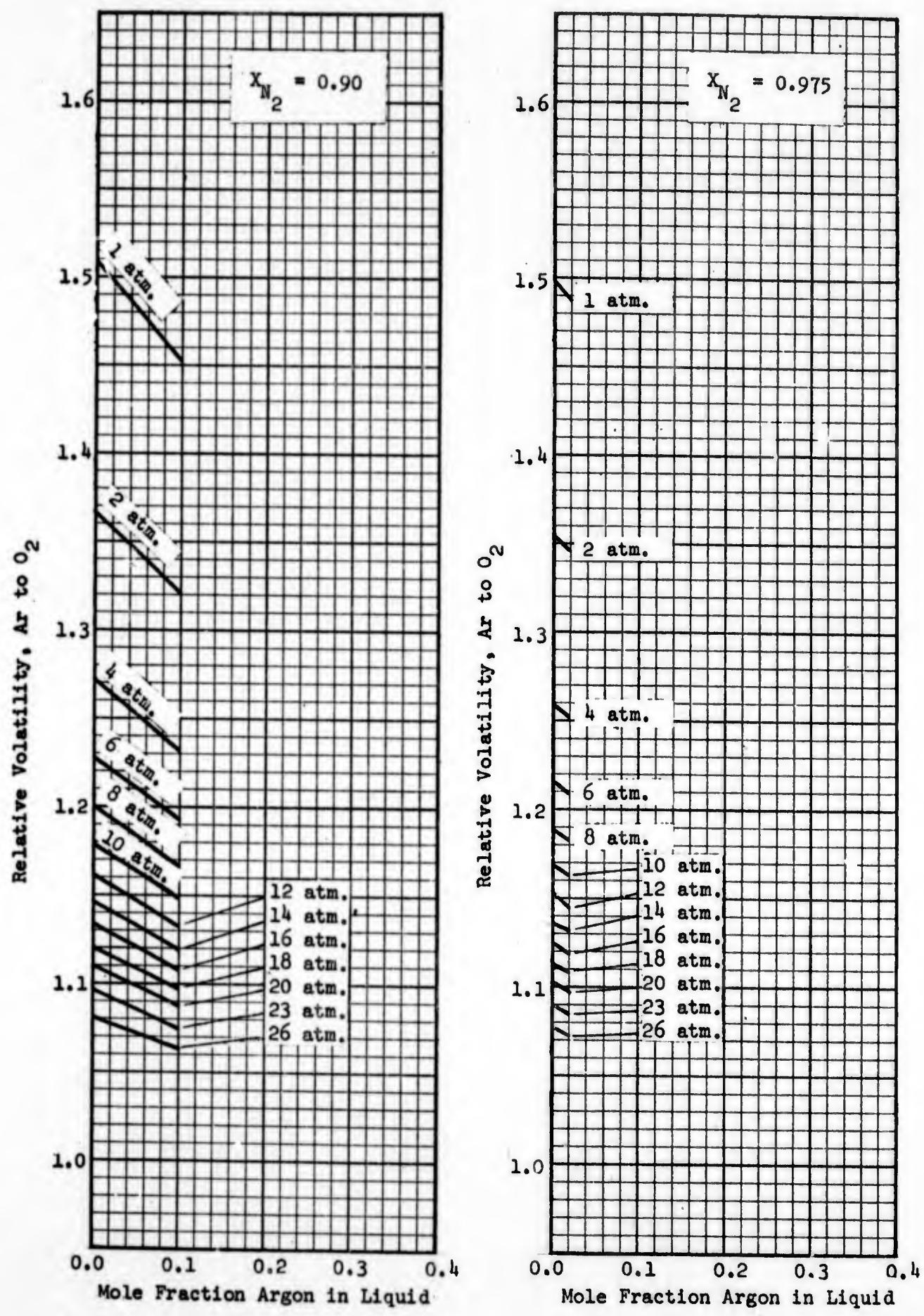


Figure 132. Relative Volatility of Argon to Oxygen.

D. Relative Volatility of Argon to Nitrogen,
Binary System

The graph to follow presents the relative volatility of argon to nitrogen in the binary system along selected isobars.

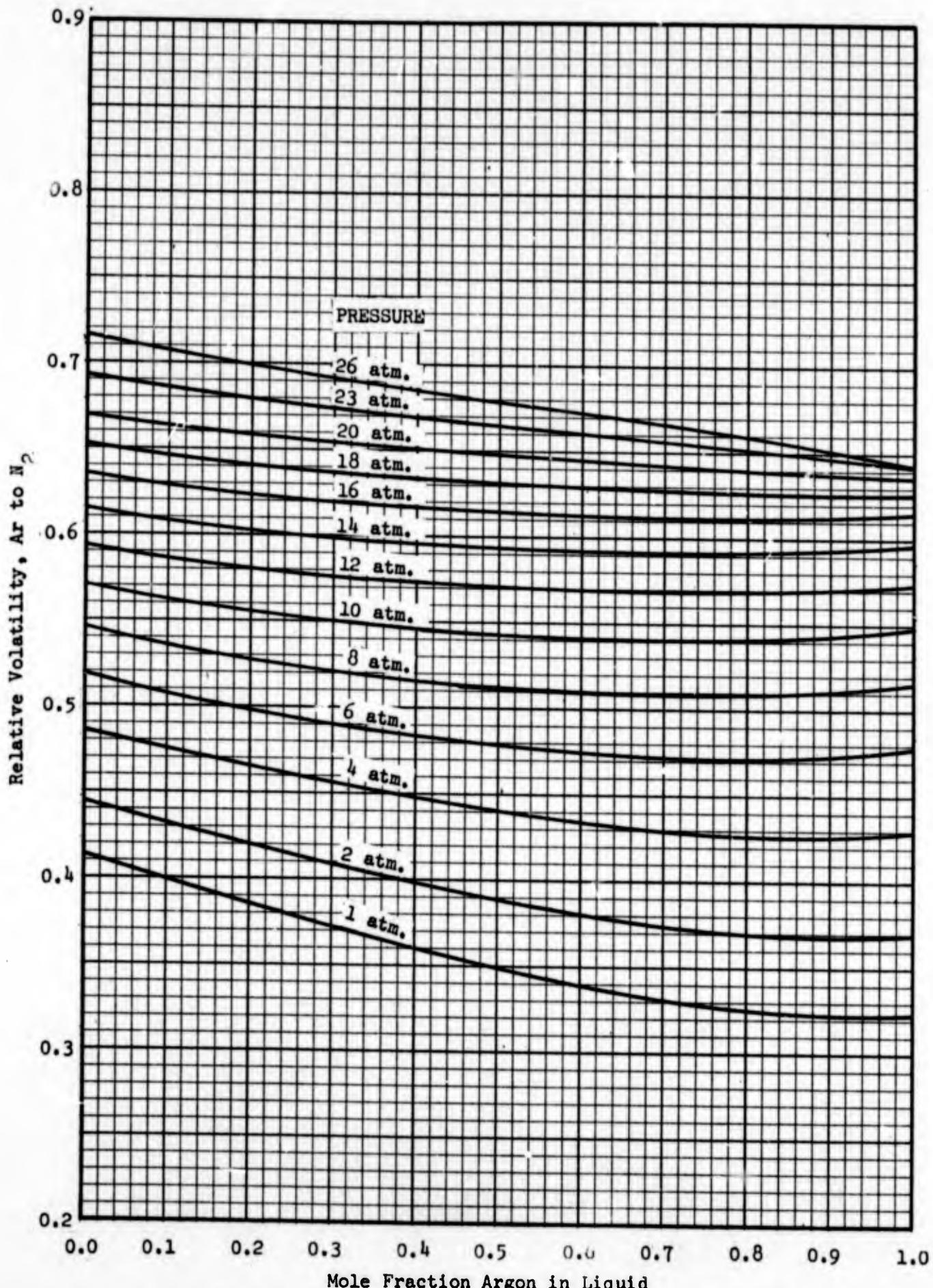


Figure 133. Relative Volatility of Argon to Nitrogen
with no Oxygen present in the System.

E. Relative Volatility of Argon to Oxygen,
Binary System

The graph to follow presents the relative volatility of argon to oxygen in the binary system along selected isobars.

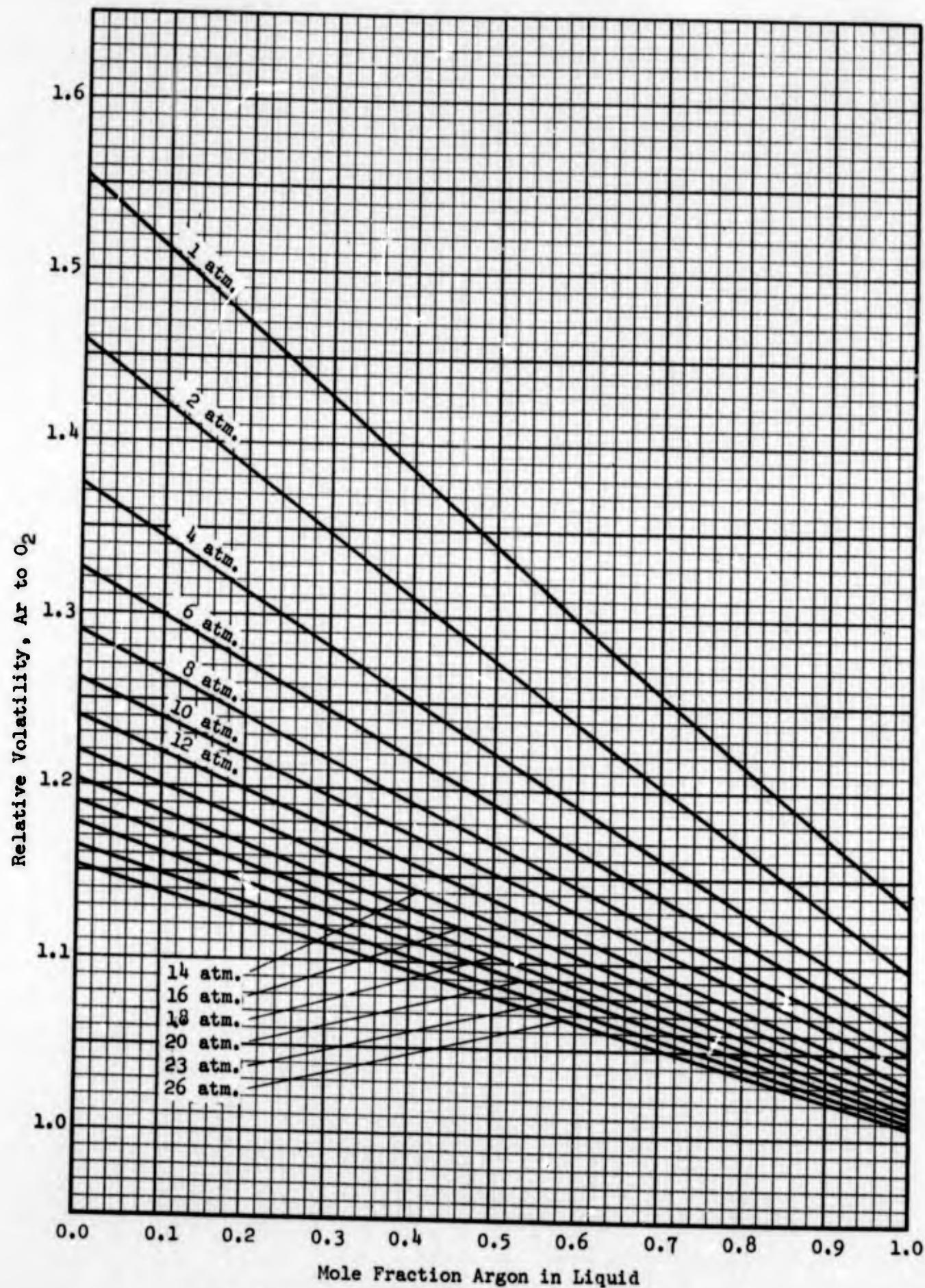


Figure 134. Relative Volatility of Argon to Oxygen with no Nitrogen present in the System.

F. Pressure Activity Coefficients

The 39 graphs to follow present the pressure activity coefficients of oxygen-argon-nitrogen as a function of composition. The pressure activity coefficient is defined as

$$\gamma_{wi} = \frac{y_i P}{x_i P^o} \quad (53)$$

This function is best understood as expressing the deviations from Raoult's Law.

The graphs are grouped in order of component: nitrogen, argon, oxygen. Inside each group they are ordered with respect to pressure.

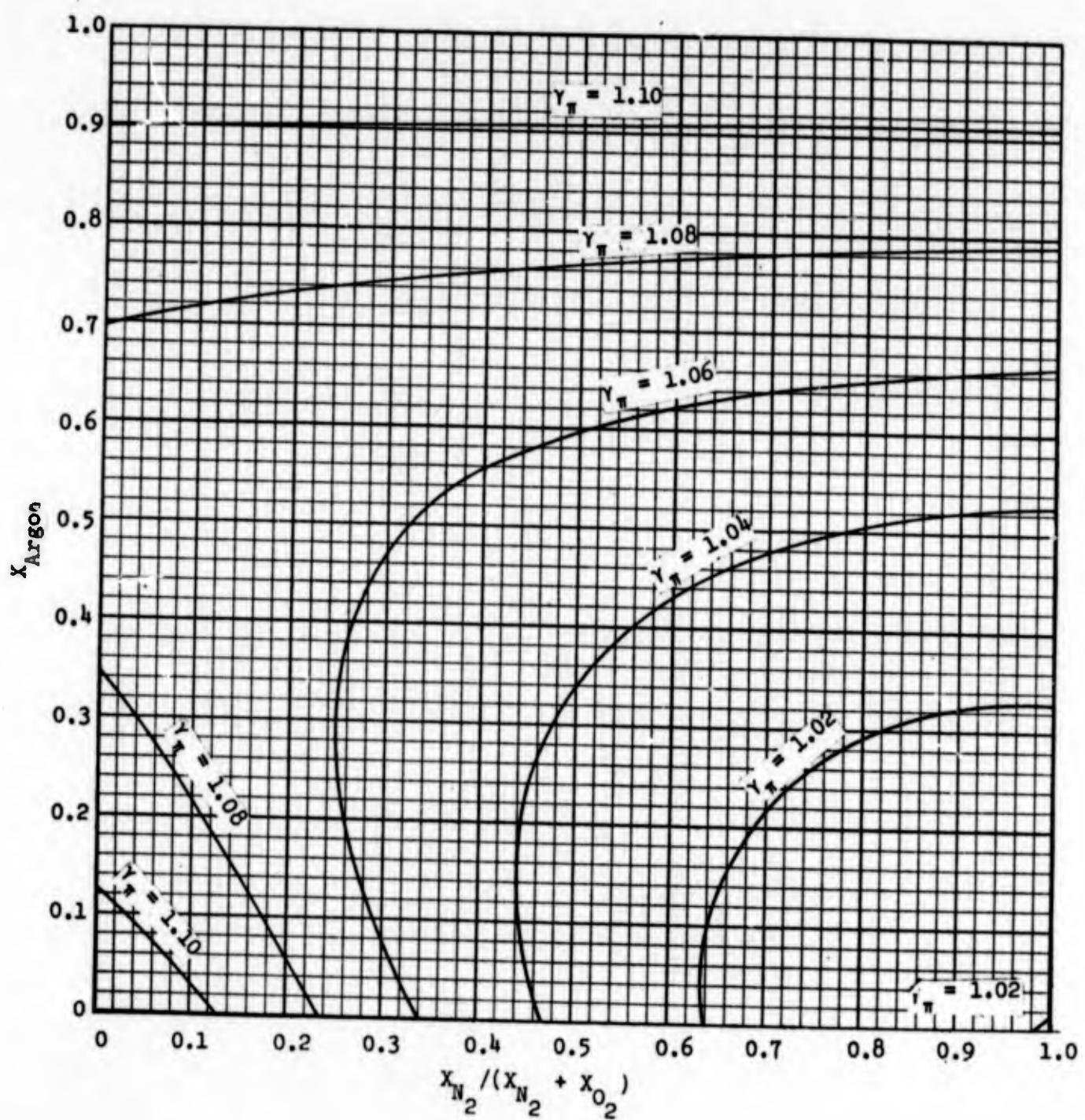


Figure 135. Nitrogen Pressure Activity Coefficients, 1 Atmosphere

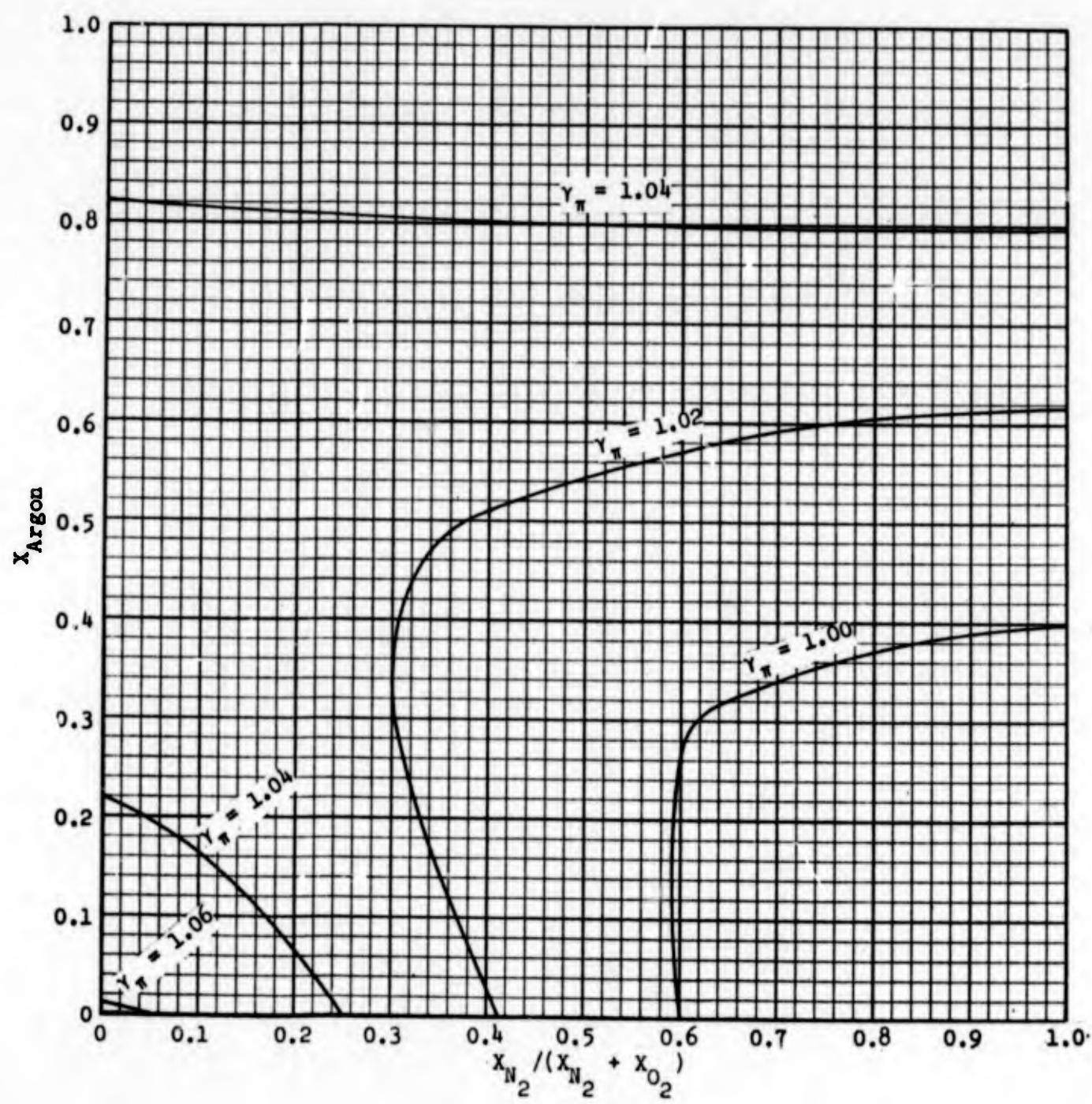


Figure 136. Nitrogen Pressure Activity Coefficients, 2 Atmospheres

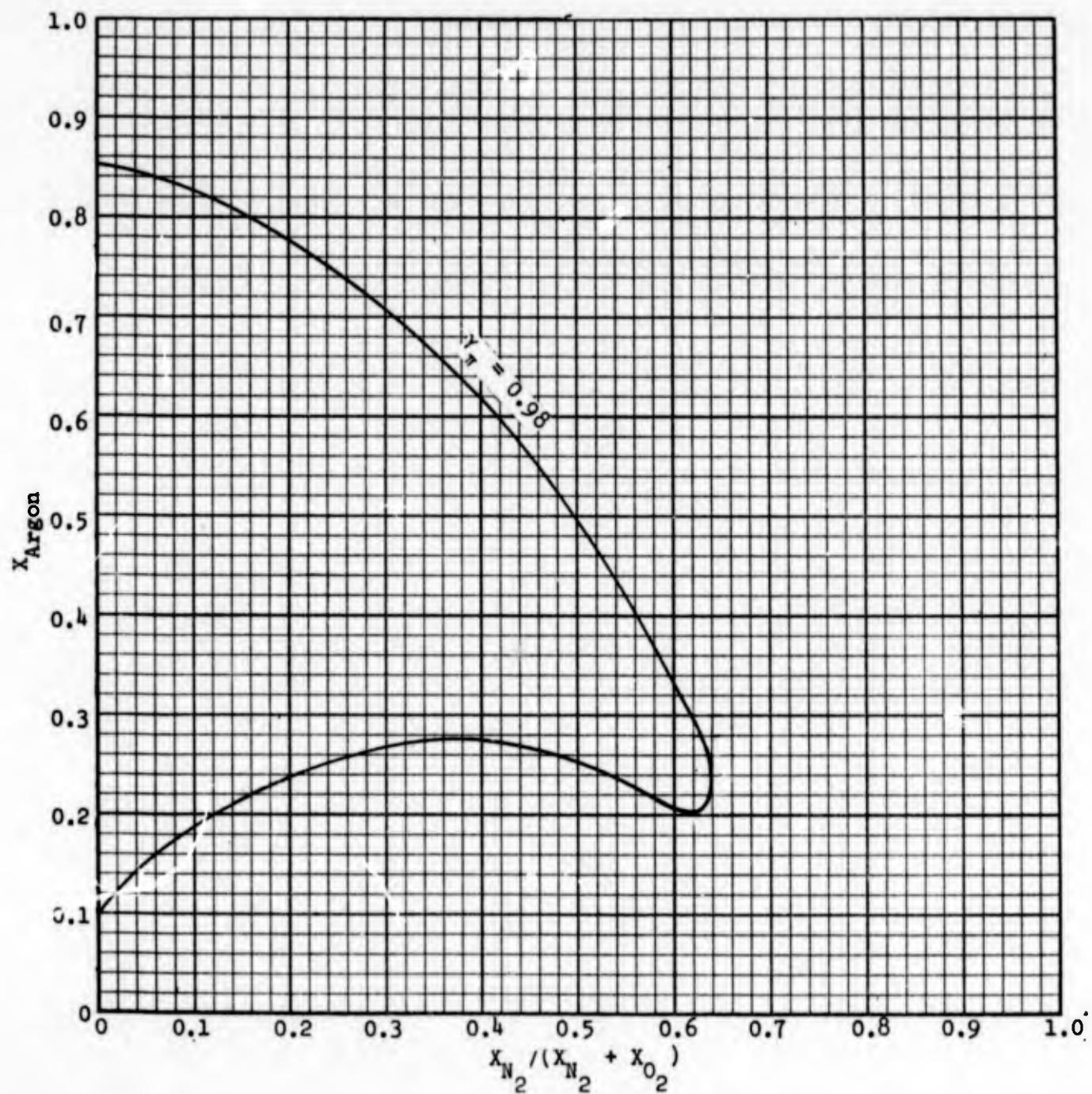


Figure 137. Nitrogen Pressure Activity Coefficients, 4 Atmospheres

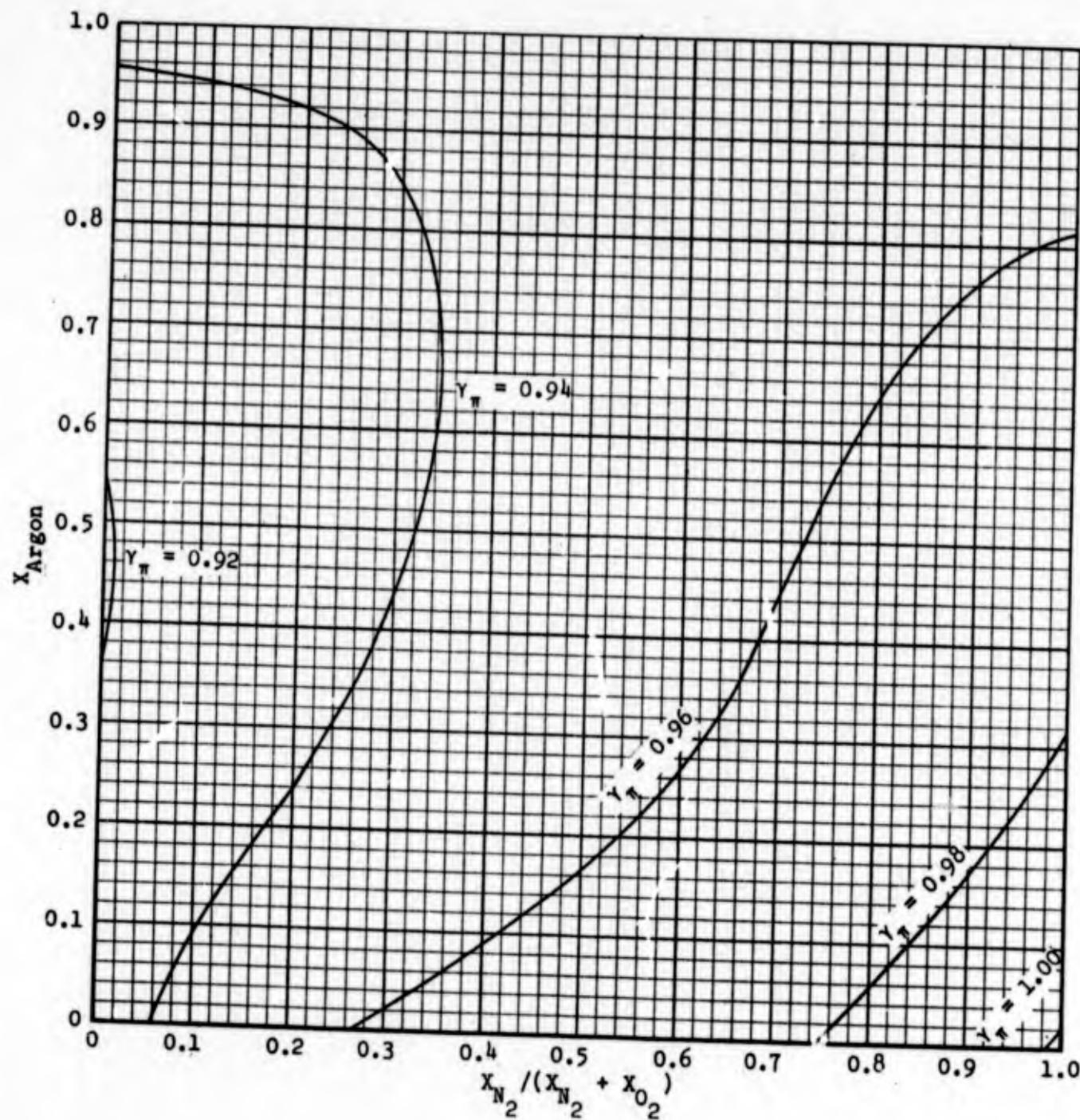


Figure 138. Nitrogen Pressure Activity Coefficients, 6 Atmospheres.

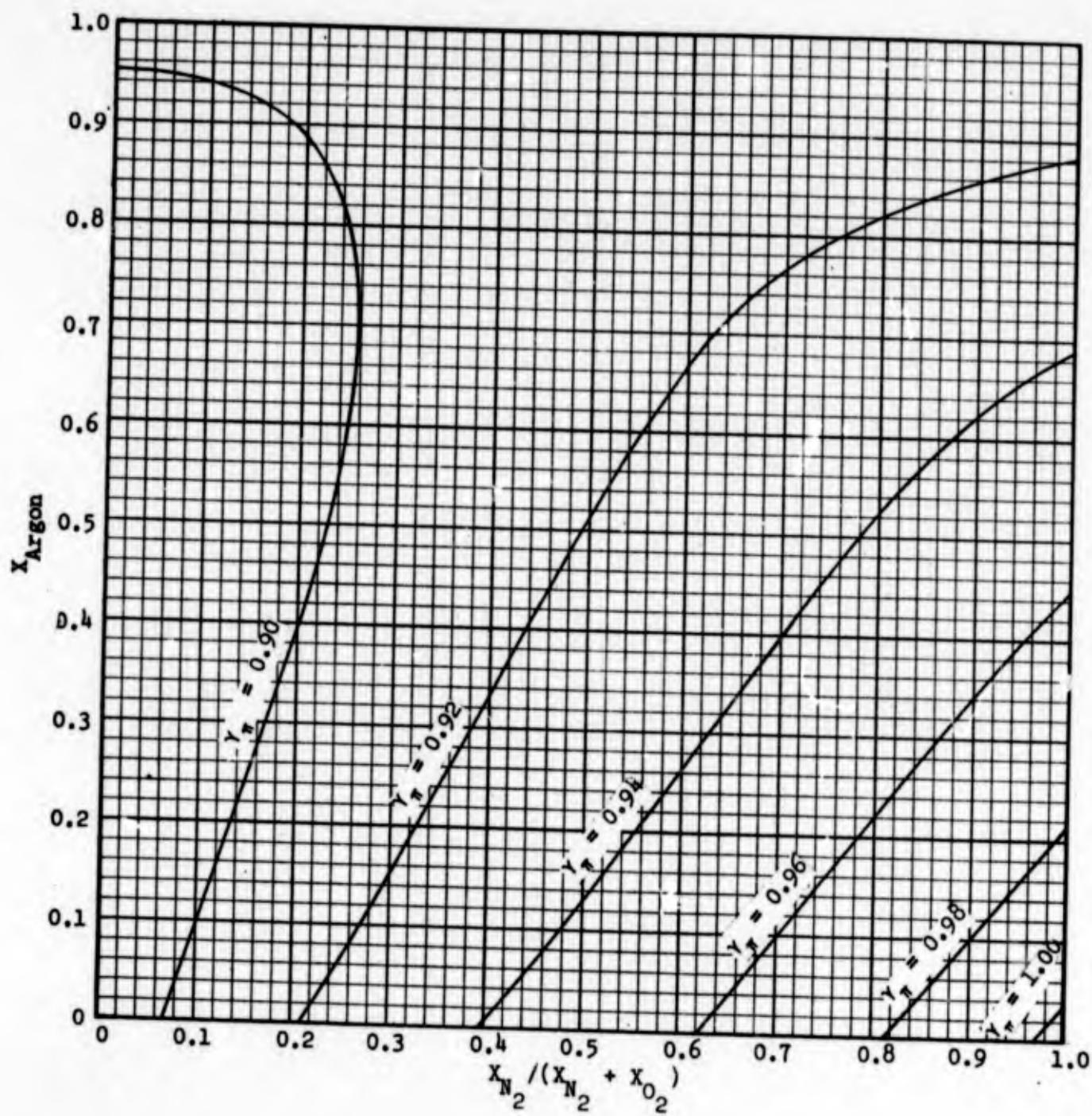


Figure 139. Nitrogen Pressure Activity Coefficients, 8 Atmospheres.

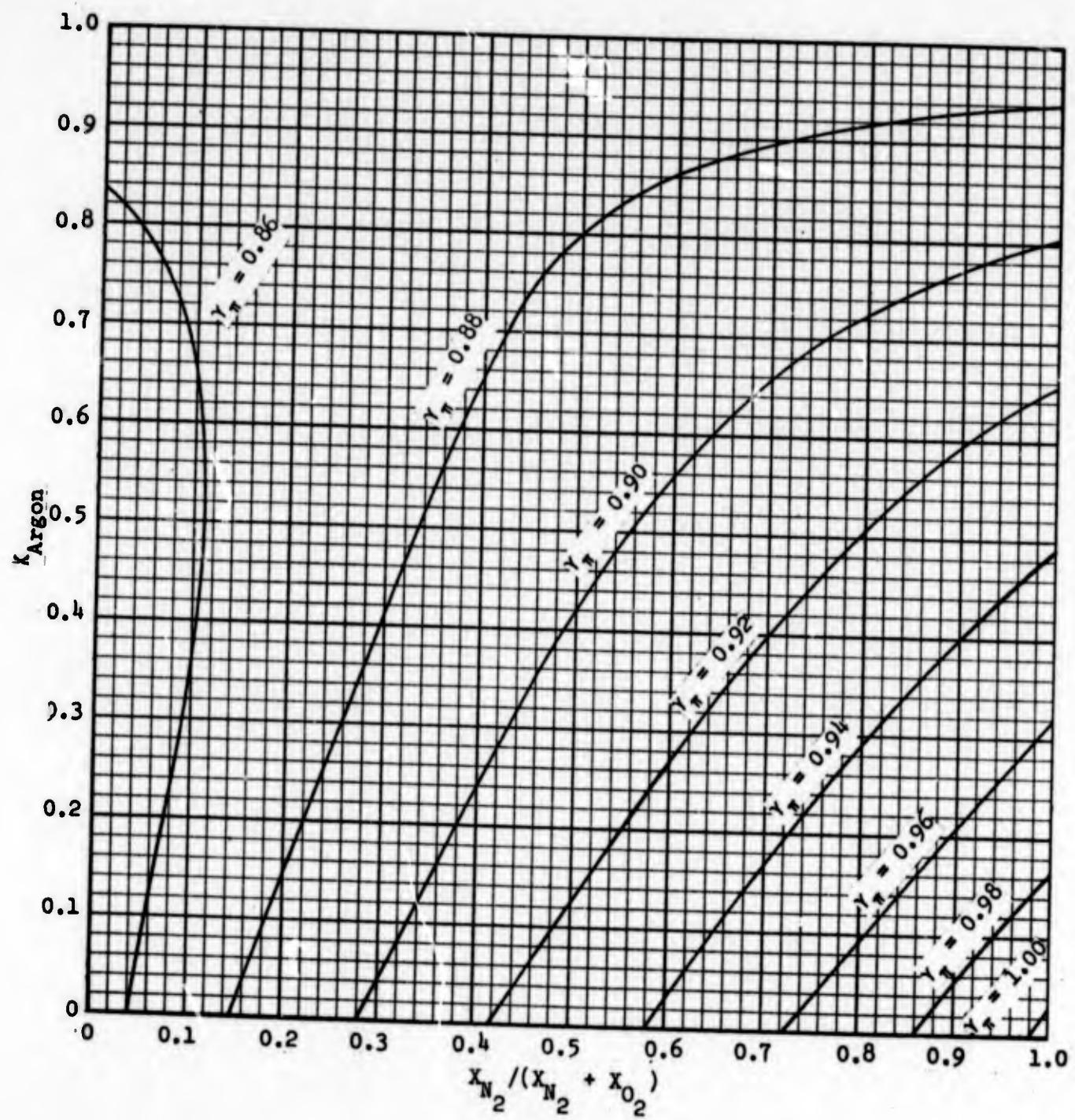


Figure 140. Nitrogen Pressure Activity Coefficients, 10 Atmospheres.

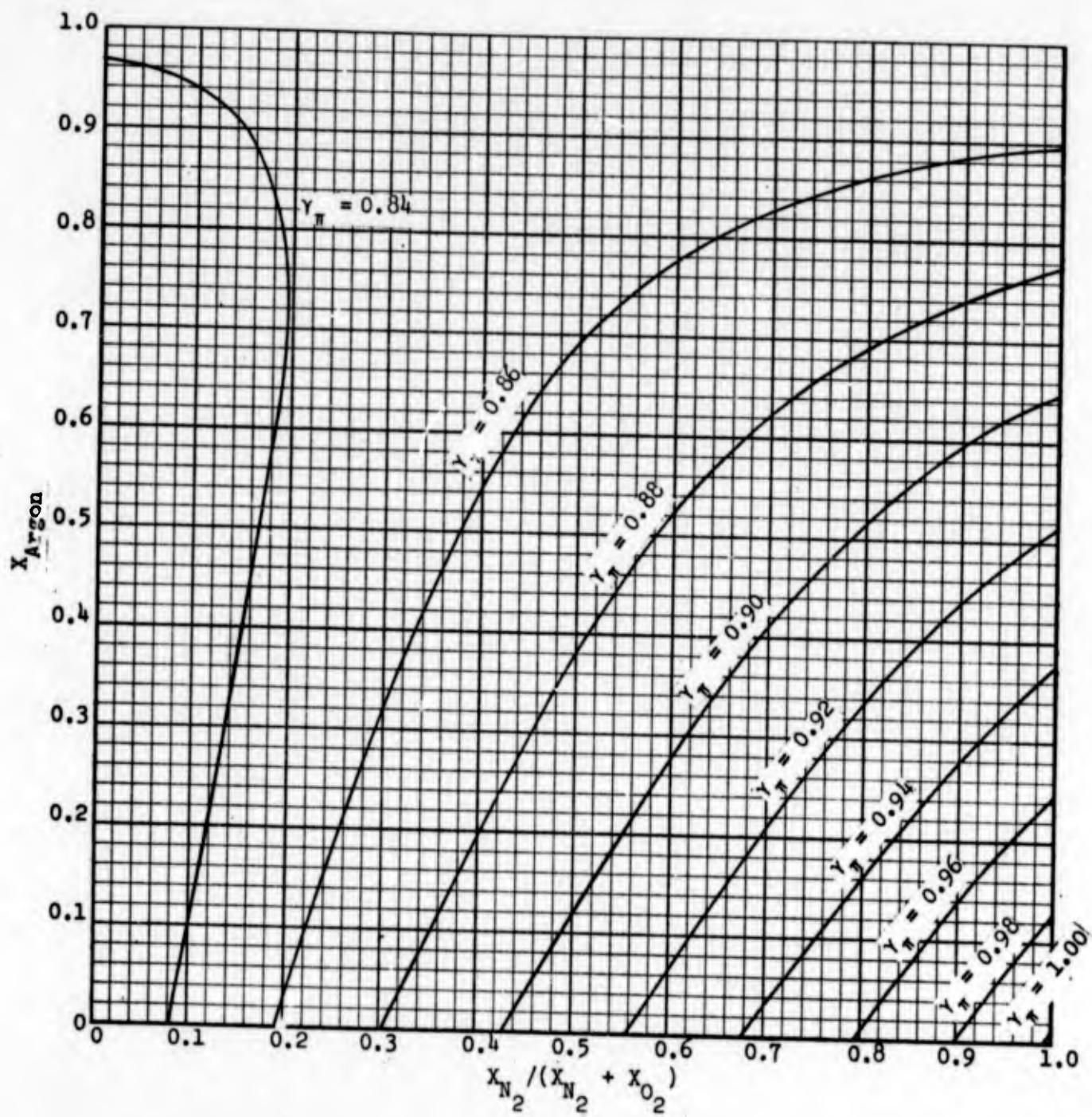


Figure 141. Nitrogen Pressure Activity Coefficients, 12 Atmospheres.

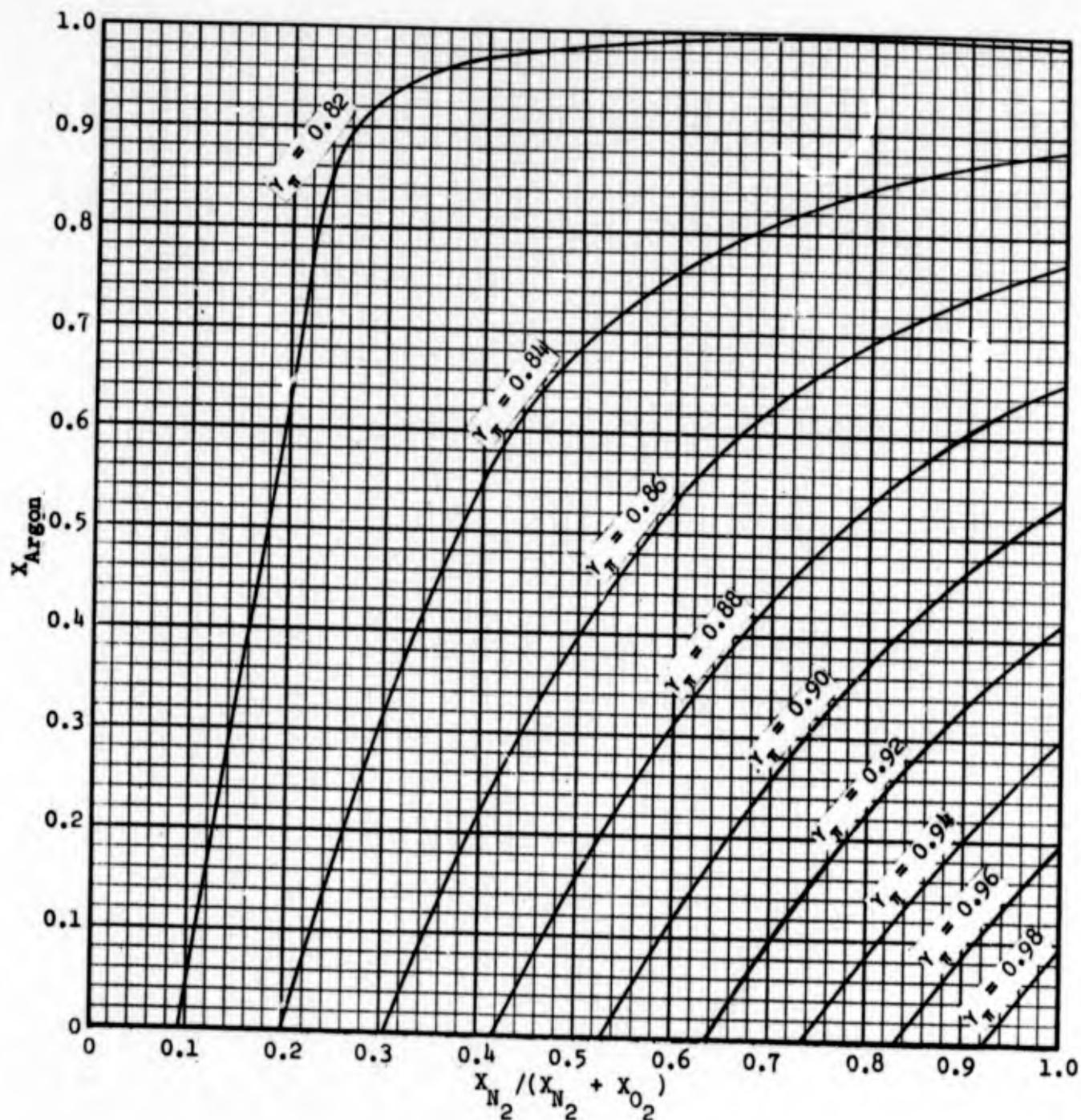


Figure 142. Nitrogen Pressure Activity Coefficients, 14 Atmospheres.

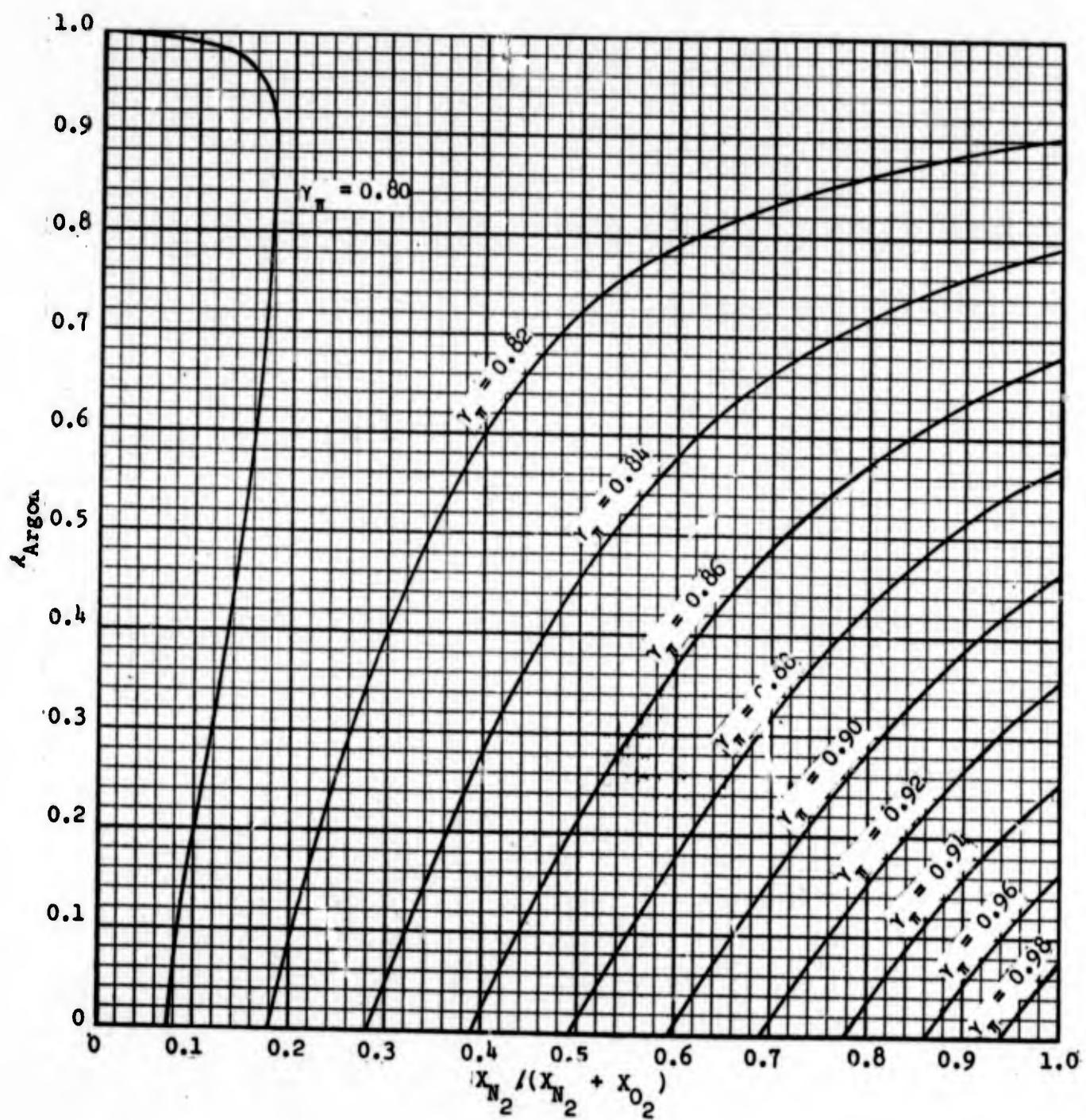


Figure 143. Nitrogen Pressure Activity Coefficients, 16 Atmospheres.

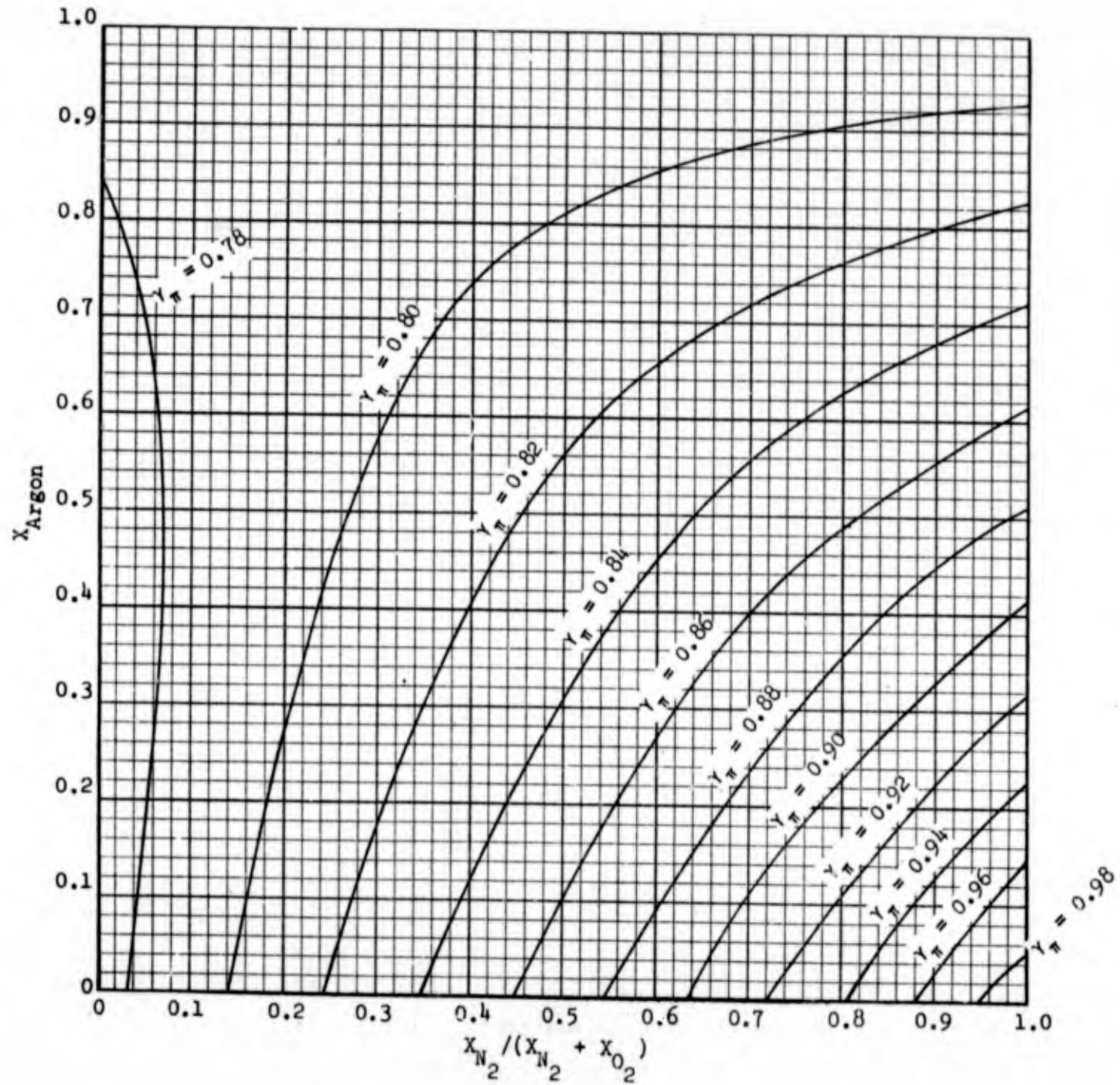


Figure 144. Nitrogen Pressure Activity Coefficients, 18 Atmospheres.

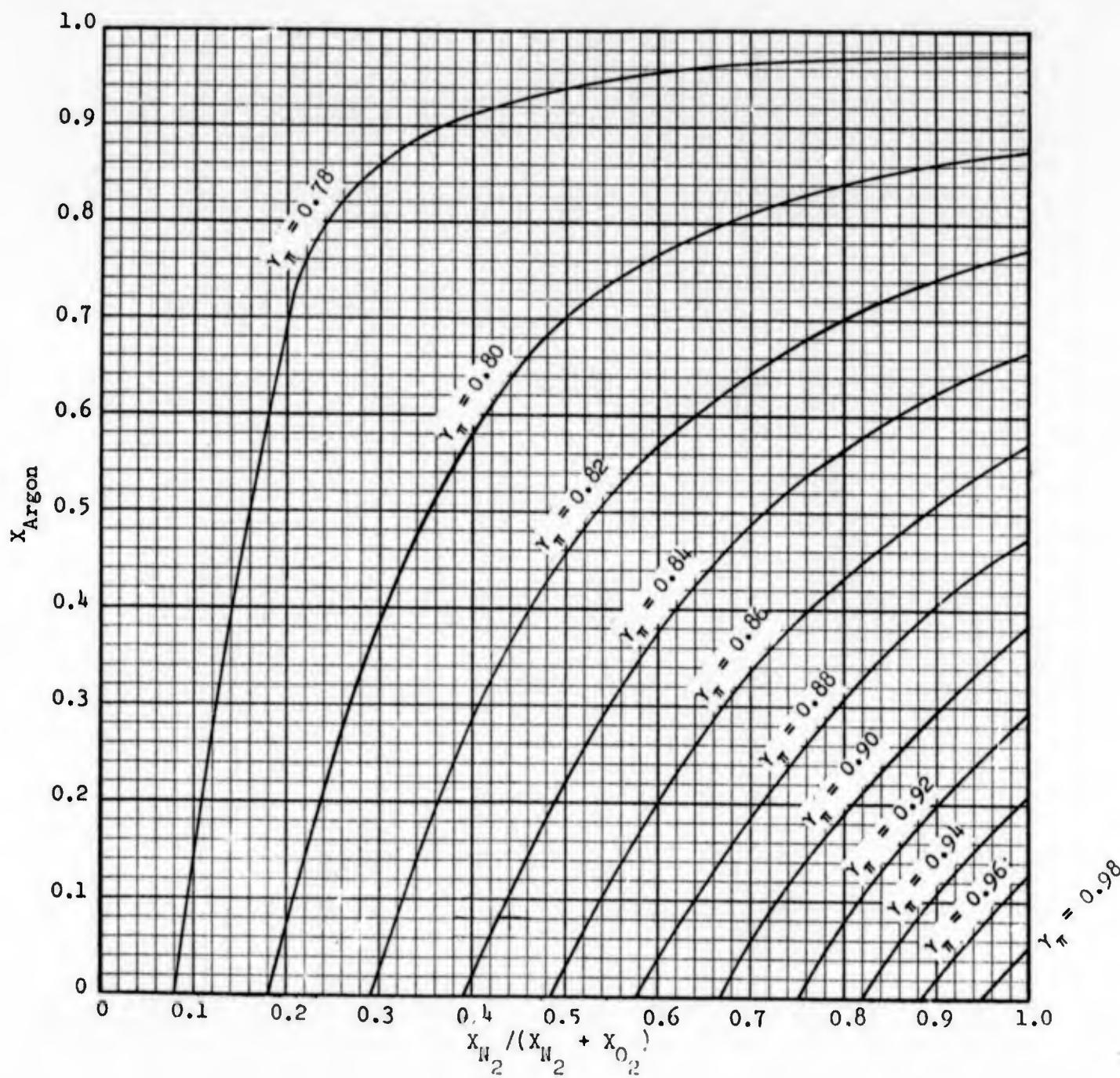


Figure 145. Nitrogen Pressure Activity Coefficients, 20 Atmospheres.

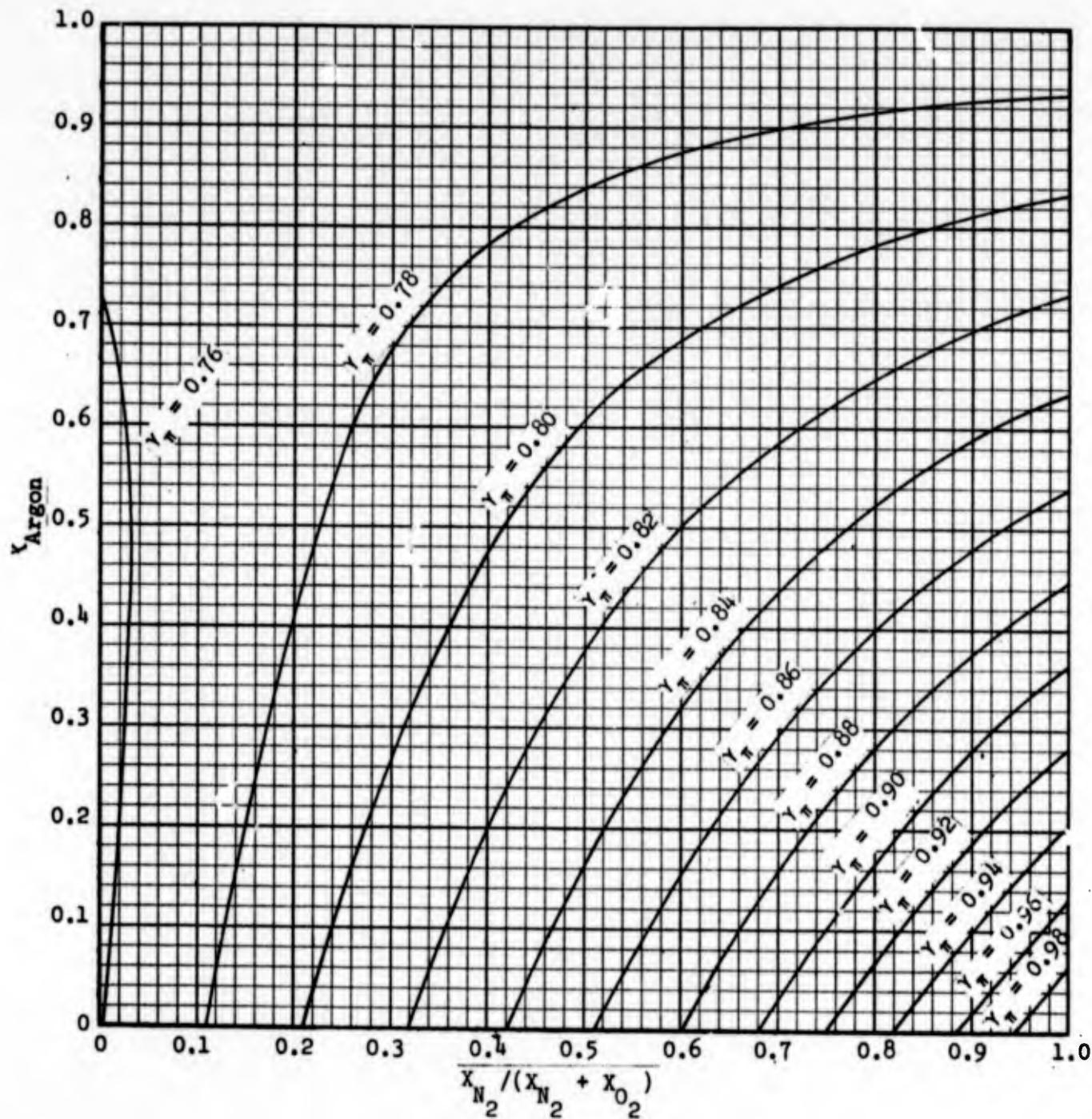


Figure 146. Nitrogen Pressure Activity Coefficients, 23 Atmospheres.

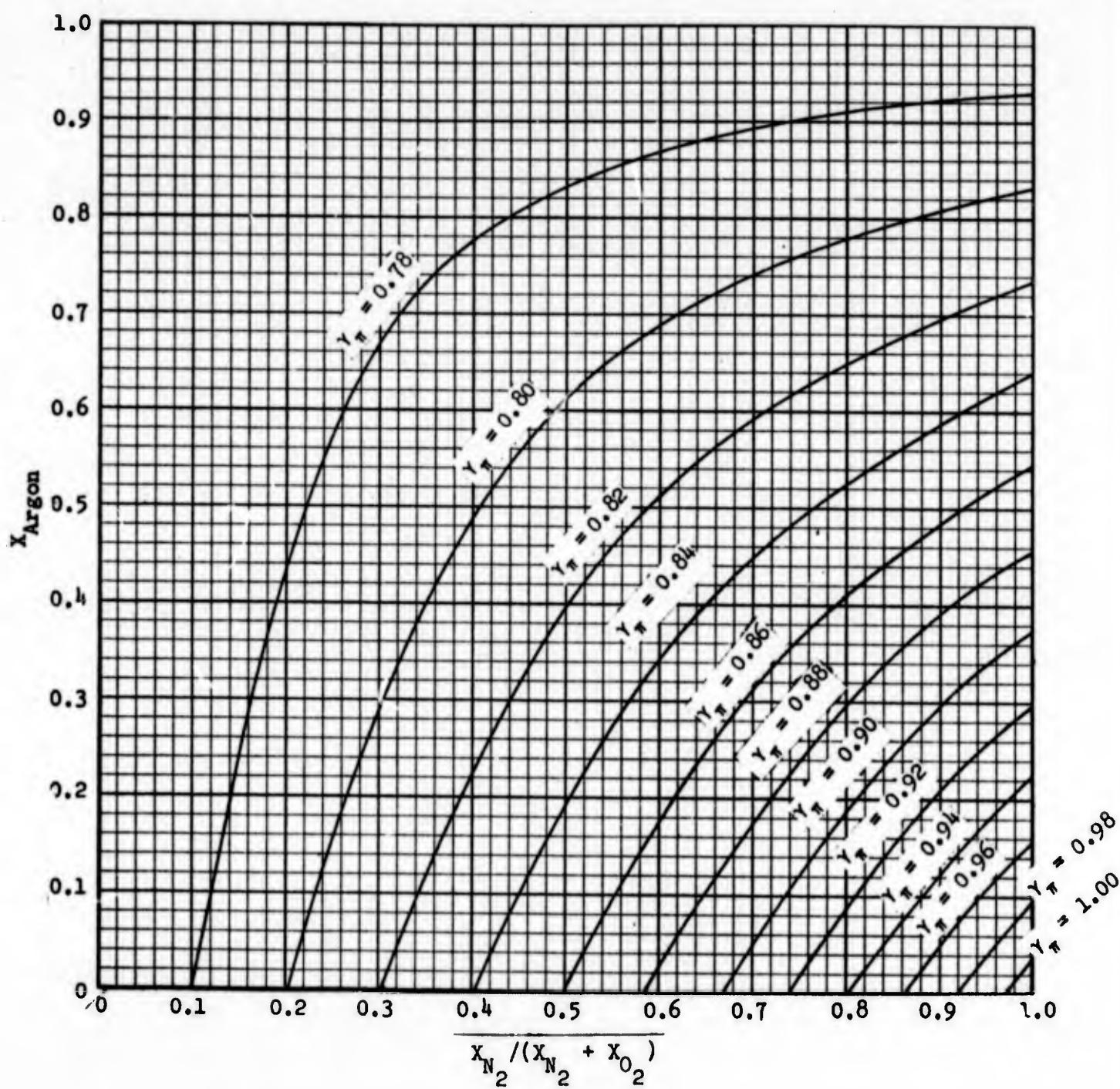


Figure 147. Nitrogen Pressure Activity Coefficients, 26 Atmospheres.

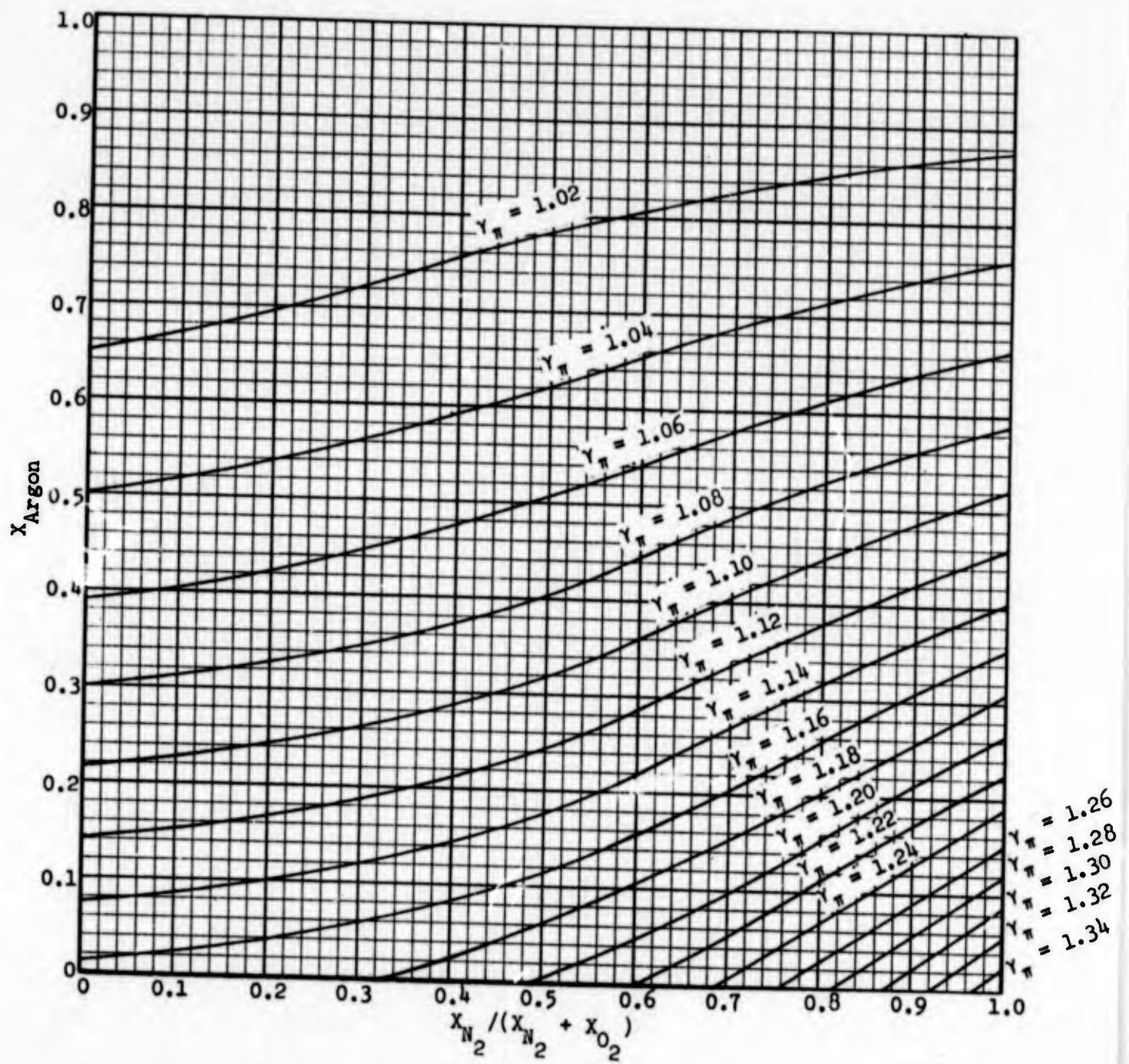


Figure 148. Argon Pressure Activity Coefficients, 1 Atmosphere.

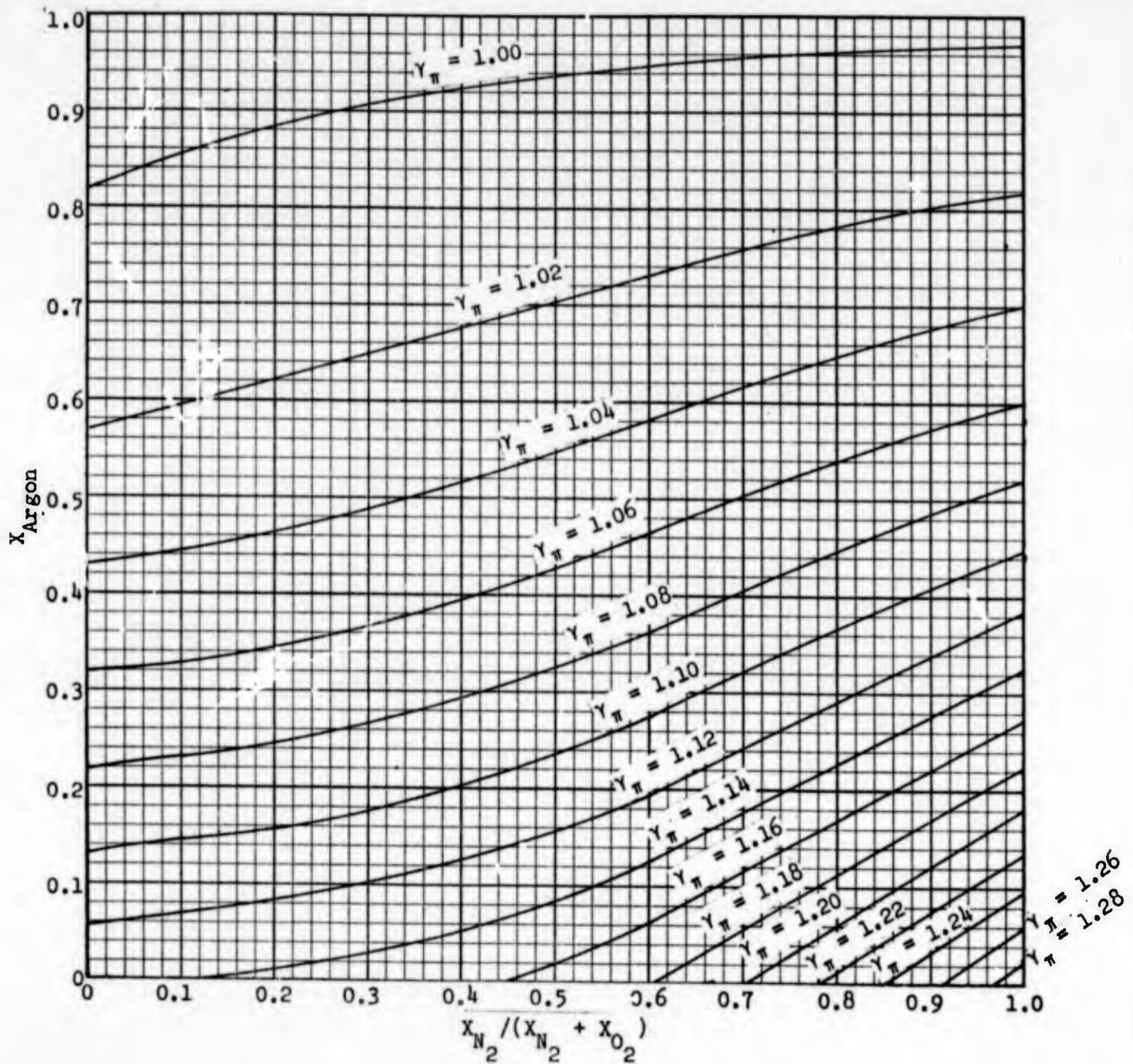


Figure 149. Argon Pressure Activity Coefficients, 2 Atmospheres.

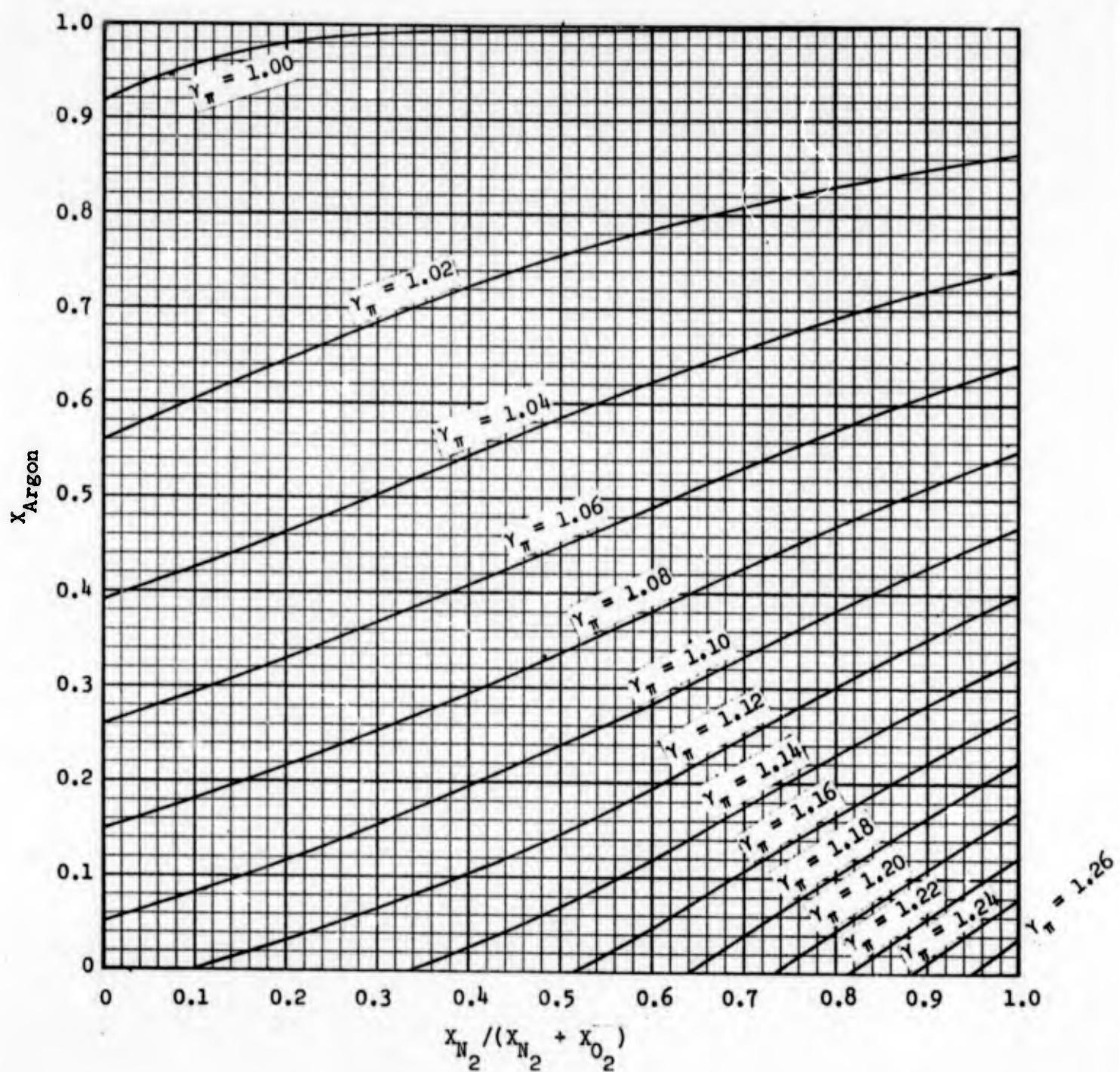


Figure 150. Argon Pressure Activity Coefficients, 4 Atmospheres.

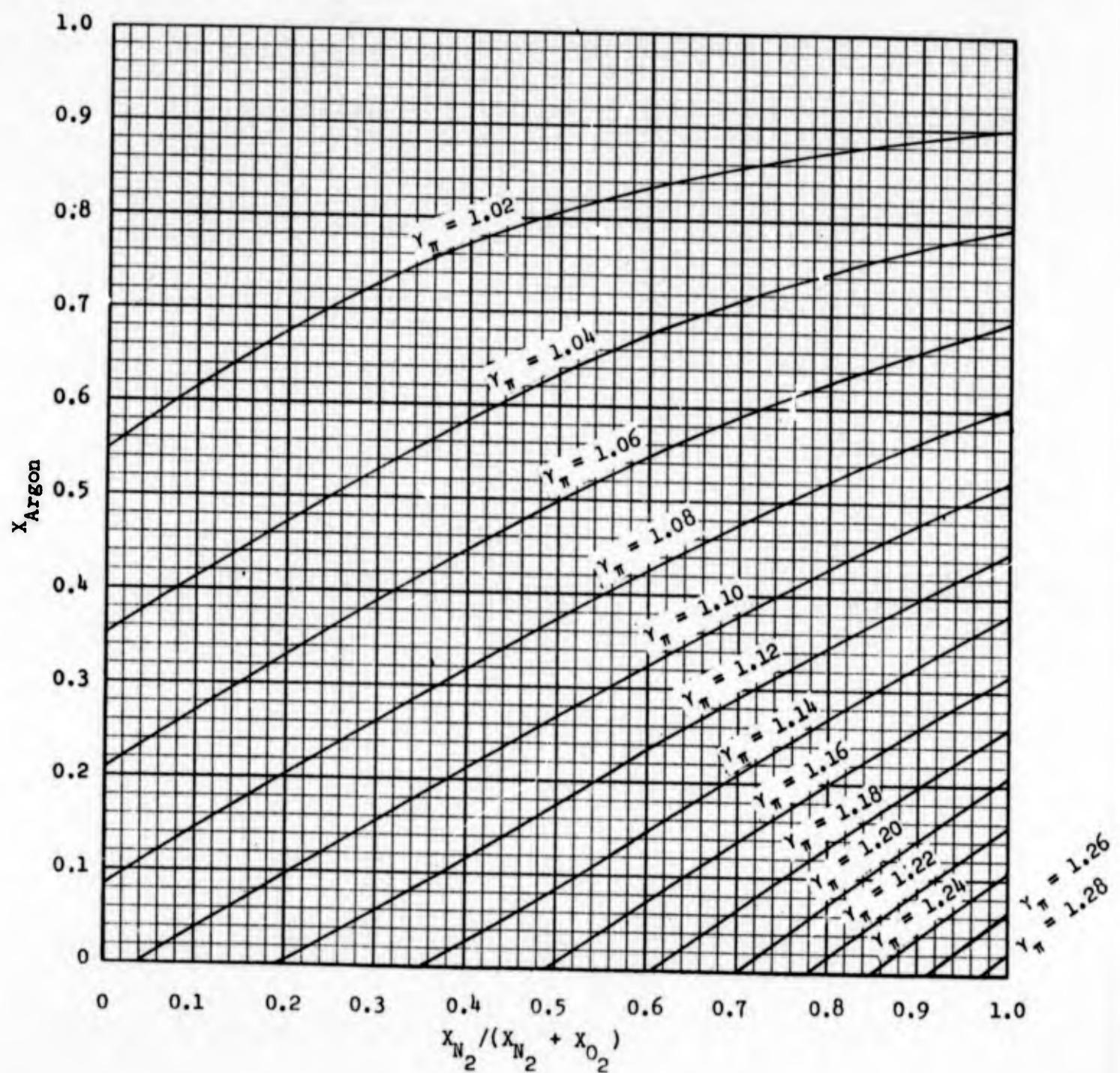


Figure 151. Argon Pressure Activity Coefficients, 6 Atmospheres.

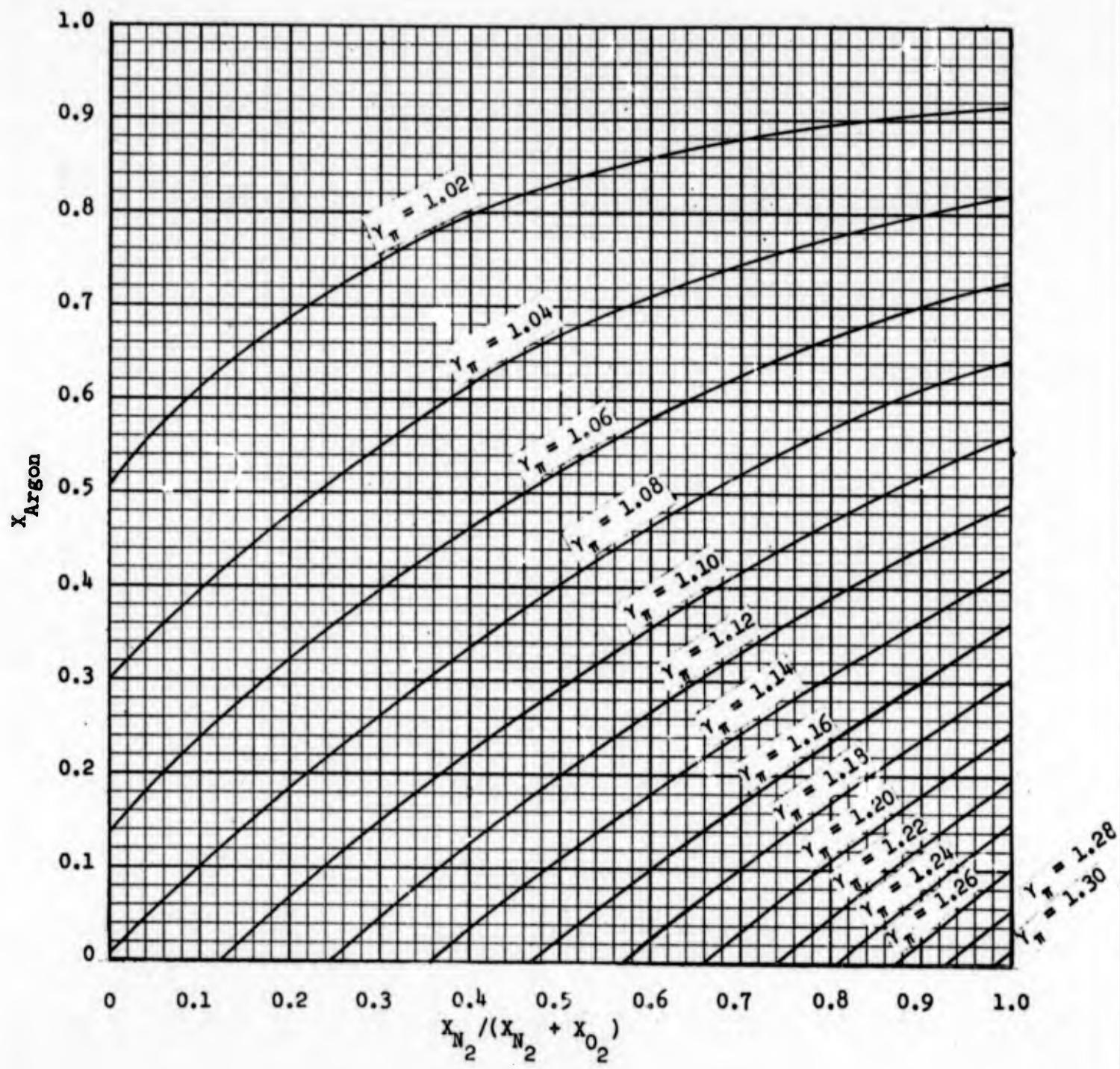


Figure 152. Argon Pressure Activity Coefficients, 8 Atmospheres.

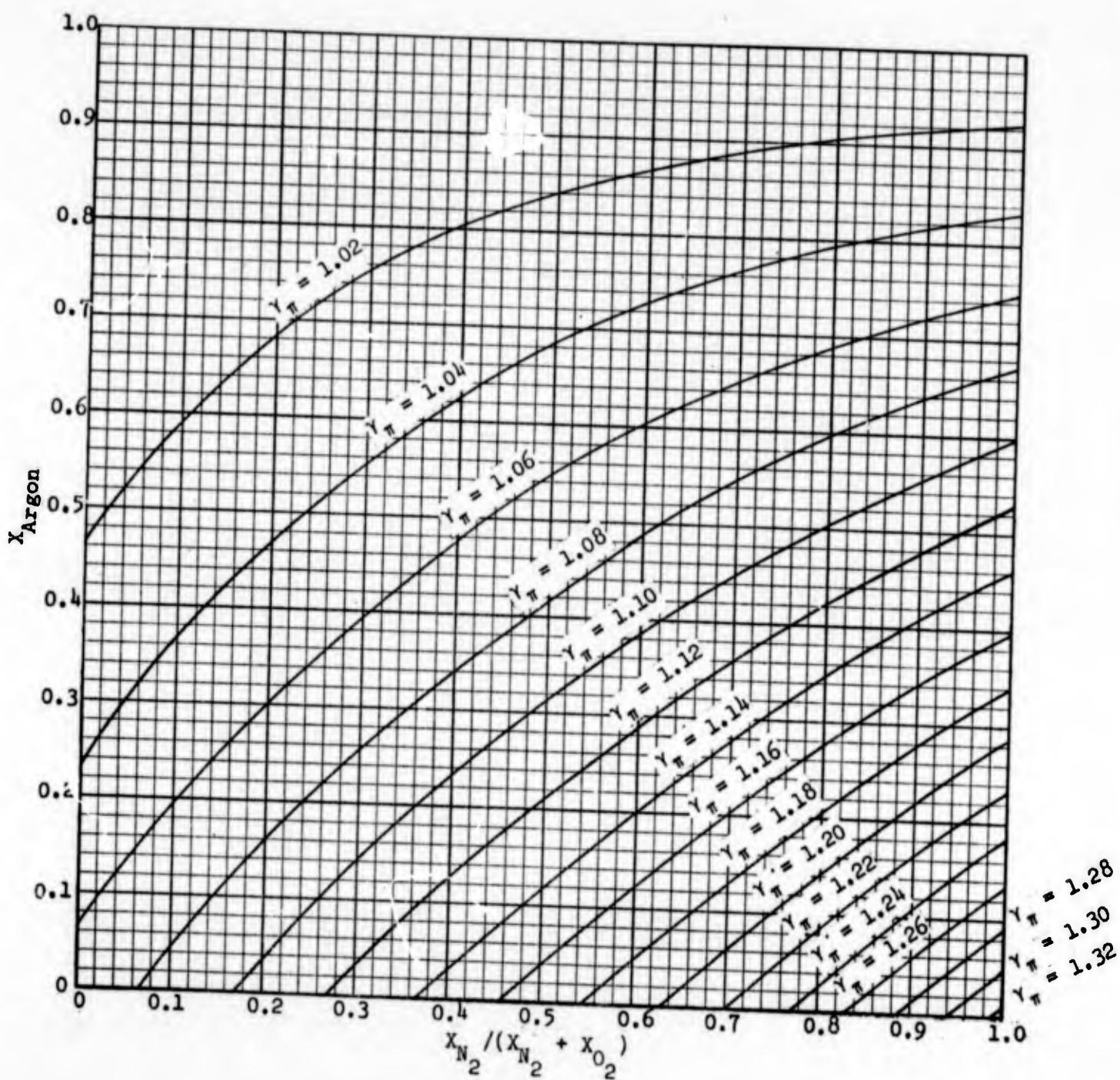


Figure 153. Argon Pressure Activity Coefficients, 10 Atmospheres.

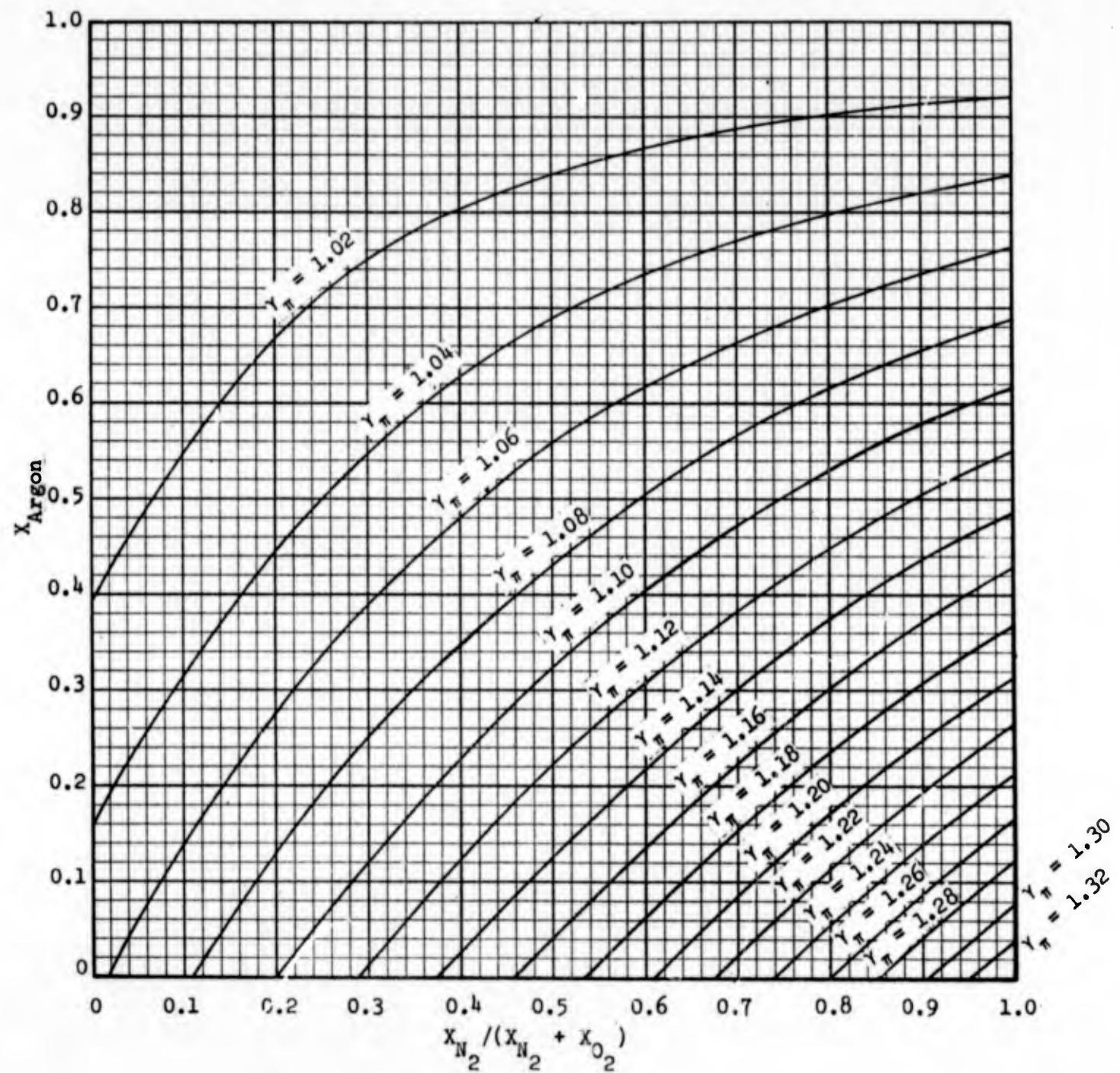


Figure 154. Argon Pressure Activity Coefficients, 12 Atmospheres.

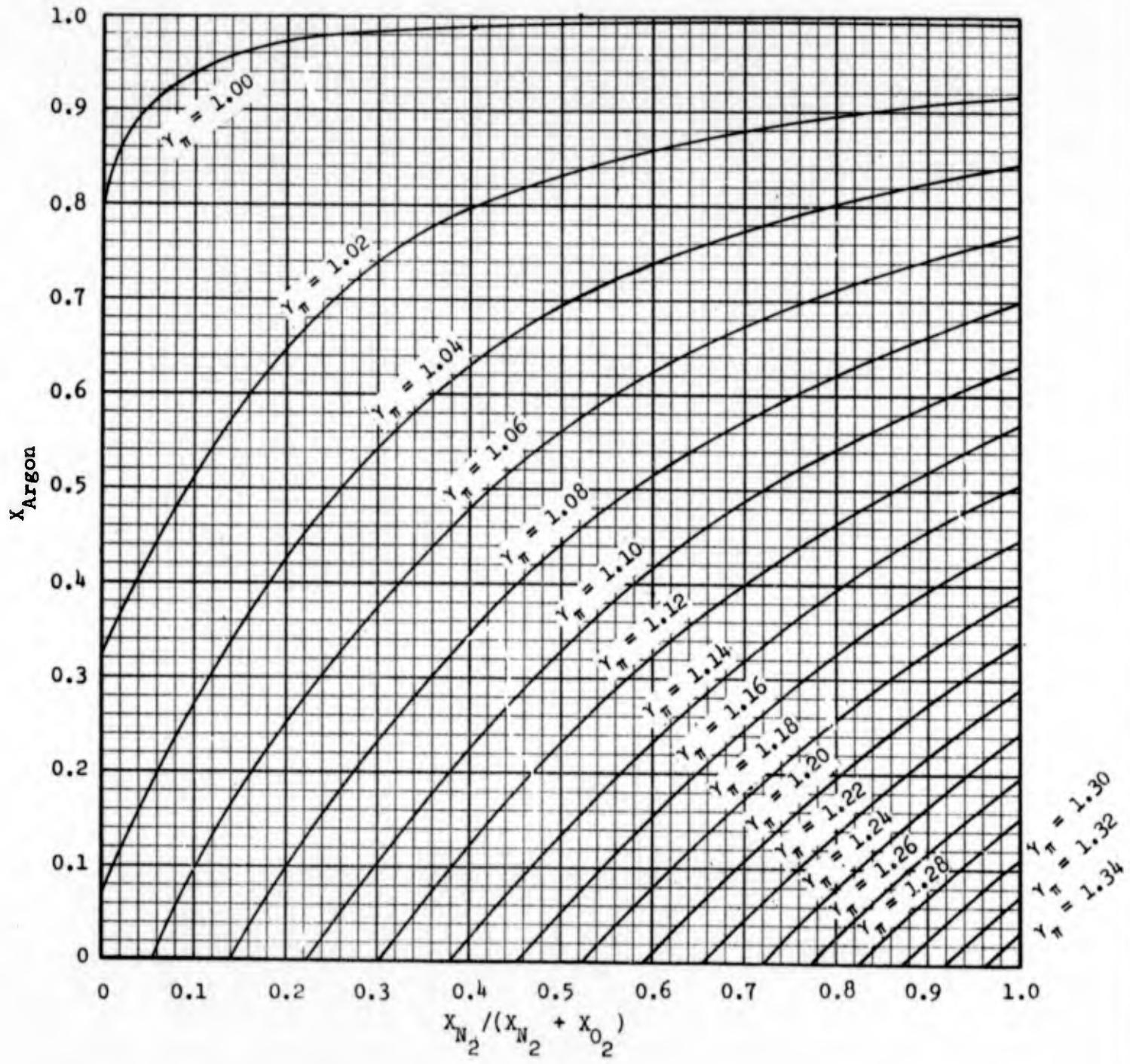


Figure 155. Argon Pressure Activity Coefficients, 14 Atmospheres.

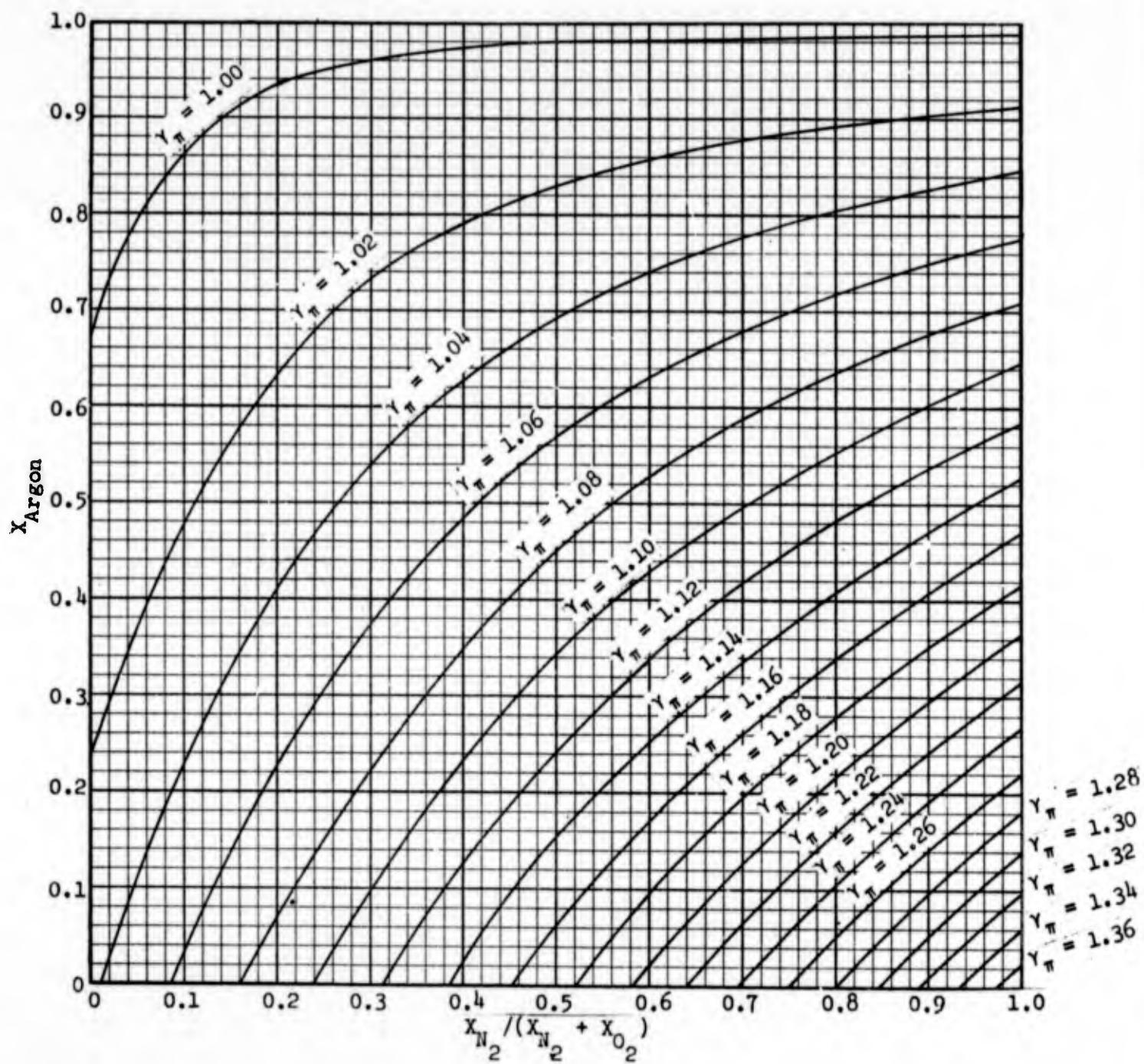


Figure 156. Argon Pressure Activity Coefficients, 16 Atmospheres.

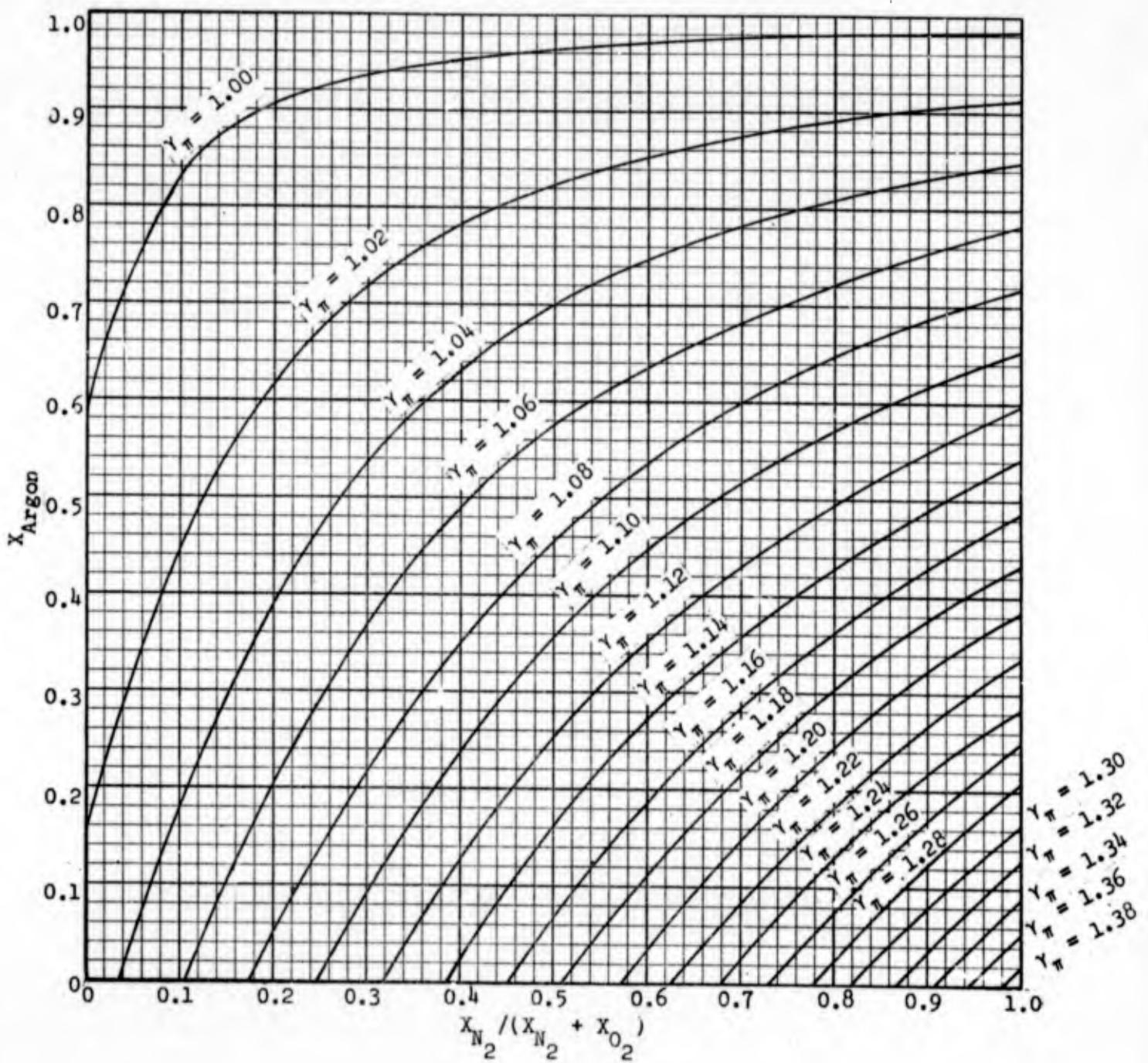


Figure 157. Argon Pressure Activity Coefficients, 18 Atmospheres.

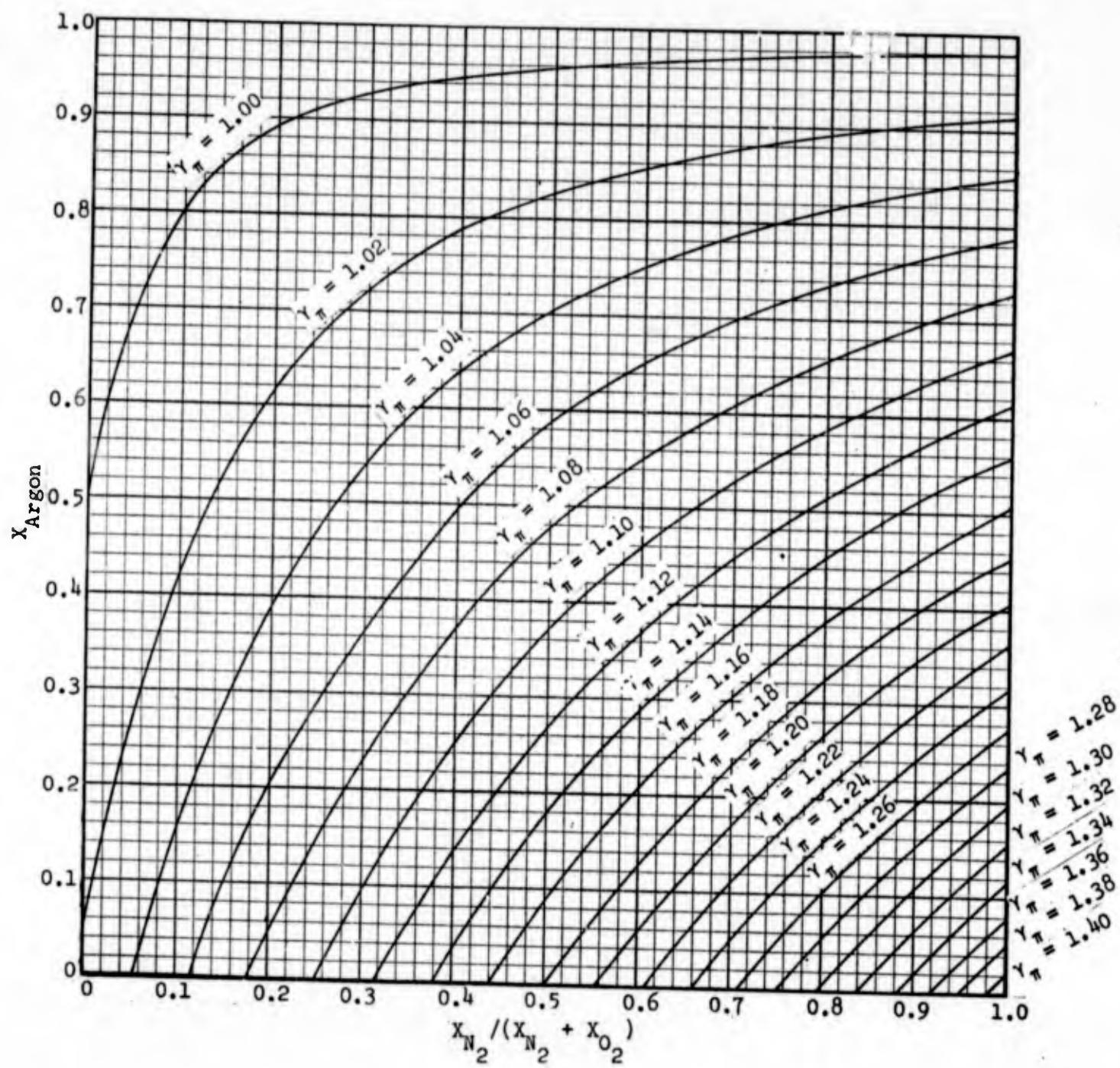


Figure 158. Argon Pressure Activity Coefficients, 20 Atmospheres.

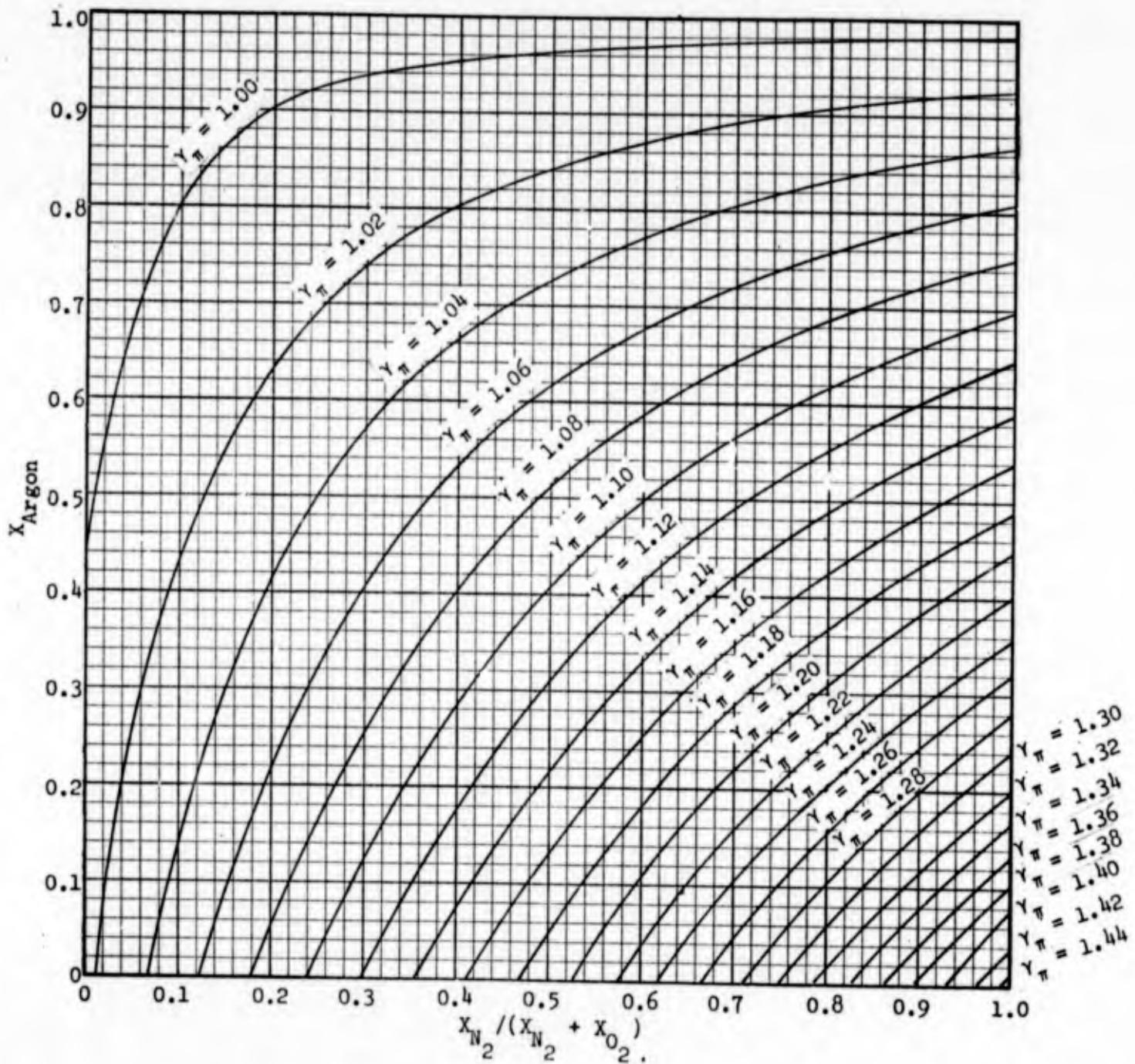


Figure 159. Argon Pressure Activity Coefficients, 23 Atmospheres.

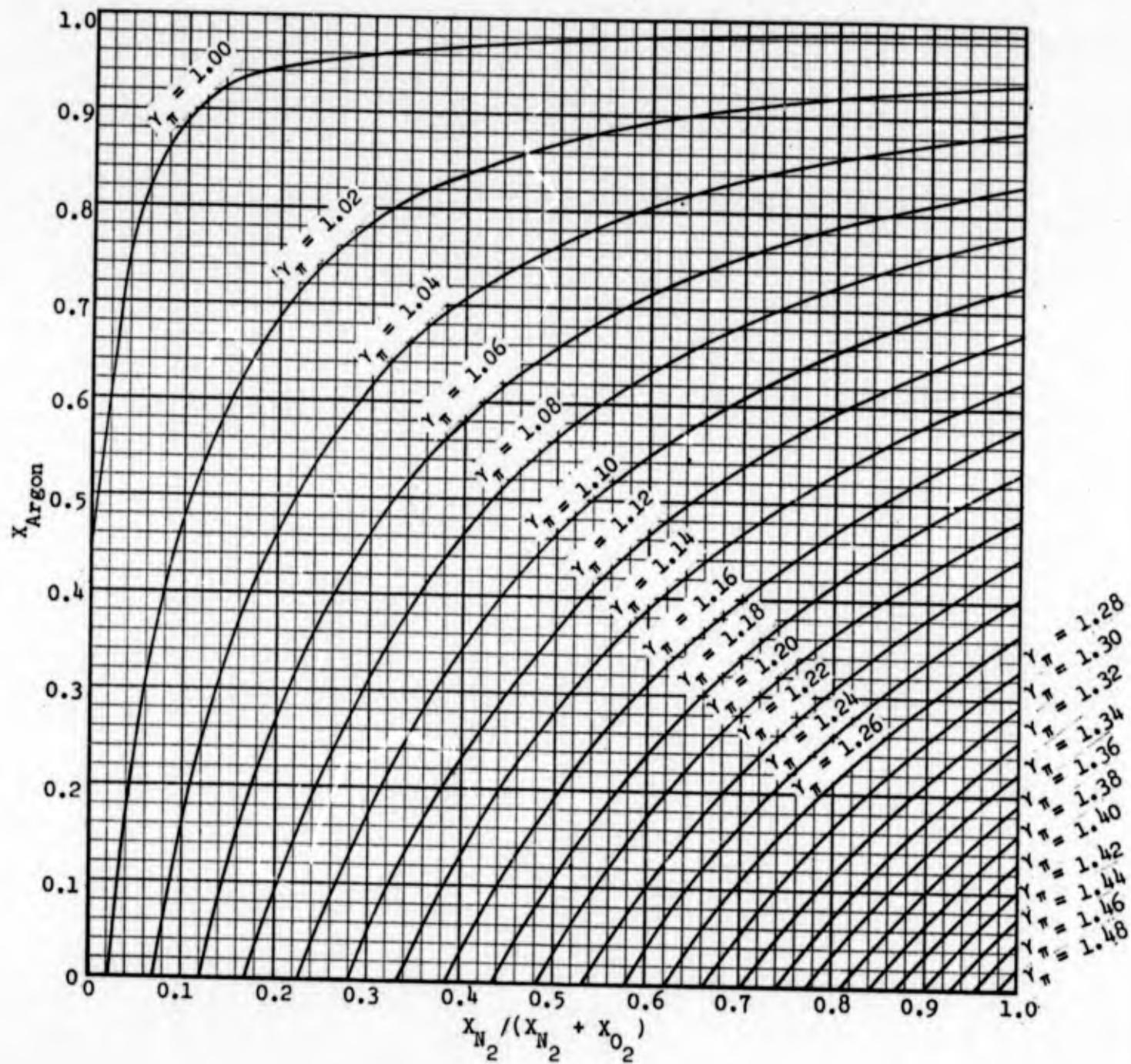


Figure 160. Argon Pressure Activity Coefficients, 26 Atmospheres.

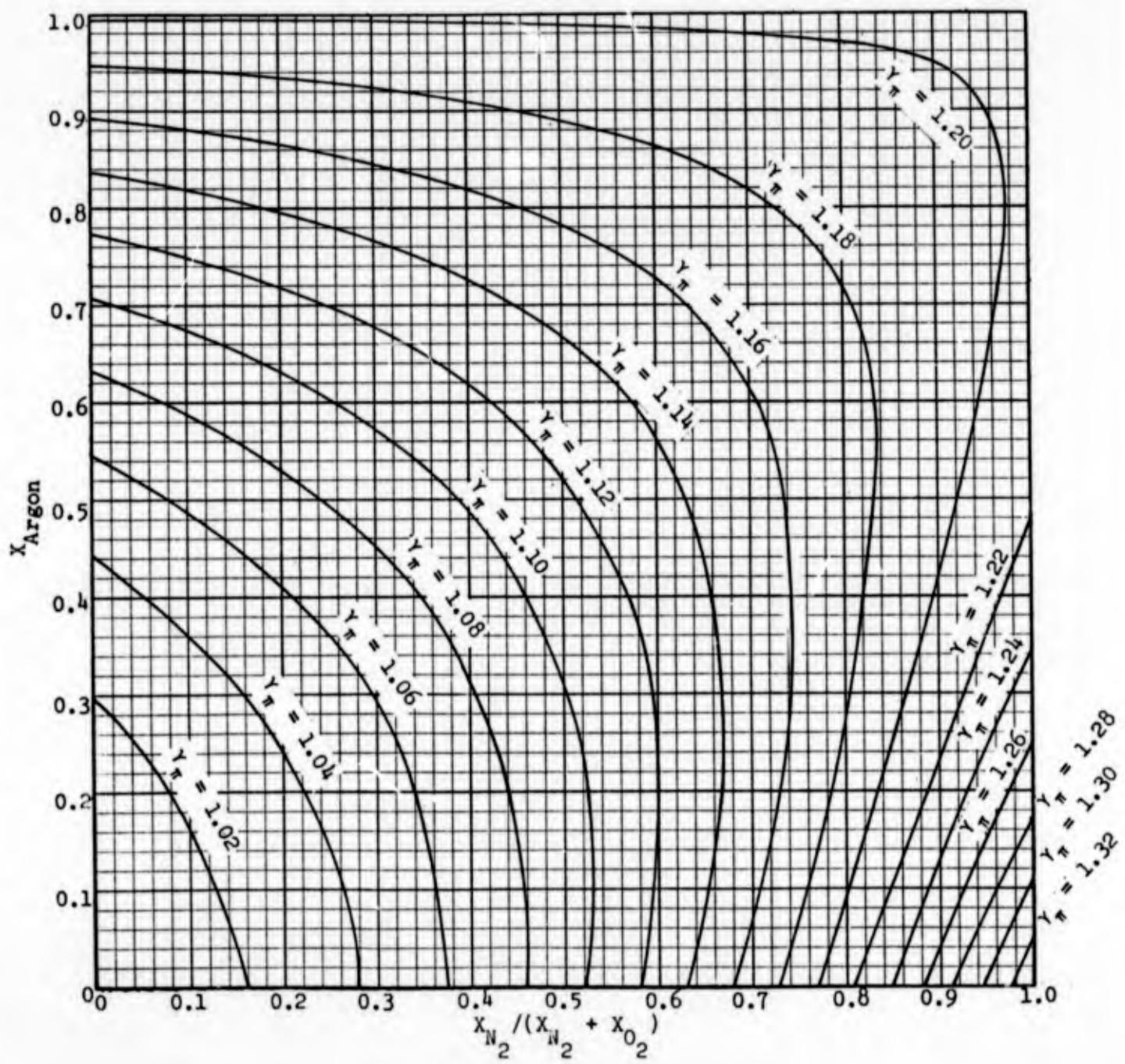


Figure 161. Oxygen Pressure Activity Coefficients, 1 Atmosphere.

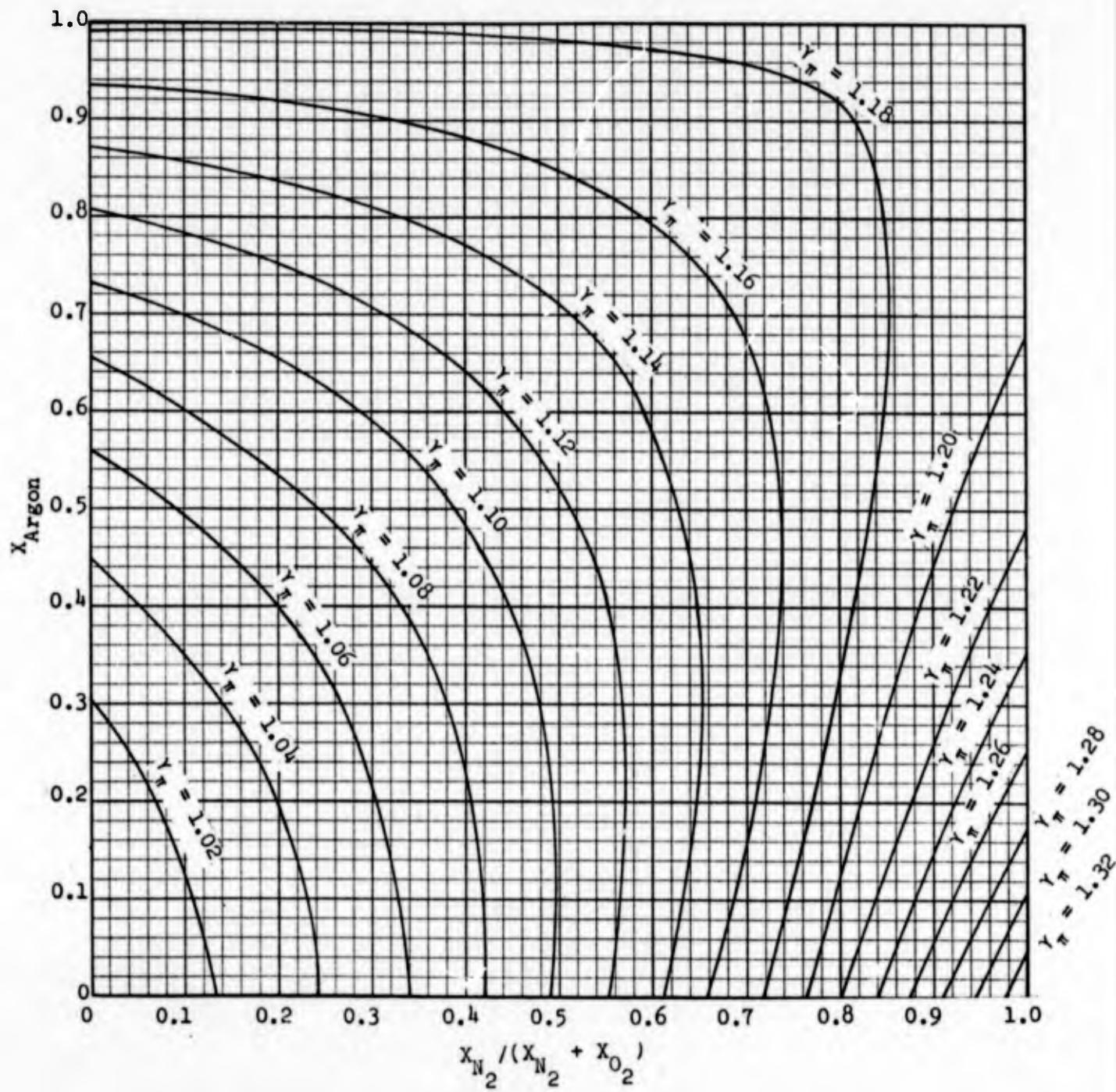


Figure 162. Oxygen Pressure Activity Coefficients, 2 Atmospheres.

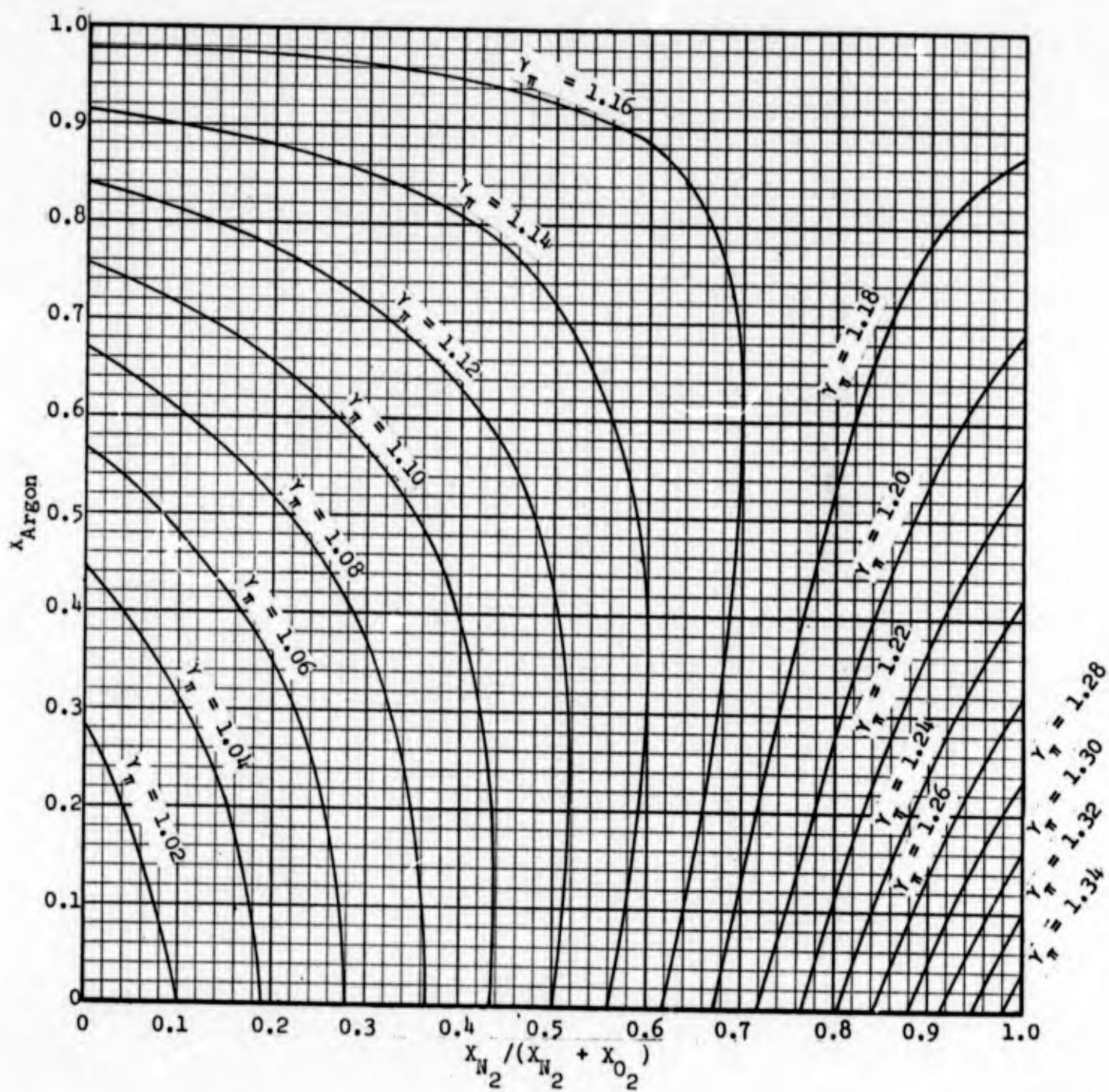


Figure 163. Oxygen Pressure Activity Coefficients, 4 Atmospheres.

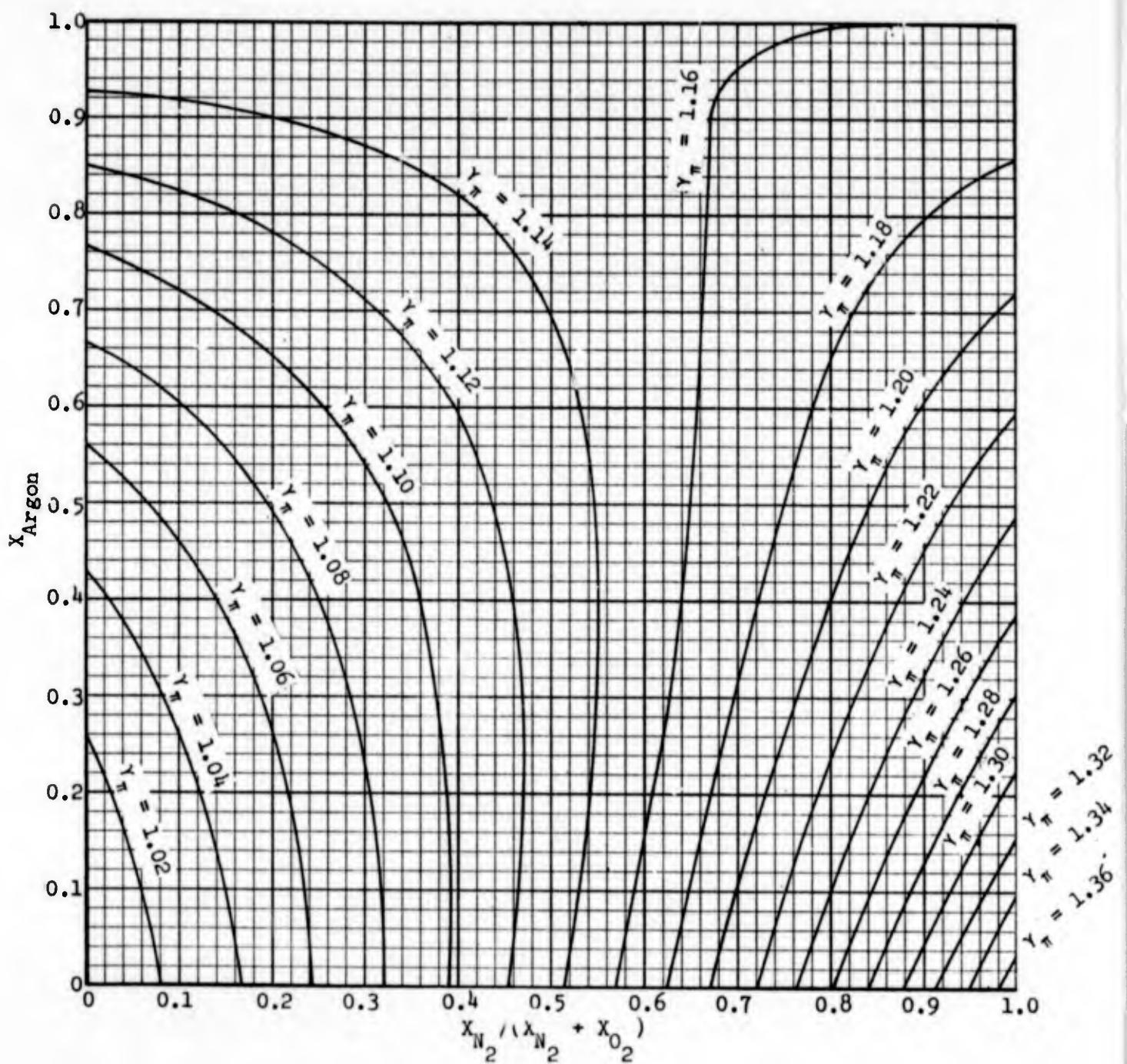


Figure 164. Oxygen Pressure Activity Coefficients, 6 Atmospheres.

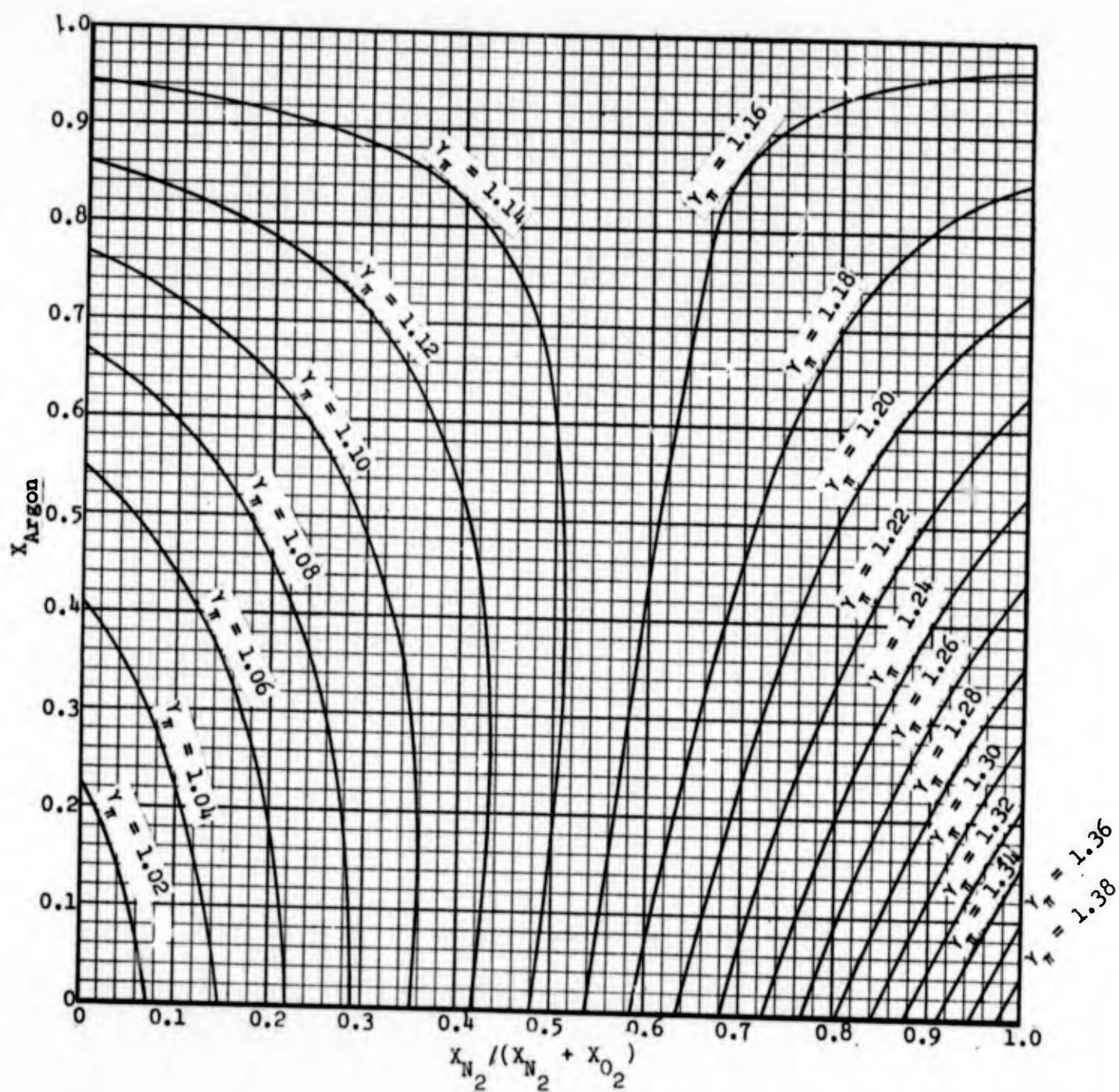


Figure 165. Oxygen Pressure Activity Coefficients, 8 Atmospheres.

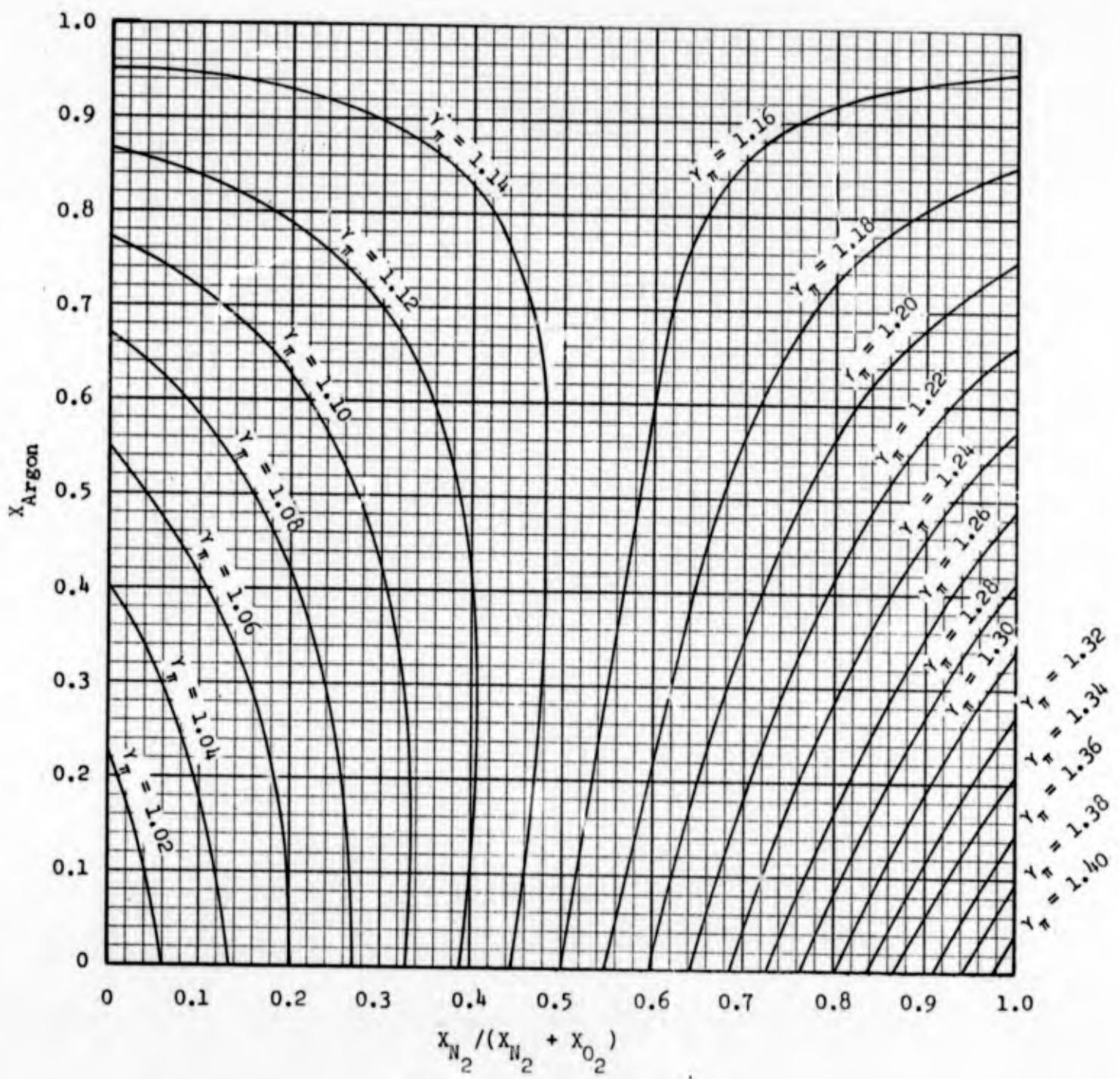


Figure 166. Oxygen Pressure Activity Coefficients, 10 Atmospheres.

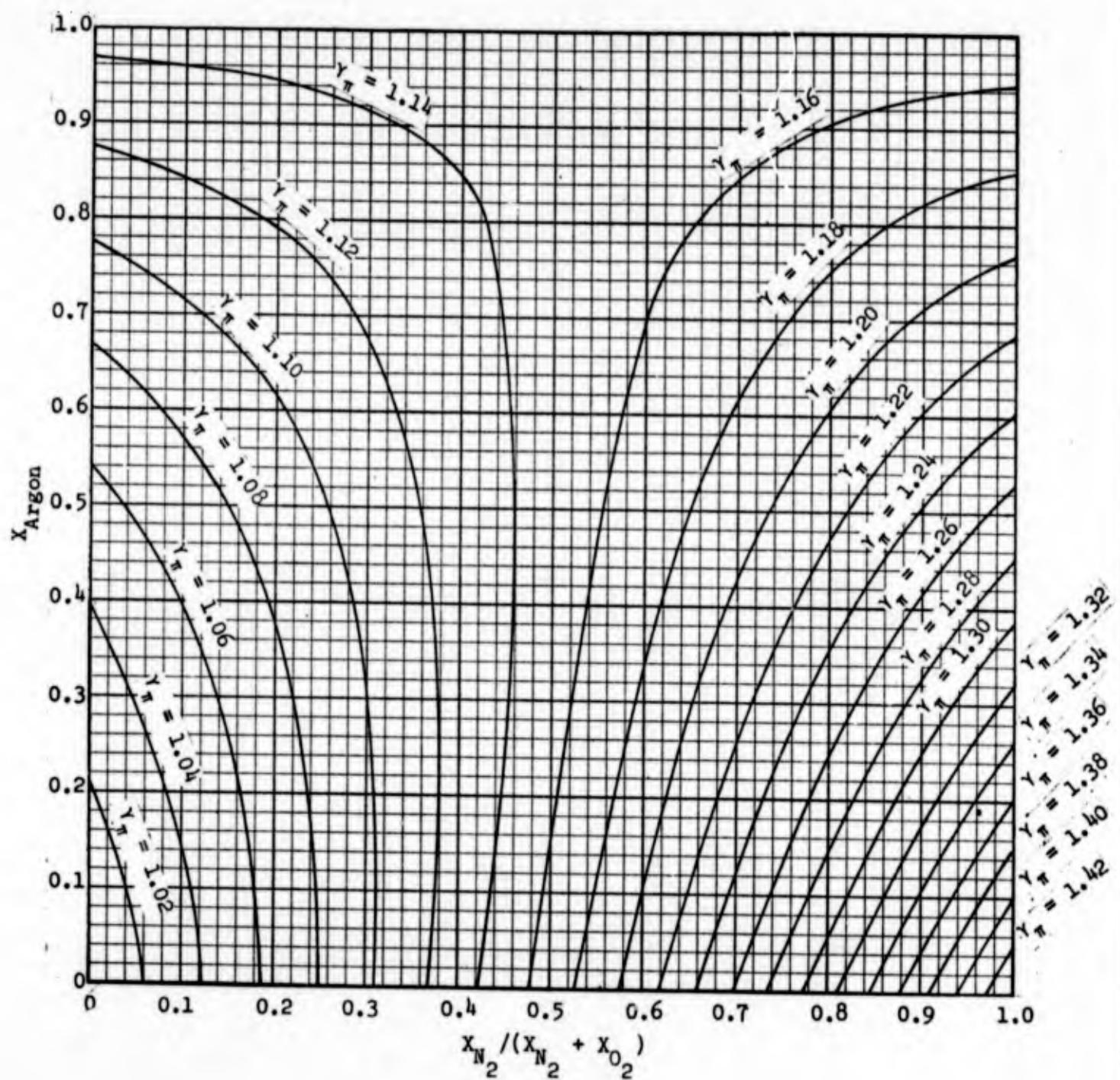


Figure 167. Oxygen Pressure Activity Coefficients, 12 Atmospheres.

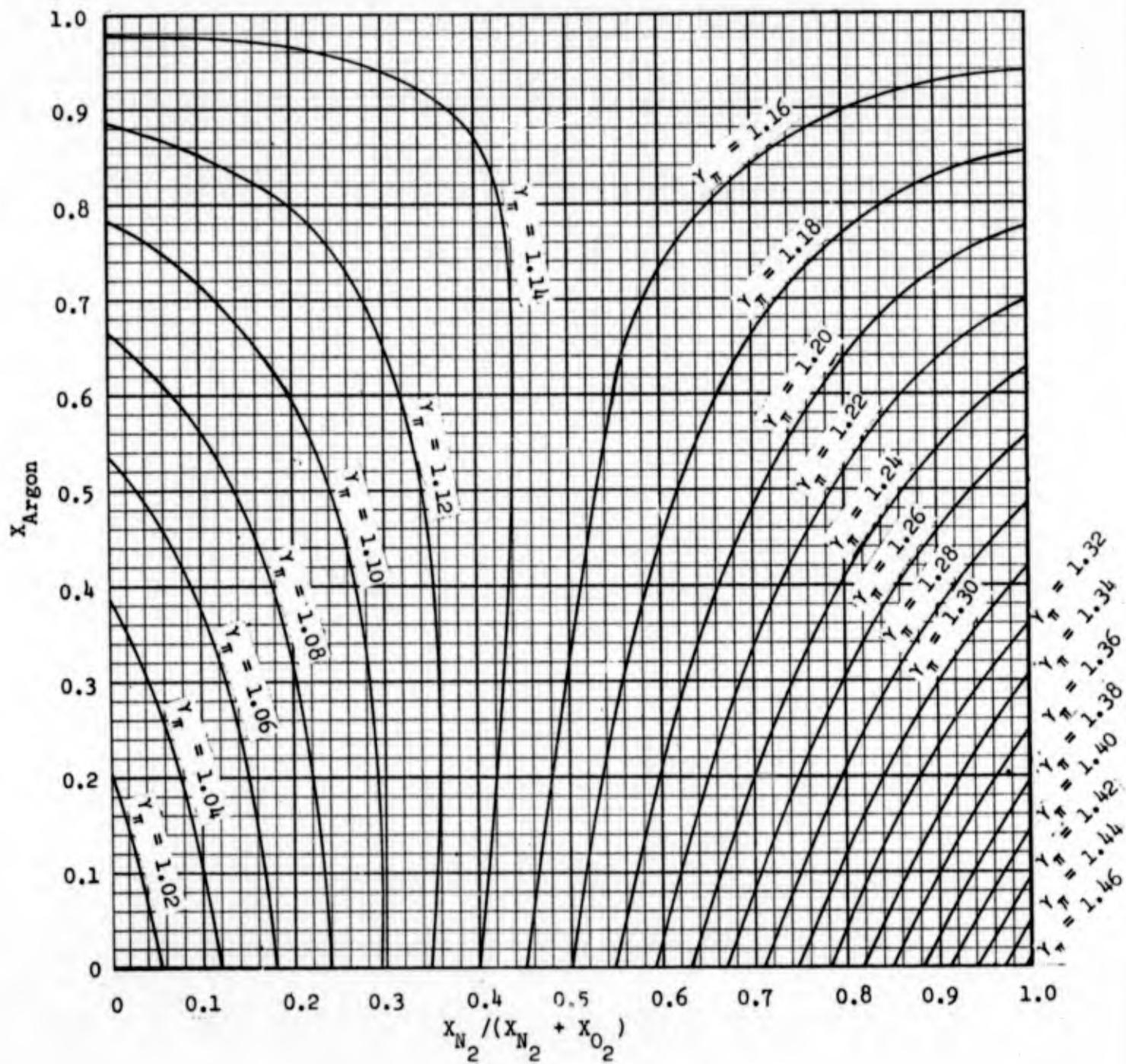


Figure 168. Oxygen Pressure Activity Coefficients, 14 Atmospheres,

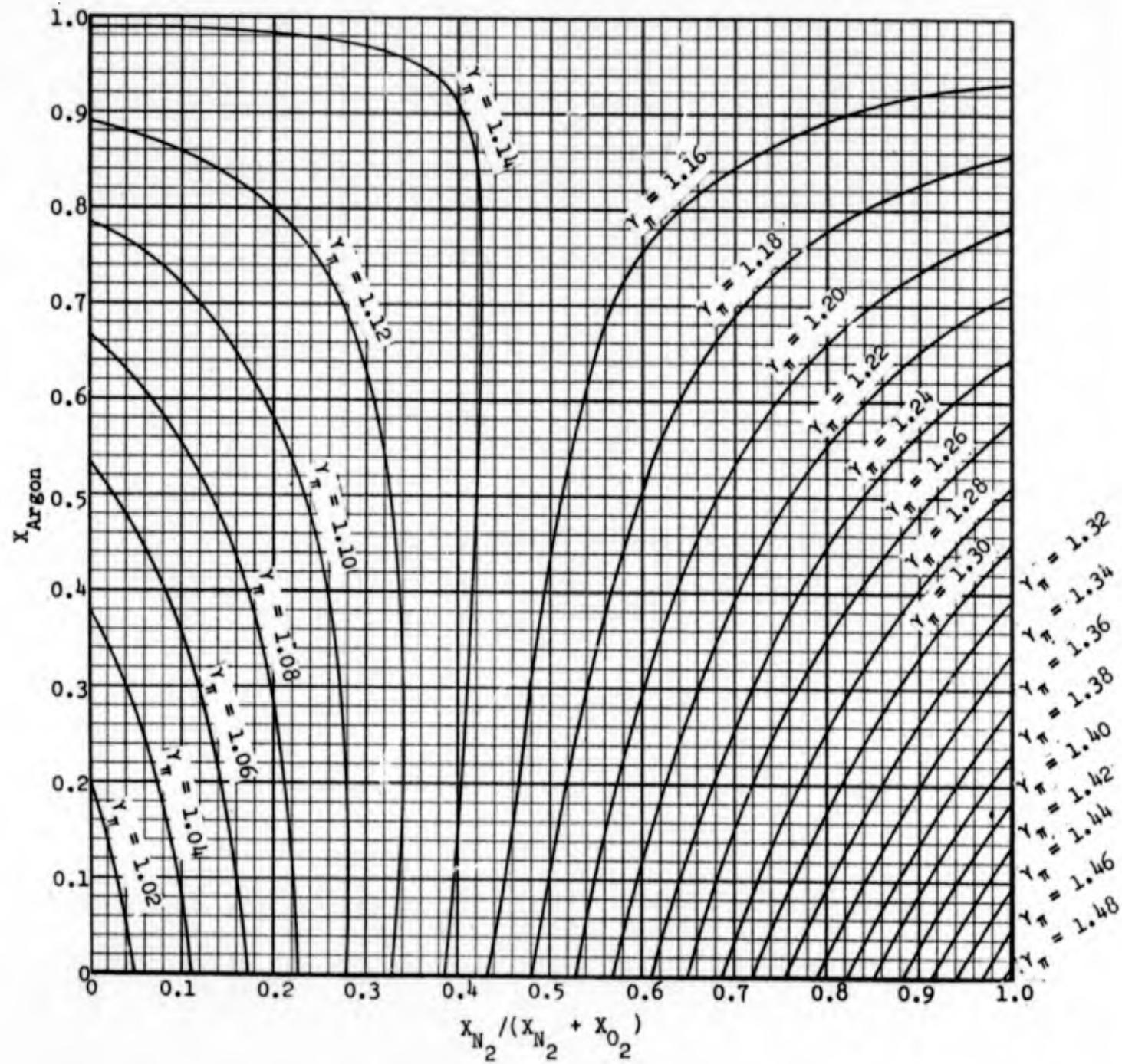


Figure 169. Oxygen Pressure Activity Coefficients, 16 Atmospheres.

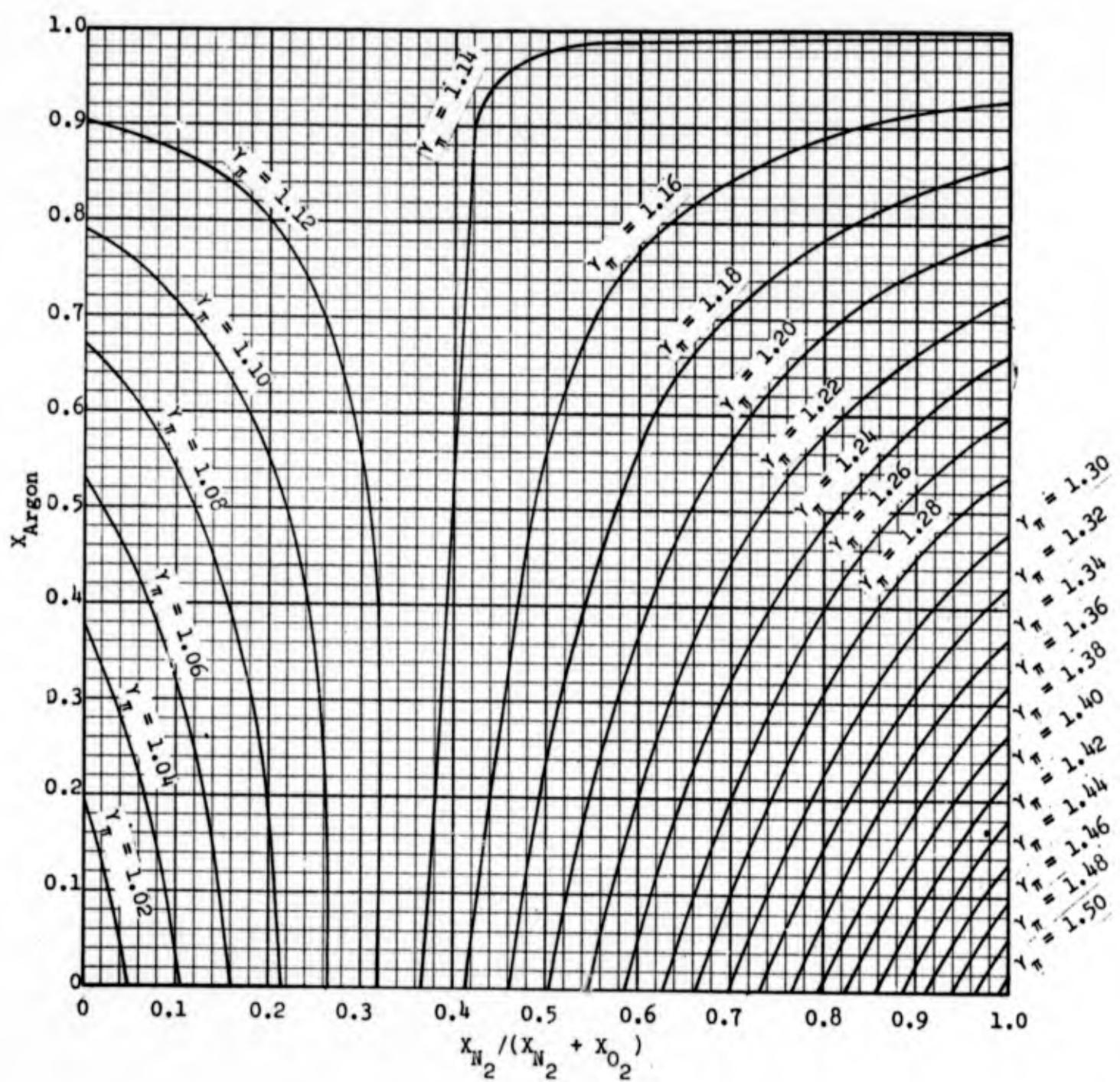


Figure 170. Oxygen Pressure Activity Coefficients, 18 Atmospheres.

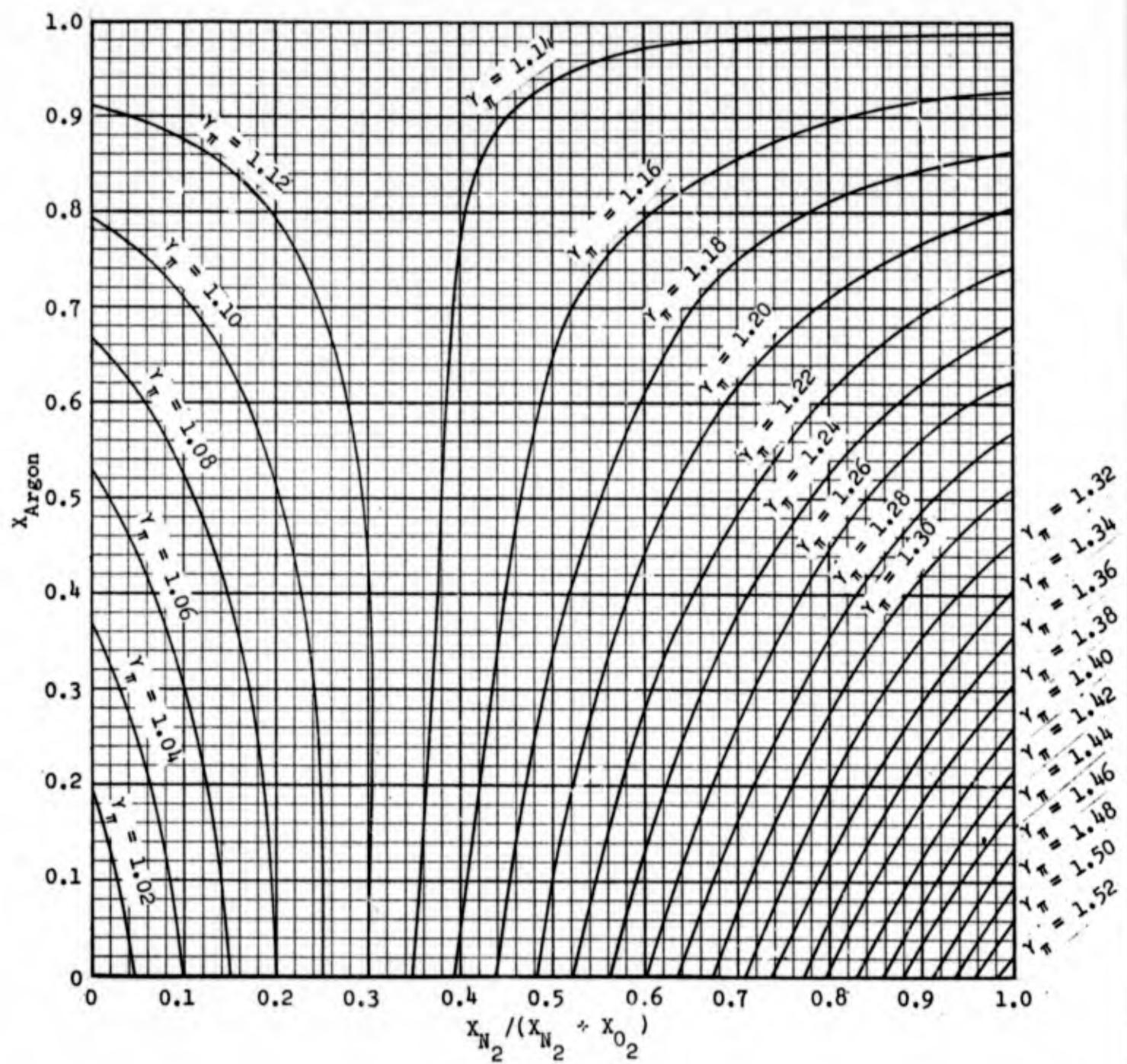


Figure 171. Oxygen Pressure Activity Coefficients, 20 Atmospheres.

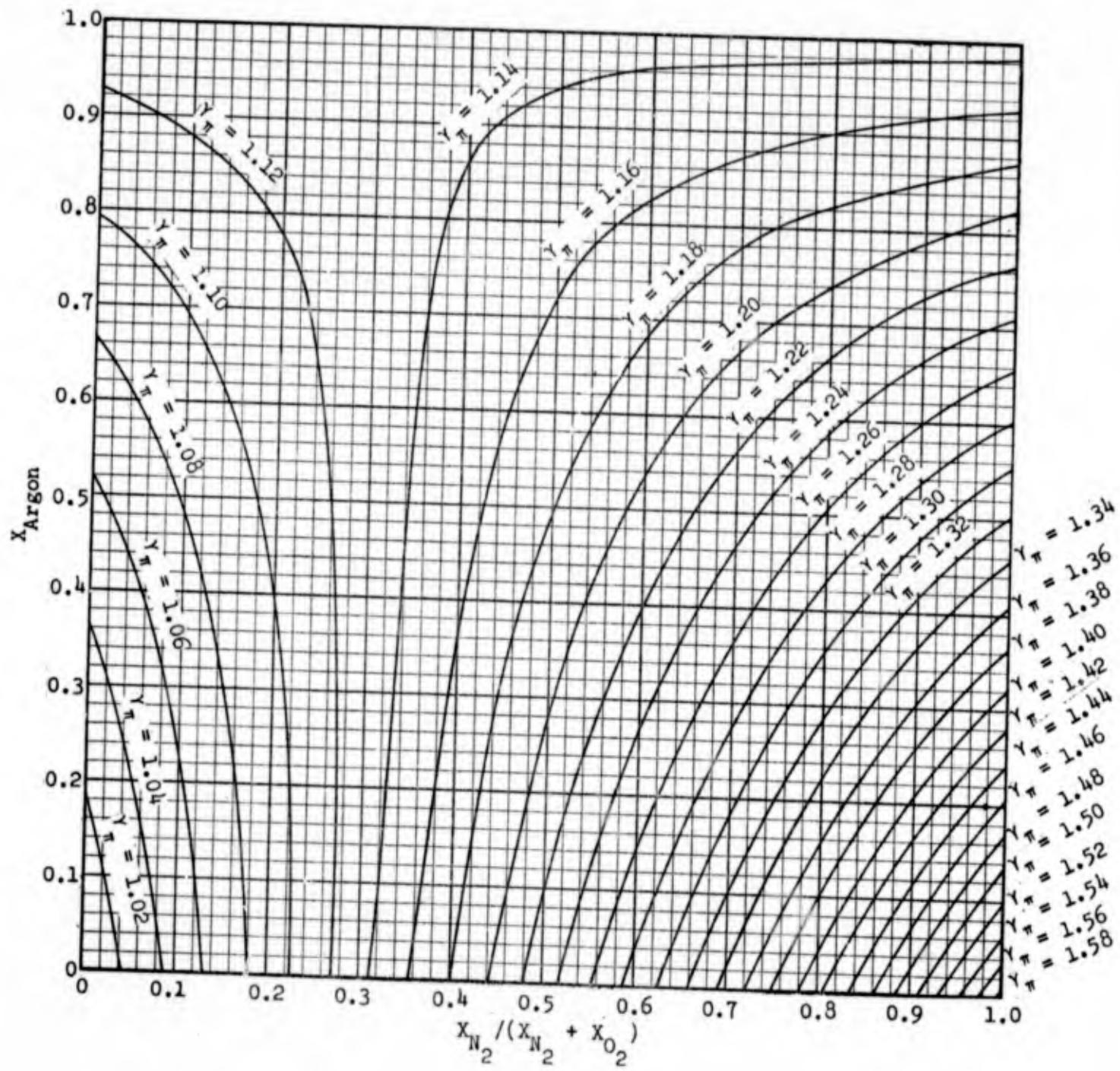


Figure 172. Oxygen Pressure Activity Coefficients, 23 Atmospheres.

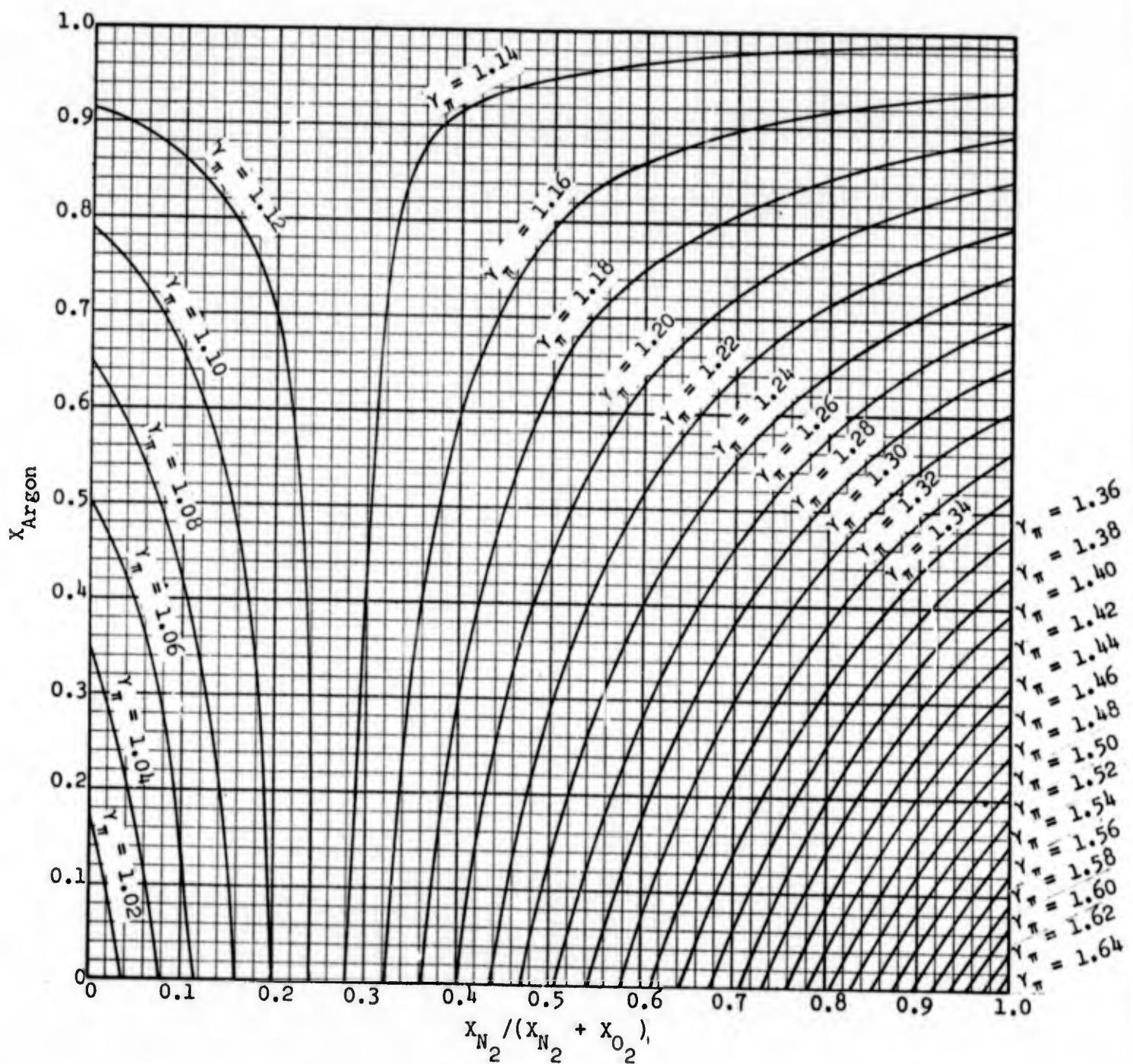


Figure 173. Oxygen Pressure Activity Coefficients, 26 Atmospheres.



G. Mixture Vapor Pressures Vs. Temperatures

The 13 graphs to follow present the vapor pressure of a number of specific mixtures as it varies with temperature. These graphs are plotted as $\log P$ vs. $1/T$. The graphs are ordered with respect to increasing mole fraction argon in the liquid.

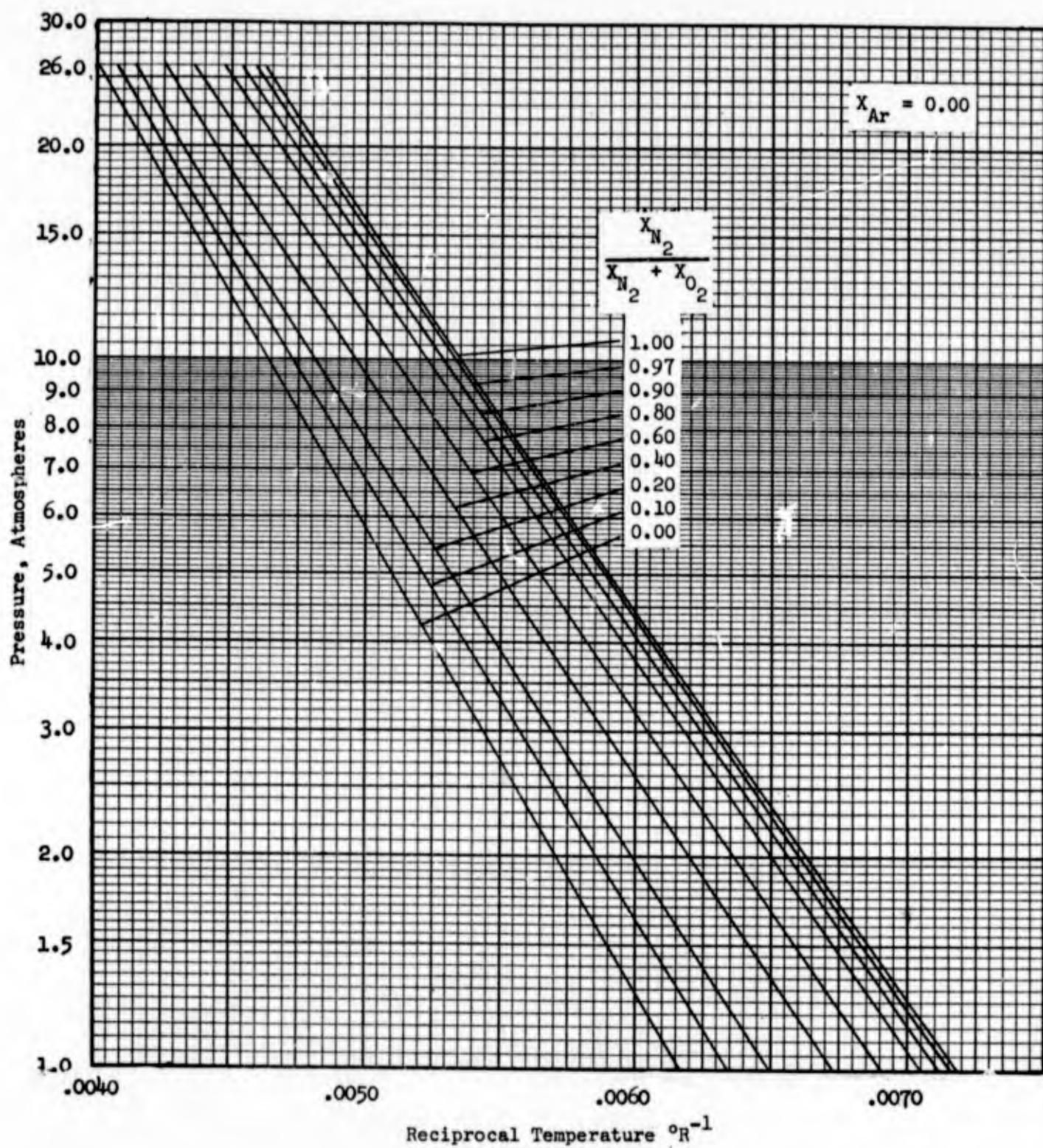


Figure 174. Vapor Pressures of Specific Mixtures of N_2 -Ar- O_2 .

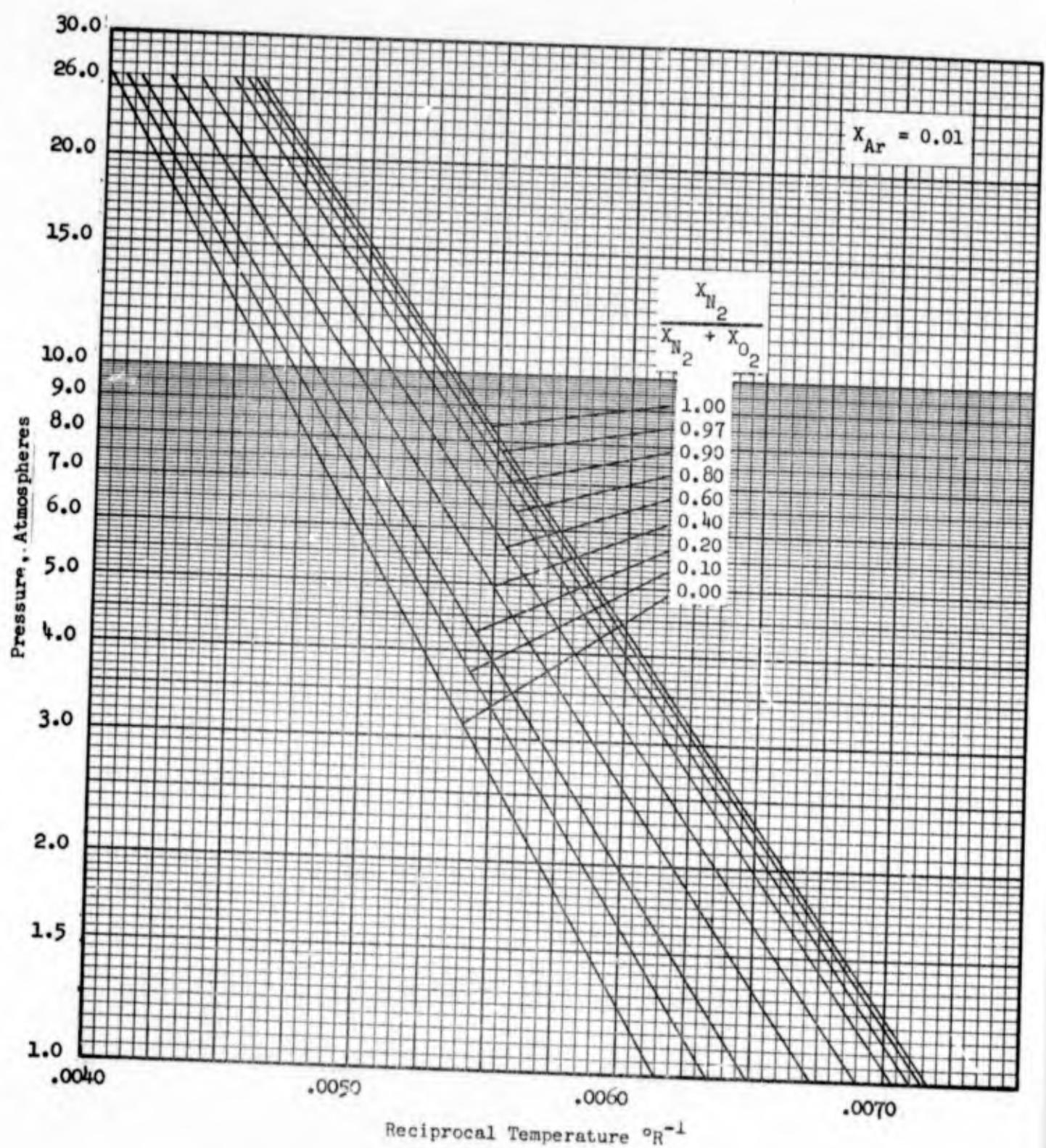


Figure 175. Vapor Pressures of Specific Mixtures of N_2 -Ar- O_2 .

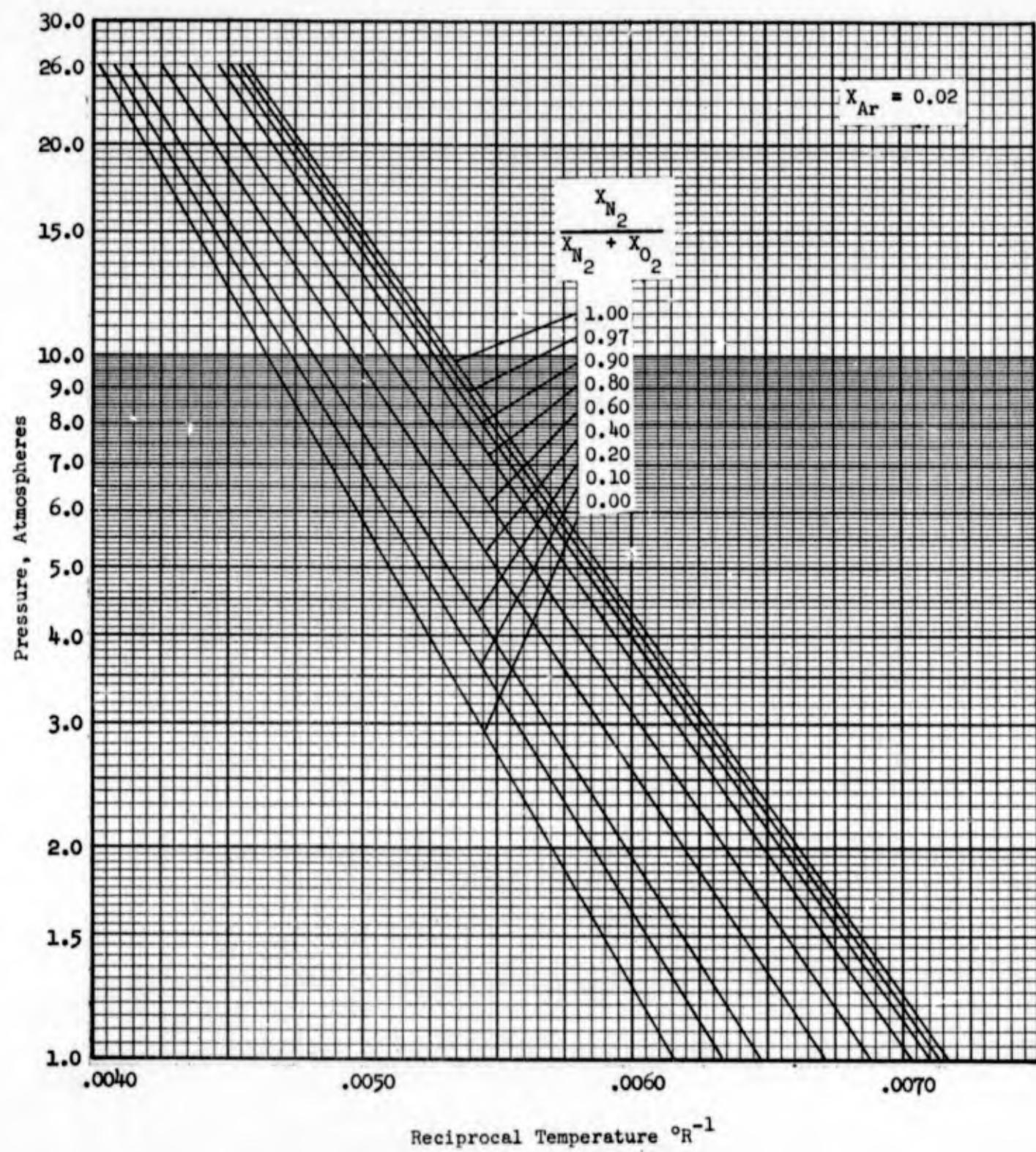


Figure 176. Vapor Pressures of Specific Mixtures of N_2 -Ar- O_2 .

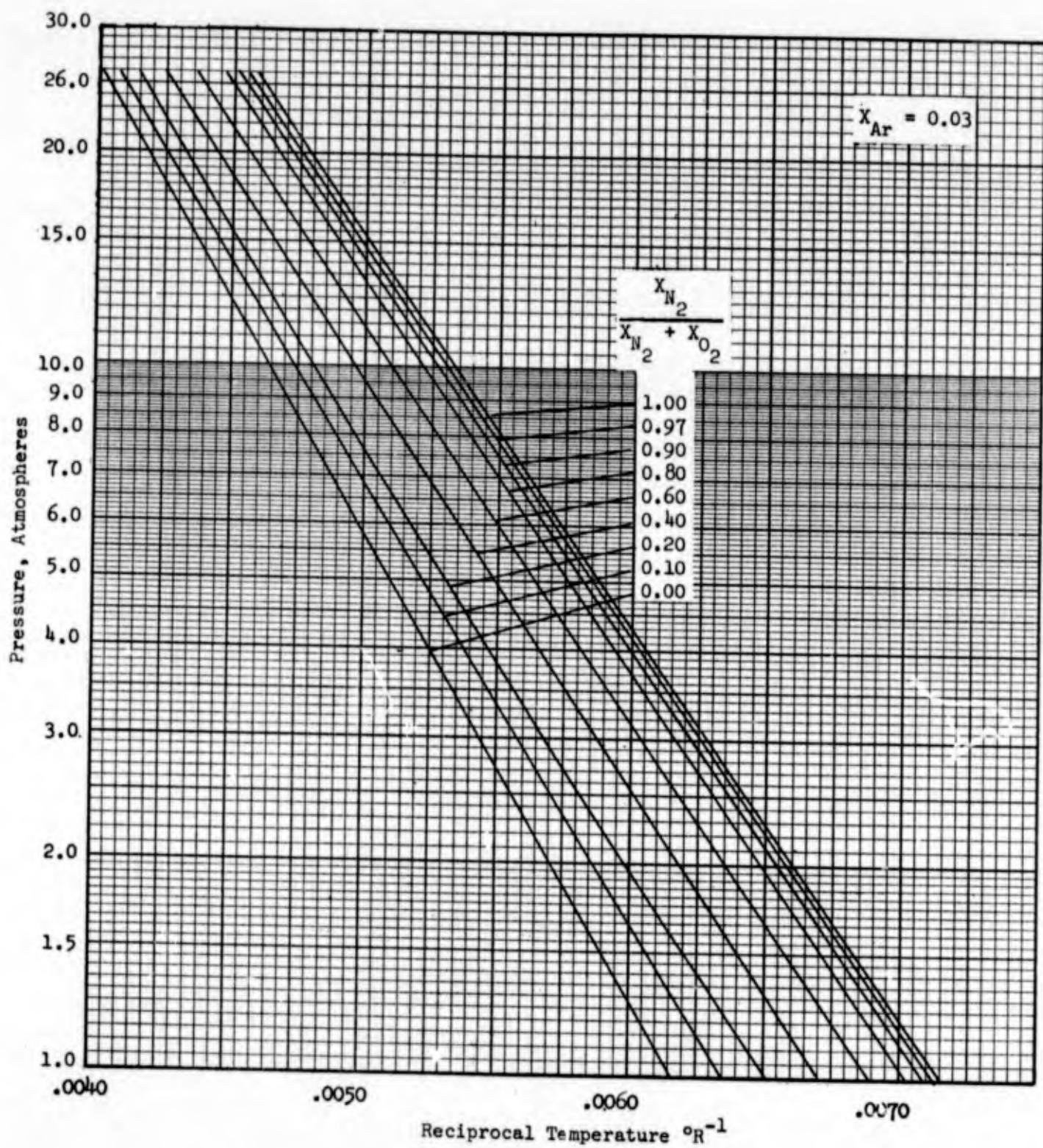


Figure 177. Vapor Pressures of Specific Mixtures of N_2 -Ar- O_2 .

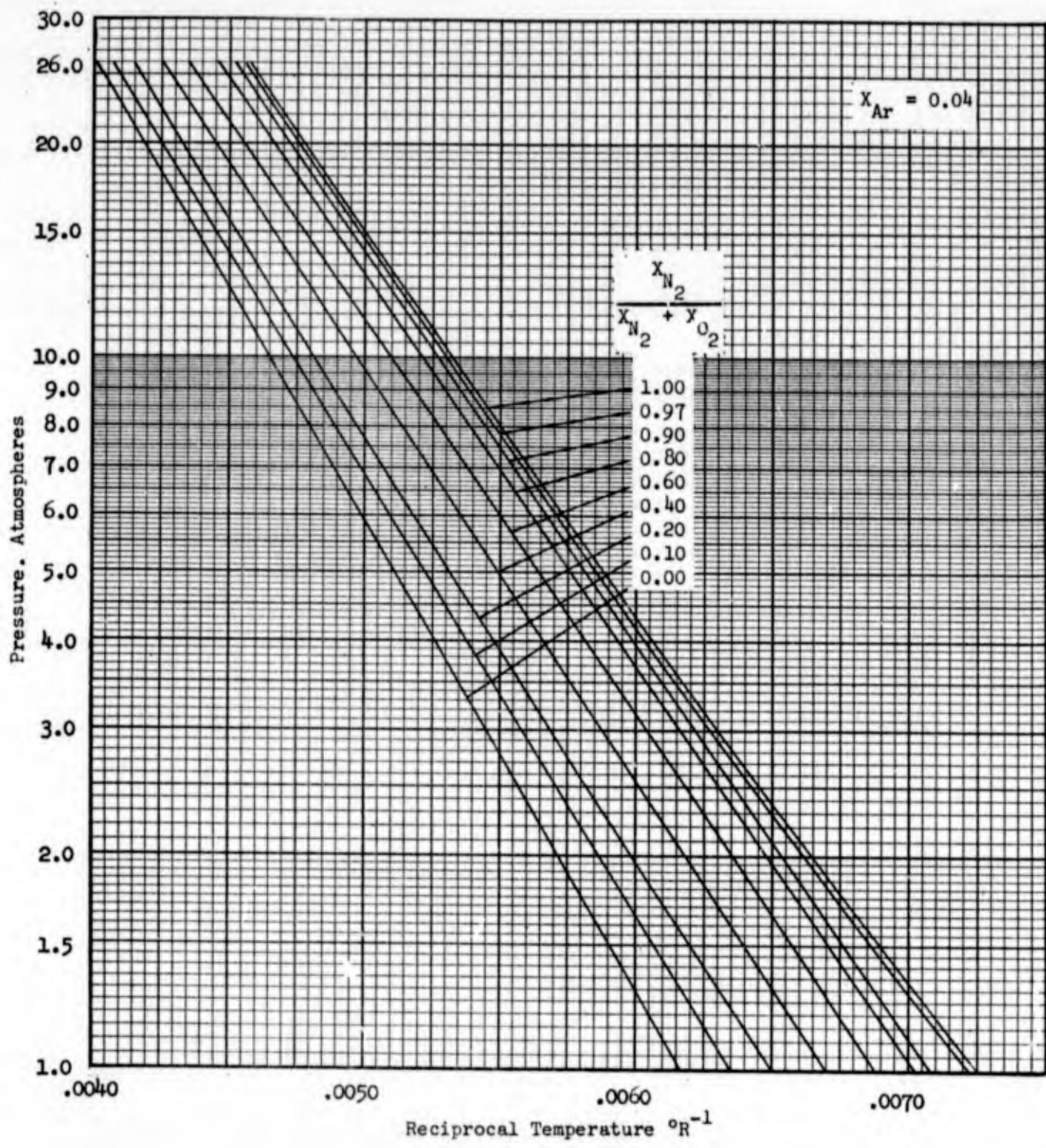


Figure 178. Vapor Pressures of Specific Mixtures of N₂-Ar-O₂.

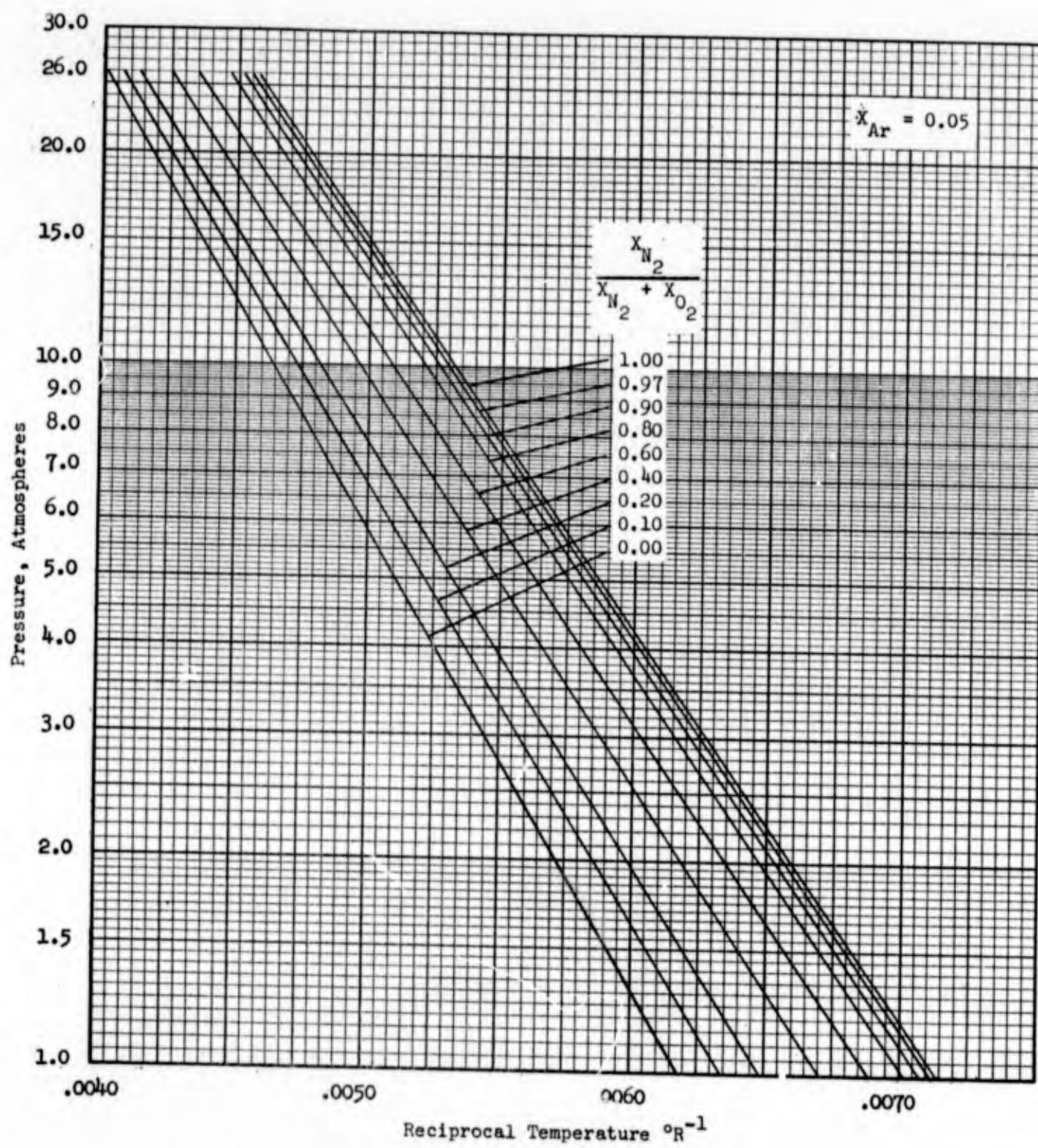


Figure 179. Vapor Pressures of Specific Mixtures of N₂-Ar-O₂.

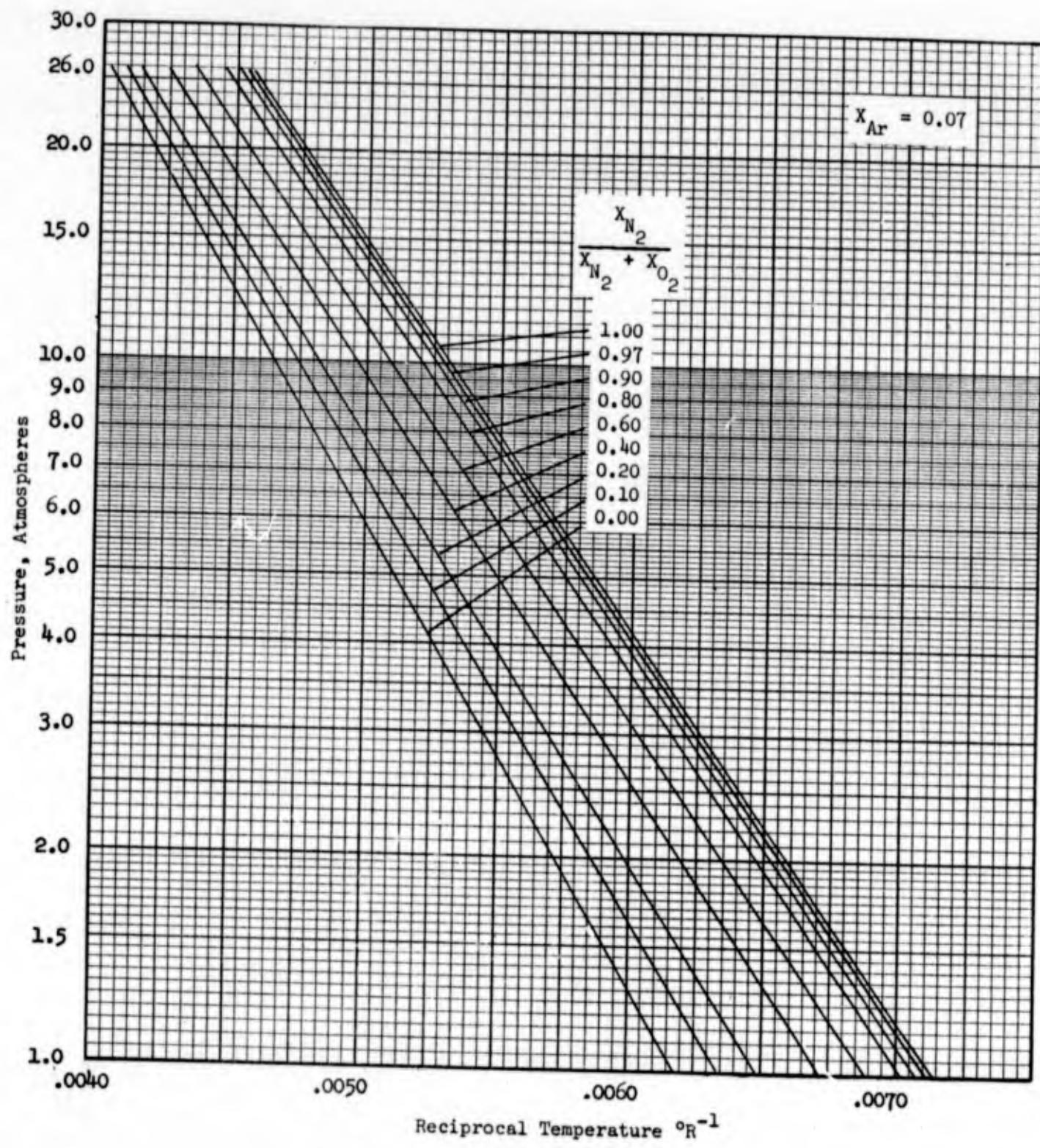


Figure 180. Vapor Pressures of Specific Mixtures of N₂-Ar-O₂.

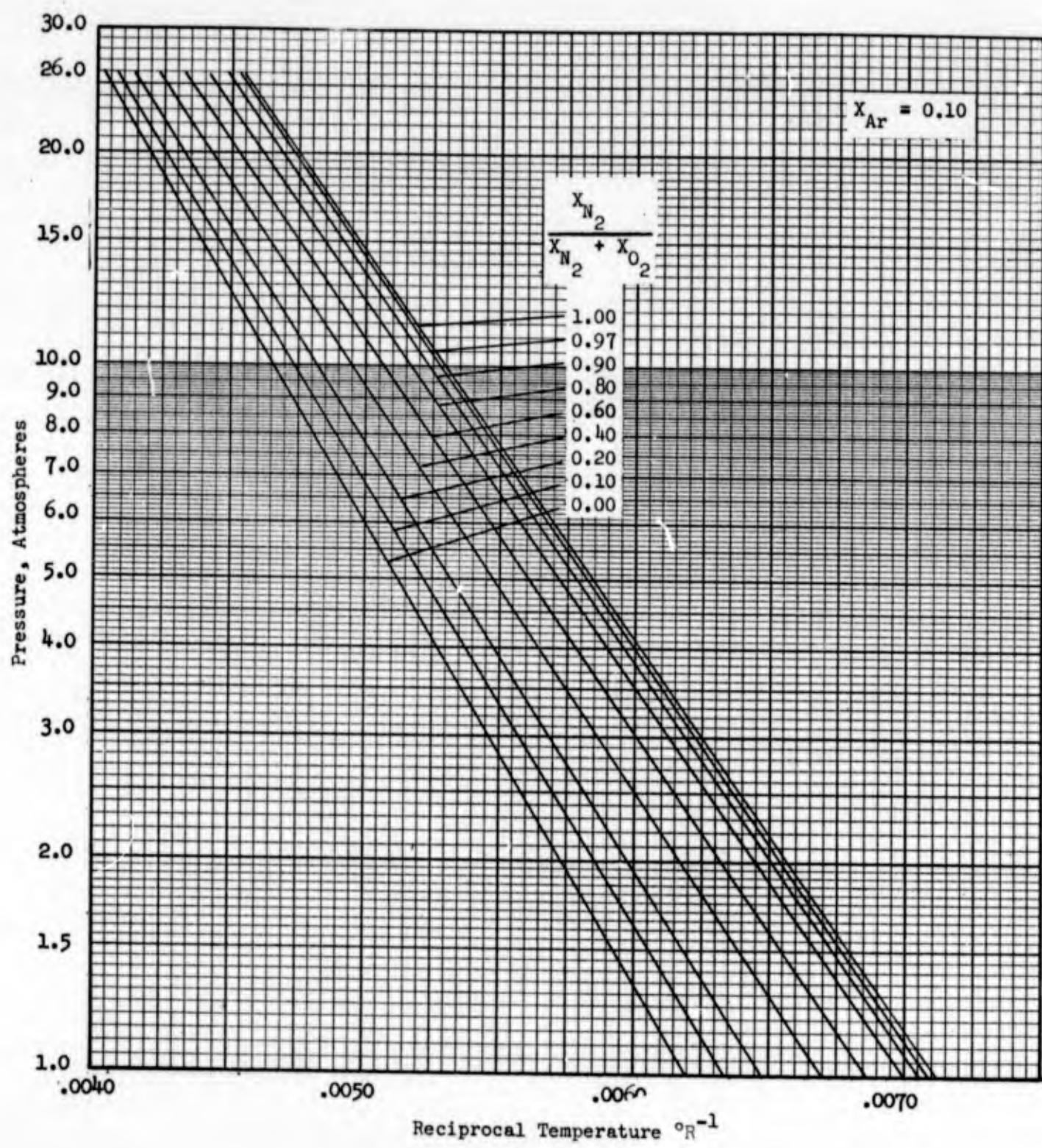


Figure 181. Vapor Pressures of Specific Mixtures of $\text{N}_2\text{-Ar-O}_2$.

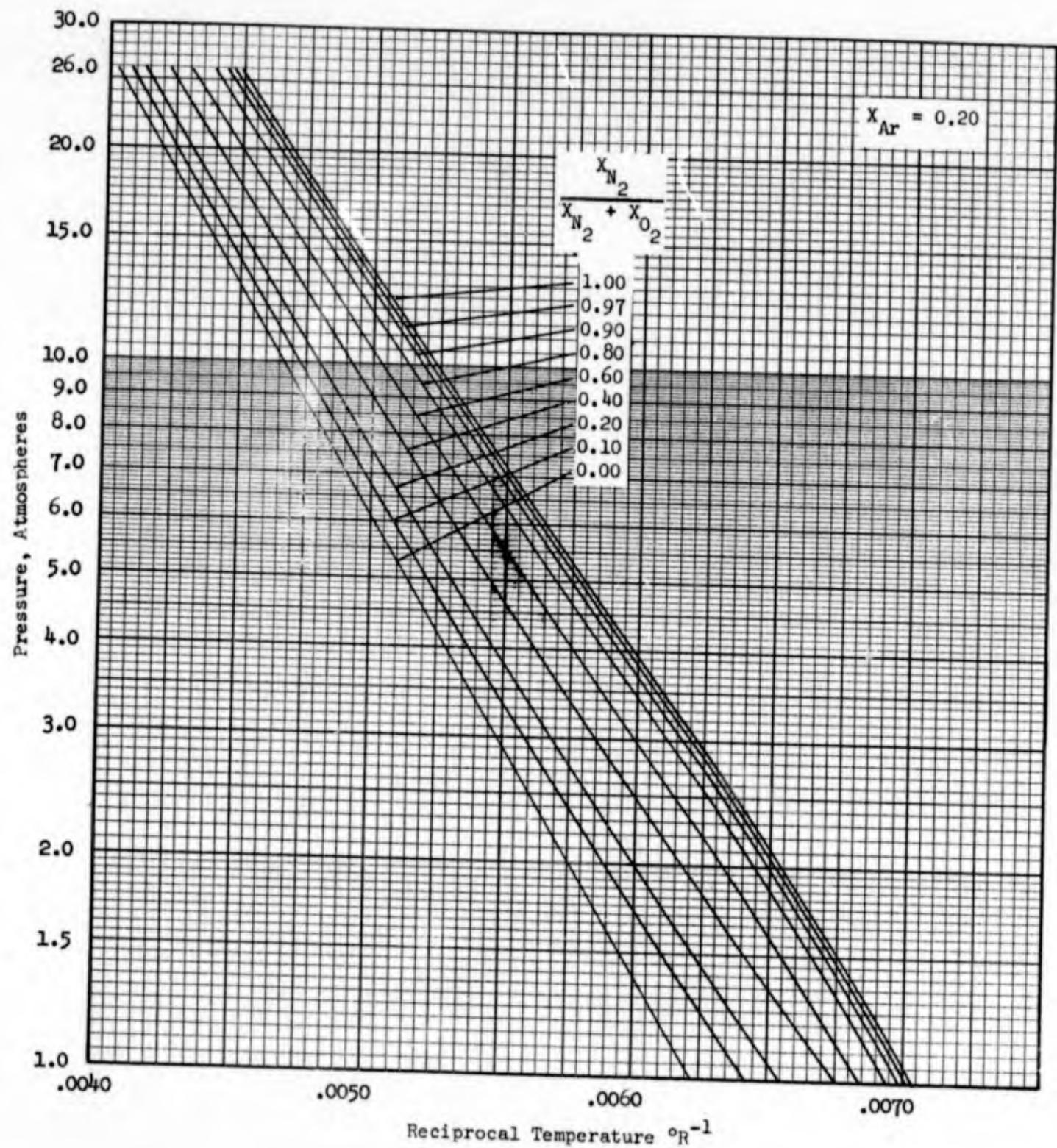


Figure 182. Vapor Pressures of Specific Mixtures of N_2 -Ar- O_2 .

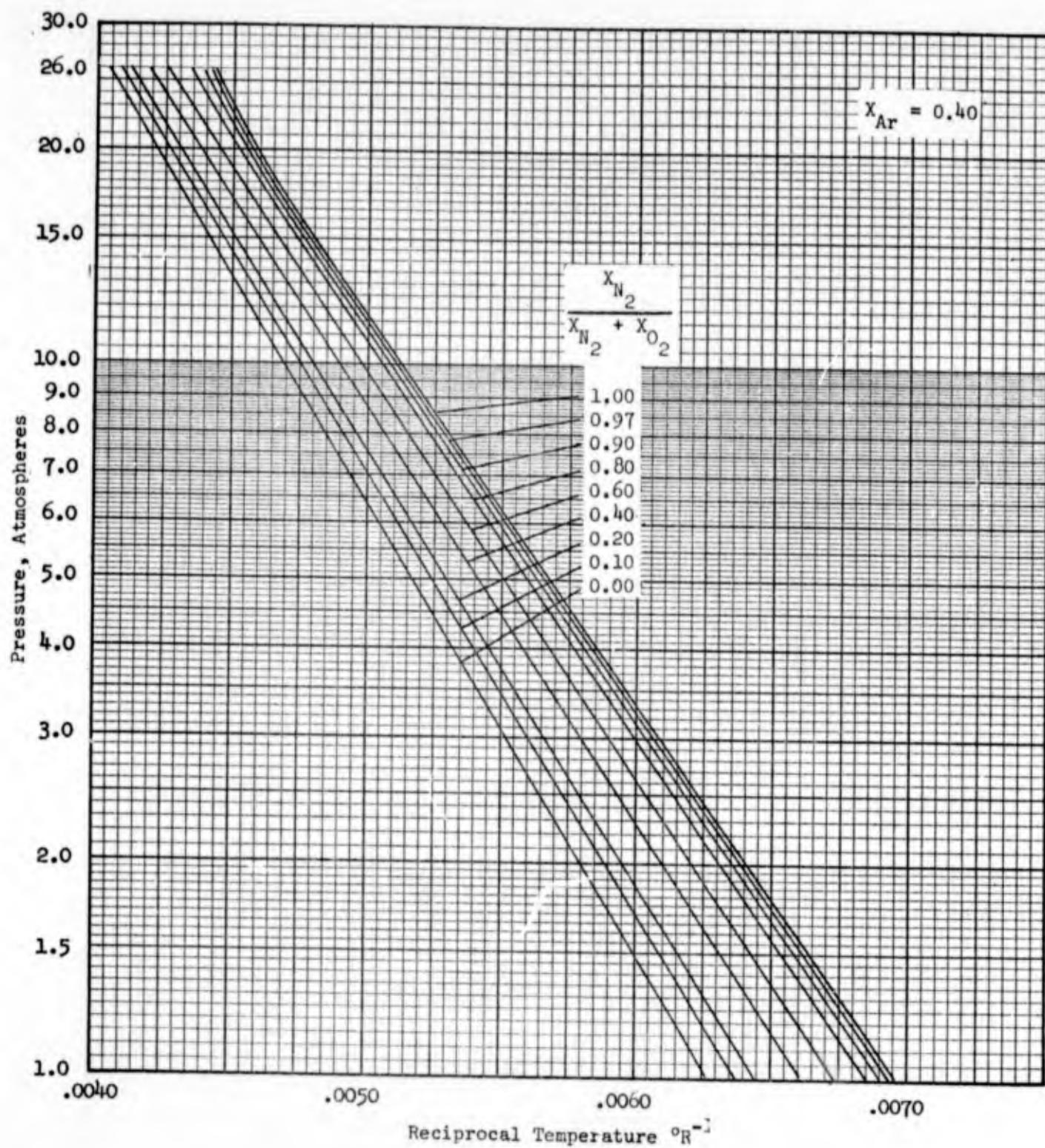


Figure 183. Vapor Pressures of Specific Mixtures of N_2 -Ar- O_2 .

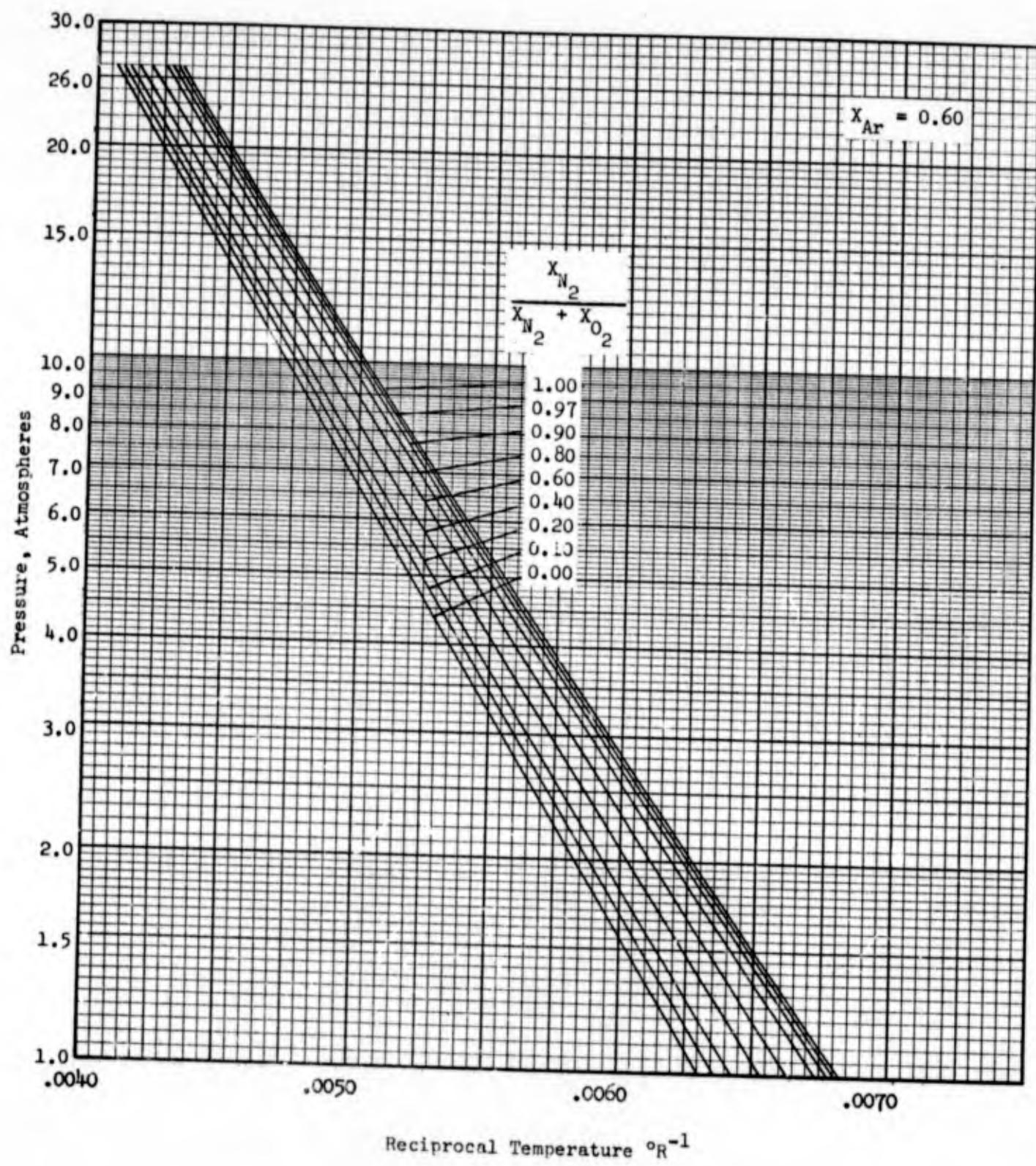


Figure 184. Vapor Pressures of Specific Mixtures of N_2 -Ar- O_2 .

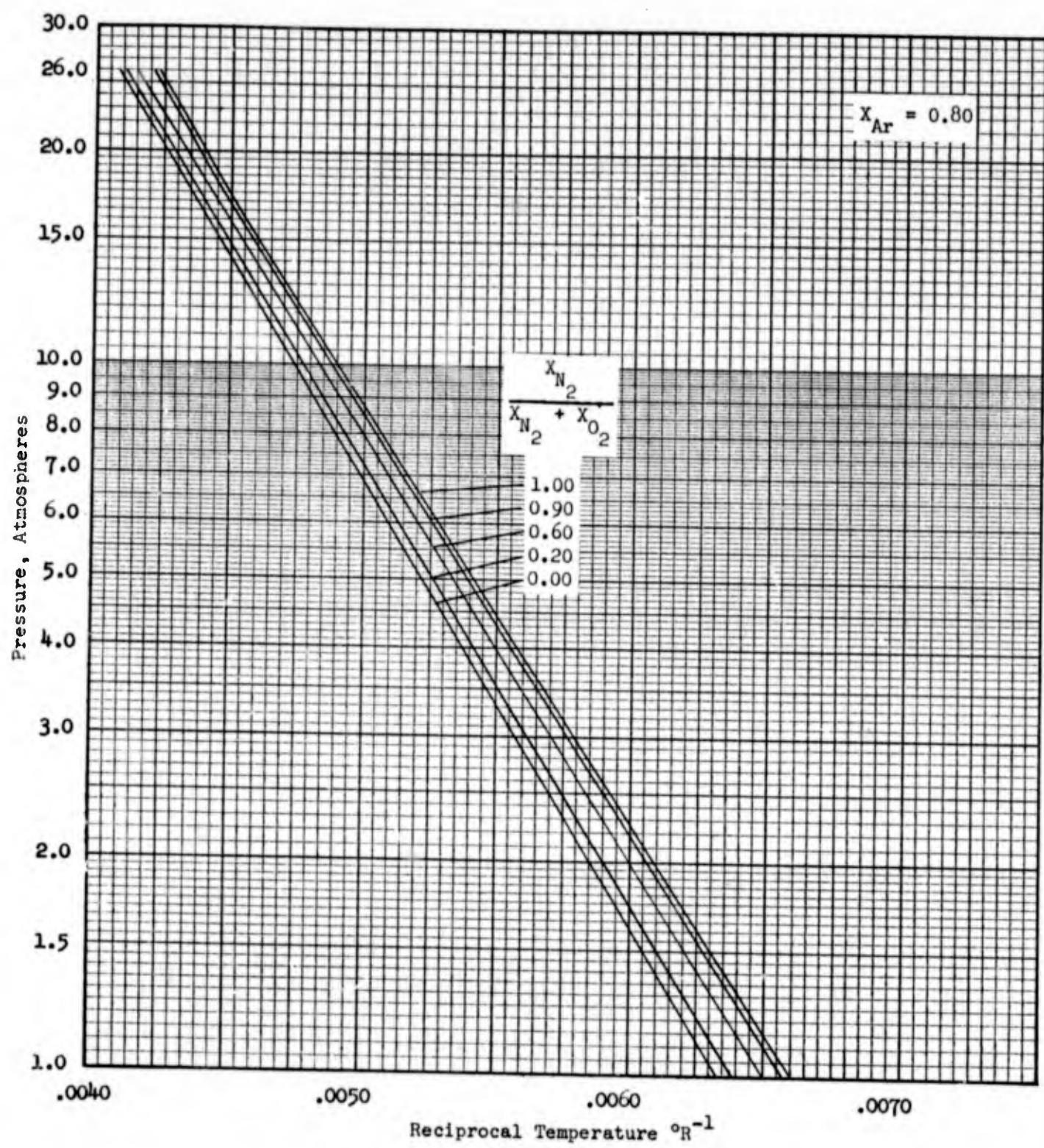


Figure 185. Vapor Pressures of Specific Mixtures of N_2 -Ar- O_2 .

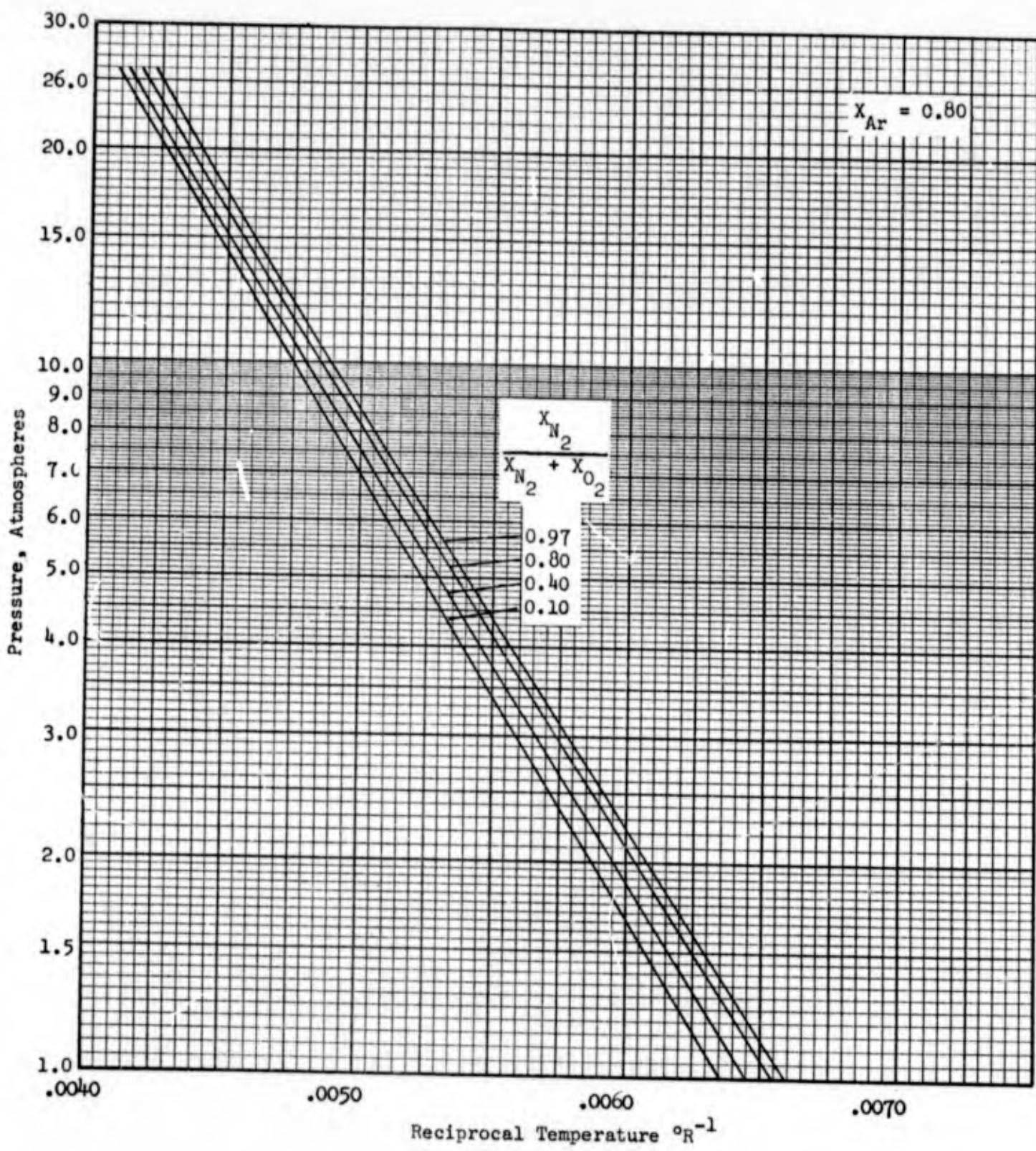


Figure 186. Vapor Pressures of Specific Mixtures of N_2 -Ar- O_2 .

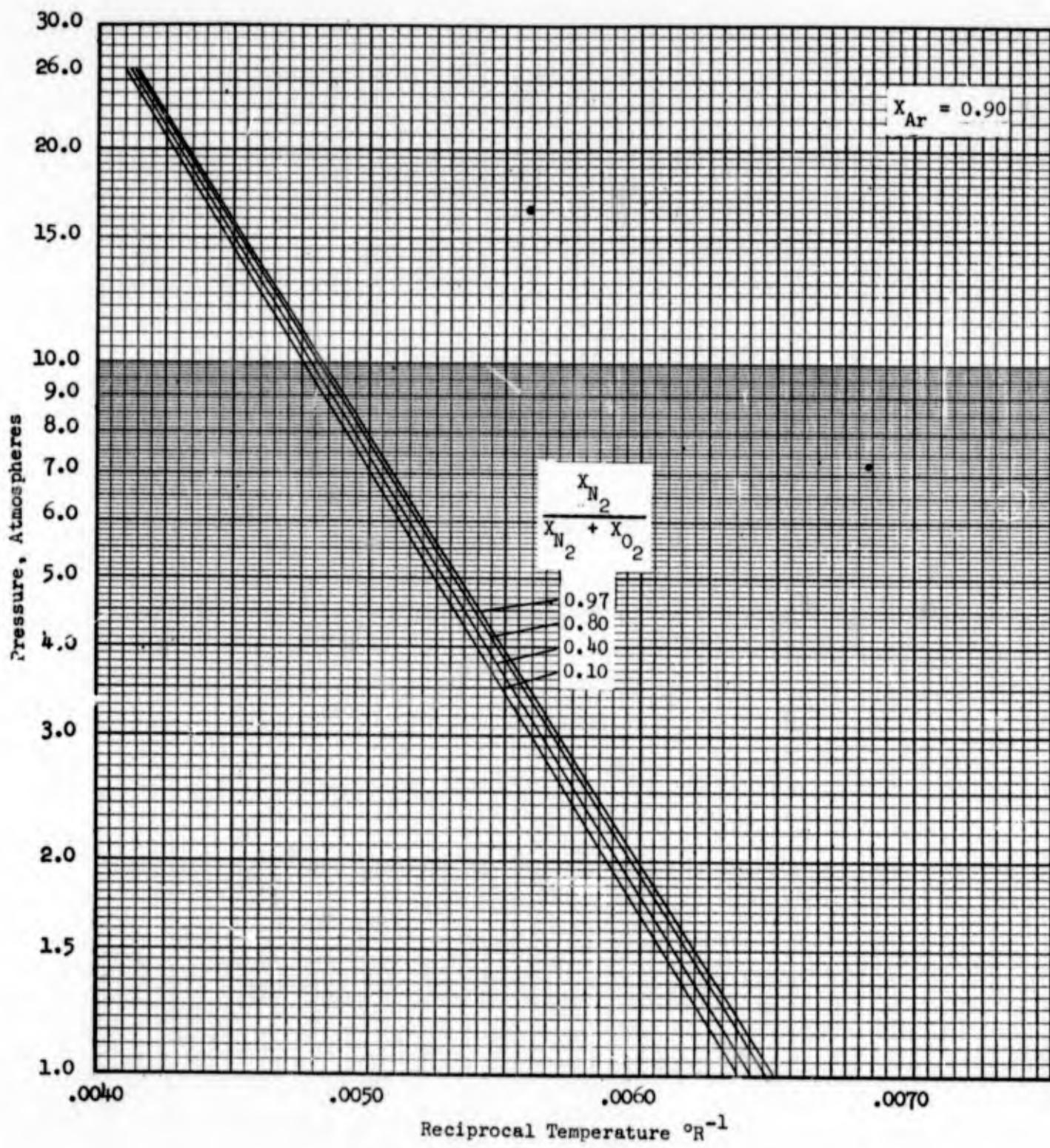


Figure 187. Vapor Pressures of Specific Mixtures of N_2 -Ar- O_2 .

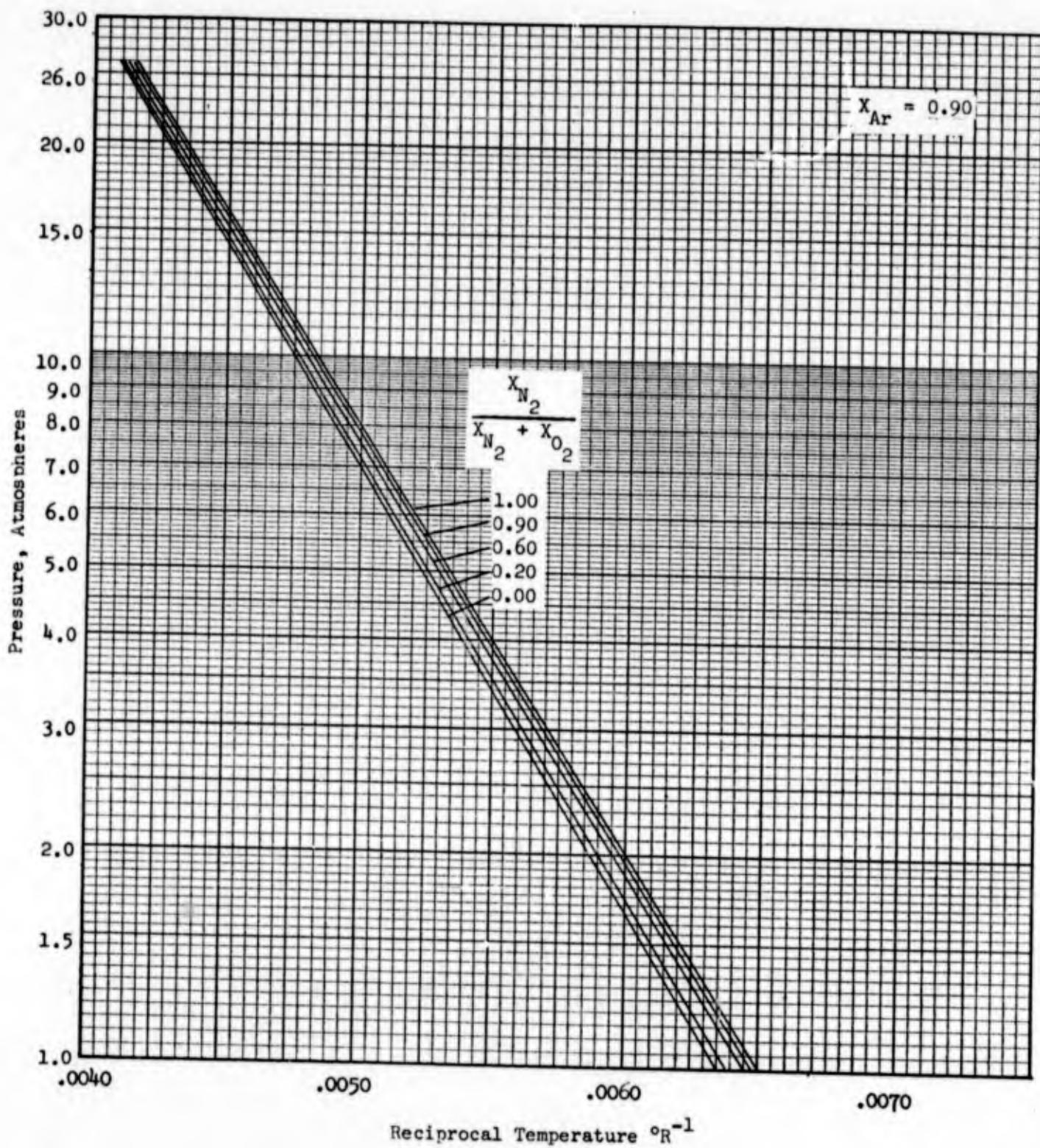


Figure 188. Vapor Pressures of Specific Mixtures of N_2 -Ar- O_2 .

APPENDIX II
TABULAR PRESENTATION OF CORRELATIONA. Isobaric Table

The table to follow presents values calculated at even pressure levels of 1, 2, 4, 6, 8, 10, 12, 14, 16, 18, 20, 23, and 26 atmospheres. They are arranged in order of increasing liquid mole fraction ratio

$$\frac{N_2}{N_2 + O_2}$$

and sub-ordered according to increasing mole fraction of argon. The quantities calculated are vapor composition, temperature, relative volatility, pressure, activity coefficient, enthalpy, and heat capacity.

Table 2% Isobaric Calculated Values

PRESSURE = 1. ATM

LIQUID MOLE FRACTION	VAPOR MOLE FRACTION		TEMP	RELATIVE VOL			PRESSURE ACT COEF			ENTHALPY		HEAT CAPACITY					
	N2/N2+O2	AR	N2	AR	O2	R	N2/AR	N2/O2	AR/O2	N2	AR	O2	Liq	Vap	Liq	Vap	
0.	0.	0.	0.	1.0000	162.4	2.575	4.010	1.957	1.118	1.169	0.999	-1841.	1993.	13.2	7.466		
0.	0.01	0.	0.0194	0.9849	162.3	2.581	4.007	1.953	1.117	1.161	1.000	-1844.	1987.	13.1	7.374		
0.	0.02	0.	0.0306	0.9694	162.2	2.586	4.004	1.948	1.115	1.158	1.000	-1847.	1982.	13.1	7.342		
0.	0.03	0.	0.0415	0.9544	162.1	2.592	4.001	1.944	1.113	1.155	1.000	-1850.	1978.	13.1	7.311		
0.	0.04	0.	0.0503	0.9397	162.0	2.597	3.998	1.940	1.112	1.151	1.001	-1853.	1971.	13.0	7.281		
0.	0.05	0.	0.0574	0.9253	161.9	2.602	3.995	1.939	1.110	1.148	1.001	-1855.	1968.	13.0	7.251		
0.	0.07	0.	0.1031	0.8970	161.7	2.613	3.989	1.926	1.107	1.142	1.002	-1860.	1958.	12.9	7.192		
0.	0.10	0.	0.1439	0.8681	161.5	2.629	3.979	1.913	1.103	1.132	1.003	-1868.	1941.	12.9	7.107		
0.	0.20	0.	0.2687	0.7313	160.7	2.652	3.941	1.469	1.091	1.104	1.010	-1892.	1971.	12.6	6.847		
0.	0.40	0.	0.4798	0.5284	159.4	2.706	3.892	1.382	1.076	1.058	1.034	-1938.	924.	11.9	6.406		
0.	0.60	0.	0.6805	0.3395	158.5	2.888	3.748	1.297	1.079	1.024	1.073	-1978.	802.	11.3	6.026		
0.	0.80	0.	0.8293	0.1767	157.7	2.991	3.632	1.214	1.087	1.009	1.127	-2019.	807.	10.7	5.666		
0.	0.90	0.	0.9126	0.0685	157.5	3.042	3.572	1.174	1.099	1.003	1.158	-2032.	779.	10.4	5.591		
0.10	0.	0.3139	0.	0.5865	157.7	2.603	4.111	1.958	1.103	1.168	1.018	-1834.	1989.	13.2	7.416		
0.10	0.01	0.3099	0.0119	0.5798	157.6	2.624	4.106	1.963	1.102	1.164	1.012	-1837.	1987.	13.1	7.386		
0.10	0.02	0.3094	0.0237	0.5767	157.6	2.631	4.100	1.958	1.100	1.161	1.012	-1839.	1983.	13.1	7.361		
0.10	0.03	0.3037	0.0354	0.6630	157.6	2.636	4.099	1.954	1.099	1.157	1.013	-1842.	1949.	13.1	7.337		
0.10	0.04	0.2978	0.0470	0.6593	157.6	2.641	4.090	1.949	1.098	1.154	1.013	-1844.	1949.	13.1	7.313		
0.10	0.05	0.2939	0.0505	0.6474	157.5	2.649	4.089	1.944	1.096	1.151	1.013	-1846.	1942.	13.0	7.289		
0.10	0.07	0.	0.8882	0.0612	0.6223	157.5	2.659	4.074	1.934	1.094	1.148	1.014	-1851.	1924.	13.0	7.242	
0.10	0.10	0.	0.2792	0.1145	0.6103	157.4	2.669	4.058	1.520	1.099	1.139	1.015	-1858.	1824.	12.9	7.173	
0.10	0.20	0.	0.3999	0.2267	0.5984	157.2	2.717	4.053	1.473	1.086	1.106	1.022	-1882.	956.	12.8	6.951	
0.10	0.40	0.	0.1759	0.4170	0.4972	157.0	2.812	3.887	1.382	1.076	1.081	1.049	-1928.	928.	11.9	6.546	
0.10	0.60	0.	0.1169	0.6036	0.2795	156.9	2.906	3.766	1.298	1.072	1.029	1.082	-1969.	871.	11.3	6.147	
0.10	0.80	0.	0.0993	0.7933	0.1471	156.9	3.001	3.646	1.213	1.086	1.009	1.134	-2009.	813.	10.7	5.766	
0.10	0.90	0.	0.393	0.8937	0.0762	157.1	3.048	3.576	1.173	1.079	1.004	1.166	-2029.	783.	10.4	5.534	
0.20	0.	0.8985	0.	0.4983	156.4	2.841	4.159	1.975	1.085	1.171	1.028	-1814.	1985.	13.2	7.222		
0.20	0.01	0.8942	0.	0.4881	156.4	2.848	4.149	1.968	1.084	1.168	1.026	-1816.	1932.	13.2	7.192		
0.20	0.02	0.8949	0.	0.4712	0.4918	156.4	2.851	4.143	1.963	1.083	1.164	1.026	-1819.	1929.	13.1	7.162	
0.20	0.03	0.8938	0.	0.4288	0.4779	156.4	2.859	4.137	1.958	1.082	1.161	1.027	-1821.	1927.	13.1	7.132	
0.20	0.04	0.8884	0.	0.3833	0.4731	156.4	2.869	4.131	1.953	1.081	1.158	1.027	-1824.	1924.	13.1	7.102	
0.20	0.05	0.8834	0.	0.4277	0.4488	156.4	2.865	4.125	1.948	1.080	1.154	1.027	-1826.	1921.	13.0	7.083	
0.20	0.07	0.	0.7432	0.0946	0.4002	156.4	2.874	4.112	1.938	1.078	1.148	1.028	-1831.	1916.	13.0	7.063	
0.20	0.10	0.	0.4988	0.0946	0.4974	156.4	2.888	4.094	1.523	1.079	1.139	1.030	-1839.	1908.	12.9	7.224	
0.20	0.20	0.	0.8983	0.1866	0.4951	156.3	2.735	4.032	1.474	1.086	1.110	1.030	-1863.	981.	12.8	7.031	
0.20	0.40	0.	0.3123	0.3680	0.3197	156.3	2.821	3.997	1.381	1.082	1.084	1.058	-1911.	936.	11.9	6.648	
0.20	0.60	0.	0.2142	0.5595	0.2268	156.4	2.921	3.779	1.294	1.088	1.032	1.093.	-1958.	877.	11.3	6.292	
0.20	0.80	0.	0.1144	0.7602	0.1294	156.4	3.009	3.647	1.212	1.086	1.011	1.140	-2004.	819.	10.7	5.817	
0.20	0.90	0.	0.3972	0.8744	0.0462	156.4	3.052	3.586	1.173	1.089	1.006	1.189	-2026.	782.	10.4	5.574	
0.40	0.	0.7333	0.	0.2867	156.7	2.829	4.124	1.969	1.080	1.187	1.085	-1748.	987.	13.3	7.452		
0.40	0.01	0.7277	0.	0.2951	0.2951	148.6	2.634	4.119	1.944	1.089	1.182	1.085	-1751.	986.	13.2	7.437	
0.40	0.02	0.7295	0.	0.3146	0.2835	148.6	2.649	4.114	1.939	1.089	1.179	1.085	-1754.	984.	13.2	7.422	
0.40	0.03	0.7172	0.	0.3216	0.2619	148.6	2.649	4.108	1.933	1.088	1.178	1.086	-1757.	982.	13.2	7.407	
0.40	0.04	0.7110	0.	0.3286	0.2682	148.6	2.659	4.103	1.928	1.087	1.176	1.086	-1760.	981.	13.2	7.392	
0.40	0.05	0.7084	0.	0.3395	0.2666	149.0	2.664	4.098	1.923	1.086	1.175	1.087	-1764.	980.	13.1	7.377	
0.40	0.07	0.	0.6956	0.	0.3491	0.2993	149.1	2.667	4.087	1.913	1.087	1.176	1.088	-1770.	980.	13.1	7.367
0.40	0.10	0.	0.6794	0.	0.3783	0.2963	149.3	2.683	4.079	1.917	1.086	1.177	1.087	-1779.	981.	13.0	7.361
0.40	0.20	0.	0.8244	0.	1.4226	0.2931	149.9	2.737	4.010	1.468	1.084	1.182	1.071	-1819.	984.	12.8	7.195
0.40	0.40	0.	0.5975	0.	0.2977	0.1948	151.2	2.841	3.987	1.375	1.084	1.174	1.088	-1871.	928.	11.9	6.811
0.40	0.60	0.	0.3743	0.	0.4776	0.1482	152.0	2.730	3.788	1.289	1.082	1.039	1.116	-1932.	885.	11.3	6.423
0.40	0.80	0.	0.2121	0.	0.7018	0.0878	154.0	3.025	3.657	1.209	1.084	1.016	1.194	-1991.	829.	10.7	5.944
0.40	0.90	0.	0.1141	0.	0.3382	0.0477	155.1	3.063	3.596	1.171	1.095	1.008	1.177	-2032.	794.	10.4	5.593
0.50	0.	0.9346	0.	0.3441	0.2144	149.8	2.592	3.971	1.941	1.094	1.124	1.029	-1667.	969.	13.8	7.471	
0.50	0.01	0.9321	0.	0.3111	0.1416	149.1	2.599	3.980	1.941	1.094	1.124	1.029	-1672.	968.	13.8	7.459	
0.50	0.03	0.9242	0.	0.3157	0.1469	149.1	2.599	3.983	1.936	1.094	1.124	1.029	-1674.	967.	13.8	7.446	
0.50	0.05	0.9275	0.	0.3224	0.1462	149.2	2.602	3.983	1.931	1.094	1.124	1.029	-1680.	966.	13.4	7.424	
0.50	0.07	0.	0.8975	0.	0.3237	0.0661	149.2	2.609	3.982	1.928	1.093	1.124	1.029	-1684.	965.	13.4	7.421
0.50	0.10	0.	0.6912	0.	0.3237	0.0661	149.2	2.640	3.913	1.901	1.093	1.124	1.029	-1692.	963.	13.3	7.396
0.50	0.20	0.	0.6952	0.	0.3447	0.0366	149.5	2.707	3.937	1.454	1.093	1.124	1.029	-1774.	963.	12.8	7.224
0.50	0.40	0.	0.5949	0.	0.3494	0.0209	149.8	2.645	3.977	1.365	1.094	1.125	1.028	-1824.	923.	12.8	6.926
0.50	0.60	0.	0.3699	0.	0.5959	0.0298	150.6	2.849	3.777	1.203	1.094	1.143	1.028	-1933.	868.	11.3	6.555
0.50	0.80	0.	0														

Table 2a. (cont.)

PRESSURE = 2. ATM

LIQUID MOLE FRACTION		VAPOR MOLE FRACTION		TEMP	RELATIVE VOL			PRESSURE ACT COEF			ENTHALPY BTU/LB MOLE			HEAT CAPACITY BTU/LB MOLE-R		
N2/N2+O2	AR	N2	AR	O2	R	N2/AR	N2/O2	AR/O2	N2	A	O2	L10	VAP	L10	VAP	
0.	0.	0.	0.	1.0000	175.3	2.307	3.368	1.460	1.062	1.136	0.999	-1670.	1159.	13.3	7.664	
0.	0.01	0.	0.0145	0.9855	175.2	2.311	3.365	1.456	1.060	1.133	1.000	-1673.	1154.	13.3	7.634	
0.	0.02	0.	0.0288	0.9712	175.1	2.315	3.363	1.452	1.059	1.130	1.000	-1677.	1148.	13.2	7.604	
0.	0.03	0.	0.0420	0.9571	175.0	2.320	3.361	1.449	1.058	1.127	1.000	-1680.	1143.	13.2	7.575	
0.	0.04	0.	0.0568	0.9432	174.9	2.324	3.358	1.445	1.057	1.125	1.001	-1683.	1137.	13.2	7.546	
0.	0.05	0.	0.0705	0.9295	174.8	2.329	3.356	1.441	1.056	1.122	1.001	-1686.	1132.	13.2	7.517	
0.	0.07	0.	0.0974	0.9026	174.6	2.337	3.351	1.434	1.053	1.116	1.002	-1692.	1122.	13.1	7.461	
0.	0.10	0.	0.1345	0.8635	174.4	2.350	3.343	1.422	1.050	1.109	1.004	-1701.	1107.	13.0	7.379	
0.	0.20	0.	0.2572	0.7428	173.6	2.392	3.313	1.385	1.040	1.084	1.010	-1730.	1061.	12.8	7.126	
0.	0.40	0.	0.4663	0.5337	172.3	2.474	3.242	1.310	1.029	1.049	1.033	-1782.	983.	12.3	6.687	
0.	0.60	0.	0.6499	0.3901	171.4	2.553	3.160	1.237	1.027	1.017	1.068	-1830.	916.	11.7	6.299	
0.	0.80	0.	0.8235	0.1765	170.6	2.632	3.070	1.166	1.034	1.001	1.117	-1873.	854.	11.2	5.930	
0.	0.90	0.	0.9104	0.0494	170.4	2.671	3.022	1.132	1.047	0.997	1.148	-1894.	824.	10.9	5.744	
0.	0.10	0.01	0.2764	0.7236	170.7	2.353	3.438	1.461	1.057	1.139	1.015	-1661.	1127.	13.4	7.670	
0.	0.10	0.02	0.2696	0.6233	170.6	2.357	3.434	1.457	1.054	1.137	1.015	-1664.	1123.	13.4	7.653	
0.	0.10	0.03	0.2662	0.348	169.6	2.365	3.427	1.449	1.054	1.134	1.015	-1667.	1119.	13.3	7.629	
0.	0.10	0.04	0.2620	0.0462	169.6	2.366	3.422	1.445	1.053	1.131	1.016	-1670.	1115.	13.3	7.609	
0.	0.10	0.05	0.2594	0.0576	169.6	2.372	3.418	1.441	1.052	1.128	1.016	-1672.	1111.	13.3	7.581	
0.	0.10	0.07	0.2520	0.0800	169.5	2.380	3.410	1.433	1.048	1.120	1.017	-1675.	1107.	13.3	7.558	
0.	0.10	0.10	0.2431	0.1130	169.4	2.391	3.398	1.421	1.045	1.112	1.019	-1681.	1100.	13.2	7.511	
0.	0.10	0.20	0.2122	0.2185	169.5	2.428	3.356	1.382	1.036	1.087	1.025	-1717.	1052.	12.8	7.219	
0.	0.10	0.40	0.1957	0.4192	169.9	2.501	3.266	1.306	1.027	1.047	1.046	-1770.	985.	12.3	6.803	
0.	0.10	0.60	0.1034	0.6032	169.8	2.572	3.173	1.234	1.027	1.020	1.070	-1820.	922.	11.7	6.403	
0.	0.10	0.80	0.0524	0.7941	169.9	2.642	3.075	1.164	1.034	1.003	1.124	-1868.	860.	11.2	5.995	
0.	0.10	0.90	0.0266	0.8943	170.0	2.676	3.025	1.130	1.048	0.998	1.152	-1891.	827.	10.9	5.786	
0.	0.20	0.	0.4444	0.	167.0	2.380	3.469	1.457	1.046	1.143	1.032	-1841.	1101.	13.5	7.495	
0.	0.20	0.01	0.4596	0.0397	167.0	2.384	3.464	1.453	1.045	1.140	1.032	-1844.	1098.	13.4	7.477	
0.	0.20	0.02	0.4546	0.0194	167.0	2.387	3.459	1.449	1.044	1.137	1.032	-1847.	1095.	13.4	7.457	
0.	0.20	0.03	0.4499	0.0291	167.0	2.391	3.455	1.445	1.043	1.134	1.033	-1850.	1092.	13.4	7.436	
0.	0.20	0.04	0.4452	0.0387	167.0	2.394	3.450	1.441	1.042	1.131	1.033	-1853.	1089.	13.3	7.416	
0.	0.20	0.05	0.4404	0.0443	167.0	2.398	3.446	1.437	1.041	1.128	1.033	-1856.	1086.	13.3	7.394	
0.	0.20	0.07	0.4309	0.0674	167.1	2.405	3.436	1.429	1.039	1.123	1.034	-1861.	1080.	13.3	7.355	
0.	0.20	0.10	0.4169	0.0954	167.1	2.414	3.422	1.417	1.037	1.119	1.035	-1870.	1071.	13.2	7.495	
0.	0.20	0.20	0.3710	0.1892	167.3	2.491	3.375	1.377	1.030	1.098	1.041	-1698.	1042.	12.9	7.296	
0.	0.20	0.40	0.2923	0.3734	167.7	2.520	3.270	1.301	1.023	1.050	1.060	-1754.	985.	12.3	6.902	
0.	0.20	0.60	0.1939	0.5622	168.4	2.587	3.180	1.229	1.026	1.022	1.070	-1809.	927.	11.7	6.496	
0.	0.20	0.80	0.1016	0.7665	169.1	2.651	3.079	1.162	1.039	1.003	1.131	-1862.	865.	11.2	6.056	
0.	0.20	0.90	0.0523	0.8785	169.6	2.681	3.027	1.129	1.048	0.999	1.156	-1888.	831.	10.9	5.814	
0.	0.40	0.	0.5684	0.	161.3	2.389	3.441	1.441	1.021	1.154	1.075	-1978.	1061.	13.9	7.747	
0.	0.40	0.01	0.6911	0.0073	161.4	2.393	3.437	1.437	1.020	1.151	1.074	-1882.	1059.	13.9	7.731	
0.	0.40	0.02	0.6585	0.0146	161.5	2.397	3.433	1.433	1.020	1.148	1.074	-1885.	1057.	13.9	7.714	
0.	0.40	0.03	0.6805	0.0219	161.5	2.401	3.429	1.429	1.019	1.145	1.075	-1888.	1055.	13.9	7.698	
0.	0.40	0.04	0.6751	0.0292	161.6	2.405	3.429	1.425	1.019	1.142	1.075	-1892.	1053.	13.4	7.682	
0.	0.40	0.05	0.6698	0.0346	161.6	2.409	3.421	1.420	1.014	1.139	1.075	-1896.	1051.	13.4	7.664	
0.	0.40	0.07	0.5991	0.0513	161.8	2.417	3.413	1.412	1.017	1.134	1.075	-1903.	1048.	13.3	7.633	
0.	0.40	0.10	0.6429	0.0735	162.0	2.420	3.401	1.401	1.016	1.125	1.075	-1913.	1042.	13.2	7.584	
0.	0.40	0.20	0.5983	0.1490	162.6	2.466	3.360	1.362	1.014	1.100	1.079	-1648.	1023.	12.9	7.418	
0.	0.40	0.40	0.4731	0.3102	164.1	2.542	3.279	1.288	1.015	1.059	1.092	-1716.	982.	12.3	7.081	
0.	0.40	0.60	0.3438	0.4942	164.2	2.609	3.193	1.220	1.024	1.024	1.114	-1784.	933.	11.7	6.656	
0.	0.40	0.80	0.1910	0.7102	167.7	2.666	3.084	1.157	1.039	1.008	1.145	-1854.	874.	11.2	6.169	
0.	0.	0.90	0.1014	0.8484	168.9	2.690	3.030	1.127	1.049	1.001	1.163	-1981.	837.	10.9	5.881	
0.	0.	0.90	0.3336	0.	167.2	2.394	3.338	1.415	1.000	1.177	1.134	-1981.	829.	13.6	7.797	
0.	0.	0.90	0.8206	0.0599	167.3	2.364	3.336	1.411	1.000	1.173	1.134	-1981.	829.	13.6	7.784	
0.	0.	0.90	0.8236	0.0110	167.4	2.374	3.332	1.404	1.000	1.170	1.133	-1981.	828.	13.6	7.770	
0.	0.	0.90	0.9185	0.0178	167.5	2.374	3.330	1.400	1.000	1.166	1.133	-1981.	827.	13.6	7.755	
0.	0.	0.90	0.05	0.8134	0.0237	167.6	2.370	3.328	1.395	0.999	1.163	1.132	-1919.	1024.	13.5	7.741
0.	0.	0.90	0.07	0.7801	0.0418	167.6	2.393	3.324	1.389	0.999	1.157	1.131	-1827.	1022.	13.4	7.720
0.	0.	0.90	0.20	0.7269	0.1237	169.0	2.400	3.317	1.378	0.999	1.147	1.130	-1940.	1018.	13.3	7.657
0.	0.	0.90	0.40	0.6089	0.2650	169.1	2.445	3.241	1.273	0.997	1.109	1.072	-1949.	1005.	13.2	7.510
0.	0.	0.90	0.60	0.4022	0.4407	169.4	2.522	3.172	1.210	1.021	1.037	1.071	-1759.	936.	11.7	6.786
0.	0.	0.90	0.80	0.2689	0.6171	169.5	2.679	3.085	1.152	1.040	1.010	1.175	-1823.	886.	11.2	6.362
0.	0.	0.90	0.90	0.3659	0.	167.5	2.275	3.110	1.367	0.991	1.225	1.274	-1981.	995.	13.0	7.870
0.	0.	0.90	0.92	0.9564	0.005	167.7	2.289	3.112	1.364	0.991	1.251	1.271	-1342.	995.	13.0	7.858
0.	0.	0.90	0.93	0.9510	0.1151	167.8	2.301	3.114	1.361	0.991	1.240	1.269	-1348.	994.	13.0	7.846
0.	0.</															

Table 25. (cont.)

PRESSURE = 4. ATM

LIQUID MOLE FRACTION	VAPOR MOLE FRACTION		TEMP	RELATIVE VOL			PRESSURE ACT COEF	ENTHALPY	HEAT CAPACITY	BTU/LB MOLE	BTU/LB MOLE-R						
	N ₂ /N ₂ O ₂	AR		N ₂	AR	O ₂						Liq	Vap	Liq	Vap		
0.	0.	0.	1.0000	190.6	2.020	2.776	1.375	0.987	1.111	1.000	-1466.	1224.	13.4	8.122			
0.	0.01	0.	0.0137	0.9863	190.5	2.023	2.775	1.372	0.986	1.109	1.001	-1470.	1218.	13.4	8.094		
0.	0.02	0.	0.0272	0.9728	190.4	2.026	2.773	1.369	0.985	1.104	1.001	-1473.	1212.	13.4	8.065		
0.	0.03	0.	0.0405	0.9595	190.3	2.030	2.772	1.366	0.985	1.104	1.002	-1477.	1207.	13.4	8.037		
0.	0.04	0.	0.0537	0.9463	190.2	2.033	2.770	1.362	0.984	1.102	1.002	-1480.	1201.	13.4	8.010		
0.	0.05	0.	0.0668	0.9332	190.1	2.037	2.768	1.359	0.983	1.100	1.003	-1484.	1196.	13.3	7.982		
0.	0.07	0.	0.0824	0.9076	189.9	2.043	2.765	1.353	0.982	1.096	1.004	-1490.	1185.	13.3	7.929		
0.	0.10	0.	0.1299	0.8701	189.6	2.053	2.759	1.344	0.980	1.089	1.005	-1500.	1169.	13.3	7.850		
0.	0.20	0.	0.2471	0.7929	188.8	2.084	2.738	1.313	0.974	1.070	1.013	-1533.	1121.	13.1	7.605		
0.	0.40	0.	0.4348	0.5452	187.5	2.118	2.688	1.251	0.967	1.038	1.034	-1593.	1037.	12.7	7.166		
0.	0.60	0.	0.6110	0.3590	186.3	2.207	2.627	1.190	0.967	1.016	1.064	-1647.	964.	12.3	6.771		
0.	0.80	0.	0.8190	0.1811	185.8	2.284	2.560	1.131	0.976	1.003	1.110	-1698.	896.	11.9	6.389		
0.	0.90	0.	0.9044	0.0916	185.5	2.292	2.524	1.101	0.983	1.000	1.137	-1723.	862.	11.6	6.196		
0.10	0.	0.2393	0.7467	186.2	2.063	2.831	1.372	0.994	1.120	1.020	-1452.	1193.	13.7	8.150			
0.10	0.01	0.2363	0.0116	0.7521	186.1	2.066	2.828	1.369	0.994	1.117	1.021	-1455.	1188.	13.6	8.126		
0.10	0.02	0.2334	0.0230	0.7434	186.1	2.050	2.825	1.365	0.993	1.115	1.021	-1459.	1184.	13.6	8.102		
0.10	0.03	0.2305	0.0344	0.7351	186.0	2.072	2.822	1.362	0.992	1.113	1.021	-1462.	1180.	13.6	8.078		
0.10	0.04	0.2277	0.0457	0.7267	186.0	2.075	2.820	1.359	0.991	1.110	1.022	-1465.	1175.	13.6	8.054		
0.10	0.05	0.2240	0.0569	0.7183	186.0	2.078	2.817	1.356	0.990	1.108	1.022	-1469.	1171.	13.5	8.031		
0.10	0.07	0.2192	0.0792	0.7017	185.9	2.083	2.811	1.349	0.988	1.104	1.023	-1475.	1163.	13.5	7.984		
0.10	0.10	0.2109	0.1120	0.6772	185.8	2.092	2.802	1.340	0.986	1.097	1.024	-1485.	1150.	13.4	7.915		
0.10	0.20	0.1943	0.2170	0.5983	185.5	2.119	2.772	1.308	0.979	1.077	1.030	-1517.	1116.	13.2	7.691		
0.10	0.40	0.1353	0.4150	0.4497	185.2	2.173	2.707	1.246	0.971	1.044	1.049	-1578.	1037.	12.8	7.269		
0.10	0.60	0.0896	0.0405	0.3054	185.0	2.224	2.638	1.168	0.971	1.020	1.078	-1637.	968.	12.4	6.160		
0.10	0.80	0.0452	0.7941	0.1588	185.1	2.273	2.564	1.120	0.978	1.000	1.117	-1693.	908.	12.0	6.144		
0.20	0.	0.0229	0.0957	0.0814	185.2	2.296	2.526	1.100	0.985	1.002	1.141	-1720.	865.	11.8	6.276		
0.20	0.	0.4170	0.	0.5831	182.4	2.094	2.861	1.366	0.997	1.120	1.041	-1431.	1166.	13.8	8.119		
0.20	0.01	0.4126	0.0099	0.5776	182.4	2.097	2.857	1.363	0.996	1.125	1.041	-1434.	1162.	13.8	8.107		
0.20	0.02	0.4082	0.0198	0.5721	182.4	2.100	2.854	1.359	0.995	1.123	1.042	-1438.	1159.	13.8	8.146		
0.20	0.03	0.4038	0.0297	0.5666	182.4	2.102	2.851	1.356	0.994	1.120	1.042	-1441.	1155.	13.8	8.125		
0.20	0.04	0.3994	0.0395	0.5611	182.4	2.105	2.847	1.353	0.993	1.118	1.042	-1445.	1152.	13.7	8.104		
0.20	0.05	0.3951	0.0493	0.5557	182.4	2.107	2.844	1.349	0.992	1.116	1.042	-1448.	1149.	13.7	8.083		
0.20	0.07	0.3864	0.0648	0.5444	182.4	2.112	2.837	1.343	0.990	1.111	1.043	-1455.	1142.	13.7	8.041		
0.20	0.10	0.3735	0.0979	0.5286	182.5	2.120	2.827	1.333	0.988	1.104	1.044	-1465.	1132.	13.6	7.978		
0.20	0.20	0.3316	0.1932	0.4752	182.6	2.145	2.792	1.301	0.982	1.083	1.049	-1498.	1099.	13.3	7.771		
0.20	0.40	0.2500	0.3808	0.3668	183.0	2.194	2.720	1.240	0.974	1.049	1.065	-1562.	1035.	12.9	7.363		
0.20	0.60	0.1766	0.5714	0.2560	183.6	2.239	2.645	1.181	0.974	1.024	1.090	-1625.	971.	12.4	6.944		
0.20	0.80	0.0883	0.7742	0.1376	184.3	2.278	2.564	1.126	0.980	1.020	1.124	-1687.	904.	12.0	6.497		
0.20	0.90	0.0452	0.8834	0.0715	184.8	2.301	2.524	1.099	0.986	1.003	1.145	-1717.	867.	11.8	6.255		
0.40	0.	0.9560	0.	0.3441	176.3	2.124	2.899	1.346	0.992	1.146	1.090	-1372.	1121.	14.1	8.277		
0.40	0.01	0.8650	0.0077	0.3417	176.4	2.127	2.856	1.343	0.991	1.143	1.090	-1376.	1119.	14.0	8.260		
0.40	0.02	0.8453	0.0145	0.3393	176.4	2.129	2.843	1.340	0.991	1.140	1.090	-1380.	1117.	14.0	8.242		
0.40	0.03	0.8400	0.0232	0.3369	176.5	2.132	2.840	1.337	0.990	1.138	1.090	-1384.	1115.	14.0	8.224		
0.40	0.04	0.8347	0.0310	0.3345	176.6	2.135	2.836	1.333	0.990	1.132	1.090	-1387.	1112.	13.9	8.206		
0.40	0.05	0.8293	0.0397	0.3320	176.6	2.137	2.843	1.330	0.989	1.133	1.090	-1391.	1110.	13.9	8.188		
0.40	0.07	0.8186	0.0543	0.3271	176.6	2.143	2.837	1.324	0.988	1.128	1.090	-1399.	1108.	13.9	8.153		
0.40	0.10	0.8025	0.0778	0.3197	177.0	2.151	2.827	1.319	0.986	1.128	1.090	-1410.	1099.	13.8	8.094		
0.40	0.20	0.5842	0.1575	0.2943	177.7	2.176	2.794	1.284	0.982	1.098	1.149	-1077.	13.5	7.919			
0.40	0.40	0.4340	0.3259	0.2393	179.2	2.223	2.725	1.226	0.979	1.061	1.100	-1529.	1029.	13.0	7.527		
0.40	0.60	0.3104	0.5141	0.1756	180.9	2.264	2.652	1.171	0.970	1.033	1.116	-1600.	975.	12.5	7.095		
0.40	0.80	0.1684	0.7334	0.0942	182.9	2.297	2.573	1.120	0.985	1.013	1.139	-1874.	915.	12.0	6.597		
0.40	0.90	0.0882	0.8595	0.0523	184.1	2.309	2.531	1.096	0.989	1.000	1.153	-1710.	872.	11.8	6.312		
0.60	0.	0.8076	0.	0.1924	171.7	2.120	2.798	1.320	0.986	1.173	1.154	-1296.	1084.	14.2	8.369		
0.60	0.01	0.8023	0.0044	0.1913	171.8	2.123	2.798	1.317	0.986	1.170	1.153	-1301.	1084.	14.2	8.354		
0.60	0.02	0.7971	0.0127	0.1902	171.9	2.127	2.794	1.314	0.985	1.167	1.152	-1305.	1083.	14.1	8.338		
0.60	0.03	0.7918	0.0192	0.1891	172.0	2.130	2.792	1.311	0.985	1.164	1.152	-1310.	1082.	14.1	8.322		
0.60	0.05	0.7812	0.0391	0.1844	172.2	2.137	2.748	1.305	0.984	1.159	1.150	-1319.	1079.	14.0	8.289		
0.60	0.07	0.7704	0.0451	0.1844	172.4	2.143	2.744	1.299	0.984	1.153	1.149	-1320.	1076.	14.0	8.257		
0.60	0.10	0.7542	0.0649	0.1810	172.6	2.153	2.778	1.290	0.983	1.144	1.148	-1343.	1072.	13.9	8.206		
0.60	0.20	0.6900	0.1332	0.1684	173.												

Table 2b. (cont.)

PRESSURE = 6. ATM

LIQUID MOLE FRACTION	VAPOR MOLE FRACTION			TEMP	RELATIVE VOL			PRESSURE ACT COEF	ENTHALPY			HEAT CAPACITY				
	N2/N2+O2	AR	N2	AR	O2	R	N2/AR	N2/O2	AR/O2	N2	AR	O2	Liq	Vap	Liq	Vap
0.	0.	0.	0.	1.0000	200.9	1.051	2.453	1.325	0.931	1.094	1.001	-1327.	1256.	13.6	0.566	
0.	0.01	0.	0.0132	0.9468	200.8	1.053	2.452	1.323	0.931	1.092	1.002	-1331.	1251.	13.6	0.538	
0.	0.02	0.	0.0247	0.9738	200.7	1.056	2.450	1.320	0.930	1.089	1.002	-1334.	1245.	13.6	0.511	
0.	0.03	0.	0.0371	0.9680	200.6	1.059	2.449	1.317	0.930	1.087	1.003	-1334.	1239.	13.6	0.494	
0.	0.04	0.	0.0519	0.9481	200.5	1.062	2.448	1.315	0.929	1.085	1.004	-1342.	1234.	13.6	0.457	
0.	0.05	0.	0.0646	0.9354	200.4	1.065	2.446	1.312	0.929	1.082	1.005	-1352.	1217.	13.6	0.430	
0.	0.07	0.	0.0895	0.9105	200.2	1.070	2.444	1.307	0.928	1.082	1.007	-1363.	1201.	13.6	0.378	
0.	0.10	0.	0.1201	0.8739	199.9	1.078	2.439	1.299	0.926	1.076	1.007	-1397.	1151.	13.4	0.302	
0.	0.20	0.	0.2412	0.7488	199.1	1.095	2.422	1.272	0.923	1.064	1.019	-1460.	1063.	13.1	0.223	
0.	0.40	0.	0.4481	0.5519	197.8	1.096	2.381	1.214	0.919	1.034	1.036	-1519.	986.	12.8	0.115	
0.	0.60	0.	0.6350	0.3462	196.8	2.004	2.332	1.164	0.920	1.016	1.066	-1573.	913.	12.6	0.080	
0.	0.80	0.	0.8163	0.1837	196.0	2.049	2.277	1.111	0.924	1.003	1.107	-1599.	877.	12.4	0.033	
0.	0.90	0.	0.9072	0.0829	195.7	2.071	2.247	1.085	0.939	1.003	1.132	-1599.	877.	12.4	0.036	
0.	1.0	0.	0.2172	0.0762	196.6	1.888	2.497	1.322	0.945	1.108	1.024	-1308.	1227.	13.9	0.608	
0.	0.01	0.2145	0.0115	0.7740	196.6	1.093	2.494	1.319	0.945	1.106	1.025	-1311.	1222.	13.9	0.584	
0.	0.02	0.2119	0.0220	0.7693	196.5	1.093	2.492	1.317	0.944	1.104	1.025	-1315.	1217.	13.9	0.560	
0.	0.03	0.2093	0.0342	0.7566	196.5	1.095	2.490	1.314	0.943	1.102	1.025	-1319.	1213.	13.9	0.536	
0.	0.04	0.2067	0.0454	0.7479	196.5	1.098	2.488	1.311	0.943	1.100	1.026	-1322.	1208.	13.9	0.512	
0.	0.05	0.2042	0.0564	0.7393	196.4	1.098	2.486	1.308	0.942	1.098	1.026	-1326.	1204.	13.8	0.489	
0.	0.07	0.1991	0.0787	0.7223	196.3	1.095	2.481	1.303	0.941	1.094	1.027	-1333.	1195.	13.8	0.447	
0.	0.10	0.1916	0.1114	0.6971	196.2	1.092	2.474	1.294	0.939	1.088	1.029	-1343.	1182.	13.8	0.373	
0.	0.20	0.1476	0.2164	0.6157	195.9	1.094	2.450	1.267	0.933	1.078	1.035	-1370.	1139.	13.6	0.148	
0.	0.40	0.1231	0.4149	0.4620	195.5	1.070	2.308	1.212	0.927	1.042	1.053	-1444.	1042.	13.2	0.722	
0.	0.60	0.0915	0.6554	0.3132	195.3	2.010	2.341	1.160	0.926	1.021	1.077	-1507.	980.	12.9	0.306	
0.	0.80	0.0410	0.7972	0.1618	195.3	2.037	2.201	1.109	0.932	1.008	1.114	-1567.	916.	12.6	0.893	
0.	0.90	0.0202	0.8960	0.0827	195.4	2.079	2.249	1.084	0.937	1.004	1.136	-1596.	879.	12.4	0.662	
0.	0.95	0.0170	0.8130	0.0193	192.8	1.918	2.925	1.317	0.955	1.128	1.044	-1285.	1199.	14.2	0.603	
0.	0.98	0.0178	0.8021	0.0103	192.8	1.920	2.923	1.314	0.955	1.118	1.045	-1288.	1195.	14.1	0.641	
0.	0.99	0.02	0.3787	0.0203	192.8	1.922	2.920	1.311	0.954	1.116	1.045	-1292.	1192.	14.1	0.619	
0.	0.99	0.03	0.3742	0.0301	0.9593	192.8	1.924	2.917	1.308	0.953	1.114	1.045	-1296.	1188.	14.1	0.597
0.	0.99	0.04	0.3705	0.0403	0.5484	192.8	1.927	2.914	1.305	0.952	1.112	1.045	-1299.	1184.	14.1	0.576
0.	0.99	0.05	0.3664	0.0500	0.5436	192.9	1.929	2.912	1.302	0.951	1.110	1.050	-1303.	1181.	14.1	0.554
0.	0.99	0.07	0.3583	0.0698	0.5719	192.9	1.933	2.908	1.297	0.950	1.105	1.050	-1310.	1173.	14.0	0.511
0.	0.99	0.10	0.3463	0.0992	0.5549	192.9	1.939	2.498	1.284	0.948	1.099	1.051	-1321.	1162.	14.0	0.447
0.	0.99	0.20	0.3310	0.3056	0.3434	193.4	1.959	2.469	1.260	0.942	1.080	1.050	-1357.	1127.	13.8	0.239
0.	0.99	0.40	0.1564	0.5772	0.2664	193.9	2.032	2.348	1.155	0.932	1.027	1.082	-1427.	1059.	13.4	0.815
0.	0.99	0.60	0.0844	0.7749	0.1408	194.6	2.064	2.284	1.104	0.935	1.011	1.122	-1495.	988.	13.0	0.706
0.	0.99	0.90	0.0400	0.8863	0.0720	195.0	2.079	2.250	1.083	0.939	1.008	1.130	-1561.	919.	12.8	0.633
0.	0.	0.0265	0.	0.3715	196.5	1.955	2.537	1.298	0.966	1.146	1.013	-1226.	1152.	14.5	0.794	
0.	0.	0.01	0.6232	0.0000	0.3608	186.6	1.057	2.534	1.295	0.966	1.144	1.013	-1230.	1149.	14.5	0.775
0.	0.	0.02	0.6178	0.0101	0.3661	186.7	1.059	2.532	1.292	0.965	1.141	1.013	-1234.	1147.	14.5	0.756
0.	0.	0.03	0.6125	0.0242	0.3633	186.7	1.061	2.529	1.289	0.964	1.139	1.012	-1238.	1144.	14.5	0.737
0.	0.	0.04	0.6072	0.0322	0.3606	186.8	1.063	2.526	1.287	0.963	1.137	1.012	-1242.	1142.	14.4	0.718
0.	0.	0.05	0.6019	0.0403	0.3570	186.9	1.065	2.523	1.284	0.963	1.134	1.012	-1246.	1140.	14.4	0.698
0.	0.	0.07	0.5912	0.0565	0.3523	187.0	1.066	2.518	1.281	0.961	1.133	1.012	-1255.	1135.	14.4	0.660
0.	0.	0.10	0.5792	0.0809	0.3439	187.2	1.075	2.509	1.271	0.959	1.123	1.012	-1267.	1127.	14.3	0.602
0.	0.	0.20	0.5213	0.1634	0.3153	187.9	1.093	2.494	1.244	0.954	1.101	1.020	-1308.	1103.	14.0	0.405
0.	0.	0.40	0.4896	0.3346	0.2939	189.5	2.024	2.420	1.193	0.946	1.066	1.108	-1389.	1051.	13.8	7.991
0.	0.	0.60	0.2891	0.5270	0.1840	191.2	2.057	2.357	1.146	0.942	1.030	1.120	-1469.	993.	13.2	7.677
0.	0.	0.90	0.1946	0.7441	0.1014	193.2	2.078	2.280	1.101	0.942	1.018	1.130	-1548.	924.	12.7	7.027
0.	0.	0.95	0.0863	0.8662	0.0535	194.3	2.086	2.253	1.080	0.943	1.011	1.148	-1586.	885.	12.5	0.741
0.	0.	0.99	0.0215	0.2105	181.5	1.945	2.501	1.273	0.973	1.108	1.171	-1153.	1112.	14.8	0.930	
0.	0.	0.99	0.02	0.7707	0.0134	207.9	1.071	2.497	1.270	0.973	1.177	1.170	-1158.	1111.	14.7	0.921
0.	0.	0.99	0.03	0.7732	0.0202	206.6	1.072	2.495	1.268	0.972	1.174	1.169	-1163.	1109.	14.7	0.902
0.	0.	0.99	0.04	0.7677	0.0270	205.3	1.078	2.492	1.265	0.971	1.171	1.169	-1168.	1100.	14.7	0.884
0.	0.	0.99	0.05	0.7622	0.0336	204.0	1.081	2.474	1.257	0.963	1.171	1.168	-1173.	1106.	14.7	0.866
0.	0.	0.99	0.07	0.7511	0.0476	204.3	1.077	2.467	1.250	0.963	1.169	1.165	-1187.	1105.	14.6	0.848
0.	0.	0.99	0.10	0.7343	0.0684	205.3	1.081	2.468	1.244	0.967	1.152	1.163	-1202.	1077.	14.5	0.811
0.	0.	0.99	0.20	0.6765	0.1402	204.3	1.087	2.411	1.224	0.963	1.127	1.150	-1230.	1060.	14.3	0.755
0.	0.	0.99	0.40	0.5499	0.2954	204.3	2.011	2.460	1.244	0.954	1.101	1.120	-1347.	1041.	13.7	0.364
0.	0.	0.99	0.60	0.4621	0.4642	204.3	2.061	2.352	1.224	0.956	1.085	1.131	-1397.	989.	13.3	7.067
0.	0.	0.99	0.													

Table 25. (cont.)

PRESSURE = 4. ATM

LIQUID MOLE FRACTION	VAPOR MOLE FRACTION	TEMP	RELATIVE VOL	PRESSURE ACT COEF	ENTHALPY			HEAT CAPACITY		
					N2/AR	N2/O2	AR/O2	BTU/LB MOLE	BTU/LB MOLE-R	
0.0	0.0	0.	1.000	2.8.9	1.737	2.240	1.290	0.000	1.000	-1216. 1275. 14.0 9.020
0.0	0.01	0.	0.0128 0.9872	2.8.8	1.739	2.239	1.287	0.007	1.079	-1220. 1269. 13.0 8.993
0.0	0.02	0.	0.0256 0.9744	2.8.7	1.742	2.238	1.285	0.007	1.077	-1224. 1243. 13.0 8.966
0.0	0.03	0.	0.0382 0.9618	2.8.6	1.744	2.237	1.283	0.007	1.075	1.004 -1227. 1250. 13.0 8.940
0.0	0.04	0.	0.0506 0.9494	2.8.5	1.746	2.236	1.280	0.006	1.074	1.004 -1231. 1252. 13.0 8.914
0.0	0.05	0.	0.0630 0.9370	2.8.4	1.749	2.234	1.278	0.006	1.073	1.005 -1235. 1246. 13.0 8.888
0.0	0.07	0.	0.0874 0.9126	2.8.2	1.753	2.232	1.273	0.005	1.070	1.006 -1242. 1235. 13.0 8.837
0.0	0.10	0.	0.1233 0.8767	2.8.0	1.760	2.228	1.266	0.004	1.065	1.009 -1253. 1219. 13.0 8.762
0.0	0.20	0.	0.2369 0.7632	2.7.1	1.782	2.213	1.242	0.002	1.052	1.017 -1268. 1168. 13.0 8.524
0.0	0.40	0.	0.4430 0.5570	2.5.5	1.825	2.177	1.193	0.000	1.030	1.030 -1354. 1077. 13.5 8.089
0.0	0.60	0.	0.6319 0.3681	2.4.7	1.865	2.135	1.144	0.002	1.014	1.007 -1414. 996. 13.3 7.606
0.0	0.80	0.	0.8143 0.1857	2.4.9	1.903	2.086	1.096	0.000	1.003	1.006 -1471. 920. 13.1 7.288
0.0	0.90	0.	0.9061 0.039	2.3.7	1.921	2.066	1.072	0.000	1.003	1.129 -1498. 802. 13.0 7.006
0.10	0.	0.2018 0.	0.7683	2.4.8	1.768	2.275	1.287	0.005	1.027	-1193. 1246. 14.2 9.076
0.10	0.01	0.1994 0.0114	0.7693	2.4.7	1.770	2.273	1.285	0.005	1.028	-1197. 1241. 14.2 9.052
0.10	0.02	0.1969 0.0227	0.7684	2.4.6	1.772	2.271	1.282	0.004	1.024	-1201. 1236. 14.2 9.028
0.10	0.03	0.1946 0.0339	0.7715	2.4.6	1.774	2.270	1.279	0.004	1.022	-1204. 1231. 14.2 9.004
0.10	0.04	0.1922 0.0451	0.7627	2.4.6	1.776	2.268	1.277	0.003	1.021	-1208. 1227. 14.2 8.981
0.10	0.05	0.1898 0.0562	0.7540	2.4.6	1.778	2.266	1.274	0.003	1.019	1.030 -1212. 1222. 14.2 8.957
0.10	0.07	0.1851 0.0782	0.7367	2.4.5	1.782	2.262	1.269	0.003	1.011	1.031 -1219. 1213. 14.1 8.911
0.10	0.10	0.1702 0.1108	0.7111	2.4.4	1.788	2.256	1.262	0.000	1.004	1.032 -1230. 1199. 14.1 8.841
0.10	0.20	0.1566 0.2159	0.6821	2.4.6	1.807	2.236	1.237	0.000	1.005	1.030 -1266. 1155. 14.0 8.617
0.10	0.40	0.1146 0.4145	0.4709	2.3.5	1.844	2.191	1.100	0.000	1.039	-1334. 1074. 13.7 8.187
0.10	0.60	0.0758 0.6566	0.3196	2.3.3	1.870	2.142	1.040	0.000	1.021	-1401. 998. 13.4 7.766
0.10	0.80	0.0481 0.7979	0.1641	2.3.3	1.909	2.089	1.094	0.000	1.009	1.114 -1464. 922. 13.2 7.336
0.10	0.90	0.0192 0.8971	0.0437	2.3.4	1.924	2.061	1.071	0.000	1.003	-1494. 804. 13.1 7.111
0.20	0.	0.3649 0.	0.3591	2.0.0	1.794	2.299	1.281	0.010	1.114	-1167. 1218. 14.5 9.149
0.20	0.01	0.3610 0.0102	0.6249	2.0.0	1.796	2.296	1.279	0.010	1.112	1.054 -1171. 1214. 14.5 9.127
0.20	0.02	0.3571 0.0203	0.6226	2.0.1	1.798	2.294	1.276	0.010	1.108	1.055 -1175. 1210. 14.5 9.104
0.20	0.03	0.3532 0.0303	0.6165	2.0.1	1.799	2.292	1.274	0.010	1.108	1.055 -1179. 1207. 14.5 9.082
0.20	0.04	0.3493 0.0404	0.6103	2.0.1	1.801	2.289	1.271	0.010	1.106	1.055 -1183. 1203. 14.4 9.060
0.20	0.05	0.3454 0.0504	0.6042	2.0.1	1.803	2.287	1.269	0.010	1.104	1.055 -1187. 1199. 14.4 9.038
0.20	0.07	0.3377 0.0784	0.5919	2.0.1	1.806	2.282	1.263	0.010	1.100	1.056 -1194. 1191. 14.4 9.095
0.20	0.10	0.3263 0.1000	0.5734	2.0.1	1.812	2.275	1.256	0.010	1.095	1.057 -1206. 1180. 14.3 9.029
0.20	0.20	0.2899 0.1975	0.5135	2.0.1	1.829	2.251	1.231	0.007	1.077	1.061 -1243. 1142. 14.2 8.714
0.20	0.40	0.2170 0.3087	0.3944	2.0.1	1.861	2.200	1.183	0.009	1.049	1.075 -1317. 1070. 13.8 8.285
0.20	0.60	0.1464 0.5810	0.2727	2.0.1	1.890	2.147	1.136	0.007	1.027	1.095 -1388. 999. 13.5 7.846
0.20	0.80	0.0749 0.7810	0.1432	2.0.2	1.916	2.092	1.092	0.000	1.012	-1457. 925. 13.2 7.303
0.20	0.90	0.1380 0.8882	0.0738	2.0.3	1.928	2.063	1.070	0.000	1.007	-1491. 806. 13.1 7.136
0.40	0.	0.0868 0.	0.3932	1.9.4	1.831	2.315	1.264	0.041	1.147	-1167. 1169. 15.0 9.328
0.40	0.01	0.0815 0.0083	0.3962	1.9.4	1.833	2.312	1.262	0.040	1.145	-1171. 1214. 15.0 9.307
0.40	0.02	0.5962 0.0164	0.3872	1.9.4	1.834	2.310	1.259	0.039	1.142	1.113 -1186. 1184. 14.9 9.287
0.40	0.03	0.5959 0.0249	0.3842	1.9.4	1.836	2.307	1.257	0.039	1.140	1.113 -1190. 1181. 14.9 9.266
0.40	0.04	0.5857 0.0332	0.3811	1.9.4	1.837	2.305	1.254	0.038	1.138	1.113 -1194. 1186. 14.9 9.246
0.40	0.05	0.3684 0.0415	0.3781	1.9.4	1.839	2.302	1.252	0.037	1.139	1.112 -1198. 1196. 14.9 9.225
0.40	0.07	0.3599 0.0582	0.3720	1.9.5	1.842	2.297	1.247	0.039	1.131	1.112 -1197. 1191. 14.9 9.184
0.40	0.10	0.3539 0.0833	0.3628	1.9.5	1.847	2.290	1.240	0.033	1.124	1.112 -1195. 1183. 14.7 9.122
0.40	0.20	0.3005 0.1640	0.3316	1.9.6	1.862	2.264	1.216	0.027	1.104	1.111 -1193. 1116. 14.5 9.113
0.40	0.40	0.3005 0.3445	0.2650	1.9.7	1.889	2.211	1.170	0.017	1.069	1.115 -1277. 1061. 14.1 8.475
0.40	0.60	0.2734 0.5933	0.1903	1.9.8	1.911	2.155	1.127	0.010	1.042	1.124 -1361. 999. 13.7 8.001
0.40	0.80	0.1449 0.7514	0.1937	2.0.1	1.928	2.096	1.087	0.006	1.020	1.130 -1443. 829. 13.3 7.475
0.40	0.90	0.0749 0.8708	0.0544	2.0.2	1.934	2.065	1.065	0.000	1.011	-1484. 809. 13.1 7.186
0.60	0.	0.7748 0.	0.2252	1.8.3	1.847	2.293	1.241	0.050	1.187	-1036. 1126. 15.3 9.534
0.60	0.01	0.7694 0.0070	0.2236	1.8.4	1.849	2.291	1.239	0.050	1.184	1.041 -1125. 1125. 15.3 9.514
0.60	0.02	0.7636 0.0140	0.2223	1.8.5	1.851	2.290	1.237	0.050	1.181	1.046 -1123. 1123. 15.3 9.494
0.60	0.03	0.7580 0.0211	0.2209	1.8.7	1.853	2.288	1.235	0.050	1.179	1.051 -1121. 1121. 15.2 9.473
0.60	0.04	0.7524 0.0282	0.2194	1.8.8	1.855	2.286	1.232	0.050	1.178	1.056 -1120. 1120. 15.2 9.453
0.60	0.05	0.7466 0.0353	0.2180	1.8.9	1.857	2.284	1.230	0.050	1.177	1.055 -1123. 1123. 15.2 9.432
0.60	0.07	0.7354 0.0496	0.2150	1.9.0	1.859	2.282	1.226	0.050	1.176	1.054 -1161. 1110. 15.2 9.412
0.60	0.10	0.7182 0.0713	0.2105	1.9.0	1.864	2.280	1.226	0.050	1.171	1.071 -1171. 1114. 15.1 9.391
0.60	0.20	0.6591 0.1459	0.1950	1.9.1	1.882	2.254	1.197	0.044	1.134	1.112 -1136. 1091. 14.9 9.115
0.60	0.40	0.3840 0.4974	0.1187	1.9.6	1.911	2.209	1.156	0.032	1.100	-1355. 1049. 14.3 8.659
0.60	0.60	0.2183 0.7229	0.0644	2.0.0	1.945	2.099	1.088	0.027	1.057	-1333. 998. 13.9 8.190
0.60	0.80	0.1449 0.8376	0.0175	2.0.1	1.947	2.067	1.067	0.021	1.024	-1429. 932. 13.3 7.565
0.60	0.90	0.0957 0.	0.3683	1.8.7	1.847	2.243	1.214	0.063	1.151	-1477. 891. 13.1 7.038
0.60	0.91	0.8942 0.0056	0.0139	1.8.7	1.849	2.242	1.212	0.077	1.234	1.276 -963. 1000. 15.0 9.758
0.60	0.92	0.8911 0.0116	0.0473	1.8.2	1.847	2.239	1.209	0.074	1.231	1.274 -968. 1007. 15.0 9.737
0.60	0.93	0.8956 0.0174	0.0471	1.8.4	1.850	2.239	1.204	0.074	1.227	1.272 -974. 1006. 15.0 9.716
0.60	0.94	0.9340 0.0232	0.0466	1.8.5	1.853	2.233	1.202	0.074	1.226	1.270 -980. 1005. 15.0 9.673
0.60	0.95	0.9244 0.0291	0.0449	1.8.7	1.855	2.230	1.191	0.075	1.225	1.268 -986. 1004. 15.0 9.651
0.60	0.97	0.9136 0.0410	0.0459	1.8.8	1.861	2.229	1.187	0.073	1.224	1.264 -996.

LIQUID MOLE FRACTION	VAPOR MOLE FRACTION			TEMP	RELATIVE VOL			PRESSURE ACT COEF	ENTHALPY			HEAT CAPACITY				
	N2	N2+O2	AR		N2	AR	O2		N2	AR	O2	Liq	Vap	Liq	Vap	
0.0	0.0	0.0	0.	1.0000	215.6	1.656	2.089	1.262	0.852	1.002	"1121-	1285.	14.3	9.498		
0.0	0.01	0.0	0.0126	0.9874	215.5	1.658	2.088	1.259	0.852	1.000	"1125-	1279.	14.3	9.472		
0.0	0.02	0.0	0.0250	0.9790	215.4	1.660	2.087	1.257	0.852	1.000	"1129-	1274.	14.3	9.446		
0.0	0.03	0.0	0.0374	0.9624	215.3	1.662	2.086	1.255	0.852	1.000	"1133-	1268.	14.3	9.420		
0.0	0.04	0.0	0.0496	0.9504	215.2	1.664	2.085	1.253	0.852	1.000	"1137-	1262.	14.3	9.395		
0.0	0.05	0.0	0.0618	0.9342	215.1	1.666	2.084	1.251	0.851	1.001	"1140-	1256.	14.3	9.369		
0.0	0.07	0.0	0.0858	0.9142	214.9	1.670	2.081	1.248	0.851	1.000	"1146-	1245.	14.3	9.319		
0.0	0.10	0.0	0.1211	0.8789	214.7	1.676	2.078	1.240	0.851	1.000	"1150-	1228.	14.2	9.245		
0.0	0.20	0.0	0.2334	0.7666	213.8	1.695	2.064	1.218	0.849	1.044	1.018	"1155-	1177.	14.1	9.011	
0.0	0.40	0.0	0.4389	0.5611	212.5	1.731	2.035	1.173	0.848	1.025	1.039	"1202-	1083.	14.0	8.577	
0.0	0.60	0.0	0.6286	0.3714	211.4	1.765	1.991	1.128	0.851	1.011	1.068	"1233-	999.	13.8	8.178	
0.0	0.80	0.0	0.8126	0.1774	210.7	1.795	1.948	1.084	0.858	1.004	1.105	"1381-	921.	13.7	7.767	
0.0	0.90	0.0	0.9053	0.0947	210.4	1.812	1.924	1.052	0.863	1.002	1.127	"1408-	882.	13.6	7.599	
0.10	0.	0.	0.1903	0.	211.6	1.686	2.115	1.259	0.872	1.088	1.030	"1095-	1257.	14.6	9.578	
0.10	0.11	0.	0.1880	0.0113	0.8007	211.5	1.688	2.112	1.256	0.871	1.088	1.030	"1099-	1252.	14.6	9.546
0.10	0.17	0.	0.1854	0.0229	0.7917	211.5	1.688	2.112	1.254	0.871	1.089	1.031	"1103-	1247.	14.6	9.522
0.10	0.20	0.	0.1835	0.0337	0.77428	211.4	1.688	2.110	1.252	0.870	1.083	1.031	"1107-	1242.	14.5	9.499
0.10	0.04	0.0	0.1813	0.0448	0.7739	211.4	1.687	2.108	1.249	0.870	1.082	1.032	"1111-	1237.	14.5	9.475
0.10	0.05	0.	0.1793	0.0558	0.7651	211.3	1.689	2.107	1.247	0.869	1.080	1.032	"1114-	1232.	14.5	9.452
0.10	0.07	0.	0.1747	0.0777	0.7476	211.3	1.693	2.103	1.243	0.869	1.077	1.033	"1122-	1223.	14.5	9.405
0.10	0.10	0.	0.1682	0.1101	0.7217	211.7	1.698	2.098	1.236	0.867	1.073	1.039	"1134-	1209.	14.5	9.338
0.10	0.20	0.	0.1474	0.2149	0.6377	210.9	1.714	2.086	1.213	0.864	1.095	1.041	"1171-	1163.	14.3	9.112
0.10	0.40	0.103	0.4137	0.4780	210.3	1.746	2.040	1.169	0.856	1.036	1.058	"1242-	1079.	14.1	8.680	
0.10	0.80	0.	0.3680	0.7981	0.1660	210.0	1.775	1.986	1.125	0.859	1.039	1.082	"1310-	1000.	13.9	8.253
0.10	0.90	0.	0.181	0.8973	0.0846	210.1	1.802	1.949	1.082	0.862	1.008	1.113	"1374-	923.	13.7	7.814
0.20	0.	0.	0.3479	0.	0.6522	207.9	1.702	2.134	1.294	0.889	1.107	1.050	"1067-	1229.	14.9	9.663
0.20	0.01	0.	0.3441	0.0102	0.6457	207.9	1.704	2.132	1.291	0.888	1.108	1.050	"1073-	1225.	14.8	9.640
0.20	0.02	0.	0.3464	0.0204	0.6393	207.9	1.705	2.130	1.289	0.887	1.104	1.050	"1075-	1221.	14.8	9.618
0.20	0.03	0.	0.3366	0.0305	0.6329	207.9	1.707	2.128	1.287	0.887	1.102	1.050	"1079-	1217.	14.8	9.596
0.20	0.04	0.	0.3329	0.0406	0.6265	207.9	1.708	2.126	1.284	0.886	1.100	1.050	"1083-	1213.	14.8	9.573
0.20	0.05	0.	0.3292	0.0507	0.6203	207.9	1.709	2.124	1.282	0.886	1.100	1.050	"1087-	1209.	14.8	9.551
0.20	0.07	0.	0.3219	0.0707	0.6074	207.9	1.713	2.120	1.277	0.884	1.100	1.050	"1095-	1201.	14.8	9.508
0.20	0.10	0.	0.3119	0.1006	0.5846	207.9	1.718	2.113	1.255	0.883	1.100	1.050	"1107-	1189.	14.7	9.446
0.20	0.20	0.	0.2752	0.1946	0.5262	207.9	1.732	2.092	1.208	0.877	1.074	1.068	"1146-	1159.	14.6	9.221
0.20	0.40	0.	0.1889	0.5038	0.2777	207.9	1.746	2.048	1.163	0.870	1.047	1.078	"1222-	1075.	14.3	8.782
0.20	0.60	0.	0.176	0.7844	0.1452	209.3	1.807	1.951	1.021	0.865	1.027	1.097	"1266-	1001.	14.0	8.334
0.20	0.80	0.	0.1359	0.6895	0.0744	209.3	1.816	1.917	1.000	0.866	1.012	1.121	"1367-	924.	13.7	7.881
0.40	0.	0.	0.5889	0.	0.4111	211.6	1.735	2.149	1.238	0.917	1.147	1.123	"1004-	1178.	15.4	9.695
0.40	0.01	0.	0.5837	0.0065	0.4079	211.4	1.737	2.147	1.236	0.917	1.145	1.123	"1009-	1175.	15.4	9.674
0.40	0.02	0.	0.5784	0.0170	0.4046	211.5	1.738	2.144	1.234	0.918	1.143	1.122	"1013-	1173.	15.3	9.652
0.40	0.03	0.	0.5732	0.0255	0.4014	211.6	1.740	2.142	1.231	0.918	1.142	1.122	"1018-	1170.	15.3	9.630
0.40	0.04	0.	0.5679	0.0340	0.3981	211.6	1.741	2.140	1.229	0.918	1.141	1.122	"1022-	1167.	15.3	9.608
0.40	0.05	0.	0.5627	0.0425	0.3949	211.7	1.742	2.138	1.227	0.913	1.138	1.121	"1026-	1184.	15.3	9.787
0.40	0.07	0.	0.5522	0.0595	0.3863	211.8	1.745	2.133	1.222	0.912	1.132	1.121	"1035-	1159.	15.2	9.743
0.40	0.10	0.	0.5364	0.0852	0.3784	212.0	1.748	2.126	1.216	0.909	1.129	1.120	"1049-	1158.	15.2	9.677
0.40	0.20	0.	0.4836	0.1715	0.3449	212.8	1.762	2.102	1.196	0.904	1.121	1.119	"1053-	1122.	15.0	9.454
0.40	0.40	0.	0.3755	0.3506	0.2739	214.3	1.782	2.082	1.194	0.902	1.109	1.119	"1063-	1053.	14.9	8.993
0.40	0.60	0.	0.2613	0.5433	0.1954	216.0	1.804	2.080	1.112	0.892	1.082	1.121	"1267-	1000.	14.2	8.497
0.40	0.80	0.	0.1370	0.7580	0.0856	218.0	1.818	1.954	1.079	0.878	1.021	1.138	"1352-	927.	13.8	7.953
0.40	0.90	0.	0.0748	0.1921	0.0380	219.0	1.823	1.927	1.057	0.872	1.011	1.144	"1394-	887.	13.7	7.859
0.60	0.	0.	0.7564	0.0073	0.7664	196.0	1.756	2.133	1.217	0.943	1.193	1.000	"934-	1133.	15.8	10.175
0.60	0.02	0.	0.7530	0.0145	0.7348	196.1	1.757	2.131	1.213	0.941	1.187	1.000	"939-	1131.	15.8	10.152
0.60	0.03	0.	0.7495	0.0218	0.7332	196.2	1.759	2.130	1.210	0.940	1.186	1.000	"944-	1129.	15.8	10.129
0.60	0.04	0.	0.7392	0.0292	0.7316	196.4	1.760	2.128	1.209	0.939	1.181	1.000	"949-	1127.	15.7	10.106
0.60	0.05	0.	0.7335	0.0365	0.7300	196.5	1.762	2.126	1.207	0.938	1.179	1.000	"954-	1125.	15.7	10.083
0.60	0.07	0.	0.7219	0.0513	0.7268	196.7	1.765	2.122	1.203	0.938	1.179	1.000	"959-	1124.	15.7	10.068
0.60	0.10	0.	0.7044	0.0737	0.7219	197.0	1.769	2.117	1.196	0.934	1.165	1.000	"969-	1120.	15.8	10.014
0.60	0.20	0.	0.6445	0.1506	0.7049	199.0	1.783	2.097	1.177	0.925	1.148	1.000	"985-	1111.	15.6	9.944
0.60	0.40	0.	0.5155	0.3173	0.1472	210.7	1.805	2.085	1.139	0.910	1.097	1.000	"1036-	1095.	15.3	9.707
0.60	0.60	0.	0.3696	0.5077	0.1227	213.5	1.820	2.088	1.103	0.907	1.080	1.000	"1208-	993.	14.3	9.268
0.6																

Table 25. (cont.)

PRESSURE = 12. ATM

LIQUID MOLE FRACTION	VAPOR				IFMP	RELATIVE VOL	PRESSURE ACT COEF	ENTHALPY			HEAT CAPACITY					
	MOLE FRACTION							N2	AR	02						
N2/N2+02	AR	N2	AR	02	R	N2/AR	N2/02	AR/02	N2	AR	02	Liq	Vap	Liq	Vap	
0.4	1.0	1.0	0.0	1.0000	221.4	1.988	1.980	1.239	0.825	1.037	1.003	-1037.	1296.	14.8	16.812	
0.5	0.01	0.0	0.0123	0.9877	221.3	1.980	1.979	1.237	0.824	1.035	1.003	-1041.	1284.	14.8	9.986	
0.5	0.02	0.0	0.0246	0.9754	221.2	1.982	1.977	1.235	0.824	1.034	1.004	-1045.	1278.	14.7	9.961	
0.5	0.03	0.0	0.0367	0.9633	221.1	1.983	1.976	1.233	0.824	1.033	1.005	-1049.	1272.	14.7	9.935	
0.5	0.04	0.0	0.0488	0.9512	221.0	1.985	1.975	1.231	0.824	1.032	1.006	-1052.	1266.	14.7	9.910	
0.5	0.05	0.0	0.0607	0.9393	220.9	1.987	1.974	1.229	0.824	1.031	1.006	-1056.	1260.	14.7	9.885	
0.5	0.06	0.0	0.0844	0.9156	220.8	1.988	1.973	1.225	0.824	1.030	1.006	-1064.	1249.	14.7	9.856	
0.5	0.07	0.0	0.0844	0.9156	220.7	1.988	1.973	1.225	0.824	1.029	1.006	-1075.	1232.	14.7	9.764	
0.5	0.08	0.0	0.1192	0.8808	220.6	1.985	1.967	1.218	0.823	1.028	1.010	-1111.	1186.	14.6	9.532	
0.5	0.09	0.0	0.2305	0.7896	219.6	1.981	1.953	1.198	0.822	1.026	1.010	-1119.	1084.	14.4	9.181	
0.5	0.10	0.0	0.4354	0.5457	218.3	1.961	1.921	1.157	0.822	1.020	1.041	-1242.	998.	14.3	8.891	
0.5	0.11	0.0	0.6259	0.3742	217.2	1.940	1.884	1.119	0.823	1.008	1.069	-1366.	917.	14.2	8.279	
0.5	0.12	0.0	0.8132	0.3489	216.5	1.917	1.844	1.074	0.821	1.002	1.104	-1328.	877.	14.1	8.067	
0.5	0.13	0.0	0.9046	0.3054	216.3	1.730	1.822	1.053	0.816	0.951	1.125	-1048.	807.	14.1	8.067	
0.10	0.0	0.01	0.3186	0.0	0.8185	217.4	1.918	1.907	1.235	0.845	1.079	1.032	-1088.	1261.	15.0	16.102
0.10	0.01	0.1794	0.0112	0.8094	217.4	1.918	1.909	1.233	0.844	1.078	1.033	-1012.	1259.	15.0	16.076	
0.10	0.02	0.1773	0.0223	0.8004	217.4	1.919	1.904	1.231	0.844	1.076	1.033	-1015.	1251.	14.9	16.055	
0.10	0.03	0.1752	0.0334	0.7914	217.3	1.921	1.902	1.229	0.843	1.075	1.034	-1029.	1240.	14.9	16.031	
0.10	0.04	0.1731	0.0445	0.7825	217.3	1.922	1.900	1.227	0.843	1.074	1.034	-1024.	1241.	14.9	16.006	
0.10	0.05	0.1710	0.0554	0.7735	217.2	1.924	1.900	1.225	0.843	1.072	1.035	-1028.	1236.	14.9	9.985	
0.10	0.06	0.1688	0.0672	0.7680	217.1	1.927	1.906	1.221	0.842	1.069	1.036	-1038.	1227.	14.9	9.938	
0.10	0.07	0.1667	0.0772	0.7620	217.0	1.931	1.901	1.219	0.841	1.065	1.037	-1048.	1212.	14.9	9.870	
0.10	0.08	0.1647	0.0872	0.7599	217.0	1.931	1.901	1.214	0.841	1.063	1.037	-1058.	1186.	14.8	9.845	
0.10	0.09	0.1626	0.0972	0.7548	216.9	1.932	1.901	1.214	0.840	1.062	1.037	-1159.	1080.	14.6	9.209	
0.10	0.10	0.1605	0.1072	0.7500	216.8	1.934	1.902	1.211	0.839	1.060	1.037	-1227.	998.	14.4	8.776	
0.10	0.11	0.1584	0.1172	0.7451	216.7	1.934	1.902	1.207	0.838	1.056	1.112	-1292.	916.	14.2	8.327	
0.10	0.12	0.1563	0.1272	0.7404	216.6	1.934	1.902	1.202	0.838	1.053	1.129	-1324.	878.	14.2	8.092	
0.20	0.0	0.3344	0.	0.8555	213.8	1.833	2.010	1.231	0.863	1.151	1.053	-978.	1234.	15.2	16.216	
0.20	0.01	0.3323	0.0102	0.8555	213.8	1.834	2.008	1.229	0.862	1.150	1.053	-982.	1229.	15.2	16.194	
0.20	0.02	0.3272	0.0204	0.8524	213.8	1.834	2.006	1.228	0.862	1.149	1.053	-986.	1225.	15.2	16.171	
0.20	0.03	0.3236	0.0306	0.8459	213.8	1.837	2.004	1.224	0.861	1.148	1.054	-990.	1221.	15.2	16.150	
0.20	0.04	0.3200	0.0407	0.8393	213.8	1.838	2.002	1.222	0.861	1.147	1.054	-995.	1217.	15.2	16.128	
0.20	0.05	0.3165	0.0508	0.8328	213.8	1.840	2.001	1.220	0.860	1.143	1.054	-999.	1213.	15.2	16.095	
0.20	0.06	0.3134	0.0608	0.8270	213.8	1.843	1.997	1.216	0.859	1.142	1.055	-1007.	1204.	15.1	16.050	
0.20	0.07	0.3094	0.0708	0.8219	213.8	1.847	1.991	1.209	0.857	1.140	1.056	-1019.	1192.	15.1	9.992	
0.20	0.08	0.3052	0.0808	0.8156	213.8	1.850	1.989	1.208	0.856	1.139	1.056	-1029.	1182.	15.0	9.769	
0.20	0.09	0.3010	0.0908	0.8090	213.8	1.852	1.987	1.208	0.852	1.137	1.057	-1037.	1074.	14.7	9.322	
0.20	0.10	0.2969	0.1008	0.8033	213.8	1.854	1.987	1.207	0.851	1.131	1.057	-1213.	998.	14.5	8.862	
0.20	0.11	0.2928	0.1108	0.7973	213.8	1.854	1.982	1.201	0.849	1.121	1.051	-1289.	920.	14.3	8.375	
0.20	0.12	0.2886	0.1208	0.7914	213.8	1.854	1.982	1.201	0.848	1.111	1.051	-1312.	881.	14.2	8.118	
0.40	0.	0.5739	0.	0.4261	217.2	1.661	2.030	1.214	0.896	1.147	1.131	-913.	1182.	15.8	16.510	
0.40	0.01	0.5687	0.0086	0.4227	217.3	1.662	2.030	1.214	0.895	1.144	1.131	-917.	1179.	15.8	16.487	
0.40	0.02	0.5655	0.0183	0.4192	217.4	1.663	2.030	1.214	0.894	1.142	1.130	-922.	1178.	15.7	16.464	
0.40	0.03	0.5623	0.0280	0.4158	217.4	1.665	2.030	1.214	0.894	1.140	1.130	-926.	1173.	15.7	16.441	
0.40	0.04	0.5591	0.0376	0.4123	217.5	1.666	2.030	1.214	0.893	1.139	1.130	-931.	1170.	15.7	16.416	
0.40	0.05	0.5559	0.0473	0.4089	217.6	1.667	2.030	1.208	0.892	1.138	1.130	-936.	1167.	15.7	16.395	
0.40	0.06	0.5525	0.0568	0.4051	217.7	1.669	2.030	1.202	0.890	1.131	1.129	-945.	1161.	15.6	16.349	
0.40	0.07	0.5491	0.0667	0.3991	217.9	1.670	2.030	1.195	0.888	1.125	1.128	-956.	1152.	15.6	16.281	
0.40	0.08	0.5456	0.0763	0.3943	218.0	1.671	2.030	1.190	0.886	1.124	1.128	-1004.	1123.	15.4	16.245	
0.40	0.09	0.5421	0.0860	0.3894	218.1	1.672	2.030	1.184	0.884	1.122	1.128	-1047.	1062.	15.6	9.557	
0.40	0.10	0.5381	0.0959	0.3856	218.2	1.673	2.030	1.180	0.882	1.120	1.128	-1163.	998.	14.7	9.336	
0.40	0.11	0.5340	0.1059	0.3816	218.3	1.674	2.030	1.176	0.881	1.119	1.128	-1276.	922.	14.3	8.472	
0.40	0.12	0.5299	0.1159	0.3765	218.4	1.674	2.030	1.170	0.880	1.119	1.128	-1312.	881.	14.2	8.168	
0.40	0.13	0.5268	0.1259	0.3724	218.5	1.674	2.030	1.164	0.879	1.118	1.128	-1364.	833.	14.3	8.219	
0.40	0.14	0.5235	0.1359	0.3684	218.6	1.675	2.030	1.158	0.878	1.117	1.128	-1412.	787.	14.2	8.067	
0.40	0.15	0.5193	0.1459	0.3645	218.7	1.675	2.030	1.152	0.877	1.116	1.128	-1464.	737.	14.1	7.937	
0.40	0.16	0.5151	0.1559	0.3604	218.8	1.676	2.030	1.146	0.876	1.115	1.128	-1512.	687.	14.0	7.806	
0.40	0.17	0.5109	0.1659	0.3564	218.9	1.676	2.030	1.140	0.875	1.114	1.128	-1560.	645.	13.9	7.669	
0.40	0.18	0.5067	0.1757	0.3525	219.0	1.677	2.030	1.134	0.874	1.113	1.128	-1608.	604.	13.8	7.537	
0.40	0.19	0.5025	0.1855	0.3484	219.1	1.678	2.030	1.128	0.873	1.112	1.128	-1656.	563.	13.7	7.406	
0.40	0.20	0.4983	0.1953	0.3443	219.2	1.678	2.030	1.122	0.872	1.111	1.128	-1704.	523.	13.6		

Table 25. (cont.)

PRESSURE = 14, ATM

LIQUID MOLE FRACTION		VAPOR MOLE FRACTION		TEMP	RELATIVE VOL			PRESSURE ACT COEF			ENTHALPY BTU/LB MOLE			HEAT CAPACITY BTU/LB MOLE-R		
N2/N2+O2	AR	N2	AR	O2	R	N2/AR	N2/O2	AR/O2	N2	AR	O2	Liq	Vap	Liq	Vap	
0.0	0.0	0.	0.	1.000	220.0	1.557	1.099	1.219	0.002	1.046	1.002	-98.0	129.0	15.2	10.571	
0.1	0.1	0.011	0.	0.0121	0.9879	226.5	1.559	1.097	1.217	0.002	1.045	1.003	-96.4	128.4	15.2	10.546
0.2	0.2	0.0242	0.	0.9757	226.4	1.560	1.096	1.215	0.002	1.045	1.004	-96.6	127.6	15.2	10.520	
0.3	0.3	0.0342	0.	0.9634	226.3	1.561	1.095	1.213	0.002	1.044	1.005	-97.1	127.2	15.2	10.496	
0.4	0.4	0.0481	0.	0.9519	226.2	1.563	1.093	1.212	0.002	1.043	1.006	-97.5	126.6	15.2	10.472	
0.5	0.5	0.0659	0.	0.9401	226.1	1.564	1.092	1.210	0.002	1.042	1.006	-97.9	126.0	15.2	10.448	
0.6	0.6	0.0832	0.	0.9288	225.9	1.567	1.089	1.208	0.002	1.040	1.006	-98.7	124.9	15.2	10.399	
0.7	0.7	0.1017	0.	0.9177	225.6	1.571	1.085	1.200	0.001	1.037	1.011	-99.6	123.2	15.1	10.320	
0.8	0.8	0.1200	0.	0.2280	0.7721	224.5	1.584	1.071	1.181	0.000	1.029	1.020	-103.5	117.9	15.1	10.190
0.9	0.9	0.1400	0.	0.4324	0.5677	223.4	1.610	1.039	1.143	0.001	1.015	1.041	-110.3	108.2	14.9	9.671
0.0	0.0	0.0624	0.	0.3764	222.4	1.635	1.084	1.104	0.004	1.005	1.069	-116.7	99.4	14.8	9.254	
0.1	0.1	0.0808	0.	0.1942	221.7	1.658	1.075	1.065	0.010	1.000	1.103	-122.5	91.0	14.7	9.031	
0.2	0.2	0.0939	0.	0.961	221.5	1.669	1.074	1.045	0.014	0.999	1.123	-125.3	86.9	14.7	8.620	
0.3	0.3	0.1749	0.	0.6251	221.6	1.760	1.098	1.216	0.023	1.072	1.034	-93.0	126.1	15.4	10.684	
0.4	0.4	0.2172	0.	0.1111	0.9161	222.6	1.570	1.097	1.214	0.022	1.070	1.035	-93.4	125.6	15.4	10.662
0.5	0.5	0.2178	0.	0.0222	0.9671	222.5	1.572	1.095	1.212	0.022	1.069	1.035	-93.6	125.1	15.4	10.639
0.6	0.6	0.1680	0.	0.0332	0.7981	222.5	1.573	1.094	1.210	0.022	1.068	1.036	-94.2	124.6	15.3	10.615
0.7	0.7	0.1666	0.	0.0441	0.7891	222.4	1.574	1.092	1.208	0.021	1.066	1.036	-94.6	124.1	15.3	10.592
0.8	0.8	0.1648	0.	0.0559	0.7802	222.4	1.576	1.091	1.206	0.021	1.065	1.037	-95.0	123.6	15.3	10.569
0.9	0.9	0.1549	0.	0.1048	0.7364	222.2	1.582	1.089	1.197	0.019	1.059	1.040	-95.6	122.6	15.3	10.523
0.10	0.10	0.1356	0.	0.2129	0.6513	221.6	1.595	1.087	1.177	0.017	1.048	1.046	-100.8	118.4	15.2	10.229
0.10	0.10	0.1000	0.	0.4117	0.4983	221.3	1.611	1.082	1.138	0.013	1.029	1.063	-108.2	107.6	15.0	9.789
0.10	0.10	0.0661	0.	0.6043	0.3294	221.0	1.641	1.085	1.100	0.012	1.014	1.084	-115.2	99.3	14.9	9.347
0.10	0.10	0.0331	0.	0.7979	0.1639	221.0	1.661	1.075	1.063	0.014	1.005	1.112	-121.7	91.1	14.7	9.088
0.10	0.10	0.167	0.	0.8974	0.0599	221.1	1.670	1.074	1.044	0.016	1.001	1.128	-124.9	87.0	14.7	8.644
0.20	0.	0.3237	0.	0.6763	219.0	1.585	1.015	1.211	0.042	1.096	1.067	-99.6	123.3	15.6	10.826	
0.20	0.01	0.3202	0.	0.0102	0.6649	219.0	1.582	1.013	1.209	0.041	1.094	1.067	-90.2	122.9	15.6	10.803
0.20	0.02	0.3167	0.	0.0204	0.6628	219.0	1.583	1.011	1.207	0.041	1.093	1.067	-90.6	122.5	15.6	10.780
0.20	0.03	0.3133	0.	0.0306	0.6562	219.0	1.585	1.010	1.205	0.040	1.091	1.068	-91.1	122.0	15.6	10.757
0.20	0.04	0.3090	0.	0.0407	0.6495	219.0	1.586	1.008	1.203	0.040	1.089	1.068	-91.5	121.6	15.5	10.735
0.20	0.05	0.3064	0.	0.0508	0.6424	219.0	1.587	1.006	1.201	0.039	1.088	1.068	-91.9	121.2	15.5	10.712
0.20	0.07	0.2995	0.	0.0709	0.6294	219.0	1.588	1.003	1.197	0.038	1.085	1.069	-92.7	120.3	15.5	10.667
0.20	0.10	0.2893	0.	0.1069	0.6098	219.0	1.593	1.000	1.191	0.036	1.081	1.070	-94.0	119.1	15.5	10.600
0.20	0.20	0.2556	0.	0.1994	0.5446	219.0	1.605	1.000	1.172	0.032	1.067	1.073	-94.1	114.9	15.4	10.573
0.20	0.40	0.1916	0.	0.3927	0.4197	219.2	1.627	1.044	1.134	0.025	1.043	1.085	-106.0	107.0	15.1	9.914
0.20	0.60	0.1287	0.	0.5802	0.2651	219.7	1.646	1.085	1.096	0.020	1.026	1.024	-113.6	99.2	14.9	9.441
0.20	0.80	0.0654	0.	0.7843	0.1483	220.4	1.664	1.075	1.061	0.019	1.010	1.120	-120.0	91.2	14.8	9.338
0.20	0.90	0.0331	0.	0.8910	0.0759	220.8	1.672	1.074	1.043	0.016	1.032	1.125	-124.5	87.1	14.7	8.672
0.40	0.	0.3612	0.	0.4388	212.4	1.602	1.016	1.198	0.076	1.146	1.139	-83.0	116.0	16.1	11.192	
0.40	0.01	0.3551	0.	0.0000	0.4352	212.5	1.603	1.017	1.196	0.077	1.144	1.139	-83.5	117.7	16.1	11.168
0.40	0.02	0.3599	0.	0.0175	0.4315	212.6	1.604	1.015	1.194	0.076	1.142	1.138	-83.9	117.4	16.1	11.144
0.40	0.03	0.3545	0.	0.0263	0.4279	212.6	1.605	1.013	1.192	0.075	1.140	1.138	-84.4	117.1	16.1	11.120
0.40	0.04	0.3547	0.	0.0351	0.4243	212.7	1.607	1.011	1.190	0.074	1.137	1.137	-84.9	116.6	16.1	11.093
0.40	0.05	0.3335	0.	0.0438	0.4206	212.8	1.608	1.010	1.188	0.073	1.135	1.137	-85.3	116.5	16.0	11.071
0.40	0.07	0.3253	0.	0.0614	0.4134	212.9	1.610	1.006	1.184	0.072	1.131	1.136	-86.3	115.9	16.0	11.022
0.40	0.10	0.2893	0.	0.1069	0.3698	213.0	1.624	1.002	1.159	0.062	1.070	1.073	-94.1	110.9	15.9	10.948
0.40	0.44	0.3537	0.	0.3588	0.2876	213.5	1.643	1.045	1.123	0.048	1.072	1.131	-101.5	105.6	15.4	10.699
0.40	0.60	0.2444	0.	0.5526	0.2030	217.1	1.658	1.058	1.089	0.037	1.044	1.133	-110.6	98.0	15.1	9.633
0.40	0.80	0.0800	0.	0.1276	0.7039	219.0	1.670	1.075	1.056	0.026	1.020	1.130	-119.4	91.3	14.8	9.541
0.40	0.90	0.0654	0.	0.8744	0.0563	220.1	1.673	1.074	1.041	0.023	1.033	1.141	-121.7	87.2	14.7	8.725
0.50	0.	0.7410	0.	0.2599	216.7	1.617	1.007	1.179	0.914	1.203	1.225	-75.0	113.0	16.7	11.670	
0.50	0.01	0.7352	0.	0.0076	0.2572	216.9	1.610	1.006	1.178	0.913	1.200	1.223	-76.3	112.8	16.7	11.641
0.50	0.02	0.7293	0.	0.0153	0.2553	217.0	1.620	1.004	1.176	0.911	1.197	1.222	-76.8	112.6	16.6	11.612
0.50	0.03	0.7235	0.	0.0230	0.2533	217.1	1.621	1.003	1.174	0.910	1.194	1.221	-77.4	112.4	16.6	11.583
0.50	0.04	0.7176	0.	0.0307	0.2516	217.2	1.622	1.001	1.172	0.909	1.191	1.220	-77.9	112.2	16.6	11.554
0.50	0.05	0.7117	0.	0.0385	0.2494	217.3	1.623	1.000	1.170	0.908	1.189	1.218	-78.4	112.0	16.6	11.525
0.50	0.07	0.6999	0.	0.0549	0.2460	217.4	1.625	1.006	1.167	0.906	1.193	1.216	-79.9	111.6	16.5	11.466
0.50	0.10	0.6621	0.	0.2776	0.2404	217.9	1.629	1.002	1.161	0.902	1.175	1.212	-81.1	110.9	16.4	11.379
0.50	0.20	0.6212	0.	0.1979	0.2268	218.0	1.630	1.001	1.160	0.901	1.174	1.212	-82.2	103.3	15.6	10.476
0.50	0.40	0.4919	0.	0.3300	0.1782	218.1	1.636	1.004	1.160	0.900	1.172	1.214	-87.7	98.4	15.3	9.834
0.50	0.60	0.1868	0.	0.7427	0											

Table 25. (cont.)

PRESSURE = 16. ATM

LIQUID MOLE FRACTION		VAPOR MOLE FRACTION		TEMP	RELATIVE VOL		PRESSURE ACT COEF			ENTHALPY BTU/LB MOLE		HEAT CAPACITY BTU/LB MOLE-R				
N2/N2+O2	AR	N2	AR	O2	R	N2/AR	N2/O2	AR/O2	N2	AR	O2	Liq	Vap	Liq	Vap	
0.0	0.0	0.0	0.0	0.000	231.5	1.530	1.840	1.263	0.785	1.037	1.002	-887.	1286.	15.8	11.188	
0.1	0.91	0.0	0.020	0.980	231.2	1.531	1.839	1.261	0.785	1.037	1.003	-891.	1286.	15.8	11.184	
0.2	0.82	0.0	0.040	0.960	231.1	1.532	1.837	1.260	0.785	1.036	1.004	-895.	1274.	15.7	11.148	
0.3	0.73	0.0	0.060	0.940	231.0	1.533	1.836	1.259	0.785	1.035	1.005	-899.	1268.	15.7	11.118	
0.4	0.64	0.0	0.075	0.935	230.9	1.534	1.834	1.258	0.785	1.034	1.006	-903.	1263.	15.7	11.091	
0.5	0.55	0.0	0.090	0.940	230.8	1.535	1.833	1.256	0.785	1.034	1.006	-907.	1257.	15.7	11.068	
0.6	0.46	0.0	0.092	0.9170	230.6	1.537	1.830	1.255	0.784	1.032	1.008	-915.	1245.	14.7	11.028	
0.7	0.37	0.0	0.092	0.8970	230.5	1.541	1.826	1.245	0.784	1.030	1.011	-926.	1228.	15.6	10.951	
0.8	0.28	0.0	0.092	0.8770	229.5	1.552	1.811	1.167	0.784	1.023	1.020	-933.	1174.	15.5	10.725	
0.9	0.19	0.0	0.092	0.8490	229.1	1.573	1.776	1.131	0.784	1.013	1.024	-933.	1076.	14.4	10.298	
1.0	0.09	0.0	0.092	0.8121	227.1	1.593	1.743	1.094	0.784	1.002	1.009	-1096.	986.	15.3	9.881	
1.1	0.00	0.0	0.092	0.7692	226.4	1.613	1.705	1.057	0.797	0.997	1.102	-1155.	902.	15.2	9.453	
1.2	0.00	0.0	0.092	0.7034	226.2	1.622	1.686	1.039	0.796	0.997	1.121	-1183.	858.	15.1	9.229	
1.3	0.00	0.0	0.0900	0.6230	227.3	1.535	1.841	1.198	0.806	1.005	1.036	-897.	1297.	15.8	11.334	
1.4	0.01	0.0	0.1479	0.5110	227.2	1.537	1.840	1.197	0.805	1.004	1.037	-862.	1252.	15.8	11.316	
1.5	0.02	0.0	0.1589	0.4220	0.8121	227.2	1.538	1.839	1.196	0.805	1.002	1.037	-866.	1247.	15.8	11.287
1.6	0.03	0.0	0.1639	0.3290	0.8032	227.1	1.539	1.837	1.194	0.805	1.001	1.038	-870.	1242.	15.8	11.224
1.7	0.04	0.0	0.1620	0.3430	0.7949	227.1	1.540	1.836	1.192	0.804	1.000	1.038	-874.	1237.	15.8	11.246
1.8	0.05	0.0	0.1600	0.3547	0.7893	227.0	1.541	1.834	1.190	0.804	1.000	1.039	-878.	1232.	15.8	11.237
1.9	0.06	0.0	0.1562	0.3742	0.7677	227.0	1.543	1.831	1.186	0.803	1.007	1.040	-886.	1222.	15.7	11.1
2.0	0.07	0.0	0.1505	0.3816	0.7414	226.8	1.547	1.826	1.181	0.802	1.005	1.042	-890.	1207.	15.7	11.0
2.1	0.08	0.0	0.1320	0.2119	0.6561	226.5	1.557	1.811	1.163	0.800	1.003	1.046	-937.	1159.	15.6	10.871
2.2	0.09	0.0	0.1292	0.1972	0.4166	225.9	1.578	1.777	1.126	0.798	1.026	1.054	-1011.	1089.	15.5	10.437
2.3	0.10	0.0	0.1263	0.1643	0.3036	225.7	1.597	1.749	1.090	0.795	1.012	1.085	-1084.	984.	15.3	9.981
2.4	0.11	0.0	0.1232	0.1797	0.1701	225.7	1.614	1.704	1.055	0.796	1.011	1.147	-901.	15.2	9.507	
2.5	0.12	0.0	0.1162	0.1973	0.0669	225.8	1.624	1.685	1.038	0.798	1.009	1.126	-1179.	859.	15.2	9.296
2.6	0.13	0.0	0.1154	0.1456	0.0382	225.6	1.542	1.843	1.195	0.800	1.002	1.071	-825.	1229.	15.0	11.569
2.7	0.14	0.0	0.1120	0.1124	0.6778	225.6	1.543	1.841	1.193	0.802	1.001	1.071	-829.	1224.	15.0	11.466
2.8	0.15	0.0	0.1050	0.3050	0.6642	225.6	1.544	1.839	1.191	0.802	1.000	1.071	-833.	1220.	15.0	11.463
2.9	0.16	0.0	0.1014	0.3017	0.5575	225.6	1.546	1.838	1.189	0.802	1.000	1.072	-836.	1216.	15.0	11.446
3.0	0.17	0.0	0.0985	0.2989	0.4507	225.6	1.547	1.837	1.187	0.802	1.000	1.072	-842.	1211.	15.0	11.417
3.1	0.18	0.0	0.0951	0.2918	0.3737	225.6	1.548	1.835	1.185	0.802	1.000	1.072	-846.	1207.	15.0	11.394
3.2	0.19	0.0	0.0920	0.2849	0.2511	225.6	1.553	1.827	1.176	0.802	1.000	1.074	-857.	1198.	15.0	11.348
3.3	0.20	0.0	0.0895	0.2745	0.1551	225.6	1.564	1.821	1.159	0.802	1.000	1.074	-867.	1185.	15.0	11.279
3.4	0.21	0.0	0.0870	0.2629	0.0426	225.9	1.584	1.776	1.120	0.800	1.001	1.077	-909.	1143.	15.7	11.048
3.5	0.22	0.0	0.0840	0.2387	0.2879	224.3	1.584	1.741	1.087	0.804	1.022	1.102	-959.	1082.	15.6	10.577
3.6	0.23	0.0	0.0810	0.2380	0.7886	224.0	1.586	1.704	1.053	0.801	1.008	1.120	-1056.	983.	15.4	10.086
3.7	0.24	0.0	0.0780	0.2322	0.5934	223.5	1.595	1.685	1.037	0.800	1.002	1.139	-902.	15.2	9.583	
3.8	0.25	0.0	0.0750	0.2297	0.3764	223.5	1.596	1.683	1.037	0.800	1.002	1.139	-1175.	868.	15.2	9.288
3.9	0.26	0.0	0.0720	0.2270	0.2493	223.6	1.597	1.680	1.037	0.802	1.002	1.171	-825.	1229.	15.0	11.569
4.0	0.27	0.0	0.0690	0.2077	0.4416	223.6	1.598	1.679	1.031	0.802	1.001	1.171	-759.	1171.	15.5	11.339
4.1	0.28	0.0	0.0660	0.2057	0.3412	223.6	1.600	1.674	1.024	0.802	1.001	1.171	-764.	1168.	15.5	11.316
4.2	0.29	0.0	0.0630	0.2034	0.2642	223.6	1.601	1.669	1.019	0.802	1.001	1.171	-769.	1165.	15.4	11.288
4.3	0.30	0.0	0.0600	0.2014	0.1834	223.6	1.602	1.664	1.014	0.802	1.001	1.171	-773.	1162.	15.4	11.262
4.4	0.31	0.0	0.0570	0.1984	0.1303	223.6	1.603	1.659	1.009	0.802	1.001	1.171	-778.	1159.	15.4	11.236
4.5	0.32	0.0	0.0540	0.1954	0.0856	223.6	1.604	1.654	1.004	0.802	1.001	1.171	-802.	1143.	15.3	11.205
4.6	0.33	0.0	0.0510	0.1924	0.0429	223.6	1.605	1.649	1.000	0.802	1.001	1.171	-849.	1112.	15.1	11.140
4.7	0.34	0.0	0.0480	0.1894	0.0153	223.6	1.606	1.644	1.000	0.802	1.001	1.171	-884.	1100.	15.1	11.040
4.8	0.35	0.0	0.0450	0.1864	0.2927	223.6	1.607	1.639	1.000	0.802	1.001	1.171	-924.	1087.	15.0	10.920
4.9	0.36	0.0	0.0420	0.1834	0.1298	223.6	1.608	1.634	1.000	0.802	1.001	1.171	-965.	1066.	15.0	10.845
5.0	0.37	0.0	0.0390	0.1804	0.0856	223.6	1.609	1.629	1.000	0.802	1.001	1.171	-1005.	1046.	15.0	10.768
5.1	0.38	0.0	0.0360	0.1774	0.0429	223.6	1.610	1.624	1.000	0.802	1.001	1.171	-1045.	1024.	15.0	10.696
5.2	0.39	0.0	0.0330	0.1744	0.1134	223.6	1.611	1.619	1.000	0.802	1.001	1.171	-1085.	1002.	15.0	10.626
5.3	0.40	0.0	0.0300	0.1714	0.0745	223.6	1.612	1.614	1.000	0.802	1.001	1.171	-1125.	982.	15.0	10.553
5.4	0.41	0.0	0.0270	0.1684	0.0374	223.6	1.613	1.609	1.000	0.802	1.001	1.171	-1165.	962.	15.0	10.471
5.5	0.42	0.0	0.0240	0.1654	0.0074	223.6	1.614	1.604	1.000	0.802	1.001	1.171	-1205.	940.	15.0	10.399
5.6	0.43	0.0	0.0210	0.1624	0.0674	223.6	1.615	1.600	1.000	0.802	1.001	1.171	-1245.	918.	15.0	10.344
5.7	0.44	0.0	0.0180	0.1594	0.0324	223.6	1.616	1.595	1.000	0.802	1.001	1.171	-1285.	897.	15.0	10.268
5.8	0.45	0.0	0.0150	0.1564	0.0084	223.6	1.617	1.590	1.000	0.802	1.001	1.171	-1325.	876.	15.0	10.190
5.9	0.46	0.0	0.0120	0.1534	0.0714	223.6	1.618	1.585	1.000	0.802	1.001	1.171	-1365.	855.	15.0	10.110
6.0	0.47	0.0	0.0090	0.1504	0.0364	223.6	1.619	1.580	1.000	0.						

Table 25. (cont.)

PRESSURE = 14. atm

LIQUID MOLE FRACTION	VAPOR MOLE FRACTION				TEMP	RELATIVE VOL	PRESSURE ACT CUBF	ENTHALPY			HEAT CAPACITY				
	N2/N2+O2	Ar	N2	O2	P	N2/Ar	N2/O2	Ar/O2	N2	Ar	O2	Liq	Vap	Liq	Vap
0+	0+	0+	1.0000	235.5	1.913	1.799	1.189	0.772	1.030	1.082	+819.	1289.	16.3	11.878	
0+	0+0.1	0+	0.9128	0.0872	235.4	1.914	1.798	1.187	0.772	1.029	1.083	-823.	1274.	16.3	11.855
0+	0+0.2	0+	0.8258	0.1744	235.1	1.915	1.798	1.185	0.772	1.028	1.083	-827.	1268.	16.3	11.831
0+	0+0.3	0+	0.7383	0.2647	235.2	1.916	1.795	1.184	0.772	1.028	1.084	-831.	1262.	16.3	11.807
0+	0+0.4	0+	0.6509	0.3531	235.1	1.917	1.793	1.182	0.772	1.027	1.085	-835.	1254.	16.3	11.784
0+	0+0.5	0+	0.5635	0.4415	235.0	1.918	1.792	1.180	0.772	1.026	1.086	-839.	1256.	16.2	11.761
0+	0+0.6	0+	0.4761	0.5298	234.9	1.919	1.791	1.177	0.772	1.025	1.088	-847.	1238.	16.2	11.715
0+	0+0.7	0+	0.3884	0.6186	234.8	1.920	1.790	1.175	0.772	1.023	1.091	-856.	1223.	16.2	11.646
0+	0+0.8	0+	0.3010	0.7068	234.6	1.922	1.784	1.172	0.772	1.021	1.094	-866.	1187.	16.1	11.429
0+	0+0.9	0+	0.2136	0.7950	234.4	1.924	1.779	1.167	0.771	1.017	1.098	-866.	1067.	15.9	11.001
0+	0+1.0	0+	0.1262	0.8832	234.2	1.926	1.774	1.162	0.771	1.007	1.098	-866.	975.	15.7	10.981
0+	0+1.1	0+	0.0389	0.9714	234.0	1.928	1.768	1.158	0.770	1.001	1.099	-871.	886.	15.7	10.143
0+	0+1.2	0+	0.0000	0.9971	233.5	1.930	1.763	1.154	0.768	0.995	1.119	-877.	845.	15.6	9.912
0+1.0	0+	0+1.0000	0+	0.9334	231.5	1.913	1.793	1.189	0.793	1.059	1.038	-770.	1256.	16.2	12.067
0+1.0	0+0.91	0+1.0000	0+0.1100	0.8249	231.4	1.914	1.791	1.183	0.793	1.058	1.039	-794.	1244.	16.2	12.044
0+1.0	0+0.82	0+1.0000	0+0.2190	0.8159	231.4	1.915	1.790	1.182	0.792	1.057	1.039	-798.	1239.	16.2	12.021
0+1.0	0+0.93	0+1.0000	0+0.3272	0.8070	231.3	1.916	1.788	1.180	0.792	1.056	1.040	-802.	1234.	16.2	11.998
0+1.0	0+0.84	0+1.0000	0+0.4352	0.7985	231.3	1.917	1.787	1.178	0.792	1.055	1.040	-807.	1229.	16.2	11.975
0+1.0	0+0.95	0+1.0000	0+0.5433	0.7892	231.2	1.918	1.785	1.178	0.791	1.054	1.041	-811.	1224.	16.2	11.952
0+1.0	0+0.87	0+1.0000	0+0.6513	0.7795	231.2	1.919	1.783	1.173	0.791	1.052	1.042	-819.	1214.	16.2	11.906
0+1.0	0+0.88	0+1.0000	0+0.7692	0.7695	231.2	1.920	1.782	1.168	0.790	1.049	1.044	-831.	1199.	16.1	11.838
0+1.0	0+0.89	0+1.0000	0+0.8791	0.7597	231.2	1.921	1.780	1.167	0.789	1.048	1.044	-836.	1186.	16.1	11.812
0+1.0	0+0.90	0+1.0000	0+0.9872	0.7497	231.1	1.922	1.779	1.162	0.788	1.046	1.045	-837.	1156.	16.1	11.792
0+1.0	0+0.91	0+1.0000	0+1.0952	0.7395	231.2	1.923	1.776	1.156	0.784	1.043	1.046	-845.	1056.	15.9	11.192
0+1.0	0+0.92	0+1.0000	0+0.1050	0.8288	230.9	1.924	1.774	1.157	0.782	1.042	1.046	-846.	1057.	15.8	10.988
0+1.0	0+0.93	0+1.0000	0+0.2135	0.7974	230.8	1.925	1.773	1.156	0.783	1.041	1.046	-851.	973.	15.8	10.969
0+1.0	0+0.94	0+1.0000	0+0.3215	0.7794	230.8	1.926	1.772	1.155	0.784	1.040	1.046	-856.	889.	15.7	10.265
0+1.0	0+0.95	0+1.0000	0+0.4299	0.7597	230.8	1.927	1.771	1.154	0.785	1.039	1.046	-861.	846.	15.6	9.944
0+1.0	0+0.96	0+1.0000	0+0.5389	0.7399	230.8	1.928	1.770	1.153	0.786	1.038	1.045	-867.	1221.	16.3	12.268
0+1.0	0+0.97	0+1.0000	0+0.6462	0.7202	230.8	1.929	1.769	1.152	0.787	1.037	1.045	-870.	1216.	16.3	12.245
0+1.0	0+0.98	0+1.0000	0+0.7549	0.7004	230.8	1.930	1.768	1.151	0.788	1.036	1.044	-874.	1203.	16.3	12.219
0+1.0	0+0.99	0+1.0000	0+0.8637	0.6807	230.8	1.931	1.767	1.150	0.789	1.035	1.043	-877.	1198.	16.3	12.172
0+1.0	0+1.00	0+1.0000	0+0.9725	0.6597	230.8	1.932	1.766	1.149	0.790	1.034	1.042	-880.	1177.	16.2	12.055
0+1.0	0+1.01	0+1.0000	0+0.1082	0.7494	230.8	1.933	1.765	1.148	0.791	1.033	1.041	-884.	1134.	16.1	11.820
0+1.0	0+1.02	0+1.0000	0+0.2168	0.7292	230.8	1.934	1.764	1.147	0.792	1.032	1.041	-887.	1052.	15.9	11.332
0+1.0	0+1.03	0+1.0000	0+0.3254	0.7093	230.8	1.935	1.763	1.146	0.793	1.031	1.040	-890.	971.	15.8	10.816
0+1.0	0+1.04	0+1.0000	0+0.4341	0.6893	230.8	1.936	1.762	1.145	0.794	1.030	1.040	-893.	889.	15.7	10.266
0+1.0	0+1.05	0+1.0000	0+0.5426	0.6691	230.8	1.937	1.761	1.144	0.795	1.029	1.039	-897.	846.	15.6	9.976
0+1.0	0+1.06	0+1.0000	0+0.6519	0.6489	230.8	1.938	1.760	1.143	0.796	1.028	1.038	-905.	1165.	16.8	12.592
0+1.0	0+1.07	0+1.0000	0+0.7610	0.6287	230.8	1.939	1.759	1.142	0.797	1.027	1.038	-910.	1162.	16.8	12.534
0+1.0	0+1.08	0+1.0000	0+0.8695	0.6085	230.8	1.940	1.758	1.141	0.798	1.026	1.038	-914.	1158.	16.8	12.487
0+1.0	0+1.09	0+1.0000	0+0.9782	0.5883	230.8	1.941	1.757	1.140	0.799	1.025	1.038	-918.	1155.	16.7	12.429
0+1.0	0+1.10	0+1.0000	0+0.1069	0.5681	230.8	1.942	1.756	1.139	0.800	1.024	1.038	-922.	1152.	16.7	12.379
0+1.0	0+1.11	0+1.0000	0+0.2156	0.5479	230.8	1.943	1.755	1.138	0.801	1.023	1.038	-926.	1150.	16.7	12.337
0+1.0	0+1.12	0+1.0000	0+0.3243	0.5276	230.8	1.944	1.754	1.137	0.802	1.022	1.038	-930.	1148.	16.7	12.295
0+1.0	0+1.13	0+1.0000	0+0.4330	0.5073	230.8	1.945	1.753	1.136	0.803	1.021	1.038	-934.	1146.	16.7	12.255
0+1.0	0+1.14	0+1.0000	0+0.5417	0.4870	230.8	1.946	1.752	1.135	0.804	1.020	1.038	-938.	1144.	16.7	12.215
0+1.0	0+1.15	0+1.0000	0+0.6504	0.4667	230.8	1.947	1.751	1.134	0.805	1.019	1.038	-942.	1142.	16.7	12.173
0+1.0	0+1.16	0+1.0000	0+0.7591	0.4464	230.8	1.948	1.750	1.133	0.806	1.018	1.038	-946.	1140.	16.7	12.133
0+1.0	0+1.17	0+1.0000	0+0.8678	0.4262	230.8	1.949	1.749	1.132	0.807	1.017	1.038	-950.	1138.	16.7	12.091
0+1.0	0+1.18	0+1.0000	0+0.9765	0.4059	230.8	1.950	1.748	1.131	0.808	1.016	1.038	-954.	1136.	16.7	12.049
0+1.0	0+1.19	0+1.0000	0+0.1056	0.3856	230.8	1.951	1.747	1.130	0.809	1.015	1.038	-958.	1134.	16.7	12.007
0+1.0	0+1.20	0+1.0000	0+0.2143	0.3654	230.8	1.952	1.746	1.129	0.810	1.014	1.038	-962.	1132.	16.7	11.965
0+1.0	0+1.21	0+1.0000	0+0.3230	0.3452	230.8	1.953	1.745	1.128	0.811	1.013	1.038	-966.	1130.	16.7	11.923
0+1.0	0+1.22	0+1.0000	0+0.4317	0.3249	230.8	1.954	1.744	1.127	0.812	1.012	1.038	-970.	1128.	16.7	11.881
0+1.0	0+1.23	0+1.0000	0+0.5404	0.3046	230.8	1.955	1.743	1.126	0.813	1.011	1.038	-974.	1126.	16.7	11.839
0+1.0	0+1.24	0+1.0000	0+0.6491	0.2843	230.8	1.956	1.742	1.125	0.814	1.010	1.038	-978.	1124.	16.7	11.797
0+1.0	0+1.25	0+1.0000	0+0.7578	0.2641	230.8	1.957	1.741	1.124	0.815	1.009	1.038	-982.	1122.	16.7	11.755
0+1.0	0+1.26	0+1.0000	0+0.8665	0.2438	230.8	1.958	1.740	1.123	0.816	1.008	1.038	-986.	1120.	16.7	11.713
0+1.0	0+1.27	0+1.0000	0+0.9752	0.2235	230.8	1.959	1.739	1.122	0.817	1.007	1.038	-990.	1118.	16.7	11.671
0+1.															

Table 25. (cont.)

PRESSURE = 21. ATM

LIQUID MOLE FRACTION	VAPOR MOLE FRACTION		TEMP	RELATIVE VOL	PRESSURE	AUT COEF	ENTHALPY BTU/LB MOLE	HEAT CAPACITY BTU/LB MOLE-R								
	N2/N2+O2	AR	N2	O2	R	N2/O2	AR/O2	N2	AR	O2	Liq	Vap	Liq	Vap		
0.0	0.0	0.0	0.0	1.0000	234.9	1.907	1.774	1.178	0.764	1.023	1.001	-793.	1271.	16.9	12.659	
0.0	0.01	0.0	0.0117	0.9883	239.4	1.907	1.773	1.176	0.764	1.023	1.002	-757.	1269.	16.9	12.636	
0.0	0.02	0.0	0.0234	0.9784	239.3	1.908	1.771	1.174	0.764	1.022	1.003	-72.	1258.	16.9	12.613	
0.0	0.03	0.0	0.0350	0.9686	239.2	1.909	1.769	1.173	0.764	1.022	1.004	-70.	1252.	16.9	12.591	
0.0	0.04	0.0	0.0465	0.9583	239.1	1.909	1.767	1.171	0.764	1.021	1.005	-77.	1246.	16.8	12.568	
0.0	0.05	0.0	0.0580	0.9482	239.0	1.910	1.766	1.170	0.764	1.020	1.006	-77.	1241.	16.8	12.546	
0.0	0.07	0.0	0.0807	0.9193	238.8	1.911	1.762	1.166	0.764	1.019	1.008	-78.	1229.	16.8	12.501	
0.0	0.10	0.0	0.1143	0.8687	238.6	1.913	1.757	1.161	0.763	1.018	1.011	-79.	1211.	16.7	12.435	
0.0	0.14	0.0	0.1722	0.7779	237.7	1.914	1.739	1.145	0.763	1.013	1.021	-83.	1156.	16.6	12.220	
0.0	0.24	0.0	0.2425	0.5743	233.3	1.932	1.704	1.112	0.762	1.004	1.043	-93.	1055.	16.4	11.802	
0.0	0.81	0.0	0.6181	0.3818	235.3	1.946	1.688	1.079	0.764	0.997	1.059	-98.	982.	16.2	11.378	
0.0	0.91	0.0	0.8761	0.1929	234.6	1.950	1.631	1.046	0.769	0.994	1.100	-102.	874.	16.1	10.930	
0.10	0.0	0.0	0.0	0.9026	0.974	234.4	1.947	1.633	1.029	0.770	0.994	1.110	-104.	83.	16.1	10.691
0.10	0.01	0.0	0.0116	0.919	0.9274	235.3	1.949	1.759	1.173	0.764	1.035	1.041	-77.	1239.	16.7	12.93
0.10	0.02	0.0	0.0197	0.9217	0.8186	235.2	1.951	1.766	1.171	0.764	1.034	1.041	-73.	1233.	16.7	12.89
0.10	0.03	0.0	0.0378	0.9325	0.8097	235.2	1.952	1.784	1.170	0.764	1.033	1.042	-73.	1228.	16.7	12.84
0.10	0.04	0.0	0.0386	0.9432	0.8086	235.1	1.953	1.763	1.165	0.763	1.031	1.043	-74.	1216.	16.7	12.844
0.10	0.05	0.0	0.0374	0.9539	0.7929	235.1	1.953	1.751	1.165	0.763	1.030	1.043	-74.	1213.	16.8	12.798
0.10	0.07	0.0	0.0594	0.9752	0.7744	235.0	1.956	1.748	1.161	0.762	1.048	1.045	-78.	1202.	16.8	12.753
0.10	0.10	0.0	0.1449	0.1948	0.7469	234.9	1.957	1.743	1.157	0.761	1.046	1.046	-78.	1157.	16.8	12.684
0.10	0.12	0.0	0.2172	0.2994	0.6862	234.5	1.958	1.728	1.149	0.760	1.037	1.053	-80.	1139.	16.5	12.450
0.10	0.14	0.0	0.2938	0.4884	0.4978	234.1	1.951	1.695	1.188	0.755	1.021	1.066	-82.	1047.	16.3	11.999
0.10	0.18	0.0	0.6249	0.6302	0.3359	233.9	1.946	1.662	1.075	0.755	1.009	1.083	-95.	959.	16.2	11.519
0.10	0.21	0.0	0.1511	0.7971	0.1718	233.9	1.945	1.628	1.044	0.773	1.006	1.110	-103.	874.	16.1	11.003
0.10	0.24	0.0	0.159	0.8971	0.0473	234.1	1.947	1.611	1.028	0.774	0.997	1.120	-106.	83.	16.1	10.728
0.20	0.0	0.0	0.0446	0.0460	0.2116	231.6	1.946	1.747	1.168	0.764	1.086	1.080	-95.	1209.	16.7	13.200
0.20	0.01	0.0	0.0567	0.0603	0.0891	231.6	1.947	1.745	1.168	0.763	1.089	1.080	-99.	1244.	16.7	13.176
0.20	0.02	0.0	0.0795	0.0626	0.0893	231.6	1.948	1.744	1.165	0.763	1.084	1.080	-70.	1200.	16.7	13.153
0.20	0.03	0.0	0.2942	0.0308	0.06794	231.6	1.949	1.743	1.163	0.762	1.082	1.081	-70.	1195.	16.7	13.129
0.20	0.04	0.0	0.2912	0.0308	0.06686	231.6	1.949	1.741	1.161	0.762	1.081	1.081	-72.	1191.	16.7	13.105
0.20	0.05	0.0	0.2877	0.0305	0.06617	231.6	1.950	1.740	1.160	0.761	1.079	1.081	-71.	1186.	16.7	13.081
0.20	0.07	0.0	0.2814	0.0305	0.06441	231.6	1.950	1.737	1.159	0.760	1.077	1.082	-72.	1177.	16.8	13.033
0.20	0.10	0.0	0.2719	0.0304	0.06277	231.6	1.956	1.735	1.151	0.759	1.075	1.082	-73.	1164.	16.8	13.028
0.20	0.20	0.0	0.2410	0.1998	0.5656	231.6	1.954	1.718	1.135	0.754	1.051	1.085	-77.	1121.	16.9	12.718
0.20	0.20	0.0	0.1810	0.3926	0.24773	231.6	1.953	1.688	1.103	0.753	1.039	1.094	-86.	1038.	16.4	12.207
0.20	0.20	0.0	0.1211	0.5876	0.22921	232.5	1.956	1.657	1.072	0.782	1.021	1.105	-93.	958.	16.2	11.664
0.20	0.20	0.0	0.0311	0.7971	0.1718	231.7	1.957	1.612	1.044	0.776	1.008	1.120	-101.	873.	16.1	11.577
0.20	0.24	0.0	0.0346	0.0451	0.2116	231.6	1.946	1.725	1.155	0.763	1.149	1.154	-82.	1151.	17.1	13.932
0.20	0.40	0.0	0.0299	0.0450	0.2151	235.1	1.945	1.724	1.153	0.762	1.140	1.153	-82.	1148.	17.1	13.902
0.20	0.42	0.0	0.0249	0.0451	0.2179	235.1	1.946	1.722	1.152	0.761	1.141	1.152	-83.	1144.	17.1	13.872
0.20	0.45	0.0	0.0219	0.0452	0.2193	235.2	1.947	1.721	1.150	0.760	1.142	1.152	-83.	1141.	17.0	13.842
0.20	0.48	0.0	0.0219	0.0454	0.2195	235.2	1.948	1.720	1.149	0.760	1.142	1.152	-84.	1138.	17.0	13.811
0.20	0.50	0.0	0.0217	0.0452	0.2195	235.2	1.949	1.719	1.147	0.759	1.143	1.151	-84.	1135.	17.0	13.781
0.20	0.57	0.0	0.0204	0.0452	0.2197	235.2	1.950	1.715	1.147	0.758	1.143	1.151	-85.	1132.	17.0	13.751
0.20	0.60	0.0	0.0199	0.0456	0.2197	235.2	1.950	1.713	1.146	0.757	1.142	1.150	-86.	1128.	17.0	13.720
0.20	0.61	0.0	0.0199	0.0456	0.2198	235.2	1.950	1.712	1.145	0.756	1.142	1.149	-87.	1126.	17.0	13.628
0.20	0.62	0.0	0.0199	0.0456	0.2198	235.2	1.950	1.711	1.145	0.756	1.141	1.148	-87.	1124.	17.0	13.515
0.20	0.63	0.0	0.0199	0.0457	0.2198	235.2	1.950	1.710	1.145	0.755	1.141	1.147	-88.	1123.	17.0	13.486
0.20	0.65	0.0	0.0199	0.0457	0.2198	235.2	1.950	1.709	1.145	0.755	1.140	1.146	-89.	1121.	17.0	13.466
0.20	0.67	0.0	0.0199	0.0457	0.2198	235.2	1.950	1.708	1.145	0.754	1.139	1.145	-90.	1119.	17.0	13.446
0.20	0.70	0.0	0.0199	0.0458	0.2198	235.2	1.950	1.707	1.145	0.753	1.138	1.144	-91.	1117.	17.0	13.426
0.20	0.72	0.0	0.0199	0.0458	0.2198	235.2	1.950	1.706	1.145	0.752	1.137	1.143	-92.	1115.	17.0	13.406
0.20	0.75	0.0	0.0199	0.0458	0.2198	235.2	1.950	1.705	1.145	0.751	1.136	1.142	-93.	1113.	17.0	13.386
0.20	0.78	0.0	0.0199	0.0458	0.2198	235.2	1.950	1.704	1.145	0.750	1.135	1.141	-94.	1111.	17.0	13.366
0.20	0.80	0.0	0.0199	0.0458	0.2198	235.2	1.950	1.703	1.145	0.749	1.134	1.140	-95.	1109.	17.0	13.346
0.20	0.82	0.0	0.0199	0.0458	0.2198	235.2	1.950	1.702	1.145	0.748	1.133	1.139	-96.	1107.	17.0	13.326
0.20	0.85	0.0	0.0199	0.0458	0.2198	235.2	1.950	1.701	1.145	0.747	1.132	1.138	-97.	1105.	17.0	13.295
0.20	0.88	0.0	0.0199	0.0458	0.2198	235.2	1.950	1.700	1.145	0.746	1.131	1.137	-98.	1103.	17.0	13.273
0.20	0.90	0.0	0.0199	0.0458	0.2198	235.2	1.950	1.699	1.145	0.745	1.130	1.136	-99.	1101.	17.0	13.253
0.20	0.92	0.0	0.0199	0.0458	0.2198	235.2	1.950	1.698	1.145	0.744	1.129					

Table 25. (cont.)

PRESSURE = 21. ATM

MOLE FRACTION N2/N2+O2	LIQUID		VAPOR		TEMP	RELATIVE VOL	PRESSURE ACT COEF	ENTHALPY BTU/LB MOLE	HEAT CAPACITY BTU/LB MOLE-R						
	AR	N2	AR	O2					N2	AR	O2	Liq	Vap	Liq	Vap
0.0	0.0	0.0	0.0	1.000	244.9	1.512	1.780	1.364	0.758	1.018	1.000	-659.	1252.	17.8	14.058
0.01	0.01	0.0	0.0116	0.9984	244.9	1.523	1.788	1.162	0.758	1.019	1.001	-664.	1246.	17.8	14.037
0.02	0.02	0.0	0.0231	0.9769	244.7	1.523	1.788	1.161	0.758	1.019	1.002	-668.	1240.	17.8	14.016
0.03	0.03	0.0	0.0346	0.9654	244.6	1.523	1.788	1.159	0.758	1.014	1.003	-672.	1233.	17.8	13.996
0.04	0.04	0.0	0.0460	0.9540	244.5	1.523	1.782	1.158	0.758	1.014	1.004	-676.	1227.	17.7	13.975
0.05	0.05	0.0	0.0574	0.9424	244.4	1.523	1.782	1.156	0.758	1.014	1.005	-680.	1221.	17.7	13.955
0.07	0.07	0.0	0.0799	0.9201	244.2	1.524	1.746	1.154	0.758	1.013	1.008	-689.	1209.	17.7	13.934
0.10	0.10	0.0	0.1132	0.8868	243.9	1.519	1.740	1.149	0.757	1.008	1.011	-701.	1192.	17.6	13.853
0.12	0.12	0.0	0.1226	0.7793	243.1	1.518	1.720	1.133	0.757	1.008	1.021	-740.	1136.	17.4	13.653
0.14	0.14	0.0	0.1236	0.5764	241.7	1.523	1.682	1.102	0.756	1.003	1.044	-813.	1032.	17.2	13.292
0.16	0.16	0.0	0.1614	0.3836	240.7	1.523	1.644	1.071	0.757	0.998	1.070	-878.	937.	17.0	12.650
0.18	0.18	0.0	0.1642	0.1938	240.2	1.524	1.545	1.050	1.040	0.761	0.999	-938.	847.	16.8	12.364
0.20	0.20	0.0	0.1512	0.0738	239.8	1.523	1.589	1.025	0.763	0.993	1.017	-965.	802.	16.8	12.199
0.10	0.01	0.1594	0.0108	0.0294	240.4	1.494	1.728	1.157	0.778	1.052	1.046	-839.	1216.	17.4	14.482
0.10	0.02	0.1575	0.0215	0.6219	240.4	1.495	1.727	1.152	0.778	1.052	1.048	-844.	1210.	17.4	14.459
0.10	0.03	0.1557	0.0329	0.6122	240.3	1.495	1.725	1.154	0.778	1.051	1.047	-848.	1205.	17.4	14.441
0.10	0.04	0.1539	0.0429	0.6134	240.3	1.498	1.724	1.152	0.777	1.049	1.048	-856.	1199.	17.3	14.395
0.10	0.05	0.1521	0.0535	0.7046	240.2	1.496	1.722	1.151	0.777	1.048	1.048	-860.	1190.	17.3	14.372
0.10	0.07	0.1484	0.0746	0.2771	240.2	1.498	1.719	1.148	0.778	1.046	1.050	-868.	1179.	17.3	14.326
0.10	0.10	0.1431	0.1060	0.7510	240.1	1.499	1.714	1.143	0.779	1.044	1.051	-880.	1164.	17.3	14.257
0.10	0.20	0.1296	0.2086	0.6555	239.7	1.505	1.698	1.128	0.773	1.030	1.058	-720.	1115.	17.2	14.027
0.10	0.40	0.1049	0.4049	0.5005	239.3	1.518	1.666	1.097	0.768	1.021	1.072	-795.	1022.	17.0	13.549
0.10	0.60	0.0613	0.6009	0.3378	239.1	1.531	1.634	1.057	0.768	1.010	1.090	-865.	933.	16.8	13.034
0.10	0.90	0.0137	0.7966	0.1727	239.3	1.543	1.602	1.038	0.765	1.001	1.111	-731.	846.	16.8	12.467
0.20	0.	0.2991	0.	0.7009	237.4	1.500	1.586	1.023	0.766	0.997	1.122	-902.	802.	16.8	12.166
0.20	0.01	0.2959	0.0101	0.0493	236.6	1.481	1.707	1.153	0.798	1.087	1.089	-610.	1163.	17.3	14.935
0.20	0.02	0.2928	0.0201	0.6871	236.6	1.483	1.708	1.151	0.799	1.085	1.090	-814.	1176.	17.2	14.910
0.20	0.03	0.2896	0.0302	0.6809	236.6	1.483	1.704	1.150	0.797	1.084	1.090	-818.	1174.	17.2	14.885
0.20	0.04	0.2864	0.0402	0.6733	236.6	1.483	1.703	1.148	0.796	1.082	1.090	-822.	1169.	17.2	14.860
0.20	0.05	0.2833	0.0502	0.6665	236.6	1.485	1.700	1.145	0.795	1.081	1.092	-827.	1165.	17.2	14.835
0.20	0.07	0.2777	0.0761	0.5528	236.6	1.487	1.698	1.131	0.777	1.048	1.048	-631.	1160.	17.2	14.699
0.20	0.10	0.2677	0.0991	0.3634	236.6	1.489	1.693	1.127	0.778	1.047	1.050	-840.	1151.	17.2	14.758
0.20	0.20	0.2372	0.1941	0.5644	236.7	1.493	1.689	1.122	0.788	1.062	1.094	-652.	1138.	17.2	14.661
0.20	0.40	0.1770	0.3919	0.4304	237.1	1.512	1.652	1.092	0.781	1.041	1.101	-694.	1095.	17.1	14.421
0.20	0.60	0.1194	0.5065	0.2941	237.1	1.517	1.624	1.064	0.778	1.023	1.110	-775.	1011.	17.0	13.855
0.20	0.80	0.0807	0.7873	0.1520	237.0	1.516	1.595	1.036	0.779	1.020	1.121	-821.	919.	16.8	13.241
0.20	0.91	0.0137	0.8918	0.0775	237.1	1.514	1.564	1.022	0.780	1.027	1.121	-790.	845.	16.8	12.572
0.40	0.	0.3268	0.	0.4732	239.9	1.466	1.670	1.139	0.837	1.153	1.160	-958.	802.	16.7	12.212
0.40	0.01	0.3219	0.0090	0.4691	239.8	1.467	1.669	1.137	0.836	1.153	1.160	-836.	1121.	17.5	14.932
0.40	0.02	0.3171	0.0116	0.4650	239.8	1.468	1.668	1.136	0.835	1.151	1.169	-841.	1118.	17.5	14.916
0.40	0.03	0.3122	0.0278	0.6871	239.8	1.469	1.667	1.135	0.835	1.151	1.170	-846.	1114.	17.5	14.890
0.40	0.04	0.3073	0.0359	0.4568	239.8	1.469	1.666	1.134	0.834	1.147	1.178	-851.	1111.	17.4	14.864
0.40	0.05	0.3024	0.0450	0.4567	239.8	1.470	1.665	1.132	0.833	1.145	1.177	-856.	1108.	17.4	14.838
0.40	0.07	0.2960	0.0629	0.4444	239.8	1.473	1.663	1.129	0.831	1.141	1.177	-861.	1105.	17.4	14.812
0.40	0.10	0.2780	0.0889	0.4320	239.8	1.476	1.662	1.124	0.831	1.141	1.178	-871.	1098.	17.	15.799
0.40	0.20	0.2291	0.1815	0.3944	239.8	1.478	1.661	1.120	0.829	1.139	1.174	-886.	1088.	17.3	15.688
0.40	0.40	0.1241	0.3637	0.3042	239.8	1.486	1.659	1.119	0.820	1.116	1.188	-634.	1056.	17.2	15.309
0.40	0.60	0.0904	0.2224	0.5064	239.8	1.489	1.658	1.107	0.805	1.092	1.158	-729.	989.	17.0	14.912
0.40	0.80	0.0184	0.1184	0.7697	237.1	1.519	1.598	1.039	0.779	1.021	1.142	-821.	919.	16.8	13.868
0.40	0.90	0.0160	0.8894	0.0721	237.6	1.516	1.548	1.020	0.777	1.027	1.148	-938.	843.	16.8	12.776
0.50	0.	0.3171	0.	0.2494	240.0	1.457	1.637	1.125	0.833	1.125	1.165	-951.	802.	16.7	12.314
0.50	0.01	0.7047	0.0071	0.4272	244.1	1.458	1.636	1.122	0.865	1.232	1.265	-458.	1059.	18.0	17.682
0.50	0.02	0.6988	0.0143	0.2849	244.3	1.459	1.635	1.120	0.878	1.229	1.284	-463.	1057.	18.0	17.620
0.50	0.03	0.6929	0.0245	0.2826	244.4	1.461	1.634	1.119	0.877	1.223	1.282	-468.	1055.	18.0	17.599
0.50	0.04	0.6870	0.0326	0.2833	244.5	1.462	1.634	1.118	0.876	1.224	1.281	-474.	1053.	17.9	17.497
0.50	0.05	0.6821	0.0358	0.2791	244.6	1.463	1.633	1.116	0.876	1.221	1.278	-480.	1051.	17.9	17.437
0.50	0.07	0.6762	0.0573	0.2735	244.9	1.465	1.631	1.114	0.877	1.221	1.273	-497.	1044.	17.9	17.251
0.50	0.10	0.7092	0.0749	0.1259	242.1	1.474	1.595	1.082	0.869	1.262	1.268	-514.	1038.	17.8	17.063
0.50	0.20	0.3202	0.5372	0.1364	242.3	1.499	1.586	1.060	0.860	1.187	1.289	-970.	1015.	17.6	16.458
0.50	0.40	0.1603	0.3202	0.5372	242.4	1.516	1.586	1.051	0.832	1.123	1.221	-866.	966.	17.2	15.277
0.50	0.60	0.0181	0.8665	0.0509	242.4	1.516	1.555	1.024	0.835	1.127	1.237	-755.	897.	17.1	14.629
0.50	0.80	0.0182	0.8666	0.0536	242.7	1.516	1.545	1.018	0.832						

Table 25. (cont.)
 PRESSURE = 26. ATM

LIQUID MOLE FRACTION	VAPOR MOLE FRACTION			TEMP	RELATIVE VOL	PRESSURE ACT COEF	ENTHALPY BTU/LB MOLE			HEAT CAPACITY BTU/LB MOLE-E	
	N2/AR	AR	O2				N2	AR	O2	Liq	Vap
0.10	0.	1.186	0.	0.4305	245.0	1.501	1.722	1.147	0.780	1.053	1.053
0.10	0.01	0.158	0.0107	0.8307	244.9	1.501	1.720	1.146	0.780	1.052	1.053
0.10	0.02	0.156	0.0213	0.4218	244.9	1.502	1.718	1.144	0.780	1.052	1.054
0.10	0.03	0.151	0.0319	0.1513	244.9	1.502	1.717	1.143	0.779	1.051	1.054
0.10	0.04	0.153	0.0425	0.0443	244.8	1.502	1.715	1.141	0.779	1.051	1.055
0.10	0.05	0.151	0.0530	0.0596	244.8	1.503	1.713	1.140	0.779	1.050	1.055
0.10	0.07	0.1478	0.0740	0.7792	244.7	1.504	1.710	1.137	0.778	1.048	1.057
0.10	0.10	0.1425	0.1032	0.7523	244.6	1.505	1.705	1.133	0.777	1.045	1.058
0.10	0.21	0.1252	0.2073	0.6674	244.3	1.510	1.688	1.118	0.774	1.038	1.044
0.10	0.40	0.1924	0.4054	0.5622	243.9	1.520	1.656	1.090	0.769	1.024	1.078
0.10	0.60	0.1612	0.5696	0.3399	243.8	1.530	1.625	1.062	0.766	1.013	1.095
0.10	0.80	0.1337	0.7391	0.1732	244.0	1.542	1.598	1.034	0.765	1.004	1.113
0.10	0.90	0.154	0.8957	0.4780	244.2	1.544	1.581	1.021	0.765	1.000	1.121
0.20	0.	1.2965	0.	0.735	240.9	1.478	1.686	1.140	0.800	1.092	1.092
0.20	0.01	0.2924	0.0107	0.0566	240.9	1.479	1.685	1.139	0.799	1.091	1.092
0.20	0.02	0.2903	0.0209	0.0897	240.9	1.480	1.683	1.138	0.799	1.089	1.093
0.20	0.03	0.2872	0.0300	0.0824	240.9	1.481	1.682	1.136	0.798	1.087	1.093
0.20	0.04	0.2841	0.0399	0.0760	240.9	1.481	1.681	1.135	0.798	1.087	1.092
0.20	0.05	0.2801	0.0499	0.0691	240.9	1.482	1.680	1.133	0.797	1.086	1.092
0.20	0.07	0.2748	0.0597	0.0555	241.0	1.484	1.677	1.130	0.796	1.083	1.093
0.20	0.10	0.2656	0.0993	0.0370	241.1	1.486	1.673	1.126	0.795	1.080	1.093
0.20	0.20	0.2355	0.1972	0.5674	241.1	1.493	1.660	1.112	0.790	1.060	1.065
0.20	0.40	0.1768	0.3908	0.3234	241.6	1.508	1.635	1.085	0.762	1.047	1.118
0.20	0.60	0.1189	0.5697	0.2955	242.3	1.523	1.611	1.058	0.775	1.028	1.117
0.20	0.80	0.105	0.7476	0.1925	243.2	1.539	1.584	1.032	0.769	1.011	1.125
0.20	0.90	0.136	0.8910	0.0777	243.8	1.547	1.577	1.020	0.767	1.003	1.129
0.40	0.	0.5211	0.	0.4780	234.1	1.450	1.632	1.126	0.830	1.168	1.201
0.40	0.01	0.5163	0.0090	0.0747	234.2	1.451	1.632	1.124	0.838	1.166	1.201
0.40	0.02	0.5117	0.0150	0.0785	234.2	1.452	1.631	1.123	0.837	1.163	1.200
0.40	0.03	0.5067	0.0270	0.0663	234.3	1.453	1.630	1.122	0.836	1.161	1.199
0.40	0.04	0.5014	0.0380	0.0621	234.4	1.454	1.629	1.120	0.835	1.159	1.198
0.40	0.05	0.4971	0.0449	0.0570	234.4	1.455	1.628	1.119	0.835	1.157	1.197
0.40	0.07	0.4975	0.0630	0.0495	234.6	1.457	1.627	1.116	0.833	1.153	1.196
0.40	0.10	0.4731	0.0949	0.0369	234.8	1.460	1.624	1.112	0.830	1.147	1.194
0.40	0.20	0.4255	0.1806	0.3044	235.6	1.470	1.616	1.099	0.822	1.127	1.186
0.40	0.40	0.3773	0.3046	0.3067	237.4	1.491	1.601	1.074	0.806	1.091	1.173
0.40	0.60	0.2259	0.5616	0.2134	238.1	1.511	1.587	1.050	0.792	1.058	1.161
0.40	0.80	0.1179	0.7668	0.1123	241.7	1.532	1.557	1.028	0.779	1.028	1.140
0.40	0.90	0.1605	0.8618	0.0976	243.1	1.543	1.570	1.017	0.772	1.011	1.142
0.60	0.	0.7453	0.	0.7657	228.1	1.431	1.588	1.110	0.835	1.252	1.316
0.60	0.01	0.6987	0.0082	0.2931	228.3	1.432	1.588	1.108	0.882	1.249	1.313
0.60	0.02	0.6926	0.0184	0.4999	228.4	1.433	1.587	1.107	0.881	1.248	1.311
0.60	0.03	0.6866	0.0247	0.2446	228.5	1.435	1.587	1.106	0.880	1.243	1.309
0.60	0.04	0.6819	0.0329	0.2462	228.6	1.436	1.586	1.105	0.878	1.239	1.307
0.60	0.05	0.6750	0.0412	0.2438	228.6	1.437	1.585	1.104	0.877	1.236	1.305
0.60	0.07	0.6632	0.0578	0.2797	229.0	1.439	1.585	1.101	0.874	1.230	1.301
0.60	0.10	0.6545	0.0820	0.2717	229.4	1.443	1.584	1.097	0.870	1.221	1.295
0.60	0.20	0.5853	0.1676	0.2471	230.7	1.455	1.579	1.089	0.857	1.192	1.276
0.60	0.40	0.4993	0.3455	0.1850	233.0	1.478	1.571	1.083	0.833	1.137	1.240
0.60	0.60	0.3235	0.5347	0.1779	234.7	1.501	1.565	1.082	0.810	1.088	1.216
0.60	0.80	0.1726	0.7536	0.1734	236.7	1.521	1.562	1.082	0.788	1.042	1.187
0.60	0.90	0.1890	0.8723	0.0882	242.1	1.540	1.563	1.015	0.777	1.011	1.166
0.80	0.	0.8667	0.	0.1393	222.6	1.415	1.545	1.092	0.930	1.357	1.458
0.80	0.01	0.8542	0.0076	0.1342	222.8	1.416	1.545	1.091	0.937	1.352	1.454
0.80	0.02	0.8476	0.0153	0.1371	223.0	1.418	1.545	1.090	0.935	1.347	1.450
0.80	0.03	0.8414	0.0229	0.1381	223.2	1.419	1.545	1.089	0.933	1.342	1.446
0.80	0.04	0.8344	0.0306	0.1359	223.3	1.420	1.545	1.088	0.931	1.337	1.442
0.80	0.05	0.8278	0.0383	0.1339	223.5	1.422	1.545	1.087	0.929	1.332	1.437
0.80	0.07	0.8144	0.0458	0.1318	223.9	1.425	1.545	1.085	0.924	1.323	1.432
0.80	0.10	0.7945	0.0772	0.1285	224.4	1.429	1.545	1.081	0.914	1.309	1.418
0.80	0.20	0.7254	0.1572	0.1174	226.2	1.442	1.545	1.071	0.898	1.265	1.366
0.80	0.40	0.5782	0.3292	0.0836	230.1	1.468	1.544	1.052	0.862	1.108	1.314
0.80	0.60	0.4131	0.5103	0.0860	234.3	1.494	1.545	1.034	0.830	1.019	1.255
0.80	0.80	0.2248	0.7369	0.0832	239.0	1.521	1.551	1.019	0.797	1.057	1.202
0.80	0.90	0.1179	0.8632	0.0800	241.6	1.537	1.557	1.013	0.781	1.027	1.185
0.90	0.	0.9321	0.	0.6486	220.0	1.407	1.523	1.002	0.973	1.421	1.546
0.90	0.01	0.9252	0.0074	0.6475	220.2	1.408	1.523	1.001	0.970	1.420	1.545
0.90	0.02	0.9193	0.0144	0.6470	221.4	1.410	1.523	1.001	0.967	1.408	1.540
0.90	0.03	0.9114	0.0222	0.6468	221.6	1.411	1.524	1.000	0.965	1.402	1.528
0.90	0.04	0.9044	0.0296	0.6459	221.8	1.412	1.524	1.000	0.962	1.398	1.526
0.90	0.05	0.8975	0.0371	0.6454	221.9	1.414	1.524	1.000	0.960	1.396	1.523
0.90	0.07	0.8835	0.0521	0.6444	221.4	1.418	1.524	1.000	0.956	1.378	1.506
0.90	0.10	0.8623	0.1749	0.6428	222.0	1.422	1.526	1.003	0.946	1.361	1.490
0.90	0.20	0.7996	0.1527	0.6474	224.1	1.436	1.528	1.004	0.922	1.308	1.380
0.90	0.40	0.6335	0.3206	0.6464	224.4	1.444	1.531	1.004	0.878	1.219	1.354
0.90	0.60	0.4565	0.5105	0.6330	233.1	1.479	1.545	1.003	0.838	1.130	1.278
0.90	0.80	0.2921	0.7319	0.6180	234.3	1.519	1.545	1.001	0.802	1.069	1.207
0.90	0.90	0.139	0.8588	0.094	241.3	1.536	1.554	1.002	0.784	1.030	1.171
0.97	0.	0.939	0.	0.6201	217.1	1.400	1.505	1.075	1.000	1.473	1.511
0.97	0.01	0.9298	0.0072	0.6200	218.3	1.402	1.506	1.075	0.997	1.466	1.510
0.97	0.02	0.9057	0.0145	0.1194	218.5	1.403	1.507	1.074	0.993	1.458	1.507

B. Isothermal Table

The table to follow presents values calculated at even temperature intervals of five degrees from 140°R to 245°R. They are arranged in order of increasing liquid mole fraction ratio

$$\frac{N_2}{N_2 + O_2}$$

and sub-ordered according to increasing mole fraction of argon. The quantities calculated are vapor composition, pressure, equilibrium constant (K-Values), relative volatility, enthalpy, and heat capacity.

Table 26. Isothermal Calculated Values

TEMPERATURE = 140° R

LIQUID MOLE FRACTION	VAPOR MOLE FRACTION		PRESSURE	EQUIL CONST			RELATIVE VOL			ENTHALPY		HEAT CAPACITY			
	N ₂	AR/AR+O ₂		N ₂	AR	O ₂	ATM	N ₂	AR	O ₂	N ₂ /AR	N ₂ /O ₂	AR/O ₂	L ₁₀	V _{AP}
.975 .0.	1.993 .0.	0.0071	1.02	1.019	0.421	0.282	2.419	3.011	1.493	-1481.	934.	14.4	7.549		
.975 .1.	1.9927	0.0021	0.603	1.02	1.018	0.421	0.282	2.421	3.009	1.491	-1481.	933.	14.4	7.547	
.975 .2.	1.9724	0.0021	0.0054	1.02	1.018	0.420	0.282	2.422	3.007	1.490	-1481.	933.	14.4	7.545	
.975 .3.	1.9920	0.0031	0.0049	1.02	1.017	0.420	0.282	2.423	3.005	1.488	-1482.	933.	14.4	7.543	
.975 .4.	1.9817	0.0042	0.0047	1.02	1.017	0.420	0.282	2.424	3.003	1.486	-1482.	933.	14.4	7.541	
.975 .5.	1.9913	0.0052	0.0035	1.02	1.017	0.419	0.282	2.425	3.001	1.485	-1482.	932.	14.4	7.539	
.975 .6.	1.9910	0.0063	0.0024	1.02	1.016	0.419	0.282	2.426	3.000	1.483	-1482.	932.	14.4	7.537	
.975 .7.	1.9907	0.0073	0.0021	1.02	1.016	0.419	0.283	2.427	3.007	1.482	-1482.	932.	14.4	7.535	
.975 .8.	1.9903	0.0084	0.0014	1.02	1.016	0.410	0.283	2.428	3.004	1.480	-1483.	931.	14.3	7.533	
.975 .9.	1.9900	0.0094	0.0007	1.02	1.015	0.410	0.283	2.429	3.002	1.479	-1483.	931.	14.3	7.531	
.975 1.0.	1.9897	0.0104	0.	1.02	1.015	0.410	0.283	2.430	3.000	1.477	-1483.	931.	14.3	7.529	

TEMPERATURE = 145° R

LIQUID MOLE FRACTION	VAPOR MOLE FRACTION		PRESSURE	EQUIL CONST			RELATIVE VOL			ENTHALPY		HEAT CAPACITY			
	N ₂	AR/AR+O ₂		N ₂	AR	O ₂	ATM	N ₂	AR	O ₂	N ₂ /AR	N ₂ /O ₂	AR/O ₂	L ₁₀	V _{AP}
.800 .0.	0.8988	0.	0.1432	1.00	1.428	0.599	0.358	2.572	3.987	1.998	-1482.	971.	13.6	7.486	
.800 .1.	0.8492	0.0214	0.328	1.01	1.415	0.547	0.358	2.589	3.991	1.926	-1486.	964.	13.4	7.443	
.800 .2.	0.8423	0.0431	0.1147	1.02	1.404	0.539	0.359	2.585	3.915	1.938	-1471.	958.	13.3	7.401	
.800 .3.	0.8358	0.0637	0.1089	1.02	1.393	0.531	0.359	2.624	3.880	1.479	-1475.	952.	13.2	7.360	
.800 .4.	0.8299	0.0838	0.0853	1.03	1.383	0.524	0.360	2.641	3.865	1.456	-1470.	946.	13.1	7.321	
.800 .5.	0.8246	0.1034	0.0781	1.03	1.374	0.517	0.361	2.659	3.840	1.432	-1483.	941.	13.0	7.282	
.800 .6.	0.8197	0.1225	0.0579	1.04	1.366	0.510	0.362	2.677	3.776	1.411	-1487.	935.	12.9	7.245	
.800 .7.	0.8152	0.1412	0.0435	1.05	1.359	0.504	0.363	2.684	3.702	1.389	-1491.	929.	12.7	7.208	
.800 .8.	0.8114	0.1599	0.0292	1.05	1.352	0.499	0.365	2.712	3.708	1.367	-1499.	924.	12.6	7.172	
.800 .9.	0.8086	0.1776	0.0146	1.06	1.347	0.492	0.364	2.749	3.701	1.351	-1499.	923.	12.5	7.110	
.800 1.0.	0.8057	0.1947	0.	1.07	1.343	0.487	0.366	2.756	3.686	1.336	-1703.	916.	12.4	7.081	
.700 .0.	0.8988	0.	0.1013	1.10	1.364	0.512	0.338	2.564	3.862	1.518	-1495.	967.	13.7	7.535	
.700 .1.	0.8926	0.0192	0.0813	1.11	1.377	0.508	0.358	2.591	3.776	1.498	-1498.	963.	13.6	7.506	
.700 .2.	0.8868	0.0301	0.0613	1.11	1.378	0.501	0.359	2.594	3.780	1.498	-1501.	959.	13.5	7.476	
.700 .3.	0.8842	0.0446	0.0712	1.12	1.363	0.496	0.359	2.547	3.736	1.463	-1504.	954.	13.4	7.446	
.700 .4.	0.8809	0.0589	0.0612	1.12	1.357	0.491	0.349	2.559	3.700	1.445	-1507.	953.	13.3	7.426	
.700 .5.	0.8760	0.0730	0.0511	1.13	1.351	0.487	0.341	2.572	3.679	1.429	-1610.	948.	13.2	7.393	
.700 .6.	0.8724	0.0888	0.0410	1.13	1.346	0.482	0.341	2.585	3.659	1.412	-1613.	942.	13.2	7.366	
.700 .7.	0.8689	0.1033	0.0308	1.14	1.337	0.474	0.341	2.595	3.639	1.395	-1616.	938.	13.1	7.339	
.700 .8.	0.8655	0.1137	0.0206	1.14	1.327	0.474	0.341	2.611	3.600	1.379	-1619.	934.	13.0	7.313	
.700 .9.	0.8629	0.1246	0.0103	1.15	1.323	0.470	0.345	2.624	3.576	1.363	-1623.	930.	12.9	7.288	
.700 1.0.	0.8603	0.1398	0.	1.15	1.329	0.466	0.346	2.637	3.592	1.347	-1626.	927.	12.8	7.253	
.600 .0.	0.8355	0.	0.0645	1.00	1.478	0.478	0.323	2.617	3.625	1.481	-1526.	984.	13.8	7.988	
.600 .1.	0.9325	0.0095	0.0581	1.01	1.468	0.479	0.323	2.646	3.608	1.459	-1538.	982.	13.8	7.958	
.600 .2.	0.9295	0.0186	0.0518	1.01	1.462	0.478	0.323	2.644	3.592	1.458	-1532.	959.	13.7	7.549	
.600 .3.	0.9267	0.0281	0.0454	1.01	1.458	0.469	0.324	2.672	3.576	1.448	-1534.	958.	13.7	7.531	
.600 .4.	0.9239	0.0373	0.0389	1.02	1.455	0.466	0.324	2.688	3.560	1.439	-1536.	953.	13.6	7.514	
.600 .5.	0.9213	0.0463	0.0329	1.02	1.452	0.463	0.325	2.699	3.543	1.424	-1538.	951.	13.5	7.494	
.600 .6.	0.9189	0.0559	0.0260	1.02	1.449	0.460	0.326	2.717	3.527	1.413	-1540.	948.	13.5	7.479	
.600 .7.	0.9165	0.0646	0.0196	1.03	1.444	0.457	0.326	2.739	3.512	1.402	-1542.	946.	13.4	7.462	
.600 .8.	0.9143	0.0727	0.0131	1.03	1.439	0.455	0.327	2.751	3.496	1.391	-1544.	943.	13.4	7.445	
.600 .9.	0.9122	0.0804	0.0066	1.03	1.434	0.452	0.328	2.762	3.480	1.380	-1546.	940.	13.3	7.428	
.600 1.0.	0.9102	0.0899	0.	1.04	1.430	0.450	0.328	2.773	3.464	1.369	-1548.	938.	13.2	7.411	
.500 .0.	0.8892	0.	0.0512	1.05	1.377	0.451	0.312	2.658	3.456	1.447	-1460.	981.	14.0	7.830	
.500 .1.	0.8876	0.0045	0.0281	1.05	1.379	0.450	0.312	2.692	3.446	1.442	-1461.	980.	14.0	7.830	
.500 .2.	0.8862	0.0098	0.0250	1.05	1.371	0.448	0.312	2.708	3.440	1.438	-1462.	959.	13.9	7.621	
.500 .3.	0.8849	0.0134	0.0234	1.05	1.372	0.447	0.312	2.740	3.433	1.430	-1463.	957.	13.9	7.612	
.500 .4.	0.8838	0.0178	0.0208	1.05	1.371	0.445	0.313	2.744	3.426	1.429	-1464.	956.	13.9	7.604	
.500 .5.	0.8823	0.0222	0.0156	1.05	1.369	0.444	0.313	2.768	3.417	1.419	-1465.	955.	13.8	7.596	
.500 .6.	0.8811	0.0266	0.0125	1.05	1.368	0.443	0.313	2.781	3.409	1.414	-1466.	953.	13.8	7.587	
.500 .7.	0.8599	0.0359	0.0094	1.06	1.367	0.441	0.314	2.816	3.402	1.408	-1457.	952.	13.8	7.579	
.500 .8.	0.8587	0.0352	0.0063	1.06	1.365	0.438	0.314	2.820	3.394	1.403	-1460.	951.	13.7	7.571	
.500 .9.	0.8575	0.0359	0.0031	1.06	1.364	0.437	0.314	2.824	3.386	1.397	-1469.	950.	13.7	7.562	
.500 1.0.	0.8564	0.0430	0.	1.07	1.363	0.438	0.315	2.828	3.379	1.392	-1470.	948.	13.7	7.554	
.475 .0.	0.8526	0.	0.0276	1.08	1.418	0.434	0.305	2.744	3.335	1.423	-1419.	959.	14.1	7.670	
.475 .1.	0.8522	0.0101	0.0160	1.08	1.418	0.434	0.305	2.749	3.333	1.421	-1419.	958.	14.1	7.677	
.475 .2.	0.8519	0.0229	0.0061	1.08	1.417	0.434	0.305	2.756	3.327	1.420	-1419.	958.	14.1	7.675	
.4															

LIQUID Wt. FRACTION	VAPOR Wt. FRACTION		PRESSURE	EQUIL. CONST.			RELATIVE VOL.			ENTHALPY		HEAT CAPACITY				
	N ₁	N ₂		A ₁	A ₂	N ₂	A ₁	A ₂	N ₂ /A ₁	N ₂ /A ₂	A ₁ /A ₂	Liq	Vap	Liq	Vap	
.3	.3	.6	0.2500	0.2423	0.1738	1.04	1.946	0.692	0.497	2.812	3.919	1.394	-1049.	936.	12.1	6.930
.3	.4	.6	0.2760	0.2666	0.1794	1.06	1.922	0.676	0.496	2.842	3.899	1.359	-1046.	923.	11.9	6.954
.3	.5	.6	0.2770	0.3243	0.1791	1.03	1.902	0.662	0.500	2.874	3.861	1.323	-1050.	911.	11.7	6.774
.3	.6	.6	0.2679	0.3163	0.1786	1.04	1.886	0.649	0.504	2.905	3.745	1.206	-1044.	899.	11.5	6.693
.3	.7	.6	0.2679	0.4749	0.1786	1.06	1.875	0.636	0.509	2.937	3.686	1.259	-1072.	880.	11.3	6.610
.3	.8	.6	0.2679	0.4491	0.1782	1.07	1.867	0.629	0.514	2.969	3.639	1.223	-1081.	870.	11.1	6.542
.3	.9	.6	0.2745	0.4291	0.1782	1.08	1.853	0.711	0.511	2.981	4.042	1.554	-1751.	1004.	11.1	7.270
.4	.0	.6	0.2745	0.4069	0.2425	1.09	1.792	0.602	0.449	2.925	3.989	1.320	-1730.	992.	11.1	7.197
.4	.1	.6	0.2745	0.4078	0.2193	1.10	1.763	0.605	0.446	2.956	3.937	1.406	-1745.	986.	12.0	7.321
.4	.2	.6	0.2745	0.4176	0.1879	1.11	1.730	0.650	0.447	2.975	3.886	1.453	-1752.	969.	12.0	7.247
.4	.3	.6	0.2694	0.4152	0.1611	1.13	1.710	0.636	0.447	2.788	3.845	1.420	-1759.	950.	12.0	7.177
.4	.4	.6	0.2679	0.4084	0.1344	1.14	1.697	0.623	0.448	2.725	3.785	1.359	-1766.	940.	12.4	7.109
.4	.5	.6	0.2722	0.2199	0.1459	1.15	1.680	0.611	0.450	2.791	3.735	1.398	-1773.	930.	12.2	7.043
.4	.6	.6	0.2666	0.2521	0.1414	1.16	1.667	0.600	0.452	2.776	3.687	1.328	-1780.	929.	12.0	6.980
.4	.7	.6	0.2764	0.3142	0.1279	1.17	1.655	0.591	0.455	2.802	3.639	1.298	-1787.	919.	11.8	6.917
.4	.8	.6	0.2764	0.3445	0.1151	1.19	1.644	0.582	0.458	2.829	3.591	1.270	-1794.	910.	11.7	6.856
.4	.9	.6	0.2745	0.3755	0.1051	1.22	1.549	0.625	0.411	2.546	3.861	1.320	-1803.	900.	13.4	7.538
.5	.0	.6	0.2745	0.3726	0.1440	1.23	1.549	0.613	0.411	2.566	3.819	1.492	-1808.	991.	13.3	7.470
.5	.1	.6	0.2745	0.3885	0.1458	1.24	1.531	0.601	0.411	2.586	3.778	1.464	-1814.	982.	13.1	7.420
.5	.2	.6	0.2745	0.3886	0.1458	1.25	1.521	0.590	0.411	2.606	3.736	1.437	-1818.	974.	13.0	7.364
.5	.3	.6	0.2750	0.1420	0.1332	1.26	1.500	0.580	0.412	2.621	3.696	1.410	-1826.	965.	12.8	7.310
.5	.4	.6	0.2745	0.1687	0.1428	1.27	1.497	0.562	0.413	2.641	3.656	1.384	-1822.	957.	12.7	7.257
.5	.5	.6	0.2747	0.1941	0.1424	1.28	1.487	0.554	0.410	2.682	3.576	1.333	-1830.	948.	12.5	7.206
.5	.6	.6	0.2795	0.2198	0.1610	1.29	1.479	0.547	0.410	2.783	3.537	1.309	-1710.	934.	12.4	7.156
.5	.7	.6	0.2766	0.2431	0.1610	1.30	1.472	0.540	0.421	2.724	3.499	1.284	-1715.	927.	12.0	7.100
.5	.8	.6	0.2731	0.2670	0.1610	1.31	1.466	0.533	0.424	2.746	3.461	1.261	-1721.	921.	12.0	7.060
.5	.9	.6	0.2745	0.3131	0.1531	1.35	1.412	0.561	0.303	2.481	3.880	1.485	-1831.	958.	13.5	7.598
.6	.0	.6	0.3399	0.2224	0.1178	1.36	1.400	0.561	0.303	2.497	3.857	1.464	-1599.	960.	13.4	7.554
.6	.1	.6	0.3333	0.4442	0.1726	1.36	1.389	0.593	0.303	2.512	3.629	1.443	-1604.	983.	13.3	7.512
.6	.2	.6	0.3273	0.4594	0.1874	1.37	1.379	0.545	0.304	2.526	3.593	1.421	-1609.	977.	13.2	7.478
.6	.3	.6	0.3273	0.4661	0.1923	1.38	1.379	0.530	0.305	2.544	3.562	1.400	-1613.	970.	13.0	7.430
.6	.4	.6	0.3273	0.4771	0.1971	1.39	1.361	0.532	0.306	2.560	3.531	1.379	-1616.	964.	12.9	7.390
.6	.5	.6	0.3161	0.1791	0.1619	1.39	1.354	0.526	0.307	2.576	3.500	1.359	-1623.	950.	12.8	7.351
.6	.6	.6	0.3081	0.1455	0.1604	1.40	1.347	0.520	0.308	2.592	3.469	1.339	-1627.	952.	12.7	7.314
.6	.7	.6	0.3013	0.1644	0.1512	1.41	1.341	0.514	0.309	2.610	3.439	1.319	-1630.	947.	12.6	7.277
.6	.8	.6	0.2955	0.1692	0.1517	1.42	1.335	0.509	0.309	2.621	3.409	1.299	-1637.	941.	12.4	7.240
.6	.9	.6	0.2817	0.1805	0.1517	1.43	1.331	0.504	0.304	2.641	3.379	1.280	-1642.	935.	12.3	7.204
.7	.0	.6	0.2803	0.1956	0.1977	1.40	1.267	0.520	0.362	2.424	3.524	1.454	-1527.	993.	13.2	7.659
.7	.1	.6	0.2803	0.2089	0.1978	1.40	1.256	0.519	0.362	2.435	3.501	1.430	-1530.	988.	13.1	7.629
.7	.2	.6	0.2876	0.2459	0.1762	1.40	1.254	0.510	0.363	2.446	3.470	1.422	-1534.	983.	13.0	7.599
.7	.3	.6	0.2749	0.2607	0.1659	1.41	1.249	0.504	0.364	2.458	3.455	1.406	-1537.	979.	13.4	7.570
.7	.4	.6	0.2743	0.2752	0.1647	1.41	1.243	0.501	0.349	2.461	3.419	1.391	-1541.	974.	13.3	7.541
.7	.5	.6	0.2669	0.2849	0.1639	1.41	1.230	0.504	0.366	2.474	3.411	1.379	-1544.	970.	13.2	7.513
.7	.6	.6	0.2637	0.3035	0.1639	1.42	1.234	0.493	0.367	2.492	3.388	1.359	-1548.	965.	13.1	7.485
.7	.7	.6	0.2600	0.3173	0.1621	1.43	1.230	0.490	0.368	2.504	3.366	1.344	-1551.	961.	13.0	7.450
.7	.8	.6	0.2582	0.3130	0.1611	1.43	1.226	0.485	0.369	2.520	3.322	1.314	-1555.	957.	12.9	7.432
.7	.9	.6	0.2555	0.3444	0.1607	1.44	1.223	0.481	0.370	2.539	3.300	1.302	-1562.	949.	12.8	7.379
.8	.0	.6	0.2511	0.3661	0.1607	1.45	1.184	0.492	0.346	2.367	3.366	1.422	-1459.	989.	13.0	7.722
.8	.1	.6	0.2526	0.3945	0.1605	1.46	1.169	0.489	0.346	2.374	3.324	1.391	-1461.	986.	13.7	7.783
.8	.2	.6	0.2527	0.3299	0.1606	1.46	1.157	0.466	0.347	2.382	3.337	1.301	-1463.	983.	13.6	7.684
.8	.3	.6	0.2521	0.3459	0.1672	1.46	1.153	0.483	0.347	2.389	3.323	1.339	-1468.	980.	13.6	7.666
.8	.4	.6	0.2517	0.3477	0.1646	1.46	1.150	0.480	0.348	2.397	3.301	1.308	-1468.	977.	13.5	7.648
.8	.5	.6	0.2512	0.3569	0.1629	1.46	1.147	0.477	0.349	2.408	3.294	1.336	-1473.	974.	13.5	7.630
.8	.6	.6	0.2512	0.3661	0.1621	1.46	1.144	0.474	0.349	2.412	3.279	1.306	-1473.	971.	13.4	7.612
.8	.7	.6	0.2511	0.3751	0.1614	1.46	1.142	0.472	0.350	2.419	3.265	1.349	-1475.	969.	13.3	7.593
.8	.8	.6	0.2502	0.3870	0.1607	1.46	1.136	0.467	0.351	2.434	3.236	1.329	-1480.	963.	13.2	7.577
.8	.9	.6	0.2497	0.3979	0.1607	1.46	1.135	0.464	0.352	2.442	3.222	1.320	-1482.	962.	13.1	7.560
.9	.0	.6	0.2567	0.3334	0.1734	1.74	1.074	0.465	0.334	2.372	3.216	1.301	-1301.	983.	13.9	7.767
.9	.1	.6	0.2650	0.3946	0.1731	1.74	1.073	0.463	0.334	2.316	3.209	1.304	-1302.	983.	13.8	7.778
.9	.2	.6	0.2643	0.3992	0.1734	1.74	1.071	0.462	0.335	2.319	3.202	1.301	-1303.	982.	13.8	7.769
.9	.3	.6	0.2636	0.3938	0.1734	1.75	1.070	0.461	0.335	2.323	3.195	1.378	-1304.	980.	13.8	7.760
.9	.4															

LIQUID MOLE FRACTION	VAPOR			PRESSURE	SOLN CONST.	RELATIVE VOL	ENTHALPY		HEAT CAPACITY						
	N ₂	AR/A ₄ +O ₂	N ₂	AR/02			BTU/LB MOLE	BTU/LB MOLE-R	BTU/LB MOLE	BTU/LB MOLE-R					
.100	0.0	1.2627	0.4897	0.9476	1.00	2.827	0.967	0.588	2.897	3.619	1.318	-1941.	894.	-11.5	6.393
.100	0.1	0.2580	0.5591	0.1463	1.00	2.586	0.881	0.698	2.939	3.747	1.277	-1953.	874.	-11.7	6.295
.100	0.2	0.2597	0.6102	0.1792	1.00	2.557	0.868	0.698	2.973	3.676	1.236	-1955.	854.	-10.9	6.132
.100	0.3	0.2539	0.6879	0.1434	1.00	2.539	0.843	0.704	3.013	3.607	1.197	-1977.	835.	-10.7	6.000
.100	0.4	0.2533	0.7448	0.1	1.00	2.533	0.825	0.716	3.052	3.539	1.160	-1989.	819.	-10.4	5.868
.200	0.0	0.5381	0.	0.4640	1.00	2.530	0.946	0.417	2.620	4.098	1.584	-1801.	1840.	-13.2	7.440
.200	0.1	0.4092	0.8730	0.4371	1.00	2.446	0.922	0.407	2.650	4.029	1.526	-1811.	1817.	-13.0	7.295
.200	0.2	0.4747	0.1417	0.3436	1.00	2.374	0.886	0.399	2.681	3.961	1.478	-1822.	998.	-12.7	7.141
.200	0.3	0.4847	0.2047	0.3127	1.00	2.313	0.853	0.394	2.712	3.895	1.436	-1833.	977.	-12.4	7.034
.200	0.4	0.4522	0.2630	0.2436	1.00	2.263	0.828	0.391	2.744	3.820	1.398	-1843.	958.	-12.2	6.919
.200	0.5	0.4441	0.3200	0.2359	1.00	2.221	0.808	0.388	2.776	3.765	1.356	-1854.	941.	-12.0	6.807
.200	0.6	0.4373	0.3777	0.1898	1.00	2.187	0.779	0.501	2.800	3.702	1.318	-1864.	924.	-11.8	6.708
.200	0.7	0.4319	0.4257	0.1424	1.00	2.150	0.760	0.503	2.831	3.649	1.281	-1875.	908.	-11.5	6.595
.200	0.8	0.4274	0.4765	0.1057	1.00	2.140	0.744	0.508	2.874	3.578	1.245	-1886.	893.	-11.3	6.493
.200	0.9	0.4252	0.5265	0.0483	1.00	2.128	0.731	0.508	2.908	3.518	1.216	-1898.	877.	-11.0	6.392
.200	1.0	0.4238	0.5703	0.	1.00	2.119	0.728	0.513	2.941	3.459	1.178	-1907.	862.	-10.8	6.276
.300	0.	0.5272	0.	0.3731	1.00	2.093	0.616	0.515	2.561	3.222	1.331	-1732.	1035.	-13.3	7.513
.300	0.1	0.4122	0.8359	0.3327	1.00	2.041	0.579	0.528	2.568	3.064	1.493	-1742.	1818.	-13.1	7.409
.300	0.2	0.5093	0.1770	0.2938	1.00	1.998	0.574	0.525	2.514	3.097	1.454	-1751.	1802.	-12.9	7.303
.300	0.3	0.5081	0.1559	0.2561	1.00	1.950	0.572	0.523	2.543	3.751	1.428	-1768.	987.	-12.7	7.206
.300	0.4	0.5785	0.2624	0.2192	1.00	1.920	0.572	0.522	2.567	3.698	1.389	-1789.	972.	-12.5	7.115
.300	0.5	0.5704	0.2470	0.1828	1.00	1.901	0.578	0.522	2.605	3.641	1.351	-1778.	958.	-12.2	7.026
.300	0.6	0.5630	0.2899	0.1466	1.00	1.879	0.600	0.524	2.722	3.568	1.318	-1788.	945.	-12.0	6.941
.300	0.7	0.5581	0.3319	0.1105	1.00	1.860	0.677	0.526	2.798	3.535	1.288	-1797.	932.	-11.8	6.856
.300	0.8	0.5530	0.3721	0.0742	1.00	1.840	0.665	0.536	2.778	3.483	1.254	-1807.	928.	-11.6	6.777
.300	0.9	0.5356	0.4121	0.0374	1.00	1.835	0.654	0.535	2.866	3.432	1.223	-1814.	917.	-11.4	6.697
.300	1.0	0.5400	0.4515	0.	1.00	1.829	0.645	0.541	2.835	3.361	1.193	-1825.	905.	-11.2	6.618
.400	0.	0.7143	0.	0.2856	1.00	1.784	0.713	0.478	2.605	3.751	1.478	-1684.	1838.	-13.4	7.588
.400	0.1	0.7025	0.4017	0.2599	1.00	1.756	0.695	0.474	2.597	3.704	1.447	-1677.	1817.	-13.2	7.584
.400	0.2	0.6910	0.4014	0.2669	1.00	1.730	0.679	0.473	2.549	3.639	1.436	-1686.	1805.	-13.0	7.426
.400	0.3	0.6824	0.1194	0.1983	1.00	1.708	0.654	0.472	2.571	3.611	1.405	-1688.	993.	-12.9	7.351
.400	0.4	0.6741	0.1560	0.1701	1.00	1.689	0.637	0.472	2.593	3.567	1.379	-1696.	982.	-12.7	7.280
.400	0.5	0.6669	0.1912	0.1420	1.00	1.667	0.617	0.472	2.616	3.522	1.348	-1704.	971.	-12.5	7.210
.400	0.6	0.6606	0.2254	0.1148	1.00	1.642	0.602	0.475	2.639	3.476	1.318	-1712.	968.	-12.3	7.143
.400	0.7	0.6556	0.2596	0.0899	1.00	1.630	0.589	0.477	2.662	3.434	1.290	-1719.	959.	-12.1	7.077
.400	0.8	0.6470	0.2911	0.0678	1.00	1.620	0.577	0.485	2.685	3.390	1.263	-1727.	949.	-11.9	7.013
.400	0.9	0.6445	0.3230	0.0390	1.00	1.610	0.568	0.484	2.708	3.348	1.236	-1735.	938.	-11.8	6.959
.400	1.0	0.6445	0.3545	0.	1.00	1.614	0.551	0.488	2.732	3.305	1.210	-1743.	928.	-11.8	6.888
.500	0.	0.7024	0.	0.2778	1.00	1.565	0.639	0.430	2.449	3.562	1.348	-1593.	1829.	-13.5	7.658
.500	0.1	0.7731	0.8313	0.1958	1.00	1.546	0.627	0.439	2.417	3.594	1.441	-1602.	1814.	-13.3	7.597
.500	0.2	0.7647	0.8015	0.1740	1.00	1.529	0.615	0.435	2.481	3.518	1.419	-1609.	1804.	-13.2	7.538
.500	0.3	0.7571	0.8097	0.1523	1.00	1.514	0.602	0.432	2.437	3.479	1.389	-1615.	997.	-13.0	7.461
.500	0.4	0.7554	0.1191	0.1308	1.00	1.501	0.595	0.436	2.521	3.443	1.366	-1622.	986.	-12.9	7.426
.500	0.5	0.7444	0.1466	0.1093	1.00	1.499	0.788	0.437	2.540	3.407	1.341	-1628.	980.	-12.7	7.372
.500	0.6	0.7381	0.1734	0.0877	1.00	1.478	0.758	0.439	2.558	3.378	1.318	-1635.	971.	-12.6	7.320
.500	0.7	0.7346	0.1996	0.0691	1.00	1.449	0.726	0.440	2.577	3.335	1.294	-1642.	963.	-12.4	7.269
.500	0.8	0.7347	0.2292	0.0443	1.00	1.401	0.763	0.443	2.595	3.308	1.272	-1648.	959.	-12.3	7.218
.500	0.9	0.7275	0.2595	0.0223	1.00	1.455	0.557	0.448	2.614	3.265	1.249	-1655.	947.	-12.1	7.149
.500	1.0	0.7249	0.2773	0.	1.00	1.451	0.521	0.449	2.633	3.231	1.227	-1662.	939.	-12.0	7.111
.600	0.	0.8378	0.	0.1623	1.00	1.395	0.583	0.436	2.395	3.427	1.435	-1527.	1821.	-13.6	7.132
.600	0.1	0.8316	0.8236	0.1463	1.00	1.389	0.579	0.436	2.469	3.408	1.415	-1532.	1813.	-13.5	7.087
.600	0.2	0.8247	0.4054	0.1301	1.00	1.375	0.567	0.437	2.423	3.384	1.395	-1537.	1806.	-13.3	7.044
.600	0.3	0.8190	0.0972	0.1214	1.00	1.360	0.554	0.437	2.437	3.351	1.375	-1542.	1800.	-13.2	7.002
.600	0.4	0.8130	0.0895	0.0900	1.00	1.356	0.553	0.438	2.451	3.323	1.356	-1548.	993.	-13.1	7.048
.600	0.5	0.8090	0.1094	0.0818	1.00	1.343	0.547	0.439	2.465	3.295	1.337	-1553.	984.	-13.0	7.028
.600	0.6	0.8040	0.1208	0.0857	1.00	1.321	0.541	0.441	2.480	3.267	1.318	-1559.	980.	-12.9	7.488
.600	0.7	0.8010	0.1499	0.0844	1.00	1.320	0.535	0.442	2.494	3.246	1.299	-1564.	974.	-12.7	7.411
.600	0.8	0.7947	0.1696	0.0631	1.00	1.294	0.525	0.416	2.523	3.185	1.262	-1573.	961.	-12.5	7.368
.600	0.9	0.7926	0.1973	0.0336	1.00	1.211	0.509	0.368	2.595	3.156	1.243	-1589.	955.	-12.4	7.329
.600	1.0	0.7924	0.2101	0.0663	1.00	1.195	0.503	0.368	2.597	3.125	1.215	-1575.	1811.	-12.3	7.287
.600	0.1	0.9214	0.2020	0.0595	1.00	1.152	0.500	0.369	2.592	3.109	1.209	-1595.	1805.	-12.7	7.847
.600	0.2	0.9188	0.0298	0.0517	1.00	1.149	0.497	0.369	2.516	3.069	1.204	-1598.	1802.	-13.6	7.828
.600	0.3	0.9164	0.0396	0.0444	1.00	1.146	0.494	0.370	2.537	3.048	1.206	-1606.	998.	-13.5	7.810
.600	0.4	0.9142	0.0492												

TEMPERATURE = 160. P

Table 26. (cont.)

LIQUID MOLE FRACTION	VAPOR MOLE FRACTION	PRESSURE	EQUIL CONST			RELATIVE VOL			ENTHALPY			HEAT CAPACITY				
			N ₂	AR	O ₂	ATH	N ₂	AR	O ₂	N ₂ /AR	N ₂ /O ₂	AR/O ₂	L ₁₀	V _{AP}	L ₁₀	V _{AP}
0.3	0.	0.3794	0.4207	1.00	3.459	1.265	0.807	2.736	3.902	1.426	-1917.	958.	12.2	6.016		
0.4	0.	0.4700	0.5211	1.03	3.320	1.197	0.869	2.773	3.622	1.379	-1931.	927.	11.9	6.417		
0.5	0.	0.5713	0.4287	1.07	3.211	1.143	0.857	2.810	3.745	1.333	-1946.	897.	11.7	6.231		
0.6	0.	0.6570	0.3411	1.09	3.129	1.098	0.853	2.849	3.600	1.288	-1961.	869.	11.4	6.054		
0.7	0.	0.7449	0.2561	1.12	3.069	1.063	0.854	2.887	3.595	1.245	-1976.	842.	11.1	5.881		
0.8	0.	0.8200	0.1720	1.14	3.029	1.035	0.860	2.927	3.522	1.203	-1991.	816.	10.8	5.709		
0.9	0.	0.9120	0.0472	1.16	3.109	1.014	0.872	2.966	3.451	1.163	-2005.	789.	10.5	5.534		
1.0	0.	1.0210	0.	1.17	3.107	1.000	0.889	3.007	3.341	1.124	-2014.	762.	10.2	5.352		
0.25	0.2	0.546	0.241	0.6694	1.03	3.185	1.262	0.850	2.883	3.008	1.470	-1884.	998.	12.6	6.912	
0.25	0.3	0.608	0.346	0.5713	1.06	3.235	1.190	0.837	2.718	3.007	1.422	-1890.	967.	12.3	6.700	
0.25	0.4	0.729	0.442	0.4809	1.10	3.118	1.131	0.822	2.754	3.793	1.376	-1913.	937.	12.0	6.514	
0.25	0.5	0.750	0.5270	0.3966	1.13	3.022	1.003	0.813	2.701	3.719	1.331	-1927.	909.	11.7	6.346	
0.25	0.6	0.730	0.6103	0.3100	1.15	2.950	1.043	0.810	2.828	3.642	1.288	-1941.	883.	11.4	6.174	
0.25	0.7	0.727	0.6930	0.2768	1.13	2.907	1.013	0.809	2.875	3.592	1.250	-1956.	859.	11.1	5.991	
0.25	0.8	0.710	0.7690	0.1593	1.20	2.862	0.986	0.810	2.942	3.430	1.196	-1969.	800.	10.6	5.867	
0.25	0.9	0.711	0.8482	0.1180	1.22	2.843	0.967	0.829	2.963	3.490	1.205	-1976.	833.	10.9	5.850	
0.25	1.0	0.711	0.9291	0.	1.23	2.840	0.953	0.845	2.981	3.362	1.120	-1999.	782.	10.3	5.519	
0.100	0.	0.365	0.	0.6035	1.14	3.065	1.192	0.771	2.572	3.978	1.347	-1803.	1073.	13.2	7.452	
0.100	0.1	0.2924	0.1031	0.6084	1.18	2.924	1.123	0.749	2.663	3.905	1.500	-1817.	1041.	13.0	7.233	
0.100	0.2	0.289	0.1018	0.5927	1.22	2.860	1.064	0.733	2.635	3.033	1.459	-1830.	1012.	12.7	7.075	
0.100	0.3	0.2715	0.2740	0.4542	1.25	2.713	1.017	0.721	2.667	3.763	1.411	-1843.	985.	12.4	6.911	
0.100	0.4	0.2635	0.3514	0.3852	1.28	2.635	0.970	0.709	2.699	3.694	1.369	-1857.	961.	12.2	6.759	
0.100	0.5	0.2572	0.4237	0.3102	1.30	2.572	0.941	0.709	2.732	3.627	1.327	-1870.	937.	11.9	6.614	
0.100	0.6	0.2592	0.4926	0.2551	1.33	2.523	0.912	0.709	2.765	3.561	1.287	-1883.	915.	11.6	6.476	
0.100	0.7	0.2488	0.5595	0.1920	1.35	2.466	0.888	0.711	2.808	3.494	1.249	-1896.	894.	11.4	6.341	
0.100	0.8	0.2446	0.6250	0.1298	1.37	2.400	0.863	0.717	2.834	3.432	1.211	-1910.	873.	11.1	6.208	
0.100	0.9	0.2444	0.6803	0.0593	1.39	2.445	0.852	0.726	2.865	3.369	1.179	-1923.	853.	10.8	6.074	
0.100	1.0	0.2444	0.7561	0.	1.41	2.440	0.840	0.737	2.904	3.300	1.139	-1936.	832.	10.6	5.939	
0.200	0.	0.4724	0.	0.7474	0.4534	1.43	2.362	0.920	0.630	2.944	3.759	1.474	-1740.	1043.	13.1	7.393
0.200	0.1	0.4591	0.1420	0.3942	1.46	2.296	0.893	0.622	2.972	3.694	1.439	-1750.	1021.	12.8	7.298	
0.200	0.2	0.4470	0.2087	0.3455	1.48	2.239	0.861	0.617	2.960	3.639	1.399	-1770.	1000.	12.6	7.133	
0.200	0.3	0.4385	0.2690	0.2947	1.51	2.192	0.834	0.614	2.928	3.597	1.359	-1782.	981.	12.4	7.045	
0.200	0.4	0.437	0.3242	0.2492	1.53	2.153	0.811	0.613	2.897	3.513	1.322	-1793.	963.	12.1	6.908	
0.200	0.5	0.4244	0.3703	0.1965	1.55	2.122	0.780	0.613	2.865	3.459	1.287	-1805.	945.	11.9	6.791	
0.200	0.6	0.4150	0.4494	0.0995	1.58	2.045	0.752	0.617	2.715	3.390	1.252	-1817.	920.	11.7	6.684	
0.200	0.7	0.4134	0.5385	0.1503	1.61	2.067	0.745	0.620	2.774	3.291	1.188	-1841.	895.	11.2	6.475	
0.200	0.8	0.4122	0.5988	0.	1.63	2.091	0.735	0.627	2.804	3.236	1.154	-1853.	870.	11.0	6.370	
0.200	0.	0.8115	0.	0.3007	1.64	2.035	0.626	0.557	2.464	3.053	1.483	-1865.	1061.	13.4	7.624	
0.200	0.1	0.5965	0.0380	0.3477	1.66	1.988	0.799	0.552	2.487	3.063	1.449	-1876.	1043.	13.2	7.516	
0.200	0.2	0.5844	0.1046	0.3072	1.69	1.948	0.776	0.546	2.511	3.292	1.414	-1886.	1026.	13.0	7.413	
0.200	0.3	0.5739	0.1585	0.2670	1.71	1.913	0.759	0.546	2.539	3.361	1.381	-1896.	1010.	12.8	7.319	
0.200	0.4	0.5649	0.2041	0.2202	1.73	1.883	0.736	0.546	2.559	3.491	1.349	-1917.	994.	12.6	7.222	
0.200	0.5	0.5573	0.2527	0.1911	1.75	1.850	0.719	0.546	2.583	3.462	1.317	-1927.	965.	12.2	7.045	
0.200	0.6	0.551	0.2990	0.1934	1.77	1.837	0.704	0.546	2.607	3.393	1.286	-1938.	952.	12.0	6.960	
0.200	0.7	0.5459	0.3367	0.1146	1.79	1.820	0.691	0.550	2.632	3.365	1.256	-1948.	938.	11.8	6.877	
0.200	0.8	0.5419	0.3867	0.0776	1.81	1.800	0.680	0.554	2.697	3.250	1.226	-1958.	925.	11.6	6.794	
0.200	0.9	0.5391	0.4220	0.0392	1.83	1.797	0.670	0.559	2.662	3.212	1.198	-1968.	906.	11.4	6.712	
0.200	1.0	0.5373	0.4630	0.	1.84	1.791	0.661	0.560	2.708	3.187	1.169	-1989.	892.	11.2	6.634	
0.300	0.	0.7704	0.	0.2998	1.407	1.751	0.726	0.500	2.412	3.304	1.453	-1997.	1053.	13.5	7.712	
0.300	0.1	0.6769	0.0831	0.2383	1.91	1.697	0.692	0.496	2.432	3.461	1.423	-1699.	1041.	13.3	7.629	
0.300	0.2	0.6699	0.1220	0.2083	1.94	1.675	0.676	0.486	2.452	3.419	1.395	-1714.	1020.	13.2	7.551	
0.300	0.3	0.6585	0.1630	0.1633	1.97	1.649	0.654	0.476	2.472	3.377	1.367	-1723.	1015.	13.0	7.479	
0.300	0.4	0.6422	0.2059	0.1787	2.00	1.625	0.635	0.466	2.492	3.336	1.339	-1732.	1003.	12.8	7.402	
0.300	0.5	0.6254	0.1957	0.1492	2.03	1.606	0.611	0.459	2.512	3.295	1.309	-1741.	981.	12.6	7.331	
0.300	0.6	0.6186	0.2309	0.1194	2.06	1.584	0.592	0.450	2.532	3.215	1.280	-1750.	960.	12.4	7.262	
0.300	0.7	0.6149	0.2803	0.0645	2.08	1.562	0.572	0.441	2.542	3.197	1.251	-1760.	937.	12.2	7.191	
0.300	0.8	0.6139	0.3248	0.0176	2.10	1.540	0.554	0.432	2.562	3.168	1.222	-1770.	927.	12.0	7.129	
0.300	0.9	0.6137	0.3715	0.	2.13	1.516	0.532	0.423	2.582	3.139	1.193	-1787.	917.	11.8	7.059	
0.300	1.0	0.6137	0.4237	0.	2.14	1.500	0.513	0.413	2.602	3.109	1.164	-1799.	906.	11.6	7.011	
0.400	0.	0.8223	0.	0.2716	2.31	1.341	0.598	0.429	2.311	3.220	1.337	-1937.	1043.	13.7	7.891	
0.400	0.1	0.8223	0.1230	0.1545	2.32	1.371	0.590	0.406	2.323	3.194	1.375	-1945.	1035.	13.5	7.845	
0.400	0.2	0.8144	0.1446	0.1379	2.33	1.361	0.582	0.430	2.338	3.184	1.356	-1957.	1028.	13.3	7.801	
0.400	0.3	0.8104	0.1910</													

LIQUID MOLE FRACTION		VAPOR MOLE FRACTION		PRESSURE		EQUIL. CONST.		RELATIVE VOL.		ENTHALPY BTU/LB MOLE		HEAT CAPACITY BTU/LB MOLE-R			
N ₂	AR/AR-02	N ₂	AR	O ₂	ATH	N ₂	AR	O ₂	N ₂ /AR	N ₂ /O ₂	AR/O ₂	L ₁₆	V _{AP}	L ₁₆	V _{AP}
.0.	.0.	.0.	.0.	1.0001	1.16	3.845	1.535	1.000	2.519	3.885	1.534	-1807.	1107.	13.2	7.482
.1.	.0.	.1417	.0.0584	1.12	3.413	1.47	0.954	2.551	3.789	1.485	-1823.	1080.	12.9	7.173	
.2.	.0.	.2645	.0.7356	1.08	3.415	1.32	0.920	2.583	3.754	1.438	-1839.	1020.	12.6	6.931	
.3.	.0.	.3737	.0.6264	1.03	3.288	1.246	0.895	2.615	3.641	1.392	-1855.	983.	12.4	6.715	
.4.	.0.	.4733	.0.5268	1.07	3.154	1.183	0.878	2.648	3.586	1.348	-1873.	951.	12.1	6.517	
.5.	.0.	.5662	.0.4339	1.01	3.037	1.132	0.868	2.682	3.499	1.305	-1889.	920.	11.8	6.331	
.6.	.0.	.6546	.0.3455	1.04	2.903	1.091	0.864	2.716	3.430	1.263	-1904.	891.	11.5	6.193	
.7.	.0.	.7404	.0.2995	1.07	2.899	1.058	0.865	2.750	3.361	1.223	-1920.	863.	11.2	5.979	
.8.	.0.	.8257	.0.1744	1.08	2.874	1.032	0.872	2.785	3.297	1.184	-1936.	835.	11.0	5.865	
.9.	.0.	.9117	.0.0884	1.02	2.859	1.013	0.892	2.820	3.232	1.148	-1952.	807.	10.7	5.627	
1.0	.0.	1.0001	0.	1.04	2.836	1.000	0.913	2.850	3.169	1.110	-1968.	778.	10.4	5.443	
.025	.0.	.0.0833	0.	0.107	1.95	3.574	1.426	0.924	2.556	3.826	1.507	-1789.	1105.	13.2	7.475
.025	.0.1	.0.0841	0.1293	0.7067	1.31	3.364	1.326	0.897	2.557	3.752	1.479	-1805.	1082.	13.0	7.222
.025	.0.2	.0.0799	0.1427	0.6775	1.08	3.198	1.245	0.869	2.586	3.689	1.433	-1821.	1029.	12.7	6.999
.025	.0.3	.0.0770	0.1451	0.5776	1.03	3.078	1.180	0.846	2.619	3.637	1.394	-1837.	992.	12.4	6.768
.025	.0.4	.0.0739	0.1379	0.4803	1.04	2.955	1.123	0.839	2.652	3.547	1.345	-1852.	960.	12.1	6.513
.025	.0.5	.0.0718	0.1292	0.4030	1.08	2.871	1.078	0.857	2.684	3.472	1.303	-1868.	931.	11.9	6.439
.025	.0.6	.0.0671	0.1168	0.3213	1.01	2.800	1.040	0.824	2.807	3.416	1.263	-1884.	904.	11.6	6.271
.025	.0.7	.0.0639	0.1086	0.2419	1.04	2.756	1.023	0.806	2.790	3.340	1.224	-1900.	877.	11.3	6.107
.025	.0.8	.0.0602	0.1076	0.1623	1.07	2.727	0.987	0.784	2.764	3.276	1.186	-1915.	851.	11.0	5.944
.025	.0.9	.0.0570	0.0951	0.0802	1.09	2.711	0.964	0.842	2.798	3.234	1.149	-1931.	825.	10.8	5.778
.025	1.0	.0.0577	0.0934	0.	1.01	2.705	0.950	0.899	2.832	3.153	1.113	-1947.	798.	10.5	5.602
.100	.0.	.3.2720	0.	1.7082	1.00	2.920	1.183	0.787	2.688	3.711	1.924	-1737.	1091.	13.5	7.022
.100	.0.1	.0.2791	0.1007	0.6263	1.58	2.795	1.118	0.766	2.498	3.645	1.480	-1752.	1064.	12.1	7.353
.100	.0.2	.0.2805	0.1195	0.5411	1.59	2.685	1.084	0.730	2.524	3.586	1.448	-1768.	1036.	12.0	7.176
.100	.0.3	.0.2811	0.1249	0.4637	1.59	2.613	1.018	0.715	2.564	3.547	1.384	-1781.	1015.	12.0	6.976
.100	.0.4	.0.2822	0.1352	0.3761	1.59	2.539	0.944	0.697	2.592	3.494	1.338	-1795.	982.	12.0	6.869
.100	.0.5	.0.2840	0.1426	0.3276	1.70	2.479	0.946	0.678	2.615	3.393	1.299	-1812.	958.	12.1	6.712
.100	.0.6	.0.2845	0.1498	0.2761	1.73	2.429	0.918	0.641	2.641	3.333	1.262	-1829.	935.	11.8	6.574
.100	.0.7	.0.2891	0.1583	0.1972	1.78	2.391	0.899	0.610	2.671	3.274	1.226	-1849.	913.	11.6	6.437
.100	.0.8	.0.2855	0.1630	0.1385	1.78	2.367	0.876	0.587	2.708	3.216	1.181	-1864.	892.	11.3	6.301
.100	.0.9	.0.2849	0.1744	0.0670	1.81	2.352	0.845	0.545	2.733	3.153	1.143	-1883.	867.	11.0	6.159
.100	1.0	.0.2846	0.1759	0.	1.83	2.349	0.809	0.517	2.753	3.104	1.103	-1900.	847.	10.8	6.026
.200	.0.	.4.7471	0.	0.5290	1.81	2.395	0.875	0.601	2.411	3.562	1.473	-1888.	1092.	13.4	7.651
.200	.0.1	.0.4568	0.0748	0.4000	1.95	2.282	0.928	0.551	2.442	3.498	1.438	-1901.	1087.	13.2	7.568
.200	.0.2	.0.4442	0.1414	0.4119	1.89	2.211	0.850	0.514	2.467	3.491	1.399	-1914.	1044.	13.1	7.372
.200	.0.3	.0.4337	0.2099	0.3576	1.92	2.189	0.870	0.499	2.492	3.396	1.363	-1929.	1022.	12.8	7.249
.200	.0.4	.0.4250	0.2701	0.3051	1.95	2.158	0.844	0.484	2.513	3.326	1.328	-1943.	998.	12.5	7.129
.200	.0.5	.0.4177	0.3284	0.2539	1.98	2.089	0.802	0.455	2.542	3.292	1.294	-1957.	964.	12.3	6.932
.200	.0.6	.0.4110	0.3849	0.2335	2.02	2.059	0.789	0.429	2.569	3.236	1.254	-1971.	934.	12.1	6.790
.200	.0.7	.0.4073	0.4349	0.1933	2.06	2.036	0.759	0.399	2.594	3.187	1.229	-1985.	906.	11.9	6.689
.200	.0.8	.0.4039	0.4733	0.1630	2.08	2.020	0.730	0.371	2.611	3.127	1.197	-2001.	871.	11.6	6.583
.200	.0.9	.0.4017	0.5465	0.0920	2.08	2.009	0.709	0.351	2.647	3.085	1.167	-2018.	846.	11.4	6.478
.200	1.0	.0.4017	0.5960	0.	2.13	2.024	0.674	0.349	2.673	3.039	1.137	-2037.	813.	11.2	6.468
.300	.0.	.5.8946	0.	0.4597	2.11	2.982	0.837	0.561	2.348	3.442	1.444	-1998.	1085.	13.5	7.754
.300	.0.1	.0.5815	0.0540	0.3628	2.14	2.938	0.781	0.517	2.393	3.373	1.411	-2010.	1066.	13.3	7.645
.300	.0.2	.0.5711	0.1203	0.3199	2.17	2.900	0.758	0.571	2.411	3.321	1.380	-2021.	1048.	13.1	7.541
.300	.0.3	.0.5612	0.1812	0.2799	2.20	2.867	0.728	0.549	2.432	3.282	1.349	-2032.	1031.	12.9	7.443
.300	.0.4	.0.5517	0.2499	0.2380	2.23	2.839	0.700	0.524	2.454	3.235	1.318	-2043.	1015.	12.8	7.346
.300	.0.5	.0.5445	0.2966	0.1991	2.25	2.815	0.673	0.504	2.475	3.190	1.289	-2055.	999.	12.6	7.257
.300	.0.6	.0.5386	0.3200	0.1998	2.27	2.795	0.647	0.487	2.497	3.146	1.260	-2066.	984.	12.4	7.168
.300	.0.7	.0.5331	0.3401	0.1204	2.30	2.779	0.626	0.469	2.524	3.094	1.232	-2077.	969.	12.2	7.082
.300	.0.8	.0.5275	0.3742	0.0498	2.34	2.758	0.598	0.450	2.554	3.048	1.204	-2089.	955.	12.0	6.993
.300	.0.9	.0.5259	0.4221	0.	2.36	2.735	0.563	0.422	2.585	3.002	1.174	-2100.	941.	11.8	6.913
.300	1.0	.0.5259	0.4744	0.	2.36	2.717	0.538	0.393	2.617	2.957	1.141	-2112.	927.	11.6	6.827
.400	.0.1	.0.6657	0.	0.3137	2.40	2.717	0.548	0.323	2.391	3.232	1.426	-1929.	1077.	13.5	7.690
.400	.0.2	.0.6759	0.0433	0.2812	2.42	2.695	0.522	0.349	2.359	3.249	1.387	-1938.	1043.	13.3	7.587
.400	.0.3	.0.6662	0.0846	0.2493	2.49	2.665	0.507	0.361	2.396	3.204	1.361	-1946.	1049.	13.3	7.497
.400	.0.4	.0.6570	0.1247	0.2180	2.47	2.644	0.493	0.344	2.414	3.188	1.335	-1954.	1039.	13.1	7.390
.400	.0.5	.0.6464	0.1631	0.1669	2.49	2.620	0.469	0.324	2.432	3.150	1.307	-1964.	1023.	12.9	7.246
.400	.0.6	.0.6305	0.2066	0.1293	2.53	2.598	0.441	0.304	2.452	3.090	1.281	-1974.	1012.	12.8	7.143
.400	.0.7	.0.6244	0.2271	0.0944	2.56	2.565	0.418	0.285	2.477	3.041	1.252	-1984.	998.	12.6	7.044
.400	.0.8	.0.6134	0.2449	0.0633	2.59	2.535	0.404	0.266	2.500	2.995	1.211	-1996.	9		

TEMPERATURE = 170. R

Table 26. (cont.)

LIQUID MOLE FRACTION	VAPOR MOLE FRACTION			PRESSURE	EQUIL CONST			RELATIVE VOL	ENTHALPY BTU/LB MOLE			HEAT CAPACITY BTU/LB MOLE-R			
	N2	AR/AR+O2	O2		N2	AR	O2		N2/AR	N2/O2	AR/DR	Liq	Vap		
-0.9	0+	0+	1-0.903	1.53	3.811	1.498	1-0.93	2.414	3.81	1.498	+1745	1133.	13.0	7.546	
-0.1	0.5	0.3886	0.8813	1.60	3.289	1.288	0.997	2.442	3.54	1.450	+1798	1085.	13.6	7.277	
-0.2	0+	0.2801	0.7400	1.67	3.213	1.301	0.929	2.471	3.474	1.400	+1776	1044.	12.7	7.040	
-0.3	0.5	0.2688	0.6813	1.73	3.173	1-0.29	0.902	2.500	3.407	1.363	+1793	1007.	12.5	6.827	
-0.4	0+	0.2484	0.5517	1.78	2.962	1-0.171	0.886	2.529	3.342	1.322	+1811	973.	12.2	6.631	
-0.5	0.5	0.2567	0.4384	1.83	2.877	1-0.123	0.877	2.599	3.279	1.281	+1828	941.	11.9	6.445	
-0.6	0+	0.2659	0.3493	1.87	2.868	1-0.095	0.873	2.599	3.256	1.242	+1846	911.	11.7	6.267	
-0.7	0.5	0.2737	0.2825	1.90	2.785	1-0.04	0.879	2.619	3.185	1.200	+1863	881.	11.4	6.091	
-0.8	0+	0.2826	0.1763	1.94	2.722	1-0.003	0.882	2.680	3.095	1.158	+1881	852.	11.2	5.915	
-0.9	0.5	0.2918	0.0894	1.98	2.713	1-0.001	0.884	2.681	3.036	1.132	+1898	823.	10.9	5.736	
-1.0	0+	0.2932	0+	1.98	2.713	1-0.001	0.884	2.681	3.036	1.132	+1898	823.	10.9	5.736	
-0.95	0+	0.584	0.2173	1.63	3.395	0.980	0.940	2.420	3.575	1.488	+1723	1131.	13.5	7.975	
-0.95	0.1	0.5793	0.1273	1.70	3.173	1-0.38	0.794	2.420	3.509	1.444	+1740	1087.	13.0	7.328	
-0.95	0.2	0.5756	0.2399	1.76	3.023	1-0.28	0.878	2.457	3.443	1.401	+1777	1049.	12.6	7.139	
-0.95	0.3	0.5725	0.3435	1.82	2.902	1-0.18	0.899	2.485	3.379	1.349	+1774	1014.	12.5	6.910	
-0.95	0.4	0.571	0.4322	1.87	2.809	1-0.18	0.865	2.493	3.316	1.319	+1791	985.	12.3	6.726	
-0.95	0.5	0.5682	0.5032	1.90	2.729	1-0.73	0.828	2.543	3.294	1.280	+1818	952.	12.0	6.552	
-0.95	0.6	0.5666	0.5874	1.96	2.670	1-0.38	0.858	2.572	3.194	1.242	+1824	923.	11.8	6.384	
-0.95	0.7	0.5657	0.6894	1.98	2.627	1-0.12	0.881	2.611	3.125	1.205	+1843	898.	11.6	6.215	
-0.95	0.8	0.5650	0.7775	2.02	2.599	0.988	0.845	2.631	3.077	1.169	+1860	868.	11.4	6.093	
-0.95	0.9	0.5644	0.8522	2.03	2.584	0.971	0.856	2.661	3.020	1.139	+1877	841.	11.2	5.889	
-0.95	1.0	0.5645	0.9398	2.07	2.583	0.980	0.872	2.672	3.022	1.122	+1894	813.	10.9	5.712	
-1.00	0+	0.2788	0+	1.93	2.784	1-0.76	0.471	1.498	+1870	1124.	13.4	7.662			
-1.00	0.1	0.2667	0.1003	2.03	2.687	1-0.53	0.789	2.397	3.412	1.426	+1886	1090.	13.2	7.449	
-1.00	0.2	0.2597	0.1914	2.05	2.570	1-0.53	0.788	2.443	3.391	1.387	+1902	1058.	12.9	7.293	
-1.00	0.3	0.2494	0.2792	2.10	2.490	1-0.53	0.756	2.443	3.299	1.349	+1718	1036.	12.7	7.130	
-1.00	0.4	0.2424	0.3586	2.14	2.424	0.982	0.749	2.469	3.209	1.312	+1733	1003.	12.5	6.977	
-1.00	0.5	0.2372	0.4278	2.18	2.372	0.981	0.745	2.495	3.183	1.276	+1749	977.	12.2	6.831	
-1.00	0.6	0.233	0.4991	2.22	2.330	0.984	0.742	2.521	3.128	1.241	+1765	953.	12.0	6.690	
-1.00	0.7	0.2299	0.5685	2.25	2.299	0.982	0.748	2.548	3.075	1.207	+1781	929.	11.8	6.551	
-1.00	0.8	0.2277	0.6369	2.28	2.277	0.985	0.754	2.575	3.022	1.174	+1797	908.	11.6	6.413	
-1.00	0.9	0.2265	0.7052	2.30	2.265	0.973	0.763	2.602	2.970	1.142	+1812	883.	11.4	6.274	
-1.00	1.0	0.2266	0.7741	2.34	2.262	0.982	0.775	2.629	2.921	1.110	+1828	860.	11.2	6.152	
-1.05	0+	0.2485	0+	0.5483	2.52	2.275	0.985	0.882	2.301	3.338	1.438	+1800	1115.	13.5	7.761
-1.05	0.1	0.2445	0.1784	2.58	2.207	0.942	0.872	2.743	3.287	1.403	+1814	1089.	13.3	7.637	
-1.05	0.2	0.2429	0.2486	2.61	2.149	0.909	0.864	2.865	3.236	1.368	+1828	1065.	13.1	7.503	
-1.05	0.3	0.2411	0.3212	2.66	2.100	0.880	0.859	2.887	3.187	1.329	+1842	1043.	12.9	7.377	
-1.05	0.4	0.2391	0.3975	2.70	2.059	0.855	0.856	2.910	3.138	1.302	+1858	1021.	12.7	7.256	
-1.05	0.5	0.2391	0.4353	2.72	2.025	0.833	0.855	2.930	3.098	1.271	+1874	997.	12.5	7.140	
-1.05	0.6	0.2396	0.4970	2.78	1.988	0.814	0.857	2.955	3.043	1.239	+1888	961.	12.3	7.027	
-1.05	0.7	0.2394	0.4467	2.80	1.977	0.795	0.860	2.978	2.997	1.209	+1899	942.	12.1	6.916	
-1.05	0.8	0.2393	0.5118	2.82	1.961	0.784	0.869	2.991	2.959	1.180	+1910	926.	11.9	6.808	
-1.05	0.9	0.2393	0.5866	2.83	1.951	0.773	0.871	2.995	2.956	1.151	+1928	906.	11.7	6.697	
-1.05	1.0	0.2393	0.6513	2.87	1.947	0.784	0.886	2.995	2.954	1.123	+1941	884.	11.5	6.588	
-1.10	0+	0.3792	0+	0.4212	2.68	1.931	0.848	0.804	2.777	3.209	1.410	+1930	1117.	13.7	7.904
-1.10	0.1	0.3669	0.5076	2.76	1.890	0.823	0.897	2.995	3.186	1.380	+1942	1087.	13.5	7.785	
-1.10	0.2	0.3590	0.5744	2.82	2.07	0.942	0.872	2.743	3.287	1.403	+1954	1059.	13.3	7.667	
-1.10	0.3	0.3470	0.6402	2.87	2.141	0.909	0.864	2.865	3.236	1.368	+1968	1035.	13.1	7.533	
-1.10	0.4	0.3421	0.7212	2.93	2.100	0.880	0.859	2.887	3.207	1.327	+1982	1005.	12.9	7.403	
-1.10	0.5	0.3407	0.7977	2.97	2.084	0.871	0.853	2.904	3.184	1.291	+1997	979.	12.7	7.282	
-1.10	0.6	0.3385	0.8737	2.97	2.082	0.871	0.852	2.937	3.182	1.251	+2012	952.	12.5	7.162	
-1.10	0.7	0.3357	0.9474	2.98	2.075	0.873	0.856	2.957	3.141	1.211	+2027	926.	12.3	6.942	
-1.10	0.8	0.3337	0.9877	2.98	2.072	0.873	0.856	2.965	3.139	1.171	+2042	900.	12.1	6.743	
-1.10	0.9	0.3322	0.9795	2.98	2.069	0.873	0.856	2.966	3.138	1.131	+2057	876.	11.9	6.537	
-1.10	1.0	0.3320	0.9877	2.98	2.069	0.873	0.856	2.966	3.138	1.110	+2072	854.	11.7	6.336	
-1.15	0+	0.3792	0+	0.5921	2.88	1.949	0.883	0.804	2.777	3.209	1.450	+1989	1133.	13.7	7.975
-1.15	0.1	0.3739	0.5336	2.93	1.940	0.872	0.804	2.822	3.189	1.321	+2004	1102.	13.5	7.795	
-1.15	0.2	0.3732	0.6081	2.94	1.932	0.854	0.804	2.844	3.187	1.281	+2019	1072.	13.3	7.675	
-1.15	0.3	0.3722	0.6811	2.95	1.924	0.835	0.804	2.865	3.187	1.241	+2034	1042.	13.1	7.553	
-1.15	0.4	0.3716	0.7681	2.96	1.916	0.815	0.804	2.885	3.187	1.201	+2049	1016.	12.9	7.433	
-1.15	0.5	0.3707	0.8518	2.96	1.908	0.795	0.804	2.906	3.186	1.161	+2064	990.	12.7	7.312	
-1.15	0.6	0.3703	0.9284	2.97	1.901	0.776	0.804	2.926	3.185	1.121	+2079	964.	12.5	7.191	
-1.15	0.7	0.3702	0.9966	2.97	1.894	0.756	0.804	2.946	3.184	1.081	+2094	940.	12.3	6.988	
-1.15	0.8	0.3703	0.9666	2.98	1.887	0.736	0.804	2.961	3.184	1.041	+2109	916.	12.1	6.877	
-1.15	0.9	0.3703	0.9336	2.98	1.880	0.716	0.804	2.978	3.183	1.001	+2124	891.	11.9	6.766	
-1.15	1.0	0.3703	0.8998	2.98	1.873	0.696	0.804	2.993	3.183	961.	+2139	868.	11.7	6.655	
-1.20	0+	0.3792	0+	0.5152	2.88	1.951	0.877	0.804	2.785	3.247	1.423	+1980	1102.	13.5	7.975
-1.20	0.1	0.3747	0.5497	2.92	1.944	0.827	0.804	2.817	3.247	1.333	+2				

Table 26. (con't)

LIQUID MOLE FRACTION	VAPOR MOLE FRACTION		PRESSURE	EQUIL CONST	RELATIVE VOL	ENTHALPY BTU/LB MOLE	HEAT CAPACITY BTU/LB MOLE-K						
	N ₂	AR O ₂											
.0.	.0.	.0.	1.0002	1.97	3.381	1.442	1.000	2.312	3.380	1.442	-1674.	1158.	
.1.	0.	0.1362	0.8638	2.048	3.185	1.362	0.999	2.337	3.187	1.419	-1693.	1119.	
.2.	0.	0.2593	0.7429	2.14	3.079	1.281	0.993	2.363	3.096	1.378	-1712.	1087.	
.3.	0.	0.3645	0.6387	2.22	2.992	1.219	0.999	2.389	3.197	1.338	-1730.	1029.	
.4.	0.	0.4442	0.5381	2.28	2.897	1.160	0.993	2.415	3.134	1.299	-1749.	994.	
.5.	0.	0.5379	0.4424	2.34	2.723	1.114	0.989	2.441	3.078	1.261	-1768.	962.	
.6.	0.	0.6177	0.3528	2.39	2.663	1.079	0.982	2.467	3.021	1.224	-1787.	929.	
.7.	0.	0.6735	0.2848	2.43	2.620	1.050	0.983	2.494	2.996	1.189	-1806.	898.	
.8.	0.	0.7122	0.1781	2.47	2.592	1.028	0.990	2.522	2.911	1.154	-1824.	868.	
.9.	0.	0.7410	0.0962	2.50	2.578	1.011	0.992	2.549	2.857	1.121	-1843.	838.	
1.0	0.	0.7600	0.0000	2.53	2.578	1.000	0.999	2.577	2.805	1.108	-1862.	807.	
.025	.0.	0.6770	0.1256	0.921	2.09	3.153	1.374	0.945	2.302	3.246	1.445	-1658.	1159.
.025	.0.1	0.6749	0.1256	0.7997	2.18	2.996	0.911	2.329	3.208	1.413	-1675.	1111.	
.025	.0.2	0.6715	0.2374	0.6914	2.28	2.881	1.217	0.888	2.351	3.228	1.373	-1693.	1071.
.025	.0.3	0.6688	0.3339	0.5926	2.33	2.782	1.159	0.868	2.375	3.170	1.334	-1711.	1035.
.025	.0.4	0.6656	0.4329	0.5000	2.39	2.685	1.110	0.856	2.401	3.113	1.297	-1730.	1002.
.025	.0.5	0.6649	0.5215	0.4139	2.44	2.595	1.079	0.849	2.428	3.096	1.260	-1748.	973.
.025	.0.6	0.6335	0.6165	0.3033	2.49	2.542	1.037	0.847	2.452	3.021	1.224	-1768.	943.
.025	.0.7	0.6420	0.6994	0.2484	2.54	2.503	1.011	0.849	2.476	2.947	1.189	-1787.	912.
.025	.0.8	0.6119	0.7715	0.1669	2.58	2.477	0.980	0.856	2.504	2.894	1.156	-1805.	883.
.025	.0.9	0.5918	0.8542	0.0845	2.61	2.444	0.973	0.867	2.531	2.842	1.123	-1821.	854.
.025	1.0	0.6016	0.9368	0.	2.65	2.443	0.963	0.868	2.558	2.795	1.091	-1839.	829.
.100	.0.	0.2657	0.	0.7347	1.44	2.897	1.171	0.518	2.270	2.254	1.434	-1605.	1148.
.100	.0.1	0.2549	0.1001	0.4493	2.53	2.549	1.117	0.797	2.292	2.200	1.398	-1620.	1122.
.100	.0.2	0.2461	0.1914	0.5630	2.60	2.460	1.063	0.782	2.314	2.147	1.360	-1637.	1080.
.100	.0.3	0.2307	0.2750	0.4866	2.68	2.387	1.021	0.771	2.337	2.094	1.324	-1654.	1050.
.100	.0.4	0.2227	0.3470	0.4242	2.71	2.388	0.988	0.765	2.360	2.042	1.289	-1671.	1021.
.100	.0.5	0.2239	0.4203	0.3274	2.76	2.277	0.958	0.751	2.383	2.092	1.256	-1689.	995.
.100	.0.6	0.2121	0.5733	0.2663	2.85	2.219	0.910	0.764	2.435	2.063	1.219	-1705.	969.
.100	.0.7	0.2199	0.6422	0.1386	2.98	2.199	0.893	0.770	2.454	2.045	1.180	-1738.	920.
.100	.0.8	0.2179	0.7120	0.0701	3.02	2.179	0.869	0.779	2.478	2.019	1.149	-1758.	886.
.100	.0.9	0.2176	0.7820	0.	3.05	2.176	0.870	0.781	2.502	2.072	1.105	-1778.	856.
.200	.0.	0.4395	0.	0.5110	2.02	2.197	0.988	0.781	2.228	2.133	1.497	-1593.	1137.
.200	.0.1	0.4266	0.0759	0.4975	2.08	2.133	0.949	0.691	2.247	2.087	1.374	-1547.	1110.
.200	.0.2	0.4150	0.1468	0.4379	2.13	2.079	0.917	0.684	2.268	2.041	1.342	-1562.	1084.
.200	.0.3	0.4066	0.2134	0.3808	2.18	2.033	0.889	0.679	2.288	2.006	1.311	-1577.	1051.
.200	.0.4	0.3969	0.2748	0.3244	2.23	2.004	0.854	0.665	2.305	2.008	1.288	-1592.	1038.
.200	.0.5	0.3925	0.3375	0.2700	2.27	1.963	0.844	0.679	2.326	2.008	1.259	-1607.	1017.
.200	.0.6	0.3874	0.3963	0.2164	2.32	1.937	0.826	0.676	2.346	2.005	1.221	-1622.	998.
.200	.0.7	0.3714	0.4536	0.1633	2.35	1.917	0.810	0.679	2.367	2.022	1.193	-1637.	975.
.200	.0.8	0.3635	0.5101	0.1095	2.39	1.903	0.797	0.684	2.387	2.071	1.165	-1652.	956.
.200	.0.9	0.3587	0.5661	0.0953	2.42	1.893	0.785	0.691	2.408	2.140	1.138	-1667.	936.
.200	1.0	0.3779	0.6222	0.	2.45	1.889	0.778	0.705	2.429	2.199	1.111	-1682.	916.
.300	.0.	0.5639	0.	0.4361	2.36	1.888	0.800	0.623	2.186	2.017	1.350	-1461.	1127.
.300	.0.1	0.5592	0.0585	0.3694	2.41	1.841	0.826	0.618	2.203	2.078	1.392	-1475.	1106.
.300	.0.2	0.5419	0.1138	0.3442	2.48	1.808	0.814	0.615	2.220	2.030	1.324	-1488.	1086.
.300	.0.3	0.5331	0.1669	0.3002	2.53	1.777	0.795	0.613	2.236	2.001	1.297	-1501.	1067.
.300	.0.4	0.5235	0.2177	0.2569	2.53	1.752	0.777	0.612	2.253	2.083	1.271	-1514.	1049.
.300	.0.5	0.5191	0.2607	0.2143	2.57	1.731	0.752	0.612	2.271	2.050	1.245	-1528.	1030.
.300	.0.6	0.5130	0.3144	0.1719	2.61	1.711	0.729	0.614	2.288	2.028	1.219	-1540.	1014.
.300	.0.7	0.5059	0.3616	0.1295	2.64	1.686	0.707	0.617	2.305	2.000	1.194	-1553.	998.
.300	.0.8	0.5003	0.4269	0.0869	2.67	1.662	0.687	0.621	2.323	1.976	1.170	-1567.	981.
.300	.0.9	0.504	0.4922	0.0438	2.71	1.640	0.668	0.621	2.349	1.956	1.146	-1580.	965.
.300	1.0	0.5027	0.5474	0.	2.74	1.625	0.653	0.621	2.375	1.936	1.122	-1593.	949.
.400	.0.	0.6595	0.	0.3406	2.78	1.644	0.768	0.568	2.146	2.005	1.354	-1393.	1117.
.400	.0.1	0.6497	0.0491	0.3193	2.82	1.602	0.732	0.569	2.160	2.072	1.330	-1403.	1106.
.400	.0.2	0.6449	0.0845	0.2760	2.86	1.582	0.717	0.564	2.174	2.044	1.307	-1413.	1085.
.400	.0.3	0.6332	0.1302	0.2367	2.90	1.563	0.704	0.564	2.188	2.020	1.284	-1424.	1070.
.400	.0.4	0.6244	0.1707	0.2030	2.93	1.546	0.689	0.554	2.202	2.000	1.261	-1438.	1055.
.400	.0.5	0.6216	0.2168	0.1699	2.96	1.522	0.672	0.550	2.216	1.974	1.239	-1450.	1041.
.400	.0.6	0.6157	0.2444	0.1369	2.99	1.509	0.650	0.547	2.231	1.956	1.218	-1464.	1022.
.400	.0.7	0.6116	0.2849	0.1025	3.02	1.492	0.631	0.549	2.249	1.936	1.196	-1479.	1005.
.400	.0.8	0.6084	0.3220	0.0687	3.05	1.471	0.612	0.547	2.266	1.916	1.175	-1491.	988.
.400	.0.9	0.6059	0.3596	0.0346	3.08	1.451	0.592	0.546	2.285	1.896	1.155	-1503.	972.
.400	1.0	0.6043	0.3959	0.	3.11	1.431	0.572	0.545	2.302	1.876	1.135	-1514.	955.
.500	.0.	0.7307	0.	0.2634	2.81	1.473	0.570	0.527	2.108	2.087	1.328	-1370.	1109.
.500	.0.1	0.7259	0.0344	0.2366	2.83	1.458	0.549	0.496	2.177	2.050	1.307	-1389.	1094.
.500	.0.2	0.7219	0.0676	0.2104	2.88	1.444	0.528	0.474	2.192	2.024	1.288	-1404.	1073.
.500	.0.3	0.7157	0.1003	0.1942	2.92	1.431	0.509	0.454	2.202	2.001	1.271	-1424.	1054.
.500	.0.4	0.7111	0.1320	0.1581	2.95	1.420	0.489	0.432	2.214	1.980	1.250	-1438.	1034.
.500	.0.5	0.7051	0.1633	0.1323	2.98	1.411	0.472	0.412	2.227	1.959	1.229	-1453.	1014.
.500	.0.6	0.7019	0.1933	0.1060	3.02	1.397	0.459	0.398	2.243	1.938	1.209	-1468.	998.
.500	.0.7	0.6972	0.2232	0.0798	3.04	1.384	0.439	0.389	2.257	1.920	1.188	-1484.	982.
.500	.0.8	0.6942	0.2525	0.0535	3.07	1.374	0.421	0.380	2.271	1.902	1.167	-1	

Table 26. (cont.)

LIQUID MOLE FRACTION		VAPOR MOLE FRACTION		PRESSURE		EQUIL CONST.		RELATIVE VOL.		ENTHALPY BTU/LB MOLE		HEAT CAPACITY BTU/LB MOLE-R	
N ₂	AR/AR+O ₂	N ₂	AR	O ₂	ATM	N ₂	AR	O ₂	N ₂ /AR	N ₂ /O ₂	AR/O ₂	Liq	Vap
+	0+	0+	0+	1.163	2.51	3.176	1.432	1.202	2.214	3.189	1.431	+1608.	1183.
+	0.1	0.134	0.8654	3.63	2.984	1.142	0.963	0.236	3.112	1.392	+1628.	1132.	
+	0.2	0.174	0.828	0.7479	2.72	2.854	1.284	0.954	2.299	3.056	1.353	+1447.	1088.
+	0.3	0.206	0.766	0.5388	2.86	2.743	1.202	0.914	2.282	3.001	1.319	+1667.	1049.
+	0.4	0.240	0.6894	0.5402	2.98	2.652	1.152	0.920	2.305	2.947	1.279	+1687.	1013.
+	0.5	0.274	0.5948	0.4442	2.95	2.581	1.109	0.892	2.328	2.994	1.243	+1707.	978.
+	0.6	0.306	0.4848	0.3946	3.01	2.527	1.079	0.859	2.355	2.942	1.209	+1727.	946.
+	0.7	0.331	0.3731	0.2473	3.04	2.488	1.047	0.891	2.375	2.791	1.175	+1747.	914.
+	0.8	0.352	0.2809	0.1798	3.11	2.452	1.024	0.859	2.395	2.742	1.143	+1767.	882.
+	0.9	0.370	0.1949	0.0937	3.15	2.449	1.011	0.912	2.494	2.693	1.111	+1787.	851.
+	1.0	0.385	0.1005	0.0000	7.18	2.449	1.003	0.926	2.448	2.645	1.100	+1807.	816.
-0.95	0+	0.748	0+	0.998	2.65	2.982	1.353	0.955	2.205	3.141	1.428	+1600.	1179.
-0.95	0.1	0.870	0.1241	0.8095	2.78	2.832	1.273	0.918	2.298	3.086	1.386	+1659.	1133.
-0.95	0.2	0.878	0.2255	0.8979	2.85	2.730	1.206	0.898	2.248	3.13	1.348	+1628.	1092.
-0.95	0.3	0.865	0.3386	0.5986	2.93	2.612	1.151	0.877	2.270	2.978	1.312	+1648.	1059.
-0.95	0.4	0.833	0.4368	0.5053	3.01	2.572	1.105	0.865	2.292	2.928	1.276	+1667.	1029.
-0.95	0.5	0.817	0.5020	0.4187	3.08	2.469	1.087	0.859	2.315	2.874	1.242	+1687.	988.
-0.95	0.6	0.760	0.5856	0.3342	3.14	2.420	1.038	0.867	2.342	2.824	1.208	+1708.	957.
-0.95	0.7	0.696	0.6892	0.2513	3.19	2.384	1.010	0.859	2.365	2.775	1.175	+1729.	928.
-0.95	0.8	0.619	0.7723	0.1868	3.23	2.346	0.978	0.866	2.384	2.727	1.144	+1749.	898.
-0.95	0.9	0.546	0.895	0.0855	3.27	2.346	0.978	0.876	2.447	2.670	1.113	+1764.	868.
-0.95	1.0	0.567	0.914	0.0000	3.75	2.347	0.985	0.892	2.451	2.631	1.083	+1784.	835.
-0.95	0+	0.595	0.945	0.0000	3.80	2.348	0.985	0.892	2.451	2.631	1.083	+1784.	835.
-0.95	0.1	0.543	0.9498	0.0000	3.85	2.349	1.168	0.830	2.179	3.056	1.405	+1536.	1149.
-0.95	0.2	0.534	0.914	0.5732	3.87	2.394	1.103	0.815	2.199	3.026	1.377	+1554.	1132.
-0.95	0.3	0.522	0.7873	0.4695	3.92	2.386	1.028	0.796	2.24	2.997	1.335	+1572.	1098.
-0.95	0.4	0.512	0.681	0.3573	3.98	2.372	1.015	0.786	2.292	2.904	1.302	+1589.	1067.
-0.95	0.5	0.501	0.5856	0.2513	4.04	2.349	1.007	0.779	2.315	2.874	1.262	+1607.	1026.
-0.95	0.6	0.489	0.4992	0.2513	4.19	2.344	1.000	0.776	2.342	2.824	1.208	+1628.	988.
-0.95	0.7	0.476	0.4189	0.1868	4.24	2.344	0.997	0.776	2.347	2.824	1.175	+1647.	957.
-0.95	0.8	0.464	0.3274	0.1211	4.27	2.345	0.995	0.776	2.351	2.818	1.147	+1667.	923.
-0.95	0.9	0.452	0.2155	0.0714	4.34	2.345	0.995	0.785	2.359	2.830	1.119	+1687.	891.
-0.95	1.0	0.440	0.1692	0.0000	4.57	2.342	0.995	0.785	2.361	2.830	1.103	+1707.	859.
-0.95	0+	0.421	0.1579	0.0000	4.62	2.341	0.993	0.782	2.362	2.830	1.103	+1727.	829.
-0.95	0.1	0.412	0.0768	0.5152	4.70	2.301	0.987	0.716	2.154	2.533	1.348	+1495.	1129.
-0.95	0.2	0.402	0.1482	0.4497	4.76	2.311	0.986	0.703	2.171	2.548	1.318	+1514.	1106.
-0.95	0.3	0.393	0.1918	0.3397	4.81	2.308	0.989	0.699	2.188	2.522	1.289	+1532.	1074.
-0.95	0.4	0.386	0.2820	0.3336	4.86	2.302	0.978	0.695	2.205	2.582	1.266	+1551.	1043.
-0.95	0.5	0.383	0.3892	0.2777	4.92	2.292	0.959	0.684	2.234	2.740	1.232	+1569.	1013.
-0.95	0.6	0.3755	0.4071	0.2225	4.98	2.278	0.938	0.679	2.242	2.750	1.205	+1599.	989.
-0.95	0.7	0.3718	0.4867	0.1678	5.03	2.265	0.919	0.674	2.269	2.769	1.178	+1597.	957.
-0.95	0.8	0.3691	0.5189	0.1111	5.07	2.245	0.895	0.673	2.278	2.682	1.147	+1617.	926.
-0.95	0.9	0.3574	0.5769	0.0588	5.11	2.237	0.873	0.672	2.289	2.596	1.117	+1637.	895.
-0.95	1.0	0.3466	0.6335	0.0000	5.15	2.233	0.872	0.672	2.298	2.596	1.102	+1657.	865.
-0.95	0+	0.3493	0.6451	0.0000	5.18	2.233	0.872	0.672	2.305	2.595	1.102	+1677.	835.
-0.95	0.1	0.3379	0.6594	0.0000	5.21	2.211	0.849	0.659	2.113	2.894	1.327	+1408.	1123.
-0.95	0.2	0.3282	0.6158	0.0000	5.26	2.186	0.827	0.628	2.129	2.769	1.301	+1420.	1102.
-0.95	0.3	0.3198	0.5198	0.0000	5.31	2.171	0.796	0.596	2.143	2.734	1.278	+1442.	1082.
-0.95	0.4	0.3112	0.4227	0.0000	5.36	2.162	0.766	0.565	2.156	2.704	1.251	+1468.	1063.
-0.95	0.5	0.3035	0.2714	0.0000	5.41	2.153	0.737	0.535	2.169	2.675	1.224	+1495.	1044.
-0.95	0.6	0.2955	0.1878	0.0000	5.46	2.143	0.706	0.505	2.182	2.646	1.197	+1522.	1024.
-0.95	0.7	0.2875	0.1347	0.0000	5.51	2.134	0.676	0.475	2.195	2.617	1.170	+1549.	1004.
-0.95	0.8	0.2794	0.0898	0.0000	5.56	2.125	0.646	0.445	2.206	2.588	1.140	+1571.	984.
-0.95	0.9	0.2715	0.0449	0.0000	5.61	2.116	0.616	0.415	2.217	2.559	1.110	+1599.	964.
-0.95	1.0	0.2641	0.0000	0.0000	5.66	2.107	0.586	0.385	2.228	2.529	1.080	+1617.	934.
-0.95	0+	0.2642	0.0000	0.0000	5.71	2.100	0.556	0.355	2.239	2.500	1.050	+1637.	904.
-0.95	0.1	0.2562	0.0363	0.2470	5.75	2.092	0.526	0.324	2.258	2.478	1.020	+1657.	874.
-0.95	0.2	0.2471	0.1741	0.4442	5.81	2.082	0.496	0.294	2.278	2.448	1.000	+1677.	844.
-0.95	0.3	0.2384	0.3094	0.2855	5.87	2.074	0.467	0.264	2.298	2.418	1.000	+1697.	814.
-0.95	0.4	0.2306	0.1747	0.2110	5.92	2.065	0.436	0.234	2.318	2.388	1.000	+1717.	784.
-0.95	0.5	0.2231	0.1332	0.2491	5.98	2.052	0.406	0.204	2.338	2.358	1.000	+1737.	754.
-0.95	0.6	0.2151	0.0912	0.1781	6.03	2.042	0.373	0.174	2.358	2.328	1.000	+1757.	724.
-0.95	0.7	0.2071	0.0516	0.1781	6.08	2.032	0.343	0.144	2.378	2.308	1.000	+1777.	694.
-0.95	0.8	0.1992	0.0156	0.1781	6.13	2.022	0.313	0.114	2.398	2.288	1.000	+1797.	664.
-0.95	0.9	0.1913	0.0000	0.0000	6.18	2.013	0.283	0.084	2.418	2.268	1.000	+1817.	634.
-0.95	1.0	0.1834	0.0000	0.0000	6.23	2.004	0.253	0.054	2.438	2.248	1.000	+1837.	604.
-0.95	0+	0.1835	0.0000	0.0000	6.28	1.995	0.223	0.024	2.458	2.228	1.000	+1857.	574.
-0.95	0.1	0.1751	0.2743	0.1879	6.33	1.986	0.193	0.094	2.478	2.208	1.000	+1877.	544.
-0.95	0.2	0.1662	0.1524	0.3732	6.38	1.977	0.163	0.064	2.498	2.188	1.000	+1897.	514.
-0.95	0.3	0.1574	0.0918	0.5621	6.43	1.968	0.133	0.034	2.518	2.168	1.000	+1917.	484.
-0.95	0.4	0.1484	0.0444	0.7517	6.48	1.959	0.103	0.004	2.538	2.148	1.000	+1937.	454.
-0.95	0.5	0.1393	0.0000	0.0000	6.53	1.949	0.073	0.004	2.558	2.128	1.000	+1957.	424.
-0.9													

LIQUID MOLE FRACTION	VAPOR MOLE FRACTION			PRESSURE	EQUIL CONST			RELATIVE VOL			ENTHALPY		HEAT CAPACITY			
	N2	AR	AR/AR+O2		N2	AR	O2	N2/AR	N2/O2	AR/O2	L10	VAP	L10	VAP		
+	0.	0.	0.	1.0005	3.15	2.977	1.404	2.120	2.975	1.404	+1541.	1263.	13.4	7.936		
+	0.1	0.	0.1318	0.8662	3.28	2.820	1.318	0.995	2.142	2.923	1.326	+1562.	1152.	13.2	7.686	
+	0.2	0.	0.2495	0.7595	3.40	2.694	1.248	0.938	2.159	2.872	1.330	+1583.	1107.	13.0	7.445	
+	0.3	0.	0.3569	0.6432	3.50	2.593	1.193	0.919	2.179	2.822	1.295	+1604.	1087.	12.8	7.283	
+	0.4	0.	0.4556	0.5434	3.60	2.511	1.142	0.895	2.205	2.772	1.246	+1624.	1029.	12.6	7.173	
+	0.5	0.	0.5510	0.4491	3.68	2.447	1.084	0.869	2.220	2.724	1.227	+1645.	994.	12.4	6.892	
+	0.6	0.	0.6418	0.3592	3.75	2.397	1.027	0.836	2.241	2.677	1.194	+1666.	965.	12.3	6.714	
+	0.7	0.	0.7307	0.2693	3.81	2.361	0.944	0.806	2.262	2.630	1.163	+1687.	927.	12.1	6.538	
+	0.8	0.	0.8192	0.1809	3.87	2.338	0.864	0.769	2.285	2.595	1.132	+1708.	894.	11.9	6.386	
+	0.9	0.	0.8985	0.0916	3.91	2.326	0.804	0.716	2.305	2.545	1.102	+1729.	861.	11.7	6.177	
+	1.0	0.	1.0001	0.	3.95	2.326	0.730	0.632	2.328	2.494	1.073	+1752.	828.	11.5	5.986	
-.25	0.	0.073	0.	0.9287	3.32	2.812	1.332	0.954	2.111	2.849	1.397	+1823.	1199.	13.4	7.978	
-.25	0.1	0.	0.869	0.1226	0.8165	3.44	2.676	1.297	0.924	2.298	2.994	1.361	+1843.	1152.	13.2	7.747
-.25	0.2	0.	0.842	0.2333	0.7029	3.59	2.568	1.195	0.901	2.149	2.849	1.326	+1863.	1119.	13.0	7.541
-.25	0.3	0.	0.820	0.3342	0.6139	3.65	2.478	1.143	0.885	2.169	2.801	1.291	+1884.	1072.	12.9	7.351
-.25	0.4	0.	0.811	0.4287	0.5112	3.74	2.400	1.099	0.874	2.188	2.793	1.258	+1904.	1034.	12.7	7.172
-.25	0.5	0.	0.807	0.5184	0.4230	3.82	2.348	1.053	0.868	2.205	2.768	1.225	+1924.	992.	12.5	7.000
-.25	0.6	0.	0.8076	0.4048	0.3377	3.89	2.304	1.034	0.866	2.225	2.686	1.194	+1945.	970.	12.4	6.883
-.25	0.7	0.	0.806	0.6869	0.2540	3.96	2.271	1.012	0.866	2.249	2.615	1.163	+1965.	939.	12.2	6.666
-.25	0.8	0.	0.802	0.7732	0.1764	4.01	2.249	0.991	0.875	2.269	2.571	1.133	+1985.	907.	12.0	6.497
-.25	0.9	0.	0.800	0.8570	0.0833	4.06	2.238	0.978	0.885	2.290	2.524	1.104	+2005.	876.	11.8	6.325
-.25	1.0	0.	0.959	0.9481	0.	4.19	2.238	0.968	0.900	2.311	2.485	1.079	+2126.	845.	11.7	6.145
.00	0.	0.2419	0.	0.7581	3.81	2.419	1.181	0.842	2.084	2.872	1.374	+1465.	1189.	13.6	8.108	
.00	0.1	0.	0.2329	0.8998	0.6674	3.92	2.329	1.158	0.824	2.101	2.827	1.347	+1487.	1151.	13.5	7.926
.00	0.2	0.	0.2254	0.1915	0.5933	4.02	2.284	1.084	0.810	2.139	2.782	1.313	+1505.	1116.	13.3	7.757
.00	0.3	0.	0.2191	0.2749	0.5491	4.11	2.191	1.026	0.800	2.158	2.738	1.282	+1524.	1083.	13.1	7.599
.00	0.4	0.	0.2139	0.3579	0.4266	4.19	2.139	0.993	0.794	2.194	2.695	1.251	+1543.	1053.	13.0	7.448
.00	0.5	0.	0.2098	0.4345	0.3394	4.26	2.098	0.966	0.784	2.172	2.655	1.221	+1562.	1023.	12.8	7.302
.00	0.6	0.	0.2055	0.5059	0.2946	4.32	2.045	0.943	0.761	2.141	2.611	1.193	+1580.	995.	12.6	7.159
.00	0.7	0.	0.2045	0.5918	0.2143	4.38	2.040	0.924	0.749	2.169	2.571	1.164	+1599.	968.	12.5	7.017
.00	0.8	0.	0.2023	0.6539	0.1430	4.43	2.023	0.898	0.800	2.208	2.535	1.136	+1618.	941.	12.3	6.875
.00	0.9	0.	0.2014	0.7246	0.0727	4.48	2.014	0.868	0.808	2.248	2.491	1.109	+1637.	915.	12.2	6.729
.00	1.0	0.	0.2011	0.7990	0.	4.52	2.011	0.838	0.800	2.265	2.452	1.083	+1656.	886.	12.0	6.580
.00	0.	0.2000	0.	0.8567	0.	4.55	2.047	0.899	0.758	2.048	2.772	1.353	+1393.	1175.	13.8	8.295
.00	0.1	0.	0.3903	0.8772	0.5246	4.64	1.992	0.965	0.729	2.084	2.733	1.325	+1411.	1145.	13.6	8.198
.00	0.2	0.	0.3800	0.1486	0.4617	4.82	1.944	0.935	0.721	2.079	2.695	1.296	+1428.	1118.	13.4	8.027
.00	0.3	0.	0.3808	0.2382	0.3412	4.91	1.904	0.895	0.712	2.100	2.662	1.262	+1445.	1082.	13.2	7.932
.00	0.4	0.	0.3740	0.3236	0.2426	4.75	1.870	0.868	0.714	2.110	2.626	1.232	+1461.	1057.	13.0	7.782
.00	0.5	0.	0.3664	0.3466	0.2052	4.82	1.842	0.837	0.713	2.128	2.594	1.214	+1478.	1043.	13.2	7.665
.00	0.6	0.	0.3639	0.4070	0.2289	4.88	1.819	0.802	0.714	2.141	2.546	1.190	+1495.	1022.	13.0	7.549
.00	0.7	0.	0.3614	0.4677	0.1721	4.92	1.802	0.835	0.717	2.157	2.512	1.165	+1511.	997.	12.8	7.439
.00	0.8	0.	0.3578	0.5248	0.1159	4.99	1.781	0.823	0.723	2.171	2.477	1.146	+1528.	975.	12.7	7.320
.00	0.9	0.	0.3562	0.5857	0.0503	5.03	1.761	0.813	0.729	2.190	2.443	1.124	+1545.	953.	12.6	7.204
.00	1.0	0.	0.3595	0.6447	0.	5.07	1.778	0.805	0.738	2.195	2.419	1.102	+1562.	931.	12.5	7.088
.00	0.	0.3533	0.	0.6553	5.08	1.781	0.808	0.688	2.212	2.378	1.089	+1581.	908.	12.4	6.968	
.00	0.1	0.	0.3523	0.0603	0.4161	5.13	1.748	0.862	0.641	2.194	2.443	1.054	+1600.	888.	12.3	6.849
.00	0.2	0.	0.3514	0.1177	0.3676	5.20	1.713	0.841	0.617	2.145	2.695	1.245	+1611.	860.	12.2	6.729
.00	0.3	0.	0.3506	0.1728	0.3209	5.26	1.689	0.823	0.605	2.155	2.597	1.216	+1631.	840.	12.0	6.608
.00	0.4	0.	0.3499	0.2258	0.2747	5.32	1.650	0.804	0.584	2.165	2.547	1.183	+1650.	819.	11.9	6.490
.00	0.5	0.	0.3494	0.2772	0.2291	5.38	1.647	0.792	0.564	2.182	2.516	1.153	+1668.	795.	11.7	6.394
.00	0.6	0.	0.3483	0.3273	0.1937	5.43	1.631	0.779	0.556	2.193	2.485	1.127	+1687.	776.	11.6	6.294
.00	0.7	0.	0.3465	0.3764	0.1344	5.48	1.610	0.768	0.549	2.208	2.455	1.104	+1704.	756.	11.5	6.197
.00	0.8	0.	0.3426	0.4248	0.0929	5.52	1.601	0.759	0.543	2.212	2.425	1.084	+1720.	736.	11.4	6.107
.00	0.9	0.	0.3406	0.4729	0.0468	5.57	1.592	0.751	0.535	2.222	2.396	1.064	+1737.	716.	11.3	6.034
.00	1.0	0.	0.3479	0.5200	0.	5.61	1.595	0.744	0.527	2.238	2.367	1.042	+1757.	695.	11.2	5.934
.00	0.	0.3428	0.	0.3675	5.66	1.592	0.708	0.513	2.252	2.338	1.015	+1775.	674.	11.1	5.824	
.00	0.1	0.	0.3423	0.3245	0.	5.72	1.559	0.785	0.510	2.272	2.305	1.085.	+1795.	654.	11.0	5.710
.00	0.2	0.	0.3420	0.3974	0.3245	5.74	1.534	0.741	0.502	2.281	2.284	1.041.	+1815.	636.	10.9	5.629
.00	0.3	0.	0.3419	0.4572	0.2922	5.77	1.504	0.714	0.490	2.291	2.284	+1831.	617.	10.8	5.540	
.00	0.4	0.	0.3414	0.5254	0.	5.82	1.492	0.705	0.480	2.312	2.252	+1851.	597.	10.7	5.452	
.00	0.5	0.	0.3402	0.1977	0.2190	5.87	1.477	0.745	0.472	2.327	2.224	+1871.	578.	10.6	5.365	
.00	0.6	0.	0.3392	0.2202	0.1248	5.92	1.459	0.724	0.464	2.340	2.196	+1891.	559.	10.5	5.276	
.00	0.7	0.	0.3384	0.2850	0.0404	5.98	1.439	0.705	0.456	2.357	2.167	+1911.	540.	10.4	5.187	
.00	0.8	0.	0.3375	0.1590	0.0870	6										

Table 26. (cont.)

LIQUID MOLE FRACTION		VAPOR MOLE FRACTION		PRESSURE		EQUIL CONST			RELATIVE VOL		ENTHALPY STU/LB MOLE		HEAT CAPACITY STU/LB MOLE-R		
N2	Ar	N2	Ar	O2	AIR	N2	Ar	O2	N2/Ar	N2/O2	Ar/O2	Liq	Vap	Liq	Vap
* 0.0	0.0	0.0	0.0	1.0000	3.90	2.796	1.378	1.000	2.030	2.796	1.378	+1474.	1222.	13.4	8.102
* 0.1	0.0	0.1200	0.8799	4.16	2.698	1.298	0.987	2.947	2.740	1.343	+1496.	1171.	13.3	7.864	
* 0.2	0.0	0.2440	0.7536	4.27	2.545	1.233	0.942	2.949	2.702	1.309	+1517.	1129.	13.1	7.650	
* 0.3	0.0	0.3535	0.6465	4.32	2.453	1.178	0.924	2.942	2.652	1.275	+1539.	1083.	13.0	7.453	
* 0.4	0.0	0.4532	0.5465	4.43	2.380	1.133	0.911	2.918	2.621	1.243	+1561.	1044.	12.8	7.266	
* 0.5	0.0	0.5479	0.4429	4.53	2.321	1.086	0.904	2.811	2.536	1.205	+1583.	1008.	12.6	7.087	
* 0.6	0.0	0.6393	0.3489	4.61	2.276	1.045	0.892	2.723	2.425	1.181	+1604.	972.	12.5	6.911	
* 0.7	0.0	0.7288	0.2413	4.69	2.244	1.004	0.884	2.619	2.341	1.151	+1626.	938.	12.3	6.735	
* 0.8	0.0	0.8179	0.1422	4.75	2.222	0.962	0.871	2.517	2.249	1.122	+1648.	904.	12.2	6.557	
* 0.9	0.0	0.8979	0.0422	4.80	2.212	0.909	0.922	2.192	2.398	1.094	+1669.	870.	12.0	6.373	
* 1.0	0.0	1.0000	0.0	4.84	2.202	0.955	0.955	2.211	2.358	1.088	+1691.	835.	11.8	6.181	
* .025	0.0	0.0584	0.0	0.633	4.15	2.855	1.153	0.958	2.021	2.772	1.372	+1455.	1216.	13.5	8.152
* .025	0.1	0.0533	0.1212	0.6155	4.25	2.534	1.243	0.929	2.028	2.726	1.338	+1477.	1179.	13.3	7.931
* .025	0.2	0.0509	0.2310	0.7083	4.38	2.434	1.185	0.908	2.055	2.681	1.305	+1498.	1127.	13.2	7.730
* .025	0.3	0.0500	0.3321	0.8091	4.50	2.353	1.136	0.883	2.072	2.637	1.272	+1529.	1088.	13.0	7.544
* .025	0.4	0.0472	0.4229	0.8160	4.60	2.287	1.095	0.862	2.090	2.593	1.241	+1550.	1051.	12.9	7.358
* .025	0.5	0.0459	0.5170	0.8427	4.70	2.239	1.051	0.878	2.107	2.550	1.200	+1581.	1016.	12.7	7.188
* .025	0.6	0.0449	0.6041	0.8412	4.78	2.194	1.033	0.884	2.125	2.508	1.180	+1592.	982.	12.6	7.031
* .025	0.7	0.0434	0.6894	0.8964	4.85	2.164	1.010	0.897	2.143	2.497	1.153	+1604.	949.	12.4	6.885
* .025	0.8	0.0426	0.7742	0.8724	4.92	2.145	0.993	0.904	2.161	2.427	1.123	+1629.	917.	12.3	6.696
* .025	0.9	0.0414	0.8596	0.8072	4.97	2.135	0.980	0.894	2.179	2.387	1.099	+1648.	884.	12.1	6.522
* 1.0	0.0	0.0333	0.9400	0.8000	5.03	2.124	0.971	0.909	2.197	2.358	1.077	+1667.	852.	12.0	6.351
* 1.00	0.0	0.2239	0.9	0.7682	4.67	2.309	1.197	0.895	1.997	2.702	1.389	+1699.	1200.	13.7	8.394
* 1.00	0.1	0.2227	0.9096	0.8779	4.79	2.277	1.167	0.887	2.012	2.641	1.352	+1719.	1187.	13.6	8.127
* 1.00	0.2	0.2157	0.8799	0.9395	4.91	2.197	1.064	0.823	2.027	2.620	1.292	+1748.	1133.	13.5	7.982
* 1.00	0.3	0.2100	0.8275	0.9517	5.01	2.100	1.028	0.814	2.043	2.568	1.235	+1769.	1097.	13.3	7.866
* 1.00	0.4	0.2052	0.3488	0.9436	5.11	2.048	0.997	0.808	2.059	2.541	1.234	+1787.	1069.	13.2	7.688
* 1.00	0.5	0.2013	0.4367	0.9361	5.19	2.013	0.970	0.805	2.078	2.502	1.208	+1807.	1035.	13.0	7.533
* 1.00	0.6	0.1983	0.5122	0.9267	5.27	1.983	0.948	0.805	2.091	2.464	1.178	+1826.	997.	12.9	7.228
* 1.00	0.7	0.1963	0.5881	0.9181	5.34	1.960	0.920	0.806	2.107	2.426	1.152	+1846.	959.	12.8	7.025
* 1.00	0.8	0.1944	0.6593	0.9146	5.41	1.944	0.916	0.814	2.123	2.399	1.125	+1867.	921.	12.5	6.898
* 1.00	0.9	0.1930	0.7327	0.9070	5.45	1.936	0.905	0.802	2.140	2.359	1.100	+1887.	883.	12.4	6.785
* 1.00	1.0	0.1933	0.8049	0.9000	5.50	1.933	0.897	0.809	2.157	2.326	1.079	+1909.	853.	12.3	6.678
* 1.00	0.0	0.3951	0.	0.6551	5.60	1.979	1.040	0.795	1.964	2.512	1.330	+1929.	1200.	13.7	8.394
* 1.00	0.1	0.3847	0.0778	0.5377	5.65	1.924	0.973	0.747	1.977	2.576	1.303	+1942.	1180.	13.6	8.152
* 1.00	0.2	0.3759	0.1518	0.4734	5.70	1.879	0.944	0.714	2.041	2.541	1.274	+1959.	1133.	13.5	8.037
* 1.00	0.3	0.3683	0.2205	0.4115	5.75	1.842	0.916	0.678	2.053	2.506	1.250	+1977.	1089.	13.4	8.298
* 1.00	0.4	0.3624	0.2866	0.3514	5.77	1.800	0.897	0.732	2.014	2.472	1.222	+1994.	1054.	13.3	8.136
* 1.00	0.5	0.3567	0.3511	0.2925	5.84	1.764	0.878	0.735	2.032	2.438	1.203	+2012.	1023.	13.2	8.017
* 1.00	0.6	0.3525	0.4134	0.2344	5.91	1.726	0.852	0.733	2.046	2.405	1.178	+2029.	988.	13.0	7.901
* 1.00	0.7	0.3492	0.4746	0.1765	5.98	1.746	0.827	0.738	2.050	2.373	1.152	+2046.	954.	12.9	7.786
* 1.00	0.8	0.3468	0.5355	0.1185	6.04	1.734	0.805	0.741	2.074	2.341	1.129	+2064.	921.	12.8	7.671
* 1.00	0.9	0.3453	0.5959	0.0598	6.09	1.727	0.802	0.747	2.089	2.310	1.106	+2081.	886.	12.7	7.556
* 1.00	1.0	0.3447	0.6556	0.	6.13	1.723	0.820	0.756	2.103	2.279	1.084	+2102.	850.	12.6	7.438
* 1.00	0.	0.3193	0.8049	0.5552	6.17	1.691	0.860	0.765	2.051	2.152	1.055	+2122.	813.	12.5	7.318
* 1.00	0.1	0.4465	0.	0.6145	6.21	1.733	0.859	0.887	1.992	2.524	1.308	+2145.	1191.	14.1	8.522
* 1.00	0.2	0.5000	0.6112	0.4293	6.26	1.699	0.874	0.881	2.043	2.494	1.283	+2162.	1160.	14.0	8.454
* 1.00	0.3	0.5011	0.6196	0.3706	6.37	1.670	0.845	0.854	2.056	2.464	1.262	+2180.	1128.	14.0	8.395
* 1.00	0.4	0.5030	0.6197	0.3311	6.38	1.645	0.827	0.837	2.067	2.435	1.238	+2198.	1106.	14.1	8.348
* 1.00	0.5	0.4971	0.6226	0.2835	6.42	1.624	0.802	0.819	2.079	2.406	1.216	+2214.	1084.	14.0	8.294
* 1.00	0.6	0.4917	0.6204	0.2364	6.48	1.606	0.807	0.819	2.090	2.385	1.196	+2231.	1064.	14.0	8.231
* 1.00	0.7	0.4772	0.6337	0.1995	6.55	1.591	0.784	0.794	2.090	2.377	1.174	+2248.	1044.	13.9	8.171
* 1.00	0.8	0.4733	0.6406	0.1428	6.60	1.579	0.764	0.802	2.092	2.349	1.153	+2265.	1023.	13.8	8.109
* 1.00	0.9	0.4699	0.6482	0.0403	6.67	1.573	0.759	0.804	2.093	2.306	1.132	+2282.	999.	13.7	7.993
* 1.00	1.0	0.4612	0.6552	0.0	6.71	1.561	0.766	0.805	2.092	2.267	1.112	+2307.	966.	13.6	7.875
* 1.00	0.	0.7737	0.	0.2365	6.76	1.549	0.749	0.805	2.055	2.295	1.091	+2322.	927.	13.5	7.750
* 1.00	0.1	0.7685	0.0278	0.2039	7.05	1.591	0.742	0.566	1.838	2.277	1.330	+2338.	1127.	15.4	9.594
* 1.00	0.2	0.7638	0.0267	0.1814	7.07	1.571	0.741	0.595	1.844	2.250	1.311	+2355.	1109.	15.3	9.553
* 1.00	0.3	0.7695	0.0231	0.1589	7.01	1.538	0.731	0.595	1.855	2.236	1.292	+2373.	1094.	15.2	9.512
* 1.00	0.4	0.7556	0.0182	0.1364	6.95	1.507	0.704	0.567	1.865	2.213	1.272	+2391.	1073.	15.1	9.472
* 1.00	0.5	0.7521	0.0134	0.1139	6.89	1.484	0.671	0.547	1.889	2.190	1.252	+2409.	1052.	15.1	9.392
* 1.00	0.6	0.7491	0.0158	0.0914	6.83	1.454	0.645	0.527	1.879	2.171	1.232	+2426.	1032.	15.0	9.352
* 1.00	0.7	0.7441	0.0210	0.0460	6.81	1.426	0.617	0.517	1.882	2.151	1.212	+2447.	993.	14.9	9.212
* 1.00	0.8	0.7421	0.0239	0.0231	6.84										

LIQUID MOLE FRACTION	VAPOR MOLE FRACTION	PRESSURE	EQUIL CONST.			RELATIVE VOL	ENTHALPY			HEAT CAPACITY				
			N2	AR/AR+O2	N2		AR	O2	N2/AR	N2/O2	AR/O2	LIQ	VAP	
+	0.	0.	1.0001	4.78	2.631	1.000	1.944	2.631	1.393	-1407.	1239.	13.5	8.297	
+	0.3	0.	0.1278	0.8722	4.97	2.597	1.279	0.969	1.965	2.587	1.320	-1429.	1187.	
+	0.2	0.	0.2337	0.7745	5.13	2.496	1.218	0.946	1.975	2.544	1.288	-1452.	1149.	
+	0.3	0.	0.3592	0.6590	5.27	2.392	1.187	0.929	1.990	2.502	1.257	-1474.	1097.	
+	0.4	0.	0.4505	0.5512	5.40	2.297	1.159	0.917	2.006	2.461	1.227	-1496.	1057.	
+	0.5	0.	0.5455	0.4552	5.53	2.204	1.109	0.910	2.022	2.421	1.197	-1519.	1019.	
+	0.6	0.	0.6368	0.3634	5.65	2.103	1.081	0.909	2.038	2.381	1.168	-1542.	983.	
+	0.7	0.	0.7289	0.2773	5.76	2.033	1.058	0.911	2.054	2.342	1.140	-1564.	947.	
+	0.8	0.	0.8167	0.1935	5.77	2.014	1.021	0.918	2.071	2.304	1.113	-1588.	912.	
+	0.9	0.	0.9074	0.0928	5.83	2.014	1.008	0.928	2.087	2.268	1.086	-1608.	877.	
+	1.0	0.	1.0000	0.	5.88	2.014	1.000	0.944	2.114	2.231	1.060	-1633.	841.	
+0.25	0+	0.	0.1277	0.	0.9374	5.10	2.508	1.208	0.939	1.937	2.620	1.347	-1388.	1235.
+0.25	0.1	0.	0.2060	0.1149	0.803	5.18	2.405	1.230	0.939	1.991	2.597	1.315	-1410.	1186.
+0.25	0.2	0.	0.2977	0.1229	0.734	5.33	2.310	1.175	0.915	1.968	2.526	1.284	-1435.	1142.
+0.25	0.3	0.	0.3999	0.1301	0.639	5.47	2.236	1.129	0.900	1.982	2.485	1.254	-1453.	1101.
+0.25	0.4	0.	0.4944	0.1381	0.520	5.59	2.176	1.090	0.889	1.997	2.445	1.224	-1475.	1063.
+0.25	0.5	0.	0.5929	0.1517	0.431	5.70	2.129	1.054	0.885	2.012	2.406	1.198	-1497.	1027.
+0.25	0.6	0.	0.6924	0.1634	0.344	5.80	2.081	1.021	0.883	2.028	2.367	1.168	-1519.	992.
+0.25	0.7	0.	0.7865	0.1759	0.259	5.89	2.084	1.020	0.886	2.037	2.326	1.137	-1540.	956.
+0.25	0.8	0.	0.8722	0.1873	0.174	5.96	2.084	1.018	0.888	2.043	2.296	1.107	-1564.	924.
+0.25	0.9	0.	0.9593	0.1983	0.092	6.02	2.037	0.992	0.903	2.075	2.266	1.087	-1584.	890.
+0.25	1.0	0.	1.0000	0.	0.092	6.08	2.036	0.974	0.917	2.095	2.221	1.052	-1608.	854.
+0.50	0+	0.	0.1275	0.	0.9374	5.10	2.508	1.208	0.939	1.937	2.620	1.347	-1388.	1235.
+0.50	0.1	0.	0.2060	0.1149	0.803	5.18	2.405	1.230	0.939	1.991	2.597	1.315	-1410.	1186.
+0.50	0.2	0.	0.2977	0.1229	0.734	5.33	2.310	1.175	0.915	1.968	2.526	1.284	-1435.	1142.
+0.50	0.3	0.	0.3999	0.1301	0.639	5.47	2.236	1.129	0.900	1.982	2.485	1.254	-1453.	1101.
+0.50	0.4	0.	0.4944	0.1381	0.520	5.59	2.176	1.090	0.889	1.997	2.445	1.224	-1475.	1063.
+0.50	0.5	0.	0.5929	0.1517	0.431	5.70	2.129	1.054	0.885	2.012	2.406	1.198	-1497.	1027.
+0.50	0.6	0.	0.6924	0.1634	0.344	5.80	2.081	1.021	0.883	2.028	2.367	1.168	-1519.	992.
+0.50	0.7	0.	0.7865	0.1759	0.259	5.89	2.084	1.020	0.886	2.037	2.326	1.137	-1540.	956.
+0.50	0.8	0.	0.8722	0.1873	0.174	5.96	2.084	1.018	0.888	2.043	2.296	1.107	-1564.	924.
+0.50	0.9	0.	0.9593	0.1983	0.092	6.02	2.037	0.992	0.903	2.075	2.266	1.087	-1584.	890.
+0.50	1.0	0.	1.0000	0.	0.092	6.08	2.036	0.974	0.917	2.095	2.221	1.052	-1608.	854.
+0.75	0+	0.	0.1275	0.	0.9374	5.10	2.508	1.208	0.939	1.937	2.620	1.347	-1388.	1235.
+0.75	0.1	0.	0.2060	0.1149	0.803	5.18	2.405	1.230	0.939	1.991	2.597	1.315	-1410.	1186.
+0.75	0.2	0.	0.2977	0.1229	0.734	5.33	2.310	1.175	0.915	1.968	2.526	1.284	-1435.	1142.
+0.75	0.3	0.	0.3999	0.1301	0.639	5.47	2.236	1.129	0.900	1.982	2.485	1.254	-1453.	1101.
+0.75	0.4	0.	0.4944	0.1381	0.520	5.59	2.176	1.090	0.889	1.997	2.445	1.224	-1475.	1063.
+0.75	0.5	0.	0.5929	0.1517	0.431	5.70	2.129	1.054	0.885	2.012	2.406	1.198	-1497.	1027.
+0.75	0.6	0.	0.6924	0.1634	0.344	5.80	2.081	1.021	0.883	2.028	2.367	1.168	-1519.	992.
+0.75	0.7	0.	0.7865	0.1759	0.259	5.89	2.084	1.020	0.886	2.037	2.326	1.137	-1540.	956.
+0.75	0.8	0.	0.8722	0.1873	0.174	5.96	2.084	1.018	0.888	2.043	2.296	1.107	-1564.	924.
+0.75	0.9	0.	0.9593	0.1983	0.092	6.02	2.037	0.992	0.903	2.075	2.266	1.087	-1584.	890.
+0.75	1.0	0.	1.0000	0.	0.092	6.08	2.036	0.974	0.917	2.095	2.221	1.052	-1608.	854.
+1.00	0+	0.	0.1275	0.	0.9374	5.10	2.508	1.208	0.939	1.937	2.620	1.347	-1388.	1235.
+1.00	0.1	0.	0.2060	0.1149	0.803	5.18	2.405	1.230	0.939	1.991	2.597	1.315	-1410.	1186.
+1.00	0.2	0.	0.2977	0.1229	0.734	5.33	2.310	1.175	0.915	1.968	2.526	1.284	-1435.	1142.
+1.00	0.3	0.	0.3999	0.1301	0.639	5.47	2.236	1.129	0.900	1.982	2.485	1.254	-1453.	1101.
+1.00	0.4	0.	0.4944	0.1381	0.520	5.59	2.176	1.090	0.889	1.997	2.445	1.224	-1475.	1063.
+1.00	0.5	0.	0.5929	0.1517	0.431	5.70	2.129	1.054	0.885	2.012	2.406	1.198	-1497.	1027.
+1.00	0.6	0.	0.6924	0.1634	0.344	5.80	2.081	1.021	0.883	2.028	2.367	1.168	-1519.	992.
+1.00	0.7	0.	0.7865	0.1759	0.259	5.89	2.084	1.020	0.886	2.037	2.326	1.137	-1540.	956.
+1.00	0.8	0.	0.8722	0.1873	0.174	5.96	2.084	1.018	0.888	2.043	2.296	1.107	-1564.	924.
+1.00	0.9	0.	0.9593	0.1983	0.092	6.02	2.037	0.992	0.903	2.075	2.266	1.087	-1584.	890.
+1.00	1.0	0.	1.0000	0.	0.092	6.08	2.036	0.974	0.917	2.095	2.221	1.052	-1608.	854.
+0.25	0+	0.	0.1275	0.	0.9374	5.10	2.508	1.208	0.939	1.937	2.620	1.347	-1388.	1235.
+0.25	0.1	0.	0.2060	0.1149	0.803	5.18	2.405	1.230	0.939	1.991	2.597	1.315	-1410.	1186.
+0.25	0.2	0.	0.2977	0.1229	0.734	5.33	2.310	1.175	0.915	1.968	2.526	1.284	-1435.	1142.
+0.25	0.3	0.	0.3999	0.1301	0.639	5.47	2.236	1.129	0.900	1.982	2.485	1.254	-1453.	1101.
+0.25	0.4	0.	0.4944	0.1381	0.520	5.59	2.176	1.090	0.889	1.997	2.445	1.224	-1475.	1063.
+0.25	0.5	0.	0.5929	0.1517	0.431	5.70	2.129	1.054	0.885	2.012	2.406	1.198	-1497.	1027.
+0.25	0.6	0.	0.6924	0.1634	0.344	5.80	2.081	1.021	0.883	2.028	2.367	1.168	-1519.	992.
+0.25	0.7	0.	0.7865	0.1759	0.259	5.89	2.084	1.020	0.886	2.037	2.326	1.137	-1540.	956.
+0.25	0.8	0.	0.8722	0.1873	0.174	5.96	2.084	1.018	0.888	2.043	2.296	1.107	-1564.	924.
+0.25	0.9	0.	0.9593	0.1983	0.092	6.02	2.037	0.992	0.903	2.075	2.266	1.087	-1584.	890.
+0.25	1.0	0.	1.0000	0.	0.092	6.08	2.036	0.974	0.917	2.095	2.221	1.052	-1608.	854.
+0.50	0+	0.	0.1275	0.	0.9374	5.10	2.508	1.208	0.939	1.937	2.620	1.347	-1388.	1235.
+0.50	0.1	0.	0.2060	0.1149	0.803	5.18	2.405	1.230	0.939	1.991	2.597	1.315	-1410.	1186.
+0.50	0.2	0.	0.2977	0.1229	0.734	5.33	2.310	1.175	0.915	1.968	2.526	1.284	-1435.	1142.
+0.50	0.3	0.	0.3999	0.1301	0.639	5.47	2.236	1.129	0.900	1.982	2.485	1.254	-1453.	1101.
+0.50	0.4	0.	0.4944	0.1381	0.520	5.59	2.176	1.090	0.889	1.997	2.44			

Table 26. (cont.)

LIQUID MOLE FRACTION		VAPOR MOLE FRACTION		PRESSURE		EQUIL CONST		RELATIVE VOL		ENTHALPY		HEAT CAPACITY				
N2	AR/AR+O2	N2	AR	O2	ATH	N2	AR	O2	N2/AR	N2/O2	AR/O2	Liq	Vap	Liq	Vap	
.	0.	0.	0.	1.0002	9.80	2.479	1.330	1.884	2.479	1.330	-1339	1254	13.6	8.924		
.	0.1	0.	0.1261	0.8741	9.11	2.389	1.261	0.971	1.879	2.430	1.299	-1362	1211	13.5	8.897	
.	0.2	0.	0.2409	0.7594	8.20	2.278	1.126	0.949	1.891	2.401	1.269	-1385	1154	13.4	8.858	
.	0.3	0.	0.3470	0.6533	5.37	2.053	1.057	0.933	1.905	2.356	1.240	-1408	1109	13.3	8.822	
.	0.4	0.	0.4466	0.5535	4.92	2.143	1.117	0.922	1.979	2.323	1.211	-1431	1088	13.2	7.745	
.	0.5	0.	0.5421	0.4582	5.85	2.045	1.084	0.916	1.933	2.286	1.183	-1454	1059	13.1	7.572	
.	0.6	0.	0.6344	0.3658	6.76	2.036	1.057	0.913	1.947	2.255	1.159	-1477	991	13.0	7.451	
.	0.7	0.	0.7251	0.2752	6.46	2.031	1.038	0.912	1.961	2.242	1.129	-1500	954	12.9	7.227	
.	0.8	0.	0.8156	0.1848	6.94	2.014	1.019	0.904	1.975	2.179	1.103	-1523	918	12.8	7.049	
.	0.9	0.	0.8969	0.0935	7.11	2.005	1.008	0.905	1.990	2.145	1.078	-1546	881	12.7	6.864	
1.0	0.	1.	0.9904	0.	7.06	2.005	1.000	0.906	2.004	2.111	1.053	-1569	844	12.6	6.669	
0.75	0.	0.	0.393	0.	9.48	2.373	1.278	0.985	2.087	2.459	1.324	-1319	1250	13.7	8.988	
0.25	0.1	0.	0.6569	0.1186	0.244	6.95	2.275	1.256	0.940	1.870	2.420	1.294	-1342	1202	13.6	8.886
0.25	0.2	0.	0.5548	0.2272	0.7183	8.42	2.195	1.165	0.921	1.883	2.382	1.245	-1364	1155	13.5	8.803
0.25	0.3	0.	0.532	0.3241	0.6191	6.59	2.127	1.122	0.907	1.897	2.345	1.237	-1387	1112	13.4	8.625
0.25	0.4	0.	0.5168	0.4223	0.5253	6.73	2.073	1.085	0.896	1.910	2.309	1.200	-1409	1073	13.3	7.887
0.25	0.5	0.	0.4957	0.5143	0.4353	6.86	2.023	1.055	0.883	1.924	2.273	1.162	-1431	1035	13.2	7.693
0.25	0.6	0.	0.4499	0.626	0.3474	6.97	1.995	1.033	0.872	1.937	2.237	1.129	-1454	999	13.1	7.533
0.25	0.7	0.	0.4043	0.6894	0.2617	7.07	1.971	1.011	0.869	1.951	2.203	1.098	-1478	964	13.0	7.365
0.25	0.8	0.	0.3489	0.7750	0.1757	7.15	1.954	0.995	0.861	1.965	2.189	1.074	-1499	929	13.0	7.196
0.25	0.9	0.	0.2466	0.8629	0.0864	7.22	1.946	0.963	0.851	1.979	2.154	1.051	-1521	894	12.9	7.021
0.25	1.0	0.	0.2466	0.9518	0.	7.27	1.945	0.956	0.849	1.993	2.103	1.029	-1543	859	12.8	6.856
1.00	0.	0.	0.2167	0.	0.7887	6.76	2.152	1.147	0.877	1.835	2.450	1.307	-1261	1238	14.0	8.791
1.00	0.1	0.	0.2037	0.0992	0.974	6.95	2.057	1.102	0.861	1.844	2.386	1.280	-1281	1194	14.0	8.667
1.00	0.2	0.	0.1977	0.1915	0.6110	7.11	1.979	1.064	0.848	1.860	2.322	1.248	-1302	1159	13.9	8.474
1.00	0.3	0.	0.1935	0.2784	0.5291	7.25	1.930	1.031	0.840	1.870	2.298	1.228	-1323	1119	13.8	8.397
1.00	0.4	0.	0.1899	0.3610	0.4255	7.38	1.882	1.003	0.834	1.884	2.265	1.194	-1343	1084	13.7	8.15
1.00	0.5	0.	0.1857	0.4466	0.3743	7.49	1.857	0.976	0.832	1.897	2.233	1.177	-1364	1051	13.6	8.059
1.00	0.6	0.	0.1833	0.5177	0.2994	7.65	1.830	0.956	0.832	1.905	2.201	1.153	-1385	1019	13.5	7.760
1.00	0.7	0.	0.1812	0.5937	0.2254	7.85	1.811	0.942	0.833	1.922	2.169	1.129	-1409	988	13.4	7.51
1.00	0.8	0.	0.1797	0.6691	0.1913	7.94	1.797	0.928	0.841	1.934	2.136	1.105	-1431	957	13.3	7.216
1.00	0.9	0.	0.1780	0.7447	0.0764	7.94	1.780	0.913	0.849	1.947	2.105	1.083	-1452	927	13.2	7.087
1.00	1.0	0.	0.1780	0.8213	0.	7.95	1.788	0.912	0.849	1.960	2.074	1.063	-1472	890	13.1	6.954
2.00	0.	0.3677	0.	0.6324	7.73	1.785	0.908	0.841	1.974	2.053	1.043	-1487	860	13.0	6.821	
2.00	0.1	0.	0.3507	0.0760	0.5425	7.87	1.793	0.988	0.711	1.871	2.294	1.085	-1508	1250	14.5	9.382
2.00	0.2	0.	0.351	0.1935	0.4497	8.00	1.795	0.959	0.774	1.880	2.264	1.056	-1527	1183	14.4	9.197
2.00	0.3	0.	0.3444	0.2244	0.4311	8.12	1.795	0.929	0.755	1.890	2.234	1.027	-1547	1151	14.3	8.938
2.00	0.4	0.	0.3389	0.2903	0.3683	8.23	1.804	0.894	0.736	1.901	2.204	1.000	-1567	1121	14.2	8.722
2.00	0.5	0.	0.3343	0.3592	0.3067	8.33	1.871	0.868	0.717	1.911	2.180	0.974	-1587	1093	14.1	8.509
2.00	0.6	0.	0.330	0.4238	0.2457	8.43	1.883	0.843	0.700	1.922	2.152	0.946	-1607	1063	14.0	8.384
2.00	0.7	0.	0.3277	0.4873	0.1951	8.51	1.892	0.817	0.687	1.933	2.125	0.920	-1627	1032	13.9	8.264
2.00	0.8	0.	0.3257	0.5593	0.1242	8.59	1.889	0.808	0.676	1.943	2.095	0.898	-1647	998	13.8	8.194
2.00	0.9	0.	0.3245	0.613	0.0626	8.65	1.882	0.802	0.667	1.954	2.066	0.878	-1667	955	13.6	8.035
2.00	1.0	0.	0.3239	0.6782	0.	8.72	1.880	0.802	0.662	1.965	2.036	0.847	-1687	916	13.5	7.910
3.00	0.	0.4932	0.	0.5000	8.85	1.857	0.799	0.727	1.781	2.020	1.284	-1154	1257	14.9	9.407	
3.00	0.1	0.	0.4824	0.0629	0.4549	8.77	1.868	0.768	0.722	1.790	2.027	1.244	-1170	1220	14.8	9.313
3.00	0.2	0.	0.4747	0.1231	0.4024	8.88	1.882	0.739	0.719	1.799	2.022	1.224	-1186	1149	14.7	9.221
3.00	0.3	0.	0.4660	0.1822	0.3511	8.99	1.893	0.703	0.710	1.808	2.017	1.204	-1206	1120	14.6	9.132
3.00	0.4	0.	0.4582	0.2374	0.3005	9.08	1.904	0.674	0.700	1.817	2.014	1.184	-1226	1093	14.5	9.043
3.00	0.5	0.	0.4534	0.3458	0.2010	9.16	1.925	0.641	0.689	1.827	2.009	1.164	-1246	1063	14.4	8.954
3.00	0.6	0.	0.452	0.3986	0.1514	9.25	1.935	0.612	0.678	1.838	2.005	1.145	-1266	1031	14.3	8.863
3.00	0.7	0.	0.452	0.458	0.1019	9.33	1.951	0.583	0.661	1.845	2.002	1.126	-1286	999	14.2	8.766
3.00	0.8	0.	0.4479	0.458	0.0109	9.40	1.963	0.553	0.652	1.852	1.998	1.107	-1306	961	14.1	8.641
3.00	0.9	0.	0.4463	0.5245	0.0348	9.48	1.975	0.524	0.642	1.861	1.993	1.087	-1326	923	14.0	8.533
3.00	1.0	0.	0.4462	0.5823	0.	9.55	1.975	0.504	0.632	1.874	1.984	1.067	-1346	884	13.9	8.439
4.00	0.1	0.	0.7495	0.0293	0.2214	11.46	2.149	0.733	0.615	1.710	2.044	1.420	-1081	1221	16.1	10.661
4.00	0.2	0.	0.7451	0.0581	0.1969	11.52	2.144	0.705	0.615	1.720	2.034	1.401	-1097	1196	16.0	10.559
4.00	0.3	0.	0.7412	0.0865	0.1728	11.57	2.135	0.676	0.616	1.730	2.024	1.381	-1116	1166	15.9	10.456
4.00	0.4	0.	0.7377	0.1144	0.1481	11.63	2.129	0.646	0.617	1.730	2.015	1.361	-1136	1136	15.8	10.356
4.00	0.5	0.	0.7345	0.1420	0.1237	11.68	2.124	0.618	0.605	1.730	2.005	1.341	-1156	1107	15.7	10.253
4.00	0.6	0.	0.7317	0.1682	0.0992	11.74	2.116	0.590	0.595	1.734	1.996	1.321	-1176	1072	15.6	10.153
4.00	0.7	0.	0.7293	0.1962	0.0748	11.79	2.109	0.562	0.580	1.730	1.987	1.297	-1196	1049	15.5	10.049
4.00	0.8	0.	0.7273	0.2230	0.0499	11.84	2.101	0.534	0.572</td							

Table 26. (cont.)

LIQUID MOLE FRACTION		VAPOR MOLE FRACTION		PRESSURE		EQUIL CONST		RELATIVE VOL		ENTHALPY BTU/LB MOLE		HEAT CAPACITY BTU/LB MOLE-R				
N2	AR/AR+D2	N2	AR	D2	ATM	N2	AR	D2	N2/AR	N2/D2	AR/D2	L10	VAP	L10	VAP	
+	0.	0.	0.	1.0000	8.97	2.341	1.324	1.900	1.780	2.340	1.307	+1271.	1267.	13.8	8.787	
+	0.1	0.	0.1244	0.8750	7.21	2.242	1.244	0.973	1.812	2.303	1.278	+1294.	1224.	13.7	9.582	
+	0.2	0.	0.2382	0.7422	7.42	2.160	1.151	0.953	1.814	2.267	1.250	+1317.	1164.	13.6	5.393	
+	0.3	0.	0.3440	0.6565	7.61	2.093	1.074	0.938	1.829	2.232	1.222	+1341.	1119.	13.5	4.215	
+	0.4	0.	0.4437	0.5567	7.79	2.039	1.009	0.928	1.839	2.197	1.196	+1364.	1076.	13.5	8.643	
+	0.5	0.	0.5291	0.4610	7.94	1.995	1.079	0.922	1.856	2.163	1.169	+1387.	1025.	13.4	7.71	
+	0.6	0.	0.6218	0.3663	8.07	1.961	1.053	0.921	1.882	2.130	1.144	+1411.	998.	13.4	7.703	
+	0.7	0.	0.7231	0.2770	8.18	1.937	1.033	0.923	1.879	2.097	1.119	+1434.	958.	13.3	7.531	
+	0.8	0.	0.8142	0.1860	8.28	1.921	1.028	0.930	1.887	2.085	1.104	+1458.	920.	13.2	7.554	
+	0.9	0.	0.9060	0.0941	8.39	1.913	1.027	0.941	1.890	2.032	1.070	+1485.	883.	13.1	7.568	
+	1.0	0.	0.9903	0.	8.41	1.913	1.022	0.955	1.893	2.022	1.047	+1504.	849.	13.1	8.972	
+0.05	0.	0.0562	0.	0.9442	7.74	2.249	1.291	0.968	1.742	2.322	1.352	+1259.	1282.	13.9	8.851	
+0.15	0.1	0.0940	0.1173	0.8891	7.47	2.145	1.203	0.949	1.705	2.287	1.274	+1273.	1211.	13.8	8.670	
+0.25	0.2	0.1922	0.2293	0.7230	7.66	2.067	1.155	0.927	1.687	2.252	1.246	+1296.	1169.	13.8	8.493	
+0.35	0.3	0.2900	0.3259	0.6235	7.87	2.026	1.114	0.914	1.618	2.215	1.222	+1319.	1121.	13.7	8.321	
+0.45	0.4	0.3894	0.4212	0.5295	8.03	1.977	1.080	0.915	1.630	2.184	1.193	+1342.	1080.	13.6	8.159	
+0.55	0.5	0.4884	0.5127	0.4290	8.18	1.937	1.052	0.901	1.642	2.151	1.168	+1364.	1041.	13.5	7.999	
+0.65	0.6	0.5777	0.6019	0.3550	8.31	1.895	1.028	0.892	1.654	2.119	1.143	+1387.	1004.	13.5	7.839	
+0.75	0.7	0.6671	0.6890	0.2740	8.42	1.854	1.000	0.893	1.665	2.087	1.118	+1410.	967.	13.4	7.675	
+0.85	0.8	0.7567	0.7781	0.1773	8.51	1.819	0.969	0.899	1.678	2.056	1.095	+1433.	931.	13.3	7.507	
+0.95	0.9	0.8455	0.8660	0.0984	8.58	1.781	0.936	0.916	1.690	2.025	1.071	+1456.	895.	13.3	7.331	
+1.0	1.0	0.9455	0.9556	0.	8.64	1.745	0.905	0.946	1.708	2.000	1.046	+1478.	859.	13.2	7.144	
+1.00	0.	0.2034	0.	0.7082	8.04	2.114	1.181	0.887	1.755	2.269	1.385	+1370.	1248.	14.2	9.091	
+1.00	0.1	0.1950	0.	0.9846	7.82	2.082	1.199	0.872	1.775	2.237	1.346	+1211.	1203.	14.3	8.936	
+1.00	0.2	0.1897	0.	0.9192	7.93	2.044	1.197	0.862	1.764	2.206	1.305	+1233.	1183.	14.1	8.792	
+1.00	0.3	0.1852	0.	0.7874	7.935	2.002	1.152	0.852	1.766	2.175	1.211	+1253.	1162.	14.1	8.649	
+1.00	0.4	0.1815	0.	0.6816	0.4970	7.95	1.913	1.031	0.852	1.766	2.145	1.187	+1274.	1092.	14.0	8.512
+1.00	0.5	0.1785	0.	0.4419	0.3798	7.98	1.878	1.002	0.844	1.781	2.114	1.163	+1299.	1059.	13.9	8.378
+1.00	0.6	0.1760	0.	0.5261	0.3045	8.03	1.831	0.963	0.845	1.789	2.085	1.140	+1326.	1022.	13.9	8.239
+1.00	0.7	0.1743	0.	0.5926	0.2289	8.11	1.781	0.943	0.848	1.793	2.056	1.117	+1357.	998.	13.8	8.099
+1.00	0.8	0.1731	0.	0.6735	0.1536	8.20	1.731	0.919	0.854	1.805	2.026	1.088	+1388.	958.	13.7	7.955
+1.00	0.9	0.1724	0.	0.7562	0.0776	8.27	1.724	0.906	0.862	1.804	2.002	1.074	+1419.	926.	13.7	7.845
+1.00	1.0	0.	0.1679	0.	0.8270	8.34	1.723	0.902	0.873	1.773	1.972	1.053	+1440.	899.	13.6	7.646
+1.00	0.	0.3577	0.	0.8483	7.91	2.174	1.211	0.867	1.735	2.260	1.325	+1209.	1229.	14.7	8.428	
+1.00	0.1	0.3486	0.	0.7973	0.3743	7.98	1.733	0.961	0.798	1.746	2.172	1.242	+1228.	1193.	14.6	9.317
+1.00	0.2	0.3394	0.	0.5945	0.5083	8.04	1.887	0.968	0.791	1.757	2.145	1.221	+1247.	1158.	14.6	9.255
+1.00	0.3	0.3233	0.	0.2964	0.4447	9.38	1.867	0.943	0.787	1.757	2.119	1.199	+1269.	1126.	14.1	8.649
+1.00	0.4	0.3185	0.	0.3616	0.4970	8.75	1.813	0.924	0.785	1.768	2.094	1.177	+1287.	1097.	14.0	8.512
+1.00	0.5	0.2985	0.	0.4419	0.3798	8.88	1.789	0.902	0.784	1.781	2.074	1.153	+1309.	1059.	13.9	8.378
+1.00	0.6	0.2785	0.	0.5261	0.3045	9.03	1.761	0.963	0.845	1.809	2.045	1.120	+1336.	1022.	13.9	8.239
+1.00	0.7	0.2582	0.	0.5926	0.2289	9.11	1.743	0.943	0.848	1.805	2.016	1.088	+1363.	985.	13.8	8.099
+1.00	0.8	0.2382	0.	0.6735	0.1536	9.20	1.731	0.919	0.854	1.805	1.986	1.056	+1390.	955.	13.7	7.955
+1.00	0.9	0.2184	0.	0.7562	0.0776	9.27	1.724	0.906	0.862	1.804	1.956	1.024	+1419.	926.	13.6	8.420
+1.00	1.0	0.	0.1679	0.	0.8270	9.34	1.723	0.902	0.873	1.773	1.972	1.053	+1440.	899.	13.5	8.294
+1.00	0.	0.4777	0.	0.5226	10.18	2.162	1.292	0.747	1.714	2.269	1.385	+1039.	1244.	14.2	9.091	
+1.00	0.1	0.4694	0.	0.8746	0.4473	10.30	1.865	0.928	0.747	1.714	2.133	1.344	+1245.	1123.	14.3	8.936
+1.00	0.2	0.4622	0.	0.1247	0.4135	10.42	1.941	0.861	0.738	1.722	2.110	1.225	+1264.	1101.	14.2	8.821
+1.00	0.3	0.4559	0.	0.1837	0.3608	10.54	1.920	0.875	0.725	1.734	2.085	1.191	+1283.	1076.	14.1	8.734
+1.00	0.4	0.4555	0.	0.2445	0.3240	10.65	1.887	0.943	0.717	1.745	2.054	1.160	+1302.	1049.	14.0	8.649
+1.00	0.5	0.4486	0.	0.2967	0.2877	10.76	1.847	0.968	0.738	1.755	2.024	1.129	+1321.	1028.	13.9	8.566
+1.00	0.6	0.4422	0.	0.3515	0.2668	10.85	1.814	0.977	0.737	1.764	2.005	1.100	+1340.	998.	13.8	8.482
+1.00	0.7	0.4393	0.	0.4095	0.1958	10.94	1.784	0.984	0.741	1.774	1.976	1.071	+1357.	957.	13.7	8.398
+1.00	0.8	0.4371	0.	0.4889	0.1044	11.02	1.749	0.970	0.745	1.784	1.945	1.041	+1376.	917.	13.6	8.224
+1.00	0.9	0.4356	0.	0.5622	0.0286	11.09	1.712	0.959	0.751	1.793	1.916	1.012	+1395.	889.	13.5	8.134
+1.00	1.0	0.	0.3449	0.	0.6215	11.16	1.705	0.948	0.768	1.784	1.901	1.007	+1417.	859.	13.4	8.082
+1.00	0.	0.6872	0.	0.3330	12.24	2.134	1.240	0.639	1.638	2.269	1.404	+867.	1137.	16.1	10.770	
+1.00	0.1	0.6812	0.	0.0396	0.2993	11.31	1.431	0.844	0.699	1.699	2.048	1.298	+982.	1159.	15.6	10.200
+1.00	0.2	0.6859	0.	0.0988	0.3347	11.41	1.415	0.831	0.687	1.702	2.029	1.272	+1037.	1137.	15.5	10.139
+1.00	0.3	0.6830	0.	0.1973	0.2665	12.45	1.312	0.783	0.645	1.674	2.084	1.245	+1056.	1109.	15.5	10.078
+1.00	0.4	0.6866	0.	0.2443	0.1958	12.45	1.302	0.775	0.645	1.682	2.054	1.225	+1075.	1101.	15.4	10.011
+1.00	0.5	0.6835	0.	0.3153	0.1998	12.57	1.294	0.764	0.648	1.692	2.024	1.204	+1094.	1079.	15.3	9.949
+1.00	0.6	0.6833	0.	0.3896	0.1689	12.65	1.264	0.755	0.648	1.699	2.004	1.184	+1113.	1057.	15.2	9.863
+1.00	0.7	0.6822	0.	0.4222	0.1008	12.72	1.236	0.744	0.648	1.705	1.976	1.163	+1132.	103		

Table 26. (cont.)

LIQUID MOLE FRACTION	VAPOR MOLE FRACTION		PRESSURE	EQUIL CONST		RELATIVE VOL	ENTHALPY		HEAT CAPACITY			
	NO	AR/AR+O2		NO	AR		NO	AR	O2	BTU/LB MOLE	BTU/LB MOLE-R	
+	0.	0.	0.	2.201	1.201	2.215	1.209	1.793	2.214	1.209	-121. 1277. 14.0 8.000	
+	0.1	0.	0.1297	0.6774	0.177	2.126	1.227	0.975	1.733	2.181	1.258 -125. 1222. 14.1 8.000	
+	0.2	0.	0.2359	0.7474	0.191	2.053	1.177	0.986	1.744	2.146	1.232 -124. 1172. 13.9 0.720	
+	0.3	0.	0.3408	0.6594	0.153	1.992	1.136	0.942	1.794	2.115	1.226 -127. 1126. 13.9 0.591	
+	0.4	0.	0.4445	0.5597	0.123	1.943	1.101	0.933	1.769	2.083	1.181 -126. 1082. 13.8 0.387	
+	0.5	0.	0.5349	0.4439	0.092	1.894	1.072	0.928	1.775	2.052	1.156 -125. 1049. 13.7 0.059	
+	0.6	0.	0.6294	0.3798	0.055	1.874	1.049	0.927	1.786	2.021	1.132 -134. 999. 13.7 0.059	
+	0.7	0.	0.7212	0.2795	0.027	1.851	1.020	0.926	1.797	1.991	1.088 -136. 982. 13.7 7.096	
+	0.8	0.	0.8129	0.1873	0.008	1.837	0.984	0.927	1.819	1.963	1.059 -131. 921. 13.6 7.714	
+	0.9	0.	0.8965	0.0947	0.	1.803	0.908	0.947	1.819	1.933	1.059 -131. 921. 13.6 7.927	
+	1.0	0.	1.0002	0.	0.992	1.803	1.000	0.992	1.803	1.944	1.082	13.6 7.328
+2.25	0.	0.77934	0.	0.9468	0.	2.134	1.243	0.971	1.773	2.145	1.285 -118. 1272. 14.1 9.175	
+2.25	0.1	0.8154	0.1198	0.8327	0.	2.091	1.190	0.949	1.797	2.145	1.284 -123. 1220. 14.1 8.987	
+2.25	0.2	0.8497	0.2233	0.7272	0.	1.918	1.045	0.932	1.787	2.133	1.288 -122. 1172. 14.0 8.830	
+2.25	0.3	0.8840	0.3238	0.5986	0.	1.811	0.934	0.920	1.747	2.102	1.293 -121. 1127. 14.0 8.671	
+2.25	0.4	0.9172	0.4193	0.5337	0.	1.749	0.889	0.915	1.798	2.071	1.178 -120. 1085. 13.9 8.515	
+2.25	0.5	0.9463	0.5111	0.4428	0.	1.685	0.846	0.908	1.768	2.041	1.154 -119. 1045. 13.9 8.361	
+2.25	0.6	0.9698	0.5915	0.3546	0.	1.626	0.802	0.896	1.777	2.011	1.131 -119. 1006. 13.8 8.244	
+2.25	0.7	0.9851	0.6887	0.2868	0.	1.565	0.759	0.871	1.787	1.982	1.085 -118. 968. 13.8 8.144	
+2.25	0.8	0.9948	0.7765	0.1789	0.	1.503	0.704	0.817	1.801	1.942	1.048 -117. 926. 13.8 8.059	
+2.25	0.9	0.9982	0.8592	0.0986	0.	1.441	0.658	0.797	1.811	1.903	1.009 -116. 886. 13.7 7.976	
+2.25	1.0	0.9998	0.9556	0.	1.380	0.616	0.780	1.821	1.897	1.002 -115. 843. 13.6 7.899		
+1.00	0.	0.9992	0.	0.9973	0.	1.335	0.578	0.755	1.831	1.882	1.002 -114. 806. 13.5 7.730	
+1.00	0.1	0.9871	0.0985	0.7144	0.	1.281	0.535	0.732	1.859	1.850	1.002 -113. 765. 13.4 7.444	
+1.00	0.2	0.9592	0.1949	0.4972	0.	1.225	0.495	0.682	1.793	2.120	1.241 -113. 713. 13.3 7.303	
+1.00	0.3	0.9178	0.2794	0.3438	0.	1.171	0.453	0.633	1.727	2.083	1.195 -112. 669. 13.2 7.166	
+1.00	0.4	0.8747	0.3621	0.4625	0.	1.121	0.412	0.595	1.736	2.035	1.172 -110. 625. 13.1 7.034	
+1.00	0.5	0.8219	0.4431	0.3893	0.	1.071	0.370	0.552	1.744	2.007	1.133 -109. 587. 13.0 6.933	
+1.00	0.6	0.7697	0.5292	0.3049	0.	1.021	0.329	0.509	1.755	1.981	1.086 -108. 545. 12.9 6.839	
+1.00	0.7	0.7187	0.6174	0.1959	0.	0.961	0.282	0.460	1.765	1.954	1.037 -107. 509. 12.8 6.735	
+1.00	0.8	0.6662	0.6952	0.0854	0.	0.909	0.239	0.419	1.774	1.928	1.006 -106. 479. 12.7 6.639	
+1.00	0.9	0.6163	0.7792	0.0787	0.	0.858	0.198	0.378	1.784	1.900	1.006 -105. 449. 12.6 6.539	
+1.00	1.0	0.5662	0.8541	0.	0.808	0.157	0.337	1.794	1.874	1.006 -104. 427. 12.5 6.439		
+2.00	0.	0.9429	0.	0.9874	0.	1.095	0.882	0.886	1.794	1.846	1.048 -103. 386. 12.4 6.339	
+2.00	0.1	0.8286	0.1954	0.7166	0.	1.045	0.843	0.833	1.844	1.881	1.084 -102. 346. 12.3 6.230	
+2.00	0.2	0.7886	0.2797	0.5915	0.	0.995	0.795	0.820	1.892	1.921	1.084 -101. 306. 12.2 6.120	
+2.00	0.3	0.7436	0.3529	0.4644	0.	0.945	0.755	0.783	1.942	1.971	1.084 -100. 266. 12.1 6.024	
+2.00	0.4	0.6949	0.4244	0.3369	0.	0.895	0.715	0.755	1.982	2.021	1.121 -111. 197. 12.0 5.924	
+2.00	0.5	0.6445	0.4965	0.2770	0.	0.845	0.675	0.715	1.932	2.071	1.161 -110. 159. 11.9 5.824	
+2.00	0.6	0.5932	0.5624	0.2340	0.	0.795	0.635	0.680	1.982	2.121	1.191 -109. 119. 11.8 5.724	
+2.00	0.7	0.5438	0.6296	0.1939	0.	0.745	0.595	0.635	2.032	2.171	1.191 -108. 119. 11.7 5.624	
+2.00	0.8	0.4936	0.6959	0.1498	0.	0.695	0.555	0.585	2.082	2.221	1.181 -107. 119. 11.6 5.524	
+2.00	0.9	0.4435	0.7623	0.0958	0.	0.645	0.515	0.515	2.132	2.271	1.171 -106. 119. 11.5 5.424	
+2.00	1.0	0.3943	0.8274	0.	0.595	0.475	0.475	1.982	2.321	1.121 -105. 119. 11.4 5.324		
+3.00	0.	0.9646	0.	0.9958	0.	1.205	0.755	0.785	1.893	1.952	1.022 -104. 166. 11.3 5.224	
+3.00	0.1	0.8571	0.0963	0.4791	0.	1.151	0.714	0.761	1.849	1.902	1.071 -103. 125. 11.2 5.124	
+3.00	0.2	0.7511	0.1625	0.3447	0.	1.091	0.674	0.711	1.898	1.952	1.020 -102. 119. 11.1 5.024	
+3.00	0.3	0.6511	0.2345	0.2349	0.	1.041	0.634	0.613	1.948	2.001	1.071 -101. 107. 11.0 4.924	
+3.00	0.4	0.5512	0.3064	0.1873	0.	0.991	0.594	0.573	1.998	2.051	1.111 -100. 967. 10.9 4.824	
+3.00	0.5	0.4513	0.3784	0.1439	0.	0.941	0.554	0.533	2.048	2.101	1.151 -99. 866. 10.8 4.724	
+3.00	0.6	0.3512	0.4464	0.1001	0.	0.891	0.514	0.493	2.098	2.151	1.191 -98. 766. 10.7 4.624	
+3.00	0.7	0.2512	0.5142	0.0561	0.	0.841	0.474	0.453	2.148	2.201	1.231 -97. 666. 10.6 4.524	
+3.00	0.8	0.1512	0.5822	0.0121	0.	0.791	0.434	0.413	2.198	2.251	1.271 -96. 566. 10.5 4.424	
+3.00	0.9	0.0512	0.6492	0.0081	0.	0.741	0.394	0.373	2.248	2.301	1.311 -95. 466. 10.4 4.324	
+3.00	1.0	0.0012	0.7162	0.	0.691	0.354	0.354	2.298	2.351	1.351 -94. 366. 10.3 4.224		
+4.00	0.	0.9872	0.	0.9972	0.	1.343	0.870	0.872	1.929	1.988	1.096 -103. 951. 10.2 4.124	
+4.00	0.1	0.8563	0.0954	0.3485	0.	1.293	0.830	0.863	1.978	2.037	1.147 -102. 852. 10.1 4.024	
+4.00	0.2	0.7593	0.1614	0.2885	0.	1.243	0.791	0.833	2.028	2.086	1.196 -101. 753. 10.0 3.924	
+4.00	0.3	0.6643	0.2333	0.2485	0.	1.193	0.751	0.780	2.076	2.145	1.245 -100. 653. 9.9 3.824	
+4.00	0.4	0.5653	0.3053	0.1944	0.	1.143	0.712	0.755	2.126	2.194	1.294 -99. 553. 9.8 3.724	
+4.00	0.5	0.4663	0.3773	0.1495	0.	1.093	0.672	0.725	2.175	2.254	1.334 -98. 453. 9.7 3.624	
+4.00	0.6	0.3674	0.4484	0.1055	0.	1.043	0.632	0.695	2.225	2.294	1.374 -97. 353. 9.6 3.524	
+4.00	0.7	0.2684	0.5194	0.0519	0.	0.993	0.592	0.668	2.275	2.344	1.414 -96. 253. 9.5 3.424	
+4.00	0.8	0.1694	0.5864	0.0076	0.	0.943	0.552	0.638	2.325	2.394	1.454 -95. 153. 9.4 3.324	
+4.00	0.9	0.0694	0.6534	0.0036	0.	0.893	0.512	0.588	2.375	2.443	1.494 -94. 053. 9.3 3.224	
+4.00	1.0	0.0094	0.7204	0.	0.843	0.472	0.472	2.425	2.493	1.534 -93. 953. 9.2 3.124		
+5.00	0.	0.9937	0.	0.9989	0.	1.492	0.909	0.919	1.774	1.834	1.174 -102. 153. 10.1 3.024	
+5.00	0.1	0.8642	0.0917	0.4549	0.	1.442	0.869	0.882	1.823	1.882	1.224 -101. 152. 10.0 2.924	
+5.00	0.2	0.7657	0.1636	0.3267	0.	1.392	0.829	0.842	1.872	1.931	1.272 -100. 151. 9.9 2.824	
+5.00	0.3	0.6661	0.2357	0.2933	0.	1.342	0.789	0.802	1.921	1.980	1.321 -99. 150. 9.8 2.724	
+5.00	0.4	0.5679	0.3074	0.1766	0.	1.292	0.749	0.773	1.971	2.039	1.371 -98. 150. 9.7 2.624	
+5.00	0.5	0.4686	0.3793	0.1292	0.	1.242	0.709	0.743	2.021	2.090	1.411 -97. 150. 9.6 2.524	
+5.00	0.6	0.3695	0.4491	0.0841	0.	1.192	0.669	0.714	2.071	2.140	1.451 -96. 150. 9.5 2.424	
+5.00	0.7	0.2682	0.5192	0.0398	0.	1.142						

Table 26. (continued)
TEMPERATURE = 215° R

LIQUID MOLE FRACTION		VAPOR MOLE FRACTION		PRESSURE		EQUIL CONST		RELATIVE VOL		ENTHALPY BTU/LB MOLE		HEAT CAPACITY BTU/LB MOLE-R				
N2	AR/AN=0.2	N2	AR	N2	ATH	N2	AR	O2	N2/AR	N2/02	AR/02	Liq	Vap	Liq	Vap	
+	0.	0.	0.	1.0000	9.80	2.103	1.265	1.000	1.663	2.103	1.264	+1130.	1285.	14.3	9.495	
+	0.1	0.	0.1210	0.8799	10.10	2.024	1.210	1.672	2.072	1.239	2.154.	1229.	14.3	9.274		
+	0.2	0.	0.2320	0.7673	10.38	1.958	1.184	0.959	1.881	2.041	1.214	+1178.	1178.	14.2	9.159	
+	0.3	0.	0.3378	0.6624	10.62	1.903	1.156	0.946	1.690	2.011	1.190	+1202.	1130.	14.2	8.951	
+	0.4	0.	0.4379	0.5626	10.84	1.859	1.084	0.938	1.760	1.982	1.164	+1228.	1384.	14.2	8.795	
+	0.5	0.	0.5339	0.4668	11.03	1.803	1.007	0.924	1.794	1.953	1.143	+1250.	1341.	14.1	8.640	
+	0.6	0.	0.6279	0.3732	11.20	1.756	0.905	0.913	1.718	1.925	1.120	+1274.	999.	14.1	8.480	
+	0.7	0.	0.7194	0.2865	11.34	1.716	0.828	0.926	1.728	1.897	1.098	+1298.	959.	14.1	8.314	
+	0.8	0.	0.8117	0.1886	11.45	1.763	0.519	0.943	1.737	1.870	1.078	+1321.	919.	14.0	8.139	
+	0.9	0.	0.8956	0.0953	11.54	1.715	0.166	0.953	1.747	1.843	1.058	+1345.	879.	14.0	7.951	
+	1.0	0.	1.0000	0.	12.00	1.757	0.000	0.967	1.797	1.834	1.034	+1369.	838.	14.0	7.744	
+0.25	0.	0.0785	0.	0.6468	10.13	2.033	1.226	0.974	1.688	2.088	1.259	+1107.	1279.	14.4	9.595	
+0.25	0.1	0.4912	0.	0.5346	10.43	1.961	1.177	0.953	1.666	2.058	1.235	+1132.	1226.	14.4	9.386	
+0.25	0.2	0.7475	0.	0.2213	10.69	1.912	1.135	0.938	1.679	2.088	1.211	+1156.	1177.	14.4	9.232	
+0.25	0.3	0.8463	0.	0.1327	10.83	1.893	1.105	0.926	1.684	1.999	1.187	+1179.	1131.	14.3	9.084	
+0.25	0.4	0.8453	0.	0.1727	10.97	1.873	1.073	0.916	1.693	1.971	1.164	+1202.	1087.	14.3	8.937	
+0.25	0.5	0.8445	0.	0.2044	11.02	1.779	1.045	0.916	1.702	1.943	1.141	+1225.	1046.	14.3	8.790	
+0.25	0.6	0.7428	0.	0.2994	11.08	1.753	1.025	0.916	1.711	1.915	1.117	+1249.	1005.	14.2	8.638	
+0.25	0.7	0.6424	0.	0.3682	11.12	1.735	1.008	0.916	1.721	1.886	1.097	+1272.	965.	14.2	8.481	
+0.25	0.8	0.5449	0.	0.4682	11.16	1.717	0.987	0.916	1.730	1.852	1.076	+1299.	926.	14.2	8.314	
+0.25	0.9	0.4429	0.	0.5974	11.18	1.698	0.962	0.916	1.749	1.819	1.056	+1319.	889.	14.1	8.136	
+0.25	1.0	0.3429	0.	0.7294	11.19	1.671	0.932	0.916	1.767	1.780	1.036	+1342.	851.	14.1	7.944	
+0.05	0.	0.93851	0.	0.15192	11.13	1.881	1.227	0.926	1.642	2.043	1.245	+1035.	1260.	14.6	9.869	
+0.05	0.1	0.91798	0.	0.09811	10.79	1.939	1.793	1.093	1.592	2.026	1.222	+1086.	1215.	14.6	9.739	
+0.05	0.2	0.81793	0.	0.19194	11.02	1.753	1.658	1.081	1.588	1.999	1.200	+1088.	1172.	14.7	9.615	
+0.05	0.3	0.71718	0.	0.27828	11.03	1.718	1.630	1.074	1.588	1.983	1.179	+1109.	1132.	14.7	9.493	
+0.05	0.4	0.61855	0.	0.36244	12.02	1.685	1.597	0.874	1.588	1.983	1.179	+1131.	1093.	14.7	9.372	
+0.05	0.5	0.51595	0.	0.44399	12.19	1.659	0.987	0.888	1.582	1.982	1.177	+1152.	1058.	14.7	9.248	
+0.05	0.6	0.41838	0.	0.52197	12.34	1.639	0.970	0.889	1.581	1.987	1.168	+1174.	1029.	14.6	9.170	
+0.05	0.7	0.31825	0.	0.6025	12.47	1.622	0.950	0.882	1.582	1.989	1.159	+1195.	985.	14.6	9.068	
+0.05	0.8	0.21815	0.	0.68165	12.58	1.604	0.925	0.878	1.587	1.988	1.150	+1217.	955.	14.6	8.843	
+0.05	0.9	0.11898	0.	0.75998	12.67	1.587	0.894	0.876	1.587	1.981	1.143	+1238.	917.	14.6	8.622	
+0.05	1.0	0.1189	0.	0.83994	12.74	1.569	0.853	0.876	1.582	1.972	1.139	+1260.	883.	14.5	8.398	
+0.08	0.	0.33159	0.	0.64686	12.44	1.659	1.024	0.856	1.582	1.985	1.125	+1035.	1260.	14.3	9.353	
+0.08	0.1	0.31798	0.	0.49811	12.45	1.623	0.988	0.857	1.582	1.982	1.126	+1078.	1197.	14.3	9.287	
+0.08	0.2	0.21535	0.	0.2994	12.46	1.593	0.975	0.851	1.584	1.981	1.127	+1107.	1161.	14.3	9.186	
+0.08	0.3	0.13251	0.	0.1919	12.47	1.564	0.955	0.851	1.584	1.981	1.128	+1137.	1127.	14.2	9.075	
+0.08	0.4	0.30849	0.	0.2994	12.48	1.534	0.934	0.851	1.584	1.981	1.129	+1167.	1085.	14.2	9.033	
+0.08	0.5	0.20524	0.	0.36888	12.51	1.506	0.915	0.851	1.584	1.981	1.130	+1195.	1045.	14.2	8.887	
+0.08	0.6	0.10223	0.	0.43484	12.51	1.489	0.891	0.851	1.584	1.981	1.131	+1224.	1033.	14.2	8.786	
+0.08	0.7	0.01111	0.	0.50532	12.52	1.461	0.861	0.850	1.582	1.980	1.132	+1253.	993.	14.1	8.682	
+0.08	0.8	0.00449	0.	0.58049	12.52	1.433	0.832	0.850	1.582	1.979	1.133	+1282.	953.	14.1	8.573	
+0.08	0.9	0.00214	0.	0.64686	12.52	1.405	0.803	0.850	1.582	1.978	1.134	+1311.	913.	14.1	8.464	
+0.08	1.0	0.00073	0.	0.70727	12.52	1.388	0.774	0.850	1.582	1.977	1.135	+1340.	873.	14.1	8.319	
+0.10	0.	0.44544	0.	0.6048	12.55	1.575	1.227	0.944	1.582	1.982	1.125	+1035.	1267.	14.3	9.353	
+0.10	0.1	0.43912	0.	0.4273	12.56	1.545	1.193	0.939	1.582	1.982	1.126	+1078.	1197.	14.3	9.287	
+0.10	0.2	0.31525	0.	0.2273	12.56	1.516	1.163	0.931	1.582	1.982	1.127	+1107.	1161.	14.3	9.186	
+0.10	0.3	0.21530	0.	0.1919	12.57	1.487	1.134	0.921	1.582	1.982	1.128	+1137.	1127.	14.2	9.075	
+0.10	0.4	0.24290	0.	0.24488	12.58	1.458	1.104	0.911	1.582	1.982	1.129	+1167.	1085.	14.2	9.033	
+0.10	0.5	0.19220	0.	0.30445	12.58	1.429	1.075	0.901	1.582	1.982	1.130	+1195.	1045.	14.2	8.887	
+0.10	0.6	0.11816	0.	0.37454	12.59	1.399	1.046	0.891	1.582	1.982	1.131	+1224.	1005.	14.2	8.786	
+0.10	0.7	0.05183	0.	0.44374	12.60	1.371	1.017	0.881	1.582	1.982	1.132	+1253.	965.	14.1	8.682	
+0.10	0.8	0.01913	0.	0.51735	12.60	1.343	0.988	0.881	1.582	1.982	1.133	+1282.	925.	14.1	8.573	
+0.10	0.9	0.00415	0.	0.58174	12.60	1.315	0.959	0.881	1.582	1.982	1.134	+1311.	885.	14.1	8.464	
+0.10	1.0	0.	0.000415	0.	0.64686	12.60	1.287	0.929	0.881	1.582	1.982	1.135	+1340.	845.	14.1	8.319
+0.12	0.	0.9423	0.	0.1521	12.62	1.573	1.227	0.944	1.582	1.982	1.125	+1035.	1267.	14.3	9.353	
+0.12	0.1	0.85925	0.	0.0823	12.63	1.544	1.198	0.935	1.582	1.982	1.126	+1078.	1197.	14.3	9.287	
+0.12	0.2	0.63522	0.	0.2637	12.63	1.515	1.169	0.925	1.582	1.982	1.127	+1107.	1161.	14.3	9.186	
+0.12	0.3	0.50212	0.	0.1228	12.64	1.486	1.139	0.915	1.582	1.982	1.128	+1137.	1121.	14.2	9.075	
+0.12	0.4	0.62723	0.	0.1922	12.64	1.457	1.109	0.905	1.582	1.982	1.129	+1167.	1085.	14.2	9.033	
+0.12	0.5	0.52420	0.	0.26111	12.65	1.428	1.079	0.905	1.582	1.982	1.130	+1195.	1045.	14.2	8.887	
+0.12	0.6	0.42133	0.	0.33299	12.65	1.399	1.050	0.905	1.582	1.982	1.131	+1224.	1005.	14.2	8.786	
+0.12	0.7	0.31212	0.	0.40324	12.66	1.371	1.021	0.905	1.582	1.982	1.132	+1253.	965.	14.1	8.682	
+0.12	0.8	0.19056	0.	0.47345	12.66	1.343	0.992	0.905	1.582	1.982	1.133	+1282.	925.	14.1	8.573	
+0.12	0.9	0.05182	0.	0.54352	12.66	1.315	0.963	0.905	1.582	1.98						

Table 26. (cont.)

TEMPERATURE = 220.9

LIQUID MOLE FRACTION	VAPOR MOLE FRACTION		PRESSURE	EQUIL CONST.			RELATIVE VOL	ENTHALPY BTU/LB MOLE	HEAT CAPACITY BTU/LB MOLE-R							
	N2	AR/AR+O2		N2	AR	O2										
+	0.1	0.	0.1594	0.889	11.82	2.003	1.245	1.000	1.411	2.003	1.244	+1058.	1289.	14.6	9.870	
+	0.2	0.	0.2394	0.7699	12.13	1.879	1.152	0.962	1.877	1.948	1.197	+1087.	1233.	14.6	9.720	
+	0.3	0.	0.3349	0.6655	12.40	1.828	1.118	0.951	1.835	1.920	1.174	+1106.	1180.	14.6	9.572	
+	0.4	0.	0.4346	0.5858	12.66	1.788	1.088	0.943	1.844	1.893	1.192	+1130.	1131.	14.6	9.427	
+	0.5	0.	0.5308	0.5097	12.89	1.753	1.062	0.939	1.852	1.867	1.190	+1178.	1140.	14.6	9.137	
+	0.6	0.	0.6208	0.3757	13.04	1.728	1.041	0.939	1.860	1.854	1.199	+1202.	997.	14.6	8.934	
+	0.7	0.	0.7177	0.2628	13.19	1.710	1.025	0.943	1.868	1.815	1.208	+1228.	955.	14.5	8.822	
+	0.8	0.	0.8108	0.1699	13.31	1.693	1.013	0.949	1.877	1.789	1.207	+1250.	913.	14.4	8.647	
+	0.9	0.	0.9002	0.0989	13.42	1.693	1.005	0.955	1.885	1.765	1.207	+1270.	872.	14.3	8.459	
+	1.0	0.	1.0001	0.	13.48	1.694	1.000	0.962	1.873	1.740	1.208	+1290.	83.	14.3	8.250	
+	0.1	0.1	0.1594	0.889	11.85	1.948	1.174	0.976	1.897	1.993	1.239	+1086.	1268.	14.6	9.905	
+	0.2	0.1	0.2370	0.7155	12.17	1.879	1.144	0.957	1.963	1.963	1.216	+1059.	1226.	14.6	9.851	
+	0.3	0.1	0.3246	0.5214	12.35	1.825	1.125	0.943	1.922	1.934	1.194	+1083.	1178.	14.7	9.713	
+	0.4	0.1	0.4245	0.3195	12.73	1.780	1.092	0.932	1.930	1.909	1.172	+1106.	1151.	14.7	9.570	
+	0.5	0.1	0.5243	0.2157	12.97	1.744	1.065	0.928	1.938	1.883	1.150	+1130.	1180.	14.7	9.444	
+	0.6	0.1	0.6202	0.1578	13.09	1.717	1.042	0.923	1.944	1.857	1.139	+1153.	1145.	14.7	9.305	
+	0.7	0.1	0.7143	0.0960	13.36	1.695	1.022	0.923	1.952	1.832	1.108	+1176.	1092.	14.7	9.156	
+	0.8	0.1	0.8087	0.0679	13.57	1.671	1.001	0.927	1.962	1.807	1.087	+1200.	961.	14.7	9.003	
+	0.9	0.1	0.8914	0.0368	13.73	1.653	0.986	0.933	1.972	1.782	1.067	+1223.	921.	14.7	8.837	
+	1.0	0.1	0.9744	0.0057	13.79	1.658	0.998	0.943	1.978	1.768	1.048	+1247.	881.	14.6	8.650	
+	0.1	0.2	0.1782	0.	12.95	1.762	1.120	0.914	1.992	1.955	1.207	+1026.	1262.	14.7	10.376	
+	0.2	0.2	0.2737	0.0976	13.24	1.733	1.084	0.900	1.993	1.925	1.204	+1092.	1215.	15.1	12.263	
+	0.3	0.2	0.3658	0.2776	13.57	1.688	1.058	0.884	1.913	1.871	1.183	+1135.	1175.	15.1	12.155	
+	0.4	0.2	0.4533	0.3622	13.79	1.630	1.026	0.860	1.922	1.852	1.144	+1156.	1089.	15.1	12.047	
+	0.5	0.2	0.5416	0.4443	13.99	1.580	0.987	0.876	1.937	1.822	1.124	+1178.	1054.	15.1	12.023	
+	0.6	0.2	0.6268	0.5248	14.11	1.538	0.958	0.894	1.944	1.795	1.098	+1200.	1024.	15.1	11.792	
+	0.7	0.2	0.7175	0.6043	14.25	1.497	0.928	0.900	1.942	1.763	1.068	+1221.	978.	15.1	11.573	
+	0.8	0.2	0.8056	0.6836	14.39	1.456	0.895	0.898	1.937	1.734	1.038	+1247.	942.	15.0	11.433	
+	0.9	0.2	0.8911	0.7642	14.56	1.416	0.864	0.898	1.928	1.705	1.008	+1270.	907.	15.0	11.260	
+	1.0	0.2	0.9761	0.8442	14.74	1.381	0.834	0.899	1.914	1.673	1.072	+1304.	871.	15.0	11.112	
+	0.1	0.3	0.3218	0.	12.95	1.469	1.024	0.848	1.972	1.897	1.207	+1087.	1233.	15.7	10.995	
+	0.2	0.3	0.3152	0.0799	13.21	1.456	1.056	0.840	1.974	1.876	1.208	+1101.	1194.	15.7	10.892	
+	0.3	0.3	0.3092	0.1564	13.43	1.438	1.084	0.835	1.978	1.854	1.176	+1120.	1157.	15.6	10.819	
+	0.4	0.3	0.3040	0.2330	13.68	1.401	1.124	0.831	1.980	1.833	1.153	+1139.	1129.	15.1	12.744	
+	0.5	0.3	0.2916	0.3144	13.91	1.367	1.152	0.830	1.982	1.805	1.134	+1156.	1089.	15.1	12.686	
+	0.6	0.3	0.2872	0.3912	14.05	1.330	1.182	0.830	1.983	1.779	1.113	+1178.	1055.	15.1	12.552	
+	0.7	0.3	0.2824	0.4680	14.19	1.293	1.212	0.829	1.983	1.752	1.092	+1197.	1024.	15.0	12.491	
+	0.8	0.3	0.2769	0.5473	14.30	1.250	1.243	0.828	1.982	1.722	1.071	+1214.	992.	15.0	12.392	
+	0.9	0.3	0.2704	0.6242	14.47	1.209	1.274	0.827	1.981	1.692	1.052	+1235.	952.	15.0	12.283	
+	1.0	0.3	0.2624	0.7020	14.60	1.169	1.301	0.826	1.980	1.659	1.032	+1274.	922.	15.0	12.131	
+	0.1	0.4	0.4412	0.	0.5567	15.08	1.470	0.949	0.798	1.952	1.844	1.189	+794.	1222.	16.2	11.479
+	0.2	0.4	0.4355	0.0882	15.09	1.450	0.931	0.794	1.957	1.826	1.173	+811.	1170.	16.2	11.340	
+	0.3	0.4	0.4291	0.1229	15.27	1.423	0.914	0.781	1.954	1.805	1.157	+827.	1140.	16.2	11.259	
+	0.4	0.4	0.4197	0.2491	15.35	1.390	0.880	0.770	1.957	1.780	1.142	+844.	1110.	16.2	11.154	
+	0.5	0.4	0.4152	0.3777	15.45	1.357	0.857	0.761	1.958	1.752	1.127	+861.	1082.	16.1	11.065	
+	0.6	0.4	0.4107	0.5062	15.56	1.327	0.834	0.751	1.958	1.722	1.112	+878.	1054.	16.1	11.051	
+	0.7	0.4	0.4062	0.6352	15.67	1.297	0.811	0.741	1.957	1.692	1.097	+895.	1026.	16.1	11.034	
+	0.8	0.4	0.4017	0.7647	15.75	1.267	0.788	0.730	1.957	1.662	1.082	+911.	1002.	16.1	11.023	
+	0.9	0.4	0.3962	0.8921	15.85	1.236	0.765	0.720	1.956	1.632	1.067	+928.	973.	16.1	11.014	
+	1.0	0.4	0.3924	0.9597	15.94	1.206	0.747	0.710	1.955	1.602	1.051	+945.	946.	16.1	11.049	
+	0.1	0.5	0.5245	0.	1.4857	17.37	1.361	0.888	0.799	1.931	1.775	1.207	+505.	1159.	18.7	12.855
+	0.2	0.5	0.5232	0.0519	17.40	1.346	0.877	0.798	1.938	1.777	1.207	+522.	1143.	18.7	12.857	
+	0.3	0.5	0.5233	0.1939	17.46	1.333	0.866	0.797	1.940	1.762	1.204	+539.	1117.	18.7	12.849	
+	0.4	0.5	0.5234	0.3421	17.54	1.310	0.854	0.796	1.944	1.747	1.191	+556.	1093.	18.7	12.830	
+	0.5	0.5	0.5235	0.4905	17.62	1.287	0.841	0.795	1.945	1.730	1.176	+573.	1064.	18.7	12.824	
+	0.6	0.5	0.5235	0.6385	17.70	1.264	0.828	0.795	1.946	1.715	1.162	+590.	1034.	18.7	12.814	
+	0.7	0.5	0.5236	0.7867	17.78	1.241	0.815	0.795	1.947	1.698	1.148	+607.	1004.	18.6	12.804	
+	0.8	0.5	0.5236	0.9349	17.86	1.218	0.802	0.795	1.948	1.680	1.130	+624.	975.	18.6	12.794	
+	0.9	0.5	0.5236	0.9831	17.94	1.195	0.789	0.795	1.948	1.660	1.115	+641.	945.	18.6	12.780	
+	1.0	0.5	0.5236	1.0313	18.02	1.172	0.776	0.795	1.948	1.640	1.100	+658.	915.	18.6	12.769	
+	0.1	0.6	0.5232	0.1277	18.10	1.149	0.763	0.785	1.948	1.620	1.085	+675.	886.	18.6	12.756	
+	0.2	0.6	0.5232	0.2759	18.18	1.126	0.750	0.775	1.948	1.600	1.070	+692.	856.	18.6	12.746	
+	0.3	0.6	0.5232	0.4241	18.26	1.103	0.737	0.765	1.948	1.580	1.055	+709.	826.	18.6	12.736	
+	0.4	0.6	0.5232	0.5722	18.34	1.079	0.724	0.755	1.948	1.560	1.040	+726.	796.	18.6	12.726	
+	0.5	0.6	0.5232	0.7193	18.42	1.056	0.711	0.745	1.948	1.540	1.025	+743.	766.	18.6	12.716	
+	0.6	0.														

Table 26. (cont.)
TEMPERATURE = 225. R

LIQUID MOLE FRACTION	VAPOR MOLE FRACTION	PRESSURE	EQUIL CONST			RELATIVE VOL	ENTHALPY BTU/LB MOLE		HEAT CAPACITY BTU/LB MOLE-R		
			N ₂	AR	O ₂		N ₂ /AR	N ₂ /O ₂	AR/O ₂	Liq	Vap
.0.	.0.	.0.	1.0005	1.35	1.923	1.226	1.000	1.569	1.922	1.225	-984. 1291. 15.1 15.391
.0.1	.0.	0.1179	0.8422	1.374	1.858	1.179	0.982	1.583	1.895	1.203	-1308. 1232. 15.1 15.253
.0.2	.0.	0.2280	0.7722	1.438	1.802	1.149	0.955	1.583	1.869	1.181	-1332. 1179. 15.1 15.125
.0.3	.0.	0.3320	0.6681	1.488	1.769	1.127	0.954	1.590	1.844	1.162	-1356. 1128. 15.1 9.998
.0.4	.0.	0.4310	0.5686	1.535	1.723	1.079	0.948	1.597	1.818	1.139	-1386. 1080. 15.1 9.872
.0.5	.0.	0.5280	0.4722	1.588	1.694	1.037	0.944	1.604	1.794	1.118	-1414. 1034. 15.1 9.735
.0.6	.0.	0.6223	0.3770	1.638	1.671	1.037	0.945	1.611	1.769	1.098	-1442. 996. 15.0 9.592
.0.7	.0.	0.7159	0.2845	1.675	1.655	1.023	0.948	1.619	1.745	1.078	-1452. 946. 15.0 9.433
.0.8	.0.	0.7937	0.1945	1.710	1.649	1.012	0.955	1.626	1.722	1.059	-1476. 894. 15.0 9.264
.0.9	.0.	0.8737	0.0945	1.754	1.640	1.004	0.965	1.633	1.699	1.040	-1496. 852. 15.0 9.173
.1.0	.0.	1.0002	0.	1.785	1.661	1.000	0.979	1.641	1.675	1.022	-1524. 819. 15.0 8.899
.0.05	.0.	0.0487	0.	1.935	1.777	1.194	0.978	1.564	1.903	1.221	-961. 1283. 15.0 10.532
.0.05	.0.1	0.1123	0.8427	1.413	1.819	1.151	0.965	1.571	1.884	1.199	-985. 1226. 15.0 10.488
.0.05	.0.2	0.1444	0.7279	1.787	1.746	1.139	0.947	1.578	1.956	1.178	-1008. 1176. 15.0 10.291
.0.05	.0.3	0.1733	0.6199	1.719	1.719	1.085	0.938	1.589	1.833	1.197	-1031. 1127. 15.0 10.175
.0.05	.0.4	0.1842	0.5143	1.651	1.686	1.059	0.932	1.592	1.809	1.137	-1055. 1081. 15.0 10.056
.0.05	.0.5	0.1949	0.4143	1.524	1.699	1.038	0.929	1.599	1.785	1.117	-1078. 1037. 15.0 9.929
.0.05	.0.6	0.2054	0.3156	1.462	1.711	1.016	0.926	1.606	1.761	1.097	-1101. 994. 15.0 9.794
.0.05	.0.7	0.2160	0.2173	1.394	1.682	1.006	0.923	1.613	1.735	1.078	-1125. 952. 15.0 9.646
.0.05	.0.8	0.2263	0.1766	1.353	1.613	0.998	0.920	1.620	1.715	1.059	-1146. 911. 15.0 9.482
.0.05	.0.9	0.2362	0.1675	1.303	1.608	0.998	0.915	1.627	1.693	1.041	-1172. 870. 15.0 9.351
.0.05	.1.0	0.2451	0.1510	1.250	1.609	0.998	0.905	1.634	1.671	1.028	-1196. 830. 15.0 9.100
.1.00	.0.	0.1722	0.	0.2280	2.499	1.702	2.110	0.972	2.395	1.727	-893. 1285. 15.0 51.000
.1.00	.0.1	0.1670	0.0970	0.7354	1.931	1.871	1.278	0.968	1.557	1.840	-915. 1212. 15.0 10.914
.1.00	.0.2	0.1641	0.1869	0.6472	1.860	1.841	1.190	0.969	1.563	1.826	-938. 1166. 15.0 10.828
.1.00	.0.3	0.1610	0.2769	0.5624	1.878	1.810	1.126	0.963	1.569	1.833	-958. 1123. 15.0 10.741
.1.00	.0.4	0.1583	0.3610	0.4801	1.817	1.803	1.095	0.969	1.578	1.878	-978. 1105. 15.0 10.646
.1.00	.0.5	0.1562	0.4444	0.3907	1.831	1.862	1.056	0.968	1.582	1.799	-1001. 1042. 15.0 10.546
.1.00	.0.6	0.1546	0.5226	0.3202	1.849	1.864	0.973	0.960	1.588	1.738	-1023. 1004. 15.0 10.438
.1.00	.0.7	0.1533	0.6058	0.2419	1.865	1.932	0.962	0.953	1.599	1.717	-1049. 986. 15.0 10.316
.1.00	.0.8	0.1529	0.6840	0.1619	1.877	1.925	0.953	0.949	1.601	1.696	-1066. 929. 15.0 10.179
.1.00	.0.9	0.1521	0.7646	0.0817	1.887	1.921	0.946	0.946	1.607	1.675	-1084. 893. 15.0 10.025
.1.00	.1.0	0.1521	0.8482	0.	1.884	1.922	0.943	0.939	1.614	1.656	-1100. 857. 15.0 9.882
.2.00	.0.	0.3131	0.	0.4873	1.645	1.564	1.022	0.899	1.533	1.622	-893. 1227. 14.1 11.749
.2.00	.0.1	0.3071	0.0799	0.134	1.670	1.539	0.995	0.882	1.538	1.612	-922. 1187. 14.1 11.705
.2.00	.0.2	0.3019	0.1565	0.3429	1.715	1.515	0.978	0.887	1.543	1.782	-941. 1149. 14.1 11.688
.2.00	.0.3	0.2875	0.2316	0.4725	1.737	1.487	0.954	0.884	1.548	1.763	-960. 1102. 14.1 10.646
.2.00	.0.4	0.2830	0.3024	0.5642	1.759	1.468	0.945	0.882	1.556	1.743	-979. 1076. 14.1 11.545
.2.00	.0.5	0.2805	0.3727	0.5370	1.777	1.452	0.937	0.882	1.559	1.724	-999. 1042. 14.1 11.479
.2.00	.0.6	0.2801	0.4419	0.2792	1.795	1.444	0.921	0.884	1.565	1.705	-1018. 1007. 14.1 11.403
.2.00	.0.7	0.2802	0.5114	0.2035	1.806	1.435	0.911	0.886	1.570	1.687	-1037. 977. 14.0 11.314
.2.00	.0.8	0.2856	0.5787	0.1366	1.820	1.425	0.894	0.893	1.576	1.669	-1056. 945. 14.0 11.211
.2.00	.0.9	0.2842	0.6471	0.0688	1.830	1.421	0.889	0.881	1.581	1.652	-1076. 914. 14.0 11.103
.2.00	.1.0	0.2841	0.7151	0.	1.836	1.421	0.889	0.869	1.585	1.634	-1095. 883. 14.0 10.987
.3.00	.0.	0.4319	0.	0.5683	1.429	1.344	0.955	0.812	1.514	1.711	-712. 1191. 14.0 12.688
.3.00	.0.1	0.4257	0.0944	0.501	1.852	1.409	0.935	0.805	1.515	1.730	-828. 1158. 14.0 12.583
.3.00	.0.2	0.4203	0.1288	0.451	1.733	1.401	0.925	0.805	1.520	1.739	-847. 1126. 14.0 12.475
.3.00	.0.3	0.4155	0.1955	0.3941	1.692	1.389	0.905	0.804	1.532	1.705	-879. 1085. 14.0 12.360
.3.00	.0.4	0.4117	0.2506	0.3378	1.618	1.372	0.886	0.804	1.537	1.722	-905. 1055. 14.0 12.260
.3.00	.0.5	0.4083	0.3101	0.2819	1.582	1.361	0.866	0.805	1.538	1.705	-928. 1026. 14.0 12.160
.3.00	.0.6	0.4054	0.3845	0.2262	1.541	1.356	0.877	0.808	1.541	1.674	-951. 997. 14.0 12.060
.3.00	.0.7	0.4035	0.4244	0.1704	1.504	1.345	0.870	0.811	1.546	1.656	-973. 967. 14.0 11.960
.3.00	.0.8	0.4020	0.4841	0.1142	1.466	1.340	0.864	0.816	1.550	1.642	-993. 932. 14.0 11.848
.3.00	.0.9	0.4011	0.5417	0.0575	1.475	1.337	0.865	0.822	1.555	1.627	-1013. 904. 14.0 11.744
.3.00	.1.0	0.4008	0.5996	0.	1.484	1.336	0.857	0.829	1.560	1.612	-1033. 879. 14.0 12.684
.4.00	.0.	0.5351	0.	0.4454	1.998	1.358	0.895	0.770	1.494	1.723	-822. 1192. 13.1 13.933
.4.00	.0.1	0.5293	0.0530	0.4180	2.017	1.324	0.864	0.774	1.498	1.710	-838. 1164. 13.1 13.871
.4.00	.0.2	0.5244	0.1400	0.3711	2.035	1.311	0.873	0.773	1.502	1.698	-859. 1097. 13.1 14.003
.4.00	.0.3	0.5201	0.1955	0.3247	2.053	1.300	0.864	0.773	1.505	1.682	-878. 1055. 13.1 14.024
.4.00	.0.4	0.5163	0.2053	0.2786	2.068	1.291	0.855	0.774	1.509	1.663	-893. 1021. 13.1 14.050
.4.00	.0.5	0.5108	0.2621	0.2240	2.023	1.282	0.848	0.776	1.512	1.641	-912. 997. 13.1 14.048
.4.00	.0.6	0.5085	0.3312	0.1806	2.017	1.271	0.836	0.761	1.517	1.620	-932. 974. 13.1 14.034
.4.00	.0.7	0.5070	0.3993	0.0942	2.018	1.267	0.831	0.755	1.520	1.605	-957. 951. 13.1 14.007
.4.00	.0.8	0.5059	0.4469	0.0474	2.028	1.265	0.828	0.750	1.524	1.592	-975. 928. 13.1 13.966
.4.00	.0.9	0.5054	0.4948	0.	2.036	1.264	0.824	0.749	1.532	1.589	-996. 906. 13.1 13.908
.4.00	.1.0	0.5025	0.5427	0.0316	2.035	1.262	0.820	0.747	1.537	1.575	-1016. 883. 13.1 13.855
.5.00	.0.	0.6265	0.	0.3739	2.176	1.293	0.869	0.748	1.474	1.676	-1137. 953. 12.0 15.888
.5.00	.0.1	0.6219	0.0427	0.3364	2.191	1.244	0.842	0.747	1.477	1.684	-1127. 943. 12.0 15.774
.5.00	.0.2	0.6170	0.0355	0.2991	2.06	1.235	0.835	0.745	1.480	1.697	-1117. 959. 12.0 15.696
.5.00	.0.3	0.6141	0.1243	0.2620	2.020	1.228	0.828	0.749	1.483	1.681	-1101. 961. 12.0 15.596
.5.00	.0.4	0.6115	0.1645	0.2240	2.033	1.220	0.820	0.749	1.485	1.671	-1087. 947. 12.0 15.492
.5.00	.0.5	0.6082	0.2043	0.1870	2.045	1.216	0.817	0.752	1.489	1.662	-1070. 939. 12.

TEMPERATURE = 230. R

Table 26. (cont.)

LIQUID MOLE FRACTION	VAPOR MOLE FRACTION		PRESSURE	EQUIL CONST	RELATIVE VOL	ENTHALPY		HEAT CAPACITY				
	N2	AR/AR+O2				N2	AR	O2	BTU/LB MOLE	BTU/LB MOLE-R		
.0.	.0.	.0.	1.0002	15.44	1.855	1.207	1.000	1.936	1.055	1.207	-907. 1200.	19.6 11.012
.1	.0.	.0.	0.1165 0.0837	15.86	1.707	1.149	0.902	1.943	1.030	1.186	-931. 1229.	19.6 10.908
.2	.0.	.0.	0.2257 0.7745	16.23	1.746	1.129	0.968	1.949	1.056	1.186	-955. 1174.	19.6 10.808
.3	.0.	.0.	0.3294 0.4708	16.57	1.706	1.098	0.938	1.955	1.072	1.146	-979. 1122.	19.6 10.708
.4	.0.	.0.	0.4226 0.3713	16.86	1.674	1.072	0.952	1.961	1.090	1.126	-1003. 1072.	19.6 10.598
.5	.0.	.0.	0.5226 0.4740	17.12	1.646	1.051	0.950	1.967	1.115	1.107	-1027. 1025.	19.6 10.480
.6	.0.	.0.	0.6223 0.3408	17.34	1.627	1.034	0.950	1.974	1.132	1.084	-1052. 979.	19.6 10.349
.7	.0.	.0.	0.7142 0.2062	17.52	1.612	1.020	0.954	1.981	1.150	1.073	-1076. 935.	19.6 10.200
.8	.0.	.0.	0.8082 0.1921	17.67	1.593	1.010	0.961	1.986	1.166	1.062	-1100. 891.	19.6 10.050
.9	.0.	.0.	0.8933 0.0971	17.77	1.595	1.004	0.971	1.993	1.147	1.034	-1124. 847.	19.6 9.830
1.0	.0.	.0.	1.0004 0.	17.83	1.600	1.000	0.984	1.999	1.126	1.017	-1149. 804.	19.6 9.619
.225	.0.	.0.	0.4510 0.5551	15.89	1.803	1.198	0.988	1.932	1.043	1.233	-884. 1200.	19.7 11.191
.225	.1	.0.	0.4436 0.1111 0.0494	16.30	1.753	1.139	0.943	1.938	1.019	1.183	-907. 1222.	19.7 11.101
.225	.2	.0.	0.4427 0.2157 0.7419	16.66	1.708	1.086	0.951	1.944	1.076	1.143	-931. 1176.	19.7 11.013
.225	.3	.0.	0.4416 0.3192 0.6433	16.98	1.671	1.078	0.943	1.950	1.172	1.143	-954. 1129.	19.7 10.923
.225	.4	.0.	0.4410 0.4110 0.4784	17.27	1.644	1.054	0.937	1.956	1.190	1.124	-978. 1072.	19.7 10.825
.225	.5	.0.	0.4404 0.5040 0.4560	17.52	1.615	1.034	0.935	1.962	1.227	1.109	-1001. 1027.	19.7 10.717
.225	.6	.0.	0.4399 0.5954 0.3651	17.73	1.590	1.018	0.936	1.968	1.269	1.087	-1025. 982.	19.7 10.599
.225	.7	.0.	0.4399 0.6859 0.2749	17.93	1.593	1.005	0.940	1.975	1.304	1.069	-1048. 939.	19.7 10.456
.225	.8	.0.	0.4393 0.7745 0.1846	18.05	1.574	0.996	0.947	1.981	1.342	1.052	-1072. 897.	19.7 10.296
.225	.9	.0.	0.4392 0.8680 0.0932	18.16	1.570	0.989	0.956	1.987	1.381	1.034	-1095. 855.	19.7 10.113
1.00	.0.	.0.	0.4393 0.9612 0.	18.22	1.571	0.984	0.969	1.993	1.381	1.017	-1119. 813.	19.7 9.944
.100	.0.	.0.	0.4374 0.5330	17.27	1.674	1.081	0.926	1.920	1.088	1.170	-814. 1253.	19.1 11.784
.100	.1	.0.	0.4334 0.0944 0.7467	17.62	1.634	1.071	0.914	1.925	1.087	1.171	-836. 1284.	19.1 11.744
.100	.2	.0.	0.4199 0.1881 0.6924	17.95	1.600	1.045	0.906	1.933	1.075	1.153	-857. 1197.	19.1 11.652
.100	.3	.0.	0.4176 0.2760 0.5672	18.25	1.570	1.022	0.909	1.938	1.074	1.135	-879. 1112.	19.1 11.530
.100	.4	.0.	0.4144 0.3611 0.4845	18.51	1.546	1.003	0.897	1.942	1.073	1.110	-901. 1059.	19.1 11.464
.100	.5	.0.	0.4127 0.4441 0.4034	18.74	1.527	0.987	0.896	1.947	1.073	1.091	-922. 1020.	19.1 11.405
.100	.6	.0.	0.4112 0.5257 0.3233	18.94	1.512	0.974	0.898	1.953	1.083	1.084	-944. 988.	19.1 11.392
.100	.7	.0.	0.4100 0.6067 0.2435	19.11	1.500	0.963	0.902	1.959	1.083	1.068	-966. 949.	19.1 11.281
.100	.8	.0.	0.4083 0.6875 0.1635	19.24	1.493	0.955	0.906	1.964	1.084	1.051	-987. 911.	19.1 11.150
.100	.9	.0.	0.4069 0.7688 0.0829	19.35	1.489	0.945	0.917	1.969	1.085	1.036	-1008. 874.	19.1 10.996
1.00	.0.	.0.	0.4059 0.8513 0.	19.42	1.480	0.944	0.927	1.973	1.086	1.023	-1028. 831.	19.1 10.817
.200	.0.	.0.	0.4059 0.6844	19.13	1.529	1.018	0.881	1.983	1.172	1.172	-721. 2157.	18.8 12.790
.200	.1	.0.	0.4003 0.7797 0.6229	19.43	1.562	0.998	0.881	1.988	1.173	1.196	-746. 1173.	18.8 12.792
.200	.2	.0.	0.3959 0.1564 0.5484	19.71	1.470	0.977	0.897	1.991	1.175	1.141	-759. 1133.	18.8 12.788
.200	.3	.0.	0.3919 0.2366 0.4783	19.97	1.457	0.961	0.894	1.997	1.176	1.125	-779. 1095.	18.8 12.777
.200	.4	.0.	0.3880 0.3262 0.4094	20.19	1.446	0.947	0.893	2.001	1.188	1.110	-796. 1058.	18.8 12.759
.200	.5	.0.	0.3852 0.3737 0.3414	20.40	1.436	0.934	0.894	2.006	1.197	1.095	-817. 1023.	18.8 12.719
.200	.6	.0.	0.3829 0.4433 0.2738	20.56	1.425	0.924	0.896	2.011	1.201	1.080	-837. 988.	18.8 12.668
.200	.7	.0.	0.3813 0.5122 0.2063	20.73	1.416	0.916	0.896	2.016	1.203	1.065	-856. 955.	18.8 12.594
.200	.8	.0.	0.3801 0.5919 0.1304	20.86	1.401	0.907	0.895	2.021	1.209	1.051	-875. 922.	18.8 12.507
.200	.9	.0.	0.3795 0.6512 0.0698	20.97	1.397	0.904	0.872	2.025	1.203	1.037	-894. 889.	18.8 12.393
1.00	.0.	.0.	0.3794 0.7210 0.	21.15	1.397	0.901	0.861	2.030	1.205	1.023	-914. 857.	18.8 12.253
.300	.0.	.0.	0.3724 0.5748	21.03	1.413	0.951	0.824	1.985	1.176	1.195	-628. 1172.	17.0 14.130
.300	.1	.0.	0.4181 0.0855 0.5166	21.30	1.394	0.936	0.820	1.989	1.170	1.141	-645. 1136.	17.0 14.192
.300	.2	.0.	0.4131 0.1291 0.4580	21.54	1.377	0.922	0.810	1.993	1.164	1.120	-662. 1103.	17.0 14.244
.300	.3	.0.	0.4080 0.1912 0.4003	21.76	1.363	0.910	0.817	1.997	1.158	1.101	-670. 1070.	17.0 14.287
.300	.4	.0.	0.4031 0.2529 0.3432	21.96	1.350	0.900	0.817	2.001	1.153	1.081	-688. 1039.	17.0 14.317
.300	.5	.0.	0.4021 0.3118 0.2864	22.14	1.340	0.891	0.810	2.005	1.146	1.068	-712. 1008.	17.0 14.333
.300	.6	.0.	0.3996 0.3709 0.2299	22.31	1.332	0.883	0.821	2.008	1.133	1.076	-729. 978.	17.0 14.331
.300	.7	.0.	0.3977 0.4295 0.1731	22.49	1.326	0.876	0.824	2.012	1.126	1.063	-746. 949.	17.0 14.310
.300	.8	.0.	0.3963 0.4879 0.1161	22.57	1.321	0.871	0.829	2.016	1.113	1.051	-763. 921.	17.0 14.266
.300	.9	.0.	0.3956 0.5463 0.0984	22.66	1.319	0.867	0.835	2.021	1.107	1.039	-780. 893.	17.0 14.198
1.00	.0.	.0.	0.3953 0.6020 0.	22.76	1.318	0.861	0.842	2.025	1.105	1.027	-796. 866.	17.0 14.104
.400	.0.	.0.	0.3828 0.4733	23.03	1.317	0.868	0.765	1.987	1.089	1.130	-555. 1121.	17.5 16.095
.400	.1	.0.	0.3527 0.3933 0.4294	23.29	1.304	0.866	0.766	1.970	1.056	1.127	-569. 1092.	17.5 16.231
.400	.2	.0.	0.3172 0.1034 0.3779	23.45	1.293	0.878	0.767	1.973	1.042	1.119	-584. 1064.	17.5 16.359
.400	.3	.0.	0.3132 0.1565 0.3368	23.64	1.283	0.869	0.768	1.976	1.029	1.104	-598. 1036.	17.5 16.477
.400	.4	.0.	0.3099 0.2048 0.2839	23.82	1.274	0.862	0.769	1.979	1.016	1.082	-612. 1007.	17.5 16.588
.400	.5	.0.	0.3067 0.2585 0.2371	23.99	1.267	0.855	0.780	1.982	1.003	1.082	-627. 983.	17.5 16.668
.400	.6	.0.	0.3043 0.3057 0.1908	24.14	1.261	0.849	0.793	1.985	1.001	1.071	-642. 957.	17.5 16.737
.400	.7	.0.	0.3025 0.3545 0.1433	24.27	1.256	0.844	0.796	1.988	1.001	1.061	-656. 932.	17.5 16.785
.400	.8	.0.	0.3011 0.4032 0.0980	24.39	1.253	0.840	0.800	1.991	1.001	1.050	-669. 908.	17.5 16.869
.400	.9	.0.	0.3002 0.4518 0.0483	24.46	1.251	0.837	0.803	1.993	1.004	1.040	-685. 884.	17.5 16.895
.400	1.0	.0.	0.2999 0.5002 0.	24.50	1.250	0.834	0.810	1.998	1.002	1.030	-697. 861.	17.5 16.771
.500	.0.	.0.	0.3186 0.3818	25.17	1.237	0.856	0.764	1.948	1.020	1.121	-442. 1059.	18.0 19.349
.500	.1	.0.	0.3144 0.4024 0.3436	25.35	1.223	0.849	0.764	1.948	1.019	1.112	-454. 1034.	18.0 19.623
.500	.2	.0.	0.3109 0.4642 0.3056	25.53	1.221	0.842	0.764	1.950	1.008	1.102	-	

Table 26. (con't.)

TEMPERATURE = 235° R

LIQUID MOLE FRACTION	VAPOR MOLE FRACTION	PRESSURE	EQUIL CONST			RELATIVE VOL			ENTHALPY			HEAT CAPACITY		
			N2	AR/AR+O2	N2	AR	O2	N2/AR	N2/O2	AR/O2	BTU/LB MOLE	BTU/LB MOLE-R	Liq	Vap
0+	0+	1.0004	17.73	1.809	1.191	1.000	1.519	1.804	1.191	1.000	-827.	1281.	16.2	11.790
0.1	0.	0.1152 0.8852	18.20	1.782	1.182	0.984	1.517	1.780	1.182	0.984	-822.	1221.	16.2	11.729
0.2	0.	0.2237 0.7767	18.61	1.737	1.119	0.971	1.526	1.798	1.152	0.976	-876.	1164.	16.2	11.669
0.3	0.	0.3271 0.6734	18.98	1.678	1.093	0.962	1.532	1.736	1.133	0.965	-905.	1111.	16.2	11.603
0.4	0.	0.4265 0.5737	19.32	1.636	1.056	0.956	1.537	1.734	1.115	0.954	-939.	1059.	16.2	11.532
0.5	0.	0.5232 0.4770	19.63	1.514	1.048	0.948	1.543	1.682	1.097	0.948	-968.	1010.	16.2	11.435
0.6	0.	0.6193 0.3819	19.84	1.495	1.030	0.935	1.548	1.671	1.070	0.932	-983.	983.	16.2	11.319
0.7	0.	0.7176 0.2876	20.04	1.482	1.018	0.929	1.594	1.650	1.042	0.928	-998.	917.	16.2	11.183
0.8	0.	0.8071 0.1931	20.19	1.473	1.005	0.915	1.599	1.629	1.015	0.915	-1000.	872.	16.2	11.070
0.9	0.	0.8927 0.0975	20.30	1.470	1.003	0.975	1.595	1.609	1.002	0.975	-1044.	826.	16.2	10.825
1.0	0.	1.0002 0.	20.36	1.471	1.000	0.998	1.570	1.599	1.002	0.998	-1068.	783.	16.2	10.596
.025	0+	0.0440 0+	18.25	1.785	1.164	0.981	1.511	1.793	1.187	0.984	-824.	1272.	16.3	12.326
.025	0.1	0.0428 0.1102 0.8477	18.70	1.711	1.128	0.966	1.517	1.771	1.168	0.977	-827.	1214.	16.3	11.932
.025	0.2	0.0417 0.2139 0.7444	19.11	1.668	1.097	0.955	1.522	1.749	1.149	0.951	-851.	1159.	16.3	11.932
.025	0.3	0.0409 0.3131 0.6462	19.47	1.635	1.073	0.947	1.527	1.727	1.121	0.947	-874.	1107.	16.3	11.889
.025	0.4	0.0402 0.4049 0.5511	19.78	1.617	1.046	0.942	1.533	1.706	1.113	0.938	-898.	1098.	16.3	11.851
.025	0.5	0.0393 0.4922 0.4564	20.05	1.584	1.030	0.940	1.538	1.685	1.095	0.921	-911.	1058.	16.3	11.737
.025	0.6	0.0389 0.5939 0.3672	20.29	1.547	1.013	0.942	1.543	1.668	1.078	0.915	-925.	1018.	16.3	11.637
.025	0.7	0.0386 0.6849 0.2769	20.49	1.554	1.002	0.945	1.549	1.644	1.051	0.908	-938.	977.	16.3	11.513
.025	0.8	0.0387 0.7760 0.1857	20.64	1.544	0.995	0.952	1.554	1.624	1.025	0.902	-952.	937.	16.3	11.380
.025	0.9	0.0388 0.8680 0.0937	20.79	1.543	0.988	0.961	1.559	1.604	1.028	0.901	-965.	894.	16.3	11.176
.025	1.0	0.0386 0.9617 0-	20.93	1.544	0.988	0.974	1.565	1.595	1.033	0.901	-978.	851.	16.3	10.987
.100	0.	0.3437 0-	18.82	1.637	1.091	0.930	1.503	1.781	1.174	0.930	-1240.	18.7	18.839	
.100	0.1	0.1400 0.0997 0.7446	20.22	1.690	1.083	0.918	1.505	1.741	1.157	0.914	-124.	1189.	18.7	18.846
.100	0.2	0.1960 0.1870 0.6364	20.59	1.589	1.039	0.912	1.511	1.721	1.140	0.904	-126.	1149.	18.6	18.848
.100	0.3	0.1942 0.2749 0.5732	20.93	1.542	1.018	0.897	1.514	1.701	1.123	0.897	-129.	1094.	18.6	18.841
.100	0.4	0.1920 0.3602 0.4882	21.28	1.520	1.001	0.884	1.519	1.681	1.107	0.884	-131.	1050.	18.6	18.819
.100	0.5	0.1902 0.4435 0.4086	21.48	1.502	0.988	0.864	1.524	1.662	1.097	0.874	-134.	1007.	18.6	18.780
.100	0.6	0.1488 0.5294 0.3260	21.67	1.486	0.973	0.859	1.529	1.643	1.078	0.862.	-136.	966.	18.6	18.737
.100	0.7	0.1478 0.6671 0.2455	21.86	1.478	0.964	0.859	1.533	1.625	1.060	0.854	-138.	926.	18.6	18.629
.100	0.8	0.1471 0.6685 0.1648	22.01	1.471	0.956	0.851	1.538	1.607	1.049	0.846	-140.	886.	18.6	18.552
.100	0.9	0.1466 0.7703 0.0631	22.12	1.468	0.941	0.844	1.543	1.589	1.032	0.837	-142.	846.	18.6	18.456
.100	1.0	0.1466 0.8536 0-	22.19	1.468	0.948	0.874	1.546	1.572	1.019	0.836	-144.	806.	18.6	18.370
.200	0+	0.3505 0- 0.6900	21.97	1.593	1.023	0.879	1.569	1.717	1.157	0.877	-1193.	17.1	14.297	
.200	0.1	0.2993 0.0794 0.6259	22.33	1.577	0.999	0.869	1.588	1.703	1.142	0.858.	-1159.	17.1	14.278	
.200	0.2	0.2979 0.1559 0.5534	22.44	1.545	0.976	0.865	1.592	1.682	1.127	0.858.	-1158.	17.1	14.255	
.200	0.3	0.2873 0.2330 0.4929	22.53	1.526	0.959	0.862	1.596	1.663	1.113	0.858.	-1158.	17.1	14.231	
.200	0.4	0.2839 0.3120 0.4135	22.59	1.496	0.946	0.862	1.601	1.643	1.098	0.858.	-1158.	17.1	14.197	
.200	0.5	0.2813 0.3746 0.3449	22.64	1.467	0.936	0.862	1.606	1.624	1.087	0.858.	-1158.	17.1	14.173	
.200	0.6	0.2793 0.4444 0.2767	22.69	1.438	0.926	0.865	1.610	1.605	1.075	0.858.	-1158.	17.1	14.157	
.200	0.7	0.2777 0.5142 0.2085	22.74	1.409	0.916	0.869	1.614	1.586	1.065	0.858.	-1158.	17.1	14.139	
.200	0.8	0.2767 0.5838 0.1398	22.78	1.380	0.906	0.872	1.618	1.567	1.055	0.858.	-1158.	17.1	14.123	
.200	0.9	0.2761 0.6537 0.0709	22.84	1.351	0.896	0.881	1.621	1.547	1.044	0.858.	-1158.	17.1	14.106	
.200	1.0	0.2701 0.7243 0-	22.94	1.322	0.886	0.889	1.625	1.528	1.034	0.858.	-1158.	17.1	14.086	
.300	0.	0.4127 0- 0.5827	24.25	1.592	0.949	0.832	1.593	1.730	1.142	0.837.	-1193.	17.1	14.297	
.300	0.1	0.4124 0.0694 0.5226	24.55	1.577	0.935	0.829	1.597	1.711	1.124	0.822.	-1159.	17.1	14.293	
.300	0.2	0.4077 0.1291 0.4634	24.83	1.559	0.922	0.822	1.602	1.692	1.114	0.812.	-1159.	17.1	14.264	
.300	0.3	0.4037 0.1914 0.4052	25.18	1.534	0.911	0.827	1.607	1.673	1.104	0.802.	-1159.	17.1	14.244	
.300	0.4	0.4003 0.2525 0.3479	25.31	1.513	0.902	0.822	1.612	1.654	1.095	0.792.	-1159.	17.1	14.229	
.300	0.5	0.3982 0.3127 0.2901	25.52	1.484	0.893	0.829	1.613	1.635	1.086	0.782.	-1159.	17.1	14.209	
.300	0.6	0.3952 0.3723 0.2320	25.71	1.457	0.886	0.832	1.614	1.616	1.076	0.772.	-1159.	17.1	14.187	
.300	0.7	0.3935 0.4319 0.1754	25.87	1.432	0.881	0.835	1.615	1.597	1.067	0.762.	-1159.	17.1	14.167	
.300	0.8	0.3922 0.4979 0-	25.93	1.411	0.871	0.832	1.616	1.578	1.058	0.752.	-1159.	17.1	14.147	
.300	0.9	0.3907 0.5547 0-	25.98	1.390	0.861	0.831	1.617	1.559	1.049	0.742.	-1159.	17.1	14.127	
.300	1.0	0.3892 0.6120 0-	26.04	1.369	0.851	0.830	1.618	1.540	1.040	0.732.	-1159.	17.1	14.106	
.400	0.	0.4140 0- 0.5395	27.73	1.614	1.081	0.932	1.643	1.731	1.189	0.647.	-1219.	17.3	14.322	
.400	0.1	0.3980 0.0949 0.4743	25.16	1.580	1.055	0.923	1.647	1.712	1.143	0.609.	-1169.	17.3	14.420	
.400	0.2	0.3595 0.1899 0.3933	25.27	1.550	1.033	0.918	1.652	1.684	1.104	0.591.	-1114.	17.3	14.532	
.400	0.3	0.3195 0.2738 0.3174	25.34	1.525	1.013	0.911	1.656	1.654	1.074	0.573.	-1068.	17.3	14.622	
.400	0.4	0.3195 0.3598 0.3908	25.47	1.503	0.997	0.909	1.660	1.626	1.057	0.554.	-1024.	1068.	17.3	14.711
.400	0.5	0.3195 0.4425 0.4050	25.55	1.484	0.983	0.909	1.665	1.606	1.042	0.536.	-976.	975.	17.2	14.731
.400	0.6	0.3175 0.5249 0.3279	25.68	1.455	0.972	0.901	1.670	1.587	1.027	0.517.	-926.	922.	17.2	14.737
.400	0.7	0.3166 0.6068 0.2479	25.80	1.436	0.963	0.919	1.672	1.561	1.010	0.500.	-880.	890.	17.2	14.708
.400	0.8	0.3160 0.6887 0.1687	25.17	1.409	0.954	0.921	1.676	1.535	0.993	0.481.	-821.	850.	17.2	14.614
.400	0.9	0.3157 0.7571 0.0886	25.28	1.387	0.947	0.929	1.680	1.509	0.985	0.443.	-843.	81		

APPENDIX III

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APPENDIX IV
 NOMENCLATURE TABLE

A_i	= Area of Chromatograph Peak, Section IV-B
A_{ij}	= Binary interaction coefficient, Section VI-E
Ar	= Argon
a_{ij}	= Constant in binary interaction coefficient, Section VI-E and Section VIII
B	= Second virial coefficient, Section VI-D and Section VIII-D
B_{ij}	= Mixture second virial coefficient, Section VI-D
b_{ij}	= Constant in binary interaction coefficient, Section VI-E and Section VII
C	= Third virial coefficient, Section VI-D and Section VIII-D
C_{ijk}	= Mixture third virial coefficient, Section VI-D
C_p	= Heat capacity at constant pressure
C_s	= Heat capacity of saturated fluid
c	= Number of components, Section VI-A
F	= Degrees of freedom of system, Section VI-A
$^{\circ}F$	= Degrees, Fahrenheit scale
f_i	= Fugacity of component i
f_i^*	= Fugacity of pure liquid component at the pressure and temperature of mixing
G^E	= Excess free energy
G_i	= Free energy of component i
H	= Enthalpy
H_{gi}	= Enthalpy of the real gas, pure component
H_{gi}°	= Enthalpy of the real liquid, pure component

HOMENCLATURE TABLE (continued)

h_i^*	= Ideal gas (zero pressure) enthalpy
$h_{liq.}$	= Liquid phase enthalpy
d_m	= heat of mixing
$d_{vap.}$	= Vapor phase enthalpy
K	= Equilibrium constant, Appendix I-A
d_2	= Nitrogen
O_2	= Oxygen
P	= Number of phases, Section VI-A
p	= Total pressure of the vapor
p_i^o	= Vapor pressure of pure component i
p_m	= Pressure of mixing
q_i	= Relative response factor, Section IV-B
R	= Gas constant
oR	= Degrees, Rankine scale
S	= Van Laar Volume, Section VI-E and Section VII
T	= Temperature, degrees Rankine
V	= Molar volume of vapor, Section VI-D
V	= Liquid volume in cc/gm-mole, Section VI-B
v_i^o	= Molal volume of pure component i
\bar{v}_i	= Partial molal volume of component i
x	= Temperature oR divided by 100, Section VI-B
x_i	= Mole fraction of component i in the liquid
y_i	= Mole fraction of component i in the vapor.
Z	= Compressibility factor

NOMENCLATURE TABLE (continued)

- α = Relative volatility, Appendix I, Sections B, C, and D
 γ_i = Activity coefficient of component i in the liquid
 γ_{π} = Pressure activity coefficient, Appendix I-E
 ΔG = Change in free energy
 $\overline{\Delta l}_{mi}$ = Partial molal heat of mixing
 Δl_{vi}^o = Latent heat
 ϕ_i = Fugacity coefficient of component i
 ϕ_i^o = Fugacity coefficient of pure component i