

APL TDR 64-64

30

✓
B2

ARGON-OXYGEN-NITROGEN THREE COMPONENT SYSTEM EXPERIMENTAL VAPOR-LIQUID EQUILIBRIUM DATA

TECHNICAL DOCUMENTARY REPORT NO. APL TDR 64-64
APRIL 1964

AD No. 603151

DDC FILE COPY

AF Aero Propulsion Laboratory
Research and Technology Division
Air Force Systems Command
Wright-Patterson Air Force Base, Ohio

PROJECT NO. 3048, TASK NO. 30193

DDC
RECEIVED
AUG 4 1964
DDC-IRA C

(Prepared under Contract No. AF 33(657)-8742
by Air Products and Chemicals, Inc., Research and
Development Department, Allentown, Pa.; G. M. Wilson,
P. M. Silverberg, and M. G. Zellner, authors)

343

AD No. 603151

DDC FILE COPY

APL TDR 64-64

ARGON-OXYGEN-NITROGEN THREE COMPONENT SYSTEM
EXPERIMENTAL VAPOR-LIQUID EQUILIBRIUM DATA

TECHNICAL DOCUMENTARY REPORT NO. APL TDR 64-64

April 1964

AF Aero Propulsion Laboratory
Research and Technology Division
Air Force Systems Command
Wright-Patterson Air Force Base, Ohio

Project No. 3048, Task No. 30193

(Prepared under Contract No. AF 33(657)-8742
by Air Products and Chemicals, Inc., Research and
Development Department, Allentown, Pa.; G. M. Wilson,
P. M. Silverberg, and M. G. Zellner, authors)

NOTICES

When Government drawings, specifications, or other data are used for any purpose other than in connection with a definitely related Government procurement operation, the United States Government thereby incurs no responsibility nor any obligation whatsoever; and the fact that the Government may have formulated, furnished, or in any way supplied the said drawings, specifications, or other data, is not to be regarded by implication or otherwise as in any manner licensing the holder or any other person or corporation, or conveying any rights or permission to manufacture, use, or sell any patented invention that may in any way be related thereto.

Qualified requesters may obtain copies of this report from the Defense Documentation Center (DDC), (formerly ASTIA), Cameron Station, Bldg. 5, 5010 Duke Street, Alexandria, Virginia, 22314.

This report has been released to the Office of Technical Services, U.S. Department of Commerce, Washington 25, D. C., for sale to the general public.

Copies of this report should not be returned to the Research and Technology Division, Wright-Patterson Air Force Base, Ohio, unless return is required by security considerations, contractual obligations, or notice on a specific document.

FOREWORD

This report summarizes all work done under contract to the Air Force for the experimental determination of vapor-liquid equilibrium in argon, oxygen, and nitrogen mixtures from July 15, 1962 to April 8, 1964.

The following persons were contributing authors on this subject:

L. Israel - literature search and many useful computer programs.

A. Jambhekar - mixture virial coefficients.

C. J. Sterner - former director of the vapor-liquid laboratory.

P. Fennema - improved chromatographic analysis.

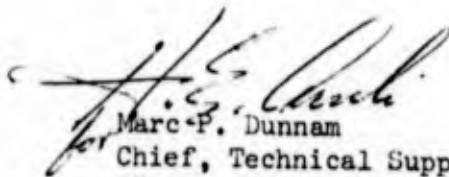
This report is dedicated to that hardy band of technicians who ran the equipment two shifts for a seemingly endless ten months. Our thanks go to E. Frederick, R. Gotthardt, J. Wallace, C. Worman, and especially to H. Donat whose perserverance, unfailing precision, and mechanical ability helped pull us over many rough spots.

ABSTRACT

This Final Technical Documentary Report presents the results from July 15, 1962 to April 15, 1964 as covered by the contract for the experimental determination of vapor-liquid equilibrium data in argon, oxygen, and nitrogen mixtures. The experimental apparatus and procedures are described. The experimental data at 26, 23, 20, 18, 16, 14, 12, 10, 8, 6, 4, 2 and 1 atmosphere levels are presented. A correlation of our experimental data is made. Plots and tables of equilibrium constants, relative volatilities and activity coefficients are presented. Experimental and calculated results are compared and a comparison of the data to the literature is made. Analytical enthalpy data is presented.

The correlation reproduces the experimental data with an error less than 2.5%; being worst at 20 atmospheres and best at 6 atmospheres.

This Technical Documentary Report has been reviewed and is approved.



Marc P. Dunnam
Chief, Technical Support Division
AF Aero-Propulsion Laboratory

TABLE OF CONTENTS

	<u>Page</u>
I. INTRODUCTION	1
II. LITERATURE SEARCH.	3
III. EXPERIMENTAL APPARATUS AND PROCEDURE	5
A. Recirculation System	5
B. Equilibrium Cell	5
C. Constant-Temperature Bath.	9
D. Operating Procedure.	9
E. Sampling Systems	11
F. Pressure Measurement	12
G. Temperature Measurement.	12
H. Time of Equilibration.	15
IV. ANALYTICAL METHODS	18
A. Analyses to Run 264.	18
B. Analyses After Run 264	18
V. EXPERIMENTAL DATA.	26
VI. CORRELATION OF EXPERIMENTAL DATA	55
A. Thermodynamic Equations.	55
B. Liquid Molar Volume.	58
C. Vapor Pressure of Pure Components.	59
D. Fugacity Coefficient	63
E. Activity Coefficient Equation.	72
VII. COMPARISON OF COPRELATION TO DATA.	77

TABLE OF CONTENTS (continued)

	<u>Page</u>
VIII. ENTHALPY CORRELATION	140
A. Heat of Mixing	140
B. Ideal Gas Heat Capacity 140-250°R.	141
C. Latent Heat.	141
D. Enthalpy of the Real Gas	142
E. Saturated Pure Component Heat Capacity	142
IX. REFERENCES	146
X. APPENDIXES	149

ILLUSTRATIONS

<u>Figure</u>	<u>Page</u>
1 Vapor-Liquid Equilibrium Apparatus	6
2 Front View of Equilibrium Apparatus	7
3 Detail of Cell and Constant-Temperature Bath.	8
4 Close-up of the Equilibrium Cell and Constant Temperature Bath.	10
5 Dead Weight Test of 500 Psi Heise Gauge	13
6 Dead Weight Test of 300 Psi Heise Gauge	13
7 Thermocouple Calibration.	14
8 Equilibration Test Run on Vapor-Liquid Apparatus.	17
9 Sample Chromatogram	20
10 Photograph of Gas Chromatograph	22
11 Close-up of Electronic Components of the Chromatograph. .	23
12 Chromatograph Calibration Curves.	24
13 Deviation of APCI Nitrogen Vapor Pressure Data from Riedel Equation	60
14. Deviation of APCI Argon Vapor Pressure Data from Riedel Equation	61
15 Deviation of Literature Oxygen Vapor Pressure Data from Riedel Equation.	62
16 Deviation of Literature Vapor Pressure from APCI Correlation for Nitrogen.	64
17 Deviation of Literature Vapor Pressure from APCI Correlation for Argon	65
18 Calculated Second and Third Virial Coefficients, B and C, for Nitrogen	68

ILLUSTRATIONS (continued)

<u>Figure</u>	<u>Page</u>
19	Calculated Second and Third Virial Coefficients, B and C, for Argon 69
20	Calculated Second and Third Virial Coefficients, B and C, for Oxygen. 70
21	Comparison of Calculated and Experimental Compressibility Data, Argon. 71
22	Comparison of Calculated and Experimental Compressibility Data, Oxygen 71
23	Comparison of Calculated and Experimental Compressibility Data, Nitrogen 73
24	Comparison of Calculated and Experimental Cross Coefficients 73
25	Comparison of Calculated and Experimental Compressibility Data, Nitrogen-Oxygen Mixtures 74
26	Comparison of Calculated and Experimental Compressibility Data, Air. 75
27	Summary of Bias of Points in Region I. 80
28	Summary of Bias of Points in Region II 81
29	Summary of Bias of Points in Region III. 82
30	Summary of Bias of Points in Region IV 83
31	Summary of Bias of Points in all Regions 84
32	Activity Coefficients in the Nitrogen-Oxygen Binary System, Calculated Vs. Experimental. 85
33	Activity Coefficients in the Nitrogen-Oxygen Binary System, Calculated Vs. Experimental. 86
34	Activity Coefficients in the Nitrogen-Oxygen Binary System, Calculated Vs. Experimental. 87
35	Activity Coefficients in the Nitrogen-Oxygen Binary System, Calculated Vs. Experimental. 88

ILLUSTRATIONS (continued)

<u>Figure</u>		<u>Page</u>
36	Activity Coefficients in the Nitrogen-Oxygen Binary System, Calculated Vs. Experimental.	89
37	Activity Coefficients in the Oxygen-Argon Binary System, Calculated Vs. Experimental.	90
38	Activity Coefficients in the Oxygen-Argon Binary System, Calculated Vs. Experimental.	91
39	Activity Coefficients in the Oxygen-Argon Binary System, Calculated Vs. Experimental.	92
40	Activity Coefficients in the Oxygen-Argon Binary System, Calculated Vs. Experimental.	93
41	Activity Coefficients in the Nitrogen-Argon Binary System, Calculated Vs. Experimental.	94
42	Activity Coefficients in the Nitrogen-Argon Binary System, Calculated Vs. Experimental.	95
43	Activity Coefficients in the Nitrogen-Argon Binary System, Calculated Vs. Experimental.	96
44	Activity Coefficients in the Nitrogen-Argon Binary System, Calculated Vs. Experimental.	97
45	Activity Coefficients in the Nitrogen-Argon Binary System, Calculated Vs. Experimental.	98
46	Comparison of Experimental Data and the Correlation, 1 Atmosphere	100
47	Comparison of Experimental Data and the Correlation, 1 Atmosphere	101
48	Comparison of Experimental Data and the Correlation, 1 Atmosphere	102
49	Comparison of Experimental Data and the Correlation, 1 Atmosphere	103
50	Comparison of Experimental Data and the Correlation, 2 Atmospheres.	104

ILLUSTRATIONS (continued)

<u>Figure</u>	<u>Page</u>
51 Comparison of Experimental Data and the Correlation, 2 Atmospheres.	105
52 Comparison of Experimental Data and the Correlation, 2 Atmospheres.	106
53 Comparison of Experimental Data and the Correlation, 2 Atmospheres.	107
54 Comparison of Experimental Data and the Correlation, 4 Atmospheres.	108
55 Comparison of Experimental Data and the Correlation, 4 Atmospheres.	109
56 Comparison of Experimental Data and the Correlation, 4 Atmospheres.	110
57 Comparison of Experimental Data and the Correlation, 6 Atmospheres.	111
58 Comparison of Experimental Data and the Correlation, 6 Atmospheres.	112
59 Comparison of Experimental Data and the Correlation, 6 Atmospheres.	113
60 Comparison of Experimental Data and the Correlation, 8 Atmospheres.	114
61 Comparison of Experimental Data and the Correlation, 8 Atmospheres.	115
62 Comparison of Experimental Data and the Correlation, 8 Atmospheres.	116
63 Comparison of Experimental Data and the Correlation, 10 Atmospheres	117
64 Comparison of Experimental Data and the Correlation, 10 Atmospheres	118
65 Comparison of Experimental Data and the Correlation, 10 Atmospheres	119

ILLUSTRATIONS (continued)

<u>Figure</u>		<u>Page</u>
66	Comparison of Experimental Data and the Correlation, 12 Atmospheres	120
67	Comparison of Experimental Data and the Correlation, 12 Atmospheres	121
68	Comparison of Experimental Data and the Correlation, 12 Atmospheres	122
69	Comparison of Experimental Data and the Correlation, 14 Atmospheres	123
70	Comparison of Experimental Data and the Correlation, 14 Atmospheres	124
71	Comparison of Experimental Data and the Correlation, 14 Atmospheres	125
72	Comparison of Experimental Data and the Correlation, 16 Atmospheres	126
73	Comparison of Experimental Data and the Correlation, 16 Atmospheres	127
74	Comparison of Experimental Data and the Correlation, 18 Atmospheres	128
75	Comparison of Experimental Data and the Correlation, 18 Atmospheres	129
76	Comparison of Experimental Data and the Correlation, 20 Atmospheres	130
77	Comparison of Experimental Data and the Correlation, 20 Atmospheres	131
78	Comparison of Experimental Data and the Correlation, 20 Atmospheres	132
79	Comparison of Experimental Data and the Correlation, 23 Atmospheres	133
80	Comparison of Experimental Data and the Correlation, 23 Atmospheres	134

ILLUSTRATIONS (continued)

<u>Figure</u>	<u>Page</u>
81 Comparison of Experimental Data and the Correlation, 26 Atmospheres	135
82 Comparison of Experimental Data and the Correlation, 26 Atmospheres	136
83 Comparison of APCI Correlation to Latimer Correlation for Nitrogen-Oxygen System	137
84 Comparison of APCI Correlation to Latimer Correlation for Argon-Nitrogen System.	138
85 Comparison of APCI Correlation to Latimer Correlation for Argon-Oxygen System.	139
86 K-Values of Nitrogen	151
87 K-Values of Nitrogen	152
88 K-Values of Nitrogen	153
89 K-Values of Nitrogen	154
90 K-Values of Nitrogen	155
91 K-Values of Nitrogen	156
92 K-Values of Nitrogen	157
93 K-Values of Nitrogen	158
94 K-Values of Argon.	159
95 K-Values of Argon.	160
96 K-Values of Argon.	161
97 K-Values of Argon.	162
98 K-Values of Argon.	163
99 K-Values of Argon.	164
100 K-Values of Argon.	165
101 K-Values of Oxygen	166
102 K-Values of Oxygen	167

ILLUSTRATIONS (continued)

<u>Figure</u>		<u>Page</u>
103	K-Values of Oxygen	168
104	K-Values of Oxygen	169
105	K-Values of Oxygen	170
106	K-Values of Oxygen	171
107	K-Values of Oxygen	172
108	K-Values of Oxygen	173
109	K-Values of Oxygen	174
110	K-Values of Oxygen	175
111	Relative Volatility of Argon to Nitrogen	177
112	Relative Volatility of Argon to Nitrogen	178
113	Relative Volatility of Argon to Nitrogen	179
114	Relative Volatility of Argon to Nitrogen	180
115	Relative Volatility of Argon to Nitrogen	181
116	Relative Volatility of Argon to Nitrogen	182
117	Relative Volatility of Argon to Nitrogen	183
118	Relative Volatility of Argon to Nitrogen	184
119	Relative Volatility of Argon to Nitrogen	185
120	Relative Volatility of Argon to Nitrogen	186
121	Relative Volatility of Argon to Nitrogen	187
122	Relative Volatility of Argon to Oxygen	189
123	Relative Volatility of Argon to Oxygen	190
124	Relative Volatility of Argon to Oxygen	191
125	Relative Volatility of Argon to Oxygen	192

ILLUSTRATIONS (continued)

<u>Figure</u>	<u>Page</u>
126	Relative Volatility of Argon to Oxygen 193
127	Relative Volatility of Argon to Oxygen 194
128	Relative Volatility of Argon to Oxygen 195
129	Relative Volatility of Argon to Oxygen 196
130	Relative Volatility of Argon to Oxygen 197
131	Relative Volatility of Argon to Oxygen 198
132	Relative Volatility of Argon to Oxygen 199
133	Relative Volatility of Argon to Nitrogen with No Oxygen Present in the System 201
134	Relative Volatility of Argon to Oxygen with No Nitrogen Present in the System 203
135	Nitrogen Pressure Activity Coefficients, 1 Atmosphere 205
136	Nitrogen Pressure Activity Coefficients, 2 Atmospheres 206
137	Nitrogen Pressure Activity Coefficients, 4 Atmospheres 207
138	Nitrogen Pressure Activity Coefficients, 6 Atmospheres 208
139	Nitrogen Pressure Activity Coefficients, 8 Atmospheres 209
140	Nitrogen Pressure Activity Coefficients, 10 Atmospheres 210
141	Nitrogen Pressure Activity Coefficients, 12 Atmospheres 211
142	Nitrogen Pressure Activity Coefficients, 14 Atmospheres 212
143	Nitrogen Pressure Activity Coefficients, 16 Atmospheres 213

ILLUSTRATIONS (continued)

<u>Figure</u>	<u>Page</u>
144 Nitrogen Pressure Activity Coefficients, 18 Atmospheres	214
145 Nitrogen Pressure Activity Coefficients, 20 Atmospheres	215
146 Nitrogen Pressure Activity Coefficients, 23 Atmospheres	216
147 Nitrogen Pressure Activity Coefficients, 26 Atmospheres	217
148 Argon Pressure Activity Coefficients, 1 Atmosphere	218
149 Argon Pressure Activity Coefficients, 2 Atmospheres	219
150 Argon Pressure Activity Coefficients, 4 Atmospheres	220
151 Argon Pressure Activity Coefficients, 6 Atmospheres	221
152 Argon Pressure Activity Coefficients, 8 Atmospheres	222
153 Argon Pressure Activity Coefficients, 10 Atmospheres	223
154 Argon Pressure Activity Coefficients, 12 Atmospheres	224
155 Argon Pressure Activity Coefficients, 14 Atmospheres	225
156 Argon Pressure Activity Coefficients, 16 Atmospheres	226
157 Argon Pressure Activity Coefficients, 18 Atmospheres	227
158 Argon Pressure Activity Coefficients, 20 Atmospheres	228
159 Argon Pressure Activity Coefficients, 23 Atmospheres	229
160 Argon Pressure Activity Coefficients, 26 Atmospheres	230
161 Oxygen Pressure Activity Coefficients, 1 Atmosphere	231
162 Oxygen Pressure Activity Coefficients, 2 Atmospheres	232
163 Oxygen Pressure Activity Coefficients, 4 Atmospheres	233
164 Oxygen Pressure Activity Coefficients, 6 Atmospheres	234
165 Oxygen Pressure Activity Coefficients, 8 Atmospheres	235

ILLUSTRATIONS (continued)

<u>Figure</u>		<u>Page</u>
166	Oxygen Pressure Activity Coefficient, 10 Atmospheres. . .	236
167	Oxygen Pressure Activity Coefficient, 12 Atmospheres. . .	237
168	Oxygen Pressure Activity Coefficient, 14 Atmospheres. . .	238
169	Oxygen Pressure Activity Coefficient, 16 Atmospheres. . .	239
170	Oxygen Pressure Activity Coefficient, 18 Atmospheres. . .	240
171	Oxygen Pressure Activity Coefficient, 20 Atmospheres. . .	241
172	Oxygen Pressure Activity Coefficient, 23 Atmospheres. . .	242
173	Oxygen Pressure Activity Coefficient, 26 Atmospheres. . .	243
174	Vapor Pressure of Specific Mixtures of N_2 -Ar- O_2	245
175	Vapor Pressure of Specific Mixtures of N_2 -Ar- O_2	246
176	Vapor Pressure of Specific Mixtures of N_2 -Ar- O_2	247
177	Vapor Pressure of Specific Mixtures of N_2 -Ar- O_2	248
178	Vapor Pressure of Specific Mixtures of N_2 -Ar- O_2	249
179	Vapor Pressure of Specific Mixtures of N_2 -Ar- O_2	250
180	Vapor Pressure of Specific Mixtures of N_2 -Ar- O_2	251
181	Vapor Pressure of Specific Mixtures of N_2 -Ar- O_2	252
182	Vapor Pressure of Specific Mixtures of N_2 -Ar- O_2	253
183	Vapor Pressure of Specific Mixtures of N_2 -Ar- O_2	254
184	Vapor Pressure of Specific Mixtures of N_2 -Ar- O_2	255
185	Vapor Pressure of Specific Mixtures of N_2 -Ar- O_2	256
186	Vapor Pressure of Specific Mixtures of N_2 -Ar- O_2	257
187	Vapor Pressure of Specific Mixtures of N_2 -Ar- O_2	258
188	Vapor Pressure of Specific Mixtures of N_2 -Ar- O_2	259

TABLES

<u>Table</u>	<u>Page</u>
1 Equilibration Test Results	16
2 Sample Long-Term Analyses.	25
3 Experimental Data at 1 Atm	28
4 Experimental Data at 2 Atm	30
5 Experimental Data at 4 Atm	32
6 Experimental Data at 6 Atm	34
7 Experimental Data at 8 Atm	36
8 Experimental Data at 10 Atm.	38
9 Experimental Data at 12 Atm.	40
10 Experimental Data at 14 Atm.	42
11 Experimental Data at 16 Atm.	44
12 Experimental Data at 18 Atm.	46
13 Experimental Data at 20 Atm.	48
14 Experimental Data at 23 Atm.	50
15 Experimental Data at 26 Atm.	52
16 Experimental Data at Mixed Pressure Levels	54
17 Liquid Molar Volume Correlation Constants.	58
18 Constants for Pure Component Vapor Pressures	59
19 Second Virial Coefficients Used in Calculations.	66
20 Third Virial Coefficients Used in Calculations	67
21 Van Laar Constants for Nitrogen-Argon-Oxygen Activity Coefficients in the Liquid Phase.	76

TABLES (continued)

<u>Table</u>		<u>Page</u>
22	Constants and Root Mean Square Error of Various Curve Fits	78
23	Summary of Positive and Negative Deviations of Experimental Points from Correlation	79
24	Comparison of Calculated and Experimental Saturated Liquid Heat Capacities, BTU/lb-Mole °R	145
25	Isobaric Calculated Values	261
26	Isothermal Calculated Values	275

I. INTRODUCTION

This project, under contract with the U. S. Air Force, was undertaken to measure and correlate vapor-liquid equilibrium data in binary and ternary mixtures of oxygen, nitrogen, and argon. This project was undertaken because much of the existing data are reported only for low pressures and few data have been obtained in the ternary system. The measurements of this project establish the vapor-liquid equilibrium properties of the oxygen-nitrogen-argon system over a wide range of pressures and over the entire range of binary and ternary compositions. One thousand nine hundred and sixty two data points were measured and this system may well be one of the most thoroughly studied ternary systems to date.

The project effort was divided into three parts as follows:

1. A literature search for existing data.
2. The measurement of vapor-liquid equilibrium data at the following combinations of pressures and compositions. The actual compositions measured are in only approximate agreement with the listed compositions and, therefore, more than one run was sometimes made in a given concentration region.

<u>Pressure, Atm</u>	<u>Mole Ratio</u>	
	$\frac{N_2}{(N_2+O_2)}$	<u>Mole Fraction Argon</u>
1	0	0
2	0.10	0.01
4	0.20	0.02
6	0.40	0.03
8	0.60	0.04
10	0.80	0.05
12	0.90	0.07
14	0.97	0.10
16	1.00	0.20
18	----	0.40
20	----	0.60
23	----	0.80
26	-----	0.90

3. The thermodynamic correlation of the equilibrium data and the analytical determination of enthalpy data.

Manuscript released by authors April 1964 for publication as an RTD Technical Documentary Report.

This report summarizes:

1. The results of the literature search.
2. A bibliography of existing vapor-liquid equilibrium, enthalpy, and related data of the oxygen-nitrogen-argon system.
3. A description of the experimental apparatus.
4. Tables of the experimental data.
5. A thermodynamic correlation of the data.
6. Tables and figures of derived vapor-liquid equilibrium and enthalpy data.

The experimental data are accurate to within + 0.5% in the pressure and + 1% in the relative volatility. By smoothing the data it is possible to obtain equilibria accurate to + 0.5% in the relative volatility. The thermodynamic correlation of the data is not quite as accurate as the experimental data due to a weakness in the correlation method at temperatures above the critical temperature of nitrogen and at pressures near the critical point of a mixture. The largest difference between the correlation and the experimental data appears to be at 20 atmospheres where the calculated pressure and relative volatilities deviate 2.5% from the experimental data. This accuracy is satisfactory for most process design calculations, but it may be desirable on occasion to interpolate directly from the experimental data.

II. LITERATURE SEARCH

A literature search was made to obtain all existing data relating to vapor-liquid equilibrium and enthalpy of the oxygen-nitrogen-argon system. The search included the following sources of information.

1. Chemical Abstracts (January 1957 - December 1962).
2. Chemical Titles (January 1961 - May 1963).
3. Armed Services Technical Information Agency (ASTIA) - A complete search of the ASTIA collection was obtained (to September 1963).
4. Cryogenic Data Center - NBS Cryogenic Engineering Laboratory, Boulder, Colorado - Two searches to January 1963 and to October 1963.
5. Existing bibliographies on the subject:
 - a. "The Compendium", Johnson, V. J. (ed.), WADD Tech. Rept. 60-56, (1961).
 - b. E. F. Yendall and Olzewski, W. J., "Saturation Properties of Oxygen-Nitrogen Mixtures", ASD Technical Rept. 61-536, Sept. 1961.
 - c. Ju Chin Chu, et al, Vapor Liquid Equilibrium Data, J. W. Edwards Co., Ann Arbor, Michigan, 1956.
 - d. E. Hala, et al, Vapor-Liquid Equilibrium, Pergamon, New York, 1958.
 - e. G. A. Cook, ed., Argon, Helium, and the Rare Gases, Vol. II, Interscience, New York, 1961.
 - f. J. Timmermans, Physico-Chemical Constants of Binary Systems, Interscience, New York, 1960.

A bibliography of the data is given in the Appendix according to the following categories:

- A. Vapor-Liquid Equilibrium Data Nitrogen-Oxygen System
- B. Vapor-Liquid Equilibrium Data Nitrogen-Argon System
- C. Vapor-Liquid Equilibrium Data Argon-Oxygen System

- D. Vapor-Liquid Equilibrium Data Nitrogen-Oxygen-Argon Ternary System
- E. Enthalpy Data
- F. Pressure-Volume-Temperature Data for Gaseous Mixtures of N_2 - O_2 -Ar (including air) used in checking the virial coefficients
- G. Vapor Pressure Data
- H. Miscellaneous References

From this search it is concluded that few vapor-liquid equilibrium data exist in three principal areas, namely:

1. Few data exist for the nitrogen-argon binary system.
2. Few data exist above pressures of 5 to 10 atmospheres.
3. Few data exist for the argon-oxygen-nitrogen ternary system.

From the search for enthalpy data it is concluded that:

1. Heat of mixing data for the binaries of the oxygen-nitrogen-argon system are reported only at low temperatures.
2. Latent heat data are reported in terms of correlations based principally on vapor pressure data. Except for argon the data appear to be satisfactory, but in the case of argon there appears to be little experimental data to back up the correlated data.

III. EXPERIMENTAL APPARATUS AND PROCEDURE

A. Recirculation System

A schematic flow diagram of the equilibrium apparatus⁽¹⁾ is presented in Figure 1. The elements which make up the complete apparatus consist of: equilibrium cell, recirculation pump, closed recirculation loop, constant-temperature bath, system pressure gauge, cell thermocouple, liquid sampling line, gas sampling coil, system volume regulator, charging manifold, vacuum pump and numerous subsidiary equipment such as valves, gauges, etc. A photograph of the apparatus is presented in Figure 2 showing the cell barricade, pressure gauges, volume regulator and temperature controller.

The recirculation method is one of the standard laboratory techniques for obtaining accurate vapor-liquid equilibrium data at temperatures below ambient. With this method, a cell partly full of liquid and of appreciable volume is maintained at a constant operating temperature. The vapor inside the cell is drawn out of the top of the cell, warmed to ambient temperature, passed through a pump which increases the pressure of the vapor slightly, cooled back to the cell temperature and introduced to the bottom of the cell. The recirculated vapor bubbles through the liquid to the vapor space and continues the cycle through the system. As the vapor bubbles through the liquid, the liquid is agitated and the liquid and vapor approach equilibrium. When equilibrium is achieved, portions of the vapor and of the liquid are withdrawn from the system and analyzed for chemical compositions.

In this apparatus, the vapors warm to ambient temperature in exposed tubing, recirculate by use of an electromagnetic pump⁽²⁾ and cool to cell temperature in a coil of tubing which is immersed in the constant-temperature bath.

B. Equilibrium Cell

A schematic diagram of the equilibrium cell is shown on Figure 3. The equilibrium cell is a vertical cylindrical tube made of laminated glass which is sealed at both ends by Teflon gaskets supported by end flanges. The end flanges are connected to each other by tie-rods outside of the cell. The glass tube, which is usable at pressures up to 800 psia and temperatures to -340°F , is $3/8$ in. ID, $11/16$ in. OD and $3-1/2$ in. long with squared-off ends ground flat and fire-polished. The liquid sampling line and the three-element thermocouple both enter the equilibrium cell at the top through the $1/4$ in. OD vapor outlet line. The recirculated vapor enters the cell through small holes in a distributor plate which caps the inlet line. Inside the cell the flow of bubbles from the vapor inlet is broken up by a series of horizontal screens. Near the top of the cell, a plug of fiberglass prevents carryover of entrained liquid.

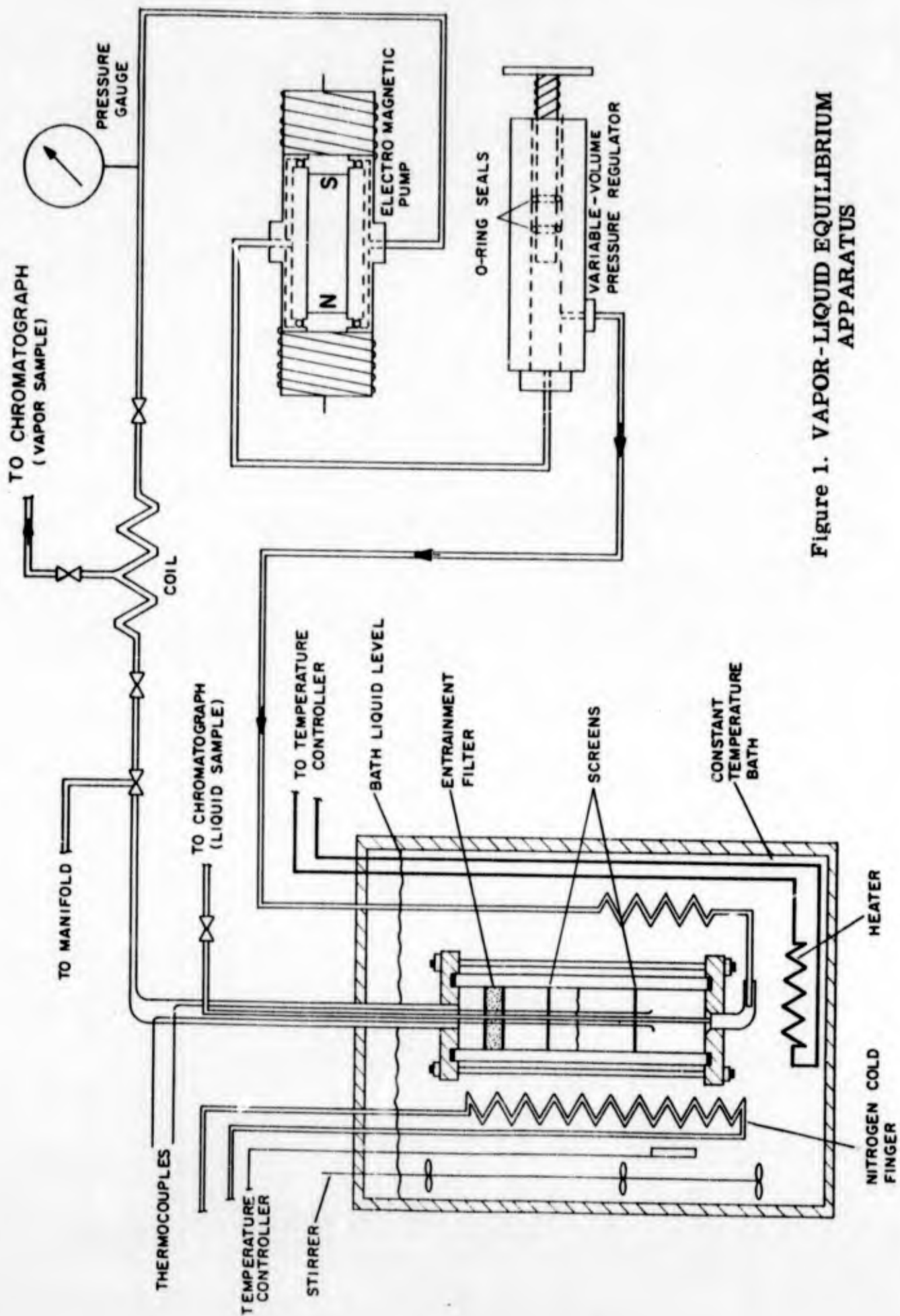


Figure 1. VAPOR-LIQUID EQUILIBRIUM APPARATUS

NOT REPRODUCIBLE

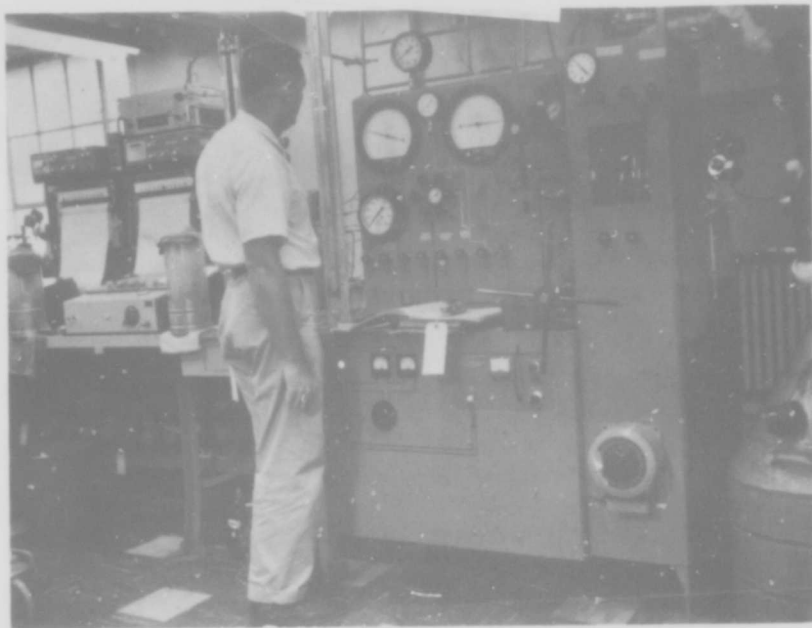


FIGURE 2. FRONT VIEW OF EQUILIBRIUM APPARATUS

7

603151

R-1556

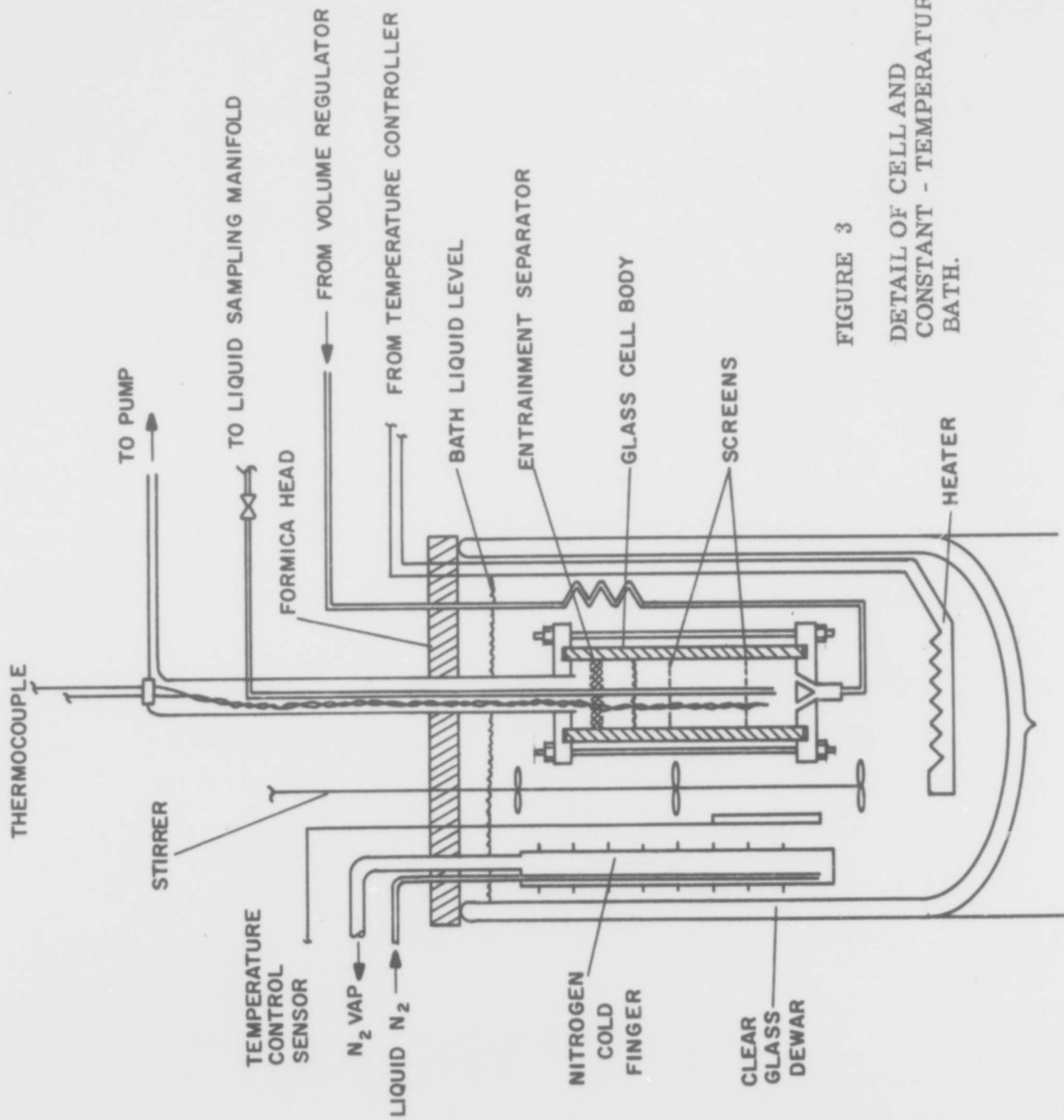


FIGURE 3

DETAIL OF CELL AND CONSTANT - TEMPERATURE BATH.

The equilibrium cell is immersed in a constant-temperature liquid bath which is contained in a clear glass dewar vessel. The dewar is supported on a pedestal within a steel barricade which is open top and bottom. The equilibrium cell is illuminated and may be viewed while operating through the clear dewar and a safety glass window in the barricade. A photograph of the cell and bath are shown in Figure 4.

C. Constant-Temperature Bath

The constant-temperature bath in which the equilibrium cell is immersed may be any of one of several fluids, depending on the operating temperature. From the highest temperature covered down to -301°F , Freon-13* was used. Liquid argon was used down to -308°F . Liquid nitrogen was used down to -320°F .

The temperature of the bath liquid is controlled to within $+ 0.01^{\circ}\text{F}$ by use of a proportional electronic controller. The bath is cooled by liquid nitrogen which flows into a "cold finger" at a constant rate and evaporates. The temperature of the bath is adjusted to operating conditions by passing an electrical current through a resistance heating element immersed in the bath. The heating current is regulated by the controller which receives temperature information from a platinum resistance thermometer which is immersed in the bath. The bath liquid is kept agitated by a motor-driven stirrer. Two additional thermocouples in the bath are used to determine the bath temperature and to check on the controller action.

D. Operating Procedure

Routine operation of the equilibrium apparatus begins with the cell at room temperature and the entire system under vacuum. Precooled bath liquid is added to the dewar vessel and the cell is cooled down to the operating temperature. Measured quantities of the component gases are introduced to the system, one component at a time, generally starting with nitrogen. The quantities of gas added are calculated beforehand and measured by pressure changes in a volume-calibrated manifold. Before any component is allowed to enter the manifold, the manifold is evacuated and purged with the appropriate gas. The recirculation pump is turned on while the components are being introduced and continues to operate until it is time to sample. When all components have been added to the system, slight adjustments of the pressure and liquid volume are made by adding small additional quantities of the appropriate component. After the desired liquid volume has formed and the pressure is established at the proper level, the apparatus is permitted to operate at constant temperature and pressure for approximately one half hour before taking samples. The sampling procedures are described under "E. Sampling Systems".

*E.I. Dupont de Nemours Inc. registered trademark.

NOT REPRODUCIBLE

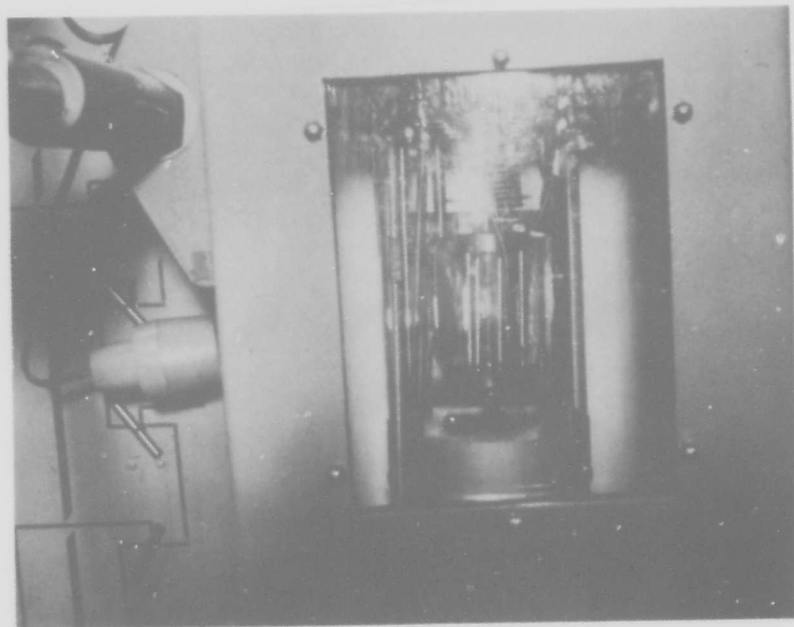


FIGURE 4. CLOSE-UP OF THE EQUILIBRIUM CELL AND
CONSTANT TEMPERATURE BATH.

The cell is the long cylinder upright in the center of the dewar.

Normally, after the samples have been taken, the pressure is released from the system, the bath liquid is recovered from dewar and the cell is allowed to warm to room temperature. The system is then evacuated and allowed to remain under vacuum overnight to be ready for operation the next day. Since more than one run is made per day, it was not necessary to allow the cell to warm up between runs on a particular day, but only at the last run.

E. Sampling Systems

After one-half hour of operation, the recirculating pump is stopped and the system pressure is recorded. At this time, a large proportion of the vapor in the system remains in the vapor sampling coil which is part of the recirculation loop. Valves at the end of this sampling coil are closed to isolate the coil from the rest of the system. When these valves are closed, gas samples can be removed at anytime from the coil through the gas sampling valve without being affected by the liquid sampling procedure.

After the vapor sample has been trapped in the vapor coil, the liquid in the cell is sampled by withdrawing a portion of it through the liquid sampling line. The liquid sampling line extends into the equilibrium cell through the vapor outlet to a point just above the vapor distributor plate. The holes in the distributor plate are so arranged that the bubbles of vapor rise clear of the end of the sampling line as they pass up through the liquid. The liquid sampling line, which is a 1/16 in. OD tube with the dead volume reduced to capillary dimensions by insertion of a 20 ga. wire, leads to the liquid sampling valve, which in turn leads to the liquid sampling manifold.

The procedure for taking liquid samples is quite critical and has a considerable effect on the accuracy of the final data. As the liquid sample passes up through the sampling line to the sampling valve, it is warmed from its saturation temperature to a temperature well in the superheat region. The liquid totally vaporizes in a short section of the sampling line, resulting in a fractionation effect in that section of the line. As liquid continues to flow, the fractionation region of the sampling line tends to accumulate the less volatile components, finally reaching approximate equilibrium with the flowing sample stream. It is necessary to throw away the first portion of sample which passes through the sampling valve and to make sure that the flow rate of sample is maintained constant during the sample period. The flow rate is maintained constant by making only one setting of the sampling valve and allowing the vapor to expand through the valve to a pressure which is less than half of the system pressure. Also, while the liquid sample is being withdrawn from the cell, the pressure in the system is maintained by screwing in on the system volume regulator.

Both liquid and vapor samples are finally collected in 75 cc. sample cylinders which are equipped with a pressure gauge at one end and a shut-off valve at the other end. Sample cylinders and manifold are normally purged with sample gas and then evacuated before being filled with the sample.

F. Pressure Measurement

The pressure in the equilibrium system is measured by a temperature-compensated Bourdon-tube gauge which has been calibrated by the manufacturer (Heise) and checked with a dead-weight gauge. The low-pressure gauge which was used for measuring pressures at 20 atmospheres and below can be read directly to the nearest 0.1 psi with a hysteresis error of + 0.005 psi. The high-pressure gauge which was used for pressures above 20 atmospheres can be read directly to the nearest 0.3 psi with a hysteresis error of + 0.1 psi.

The pressure gauges used in this experimental program have been tested with an Ashcroft Portable Dead-Weight Tester. The results of this calibration are shown in Figures 5 and 6. As can be seen on the graphs, the 500 psia gauge, Heise H16100, shows no deviation up to 220 psia and deviates only 0.1 psi above 220 psia. The 300 psia gauge, Heise H31596, shows a slight drift with increasing pressure, but the error is never larger than 0.1%. This gauge is considered satisfactory without a correction to the readings.

G. Temperature Measurement

The temperature of the equilibrium liquid is measured by a three-element copper-constantan thermocouple which is immersed in the liquid inside the cell. Melting ice is used as the warm end reference junction. Seven separate calibrations have been made of the thermocouple by measurement of the vapor pressure of oxygen. We initially calibrated against the vapor pressures of argon, oxygen and nitrogen but systematic deviations became evident. Oxygen was used as the standard because its normal boiling point is an International Standard Temperature and in this way our calibration was guaranteed to pass through this point.

All seven calibrations covered the temperature range -220°F to -300°F . One calibration extended warmer and one calibration extended colder. The data for all seven calibrations was fitted by least squares to a polynomial of millivolts vs. temperature. Figure 7 shows the deviation of the measured versus calculated millivolts with a dashed line drawn to indicate the millivolt deviation equivalent to 0.1°F . As can be seen, almost all points are within 0.1°F of the calibration equation.

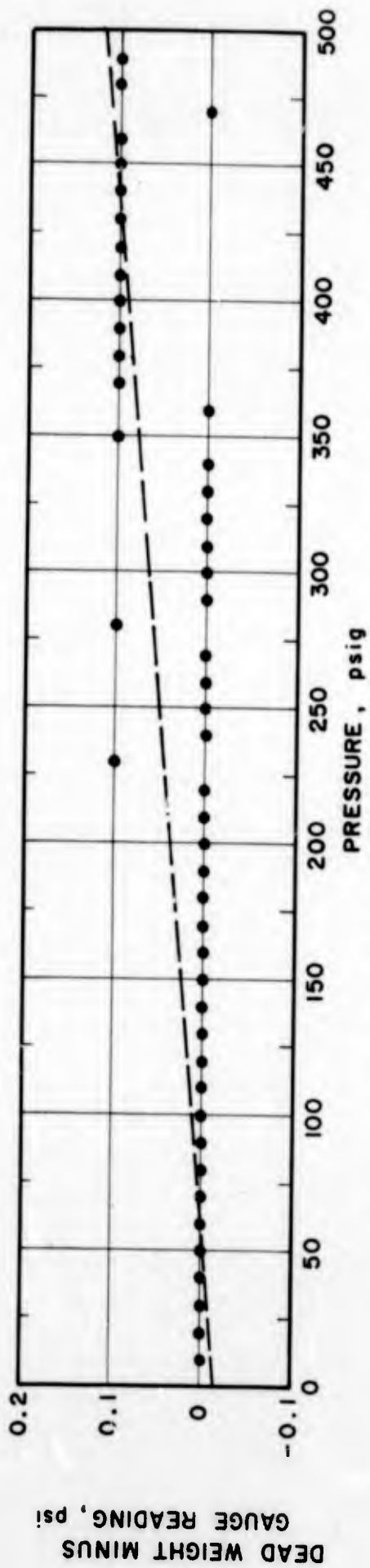


Figure 5. Dead Weight Test of 500 psi Heise Gauge.

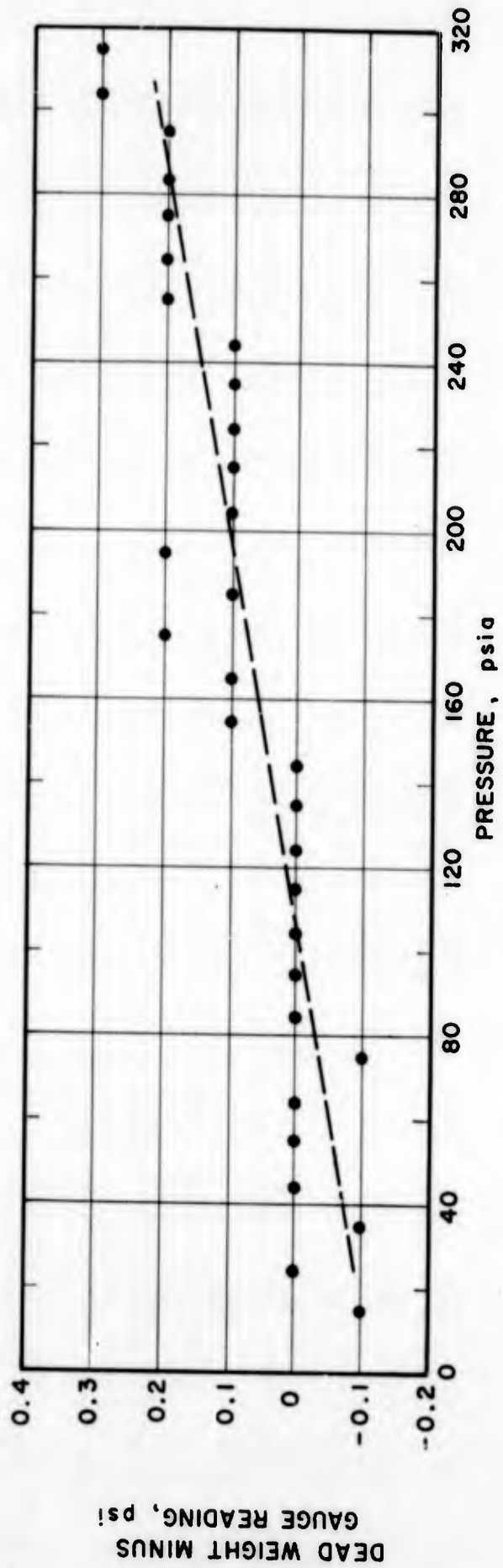


Figure 6. Dead Weight Test of 300 psi Heise Gauge.

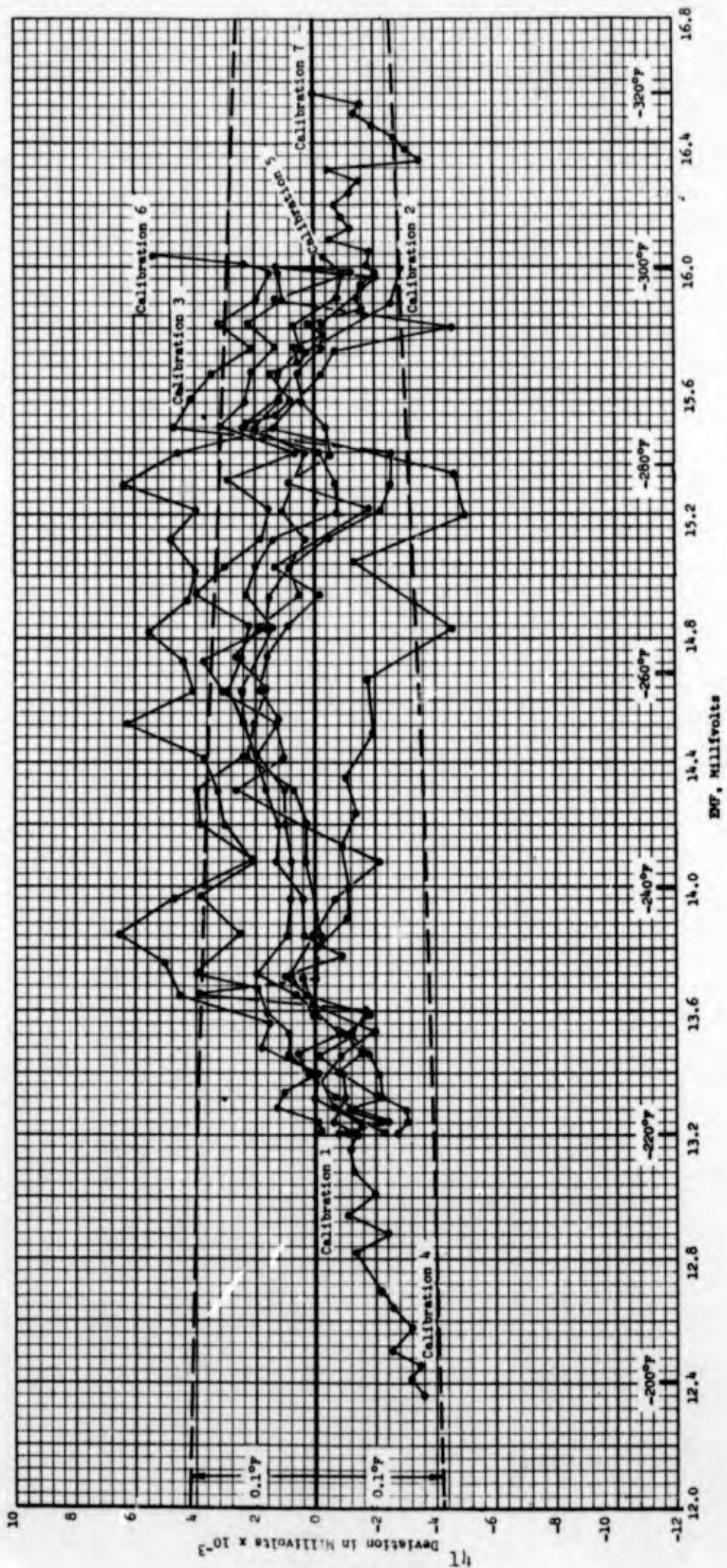


Figure 7. Thermocouple Calibration.

H. Time of Equilibration

Five runs were made to determine equilibration time of the experimental apparatus with mixtures of nitrogen and argon in the cell. Measurements were made of the following variables after adding an incremental sample of either argon or nitrogen:

1. Temperature - every five seconds
2. Pressure - every five seconds
3. Liquid level - every second on movie film
4. Composition - continuously by means of a Gow-Mac Thermal Conductivity Cell installed in parallel to the vapor recirculation line.

The conditions of the runs are given in Table 1 and the results of Run A, which can be considered typical, are shown in Figure 8. This figure indicates that all the properties change at the same time and the same way. In this case, there was a sharp rise right after the argon was added, a rapid fall-off, a slow recovery with overshoot and a settling to steady-state values. By the time six minutes had elapsed, the transient had settled out. In the measurement of vapor-liquid equilibria, thirty minutes were allowed for equilibration, so equilibrium errors are negligible and contribute a smaller error than reading the pressure and temperature.

TABLE 1
EQUILIBRATION TEST RESULTS

<u>Run</u>	<u>Temperature of</u>	<u>Initial Pressure Psia</u>	<u>Final Pressure Psia</u>	<u>Time to Equilibrate</u>	<u>% N₂ in Vapor</u>	<u>% Ar in Vapor</u>	<u>Material Added</u>
A	-255	175.6	174.0	4-1/2 min.	51.04	48.96	Argon
B	-247	293.8	290.3	4-1/2 min.	83.73	16.27	Argon
C	-228	294.1	293.7	4-1/2 min.	10.40	89.60	Argon
D	-279	58.8	60.8	5 min.	34.02	65.98	Nitrogen
E	-294	58.8	57.5	4 min.	94.21	5.79	Argon

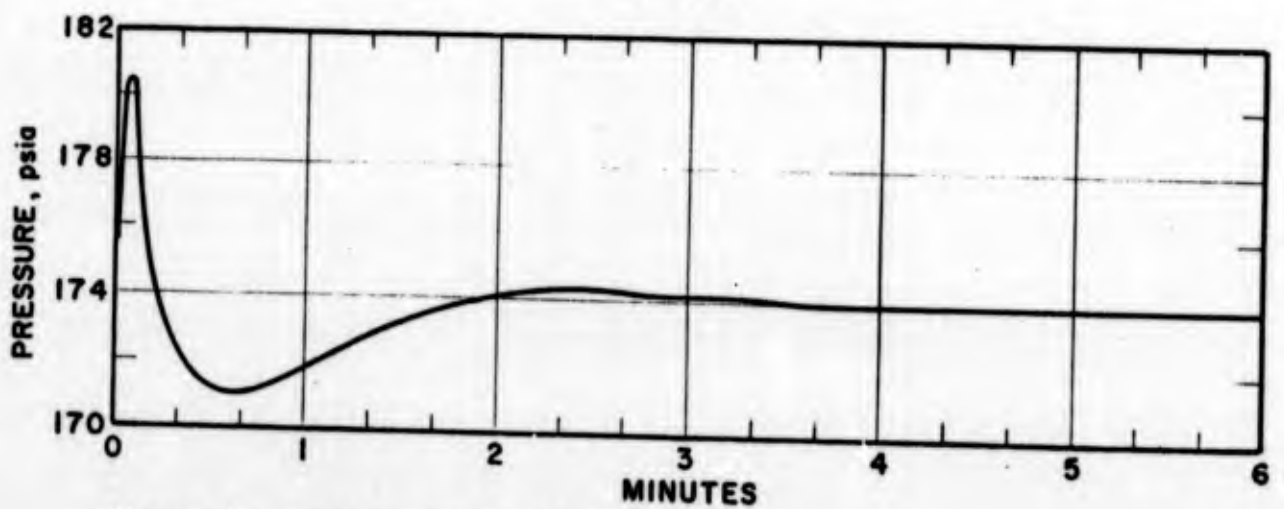
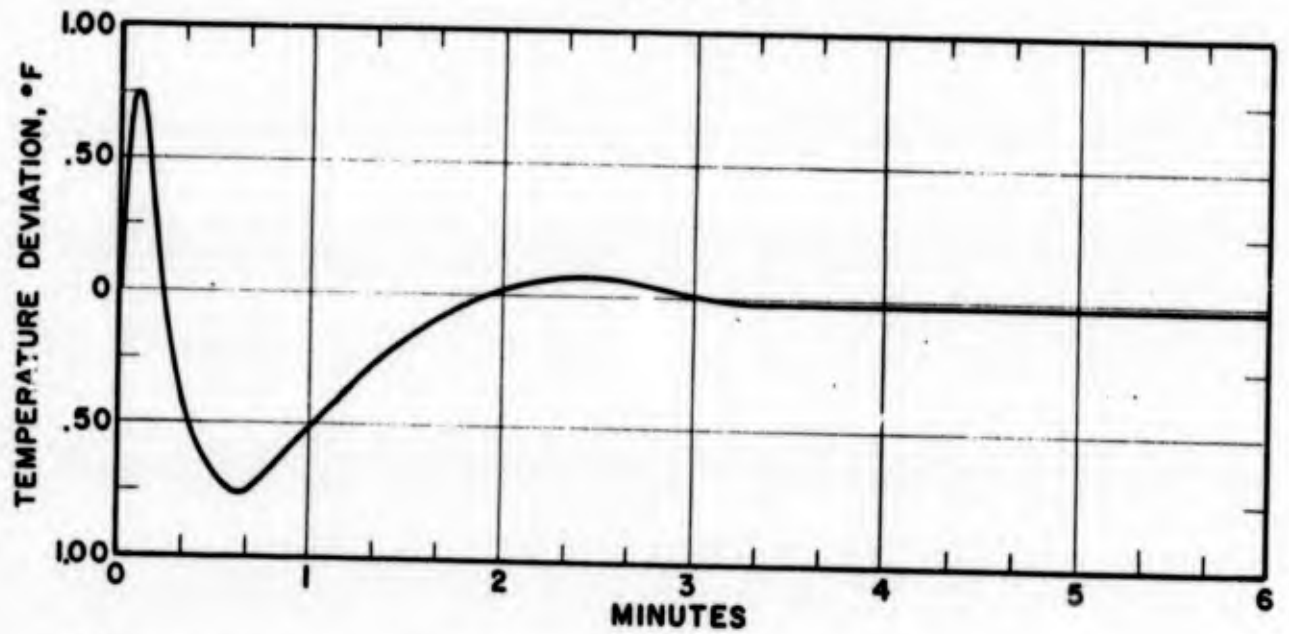
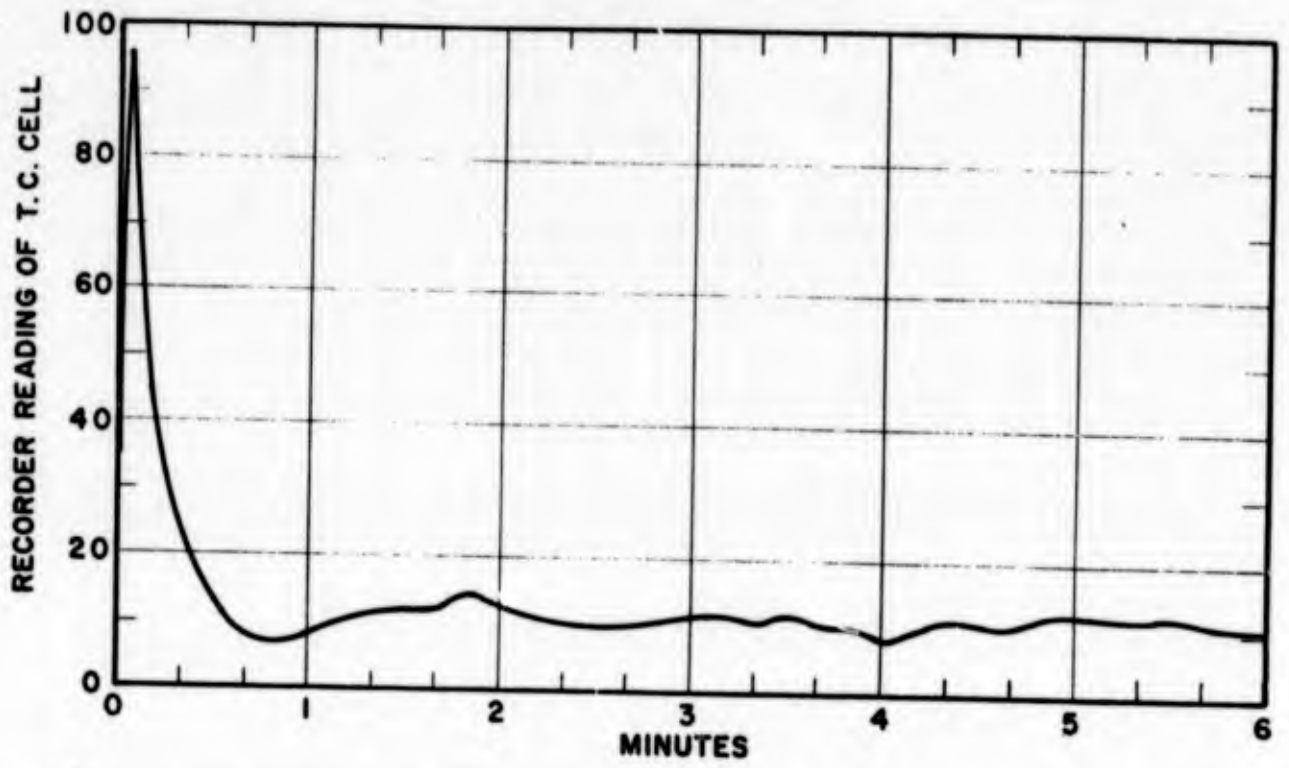


Figure 8. Equilibration Test Run on Vapor-Liquid Apparatus.

IV. ANALYTICAL METHODS

The best analytical method for analyzing the argon-oxygen-nitrogen mixtures was judged to be gas chromatography. Other techniques which were considered included: paramagnetic and electrolytic methods for oxygen, titanium sponge technique for argon, and mass spectrometry for argon, oxygen and nitrogen. These techniques were found to have limitations of accuracy and speed which make them inferior to gas chromatography.

A. Analyses to Run 264

For the first 150 experimental points a technique was used described in the first quarterly report (3). With this technique, the flow of carrier gas and sample was split, passed through two separate columns and recombined to pass through the same detector. One column was a five-foot length of 28-32 mesh molecular sieve 5A at 105°F and the other column was a six-foot length of 30-70 mesh molecular sieve 5A at -110°F. The first column was used to separate the nitrogen from the argon plus oxygen and the second column was used to separate the oxygen from the argon. In order to get proper separation of the argon it was necessary to provide a retention time of about 12.5 minutes for the oxygen. The maximum deviation with any particular sample was about 1.5% of the resulting analysis.

Between runs 150 and 264 a dual-chromatograph system was used for analysis. One chromatograph determined oxygen and nitrogen and the other chromatograph determined argon. The columns in each chromatograph were identical (6 ft 5A molecular sieves at 30°C), but one chromatograph used argon as the carrier gas and the other used oxygen as the carrier. In this way, the only separation required in either column was between the nitrogen and the other two gases. The chromatograph using argon carrier gas would only register the oxygen part of the argon + oxygen peak and in the chromatograph using oxygen carrier gas, only the argon part of the argon + oxygen peak would register. Frequent calibration standards were required to assure internal consistency of the data. There was an improvement in accuracy over the preceding method.

B. Analyses After Run 264

Beginning with run 264 a new method was adopted whereby all three components of an oxygen-nitrogen-argon mixture can be separated on a single chromatographic column. By this method it is possible to calculate the relative proportions of each component from the relative peak size. This has several advantages over the previous methods where a knowledge of the absolute peak size was required. This new method is less sensitive to drift in operating detector current and column

variations since it is only the variation during the period of elution of the peaks which affect the analysis. With the absolute method, any variation in current or column conditions from the time a standard calibration is run until the unknown sample is run will affect the analysis.

By this new method, the components are separated at liquid oxygen temperature on a chromatographic column containing tetrafluoromethane (Freon 14)*as a solvent on firebrick. The separation is made in the order of the boiling points of the gases with nitrogen emerging first from the column. A sample chromatogram of a mixture containing 77.40% nitrogen, 10.13% argon and 12.47% oxygen is shown in Figure 9 . Each of the component peaks is clearly separated from the other peaks. It is possible to obtain duplicate analyses of a mixture which agree within 0.3%. Tests with a standard blend, however, show variations of as much as 1% between analyses on separate days. This presumably is due to some interference between the peaks.

The separation is performed on a 15' x 1/4" column with a flow rate of approximately 230 cc/minute of helium. The ratio of Freon 14 to firebrick is about 1 to 3 by weight. The column is made up by first packing the column with the firebrick, then charging the column with a mixture of Freon 14 and helium at room temperature to a pressure high enough to put the required amount of Freon 14 in the column. This usually requires charging to a pressure between 900 and 1100 psig. Subsequent to pressurization with the Freon 14-helium mixture the column is submerged in boiling liquid oxygen whereupon the Freon 14 condenses as the immobile chromatographic solvent on the firebrick. This column is then used in the conventional manner to separate the components of the oxygen-nitrogen-argon mixtures. The sample size is 5 cc fed in at either 760 or 900 mm Hg (10 cc flooded the column). A sample normally fully separates in fourteen minutes.

Starting with run 1530, the method was modified. It was discovered that a mixture of 30% ethane, 60% tetrafluoromethane, and 10% helium solved the problem of the tailing of nitrogen into the argon peak. The argon retention time increased slightly bringing it closer to the oxygen peak. The charging pressure of the column was reduced to between 500 and 700 psig and the flow rate increased to 300 cc/minute. Analysis time was reduced by this improvement to nine minutes.

A specially built electronic integrator records the response of the thermal conductivity cell. The basic chromatograph is a Beckman GC-2 with two 5 cc sample loops. The column described above is external to the chromatograph box in a dewar of liquid oxygen. The integrator has

*E. I. Dupont de Nemours Inc. registered trademark.

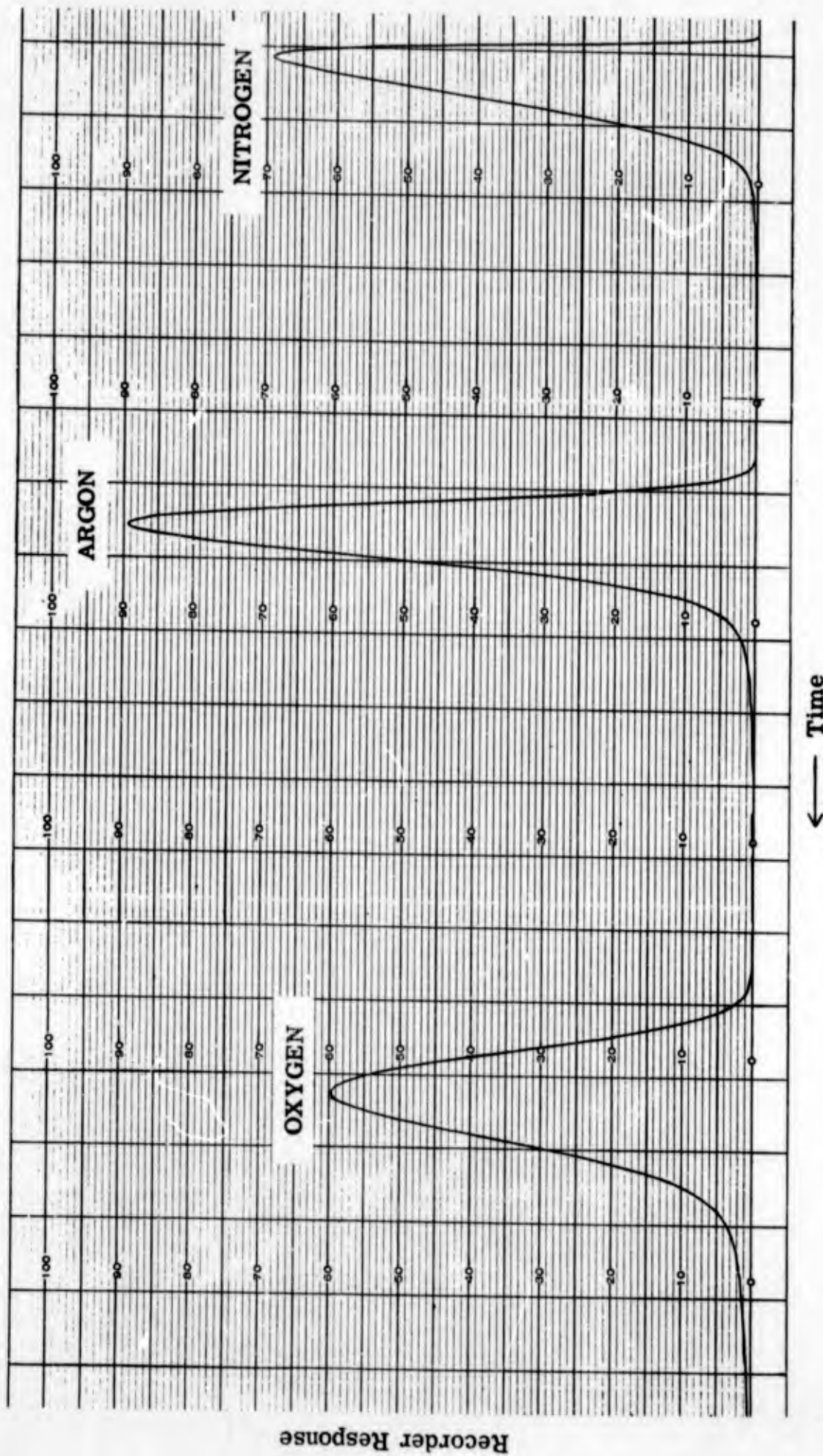


Figure 9. Sample Chromatogram.

four components:

- (1) Hewlett-Packard 5532A Electronic Counter for display
- (2) Dymec Model 2210 Voltage to Frequency Converter
- (3) Sola Type CVH-1 Harmonic-Neutralized Constant Voltage Transformer
- (4) Sanborn 860-1500-PA Amplifier

Also the output of the thermal conductivity cell is recorded as peaks by a Brown Elektronik Recorder with variable sensitivity and span. This recorder is electrically isolated from the integrator. Photographs of the chromatograph are shown in Figures 10 and 11.

The thermal conductivity detector was calibrated in December 1962 and November 1963 over a wide range of sample size and operating conditions to insure accurate analysis of the mixtures. It was found that a two-fold variation in flow rate affects the analysis only 0.3%. A change in the filament current to 2/3 the operating value only affected the analysis by 1%. During actual operation these variables would be expected to vary over only a fraction of these changes. In order to determine the effect of sample size, standard blends of oxygen, nitrogen, and argon were used to determine the response of the detector relative to a 2 cc sample of oxygen. The results of this calibration are shown in Figure 12, in which the relative response, q , is the inverse of the thermal conductivity cell response. The triangles represent points taken in 1963 and the circles represent the points taken in 1962. The lines drawn on the graph are the calibrations used in all calculations. It can be seen that for the two calibrations the response of oxygen and the response of nitrogen agree. The response of argon differs by 2% for small samples. This difference in the case of argon probably represents a variation in the standards rather than a variation in the cell response. This is indicated by the results in Table 2 which lists analyses of two mixtures which were routinely analyzed daily to determine whether the column was good or needed rebuilding. The special mix ran out at the end of August and synthetic air was first used on April 18, 1963. It is evident from examination of Table 2 that while there was scatter in the daily analyses, there was no systematic trend in the analyses with time.

Compositions were calculated using the relative responses lines shown in Figure 12. The mole fraction of a component is given in terms of peak area and relative response as

$$x_i = \frac{A_i q_i}{A_1 q_1 + A_2 q_2 + A_3 q_3} \quad (1)$$

NOT REPRODUCIBLE



Figure 10. Photograph of Gas Chromatograph.

The column is submerged in the steel dewar in the background. The Beckman GC2-A is shown in the near background. The sample bomb and sample feed system are above the operator's hand. The manometer is behind the recorder. On top of the recorder are the Electronic Counter and the Voltage to Frequency Converter. Not shown are the transformer and amplifier.

NOT REPRODUCIBLE

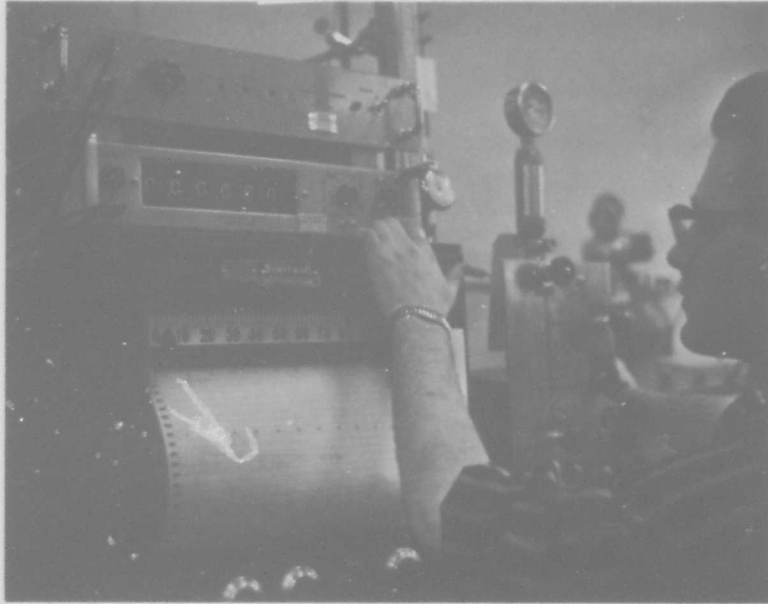


Figure 11. Close-up of Electronic Components of the Chromatograph.

60315-1

○ DEC., 1962

△ NOV., 1963

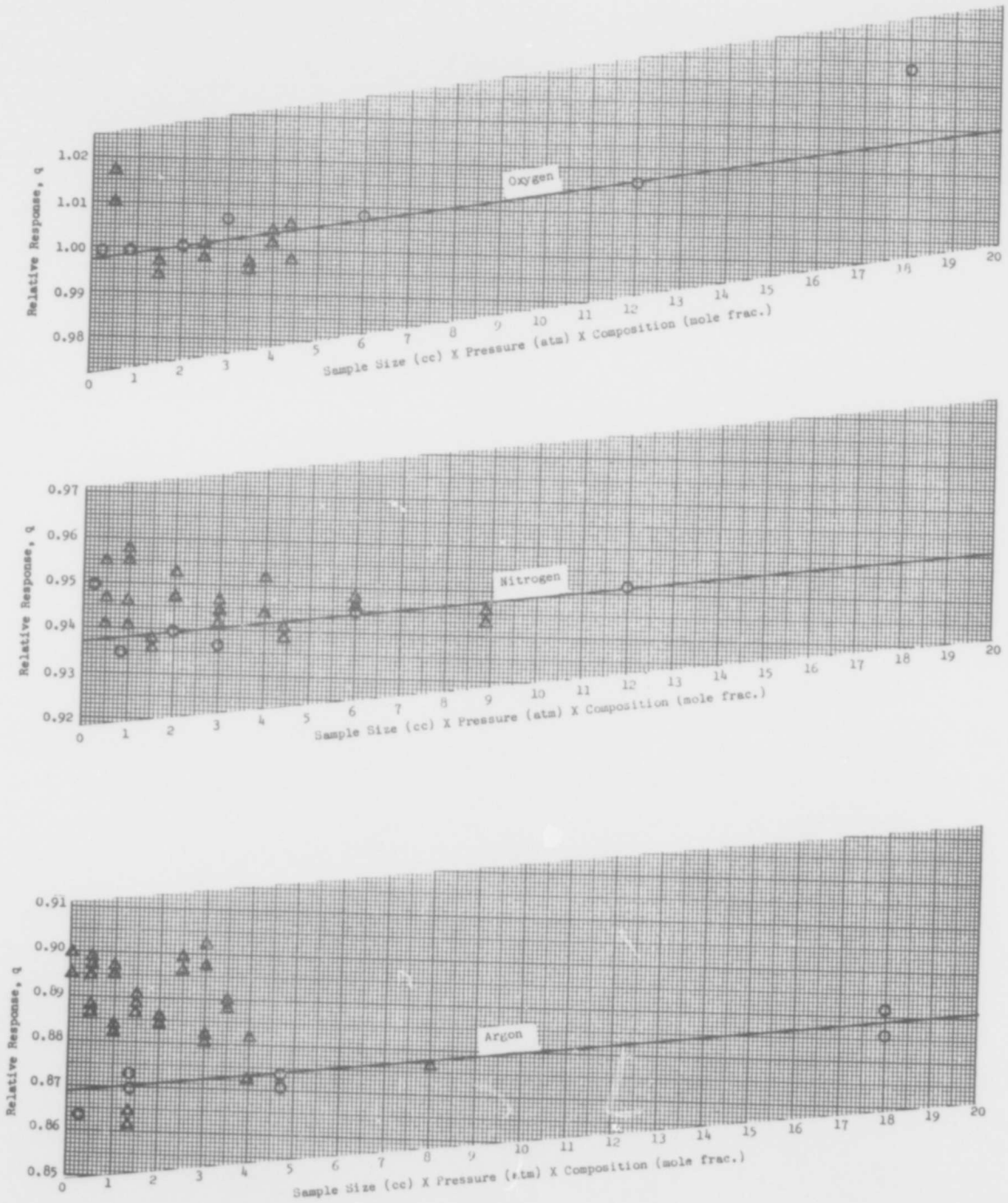


Figure 12. Chromatograph Calibration Curves.

TABLE 2

SAMPLE LONG-TERM ANALYSES

<u>Synthetic Air</u>				<u>Special Mix</u>			
<u>Date</u>	<u>N₂</u>	<u>Ar</u>	<u>O₂</u>	<u>Date</u>	<u>N₂</u>	<u>Ar</u>	<u>O₂</u>
4-18-63	77.594	0.891	21.513	1-8-63	47.035	3.771	49.195
4-29-63	77.556	0.836	21.607	1-23-63	46.602	3.835	49.563
5-13-63	78.028	0.920	21.051	3-19-63	46.844	3.805	49.350
6-3-63	77.772	0.912	21.315	4-4-63	46.692	3.754	49.555
6-13-63	77.571	0.874	21.553	4-16-63	47.028	3.678	49.295
7-4-63	77.663	0.838	21.497	4-29-63	46.683	3.764	49.552
7-18-63	77.674	0.775	21.569	5-13-63	46.648	3.800	49.550
8-1-63	77.936	0.531	21.531	6-3-63	46.925	3.783	49.291
8-16-63	77.107	0.874	22.018	6-24-63	46.861	3.755	49.383
8-29-63	77.467	0.793	21.739	7-11-63	48.841	3.630	49.527
9-17-63	77.600	0.853	21.546	7-29-63	49.074	3.533	47.394
9-30-63	77.859	0.837	21.302	8-16-63	48.377	3.533	48.089
10-4-63	78.544	0.837	20.617	8-29-63	46.974	3.726	49.299
10-21-63	77.508	0.897	21.593				

V. EXPERIMENTAL DATA

The tables to follow list the entire experimental data taken during this project. There are listed a total of 1962 points, although there are 1965 listed run numbers; the missing numbers are runs where a mishap such as a lost sample occurred. The data range from one to twenty-six atmospheres and from 139°R to 250°R. Tables 3 through 16 are arranged according to pressure level and the run numbers represent only the chronology of measurement. All runs have been included whether they were used in the correlation or discarded for badness of fit.

The component gases used for these measurements are APCI produced with typical analyses as follows:

Oxygen: 99.70% O₂, 0.30% Ar

Nitrogen: 99.997% N₂, 0.003% Ar

Argon: 99.996% Ar, 0.002% N₂, 0.002% O₂

A typical run had the following history. One hour elapsed from the time of introduction of the first gas into the equilibrium apparatus until the samples were taken. The samples were stored approximately six hours as analytical inventory and then one hour elapsed during analysis. The raw area data was sent to the computer the next morning and the calculated compositions returned in the afternoon one day later.

Modifications in procedure took place throughout the duration of the program. The first run was made Aug. 13, 1962 and the last run was made October 17, 1963. The following progressive modifications took place during the program.

- Run 151: Changed to dual chromatograph system for analysis
- Run 264: Changed to relative response, Freon column chromatograph for analysis
- Run 609: Finished initial contract
- Run 610: Started extension to contract. The 500 psia pressure gauge was installed on the equilibrium apparatus in place of the 300 psia gauge.
- Run 936: The 500 psia pressure gauge was removed from the equilibrium apparatus and the 300 psia gauge re-installed.

Runs 1361-1683, 1689-1965: Detachable sample loops used on equilibrium apparatus. All other runs used sample bombs

Run 1530: Mixed solvent Freon-Ethane replaced Freon in the column of the chromatograph

Run 1965: Last run.

TABLE 3
EXPERIMENTAL DATA AT 1 ATM.

RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION		VAPOR MOL FRACTION	VAPOR MOL FRACTION	RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION		VAPOR MOL FRACTION	VAPOR MOL FRACTION	
		N2	AR					N2	AR			N2
1576	158.9	.07559245	.2524	1611	155.9	.0758	.5913	.2055	.5522	.2423
1577	155.9	.15548446	.4239	1612	155.9	.0653	.7274	.1825	.6592	.1583
1578	150.9	.31156885	.6571	1613	155.9	.0585	.8213	.1625	.7463	.0912
1579	155.9	.0462	.95381290	1614	152.9	.2371	.0361	.5597	.0316	.4087
1580	152.9	.1411	.85893381	1615	152.9	.2378	.0639	.5465	.0564	.3971
1581	162.40299	.9701	1616	152.9	.2274	.0872	.5346	.0759	.3894
1582	162.20506	.9494	1617	152.9	.2187	.1264	.5142	.1102	.3757
1583	162.10647	.9353	1618	152.9	.2117	.2134	.4922	.1702	.3286
1584	161.80726	.9274	1619	152.9	.1899	.3600	.4403	.2955	.2642
1585	161.50985	.9015	1620	152.9	.1769	.4923	.4075	.3950	.1974
1584	161.21249	.8751	1621	152.9	.1614	.6344	.3736	.4996	.1268
1587	160.42343	.7657	1622	152.9	.1491	.7455	.3573	.5752	.0675
1588	158.95054	.4946	1623	150.9	.3151	.0141	.6573	.0112	.3315
1589	158.46682	.3318	1624	150.9	.3156	.0286	.6527	.0220	.3253
1590	157.98403	.1597	1625	150.9	.3055	.0423	.6404	.0330	.3267
1591	157.49541	.0459	1626	150.9	.3035	.0499	.6369	.0377	.3255
1592	158.9	.0743	.0197	.9156	.2341	1627	150.9	.3012	.0613	.6357	.0477	.3165
1593	158.9	.0629	.0231	.9140	.2175	1628	150.9	.3033	.0880	.6252	.0569	.3080
1594	158.9	.0629	.0335	.9036	.2116	1629	150.9	.3006	.1274	.6143	.0968	.2889
1595	158.9	.0604	.0448	.8948	.2045	1630	150.9	.2969	.2138	.6017	.1579	.2404
1596	158.9	.0591	.0559	.8850	.1977	1631	150.9	.2852	.3181	.5707	.2263	.2031
1597	158.9	.0549	.0812	.8639	.1821	1632	150.9	.2545	.4878	.5151	.3453	.1395
1598	158.9	.0574	.1087	.8339	.1621	1633	150.9	.2407	.6712	.4934	.4572	.0494
1599	158.9	.0411	.1632	.7957	.1310	1634	150.9	.3881	.0692	.7093	.0468	.2439
1600	158.9	.0239	.2824	.6937	.0792	1635	148.9	.3826	.1667	.6820	.1131	.2049
1601	155.9	.1496	.0165	.8339	.4169	1636	148.9	.3661	.2559	.6638	.1468	.1693
1602	155.9	.1451	.0266	.8242	.4091	1637	148.9	.3611	.3675	.6455	.2301	.1244
1603	155.9	.1475	.0347	.8178	.4075	1638	148.9	.3363	.5470	.6094	.3350	.0556
1604	155.9	.1432	.0478	.8090	.4024	1639	148.9	.3131	.6869	.5790	.4210
1605	155.9	.1442	.0607	.7951	.4092	1640	145.0	.5523	.4477	.7838	.2162
1606	155.9	.1381	.0846	.7773	.3871	1641	143.0	.8514	.1486	.8907	.1093
1607	155.9	.1354	.1155	.7491	.3603	1642	143.0	.73079147
1608	155.9	.1249	.1894	.6857	.3331	1643	146.9	.49618050
1609	155.9	.1030	.3263	.5707	.2785	1644	141.5	.87109627
1610	155.9	.0883	.4522	.4595	.2397	1645	140.0	.98609962

TABLE 3
EXPERIMENTAL DATA AT 1 ATM. (continued)

RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION N2	LIQUID MOL FRACTION AR	LIQUID MOL FRACTION O2	VAPOR MOL FRACTION N2	VAPOR MOL FRACTION AR	VAPOR MOL FRACTION O2	RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION N2	LIQUID MOL FRACTION AR	LIQUID MOL FRACTION O2	VAPOR MOL FRACTION N2	VAPOR MOL FRACTION AR	VAPOR MOL FRACTION O2
1646	141.5	.8457	.15439363	.0637	1682	140.0	.9766	.0102	.0132	.9917	.0025	.0057
1647	141.0	.8790	.12109506	.0494	1683	140.0	.9779	.0162	.0059	.9892	.0096	.0012
1648	140.4	.9373	.06279749	.0251	1923	162.50088	.99120142	.9858
1649	140.2	.9623	.03779843	.0157	1924	160.42559	.74413327	.6673
1650	140.0	.9822	.01789938	.0062	1925	158.90789	.90570191	.7250
1651	139.7	.9928	.00729973	.0027	1926	158.9	.0543	.0154	.8317	.2559	.0191	.7250
1652	146.9	.4775	.0150	.5075	.7892	.0093	.2016	1927	157.49754	.0236	.1778	.1431	.6790
1653	146.9	.4825	.0217	.4958	.7883	.0145	.1972	1928	155.9	.1397	.0612	.79919783	.0217
1654	146.9	.4840	.0358	.4902	.7866	.0218	.1916	1929	155.9	.1297	.1193	.7509	.3901	.0641	.5458
1655	146.9	.4800	.0485	.4715	.7864	.0295	.1841	1930	155.9	.0578	.7335	.2087	.3595	.1244	.5160
1656	146.9	.4879	.0673	.4449	.7862	.0402	.1736	1931	155.9	.0432	.9005	.0563	.1596	.6820	.1584
1657	146.9	.4894	.0924	.4182	.7794	.0544	.1661	1942	150.9	.2924	.2203	.4874	.1187	.8395	.0418
1658	146.9	.4789	.1308	.3903	.7655	.0772	.1572	1943	146.9	.4958	.0207	.4835	.5925	.1610	.2465
1659	146.9	.4743	.2292	.2965	.7512	.1298	.1190	1944	146.9	.4529	.3779	.1693	.7978	.0124	.1898
1660	146.9	.4489	.3809	.1702	.7063	.2064	.0853	1945	145.0	.5769	.3597	.0634	.7196	.2104	.0699
1661	146.9	.4344	.5184	.0471	.6981	.2818	.0201	1946	145.0	.5936	.0404	.3660	.8015	.1750	.0235
1662	145.0	.6166	.0392	.3442	.8578	.0189	.1234	1947	145.0	.6075	.0895	.3030	.8474	.0215	.1304
1663	145.0	.6106	.0873	.3021	.8481	.0407	.1112	1948	145.0	.5867	.0956	.2177	.8474	.0461	.1065
1664	145.0	.5916	.1818	.2266	.8292	.0935	.0773	1949	143.0	.7464	.0102	.2435	.8223	.0992	.0785
1665	143.0	.5823	.2789	.1388	.8111	.1354	.0535	1950	143.0	.7571	.0275	.2153	.9182	.0048	.0770
1666	143.0	.7478	.0112	.2410	.9178	.0057	.0765	1951	143.0	.7150	.2431	.0419	.9193	.0124	.0683
1667	143.0	.7522	.0250	.2228	.9174	.0107	.0719	1952	143.0	.7077	.29238707	.1073	.0141
1668	143.0	.7584	.0337	.2080	.9197	.0150	.0653	1953	141.5	.9612	.03889851	.0149
1669	143.0	.7524	.0502	.1975	.9150	.0228	.0621	1954	141.5	.86479851	.0149
1670	143.0	.7528	.0744	.1728	.9123	.0333	.0544	1955	141.5	.8504	.1496	.1353	.96060394
1671	143.0	.7464	.0921	.1615	.9078	.0414	.0508	1956	141.5	.8504	.14969387
1672	143.0	.7313	.1314	.1373	.8979	.0590	.0431	1957	141.5	.8664	.00959581	.0613
1673	143.0	.7203	.2422	.0375	.8922	.1064	.0114	1958	141.5	.8562	.1093	.1239	.9454	.0041	.0377
1674	141.5	.8569	.0280	.1351	.8545	.0048	.0114	1959	140.8	.9001	.0999	.0345	.9454	.0449	.0097
1675	141.5	.8573	.0186	.1241	.9545	.0048	.0407	1959	140.1	.9622	.03789598	.0402
1676	141.5	.8378	.0395	.1027	.9549	.0078	.0373	1960	140.2	.9549	.04519852	.0148
1677	141.5	.8515	.0499	.0986	.9544	.0170	.0286	1961	140.3	.9523	.04779818	.0182
1678	141.5	.8544	.0615	.0841	.9500	.0205	.0295	1962	129.9	.9845	.01559808	.0192
1679	141.5	.8502	.0875	.0641	.9492	.0251	.0251	1963	140.0	.9838	.00439940	.0060
1680	141.5	.8616	.1097	.0623	.9458	.0360	.0181	1964	140.0	.9844	.0098	.0119	.9953	.0016	.0030
1681	140.0	.9788	.0080	.0132	.9490	.0425	.0085	1965	140.0	.9778	.0151	.0058	.9948	.0038	.0014
					.9934	.0022	.0044						.9924	.0057	.0019

TABLE 4
EXPERIMENTAL DATA AT 2 ATM.

RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION N2	LIQUID MOL FRACTION AR	LIQUID MOL FRACTION O2	VAPOR MOL FRACTION N2	VAPOR MOL FRACTION AR	VAPOR MOL FRACTION O2	TEMP. DEG.R	LIQUID MOL FRACTION N2	LIQUID MOL FRACTION AR	LIQUID MOL FRACTION O2	VAPOR MOL FRACTION N2	VAPOR MOL FRACTION AR	VAPOR MOL FRACTION O2
1466	171.9	.07219279	.21607840	1500	168.9	.1258	.1657	.3082	.1703	.5215
1467	168.9	.14708530	.37696231	1501	168.9	.1058	.2999	.2589	.2997	.4414
1468	162.9	.34376563	.64073593	1502	168.9	.0845	.4310	.2239	.4141	.3620
1469	158.9	.51394861	.78232177	1503	168.9	.0725	.5494	.1775	.5296	.2928
1470	160.9	.3406	.65945779	.4221	1504	168.9	.0623	.6623	.1506	.6330	.2164
1471	165.9	.1371	.86293001	.6999	1505	168.9	.0484	.7692	.1205	.7307	.1487
1472	167.9	.0708	.92921762	.8238	1506	165.9	.2297	.0280	.5029	.0258	.4713
1473	175.10464	.95360644	.9356	1507	165.9	.2228	.0672	.4845	.0616	.4538
1474	175.30195	.98050288	.9712	1508	165.9	.2160	.1350	.4619	.1202	.4179
1475	175.00524	.94760753	.9247	1509	165.9	.2012	.2539	.4280	.2190	.3531
1476	174.80690	.93100975	.9025	1510	165.9	.1812	.4112	.3848	.3475	.2677
1477	174.70808	.91921138	.8862	1511	165.9	.1646	.5671	.3518	.4692	.1790
1478	174.50962	.90381335	.8665	1512	165.9	.1461	.7326	.3194	.5955	.0851
1479	174.31180	.88201594	.8406	1513	165.9	.1390	.8357	.3044	.6784	.0173
1480	173.42357	.76432972	.7028	1514	162.9	.3364	.0131	.6306	.0129	.3565
1481	171.95050	.49415674	.4326	1515	162.9	.3317	.0286	.6273	.0225	.3502
1482	171.45902	.40986432	.3568	1516	162.9	.3331	.0402	.6282	.0315	.3403
1483	170.67881	.21198151	.1849	1517	162.9	.3288	.0531	.6228	.0411	.3361
1484	170.39722	.02789762	.0238	1518	162.9	.3324	.0666	.6225	.0515	.3260
1485	171.9	.0719	.0094	.9187	.2081	.0122	.7797	1519	162.9	.3240	.0965	.6245	.0701	.3054
1486	171.9	.0717	.0187	.9096	.2118	.0233	.7648	1520	162.9	.3220	.1370	.5970	.1048	.2982
1487	171.9	.0699	.0332	.8969	.2009	.0414	.7577	1521	162.9	.3146	.2092	.5787	.1577	.2636
1488	171.9	.0658	.0507	.8835	.1892	.0627	.7481	1522	162.9	.2930	.3768	.5382	.2757	.1861
1489	171.9	.0652	.0619	.8729	.1856	.0767	.7378	1523	162.9	.2740	.5469	.5058	.3903	.1039
1490	171.9	.0565	.0680	.8555	.1619	.1083	.7298	1524	162.9	.2601	.6540	.4860	.4610	.0530
1491	171.9	.0505	.1286	.8209	.1439	.1568	.6993	1525	160.9	.4083	.0573	.6986	.0388	.2626
1492	171.9	.0282	.2552	.7167	.0804	.3037	.6159	1526	160.9	.4062	.0949	.6882	.0653	.2465
1493	168.9	.1393	.0098	.8509	.3684	.0108	.6208	1527	160.9	.3932	.1777	.6643	.1206	.2150
1494	168.9	.1370	.0266	.8364	.3545	.0283	.6172	1528	160.9	.3766	.3155	.6311	.2144	.1545
1495	168.9	.1353	.0374	.8273	.3490	.0388	.6122	1529	160.9	.3595	.4856	.6029	.3140	.0831
1496	168.9	.1388	.0482	.8130	.3401	.0512	.6087	1530	158.9	.5052	.0127	.7761	.0178	.2161
1497	168.9	.1363	.0581	.8056	.3482	.0620	.5899	1531	158.9	.5088	.0255	.7757	.0132	.2081
1498	168.9	.1318	.0880	.7802	.3397	.0893	.5710	1532	158.9	.5039	.0404	.7711	.0256	.2033
1499	168.9	.1323	.1132	.7545	.3284	.1183	.5533	1533	158.9	.5052	.0595	.7653	.0382	.1966

TABLE 4
EXPERIMENTAL DATA AT 2 ATM. (continued)

RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION		RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION		VAPOR MOL FRACTION N ₂	VAPOR MOL FRACTION O ₂	VAPOR MOL FRACTION N ₂	VAPOR MOL FRACTION O ₂
		N ₂	AR			N ₂	AR				
1534	158.9	.5070	.0721	1569	151.5	.9719	.0281	.9880	.0120	.9880	.0120
1535	158.9	.5024	.0979	1570	151.7	.9529	.0471	.9798	.0202	.9798	.0202
1536	158.9	.4960	.1387	1571	151.8	.9410	.0590	.9738	.0262	.9738	.0262
1537	158.9	.4978	.2360	1572	152.2	.9001	.0999	.9547	.0453	.9547	.0453
1538	158.9	.4725	.3439	1573	152.9	.8450	.1550	.9283	.0717	.9283	.0717
1539	158.9	.4560	.4730	1574	154.9	.6956	.3044	.8500	.1500	.8500	.1500
1540	156.9	.6172	.9377	1575	157.9	.4978	.5022	.7189	.2811	.7189	.2811
1541	156.9	.6072	.1204	1896	175.2	.0000	.0274	.0000	.0395	.0000	.0395
1542	156.9	.6061	.1386	1897	171.9	.0000	.4999	.0000	.5608	.0000	.5608
1543	156.9	.6027	.1926	1898	171.9	.0000	.0105	.0000	.0133	.0000	.0133
1544	156.9	.5723	.3893	1899	170.2	.0000	.9785	.2172	.0133	.2172	.7694
1545	154.9	.7392	.0133	1900	168.9	.0417	.8890	.1059	.9799	.1059	.0201
1546	154.9	.7376	.0279	1901	168.3	.1417	.0402	.3576	.0364	.3576	.0577
1547	154.9	.7343	.0418	1902	168.3	.1349	.0919	.3357	.0434	.3357	.5990
1548	154.9	.7318	.0541	1903	168.3	.0834	.4342	.2050	.0976	.2050	.5668
1549	154.9	.7273	.0693	1904	168.9	.0586	.6829	.1456	.4284	.1456	.3666
1550	154.9	.7220	.0992	1905	167.9	.0670	.9330	.1654	.6495	.1654	.2049
1551	154.9	.7246	.1281	1906	165.9	.2359	.0000	.5189	.8346	.5189	.0000
1552	154.9	.7038	.2521	1907	165.9	.1335	.8386	.2960	.0000	.2960	.4811
1553	152.9	.8681	.0164	1908	162.9	.3365	.0150	.6354	.6938	.6354	.0202
1554	152.9	.8756	.0249	1909	162.9	.3271	.0952	.6103	.0119	.6103	.3527
1555	152.9	.8732	.0380	1910	160.9	.4144	.0331	.7069	.0743	.7069	.3152
1556	152.9	.8722	.0465	1911	160.9	.4192	.0539	.7036	.0238	.7036	.2693
1557	152.9	.8633	.0539	1912	158.9	.4848	.2341	.7284	.0373	.7284	.2591
1558	152.9	.8654	.0724	1913	158.9	.5032	.0524	.7685	.1428	.7685	.1289
1559	152.9	.8595	.0952	1932	156.9	.6123	.0688	.8304	.0341	.8304	.1974
1560	151.9	.9460	.0071	1933	156.9	.5909	.1957	.8013	.0385	.8013	.1311
1561	151.9	.9409	.0207	1934	152.9	.6464	.1261	.8013	.1091	.8013	.0896
1562	151.9	.9349	.0339	1935	152.9	.8576	.0244	.9320	.0580	.9320	.0101
1563	151.9	.9343	.0424	1936	152.9	.8636	.0449	.9511	.0117	.9511	.0372
1564	154.9	.7401	.0000	1937	152.9	.8583	.0582	.9476	.0208	.9476	.0316
1565	152.9	.8744	.0000	1938	151.9	.9330	.0343	.9436	.0273	.9436	.0291
1566	151.9	.9449	.0000	1939	151.9	.9277	.0634	.9737	.0153	.9737	.0110
1567	151.2	.9949	.0051	1940	151.9	.9336	.0434	.9691	.0281	.9691	.0028
1568	151.4	.9810	.0190	1941	151.2	.9930	.0070	.9731	.0191	.9731	.0078
								.9972	.0028		

TABLE 5
EXPERIMENTAL DATA AT 4 ATM.

RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION		VAPOR MOL FRACTION		RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION		VAPOR MOL FRACTION	
		N2	AR	N2	AR			N2	AR	N2	AR
1361	182.8	.0702	.9298	.0000	.8453	1394	186.8	.0717	.0609	.1783	.0721
1362	180.8	.1320	.8660	.0000	.7297	1395	186.8	.0679	.0781	.1672	.0905
1363	174.8	.3687	.6313	.0000	.4268	1396	186.8	.0639	.1128	.1543	.1302
1364	171.9	.5277	.4723	.0000	.2870	1397	186.8	.0547	.1363	.1360	.1598
1365	168.4	.7372	.2628	.0000	.1417	1398	186.8	.0474	.1859	.1162	.2150
1366	166.9	.8444	.1556	.0000	.0786	1399	186.8	.0252	.3400	.0615	.3913
1367	165.9	.9181	.0819	.0000	.0386	1400	183.8	.1581	.0139	.3473	.0148
1368	165.6	.9373	.0627	.0000	.0292	1401	183.8	.1524	.0274	.3422	.0296
1369	165.4	.9529	.0471	.0000	.0222	1402	183.8	.1490	.0435	.3320	.0454
1370	165.3	.9632	.0368	.0000	.0172	1403	183.8	.1492	.0589	.3286	.0510
1371	165.1	.9775	.0225	.0000	.0098	1404	183.8	.1444	.0767	.3186	.0903
1372	165.0	.9872	.0128	.0000	.0059	1405	183.8	.1403	.1073	.3108	.1133
1373	186.8	.0860	.0000	.9140	.0000	1406	183.8	.1315	.1320	.2935	.1379
1374	183.8	.1591	.0000	.8409	.0000	1407	183.8	.1243	.1982	.2683	.2019
1375	177.8	.3454	.0000	.6546	.0000	1408	183.8	.0937	.4243	.2014	.4176
1376	171.9	.5987	.0000	.4013	.0000	1409	183.8	.0738	.5904	.1592	.5689
1377	168.4	.7788	.0000	.2212	.0000	1410	183.8	.0552	.7561	.1207	.7216
1378	166.9	.8697	.0000	.1303	.0000	1411	183.8	.0454	.9092	.1007	.8608
1379	165.4	.9620	.0000	.0380	.0000	1412	180.8	.2469	.0276	.4821	.0255
1380	190.6	.0000	.0252	.9748	.0000	1413	180.8	.2334	.0689	.4625	.0633
1381	190.4	.0000	.0514	.9466	.0346	1414	180.8	.2262	.1275	.4410	.4742
1382	190.3	.0000	.0446	.9554	.0677	1415	180.8	.2021	.2884	.3889	.4407
1383	190.2	.0000	.0471	.9529	.0605	1416	180.8	.1738	.5136	.3345	.4451
1384	190.1	.0000	.0519	.9481	.0640	1417	180.8	.1579	.6464	.3087	.4517
1385	189.8	.0000	.0804	.9196	.1077	1418	180.8	.1447	.7674	.2880	.6488
1386	188.8	.0000	.1947	.8053	.2444	1419	180.8	.1415	.8257	.2784	.6971
1387	187.3	.0000	.4232	.5768	.4807	1420	177.8	.3435	.0091	.6006	.0245
1388	186.3	.0000	.6296	.3704	.6616	1421	177.8	.3423	.0211	.5966	.0074
1389	185.8	.0000	.7869	.2131	.8077	1422	177.8	.3407	.0387	.5906	.0167
1390	185.4	.0000	.9313	.0687	.9399	1423	177.8	.3380	.0472	.5906	.0315
1391	186.8	.0812	.0154	.9033	.0182	1424	177.8	.3305	.0867	.5889	.0384
1392	186.8	.0765	.0316	.8920	.0378	1425	177.8	.3200	.1328	.5729	.0709
1393	186.8	.0748	.0478	.8774	.0563	1426	177.8	.3152	.1763	.5560	.1071
										.5436	.1412
											.3152

TABLE 5
EXPERIMENTAL DATA AT 4 ATM. (continued)

RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION		VAPOR MOL FRACTION		RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION		VAPOR MOL FRACTION	
		N ₂	AR	N ₂	O ₂			N ₂	AR	N ₂	AR
1427	177.8	.3092	.2168	.4740	.2885	1460	166.9	.8683	.0650	.9408	.0324
1428	177.8	.2841	.4007	.3153	.1978	1461	166.9	.8583	.1006	.9340	.0505
1429	177.8	.3054	.5906	.1040	.0743	1462	166.9	.8557	.1279	.9290	.0650
1430	174.8	.4548	.0319	.5132	.2771	1463	165.4	.9614	.0120	.9847	.0053
1431	174.8	.4474	.0906	.4621	.2509	1464	165.4	.9625	.0228	.9836	.0107
1432	174.8	.4374	.1559	.4068	.2229	1465	165.4	.9634	.0187	.9843	.0086
1433	174.8	.4171	.2735	.3094	.1670	1869	190.6	.0000	.0110	.0000	.0148
1434	174.8	.3981	.4444	.1574	.0833	1870	190.4	.0000	.0291	.0000	.0401
1435	174.8	.3890	.5421	.0689	.0405	1871	190.1	.0000	.0558	.0000	.0759
1436	171.9	.5909	.0114	.3887	.1861	1872	189.3	.0000	.1417	.0000	.1928
1437	171.9	.5913	.0251	.3837	.1850	1873	185.4	.0000	.9506	.0000	.9552
1438	171.9	.5940	.0341	.3718	.1850	1874	183.8	.1527	.0399	.3369	.0422
1439	171.9	.5931	.0512	.3557	.1757	1875	180.8	.1991	.2954	.3831	.2630
1440	171.9	.5932	.0618	.3451	.1706	1876	180.8	.1445	.7618	.2849	.6459
1441	171.9	.5898	.0880	.3222	.1674	1877	177.8	.2448	.7552	.4251	.5749
1442	171.9	.5868	.1162	.2970	.1555	1878	177.8	.3354	.0739	.5785	.0602
1443	171.9	.5664	.2279	.2057	.1438	1879	177.8	.2571	.6278	.4479	.4771
1444	171.9	.5505	.3544	.0951	.1011	1880	176.8	.3830	.0000	.6380	.0000
1445	169.9	.6897	.0641	.2461	.1074	1881	174.8	.3849	.5483	.5908	.3705
1446	169.9	.6811	.1252	.1936	.0859	1882	171.9	.5931	.0120	.8019	.0076
1447	169.9	.6678	.2317	.1005	.0451	1883	171.9	.5895	.0243	.7980	.0153
1448	168.4	.7814	.0118	.2068	.0890	1884	171.9	.5410	.3648	.7306	.2215
1449	168.4	.7764	.0259	.1977	.0826	1885	169.9	.6860	.0675	.8502	.0392
1450	168.4	.7744	.0406	.1850	.0792	1886	168.4	.7741	.0273	.9005	.0148
1451	168.4	.7694	.0565	.1741	.0738	1887	168.4	.7714	.0427	.8981	.0233
1452	168.4	.7686	.0645	.1669	.0696	1888	166.9	.8638	.0168	.9443	.0084
1453	168.4	.7668	.0929	.1403	.0599	1889	166.9	.8492	.1004	.9279	.0519
1454	168.4	.7614	.1346	.1040	.0449	1890	166.9	.8456	.1359	.9226	.0698
1455	168.4	.7486	.2051	.0463	.0200	1891	165.4	.9552	.0175	.9613	.0081
1456	166.9	.8655	.0126	.1219	.0461	1892	165.4	.9547	.0270	.9790	.0132
1457	166.9	.8678	.0255	.1067	.0421	1893	165.4	.9535	.0215	.9799	.0079
1458	166.9	.8681	.0344	.0975	.0394	1894	165.4	.9528	.0347	.9780	.0104
1459	166.9	.8667	.0487	.0846	.0344	1895	165.1	.9737	.0263	.9872	.0128

TABLE 6
EXPERIMENTAL DATA AT 6 ATM.

RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION		VAPOR MOL FRACTION		RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION		VAPOR MOL FRACTION	
		N ₂	AR	N ₂	AR			N ₂	AR	N ₂	AR
453	197.8	.07219279	.1646	492	186.8	.3645	.1810	.5705	.1430
454	195.8	.12138787	.2595	493	182.8	.5443	.0363	.7464	.0253
455	191.8	.22857715	.4310	494	182.8	.5410	.0555	.7405	.0377
456	187.8	.35486452	.5440	495	182.8	.5387	.0725	.7410	.0484
457	183.8	.50694931	.7208	496	182.8	.5354	.0936	.7308	.0650
458	179.8	.68903110	.8468	497	182.8	.5276	.1321	.7362	.0930
459	176.8	.84131587	.9284	498	182.8	.5153	.1887	.7076	.1292
460	174.8	.95130487	.9794	499	179.8	.6730	.0355	.8351	.0222
461	200.80274	.9726	500	179.8	.6730	.0574	.8296	.0358
462	200.50550	.9450	501	179.8	.6710	.0755	.8398	.0433
463	200.20868	.9132	502	179.8	.6679	.0953	.8236	.0591
464	199.91198	.8802	503	179.8	.6630	.1332	.8149	.0831
465	174.8	.9373	.06276666	504	179.8	.6536	.1906	.8404	.0957
466	175.3	.9035	.09659314	505	177.8	.7714	.0625	.8849	.0367
467	175.8	.8728	.12729107	506	177.8	.7655	.1372	.8814	.0540
468	176.3	.8395	.16059137	507	177.8	.7566	.1975	.8750	.0797
469	198.8	.6441	.0307	.9252	.0966	508	177.8	.8903	.0240	.9500	.0125
470	198.8	.0408	.0474	.9116	.0879	509	175.8	.8651	.0857	.9377	.0455
471	198.8	.0261	.0623	.9116	.0879	510	175.8	.8651	.0511	.9466	.0274
472	198.8	.0354	.0794	.8852	.0619	511	175.8	.8796	.0670	.9407	.0358
473	198.8	.0247	.1000	.8714	.0666	512	175.8	.9823	.0800	.9377	.0455
474	198.8	.0190	.1561	.8249	.0441	513	175.8	.9782	.0972	.9364	.0527
475	194.8	.1400	.0319	.8261	.2413	514	175.8	.9428	.1140	.9325	.0175
476	194.8	.1371	.0486	.8142	.2413	515	174.8	.9461	.0383	.9760	.0175
477	194.8	.1334	.0676	.7990	.2769	516	174.8	.9428	.0074	.9748	.0039
478	194.8	.1317	.0814	.7869	.2707	517	174.8	.9428	.0074	.9748	.0039
479	194.8	.1242	.1130	.7628	.2552	518	198.8	.0440	.0191	.9369	.0214
480	194.8	.1154	.1685	.7161	.2392	519	198.8	.0366	.0636	.8996	.8727
481	190.8	.2531	.0327	.7142	.4605	520	194.8	.1436	.0191	.8372	.8357
482	190.8	.2483	.0529	.6988	.4519	521	190.8	.2565	.0193	.7242	.6853
483	190.8	.2477	.0683	.6841	.4485	522	186.8	.3669	.0200	.4623	.5195
484	190.8	.2441	.0834	.6724	.4436	523	186.8	.3786	.0509	.6130	.3709
485	190.8	.2388	.1232	.6379	.4303	524	182.8	.5444	.0182	.6046	.0410
486	190.8	.2294	.1742	.5963	.4126	525	182.8	.5335	.0760	.7475	.0128
487	186.8	.3858	.0344	.5796	.6105	526	182.8	.5268	.1323	.7214	.0513
488	186.8	.3641	.0522	.5636	.6893	527	179.8	.6769	.0136	.8395	.0909
489	186.8	.3826	.0684	.5489	.6016	528	179.8	.6685	.0731	.8257	.0042
490	186.8	.3773	.0899	.5328	.5953	529	179.8	.5516	.1921	.8257	.0450
491	186.8	.3725	.1243	.5032	.5856	530	177.8	.7764	.0179	.8944	.1181
						531	177.8	.7785	.0314	.8934	.0097
						532					.0175
						533					.0090
						534					.0042
						535					.1294
						536					.0781
						537					.0959
						538					.0090
						539					.0097
						540					.0097
						541					.0097
						542					.0097
						543					.0097
						544					.0097
						545					.0097
						546					.0097
						547					.0097
						548					.0097
						549					.0097
						550					.0097
						551					.0097
						552					.0097
						553					.0097
						554					.0097
						555					.0097
						556					.0097
						557					.0097
						558					.0097
						559					.0097
						560					.0097
						561					.0097
						562					.0097
						563					.0097
						564					.0097
						565					.0097
						566					.0097
						567					.0097
						568					.0097
						569					.0097
						570					.0097
						571					.0097
						572					.0097
						573					.0097
						574					.0097
						575					.0097
						576					.0097
						577					.0097
						578					.0097
						579					.0097
						580					.0097
						581					.0097
						582					.0097
						583					.0097
						584					.0097
						585					.0097
						586					.0097
						587					.0097
						588					.0097
						589					.0097
						590					.0097
						591					.0097
						592					.0097
						593					.0097
						594					.0097
						595					.0097
						596					.0097
						597					.0097
						598					.0097
						599					.0097
						600					.0097
						601					.0097
						602					.0097
						603					.0097
						604					.0097
						605					.0097
						606					.0097
						607					.0097
						608					.0097
						609					.0097

TABLE 6
EXPERIMENTAL DATA AT 6 ATM. (continued)

RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION		VAPOR MOL FRACTION		RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION		VAPOR MOL FRACTION	
		N2	AR	N2	AR			N2	AR	N2	AR
1304	190.8	.1452	.0548	.2666	.7334	1343	184.8	.3940	.4997	.5819	.3544
1305	184.8	.3758	.6242	.5580	.4420	1344	182.8	.5392	.0093	.7502	.0067
1306	179.8	.6219	.3781	.7683	.2317	1345	182.8	.5397	.0301	.7436	.0210
1307	177.8	.7409	.2591	.8515	.1485	1346	182.8	.4958	.3724	.6788	.2482
1308	174.6	.9522	.0478	.9759	.0241	1347	182.8	.4823	.4513	.6649	.2986
1309	174.4	.9610	.0390	.9807	.0193	1348	179.8	.6843	.0171	.8404	.0101
1310	174.3	.9701	.0299	.9851	.0149	1349	179.8	.6809	.0317	.8404	.0198
1311	174.2	.9802	.0198	.9907	.0097	1350	179.8	.6735	.0423	.8365	.0255
1312	174.1	.9918	.0082	.9968	.0032	1351	179.8	.6454	.2702	.7922	.1647
1313	201.0	.0000	.0036	.0000	.0032	1352	177.8	.7869	.0095	.8998	.0057
1314	200.9	.0000	.0035	.0000	.0052	1353	177.8	.7800	.0233	.8953	.0135
1315	200.7	.0000	.0232	.0000	.0353	1354	177.8	.7785	.0440	.8928	.0253
1316	198.8	.0000	.2430	.0000	.2850	1355	177.8	.7675	.0545	.8892	.0302
1317	197.8	.0000	.3928	.0000	.4407	1356	175.8	.8920	.0132	.9517	.0076
1318	196.8	.0000	.5850	.0000	.6192	1357	175.8	.8864	.0442	.9459	.0237
1319	196.4	.0000	.6895	.0000	.7147	1358	174.8	.9488	.0118	.9767	.0057
1320	195.1	.0000	.7832	.0000	.7986	1359	174.8	.9488	.0241	.9773	.0119
1321	198.8	.0464	.0120	.1097	.0151	1360	174.8	.9488	.0358	.9741	.0187
1322	194.8	.1446	.0118	.2994	.0129	1838	201.0	.0000	.0073	.0000	.0095
1323	194.8	.1371	.0524	.2818	.0564	1839	200.7	.0000	.0153	.0000	.0196
1324	194.8	.1188	.1409	.2442	.1482	1840	195.8	.0000	.0344	.0000	.0461
1325	194.8	.0854	.3512	.1747	.3583	1841	194.8	.0000	.0390	.0000	.0958
1326	194.8	.0618	.5288	.1263	.5268	1842	194.8	.0275	.9265	.0580	.8998
1327	194.8	.0469	.6631	.0953	.6543	1843	193.8	.0523	.9477	.1079	.8921
1328	194.8	.0377	.7657	.0501	.7481	1844	190.8	.2100	.3220	.3751	.2863
1329	190.8	.2539	.0170	.4645	.0151	1845	190.8	.2571	.0136	.4675	.0126
1330	190.8	.2444	.0603	.4439	.0563	1846	190.8	.1535	.8028	.2801	.6968
1331	190.8	.1907	.4286	.3430	.3771	1847	190.8	.1497	.8332	.2757	.7114
1332	190.8	.1711	.6049	.3080	.5238	1848	186.8	.3922	.0123	.6193	.0101
1333	190.8	.1592	.7272	.2896	.6239	1849	186.8	.3872	.0404	.6134	.0326
1334	190.8	.2109	.7528	.2772	.6896	1850	184.8	.4579	.0795	.6707	.0587
1335	190.8	.1435	.8454	.2791	.7093	1851	179.8	.6835	.0236	.8409	.0147
1336	186.8	.3855	.0331	.6140	.0226	1852	177.8	.7831	.0180	.8964	.0103
1337	186.8	.3277	.4581	.5188	.3458	1853	177.8	.7787	.0539	.8891	.0314
1338	186.8	.3115	.5889	.4912	.4444	1854	175.8	.8935	.0175	.8918	.0795
1339	186.8	.2999	.6581	.4787	.4928	1855	174.8	.9493	.0145	.9773	.0092
1340	184.8	.4486	.0794	.6718	.0504	1856	174.8	.9483	.0284	.9753	.0075
1341	184.8	.4397	.1528	.6490	.1110	1857	174.2	.9821	.0179	.9908	.0146
1342	184.8	.4238	.2668	.6226	.1935	1858	174.1	.9884	.0116	.9942	.0092

TABLE 7
EXPERIMENTAL DATA AT 8 ATM.

RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION		VAPOR MOL FRACTION		RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION		VAPOR MOL FRACTION	
		N ₂	AR	N ₂	O ₂			N ₂	AR	N ₂	AR
389	206.8	.0512	.9488	.1127	.8873	425	195.8	.3450	.0669	.5881	.3963
390	202.8	.1495	.8505	.2931	.7069	426	195.8	.3412	.0872	.5717	.3879
391	197.8	.2940	.7060	.4939	.5061	427	195.8	.3368	.1212	.5420	.3690
392	193.8	.4290	.5710	.6371	.3629	428	195.8	.3265	.1740	.4995	.3408
393	189.8	.5830	.4170	.7638	.2362	429	191.8	.4940	.0352	.4708	.2848
394	186.8	.7138	.2862	.8507	.1493	430	191.8	.4900	.0590	.4510	.2725
395	184.8	.8085	.1915	.9051	.0949	431	191.8	.4926	.0714	.4360	.2633
396	182.8	.9125	.0875	.9586	.0414	432	191.8	.4878	.0915	.4208	.2542
397	209.0	.0000	.9884	.0000	.0151	433	191.8	.4815	.1308	.3877	.2341
398	208.7	.0000	.9619	.0000	.0493	434	191.8	.4714	.1979	.3307	.2015
399	208.4	.0000	.9327	.0000	.0854	435	187.8	.6665	.0382	.2953	.1590
400	208.1	.0000	.9015	.0000	.1231	436	187.8	.6616	.0552	.2832	.1530
401	181.8	.9620	.0380	.9790	.0210	437	187.8	.6600	.0770	.2630	.1416
402	182.3	.9306	.0694	.9606	.0394	438	187.8	.6551	.0967	.2482	.1347
403	182.8	.8985	.1015	.9425	.0575	439	187.8	.6507	.1344	.2149	.1165
404	183.3	.8647	.1353	.9218	.0782	440	187.8	.6408	.1928	.1664	.0909
405	205.8	.0690	.9316	.1456	.8160	441	185.8	.7532	.0597	.1871	.0959
406	205.8	.0657	.8877	.1385	.8071	442	185.8	.7446	.1011	.1542	.0792
407	205.8	.0625	.8739	.1318	.7938	443	185.8	.7415	.1363	.1222	.0722
408	205.8	.0592	.8644	.1236	.7869	444	185.8	.7317	.1950	.0733	.0628
409	205.8	.0525	.8404	.1105	.7655	445	183.8	.8567	.0327	.1106	.0375
410	205.8	.0444	.8021	.0933	.7308	446	183.8	.8552	.0484	.0964	.0544
411	201.8	.1699	.7972	.3202	.6454	447	183.8	.8513	.0749	.0737	.0475
412	201.8	.1678	.7838	.3166	.6330	448	183.8	.9487	.0992	.0521	.0357
413	201.8	.1636	.7687	.3068	.6242	449	183.8	.8451	.1211	.0338	.0256
414	201.8	.1606	.7560	.3015	.6130	450	183.8	.8425	.1410	.0166	.0157
415	201.8	.1545	.7295	.2898	.5920	451	182.8	.9107	.0323	.0570	.0081
416	201.8	.1461	.6866	.2734	.5555	452	182.8	.9027	.0711	.0263	.0278
417	197.8	.2870	.6795	.4816	.4880	584	205.8	.0700	.0189	.0263	.0126
418	197.8	.2853	.6616	.4779	.4733	585	201.8	.1714	.0192	.0995	.8294
419	197.8	.2829	.6468	.4728	.4651	586	197.8	.2901	.0201	.6898	.6545
420	197.8	.2797	.6345	.4672	.4543	587	195.8	.3550	.0180	.6270	.4961
421	197.8	.2749	.6037	.4572	.4337	588	191.8	.4968	.0181	.4851	.4237
422	197.8	.2650	.5583	.4402	.4020	589	191.8	.4889	.0710	.4401	.2920
423	195.8	.3509	.6148	.5541	.4163	590	187.8	.6647	.0212	.3142	.2656
424	195.8	.3487	.5999	.5504	.4067	591	185.8	.7562	.0203	.2235	.1694
											.1148

TABLE 7
EXPERIMENTAL DATA AT 8 ATM. (continued)

RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION		VAPOR MOL FRACTION		RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION		VAPOR MOL FRACTION		
		N ₂	AR	N ₂	AR			N ₂	AR	N ₂	AR	
592	185.8	.7534	.0354	.2113	.1075	1279	195.8	.3411	.0417	.5485	.0347	.4168
593	183.8	.8564	.0207	.1229	.0604	1280	195.8	.3143	.2450	.4933	.2042	.3025
594	182.8	.9033	.0201	.0766	.0346	1281	195.8	.2997	.3660	.4710	.2978	.2312
595	182.8	.9044	.0457	.0499	.0239	1282	195.8	.2740	.5207	.4346	.4200	.1455
1246	181.8	.96450355	.0166	1283	195.8	.2585	.6835	.4130	.5460	.0410
1247	199.8	.1126	.8874	1284	191.8	.4970	.0086	.6947	.0065	.2988
1248	197.8	.1775	.8225	1285	191.8	.4926	.0517	.6850	.0384	.2766
1249	191.8	.4142	.5858	1286	191.8	.4462	.3391	.6202	.2462	.1336
1250	187.8	.6073	.3927	1287	191.8	.4224	.5123	.5912	.3688	.0400
1251	184.8	.7771	.2229	1288	189.8	.5739	.0373	.7521	.0264	.2215
1252	182.0	.9466	.0534	1289	189.8	.5669	.0828	.7357	.0599	.2044
1253	181.6	.9691	.0309	1290	189.8	.5621	.1163	.7340	.0819	.1841
1254	181.4	.9835	.0165	1291	189.8	.5426	.2457	.7074	.1695	.1230
1255	181.2	.9965	.0035	1292	189.8	.5223	.3915	.6826	.2669	.0505
1256	209.00089	.9912	.9894	1293	187.8	.6227	.3095	.7633	.1989	.0378
1257	208.80260	.9740	.9687	1294	187.8	.6094	.3581	.7529	.2294	.0177
1258	208.40709	.9291	.9123	1295	185.8	.7578	.0059	.8790	.0033	.1177
1259	207.32000	.8000	.7609	1296	185.8	.7597	.0266	.8743	.0160	.1097
1260	205.84186	.5814	.5372	1297	185.8	.7517	.0702	.8669	.0422	.0909
1261	204.86224	.3776	.3476	1298	185.8	.7256	.2362	.8368	.1435	.0197
1262	204.08511	.1489	1299	182.8	.9085	.0139	.9588	.0062	.0350
1263	205.8	.0707	.0113	.9180	.8357	1300	182.8	.9042	.0596	.9497	.0335	.0168
1264	205.8	.0257	.2503	.7240	.6640	1301	181.8	.9644	.0080	.9835	.0040	.0125
1265	201.8	.1728	.0128	.8145	.6594	1302	181.8	.9609	.0170	.9810	.0090	.0100
1266	201.8	.1044	.4105	.4851	.4023	1303	181.8	.9582	.3317	.9785	.0172	.0043
1267	201.8	.0613	.5967	.3220	.2713	1827	209.001100148	.9852
1268	201.8	.0679	.7204	.2118	.1790	1928	208.803020398	.9602
1269	201.8	.0587	.8326	.1087	.0962	1829	197.8	.2801	.0685	.4706	.0621	.4673
1270	199.8	.0546	.8906	.0548	.0475	1830	195.8	.3500	.0454	.5525	.0383	.4092
1271	199.8	.1785	.3013	.5202	.4020	1831	203.892489294	.0706
1272	199.8	.1560	.4659	.3780	.2972	1832	185.8	.7611	.01180072	.1146
1273	199.8	.1362	.6018	.2619	.2093	1833	183.8	.8432	.1271	.8782	.0738	.0141
1274	199.8	.1215	.7635	.1151	.0940	1834	182.8	.9144	.0155	.9121	.0087	.0322
1275	197.8	.2154	.4646	.3200	.2378	1835	181.8	.9653	.0124	.9841	.0064	.0095
1276	197.8	.1972	.6106	.1923	.1466	1836	181.8	.9582	.0418	.9769	.0231
1277	197.8	.1641	.7776	.0382	.0295	1837	181.2	.9957	.0043	.9977	.0023

TABLE 8
EXPERIMENTAL DATA AT 10 ATM.

RUN NO.	TEMP. DEG. R	LIQUID MOL FRACTION N ₂	LIQUID MOL FRACTION AR	VAPOR MOL FRACTION N ₂	VAPOR MOL FRACTION AR	RUN NO.	TEMP. DEG. R	LIQUID MOL FRACTION N ₂	LIQUID MOL FRACTION AR	VAPOR MOL FRACTION N ₂	VAPOR MOL FRACTION AR
325	212.8	.07061439	365	197.8	.5153	.0624	.6903	.0464
326	209.8	.14632719	366	197.8	.5171	.0566	.6927	.0430
327	205.8	.25874329	367	197.8	.5155	.0722	.6888	.0547
328	201.8	.38445767	368	197.8	.5117	.0890	.6850	.0668
329	197.8	.52847067	369	197.8	.5055	.1278	.6753	.0949
330	193.8	.68818249	370	197.8	.4974	.1829	.6644	.1363
331	190.8	.82439077	371	193.8	.6860	.0358	.8183	.0248
332	188.8	.92039606	372	193.8	.6813	.0565	.8137	.0385
333	215.800760099	373	193.8	.6607	.0741	.8121	.0503
334	215.503520445	374	193.8	.6752	.0950	.8076	.0633
335	215.206810833	375	193.8	.6680	.1326	.7968	.0901
336	214.910241240	376	193.8	.6624	.1813	.7901	.1207
337	187.7	.9666	.0334	.9810	377	191.8	.7714	.0556	.8707	.0356
338	188.2	.9384	.0614	.9640	378	191.8	.7636	.0948	.8625	.0609
339	188.8	.9090	.0910	.9460	379	191.8	.7556	.1378	.8543	.0984
340	189.3	.8801	.1199	.9282	380	191.8	.7474	.1895	.8461	.1206
341	212.8	.0652	.0278	.1306	.0377	381	189.8	.8714	.0228	.9314	.0139
342	212.8	.0611	.0453	.1218	.0254	382	189.8	.8689	.0300	.9289	.0188
343	212.8	.0567	.0594	.1154	.0150	383	189.8	.8663	.0502	.9257	.0311
344	212.8	.0536	.0779	.1079	.0909	384	189.8	.8628	.0717	.9220	.0445
345	212.8	.0470	.1085	.0947	.1240	385	189.8	.8578	.0996	.9168	.0608
346	212.8	.0395	.1524	.0791	.1736	386	188.8	.8518	.1285	.9109	.0787
347	208.8	.1662	.0330	.3027	.0344	387	188.8	.9208	.0285	.9553	.0169
348	208.8	.1621	.0496	.2971	.0505	388	188.8	.9126	.0616	.9507	.0364
349	208.8	.1592	.0653	.2992	.0682	571	188.8	.9184	.0283	.9574	.0163
350	208.8	.1566	.0814	.2847	.0856	572	188.8	.9203	.0097	.9600	.0054
351	208.8	.1524	.1131	.2741	.1160	573	191.8	.7752	.0174	.9600	.0054
352	208.8	.1430	.1481	.2580	.1519	574	191.8	.7683	.0396	.8726	.0092
353	204.8	.2805	.0320	.4575	.0299	575	193.8	.6833	.0188	.8203	.0126
354	204.8	.2797	.0493	.4575	.0455	576	197.8	.5209	.0117	.7018	.0092
355	204.8	.2768	.0635	.4496	.0592	577	197.8	.5195	.0317	.6955	.0243
356	204.8	.2714	.0816	.4419	.0756	578	200.8	.4110	.0170	.6008	.0142
357	204.8	.2698	.1141	.4355	.1020	579	204.8	.2810	.0176	.4571	.0162
358	204.8	.2595	.1655	.4173	.1505	580	204.8	.2705	.0483	.4458	.0433
359	200.8	.4122	.0375	.6006	.0307	581	208.8	.1676	.0171	.3039	.0186
360	200.8	.4086	.0535	.5960	.0437	582	208.8	.1569	.0667	.2841	.0697
361	200.8	.4056	.0703	.5864	.0644	583	190.8	.7971	.1572	.8774	.0992
362	200.8	.4002	.0881	.5328	.0750	1189	187.6	.98879944
363	200.8	.3935	.1234	.5741	.1000	1190	205.8	.14522469
364	200.8	.3857	.1770	.5611	.1441	1191	202.8	.2515	.7485	.3883	.6117

TABLE 8
EXPERIMENTAL DATA AT 10 ATM. (continued)

RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION		VAPOR MOL FRACTION		RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION		VAPOR MOL FRACTION	
		N2	AR	N2	AR			N2	AR	N2	AR
1192	197.8	.4502	.5498	.5035	.3965	1233	195.8	.5945	.0607	.7537	.0434
1193	193.8	.6400	.3600	.7632	.2368	1234	195.8	.5862	.1151	.7403	.0816
1194	190.8	.8015	.1985	.8780	.1220	1235	195.8	.5754	.1983	.7288	.1377
1195	188.2	.9529	.0471	.9728	.0272	1236	195.8	.5438	.3528	.6963	.2416
1196	188.0	.9657	.0343	.9800	.0200	1237	193.8	.6847	.0094	.8209	.0075
1197	187.5	.9948	.0052	.9983	.0017	1238	193.8	.6349	.3232	.7592	.2172
1198	215.6	.0000	.0488	.0000	.0654	1239	191.8	.7736	.0123	.8738	.0078
1199	215.4	.0000	.0683	.0000	.0855	1240	191.8	.7717	.0223	.8774	.0130
1200	215.3	.0000	.0723	.0000	.0894	1241	191.8	.7705	.0372	.8737	.0228
1201	213.8	.0000	.2500	.0000	.0894	1242	188.8	.9273	.0074	.9621	.0044
1202	212.3	.0000	.4866	.0000	.2866	1243	188.8	.9286	.0202	.9626	.0116
1203	211.3	.0000	.7066	.0000	.7254	1244	188.8	.9272	.0399	.9611	.0228
1204	210.6	.0000	.9671	.0000	.9681	1245	188.8	.9242	.0463	.9589	.0264
1205	212.8	.0297	.0130	.1394	.0133	1800	215.7	.0000	.0153	.0000	.0195
1206	212.8	.0623	.0232	.1305	.0288	1801	215.6	.0000	.0279	.0000	.0350
1207	212.8	.0179	.2537	.0363	.2861	1802	211.0	.0000	.7560	.0000	.7721
1208	208.8	.1617	.0251	.3009	.0268	1803	210.6	.0000	.9094	.0000	.9143
1209	208.8	.1574	.0409	.2884	.0431	1804	212.8	.0676	.0144	.1357	.0167
1210	208.8	.1281	.1969	.2357	.1981	1805	212.8	.0643	.0286	.1292	.0327
1211	208.8	.1058	.3809	.1885	.3776	1806	208.8	.1683	.0115	.3073	.0118
1212	208.8	.0793	.5783	.1416	.5635	1807	208.8	.1659	.0253	.3013	.0255
1213	208.8	.0625	.7524	.1128	.7235	1808	204.8	.2634	.1119	.4303	.1023
1214	208.8	.0508	.9123	.0935	.8744	1809	212.8	.0672	.0100	.1355	.0113
1215	204.8	.2811	.0274	.4585	.0253	1810	204.8	.1893	.6308	.3082	.5510
1216	204.8	.2745	.0671	.4475	.0615	1811	200.8	.3992	.0743	.5841	.0619
1217	204.8	.2430	.2485	.3938	.2236	1812	200.8	.3964	.0999	.5782	.0824
1218	204.8	.2100	.4539	.3420	.4003	1813	197.8	.5210	.0104	.7001	.0078
1219	204.8	.1939	.6274	.3089	.5503	1814	195.8	.5936	.0229	.7588	.0166
1220	204.8	.1813	.7375	.2979	.6362	1815	195.8	.5691	.1958	.7189	.1384
1221	202.8	.2963	.3051	.4520	.2627	1816	193.8	.6843	.0137	.8199	.0094
1222	202.8	.2644	.5489	.4063	.4562	1817	193.8	.6382	.3279	.7645	.2166
1223	202.8	.2468	.7069	.3825	.5829	1818	191.8	.7775	.0138	.8794	.0091
1224	200.8	.4077	.0109	.5980	.0089	1819	191.8	.7757	.0264	.8770	.0167
1225	200.8	.4020	.0353	.5899	.0290	1820	191.8	.7776	.0160	.8807	.0101
1226	200.8	.3433	.4331	.5013	.3432	1821	191.8	.7735	.0374	.8758	.0238
1227	200.8	.3267	.5761	.4790	.0693	1822	191.8	.7500	.1960	.8481	.1230
1228	197.8	.5163	.0263	.6931	.0198	1823	190.8	.8212	.0000	.9078	.0000
1229	197.8	.5092	.0500	.6860	.0375	1824	187.8	.9826	.0000	.9923	.0000
1230	197.8	.4729	.3089	.6337	.2275	1825	187.5	.9839	.0161	.9917	.0083
1231	197.8	.4624	.3994	.6188	.2918	1826	188.8	.9213	.0165	.9591	.0090
					.0893				.0622		.0319

TABLE 9
EXPERIMENTAL DATA AT 12 ATM.

RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION N2	LIQUID MOL FRACTION AR	LIQUID MOL FRACTION O2	VAPOR MOL FRACTION N2	VAPOR MOL FRACTION AR	VAPOR MOL FRACTION O2	TEMP. DEG.R	RUN NO.	LIQUID MOL FRACTION N2	LIQUID MOL FRACTION AR	LIQUID MOL FRACTION O2	VAPOR MOL FRACTION N2	VAPOR MOL FRACTION AR	VAPOR MOL FRACTION O2
258	216.7	.11938817	.21857815	206.8	295	.4015	.0376	.5610	.5758	.0319	.3923
259	212.8	.22477753	.36436357	206.8	296	.3987	.0571	.5442	.5739	.0479	.3783
260	208.8	.34216579	.52144786	206.8	297	.3965	.0748	.5287	.5670	.0637	.3693
261	204.8	.46025198	.64963504	206.8	298	.3926	.0923	.5151	.5615	.0776	.3609
262	200.8	.62613739	.77122288	206.8	299	.3843	.1320	.4837	.5514	.1104	.3382
263	197.8	.75242476	.85921408	206.8	300	.3749	.1866	.4365	.5374	.1558	.3068
264	195.8	.84121556	.91070893	202.8	301	.5453	.0390	.4156	.7048	.0300	.2652
265	194.8	.88481152	.93850615	202.8	302	.5406	.0583	.4011	.7017	.0447	.2536
266	221.40158	.98420197	.9803	202.8	303	.5377	.0803	.3821	.6962	.0610	.2428
267	221.10444	.95560547	.9453	202.8	304	.5363	.0987	.3650	.6894	.0756	.2350
268	220.80787	.92130963	.9037	202.8	305	.5307	.1392	.3302	.6840	.1044	.2116
269	220.51102	.88981322	.8677	202.8	306	.5204	.2120	.2677	.6701	.1584	.1715
270	194.8	.8688	.13129180	.0820	199.8	307	.6663	.0379	.2958	.7960	.0270	.1770
271	195.3	.8418	.15828998	.1002	199.8	308	.6620	.0603	.2777	.7915	.0426	.1659
272	195.8	.8135	.18658808	.1192	199.8	309	.6583	.0852	.2565	.7860	.0603	.1537
273	196.3	.7658	.21428620	.1380	199.8	310	.6560	.1063	.2377	.7825	.0755	.1419
274	218.7	.0591	.0313	.9097	.1153	.0371	.8476	199.8	311	.6476	.1456	.2068	.7748	.1013	.1240
275	218.7	.0540	.0499	.8961	.1057	.0573	.8359	199.8	312	.6382	.2193	.1425	.7603	.1534	.0863
276	218.7	.0493	.0675	.8833	.0974	.0772	.8255	198.8	313	.7024	.0614	.2362	.8193	.0423	.1385
277	218.7	.0436	.0927	.8637	.0858	.1061	.8080	198.8	314	.6954	.1093	.1953	.8098	.0749	.1154
278	193.3	.9528	.04729711	.0289	198.8	315	.6885	.1510	.1604	.8020	.1031	.0950
279	193.8	.9228	.07729524	.0476	198.8	316	.6789	.2164	.1048	.7904	.1476	.0621
280	218.7	.0411	.1223	.8365	.0783	.1393	.7825	196.8	317	.7936	.0377	.1687	.8804	.0245	.0951
281	218.7	.0307	.1684	.8009	.0584	.1913	.7504	196.8	318	.7899	.0575	.1526	.8767	.0376	.0856
282	194.3	.8981	.10199370	.0630	196.8	319	.7867	.0749	.1384	.8732	.0494	.0774
283	214.8	.1682	.0366	.8032	.2823	.0379	.6798	196.8	320	.7828	.0974	.1198	.8683	.0642	.0675
284	214.8	.1544	.0531	.7905	.2752	.0548	.6700	196.8	321	.7764	.1333	.0903	.8622	.0871	.0507
285	214.8	.1524	.0698	.7779	.2697	.0718	.6585	196.8	322	.7656	.1836	.0508	.8533	.1183	.0284
286	214.8	.1474	.0879	.7648	.2614	.0911	.6476	195.8	323	.8333	.0564	.1103	.9015	.0371	.0614
287	214.8	.1482	.1303	.7295	.2480	.1331	.6189	195.8	324	.8270	.0934	.0797	.6959	.0597	.0444
288	214.8	.1287	.1835	.6878	.2266	.1868	.5867	199.8	565	.6629	.0226	.3145	.7992	.0172	.1836
289	210.8	.2700	.0337	.6962	.4338	.0315	.5348	198.8	566	.7069	.0190	.2741	.8266	.0126	.1609
290	210.8	.2670	.0545	.6785	.4260	.0512	.5228	198.8	567	.7021	.0435	.2544	.8231	.0300	.1470
291	210.8	.2627	.0490	.6683	.4197	.0651	.5152	196.8	568	.7930	.0203	.1667	.8837	.0123	.1040
292	210.8	.2592	.0842	.6567	.4155	.0788	.5057	195.8	569	.8402	.0159	.1439	.9116	.0105	.0779
293	210.8	.2514	.1205	.6282	.4030	.1140	.4830	195.8	570	.8391	.0363	.1245	.9068	.0244	.0689
294	210.8	.2471	.1810	.5720	.3906	.1672	.4422	193.3	1135	.96610339	.97990201

TABLE 9
EXPERIMENTAL DATA AT 12 ATM. (continued)

RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION		VAPOR MOL FRACTION		RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION		VAPOR MOL FRACTION	
		N ₂	AR	N ₂	AR			N ₂	AR	N ₂	AR
1136	212.8	.1072	.8928	.1768	.8232	1174	199.8	.6227	.3280	.7438	.2269
1137	210.8	.1699	.8301	.2717	.7283	1175	198.8	.6730	.2711	.7845	.1925
1138	204.8	.3896	.6104	.5327	.4673	1176	196.8	.8044	.0061	.8876	.0052
1139	199.8	.6152	.3848	.7357	.2643	1177	196.8	.7998	.0188	.8863	.0121
1140	193.0	.9778	.0222	.9867	.0133	1178	196.8	.7973	.0340	.8832	.0224
1141	221.501980273	1179	195.8	.8308	.1209	.8961	.0774
1142	221.205540677	1180	194.3	.9237	.0075	.9592	.0047
1143	221.007260879	1181	194.3	.9223	.0184	.9575	.0116
1144	219.820942405	1182	194.3	.9233	.0224	.9575	.0153
1145	218.736704032	1183	194.3	.9182	.0370	.9538	.0227
1146	217.753775677	1184	194.3	.9158	.0484	.9512	.0293
1147	216.854395727	1185	194.3	.9138	.0667	.9474	.0424
1148	216.491599190	1186	193.3	.9684	.0069	.9835	.0045
1149	218.7	.0665	.0207	.1262	.0236	1187	193.3	.9676	.0143	.9830	.0042
1150	218.7	.0622	.0431	.1173	.0497	1188	193.3	.9662	.0233	.9798	.0139
1151	214.8	.1639	.0277	.3039	.0277	1777	221.501200131
1152	214.8	.1954	.0299	.2898	.0303	1778	221.203970488
1153	214.8	.1643	.0453	.2869	.0463	1779	221.005670694
1154	214.9	.1026	.3876	.1785	.3839	1780	216.872267403
1155	214.8	.0787	.5847	.1359	.5695	1781	216.678717999
1156	214.8	.0662	.7090	.1151	.6831	1782	216.485768639
1157	214.8	.0591	.7811	.1004	.7566	1783	218.7	.0642	.0106	.1236	.0124
1158	214.8	.0511	.8776	.0899	.8448	1784	214.8	.1618	.0253	.2838	.0266
1159	210.8	.2265	.3393	.3554	.3098	1785	214.8	.1603	.0324	.2810	.0340
1160	210.8	.2143	.4317	.3343	.3865	1786	214.8	.1643	.0120	.2881	.0127
1161	210.8	.1940	.5738	.3060	.5081	1787	212.8	.22093698
1162	210.8	.1817	.7027	.2865	.6189	1788	206.8	.4024	.0148	.5787	.0123
1163	210.8	.1740	.7958	.2772	.6975	1789	199.8	.6618	.0243	.7957	.0169
1164	206.8	.4075	.0117	.5854	.0106	1790	199.8	.6602	.0347	.7929	.0242
1165	206.8	.4035	.0375	.5755	.0317	1791	198.8	.7052	.0229	.8259	.0158
1166	206.8	.3570	.3151	.5096	.2589	1792	196.8	.7948	.0138	.8834	.0089
1167	206.8	.3414	.4626	.4836	.3747	1793	195.8	.8356	.0433	.9052	.0274
1168	206.8	.3203	.6032	.4598	.4848	1794	194.3	.9068	.0289	.9482	.0182
1169	202.8	.4970	.3674	.6387	.2724	1795	194.3	.91029522
1170	202.8	.4835	.4568	.6250	.3366	1796	193.3	.95829774
1171	199.8	.6670	.0111	.8015	.0077	1797	193.3	.9564	.0082	.9770	.0048
1172	199.8	.6635	.0238	.7982	.0160	1798	193.3	.9555	.0249	.9743	.0152
1173	199.8	.6642	.0298	.8016	.0183	1799	193.0	.9679	.0321	.9807	.0193

TABLE 10
EXPERIMENTAL DATA AT 14 ATM.

RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION		VAPOR MOL FRACTION		RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION		VAPOR MOL FRACTION		
		N ₂	AR	N ₂	O ₂			N ₂	AR	O ₂	N ₂	AR
194	223.7	.0603	.0307	.1308	.0692	235	204.8	.6525	.0682	.7761	.0507	.1732
195	219.7	.1716	.0254	.2923	.7077	236	204.8	.6475	.0943	.7713	.0593	.1594
196	216.7	.2586	.7414	.4055	.5945	237	204.8	.6426	.1179	.7658	.0951	.1494
197	211.8	.4055	.5945	.5725	.4275	238	204.8	.6425	.1406	.7627	.1023	.1350
198	207.8	.5506	.4404	.7035	.2965	239	204.8	.6299	.2082	.7520	.1479	.1001
199	203.8	.7025	.2975	.8198	.1802	240	202.8	.7392	.0403	.8419	.0282	.1299
200	200.8	.8272	.1726	.9017	.0993	241	202.8	.7351	.0671	.8303	.0470	.1227
201	198.8	.9149	.0851	.9537	.0463	242	202.8	.7270	.0857	.8275	.0595	.1130
202	226.5	.0215	.9785	.0263	.9737	243	202.8	.7254	.1035	.8249	.0723	.1028
203	226.2	.0452	.9546	.0523	.9447	244	202.8	.7159	.1462	.8168	.1021	.0811
204	225.9	.0620	.9150	.0983	.9017	245	202.8	.7075	.1964	.8081	.1344	.0575
205	225.6	.0902	.8096	.1268	.8732	246	201.8	.7721	.0651	.8594	.0452	.0954
206	197.8	.0412	.0682	.9740	.0260	247	201.8	.7655	.1066	.8544	.0722	.0734
207	198.3	.9318	.0682	.9565	.0435	248	201.8	.7601	.1554	.8463	.1044	.0493
208	198.8	.8998	.0682	.9355	.0645	249	201.8	.7486	.2039	.8374	.1351	.0275
209	199.3	.6757	.1243	.9204	.0796	250	199.8	.8650	.0439	.9204	.0285	.0510
210	224.7	.0422	.9410	.0821	.8981	251	199.8	.8602	.0713	.9145	.0475	.0380
211	224.7	.0391	.9341	.0766	.8915	252	199.8	.8564	.0962	.9088	.0623	.0288
212	224.7	.0357	.9384	.0697	.8851	253	199.8	.8533	.1146	.9069	.0750	.0181
213	224.7	.0329	.9514	.0641	.8756	254	199.8	.8510	.1292	.9057	.0833	.0111
214	224.7	.0273	.9769	.0533	.8570	255	199.8	.8693	.0251	.9251	.0164	.0586
215	224.7	.0173	.1209	.0353	.1342	256	198.8	.9114	.0510	.9442	.0332	.0226
216	219.7	.1672	.0197	.2854	.0197	257	198.8	.9042	.0772	.9410	.0485	.0105
217	219.7	.1644	.0306	.2826	.0321	556	225.5	.0000	.1190	.0000	.1407	.8593
218	219.7	.1613	.0473	.2735	.0493	559	203.8	.7041	.0000	.8108	.0000	.1812
219	219.7	.1599	.0607	.2706	.0633	560	202.8	.7365	.0639	.8345	.0458	.1197
220	219.7	.1509	.0976	.2562	.0832	561	201.8	.7773	.0623	.8631	.0418	.0951
221	214.8	.1420	.1531	.2400	.1580	562	199.8	.8712	.0405	.9234	.0269	.0497
222	214.8	.3098	.0239	.4611	.4019	628	200.8	.8098	.0000	.8897	.0000	.1103
223	214.8	.3194	.0369	.4511	.5171	1064	197.8	.8093	.0000	.8835	.0000	.0165
224	214.8	.3080	.0490	.4595	.5043	1065	217.7	.9693	.0000	.9835	.0000	.0000
225	214.8	.3031	.0671	.4499	.5009	1065	217.7	.1041	.8959	.1713	.8287	.0000
226	214.8	.2906	.1150	.4355	.4977	1066	214.8	.2014	.7986	.3079	.6921	.0000
227	214.8	.2779	.1691	.4355	.4908	1067	209.8	.3866	.6134	.5224	.4776	.0000
228	209.8	.4715	.0242	.4172	.4282	1068	204.8	.6032	.3968	.7230	.2770	.0000
229	209.8	.4641	.0440	.6339	.3460	1069	201.8	.7552	.2448	.8367	.1533	.0000
230	209.8	.4626	.4562	.6263	.3373	1070	198.0	.9577	.0423	.9749	.0251	.0000
231	209.8	.4579	.4354	.6201	.3129	1071	197.7	.9752	.0248	.9846	.0154	.0000
232	209.8	.4482	.4354	.6114	.3012	1072	197.5	.9842	.0158	.9909	.0091	.0000
233	209.6	.4362	.3366	.6000	.2792	1073	197.4	.9890	.0110	.9939	.0061	.0000
234	204.8	.6558	.3012	.5954	.2341	1074	226.6	.0000	.0138	.0000	.0182	.9818
				.7805	.1879	1075	226.4	.0000	.0382	.0000	.0480	.9520

TABLE 10
EXPERIMENTAL DATA AT 14 ATM. (continued)

RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION		VAPOR MOL FRACTION		RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION		VAPOR MOL FRACTION	
		N2	AR	N2	AR			N2	AR	N2	AR
1076	226.30499	.9501	1117	207.8	.4931	.3793	.6267	.2969
1077	225.51330	.8670	1118	207.8	.4829	.4651	.6148	.3496
1078	224.72356	.7644	1119	204.8	.6684	.0111	.7917	.0081
1079	223.24624	.5376	1120	204.8	.6659	.0233	.7915	.0159
1080	222.26800	.3200	1121	204.8	.6633	.0393	.7860	.0290
1081	221.68804	.1196	1122	204.8	.6208	.3073	.7355	.2187
1082	221.49653	.0347	1123	201.8	.7926	.0119	.8749	.0079
1083	224.70449	.9551	1124	201.8	.7934	.0227	.8774	.0151
1084	219.7	.1703	.0209	.9791	.0258	1125	201.8	.7896	.0380	.8731	.0255
1085	219.7	.1594	.0730	.9270	.2684	1126	201.8	.7875	.0525	.8711	.0352
1086	219.7	.1529	.0997	.9003	.2578	1127	201.8	.7866	.0619	.8706	.0417
1087	219.7	.1295	.2491	.7505	.2171	1128	198.8	.9592	.0076	.9609	.0041
1088	219.7	.0967	.4596	.5433	.1599	1129	198.8	.9260	.0207	.9588	.0124
1089	219.7	.0746	.6313	.3687	.1253	1130	198.8	.9232	.0262	.9591	.0156
1090	219.7	.0608	.7751	.2249	.1036	1131	198.8	.9266	.0389	.9538	.0248
1091	219.7	.0559	.8547	.1453	.0946	1132	197.8	.9766	.0062	.9860	.0032
1092	217.7	.2291	.0198	.9802	.3568	1133	197.8	.9725	.0139	.9840	.0082
1093	217.7	.2127	.0979	.9021	.3393	1134	197.8	.9664	.0255	.9793	.0161
1094	217.7	.1870	.2463	.7537	.2961	1755	226.205040409
1095	217.7	.1563	.4359	.5641	.2489	1756	221.493189322
1096	217.7	.1283	.6746	.3257	.2054	1757	224.7	.0189	.1225	.0349	.1412
1097	217.7	.1093	.8810	.1190	.1783	1758	219.7	.1664	.0085	.2818	.0090
1098	214.8	.3146	.0175	.9825	.4743	1759	219.7	.1440	.0181	.2791	.0194
1099	214.8	.3063	.0530	.9467	.4616	1760	214.8	.2580	.0492	.4512	.0442
1100	214.8	.3011	.0898	.9102	.4507	1761	211.8	.3986	.0477	.5545	.0408
1101	214.8	.2699	.2737	.7263	.4014	1762	204.8	.6563	.0237	.7830	.0173
1102	214.8	.2469	.4283	.5731	.3567	1763	201.8	.7464	.2536	.8291	.1709
1103	214.8	.2187	.6567	.3433	.3301	1764	199.8	.8590	.1034	.9115	.0669
1104	214.8	.2135	.7334	.2666	.3217	1765	198.8	.9192	.0089	.9535	.0057
1105	211.8	.4064	.0473	.9527	.5681	1766	198.8	.9171	.0231	.9516	.0149
1106	211.8	.3939	.1114	.8886	.5473	1767	198.8	.9162	.0303	.9501	.0193
1107	211.8	.3854	.1701	.8296	.5351	1768	198.8	.9156	.0445	.9494	.0285
1108	211.8	.3462	.4446	.6554	.4779	1769	198.8	.9117	.0549	.9469	.0346
1109	211.8	.3242	.5921	.4079	.4557	1770	197.8	.9673	.0077	.9814	.0047
1110	209.8	.4608	.0130	.9870	.6410	1771	197.8	.9659	.0158	.9804	.0097
1111	209.8	.4750	.0313	.9687	.6353	1772	197.8	.9650	.0248	.9791	.0154
1112	209.8	.4696	.0614	.9386	.6265	1773	198.0	.9507	.0493	.9684	.0316
1113	209.8	.4297	.3123	.6873	.5723	1774	198.7	.9662	.0338	.9786	.0214
1114	209.8	.4002	.5358	.4000	.5374	1775	197.5	.9791	.0209	.9870	.0130
1115	207.8	.5382	.0951	.4628	.5374	1776	197.4	.9851	.0149	.9912	.0088
1116	207.8	.5180	.2138	.4820	.6582	1868	197.7	.9632	.0368	.9766	.0232

TABLE 11
EXPERIMENTAL DATA AT 16 ATM.

RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION		VAPOR MOL FRACTION		RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION		VAPOR MOL FRACTION	
		N2	AR	N2	AR			N2	AR	N2	AR
130	227.7	.06709130	.8535	171	209.8	.6352	.0328	.3320	.7615
131	224.7	.15898412	.7431	172	209.8	.6290	.0500	.3209	.7574
132	220.7	.27417259	.5909	173	209.8	.6275	.0777	.2948	.7489
133	216.7	.39816019	.4644	174	209.8	.6233	.1166	.2601	.7434
134	211.8	.54444556	.2958	175	209.8	.6075	.1773	.2152	.7287
135	207.8	.71742826	.1755	176	206.8	.7593	.0206	.2201	.8455
136	204.8	.85011499	.0946	177	206.8	.7542	.0345	.2113	.8412
137	202.8	.92920708	.0392	178	206.8	.7515	.0565	.1920	.8368
138	231.20125	.9875	.9841	179	206.8	.7487	.0750	.1763	.8339
139	230.90412	.9588	.9500	180	206.8	.7435	.1114	.1452	.8291
140	230.60744	.9256	.9064	181	206.8	.7277	.1631	.1092	.8179
141	230.31043	.8957	.8793	182	205.8	.7915	.0433	.1652	.8705
142	201.8	.9725	.02729824	183	205.8	.7845	.0653	.1503	.8665
143	202.3	.9424	.05769633	184	205.8	.7823	.0952	.1225	.8575
144	202.8	.9153	.08479451	185	205.8	.7680	.1576	.0743	.8469
145	203.3	.8658	.11429252	186	203.8	.8830	.0232	.0938	.9309
146	229.7	.8308	.0123	.9570	.0141	187	203.8	.8764	.0395	.0840	.9263
147	229.7	.0315	.0238	.9448	.0569	188	203.8	.8731	.0581	.0688	.9208
148	229.7	.0262	.0343	.9395	.0490	189	203.8	.8735	.0616	.0649	.9161
149	229.7	.0271	.0407	.9322	.0463	190	203.8	.8648	.1166	.0186	.9143
150	229.7	.0232	.0678	.9090	.0435	191	203.8	.8643	.1232	.0125	.9125
151	229.7	.0124	.1249	.8626	.0214	192	202.8	.9208	.0400	.0393	.9525
152	224.7	.1604	.0156	.8240	.2664	193	202.8	.9183	.0637	.0180	.9460
153	224.7	.1576	.0289	.8135	.2617	547	220.7	.27287272	.4132
154	224.7	.1560	.0367	.8073	.2572	548	216.7	.39436057	.5491
155	224.7	.1525	.0467	.8008	.2517	549	212.8	.50404960	.6542
156	224.7	.1452	.0790	.7758	.2421	550	204.8	.84481552	.9070
157	224.7	.1337	.1375	.7286	.2214	551	202.8	.93220678	.9604
158	219.7	.3048	.0178	.6774	.4422	552	225.7	.1413	.0100	.8487	.2250
159	219.7	.3914	.0304	.6893	.4390	553	224.7	.1587	.0121	.8292	.2653
160	219.7	.2974	.0478	.6549	.4330	554	219.7	.3030	.0142	.6827	.4469
161	219.7	.2941	.0557	.6502	.4293	555	209.8	.6306	.0622	.3072	.7612
162	219.7	.2651	.1130	.6019	.4135	556	206.8	.7391	.1599	.1010	.8236
163	219.7	.2747	.1553	.5681	.3994	1000	201.8	.98080192	.9897
164	214.8	.4557	.0215	.5226	.6083	1001	221.7	.1232	.87681940
165	214.8	.4576	.0316	.5147	.6049	1002	218.7	.2239	.77613309
166	214.8	.4524	.0458	.5016	.6026	1003	214.8	.3707	.62934960
167	214.8	.4507	.0607	.4886	.5995	1004	209.8	.5809	.41916905
168	214.8	.4419	.1003	.4576	.5880	1005	204.8	.8179	.18218765
169	214.8	.4278	.1684	.4039	.5718	1006	201.5	.9368	.06329592
170	209.8	.6389	.0194	.3417	.7644	1007	202.0	.9650	.03509774

TABLE 11
EXPERIMENTAL DATA AT 16 ATM. (continued)

RUN NO.	TEMP. DEG. F	LIQUID MOL FRACTION N ₂	LIQUID MOL FRACTION O ₂	VAPOR MOL FRACTION N ₂	VAPOR MOL FRACTION O ₂	RUN NO.	TEMP. DEG. F	LIQUID MOL FRACTION N ₂	LIQUID MOL FRACTION O ₂	VAPOR MOL FRACTION N ₂	VAPOR MOL FRACTION O ₂
1004	201.6	.9852	.0148	.9910	.0090	1049	211.8	.5058	.4295	.6296	.3262
1009	226.0	.9302	.0698	.9323	.0677	1050	209.8	.6467	.0124	.7697	.0093
1010	226.3	.805A	.1942	.8147	.1853	1051	209.8	.6392	.0502	.7615	.0375
1011	226.7	.6902	.3098	.7078	.2922	1052	209.8	.6166	.1911	.7328	.1423
1012	227.2	.4736	.5264	.5026	.4974	1053	209.8	.6016	.2864	.7158	.2112
1013	229.2	.2391	.7609	.2686	.7314	1054	206.8	.7649	.0096	.8550	.0061
1014	230.8	.0573	.9427	.0690	.9310	1055	206.8	.7601	.0411	.8470	.0299
1015	231.0	.0407	.9593	.0478	.9522	1056	206.8	.7413	.1920	.8256	.1327
1016	231.1	.0348	.9657	.0410	.9590	1057	205.8	.7774	.1904	.8546	.1273
1017	224.7	.1558	.8065	.0393	.7046	1058	203.8	.8889	.0170	.9358	.0094
1018	224.7	.1049	.8110	.1795	.5378	1059	203.8	.8900	.0298	.9318	.0200
1019	224.7	.0819	.8680	.1437	.4151	1060	203.8	.8777	.0904	.9213	.0602
1020	224.7	.0603	.8719	.1135	.3336	1061	202.8	.9316	.0405	.9569	.0256
1021	224.7	.0510	.8744	.0856	.1955	1062	201.8	.9795	.0060	.9884	.0038
1022	224.7	.0390	.8894	.0662	.0830	1063	201.8	.9808	.0112	.9897	.0063
1023	224.7	.0346	.8964	.0599	.0920	1733	231.3	.9932	.0068	.9932	.0095
1024	221.7	.2285	.7741	.3569	.0711	1734	231.2	.9814	.0186	.9761	.0239
1025	221.7	.2152	.8376	.3339	.1427	1735	230.6	.9227	.0773	.9227	.0910
1026	221.7	.2006	.8036	.3241	.1790	1736	229.7	.0278	.0443	.0513	.0515
1027	221.7	.1475	.8015	.2274	.1713	1737	228.7	.9899	.3101	.6899	.3408
1028	221.7	.1319	.8498	.2048	.0432	1738	225.7	.8487	.0166	.2273	.0178
1029	219.7	.3018	.6760	.4465	.0208	1739	224.7	.1652	.9341	.2694	.7306
1030	219.7	.2887	.6164	.4248	.0881	1740	224.7	.1373	.1341	.2246	.1385
1031	219.7	.2589	.4909	.3819	.2277	1741	224.7	.1217	.2173	.2011	.2197
1032	219.7	.2390	.3682	.3513	.2934	1742	224.7	.0832	.4512	.1312	.4478
1033	219.7	.2229	.2787	.3293	.2269	1743	224.7	.0352	.9595	.0684	.9240
1034	219.7	.2091	.1834	.3114	.1500	1744	214.8	.4561	.0144	.6076	.0117
1035	219.7	.1863	.0492	.2854	.0406	1745	212.8	.5290	.9932	.6740	.3260
1036	216.7	.3752	.5480	.5273	.4070	1746	209.8	.6243	.0775	.7470	.0581
1037	216.7	.3644	.5034	.5133	.3731	1747	206.8	.7357	.1429	.8232	.1009
1038	216.7	.3417	.3192	.4709	.2401	1748	206.8	.7589	.0066	.8468	.0056
1039	216.7	.3140	.1311	.4341	.1009	1749	205.8	.7707	.1967	.8438	.1365
1040	216.7	.3005	.0414	.4192	.0317	1750	203.8	.8788	.0661	.9224	.0440
1041	214.8	.4632	.5254	.6153	.0091	1751	203.8	.8864	.0164	.9311	.0109
1042	214.8	.4447	.4599	.5944	.0759	1752	202.8	.9247	.0434	.9525	.0286
1043	214.8	.4259	.3407	.5624	.3297	1753	201.8	.9741	.0155	.9841	.0098
1044	214.8	.4061	.2256	.5384	.1628	1754	226.6	.9887	.0113	.9887	.0141
1045	214.8	.3783	.0464	.5055	.4607	1860	231.3	.9918	.0082	.9918	.0103
1046	211.8	.5556	.0665	.6920	.2401	1861	224.7	.1455	.0833	.2387	.0860
1047	211.8	.5306	.2475	.6596	.1895	1862	224.7	.0354	.9548	.0590	.9327
1048	211.8	.5174	.3409	.6422	.2611	1866	206.8	.7591	.0164	.8481	.0117

TABLE 12
EXPERIMENTAL DATA AT 18 ATM.

RUN NO.	TEMP. DEGR.	LIQUID MOL FRACTION		VAPOR MOL FRACTION		RUN NO.	TEMP. DEGR.	LIQUID MOL FRACTION		VAPOR MOL FRACTION		
		N ₂	AP	N ₂	O ₂			N ₂	AR	N ₂	AR	N ₂
56	231.8	.08739127	.8573	109	214.8	.5674	.1665	.6829	.1306	.1865
57	227.8	.19598041	.6957	110	209.8	.7935	.0189	.8716	.0114	.1171
58	224.7	.27847216	.5832	111	209.8	.7874	.0341	.8696	.0211	.1093
59	220.7	.40235977	.4600	112	209.8	.7851	.0539	.8624	.0368	.1007
70	216.7	.53204680	.3345	113	209.8	.7810	.0733	.8597	.0494	.0909
71	211.8	.71202880	.1824	114	209.8	.7754	.1114	.8560	.0777	.0663
72	208.8	.84511549	.1034	115	209.8	.7623	.1844	.8399	.1269	.0332
73	206.8	.92830717	.0424	116	207.8	.8780	.0177	.9257	.0102	.0640
74	235.20372	.9628	.9565	117	207.8	.8736	.0310	.9249	.0186	.0566
75	234.90682	.9318	.9195	118	207.8	.8745	.0486	.9230	.0310	.0460
76	234.61035	.8965	119	207.8	.8670	.0662	.9195	.0421	.0384
77	234.31340	.8660	.8447	120	207.8	.8598	.0905	.9137	.0598	.0264
78	205.3	.9886	.0114	121	207.8	.8587	.1217	.9048	.0818	.0134
79	205.8	.9603	.0397	122	206.8	.9213	.0305	.9456	.0302	.0242
80	206.3	.9341	.0659	123	206.8	.9143	.0471	.9451	.0393	.0155
81	206.8	.9040	.09600652	124	206.8	.9159	.0603	.9404	.0522	.0074
82	233.7	.0345	.0240	.9414	.0291	125	205.8	.9067	.0811	.9782	.0101	.0116
83	233.7	.0292	.0475	.9233	.8937	126	205.8	.9671	.0127	.9824	.0029	.0147
84	233.7	.0238	.0621	.9141	.8838	127	205.8	.9696	.0045	.9824	.0029	.0147
85	233.7	.0172	.1076	.8752	.8459	128	205.8	.9670	.0136	.9787	.0101	.0112
86	229.7	.1411	.0168	.8431	.7548	129	205.8	.9617	.0323	.9755	.0215	.0030
87	229.7	.1303	.0221	.8476	.7554	534	231.8	.085215128488
88	229.7	.1350	.0356	.8294	.7437	535	224.7	.276540965904
89	229.7	.1307	.0455	.8238	.7404	536	211.8	.727082221778
90	229.7	.1182	.0729	.8089	.7250	537	208.8	.842690890911
91	229.7	.1105	.1193	.7702	.6907	538	235.203840468	.9532
92	224.7	.2754	.0153	.7093	.5786	539	229.7	.1440	.0111	.2325	.0119	.7556
93	224.7	.2656	.0246	.7098	.5817	540	224.7	.2770	.0271	.4075	.0263	.5662
94	224.7	.2718	.0350	.6932	.5731	541	224.7	.2742	.0400	.4040	.0385	.5575
95	224.7	.2599	.0484	.6917	.5638	542	219.7	.4326	.0183	.5750	.0158	.4092
96	224.7	.2626	.0940	.6434	.5279	543	219.7	.4285	.0424	.5649	.0361	.3990
97	224.7	.2479	.1393	.6128	.4991	544	214.8	.6028	.0431	.7258	.0346	.2396
98	219.7	.4205	.0182	.5613	.4295	545	207.8	.8698	.0333	.9242	.0228	.0530
99	219.7	.4316	.0268	.5416	.4239	546	214.8	.5873	.1498	.6982	.1183	.1831
100	219.7	.4276	.0430	.5294	.4075	563	209.8	.7885	.0968	.8580	.0692	.0728
101	219.7	.4218	.0557	.5225	.4080	564	205.8	.9719	.0233	.9796	.0170	.0034
102	219.7	.4218	.0899	.4883	.3755	936	205.8	.971098220178
103	219.7	.4038	.1551	.4411	.3478	937	224.7	.1669	.8331	.2503	.7497
104	214.8	.5917	.0180	.3902	.2628	938	221.7	.2698	.7302	.3778	.6222
105	214.8	.5882	.0269	.3849	.2596	939	216.7	.4584	.5416	.5761	.4239
106	214.8	.5906	.0423	.3670	.2503	940	209.8	.7692	.2308	.8388	.1612
107	214.8	.5806	.0601	.3593	.2423	941	207.8	.8705	.1295	.9116	.0884
108	214.8	.5797	.0974	.3229	.2168	942	206.0	.9587	.0413	.9725	.0275

TABLE 12
EXPERIMENTAL DATA AT 18 ATM. (continued)

RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION N2	LIQUID MOL FRACTION AR	VAPOR MOL FRACTION N2	VAPOR MOL FRACTION AR	RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION N2	LIQUID MOL FRACTION AR	VAPOR MOL FRACTION N2	VAPOR MOL FRACTION AR
943	205.6	.9748	.0252	.9825	.0175	986	214.8	.6009	.0127	.7312	.0094
944	205.5	.9797	.0203	.9863	.0137	987	214.8	.5568	.3236	.6686	.2490
945	235.4	988	212.8	.6834	.0119	.7895	.0094
946	235.398199771	989	212.8	.6763	.0542	.7805	.0405
947	235.097359694	990	212.8	.6678	.0966	.7716	.0720
948	233.794429340	991	212.8	.6553	.1892	.7544	.1433
949	232.497619709	992	212.8	.6420	.2815	.7408	.2083
950	231.461085826	993	209.8	.8003	.0124	.8727	.0091
951	230.542304001	994	209.8	.7974	.0425	.8677	.0305
952	230.318111732	995	209.8	.7730	.1992	.8411	.1416
953	229.709360903	996	207.8	.8863	.0106	.9304	.0073
954	229.782417395	997	207.8	.8817	.0404	.9258	.0266
955	229.769916279	998	206.8	.9308	.0057	.9583	.0034
956	229.759015318	999	206.8	.9278	.0160	.9569	.0098
957	229.745834172	1707	235.501000121
958	229.732603013	1708	235.402120247
959	226.780206378	1709	230.392069216
960	226.771046038	1710	233.701600186
961	226.760625222	1711	229.790548974
962	226.751464395	1712	226.790068398
963	226.726542321	1713	226.723812287
964	226.726542321	1714	224.706000566
965	224.709550852	1715	219.703000256
966	224.785318006	1716	219.707630653
967	224.704420416	1717	219.720021708
968	224.768285575	1718	214.803760302
969	224.764635272	1719	214.859865278
970	224.754474490	1720	214.859555264
971	224.740813375	1721	216.760206404
972	221.728272378	1722	212.850995099
973	221.710790922	1723	209.813421093
974	221.703430303	1724	209.838022945
975	221.754874261	1725	208.802010138
976	219.754873621	1726	207.802010138
977	219.746513621	1727	207.803230235
978	219.738192985	1728	207.8
979	219.714751177	1729	207.8
980	219.714751177	1730	206.8
981	216.704480359	1731	206.8
982	216.755414128	1732	205.8
983	216.736532759	1733	219.7
984	216.726802012	1863	219.7
985	216.706170491	1864	214.8
	44253120	1867	205.8
	02600213		
	09220749		
	14021082		
	27322184		
	41883326		
	10910794		
	42513120		
	38862727		
	36672499		
	23651684		
	10910794		
	41883326		
	10910794		
	42513120		
	38862727		
	36672499		
	23651684		
	10910794		
	41883326		
	10910794		
	42513120		
	38862727		
	36672499		
	23651684		
	10910794		
	41883326		
	10910794		
	42513120		
	38862727		
	36672499		
	23651684		
	10910794		
	41883326		
	10910794		
	42513120		
	38862727		
	36672499		
	23651684		
	10910794		
	41883326		
	10910794		
	42513120		
	38862727		
	36672499		
	23651684		
	10910794		
	41883326		
	10910794		
	42513120		
	38862727		
	36672499		
	23651684		
	10910794		
	41883326		
	10910794		
	42513120		
	38862727		
	36672499		
	23651684		
	10910794		
	41883326		
	10910794		
	42513120		
	38862727		
	36672499		
	23651684		
	10910794		
	41883326		
	10910794		
	42513120		
	38862727		
	36672499		
	23651684		
	10910794		
	41883326		
	10910794		
	42513120		
	38862727		
	36672499		
	23651684		
	10910794		
	41883326		
	10910794		
	42513120		
	38862727		
	36672499		
	23651684		
	10910794		
	41883326		
	10910794		
	42513120		
	38862727		
	36672499		
	23651684		
	10910794		
	41883326		
	10910794		
	42513120		
	38862727		
	36672499		
	23651684		
	10910794		</			

TABLE 13
EXPERIMENTAL DATA AT 20 ATM.

RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION N2	LIQUID MOL FRACTION AP	LIQUID MOL FRACTION O2	VAPOR MOL FRACTION N2	VAPOR MOL FRACTION AR	VAPOR MOL FRACTION O2	TEMP. DEG.R	RUN NO.	LIQUID MOL FRACTION N2	LIQUID MOL FRACTION AR	LIQUID MOL FRACTION O2	VAPOR MOL FRACTION N2	VAPOR MOL FRACTION AR	VAPOR MOL FRACTION O2
1	232.5	.17498251	.27247276	214.8	42	.7389	.0444	.2167	.8230	.0321	.1449
2	223.7	.42325768	.56334367	214.8	43	.7353	.0647	.2000	.8226	.0481	.1293
3	214.1	.77152285	.85041496	214.8	44	.7315	.0763	.1923	.8149	.0581	.1270
4	211.0	.89871013	.93680622	214.8	45	.7234	.1231	.1535	.8048	.0943	.1009
5	235.6	.09409060	.15538447	214.8	46	.7184	.1789	.1027	.7964	.1362	.0674
6	227.6	.31446856	.43315659	212.8	47	.8161	.0644	.1195	.8814	.0457	.0729
7	221.7	.48035197	.61643836	212.8	48	.8123	.0449	.1429	.8766	.0319	.0915
8	212.8	.82221778	.89111189	212.8	49	.8177	.0171	.1652	.8848	.0114	.1038
9	239.50980	.99200102	.9898	212.8	51	.8115	.0711	.1174	.8873	.0504	.0772
10	235.40161	.98390197	.9803	212.8	52	.8023	.1073	.0904	.8646	.0769	.0585
11	239.20449	.95510519	.9491	212.8	53	.7960	.1451	.0590	.8646	.0549	.0585
12	238.90581	.94190633	.9367	211.8	54	.8608	.0253	.1139	.8592	.1037	.0371
13	208.800870057	211.8	55	.8552	.0539	.0909	.9109	.0171	.0720
14	209.303720266	211.8	56	.8492	.0942	.0566	.8777	.0373	.0569
15	209.806340443	211.8	57	.8466	.1243	.0290	.8977	.0659	.0364
16	210.309040644	210.8	58	.9045	.0103	.0852	.8870	.0941	.0189
17	234.70211	.87220222	.7977	210.8	59	.9012	.0237	.0751	.9409	.0064	.0527
18	234.70307	.86490341	.7921	210.8	60	.8979	.0380	.0641	.9361	.0171	.0468
19	234.70341	.85750373	.7901	210.8	61	.8988	.0448	.0564	.9343	.0262	.0395
20	234.70594	.83730646	.7674	210.8	62	.8989	.0575	.0437	.9339	.0281	.0381
21	234.70102	.87270113	.8022	210.8	63	.8947	.0901	.0153	.9318	.0401	.0281
22	234.70175	.86620187	.7982	209.8	64	.8943	.0254	.0307	.9264	.0639	.0098
23	229.70090	.73150095	.6154	209.8	65	.9445	.0453	.0102	.9657	.0160	.0183
24	229.70151	.71920152	.6094	209.8	65	.9445	.0453	.0102	.9657	.0160	.0183
25	229.70231	.72540231	.6080	214.1	517	.78040102	.9428	.0308	.0064
26	229.70326	.71920324	.6056	221.7	518	.49812196	.8555	.0308	.0064
27	229.70476	.70660471	.5825	217.7	519	.49815019	.8555	.0308	.0064
28	229.71037	.66261003	.5494	217.7	519	.63943606	.6319	.0308	.0064
29	224.70247	.58600212	.4576	209.8	520	.63943606	.7486	.0308	.0064
30	224.70370	.58060324	.4492	212.8	521	.94670152	.9635	.0308	.0064
31	224.70581	.56860508	.4397	214.8	522	.82161007	.8795	.0308	.0064
32	224.70863	.54260767	.4215	219.7	523	.74271769	.8194	.0308	.0064
33	224.71326	.50291164	.3862	219.7	524	.56864132	.6902	.0308	.0064
34	224.72330	.41952052	.3271	234.7	525	.25217364	.3689	.0308	.0064
35	219.70371	.41430291	.2891	229.7	526	.11948571	.1881	.0308	.0064
36	219.70371	.41040269	.2894	234.7	527	.11448766	.1881	.0308	.0064
37	219.70589	.39440462	.2978	229.7	527	.24407444	.3330	.0308	.0064
38	219.70990	.37660812	.2702	229.7	528	.24466895	.3466	.0308	.0064
39	219.71530	.33381246	.2318	219.7	529	.56113714	.3466	.0308	.0064
40	219.72283	.26751809	.1944	210.8	530	.90910486	.6859	.0308	.0064
41	214.80255	.23340189	.1537	227.6	531	.84990288	.9007	.0308	.0064
		212.8	532	.31536847	.4583	.0308	.0064
		212.8	533	.82101790	.8952	.0308	.0064
		212.8	557	.82621162	.8867	.0308	.0064

TABLE 13
EXPERIMENTAL DATA AT 20 ATM. (continued)

RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION		VAPOR MOL FRACTION		RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION		VAPOR MOL FRACTION	
		N ₂	AR	N ₂	AR			N ₂	AR	N ₂	AR
834	208.7	.9951	.0049	.0035	.0035	876	221.7	.4510	.2474	.5695	.2058
835	209.0	.9792	.0208	.0144	.0144	877	221.7	.4420	.3213	.5593	.2652
836	209.4	.9599	.0401	.0275	.0275	878	221.7	.4154	.4958	.5281	.4042
837	212.8	.7936	.2064	.1487	.1487	879	219.7	.5591	.0132	.6831	.0107
838	217.7	.5707	.4293	.3297	.3297	880	219.7	.5575	.0472	.6776	.0380
839	229.7	.1290	.8710	.8079	.8079	881	219.7	.5508	.0786	.6689	.0636
840	231.7	.0671	.9329	.8968	.8968	882	219.7	.5029	.3786	.6113	.3010
841	209.3	.2697	.7303	.6370	.6370	883	217.7	.6227	.0770	.7294	.0606
842	219.7	.5615	.4385	.3126	.3126	884	217.7	.6126	.1353	.7181	.1064
843	239.2	.9371	.0629	.0288	.0288	885	217.7	.5891	.2892	.6894	.2247
844	238.8	.9371	.0629	.0727	.0727	886	214.8	.7420	.0138	.8307	.0108
845	238.5	.9068	.0932	.1074	.1074	887	214.8	.7443	.0301	.8274	.0223
846	237.9	.8395	.1605	.1807	.1807	888	214.8	.7409	.0591	.8201	.0443
847	236.6	.6637	.3363	.3630	.3630	889	214.8	.7059	.2679	.7848	.1965
848	235.6	.4975	.5025	.5267	.5267	890	209.3	.9674	.0134	.9813	.0093
849	234.7	.2873	.7127	.7243	.7243	891	209.3	.9673	.0211	.9785	.0141
850	234.3	.1599	.8401	.8450	.8450	892	209.3	.9634	.0305	.9751	.0205
851	234.7	.7928	.1164	.1243	.1243	1684	238.9	.0807	.0626	.1329	.0376
852	234.7	.6154	.3344	.3489	.3489	1685	234.7	.0807	.1706	.1329	.1798
853	234.7	.5134	.4557	.4704	.4704	1686	234.7	.0038	.6748	.0065	.7040
854	234.7	.4268	.5585	.5752	.5752	1687	231.7	.1680	.1451	.2531	.1455
855	234.7	.3022	.6968	.7098	.7098	1688	231.7	.0785	.8097	.1221	.7783
856	231.7	.6885	.1482	.1501	.1501	1689	229.7	.2489	.0138	.3670	.0139
857	231.7	.4828	.3945	.3858	.3858	1690	229.7	.2389	.0651	.3494	.0540
858	231.7	.2904	.6179	.5982	.5982	1691	229.7	.2357	.0790	.3447	.0767
859	231.7	.0682	.8408	.8086	.8086	1692	229.7	.2295	.1105	.3365	.1071
860	231.7	.3752	.8533	.8193	.8193	1693	227.7	.2959	.0610	.4200	.0576
861	229.7	.5320	.2720	.2610	.2610	1694	227.6	.3111	.0000	.4378	.0000
862	229.7	.4023	.4257	.4022	.4022	1695	224.7	.2954	.7046	.4018	.5982
863	229.7	.2578	.5926	.5506	.5506	1696	221.7	.4034	.5966	.5080	.4920
864	229.7	.1601	.6973	.6503	.6503	1697	224.7	.3940	.0121	.5268	.0109
865	227.7	.5948	.1229	.1156	.1156	1698	224.7	.3429	.3241	.4575	.2801
866	227.7	.5303	.2022	.1873	.1873	1699	219.7	.5377	.1531	.6519	.1245
867	227.7	.4104	.3442	.3172	.3172	1700	212.8	.8273	.0000	.8876	.0000
868	227.7	.2222	.5622	.5078	.5078	1701	212.8	.8277	.0187	.8860	.0137
869	227.7	.0569	.7460	.6703	.6703	1702	211.8	.8508	.1248	.8955	.0885
870	224.7	.5890	.0192	.0176	.0176	1703	210.8	.9039	.0455	.9353	.0320
871	224.7	.5479	.0690	.0606	.0606	1704	210.8	.9034	.0191	.9380	.0133
872	224.7	.2161	.4632	.3996	.3996	1705	209.3	.9732	.0089	.9823	.0061
873	224.7	.0811	.6175	.5299	.5299	1706	209.3	.9698	.0195	.9809	.0135
874	221.7	.4399	.0835	.0706	.0706	1859	238.9	.0000	.0689	.0000	.0759
875	221.7	.3825	.1525	.1272	.1272	1865	209.3	.9664	.0240	.9776	.0169

TABLE 14
EXPERIMENTAL DATA AT 23 ATM.

RUN NO.	TEMP. DEG.R	LIGUID MOL FRACTION N2	AR	O2	VAPOR MOL FRACTION N2	AR	O2	RUN NO.	TEMP. DEG.R	LIGUID MOL FRACTION N2	AR	O2	VAPOR MOL FRACTION N2	AR	O2
724	240.2	.11258675	.17428258	756	240.2	.1054	.0281	.8665	.1640	.0301	.8058
725	236.7	.20487952	.30046996	757	240.2	.1033	.0450	.8517	.1606	.0480	.7915
726	229.7	.40825918	.53014699	758	240.2	.1005	.0583	.8413	.1555	.0618	.7827
727	223.7	.58714129	.69563044	759	240.2	.0925	.0952	.8122	.1434	.1012	.7554
728	218.2	.80681932	.86561344	760	240.2	.0841	.1432	.7727	.1302	.1526	.7172
729	215.3	.92330767	.95060494	761	240.2	.0653	.2390	.6957	.1003	.2506	.6491
730	213.8	.96070193	.98770123	762	240.2	.0303	.4482	.5215	.0451	.4636	.4913
731	236.7	.0767	.92331140	.9860	763	240.2	.0059	.6265	.3666	.0116	.6415	.3470
732	232.7	.2043	.79572814	.7186	764	236.7	.2063	.0070	.7867	.2963	.0077	.6959
733	226.7	.4147	.58535160	.4840	765	236.7	.1992	.0389	.7619	.2906	.0392	.6703
734	220.7	.6574	.34267367	.2633	766	236.7	.1959	.0579	.7462	.2850	.0574	.6577
735	216.7	.8409	.15918836	.1164	767	236.7	.1934	.0735	.7330	.2796	.0737	.6467
736	215.3	.9108	.08929349	.0651	768	236.7	.1875	.0929	.7195	.2734	.0932	.6334
737	214.5	.9488	.05129635	.0365	769	236.7	.1780	.1313	.6906	.2593	.1315	.6093
738	214.1	.9662	.03389765	.0235	770	236.7	.1703	.1704	.6594	.2486	.1701	.5813
739	213.9	.9728	.02729801	.0199	771	236.7	.1600	.2276	.6124	.2339	.2263	.5398
740	213.7	.9821	.01799871	.0129	772	236.7	.1253	.4463	.4285	.1839	.4343	.3818
741	213.5	.9942	.00599950	.0050	773	236.7	.1054	.6107	.2839	.1541	.5894	.2565
742	244.70134	.98660157	.9843	774	236.7	.0935	.7365	.1700	.1372	.7064	.1564
743	244.60233	.97670269	.9731	775	236.7	.0812	.8847	.0341	.1205	.8478	.0317
744	244.50331	.96690378	.9622	776	232.7	.3161	.0153	.6685	.4323	.0154	.5524
745	244.40407	.95930467	.9533	777	232.7	.3050	.0693	.6258	.4169	.0656	.5175
746	244.20611	.93890718	.9282	778	232.7	.2961	.1243	.5796	.4037	.1167	.4796
747	243.90948	.90521084	.8916	779	232.7	.2808	.2100	.5092	.3808	.1948	.4244
748	243.41528	.84721709	.8291	780	232.7	.2661	.2933	.4406	.3604	.2709	.3687
749	242.32852	.71483092	.6908	781	232.7	.2436	.4509	.3055	.3308	.4118	.2575
750	241.34386	.56144621	.5379	782	232.7	.2235	.6114	.1651	.3053	.5545	.1403
751	240.26679	.33216809	.3191	783	232.7	.2087	.7707	.0206	.2873	.6968	.0159
752	239.88177	.16238229	.1771	784	229.7	.4072	.0149	.5779	.5290	.0135	.4575
753	240.2	.1134	.0078	.8789	.1753	.0103	.8144	785	229.7	.4093	.0257	.5650	.5245	.0232	.4522
754	240.2	.1141	.0141	.8718	.1732	.0146	.8120	786	229.7	.4025	.0395	.5581	.5214	.0396	.4430
755	240.2	.1071	.0223	.8706	.1680	.0241	.8080	787	229.7	.3996	.0545	.5458	.5154	.0497	.4349

TABLE 14
EXPERIMENTAL DATA AT 23 ATM. (continued)

RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION N2	AR	O2	VAPOR MOL FRACTION N2	AR	O2	RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION N2	AR	O2	VAPOR MOL FRACTION N2	AR	O2
786	229.7	.3955	.0684	.5361	.5174	.0614	.4212	820	218.2	.7919	.1018	.1063	.8512	.0767	.0721
789	229.7	.3655	.0973	.5142	.5053	.0870	.4077	821	218.2	.7798	.1898	.0304	.8351	.1440	.0209
790	229.7	.3665	.1250	.4886	.5013	.1103	.3885	822	216.7	.8622	.0273	.1105	.9054	.0201	.0744
791	229.7	.3742	.1770	.4488	.4842	.1563	.3594	823	216.7	.8503	.1216	.0280	.8909	.0919	.0172
792	229.7	.3541	.3147	.3312	.4574	.2756	.2670	824	216.7	.8550	.0743	.0708	.8954	.0559	.0488
793	229.7	.3277	.4964	.1759	.4258	.4325	.1417	825	215.3	.9255	.0076	.0669	.9492	.0054	.0454
794	226.7	.5041	.0184	.4775	.6175	.0162	.3663	826	215.3	.9242	.0226	.0532	.9466	.0168	.0366
795	226.7	.4953	.0501	.4547	.6096	.0437	.3467	827	215.3	.9223	.0347	.0431	.9462	.0243	.0295
796	226.7	.4899	.0822	.4279	.6057	.0705	.3239	828	215.3	.9184	.0467	.0349	.9429	.0336	.0235
797	226.7	.4794	.1392	.3813	.5899	.1164	.2936	829	215.3	.9187	.0604	.0210	.9414	.0438	.0148
798	226.7	.4666	.2455	.2879	.5718	.2114	.2169	830	215.3	.9158	.0767	.0075	.9390	.0562	.0049
799	226.7	.4479	.3526	.1995	.5494	.2978	.1528	831	213.8	.9827	.0058	.0115	.9901	.0031	.0067
800	223.7	.6066	.0106	.3828	.7104	.0091	.2805	832	213.8	.9830	.0103	.0067	.9884	.0075	.0041
801	223.7	.6035	.0246	.3719	.7102	.0204	.2695	833	213.8	.9831	.0137	.0032	.9881	.0098	.0022
802	223.7	.6005	.0362	.3633	.7048	.0297	.2655	918	213.5	.9946	.0023	.0031	.9963	.0016	.0021
803	223.7	.6003	.0519	.3476	.7035	.0423	.2542	919	215.3	.9212	.0377	.0411	.9447	.0273	.0280
804	223.7	.5982	.0652	.3367	.7008	.0530	.2462	920	216.7	.8591	.0757	.0653	.8977	.0572	.0451
805	223.7	.5940	.0932	.3129	.6935	.0762	.2303	921	218.2	.8063	.0080	.1857	.8670	.0064	.1266
806	223.7	.5882	.1185	.2932	.6882	.0967	.2151	922	220.7	.7170	.0235	.2595	.7940	.0185	.1875
807	223.7	.5731	.2137	.2131	.6699	.1739	.1562	923	220.7	.6765	.2474	.0761	.7548	.1925	.0528
808	223.7	.5478	.3766	.0756	.6409	.3008	.0583	924	223.7	.6025	.0258	.3717	.7094	.0209	.2697
809	220.7	.7121	.0193	.2687	.7978	.0140	.1882	925	223.7	.61053895	.71422658
810	220.7	.7031	.0593	.2376	.7855	.0459	.1686	926	226.7	.4305	.4799	.0896	.5317	.3999	.0684
811	220.7	.7006	.093A	.2056	.7815	.0737	.1449	927	229.7	.3160	.6183	.0656	.4111	.5354	.0535
812	220.7	.6824	.1904	.1272	.7658	.1481	.0861	928	229.7	.3092	.69084022	.5978
813	220.7	.6693	.2913	.0394	.7472	.2253	.0275	929	232.7	.2113	.7446	.0442	.2896	.6725	.0380
814	218.2	.8080	.0092	.1828	.8663	.0082	.1255	930	236.7	.2018	.0268	.7714	.2951	.0268	.0781
815	218.2	.8068	.0209	.1723	.8616	.0158	.1226	931	239.69093	.09079122	.0678
816	218.2	.8055	.0330	.1615	.8613	.0260	.1127	932	240.2	.1138	.0080	.8782	.1757	.0083	.8160
817	218.2	.8033	.044A	.1518	.8613	.0340	.1047	933	240.2	.1093	.0389	.8517	.1641	.0431	.7928
818	218.2	.8030	.0540	.1430	.8610	.0408	.0982	934	240.2	.0297	.4579	.5124	.0456	.4712	.4832
819	218.2	.7971	.0743	.1286	.8552	.0571	.0877	935	240.2	.0090	.6332	.3578	.0112	.6492	.3396

TABLE 15
EXPERIMENTAL DATA AT 26 ATM.

RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION N2	LIQUID MOL FRACTION AR	VAPOR MOL FRACTION N2	VAPOR MOL FRACTION AR	RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION N2	LIQUID MOL FRACTION AR	VAPOR MOL FRACTION N2	VAPOR MOL FRACTION AR
610	245.1	.10711659	646	242.7	.0502	.8991	.0730	.8773
611	240.7	.23193236	647	240.7	.2281	.0049	.3203	.0051
612	234.7	.40575152	648	240.7	.2290	.0077	.3190	.0082
613	228.7	.59766942	649	240.7	.2256	.0118	.3148	.0120
614	222.7	.80948626	650	240.7	.2268	.0173	.3133	.0178
615	219.7	.92509464	651	240.7	.2189	.0271	.3125	.0277
616	218.2	.97909868	652	240.7	.2214	.0310	.3093	.0307
617	240.7	.1055	.8945	.1481	.8519	653	240.7	.2137	.0608	.2994	.0608
618	237.7	.2004	.7994	.2700	.7300	654	240.7	.1901	.1587	.2693	.1560
619	231.7	.4090	.5920	.4973	.5027	655	240.7	.1512	.3826	.2132	.3709
620	225.7	.6378	.3622	.7109	.2891	656	240.7	.1194	.6170	.1722	.5985
621	221.2	.8373	.1627	.8753	.1247	657	240.7	.1072	.7296	.1549	.6969
622	219.2	.9301	.0690	.9471	.0529	658	240.7	.0963	.8469	.1409	.8055
623	218.8	.94949612	659	237.7	.3134	.0044	.4187	.0043
624	218.4	.9654	.0346	.9736	.0264	660	237.7	.3115	.0131	.4159	.0122
625	218.2	.9739	.0261	.9806	.0194	661	237.7	.3123	.0144	.4150	.0156
626	217.8	.9864	.0136	.9896	.0104	662	237.7	.3101	.0252	.4111	.0238
627	217.8	.99509966	663	237.7	.3085	.0432	.4095	.0409
628	244.50050	664	237.7	.3034	.0644	.4024	.0519
629	244.493009310	665	237.7	.2971	.0920	.3949	.0869
630	244.585308585	666	237.7	.2813	.2021	.3707	.1918
631	244.680678134	667	237.7	.2569	.3154	.3435	.2927
632	244.777197790	668	237.7	.2261	.5436	.3015	.4991
633	244.970877221	669	237.7	.2032	.7612	.2725	.6964
634	245.265196624	670	234.7	.3880	.0743	.4936	.0687
635	245.655945760	671	234.7	.3765	.1626	.4845	.1484
636	246.048054999	672	234.7	.3433	.3138	.4378	.2808
637	246.735913827	673	234.7	.3211	.5075	.4085	.4491
638	248.117021888	674	234.7	.3134	.5817	.3987	.5133
639	249.007280807	675	234.7	.3075	.6407	.3921	.5642
640	249.006610672	676	231.7	.4964	.0100	.6039	.0087
641	242.7	.1533	.7806	.2282	.7045	677	231.7	.4966	.0147	.6039	.0127
642	242.7	.1351	.6608	.1935	.6002	678	231.7	.4966	.0259	.6020	.0229
643	242.7	.0965	.4374	.1375	.4291	679	231.7	.0000	.0000	.5988	.0322
644	242.7	.0873	.4111	.1244	.3794						
645	242.7	.0571	.7902	.0825	.1437						

TABLE 15
EXPERIMENTAL DATA AT 26 ATM. (continued)

RUN NO.	TEMP. DEG.R	LIQUID MOL FRACTION		VAPOR MOL FRACTION	VAPOR N2	VAPOR MOL FRACTION	TEMP. DEG.R	LIQUID MOL FRACTION		VAPOR N2	VAPOR MOL FRACTION				
		N2	AR					N2	AR			N2	AR		
681	231.7	.4934	.0424	.4642	.5977	.0376	.3647	.715	219.2	.9397	.0216	.0386	.9571	.0161	.0268
682	231.7	.4874	.0683	.4443	.5910	.0598	.3492	716	219.2	.9393	.0303	.0304	.9553	.0228	.0220
683	231.7	.4813	.0934	.4253	.5835	.0809	.3356	717	219.2	.9367	.0406	.0226	.9527	.0311	.0163
684	231.7	.4650	.1800	.3550	.5632	.1555	.2813	718	219.2	.9334	.0513	.0153	.9490	.0375	.0135
685	231.7	.4271	.4067	.1662	.5245	.3444	.1311	719	219.2	.9332	.0552	.0117	.9491	.0422	.0087
686	231.7	.4119	.5352	.0530	.5037	.4528	.0434	720	218.2	.9799	.0085	.0116	.9851	.0066	.0083
687	228.7	.5945	.0265	.3791	.6864	.0228	.2908	721	218.2	.9780	.0167	.0053	.9838	.0126	.0036
688	228.7	.5884	.0465	.3551	.6822	.0389	.2795	722	231.7	.4934	.0329	.4736	.5985	.0288	.3727
689	228.7	.5875	.0624	.3500	.6768	.0523	.2710	723	247.22902	.70983117	.6883
690	228.7	.5749	.1455	.2796	.6641	.1216	.2143	893	249.60196	.98040222	.9778
691	228.7	.5580	.2422	.1998	.6431	.2021	.1548	894	249.40372	.96280426	.9574
692	225.7	.5335	.3975	.0690	.6216	.3256	.0528	895	249.20547	.94530615	.9385
693	225.7	.7014	.0103	.2883	.7782	.0083	.2135	896	248.80970	.90301088	.8912
694	225.7	.6996	.0209	.2796	.7755	.0173	.2072	897	245.2	.1094	.0190	.8715	.1592	.0204	.8204
695	225.7	.6981	.0283	.2735	.7740	.0232	.2028	898	245.2	.1008	.0611	.8380	.1492	.0649	.7859
696	225.7	.6963	.0393	.2644	.7713	.0321	.1965	899	245.2	.0849	.1341	.7810	.1244	.1424	.7331
697	225.7	.6936	.0465	.2599	.7721	.0382	.1896	900	245.2	.0744	.1846	.7409	.1101	.1951	.6948
698	225.7	.6929	.0615	.2457	.7675	.0504	.1821	901	245.2	.0516	.3086	.6398	.0755	.3215	.6031
699	225.7	.6884	.0909	.2207	.7634	.0740	.1626	902	242.7	.1369	.2029	.6602	.1950	.2053	.5996
700	225.7	.6708	.1924	.1368	.7408	.1552	.1040	903	242.7	.0501	.9251	.0247	.0721	.9041	.0238
701	222.7	.8019	.0563	.1418	.8552	.0306	.1142	904	240.7	.2312	.0098	.7591	.3214	.0096	.6690
702	222.7	.7967	.0855	.1176	.8529	.0436	.1034	905	240.7	.2277	.0237	.7487	.3164	.0237	.6599
703	222.7	.7630	.1664	.0505	.8472	.0671	.0857	906	240.7	.2208	.0575	.7217	.3063	.0571	.6366
704	221.2	.8652	.0117	.1230	.8324	.1297	.0379	907	237.7	.2155	.6597	.1248	.2869	.6035	.1096
705	221.2	.8642	.0235	.1123	.9014	.0089	.0897	908	234.7	.3766	.1479	.4754	.4777	.1366	.3857
706	221.2	.8561	.0491	.0948	.8990	.0183	.0827	909	231.7	.4913	.0488	.4599	.5959	.0429	.3612
707	221.2	.8564	.0694	.0742	.8921	.0394	.0685	910	225.7	.6978	.0463	.2559	.7719	.0374	.1906
708	221.2	.8517	.0931	.0552	.8939	.0538	.0523	911	225.7	.6649	.2567	.0784	.7361	.2049	.0590
709	221.2	.8500	.1144	.0356	.8896	.0708	.0396	912	221.2	.8649	.0318	.1033	.9018	.0243	.0739
710	221.2	.8463	.1360	.0177	.8844	.0868	.0268	913	221.2	.8634	.0401	.0965	.8982	.0310	.0706
711	220.2	.9014	.0211	.0776	.8816	.1049	.0136	914	219.2	.9330	.0464	.0206	.9516	.0347	.0137
712	220.2	.8982	.0365	.0653	.9291	.0162	.0546	915	218.2	.97940206	.98580142
713	220.2	.8902	.0915	.0183	.9252	.0231	.0467	916	218.2	.9751	.0184	.0065	.9822	.0135	.0044
714	219.2	.9416	.0077	.0507	.9163	.0701	.0136	917	217.8	.9949	.00519960	.0040
					.9577	.0060	.0364								

TABLE 16
 EXPERIMENTAL DATA AT MIXED PRESSURE LEVELS

<u>Run No.</u>	<u>Press.</u> <u>Atm.</u>	<u>Temp.</u> <u>Deg. R</u>	<u>Liquid Mol Fraction</u>			<u>Vapor Mol Fraction</u>		
			<u>N₂</u>	<u>Ar</u>	<u>O₂</u>	<u>N₂</u>	<u>Ar</u>	<u>O₂</u>
50	19.5	212.8	.7875	.0869	.1256	.8562	.0623	.0815
1914	1.03	163.0	.0039	-----	.9961	.0166	-----	.9834
1915	1.05	162.5	.0130	-----	.9870	.0491	-----	.9509
1916	0.97	162.0	.0035	-----	.9965	.0144	-----	.9856
1917	0.99	162.0	.0066	-----	.9934	.0248	-----	.9752
1918	0.98	161.3	.0179	-----	.9821	.0677	-----	.9323
1919	0.99	160.3	.0364	-----	.9636	.1313	-----	.8687
1920	0.97	160.0	.0385	-----	.9615	.1404	-----	.8596
1921	1.05	159.8	.0746	-----	.9254	.2397	-----	.7603
1922	1.01	159.0	.0833	-----	.9167	.2627	-----	.7373

VI. CORRELATION OF EXPERIMENTAL DATA

 A. Thermodynamic Equations

The problem of correlation of vapor-liquid equilibrium data at high pressures is more complicated than at low pressures since the effect of pressure on the free energy of the liquid and also the effect of deviations from ideality in the vapor must be taken into account. A derivation of the equilibrium equations which take these effects into account follows.

The effect of pressure upon the free energy of a component in the liquid is given by the relation

$$dG_i = \bar{V}_i dp \quad (2)$$

and the effect of nonideality in the vapor is accounted for by means of the fugacity coefficient defined as

$$\phi_i = \frac{f_i}{p y_i} \quad (3)$$

The activity coefficient of component i in the liquid is now defined as

$$\ln \gamma_i = \ln \frac{f_i}{f_i^* x_i} = \left[\frac{\partial(G^E/RT)}{\partial n_i} \right]_{T,p,n_j} \quad (4)$$

The derivation of the equilibrium equations involves a seven-step process:

1. The component is taken as a vapor from a standard pressure at which the vapor behaves ideally to the vapor pressure p_i° .

$$\frac{\Delta G^I}{RT} = \ln p_i^\circ + \ln \phi_i^\circ \quad (5)$$

2. The vapor is condensed at the pressure p_i° to liquid.

$$\frac{\Delta G^{II}}{RT} = 0 \quad (6)$$

3. The liquid is taken from the pressure p_i^o to the pressure of mixing p_m .

$$\frac{\Delta G^{III}}{RT} = \int_{p_i^o}^{p_m} \frac{v_i^o}{RT} dp \quad (7)$$

4. The component is mixed at the pressure p_m .

$$\frac{\Delta G^{IV}}{RT} = \ln x_i \gamma_i \quad (8)$$

5. The mixture is taken from the pressure p_m to the total vapor pressure of the mixture.

$$\frac{\Delta G^V}{RT} = \int_{p_m}^p \frac{\bar{v}_i}{RT} dp \quad (9)$$

6. The component in the liquid mixture is in equilibrium with the vapor at the pressure p and composition y_i .

$$\frac{\Delta G^{VI}}{RT} = 0 \quad (10)$$

7. The vapor is taken from the pressure p and composition y to a standard pressure at which the vapor behaves ideally, and then is separated into the various components.

$$\frac{\Delta G^{VII}}{RT} = \ln py_i - \ln \phi_i \quad (11)$$

Now since the free energy is a property of state and independent of the route by which the state is obtained, the sum of all these changes should add to zero since the initial and final states are the same. Thus the following relation for equilibrium is obtained.

$$\Sigma \frac{\Delta G}{RT} = \ln p_i^o \phi_i^o + \int_{p_i^o}^{p_m} \frac{v_i^o}{RT} dp + \ln x_i \gamma_i + \int_{p_m}^p \frac{\bar{v}_i}{RT} dp - \ln py_i \phi_i = 0 \quad (12)$$

If this equation is solved for py_i , the following is obtained:

$$\ln py_i = \ln \frac{p_i^{\circ} \phi_i^{\circ} x_i \gamma_i}{\phi_i} + \int_{p_i^{\circ}}^{p_m} \frac{v_i^{\circ}}{RT} dp + \int_{p_m}^p \frac{\bar{v}_i}{RT} dp \quad (13)$$

For the correlation of the nitrogen-argon-oxygen vapor liquid data there were insufficient partial molar volume data to use this equation as it stands, and it was necessary to simplify it. Thus it was assumed that the partial molar volume of a component in solution is equivalent to the liquid molar volume of that component and that the liquid volume is independent of pressure. With these assumptions, the equilibrium relation simplifies to the following equation which is the one used in correlating the nitrogen-argon-oxygen data.

$$py_i = \left[\frac{p_i^{\circ} x_i \gamma_i \phi_i^{\circ}}{\phi_i} \right] e^{v_i^{\circ} (p - p_i^{\circ})/RT} \quad (14)$$

These assumptions regarding the molar volume are partly justified by the fact that the correction is usually small amounting to less than 20% in most cases and any errors which are made in this correction can be partially compensated for with other parameters. However, in the neighborhood of the critical point this correction is undoubtedly larger and deviates significantly from the simplifying assumptions made here. Therefore it is improbable that this simplified equation will be applicable in the neighborhood of the critical point.

In the calculation of equilibria it is helpful to bear in mind that according to the phase rule, $F = c - P + 2$; c variables must be specified (since $P = 2$) before the equilibrium point can be calculated. Thus one might specify the liquid composition and the temperature (the liquid composition involves $c - 1$ variables since $\sum_i x_i = 1$) or perhaps the mole fraction of one component in the liquid, the temperature and the pressure. If it is necessary to calculate not only the equilibrium point but also the number of moles in each phase, one more variable must be specified since the phase rule includes only intensive variables. Thus for example, one might specify an overall composition of the two-phase system, the pressure and the temperature.

The ease of numerical calculation varies depending upon which variables are specified; however even in the simplest cases iterative type calculations are necessary. This iteration is necessary since the functions ϕ_i , γ_i and $e^{V_i(p-p_i)/RT}$ are not specified in terms of any one set of variables. For this reason the task of manual calculation would be prohibitive and calculations were done on a GE-225 computer.

B. Liquid Molar Volume

The liquid molar volume of the three components were determined by a least squares fit of existing data to the equation

$$V = a + b x + c x^2 + d x^3 + e x^4 + f x^5 \quad (15)$$

Table 17 lists the constants obtained and the literature source for the data. Above the critical temperature of nitrogen the molar volume of nitrogen represents an extrapolation of the data from below the critical temperature. Data close to the critical point were not fitted.

TABLE 17

LIQUID MOLAR VOLUME CORRELATION CONSTANTS

Component	a	b	c	d	e	f	Lit. Ref.
Nitrogen	- 0.7	147.1	-264.1	227.08	- 92.29	14.649	(4)
Argon	-98.7	451.5	-610.2	393.62	-122.11	14.803	(4)
Oxygen	-34.0	178.6	-221.5	139.05	.. 43.09	5.341	(5)

C. Vapor Pressure of Pure Components

Vapor pressure data for oxygen were taken from the literature. These data were used for the calibration of the three junction thermocouple of the equilibrium cell. Vapor pressure data for nitrogen and argon were measured in the cell based upon the temperature scale obtained from the oxygen data. Initially, it was attempted to calibrate the thermocouple from literature data on all three components, but calculated temperatures disagreed by as much as 0.2°R; therefore, only the data for oxygen were used in the calibration. If the oxygen temperature scale is in error by 0.2°R, then our temperature scale is in error by 0.2°R, but the ratio of vapor pressures will be more nearly correct than as calculated from the literature data.

Our value for the boiling point of oxygen is 162.36°R compared to the accepted value of 162.34°R⁽⁶⁾.

The vapor pressure data were fitted to the Riedel equation⁽⁷⁾.

$$\ln p_1^o = A - \frac{B}{T} + C \ln T + DT^6 \quad (16)$$

The constants obtained by a least squares fit to the data are summarized in Table 18 and deviation plots of the data are given in Figures 13, 14, and 15. The agreement with the data is generally within + 0.3% although there are some deviations as high as 1% from the correlated curves.

The vapor pressure of nitrogen calculated above the nitrogen critical temperature represents an extrapolation of the data from below the critical temperature.

TABLE 18

CONSTANTS FOR PURE COMPONENT VAPOR PRESSURES

Component	A	B	C	D	Data Source
Nitrogen	25.2115	1598.96	-2.24519	1.5445 x 10 ⁻¹⁵	This Work
Argon	18.7043	1621.12	-1.12969	0.4132 x 10 ⁻¹⁵	This Work
Oxygen	21.6017	1781.43	-1.56188	0.4032 x 10 ⁻¹⁵	8,9,10,11,12

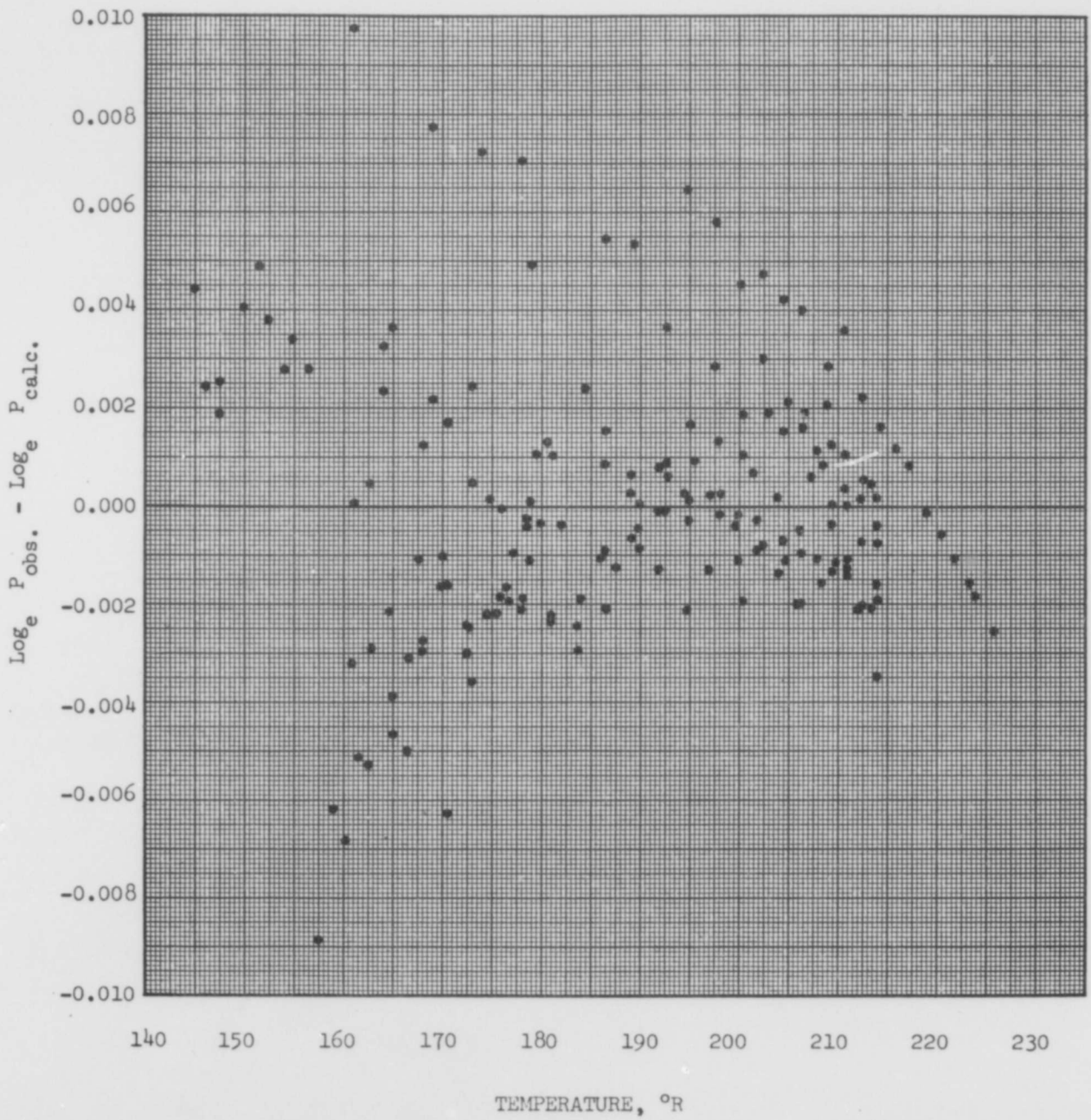


Figure 13. Deviation of APCI Nitrogen Vapor Pressure Data from Riedel Equation.

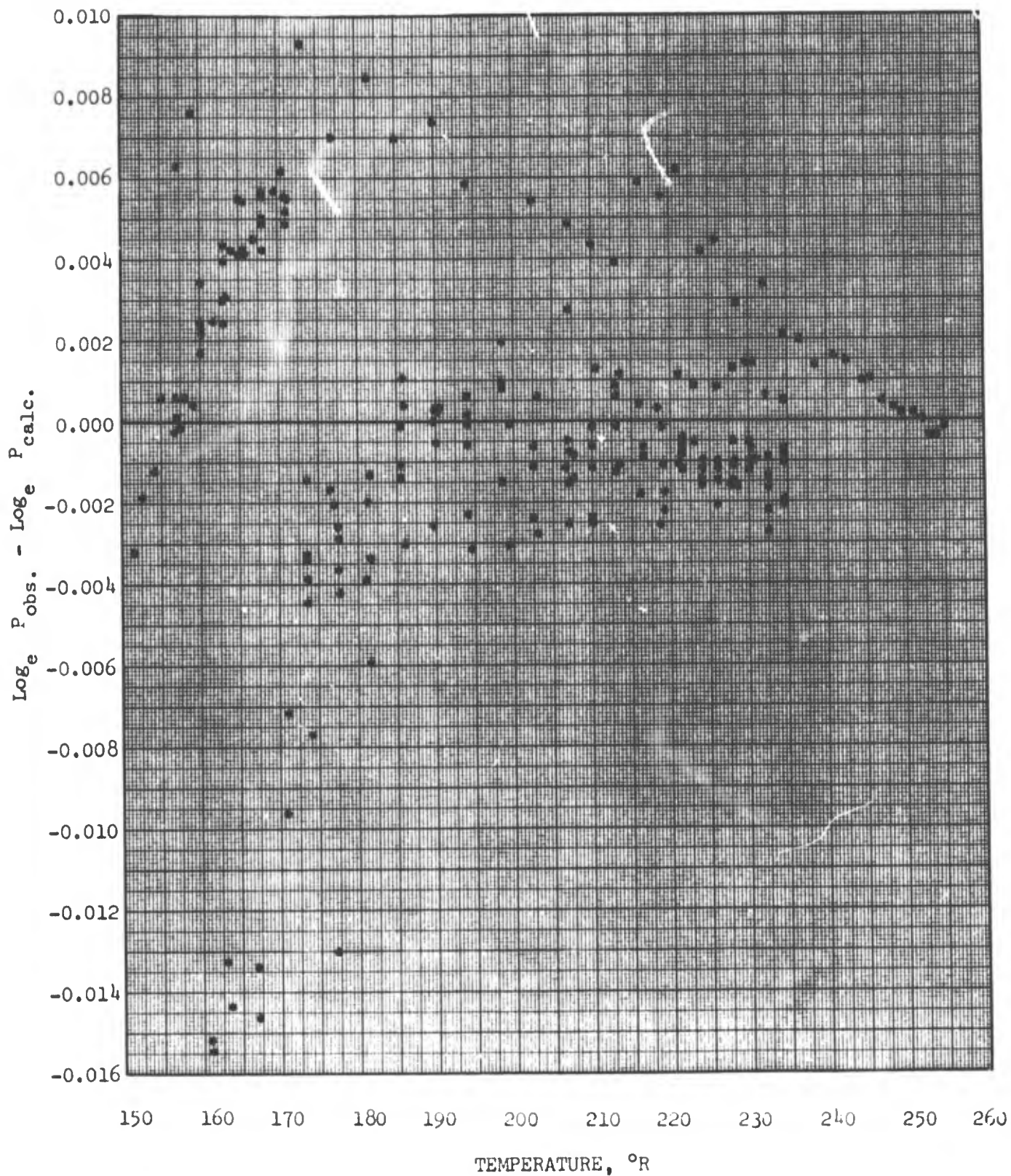


Figure 14. Deviation of APCI Argon Vapor Pressure Data from Riedel Equation.

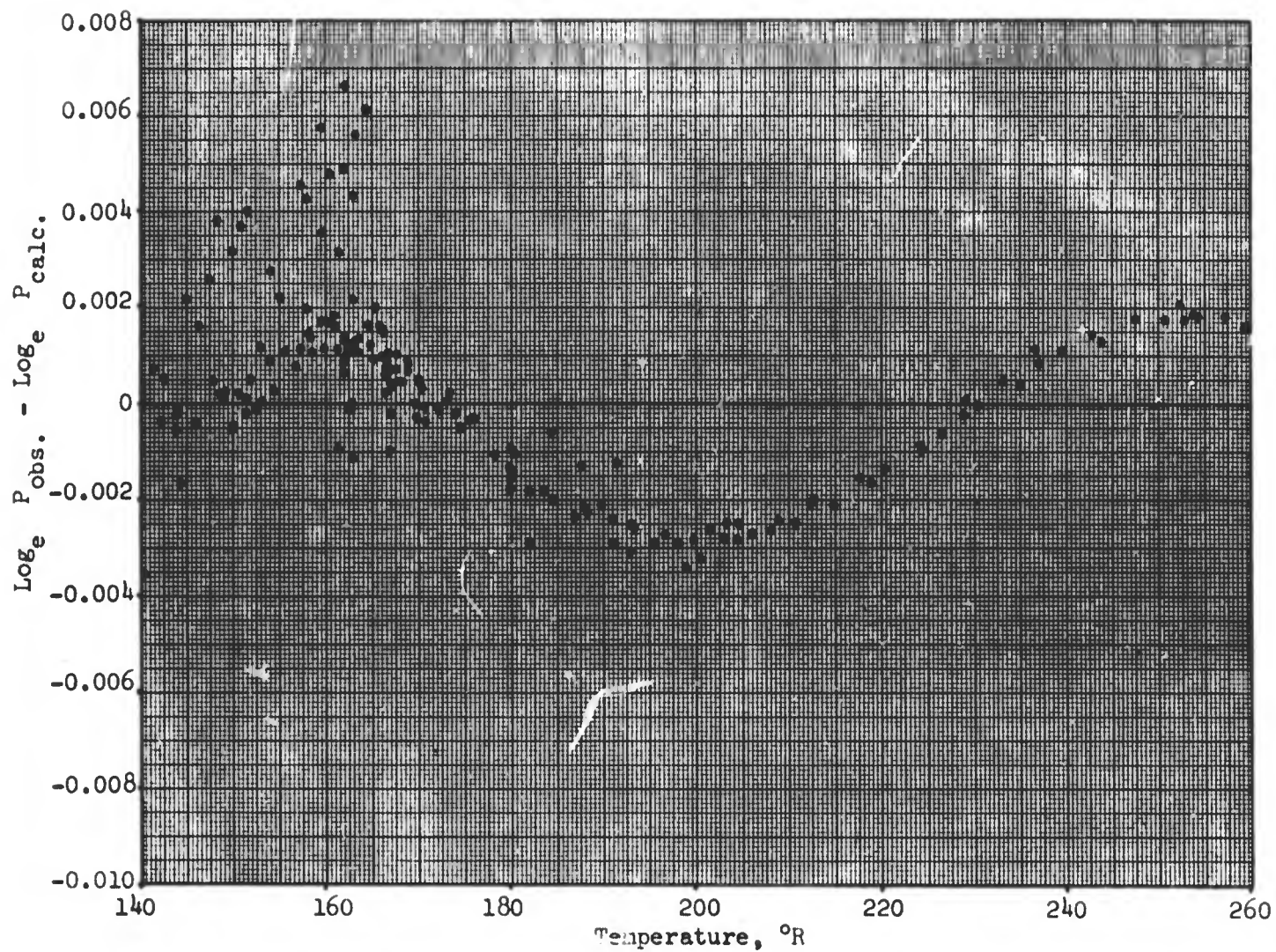


Figure 15. Deviation of Literature Oxygen Vapor Pressure Data from Riedel Equation.

A comparison of vapor pressure data from the literature for nitrogen^(5,8,13,14,15) and argon^(5,16,17) is given in Figures 16 and 17. The data for nitrogen deviate systematically about 0.7% from the calculated curve; the vapor pressures from the literature being too high. The data for argon are in good agreement with the correlation at high temperatures but at low temperatures the disagreement is of the order of 1%. These differences were part of the source of difficulty in correlating the data when the equilibrium cell thermocouple was calibrated from these data. This inconsistency then led to the calibration of the thermocouple from the vapor pressure of oxygen alone.

D. Fugacity Coefficient

The fugacity coefficient in the vapor phase is calculated from the virial equation of state terminating with the third virial coefficient

$$\frac{pV}{RT} = Z = 1 + \frac{B}{V} + \frac{C}{V^2} \quad (17)$$

The equation for the fugacity coefficient is as follows:

$$\ln \phi_i = \frac{2}{V} \sum_{j=1}^n y_j B_{ij} + \frac{3}{2V^2} \sum_{j=1}^n \sum_{k=1}^n y_j y_k C_{ijk} - \ln Z \quad (18)$$

The cross coefficients B_{ij} and C_{ijk} are calculated by methods similar to those presented by Pitzer⁽¹⁸⁾ and by Prausnitz⁽¹⁹⁾. The values of the second and third coefficients are given in Tables 19 and 20.

The calculated coefficients for the pure components are in good agreement with literature data^(20,30) as is indicated in Figures 18, 19, and 20. The third virial coefficient deviates more than does the second; however, an error of $0.1 \text{ (ft}^3/\text{lb-mole)}^2$ in the third virial coefficient produces a maximum error of only about 0.2% in the calculated fugacity coefficient.

The virial equation terminated at the third virial coefficient deviates negligibly from experimental P-V-T data at densities up to one half the critical density as shown in Figures 21, 22, and 23. At the experimental pressures of measurement the density of the vapor was always less than one half the critical density.

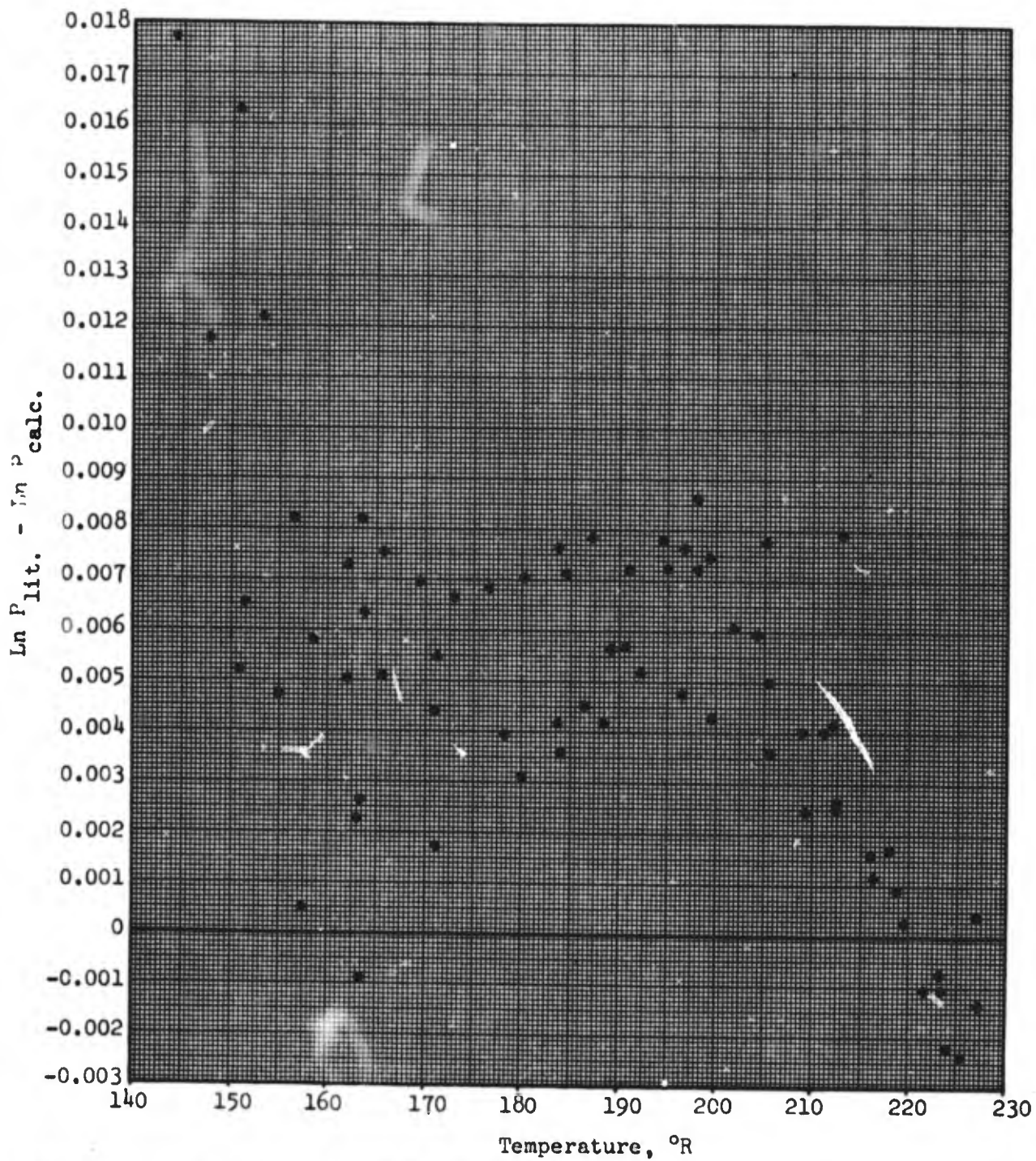


Figure 16. Deviation of Literature Vapor Pressure from APCI Correlation for Nitrogen.

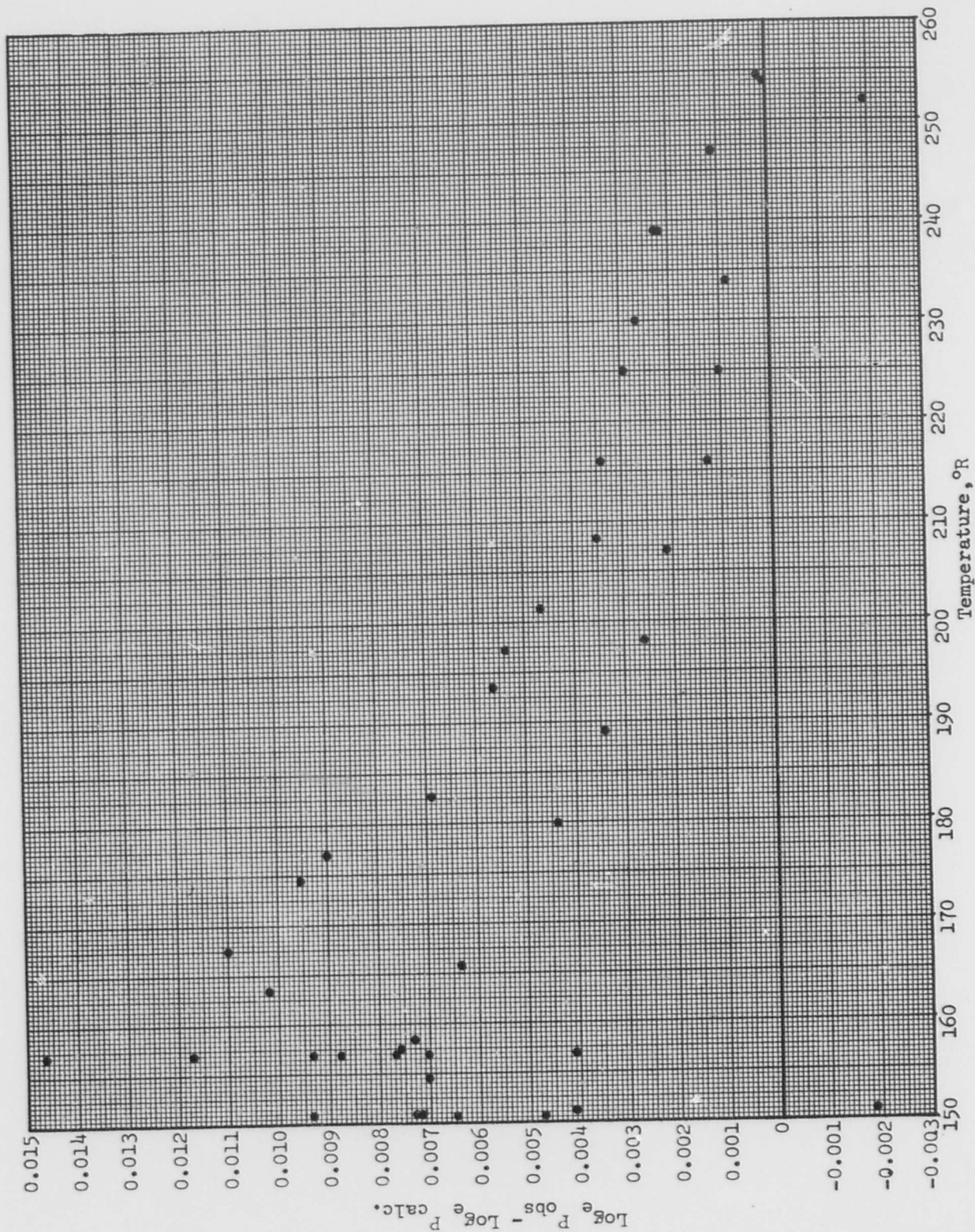


Figure 17. Deviation of Literature Vapor Pressure from APCI correlation for Argon.

TABLE 19

 SECOND VIRIAL COEFFICIENTS USED IN CALCULATIONS
 Cubic Feet/Pound Mole

Nitrogen = 1, Argon = 2, Oxygen = 3

<u>T, °R</u>	<u>-B₁₁</u>	<u>-B₁₂</u>	<u>-B₁₃</u>	<u>-B₂₂</u>	<u>-B₂₃</u>	<u>-B₃₃</u>
130	4.886	5.063	5.340	5.150	5.484	6.054
140	4.226	4.398	4.595	4.527	4.748	5.154
150	3.703	3.868	4.015	4.014	4.168	4.475
160	3.277	3.435	3.549	3.587	3.699	3.941
170	2.922	3.074	3.165	3.226	3.311	3.508
180	2.623	2.769	2.843	2.918	2.983	3.149
190	2.366	2.507	2.568	2.653	2.704	2.845
200	2.144	2.281	2.331	2.423	2.463	2.585
210	1.951	2.083	2.125	2.221	2.253	2.360
220	1.780	1.909	1.945	2.043	2.069	2.163
230	1.629	1.754	1.784	1.885	1.906	1.990
240	1.494	1.616	1.642	1.744	1.760	1.835
250	1.373	1.493	1.514	1.617	1.630	1.697
260	1.264	1.381	1.400	1.503	1.512	1.574

TABLE 20

THIRD VIRIAL COEFFICIENTS USED IN CALCULATIONS (Cubic Feet/Pound Mole)²

Nitrogen = 1, Argon = 2, Oxygen = 3

T, °R	C_{111}	C_{112}	C_{113}	C_{122}	C_{123}	C_{133}	C_{222}	C_{223}	C_{233}	C_{333}
130	-1.024	-2.175	-2.371	-3.662	-3.927	-4.205	-5.581	-5.933	-6.303	-6.692
140	0.035	-0.685	-0.799	-1.614	-1.770	-1.935	-2.809	-3.020	-3.241	-3.474
150	0.578	0.110	0.043	-0.492	-0.586	-0.685	-1.264	-1.393	-1.529	-1.672
160	0.850	0.533	0.495	0.130	0.073	0.013	-0.386	-0.466	-0.551	-0.640
170	0.974	0.753	0.731	0.473	0.439	0.403	0.117	0.067	0.015	-0.041
180	1.018	0.858	0.847	0.657	0.638	0.617	0.405	0.374	0.342	0.307
190	1.019	0.898	0.894	0.750	0.740	0.728	0.566	0.547	0.527	0.506
200	0.995	0.902	0.902	0.789	0.785	0.779	0.651	0.640	0.629	0.616
210	0.960	0.885	0.888	0.797	0.796	0.795	0.690	0.684	0.679	0.672
220	0.919	0.857	0.862	0.786	0.788	0.789	0.701	0.699	0.697	0.695
230	0.877	0.824	0.830	0.765	0.768	0.771	0.695	0.696	0.697	0.697
240	0.835	0.789	0.795	0.738	0.743	0.747	0.680	0.683	0.685	0.687
250	0.795	0.754	0.760	0.709	0.714	0.719	0.660	0.663	0.667	0.670
260	0.757	0.719	0.726	0.679	0.685	0.691	0.636	0.641	0.645	0.649

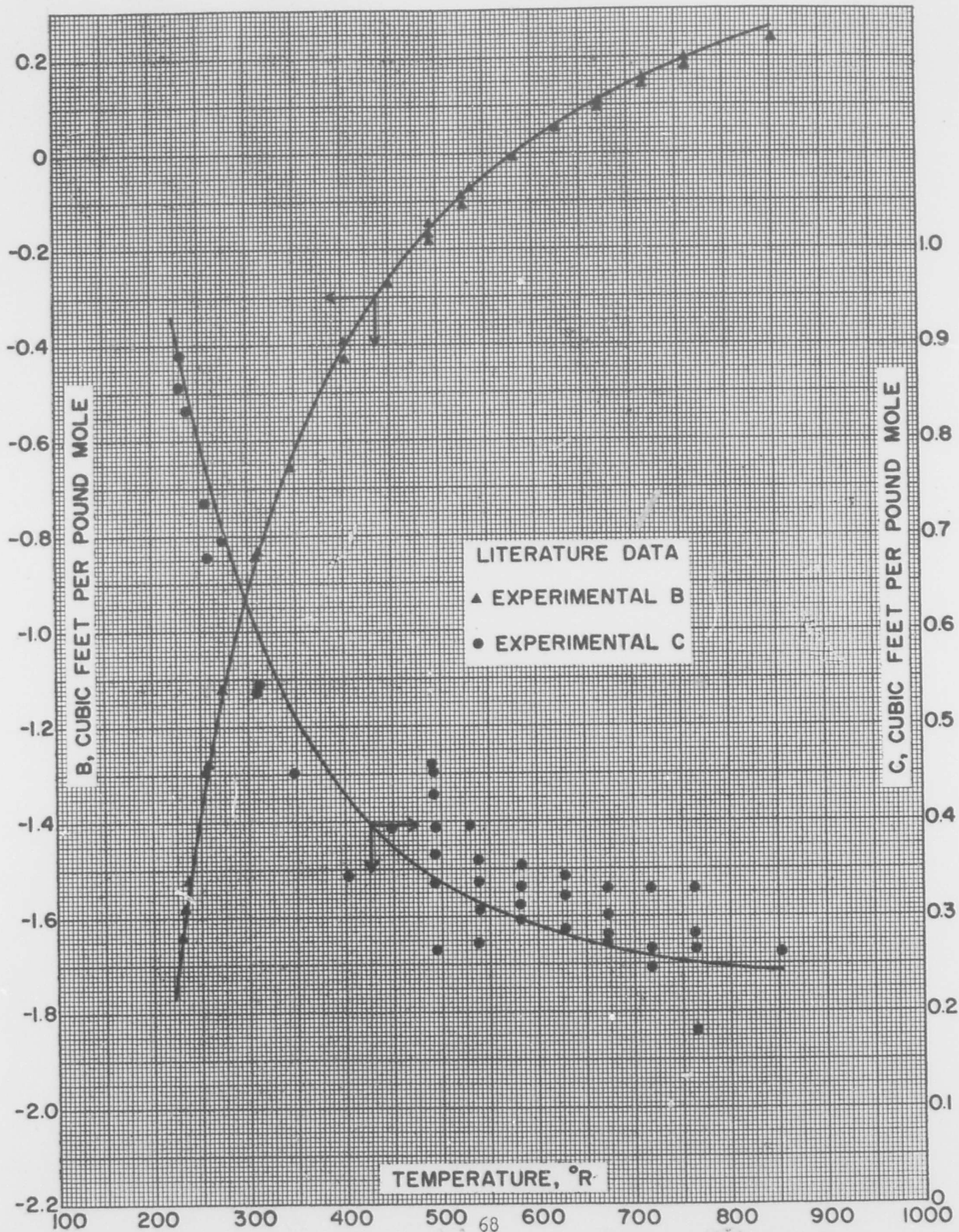


Figure 18. Calculated Second and Third Virial Coefficients, B and C, for Nitrogen.

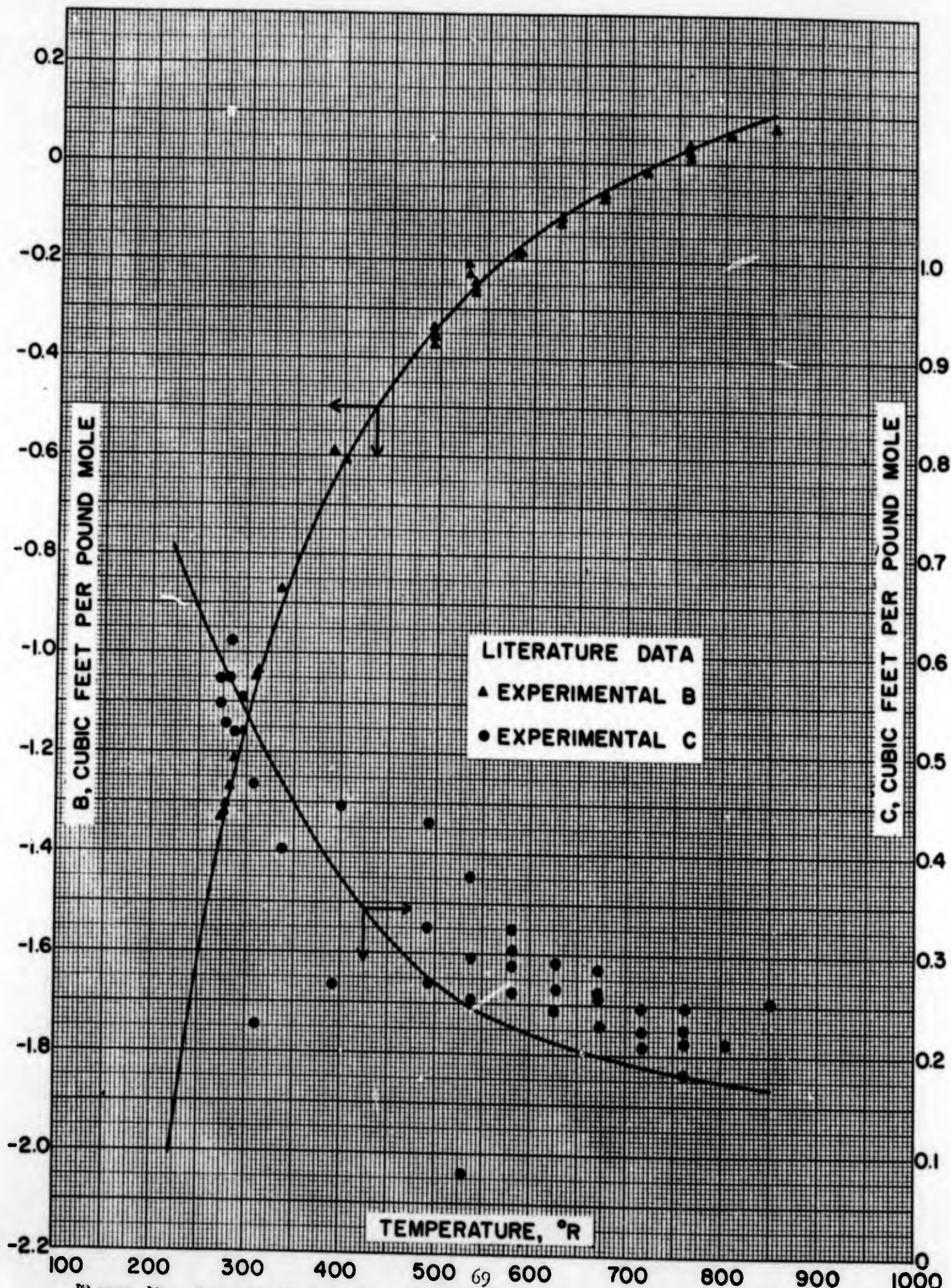


Figure 19. Calculated Second and Third Virial Coefficients, B and C, for Argon.

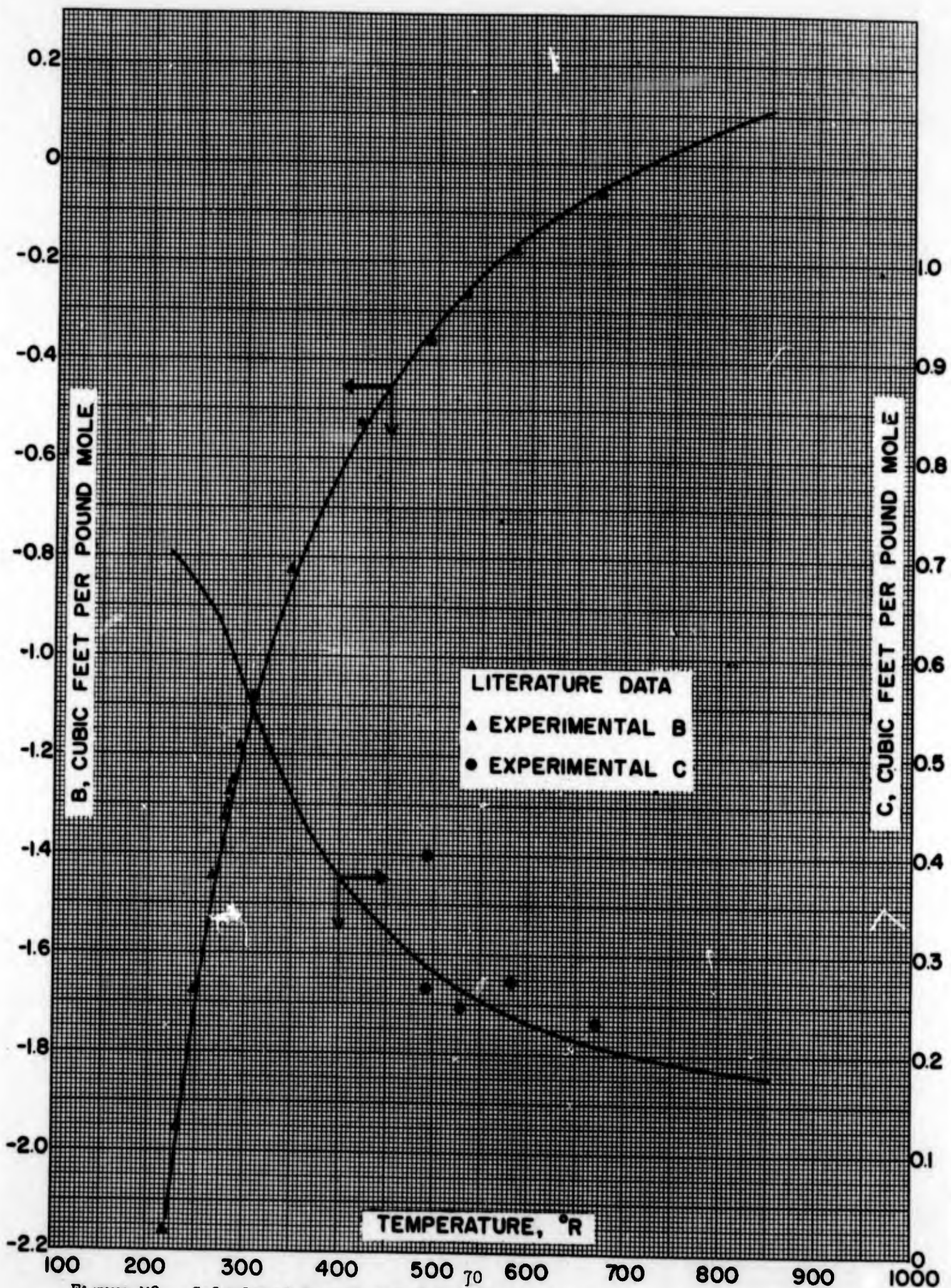


Figure 20. Calculated Second and Third Virial Coefficient, B and C, for Oxygen.

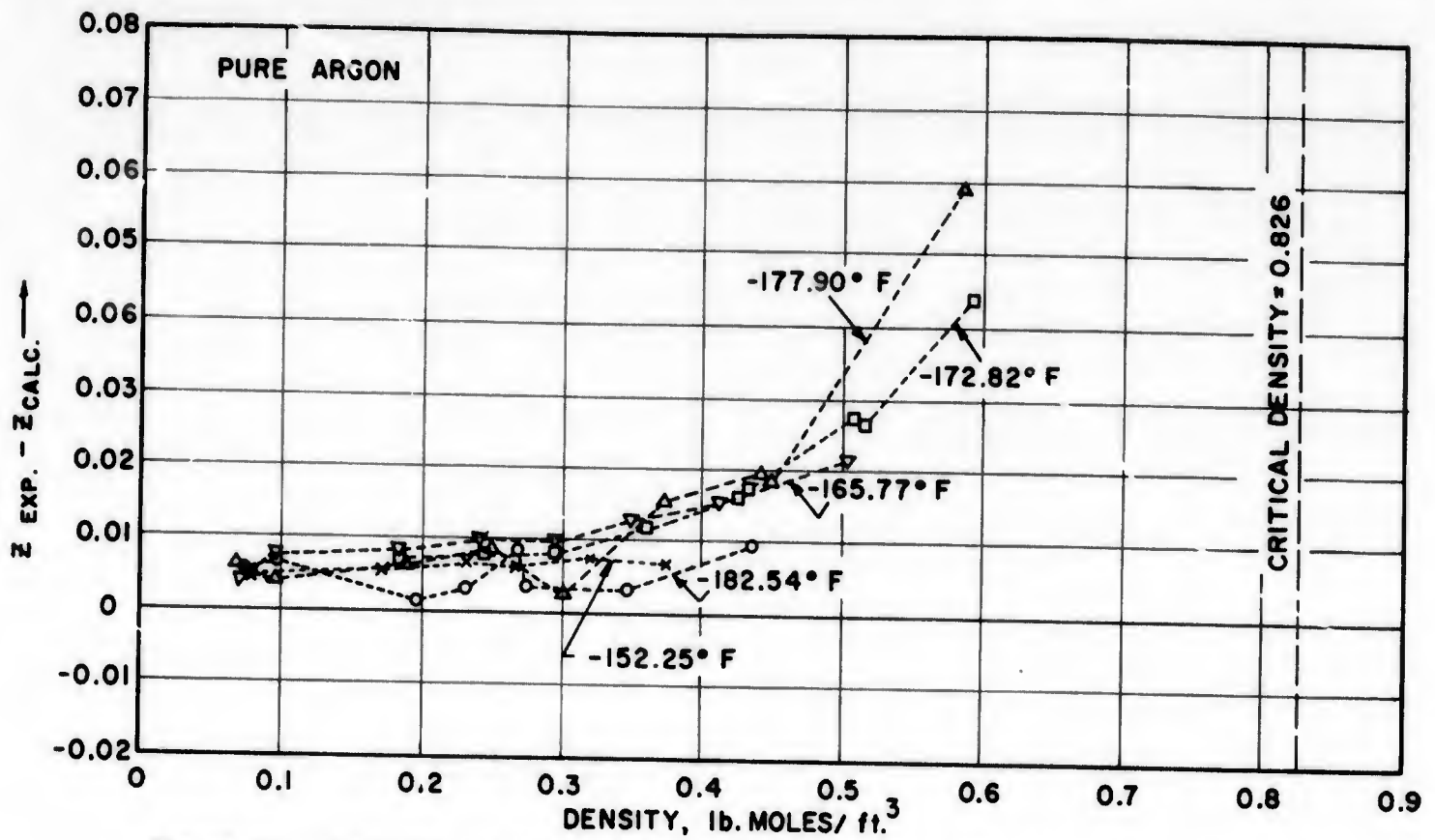


Figure 21. Comparison of Calculated and Experimental Compressibility Data, Argon.

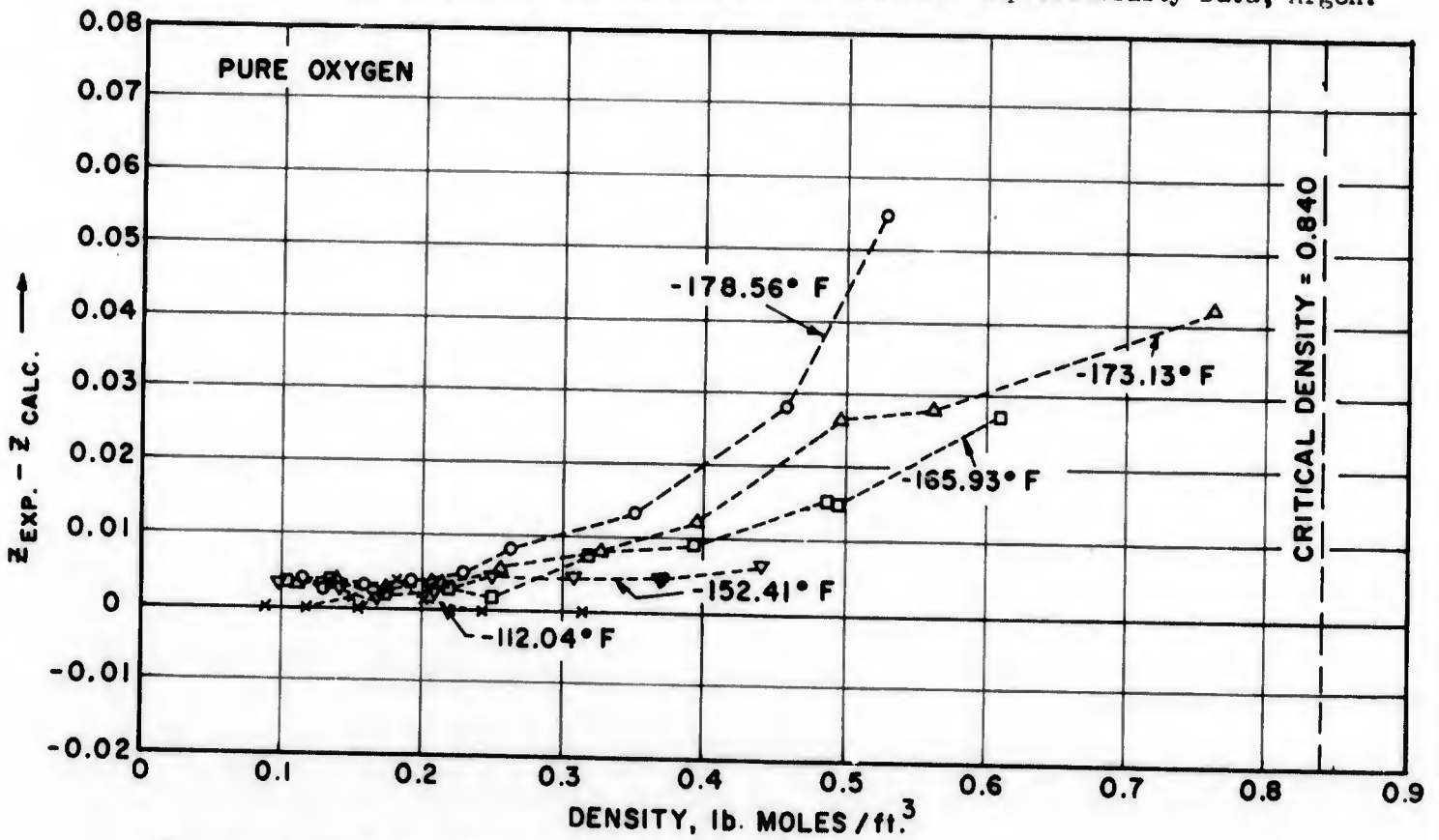


Figure 22. Comparison of Calculated and Experimental Compressibility Data, Oxygen.

Knobler and co-workers⁽³¹⁾ have measured the cross coefficients of argon-oxygen, oxygen-nitrogen, and nitrogen-argon at 90°K. These data are shown in Figure 24 plotted along with the calculated curves. No other cross coefficient data were found.

Keunen, Virschoyle and Van Urk⁽³²⁾ have measured the compressibility of two oxygen-nitrogen mixtures and Penning⁽³³⁾ has made measurements on air. Deviations in compressibility are shown plotted in Figures 25 and 26 where the difference is small as in the case of the pure components.

In view of these comparisons it is felt that the virial equation and the virial coefficients are within the experimental range of accuracy of existing P-V-T data and holds for mixtures as well as for pure components. The deviation in compressibility factor is of the order of 0.005 which probably corresponds to the uncertainty in the fugacity coefficient.

E. Activity Coefficient Equation

The liquid activity coefficient data calculated from the experimental data were correlated by means of the Van Laar equation. In a binary mixture it may be written as

$$\ln \gamma_1 = S_1 \left[\frac{S_2 x_2}{S_1 x_1 + S_2 x_2} \right]^2 A_{12} \quad (19)$$

or in a multicomponent mixture as

$$\ln \gamma_i = S_i \left[\sum_{j=1}^n \theta_j A_{i,j} - \frac{1}{2} \sum_{j=1}^n \sum_{k=1}^n \theta_j \theta_k A_{jk} \right] \quad (20)$$

where $\theta_j = \frac{S_j x_j}{\sum_{k=1}^n S_k x_k}$

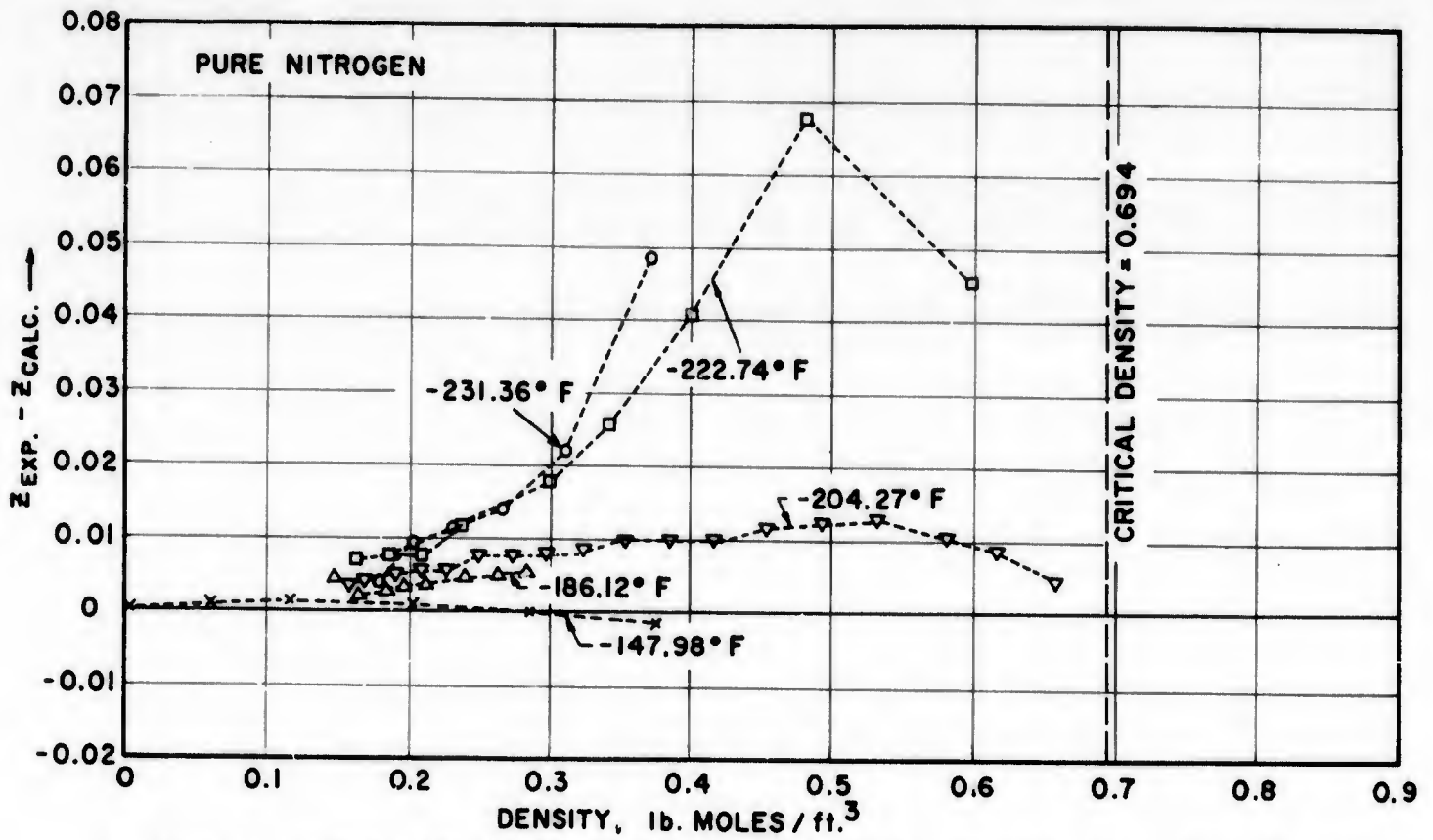


Figure 23. Comparison of Calculated and Experimental Compressibility Data, Nitrogen.

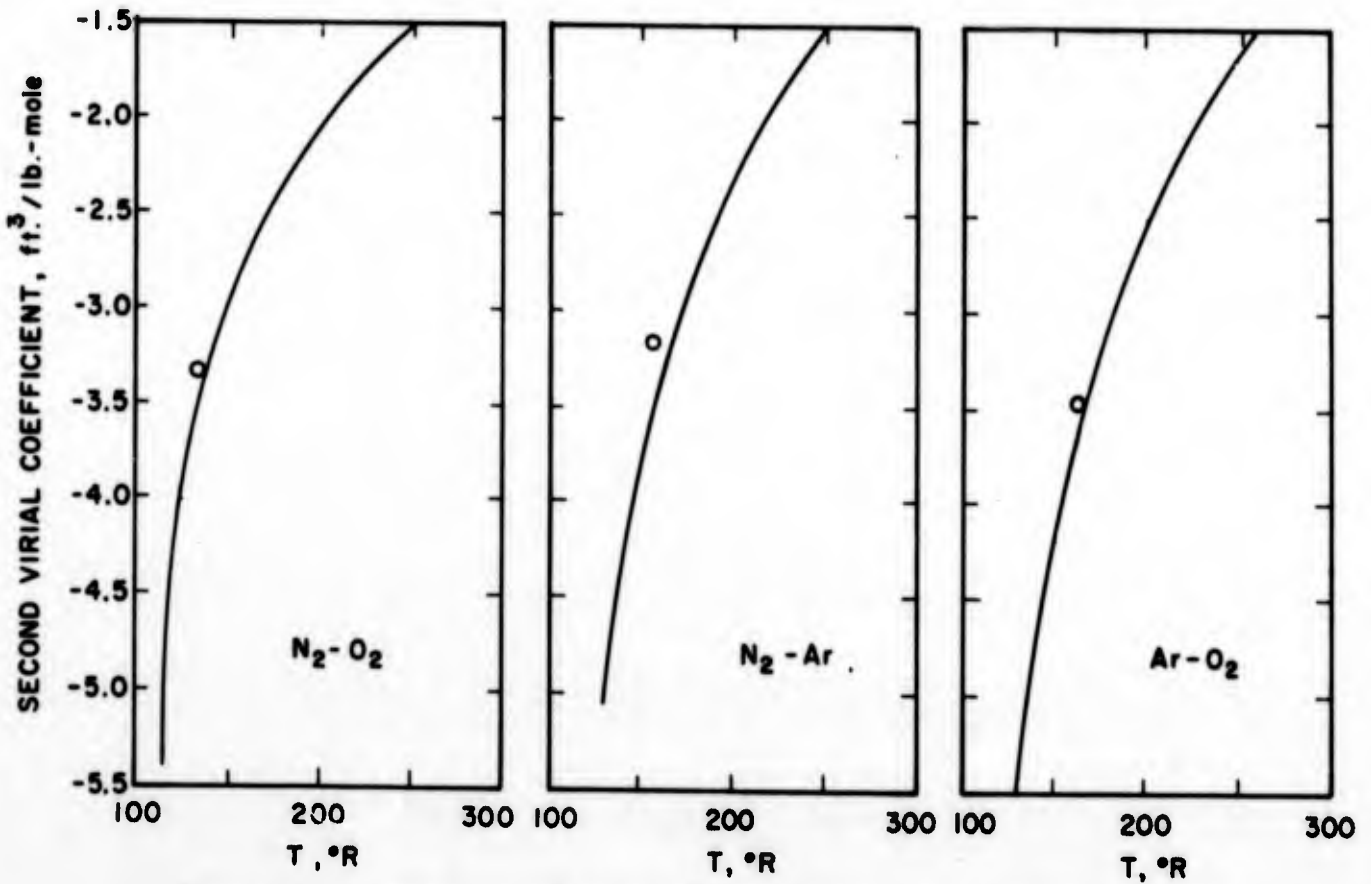


Figure 24. Comparison of Calculated and Experimental Cross Coefficients.

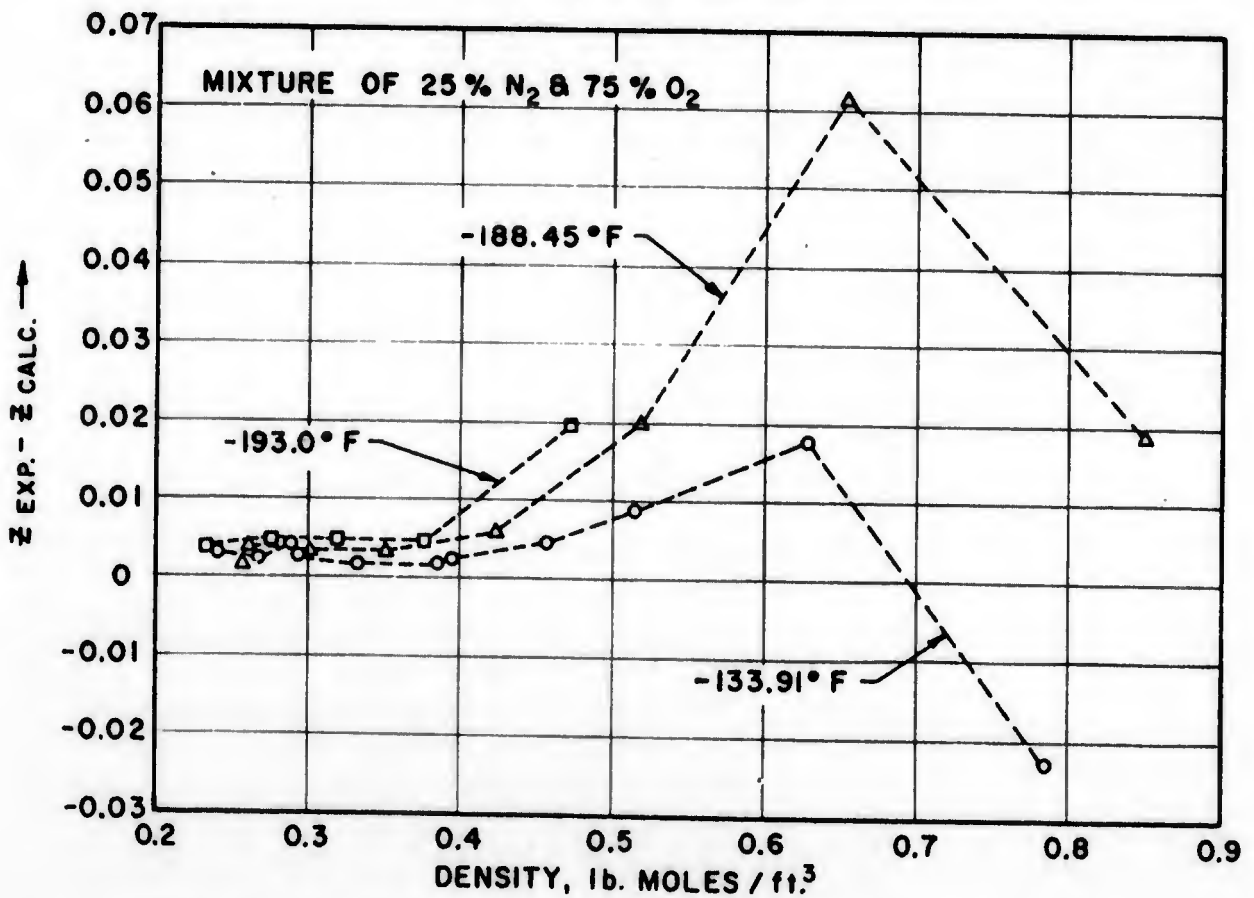
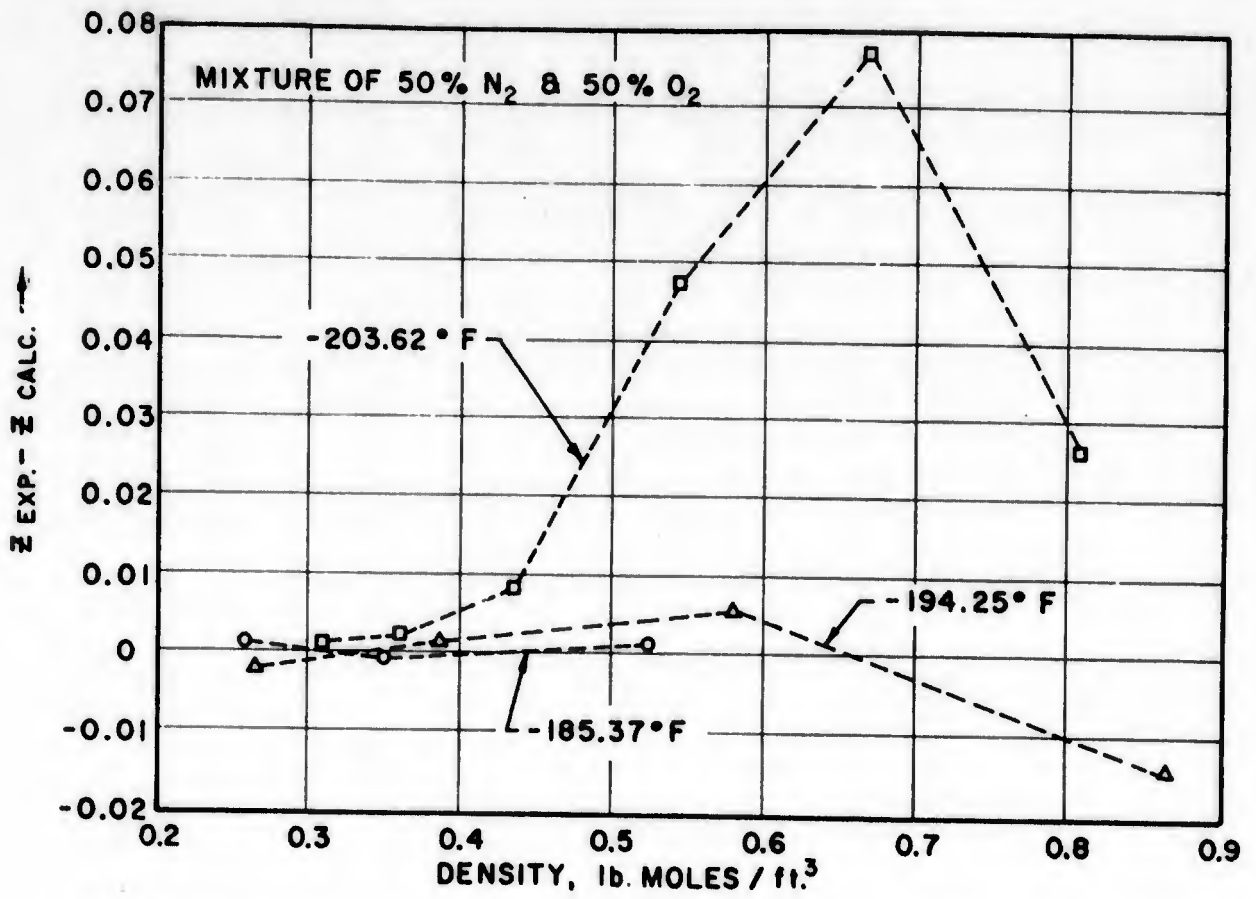


Figure 25. Comparison of Calculated and Experimental Compressibility Data, Nitrogen-Oxygen Mixture.

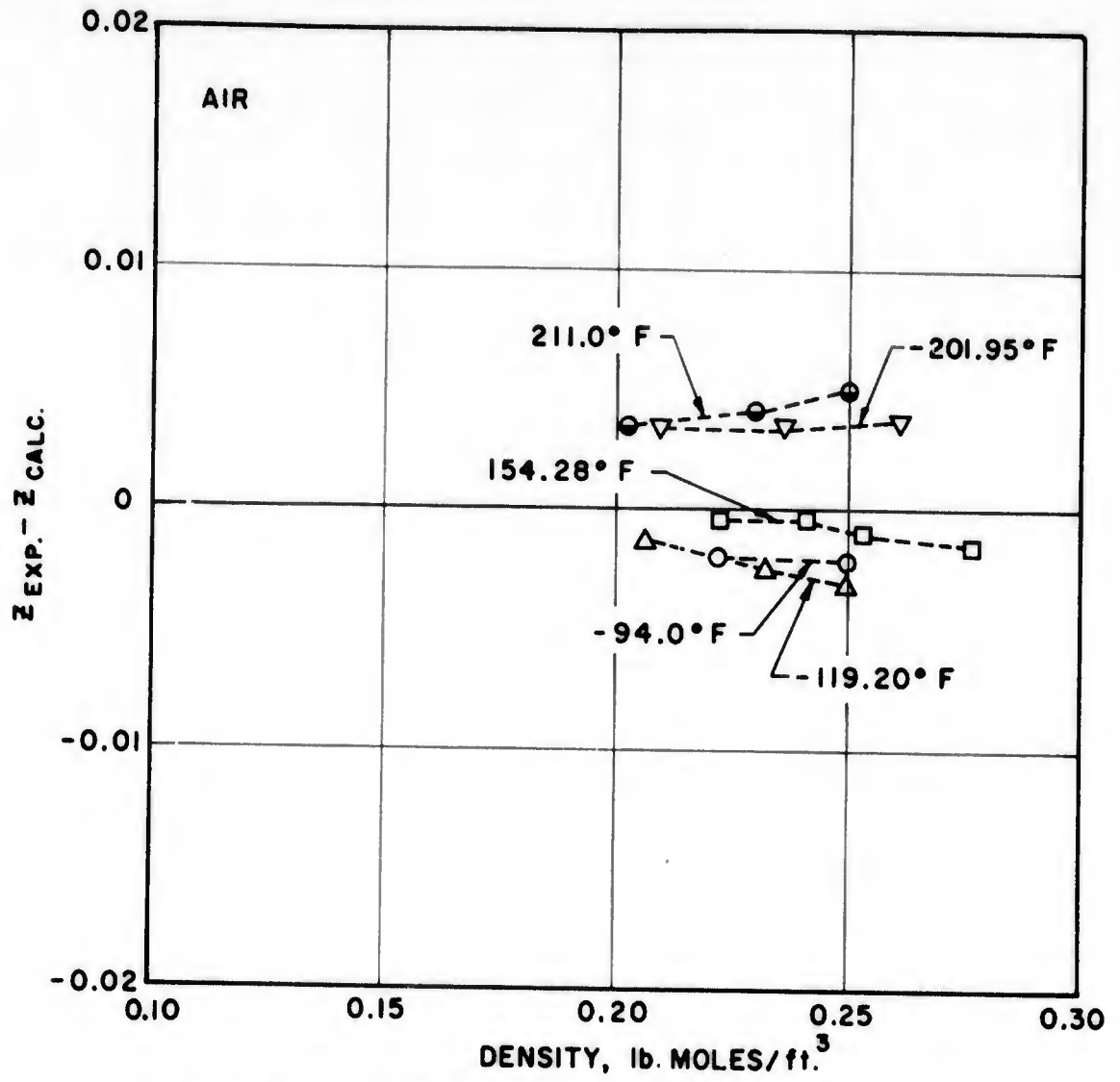


Figure 26. Comparison of Calculated and Experimental Compressibility Data, Air.

The interaction coefficients A_{ij} were assumed to be temperature dependent according to the relation

$$A_{ij} = a_{ij} + b_{ij}/T \tag{21}$$

The constants in the Van Laar equation were determined by a least squares fit to the entire set of vapor-liquid equilibrium data. The constants obtained are given in Table 21. A discussion of the correlation and comparisons with data are given in the following section.

TABLE 21
VAN LAAR CONSTANTS FOR NITROGEN-ARGON-OXYGEN
ACTIVITY COEFFICIENTS IN THE LIQUID PHASE

Component	Van Laar Volume	a_{ij}			b_{ij}		
		N ₂	Ar	O ₂	N ₂	Ar	O ₂
Nitrogen	1.00	0	-.1515	-.0669	0	51.8	43.9
Argon	1.00	-.1515	0	-.0837	51.8	0	40.7
Oxygen	1.00	-.0669	-.0837	0	43.9	40.7	0

VII. COMPARISON OF CORRELATION TO DATA

The experimental vapor-liquid equilibrium data were fitted by the method of least squares to the constants in the logarithm of the activity coefficient of each component. By this method a single vapor-liquid equilibrium point provided two activity coefficient points in a binary mixture and three points in a ternary mixture. With 1962 equilibrium points this produced 5344 activity coefficient points, requiring considerable running time on the computer each time a least squares analysis was made. Each experimental point was weighted equally because equal weight seems as logical for this set of data as other methods of weighting. If the Gibbs free energy of mixing had been fitted, it would have been more logical to weight the data differently because data at low concentrations of a component would not receive sufficient weight.

A summary of the various least square analysis runs made on the computer is given in Table 22, where the curve-fit number is in the chronological order of the analysis made. Runs 1, 2, 3, and 4 show that it makes little difference in the RMS error whether the three binaries are assumed to be symmetrical or unsymmetrical in the activity coefficient. Runs 5 and 6 are equivalent to Runs 4 and 1 respectively, except that points deviating more than three times the RMS error were deleted. The percentage of points deleted was five times the theoretical number of 0.3% based on a random error distribution, and the RMS error was reduced approximately 50%--38 times the theoretical value of 1.3%--justifying the deletion of the points. Runs 5 and 6 show that it makes little difference in the RMS error whether the constants a_{ij} are set to zero or not; the error only increasing from .0235 to .0261. Because of this insensitivity, the constants b_{ij} have been fixed consistent with heat of mixing data from the literature and the coefficients a_{ij} have been adjusted to fit the activity coefficient data. Runs 7 and 8 correspond to this restriction, however, it was found that there was a systematic bias in the correlation due to errors in the vapor pressures of the pure components.

This bias is shown in Table 23 where there were 1517 nitrogen points in Run 8 with positive deviation compared with only 229 points with negative deviation. An examination of the data showed that the correlation could be improved if the vapor pressures of the pure components were adjusted slightly. An adjustment of the data was made by the use of vapor pressure data measured under the present project in place of data reported in the literature as described in Section III-G. The results of the adjustment are shown as the difference between Runs 8 and 10 in Tables 22 and 23. The RMS error dropped slightly and the number of positive and negative deviations became more nearly the same.

TABLE 22

CONSTANTS AND ROOT MEAN SQUARE ERROR OF VARIOUS CURVE-FITS

Constant	Curve-Fit Number									
	1	2	3	4	5	6	7	8	9	10
S_{N_2}	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0
S_{Ar}	1.0	.9743*	.9743	1.0	1.0	1.0	1.0	1.0	1.0	1.0
S_{O_2}	1.0	.9469*	.9469	1.0	1.0	1.0	1.0	1.0	1.0	1.0
a_{N_2-Ar}	0.0	0.0	.0696*	.0698*	.1237*	0.0	-.1415*	-.1397*	-.1555*	-.1515*
b_{N_2-Ar}	24.54*	24.54	11.61*	11.16*	1.01*	24.60*	51.8	51.8	51.8	51.8
$a_{N_2-O_2}$	0.0	0.0	.1849*	.1818*	.2191*	0.0	-.0432*	-.0439*	-.0653*	-.0669*
$b_{N_2-O_2}$	34.81*	34.81	-.60*	0.0*	-7.74*	34.51*	43.9	43.9	43.9	43.9
a_{Ar-O_2}	0.0	0.0	-.1096*	-.1046*	-.0984*	0.0	-.0864*	-.0893*	-.0808*	-.0837*
b_{Ar-O_2}	23.31*	23.31	46.45*	44.47*	42.64*	22.78*	40.7	40.7	40.7	40.7
RMS Error	.0456	.0455	.0444	.0445	.0235	.0261	.0466	.0284	.0431	.0250
Points Deleted	0	0	0	0	87	86	0	81	0	92

*Coefficient Varied in That Run

TABLE 23

 SUMMARY OF POSITIVE AND NEGATIVE
 DEVIATIONS OF EXPERIMENTAL POINTS FROM CORRELATION

Run No.	Nitrogen		Argon		Oxygen	
	Plus	Minus	Plus	Minus	Plus	Minus
8	1517	229	829	935	533	1201
10	1135	614	1024	733	570	1176

Run 10 has been adopted as the final correlation although there still remain systematic deviations in the data as shown in Figures 27 to 31. The various regions designated in these figures correspond to the following:

Region I, nitrogen mole fraction greater than 0.5

Region II, argon mole fraction greater than 0.5

Region III, oxygen mole fraction greater than 0.5

Region IV, mole fraction of all three components less than 0.5.

These figures indicate systematic deviations at low temperatures; a relatively even distribution at between 170 and 180°R; systematic deviations between 190 and 210°R; a relatively even distribution between 220 and 230°R; and systematic deviations above 230°R. This pattern exists somewhat independent of the region examined, but is most predominant in Regions II, III, and IV.

A comparison of calculated vs. measured activity coefficients in each of the binaries are presented in Figures 32 to 45. The data were divided into approximately 20°R intervals and plotted on separate graphs. The solid lines represent the calculated activity coefficient at the two extremes of temperature. In this comparison the same systematic deviation is observed as in Figures 27 to 31 for the nitrogen-oxygen and nitrogen-argon system, the largest systematic error being approximately 2.5% in the nitrogen-argon system. The oxygen-argon system seems to show no systematic deviations.

A comparison of calculated and measured equilibria in the binary and ternary systems is given in Figures 46 to 82 which show tie lines in a ternary phase diagram at constant temperature and pressure. The figures are ordered

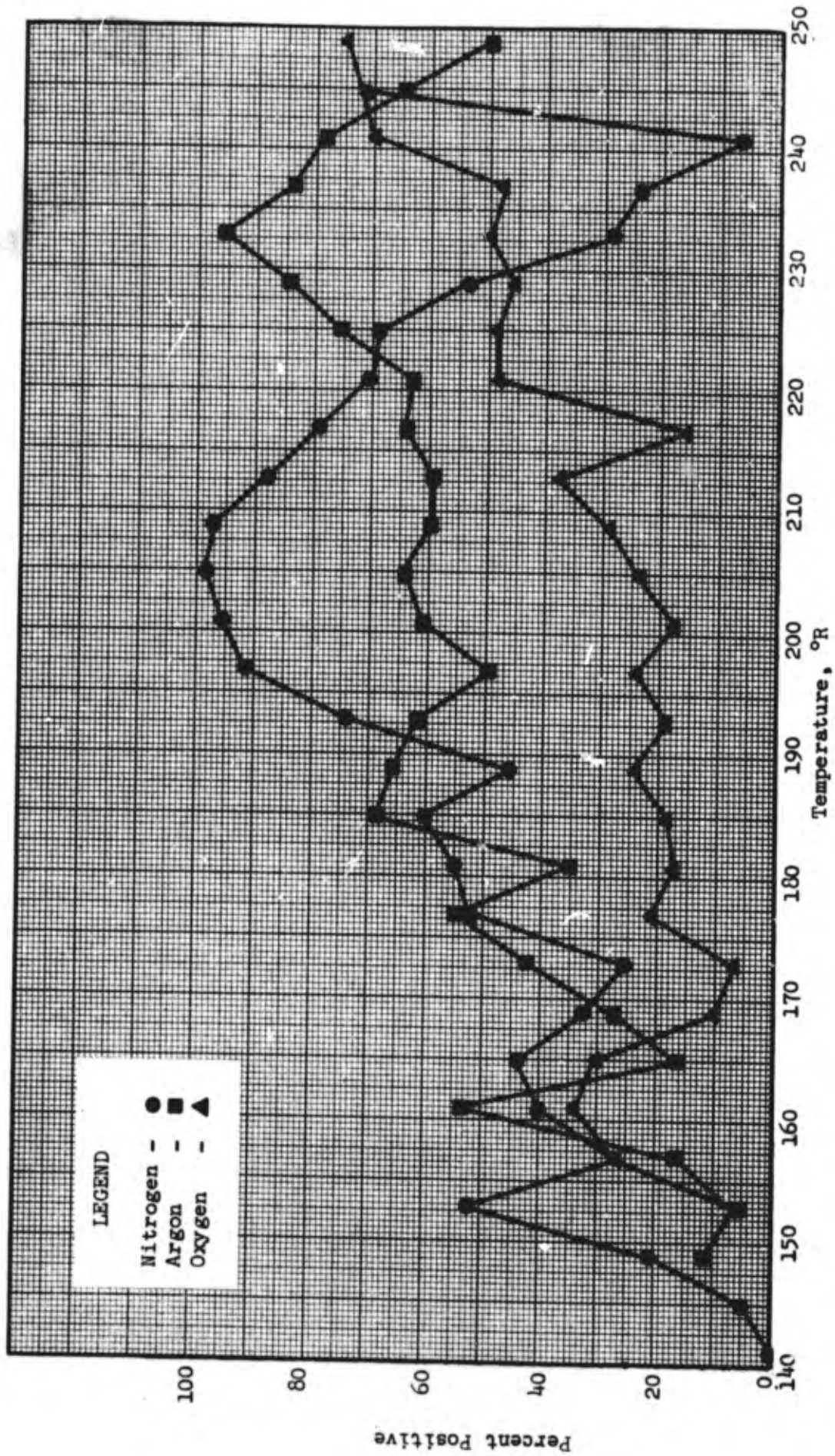


Figure 27. Summary of Bias of Points in Region I.

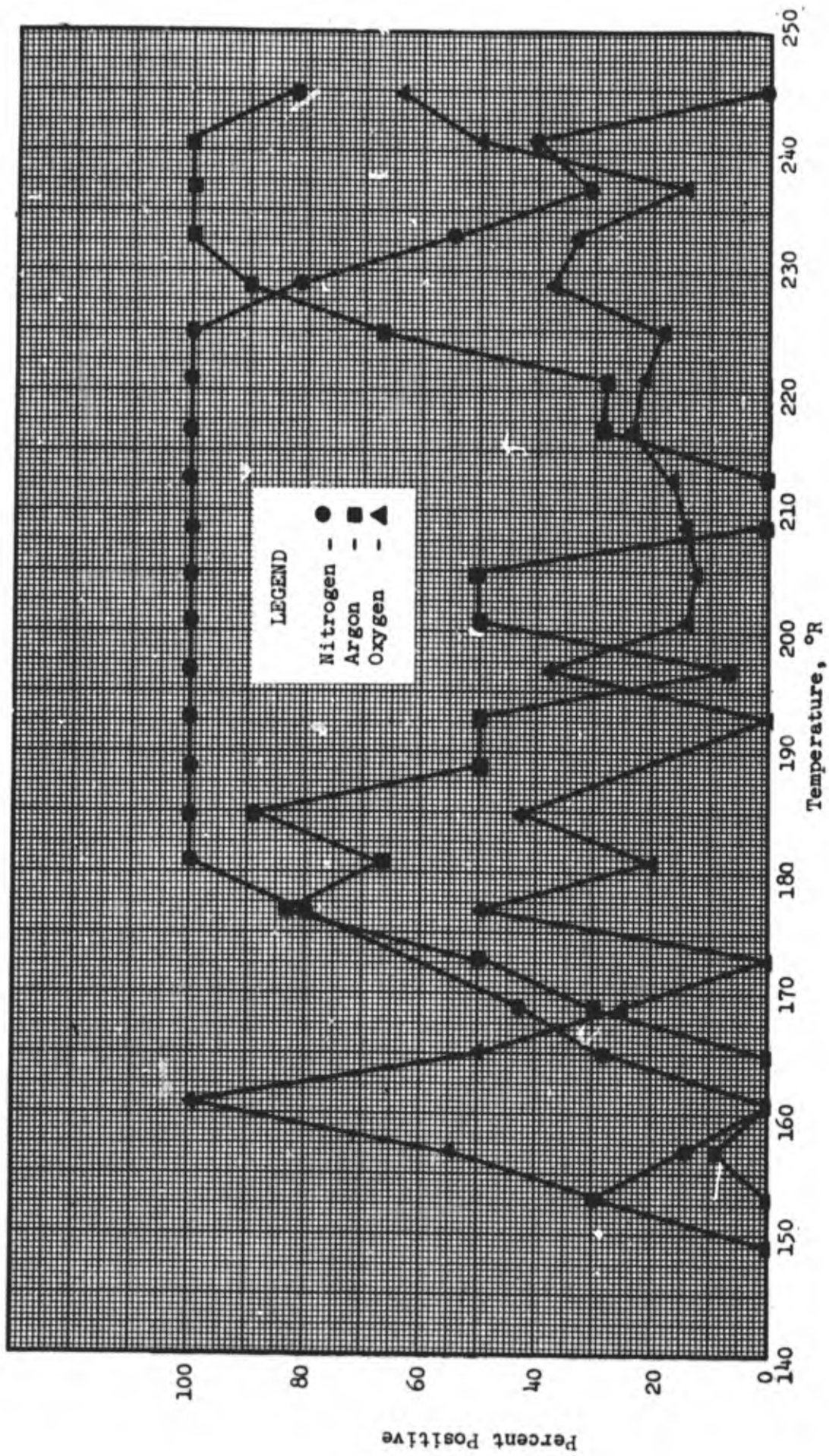


Figure 28. Summary of Bias of Points in Region II.

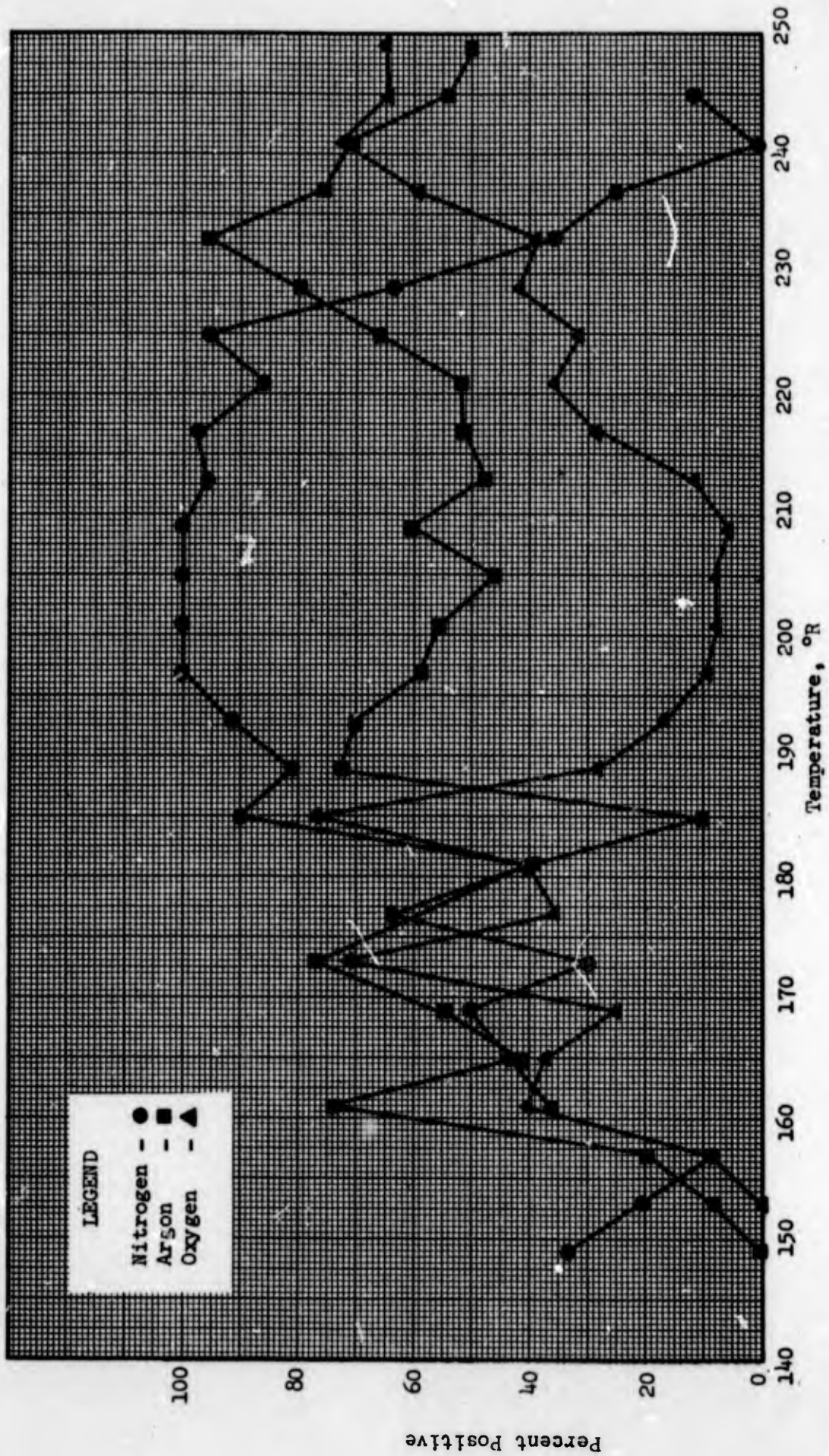


Figure 29. Summary of Bias of Points in Region III.

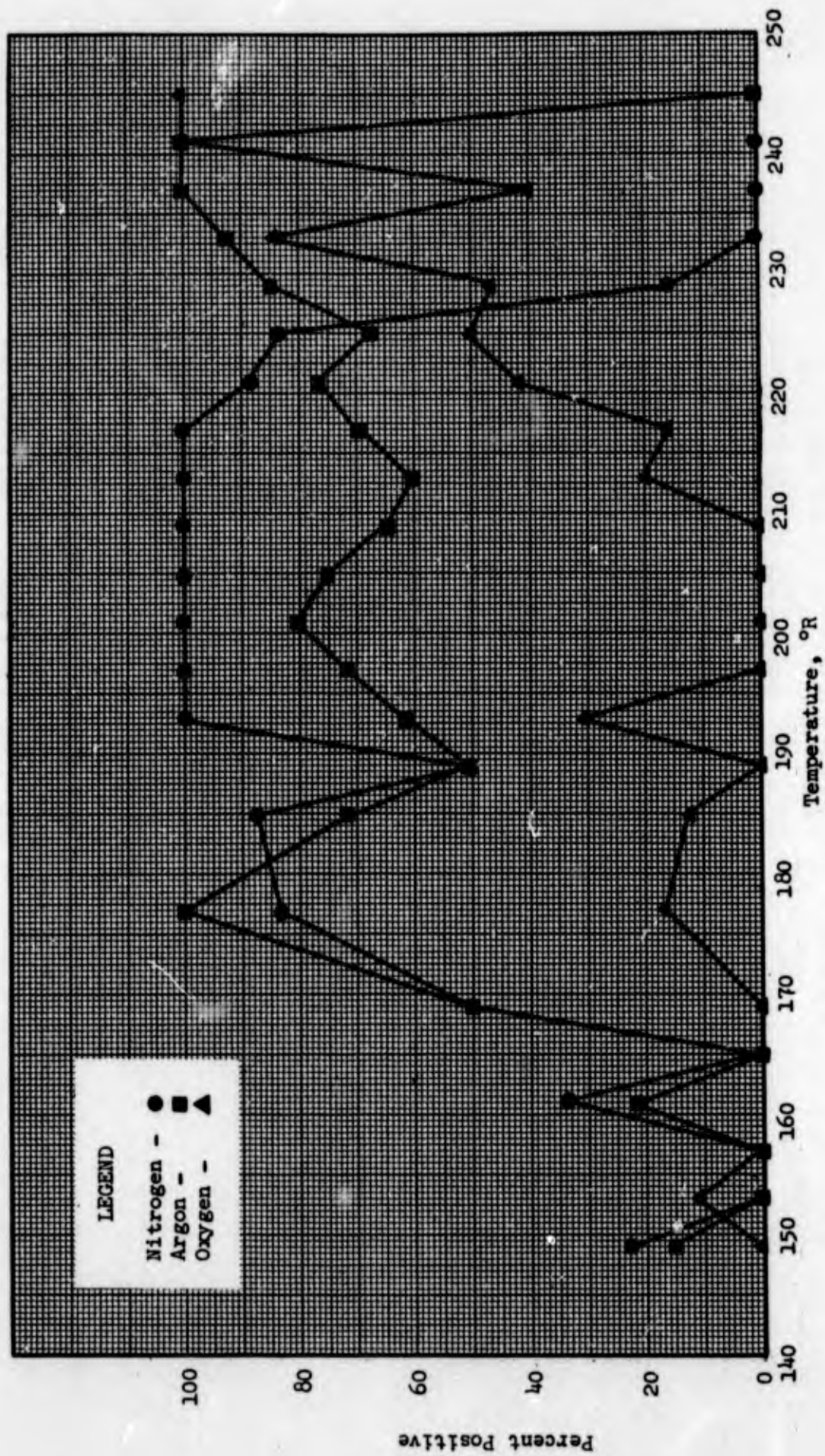


Figure 30. Summary of Bias of Points in Region IV.

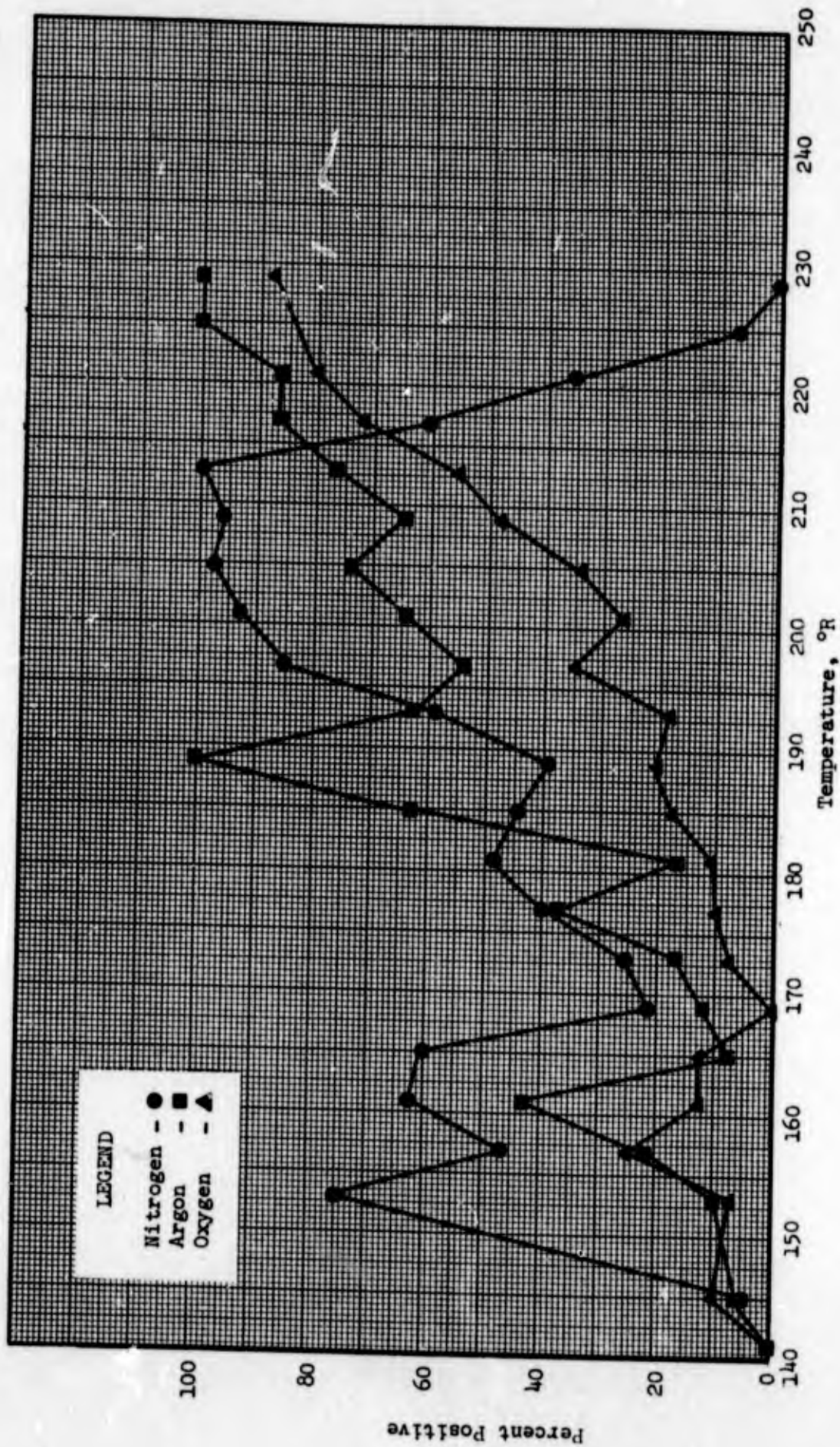


Figure 31. Summary of Bias of Points in all Regions.

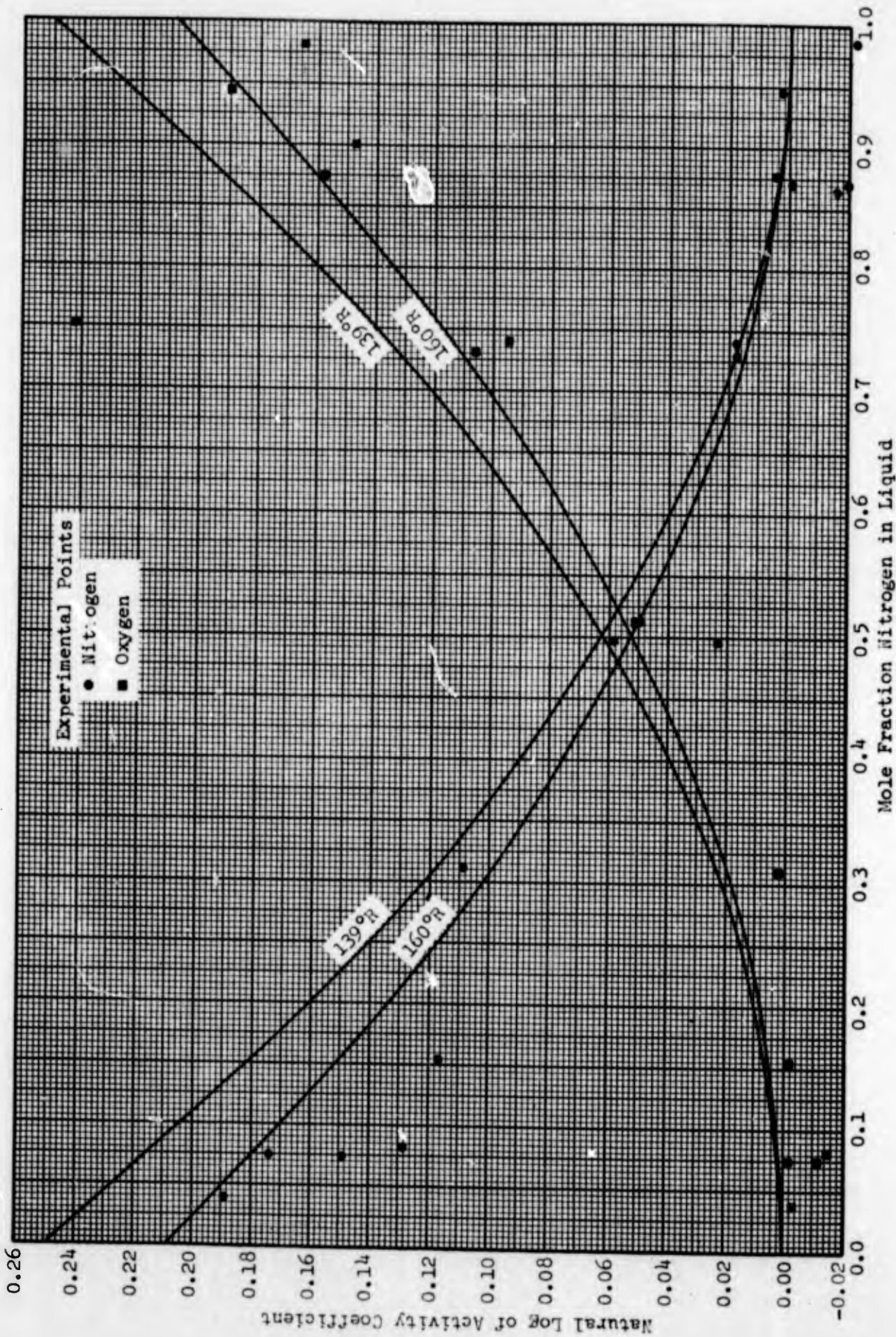


Figure 32. Activity Coefficients in the Nitrogen-Oxygen Binary System, Calculated vs. Experimental.

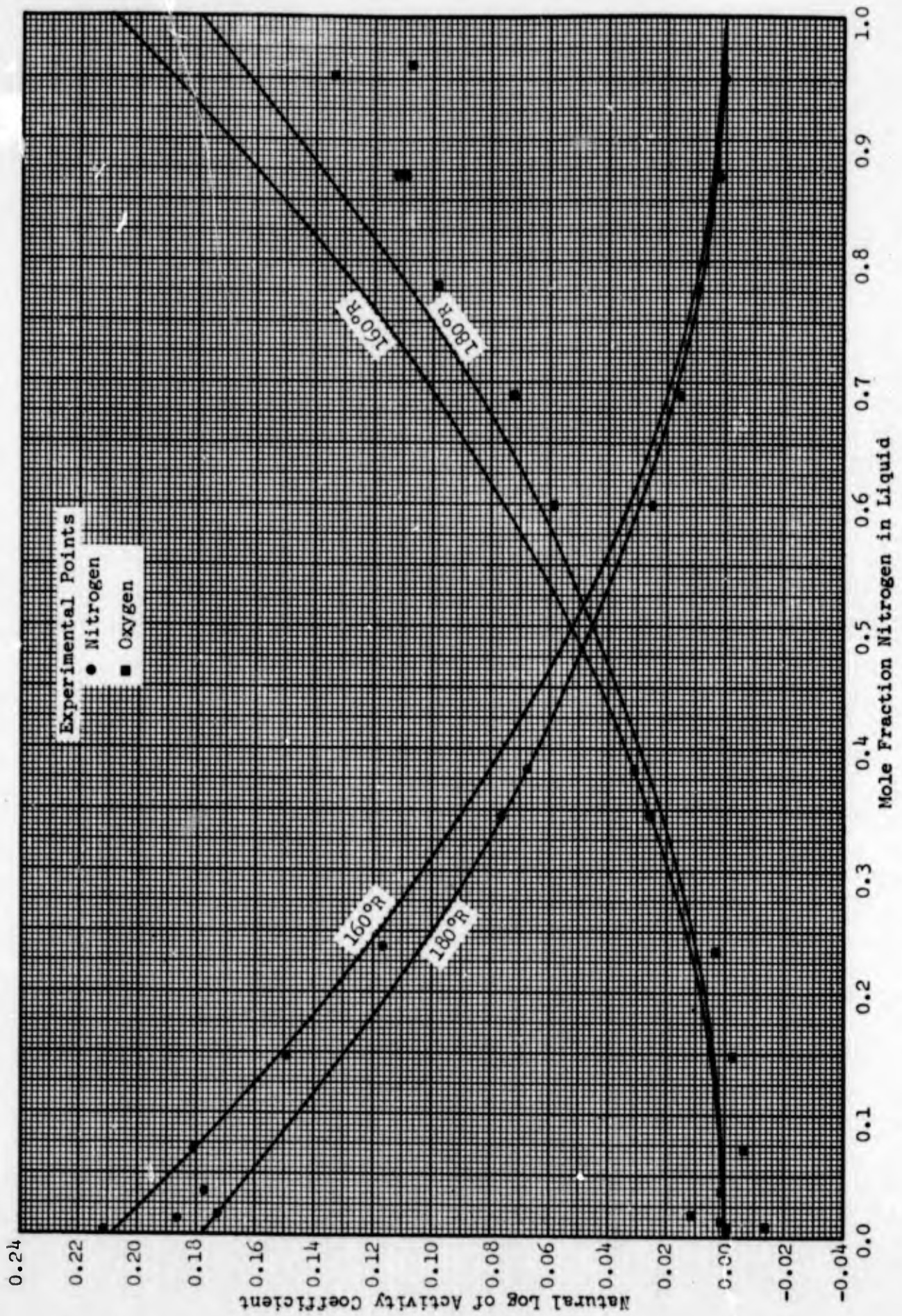


Figure 33. Activity Coefficients in the Nitrogen-Oxygen Binary System, Calculated vs. Experimental.

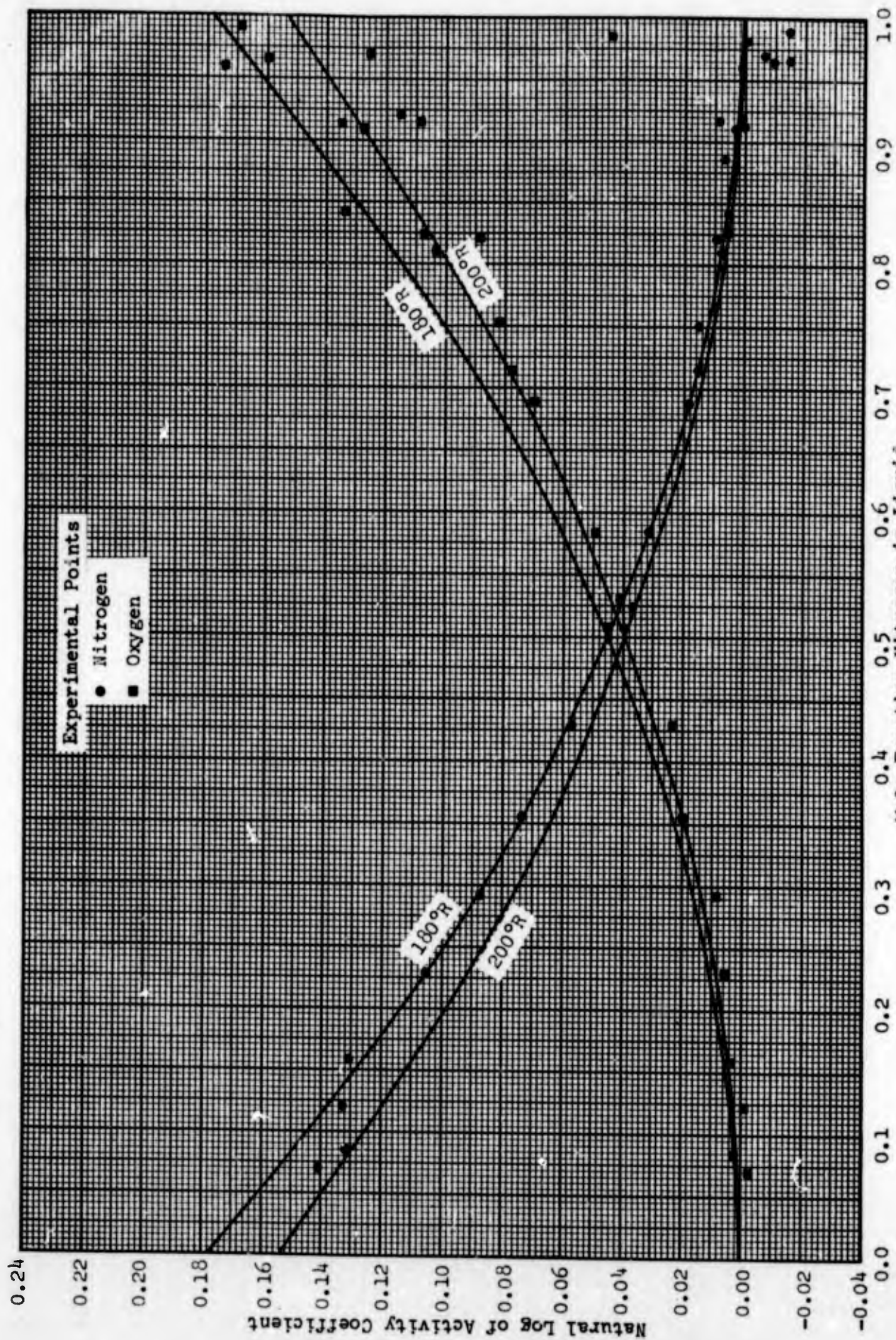


Figure 34. Activity Coefficients in the Nitrogen-Oxygen Binary System, Calculated vs. Experimental.

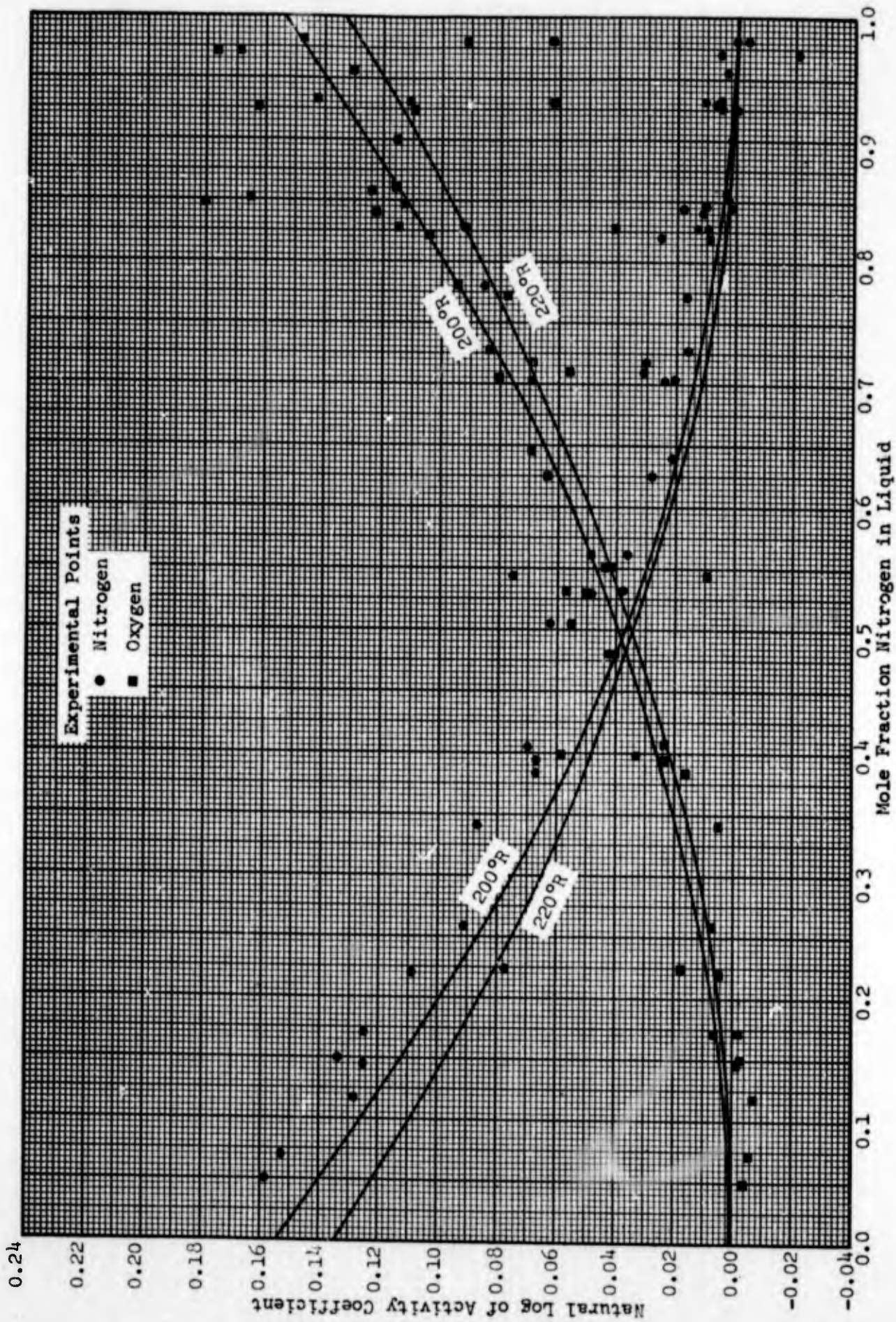


Figure 35. Activity Coefficients in the Nitrogen-Oxygen Binary System, Calculated vs. Experimental.

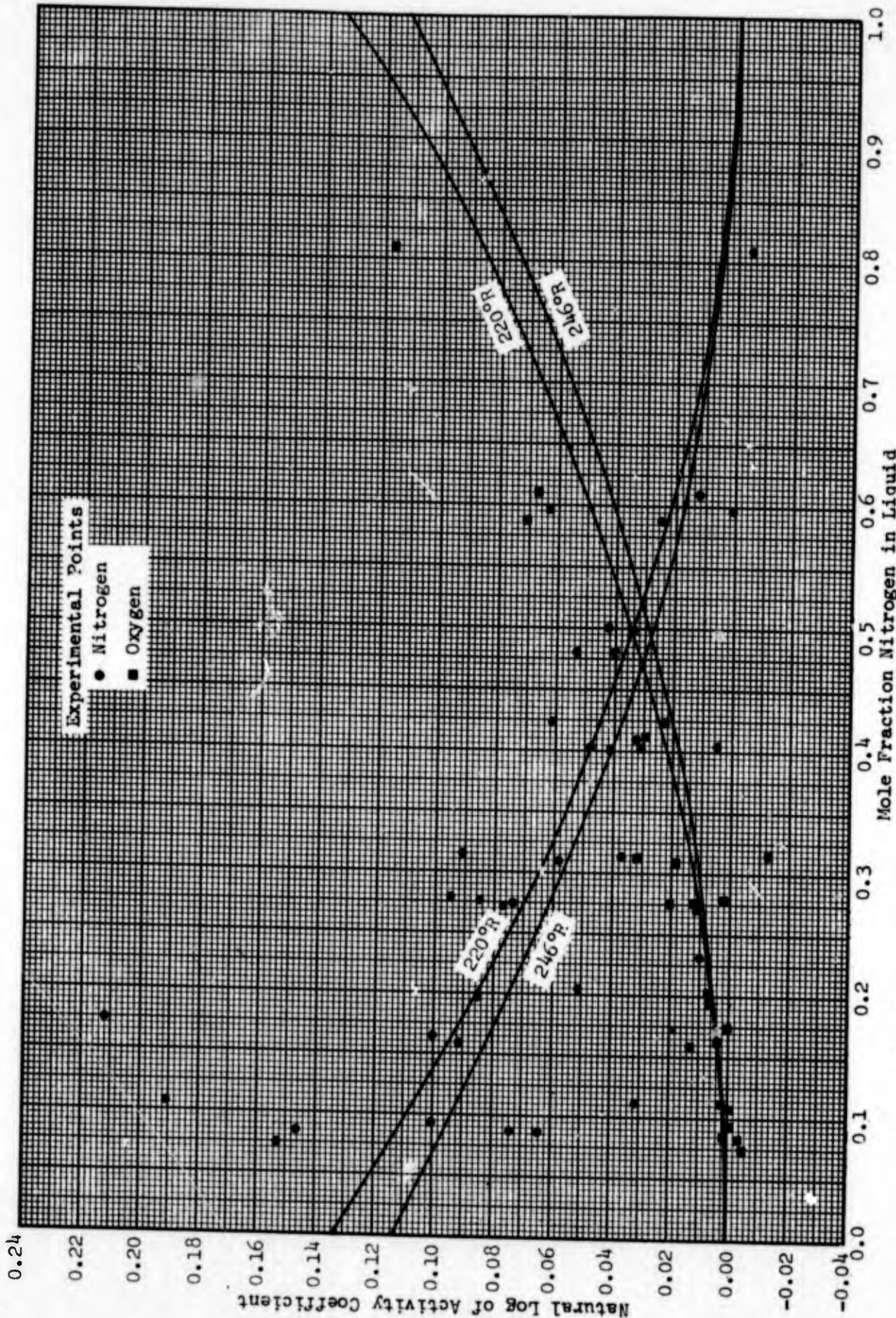


Figure 36. Activity Coefficients in the Nitrogen-Oxygen Binary System, Calculated vs. Experimental.

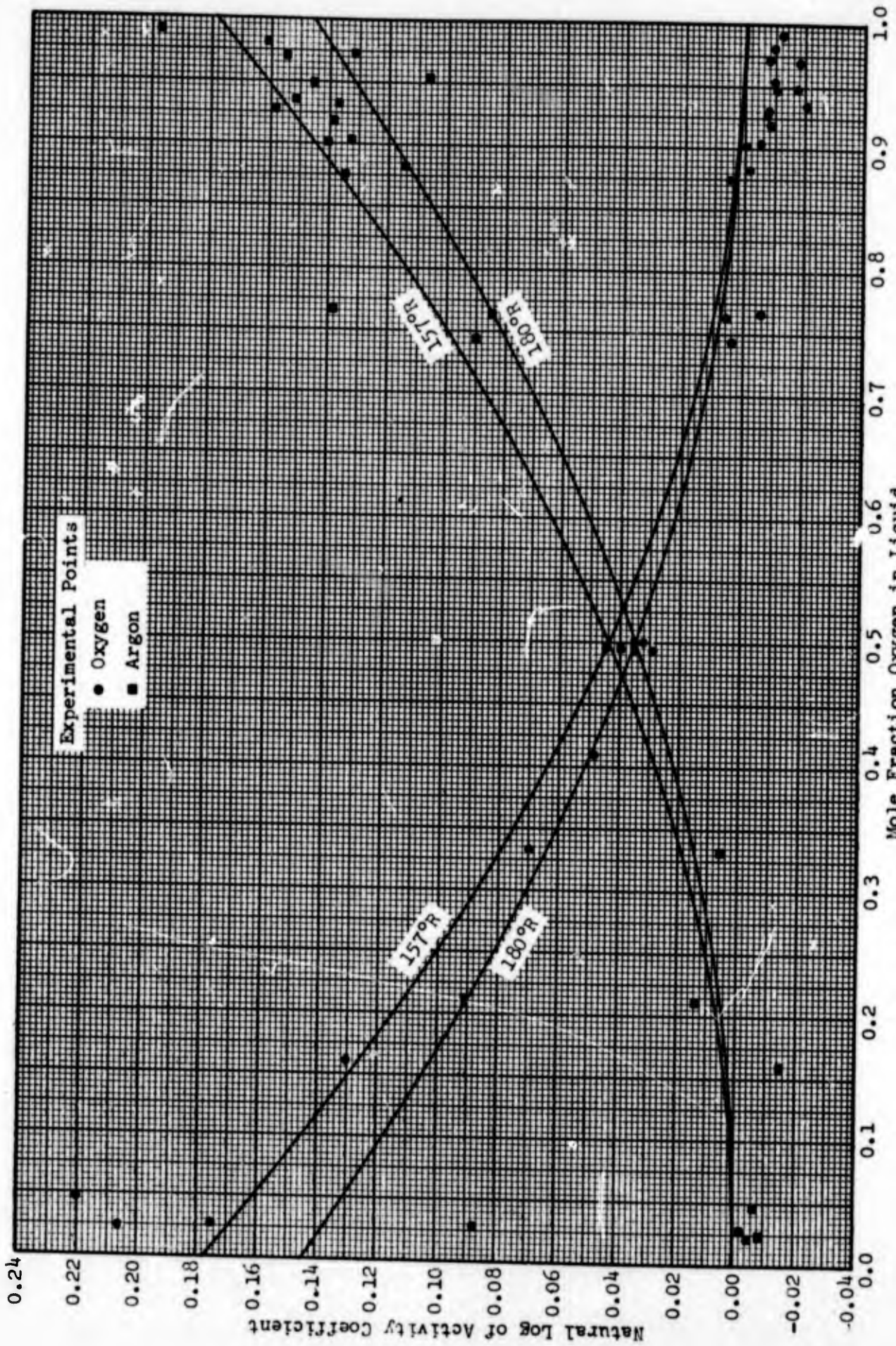


Figure 37. Activity Coefficients in the Oxygen-Argon Binary System, Calculated vs. Experimental.

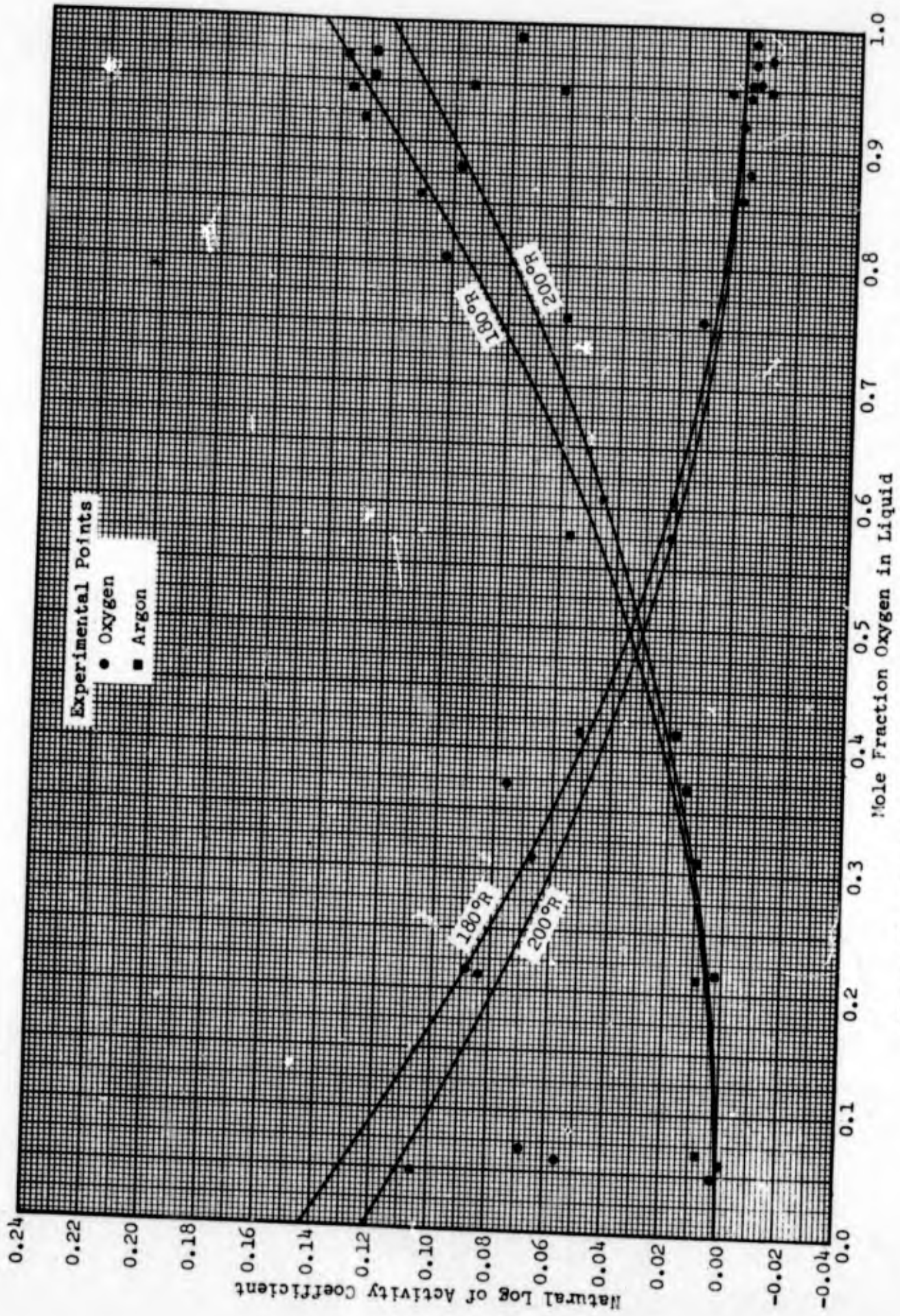


Figure 38. Activity Coefficients in the Oxygen-Argon Binary System, Calculated vs. Experimental.

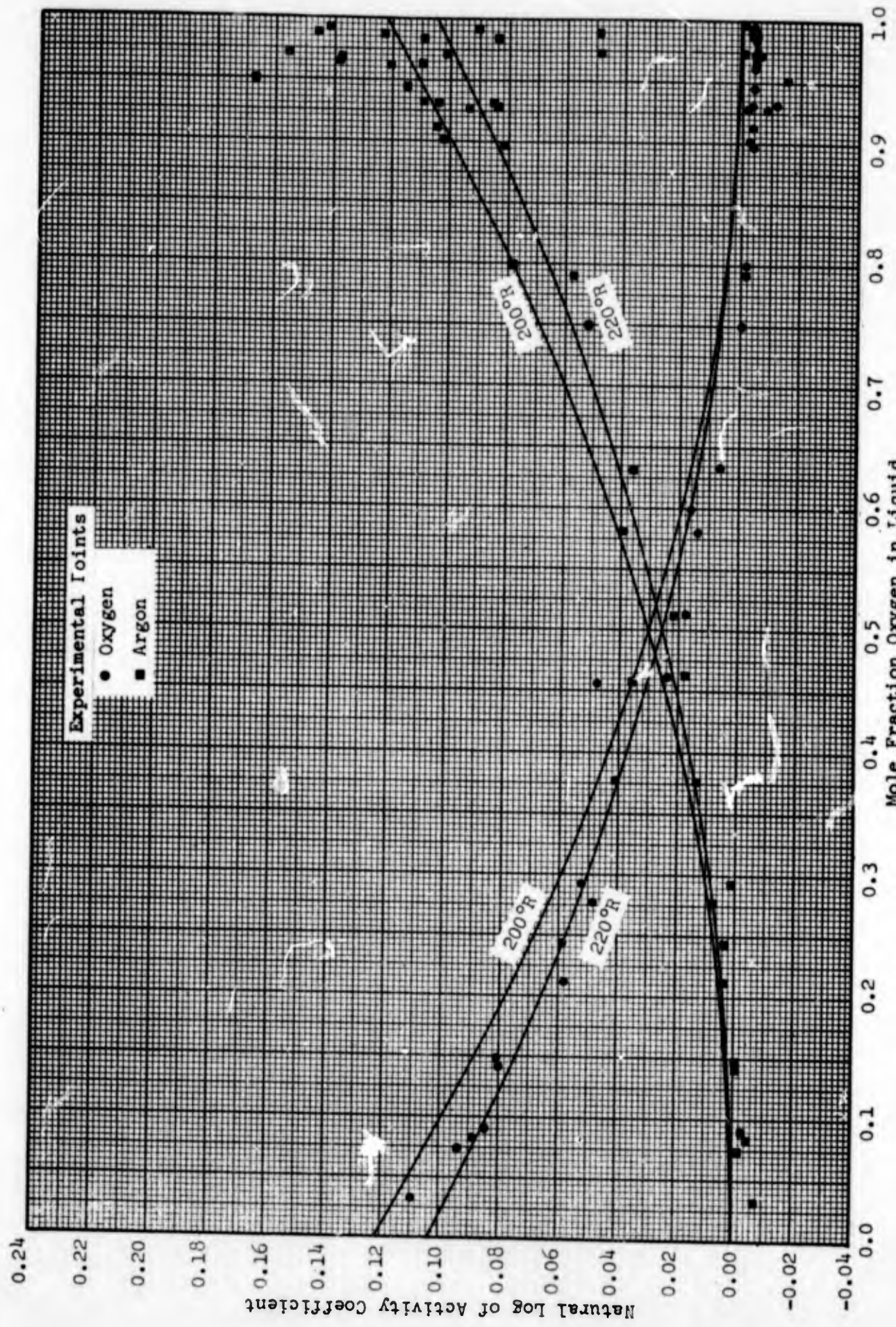


Figure 39. Activity Coefficients in the Oxygen-Argon Binary System, Calculated vs. Experimental.

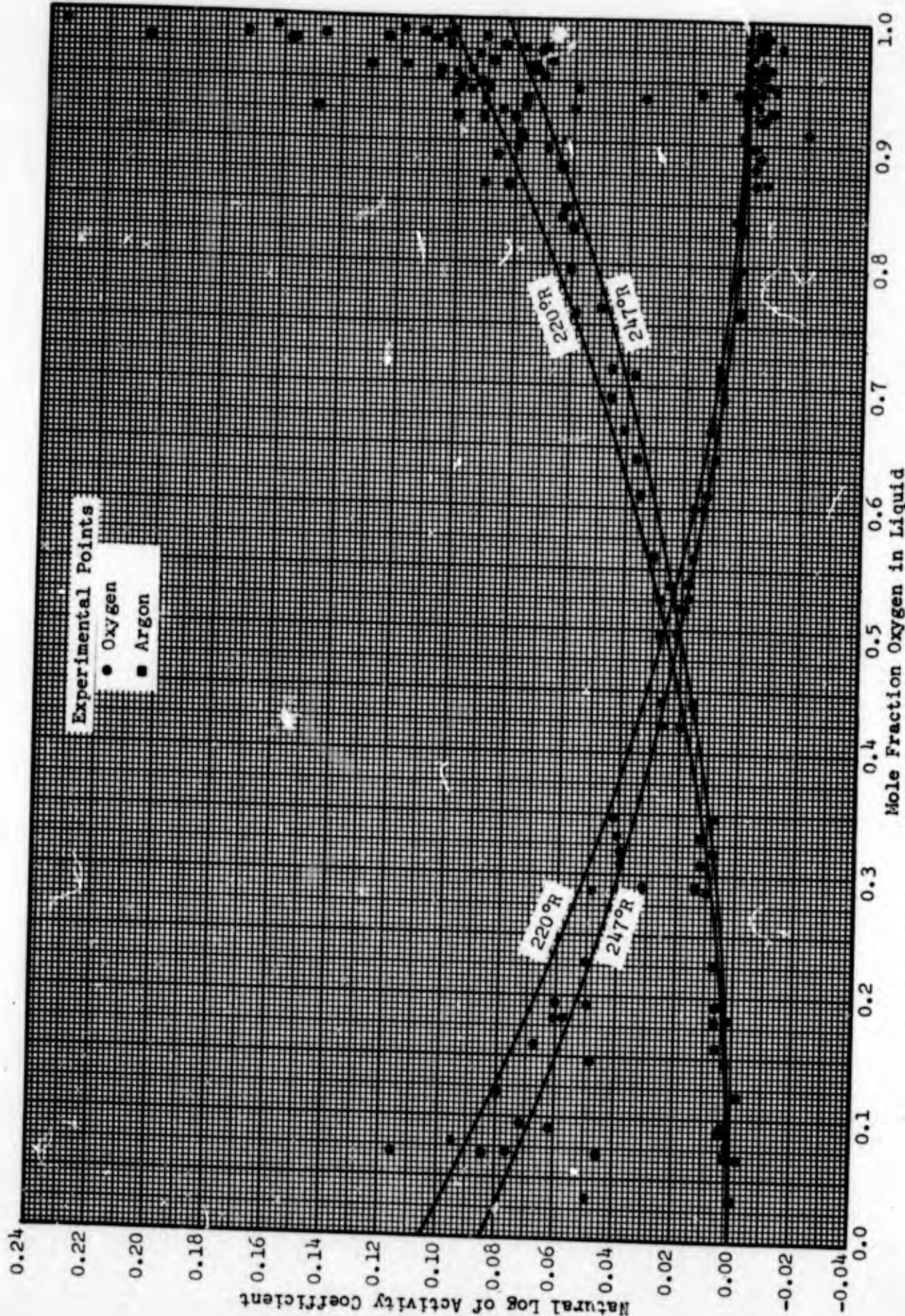


Figure 40. Activity Coefficients in the Oxygen-Argon Binary System, Calculated vs. Experimental.

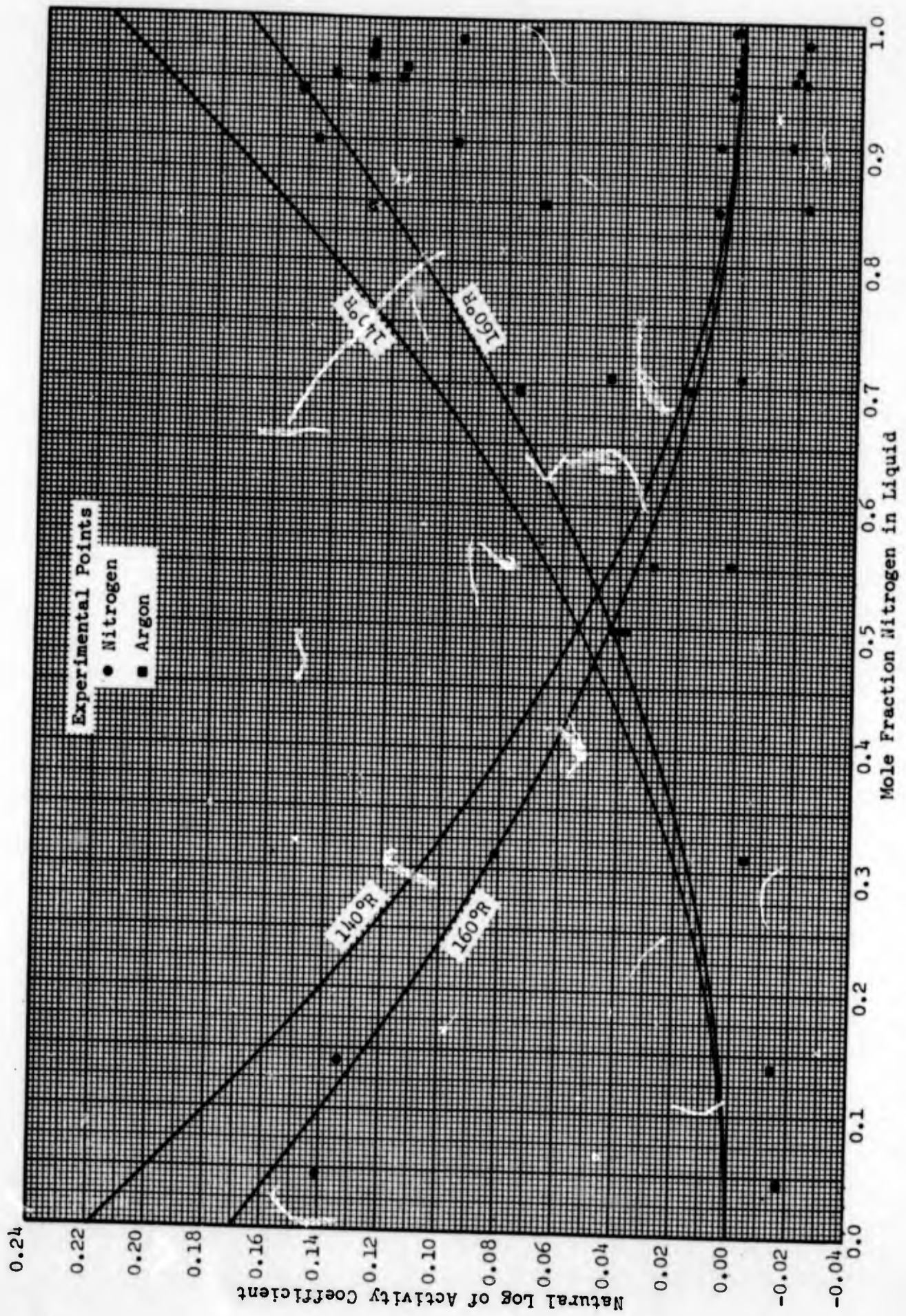


Figure 41. Activity Coefficients in the Nitrogen-Argon Binary System, Calculated vs. Experimental.

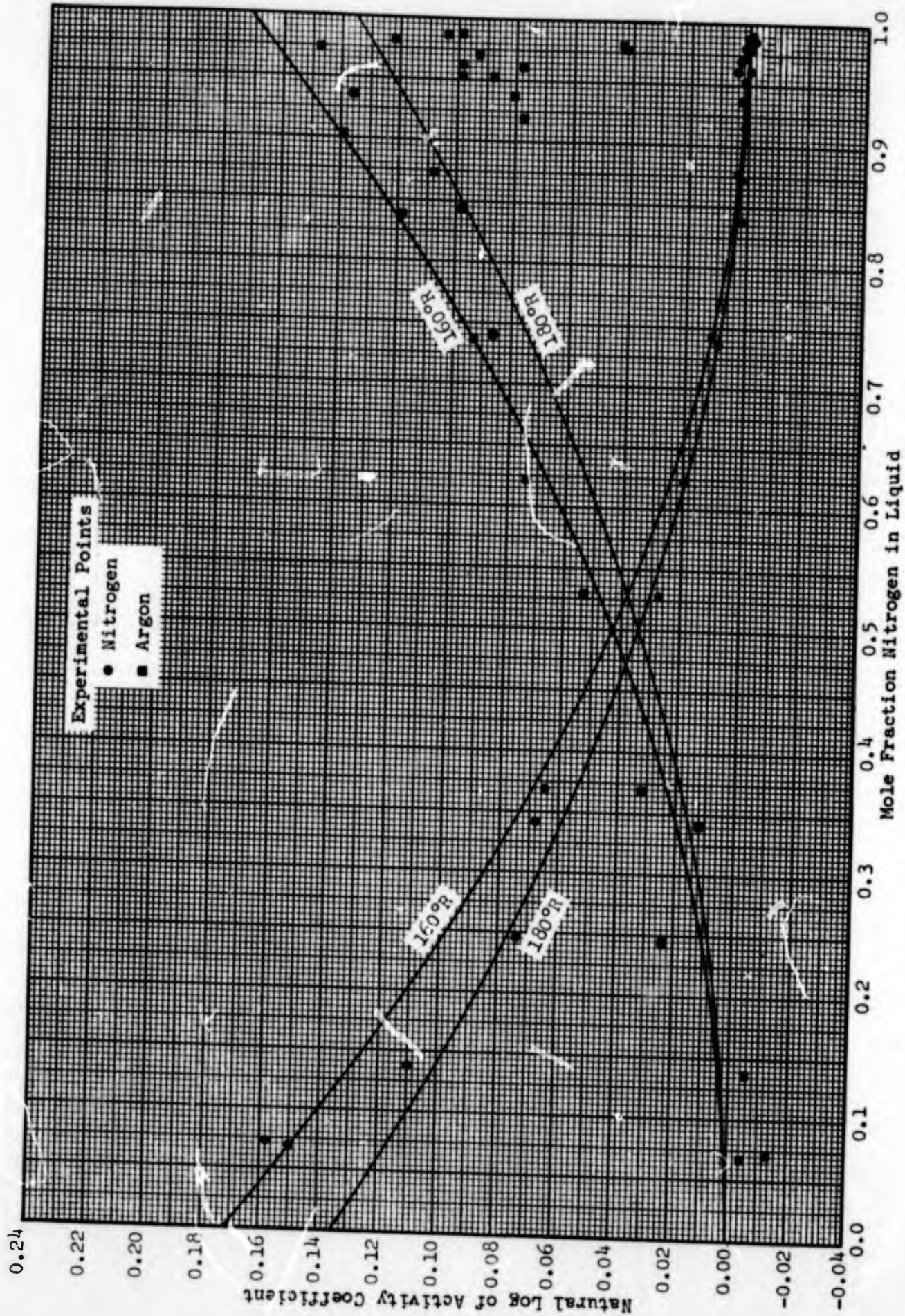


Figure 42. Activity Coefficients in the Nitrogen-Argon Binary System, Calculated vs. Experimental.

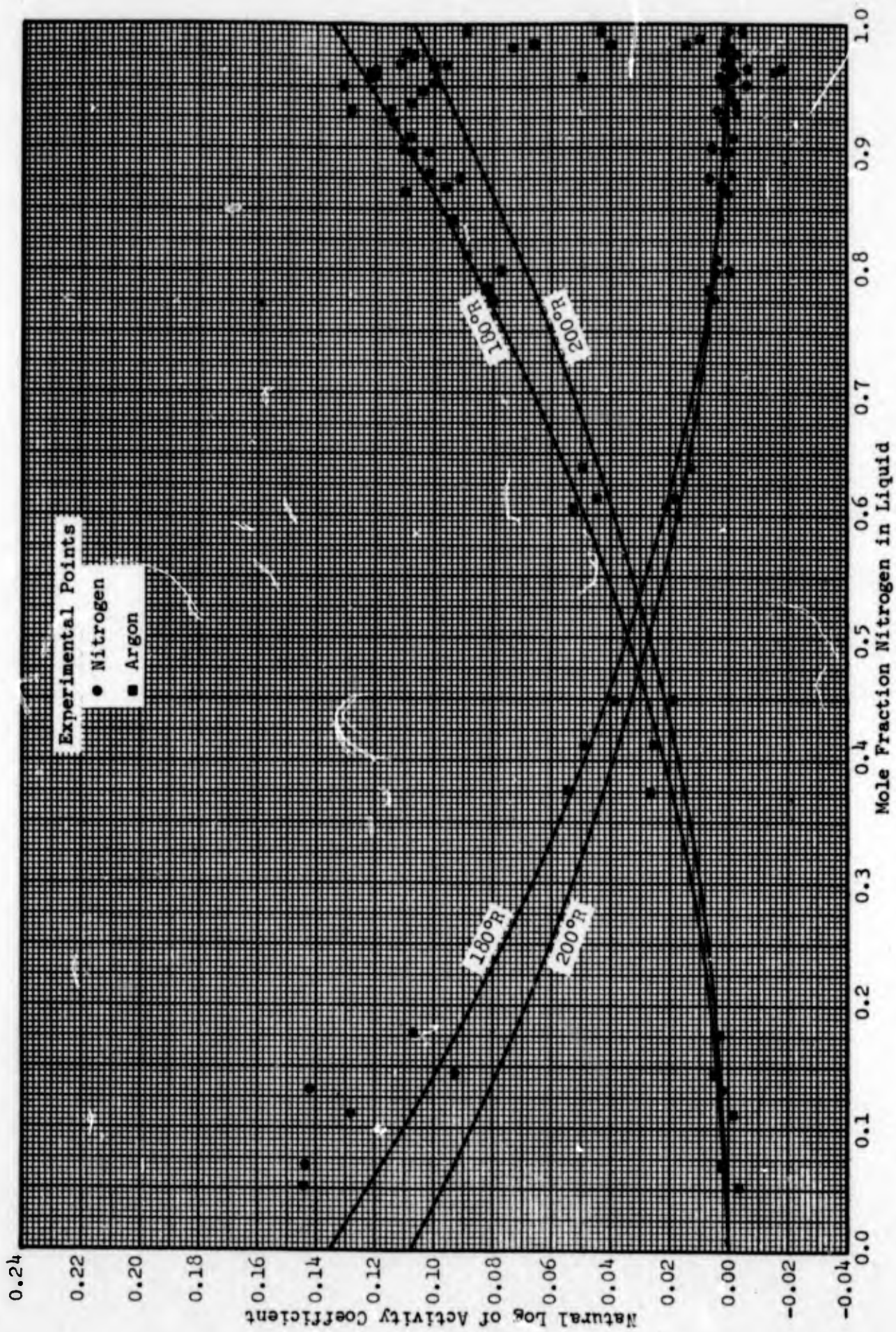


Figure 43. Activity Coefficients in the Nitrogen-Argon Binary System, Calculated vs. Experimental.

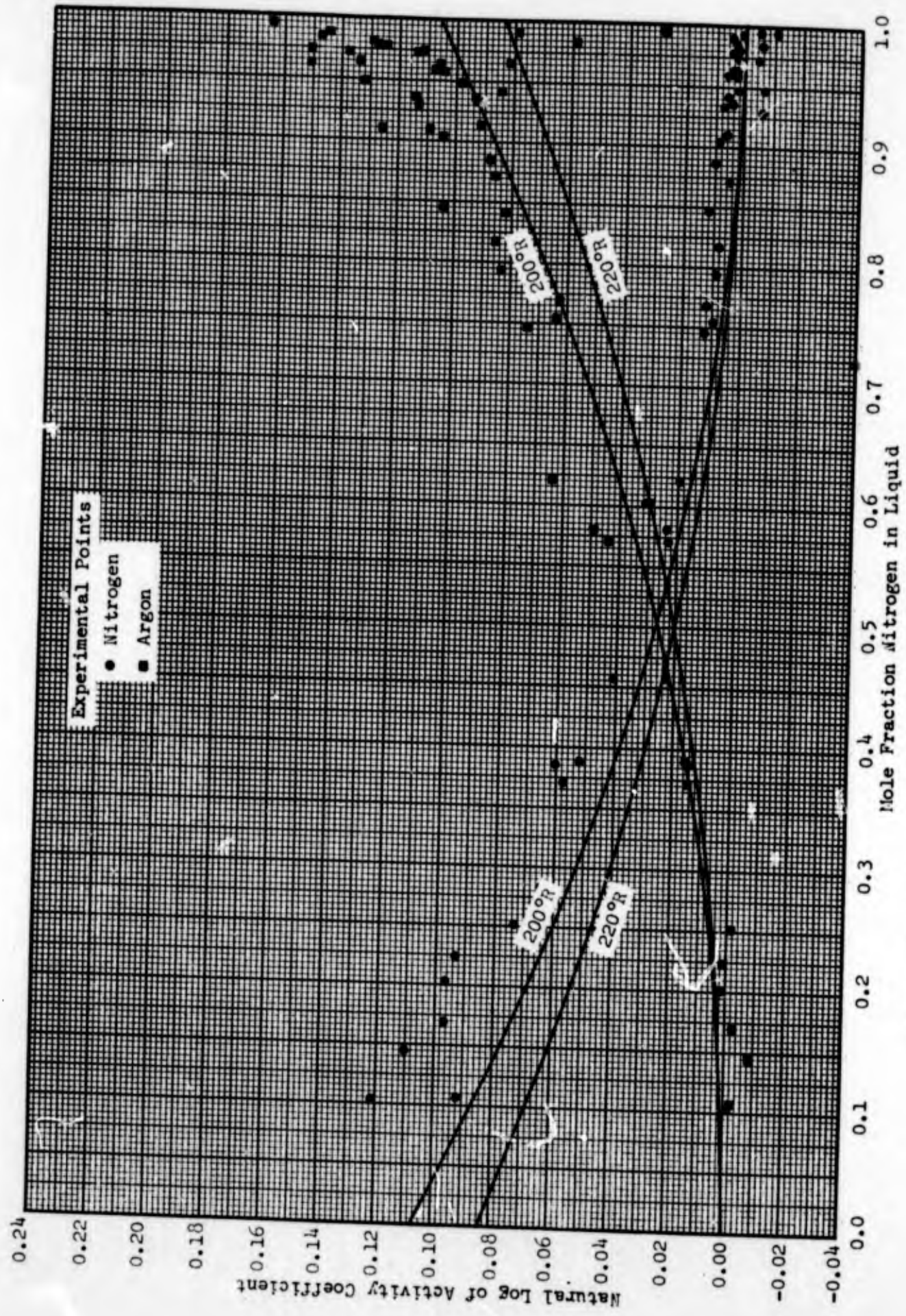


Figure 44. Activity Coefficients in the Nitrogen-Argon Binary Systems, Calculated vs. Experimental.

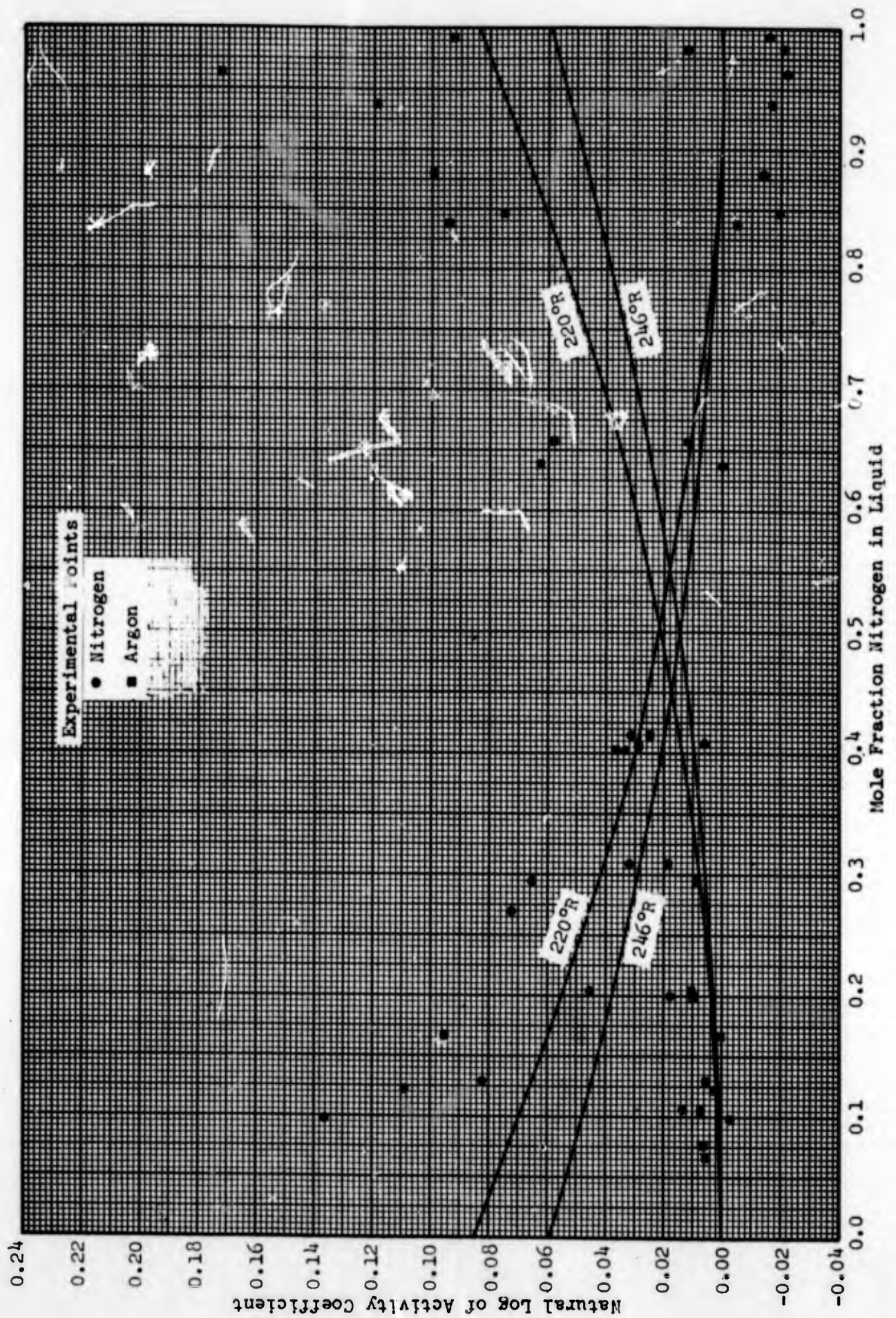


Figure 45. Activity Coefficients in the Nitrogen-Argon Binary System, Calculated vs. Experimental.

according to increasing pressure. The liquid phase corresponds to tie line points on the left and the vapor phase corresponds to tie line points on the right, and lines have been drawn connecting all points in both phases. These data show systematic deviations consistent with the deviations in activity coefficients. The largest error occurs at 20 atm where the difference corresponds to an error of 2.5% in the calculation of the pressure.

From an examination of the differences between calculated and measured data it is concluded that the correlation represents the data with a difference less than 2.5% in relative volatility and pressure in most regions. The largest difference is probably about 2.5%. The experimental data scatter less than this with an accuracy of about $\pm 0.5\%$ in the pressure and $\pm 1\%$ in the relative volatility.

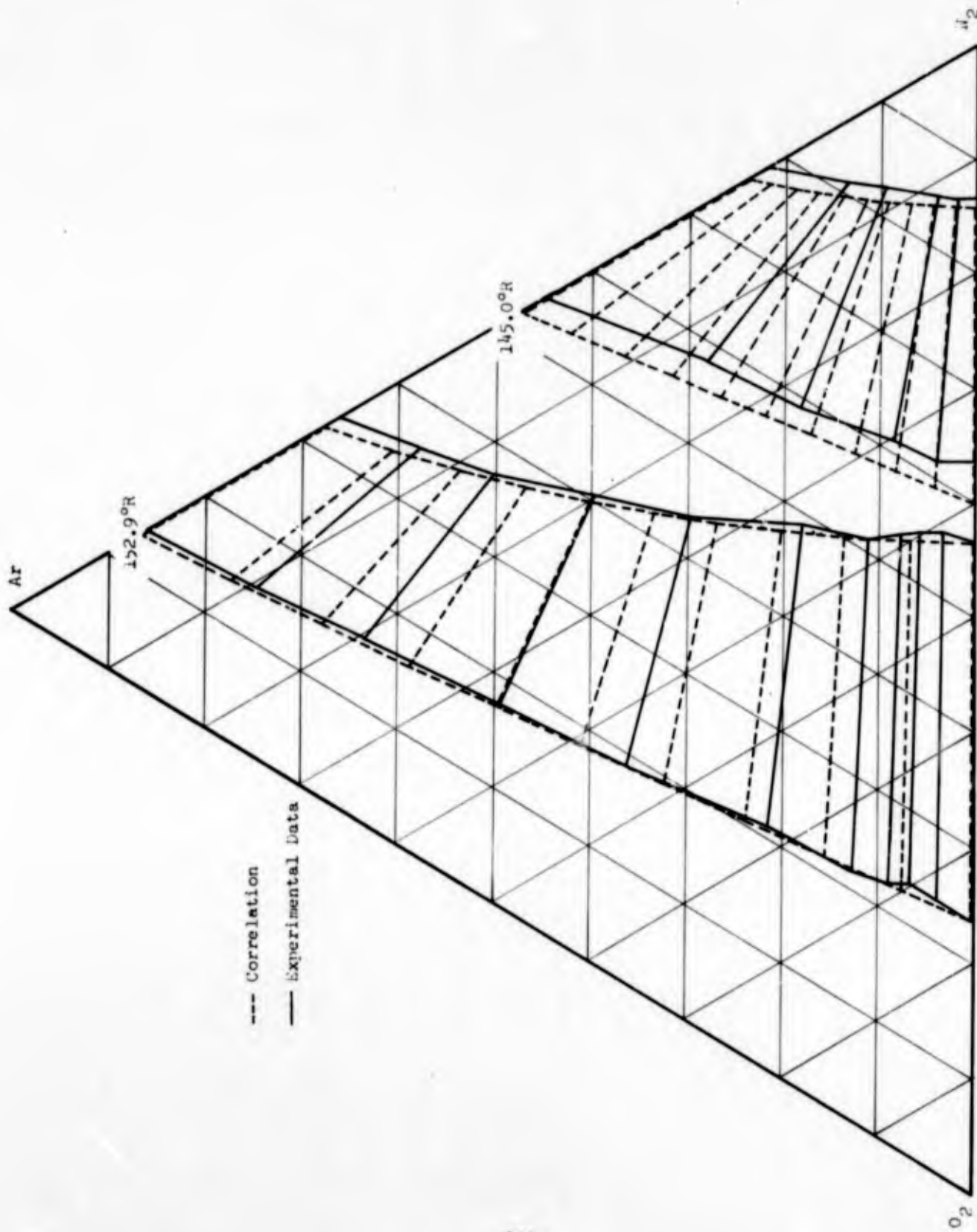
A comparison of the correlation with literature data can probably be best made in terms of comparisons with the Latimer⁽³⁴⁾ correlation, since it represents a good summary of existing data. This comparison is given in Figures 83 to 85 for each of the binary systems. In the nitrogen-oxygen system the difference varies up to about 2% depending on the composition and pressure. In the nitrogen-argon system the difference varies up to 10% at 20 atm, and in the argon-oxygen system the difference varies up to about 5%.

Factors which influence this correlation are:

1. The properties of "liquid" nitrogen above the critical temperature of nitrogen.
2. The partial molar volume of the components at pressures approaching the critical pressure of a mixture.
3. The assumption of a separate free energy expression for the vapor phase and the liquid phase.

These factors are inherent problems in the correlation of data by means of activity coefficients based upon the pure liquid component as the standard state. The systematic errors observed with this correlation probably are due to the uncertainty of these factors.

An alternate but more difficult approach would be to correlate the data in terms of an equation of state applicable to both the vapor and the liquid phases. This method would eliminate the need for a pure liquid reference state. The partial molar volume could be calculated from the equation of state, and the free energy equation would be continuous in going from vapor to liquid.



--- Correlation
 — Experimental Data

Figure 46. Comparison of Experimental Data and the Correlation, 1 Atmosphere.

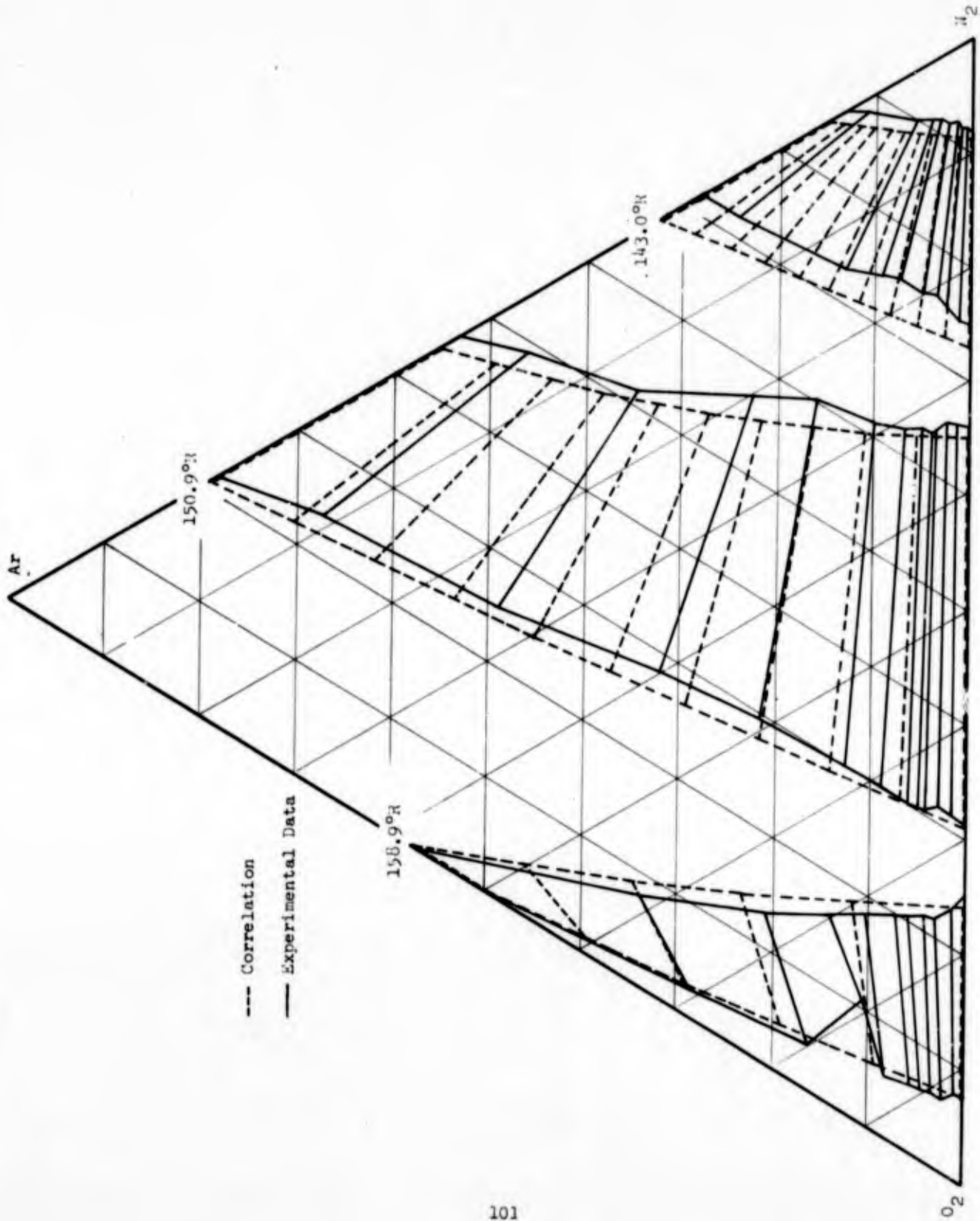


Figure 47. Comparison of Experimental Data and the Correlation, 1 Atmosphere.

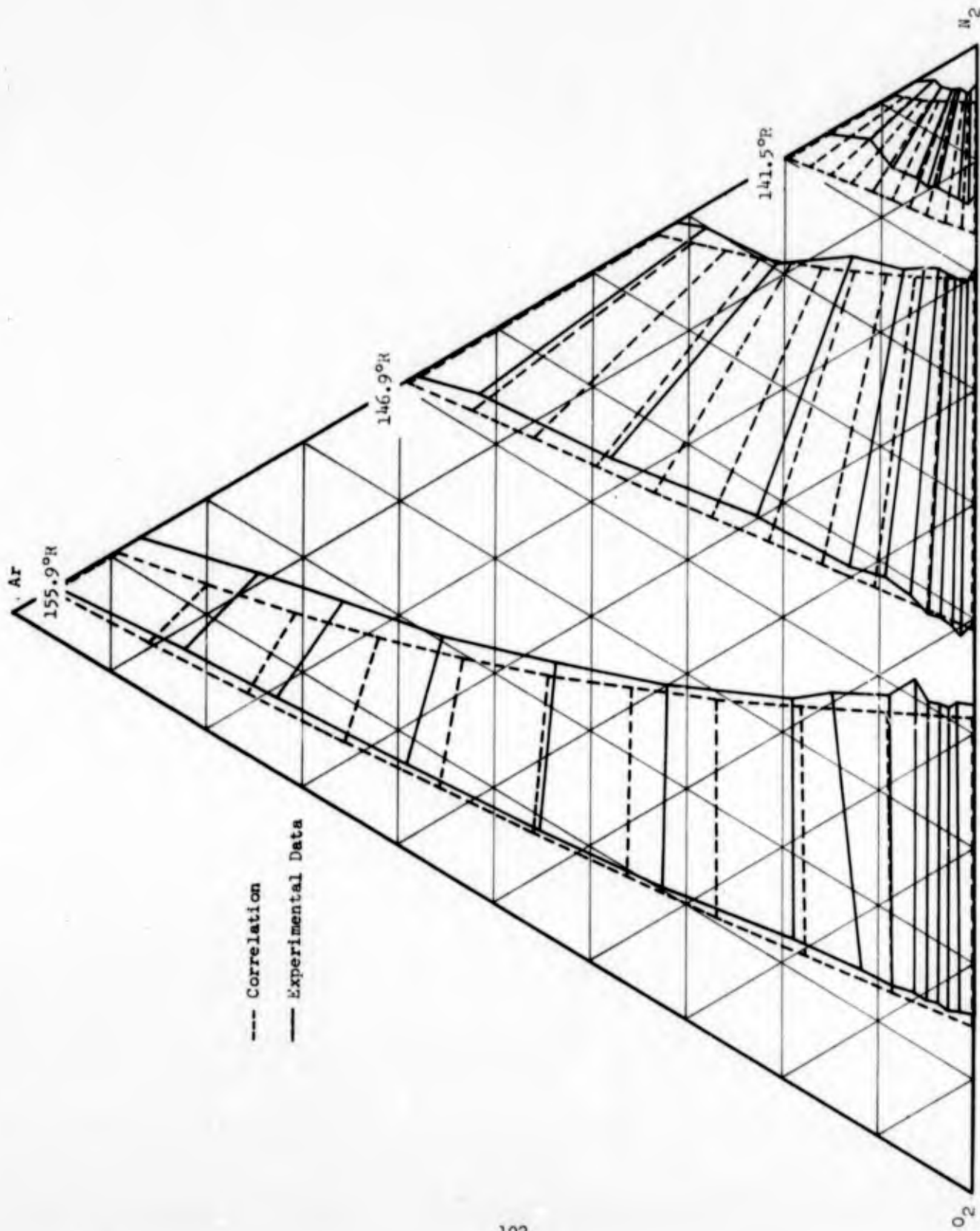


Figure 48. Comparison of Experimental Data and the Correlation, 1 Atmosphere.

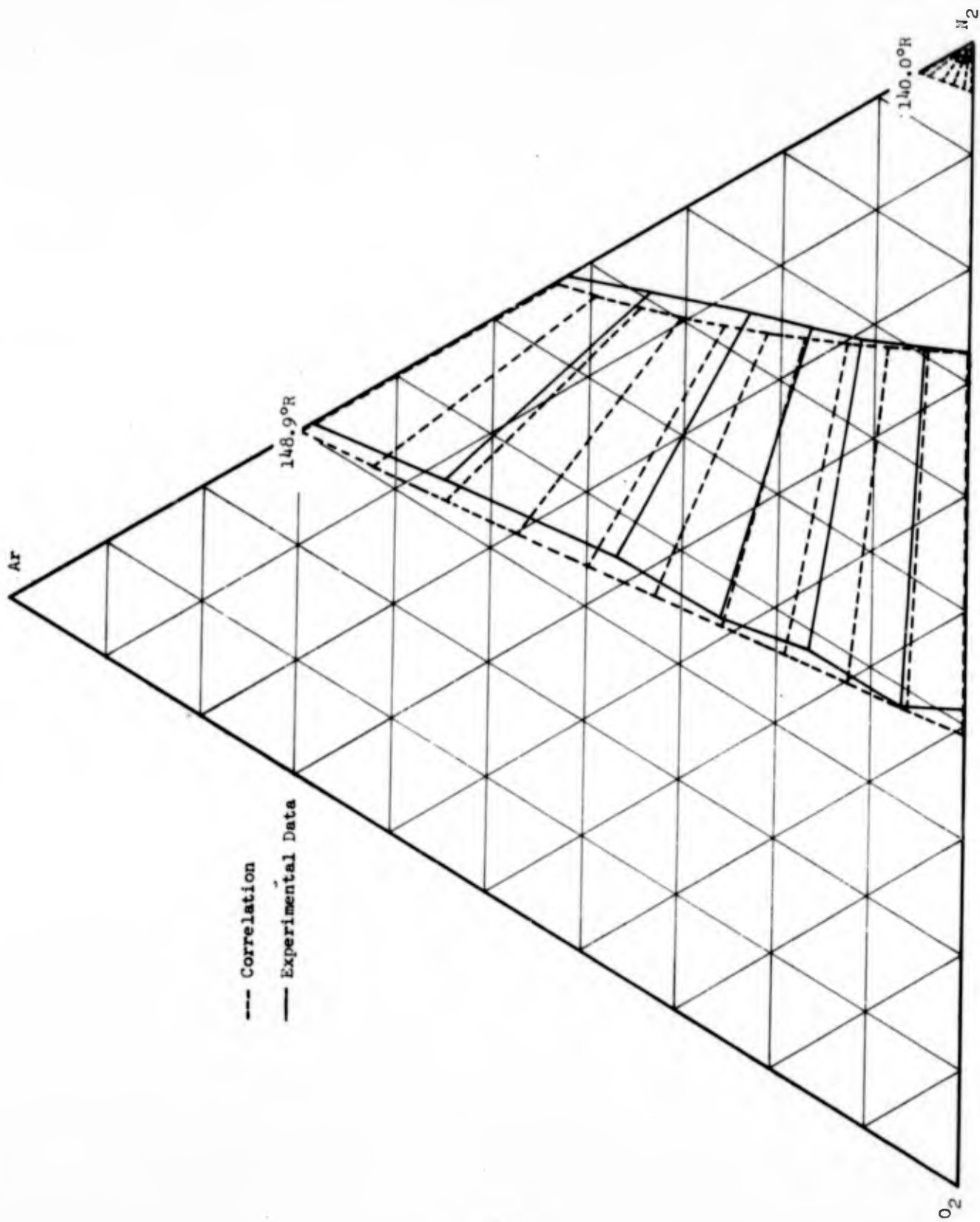


Figure 49. Comparison of Experimental Data and the Correlation, 1 Atmosphere.

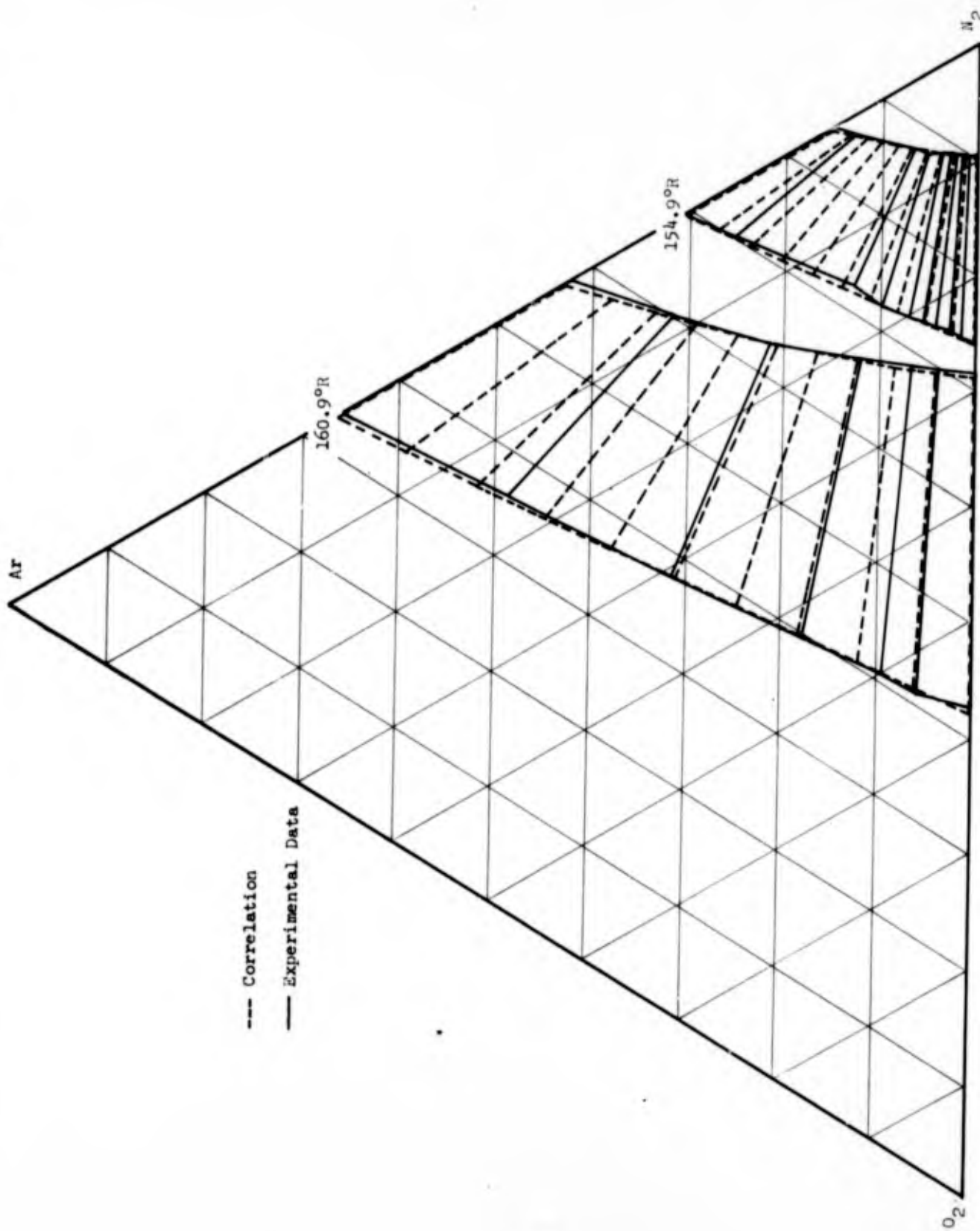


Figure 50. Comparison of Experimental Data and the Correlation, 2 Atmospheres.

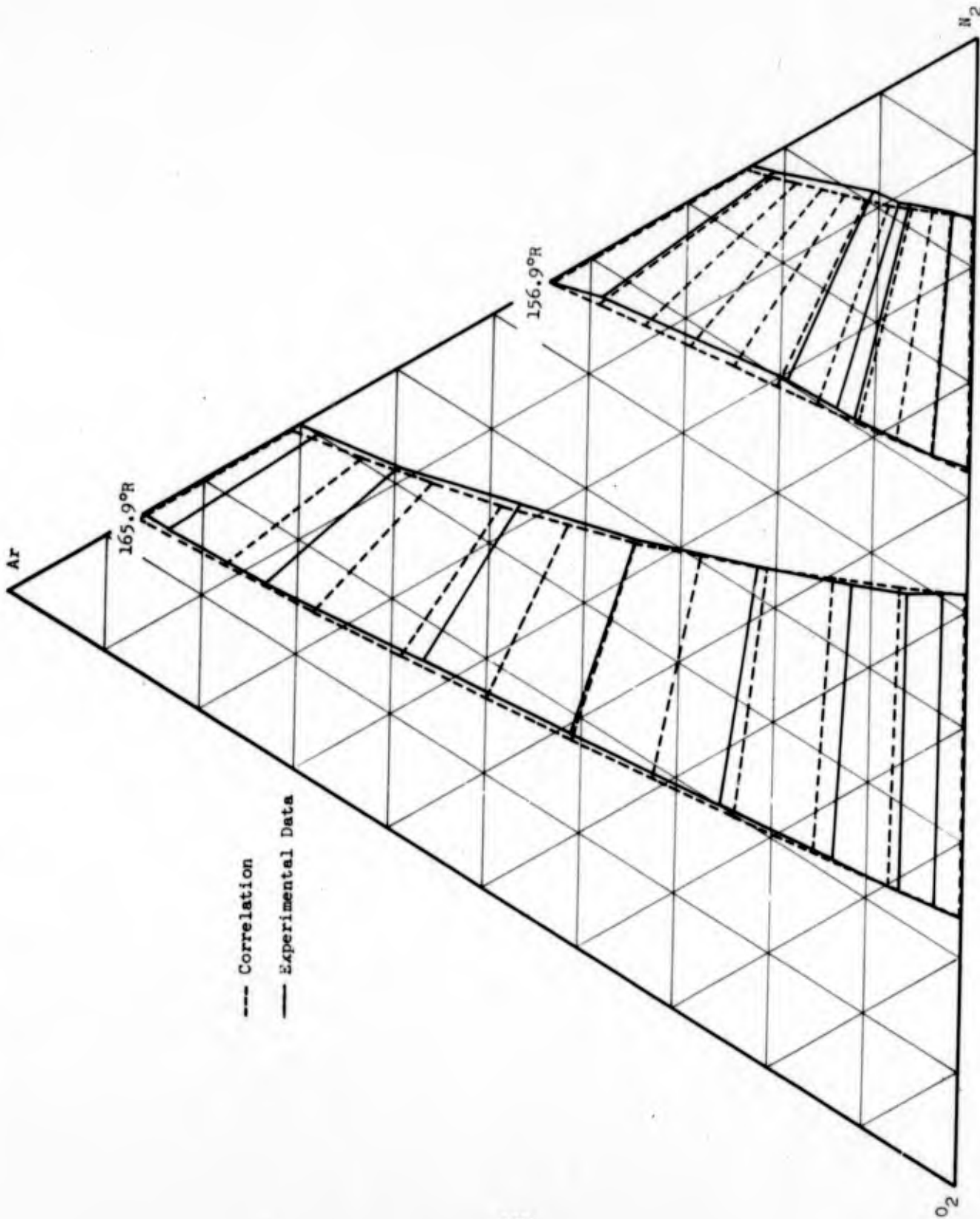


Figure 51. Comparison of Experimental Data and the Correlation, 2 Atmospheres.

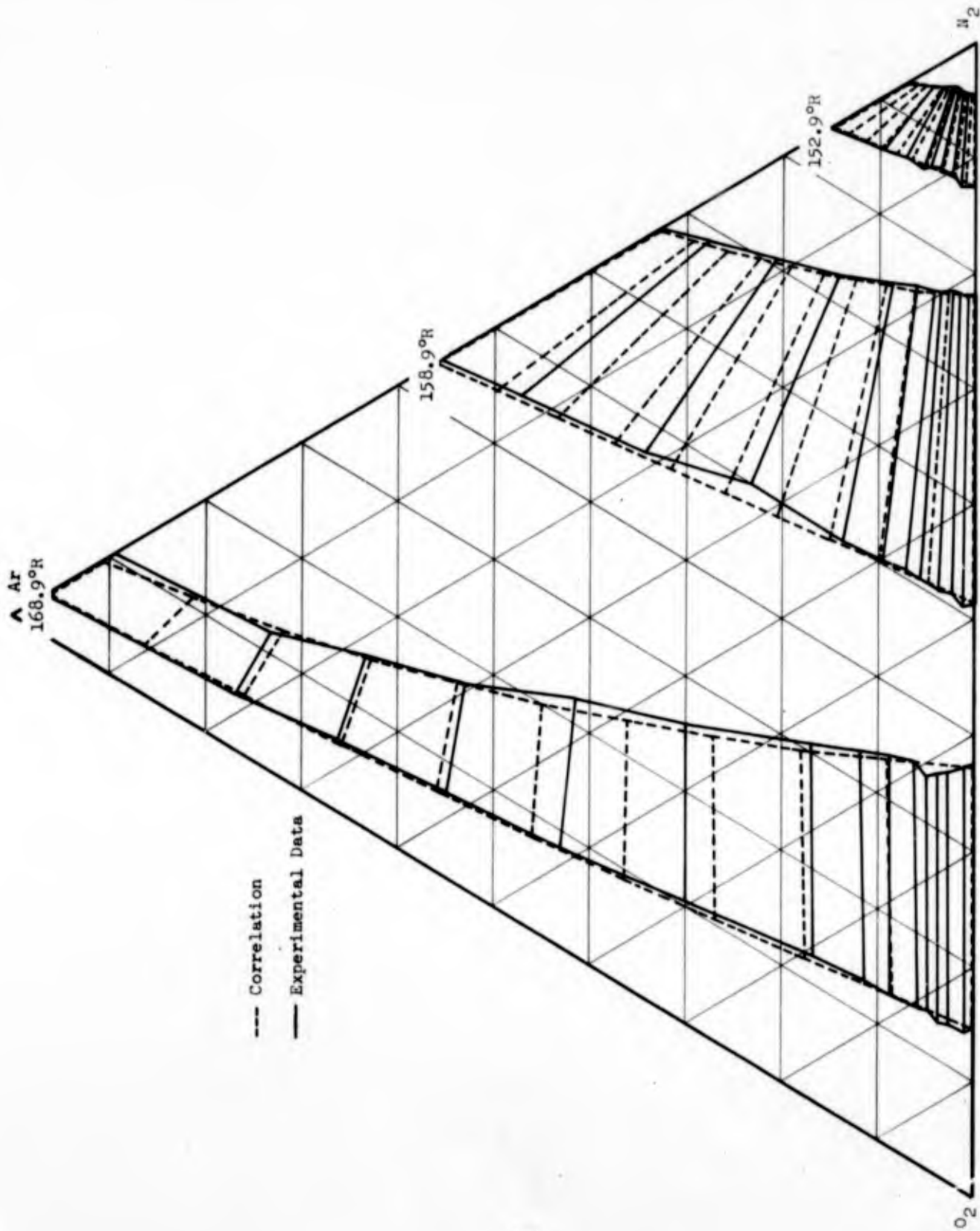


Figure 52. Comparison of Experimental Data and the Correlation, 2 Atmospheres.

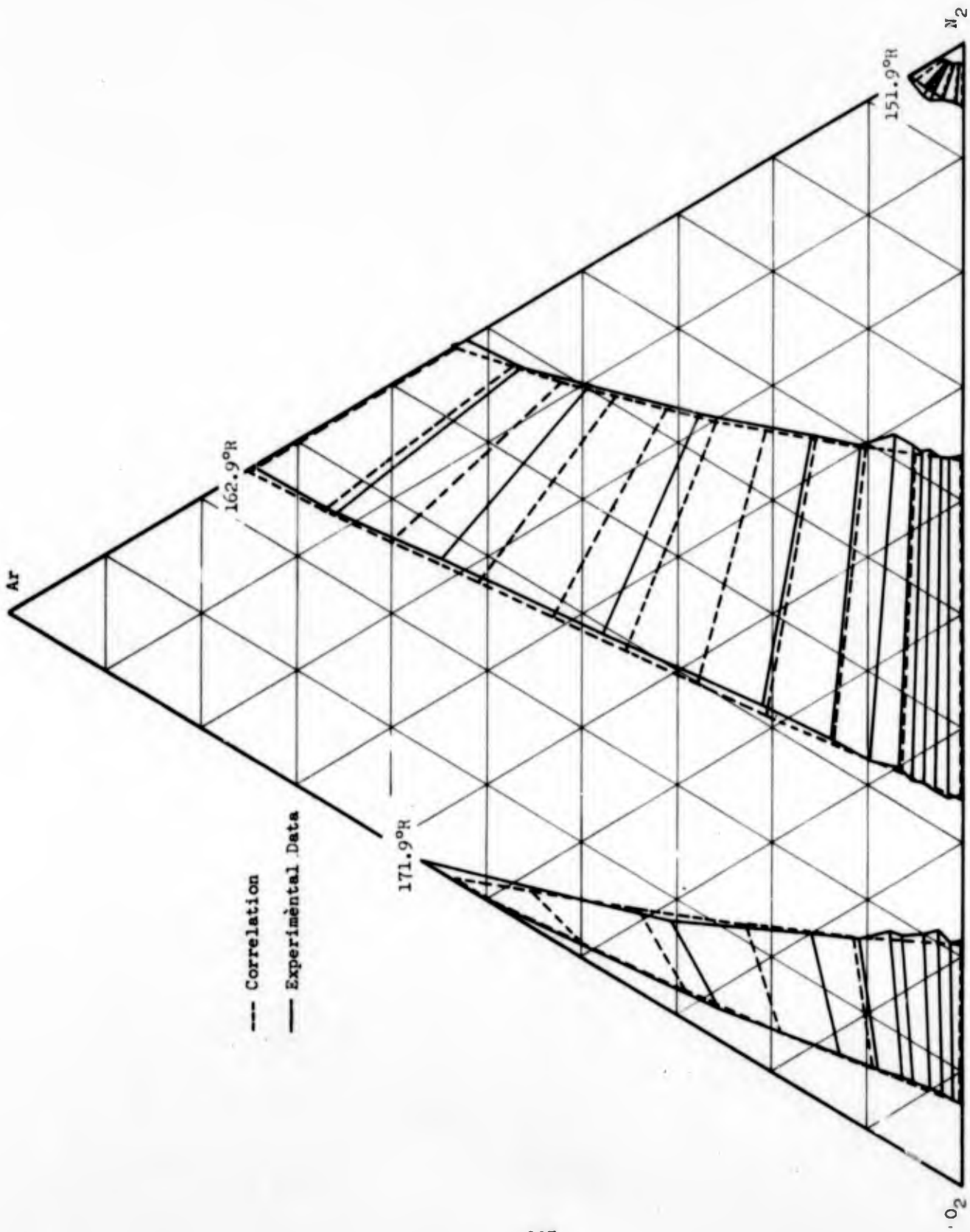


Figure 53. Comparison of Experimental Data and the Correlation, 2 Atmospheres.

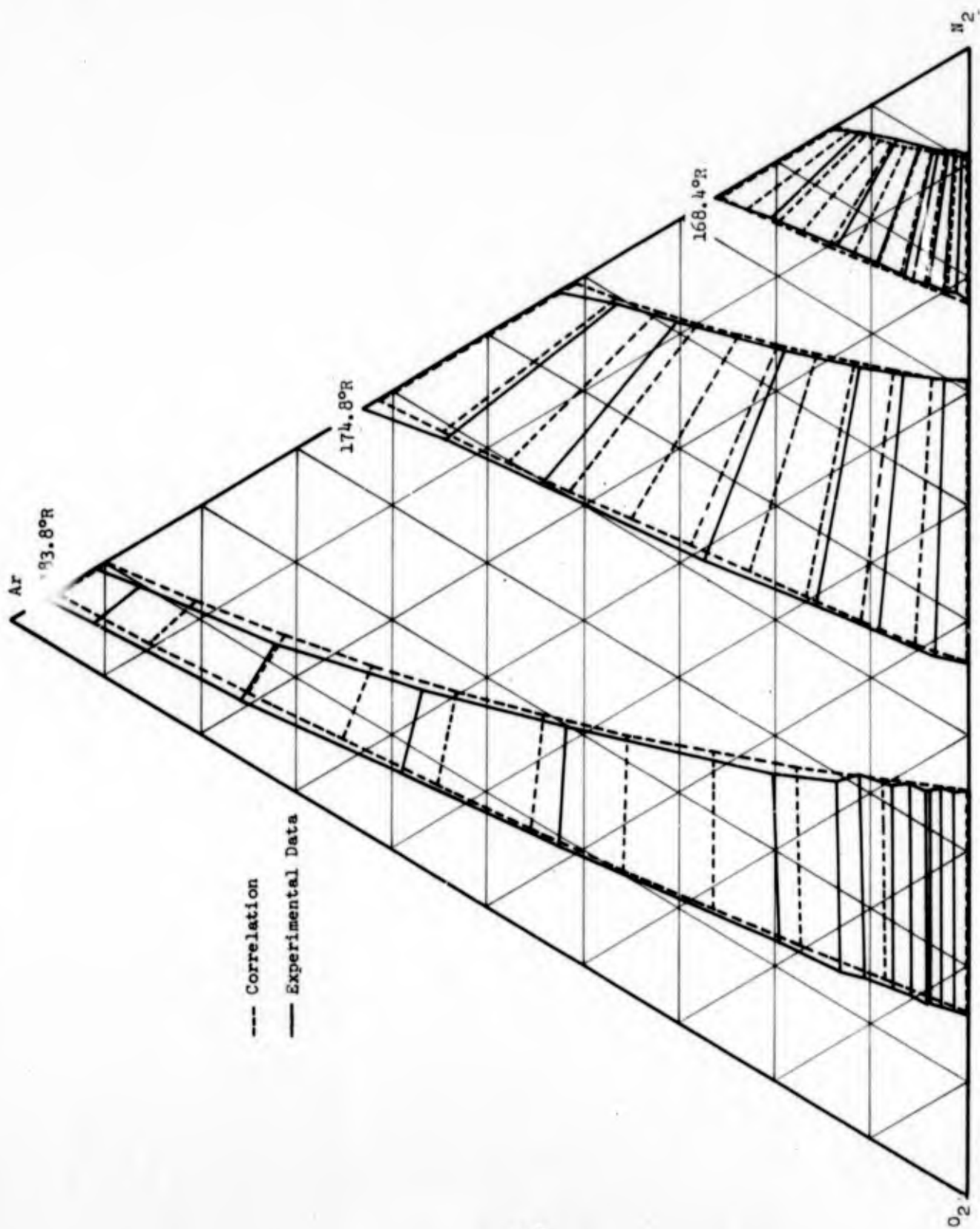


Figure 54. Comparison of Experimental Data and the Correlation, 4 Atmospheres.

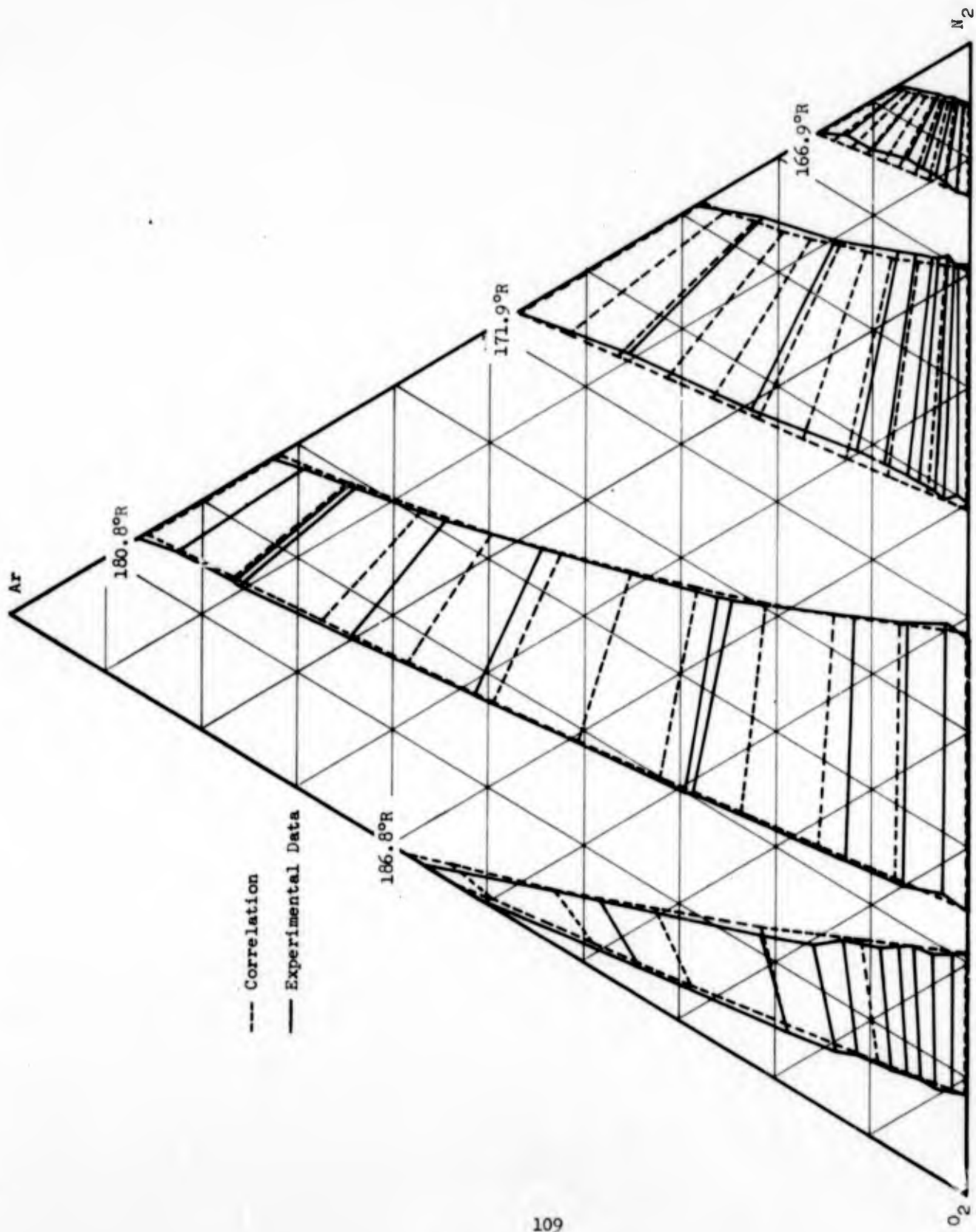


Figure 55. Comparison of Experimental Data and the Correlation, 4 Atmospheres.

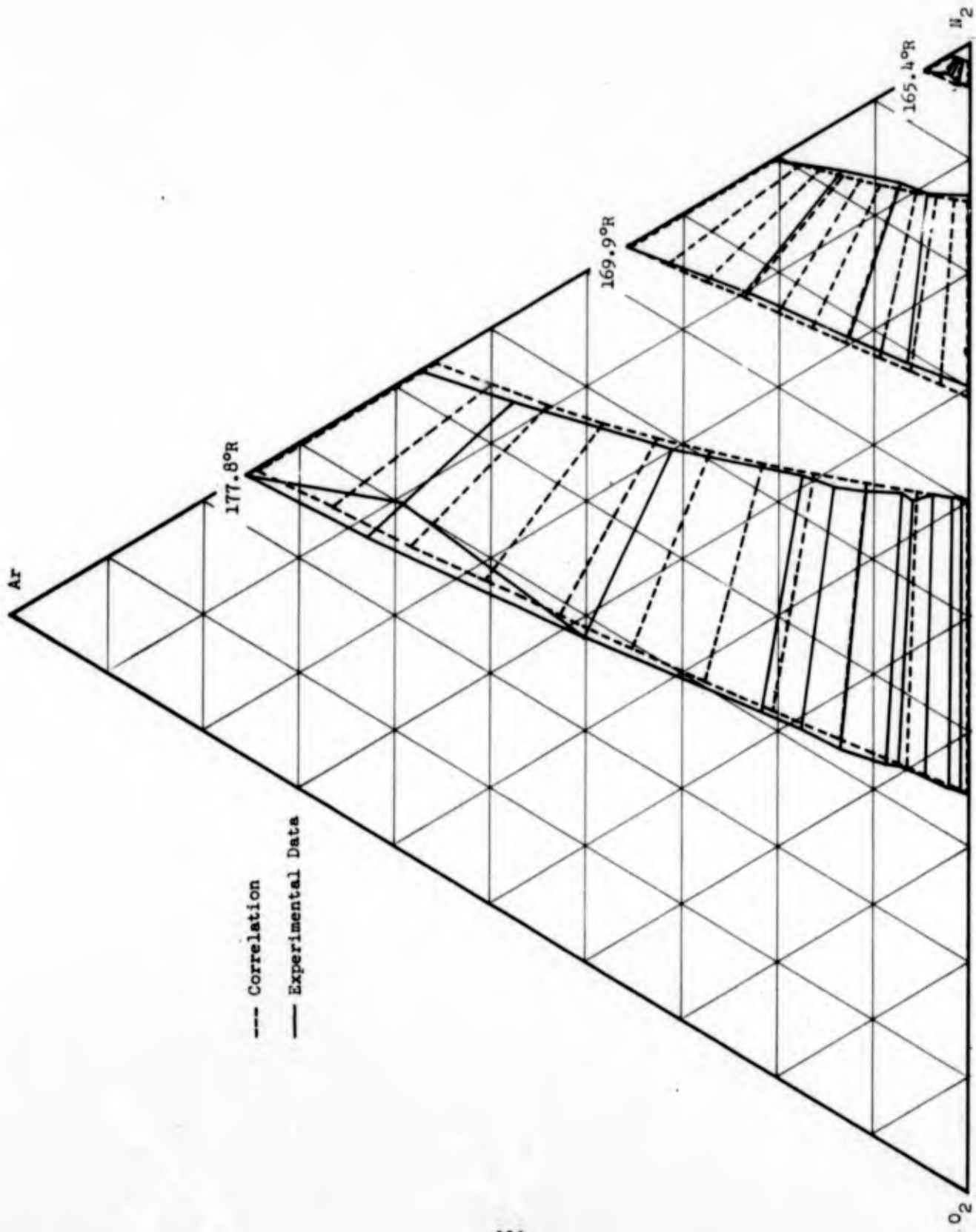


Figure 56. Comparison of Experimental Data and the Correlation, 4 Atmospheres.

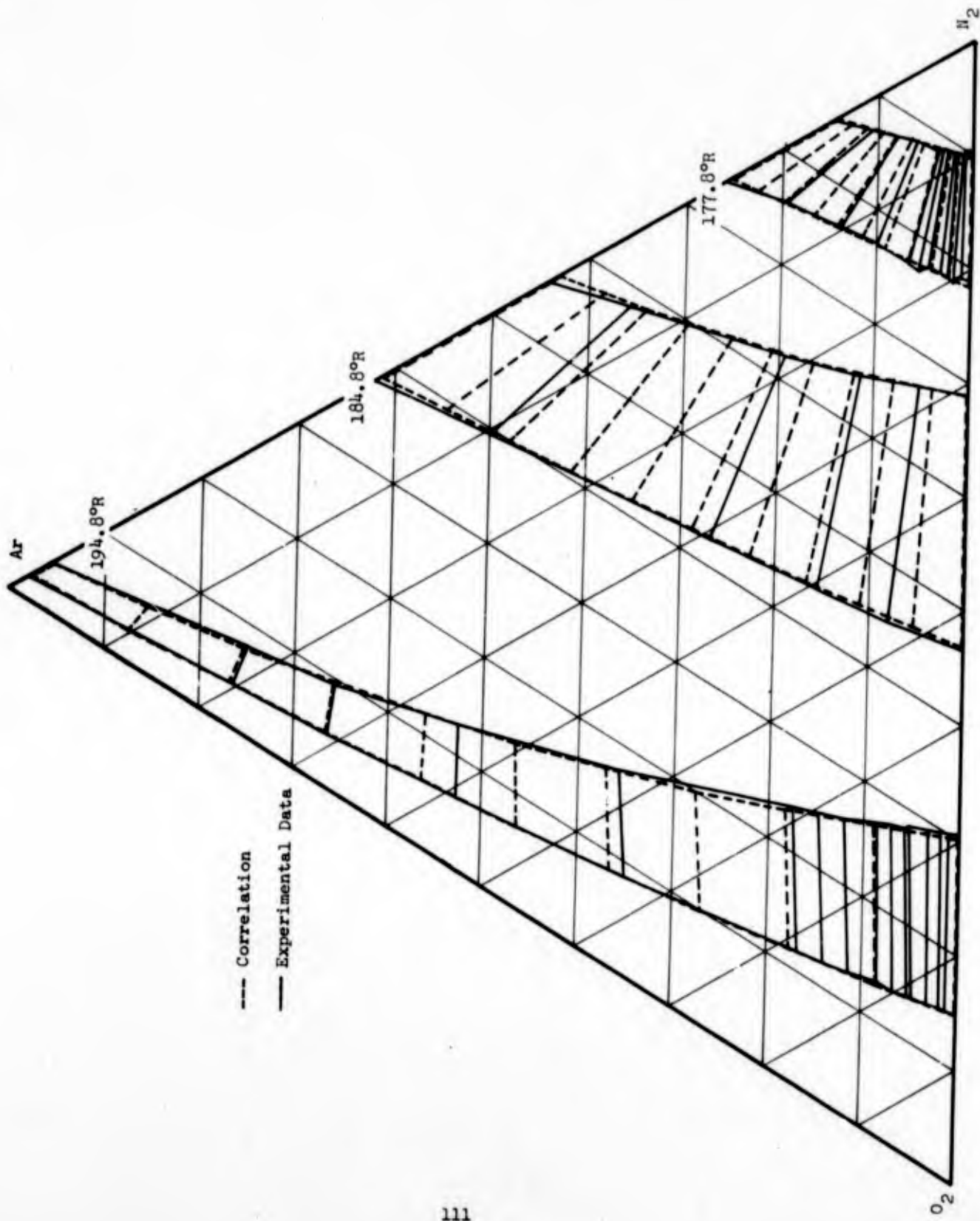


Figure 57. Comparison of Experimental Data and the Correlation, 6 Atmospheres.

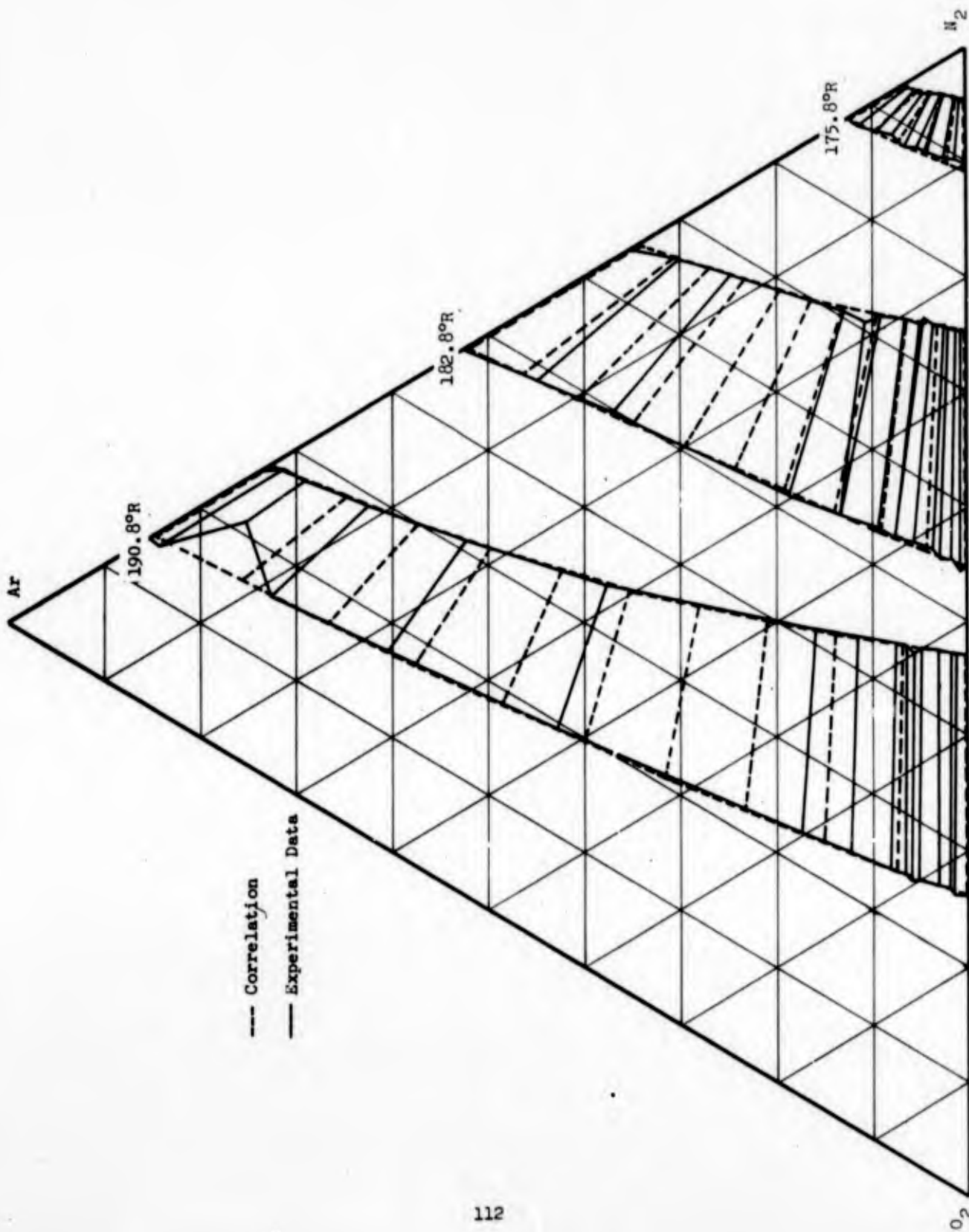


Figure 58. Comparison of Experimental Data and the Correlation, 6 Atmospheres.

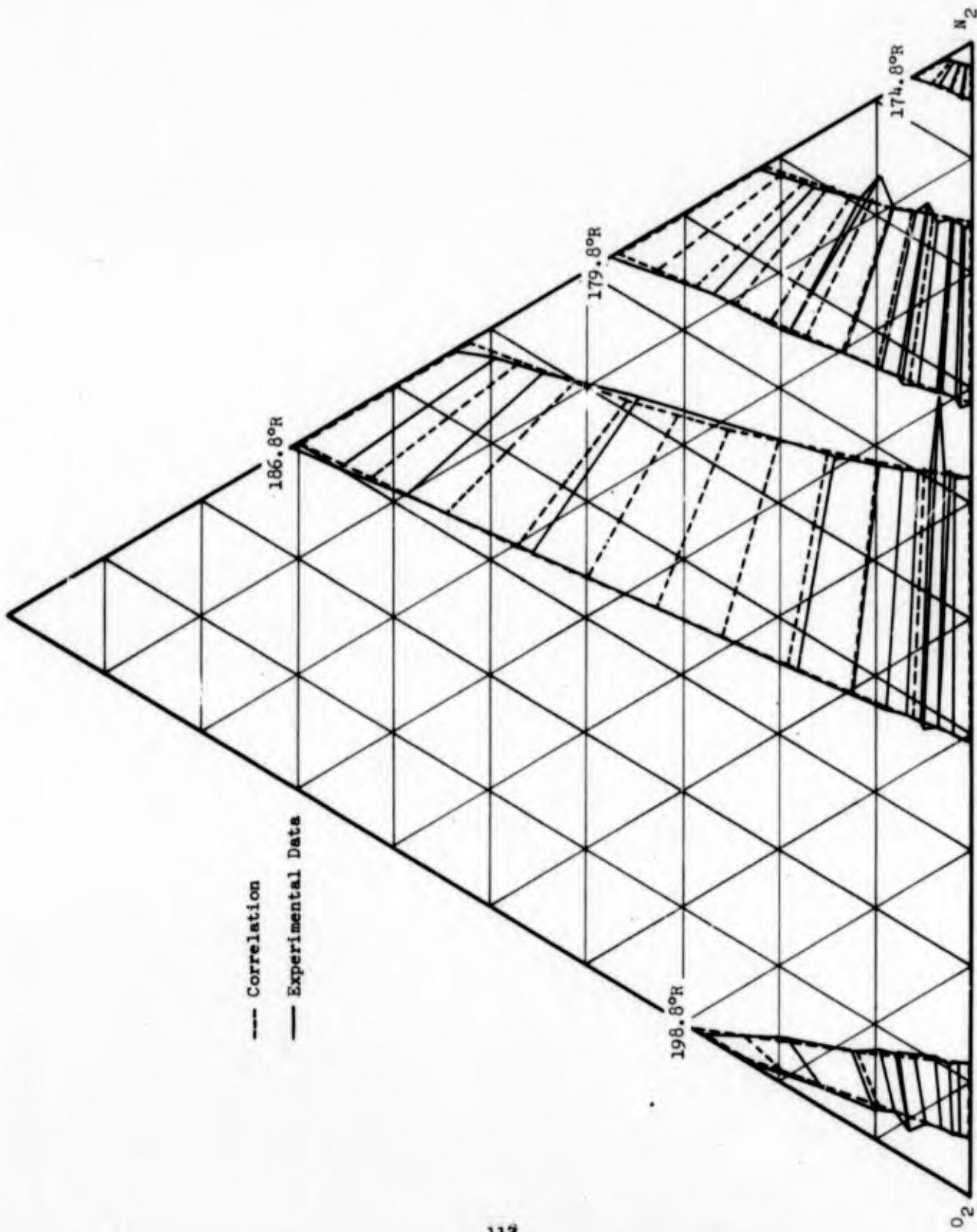


Figure 59. Comparison of Experimental Data and the Correlation, 6 Atmospheres.

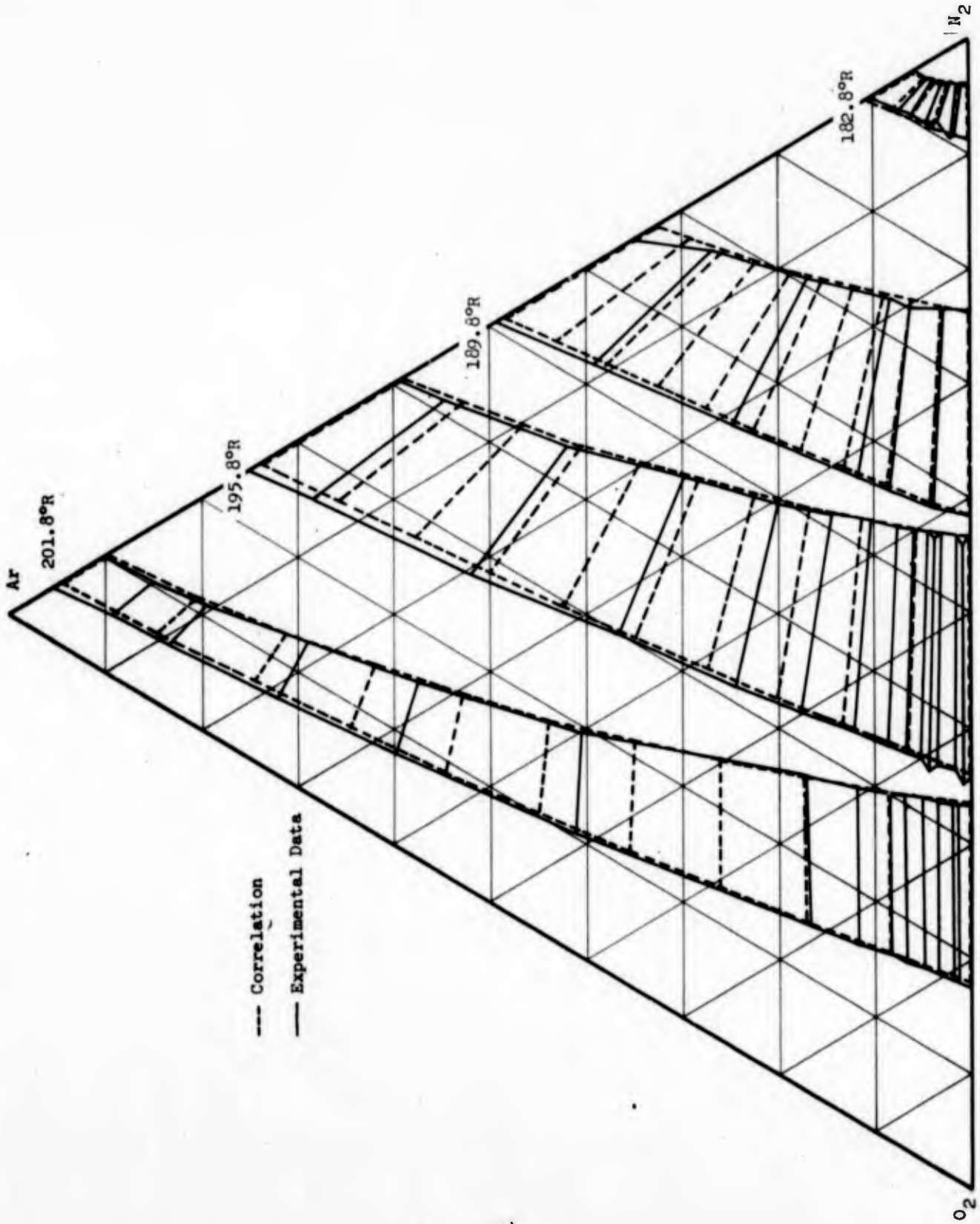


Figure 60. Comparison of Experimental Data and the Correlation, 8 Atmospheres.

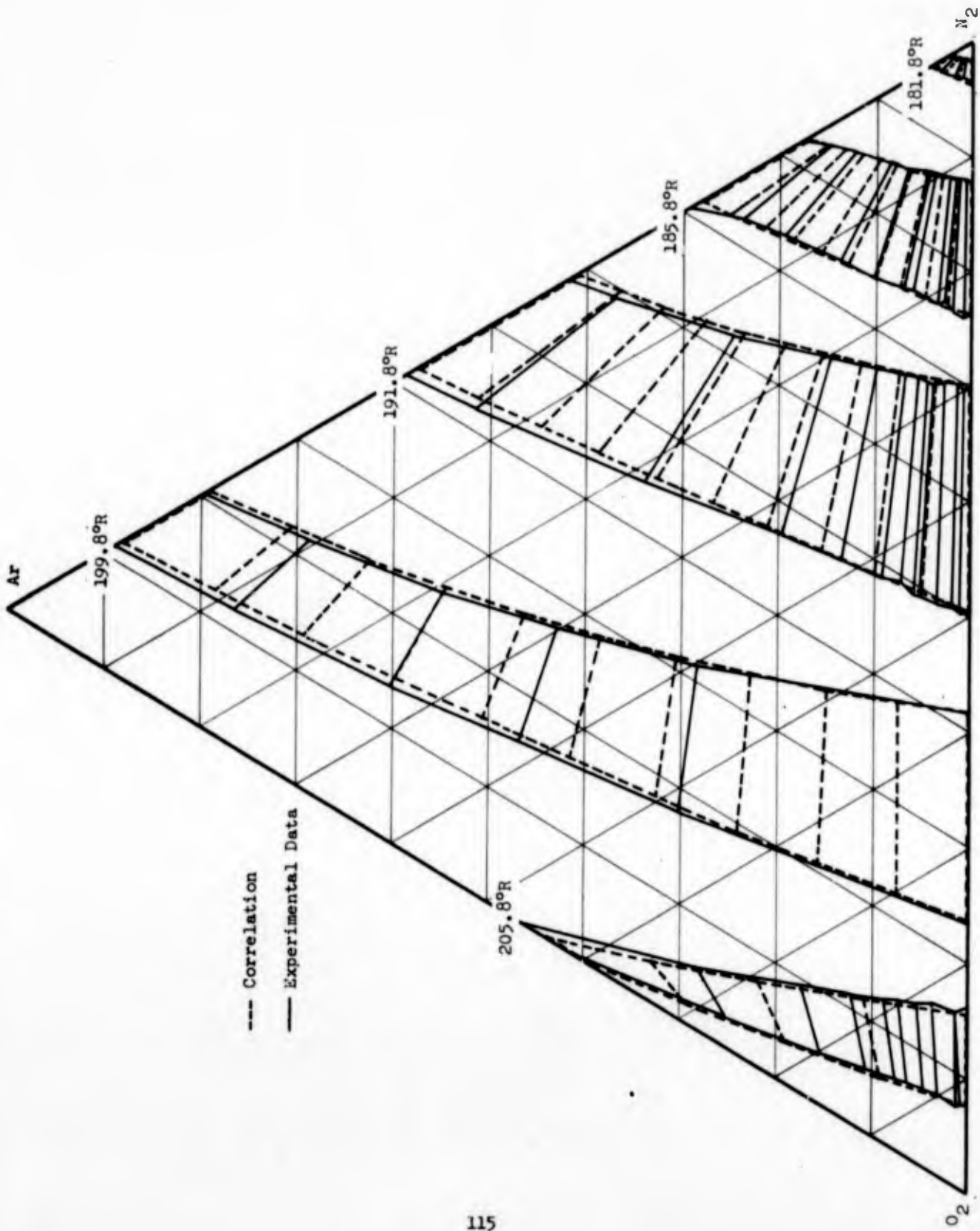


Figure 61. Comparison of Experimental Data and the Correlation, 8 Atmospheres.

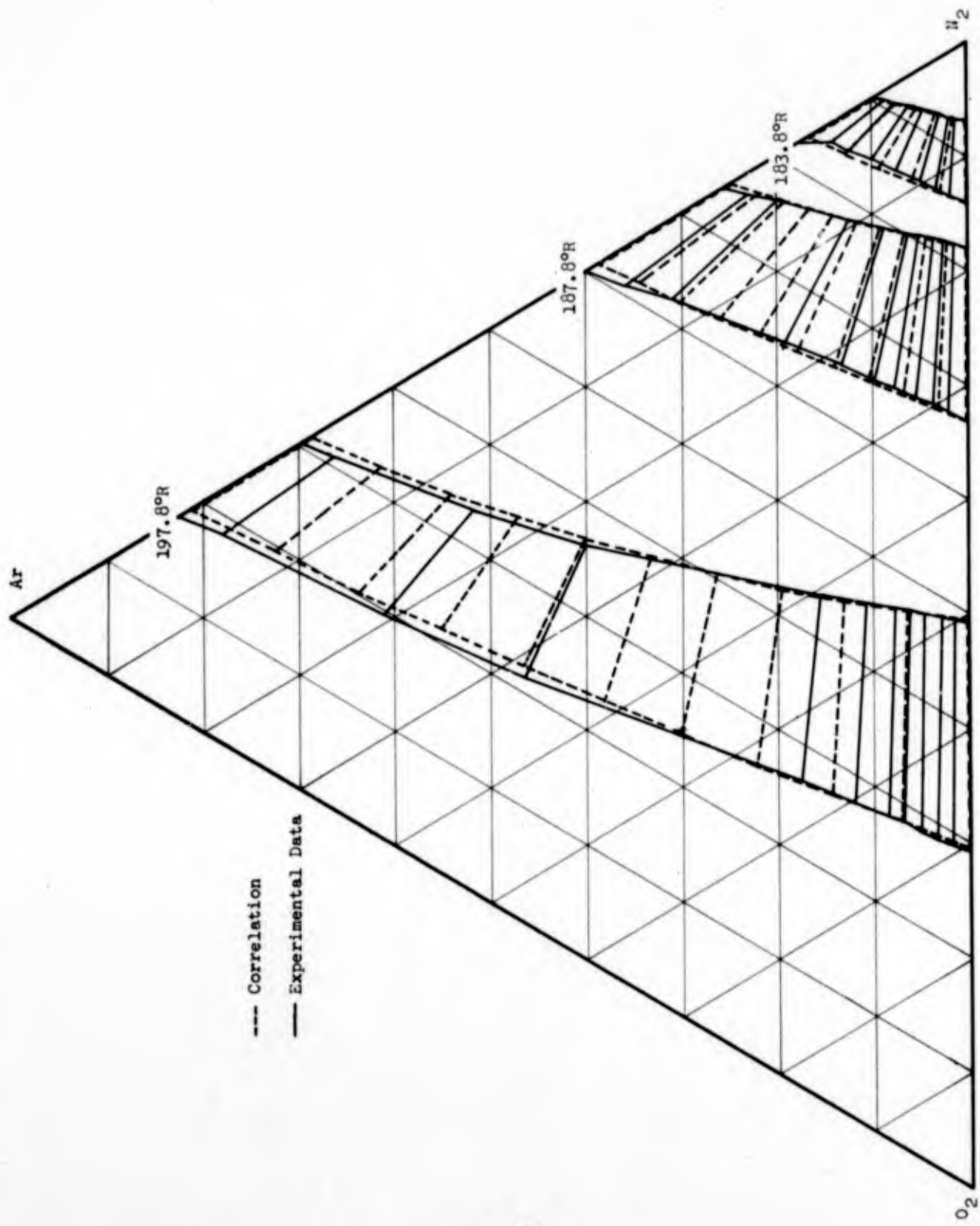


Figure 62. Comparison of Experimental Data and the Correlation, 8 Atmospheres.

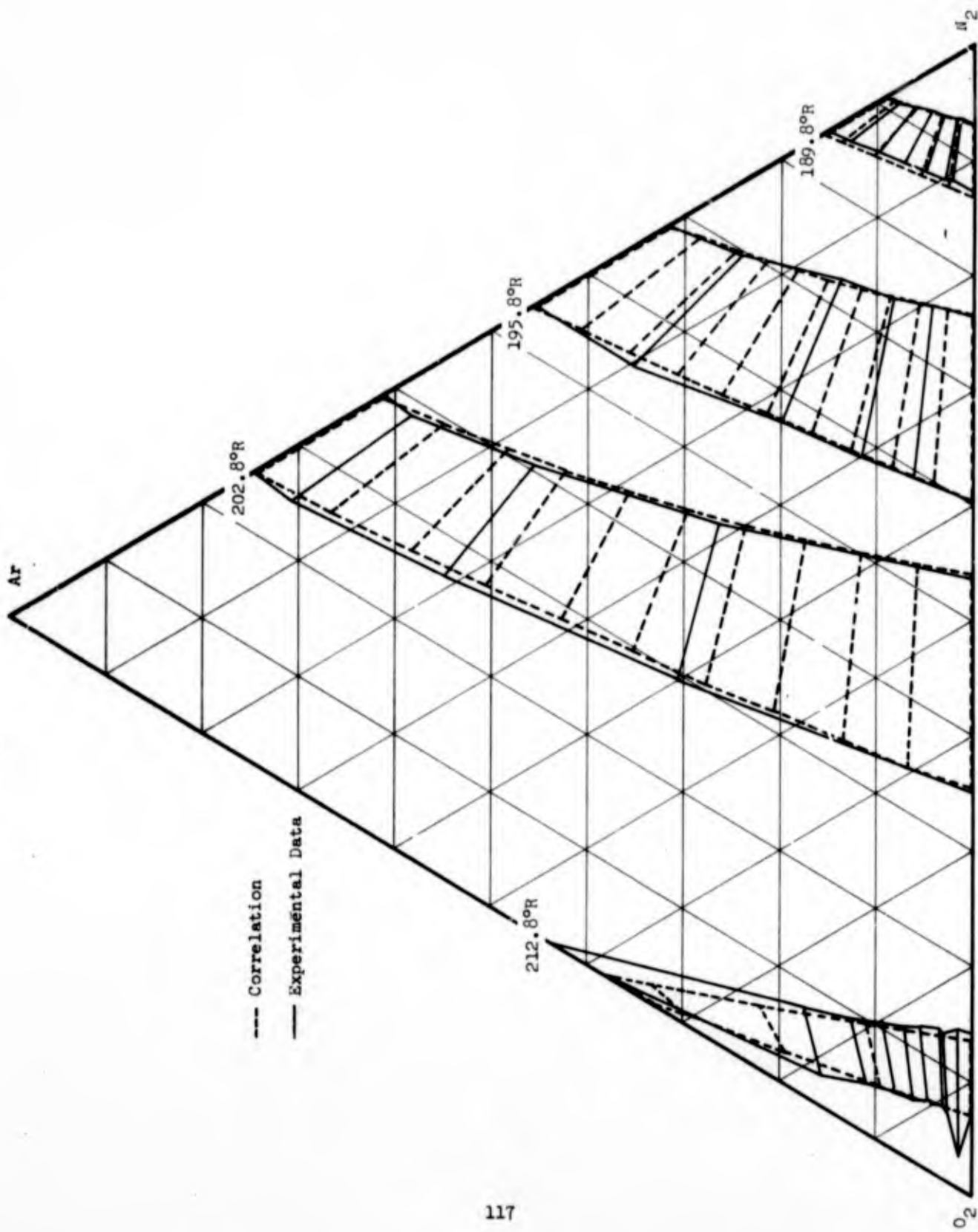


Figure 63. Comparison of Experimental Data and the Correlation, 10 Atmospheres.

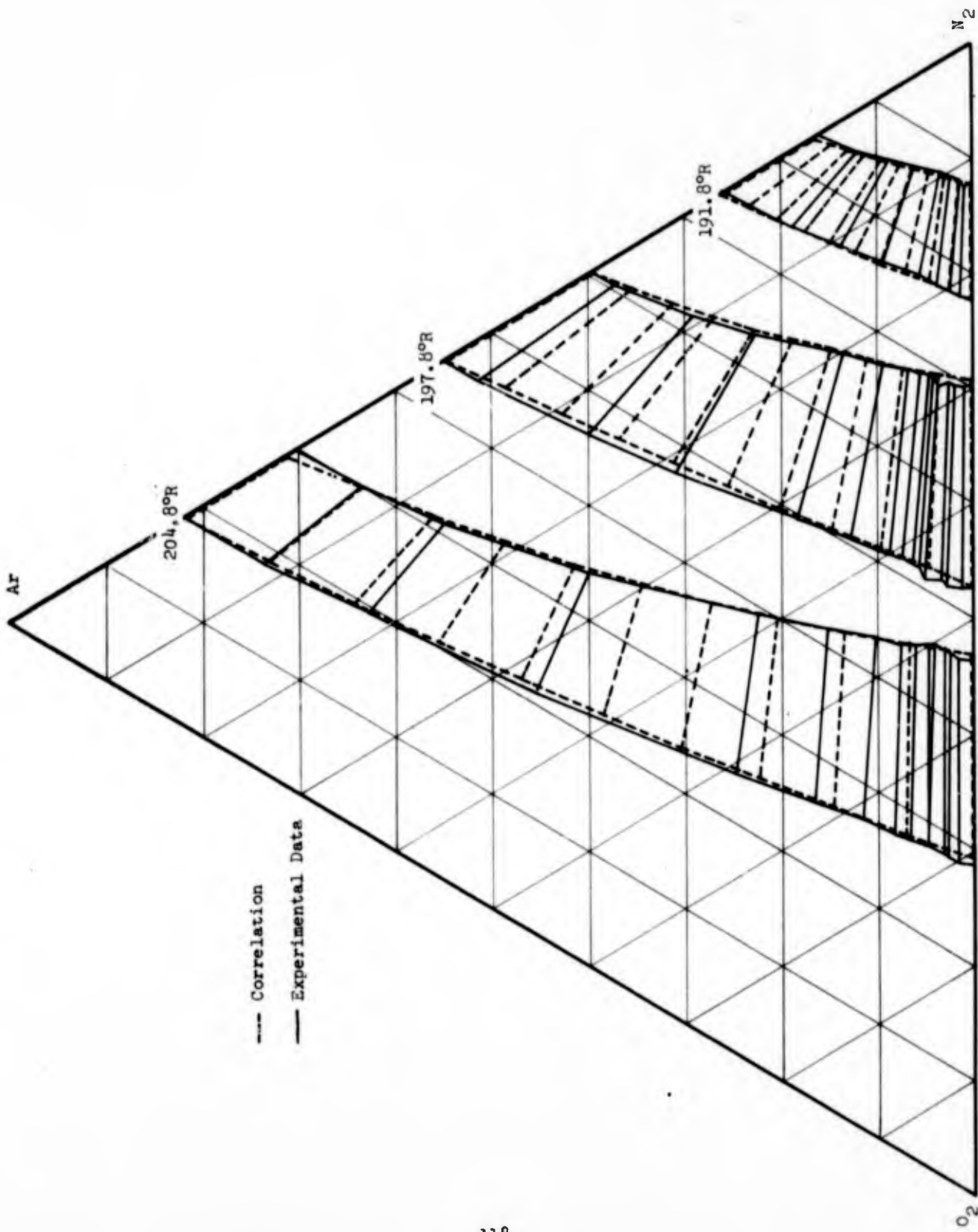


Figure 64. Comparison of Experimental Data and the Correlation, 10 Atmospheres.

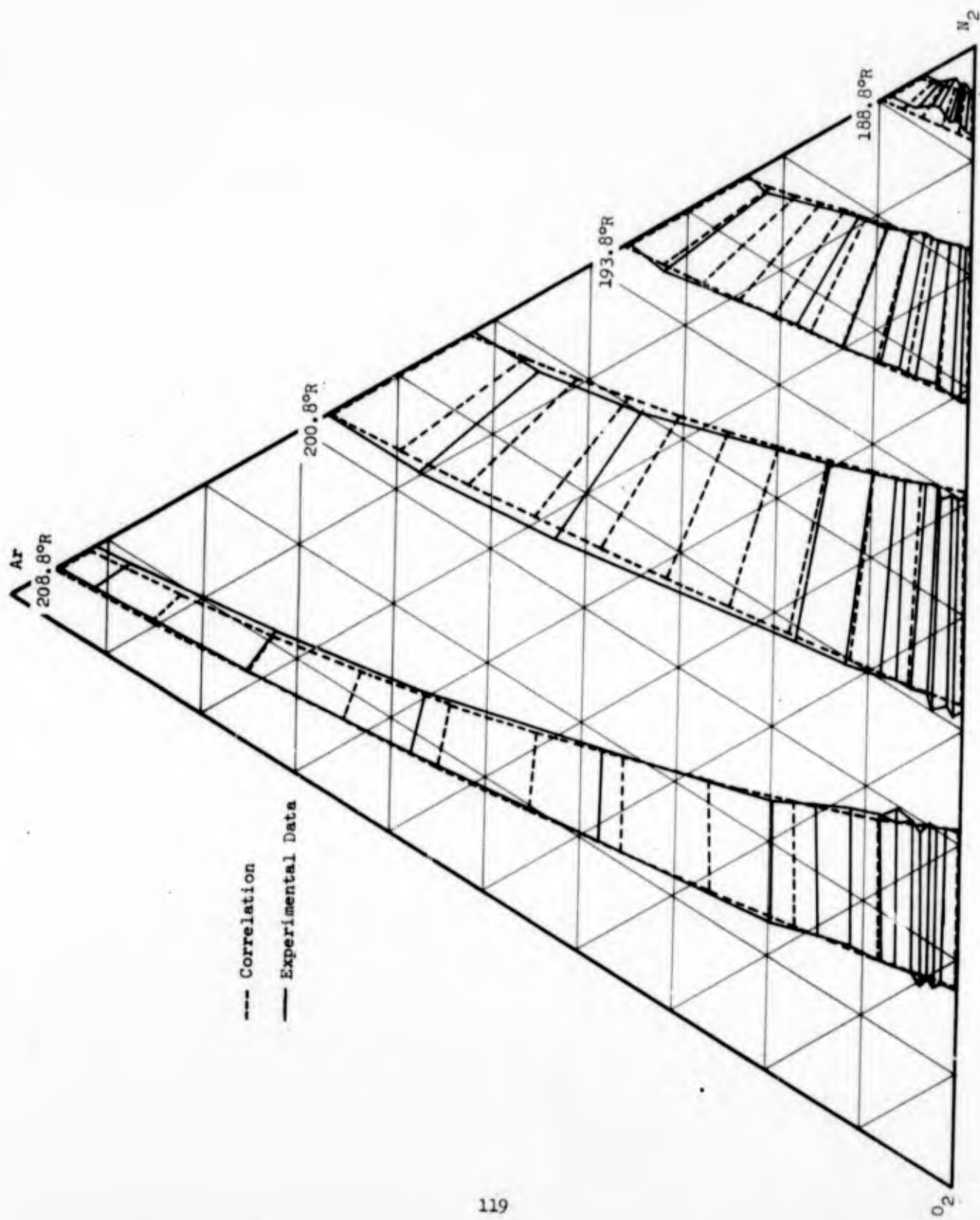


Figure 65. Comparison of Experimental Data and the Correlation, 10 Atmospheres.

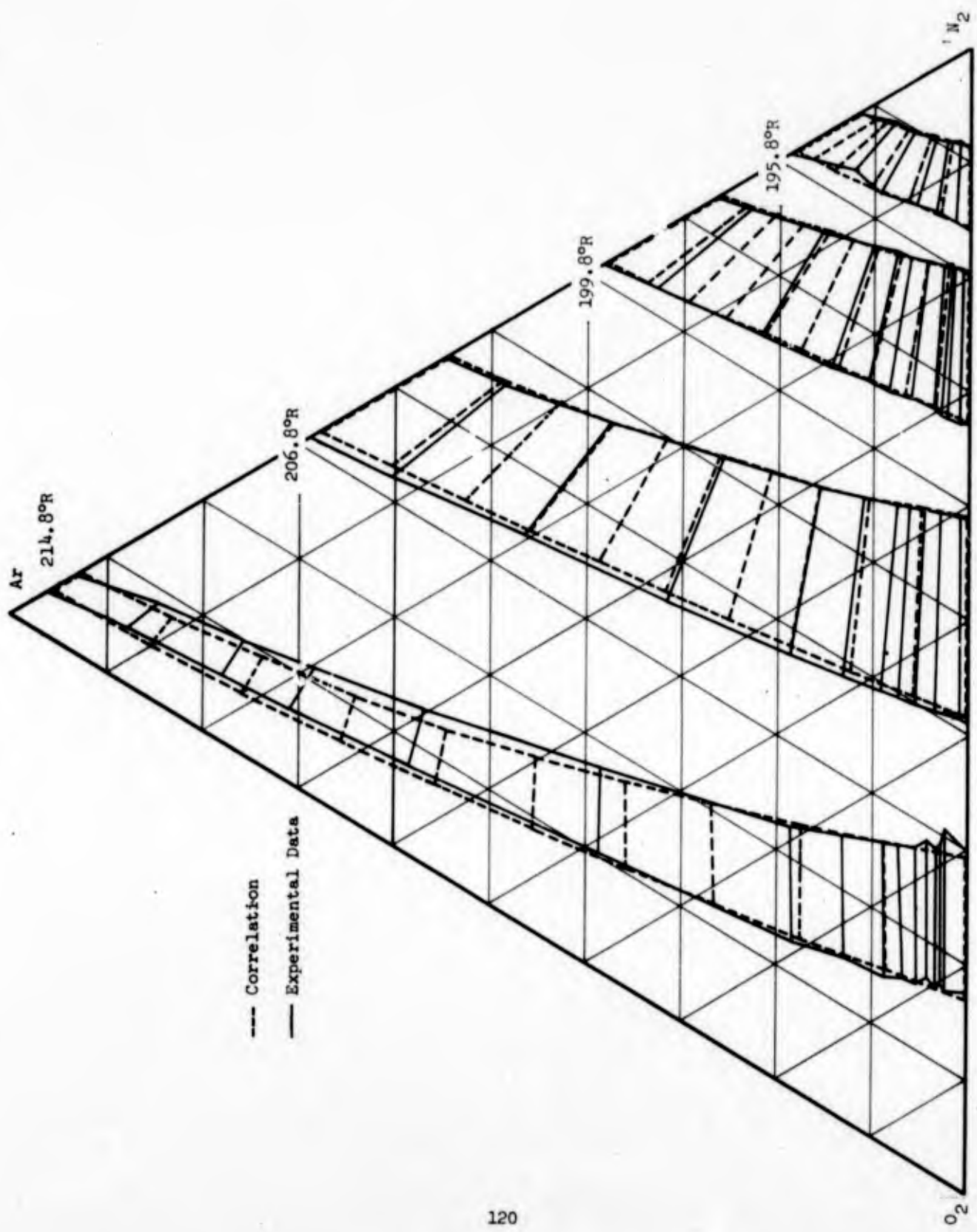


Figure 66. Comparison of Experimental Data and the Correlation, 12 Atmospheres.

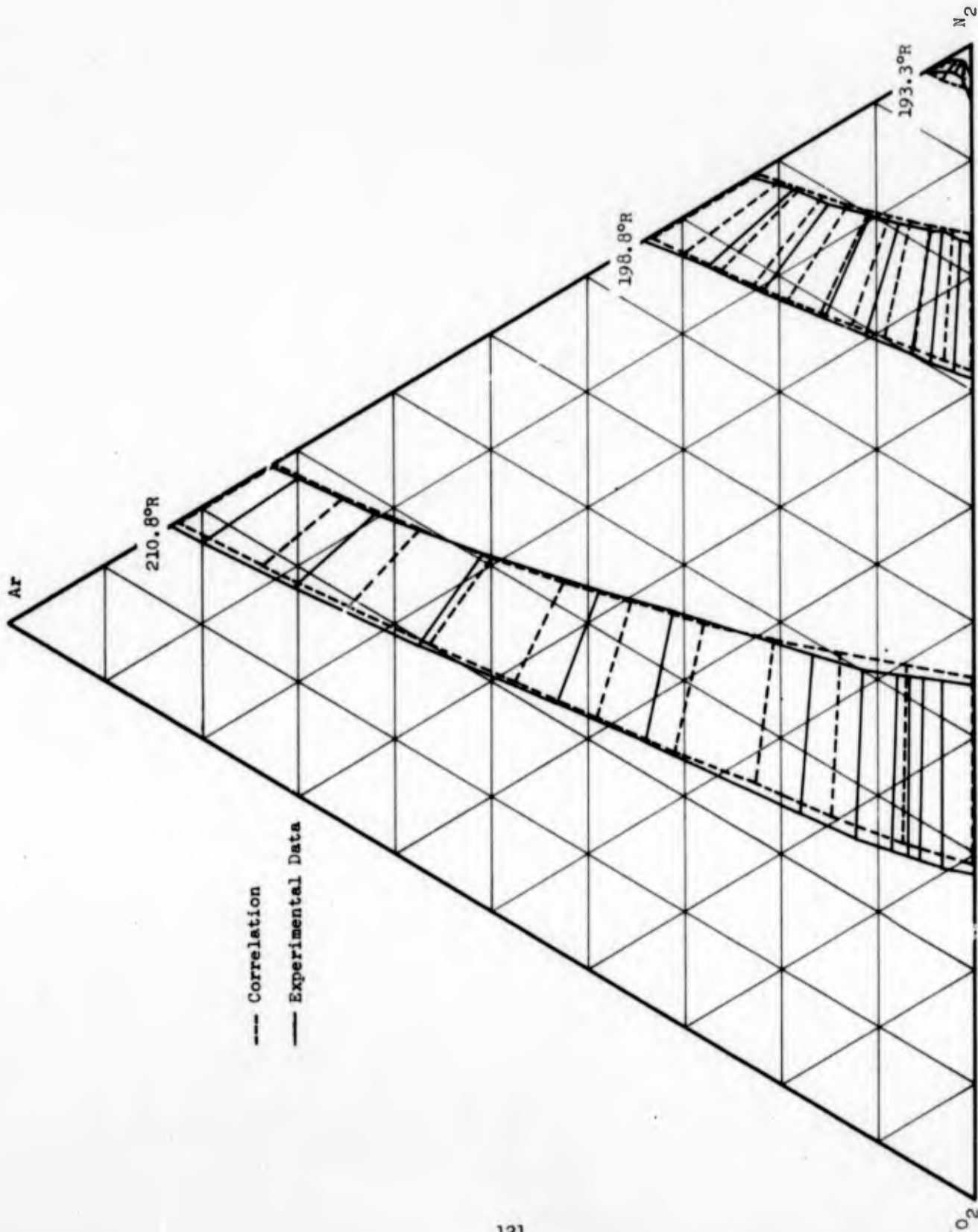


Figure 67. Comparison of Experimental Data and the Correlation, 12 Atmospheres.

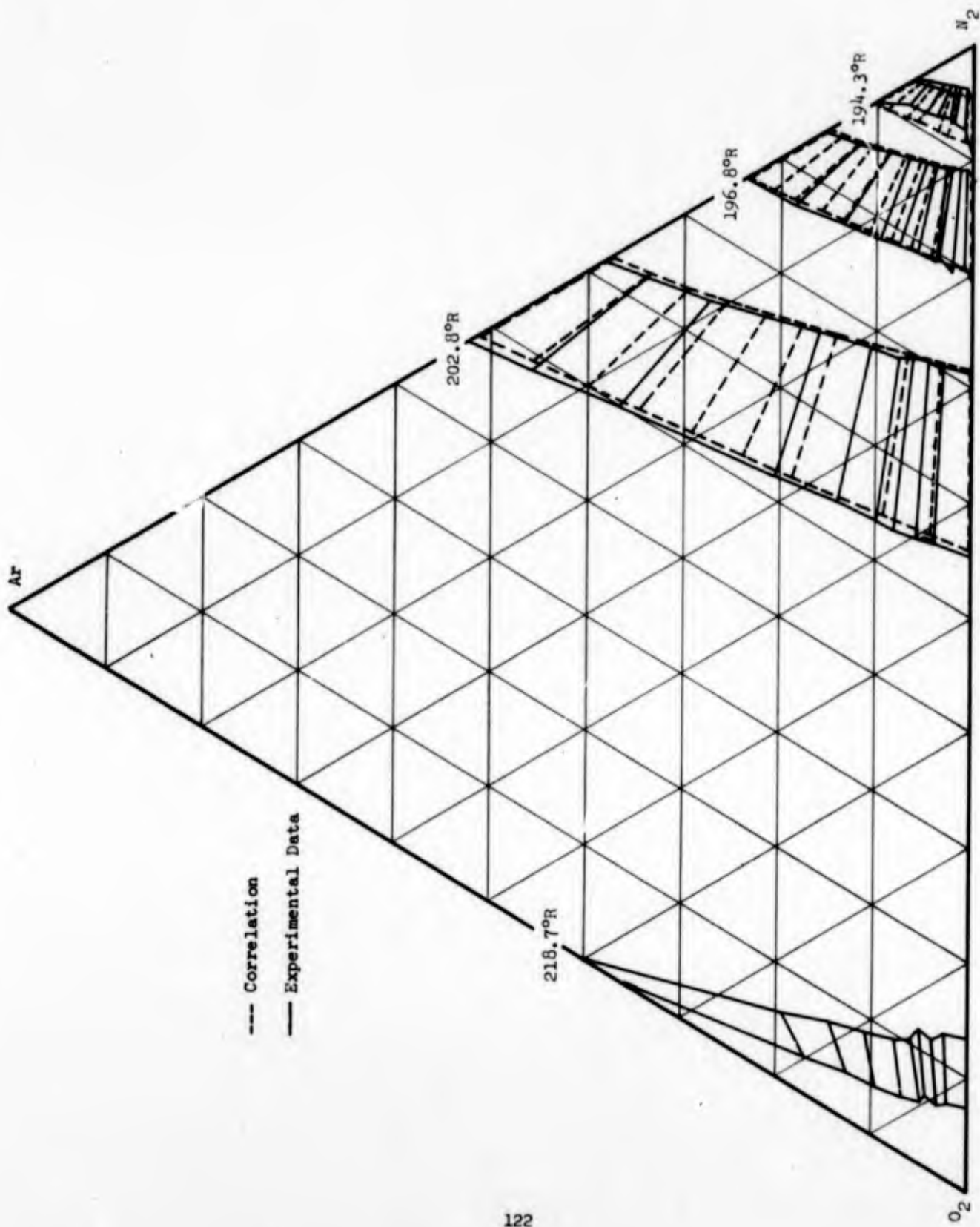


Figure 68. Comparison of Experimental Data and the Correlation, 12 Atmospheres.

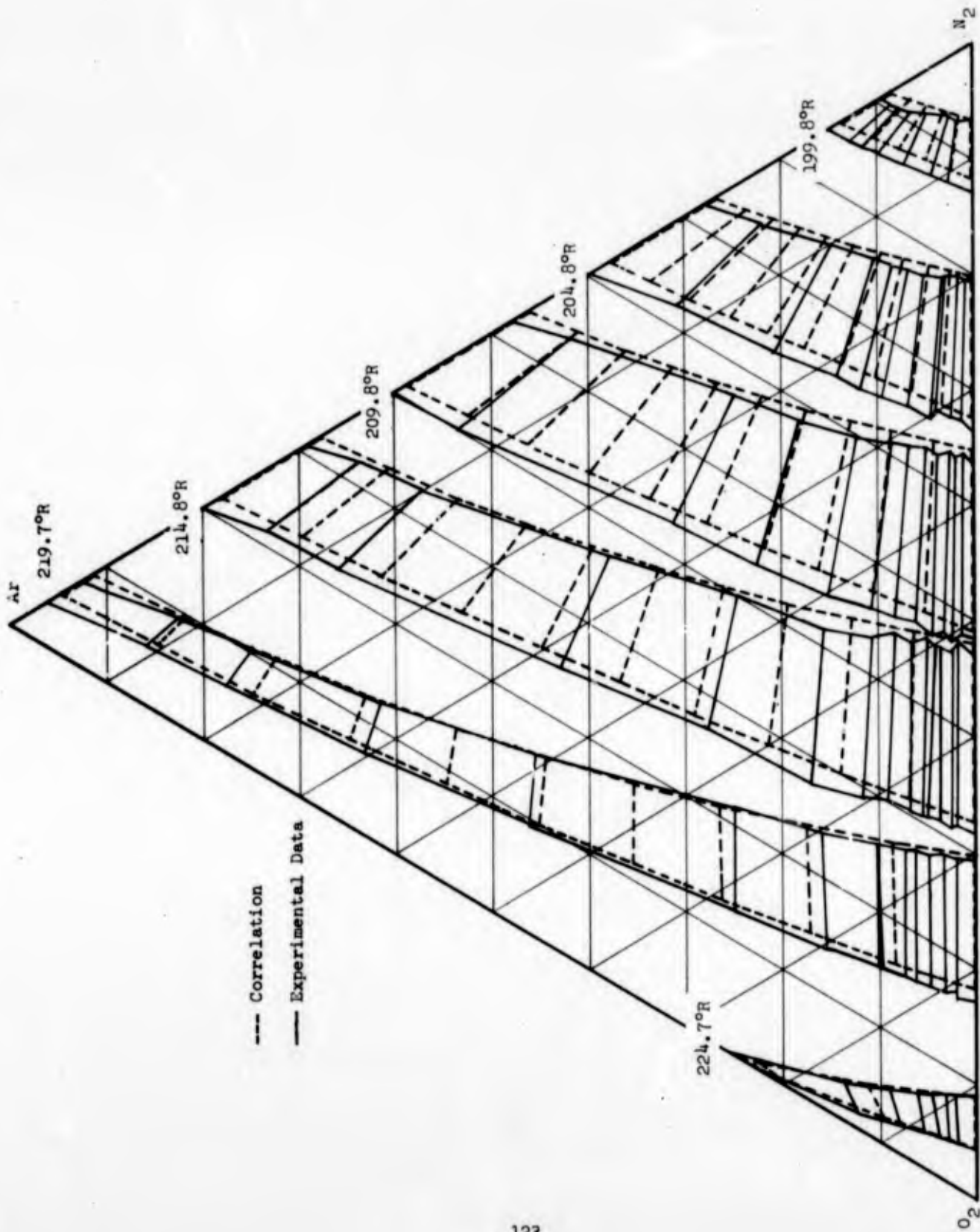


Figure 69. Comparison of Experimental Data and the Correlation, 14 Atmospheres.

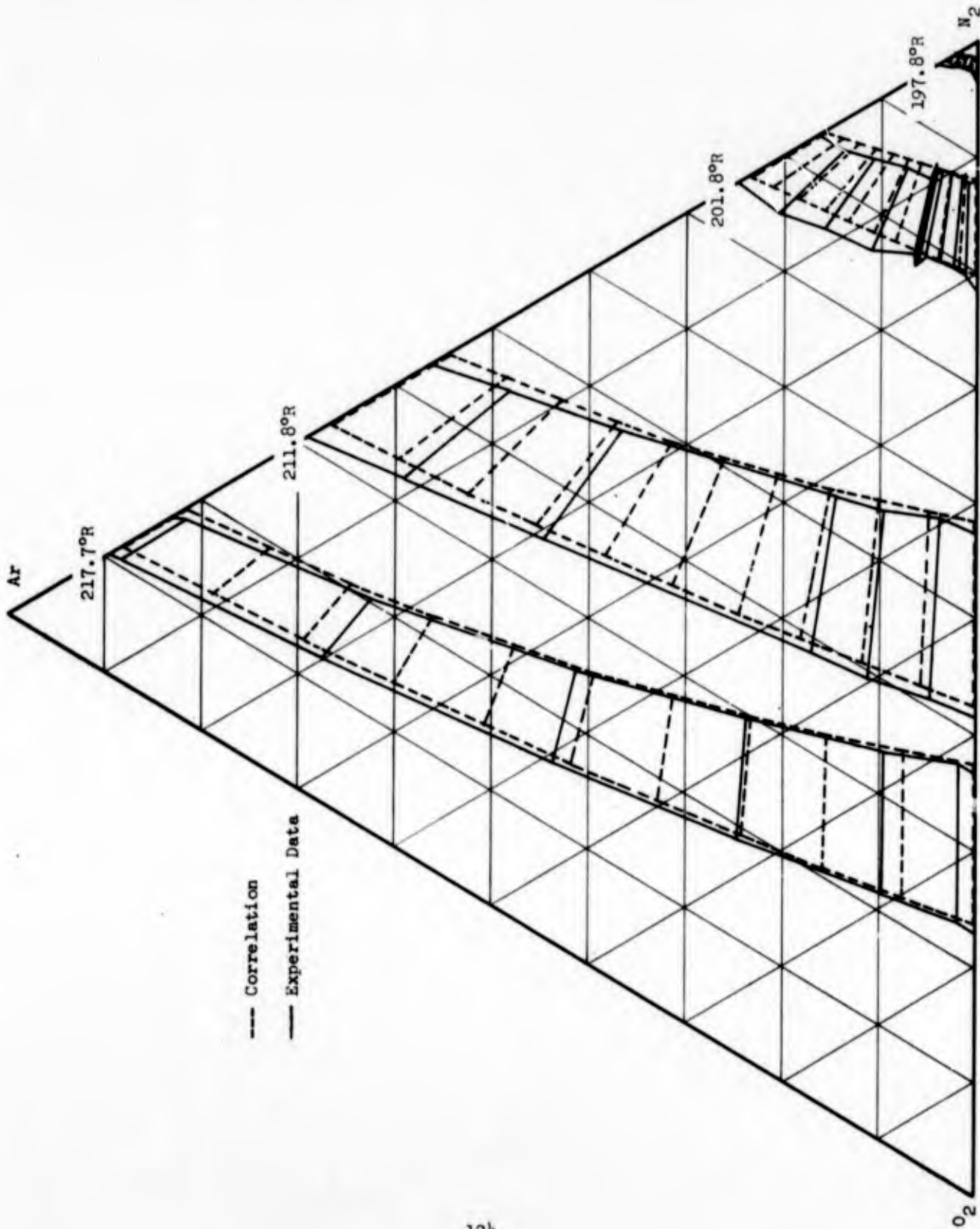


Figure 70. Comparison of Experimental Data and the Correlation, 14 Atmospheres.

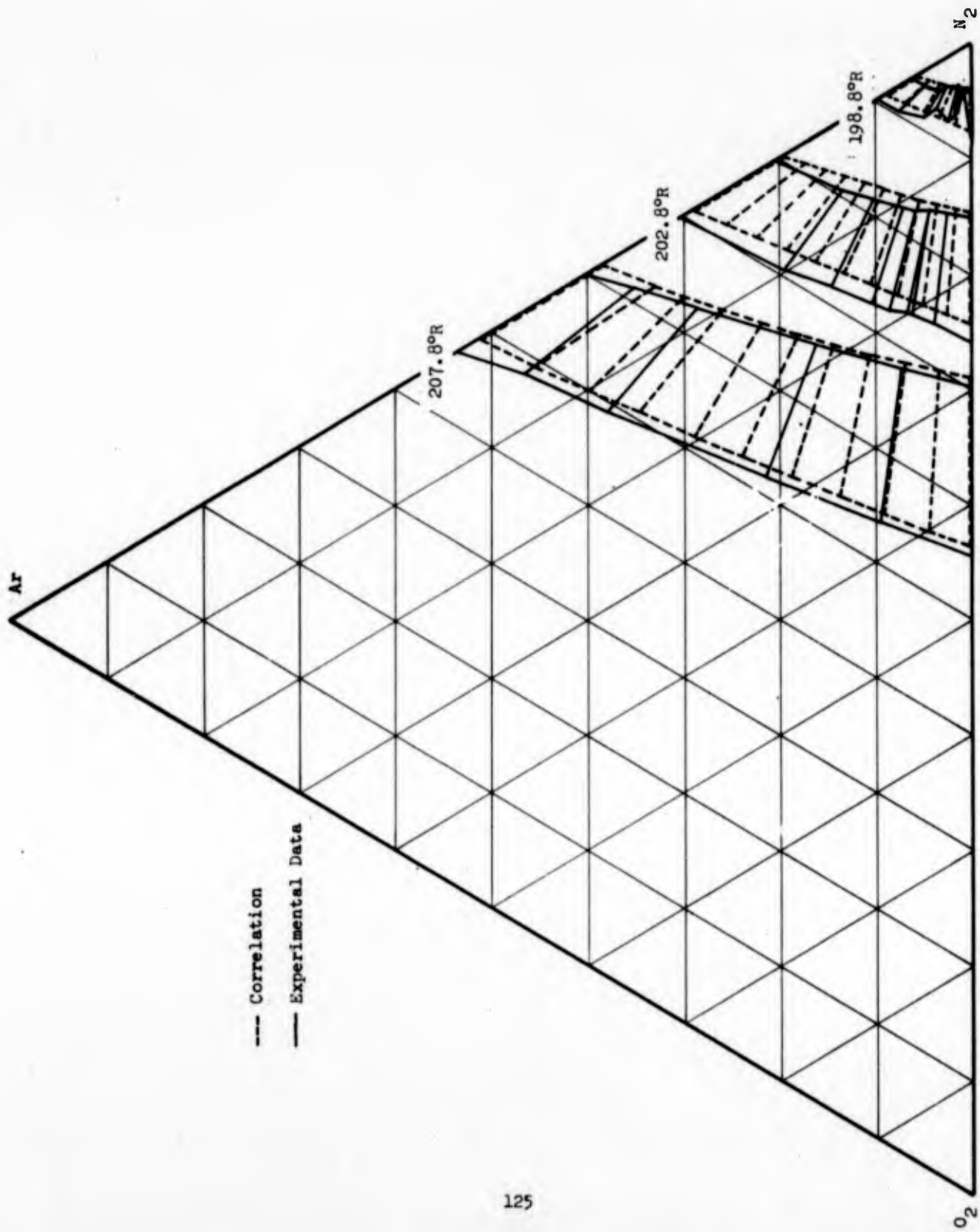


Figure 71. Comparison of Experimental Data and the Correlation, 14 Atmospheres.

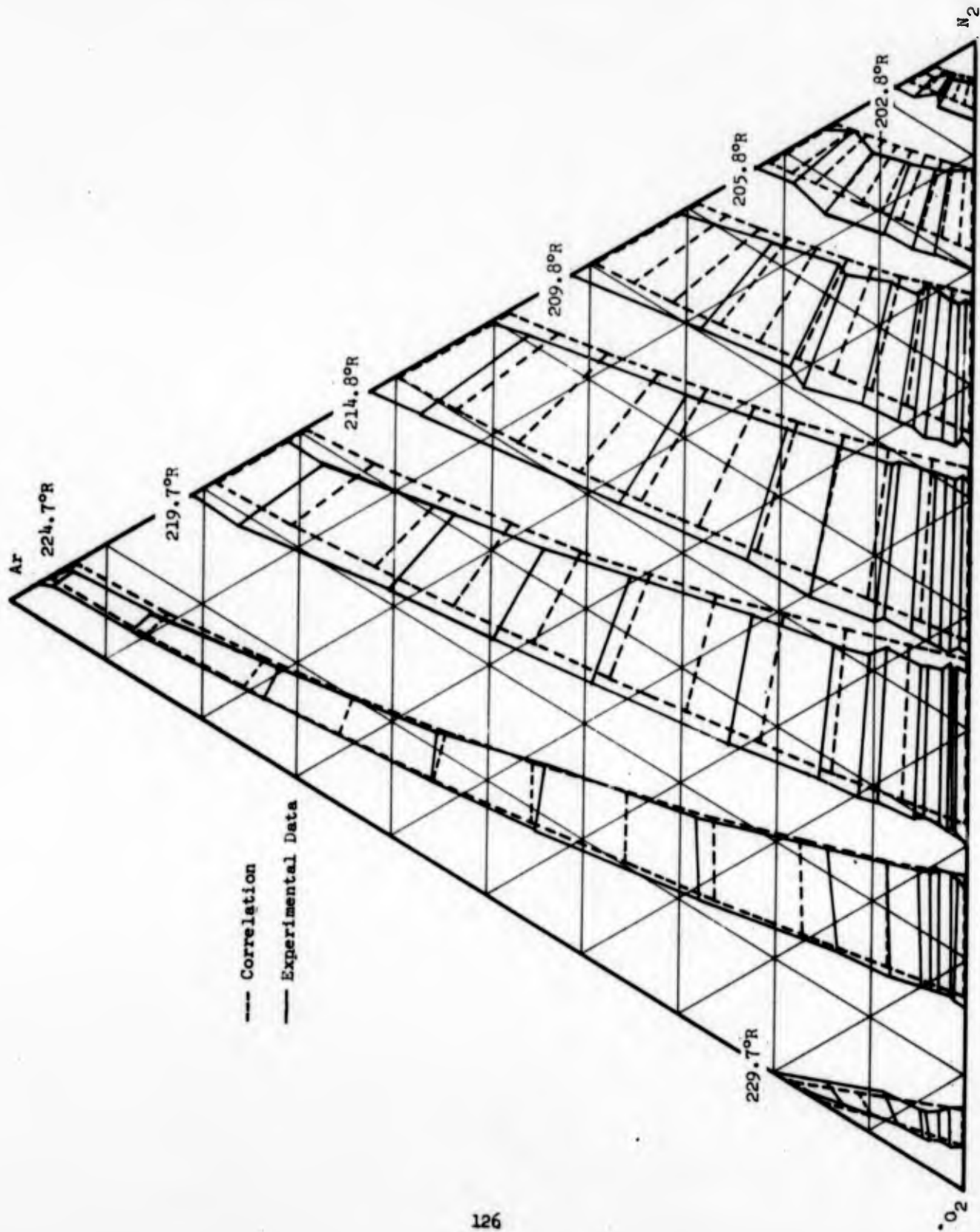


Figure 72. Comparison of Experimental Data and the Correlation, 16 Atmospheres.

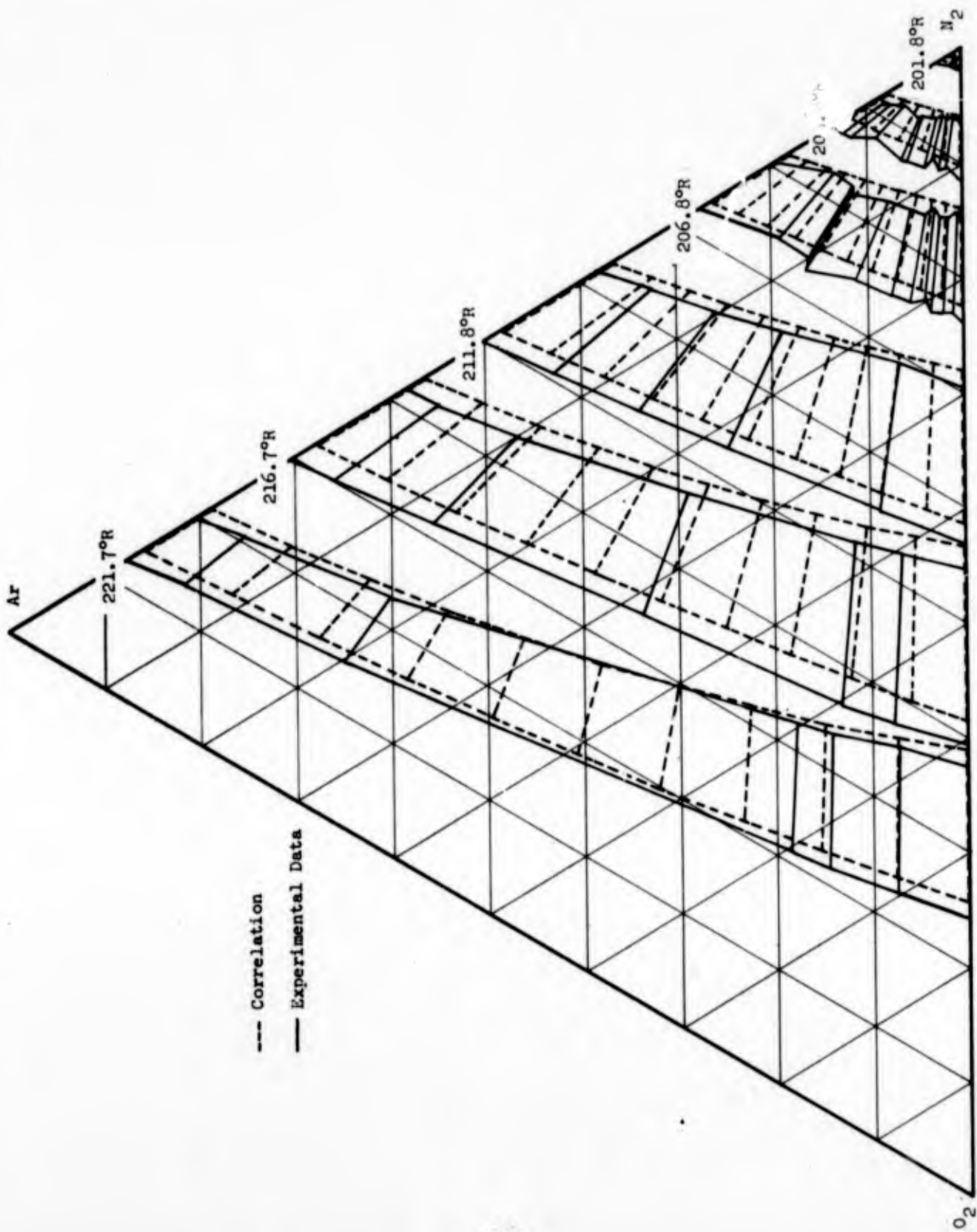


Figure 73. Comparison of Experimental Data and the Correlation, 16 Atmospheres.

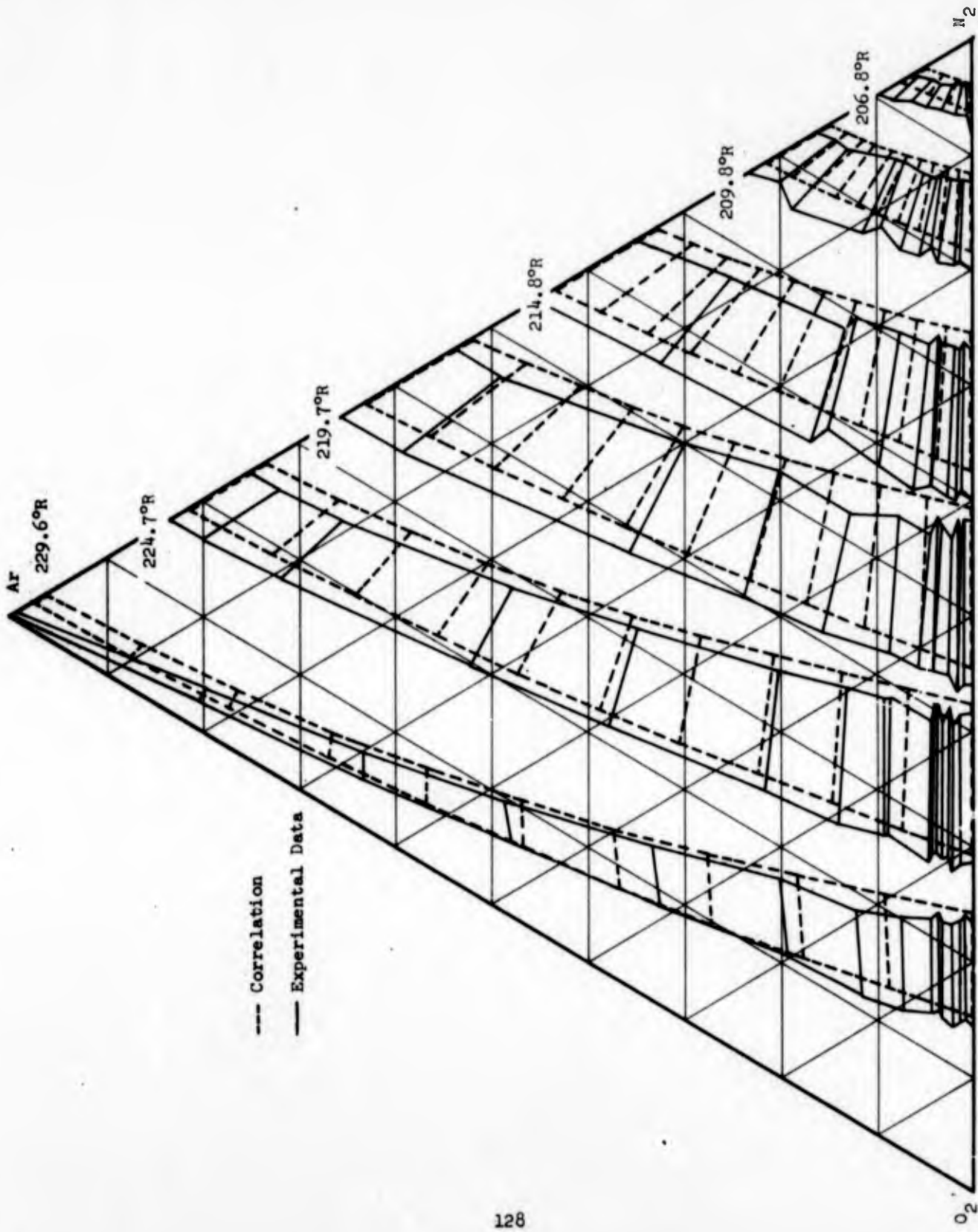


Figure 74. Comparison of Experimental Data and the Correlation, 18 Atmospheres.

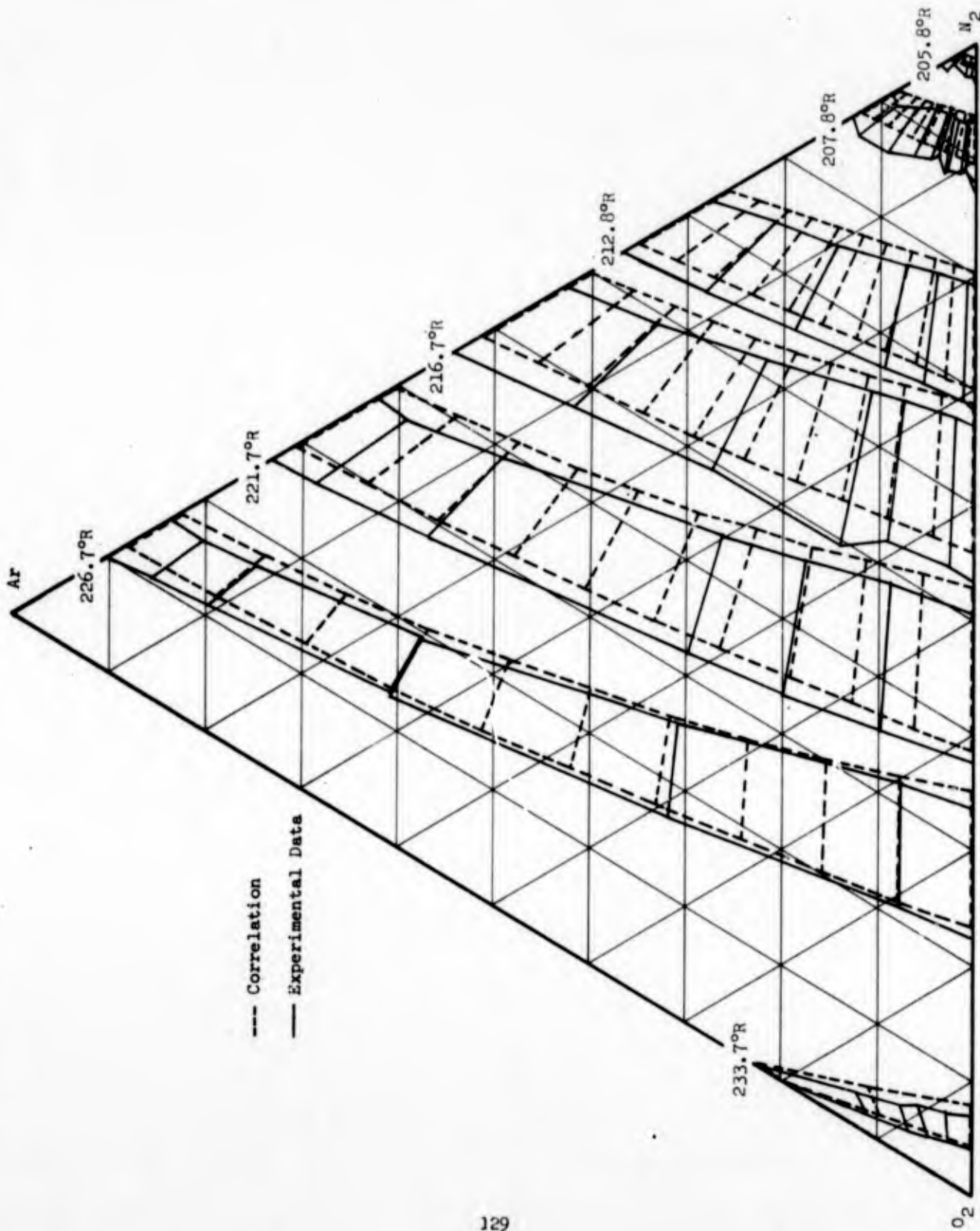


Figure 75. Comparison of Experimental Data and the Correlation, 18 Atmospheres.

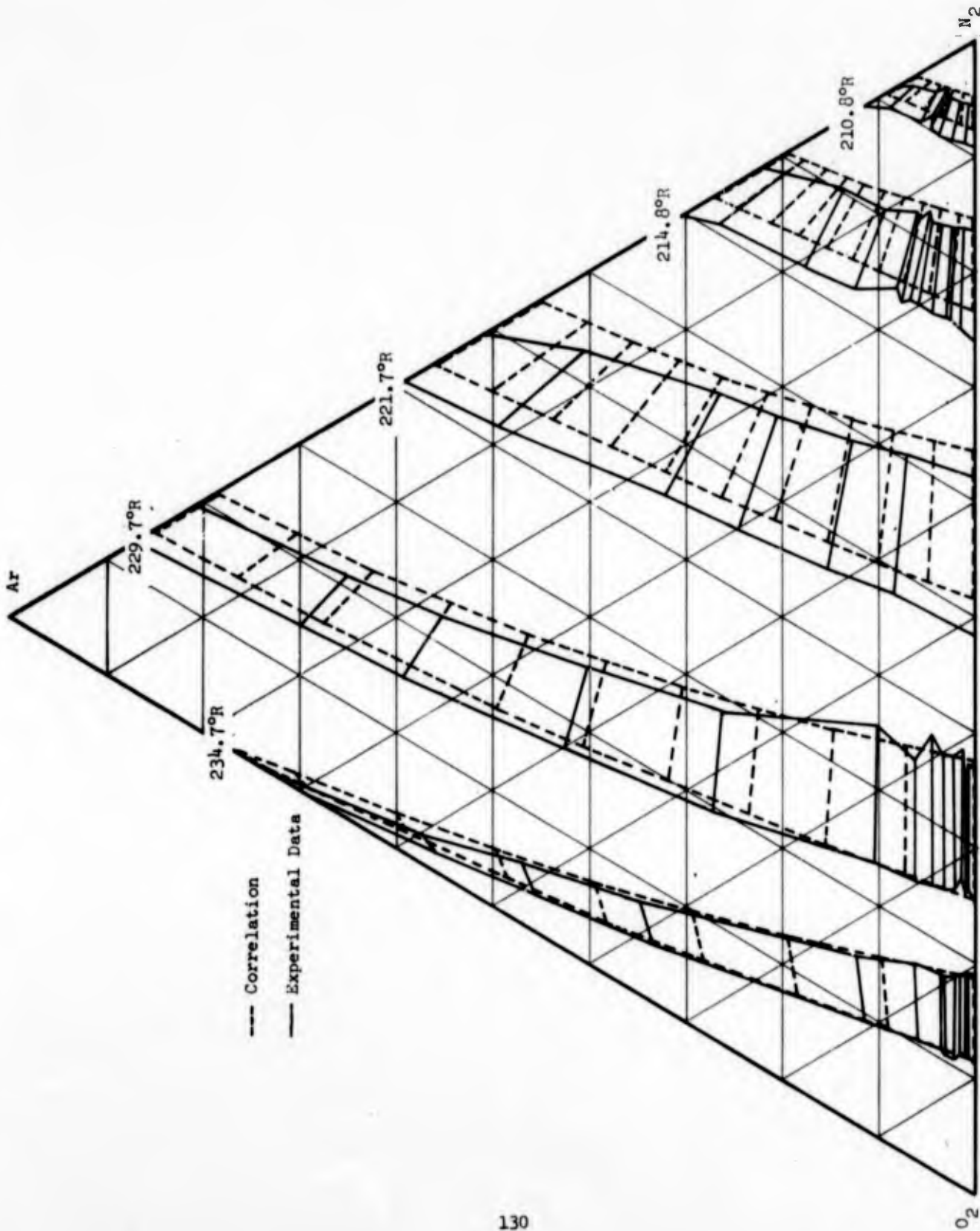


Figure 76. Comparison of Experimental Data and the Correlation, 20 Atmospheres.

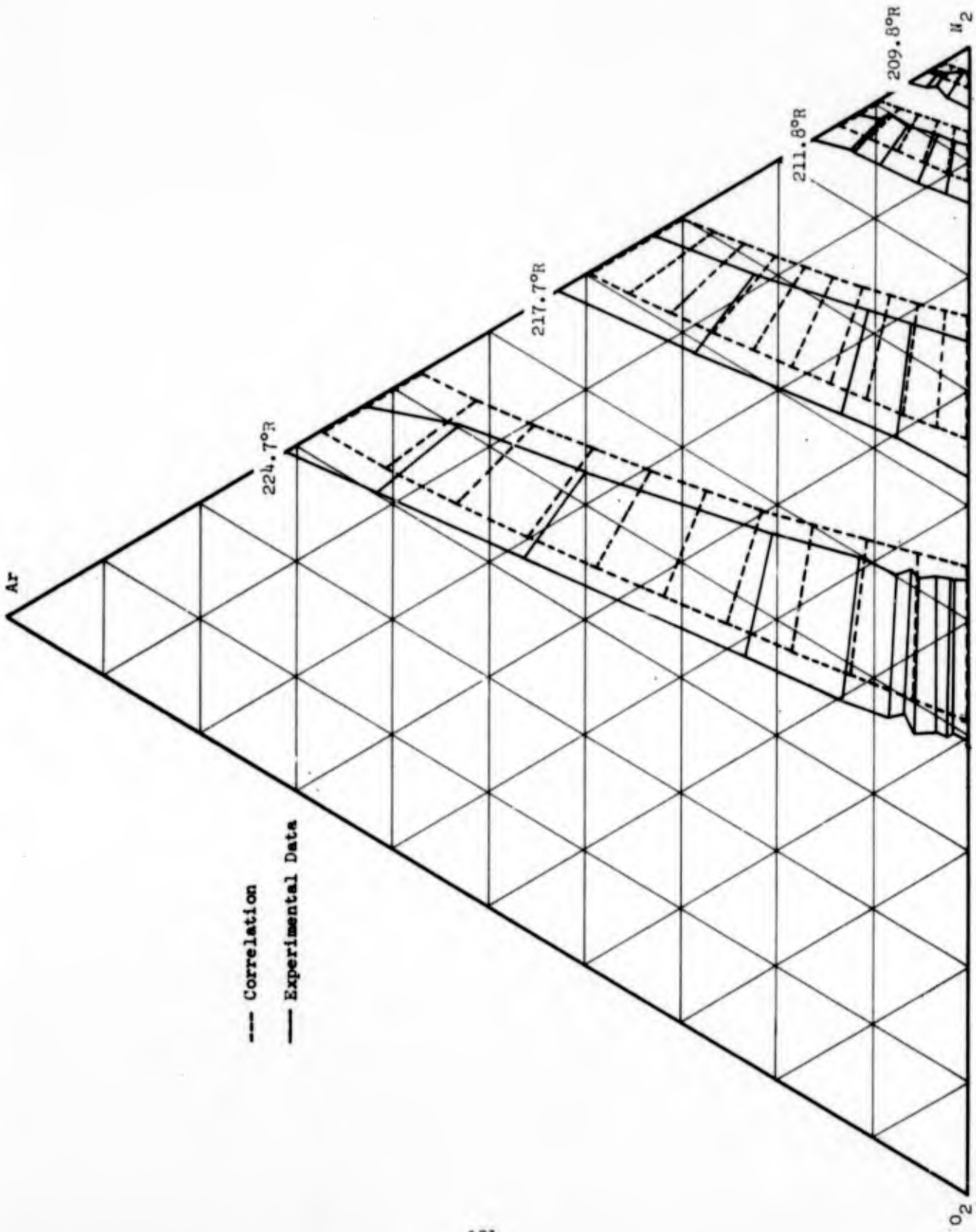


Figure 77. Comparison of Experimental Data and the Correlation, 20 Atmospheres.

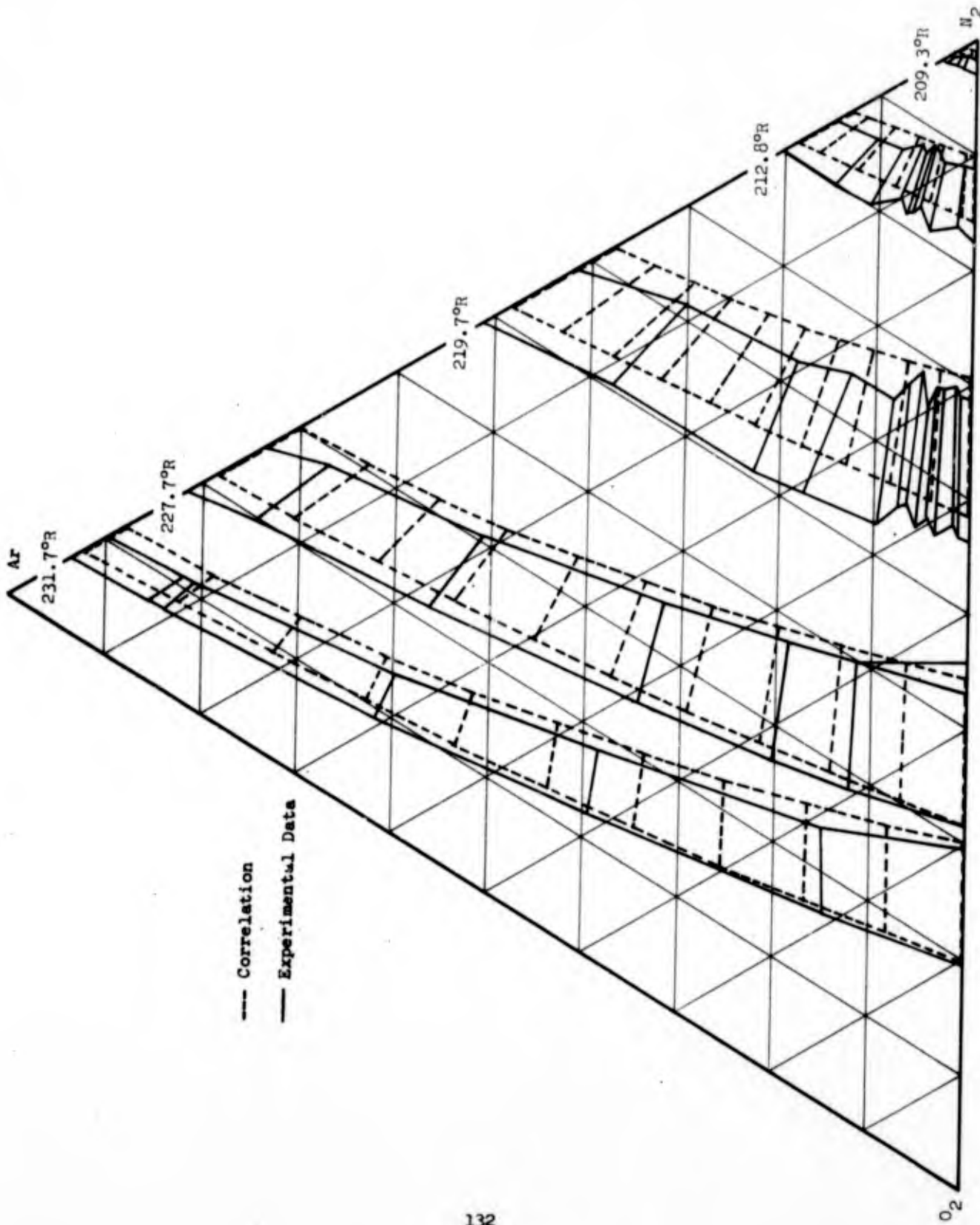


Figure 78. Comparison of Experimental Data and the Correlation, 20 Atmospheres.

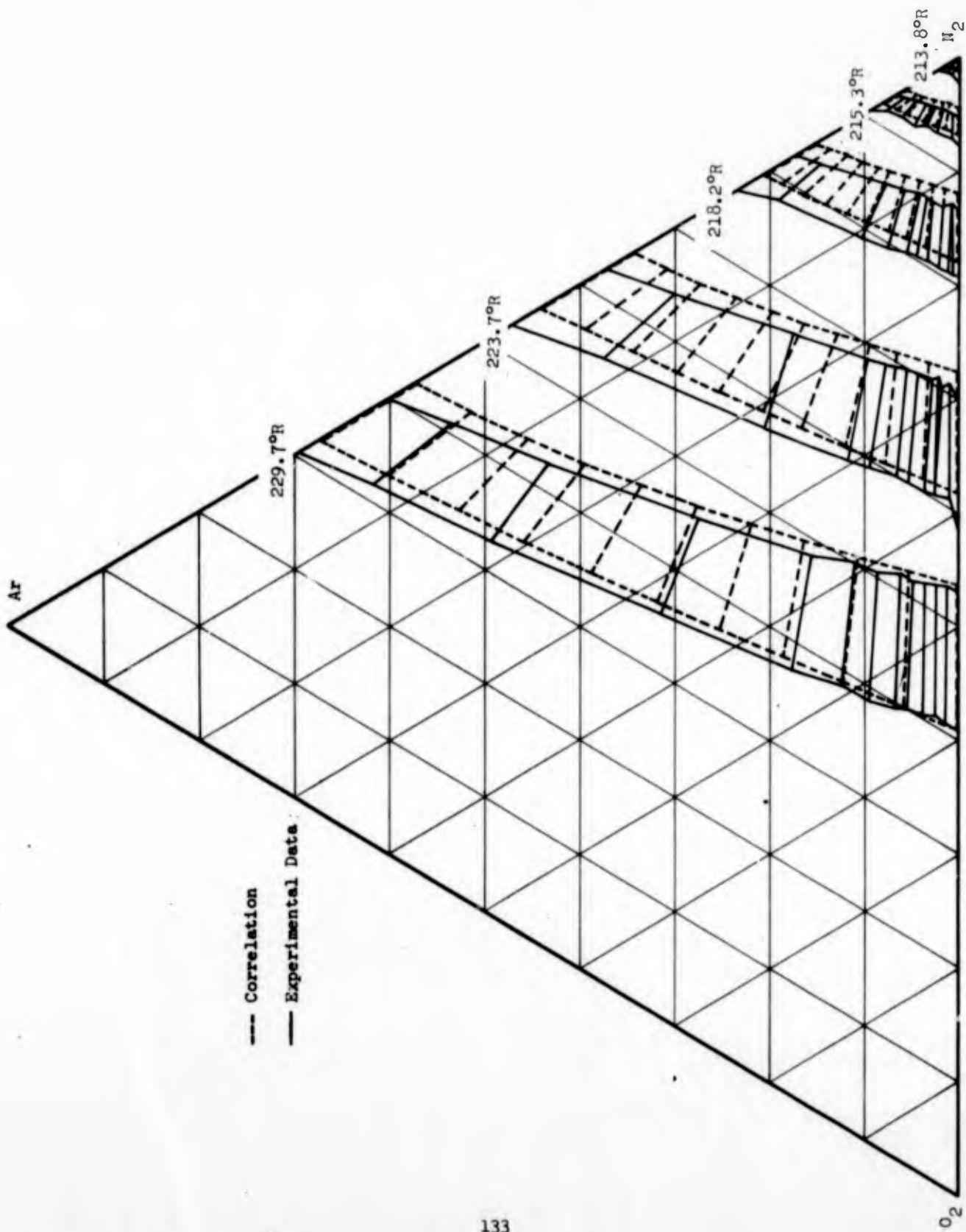


Figure 79. Comparison of Experimental Data and the Correlation, 23 Atmospheres.

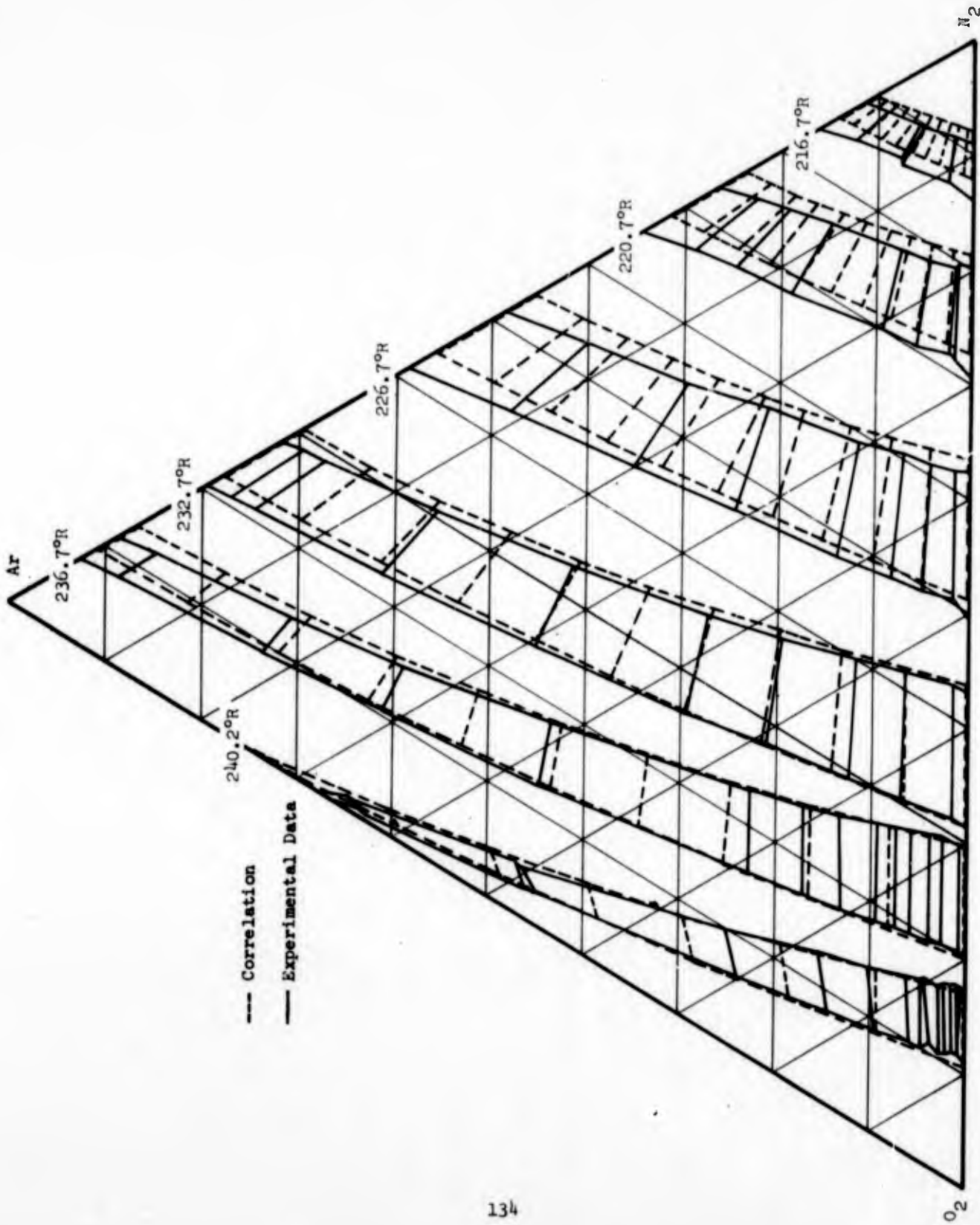


Figure 80. Comparison of Experimental Data and the Correlation, 23 Atmospheres.

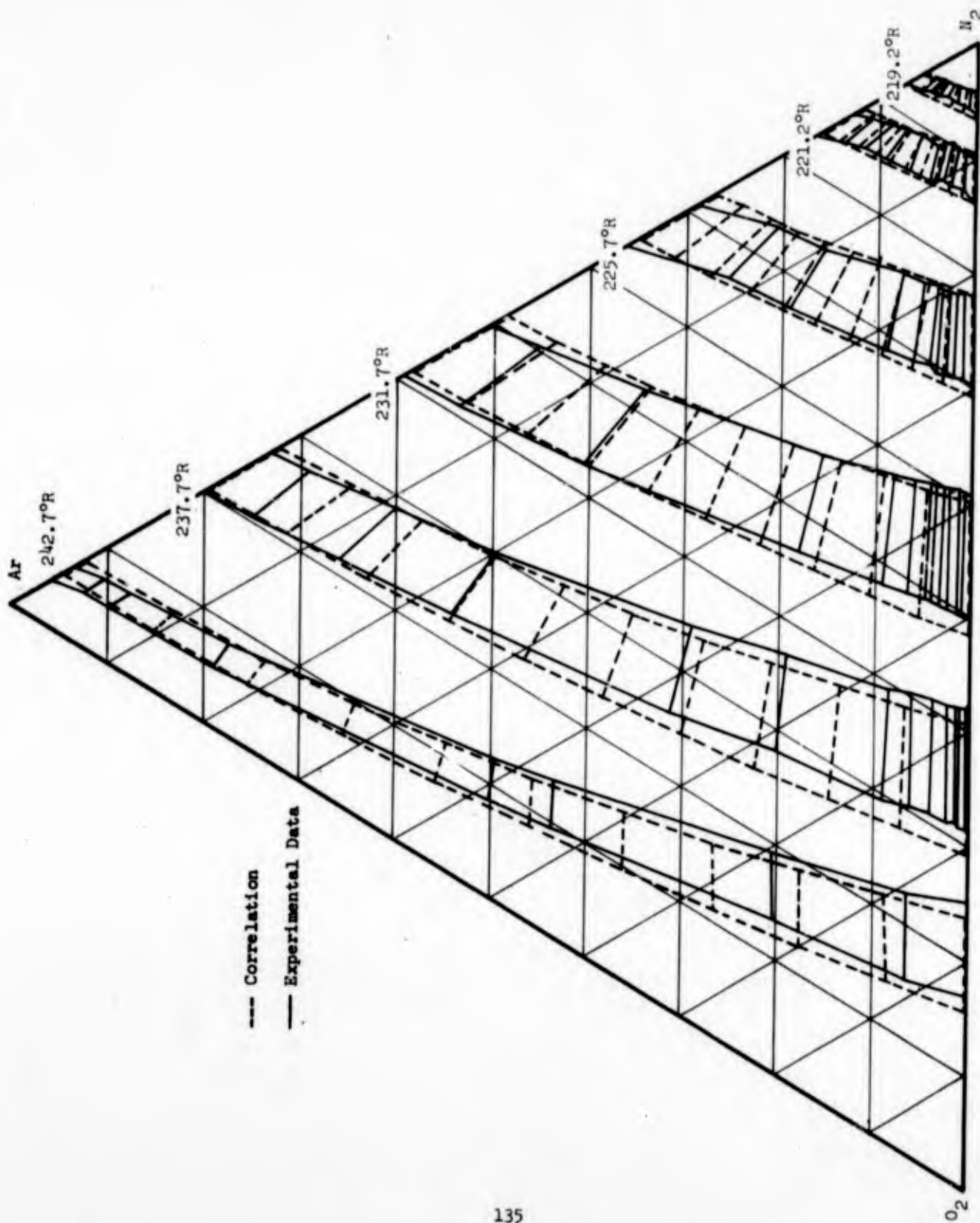


Figure 81. Comparison of Experimental Data and the Correlation, 26 Atmospheres.

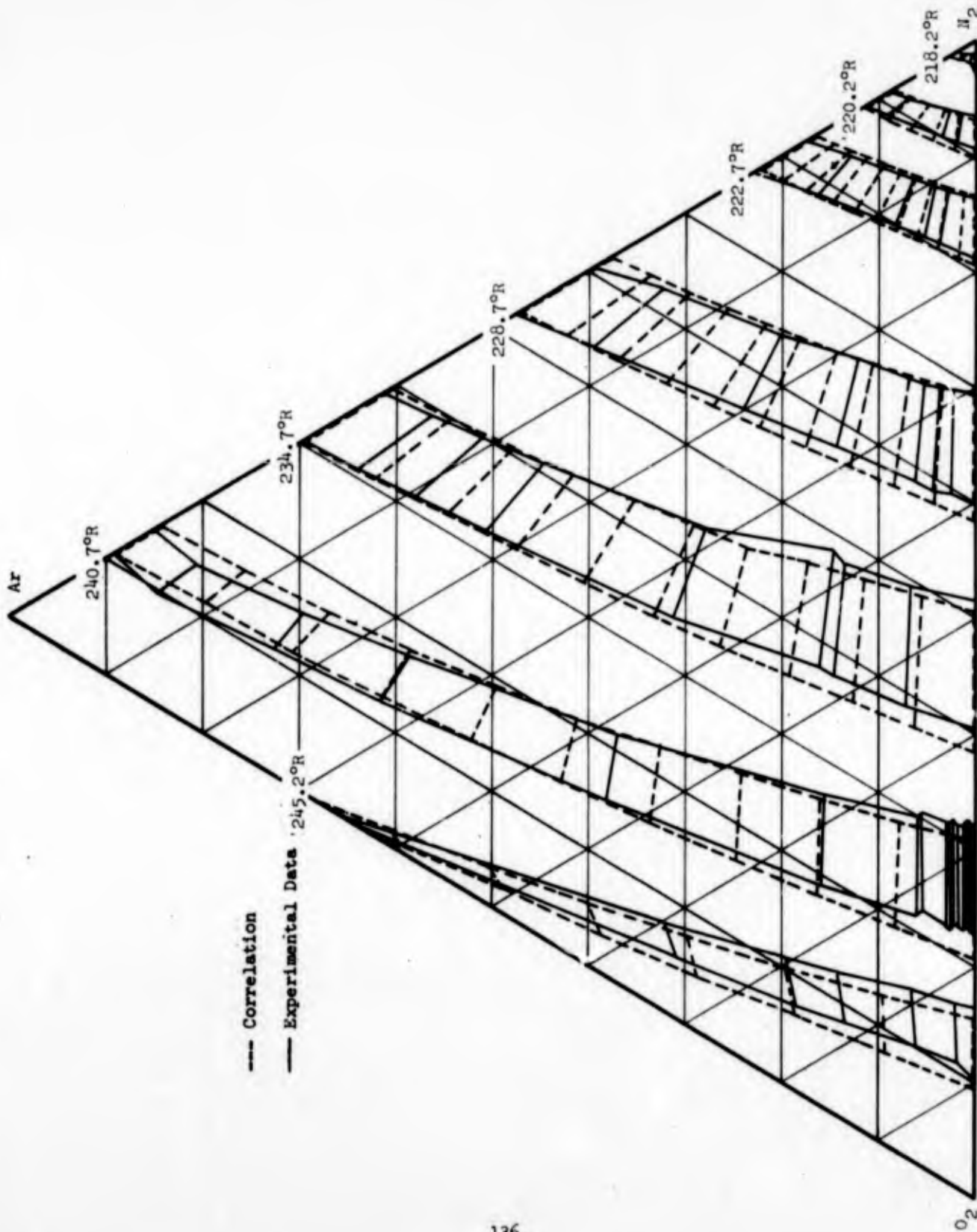


Figure 82. Comparison of Experimental Data and the Correlation, 26 Atmospheres.

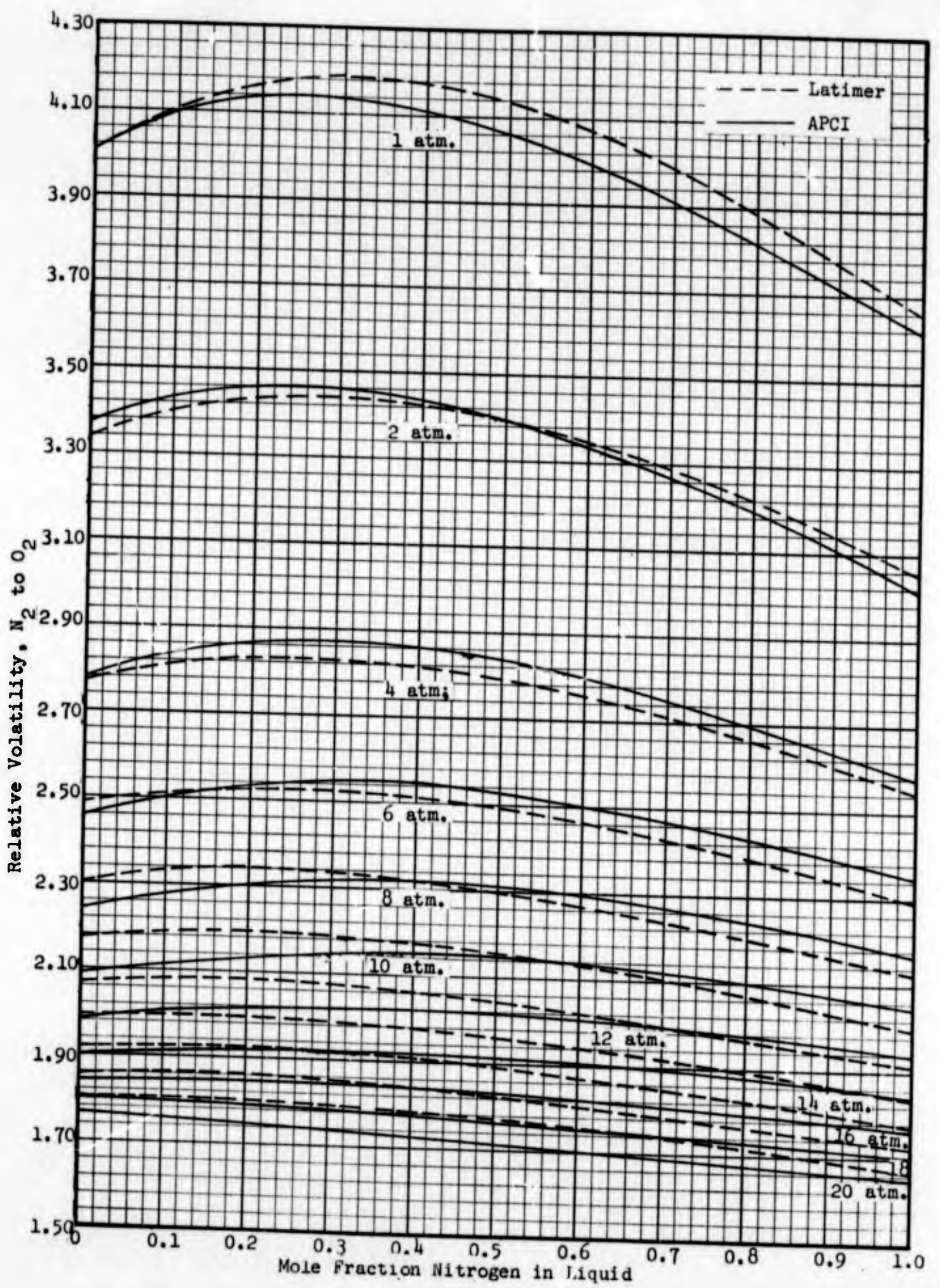


Figure 83. Comparison of APCI Correlation to Latimer Correlation for Nitrogen-Oxygen System.

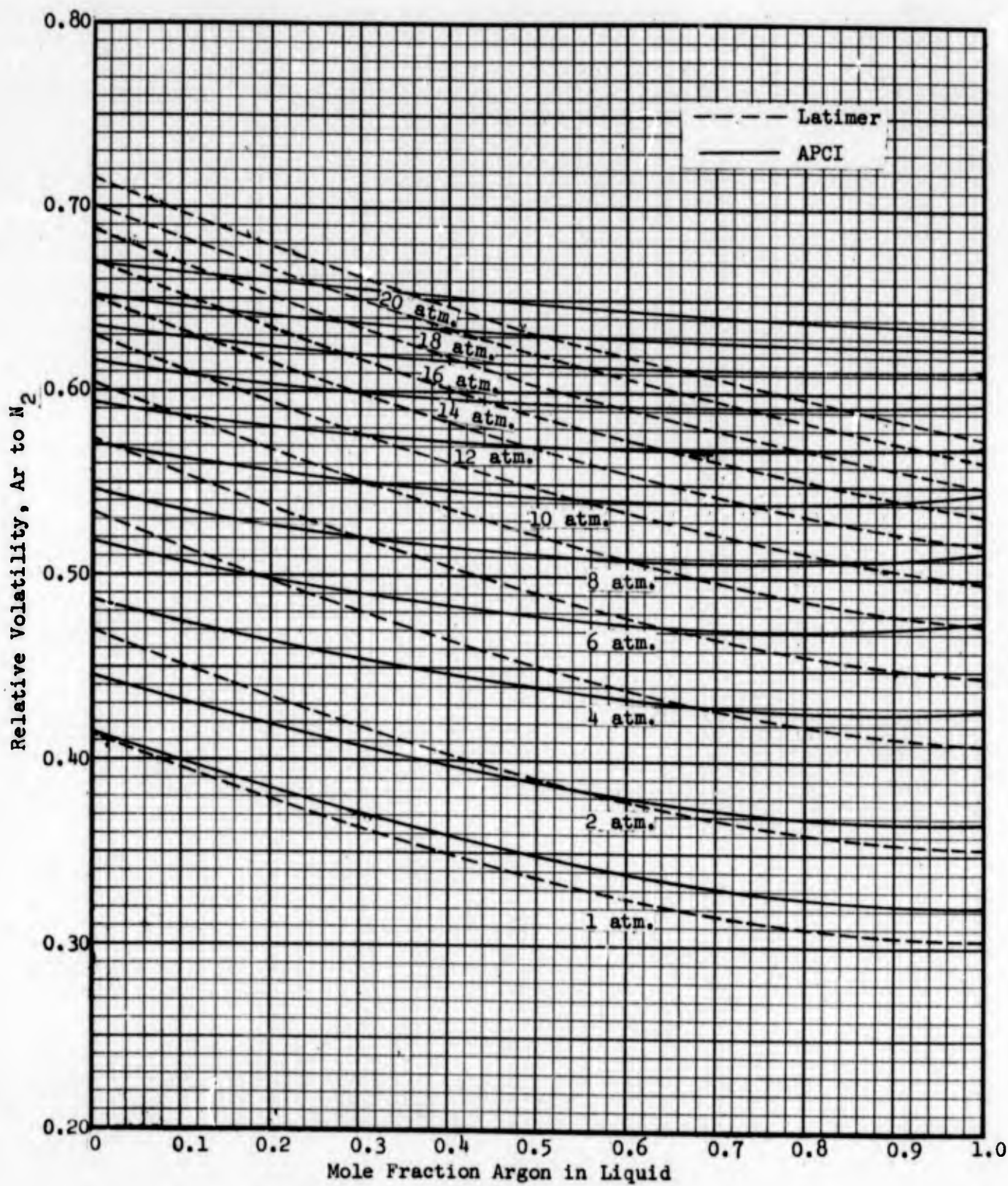


Figure 84. Comparison of APCI Correlation to Latimer Correlation for Argon-Nitrogen System.

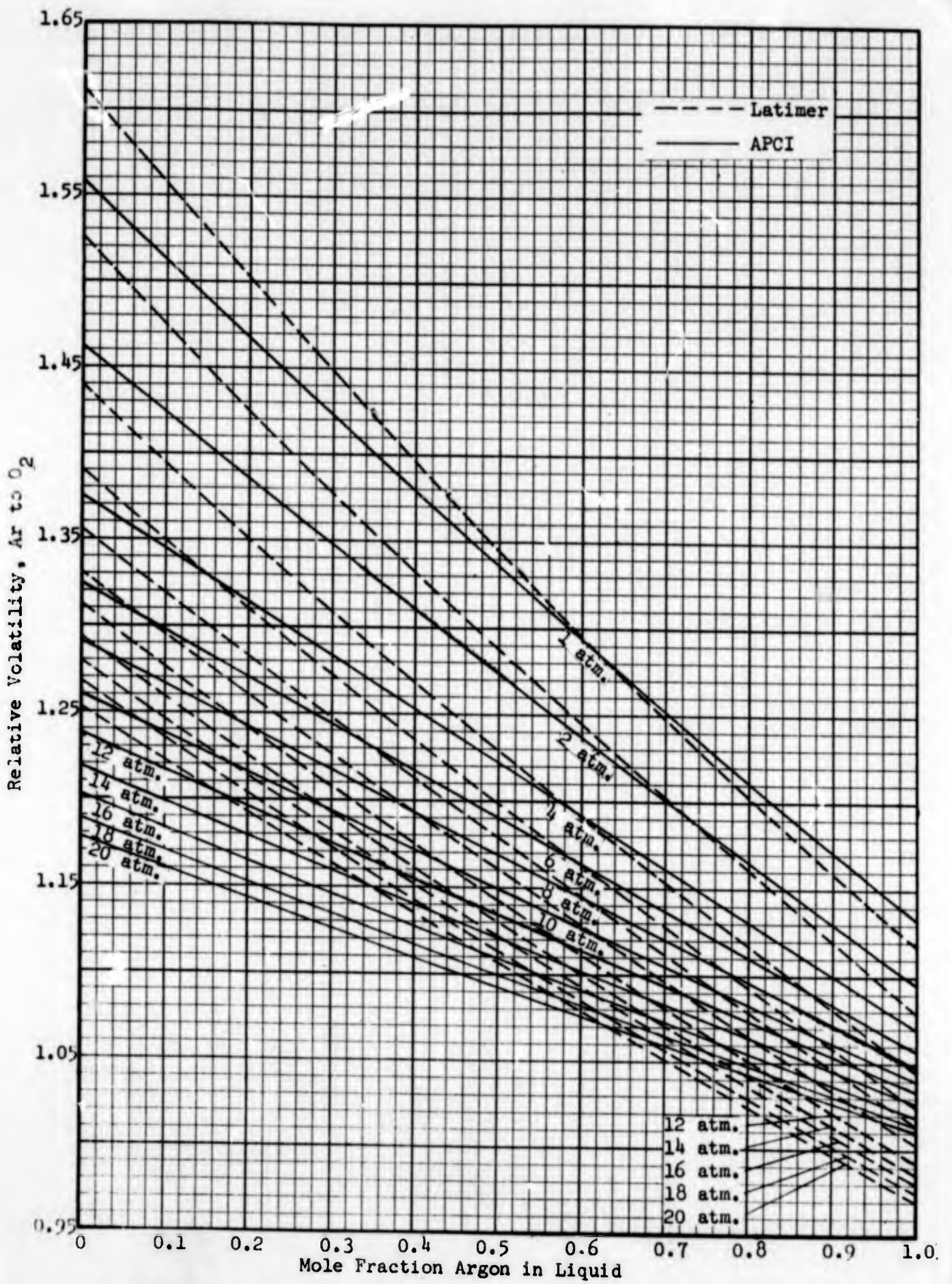


Figure 85. Comparison of APCI Correlation to Latimer Correlation for Argon-Oxygen System.

VIII. ENTHALPY CORRELATION

Enthalpy data obtained from the literature were correlated for computer usage in calculating the enthalpy of the vapor and enthalpy of the liquid according to the equations

$$H_{\text{vap.}} = \sum_i x_i H_i^* + \sum_i x_i (H_{g_i} - H_i^*) \quad (22)$$

$$H_{\text{liq.}} = \sum_i x_i H_i^* + \sum_i x_i (H_{g_i}^{\circ} - H_i^*) - \sum_i x_i \Delta H_{vi}^{\circ} \\ + \sum_i x_i V_i^{\circ} (p - p_i^{\circ}) + \sum_i x_i \Delta \bar{H}_{m_i} \quad (23)$$

Reported below are the correlations to the data with referencing and commentary about accuracy.

 A. Heat of Mixing

1. Argon-Oxygen - The data of Pool and co-workers⁽³⁵⁾ at 84°K appear more consistent than that of Knobler and co-workers⁽³⁶⁾ at 86°K. Pool's least squares fit of the data converted to BTU/lb-mole is:

$$H_m = x_{O_2} x_{Ar} [103 + 13.5 (x_{O_2} - x_{Ar})] \quad (24)$$

2. Nitrogen-Argon - The only data found were that of Pool and co-workers⁽³⁵⁾ at 84°K. Their least squares fit converted to BTU/lb-mole is:

$$H_m = x_{Ar} x_{N_2} [86.9 - 23.2 (x_{Ar} - x_{N_2})] \quad (25)$$

3. Nitrogen-Oxygen - The only data found were that of Knobler, van Heijningen and Beenakker⁽³⁶⁾ at 77°K. Weighting the points at oxygen mole fraction of 0.14 half as heavily as the rest, a method of averages curve fit gives within 10% accuracy:

$$H_m = x_{N_2} x_{O_2} [82.8 + 29 (x_{O_2} - x_{N_2})] \text{ BTU/lb-mole.} \quad (26)$$

For a heat of mixing of the form $H_m = x_1 x_2 [A + B (x_1 - x_2)]$, the partial molal heat of mixing is:

$$\overline{\Delta H_{m1}} = x_2^2 [A + B (3x_1 - x_2)] \quad (27)$$

$$\overline{\Delta H_{m2}} = x_1^2 [A + B (x_1 - 3x_2)] \quad (28)$$

B. Ideal Gas Heat Capacity 140-250°R

1. Argon - from Nat. Bur. Stds.⁽³⁷⁾: $C_p^\circ = 4.9647 \text{ BTU/mole } ^\circ\text{R}$ (29)

2. Oxygen - tabulation by Wooley⁽³⁸⁾: $C_p^\circ = 6.9558 \text{ BTU/mole } ^\circ\text{R}$ (30)

3. Nitrogen - from Goff and Gratch⁽³⁹⁾. Least squares curve fit:
 $C_p^\circ = 6.950571 + 0.27735687 \times 10^{-5}T + 0.3438922 \times 10^{-8}T^2$ (31)
 Sum of squares error = 1×10^{-9} .

C. Latent Heat

1. Nitrogen - The correlation is a least squares curve fit of the data from Mage, Jones, Katz, and Roebuck⁽⁴⁰⁾ and of Strobridge⁽⁴¹⁾
 ΔH_{vi}° in BTU/lb-mole, T in °R.

$$\ln \Delta H_{vi}^\circ = 6.36376 + 0.121474 \ln (226.91 - T) + 0.0880106 [\ln (226.91 - T)]^2 - 0.00987388 [\ln (226.91 - T)]^3 \quad (32)$$

Root mean square error = 8.1 BTU/lb-mole

A simpler fit is: $\ln \Delta H_{vi}^\circ = 6.19701 + 0.354836 \ln (226.91 - T)$ (33)

Root mean square error = 22 BTU/lb-mole

2. Argon - The correlation is a least squares curve fit of the data of Flubacher, Leadbetter, and Morrison⁽⁴²⁾ and of Din⁽⁴⁾.

ΔH_{vi}° in BTU/lb-mole, T in °R

$$\ln \Delta H_{vi}^\circ = 7.35231 - 0.733687 \ln (271.30 - T) + 0.331584 [\ln (271.30 - T)]^2 - 0.0317968 [\ln (271.30 - T)]^3 \quad (34)$$

Root mean square error = 2.8 BTU/lb-mole

A simpler fit is: $\ln \Delta H_{vi}^\circ = 6.20952 + 0.366142 \ln (271.30 - T)$ (35)

Root mean square error = 27.6 BTU/lb-mole

3. Oxygen - The correlation is a least squares fit synthesized from the data given by Fukurawa and McCoskey⁽⁴³⁾, Alikhanov⁽⁴⁴⁾, Claitor and Crawford⁽⁴⁵⁾ and the graphical data of Wilbers⁽⁴⁶⁾.

ΔH_{vi}° in BTU/lb-mole, T in °R

$$\ln \Delta H_{vi}^{\circ} = 5.61017 + 0.733877 \ln (278.60 - T) - 0.0572340 [\ln (278.60 - T)]^2 + 0.0016562 [\ln (278.60 - T)]^3 \quad (36)$$

Root mean square error = 6.9 BTU/lb-mole

$$\text{A simple fit is: } \ln \Delta H_{vi}^{\circ} = 6.16014 + 0.384736 \ln (278.60 - T) \quad (37)$$

Root mean square error = 77 BTU/lb-mole

- D. Enthalpy of the Real Gas - The commonly used symbol $(H - H^*)_T$ represents the effect of pressure at constant temperature on the enthalpy of a real gas. This quantity can be computed from the virial equation of state terminating with the third virial coefficient.

$$\frac{PV}{RT} = Z = 1 + \frac{B}{V} + \frac{C}{V^2} \quad (38)$$

Since B and C are functions of temperature only, the following equation is derived:

$$\frac{(H_{gi} - H_i^*)_T}{RT} = \left[\frac{1}{V} (B - T \frac{dB}{dT}) + \frac{1}{V^2} (C - \frac{1}{2} T \frac{dC}{dT}) \right] \quad (39)$$

The coefficients for argon, oxygen, and nitrogen are given in Section VID.

- E. Saturated Pure Component Heat Capacity

1. Argon Liquid - from WADD Compendium⁽⁵⁾

$$C_p = 0.22 + 0.00468 \frac{T}{(151 - T)^{1/2}} \quad (40)$$

C_p units cal/gm-°K, T in °K

2. Oxygen Liquid - insufficient data to correlate.

3. Nitrogen Liquid - Correlation of Strobridge⁽⁴¹⁾

$$C_s = \frac{6.24688186T}{(126.26-T)^2} + 39.39006895 + 0.6821295539T - 0.01052432772T^2 \quad (41)$$

$$+ 0.00006001046981T^3$$

C_s units joule/gm-mole °K, T in °K

4. Argon Vapor - from Din⁽⁴⁾

$$C_s = 325.63362 - 8.8669510T + 0.08828184T^2 - 0.00031196544T^3 \quad (42)$$

C_s units joule/gm-mole °K, T in °K

5. Oxygen Vapor - from Claitor and Crawford⁽⁴⁵⁾

$$C_s = -468.26228 - 2.6649068T + 0.010328679T^2 + 9.0958184 \times 10^{-5}T^3 \quad (43)$$

$$+ 1.4860065 \times 10^{-7}T^4$$

C_s units BTU/lb-mole °F, T in °F

6. Nitrogen Vapor - from Strobridge⁽⁴¹⁾

$$C_s = 48.332643 - 0.7791322T - 0.0065282424T^2 + 1.7403752 \times 10^{-4}T^3 \quad (44)$$

$$- 7.9049655 \times 10^{-7}T^4$$

C_s units joule/gm °K, T in °K

Enthalpy data presented in the Appendix were calculated for the vapor from the virial equation of state and the ideal gas heat capacities; the reference state is the ideal gas at 0°R. The liquid enthalpy was calculated from a curve fit of liquid enthalpy data for the pure components calculated from the latent heat of vaporization and the enthalpy of the vapor. The

following are the analytical equations obtained for the saturated liquid enthalpy of nitrogen, argon, and oxygen; temperature in °R.

Nitrogen:

$$H_{\text{liq.}} = -9774 + 158.74T - 1.2087T^2 + 4.3451 \times 10^{-3}T^3 - 5.589 \times 10^{-6}T^4 \quad (45)$$

Argon:

$$H_{\text{liq.}} = -3634 + 12.71T - 2.976 \times 10^{-2}T^2 + 6.08 \times 10^{-5}T^3 + 1.418 \times 10^{-7}T^4 \quad (46)$$

Oxygen:

$$H_{\text{liq.}} = -882 - 56.32T + 0.58608T^2 - 2.2058 \times 10^{-3}T^3 + 3.131 \times 10^{-6}T^4 \quad (47)$$

Based upon the scatter in the experimental enthalpy data, these equations are estimated to be correct within + 20 BTU/lb-mole. Because of this large uncertainty no correction was made for the effect of the heat of mixing and the effect of pressure on the enthalpy of the liquid. The enthalpy was calculated simply as

$$H_{\text{liq.}} = \sum_i x_i H_{i \text{ liq.}} \quad (48)$$

The correction for the heat of mixing varies up to 25 BTU/lb-mole and the correction for the effect of pressure on the enthalpy is only significant at the higher pressures where it varies up to 40 BTU/lb-mole. A check on the thermodynamic consistency of the data was made by comparison of calculated values of the saturated heat capacity with experimental data by means of the following equation neglecting the second term.

$$C_{\text{sat.}} = \left(\frac{\partial H}{\partial T} \right)_{\text{sat.}} - v \left(\frac{\partial p}{\partial T} \right)_{\text{sat.}} \quad (49)$$

The comparison of the data is given in Table 24.

At low temperatures the calculated and experimental heat capacities are in good agreement for nitrogen and oxygen, and somewhat poorer agreement for argon. The largest deviations of about 10% occur at high temperatures where the effect of pressure on the enthalpy may begin to be significant. The agreement is considered good enough that the calculated heat capacities given in the appendix are based upon a temperature differentiation of the enthalpy equations.

TABLE 24

COMPARISON OF CALCULATED AND EXPERIMENTAL
SATURATED LIQUID HEAT CAPACITIES, BTU/lb-MOLE-°R

Temperature °F	Nitrogen		Argon		Oxygen	
	Exp. (41)	Calc.	Exp. (5)	Calc.	Exp. (47)	Calc.
-320	12.8	12.4
-310	13.9	14.0	10.7	9.8	12.9	12.9
-300	14.2	14.1	10.9	10.2	13.0	13.1
-290	14.6	14.6	11.2	10.6	13.2
-280	15.1	15.5	11.5	11.2	13.3
-270	15.8	16.6	11.7	11.9	13.4
-260	16.9	17.8	12.0	12.6	13.6
-250	18.9	18.9	12.2	13.5	14.0
-240	13.1	14.4	14.6
-230	14.6	15.5	15.6

IX. REFERENCES

1. F. P. Stein, C. J. Sterner, and J. M. Geist, Chem. Eng. Progress, 58, No. 11, 70 (1962).
2. C. J. Sterner, Review of Scientific Instruments, 31, No. 10, 1159 (1960).
3. L. Israel, C. J. Sterner, and G. M. Wilson, Argon-Oxygen-Nitrogen Three Component System Experimental Vapor-Liquid Equilibrium Data, Air Products and Chemicals Quarterly Progress Report I, Contract No. AF 33(657)-8742, October 1962.
4. F. Din, Editor, Thermodynamic Functions of Gases, 2, Butterworths Scientific Publications, London, 1956.
5. V. J. Johnson, Editor, "The Compendium", WADD Tech. Rept. 6056 (1961).
6. J. G. Aston and G. W. Moessen, J. Chem. Phys., 21, 948 (1953).
7. L. Riedel, Chem. Ing. Tech., 26, 83 (1954).
8. B. F. Dodge and H. N. Davis, J. Amer. Chem. Soc., 49, 610 (1927).
9. F. Henning and W. Heuse, Z. Physik, 23, 105 (1924).
10. J. G. Aston, E. Willihinganz and G. H. Messerly, J. Am. Chem. Soc., 57, 1642 (1935).
11. H. J. Hoge, The NBS-NACA Table of Thermal Properties, Table 9.50 (1949).
12. H. J. Hoge, J. Res. Nat. Bur. Stds., 44, 321 (1950).
13. G. T. Armstrong, J. Res. Nat. Bur. Stds., 53, No. 4, 263 (1954).
14. A. Michels, T. Wassenaar, W. DeGraaff, and C. Prins, Physica, 19, 26 (1953).
15. W. F. Giaque and J. O. Clayton, J. Am. Chem. Soc., 55, 4875 (1933).
16. M. P. Freeman and G. D. Halsey, Jr., J. Phys. Chem., 60, 1119 (1956).
17. F. Din, J. Robb, and A. M. Clark, Physica, 17, 876 (1951).
18. K. Pitzer and R. F. Curl, J. Am. Chem. Soc., 79, 2369 (1957).

19. J. Prausnitz, A.I.Ch.E. Journal, 5, 3 (1959).
20. L. Holborn and J. Otto, Zeit. F. Physik, 33, 1 (1925).
21. T. T. H. Verschoyle, Proc. Roy. Soc. A, 111, 552 (1926).
22. H. Kamerlingh Onnes and H. W. Van Urk, Comm. Lab. Leiden 169, d, e, (1924).
23. J. Otto, A. Michels, and H. Wouters, Phys. Zeit., 35, 97 (1934).
24. A. Michels, H. Wouters, and J. deBoer, Physica, 1, 587 (1934).
25. A. Michels, R. J. Lunbeck, and G. J. Wolkers, Physica, 17, 801 (1951).
26. A. Michels, H. Wijker, and H. K. Wijker, Physica, 15, 627 (1949).
27. C. C. Tanner and I. Masson, Proc. Roy. Soc. A 126 (1930).
28. H. Kamerlingh Onnes and G. Crommelin, Comm. Lab. Leiden, 118, b (1910).
29. H. A. Kuypers and H. K. Onnes, Arch. Heerlandaises, 6, 277 (1923).
30. G. P. Nijhoff and W. H. Keesom, Comm. Lab. Leiden 179, b (1925).
31. C. M. Knobler, J. J. M. Beenaker, and H. F. P. Knaap, Physica, 25, 909 (1959).
32. J. P. Kuennen, T. Verschoyle, and A. Tk. Van Urk, Comm. Phys. Lab. Leiden, No. 161 (1922).
33. F. M. Penning, Comm. Phys. Lab. Leiden, No. 166 (1923).
34. R. E. Latimer, A.I.Ch.E. Journal, 3, 75 (1957).
35. R. A. H. Pool, G. Saville, T. M. Herrington et al, Trans. Faraday Soc., 58, 1692 (1962).
36. K. M. Knobler, J. J. Van Heijningen, and J. S. M. Beenakker, Physica, 27, 296 (1961).
37. J. Hilsenrath, C. W. Beckett, W. S. Benedict et al, Nat. Bur. Stds. Circular 564, 132 (1955).
38. H. W. Wooley, J. Res. Nat. Bur. Stds., 40, 163 (1948).

39. J. A. Goff, and S. Gratch, Trans. ASME, 72, 741 (1950).
40. D. T. Mage, M. L. Jones, Jr., O. L. Katz, and J. R. Roebuck, Chem. Eng. Prog. Symposium Series, 59:44, 61 (1963).
41. T. R. Strobridge, NBS Technical Note 129, 17 (Jan. 1962).
42. P. Flubacher, A. J. Leadbetter, and J. A. Morrison, Proc. Phys. Soc. (London), 72, 1449 (1961).
43. G. T. Furukawa and R. E. McCoskey, National Advisory Committee for Aeronautics Technical Note 2969, 13 (1953).
44. R. A. Alikhanov, J. Exper. Theor. Phys. U.S.S.R., 2, 771 (1956).
45. L. C. Claitor and D. B. Crawford, Trans. ASME, 71 (1949).
46. O. J. Wilbers, "Thermodynamic Properties of Oxygen-Nitrogen Mixtures", ASD TR61-699, Vol. I, Part II (1963).
47. W. F. Giauque and H. L. Johnston, J. Am. Chem. Soc., 51, 2300 (1929).

APPENDIXES

	<u>Page</u>
I. Graphical Presentation of Correlation	150
A. K-Values Vs. Pressure	150
B. Relative Volatility of Argon to Nitrogen in Ternary System	176
C. Relative Volatility of Argon to Oxygen in Ternary System	188
D. Relative Volatility of Argon to Nitrogen, Binary System	200
E. Relative Volatility of Argon to Oxygen, Binary System	202
F. Pressure Activity Coefficients	204
G. Mixture Vapor Pressures Vs. Temperature	244
II. Tabular Presentation of Correlation	260
A. Isobaric Table	260
B. Isothermal Table	274
III. Bibliography from Literature Search	294
IV. Nomenclature Table	312

APPENDIX I

GRAPHICAL PRESENTATION OF CORRELATION

A. K-Values Vs. Pressure

The 36 graphs to follow present the K-values defined as:

$$K_i = \frac{y_i}{x_i} \quad (50)$$

of the three components as a function of pressure along selected isotherms. Envelopes defining the binary compositions are drawn as dashed lines.

The graphs are grouped in order of component: nitrogen, argon, oxygen. Inside each group they are ordered with respect to increasing mole fraction nitrogen in the liquid.

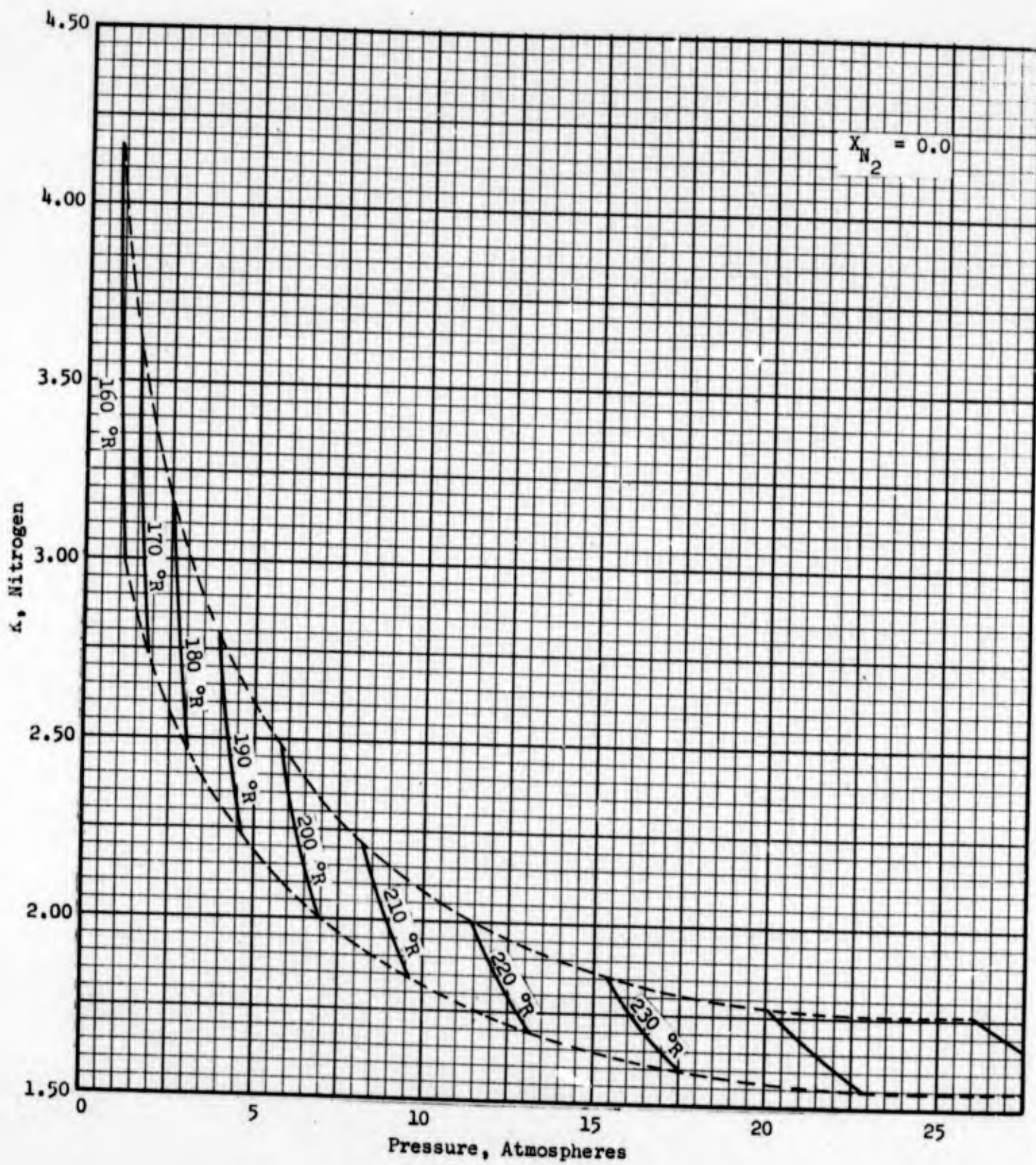


Figure 86. K-Values of Nitrogen.

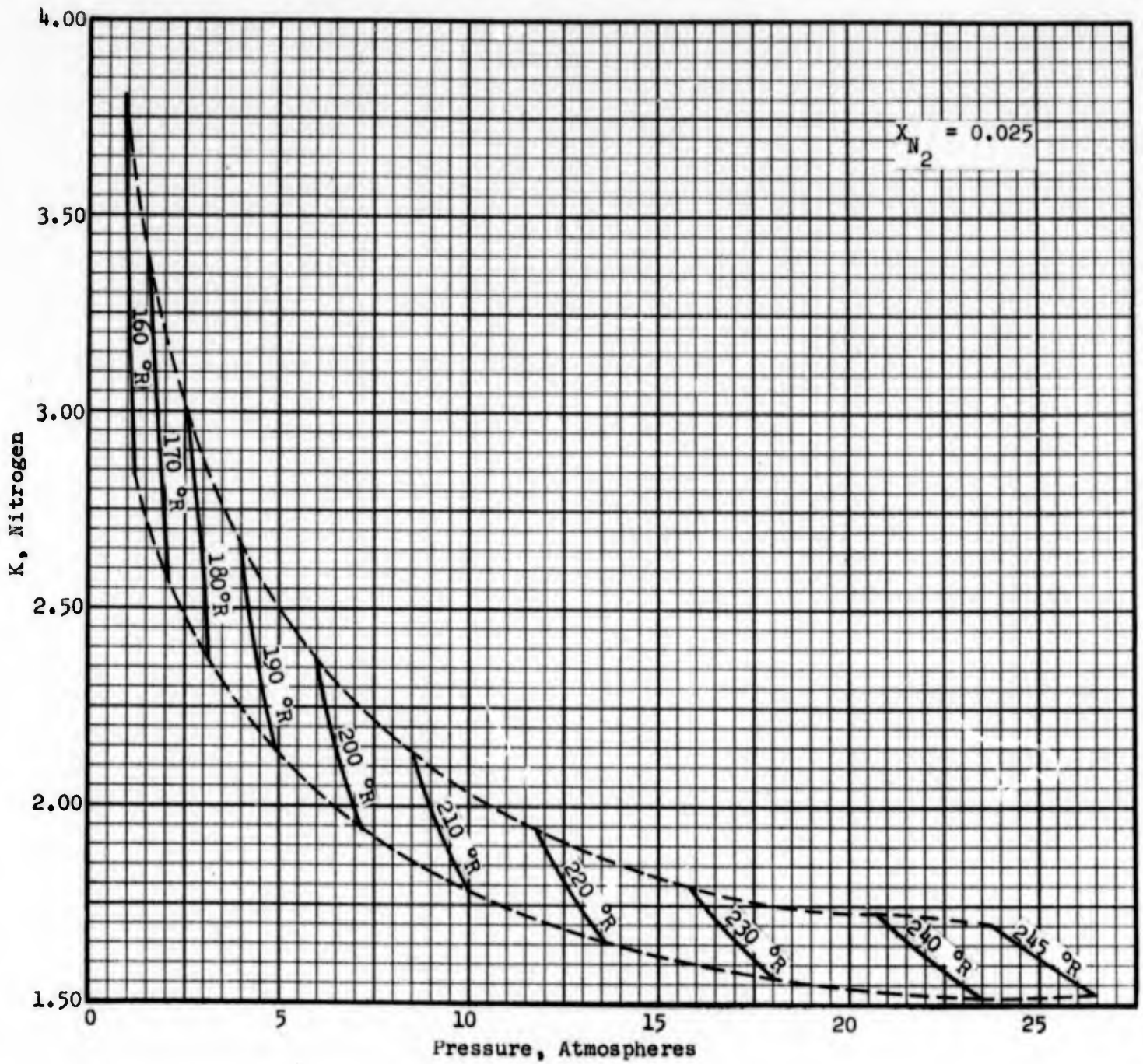


Figure 87. K-Values of Nitrogen.

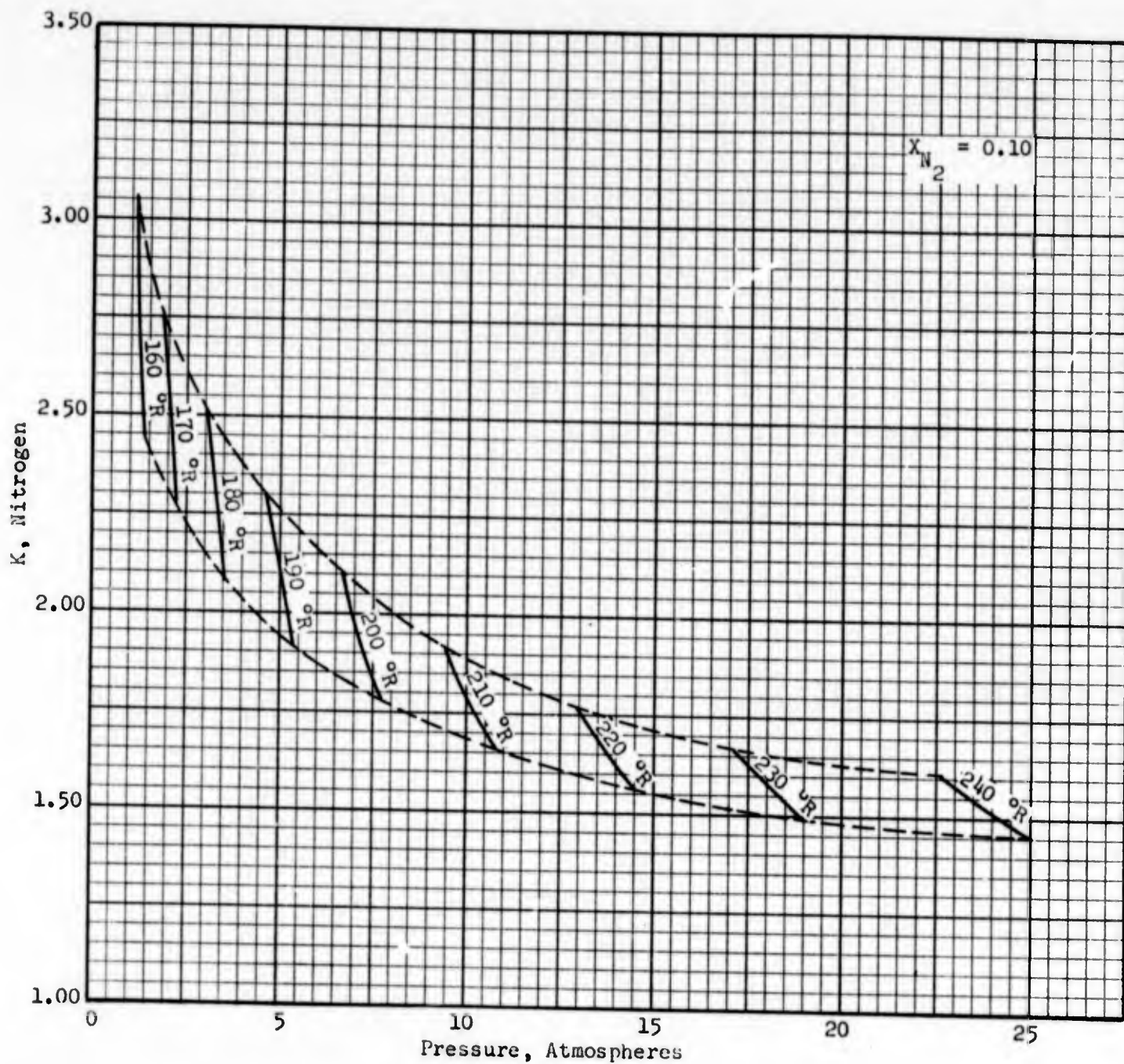


Figure 88. K-Values of Nitrogen.

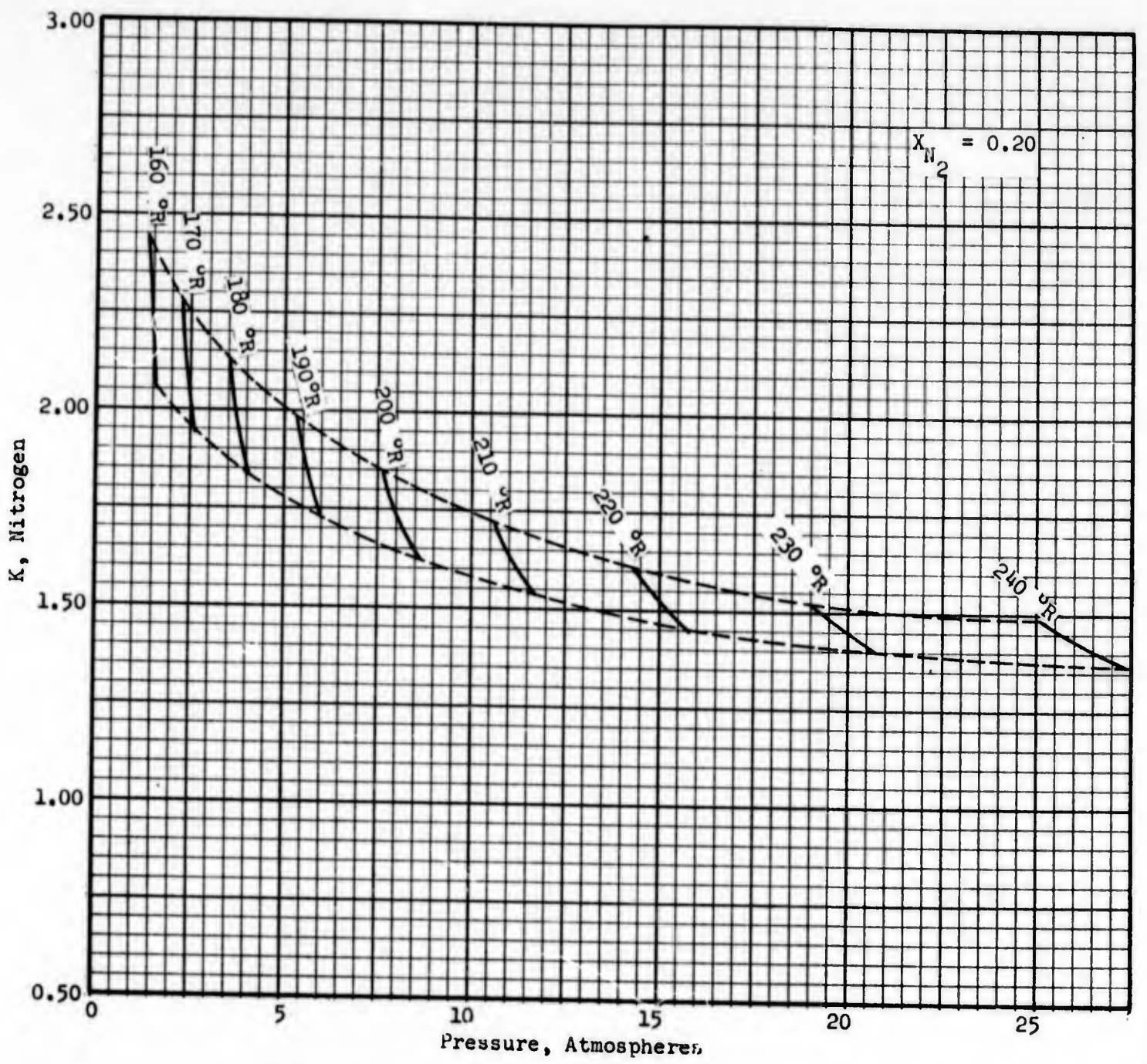


Figure 89. K-Values of Nitrogen.

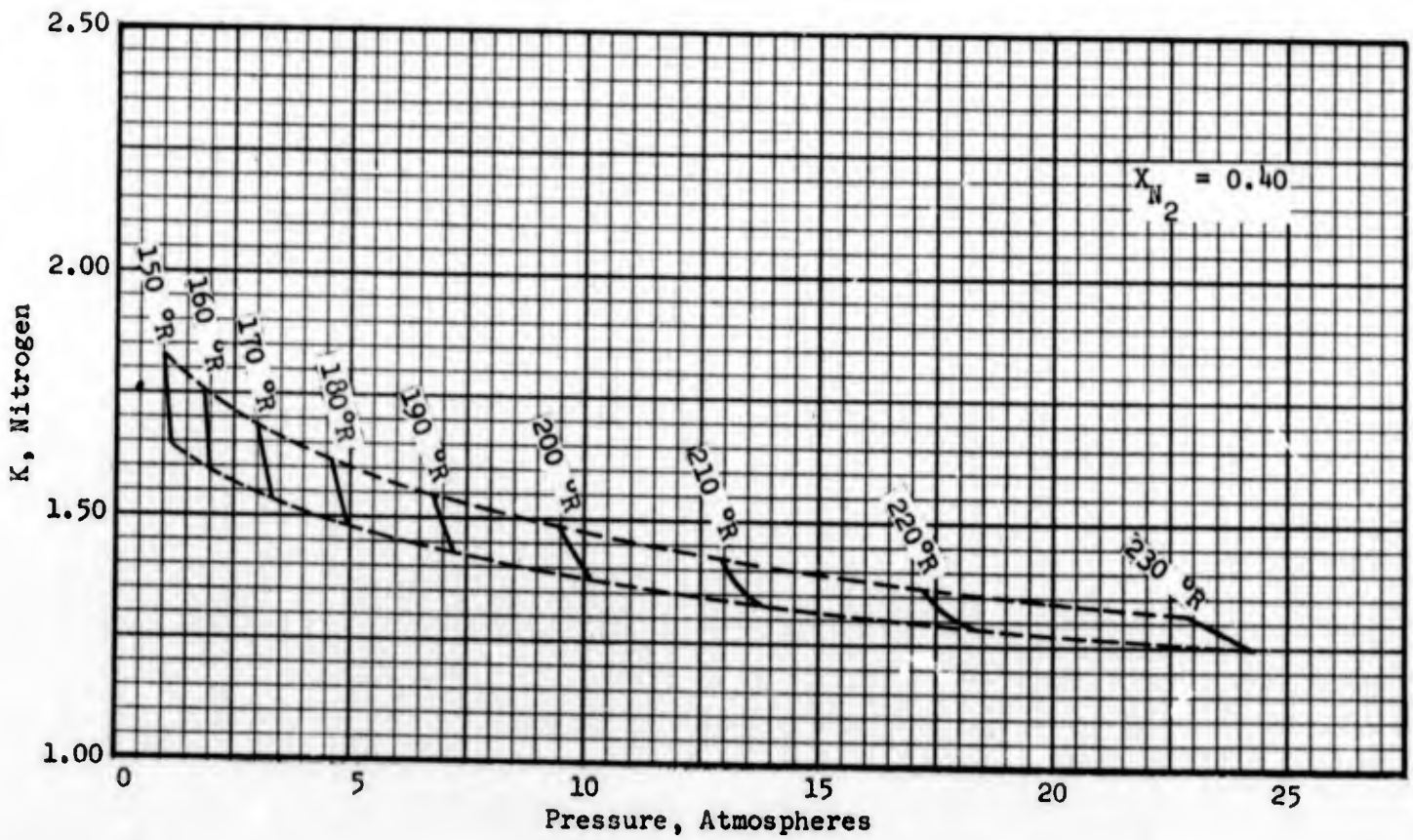
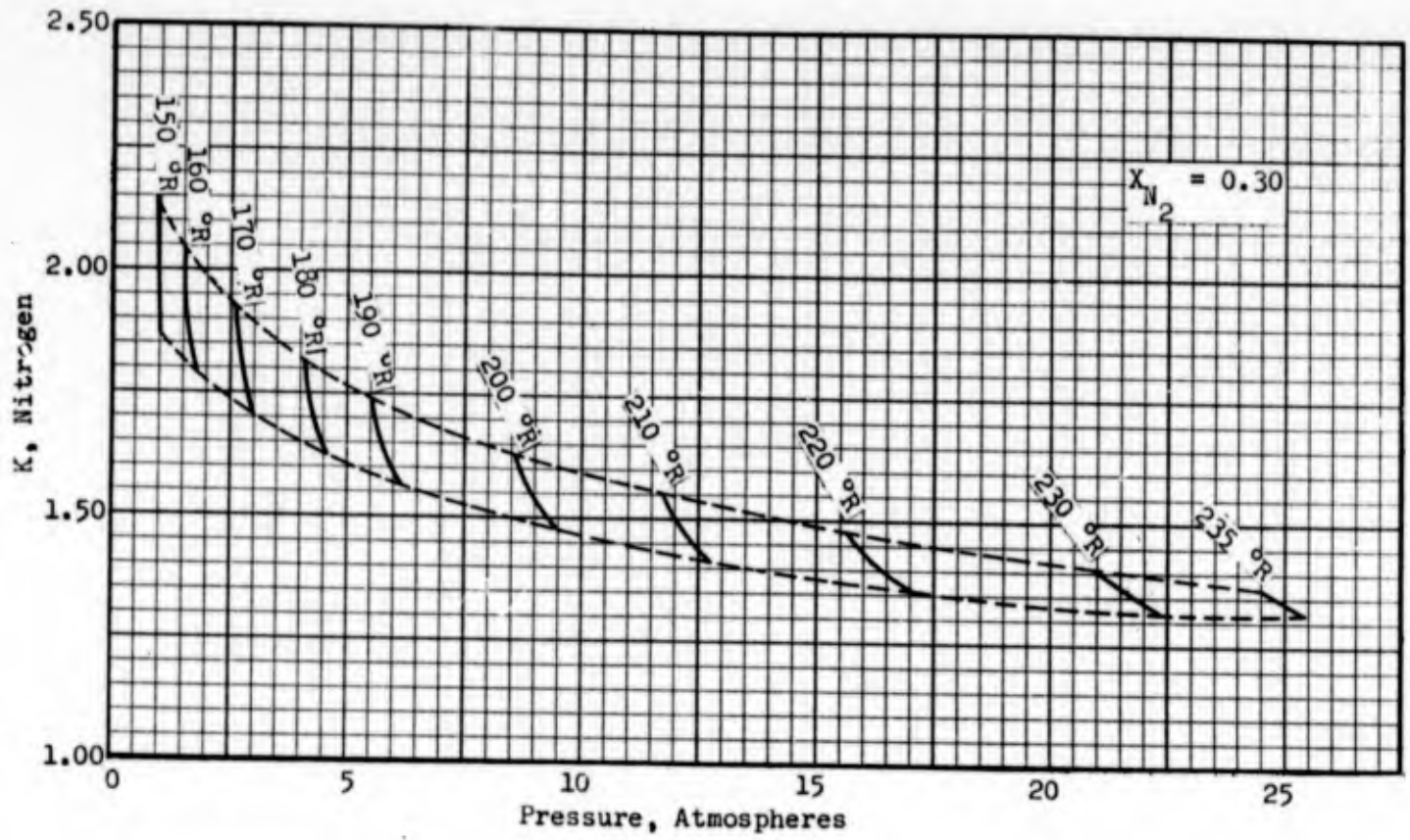


Figure 90. K-Values of Nitrogen.

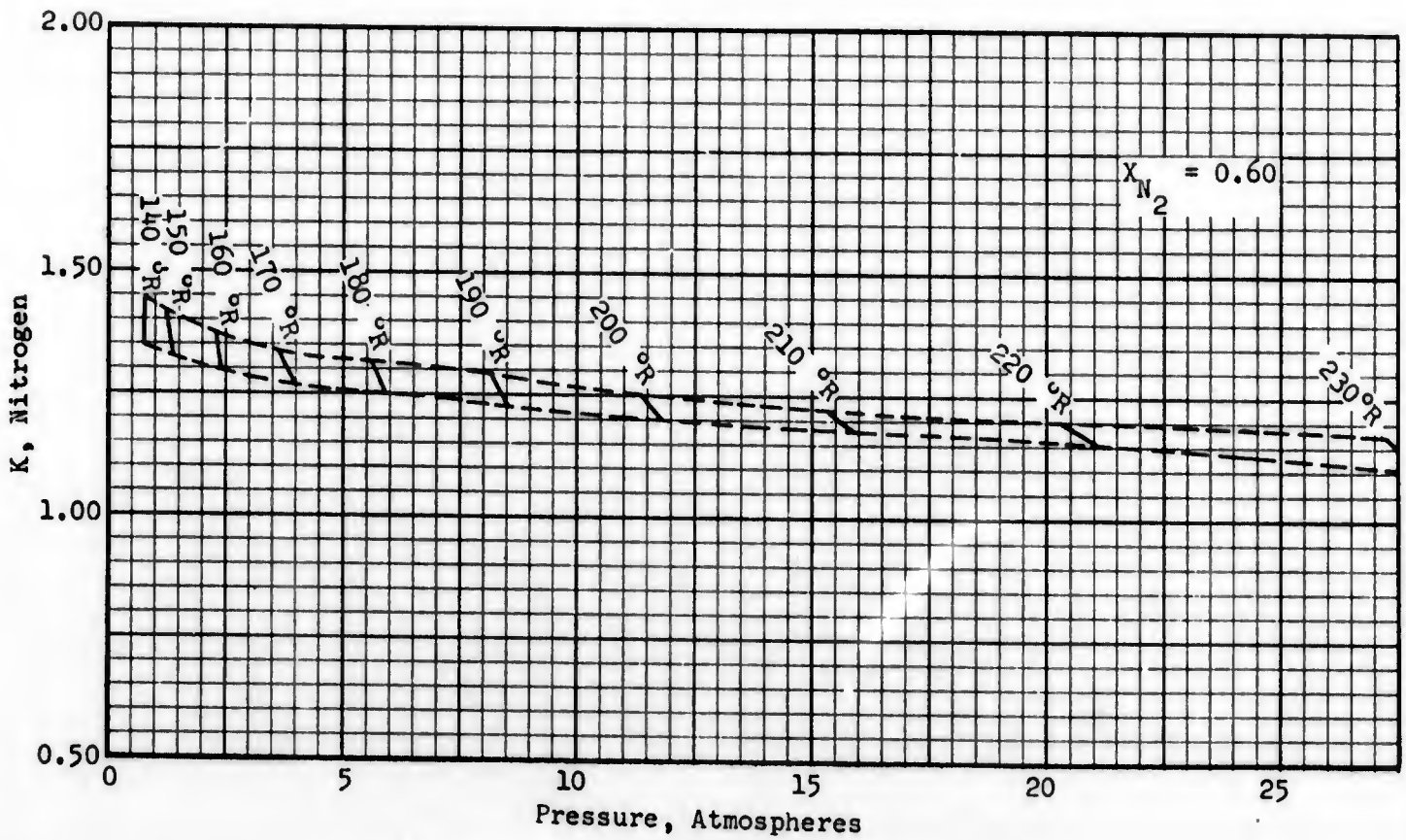
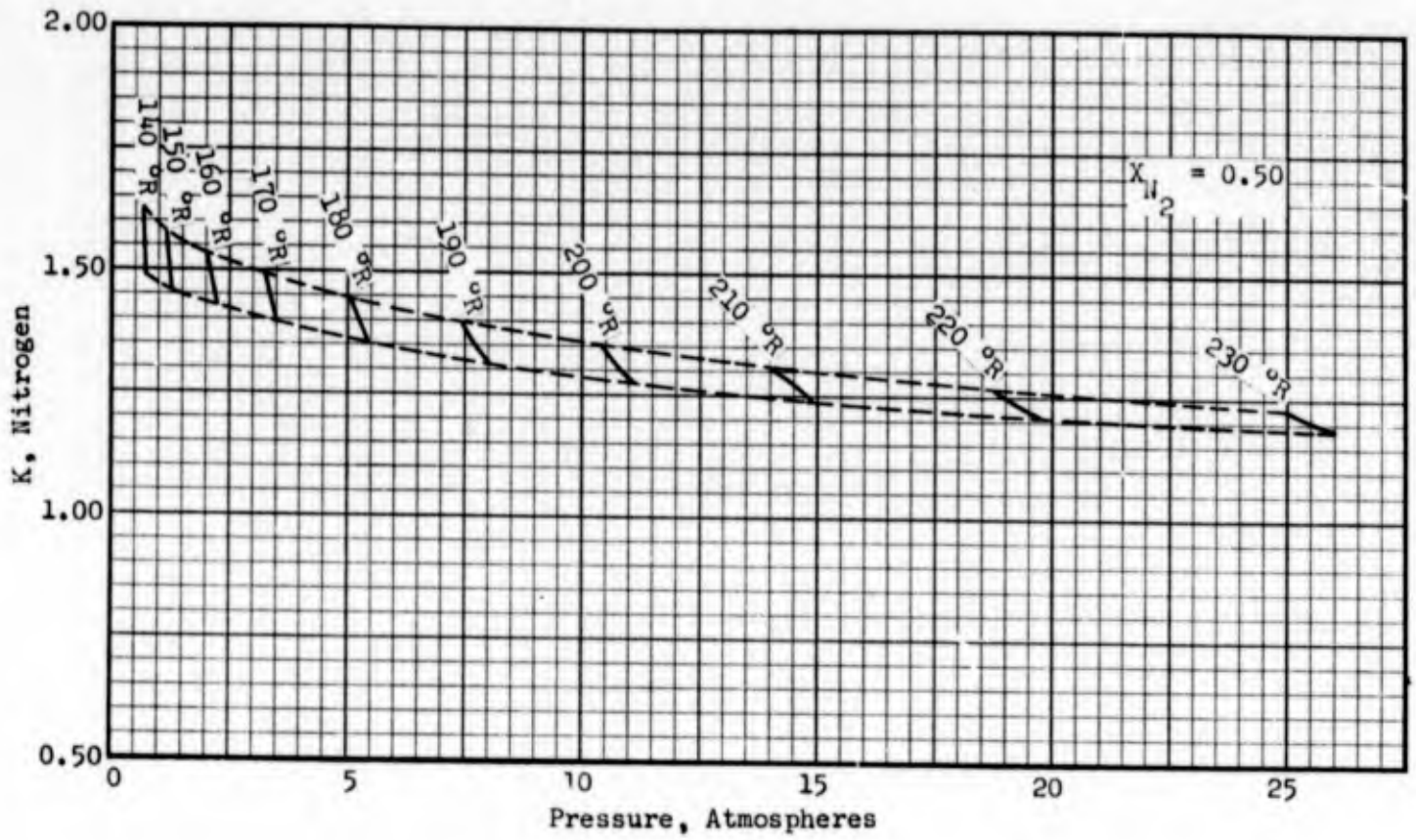


Figure 91. K-Values of Nitrogen.

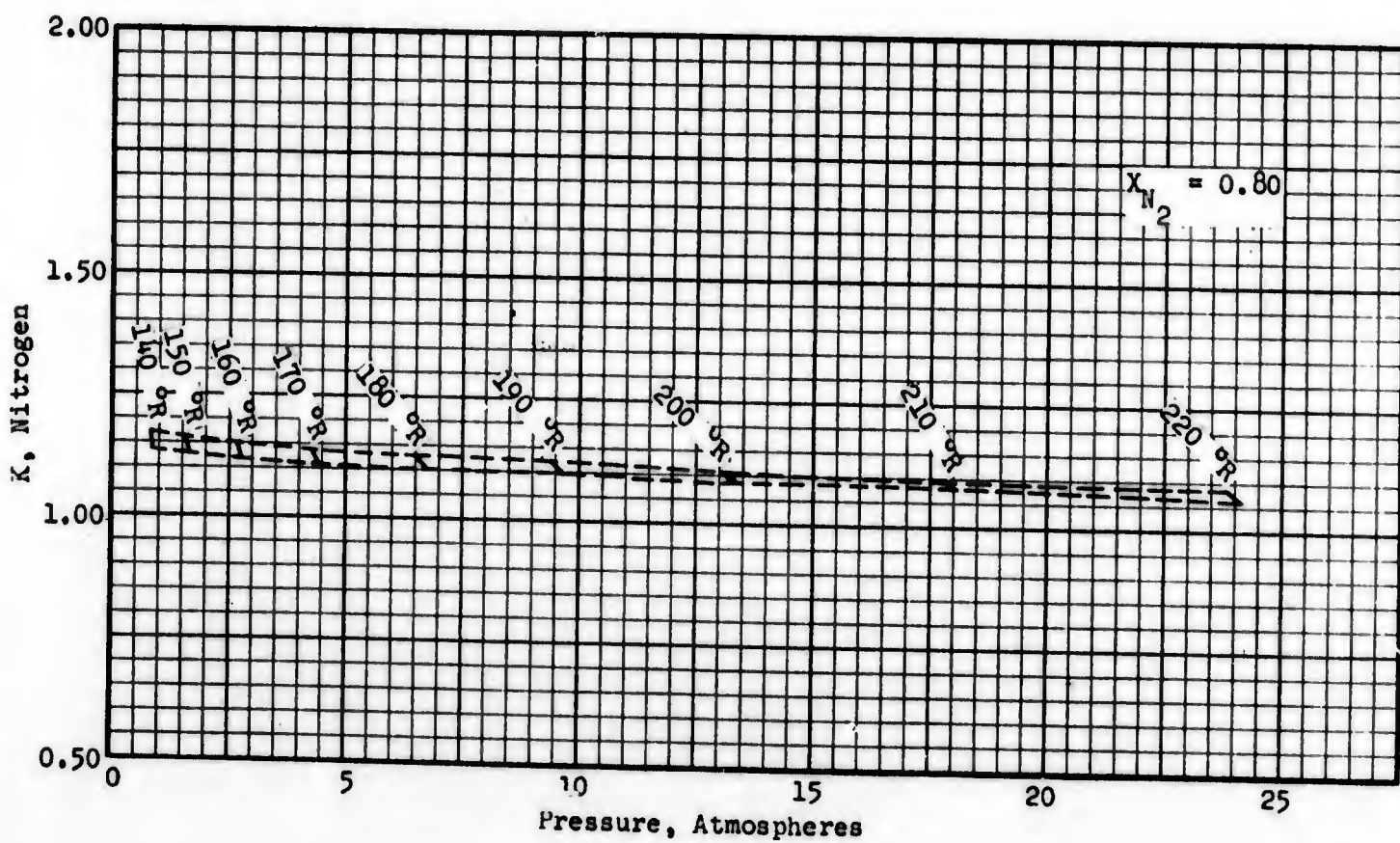
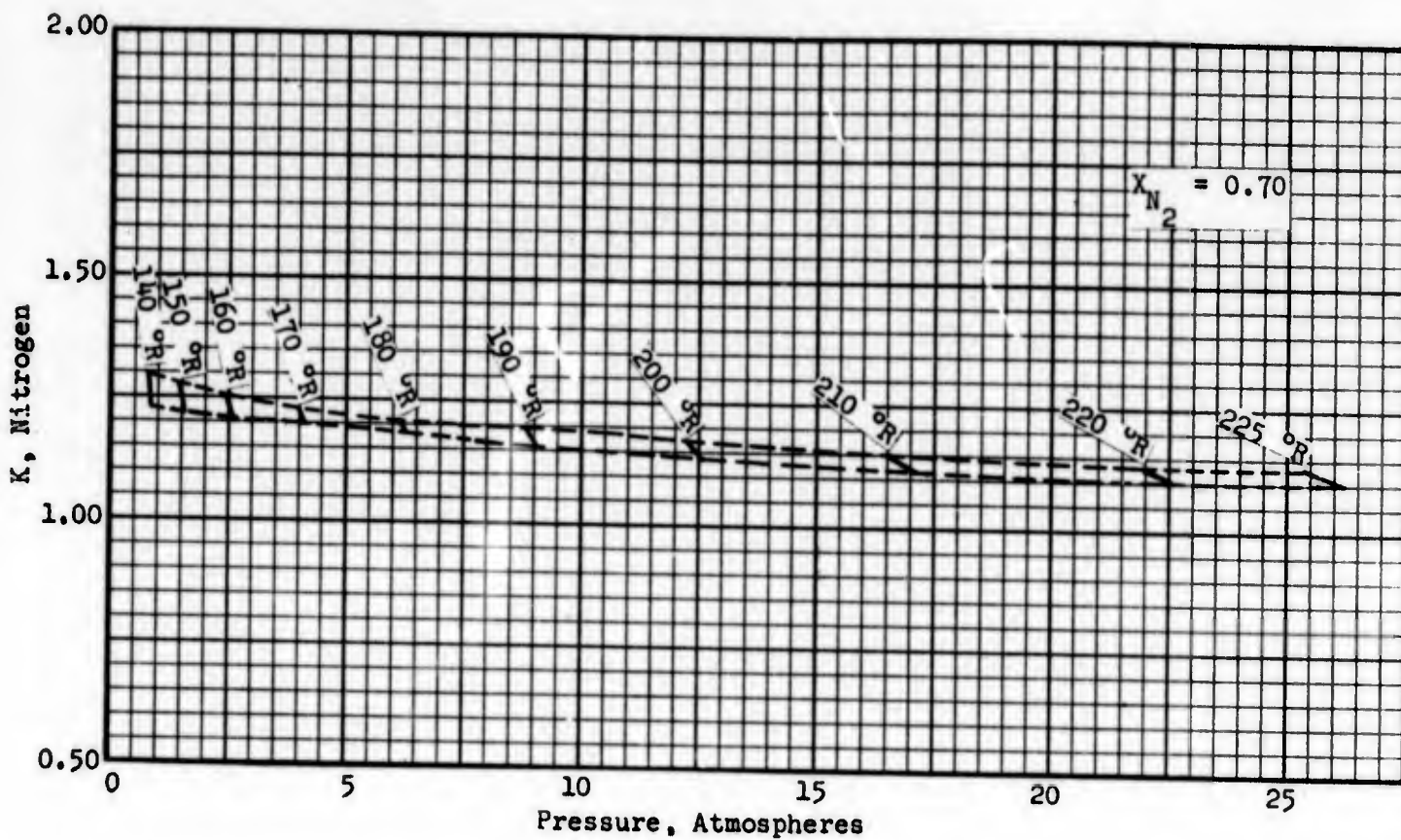


Figure 92. K-Values of Nitrogen.

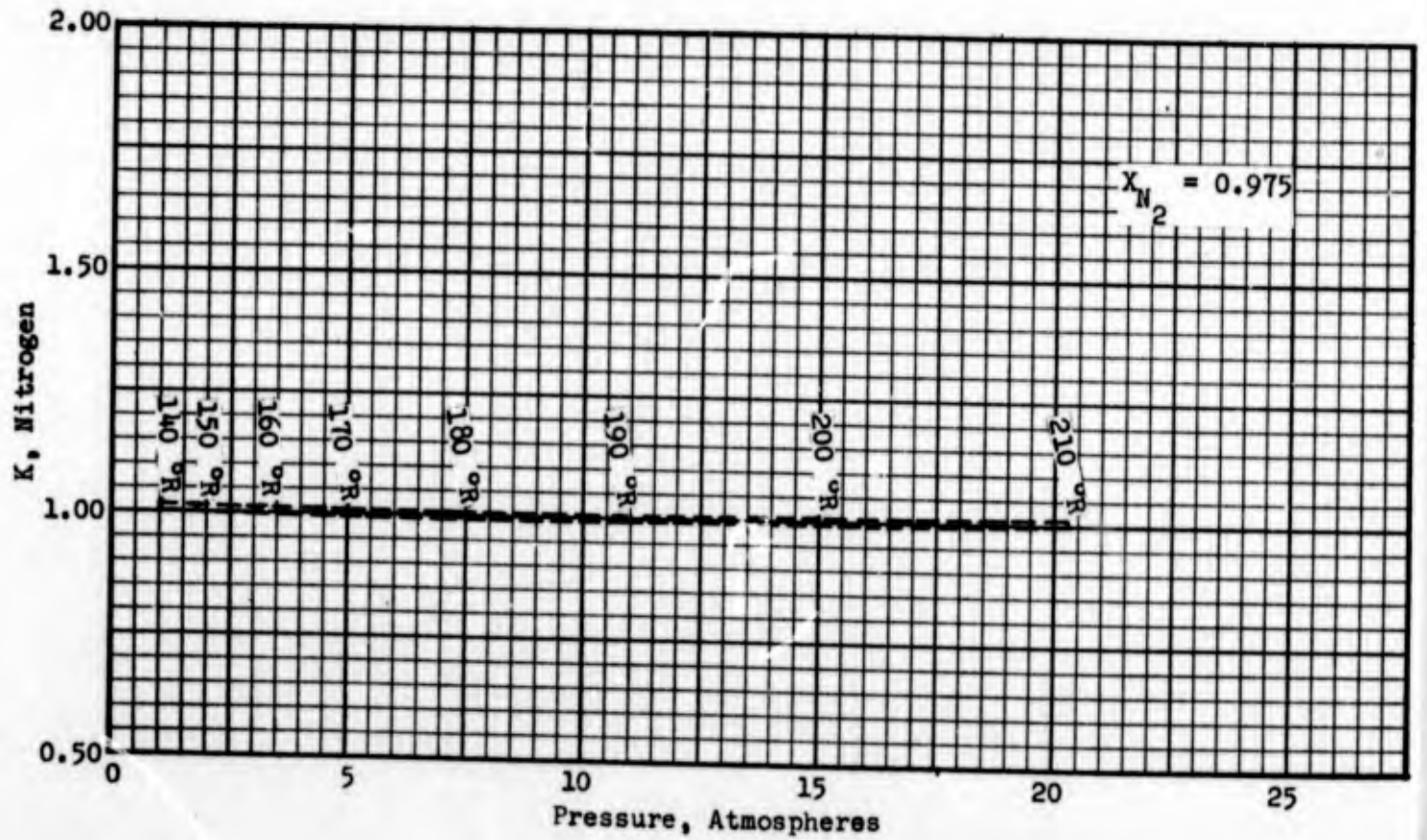
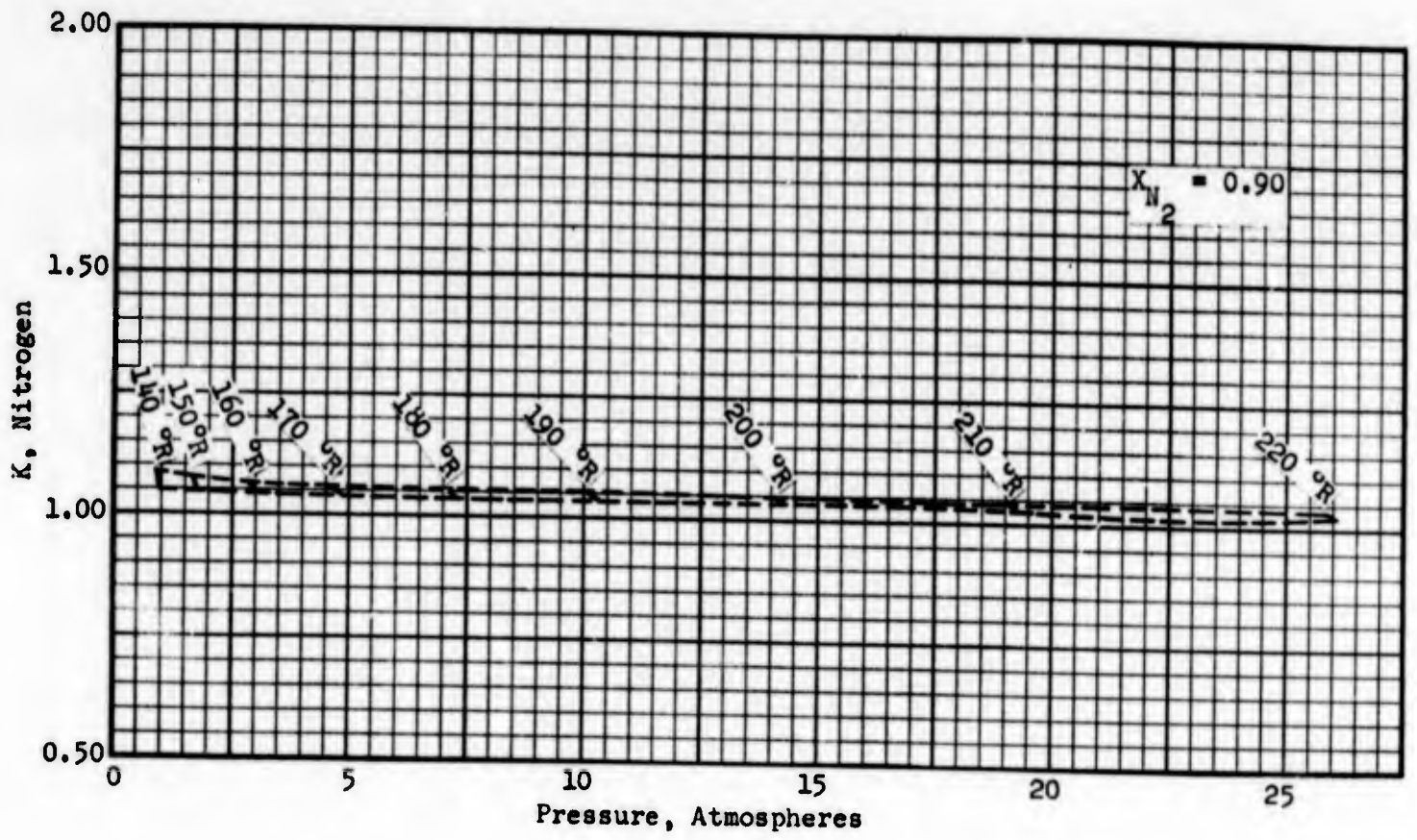


Figure 93. K-Values of Nitrogen.

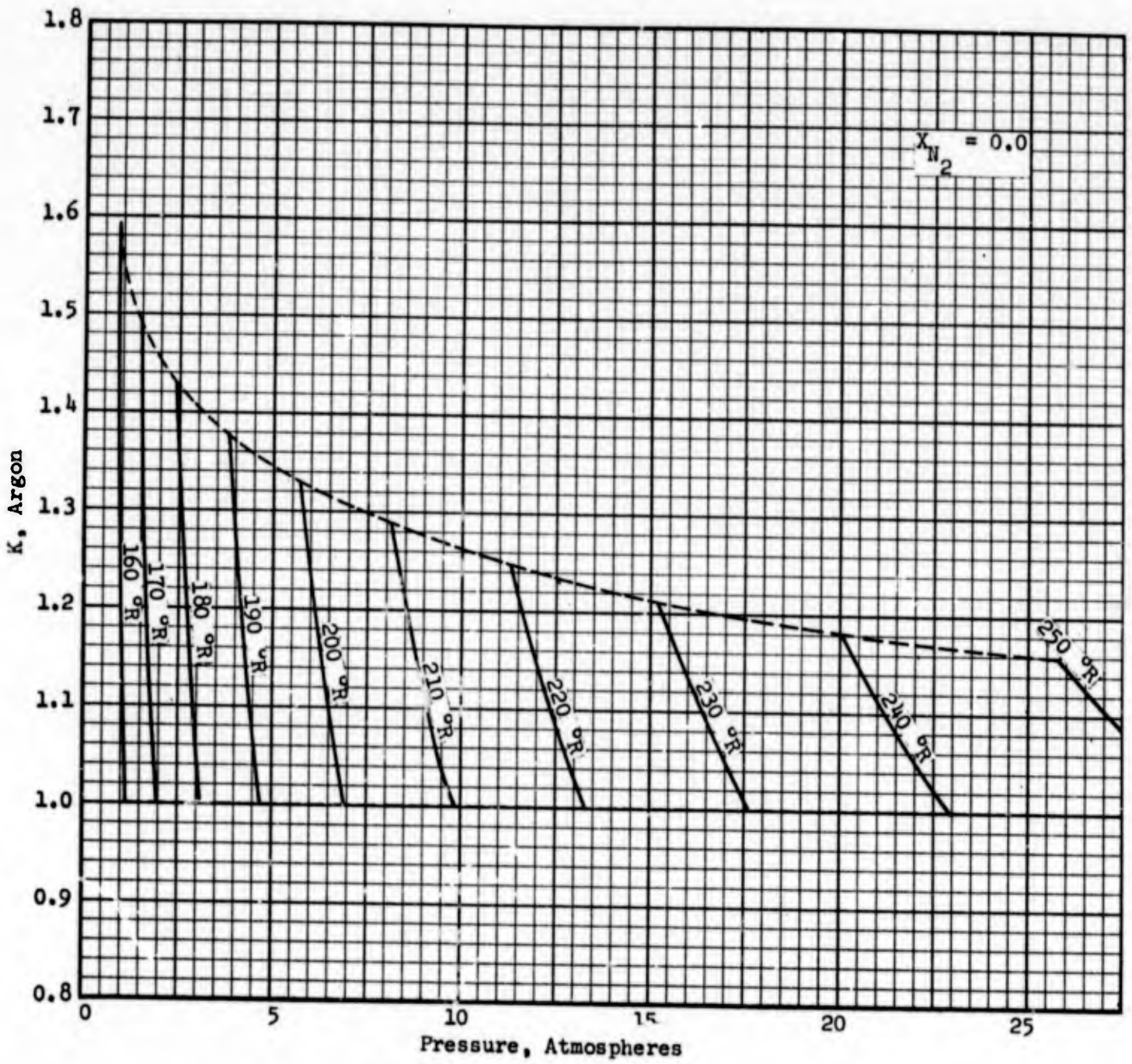


Figure 94. K-Values of Argon.

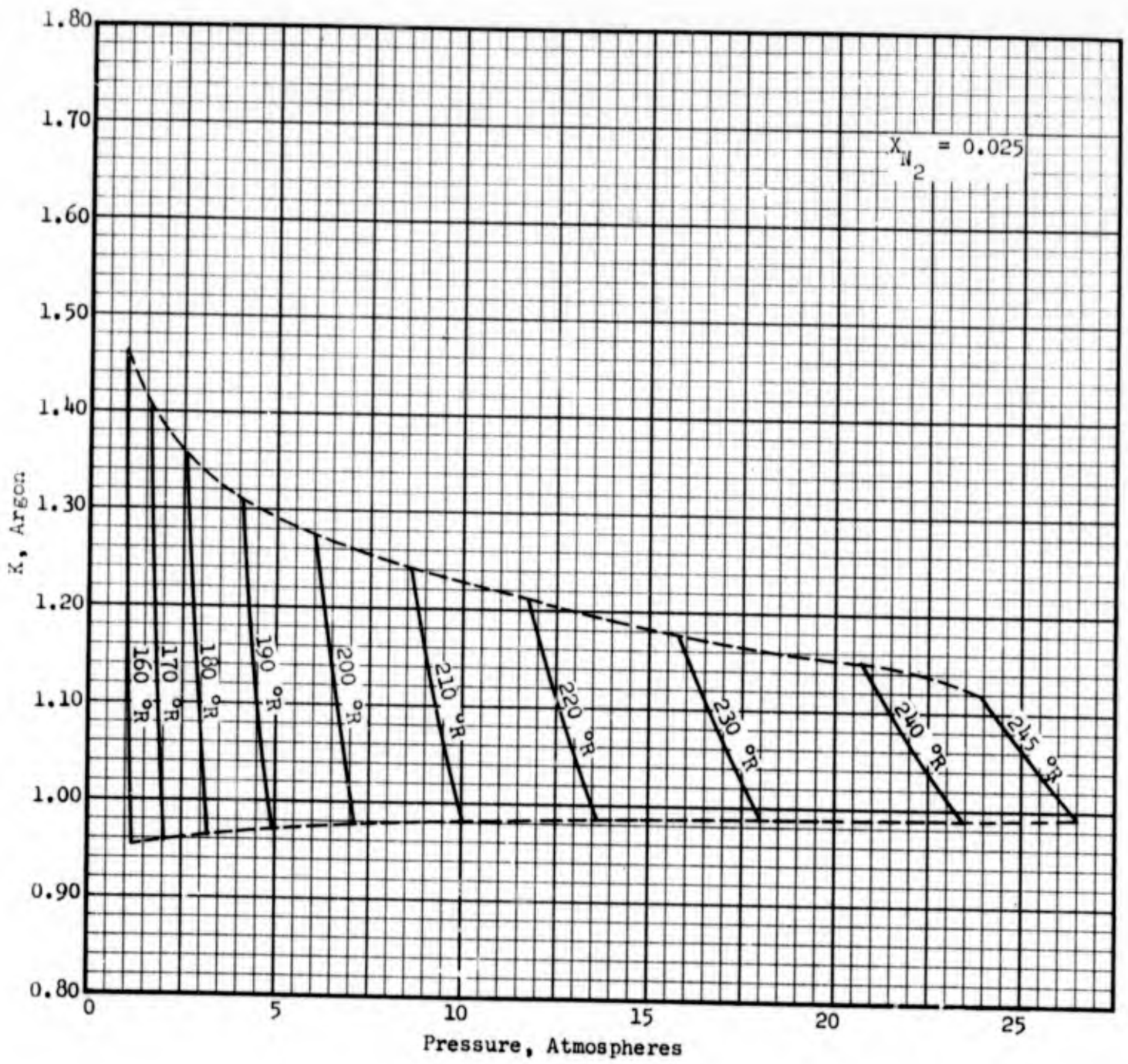


Figure 95. K-Values of Argon

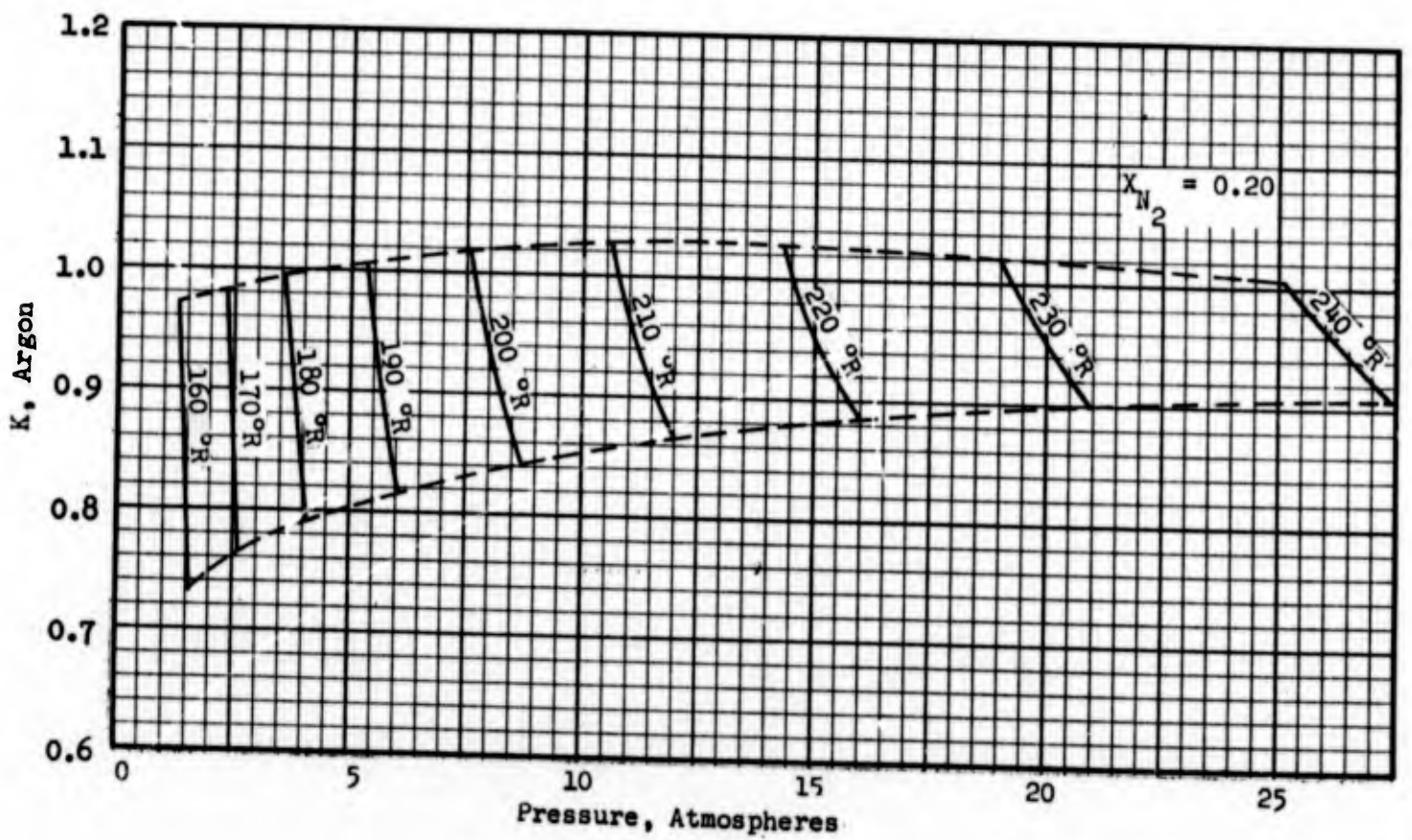
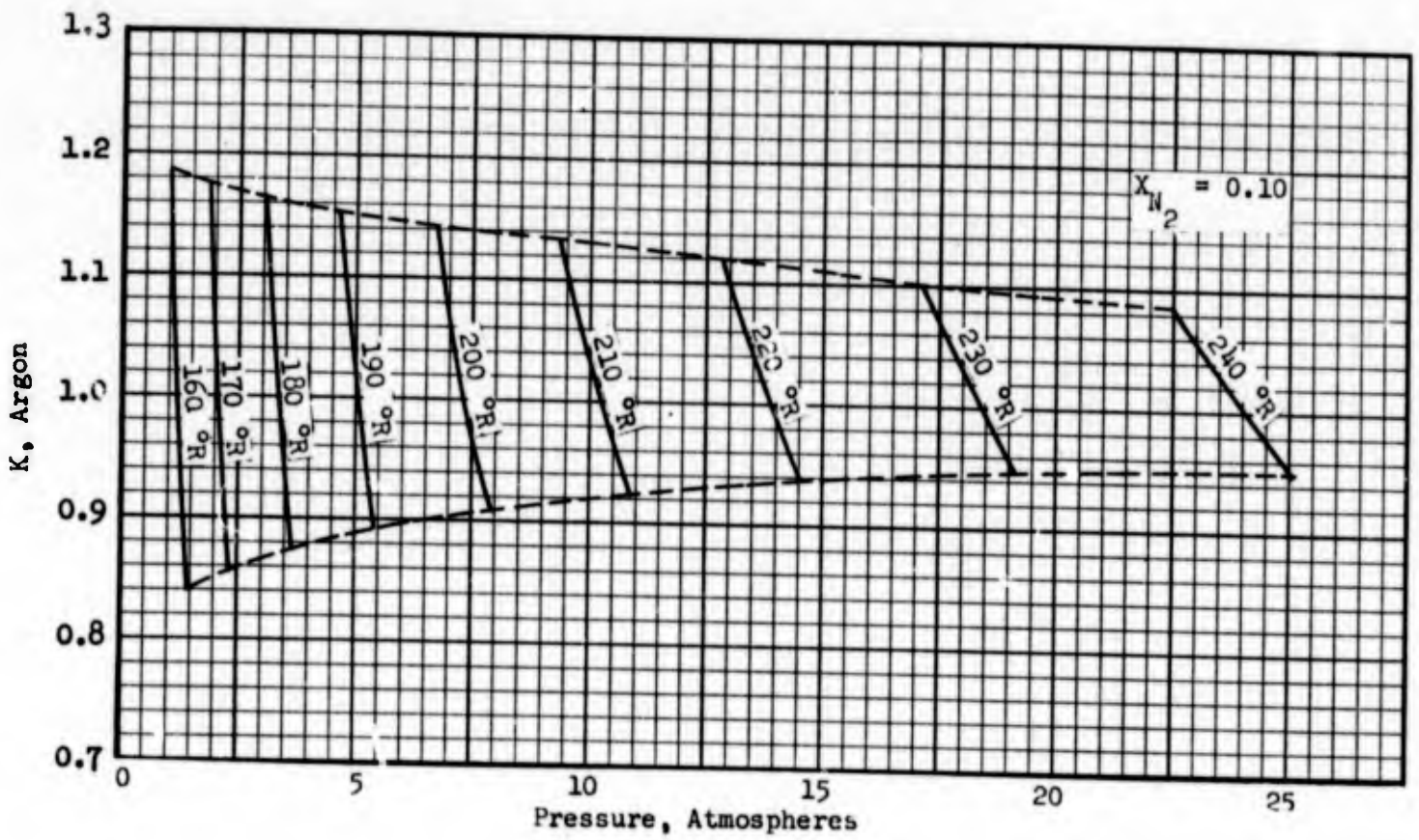


Figure 96. K-Values of Argon.

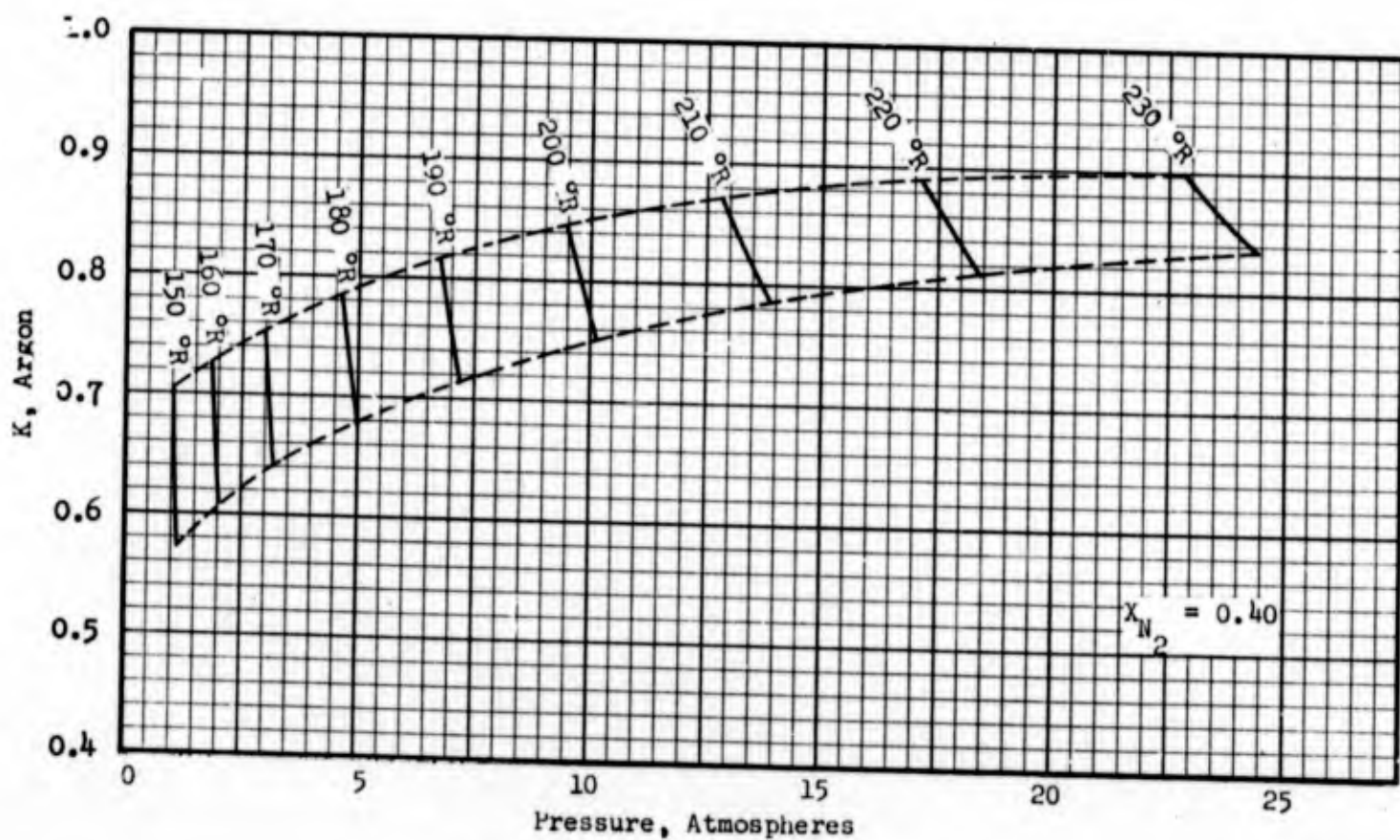
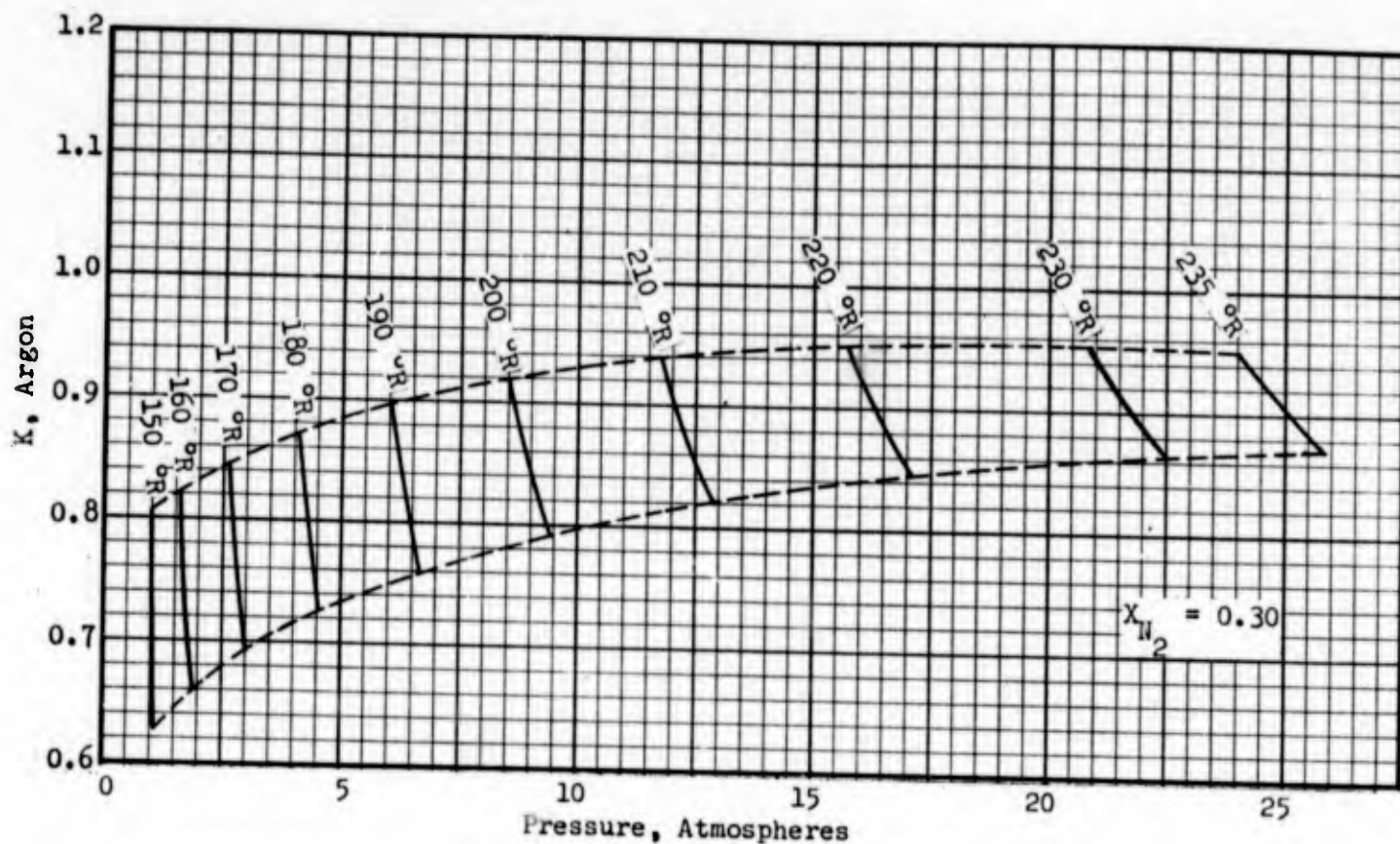


Figure 97. K-Values of Argon.

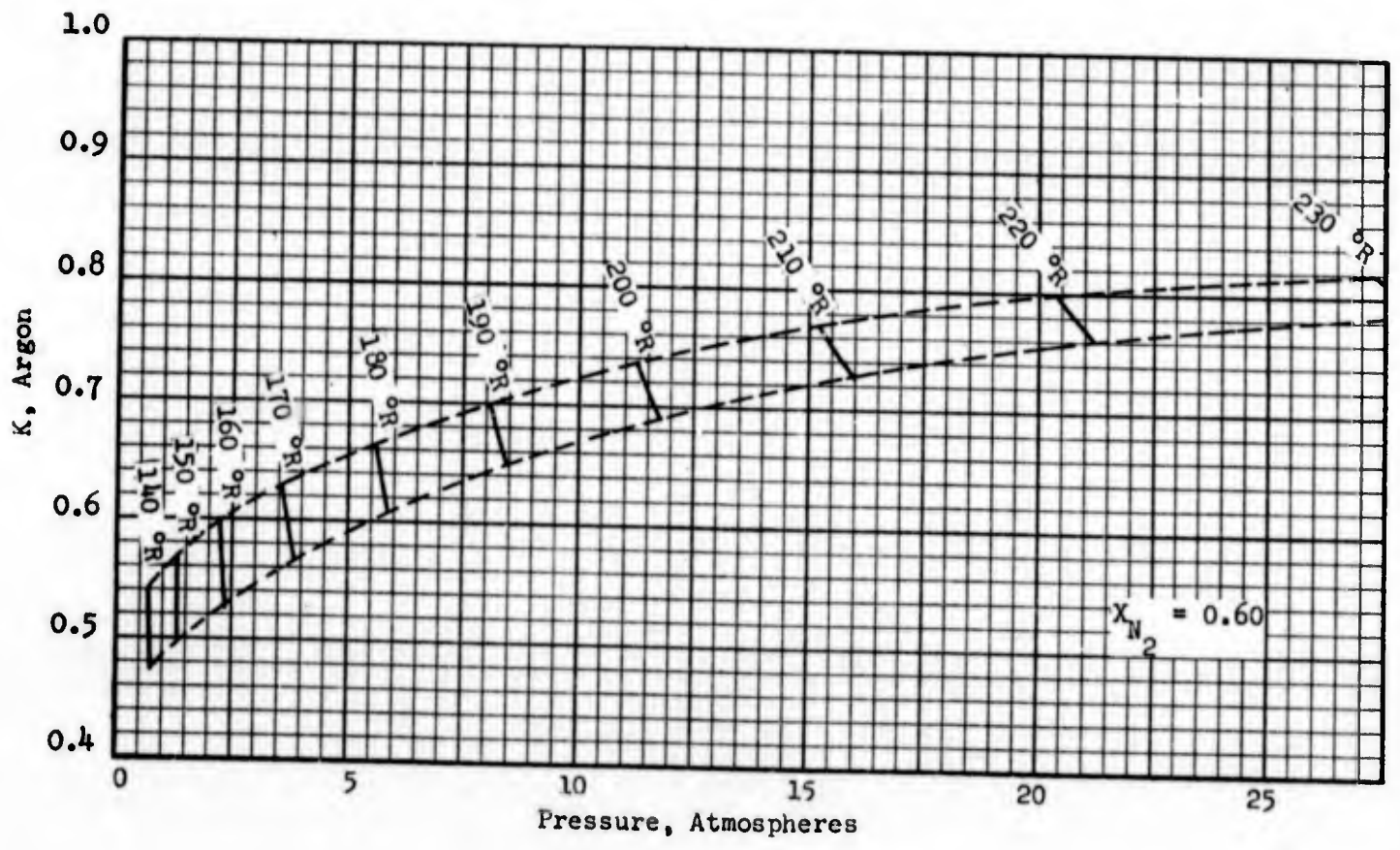
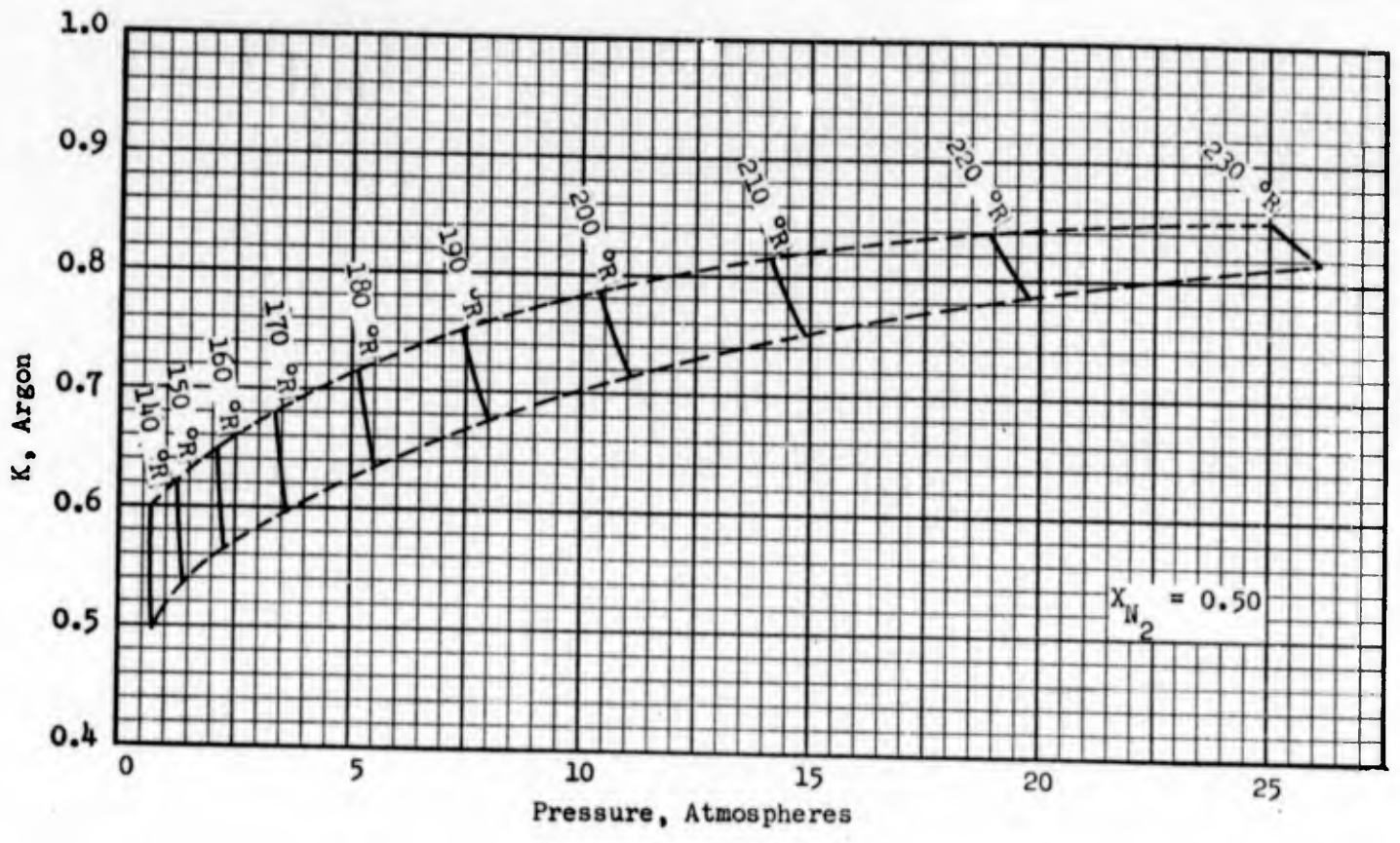


Figure 98. K-Values of Argon.

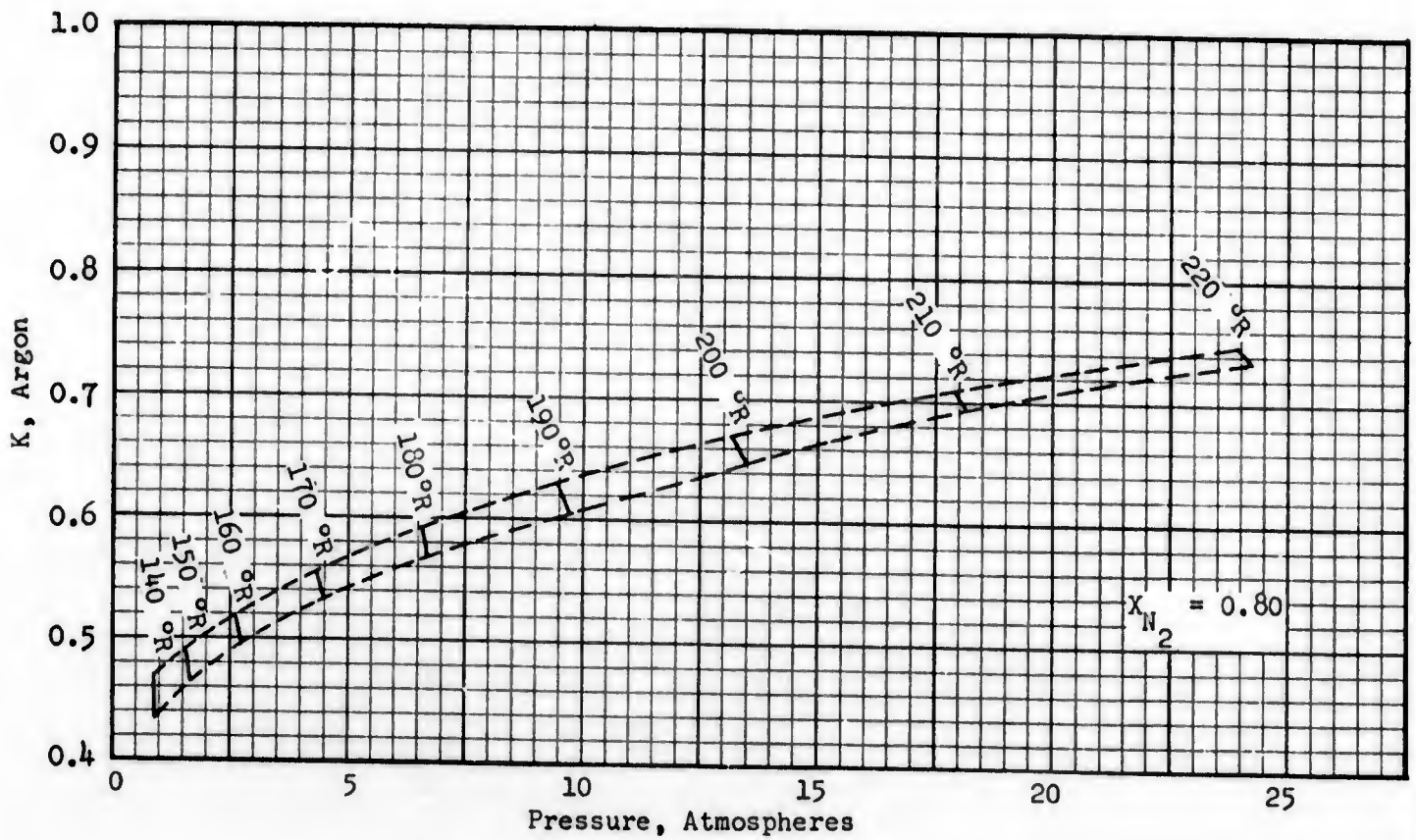
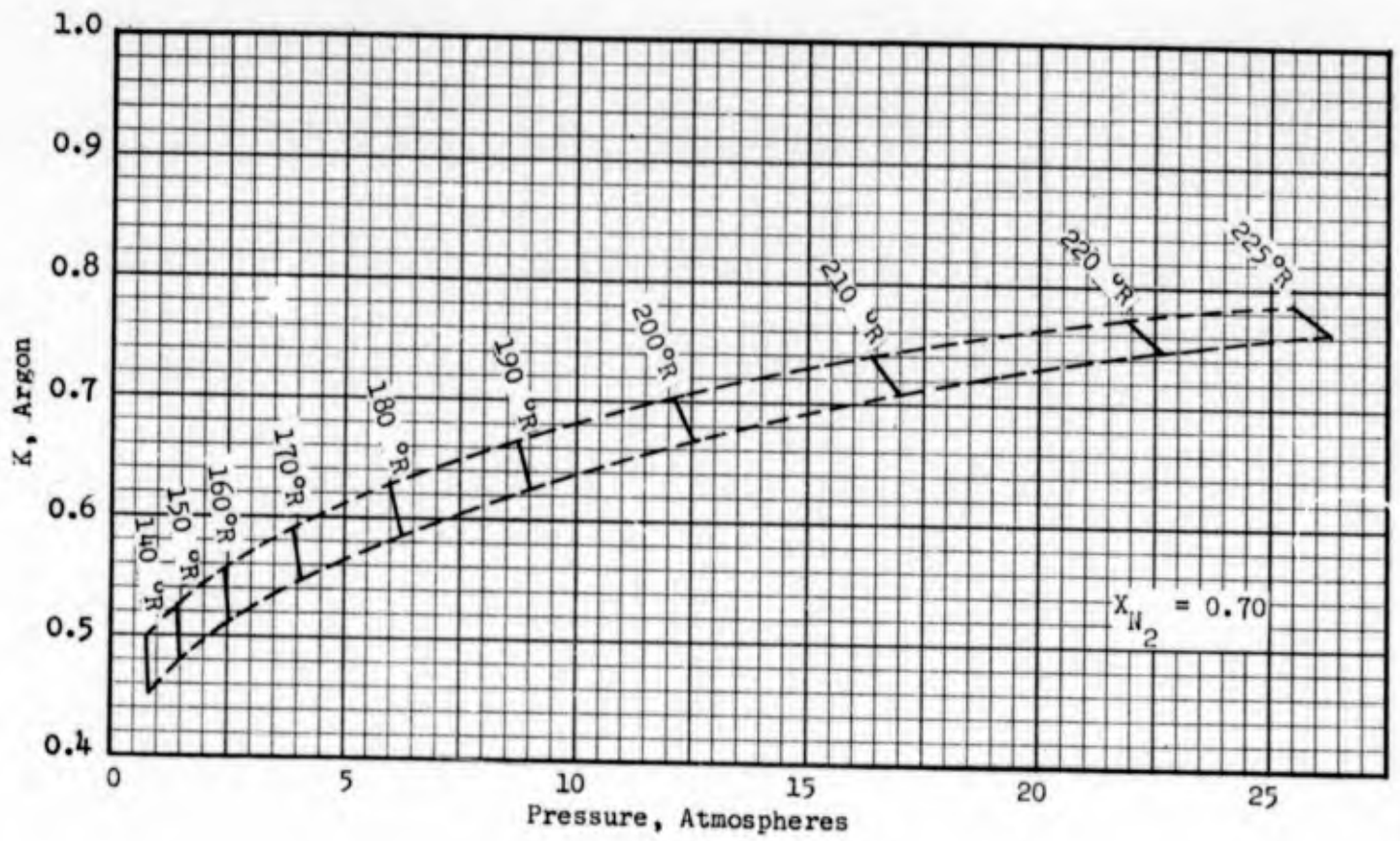
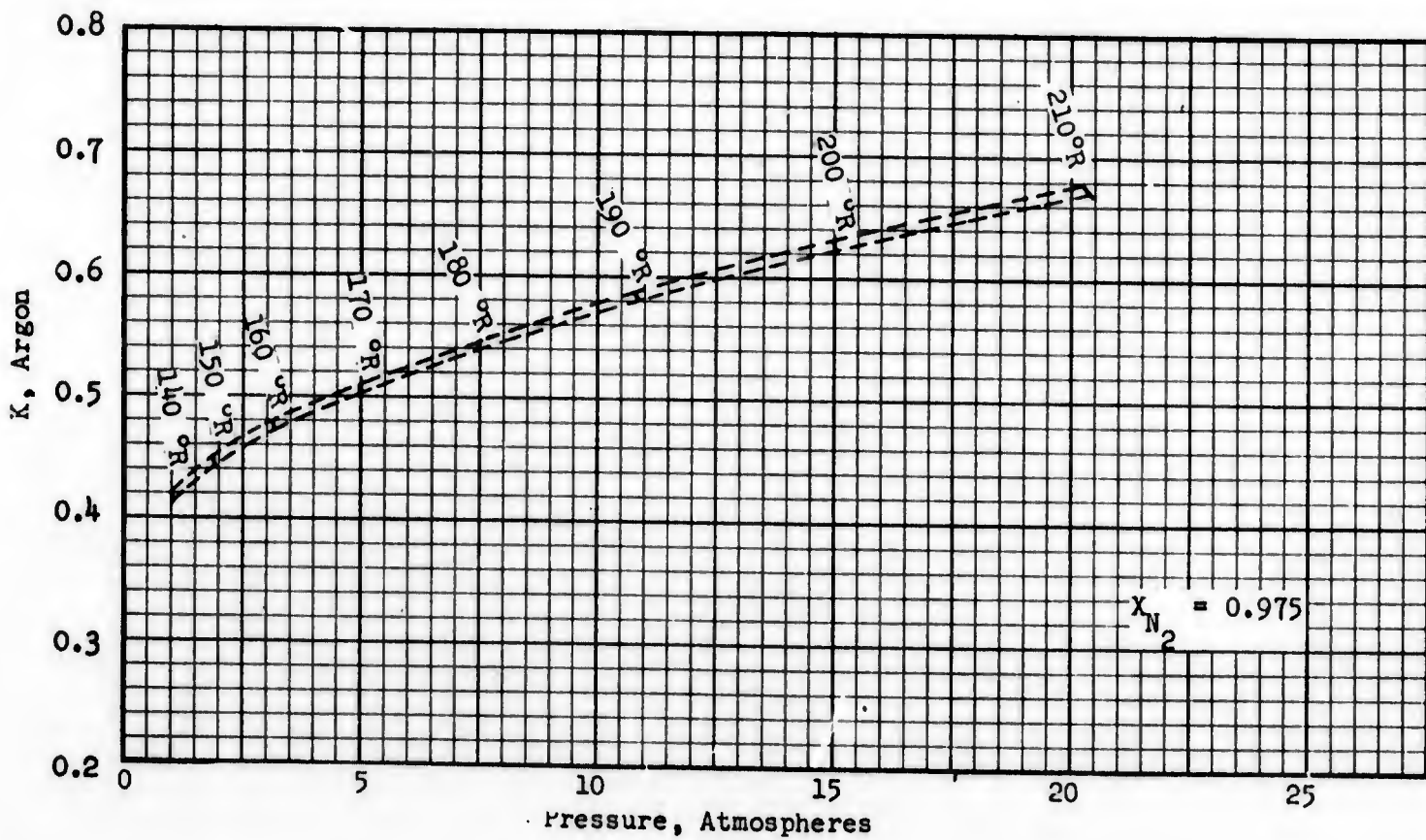
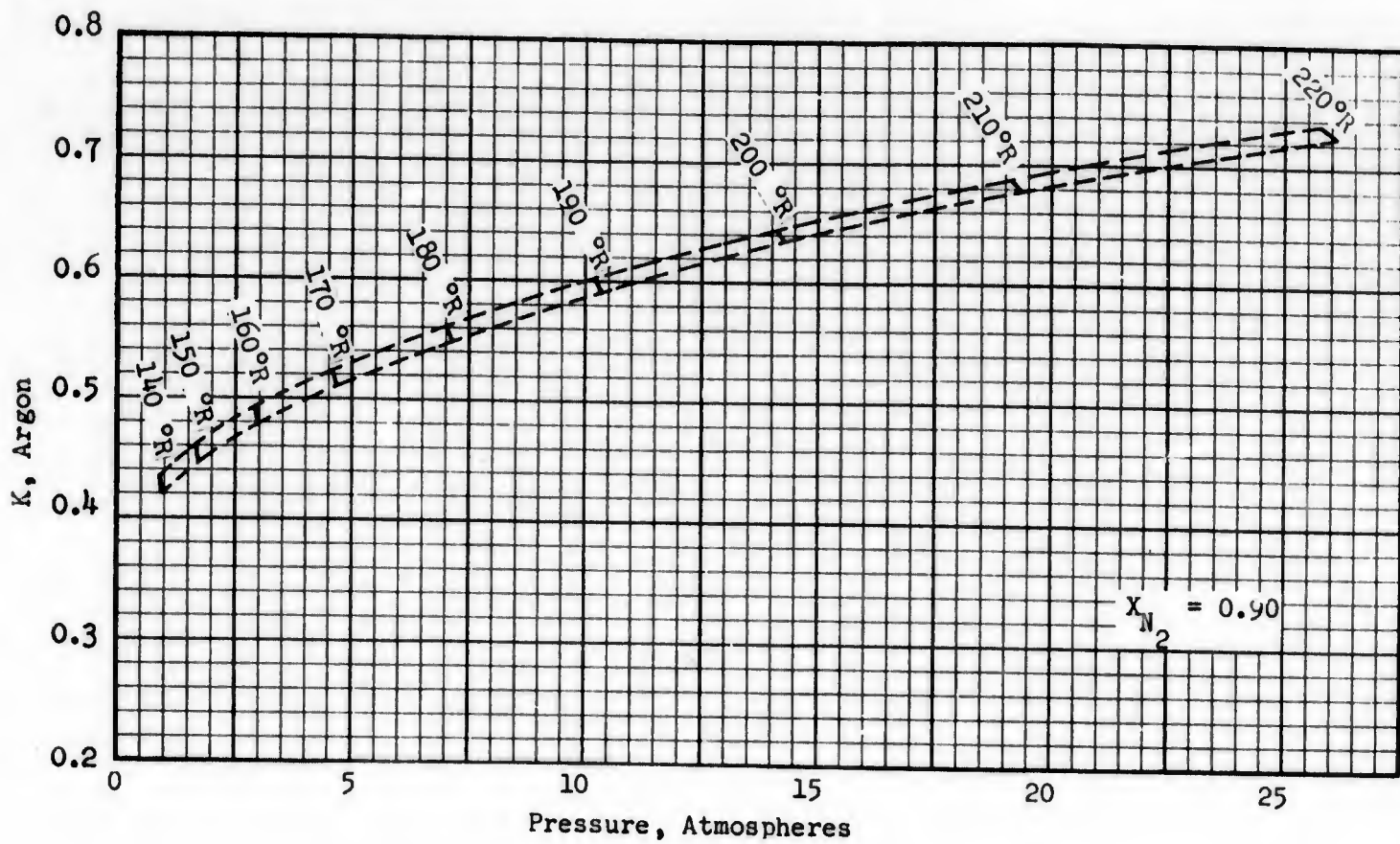


Figure 99. K-Values of Argon.



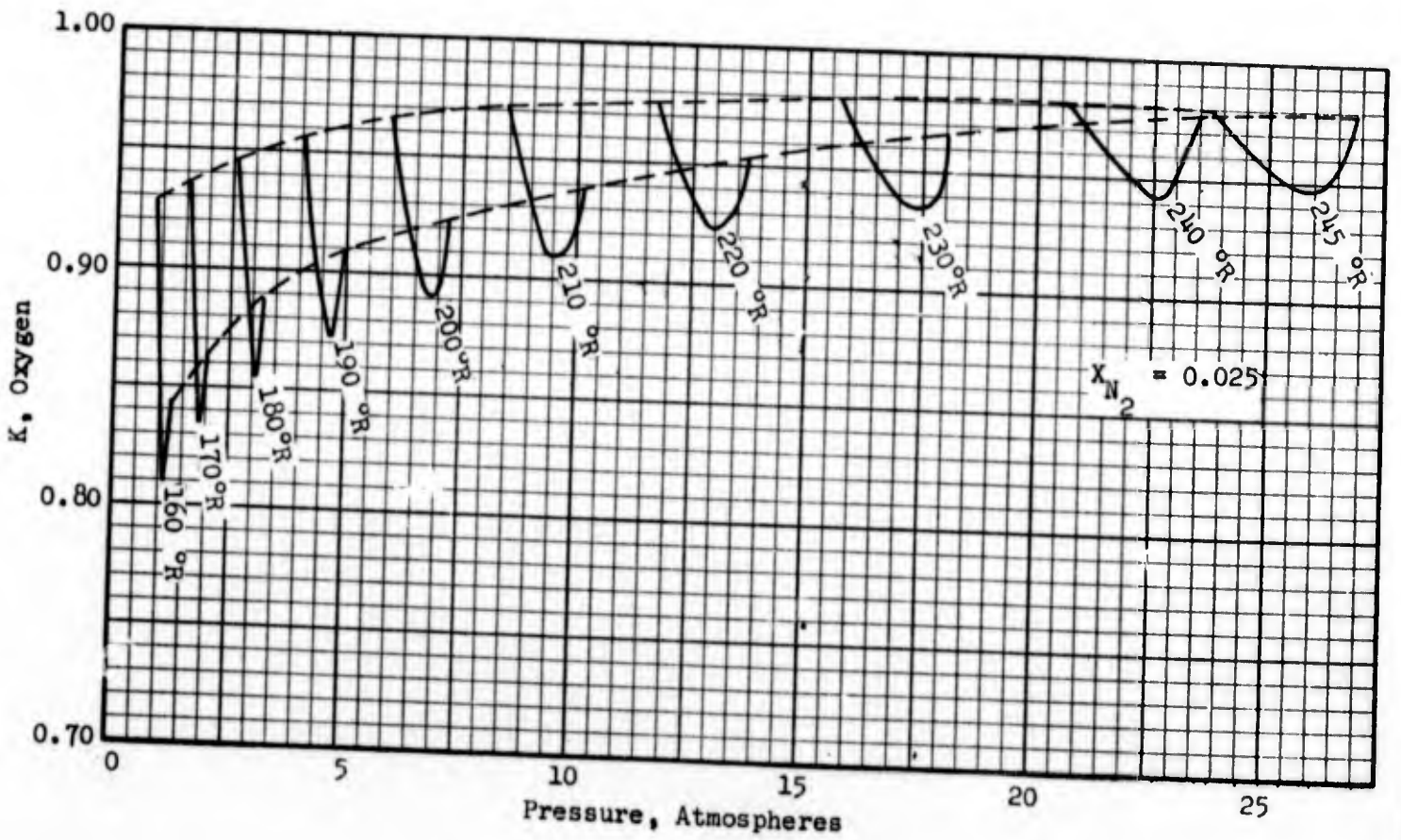
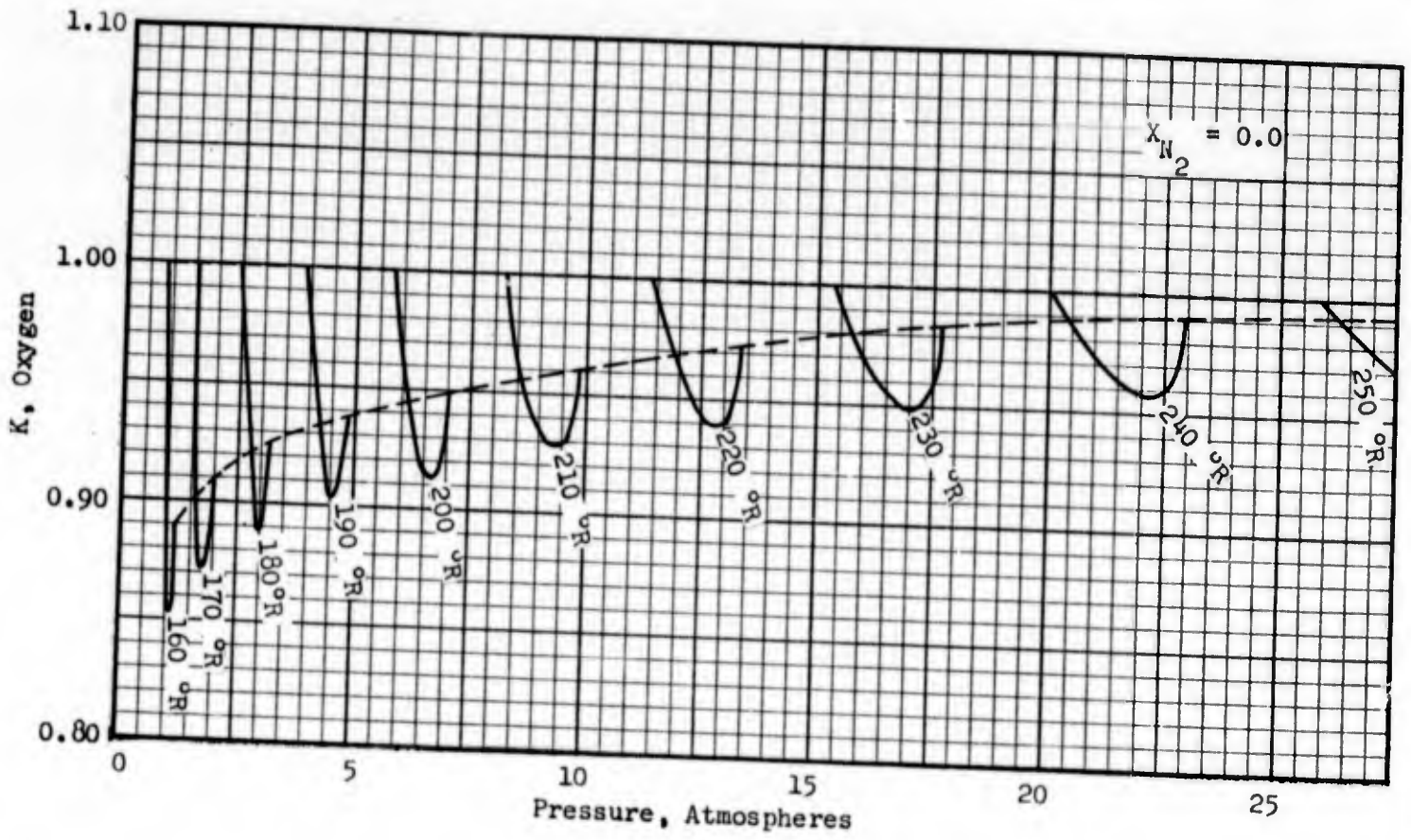


Figure 101. K-Values of Oxygen.

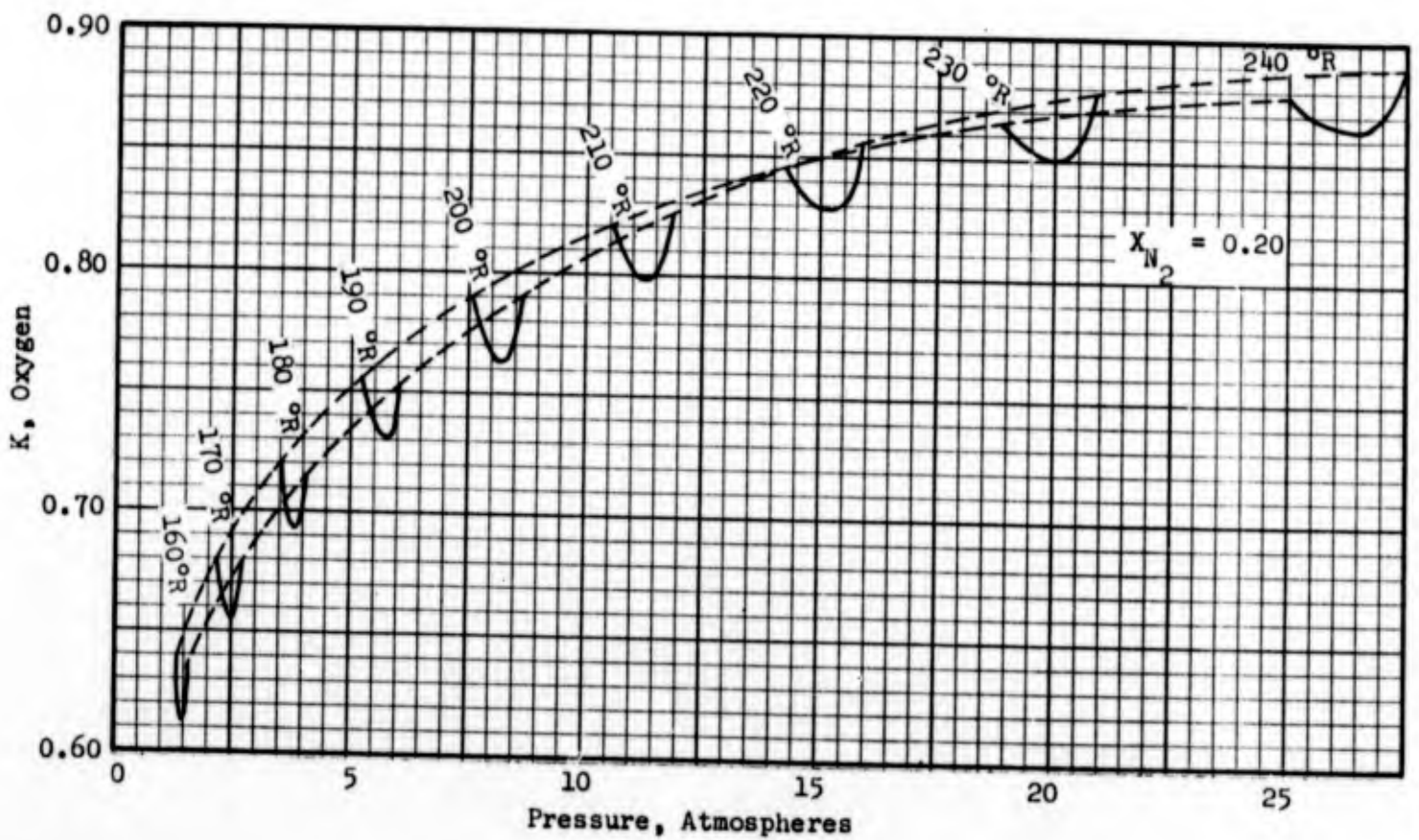
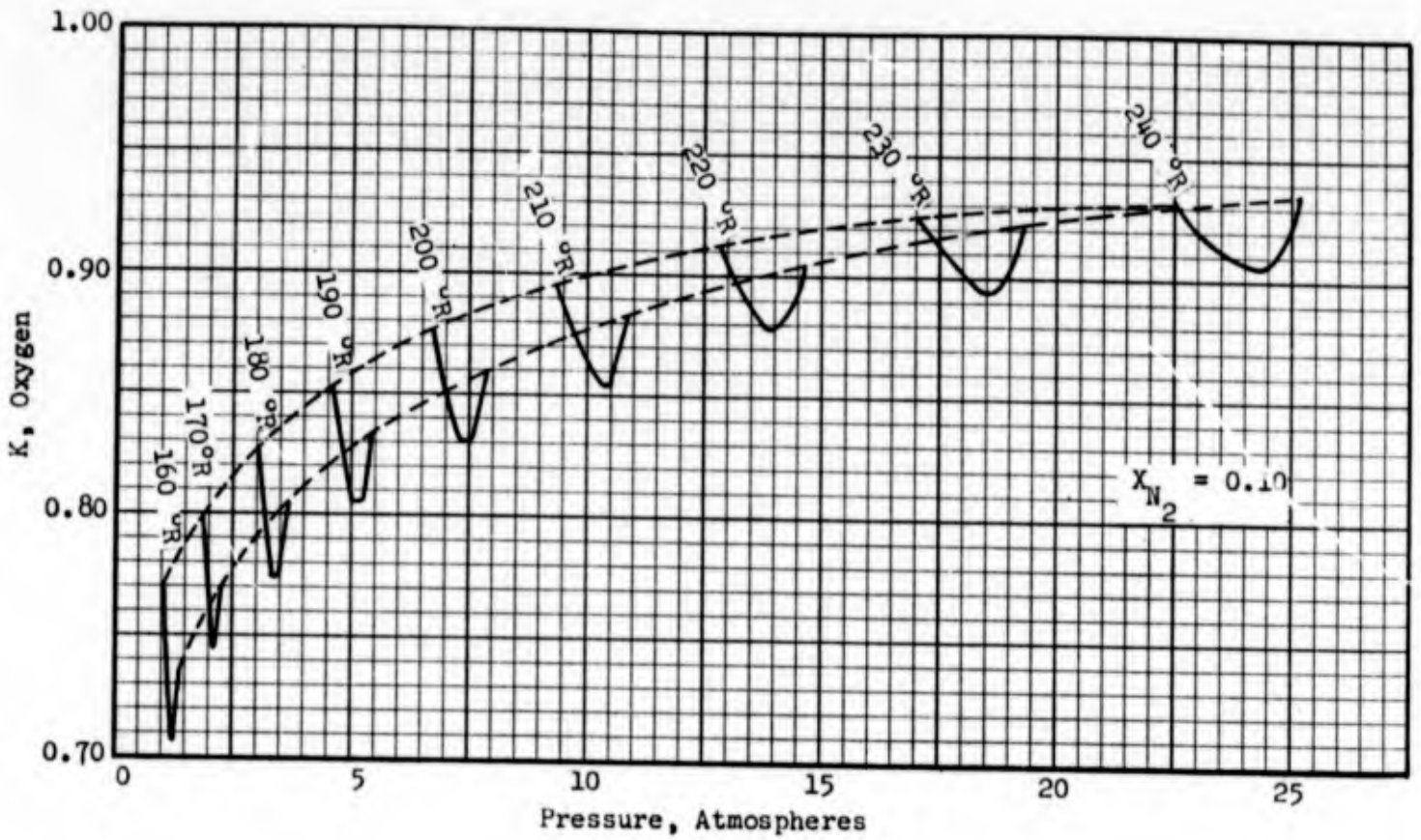


Figure 102. K -Values of Oxygen.

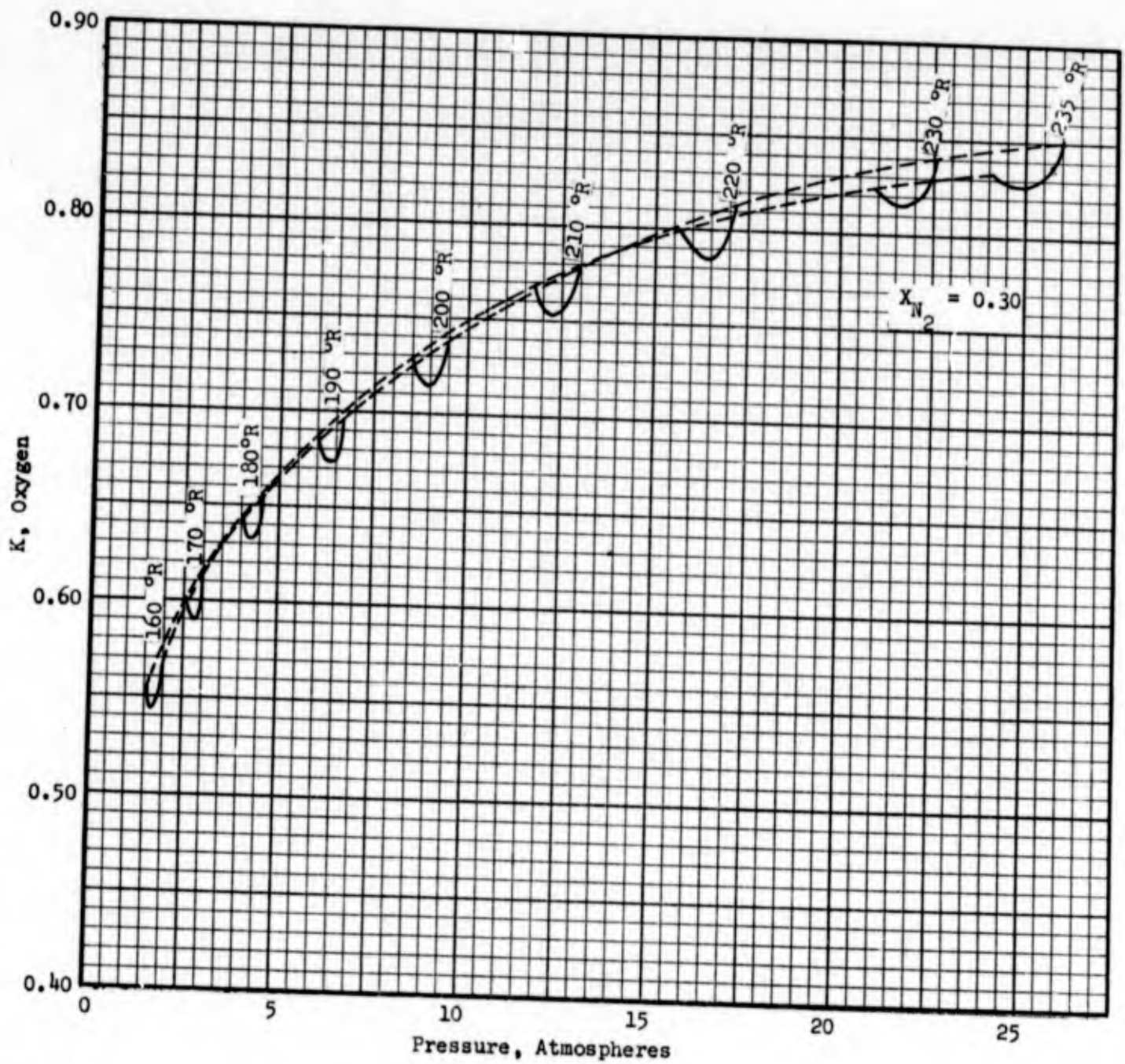


Figure 103. K-Values of Oxygen.

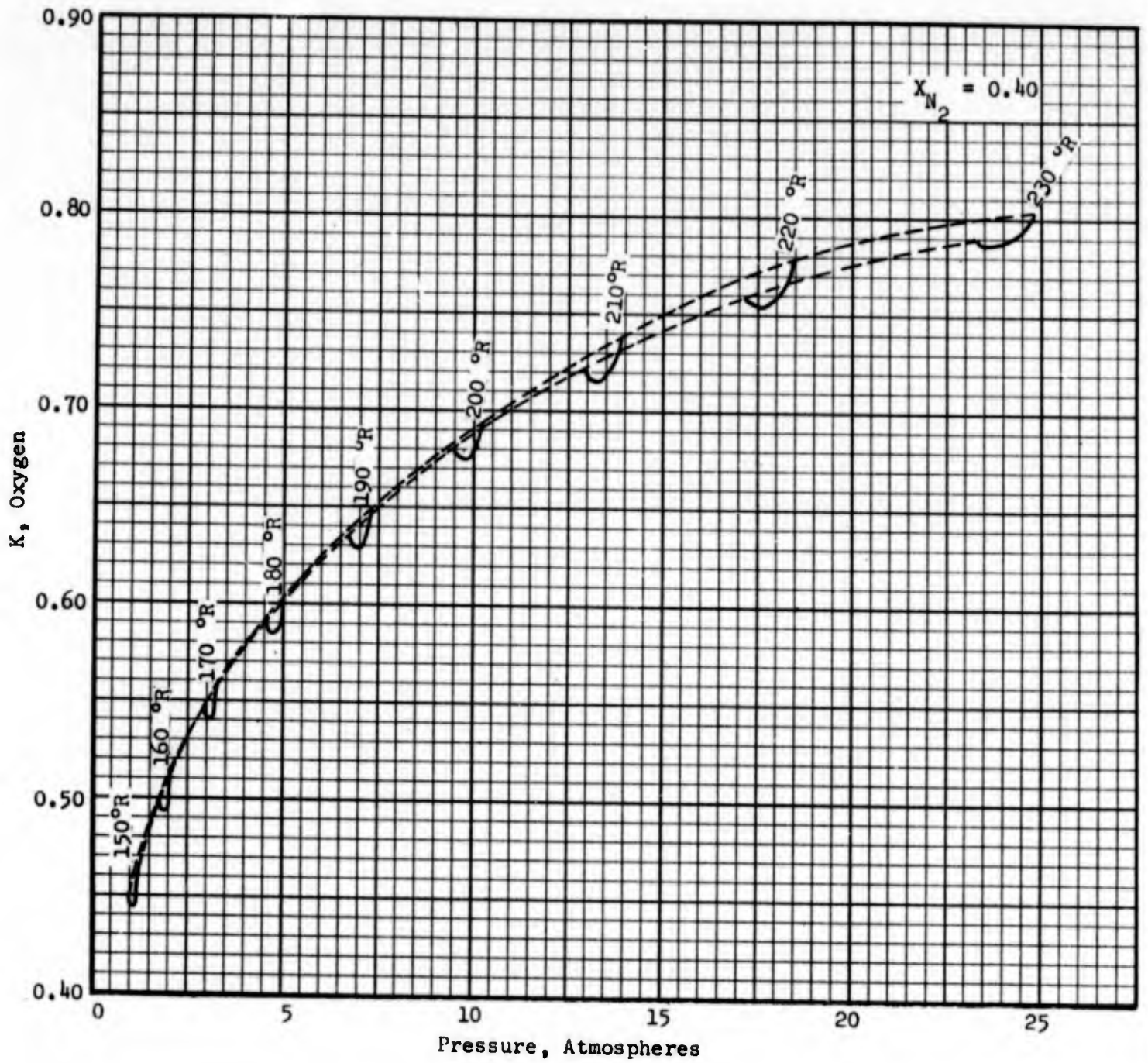


Figure 104. K-Values of Oxygen.

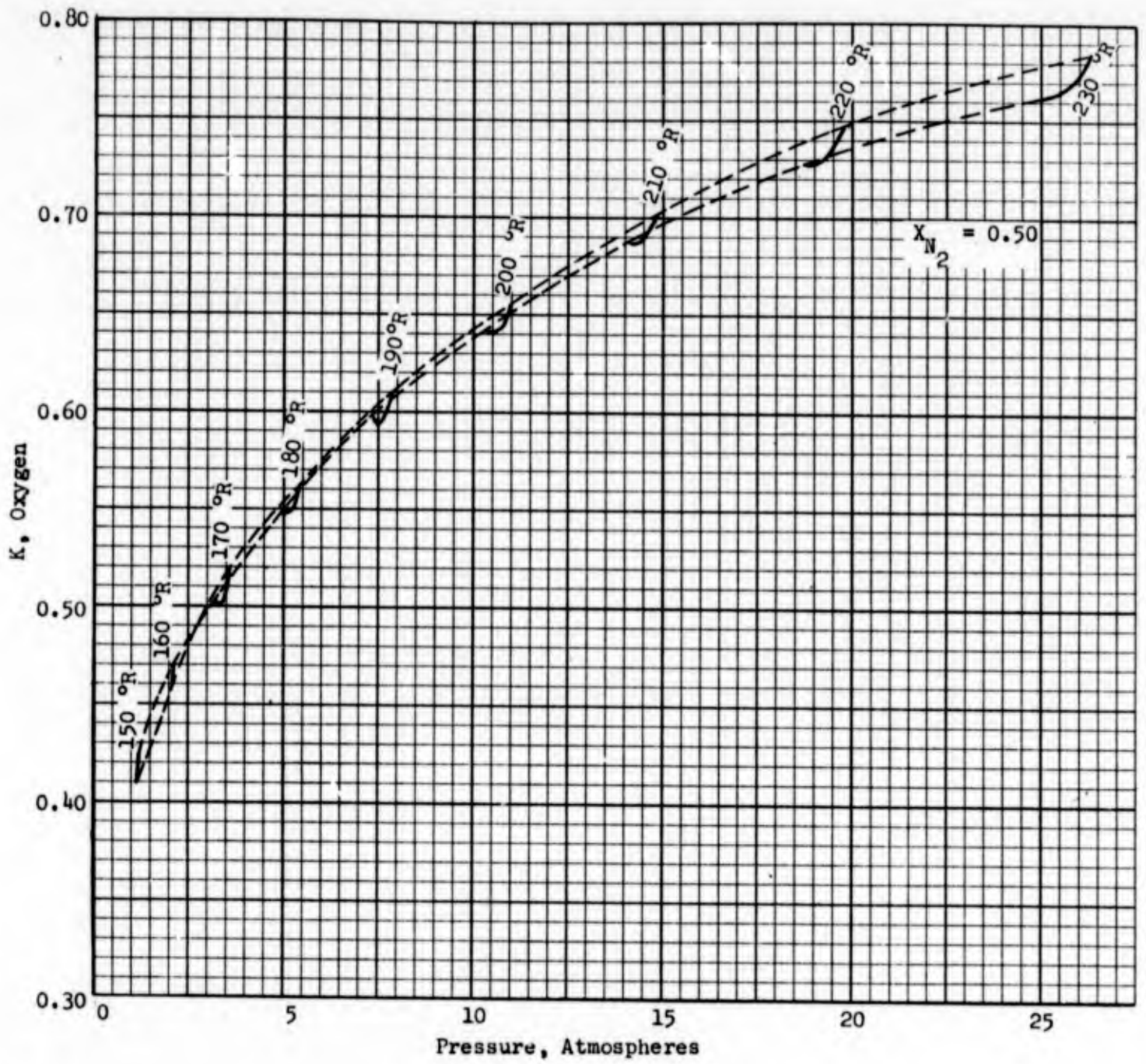


Figure 105. K-Values of Oxygen

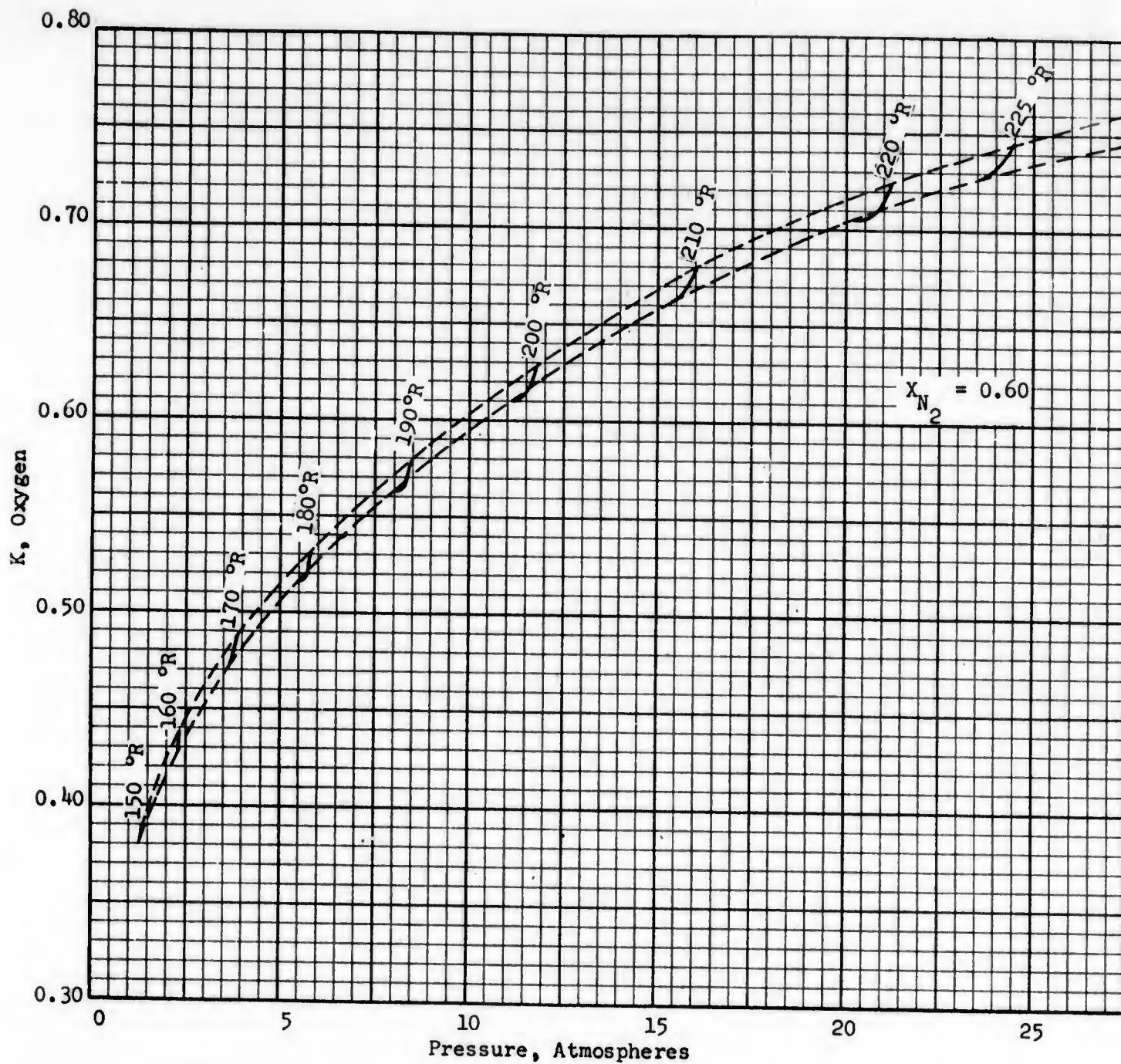


Figure 106. K-Values of Oxygen

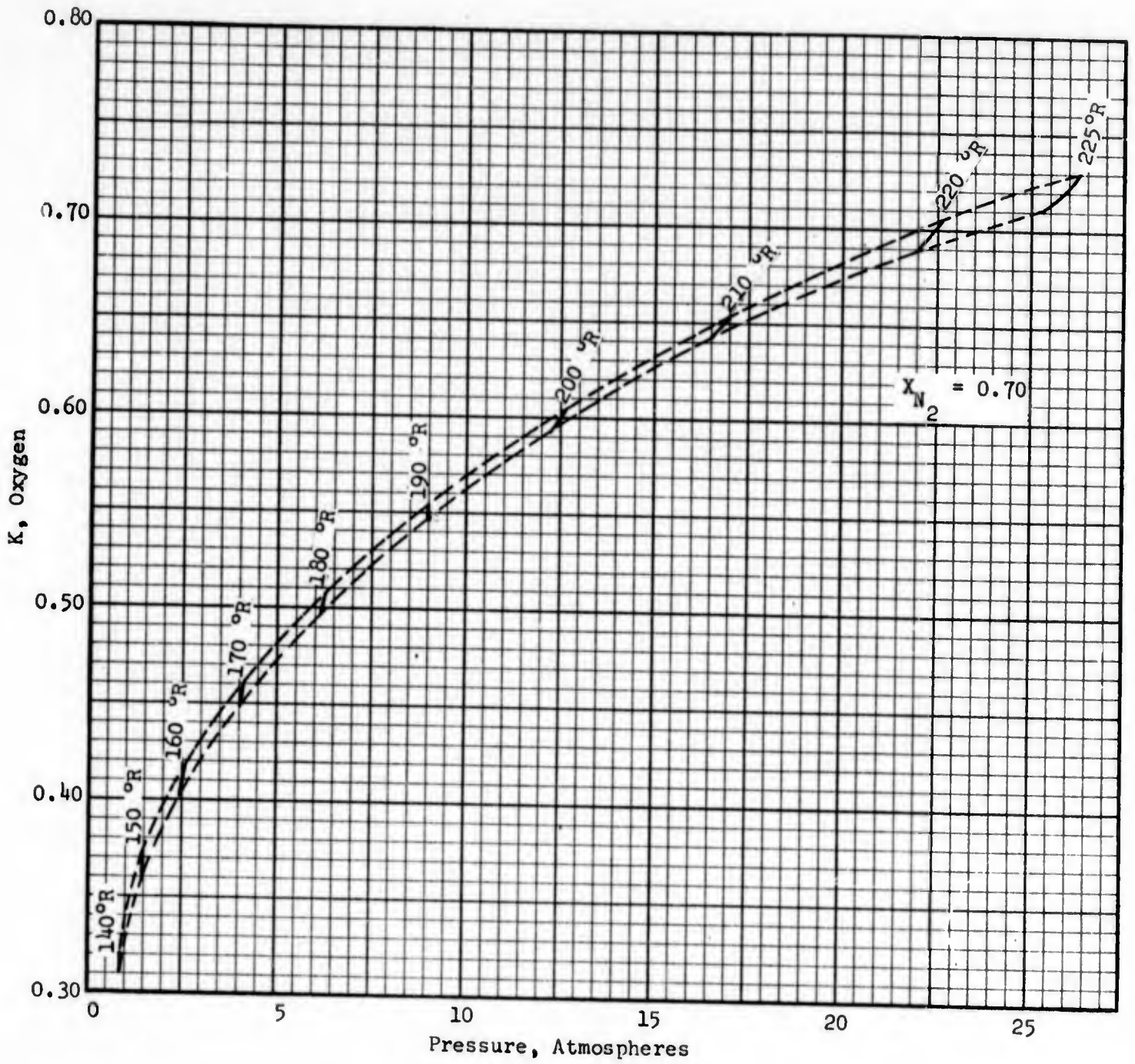


Figure 107. K-Values of Oxygen.

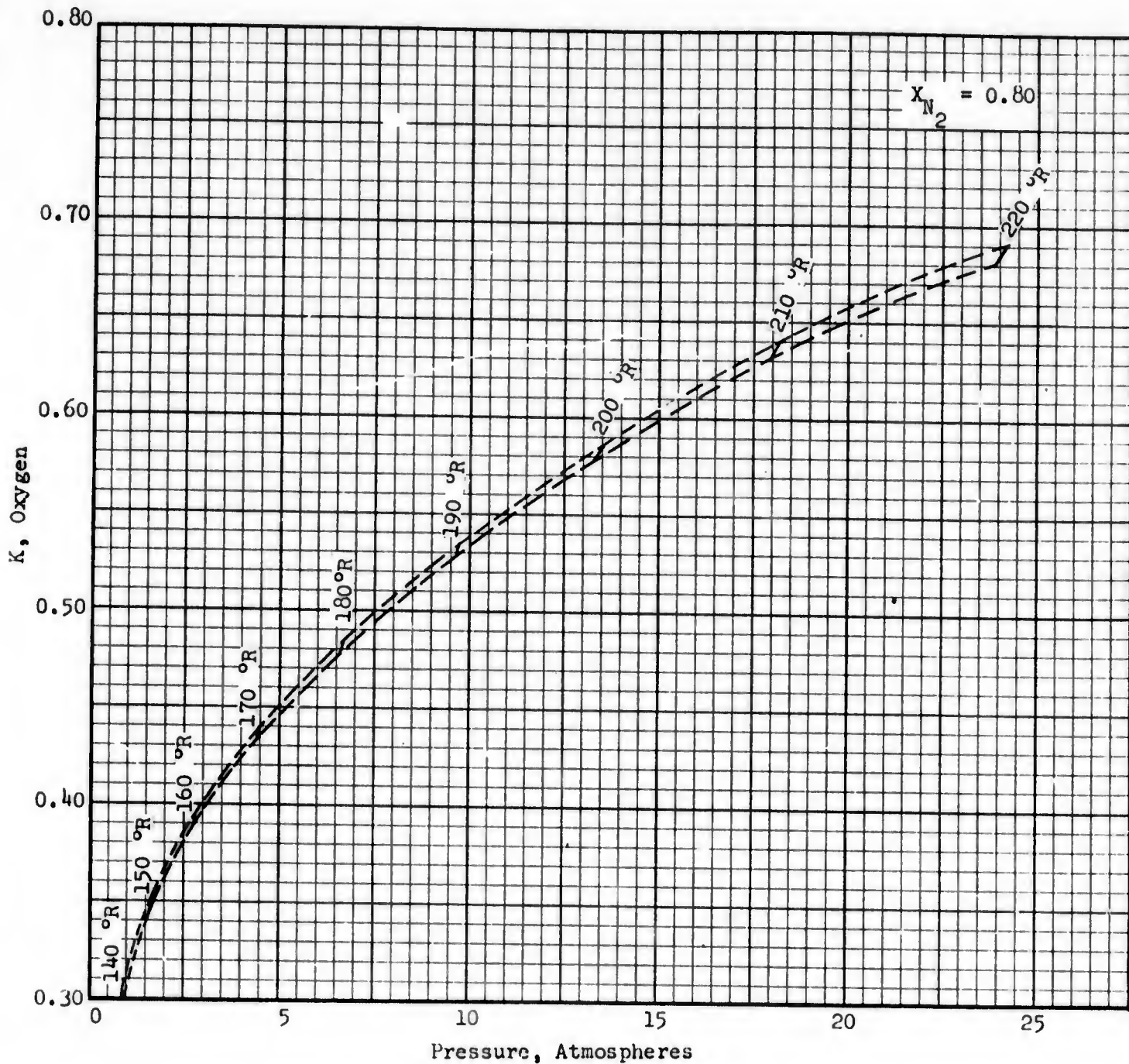


Figure 108. K-Values of Oxygen.

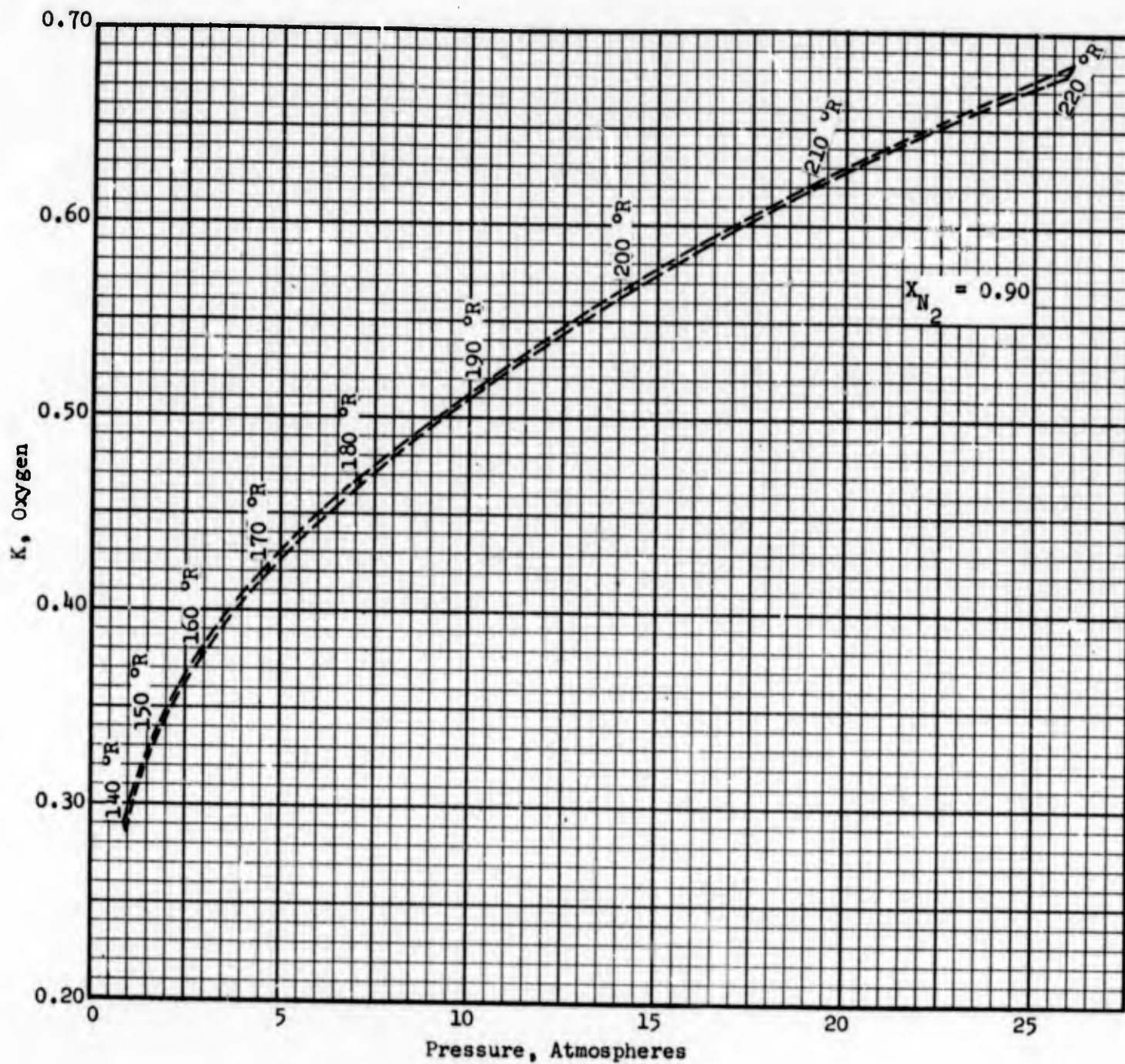


Figure 109. K-Values of Oxygen.

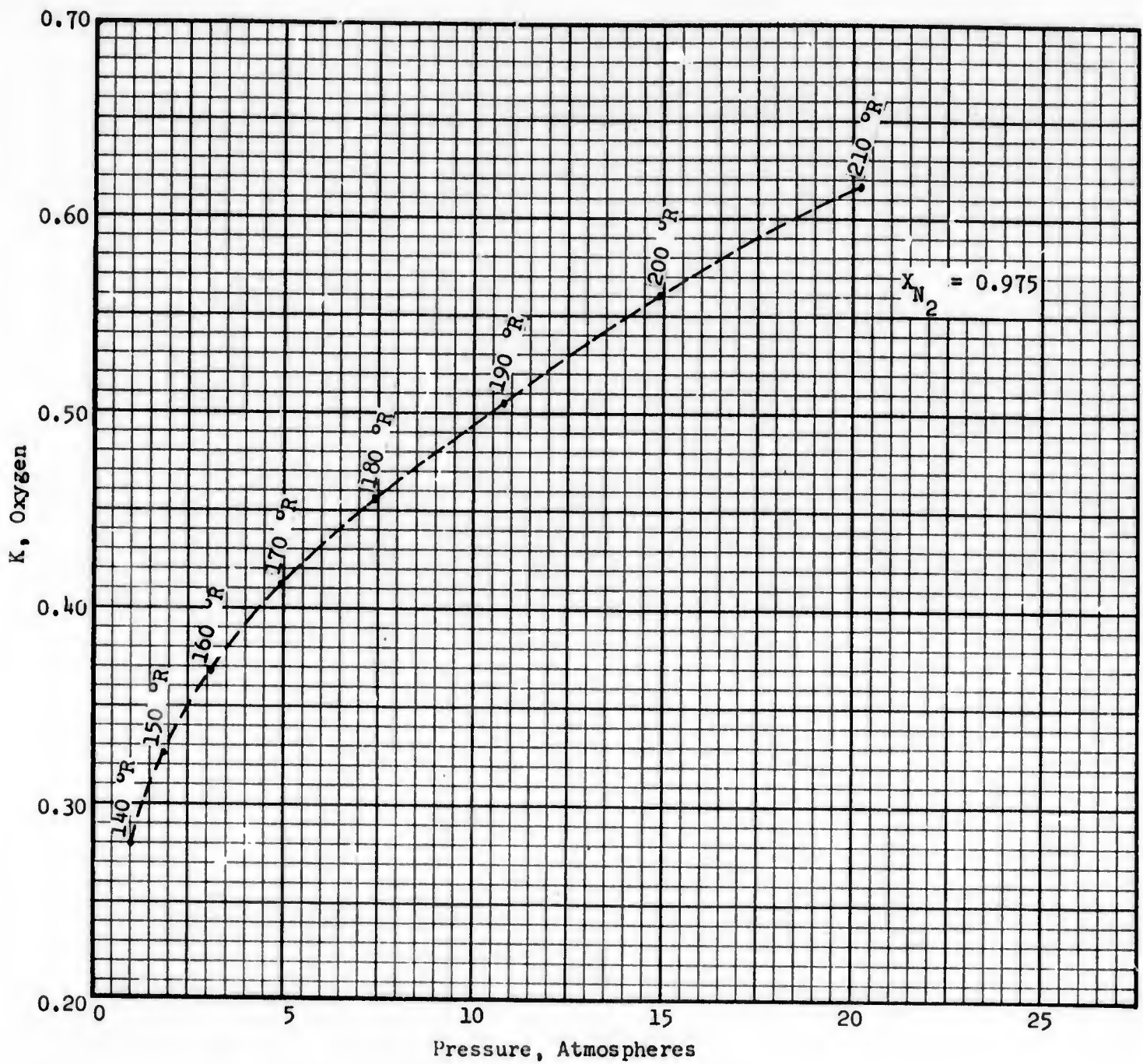


Figure 110. K-Values of Oxygen.

B. Relative Volatility of Argon to Nitrogen in Ternary System

The 12 graphs to follow present the relative volatility of argon to nitrogen defined

$$\alpha_{\text{Ar-N}_2} = \frac{y_{\text{Ar}}}{x_{\text{Ar}}} \frac{x_{\text{N}_2}}{y_{\text{N}_2}} \quad (51)$$

as a function of mole fraction argon in the liquid along selected isobars. The graphs are arranged in order of increasing mole percent nitrogen in the liquid.

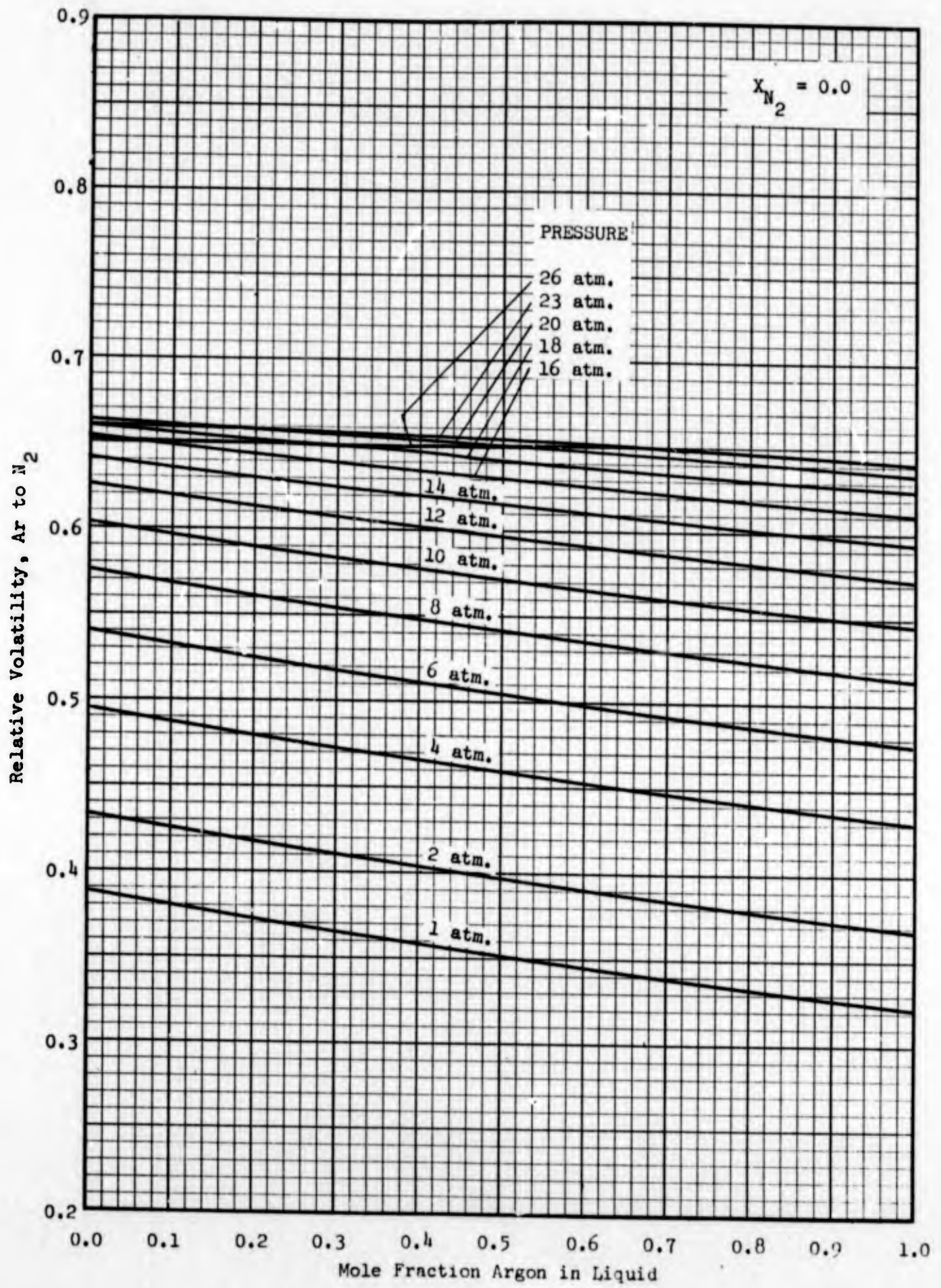


Figure 111. Relative Volatility of Argon to Nitrogen.

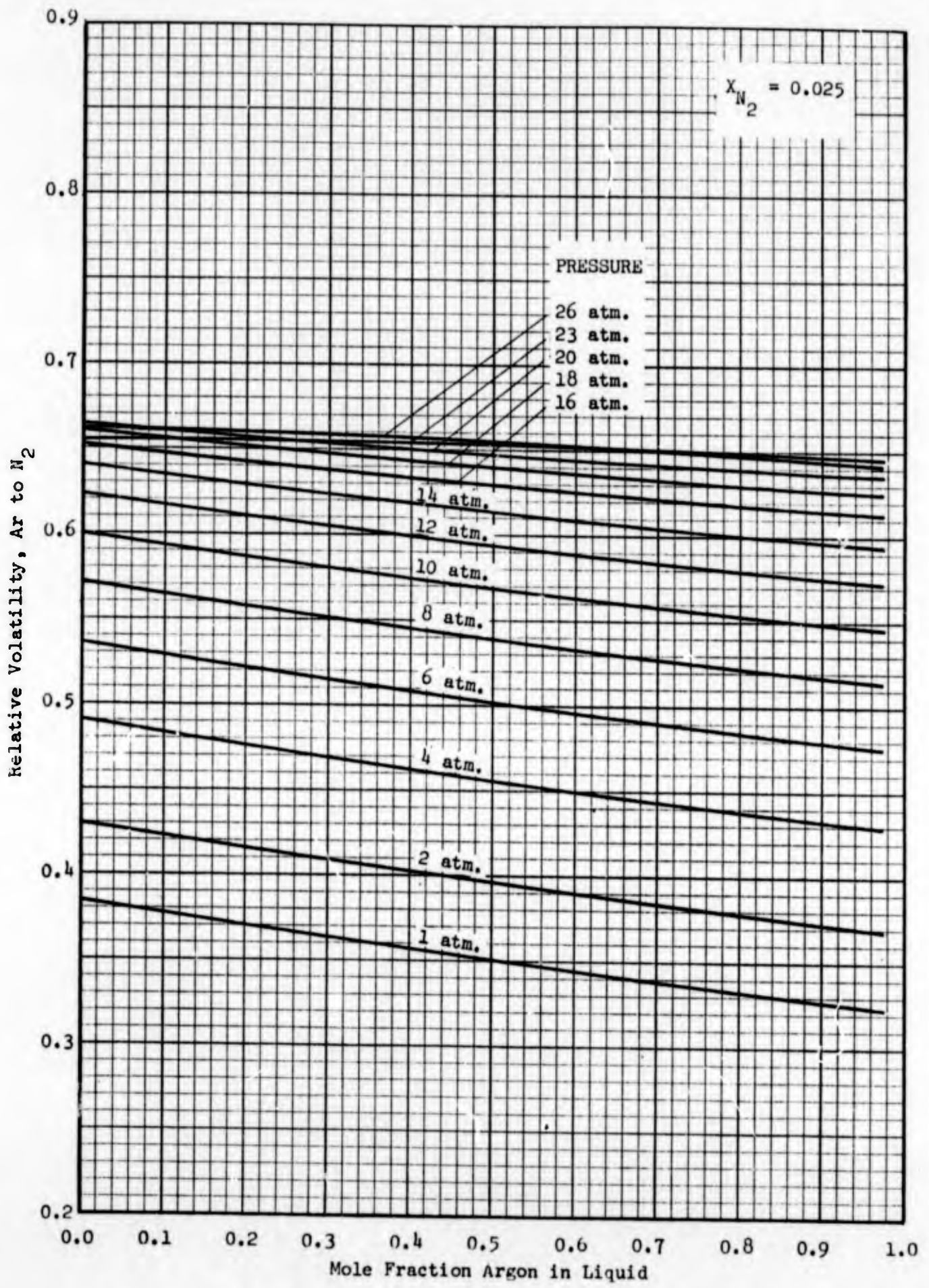


Figure 112. Relative Volatility of Argon to Nitrogen.

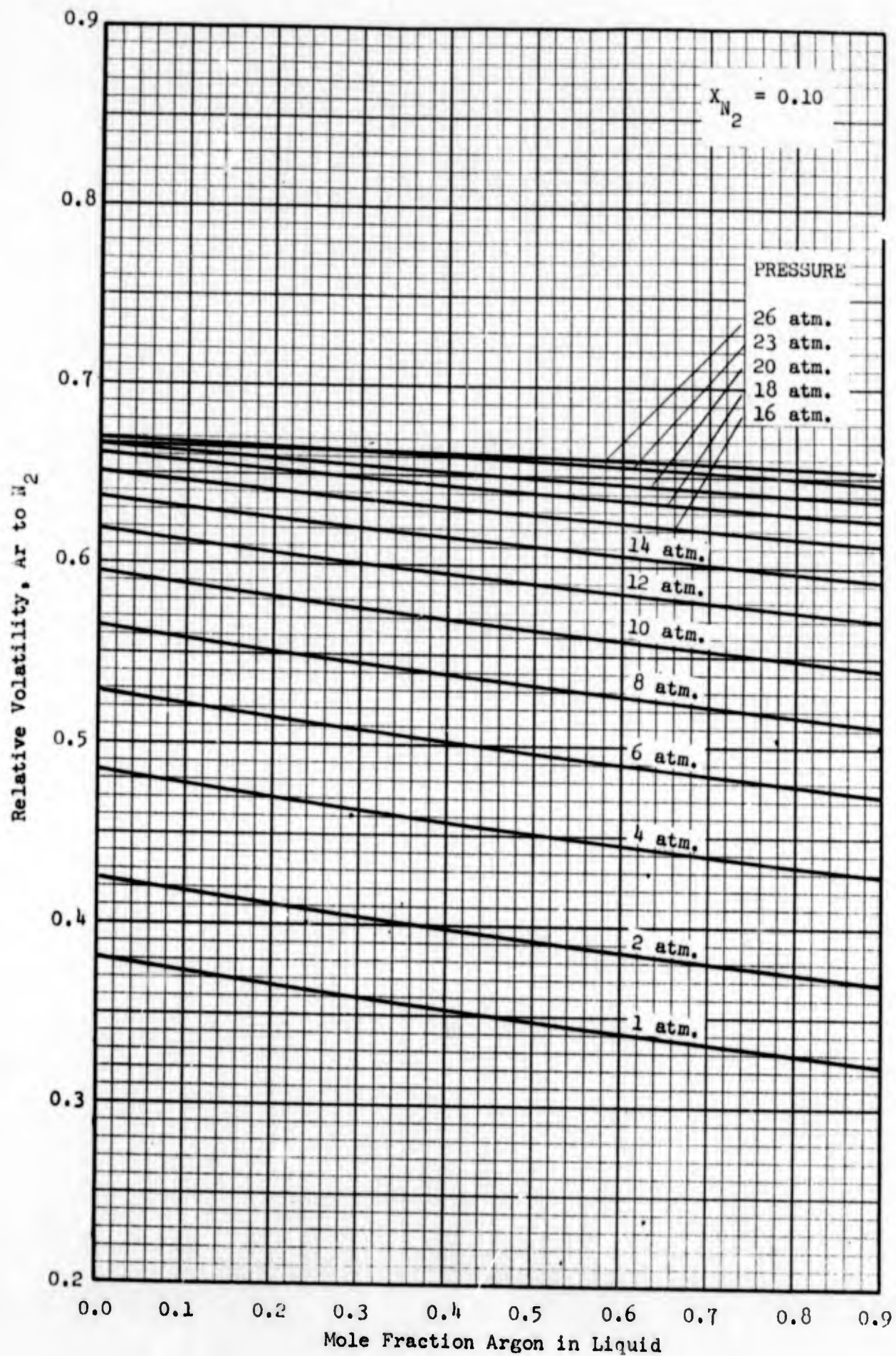


Figure 113. Relative Volatility of Argon to Nitrogen.

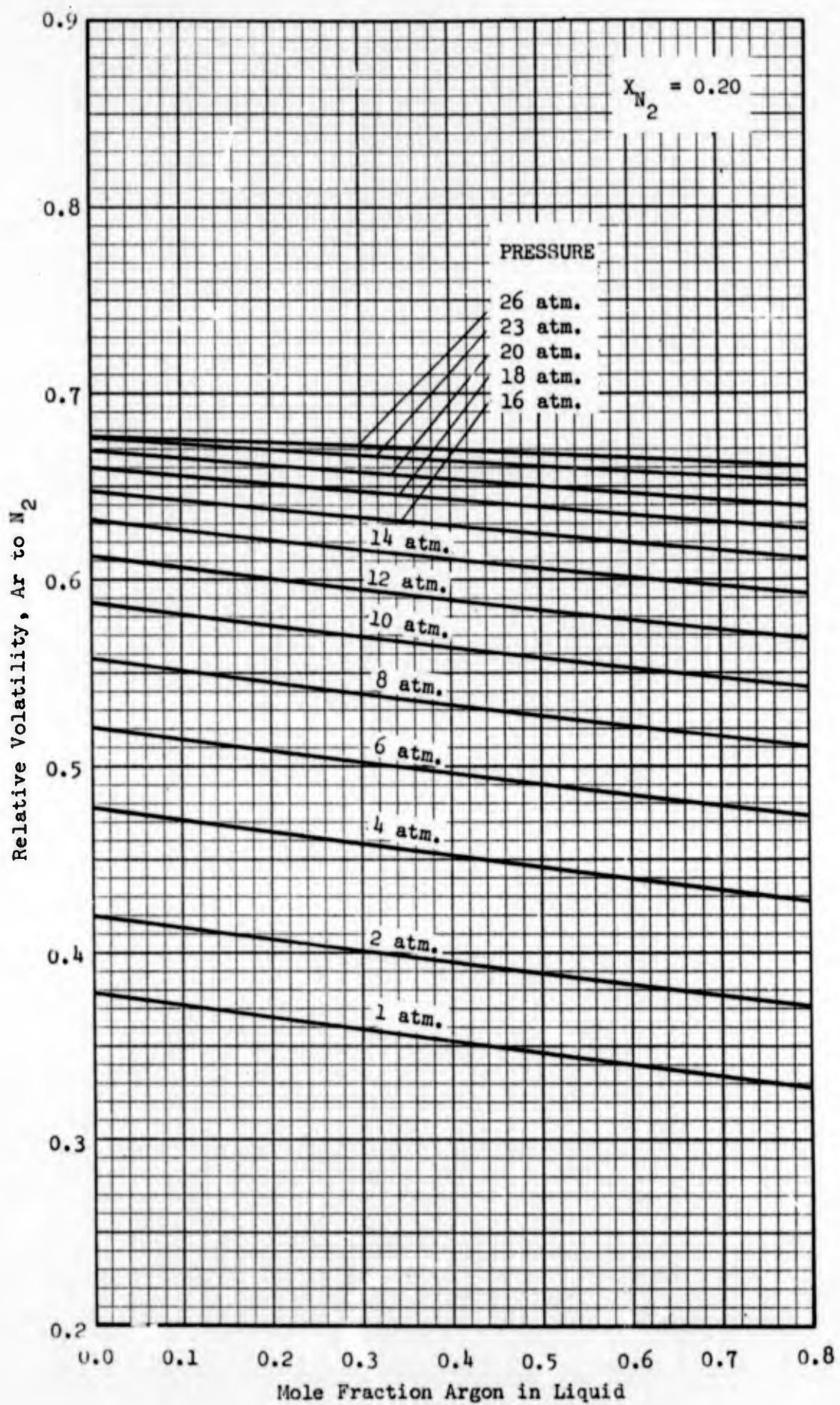


Figure 114. Relative Volatility of Argon to Nitrogen.

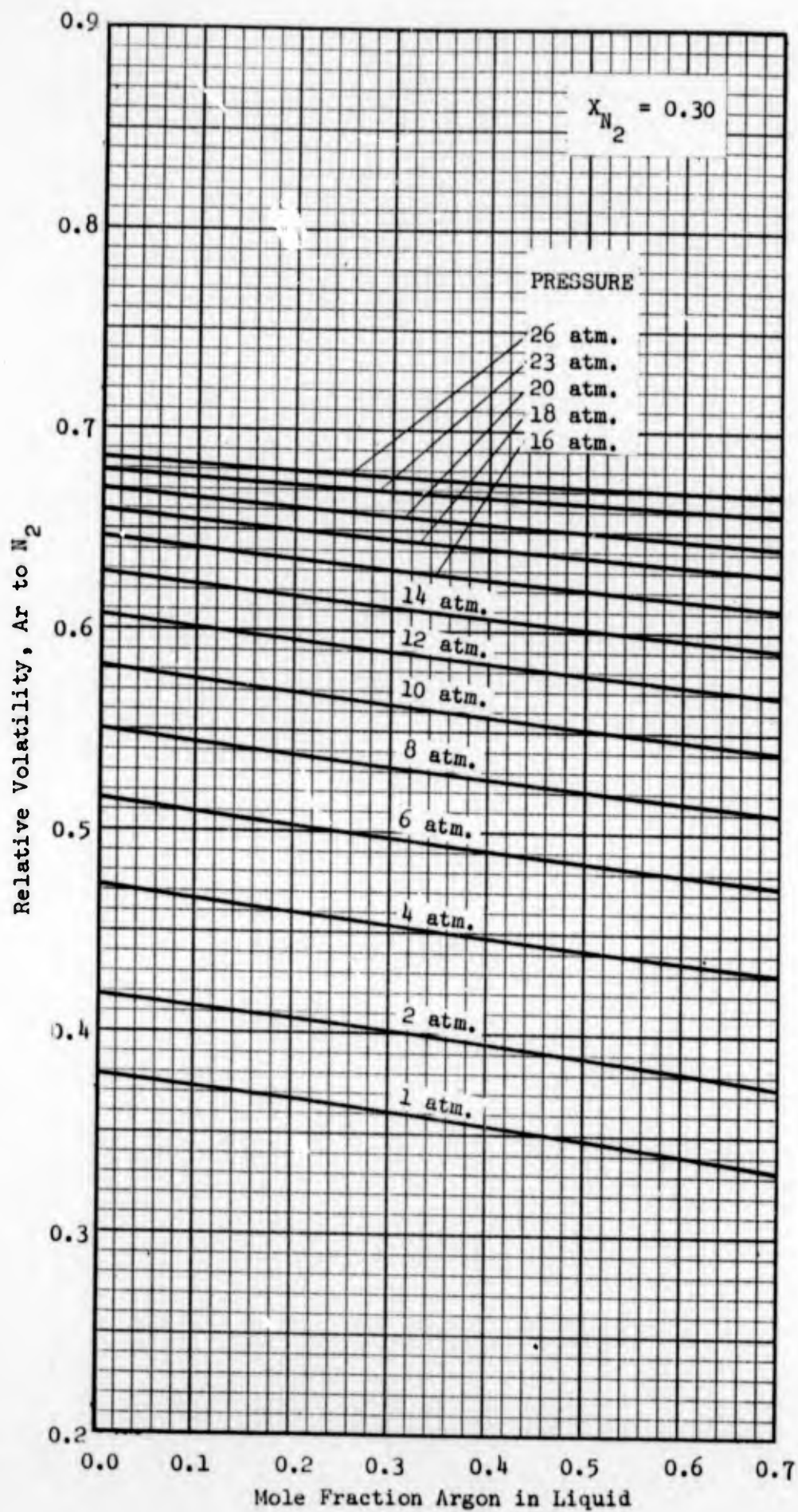


Figure 115. Relative Volatility of Argon to Nitrogen.

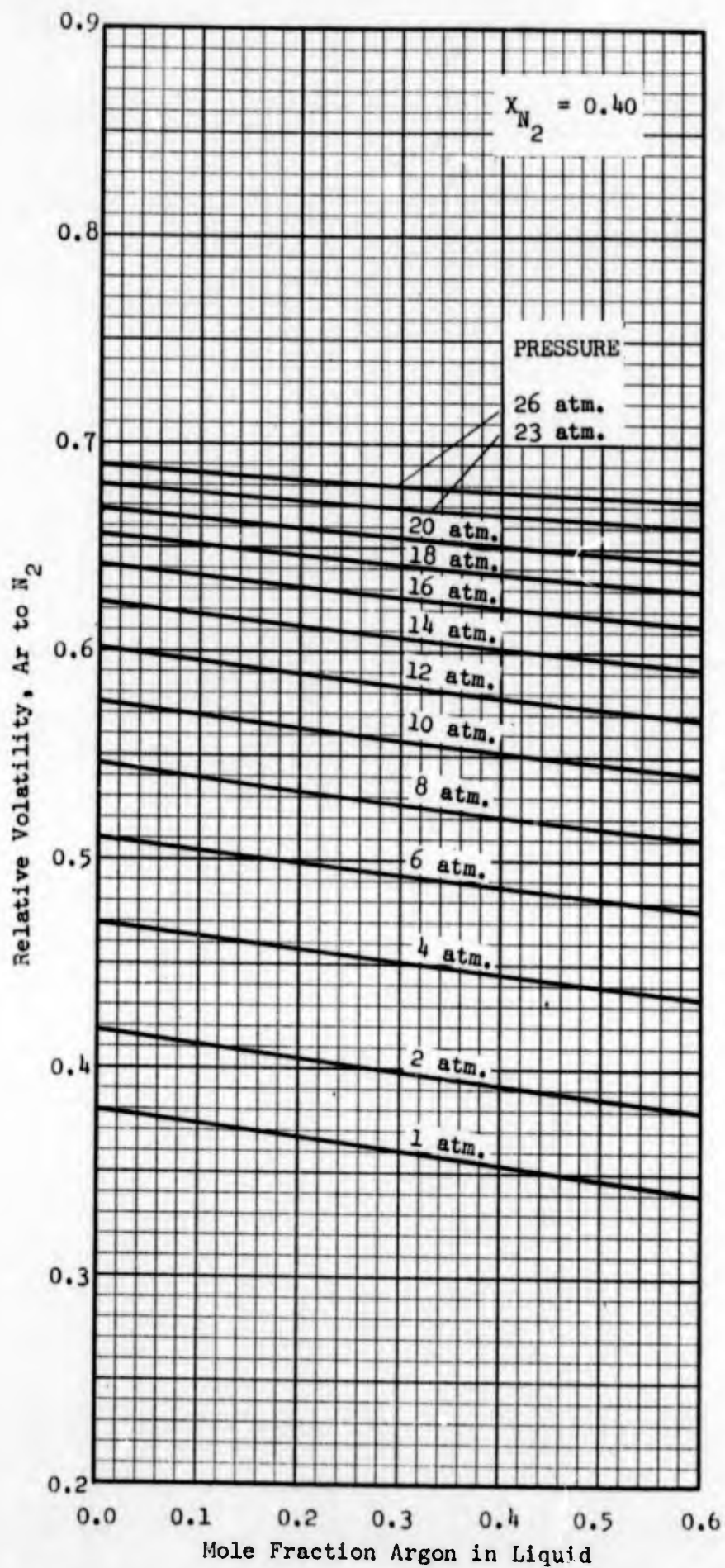


Figure 116. Relative Volatility of Argon to Nitrogen.

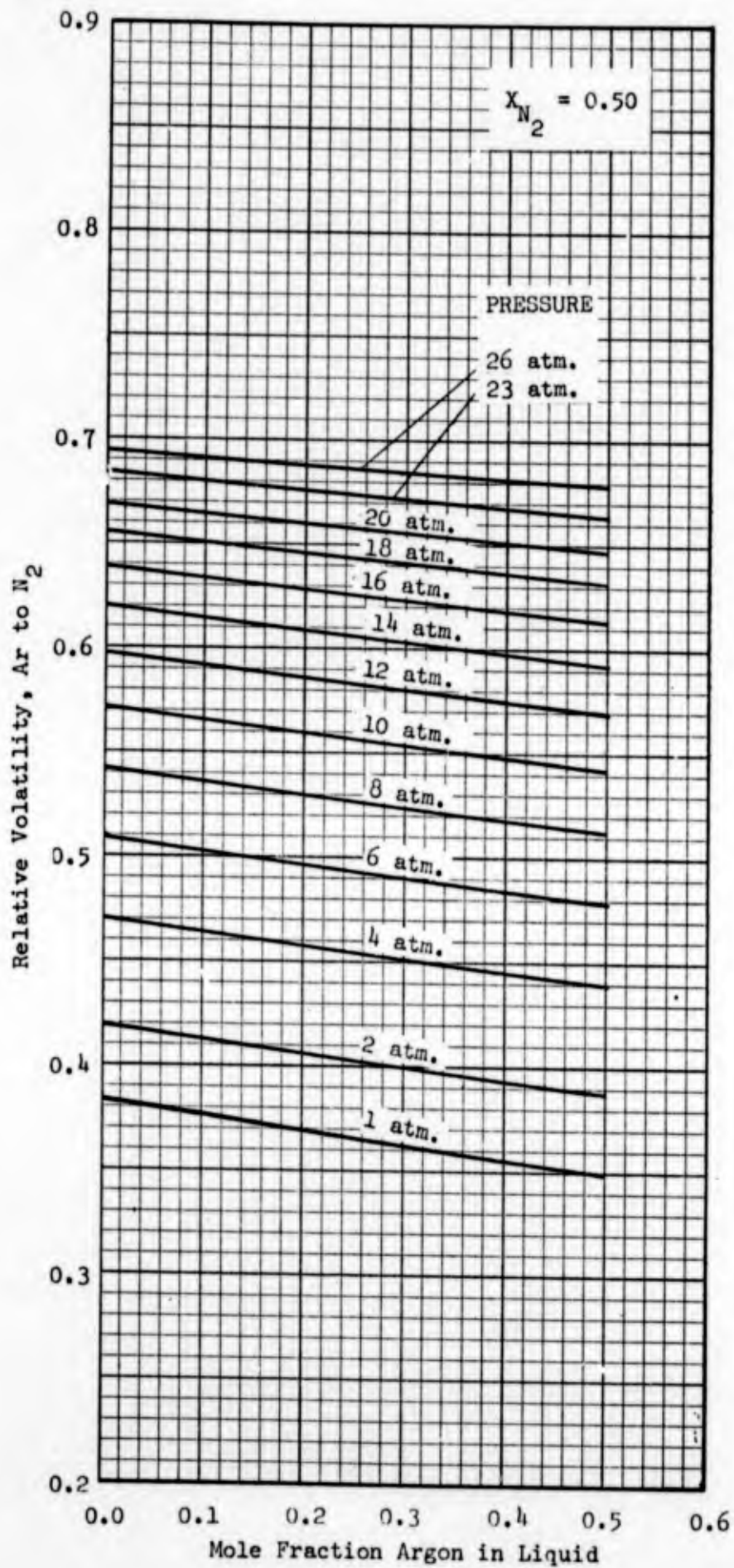


Figure 117. Relative Volatility of Argon to Nitrogen.

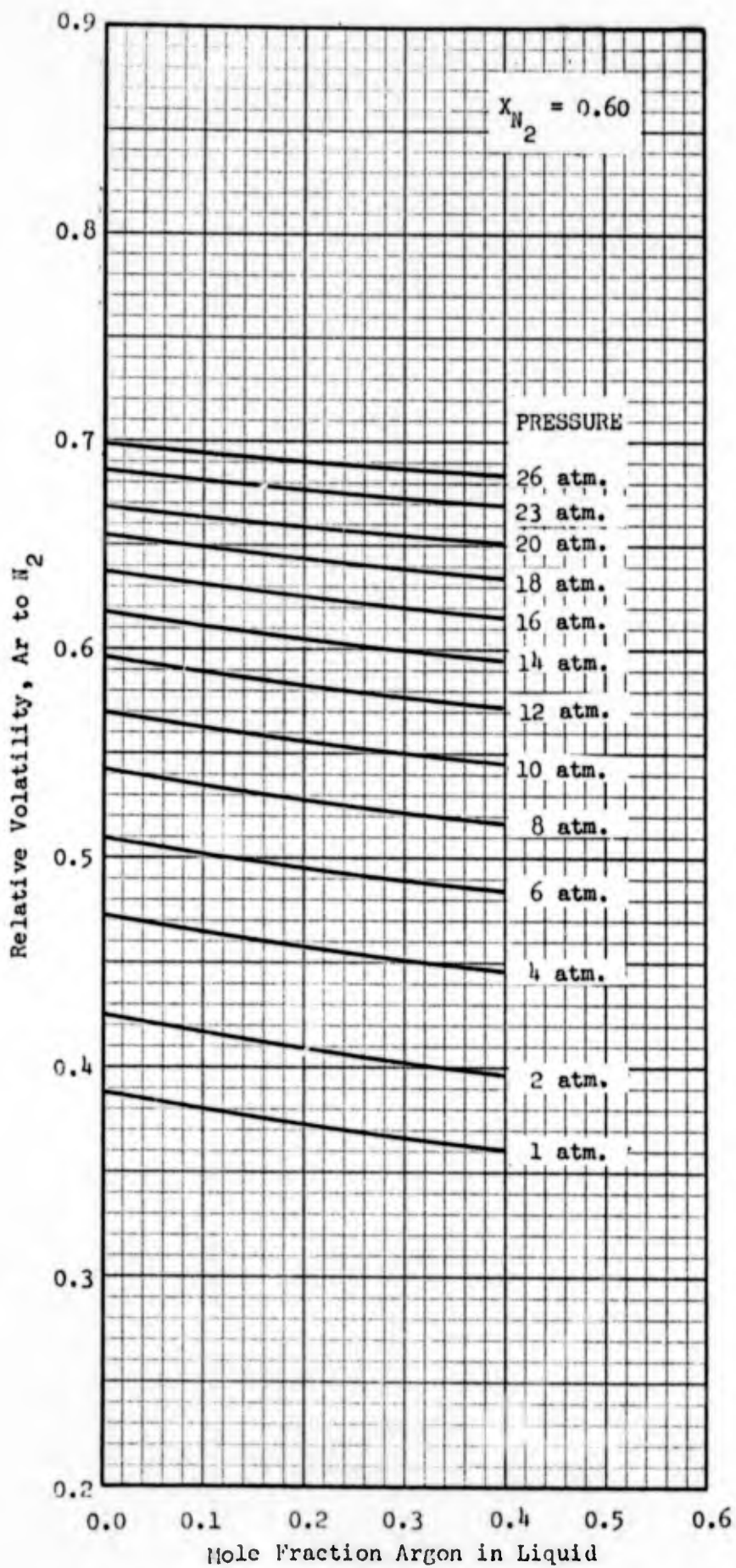


Figure 118. Relative Volatility of Argon to Nitrogen.

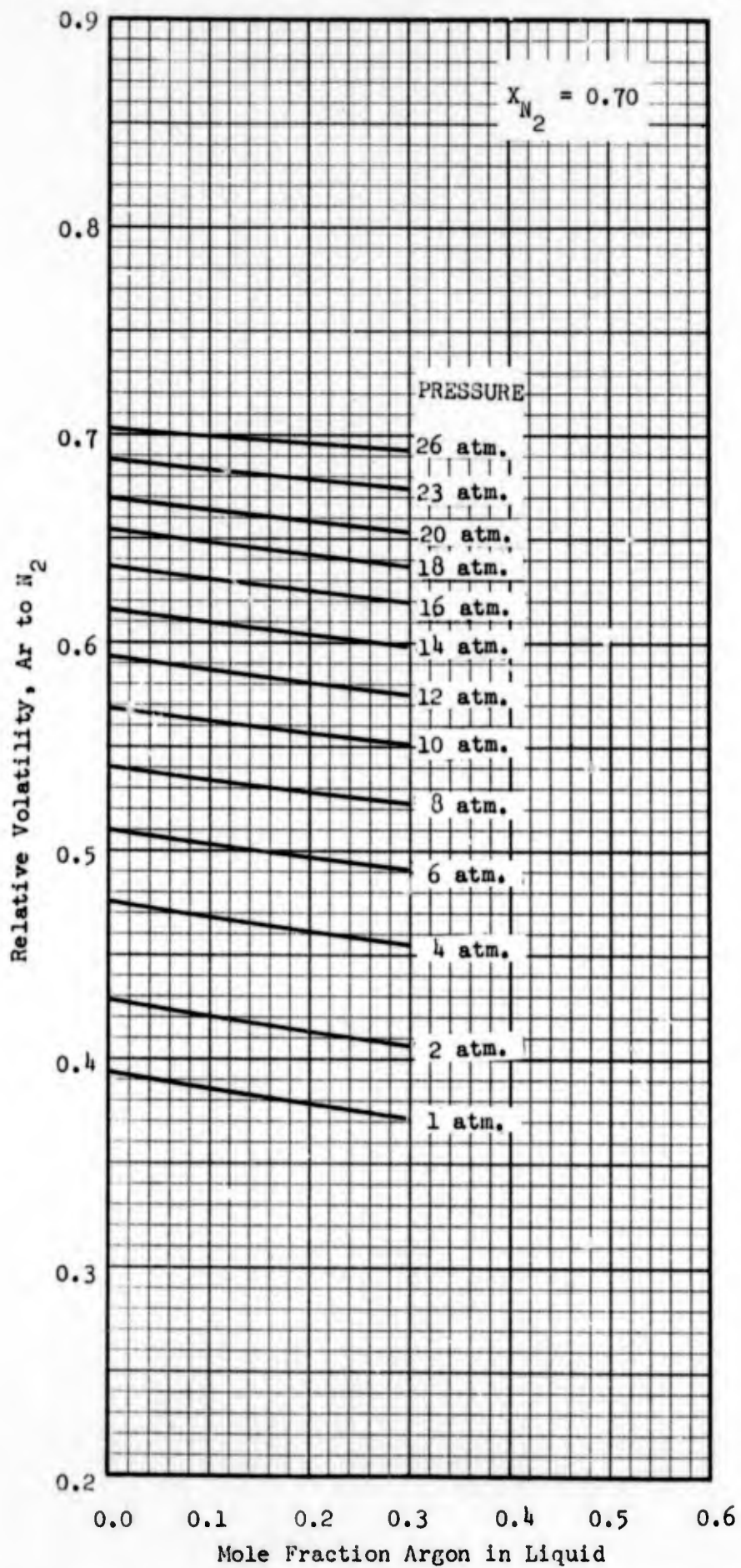


Figure 119. Relative Volatility of Argon to Nitrogen.

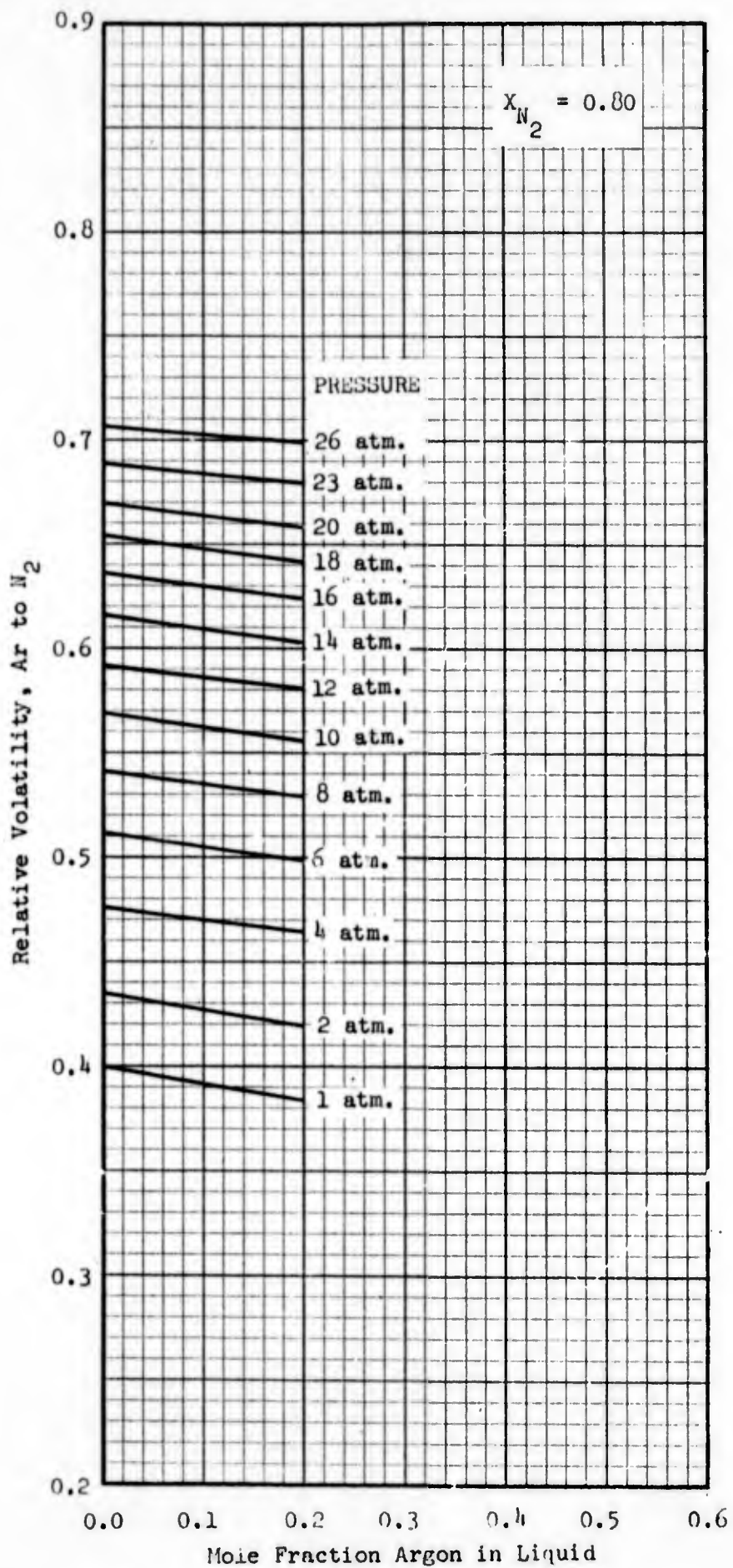


Figure 120. Relative Volatility of Argon to Nitrogen.

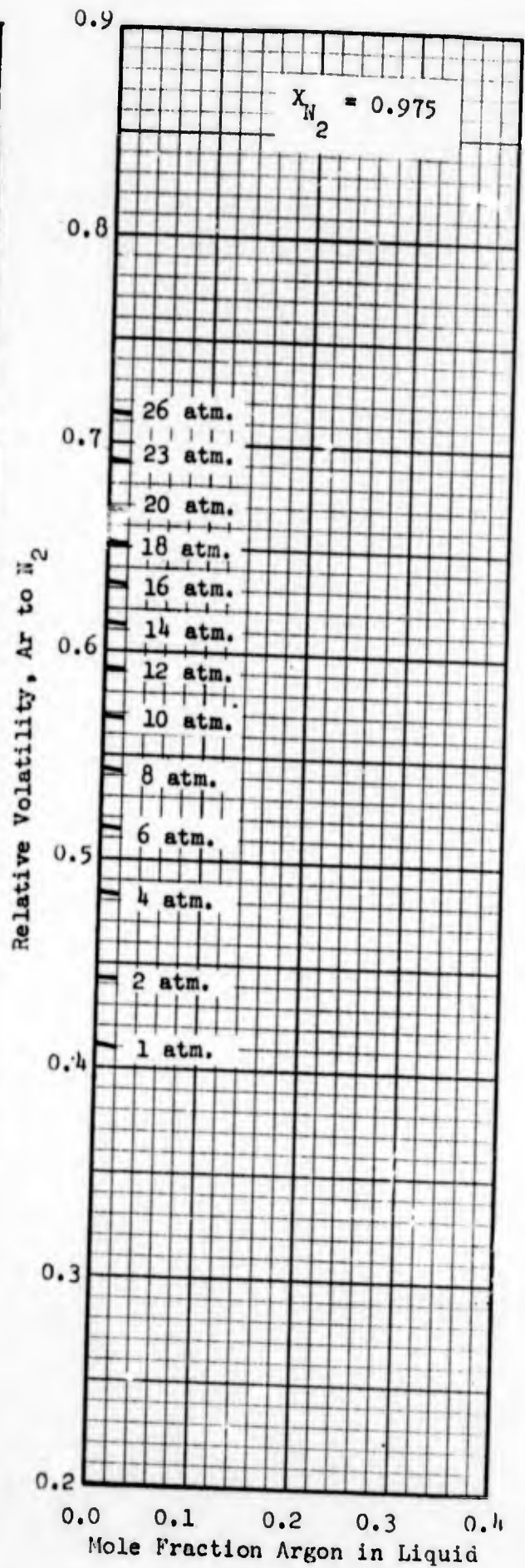
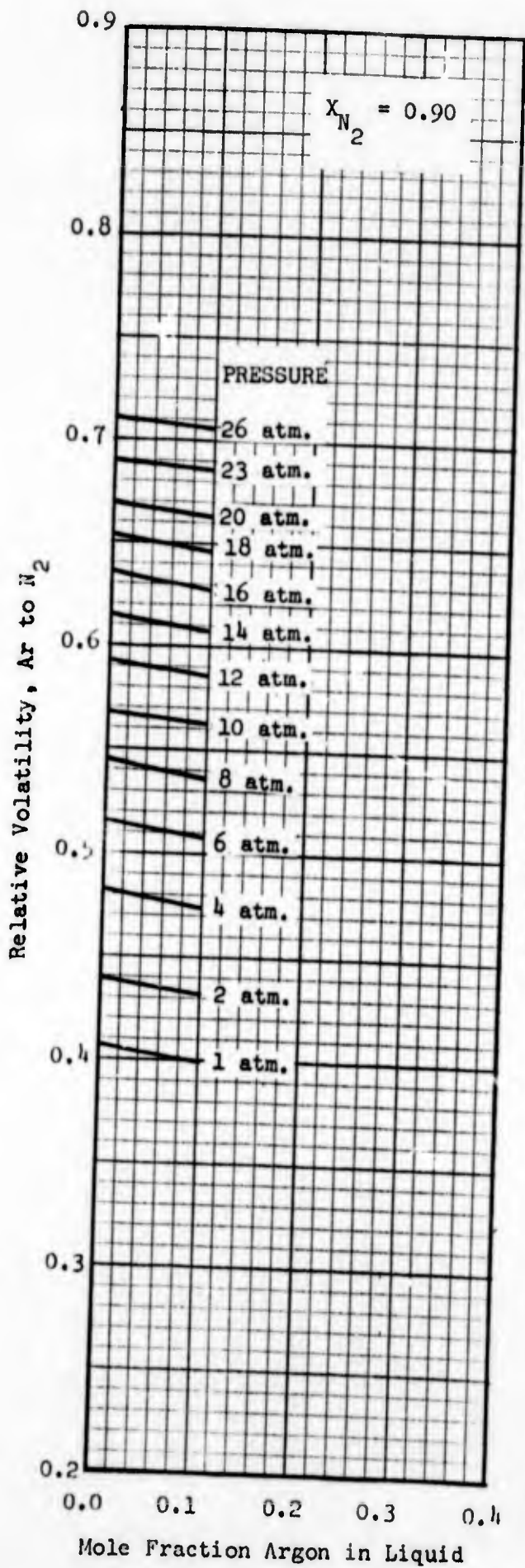


Figure 121. Relative Volatility of Argon to Nitrogen.

C. Relative Volatility of Argon to Oxygen
in Ternary System

The 12 graphs to follow present the relative volatility of argon to oxygen defined

$$\alpha_{\text{Ar-O}_2} = \frac{y_{\text{Ar}}}{x_{\text{Ar}}} \cdot \frac{x_{\text{O}_2}}{y_{\text{O}_2}} \quad (52)$$

as a function of mole fraction argon in the liquid along selected isobars. The graphs are arranged in order of increasing mole percent nitrogen in the liquid.

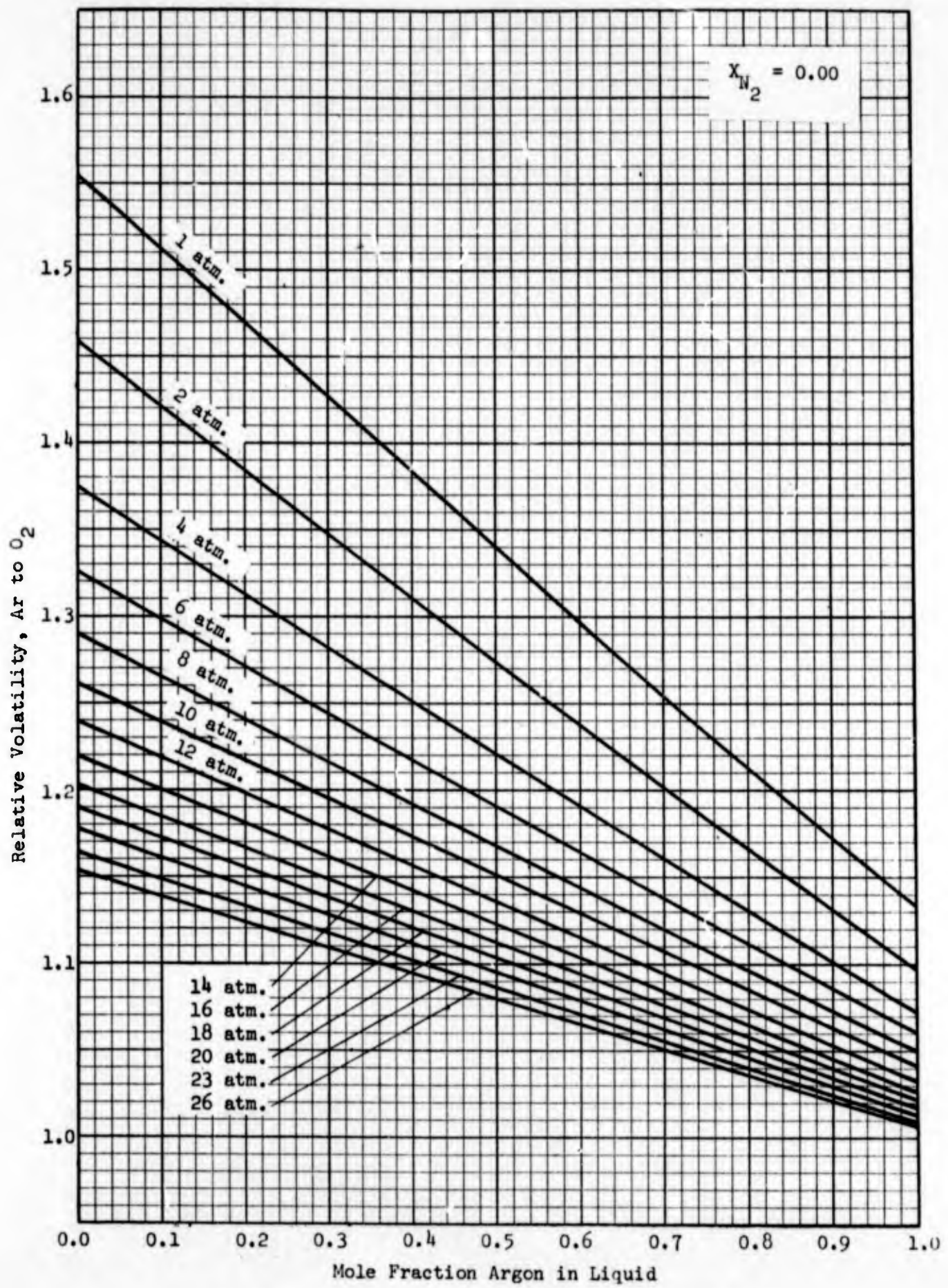


Figure 122. Relative Volatility of Argon to Oxygen.

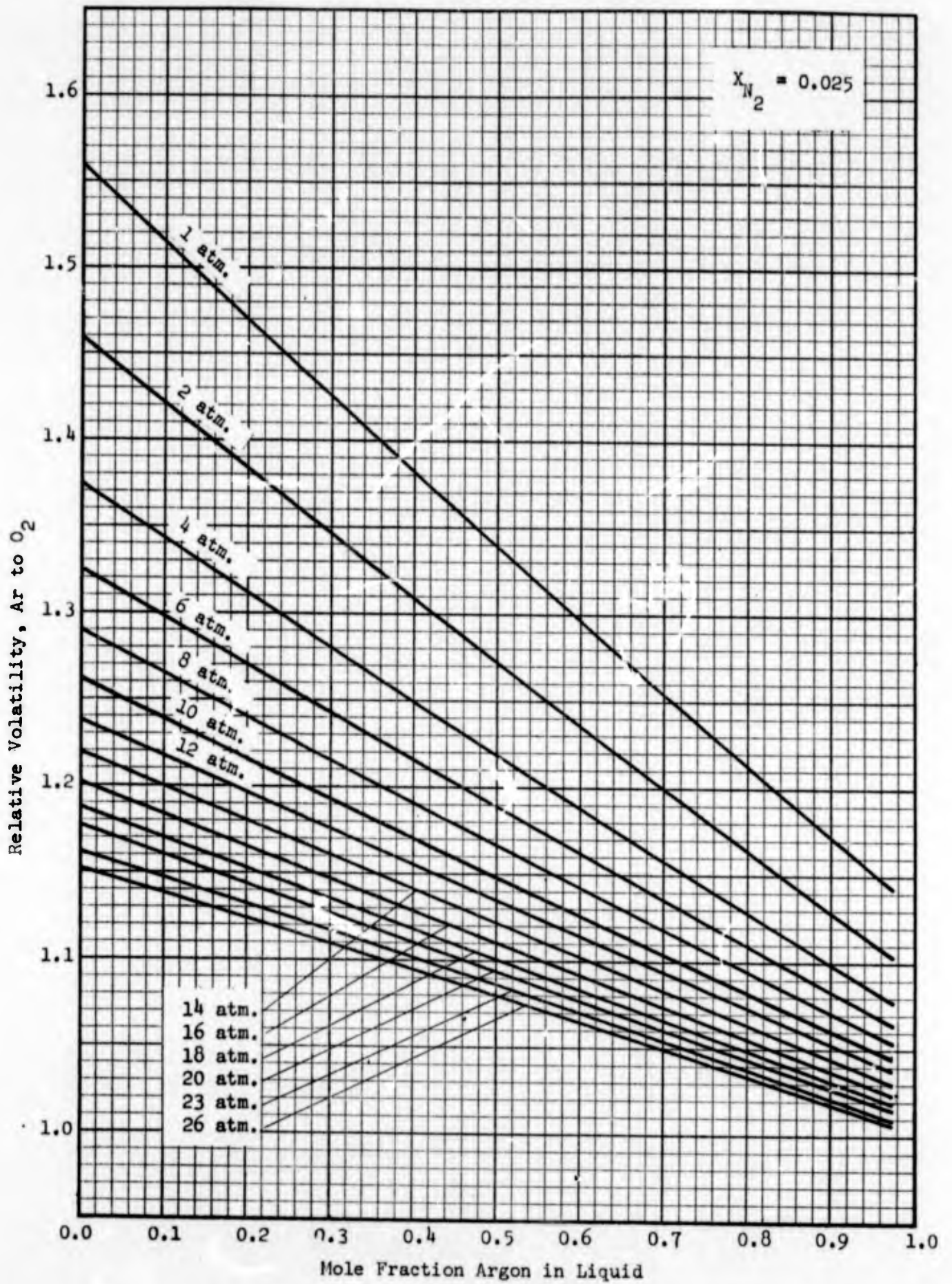


Figure 123. Relative Volatility of Argon to Oxygen.

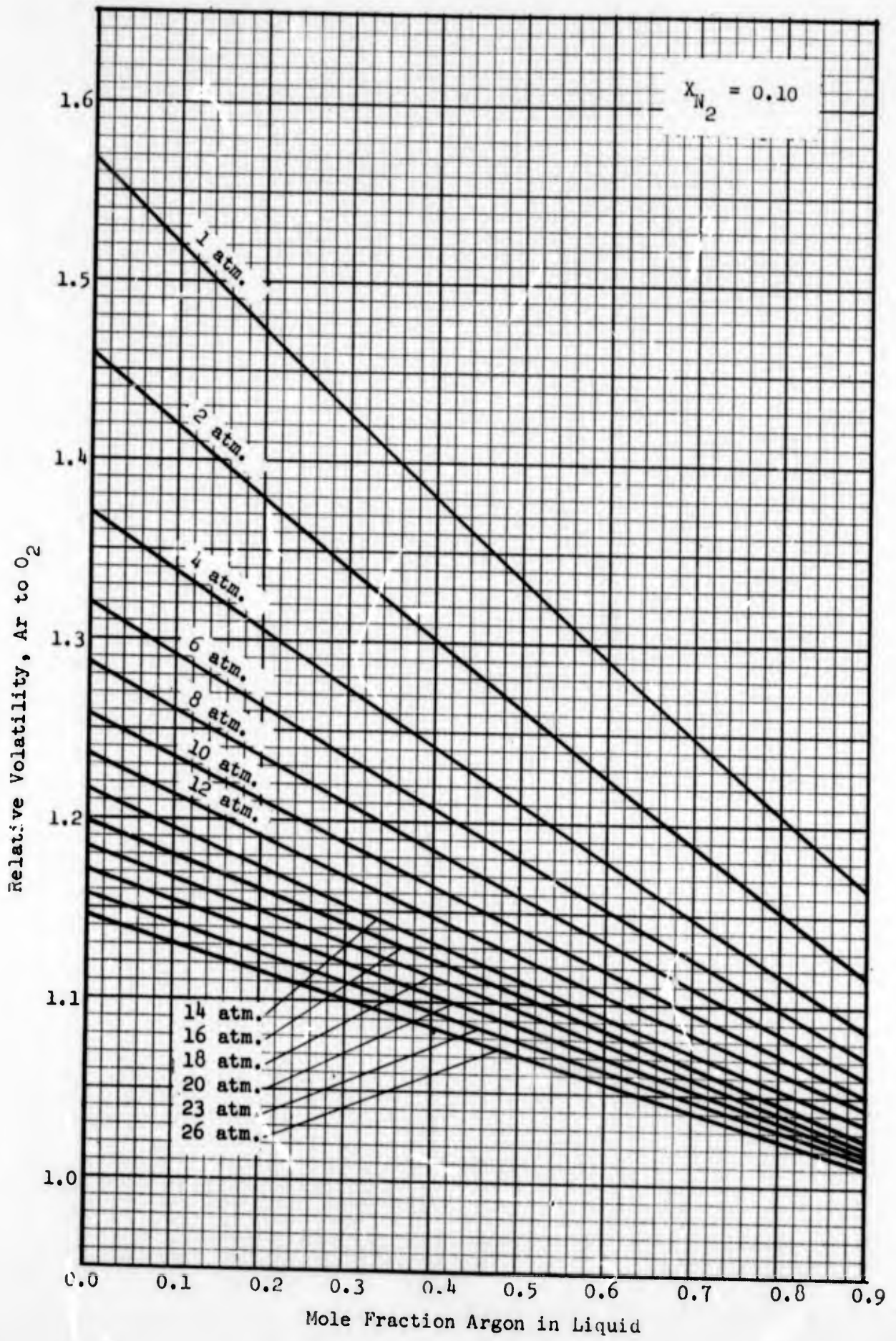


Figure 124. Relative Volatility of Argon to Oxygen.

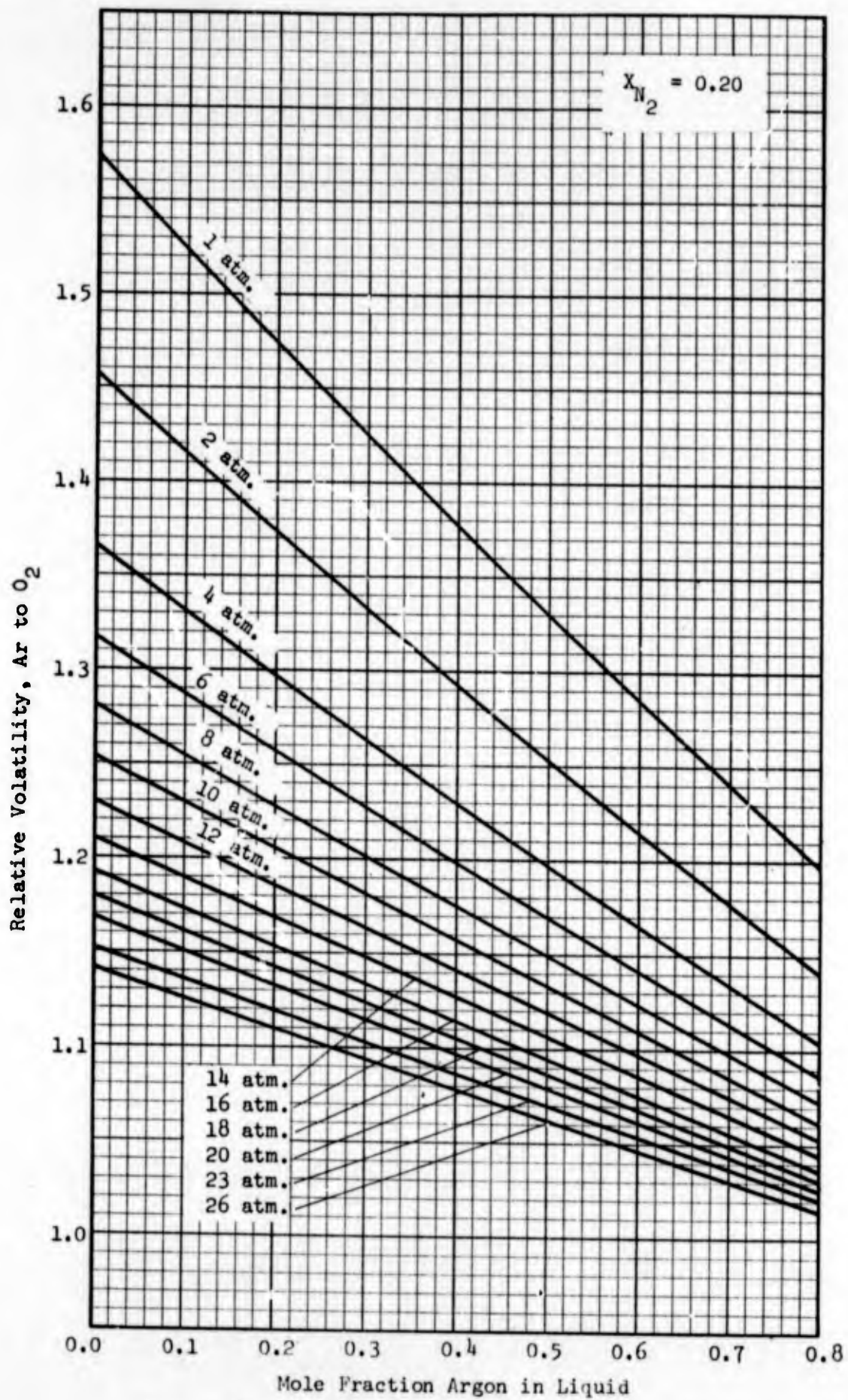


Figure 125. Relative Volatility of Argon to Oxygen.

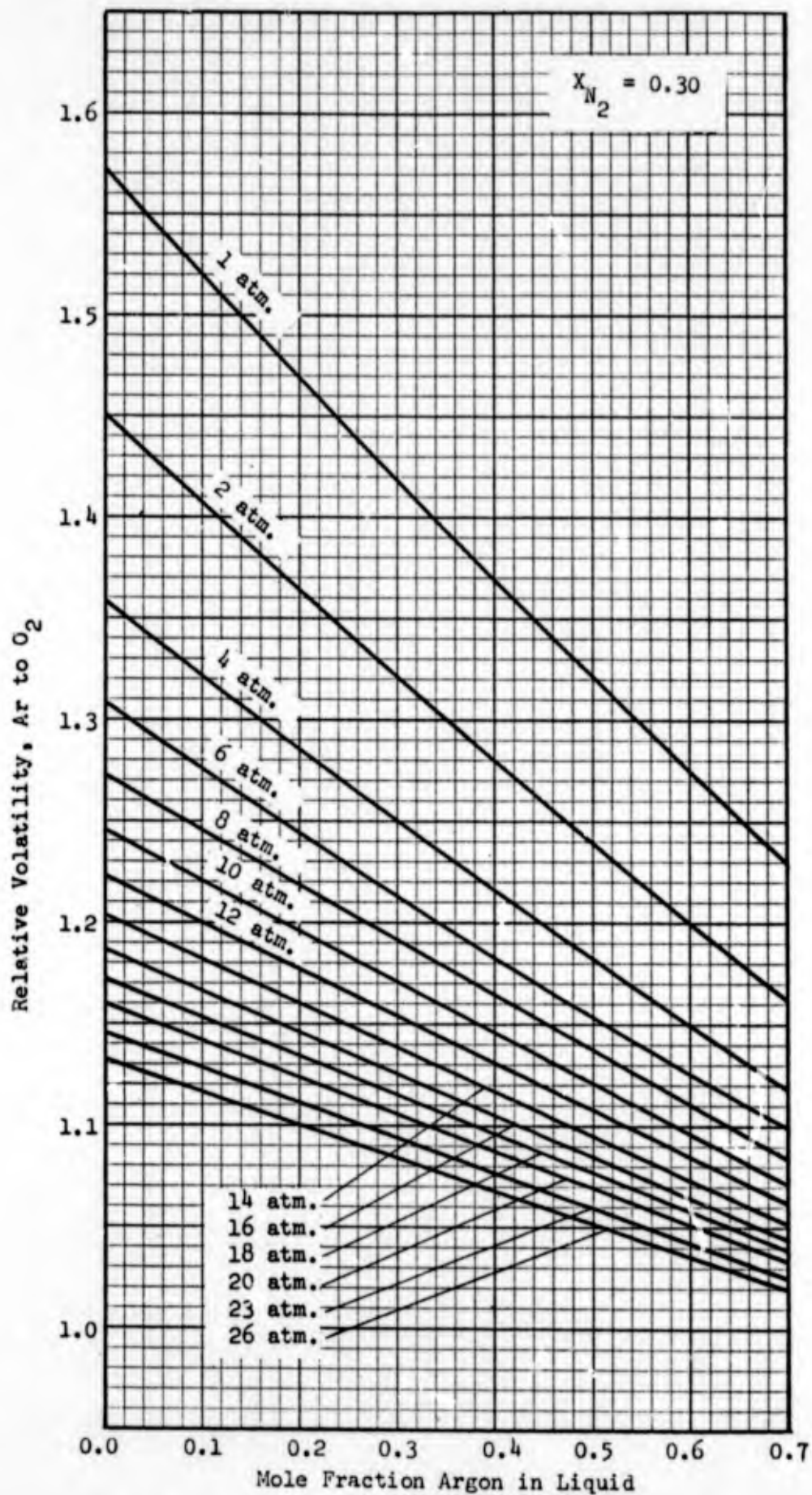


Figure 126. Relative Volatility of Argon to Oxygen.

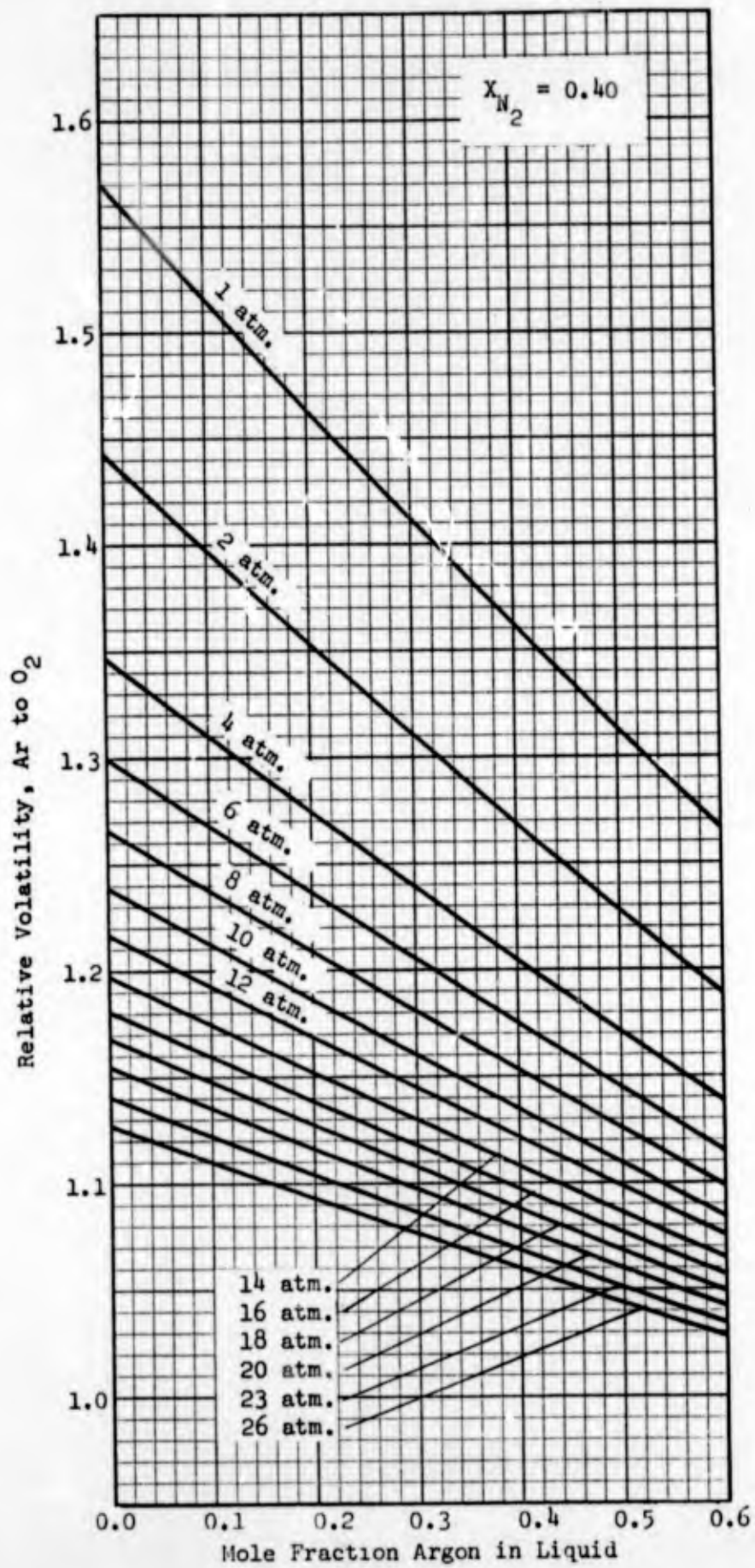


Figure 127. Relative Volatility of Argon to Oxygen.

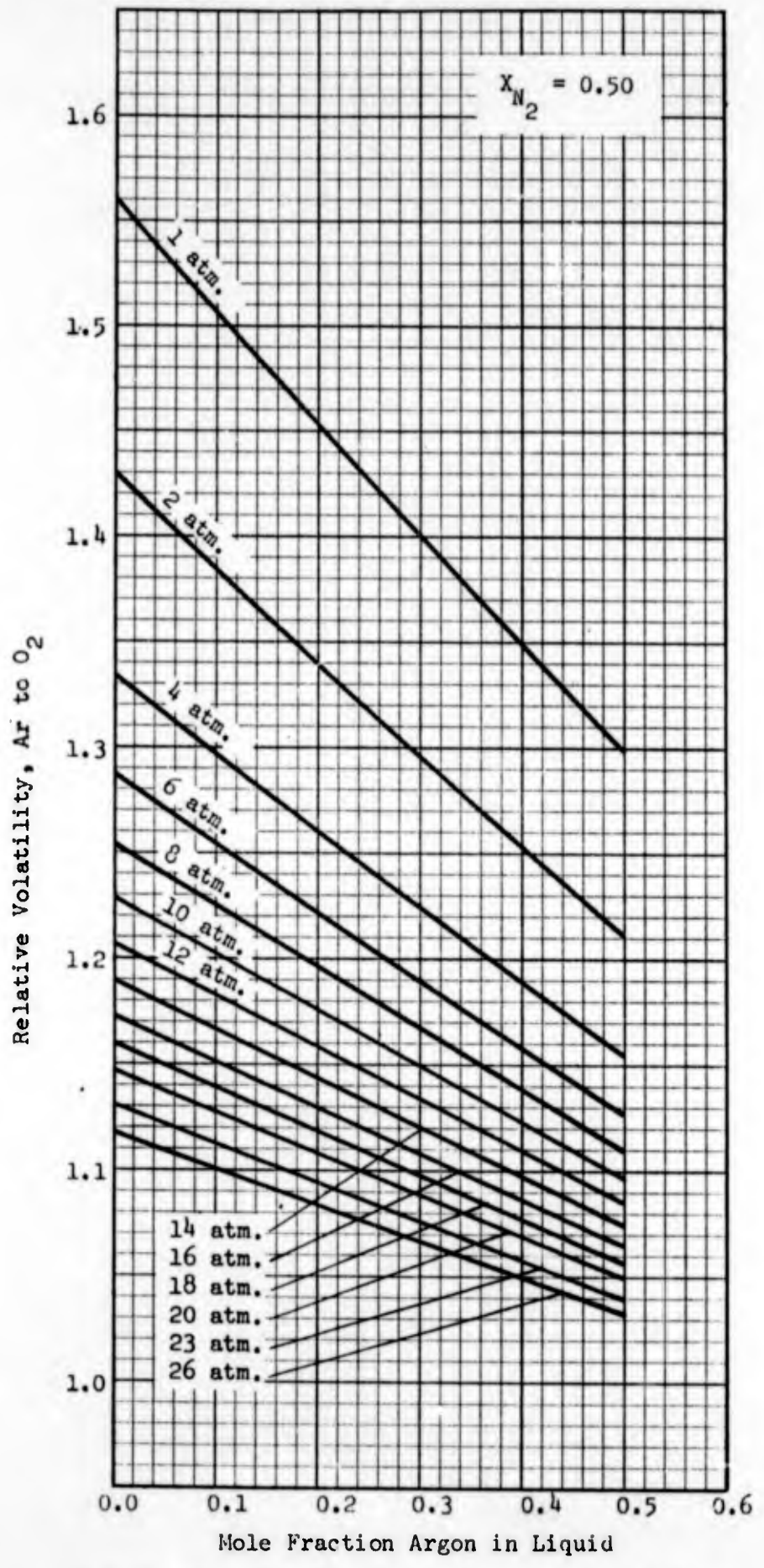


Figure 128. Relative Volatility of Argon to Oxygen.

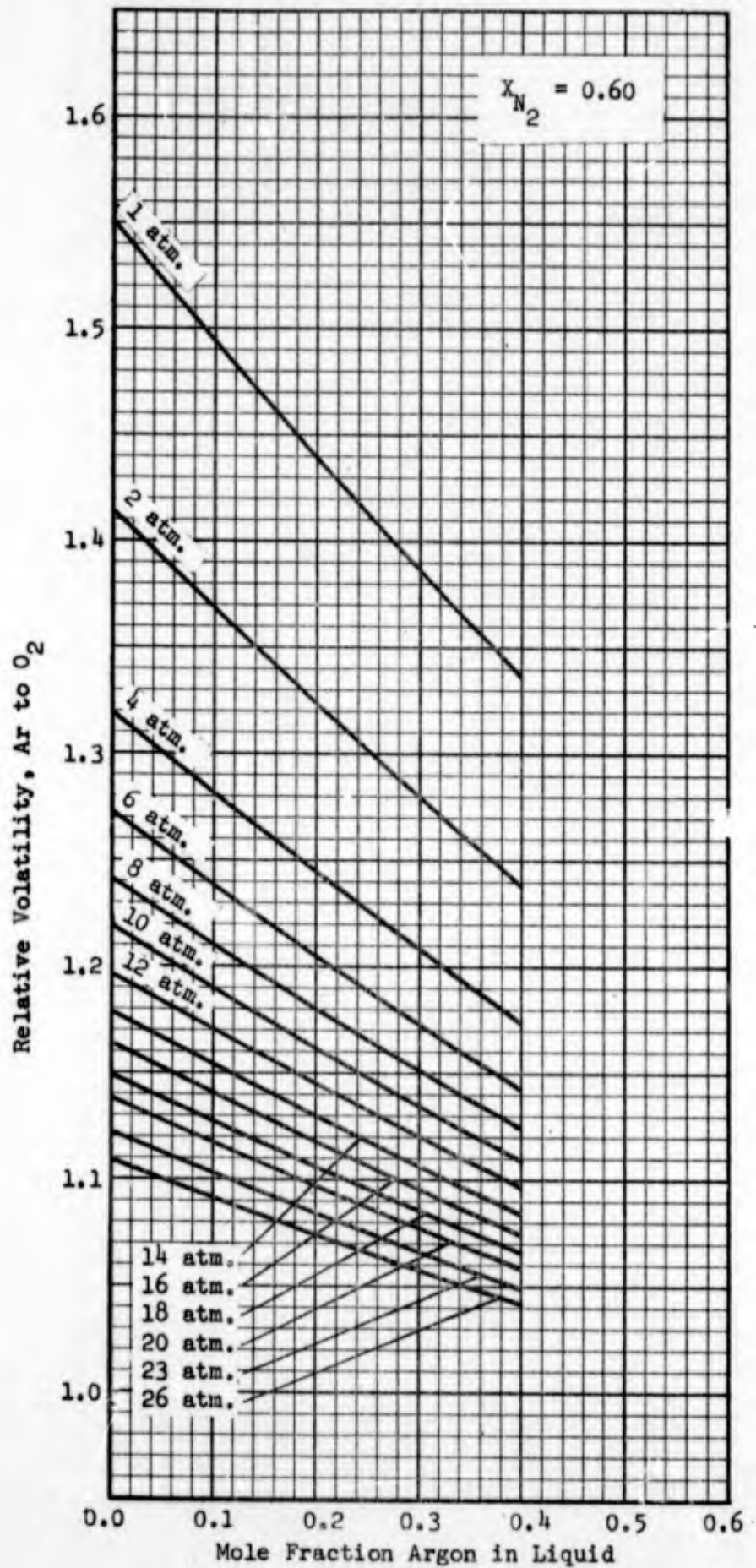


Figure 129. Relative Volatility of Argon to Oxygen.

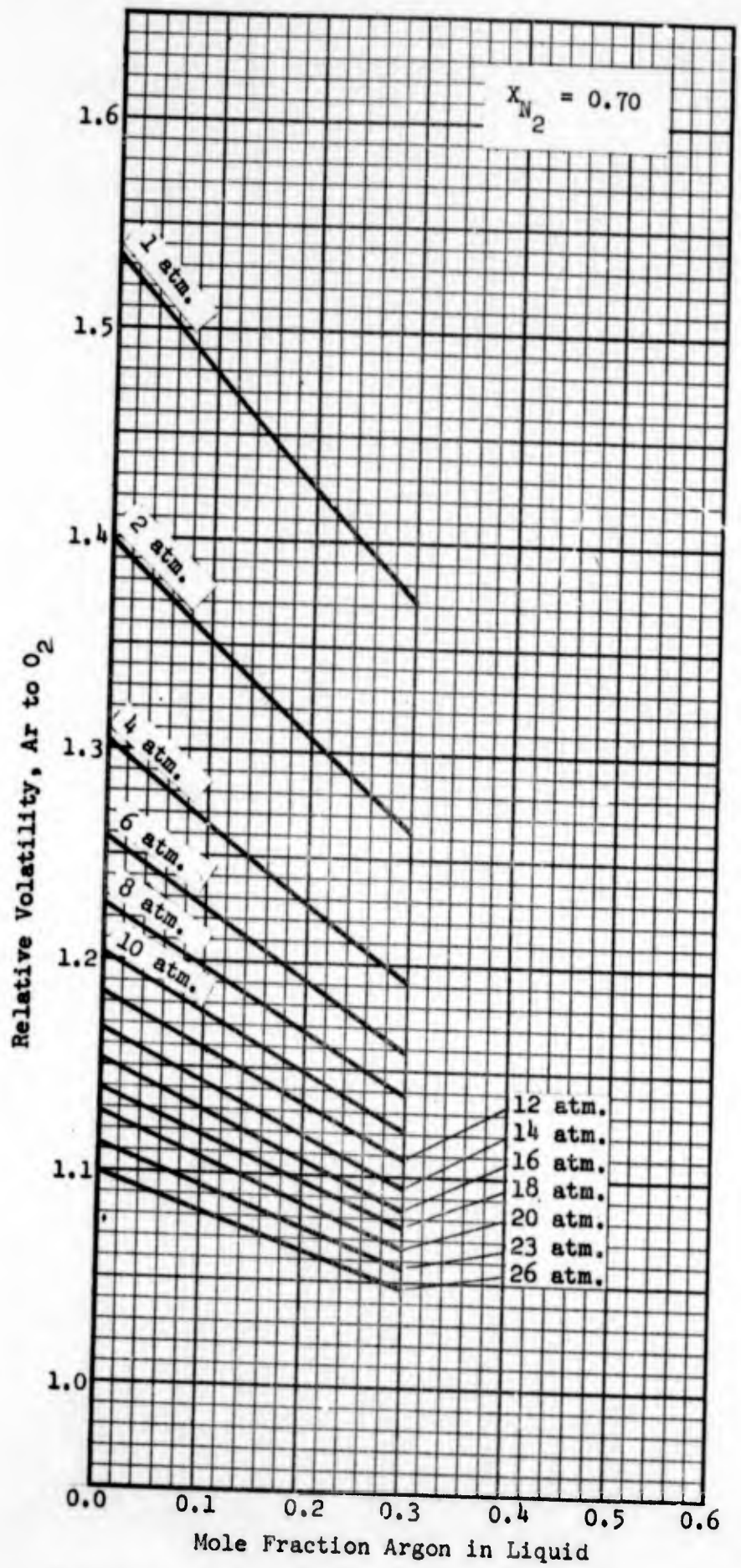


Figure 130. Relative Volatility of Argon to Oxygen.

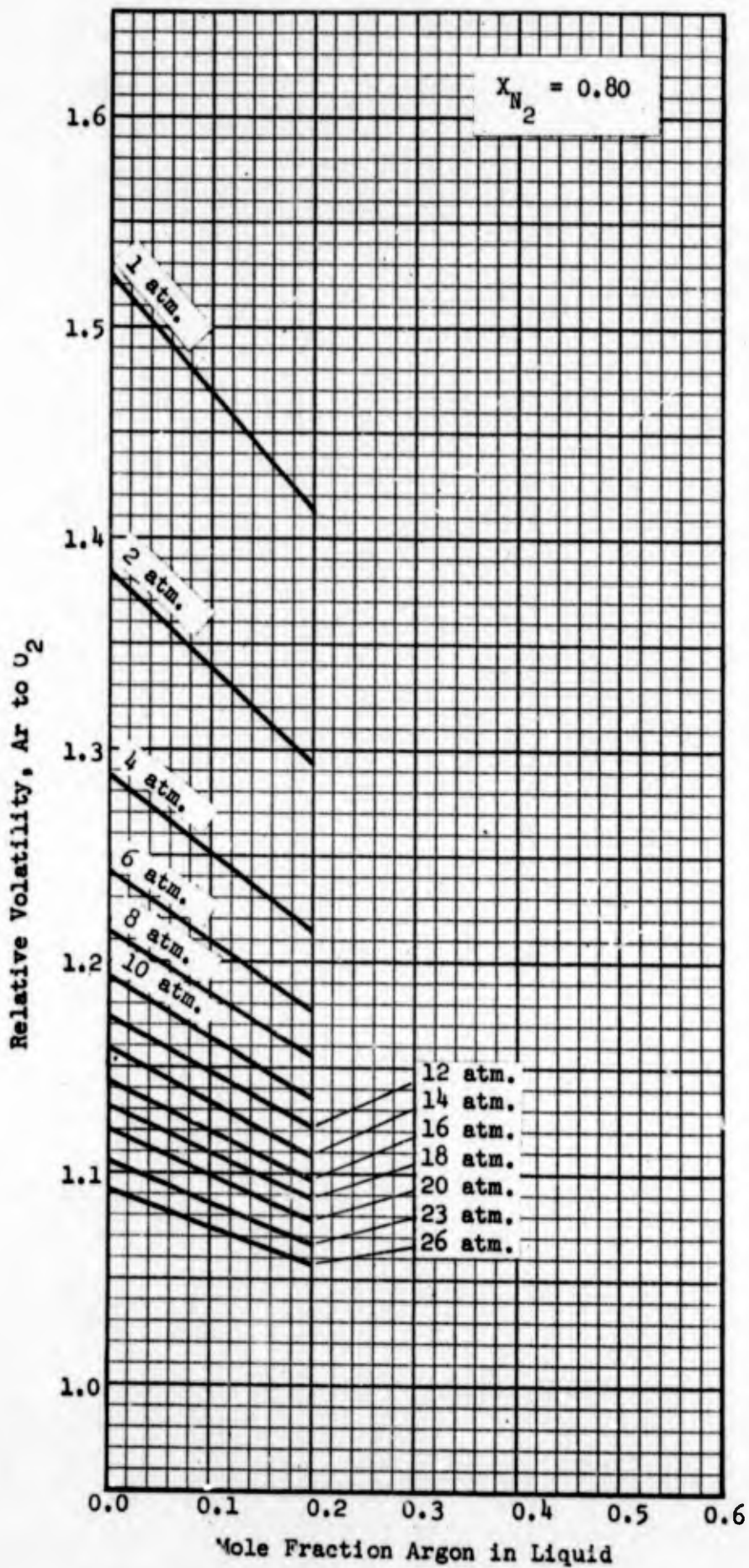


Figure 131. Relative Volatility of Argon to Oxygen.

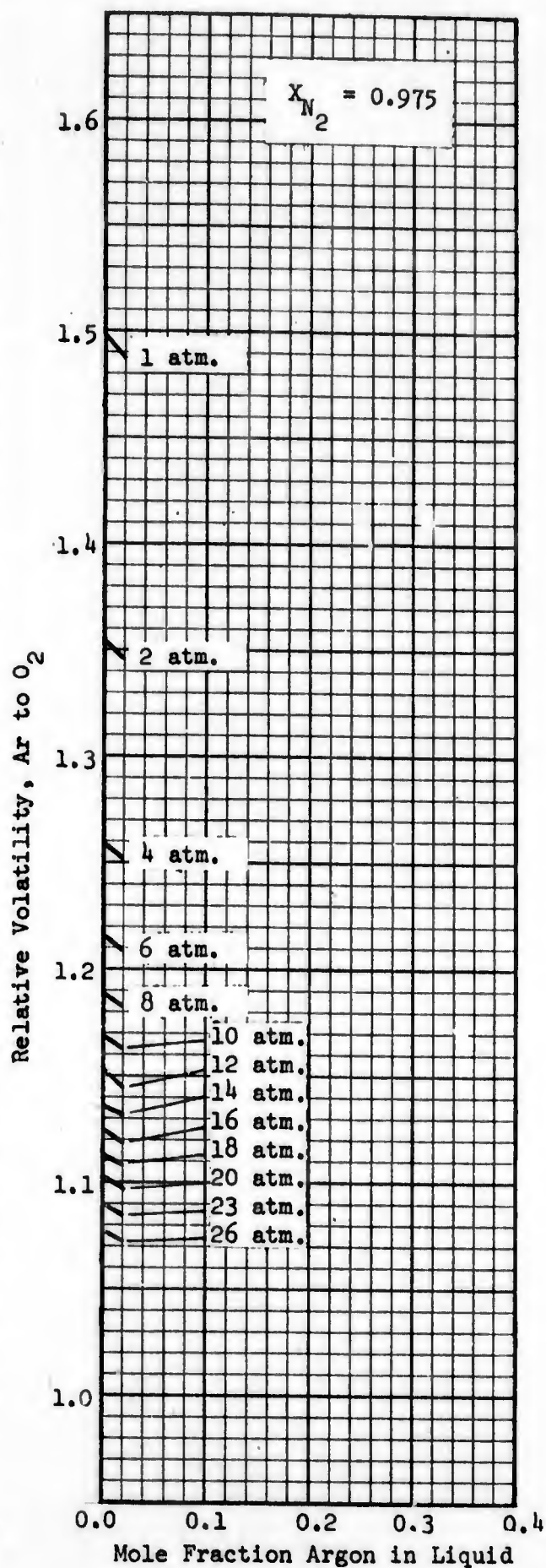
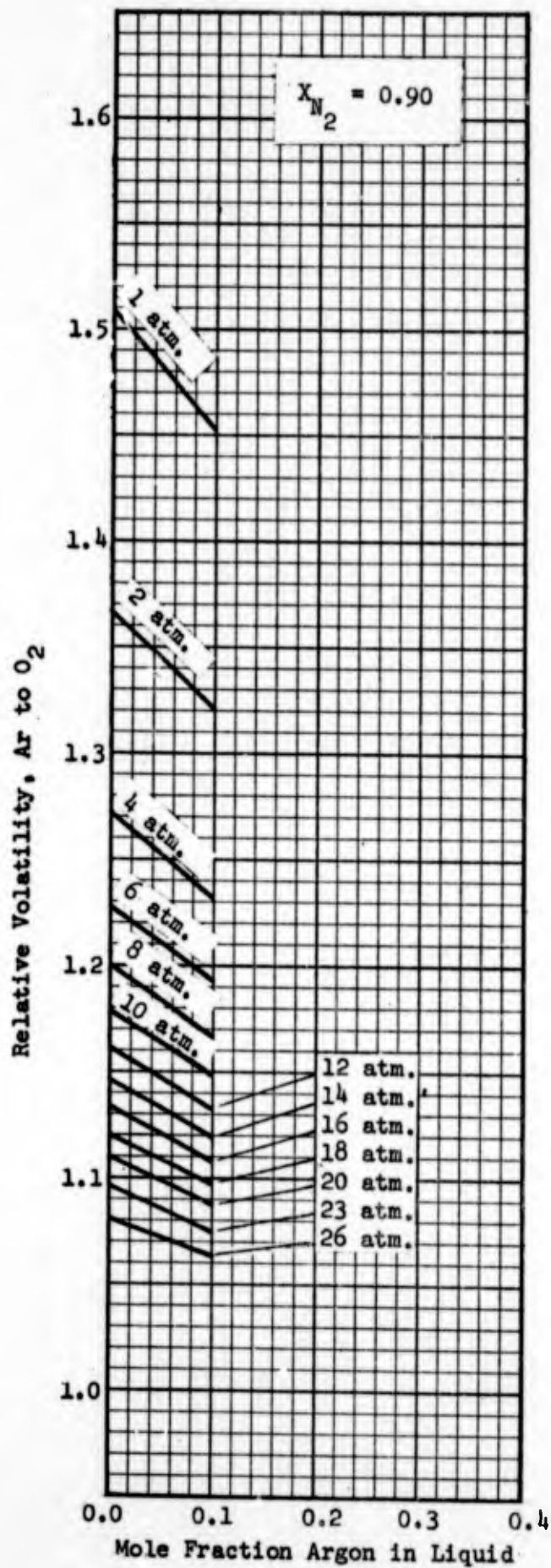


Figure 132. Relative Volatility of Argon to Oxygen.

D. Relative Volatility of Argon to Nitrogen,
Binary System

The graph to follow presents the relative volatility of argon to nitrogen in the binary system along selected isobars.

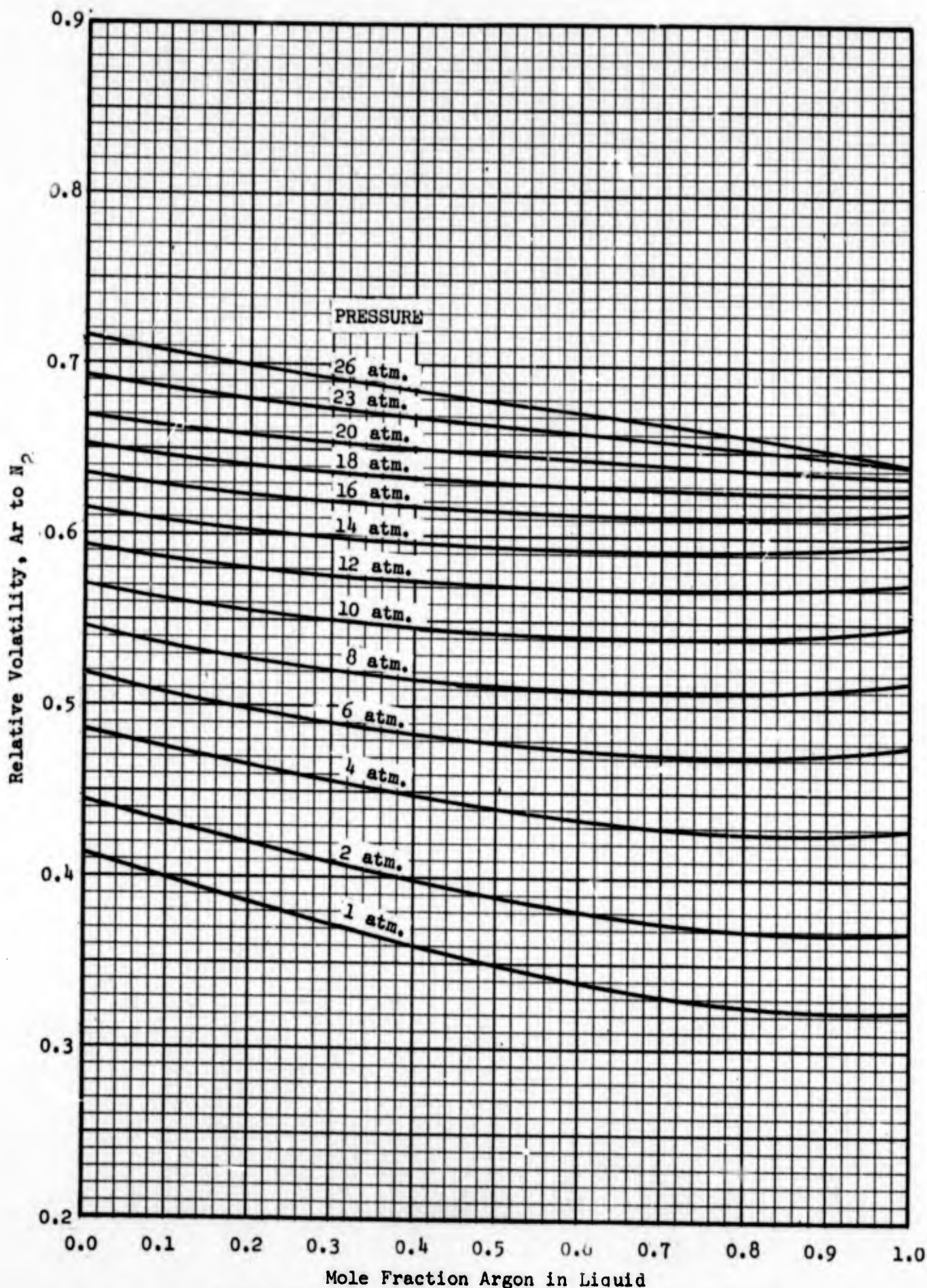


Figure 133. Relative Volatility of Argon to Nitrogen with no Oxygen present in the System.

E. Relative Volatility of Argon to Oxygen,
Binary System

The graph to follow presents the relative volatility of argon to oxygen in the binary system along selected isobars.

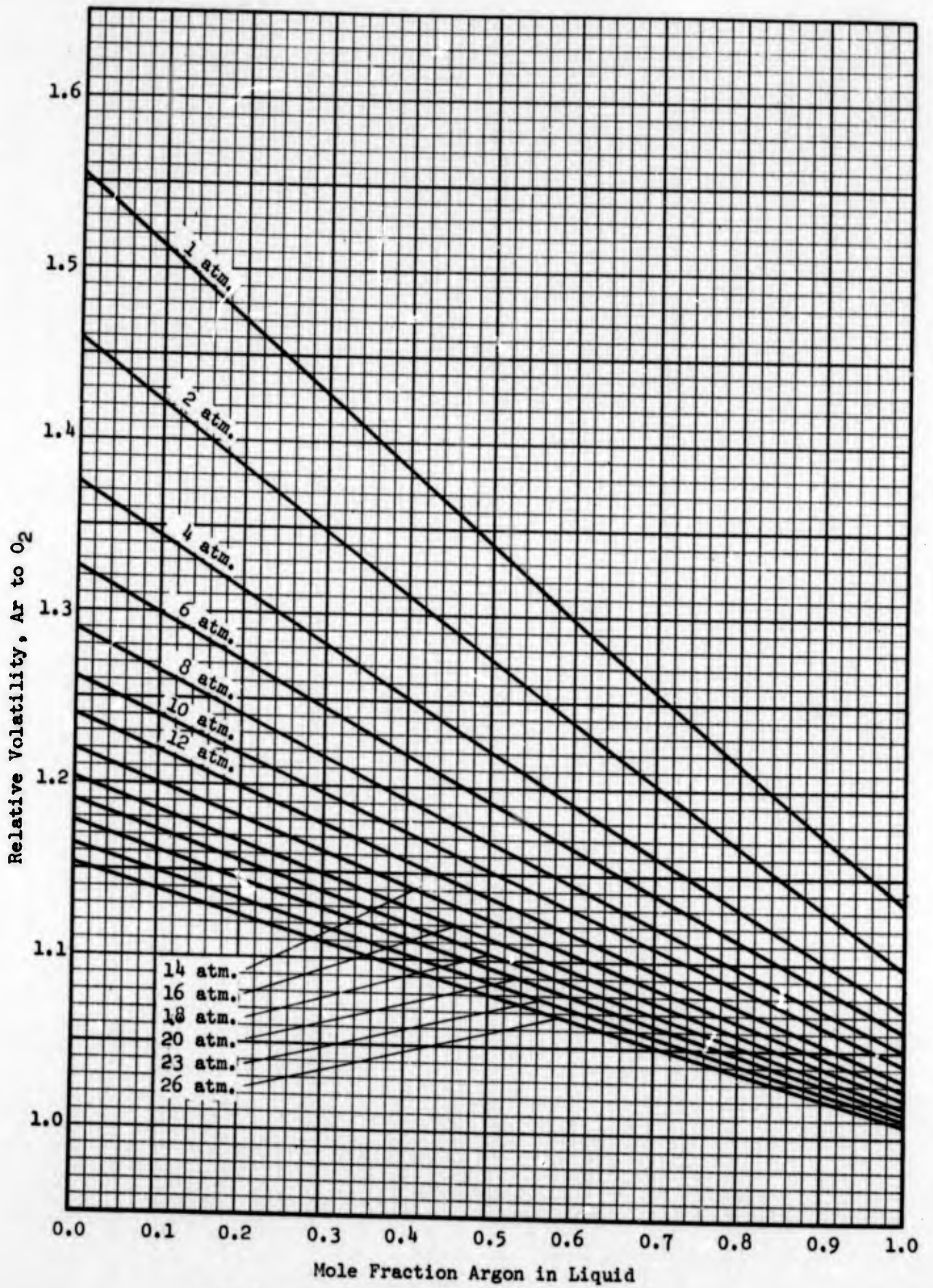


Figure 134. Relative Volatility of Argon to Oxygen with no Nitrogen present in the System.

F. Pressure Activity Coefficients

The 39 graphs to follow present the pressure activity coefficients of oxygen-argon-nitrogen as a function of composition. The pressure activity coefficient is defined as

$$\gamma_{pi} = \frac{y_i P}{x_i p^0} \quad (53)$$

This function is best understood as expressing the deviations from Raoult's Law.

The graphs are grouped in order of component: nitrogen, argon, oxygen. Inside each group they are ordered with respect to pressure.

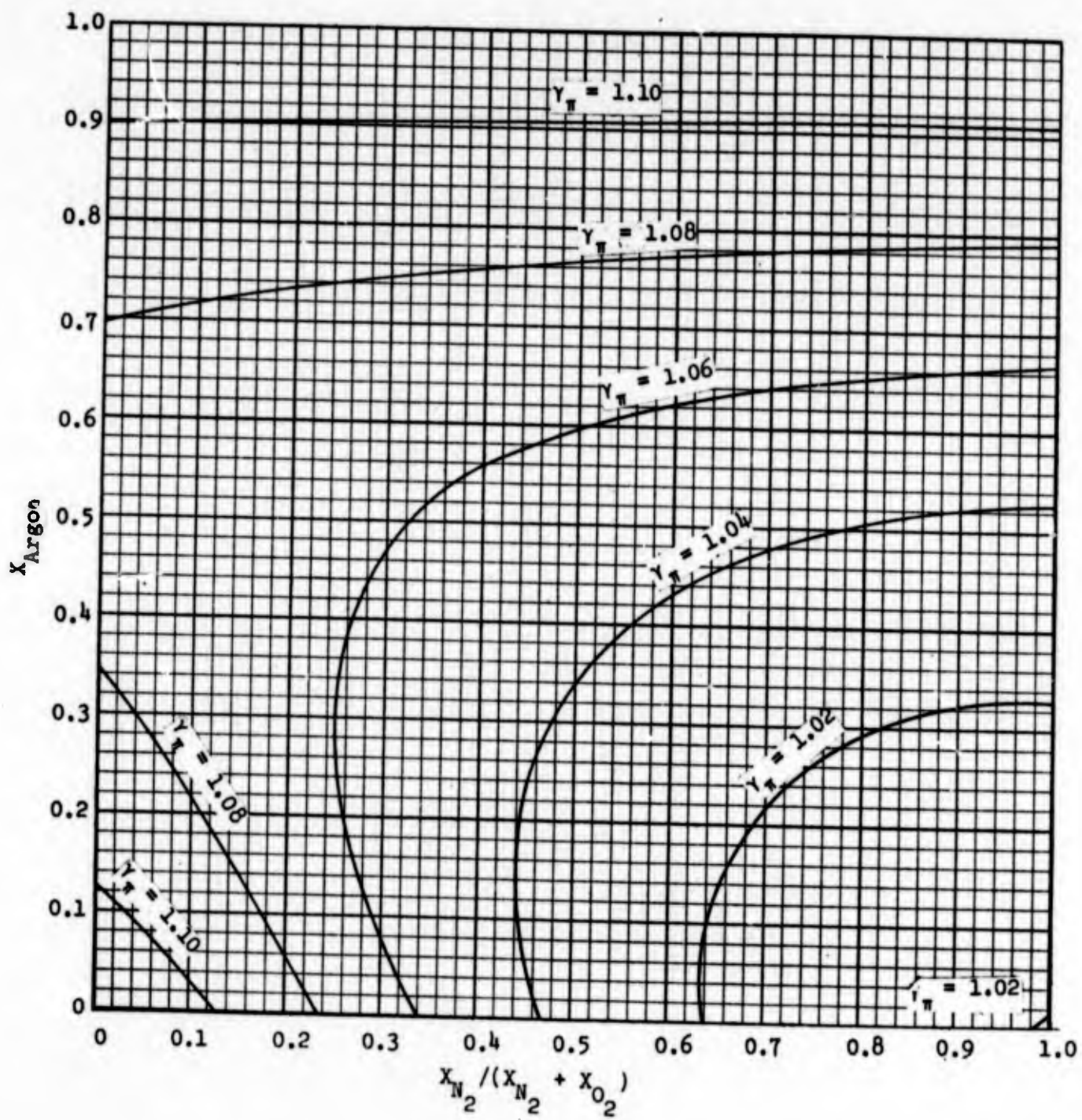


Figure 135. Nitrogen Pressure Activity Coefficients, 1 Atmosphere

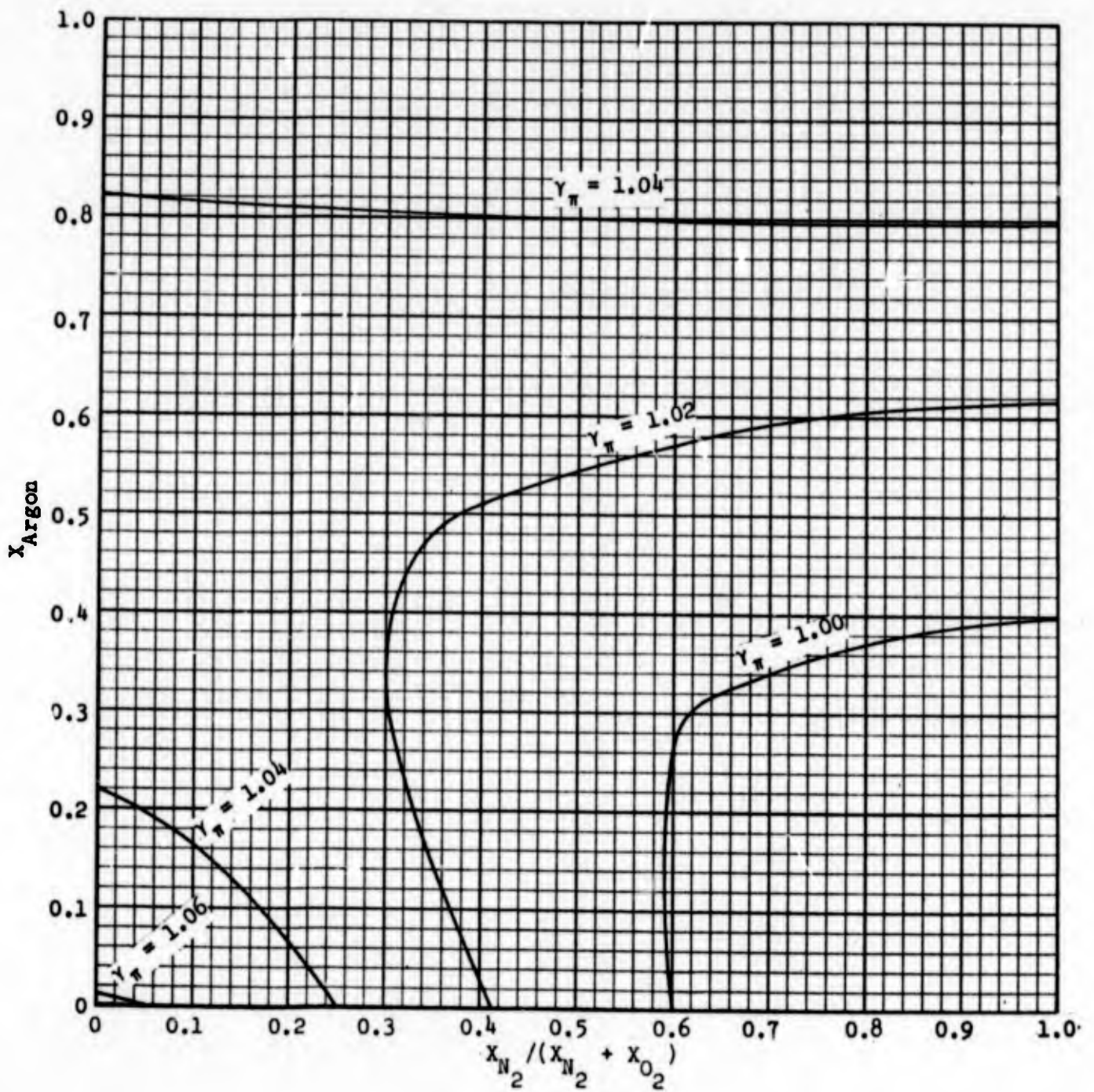


Figure 136. Nitrogen Pressure Activity Coefficients, 2 Atmospheres

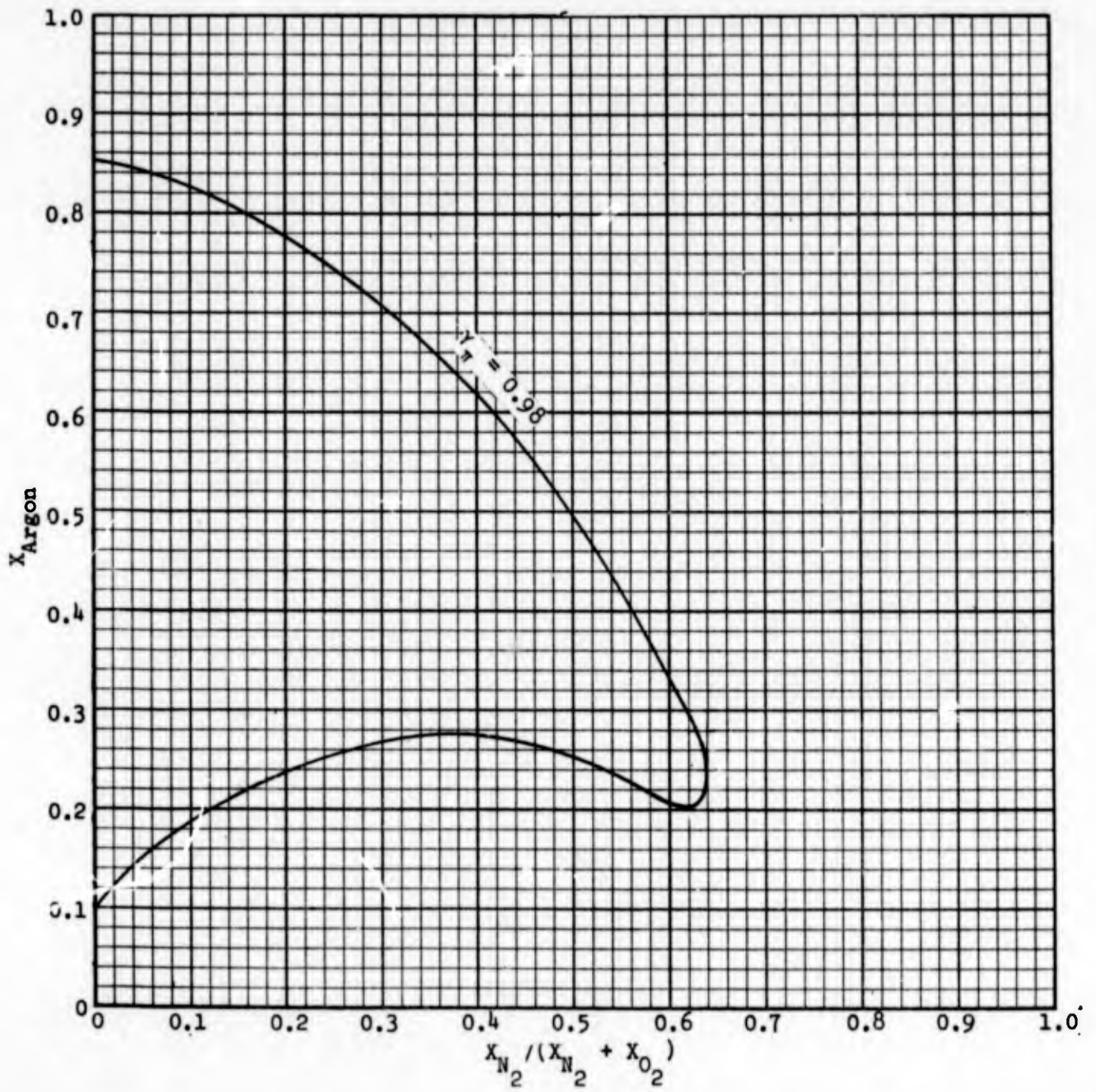


Figure 137. Nitrogen Pressure Activity Coefficients, 4 Atmospheres

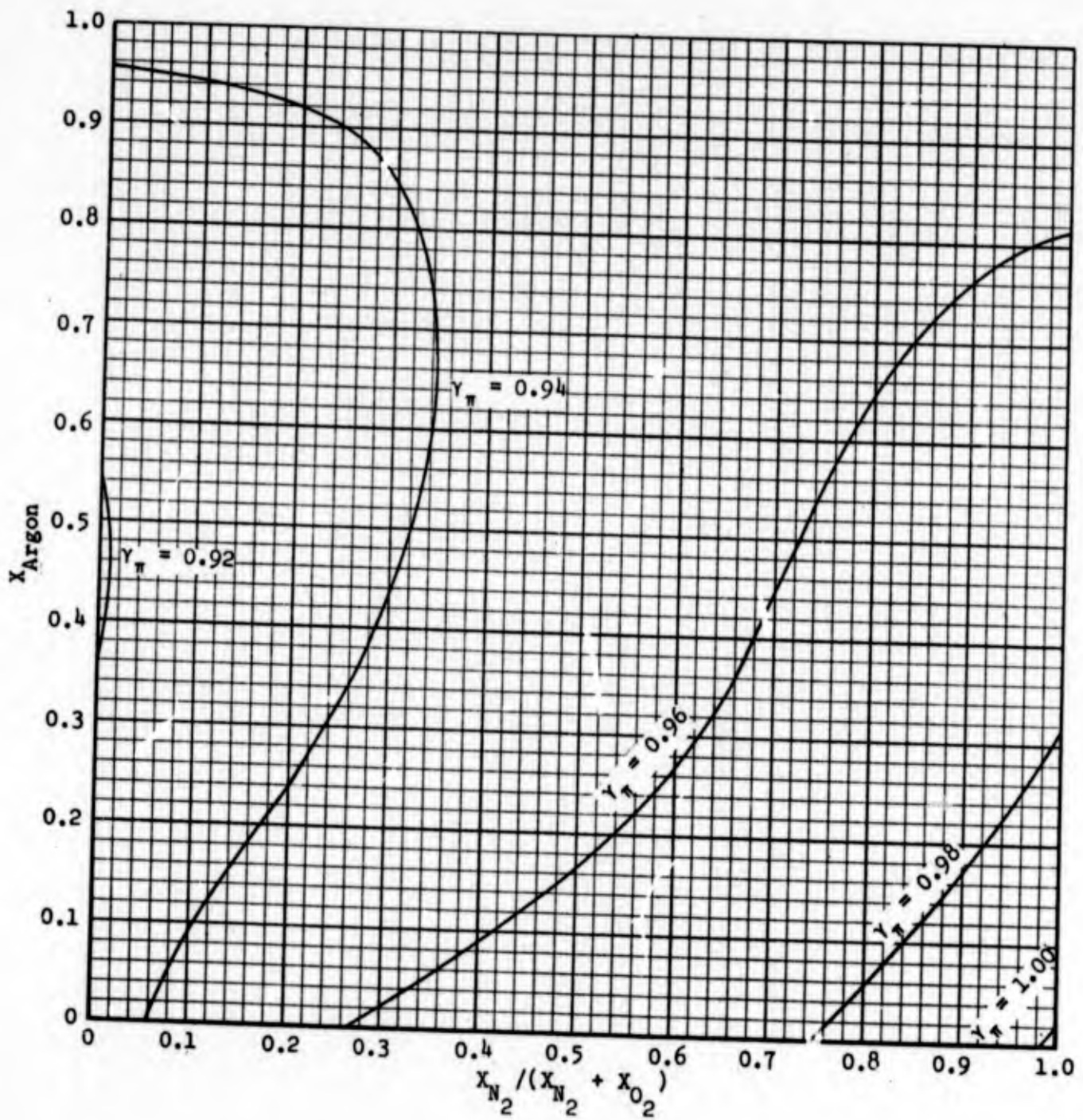


Figure 138. Nitrogen Pressure Activity Coefficients, 6 Atmospheres.

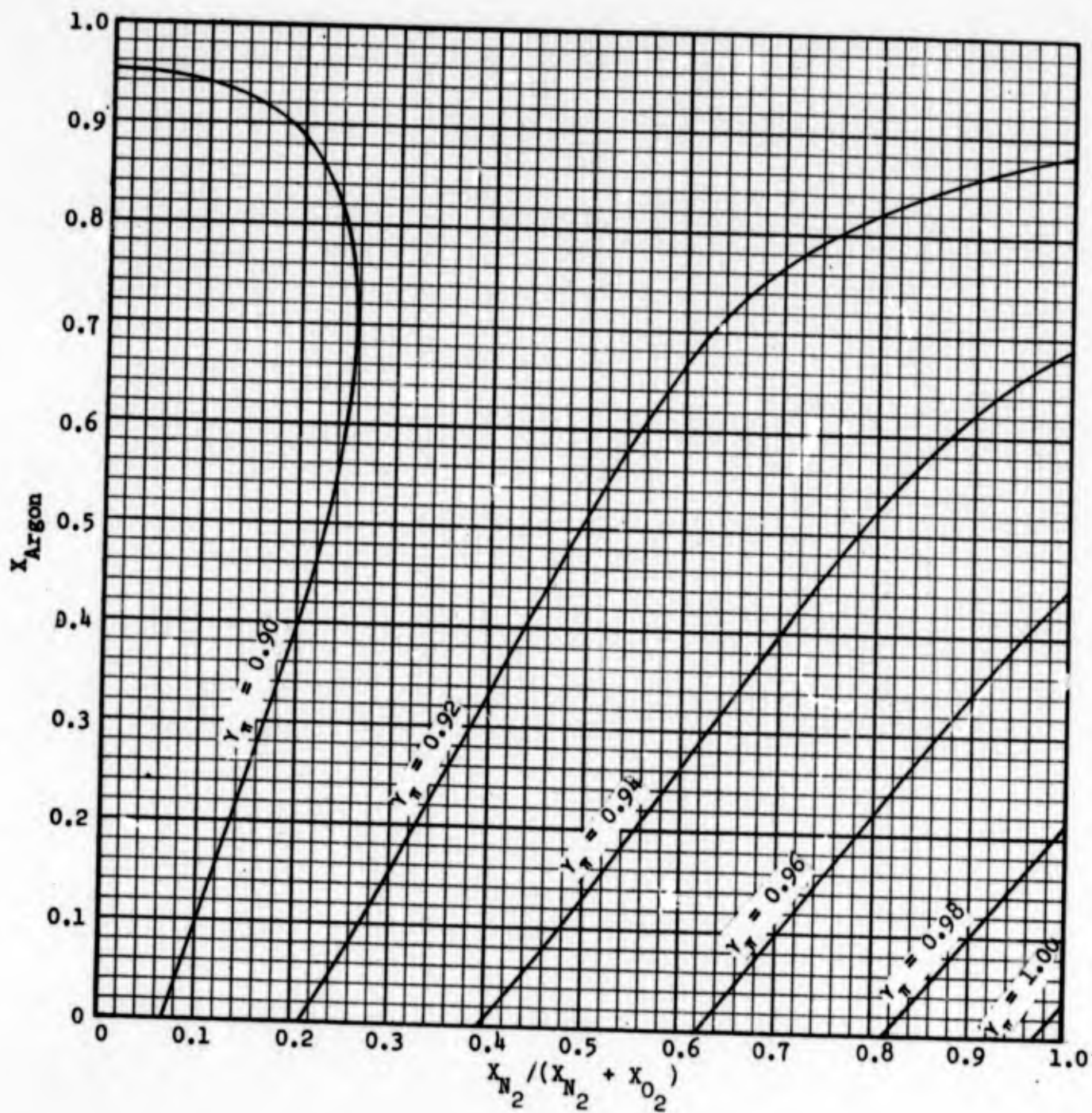


Figure 139. Nitrogen Pressure Activity Coefficients, 8 Atmospheres.

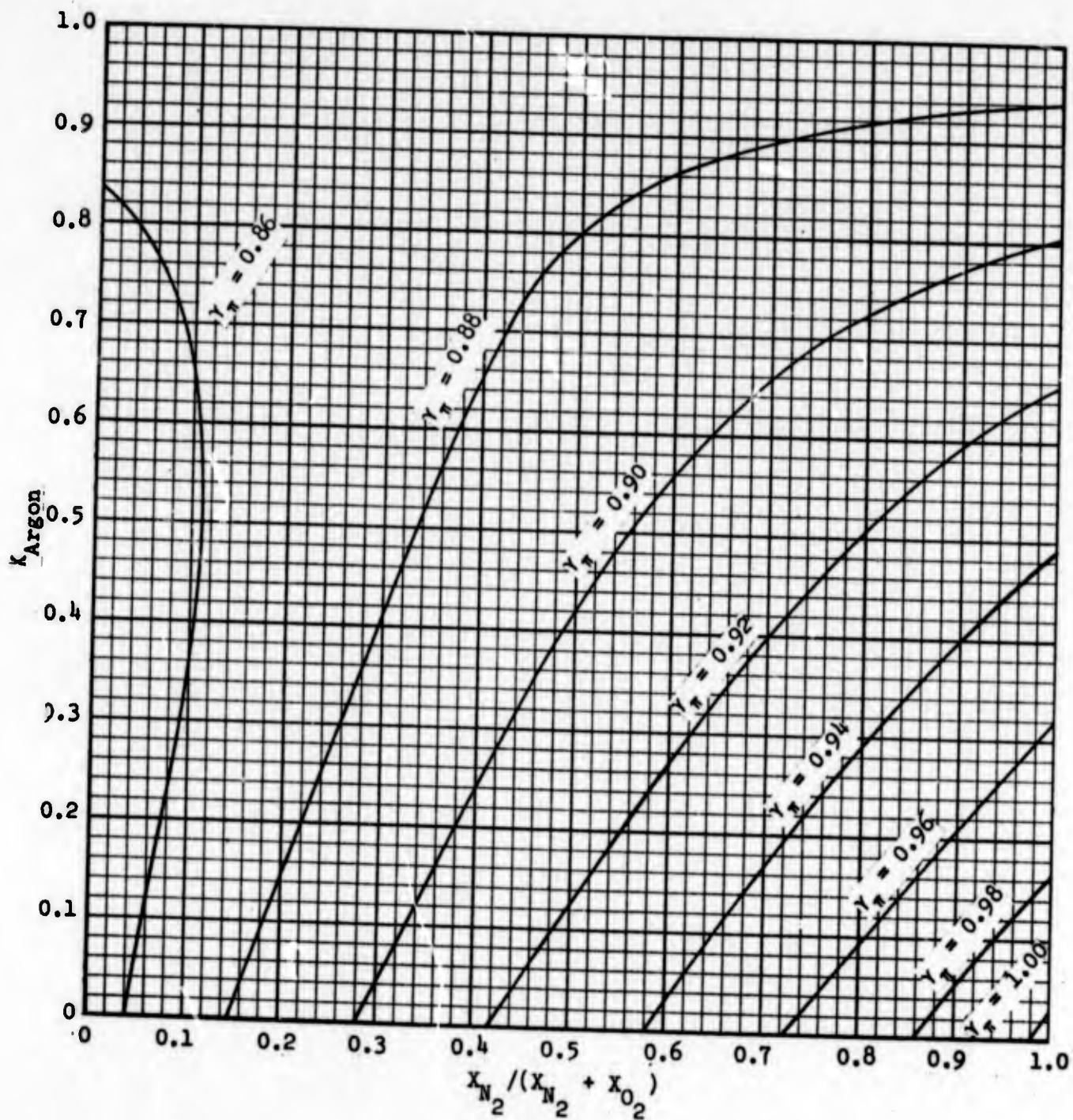


Figure 1b0. Nitrogen Pressure Activity Coefficients, 10 Atmospheres.

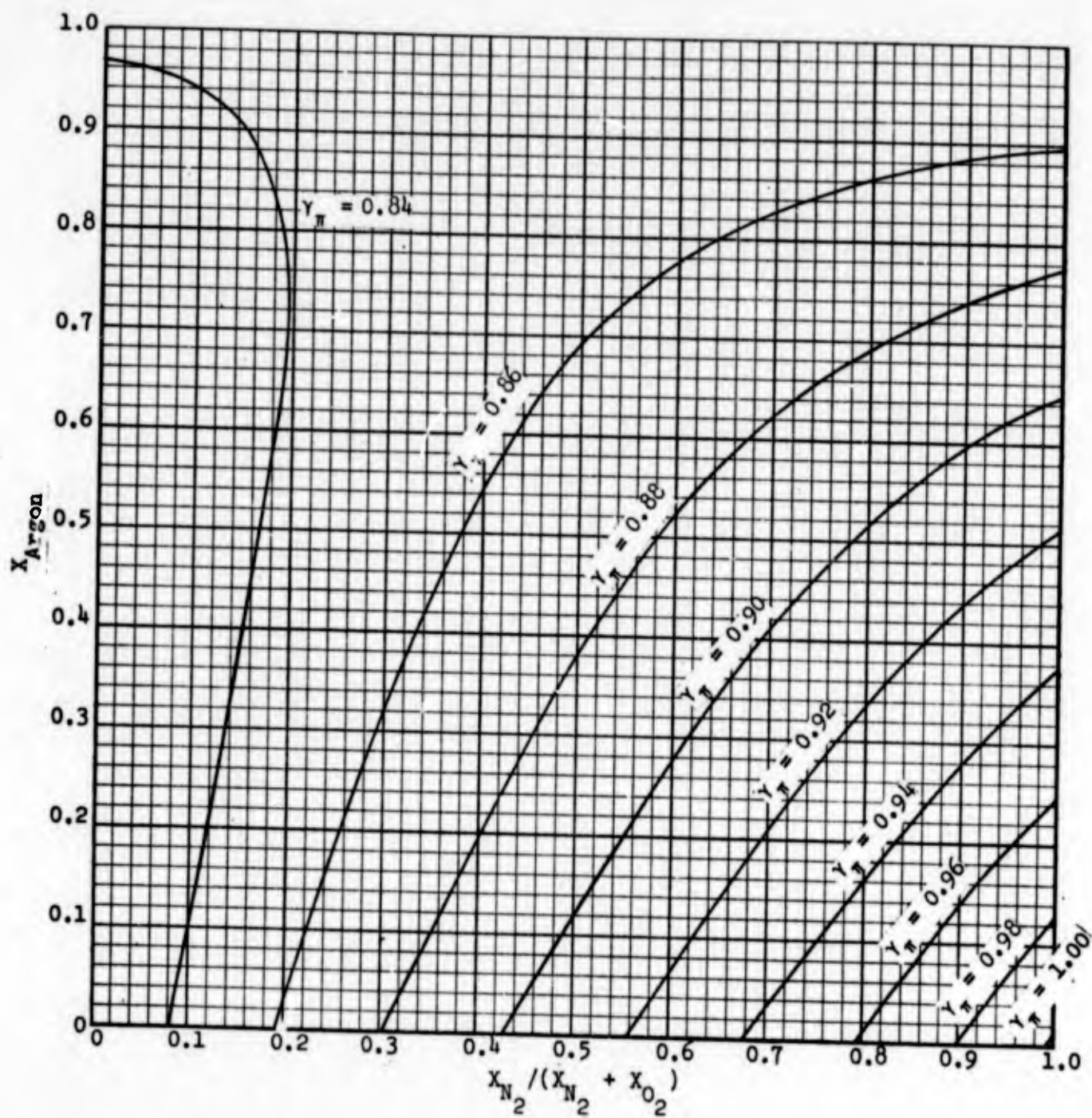


Figure 141. Nitrogen Pressure Activity Coefficients, 12 Atmospheres.

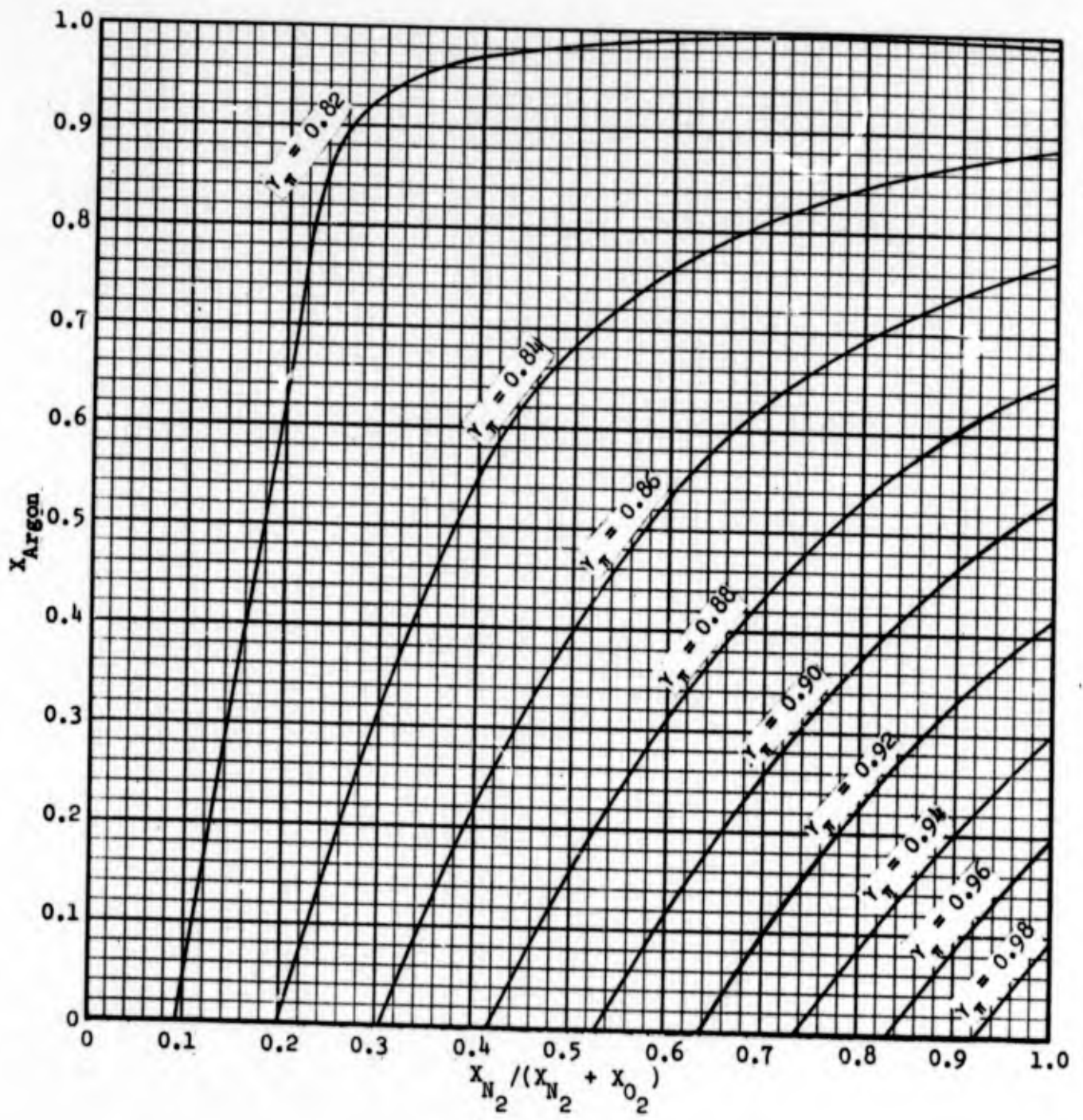


Figure 142. Nitrogen Pressure Activity Coefficients, 14 Atmospheres.

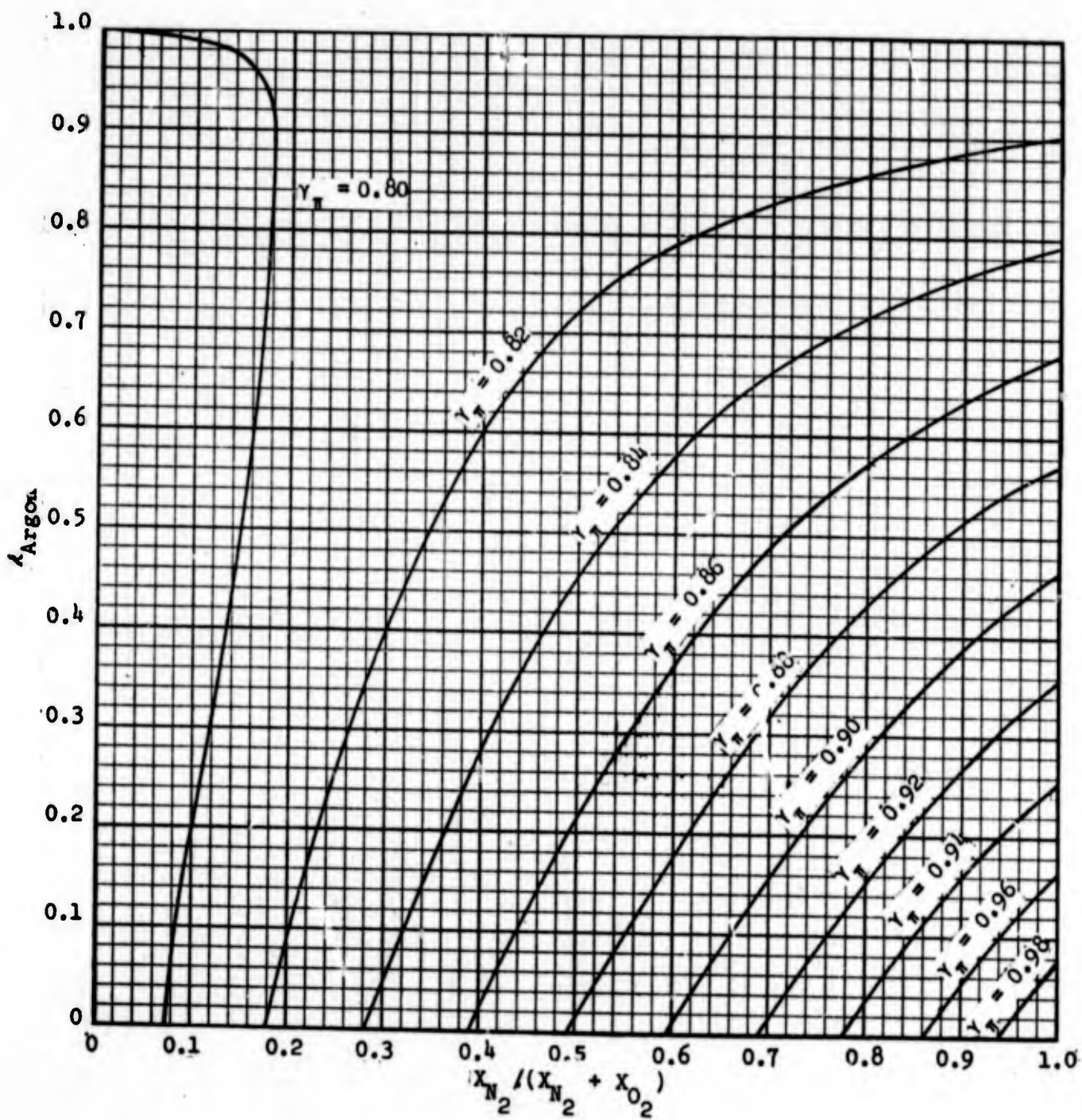


Figure 143. Nitrogen Pressure Activity Coefficients, 16 Atmospheres.

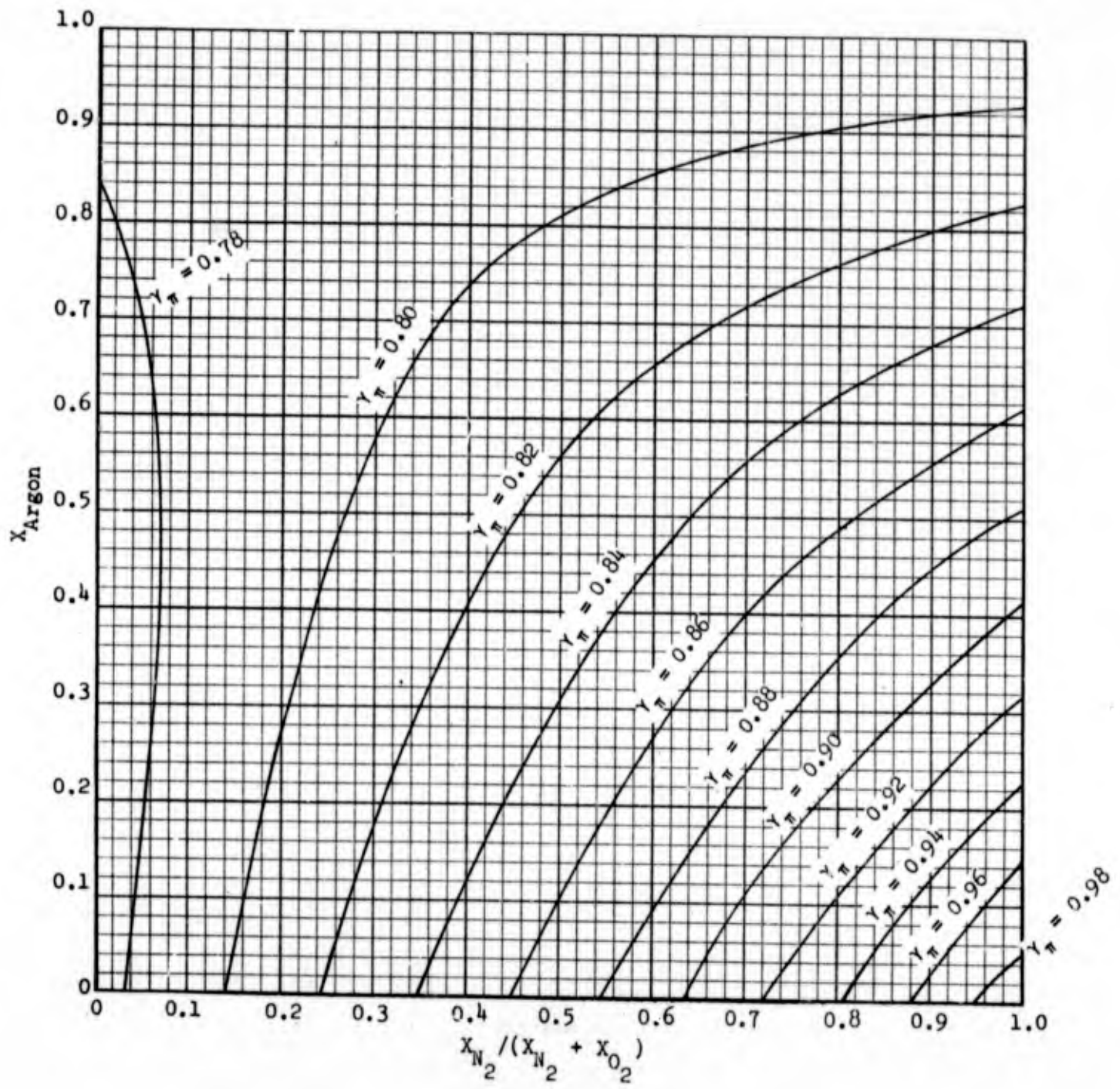


Figure 144. Nitrogen Pressure Activity Coefficients, 18 Atmospheres.

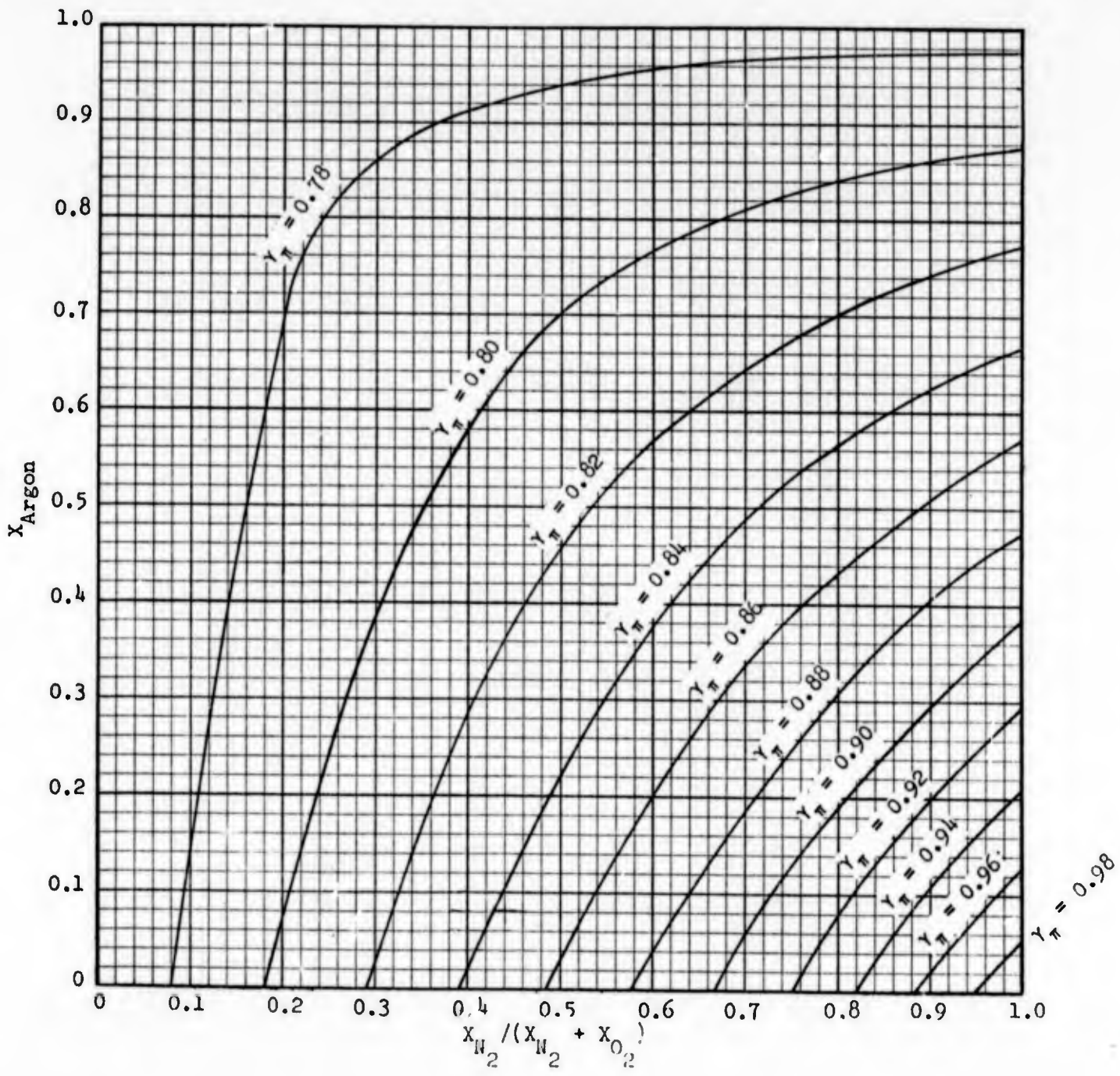


Figure 145. Nitrogen Pressure Activity Coefficients, 20 Atmospheres.

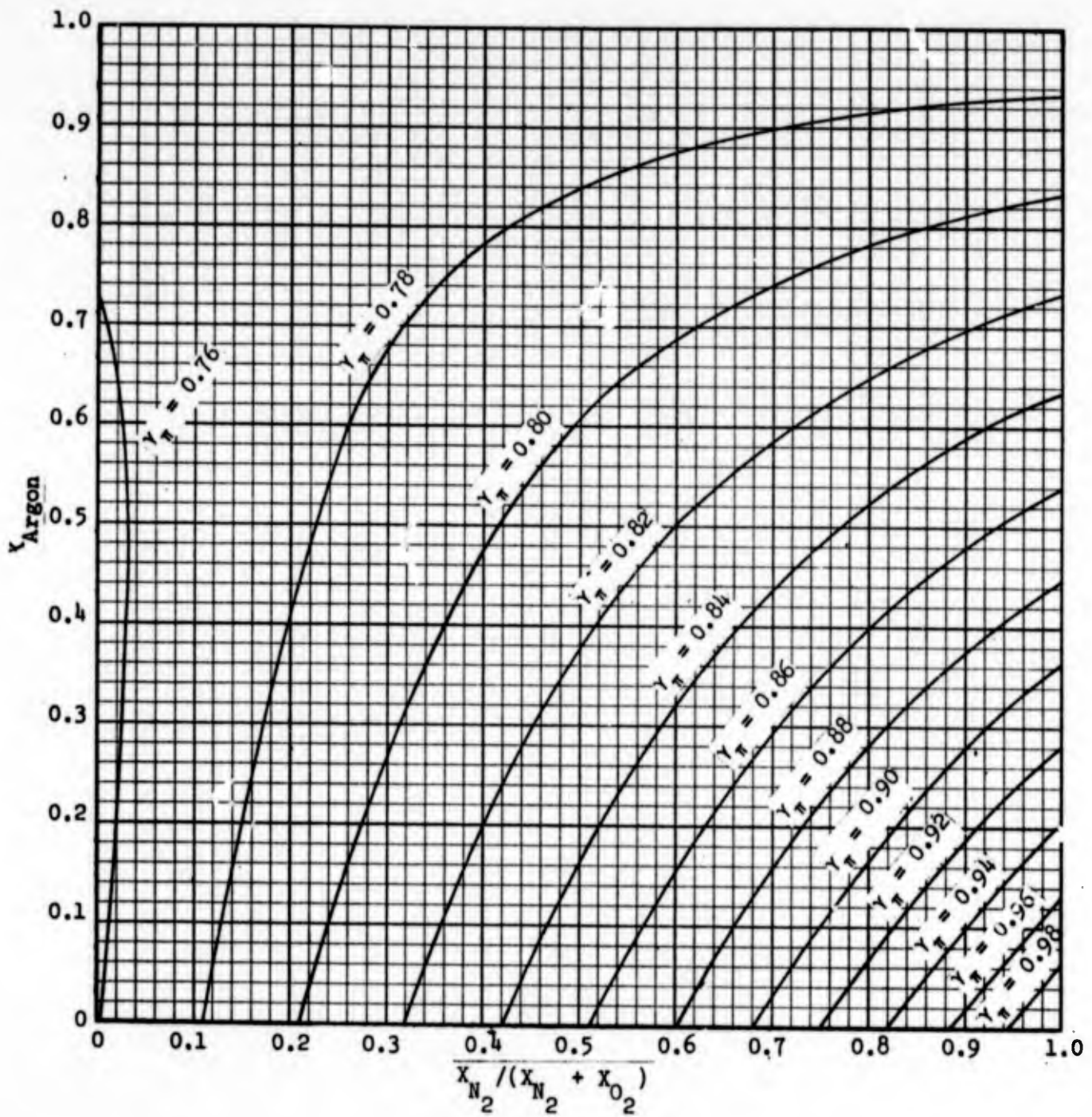


Figure 146. Nitrogen Pressure Activity Coefficients, 23 Atmospheres.

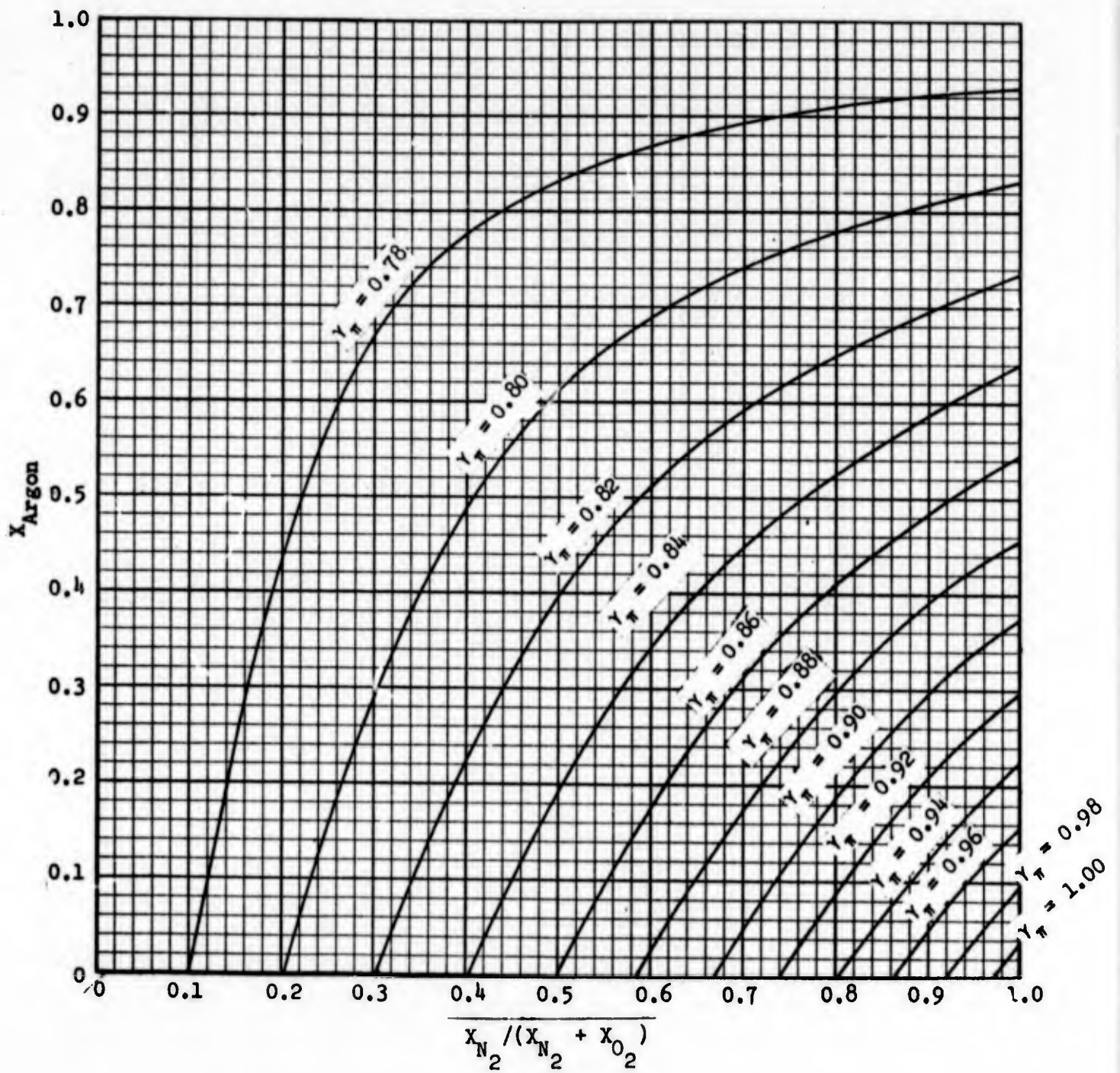


Figure 147. Nitrogen Pressure Activity Coefficients, 26 Atmospheres.

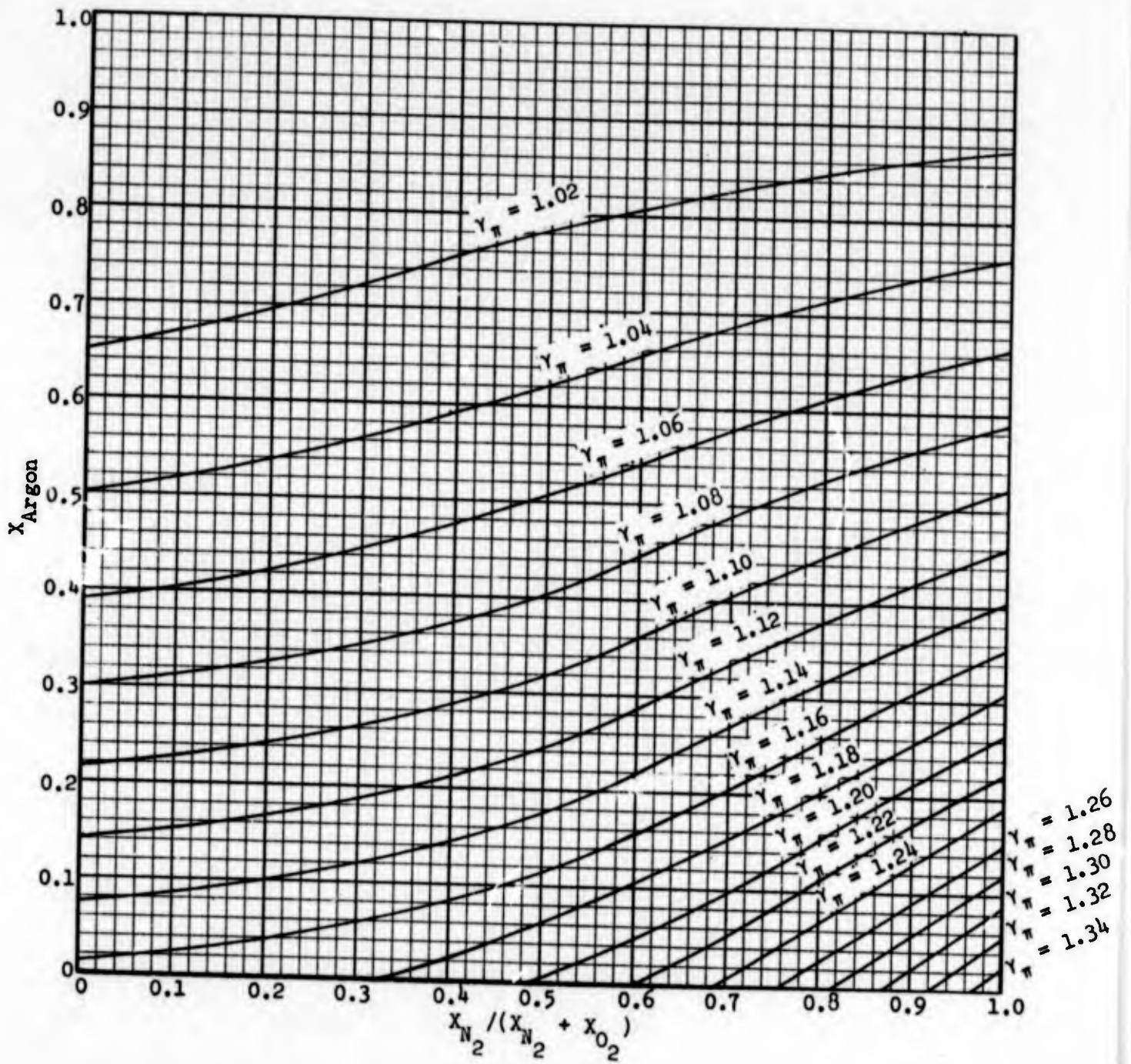


Figure 148. Argon Pressure Activity Coefficients, 1 Atmosphere.

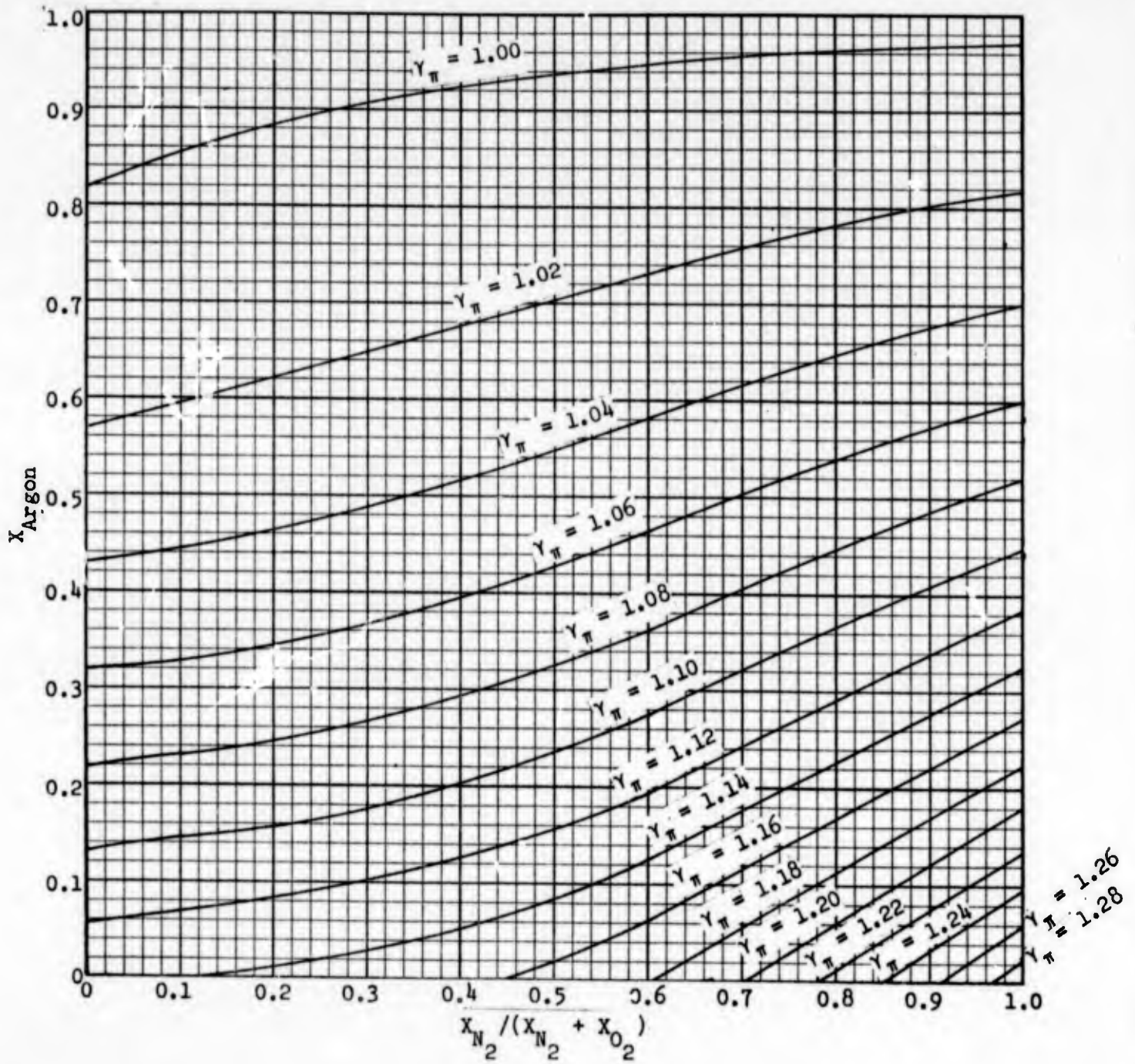


Figure 149. Argon Pressure Activity Coefficients, 2 Atmospheres.

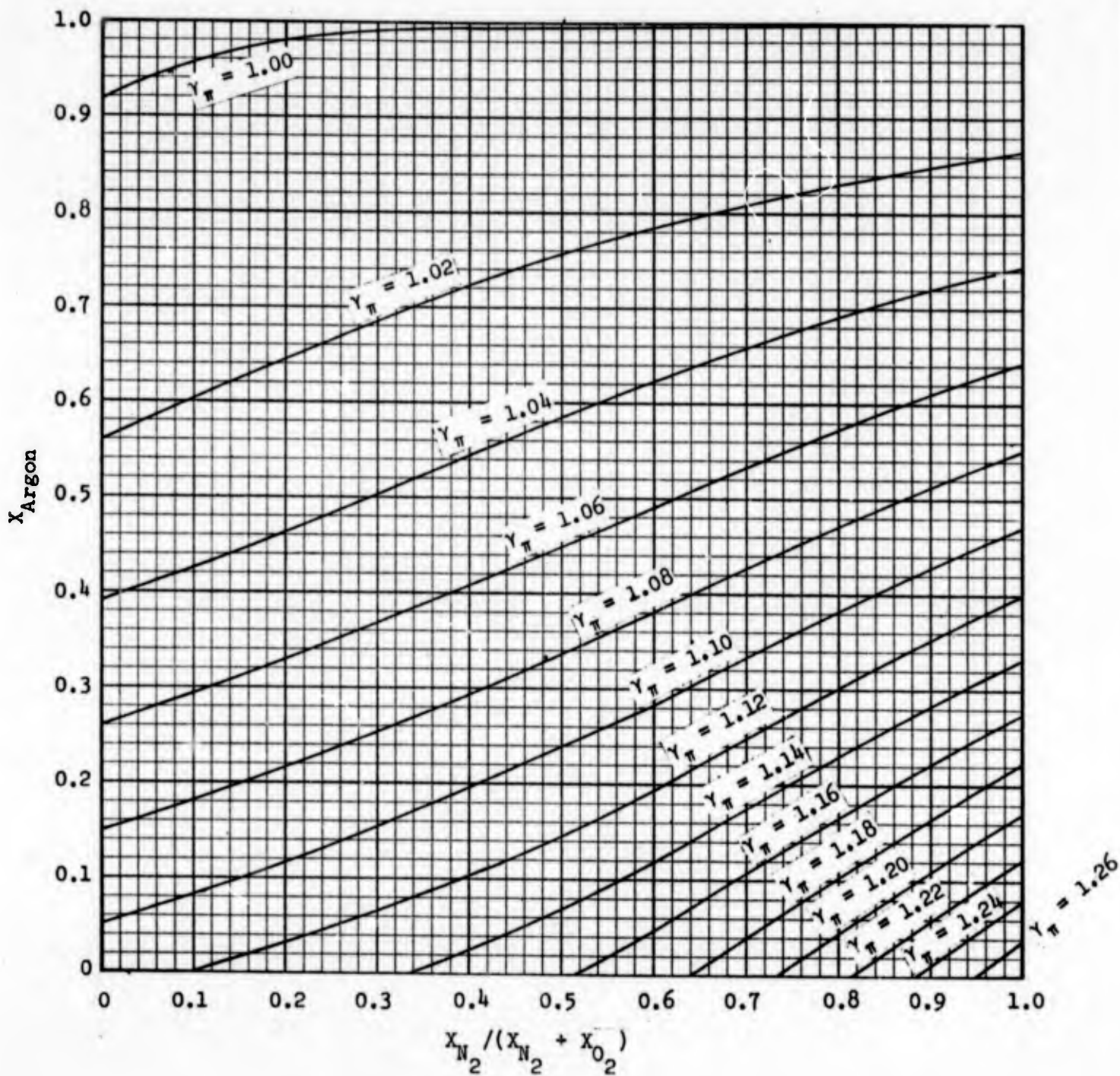


Figure 150. Argon Pressure Activity Coefficients, 4 Atmospheres.

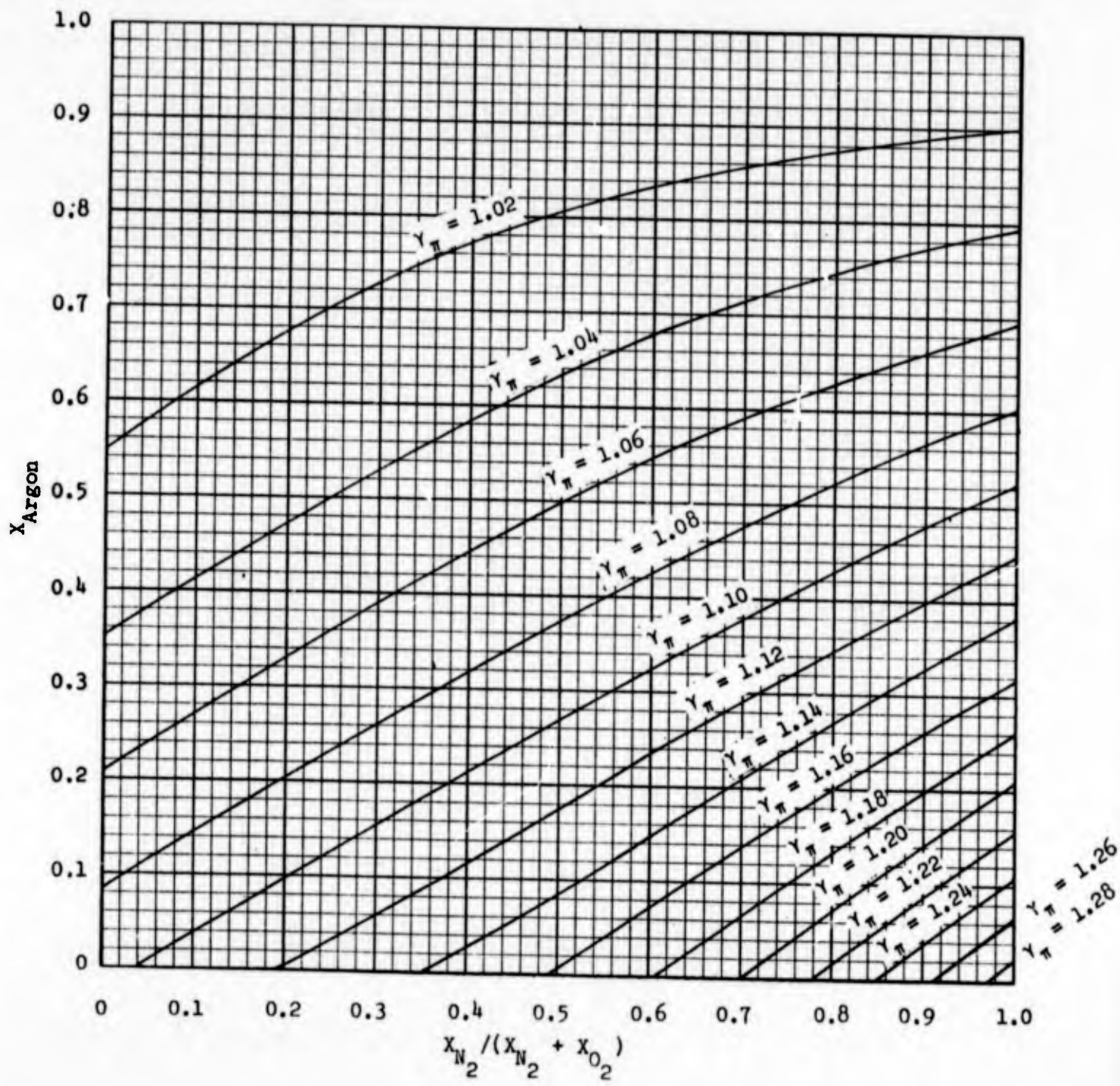


Figure 151. Argon Pressure Activity Coefficients, 6 Atmospheres.

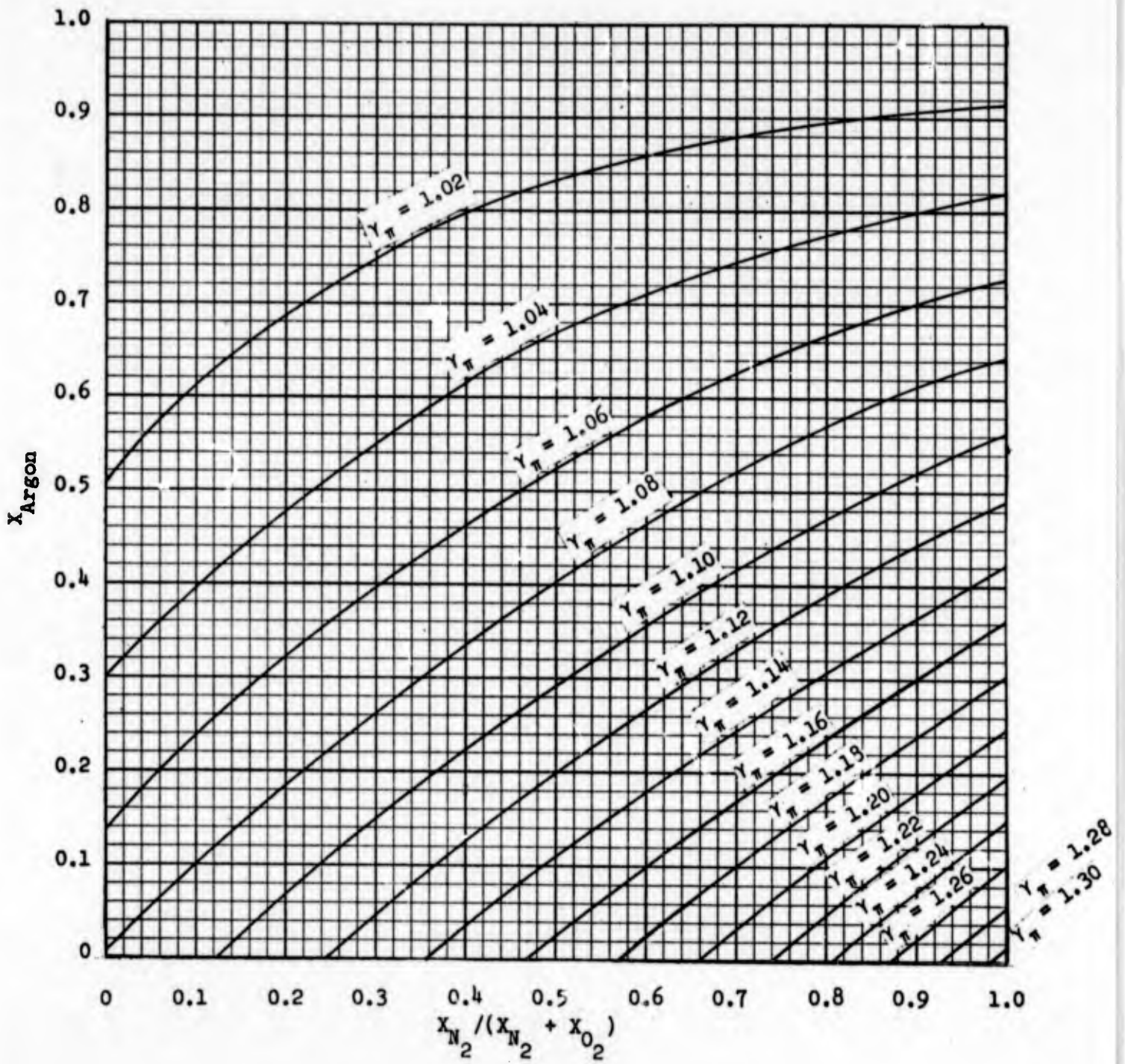


Figure 152. Argon Pressure Activity Coefficients, 8 Atmospheres.

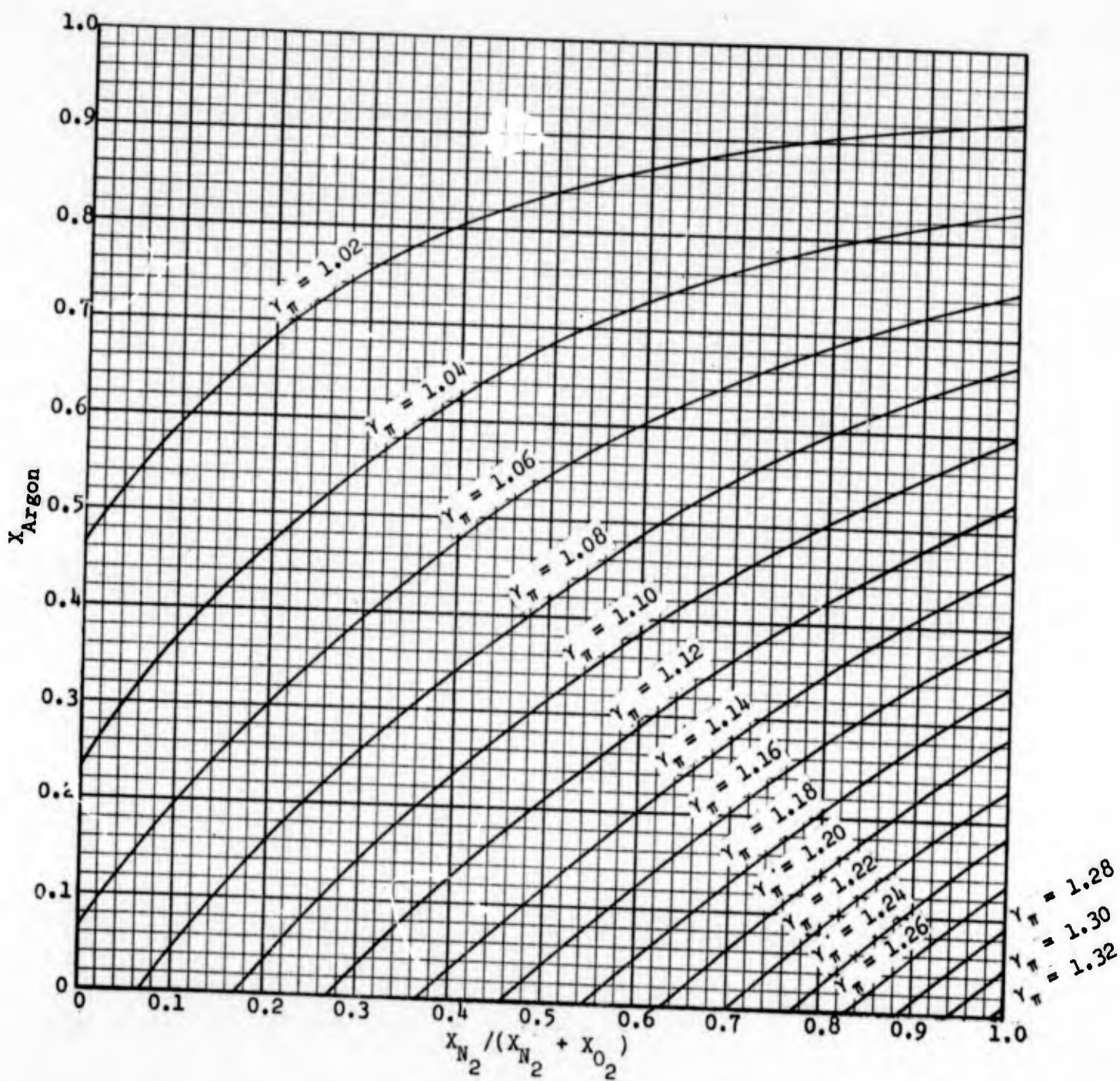


Figure 153. Argon Pressure Activity Coefficients, 10 Atmospheres.

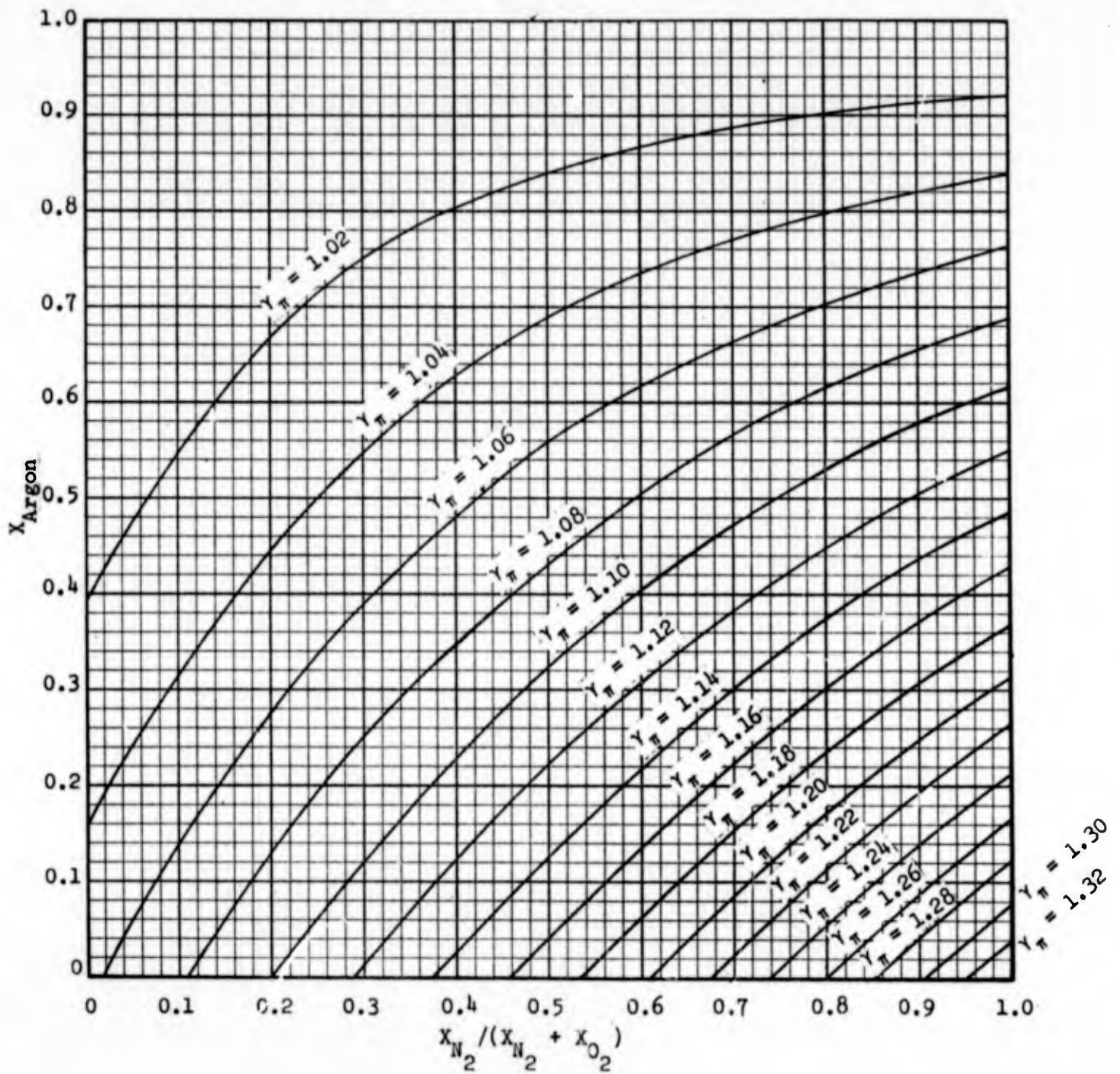


Figure 154. Argon Pressure Activity Coefficients, 12 Atmospheres.

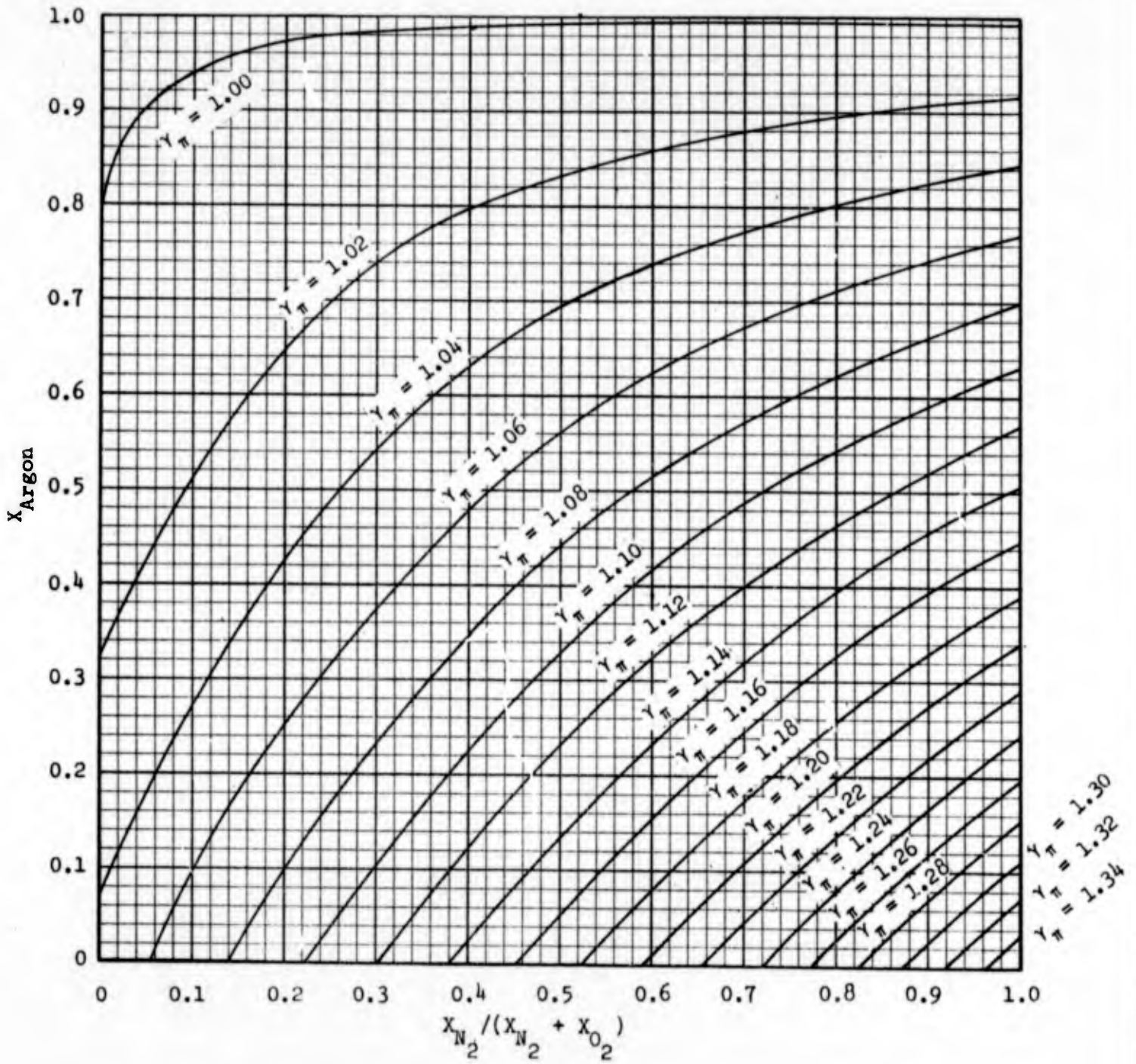


Figure 155. Argon Pressure Activity Coefficients, 14 Atmospheres.

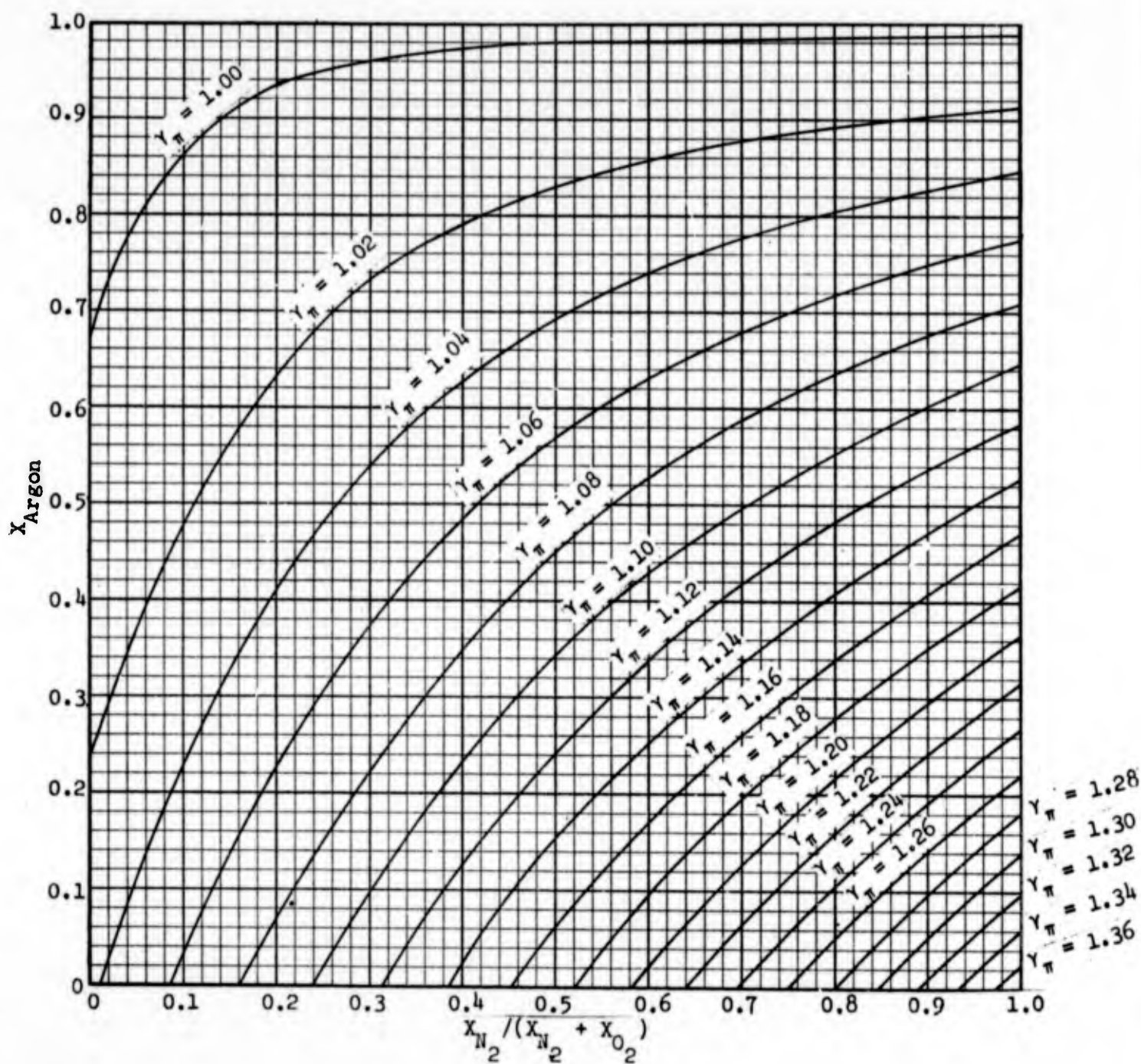


Figure 156. Argon Pressure Activity Coefficients, 16 Atmospheres.

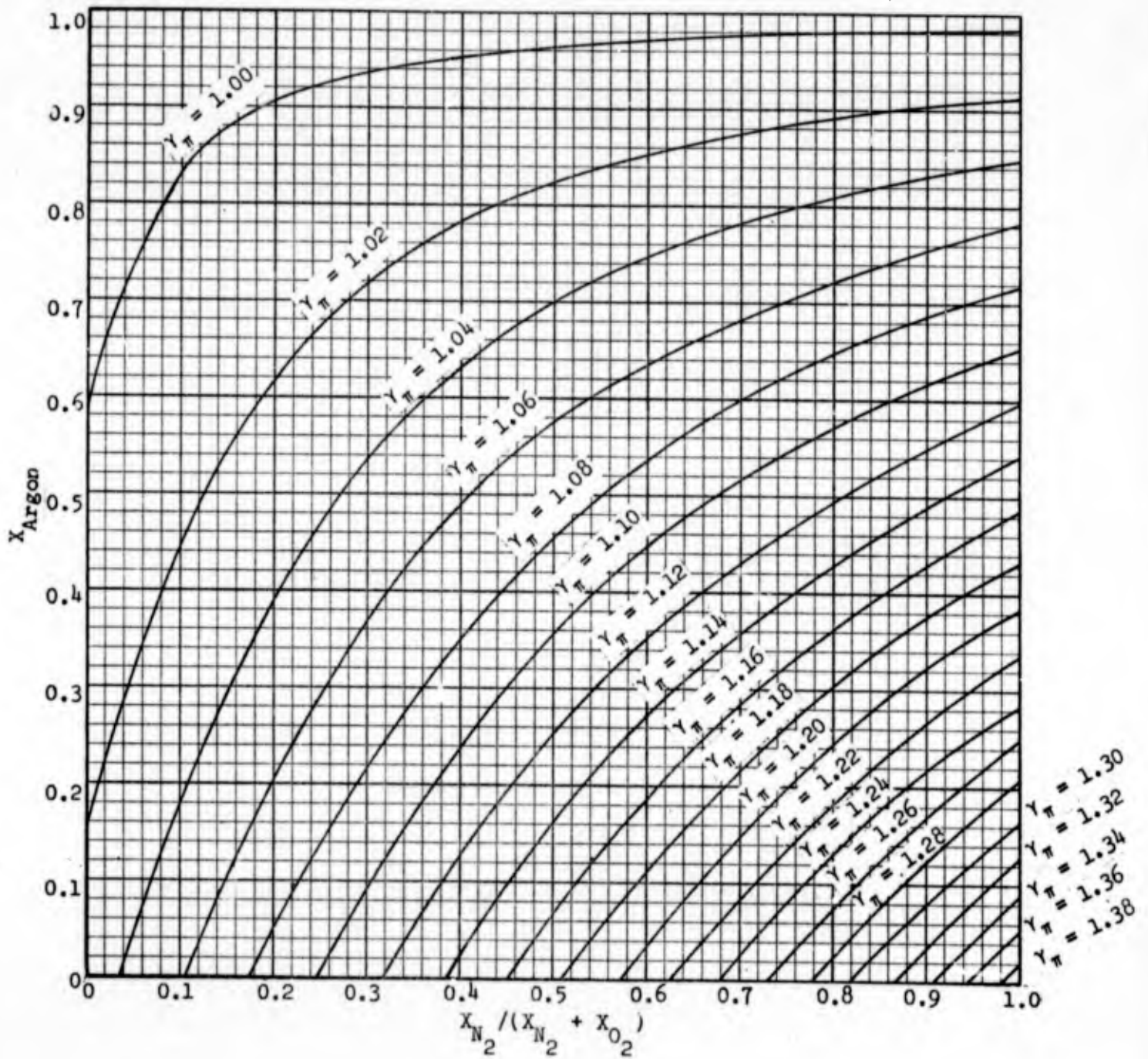


Figure 157. Argon Pressure Activity Coefficients, 18 Atmospheres.

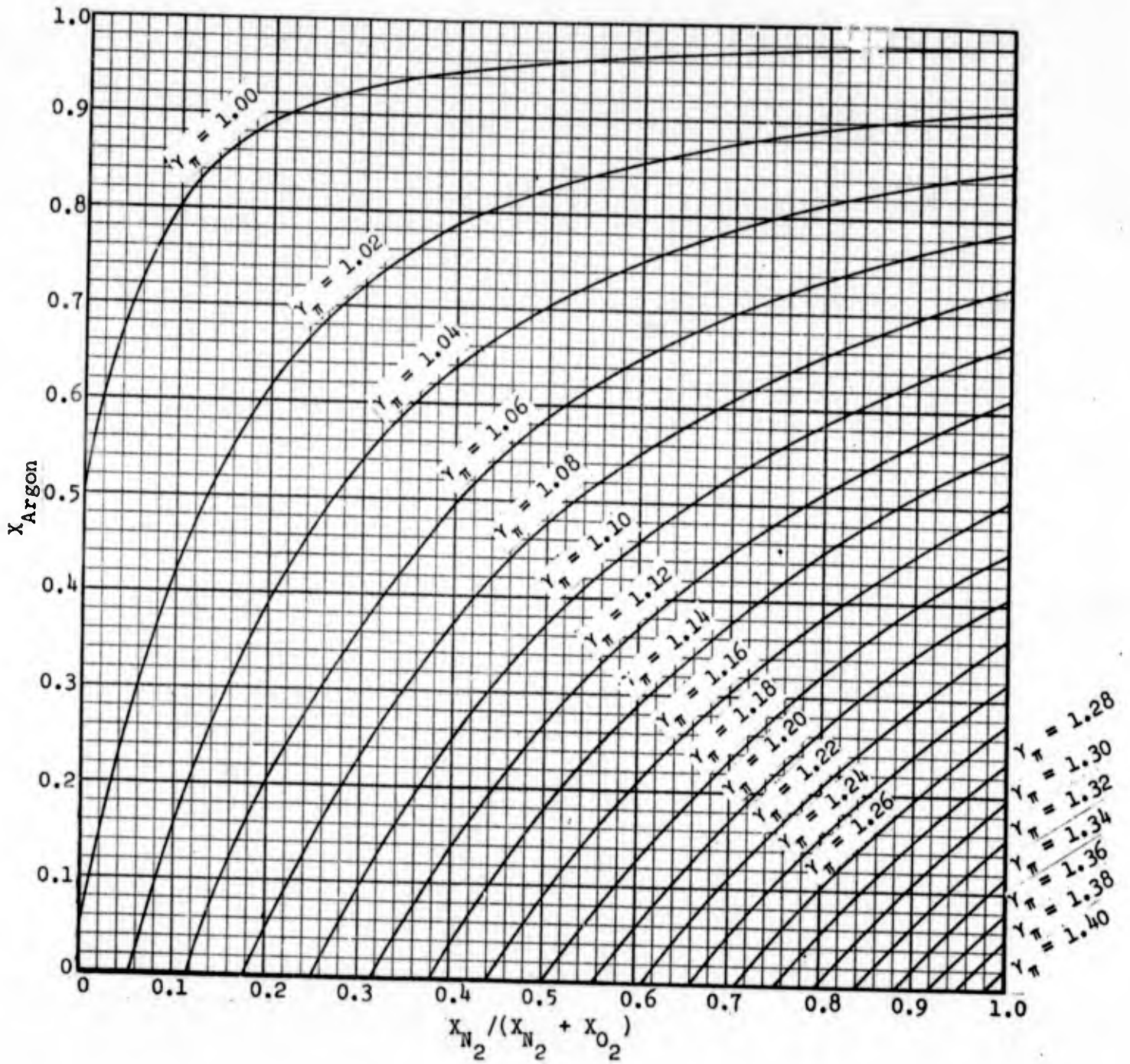


Figure 158. Argon Pressure Activity Coefficients, 20 Atmospheres.

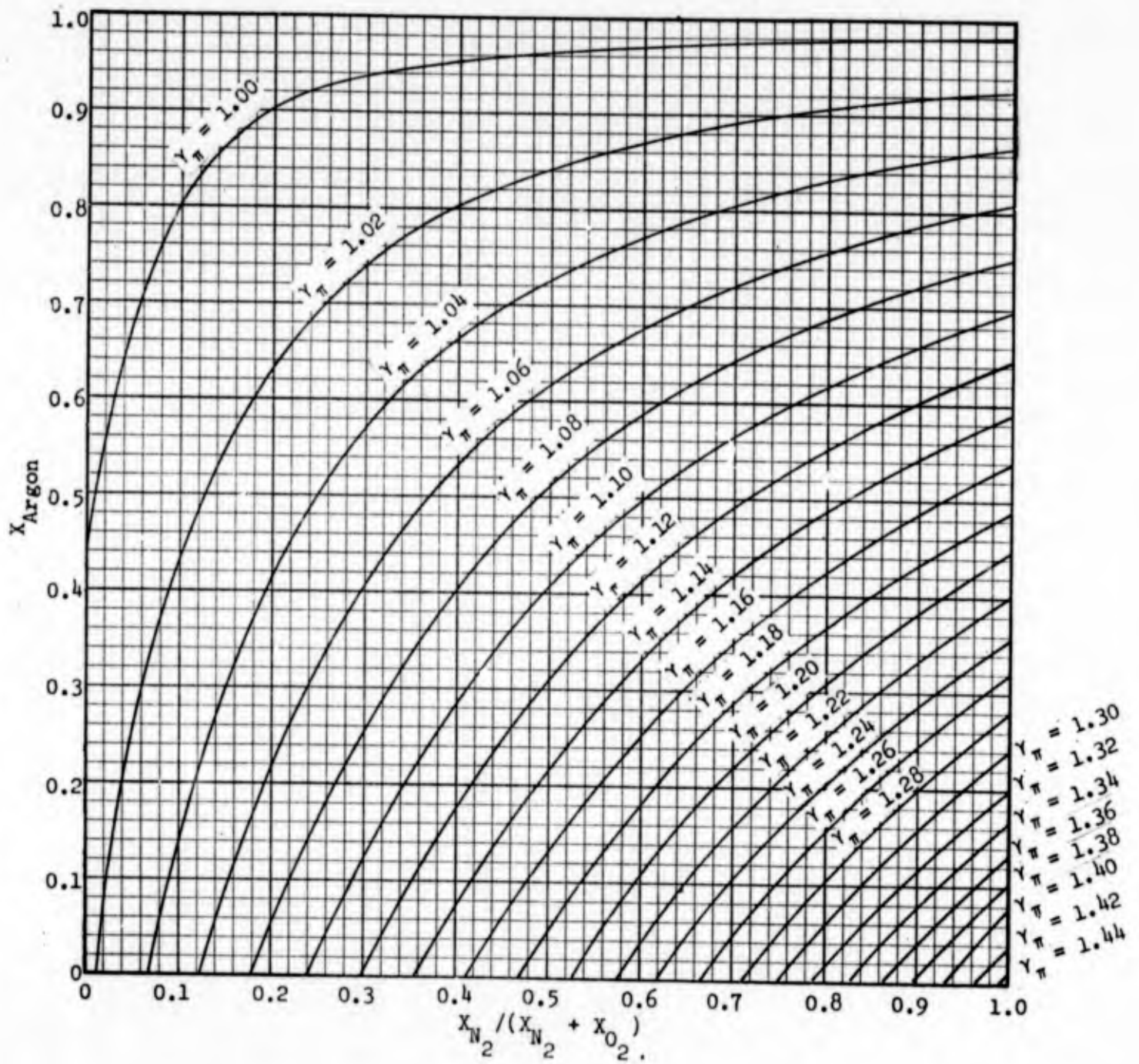


Figure 159. Argon Pressure Activity Coefficients, 23 Atmospheres.

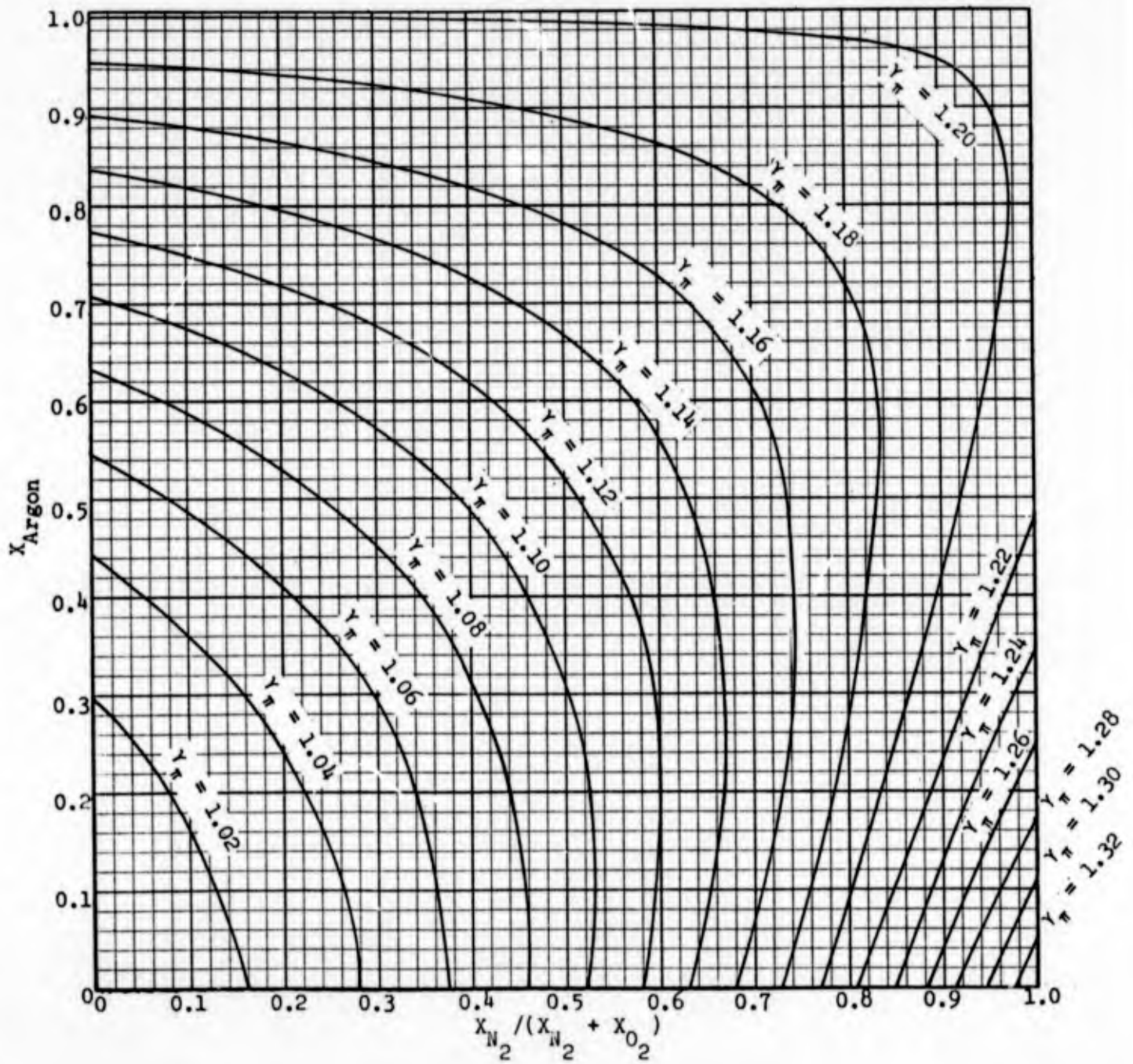


Figure 161. Oxygen Pressure Activity Coefficients, 1 Atmosphere.

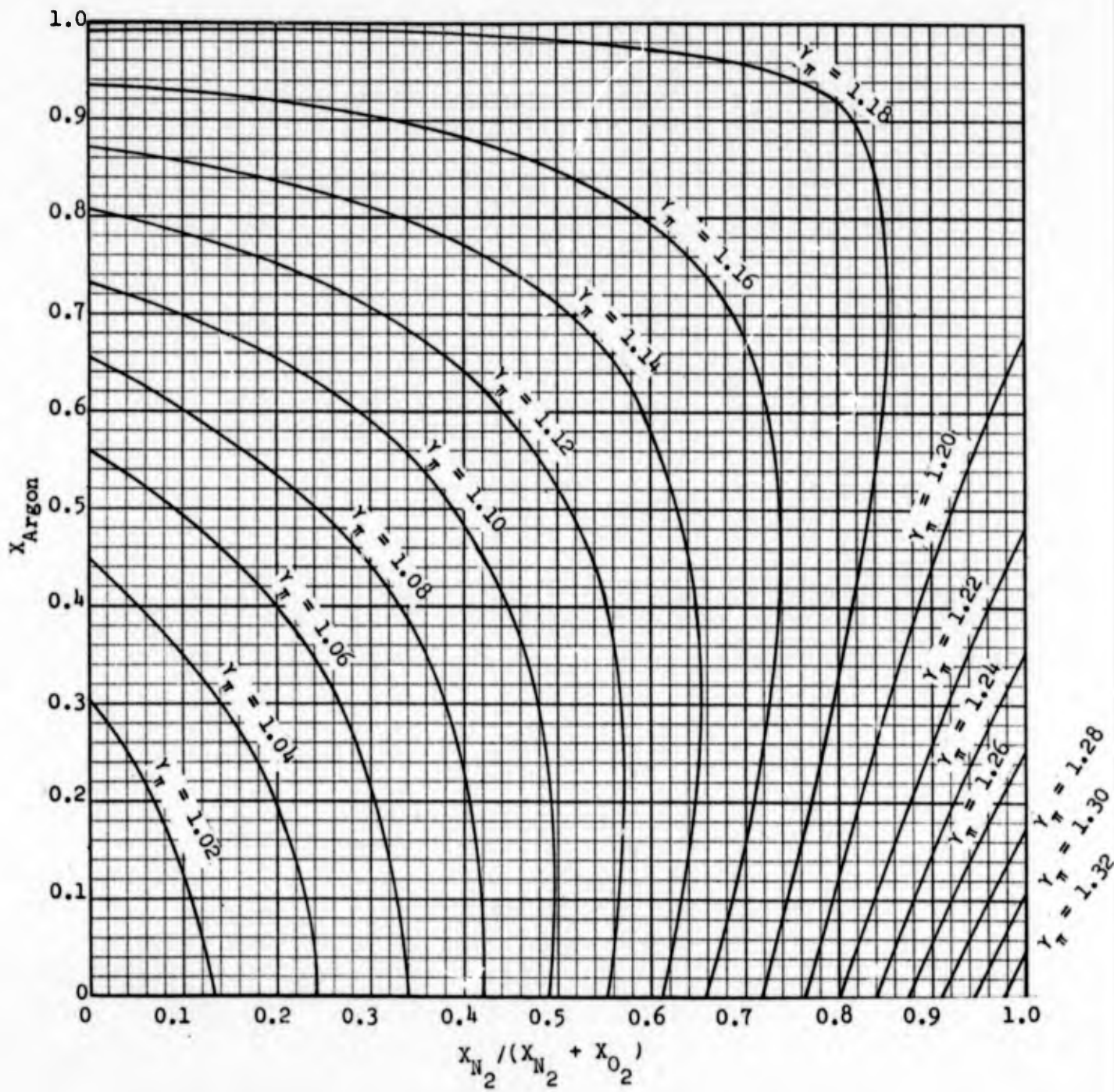


Figure 162. Oxygen Pressure Activity Coefficients, 2 Atmospheres.

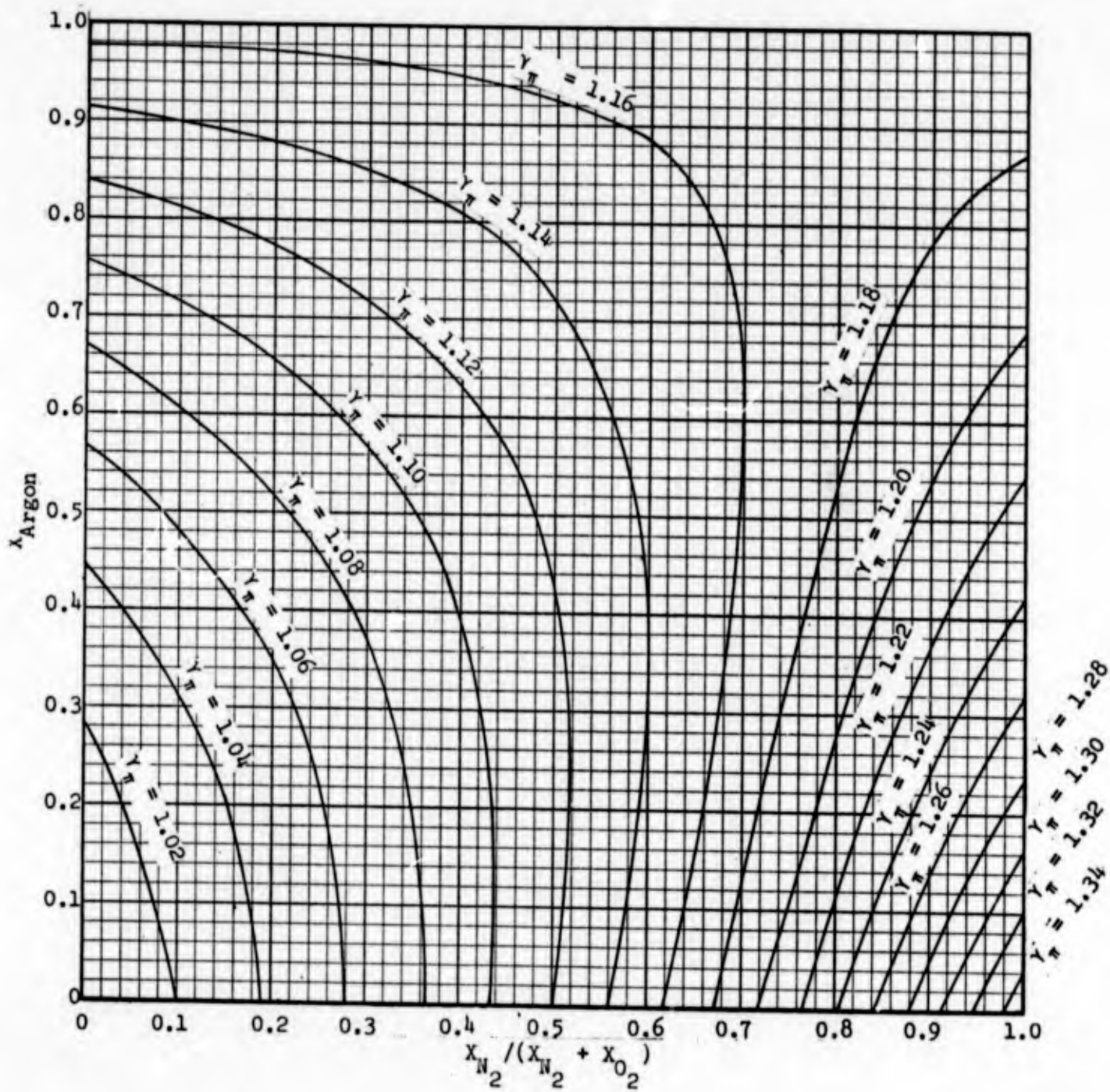


Figure 163. Oxygen Pressure Activity Coefficients, 4 Atmospheres.

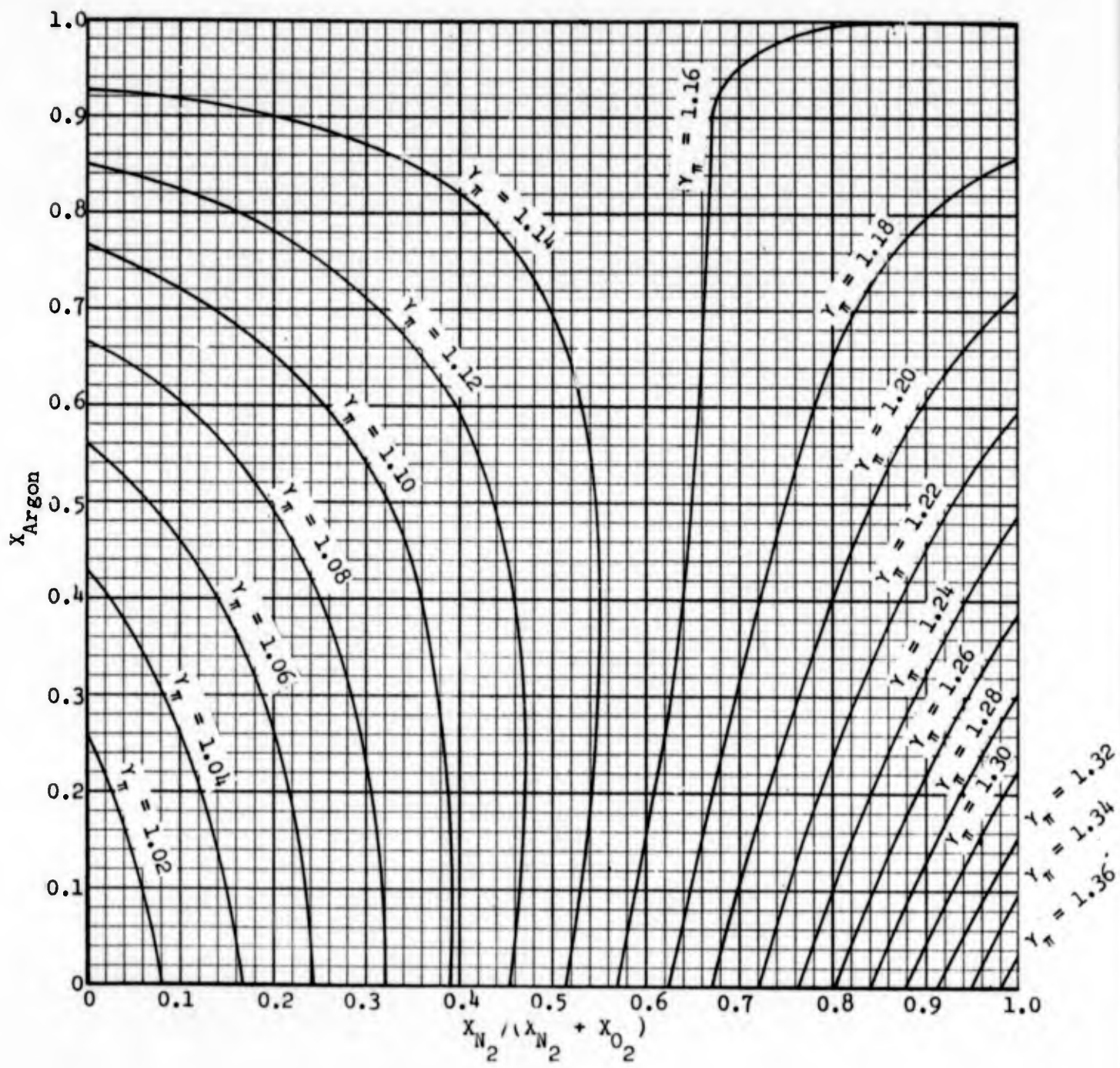


Figure 164. Oxygen Pressure Activity Coefficients, 6 Atmospheres.

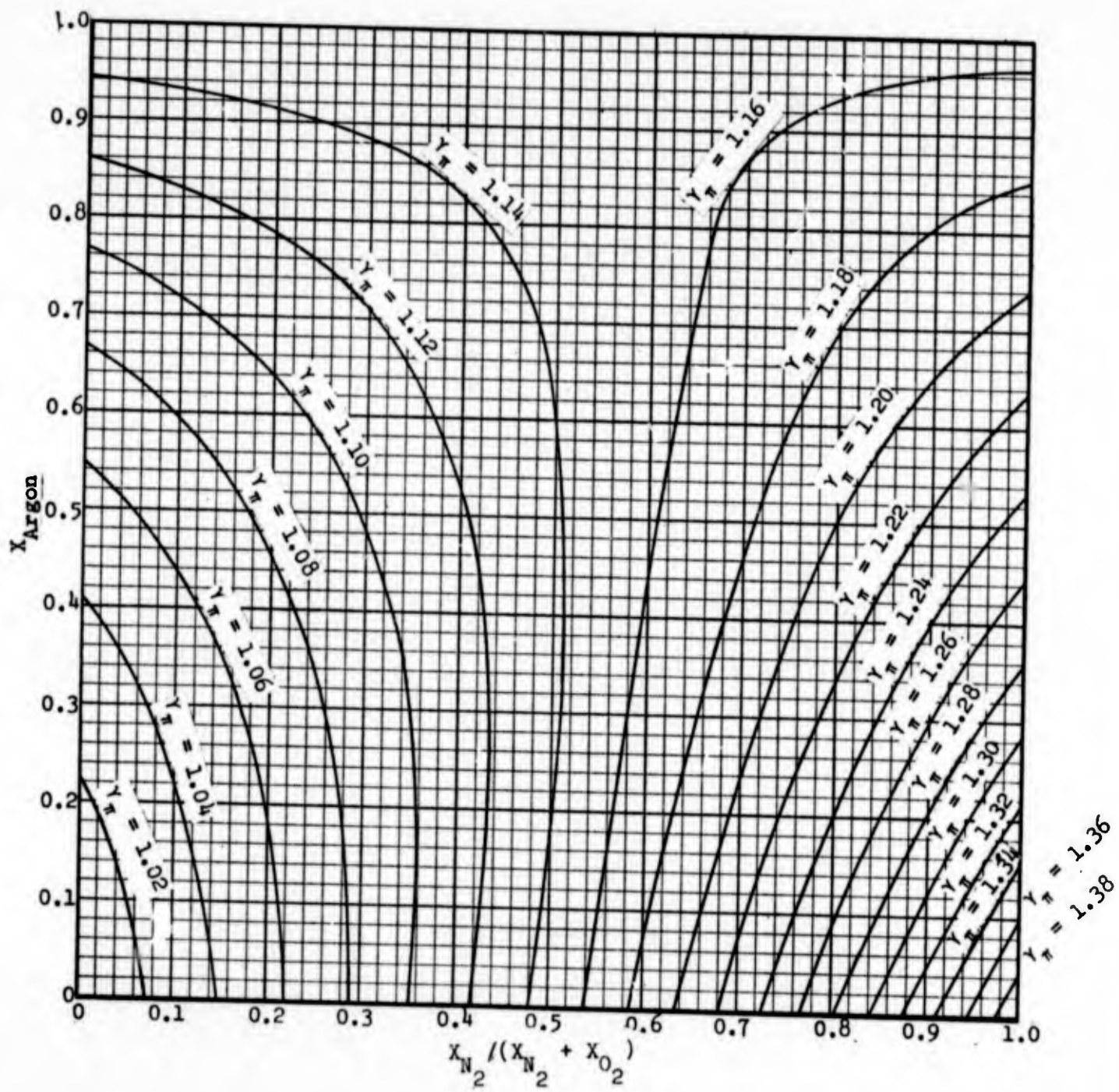


Figure 165. Oxygen Pressure Activity Coefficients, 8 Atmospheres.

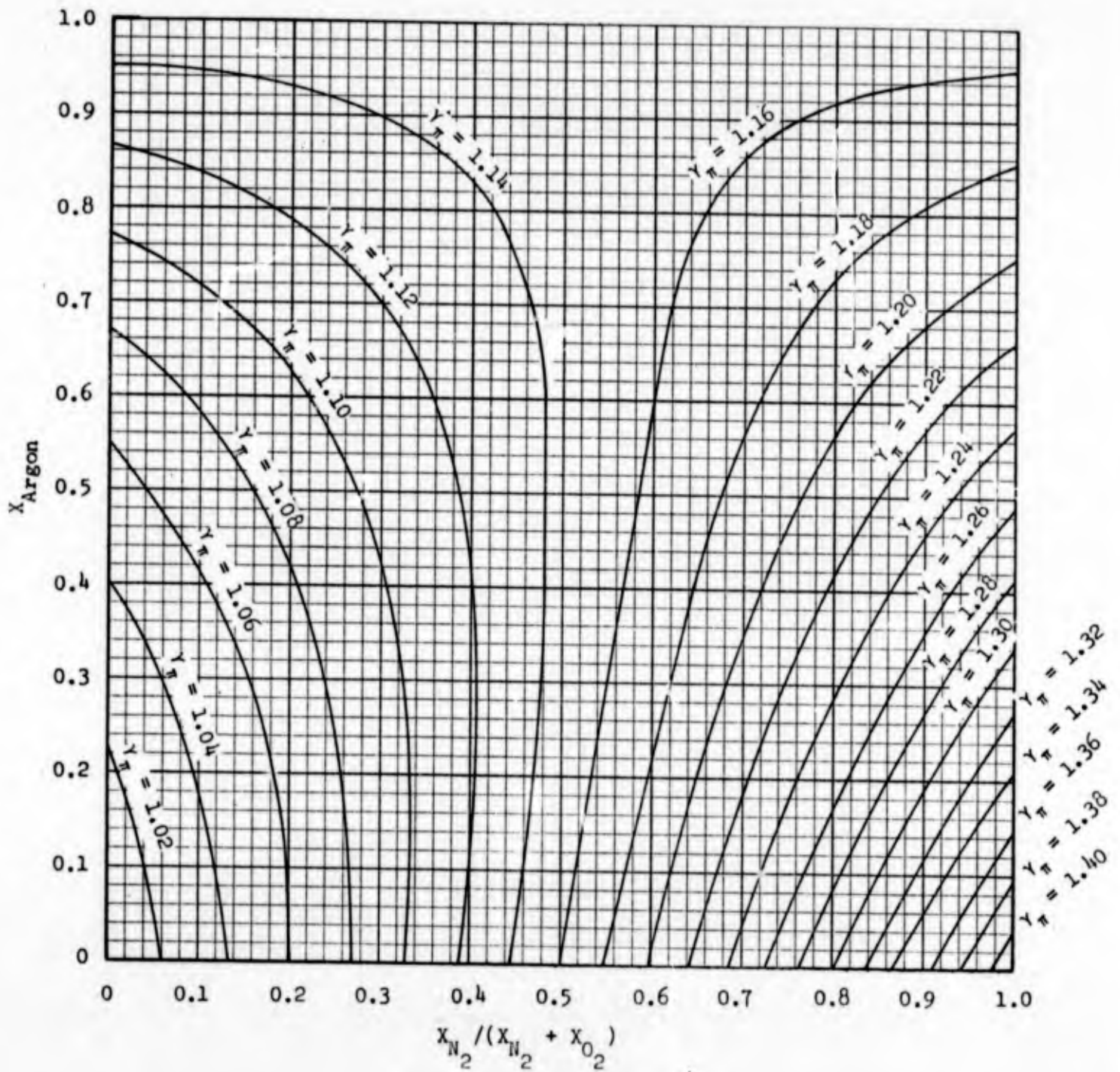


Figure 166. Oxygen Pressure Activity Coefficients, 10 Atmospheres.

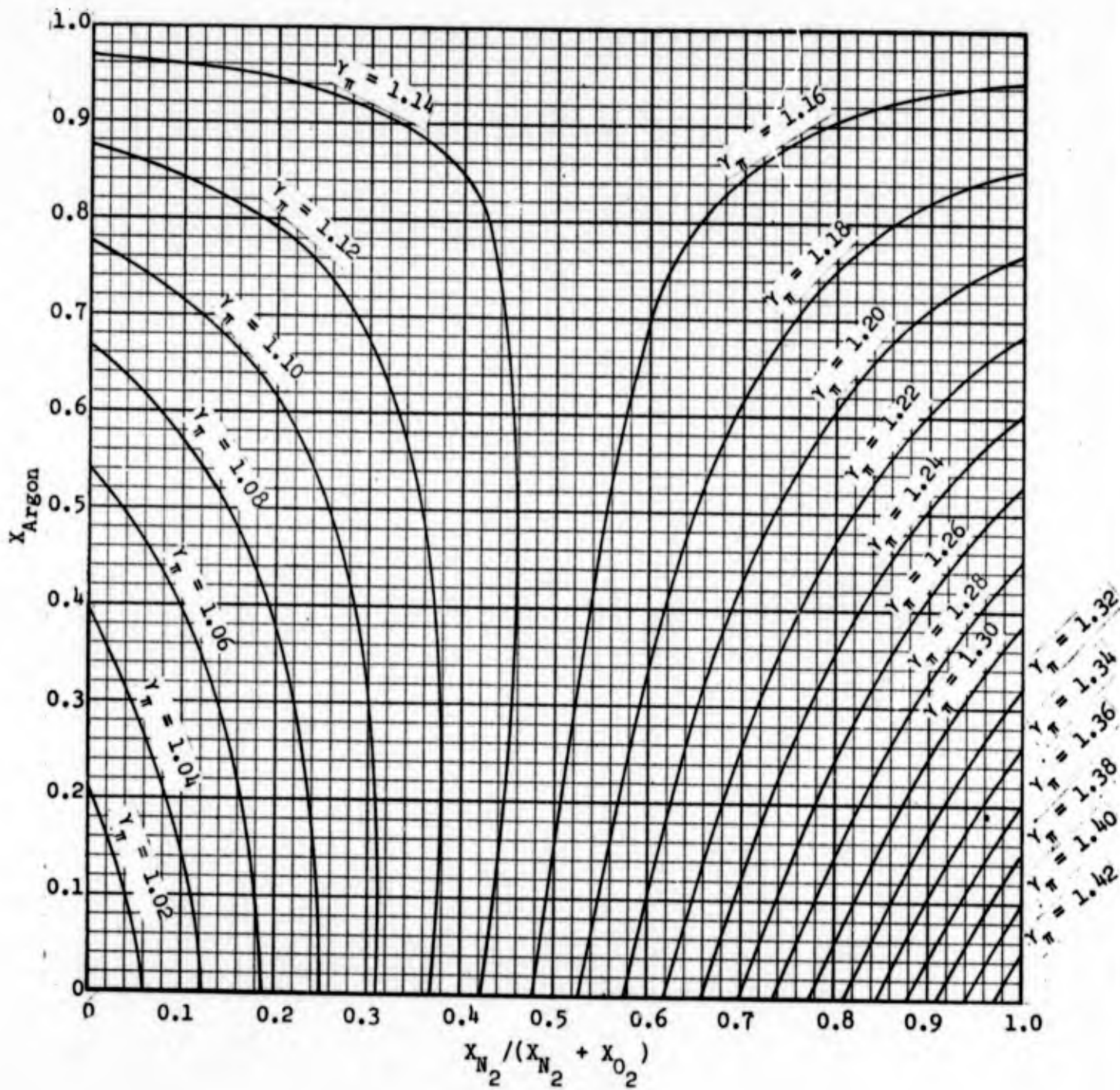


Figure 167. Oxygen Pressure Activity Coefficients, 12 Atmospheres.

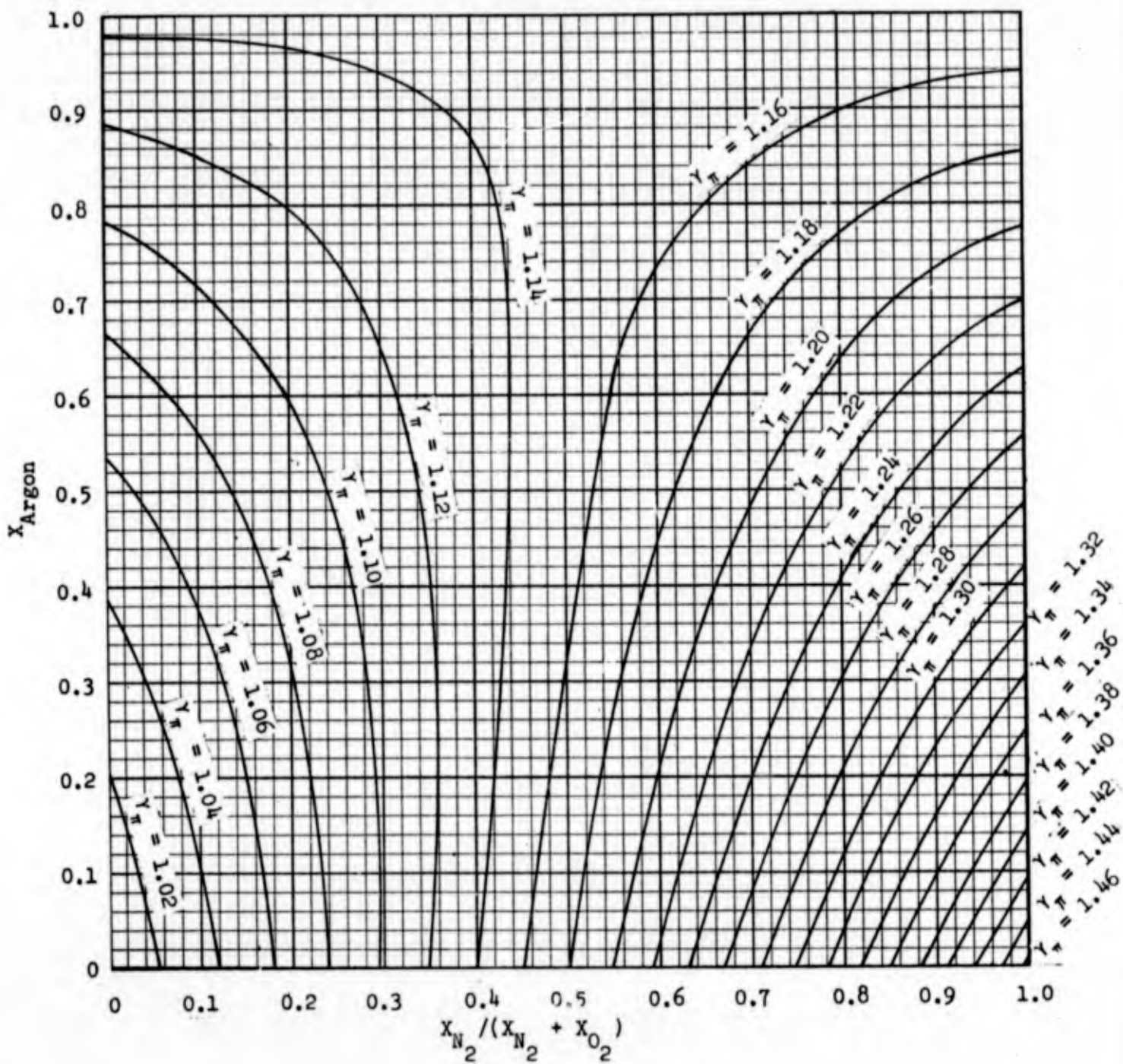


Figure 168. Oxygen Pressure Activity Coefficients, 14 Atmospheres,

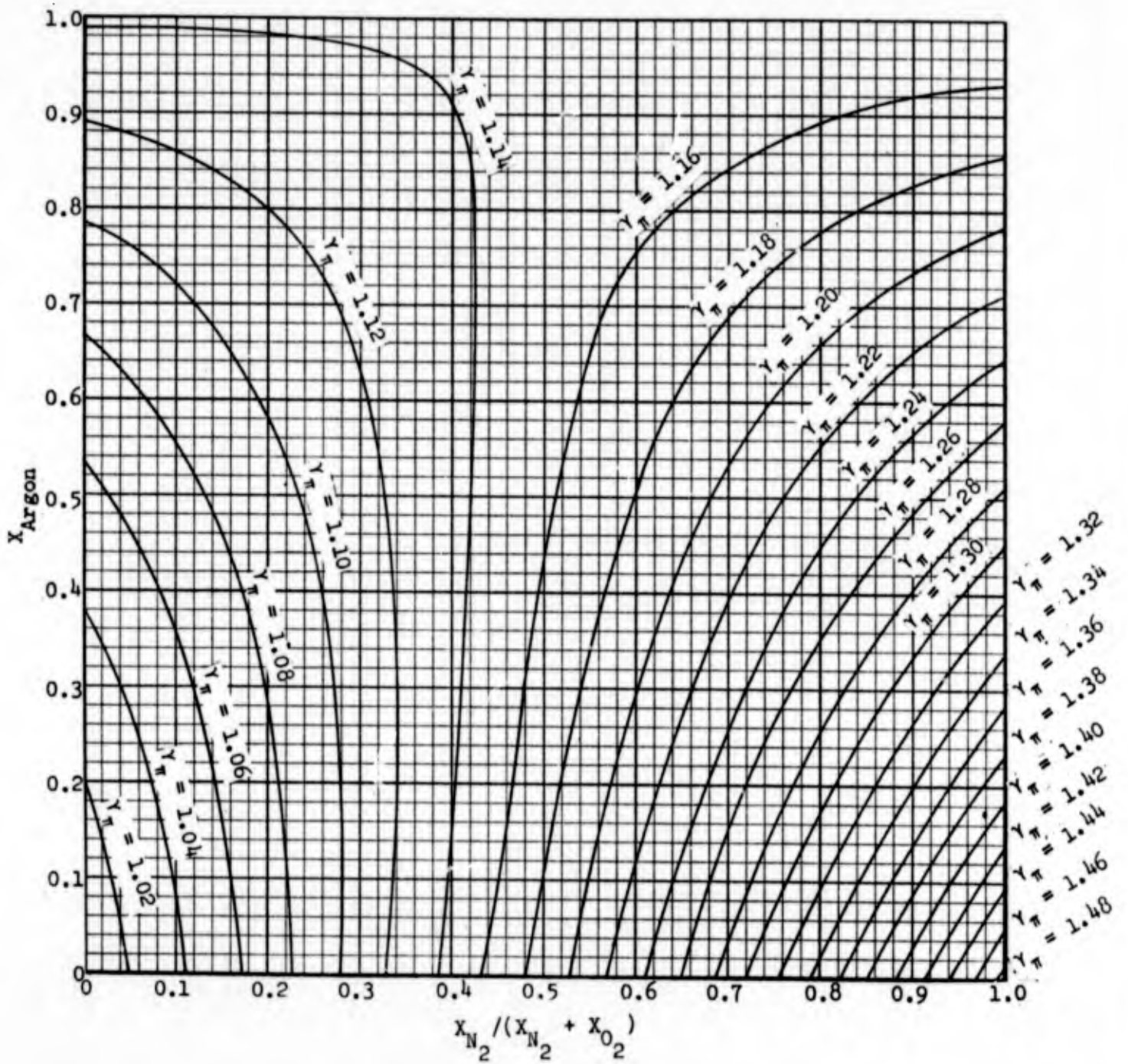


Figure 169. Oxygen Pressure Activity Coefficients, 16 Atmospheres.

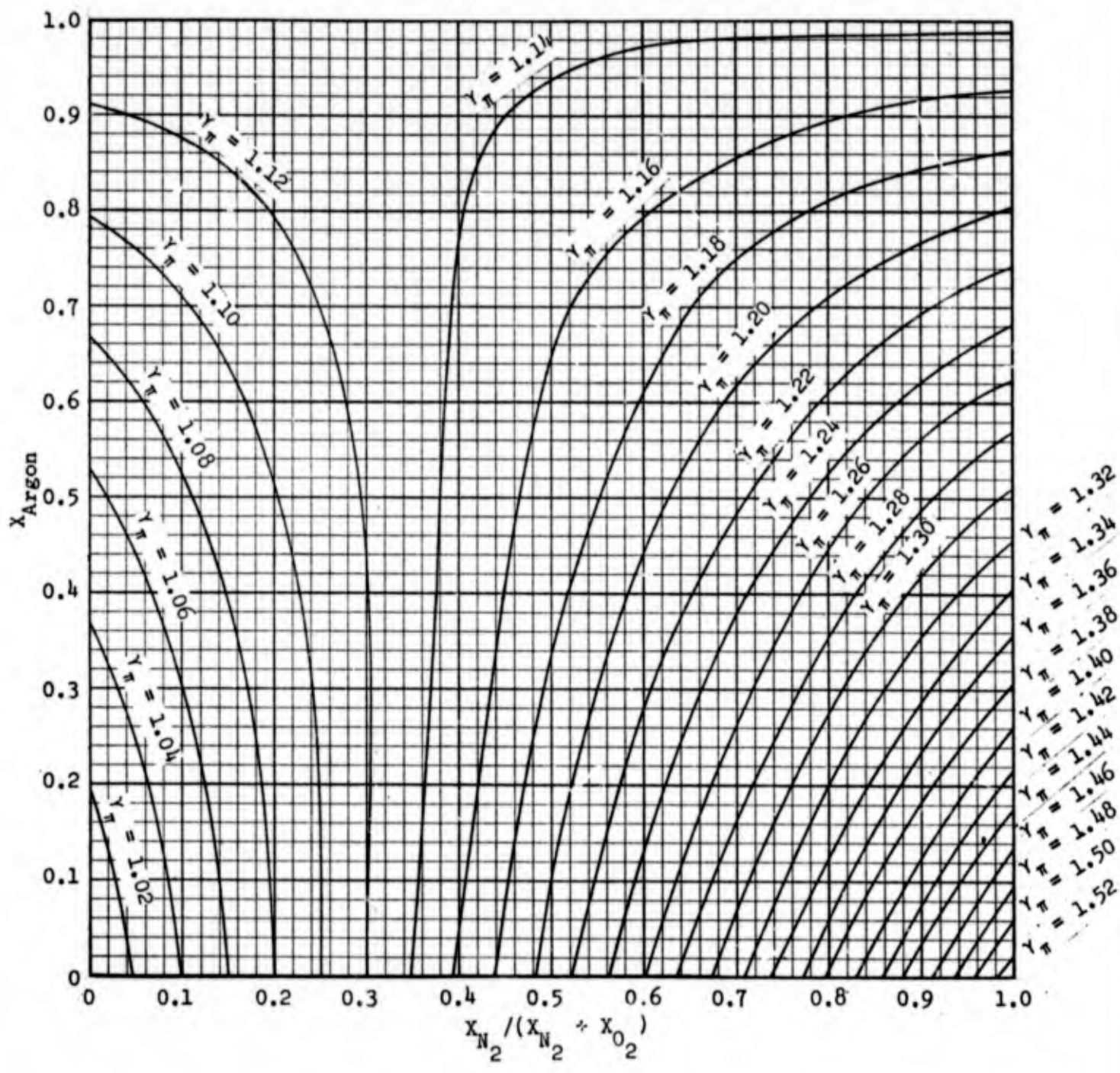


Figure 171. Oxygen Pressure Activity Coefficients, 20 Atmospheres.

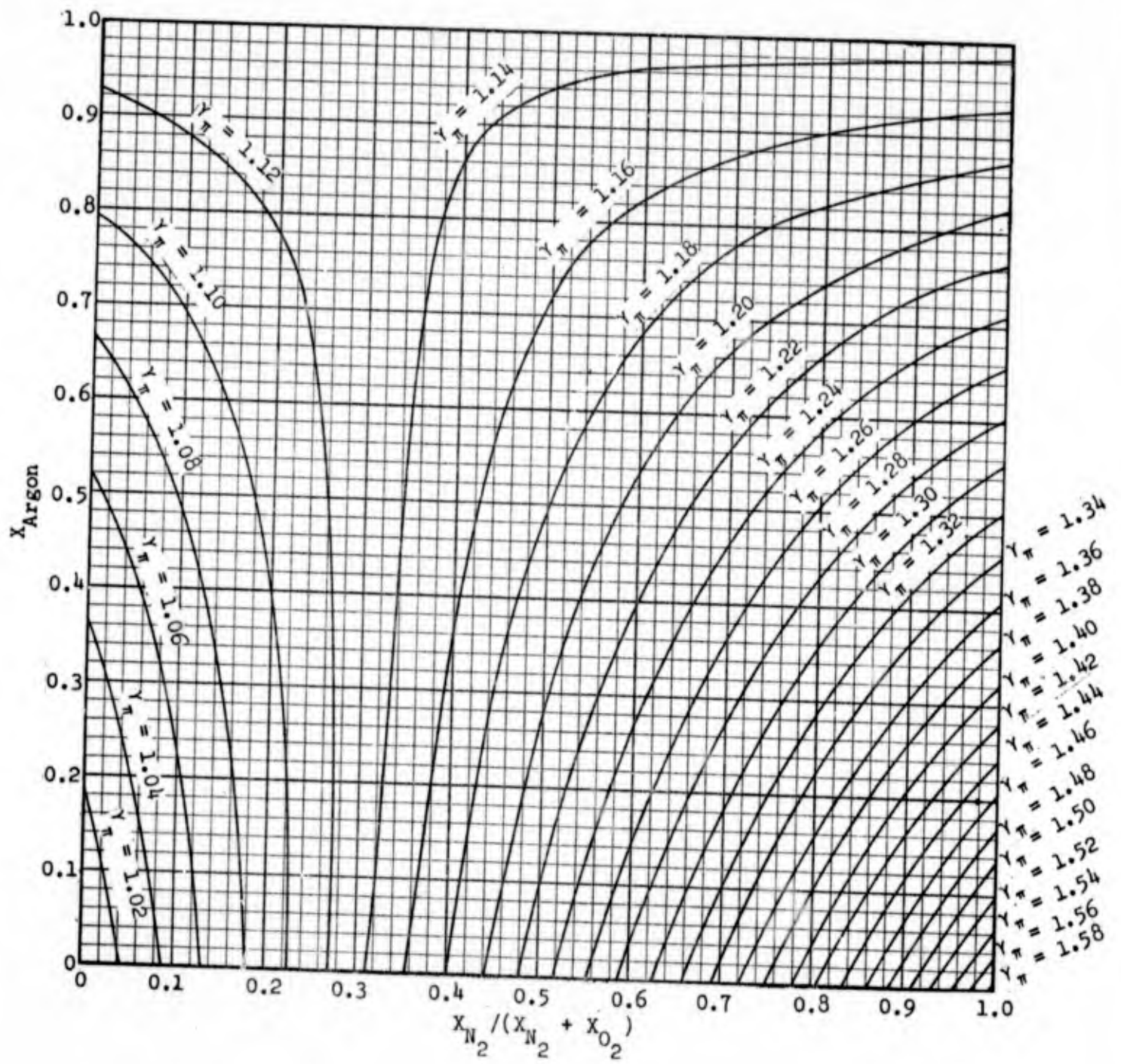


Figure 172. Oxygen Pressure Activity Coefficients, 23 Atmospheres.

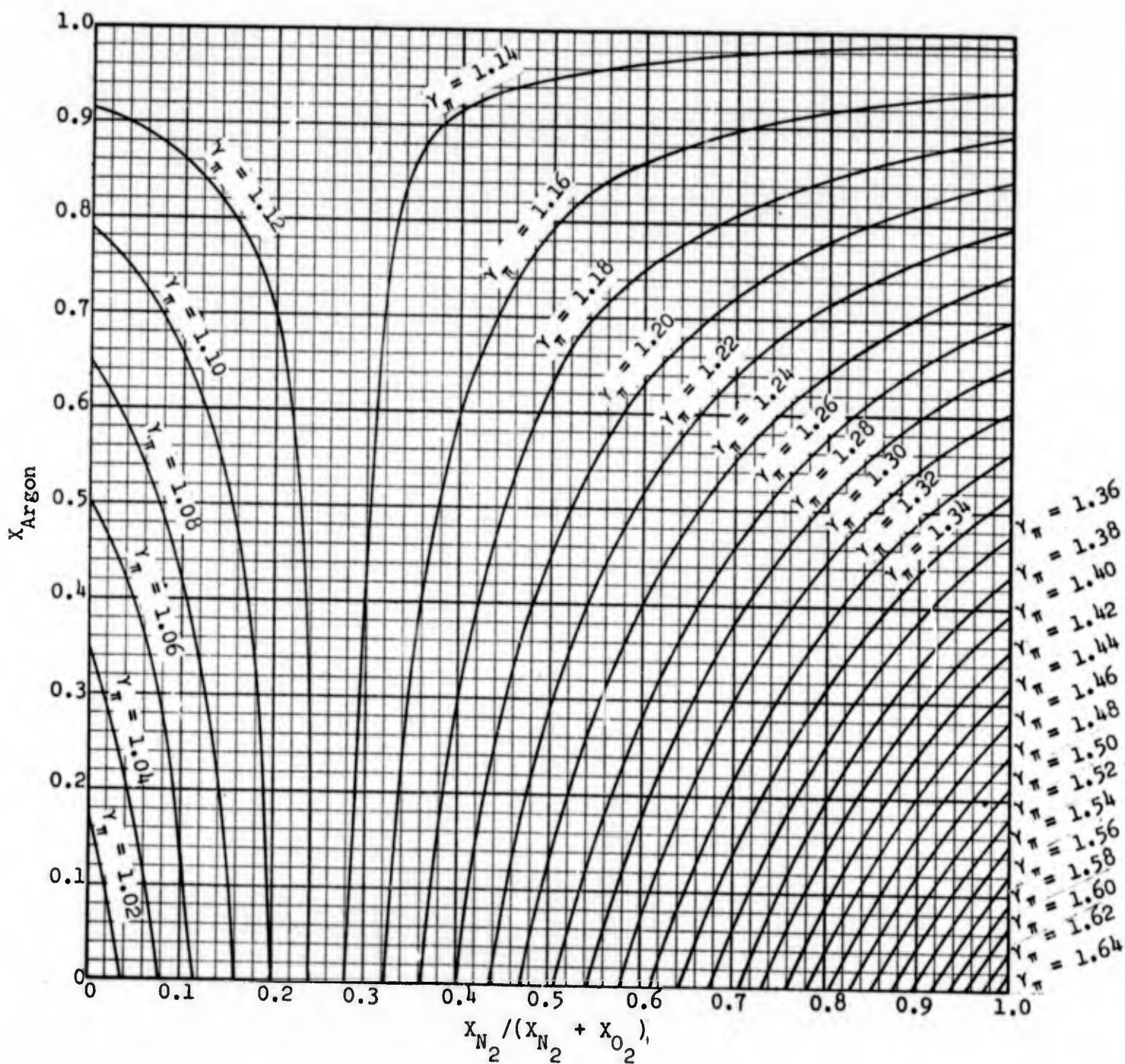


Figure 173. Oxygen Pressure Activity Coefficients, 26 Atmospheres.

G. Mixture Vapor Pressures Vs. Temperatures

The 13 graphs to follow present the vapor pressure of a number of specific mixtures as it varies with temperature. These graphs are plotted as $\log P$ vs. $1/T$. The graphs are ordered with respect to increasing mole fraction argon in the liquid.

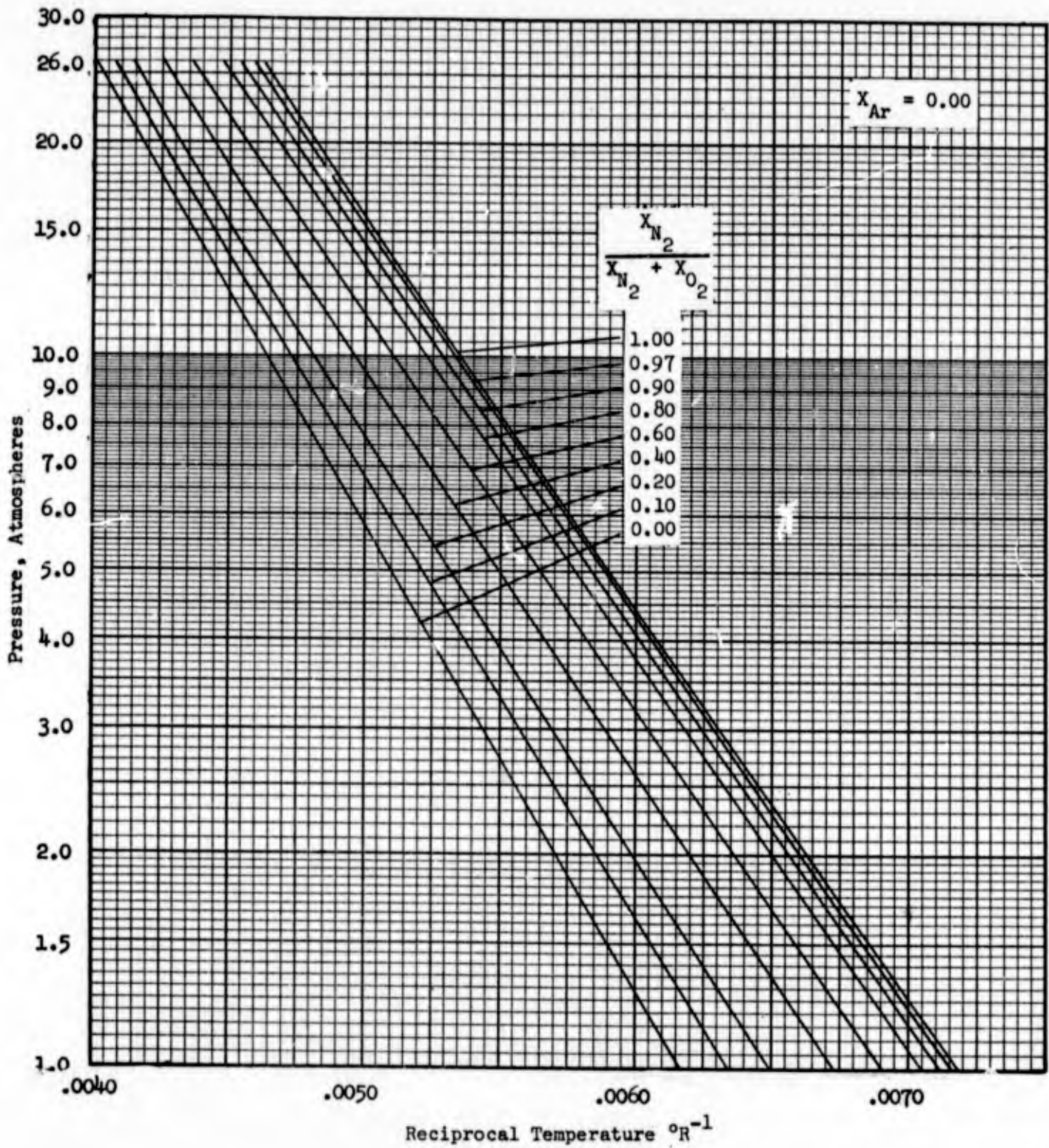


Figure 174. Vapor Pressures of Specific Mixtures of N_2 -Ar- O_2 .

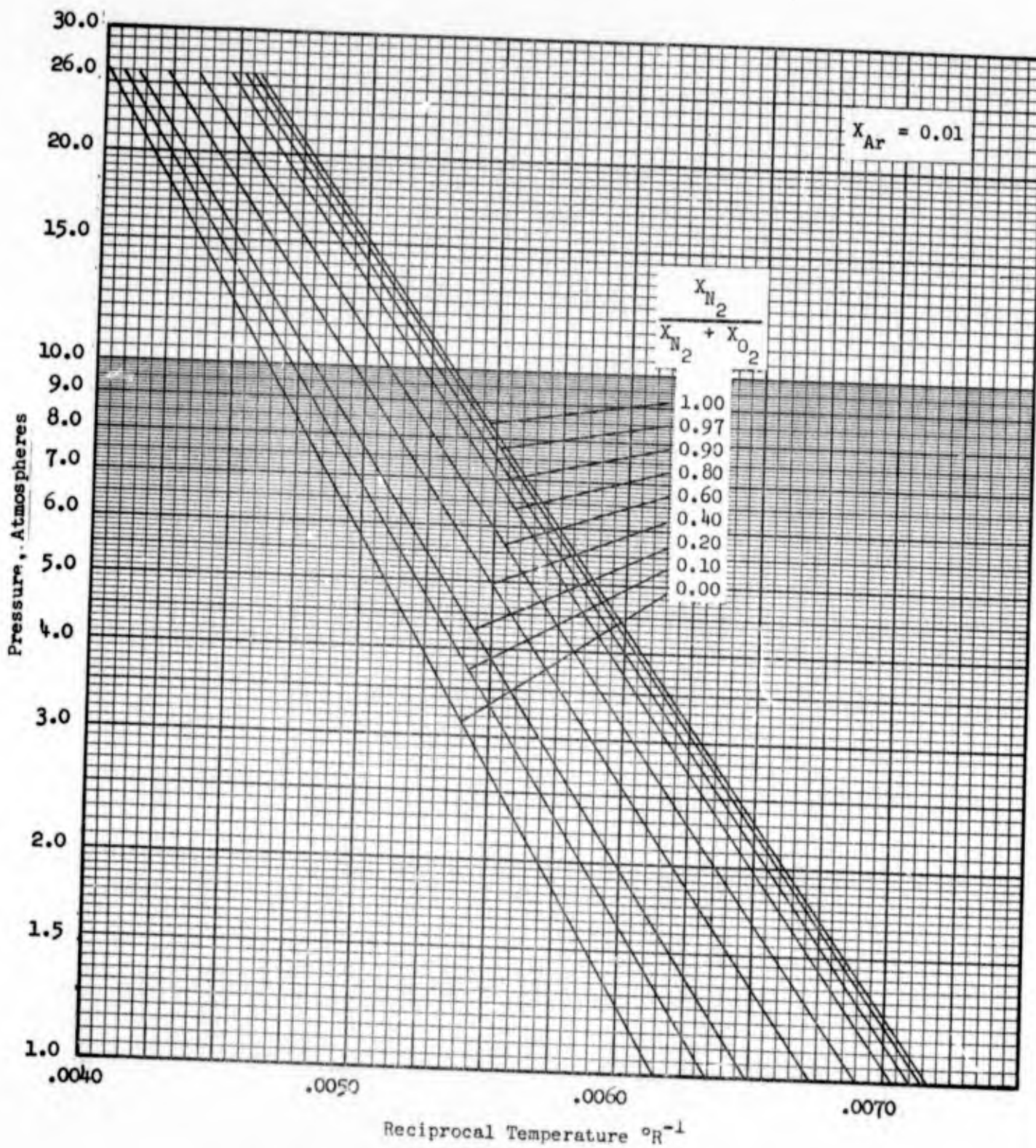


Figure 175. Vapor Pressures of Specific Mixtures of N_2 -Ar- O_2 .

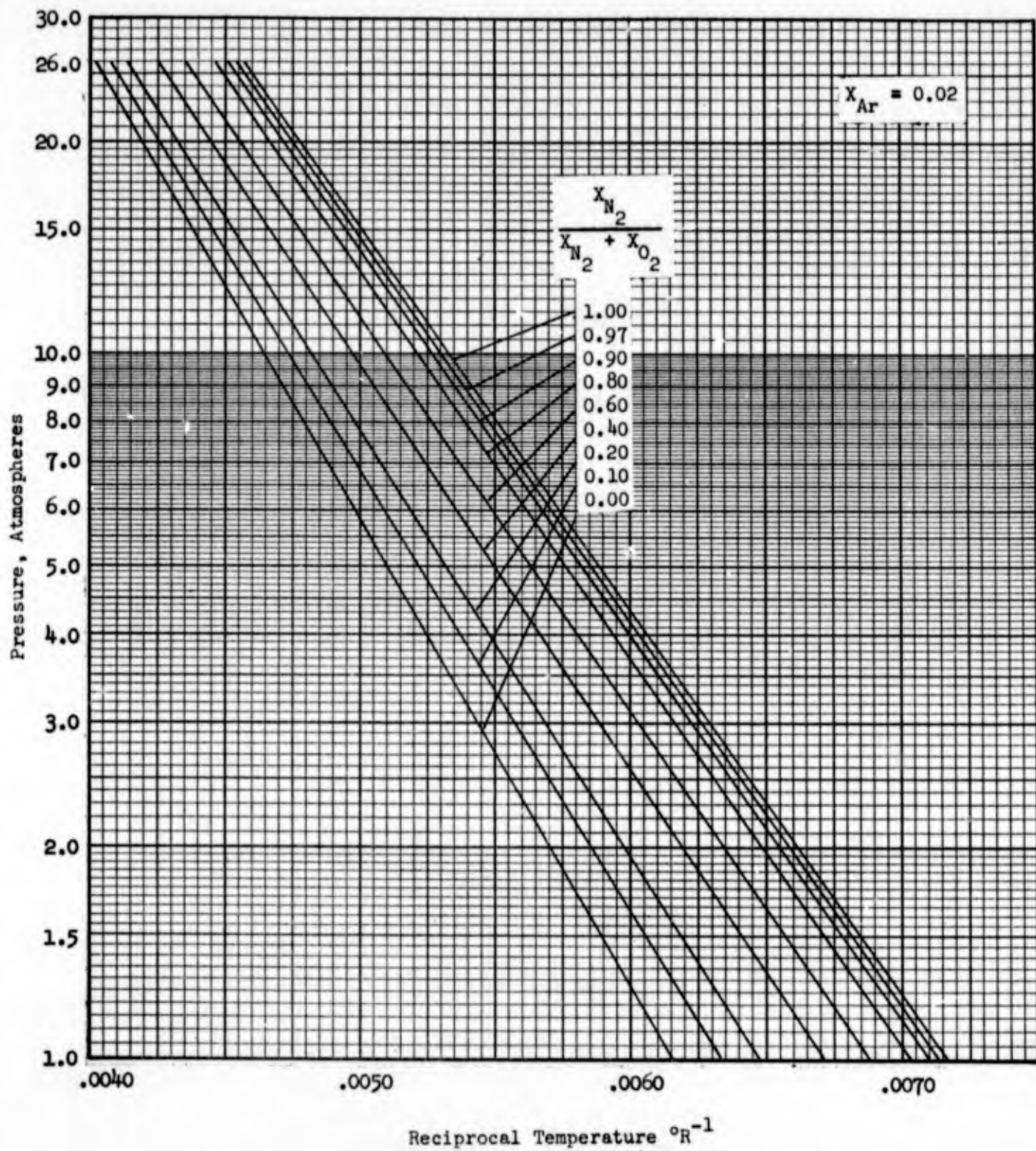


Figure 176. Vapor Pressures of Specific Mixtures of N_2 -Ar- O_2 .

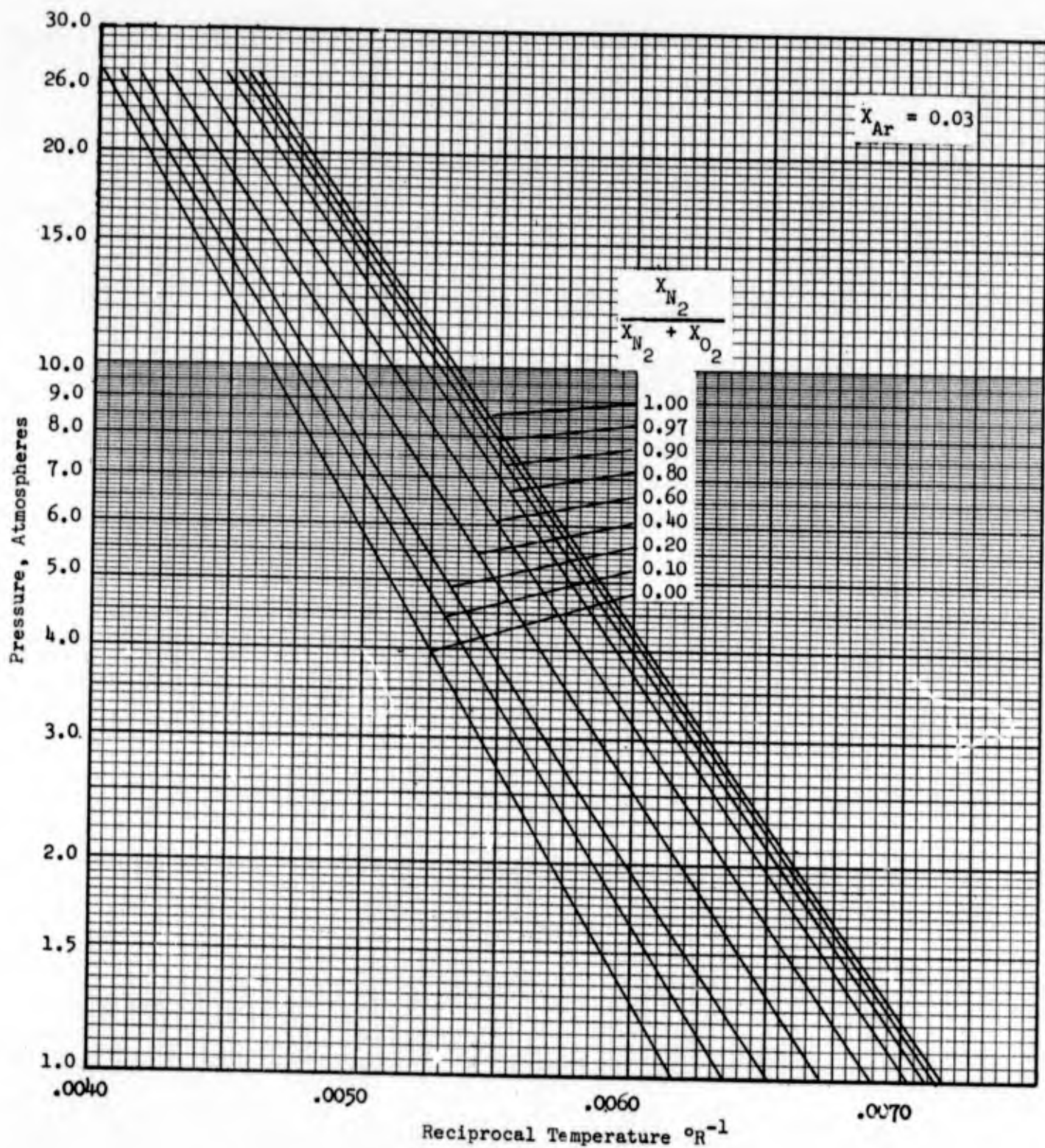


Figure 177. Vapor Pressures of Specific Mixtures of N_2 -Ar- O_2 .

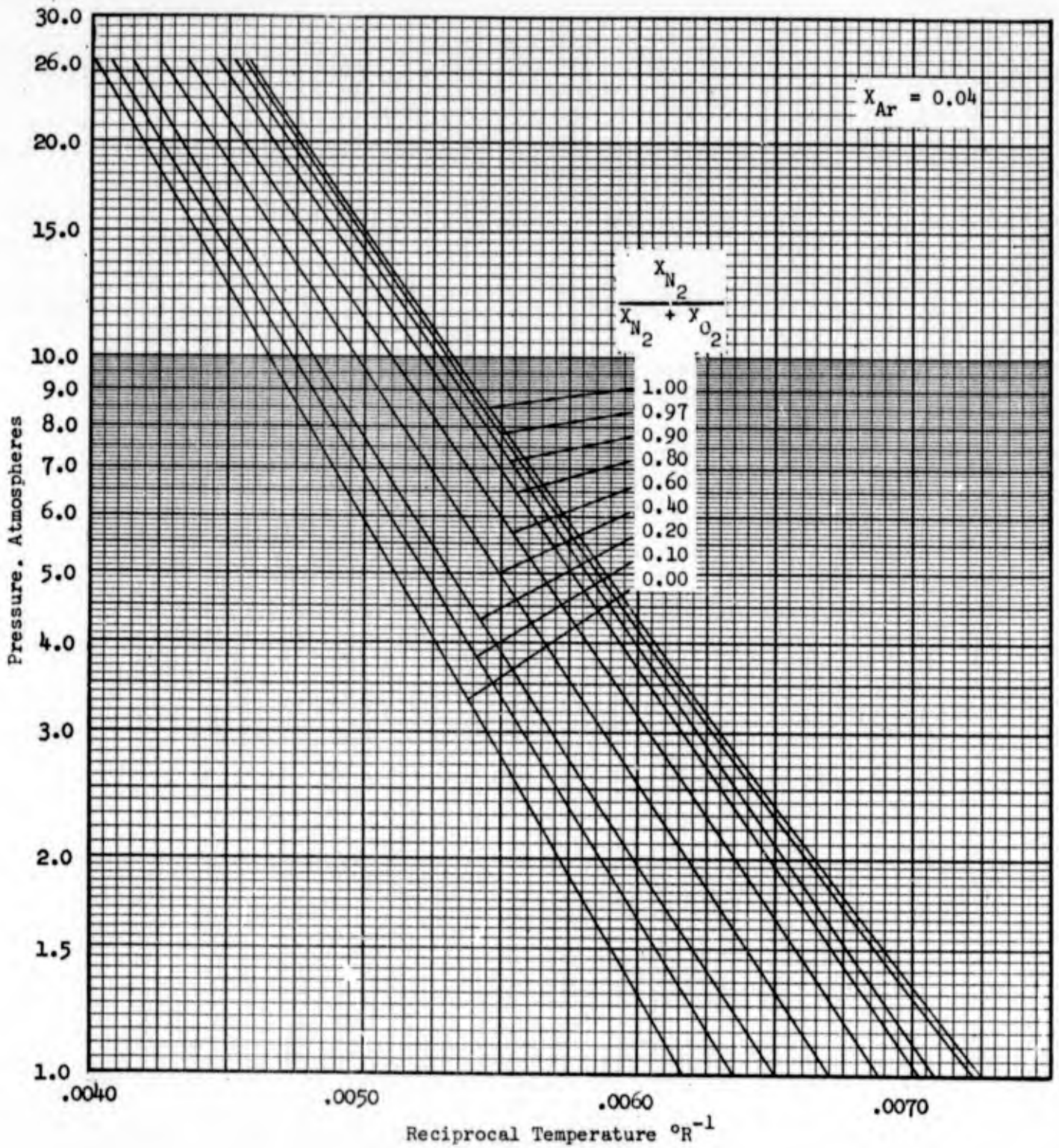


Figure 178. Vapor Pressures of Specific Mixtures of N_2 -Ar- O_2 .

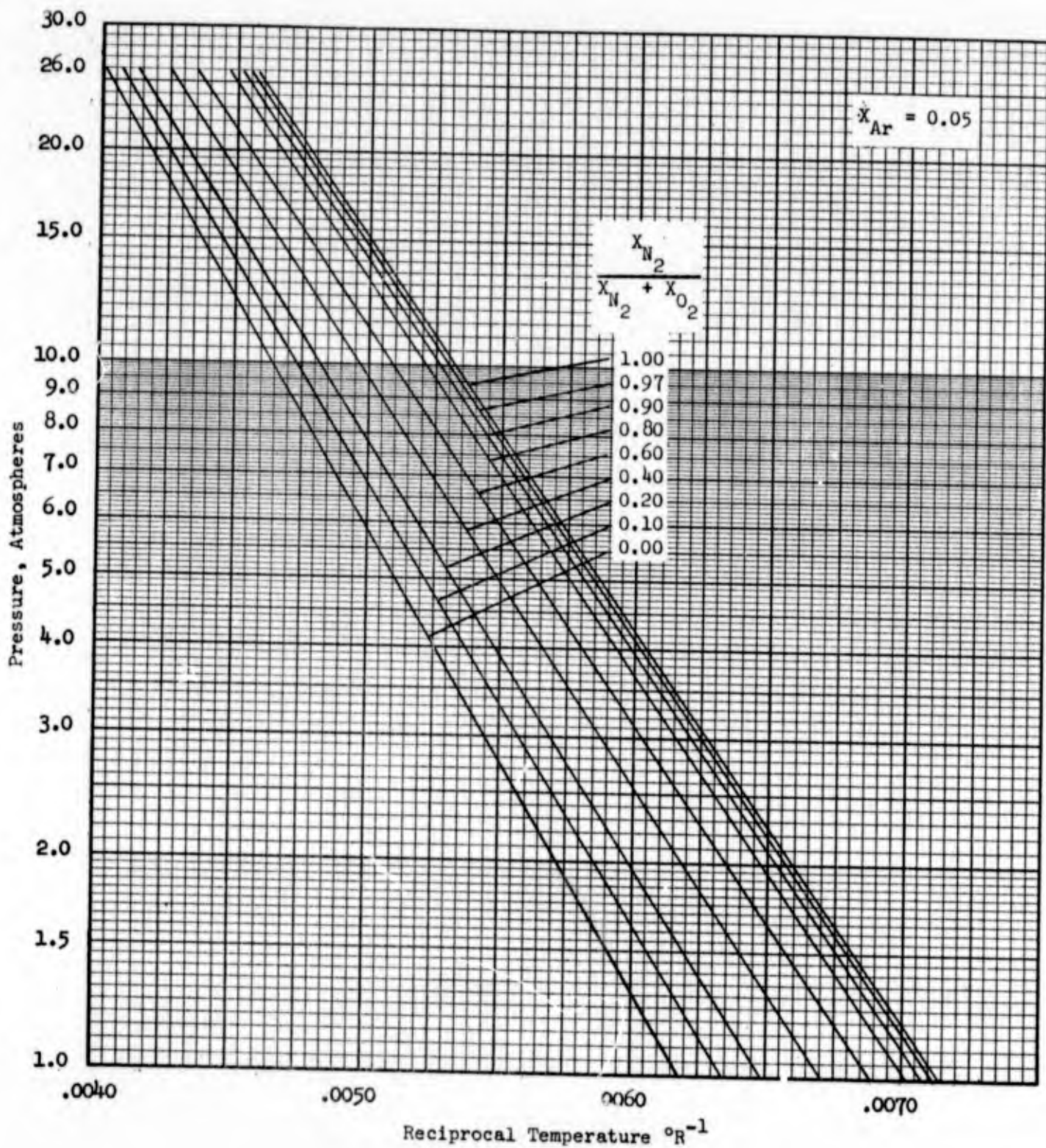


Figure 179. Vapor Pressures of Specific Mixtures of N_2 -Ar- O_2 .

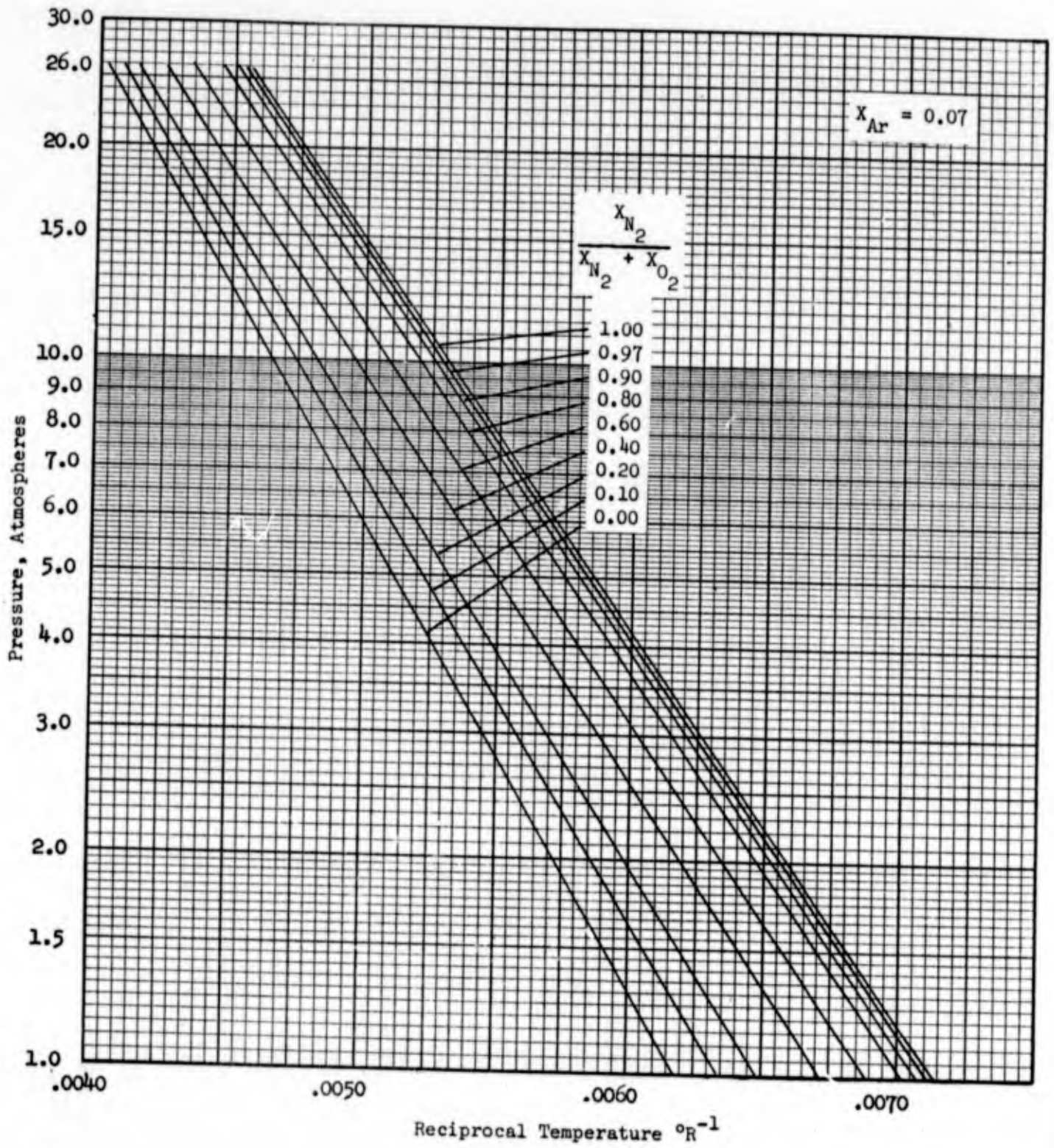


Figure 180. Vapor Pressures of Specific Mixtures of N_2 -Ar- O_2 .

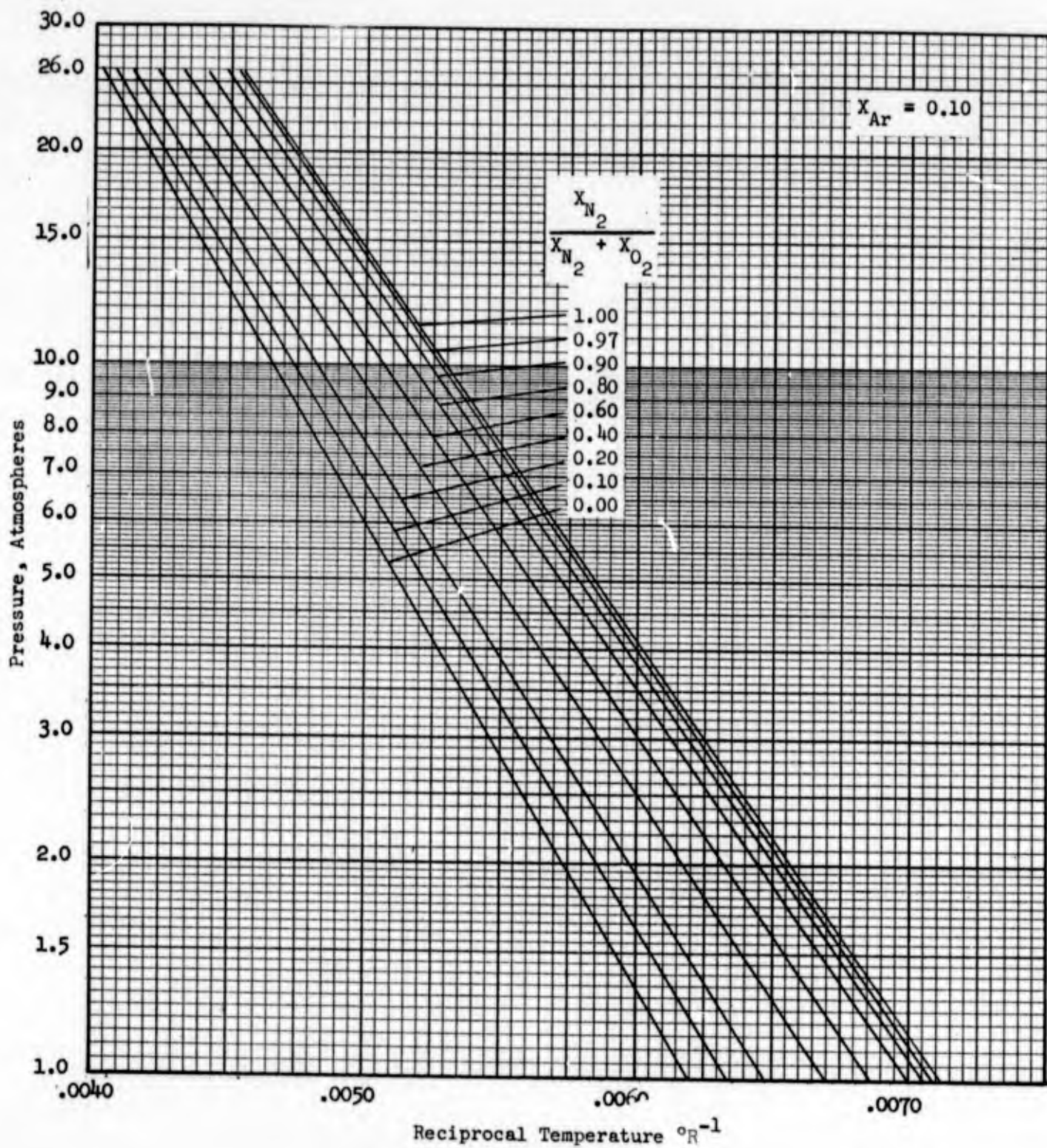


Figure 181. Vapor Pressures of Specific Mixtures of N_2 -Ar- O_2 .

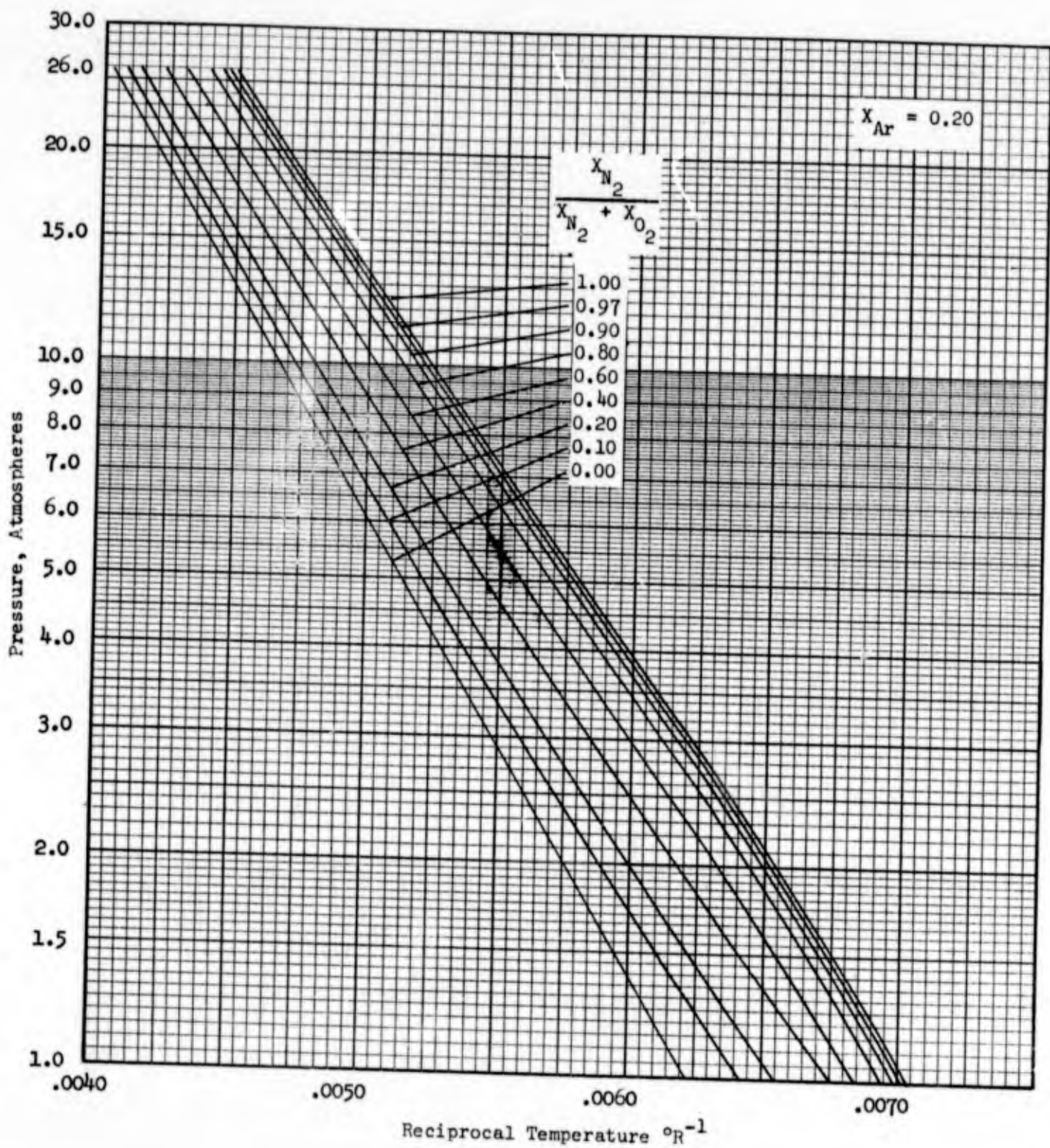


Figure 182. Vapor Pressures of Specific Mixtures of N_2 -Ar- O_2 .

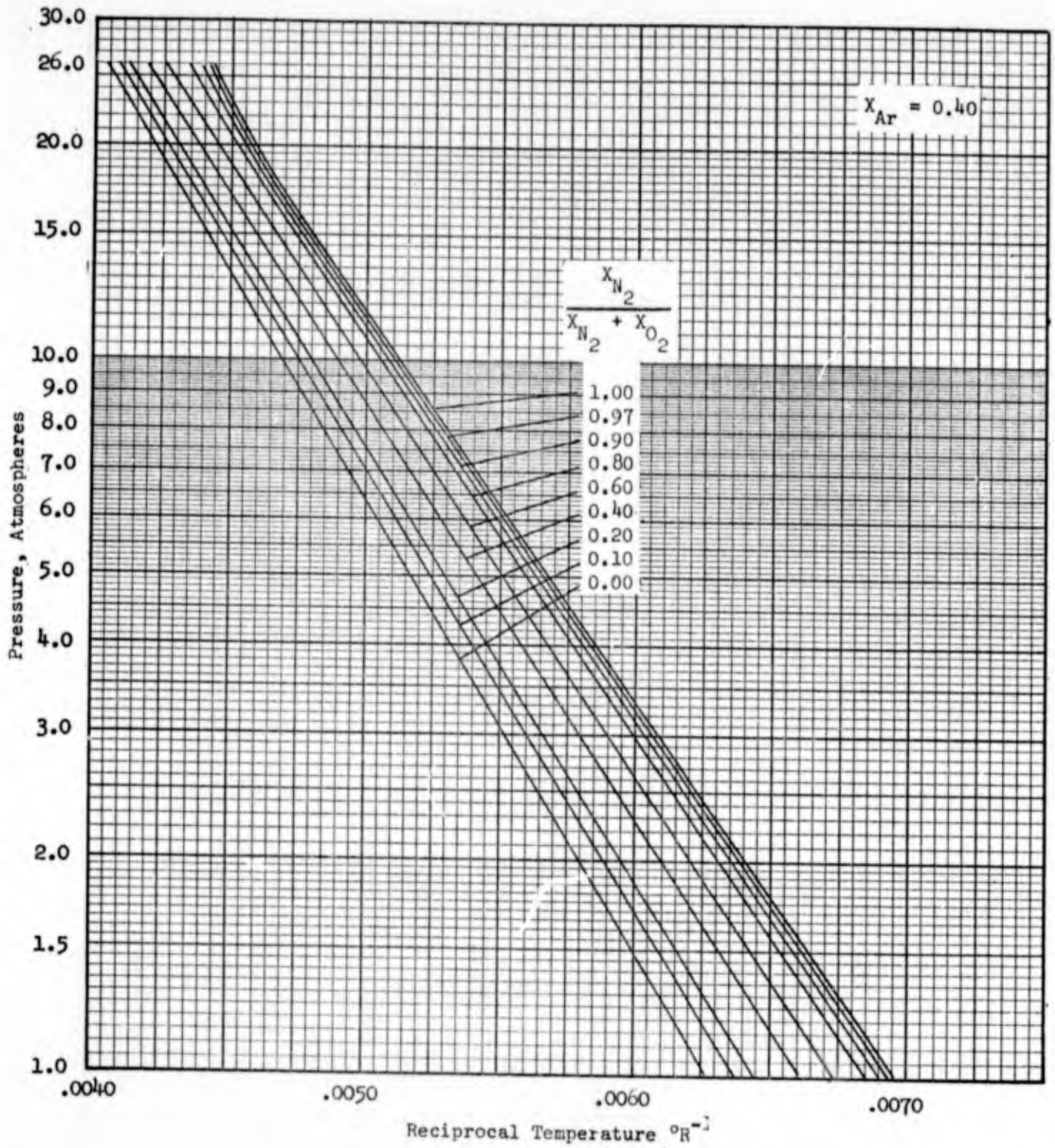


Figure 183. Vapor Pressures of Specific Mixtures of N_2 -Ar- O_2 .

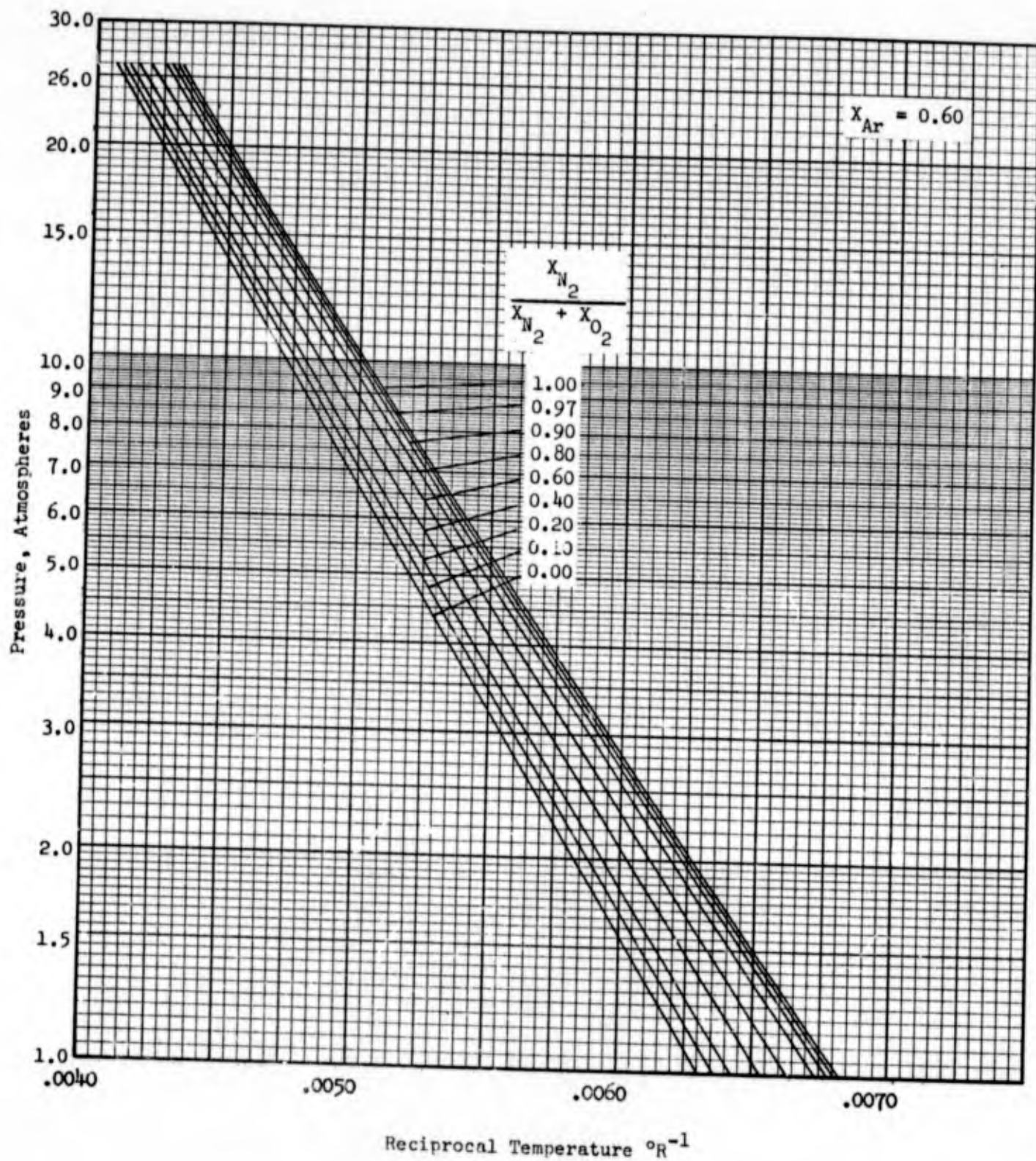


Figure 184. Vapor Pressures of Specific Mixtures of N_2 -Ar- O_2 .

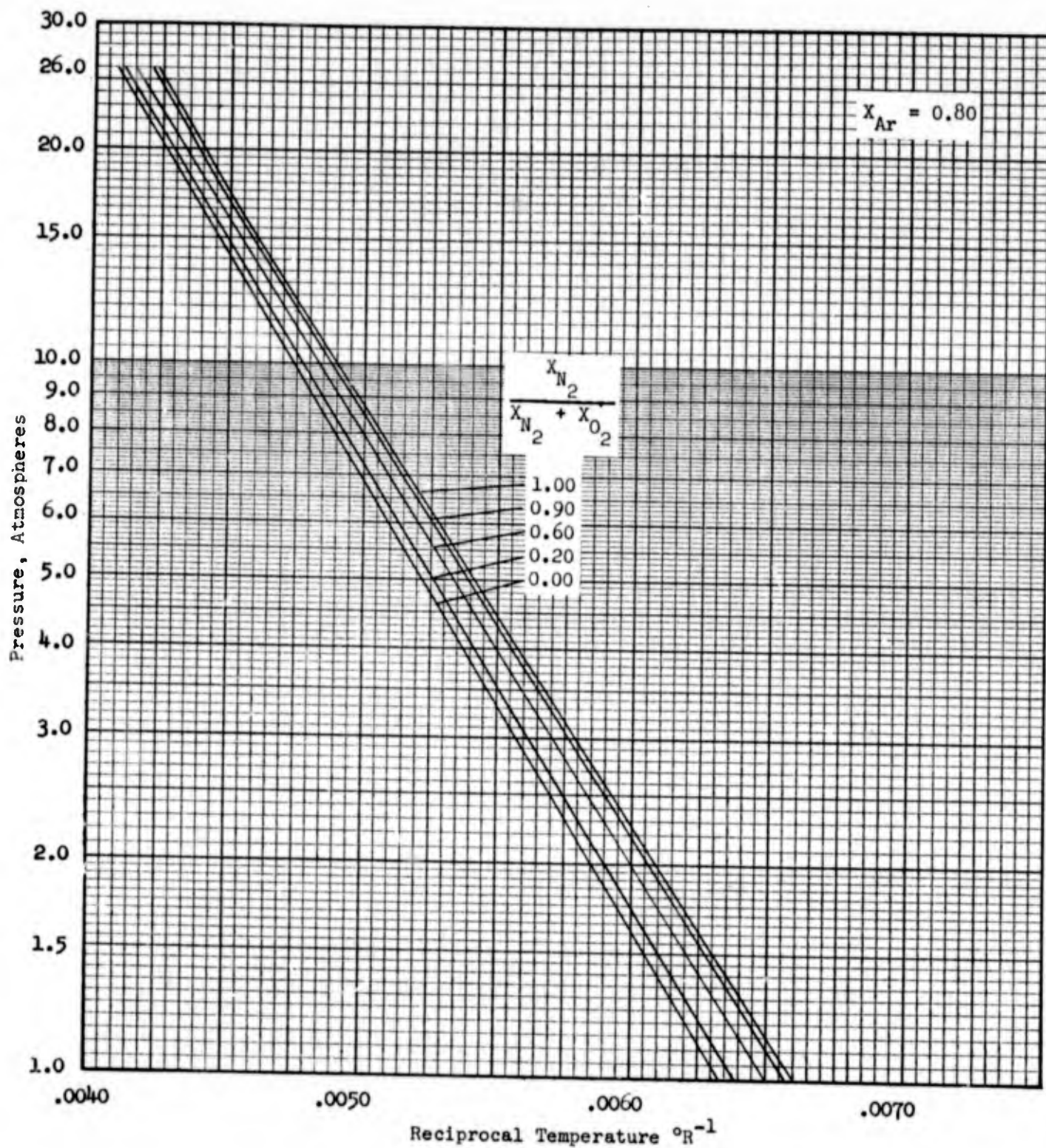


Figure 185. Vapor Pressures of Specific Mixtures of N_2 -Ar- O_2 .

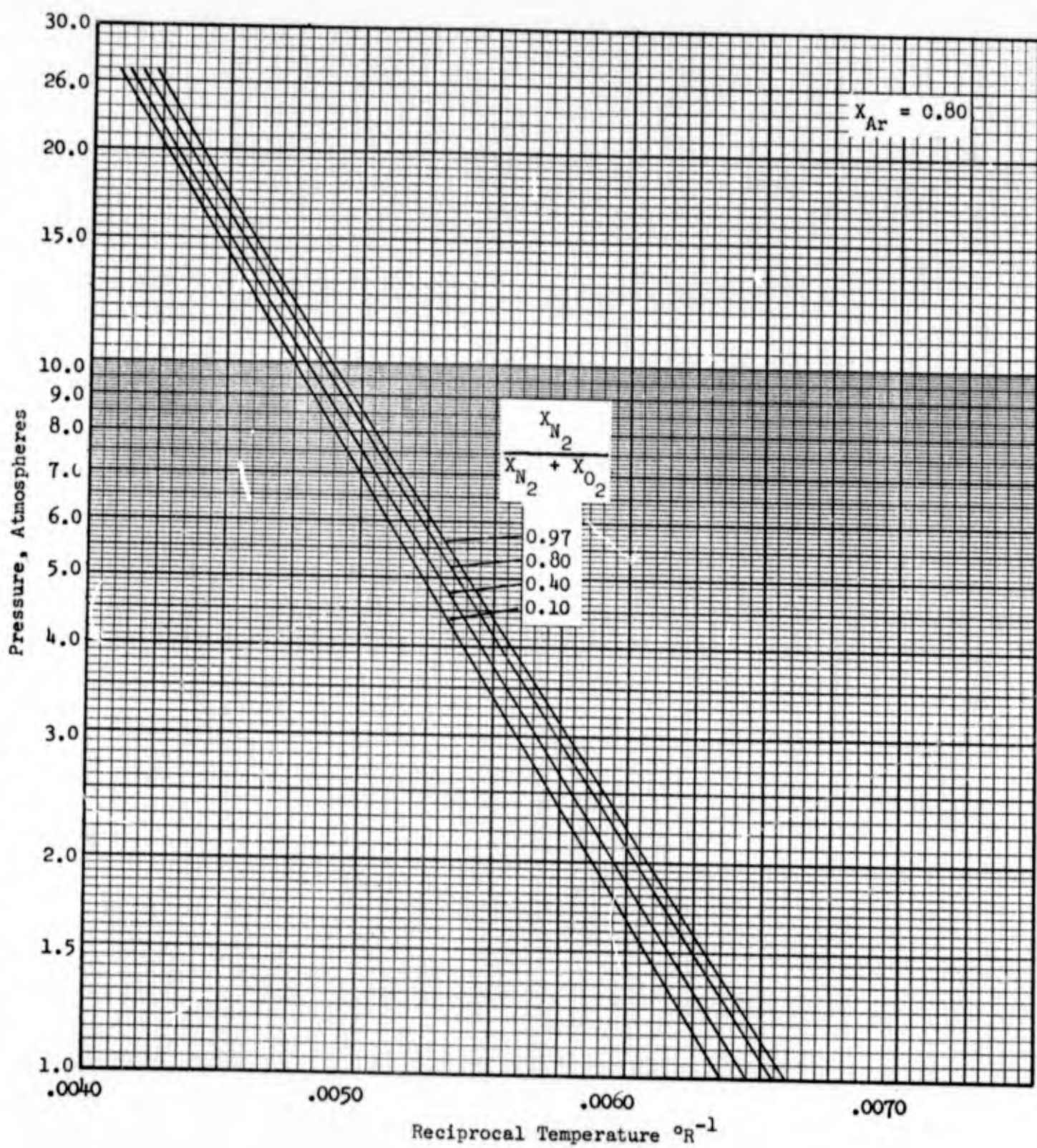


Figure 186. Vapor Pressures of Specific Mixtures of N_2 -Ar- O_2 .

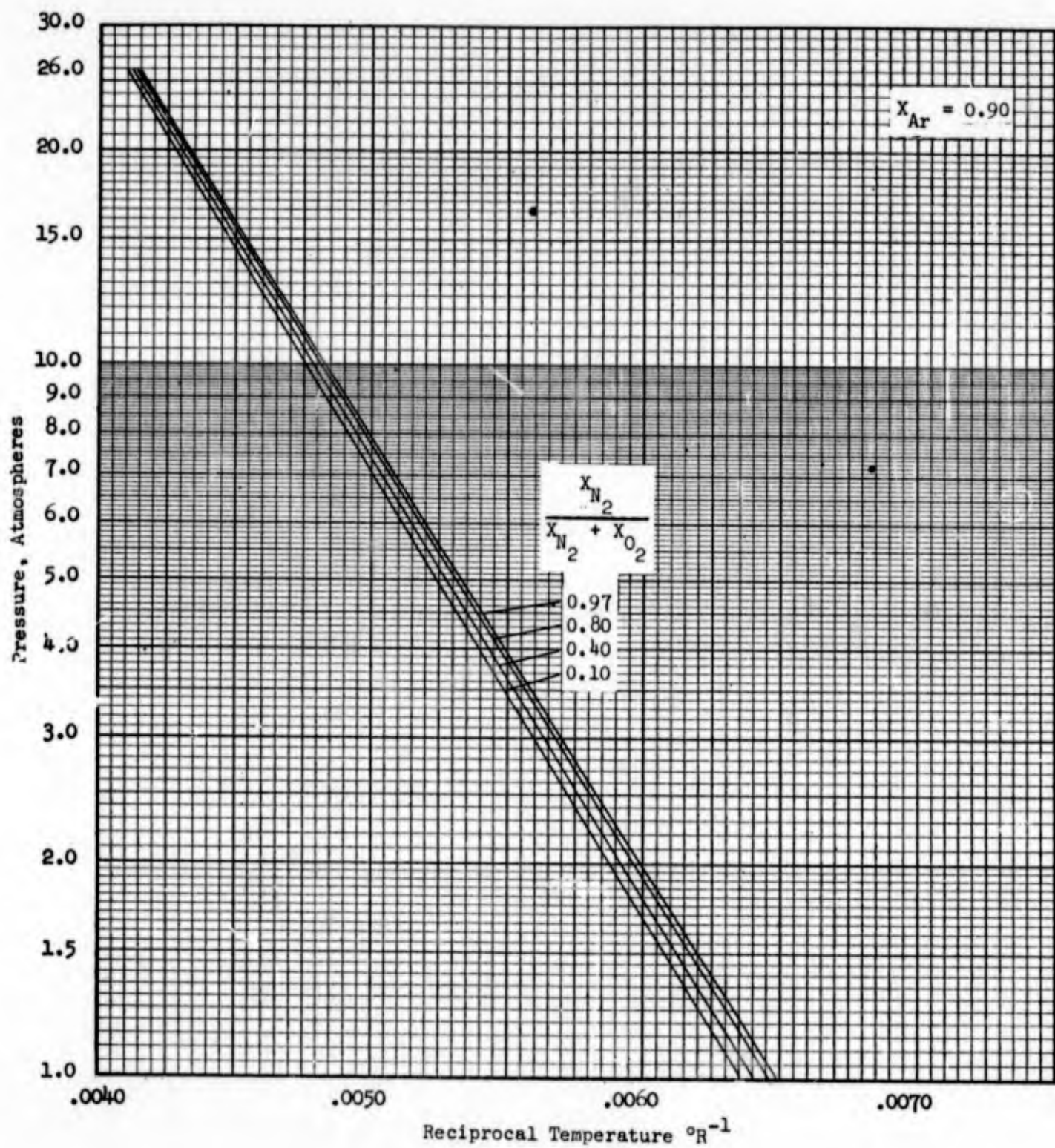


Figure 187. Vapor Pressures of Specific Mixtures of N_2 -Ar- O_2 .

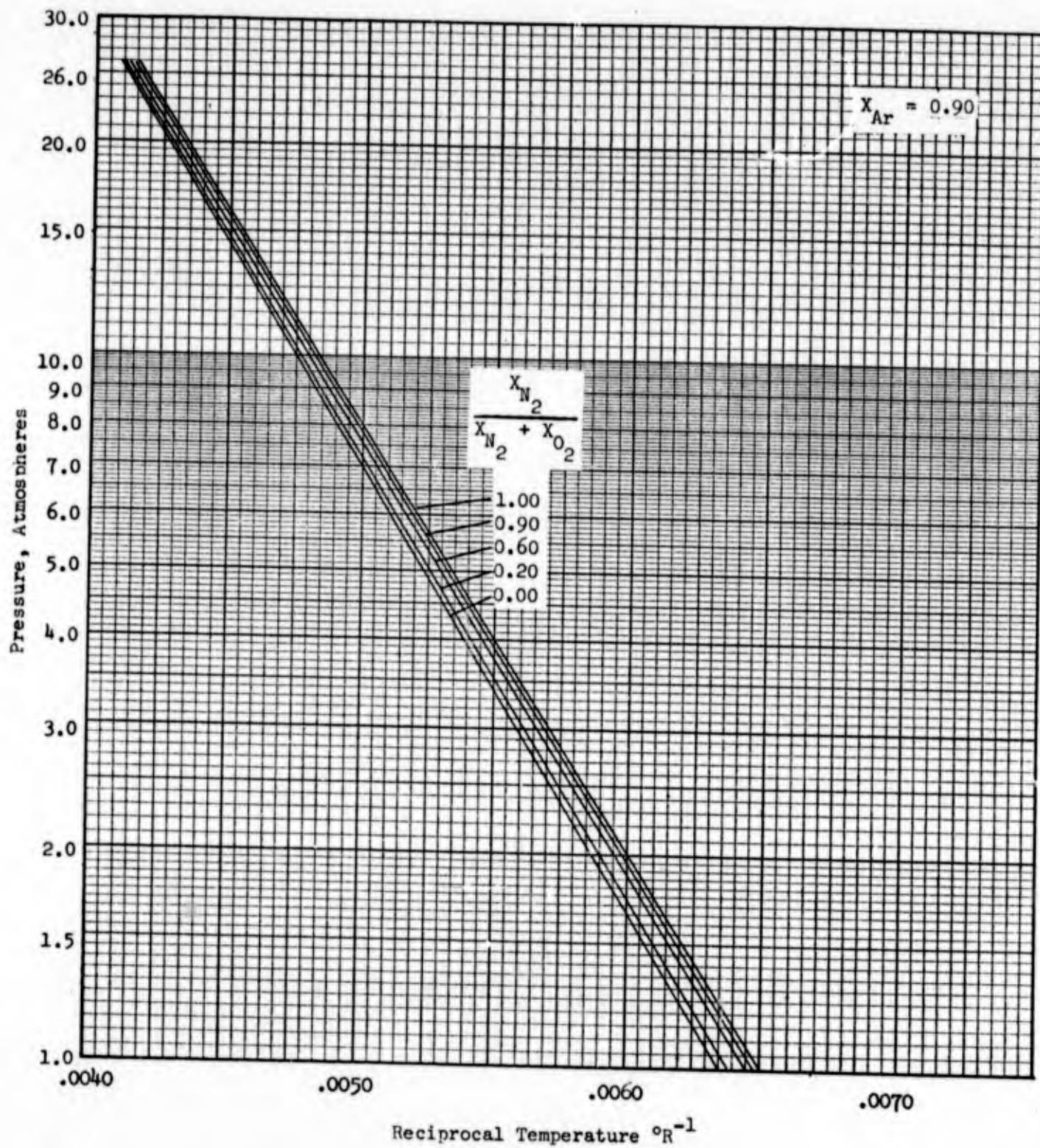


Figure 188. Vapor Pressures of Specific Mixtures of N_2 -Ar- O_2 .

APPENDIX II

TABULAR PRESENTATION OF CORRELATION

A. Isobaric Table

The table to follow presents values calculated at even pressure levels of 1, 2, 4, 6, 8, 10, 12, 14, 16, 18, 20, 23, and 26 atmospheres. They are arranged in order of increasing liquid mole fraction ratio

$$\frac{N_2}{N_2 + O_2}$$

and sub-ordered according to increasing mole fraction of argon. The quantities calculated are vapor composition, temperature, relative volatility, pressure, activity coefficient, enthalpy, and heat capacity.

Table 25. Isobaric Calculated Values

PRESSURE = 1. ATM.

LIQUID MOLE FRACTION			VAPOR MOLE FRACTION			TEMP	RELATIVE VOL			PRESSURE ACT COEF			ENTHALPY BTU/LB MOLE		HEAT CAPACITY BTU/LB MOLE-R	
N2/N2+O2	AR	O2	N2	AR	O2		R	N2/AR	N2/O2	AR/O2	N2	AR	O2	LIQ	VAP	LIQ
0.	0.	0.	0.	0.	1.0000	162.4	2.579	4.010	1.957	1.118	1.169	0.999	-1841.	1893.	13.2	7.486
0.	0.01	0.	0.0194	0.9805	162.3	2.581	4.007	1.953	1.117	1.161	1.000	-1844.	1897.	13.1	7.374	
0.	0.02	0.	0.0388	0.9694	162.2	2.584	4.004	1.948	1.115	1.158	1.000	-1847.	1902.	13.1	7.342	
0.	0.03	0.	0.0582	0.9584	162.1	2.587	4.001	1.944	1.113	1.155	1.000	-1850.	1907.	13.1	7.311	
0.	0.04	0.	0.0776	0.9474	162.0	2.590	3.998	1.940	1.112	1.151	1.001	-1853.	1911.	13.0	7.281	
0.	0.05	0.	0.0970	0.9364	161.9	2.592	3.995	1.935	1.110	1.148	1.001	-1856.	1916.	13.0	7.251	
0.	0.07	0.	0.1358	0.8972	161.7	2.613	3.989	1.926	1.107	1.142	1.002	-1860.	1926.	12.9	7.192	
0.	0.10	0.	0.1839	0.8581	161.5	2.629	3.979	1.913	1.103	1.132	1.003	-1866.	1941.	12.9	7.107	
0.	0.20	0.	0.2687	0.7313	161.7	2.602	3.941	1.869	1.091	1.104	1.010	-1893.	1997.	12.6	6.847	
0.	0.40	0.	0.4794	0.5204	159.4	2.784	3.852	1.802	1.076	1.090	1.024	-1936.	2024.	11.9	6.406	
0.	0.60	0.	0.6625	0.3399	158.5	2.888	3.744	1.727	1.078	1.026	1.072	-1978.	2062.	11.3	6.026	
0.	0.80	0.	0.8293	0.1707	157.7	2.991	3.632	1.614	1.087	1.008	1.127	-2019.	2077.	10.7	5.606	
0.	0.90	0.	0.9134	0.0865	157.9	3.042	3.572	1.474	1.099	1.003	1.162	-2032.	2079.	10.4	5.491	
0.10	0.	0.3135	0.	0.6865	157.7	2.621	4.111	1.948	1.103	1.148	1.014	-1834.	1899.	13.0	7.410	
0.10	0.01	0.3095	0.0119	0.6786	157.6	2.624	4.104	1.943	1.102	1.144	1.012	-1837.	1907.	13.1	7.386	
0.10	0.02	0.3056	0.0237	0.6707	157.4	2.631	4.100	1.938	1.100	1.141	1.012	-1840.	1913.	13.1	7.361	
0.10	0.03	0.3017	0.0354	0.6628	157.6	2.636	4.099	1.934	1.099	1.137	1.013	-1842.	1919.	13.1	7.337	
0.10	0.04	0.2978	0.0470	0.6549	157.4	2.641	4.096	1.930	1.098	1.134	1.013	-1844.	1925.	13.1	7.313	
0.10	0.05	0.2939	0.0585	0.6474	157.5	2.645	4.095	1.926	1.098	1.131	1.013	-1846.	1932.	13.0	7.289	
0.10	0.07	0.2863	0.0812	0.6393	157.9	2.659	4.074	1.924	1.094	1.144	1.014	-1851.	1924.	13.0	7.242	
0.10	0.10	0.2792	0.1145	0.6103	157.4	2.669	4.058	1.920	1.092	1.139	1.015	-1859.	1924.	12.9	7.173	
0.10	0.20	0.2389	0.2247	0.5304	157.2	2.717	4.003	1.873	1.080	1.104	1.022	-1880.	1990.	12.9	6.991	
0.10	0.40	0.1759	0.4170	0.4072	157.0	2.812	3.887	1.803	1.070	1.061	1.049	-1926.	2026.	11.9	6.646	
0.10	0.60	0.1169	0.6036	0.2709	156.9	2.904	3.764	1.724	1.072	1.029	1.082	-1969.	2071.	11.3	6.147	
0.10	0.80	0.0595	0.7933	0.1471	156.9	2.991	3.640	1.613	1.080	1.009	1.134	-2009.	2113.	10.7	5.746	
0.10	0.90	0.0033	0.8937	0.0763	157.1	3.048	3.576	1.473	1.099	1.004	1.166	-2032.	2113.	10.4	5.534	
0.20	0.	0.3995	0.	0.6005	154.0	2.641	4.199	1.973	1.088	1.171	1.026	-1814.	1899.	13.0	7.422	
0.20	0.01	0.3942	0.0096	0.5904	154.0	2.644	4.149	1.968	1.084	1.168	1.026	-1816.	1902.	13.0	7.402	
0.20	0.02	0.3898	0.0192	0.5819	154.0	2.651	4.143	1.963	1.083	1.164	1.026	-1819.	1909.	13.1	7.382	
0.20	0.03	0.3854	0.0288	0.5739	154.1	2.659	4.137	1.958	1.082	1.161	1.027	-1821.	1917.	13.1	7.362	
0.20	0.04	0.3810	0.0383	0.5663	154.1	2.666	4.131	1.953	1.081	1.158	1.027	-1824.	1924.	13.1	7.342	
0.20	0.05	0.3766	0.0477	0.5590	154.1	2.669	4.125	1.948	1.080	1.154	1.027	-1826.	1931.	13.0	7.322	
0.20	0.07	0.3722	0.0566	0.5520	154.1	2.674	4.112	1.938	1.078	1.148	1.028	-1828.	1938.	13.0	7.293	
0.20	0.10	0.3678	0.0646	0.5454	154.2	2.688	4.094	1.923	1.075	1.139	1.030	-1833.	1928.	13.0	7.224	
0.20	0.20	0.3483	0.1866	0.4051	154.3	2.735	4.032	1.874	1.068	1.110	1.036	-1863.	1981.	12.6	7.031	
0.20	0.40	0.3123	0.3680	0.3197	154.8	2.829	3.907	1.801	1.062	1.084	1.053	-1911.	2031.	11.9	6.646	
0.20	0.60	0.2742	0.5990	0.2286	155.4	2.921	3.779	1.729	1.060	1.032	1.093	-1958.	2077.	11.3	6.292	
0.20	0.80	0.2144	0.7602	0.1254	156.2	3.009	3.647	1.612	1.066	1.011	1.140	-2004.	2119.	10.7	5.917	
0.20	0.90	0.0993	0.8744	0.0663	156.7	3.092	3.588	1.473	1.089	1.004	1.168	-2032.	2119.	10.4	5.724	
0.40	0.	0.7333	0.	0.2667	148.7	2.629	4.194	1.969	1.095	1.187	1.009	-1748.	1877.	13.3	7.492	
0.40	0.01	0.7279	0.0076	0.2601	148.8	2.634	4.119	1.964	1.049	1.183	1.009	-1751.	1886.	13.3	7.427	
0.40	0.02	0.7226	0.0146	0.2539	148.8	2.644	4.114	1.959	1.049	1.179	1.009	-1754.	1894.	13.3	7.402	
0.40	0.03	0.7172	0.0216	0.2481	148.9	2.649	4.108	1.953	1.048	1.176	1.009	-1757.	1902.	13.3	7.377	
0.40	0.04	0.7118	0.0286	0.2422	148.9	2.659	4.103	1.948	1.048	1.172	1.009	-1760.	1911.	13.3	7.352	
0.40	0.05	0.7064	0.0356	0.2366	149.0	2.664	4.098	1.943	1.047	1.169	1.009	-1763.	1920.	13.3	7.327	
0.40	0.07	0.6996	0.0491	0.2293	149.1	2.667	4.087	1.933	1.047	1.162	1.009	-1766.	1929.	13.1	7.307	
0.40	0.10	0.6794	0.0703	0.2093	149.3	2.683	4.072	1.917	1.046	1.152	1.007	-1779.	1981.	13.0	7.301	
0.40	0.20	0.6244	0.1426	0.2331	149.9	2.737	4.010	1.868	1.044	1.122	1.071	-1819.	2044.	12.6	7.149	
0.40	0.40	0.5675	0.2977	0.1944	151.2	2.841	3.897	1.775	1.040	1.074	1.088	-1871.	2098.	11.9	6.811	
0.40	0.60	0.4743	0.4776	0.1402	152.0	2.930	3.788	1.709	1.042	1.039	1.116	-1932.	2095.	11.3	6.423	
0.40	0.80	0.3121	0.7010	0.0878	154.0	3.025	3.657	1.629	1.044	1.016	1.154	-1991.	2099.	10.7	5.944	
0.40	0.90	0.1141	0.8802	0.0777	155.9	3.092	3.586	1.474	1.069	1.008	1.177	-2032.	2104.	10.4	5.691	
0.60	0.	0.8648	0.	0.1352	144.0	2.679	3.993	1.991	1.084	1.218	1.026	-1843.	1876.	13.6	7.483	
0.60	0.01	0.8594	0.0096	0.1424	144.0	2.682	3.991	1.944	1.084	1.214	1.026	-1846.	1884.	13.6	7.471	
0.60	0.02	0.8542	0.0111	0.1416	144.1	2.689	3.986	1.941	1.084	1.210	1.025	-1849.	1892.	13.6	7.459	
0.60	0.03	0.8490	0.0167	0.1409	144.1	2.699	3.989	1.936	1.084	1.206	1.024	-1852.	1900.	13.6	7.446	
0.60	0.04	0.8437	0.0224	0.1402	144.2	2.698	3.983	1.931	1.084	1.202	1.024	-1855.	1908.	13.6	7.434	
0.60	0.05	0.8384	0.0280	0.1395	144.3	2.699	3.980	1.926	1.084	1.198	1.023	-1858.	1916.	13.6	7.421	
0.60	0.07	0.8327	0.0394	0.1388	144.5	2.698	3.979	1.916	1.083	1.190	1.023	-1862.	1924.	13.3	7.396	
0.60	0.10	0.8276	0.0566	0.1387	144.7	2.692	3.966	1.901	1.083	1.179	1.021	-1866.	1932.	13.0	7.397	
0.60	0.20	0.7957	0.1143	0.1390	146.5	2.767	3.937	1.854	1.079	1.148	1.020	-1744.	1948.	12.8	7.224	
0.60	0.40	0.6391	0.2907	0.1102	148.4	2.835	3.867	1.805	1.076	1.120	1.026	-1824.	2026.	12.6	6.926	
0.60	0.60	0.4930	0.4191	0.0871	150.0	2.949	3.777	1.803	1.074	1.049	1.043	-1923.	2088.	11.3	6.596	
0.60	0.80	0.3461	0.6900	0.0539	153.9	3.037	3.660	1.706	1.083	1.021	1.109	-1978.	2137.	10.7	6.259	
0.60	0.90	0.1647	0.8347	0.0366	159.2	3.071	3.592	1.478	1.099	1.013	1.185	-2032.	2144.	10.4	5.723	
0.80	0.	0.9284	0.	0.0716	142.0	2.761	3.811	1.984	1.013	1.273	1.014	-1876.	1940.	14.0	7.914	
0.80	0.01	0.9240	0.0047	0.0613	142.0	2.769	3.811	1.919	1.013	1.268	1.012	-1879.	1948.	13.9	7.903	
0.80	0.															

Table 20. (cont.)

PRESSURE = 2. ATH

LIQUID MOLE FRACTION		VAPOR MOLE FRACTION			TEMP	RELATIVE VOL			PRESSURE ACT COEF			ENTHALPY BTU/LB MOLE		HEAT CAPACITY BTU/LB MOLE-R	
N2/N2+O2	AR	N2	AR	O2		N2/AR	N2/O2	AR/O2	N2	A	O2	L10	VAP	L10	VAP
0.	0.	0.	0.	1.0000	175.3	2.307	3.368	1.460	1.002	1.136	0.999	-1670.	1159.	13.3	7.664
0.	0.01	0.	0.	0.0145	175.2	2.311	3.365	1.456	1.000	1.133	1.000	-1673.	1154.	13.3	7.634
0.	0.02	0.	0.	0.0288	175.1	2.315	3.363	1.452	1.000	1.130	1.000	-1677.	1148.	13.2	7.604
0.	0.03	0.	0.	0.0429	175.0	2.320	3.361	1.449	1.000	1.127	1.000	-1680.	1143.	13.1	7.575
0.	0.04	0.	0.	0.0568	174.9	2.324	3.358	1.445	1.000	1.125	1.001	-1683.	1137.	13.2	7.546
0.	0.05	0.	0.	0.0705	174.8	2.329	3.356	1.441	1.000	1.122	1.001	-1686.	1132.	13.2	7.517
0.	0.07	0.	0.	0.0974	174.6	2.337	3.351	1.434	1.000	1.116	1.002	-1692.	1122.	13.1	7.461
0.	0.10	0.	0.	0.1345	174.4	2.350	3.343	1.422	1.000	1.109	1.004	-1701.	1107.	13.0	7.379
0.	0.20	0.	0.	0.2572	173.6	2.392	3.313	1.385	1.040	1.004	1.010	-1730.	1061.	12.8	7.126
0.	0.40	0.	0.	0.4663	172.3	2.474	3.242	1.310	1.029	1.045	1.033	-1782.	983.	12.3	6.667
0.	0.60	0.	0.	0.6499	171.4	2.593	3.160	1.237	1.027	1.017	1.066	-1830.	916.	11.7	6.299
0.	0.80	0.	0.	0.8235	170.6	2.632	3.070	1.166	1.034	1.001	1.117	-1873.	854.	11.2	5.930
0.	0.90	0.	0.	0.9106	170.4	2.671	3.022	1.132	1.047	0.997	1.148	-1894.	824.	10.9	5.744
0.10	0.	0.2764	0.	0.7236	170.7	2.353	3.438	1.461	1.057	1.139	1.015	-1661.	1127.	13.4	7.678
0.10	0.01	0.2730	0.0117	0.7154	170.7	2.357	3.434	1.457	1.055	1.137	1.015	-1664.	1123.	13.4	7.648
0.10	0.02	0.2696	0.0233	0.7072	170.6	2.361	3.430	1.453	1.054	1.134	1.015	-1667.	1119.	13.3	7.619
0.10	0.03	0.2662	0.0348	0.6991	170.6	2.365	3.427	1.449	1.053	1.131	1.016	-1670.	1115.	13.3	7.590
0.10	0.04	0.2628	0.0462	0.6910	170.6	2.369	3.422	1.445	1.052	1.128	1.016	-1672.	1111.	13.3	7.561
0.10	0.05	0.2594	0.0576	0.6831	170.6	2.372	3.418	1.441	1.051	1.125	1.016	-1675.	1107.	13.3	7.532
0.10	0.07	0.2529	0.0800	0.6733	170.4	2.380	3.410	1.433	1.048	1.120	1.017	-1680.	1100.	13.2	7.511
0.10	0.10	0.2431	0.1130	0.6639	170.2	2.391	3.398	1.421	1.049	1.112	1.019	-1689.	1089.	13.1	7.441
0.10	0.20	0.2122	0.2185	0.5692	169.9	2.428	3.356	1.382	1.036	1.087	1.025	-1717.	1052.	12.8	7.219
0.10	0.40	0.1557	0.4192	0.4201	169.9	2.501	3.266	1.306	1.027	1.047	1.046	-1778.	985.	12.3	6.803
0.10	0.60	0.1034	0.6032	0.2934	169.9	2.572	3.173	1.234	1.027	1.020	1.078	-1820.	922.	11.7	6.403
0.10	0.80	0.0324	0.7941	0.1535	169.9	2.642	3.075	1.164	1.034	1.003	1.124	-1868.	860.	11.2	6.035
0.10	0.90	0.0266	0.8943	0.0791	170.0	2.676	3.025	1.130	1.048	0.998	1.152	-1891.	827.	10.9	5.780
0.20	0.	0.4844	0.	0.5156	167.0	2.380	3.460	1.457	1.045	1.143	1.032	-1641.	1101.	13.5	7.695
0.20	0.01	0.4896	0.0097	0.5103	167.0	2.384	3.454	1.453	1.045	1.140	1.032	-1644.	1098.	13.4	7.677
0.20	0.02	0.4948	0.0194	0.5050	167.0	2.387	3.450	1.449	1.044	1.137	1.032	-1647.	1095.	13.4	7.657
0.20	0.03	0.4499	0.0291	0.5210	167.0	2.391	3.445	1.445	1.043	1.134	1.033	-1650.	1092.	13.4	7.637
0.20	0.04	0.4452	0.0387	0.5161	167.0	2.394	3.440	1.441	1.042	1.131	1.033	-1653.	1089.	13.3	7.616
0.20	0.05	0.4404	0.0483	0.5113	167.0	2.398	3.434	1.437	1.041	1.128	1.033	-1656.	1086.	13.3	7.596
0.20	0.07	0.4359	0.0674	0.5016	167.1	2.405	3.426	1.429	1.039	1.123	1.034	-1661.	1080.	13.3	7.559
0.20	0.10	0.4169	0.0959	0.4873	167.1	2.416	3.422	1.417	1.037	1.119	1.035	-1670.	1071.	13.2	7.495
0.20	0.20	0.3710	0.1802	0.4397	167.3	2.451	3.375	1.377	1.030	1.090	1.041	-1698.	1042.	12.9	7.296
0.20	0.40	0.2823	0.3734	0.3444	167.7	2.520	3.270	1.301	1.023	1.050	1.060	-1754.	985.	12.3	6.902
0.20	0.60	0.1939	0.5622	0.2439	168.4	2.587	3.180	1.229	1.024	1.022	1.090	-1809.	927.	11.7	6.496
0.20	0.80	0.1016	0.7665	0.1320	169.1	2.651	3.079	1.162	1.039	1.005	1.131	-1862.	865.	11.2	6.056
0.20	0.90	0.0323	0.8785	0.0692	169.6	2.681	3.027	1.129	1.048	0.999	1.156	-1888.	831.	10.9	5.814
0.40	0.	0.6964	0.	0.3036	161.3	2.380	3.441	1.441	1.021	1.154	1.075	-1578.	1041.	13.9	7.747
0.40	0.01	0.6911	0.0073	0.3016	161.4	2.383	3.437	1.437	1.020	1.151	1.074	-1582.	1039.	13.9	7.731
0.40	0.02	0.6858	0.0146	0.2996	161.5	2.387	3.433	1.433	1.020	1.148	1.074	-1585.	1037.	13.9	7.714
0.40	0.03	0.6805	0.0219	0.2976	161.5	2.391	3.429	1.429	1.019	1.145	1.075	-1588.	1035.	13.9	7.698
0.40	0.04	0.6751	0.0292	0.2956	161.6	2.395	3.425	1.425	1.019	1.142	1.075	-1592.	1033.	13.4	7.682
0.40	0.05	0.6698	0.0366	0.2936	161.6	2.399	3.421	1.421	1.018	1.139	1.075	-1596.	1031.	13.4	7.666
0.40	0.07	0.6591	0.0513	0.2896	161.8	2.417	3.413	1.412	1.017	1.134	1.075	-1603.	1024.	13.3	7.633
0.40	0.10	0.6429	0.0735	0.2839	162.0	2.429	3.401	1.401	1.016	1.129	1.075	-1613.	1012.	13.2	7.584
0.40	0.20	0.5883	0.1490	0.2624	162.6	2.488	3.360	1.362	1.014	1.100	1.079	-1648.	1023.	12.9	7.410
0.40	0.40	0.4731	0.3102	0.2167	164.1	2.542	3.279	1.288	1.015	1.059	1.092	-1716.	982.	12.3	7.051
0.40	0.60	0.3438	0.4942	0.1620	165.7	2.609	3.193	1.220	1.024	1.029	1.114	-1784.	933.	11.7	6.656
0.40	0.80	0.1910	0.7162	0.0929	167.7	2.666	3.084	1.157	1.039	1.008	1.145	-1858.	874.	11.2	6.169
0.40	0.90	0.1014	0.8984	0.0382	168.9	2.690	3.030	1.127	1.049	1.001	1.163	-1881.	837.	10.9	5.901
0.60	0.	0.8536	0.	0.1464	157.2	2.359	3.338	1.415	1.000	1.160	1.135	-1497.	1031.	13.6	7.797
0.60	0.01	0.8286	0.0059	0.1656	157.3	2.364	3.336	1.411	1.000	1.157	1.134	-1499.	1031.	13.6	7.779
0.60	0.02	0.8236	0.0118	0.1647	157.4	2.368	3.334	1.408	1.000	1.154	1.134	-1501.	1029.	13.6	7.764
0.60	0.03	0.8185	0.0178	0.1638	157.5	2.372	3.332	1.404	1.000	1.151	1.133	-1505.	1028.	13.6	7.750
0.60	0.04	0.8134	0.0237	0.1629	157.6	2.377	3.330	1.400	0.999	1.148	1.133	-1510.	1027.	13.9	7.735
0.60	0.05	0.8083	0.0297	0.1619	157.6	2.383	3.328	1.396	0.999	1.145	1.133	-1514.	1026.	13.9	7.721
0.60	0.07	0.7981	0.0418	0.1601	157.8	2.393	3.324	1.389	0.999	1.142	1.132	-1519.	1024.	13.9	7.720
0.60	0.10	0.7826	0.0602	0.1573	158.1	2.400	3.317	1.378	0.999	1.139	1.131	-1527.	1022.	13.4	7.700
0.60	0.20	0.7289	0.1237	0.1475	159.0	2.456	3.294	1.341	1.000	1.110	1.120	-1540.	1010.	13.3	7.657
0.60	0.40	0.6089	0.2658	0.1293	161.0	2.545	3.241	1.273	1.000	1.100	1.120	-1584.	1005.	13.1	7.510
0.60	0.60	0.4622	0.4407	0.0971	163.4	2.622	3.172	1.210	1.007	1.072	1.130	-1671.	975.	12.3	7.183
0.60	0.80	0.2699	0.6717	0.0583	166.4	2.679	3.085	1.152	1.021	1.037	1.141	-1755.	936.	11.7	6.786
0.60	0.90	0.1475	0.8201	0.0324	168.2	2.698	3.033	1.124	1.040	1.013	1.160	-1837.	880.	11.2	6.270
0.80	0.	0.9274	0.	0.0726	154.0	2.366	3.192	1.384	1.000	1.064	1.171	-1676.	942.	10.9	5.944
0.80	0.01	0.9227	0.0050	0.0723	154.0	2.363	3.189	1.380	0.999	1.061	1.170	-1679.	940.	10.9	5.928
0.80	0.02	0.9180	0.0101	0.0719	154.1	2.369	3.183	1.377	0.999	1.058	1.169	-1682.	938.	10.9	5.912
0.80	0.03	0.9133	0.0152	0.0715	154.2	2.375	3.177	1.374	0.999	1.055	1.168	-1685.	936.	10.9	5.896
0.80	0.04	0.9086	0.0203	0.0711	154.3	2.381	3.171	1.370	0.999	1.052	1.167	-1688.	934.	10.9	5.880
0.80	0.05	0.9038	0.0254	0.0707	154.4	2.387	3.165	1.367	0.999	1.049	1.166	-1691.	932.	10.9	5.864
0.80	0.07	0.8942	0.0398	0.0700	154.6	2.399	3.155	1.358	0.999	1.046	1.165	-1696.	929.	10.9	5.848
0.80	0.10	0.8796	0.0516	0.0688	154.9	2.407	3.145	1.350	0.999	1.043	1.164	-1701.	926.	10.9	5.832
0.80	0.20	0.8285	0.1067	0.0648	156.0	2.426	3.106	1.309	0.999	1.040	1.164	-1709.	920.	10.9	5.795
0.80	0.40	0.7106	0.2336	0.0590	158.4	2.535	3.084	1.317	0.992	1.140	1.191	-1513.	989.	13.0	7.519
0.80	0.60	0.5976	0.3941												

LIQUID MOLE FRACTION		VAPOR MOLE FRACTION			TEMP	RELATIVE VOL			PRESSURE ACT COEF			ENTHALPY BTU/LB MOLE		HEAT CAPACITY BTU/LB MOLE-R	
N2/N2+O2	AR	N2	AR	O2		R	N2/AR	N2/O2	AR/O2	N2	AR	O2	LIO	VAP	LIO
0.	0.	0.	0.	1.0000	190.6	2.020	2.776	1.375	0.981	1.111	1.000	-1466.	1224.	13.4	8.122
0.	0.01	0.	0.	0.0137	190.5	2.023	2.775	1.372	0.986	1.109	1.001	-1470.	1218.	13.4	8.694
0.	0.02	0.	0.	0.0272	190.4	2.026	2.773	1.369	0.985	1.106	1.001	-1473.	1212.	13.4	8.665
0.	0.03	0.	0.	0.0405	190.3	2.030	2.772	1.366	0.985	1.104	1.002	-1477.	1207.	13.4	8.637
0.	0.04	0.	0.	0.0537	190.2	2.033	2.770	1.362	0.984	1.102	1.002	-1480.	1201.	13.4	8.610
0.	0.05	0.	0.	0.0668	190.1	2.037	2.768	1.359	0.983	1.100	1.003	-1484.	1196.	13.3	7.982
0.	0.07	0.	0.	0.0924	189.9	2.043	2.765	1.353	0.982	1.096	1.004	-1489.	1191.	13.3	7.959
0.	0.10	0.	0.	0.1299	189.6	2.053	2.759	1.344	0.980	1.089	1.005	-1500.	1185.	13.3	7.929
0.	0.20	0.	0.	0.2471	188.8	2.084	2.738	1.313	0.974	1.070	1.013	-1533.	1121.	13.1	7.605
0.	0.40	0.	0.	0.4548	187.5	2.148	2.688	1.251	0.967	1.038	1.034	-1593.	1037.	12.7	7.166
0.	0.60	0.	0.	0.6410	186.5	2.207	2.627	1.190	0.967	1.016	1.066	-1647.	964.	12.3	6.771
0.	0.80	0.	0.	0.8190	185.8	2.264	2.560	1.131	0.976	1.003	1.110	-1698.	896.	11.9	6.389
0.	0.90	0.	0.	0.9044	185.5	2.292	2.524	1.101	0.983	1.000	1.137	-1723.	862.	11.8	6.196
0.10	0.	0.2393	0.	0.7407	186.2	2.063	2.831	1.372	0.994	1.120	1.020	-1452.	1193.	13.7	8.150
0.10	0.01	0.2363	0.0116	0.7521	186.1	2.066	2.828	1.369	0.994	1.117	1.021	-1455.	1188.	13.6	8.126
0.10	0.02	0.2334	0.0230	0.7434	186.1	2.069	2.825	1.365	0.993	1.115	1.021	-1459.	1184.	13.6	8.102
0.10	0.03	0.2305	0.0344	0.7351	186.0	2.072	2.822	1.362	0.992	1.113	1.021	-1462.	1180.	13.6	8.078
0.10	0.04	0.2277	0.0457	0.7267	186.0	2.075	2.820	1.359	0.991	1.110	1.022	-1465.	1175.	13.6	8.054
0.10	0.05	0.2248	0.0569	0.7183	186.0	2.078	2.817	1.356	0.990	1.108	1.022	-1469.	1171.	13.5	8.031
0.10	0.07	0.2192	0.0792	0.7017	185.9	2.083	2.811	1.349	0.988	1.104	1.023	-1479.	1163.	13.5	7.984
0.10	0.10	0.2109	0.1120	0.6772	185.8	2.092	2.802	1.340	0.986	1.097	1.024	-1489.	1155.	13.4	7.915
0.10	0.20	0.1843	0.2174	0.5983	185.5	2.119	2.772	1.308	0.979	1.077	1.030	-1517.	1118.	13.2	7.691
0.10	0.40	0.1353	0.4150	0.4497	185.2	2.173	2.707	1.246	0.971	1.044	1.049	-1578.	1037.	12.8	7.269
0.10	0.60	0.0896	0.6045	0.3054	185.0	2.224	2.638	1.186	0.971	1.020	1.078	-1637.	968.	12.4	6.846
0.10	0.80	0.0492	0.7961	0.1588	185.1	2.273	2.564	1.129	0.978	1.008	1.117	-1693.	900.	12.0	6.444
0.10	0.90	0.0229	0.8957	0.0814	185.2	2.294	2.526	1.100	0.985	1.002	1.141	-1720.	865.	11.8	6.246
0.20	0.	0.4170	0.	0.5831	182.4	2.094	2.861	1.366	0.997	1.128	1.041	-1431.	1166.	13.8	8.119
0.20	0.01	0.4126	0.0099	0.5776	182.4	2.097	2.857	1.363	0.996	1.125	1.041	-1434.	1162.	13.8	8.101
0.20	0.02	0.4082	0.0198	0.5721	182.4	2.100	2.854	1.359	0.995	1.123	1.042	-1438.	1159.	13.8	8.146
0.20	0.03	0.4038	0.0297	0.5666	182.4	2.102	2.851	1.356	0.994	1.120	1.042	-1441.	1155.	13.8	8.125
0.20	0.04	0.3994	0.0395	0.5611	182.4	2.105	2.847	1.353	0.993	1.118	1.042	-1445.	1152.	13.7	8.104
0.20	0.05	0.3951	0.0493	0.5557	182.4	2.107	2.844	1.349	0.992	1.116	1.042	-1448.	1149.	13.7	8.083
0.20	0.07	0.3864	0.0688	0.5444	182.4	2.112	2.837	1.343	0.990	1.113	1.043	-1455.	1142.	13.7	8.041
0.20	0.10	0.3735	0.0979	0.5286	182.5	2.120	2.827	1.333	0.988	1.104	1.044	-1465.	1132.	13.6	7.978
0.20	0.20	0.3316	0.1932	0.4752	182.6	2.145	2.792	1.301	0.982	1.083	1.049	-1498.	1099.	13.3	7.771
0.20	0.40	0.2566	0.3868	0.3666	183.0	2.194	2.720	1.240	0.974	1.049	1.065	-1562.	1035.	12.9	7.363
0.20	0.60	0.1760	0.5714	0.2588	183.6	2.239	2.645	1.181	0.974	1.024	1.090	-1625.	971.	12.4	6.944
0.20	0.80	0.0883	0.7742	0.1374	184.3	2.291	2.568	1.124	0.980	1.008	1.124	-1687.	904.	12.0	6.497
0.20	0.90	0.0452	0.8834	0.0715	184.8	2.301	2.529	1.099	0.986	1.003	1.145	-1717.	867.	11.8	6.255
0.40	0.	0.6560	0.	0.3441	176.3	2.124	2.890	1.346	0.992	1.146	1.090	-1372.	1121.	14.1	8.277
0.40	0.01	0.6506	0.0077	0.3417	176.4	2.127	2.886	1.343	0.991	1.143	1.090	-1376.	1119.	14.0	8.260
0.40	0.02	0.6453	0.0155	0.3393	176.4	2.129	2.883	1.340	0.991	1.140	1.090	-1380.	1117.	14.0	8.242
0.40	0.03	0.6400	0.0232	0.3369	176.5	2.132	2.880	1.337	0.990	1.138	1.090	-1384.	1115.	14.0	8.224
0.40	0.04	0.6347	0.0310	0.3345	176.5	2.135	2.876	1.333	0.990	1.135	1.090	-1387.	1112.	13.9	8.206
0.40	0.05	0.6293	0.0387	0.3321	176.6	2.137	2.873	1.330	0.989	1.133	1.090	-1391.	1110.	13.9	8.188
0.40	0.07	0.6186	0.0543	0.3271	176.8	2.143	2.857	1.324	0.988	1.128	1.090	-1399.	1108.	13.9	8.153
0.40	0.10	0.6025	0.0778	0.3197	177.0	2.151	2.827	1.315	0.986	1.120	1.090	-1410.	1099.	13.8	8.098
0.40	0.20	0.5482	0.1575	0.2943	177.7	2.176	2.794	1.284	0.982	1.098	1.091	-1449.	1077.	13.5	7.915
0.40	0.40	0.4348	0.3259	0.2393	179.2	2.223	2.725	1.226	0.979	1.061	1.100	-1525.	1029.	13.0	7.527
0.40	0.60	0.3104	0.5141	0.1756	180.9	2.264	2.652	1.171	0.979	1.033	1.110	-1600.	975.	12.5	7.095
0.40	0.80	0.1684	0.7334	0.0942	182.9	2.297	2.573	1.120	0.985	1.013	1.139	-1674.	915.	12.0	6.597
0.40	0.90	0.0802	0.8595	0.0523	184.1	2.309	2.531	1.096	0.989	1.008	1.153	-1718.	872.	11.8	6.312
0.60	0.	0.8076	0.	0.1924	171.7	2.120	2.798	1.320	0.986	1.173	1.194	-1296.	1086.	14.2	8.369
0.60	0.01	0.8023	0.0064	0.1913	171.8	2.123	2.796	1.317	0.986	1.170	1.193	-1301.	1084.	14.2	8.354
0.60	0.02	0.7971	0.0127	0.1902	171.9	2.127	2.794	1.314	0.985	1.167	1.192	-1305.	1083.	14.1	8.338
0.60	0.03	0.7918	0.0192	0.1891	172.0	2.130	2.792	1.311	0.985	1.164	1.192	-1310.	1082.	14.1	8.322
0.60	0.04	0.7865	0.0256	0.1879	172.1	2.133	2.790	1.308	0.985	1.161	1.191	-1315.	1080.	14.1	8.306
0.60	0.05	0.7812	0.0321	0.1868	172.2	2.137	2.788	1.305	0.984	1.159	1.190	-1319.	1079.	14.0	8.289
0.60	0.07	0.7704	0.0451	0.1845	172.4	2.143	2.784	1.299	0.984	1.153	1.189	-1329.	1076.	14.0	8.257
0.60	0.10	0.7542	0.0649	0.1810	172.6	2.153	2.778	1.290	0.983	1.144	1.188	-1343.	1072.	13.9	8.208
0.60	0.20	0.6808	0.1332	0.1604	173.7	2.184	2.747	1.262	0.981	1.119	1.183	-1389.	1056.	13.6	8.038
0.60	0.40	0.5739	0.2848	0.1413	175.9	2.239	2.704	1.209	0.980	1.076	1.181	-1482.	1021.	13.0	7.664
0.60	0.60	0.4261	0.4667	0.1073	178.5	2.283	2.648	1.160	0.984	1.043	1.185	-1573.	976.	12.5	7.228
0.60	0.80	0.2413	0.6943	0.0629	181.6	2.311	2.574	1.115	0.989	1.019	1.195	-1661.	916.	12.0	6.690
0.60	0.90	0.1293	0.8347	0.0340	183.4	2.317	2.533	1.093	0.992	1.009	1.161	-1734.	876.	11.8	6.367
0.80	0.	0.9152	0.	0.0848	168.0	2.095	2.699	1.288	0.986	1.216	1.239	-1109.	1057.	14.3	8.462
0.80	0.01	0.9102	0.0095	0.0843	168.1	2.099	2.699	1.286	0.986	1.212	1.237	-1115.	1056.	14.2	8.447
0.80	0.02	0.9052	0.0181	0.0839	168.2	2.103	2.699	1.283	0						

LIQUID MOLE FRACTION		VAPOR MOLE FRACTION			TEMP	RELATIVE VOL			PRESSURE ACT COEF			ENTHALPY		HEAT CAPACITY	
N2/N2+O2	AR	N2	AR	O2		R	N2/AR	N2/O2	AR/O2	N2	AR	O2	LIQ	VAP	LIQ
0.	0.	0.	0.	1.0000	200.9	1.851	2.453	1.325	0.931	1.094	1.001	-1327.	1256.	13.6	8.566
0.	0.01	0.	0.	0.0132	200.8	1.853	2.452	1.323	0.931	1.092	1.002	-1331.	1251.	13.6	8.538
0.	0.02	0.	0.	0.0262	200.7	1.856	2.450	1.320	0.930	1.090	1.002	-1334.	1245.	13.6	8.511
0.	0.03	0.	0.	0.0391	200.6	1.859	2.448	1.317	0.930	1.089	1.003	-1338.	1239.	13.6	8.484
0.	0.04	0.	0.	0.0519	200.5	1.862	2.446	1.315	0.929	1.087	1.003	-1342.	1234.	13.6	8.457
0.	0.05	0.	0.	0.0646	200.4	1.865	2.444	1.312	0.928	1.085	1.004	-1345.	1228.	13.6	8.430
0.	0.06	0.	0.	0.0895	200.2	1.870	2.444	1.307	0.928	1.082	1.005	-1349.	1223.	13.6	8.403
0.	0.07	0.	0.	0.1241	199.9	1.878	2.439	1.299	0.928	1.078	1.007	-1352.	1217.	13.6	8.376
0.	0.10	0.	0.	0.2412	199.1	1.905	2.422	1.272	0.925	1.076	1.007	-1363.	1201.	13.6	8.302
0.	0.20	0.	0.	0.4481	197.8	1.956	2.361	1.218	0.919	1.074	1.015	-1397.	1151.	13.4	8.080
0.	0.40	0.	0.	0.6358	196.8	2.004	2.332	1.164	0.920	1.074	1.036	-1440.	1063.	13.1	7.823
0.	0.60	0.	0.	0.8163	196.0	2.049	2.277	1.111	0.928	1.070	1.066	-1519.	986.	12.8	7.223
0.	0.80	0.	0.	0.9972	195.7	2.071	2.247	1.085	0.935	1.063	1.132	-1599.	913.	12.6	6.833
0.	0.90	0.	0.	0.2172	196.6	1.888	2.497	1.322	0.945	1.108	1.024	-1308.	1227.	13.6	8.468
0.10	0.01	0.2145	0.0115	0.7740	196.6	1.891	2.494	1.319	0.945	1.106	1.025	-1311.	1222.	13.6	8.504
0.10	0.02	0.2119	0.0228	0.7653	196.5	1.893	2.492	1.317	0.944	1.104	1.025	-1315.	1217.	13.6	8.560
0.10	0.03	0.2093	0.0342	0.7566	196.5	1.895	2.490	1.314	0.943	1.102	1.025	-1319.	1213.	13.6	8.596
0.10	0.04	0.2067	0.0454	0.7479	196.4	1.898	2.488	1.311	0.943	1.100	1.026	-1322.	1208.	13.6	8.632
0.10	0.05	0.2042	0.0566	0.7393	196.4	1.900	2.486	1.308	0.942	1.098	1.026	-1326.	1204.	13.6	8.668
0.10	0.07	0.1991	0.0787	0.7223	196.2	1.912	2.474	1.303	0.941	1.094	1.027	-1333.	1195.	13.6	8.447
0.10	0.10	0.1916	0.1114	0.6971	195.9	1.934	2.459	1.294	0.939	1.088	1.029	-1343.	1182.	13.6	8.371
0.10	0.20	0.1676	0.2166	0.6157	195.5	1.978	2.398	1.212	0.933	1.070	1.035	-1378.	1139.	13.6	8.148
0.10	0.40	0.1231	0.4149	0.4620	195.3	2.018	2.341	1.160	0.926	1.061	1.053	-1444.	1062.	13.2	7.722
0.10	0.60	0.0815	0.6954	0.3132	195.3	2.018	2.341	1.160	0.926	1.061	1.053	-1444.	1062.	13.2	7.722
0.10	0.80	0.0410	0.7972	0.1618	195.3	2.037	2.291	1.109	0.932	1.058	1.114	-1507.	986.	12.9	7.306
0.10	0.90	0.0207	0.8960	0.0227	195.4	2.075	2.249	1.064	0.937	1.054	1.136	-1596.	916.	12.6	6.803
0.20	0.	0.3870	0.	0.6130	192.0	1.918	2.525	1.317	0.955	1.120	1.046	-1289.	1199.	14.2	8.663
0.20	0.01	0.3829	0.0101	0.6070	192.0	1.920	2.523	1.314	0.955	1.118	1.049	-1290.	1195.	14.1	8.641
0.20	0.02	0.3787	0.0201	0.6012	192.0	1.922	2.520	1.311	0.954	1.116	1.049	-1292.	1192.	14.1	8.619
0.20	0.03	0.3746	0.0301	0.5953	192.0	1.924	2.517	1.308	0.953	1.114	1.049	-1294.	1189.	14.1	8.597
0.20	0.04	0.3705	0.0401	0.5894	192.0	1.927	2.514	1.305	0.952	1.112	1.049	-1297.	1184.	14.1	8.576
0.20	0.05	0.3664	0.0500	0.5836	192.9	1.929	2.512	1.302	0.951	1.110	1.050	-1303.	1181.	14.1	8.554
0.20	0.07	0.3583	0.0698	0.5719	192.9	1.939	2.498	1.290	0.948	1.099	1.051	-1310.	1173.	14.0	8.511
0.20	0.10	0.3463	0.0892	0.5549	193.0	1.959	2.469	1.260	0.942	1.080	1.056	-1321.	1162.	14.0	8.447
0.20	0.20	0.3069	0.1998	0.4973	193.4	1.997	2.410	1.207	0.934	1.049	1.070	-1357.	1127.	13.8	8.235
0.20	0.40	0.2318	0.3896	0.3834	193.9	2.032	2.348	1.155	0.932	1.027	1.070	-1427.	1059.	13.4	7.815
0.20	0.60	0.1844	0.5772	0.2664	194.6	2.064	2.284	1.106	0.935	1.011	1.122	-1495.	990.	13.0	7.306
0.20	0.80	0.1409	0.7749	0.1408	195.0	2.079	2.250	1.083	0.939	1.008	1.140	-1593.	901.	12.2	6.888
0.20	0.90	0.1028	0.8863	0.0720	195.0	2.095	2.209	1.063	0.946	1.004	1.160	-1686.	825.	12.0	6.488
0.40	0.	0.6232	0.0000	0.3668	186.5	1.955	2.537	1.298	0.966	1.144	1.103	-1226.	1152.	14.9	8.794
0.40	0.01	0.6178	0.0101	0.3611	186.7	1.959	2.532	1.292	0.965	1.141	1.103	-1230.	1149.	14.9	8.775
0.40	0.02	0.6125	0.0202	0.3553	186.7	1.961	2.529	1.289	0.965	1.139	1.102	-1234.	1147.	14.9	8.756
0.40	0.03	0.6072	0.0302	0.3496	186.8	1.963	2.526	1.287	0.964	1.137	1.102	-1238.	1144.	14.9	8.737
0.40	0.04	0.6019	0.0403	0.3439	186.9	1.965	2.523	1.284	0.963	1.135	1.102	-1242.	1142.	14.4	8.718
0.40	0.05	0.5966	0.0504	0.3382	187.0	1.966	2.518	1.279	0.963	1.134	1.102	-1246.	1140.	14.4	8.698
0.40	0.07	0.5892	0.0698	0.3325	187.2	1.975	2.509	1.271	0.961	1.130	1.102	-1255.	1135.	14.4	8.660
0.40	0.10	0.5792	0.1034	0.3153	187.9	1.994	2.480	1.244	0.959	1.123	1.102	-1267.	1127.	14.3	8.602
0.40	0.20	0.4896	0.3366	0.2939	189.5	2.028	2.420	1.193	0.954	1.101	1.102	-1308.	1103.	14.0	8.495
0.40	0.40	0.2891	0.5270	0.1840	191.2	2.057	2.357	1.146	0.946	1.086	1.108	-1389.	1051.	13.6	7.991
0.40	0.60	0.1946	0.7441	0.1014	193.2	2.074	2.289	1.101	0.942	1.070	1.120	-1469.	993.	13.1	7.538
0.40	0.80	0.1003	0.8662	0.0335	194.3	2.086	2.253	1.080	0.943	1.068	1.140	-1548.	924.	12.7	7.027
0.60	0.	0.7895	0.	0.2105	181.9	1.945	2.501	1.273	0.973	1.180	1.171	-1153.	1112.	14.8	8.939
0.60	0.01	0.7841	0.0047	0.2092	181.6	1.947	2.499	1.270	0.973	1.177	1.170	-1156.	1110.	14.7	8.921
0.60	0.02	0.7787	0.0134	0.2079	181.7	1.949	2.497	1.268	0.972	1.174	1.169	-1160.	1107.	14.7	8.902
0.60	0.03	0.7732	0.0222	0.2066	181.8	1.952	2.495	1.265	0.971	1.171	1.169	-1164.	1104.	14.7	8.884
0.60	0.04	0.7677	0.0310	0.2053	182.0	1.954	2.493	1.263	0.971	1.169	1.168	-1168.	1101.	14.7	8.866
0.60	0.05	0.7622	0.0398	0.2040	182.1	1.957	2.491	1.260	0.970	1.167	1.167	-1172.	1098.	14.6	8.848
0.60	0.07	0.7511	0.0476	0.2013	182.3	1.961	2.487	1.255	0.969	1.160	1.165	-1187.	1085.	14.6	8.811
0.60	0.10	0.7343	0.0644	0.1971	182.6	1.968	2.481	1.248	0.967	1.152	1.163	-1202.	1077.	14.5	8.755
0.60	0.20	0.6765	0.1402	0.1833	183.7	2.011	2.460	1.224	0.963	1.127	1.150	-1259.	1006.	14.2	8.364
0.60	0.40	0.5499	0.2982	0.1519	186.1	2.049	2.413	1.170	0.956	1.085	1.151	-1347.	1041.	13.7	8.151
0.60	0.60	0.4021	0.4842	0.1137	188.8	2.076	2.358	1.135	0.952	1.051	1.150	-1441.	992.	13.2	7.677
0.60	0.80	0.2233	0.7117	0.0649	191.9	2.092	2.292	1.096	0.949	1.024	1.154	-1534.	929.	12.7	7.117
0.60	0.90	0.1182	0.8469	0.0369	193.6	2.094	2.256	1.077	0.946	1.013	1.156	-1628.	860.	12.5	6.792
0.80	0.	0.9068	0.	0.0933	177.4	1.954	2.431	1.244	0.984	1.224	1.250	-1071.	1076.	14.0	9.080
0.80	0.01	0.9015	0.0098	0.0927	177.6	1.957	2.430	1.241	0.983	1.223	1.250	-1076.	1076.	14.0	9.071
0.80	0.02	0.8961	0.0117	0.0922	177.7	1.961	2.430	1.239	0.982	1.219	1.250	-1082.	1077.	14.0	9.053
0.80	0.03	0.8908	0.0135	0.0917	177.8	1.964	2.430	1.237	0.981	1.215	1.250	-1088.	1076.	14.0	9.035
0.80	0.04	0.8854	0.0154	0.0911	177.9	1.967	2.429	1.235	0.981	1.211	1.250	-1094.	1075.	14.0	9.017
0.80	0.05	0.8800	0.0173	0.0906	178.1	1.970	2.429	1.233	0.980	1.208	1.249	-1100.	1074.	14.0	9.000
0.80	0.07	0.8691	0.0294	0.0896	178.3	1.976	2.427	1.228	0.979	1.201	1.246	-1111.	1072.	14.0	8.982
0.80	0.10	0.8525	0.0596	0.0879	178.7	1.985	2.424	1.222	0.977	1.191	1.241	-1129.	1069.	14.0	8.967
0.80	0.20	0.7945	0.1233	0.0822	180.0	2.013	2.417	1.201	0.972	1.160	1.225	-1186.	1050.	14.3	8.716
0.80	0.40	0.6827	0.2681	0.0693	183.0	2.060	2.392	1.161	0.966	1.107	1.201	-1300.	1030.	13.8	8.298
0.80	0.60	0.4993	0.4476	0.0531	186.5	2.092	2.352	1.124	0.961	1.065	1.183	-1412.	990.	13.3	7.807
0.80	0.80	0													

LIQUID MOLE FRACTION		VAPOR MOLE FRACTION			TEMP	RELATIVE VOL			PRESSURE ACT COEF			ENTHALPY BTU/LB MOLE		HEAT CAPACITY BTU/LB MOLE-R	
N2/N2+O2	AR	N2	AR	O2		N2/AR	N2/O2	AR/O2	N2	AR	O2	LIQ	VAP	LIQ	VAP
0.0	0.0	0.0	0.0	1.0000	208.9	1.737	2.240	1.290	0.000	1.000	1.000	-1216.1275	14.0	9.920	
0.0	0.01	0.0	0.0128	0.9872	208.6	1.739	2.230	1.287	0.007	1.079	1.003	-1220.1269	13.9	9.993	
0.0	0.02	0.0	0.0256	0.9744	208.7	1.742	2.238	1.285	0.007	1.077	1.003	-1224.1263	13.9	9.966	
0.0	0.03	0.0	0.0384	0.9618	208.6	1.744	2.237	1.283	0.007	1.075	1.004	-1227.1258	13.9	9.940	
0.0	0.04	0.0	0.0512	0.9494	208.5	1.746	2.236	1.280	0.006	1.074	1.004	-1231.1252	13.9	9.914	
0.0	0.05	0.0	0.0640	0.9370	208.4	1.749	2.234	1.278	0.006	1.073	1.005	-1235.1246	13.9	9.888	
0.0	0.07	0.0	0.0874	0.9126	208.2	1.753	2.232	1.273	0.005	1.070	1.006	-1242.1235	13.9	9.837	
0.0	0.10	0.0	0.1233	0.8767	208.0	1.760	2.228	1.266	0.004	1.065	1.006	-1253.1219	13.9	9.762	
0.0	0.20	0.0	0.2369	0.7632	207.1	1.782	2.213	1.242	0.002	1.052	1.017	-1288.1168	13.7	9.524	
0.0	0.40	0.0	0.4430	0.5570	205.0	1.825	2.177	1.193	0.000	1.030	1.037	-1354.1077	13.5	9.089	
0.0	0.60	0.0	0.6319	0.3681	204.7	1.865	2.135	1.144	0.002	1.014	1.046	-1414.0996	13.3	7.886	
0.0	0.80	0.0	0.8143	0.1857	204.9	1.903	2.086	1.096	0.000	1.000	1.060	-1471.0920	13.1	7.288	
0.0	0.90	0.0	0.9063	0.0930	203.7	1.921	2.060	1.072	0.000	1.000	1.120	-1498.0892	13.0	7.086	
0.10	0.01	0.2018	0.0	0.7983	204.8	1.766	2.275	1.287	0.005	1.098	1.027	-1193.1246	14.2	9.076	
0.10	0.02	0.1909	0.0114	0.7893	204.7	1.770	2.273	1.285	0.005	1.096	1.028	-1197.1241	14.2	9.052	
0.10	0.03	0.1800	0.0227	0.7804	204.7	1.772	2.271	1.282	0.004	1.094	1.028	-1201.1236	14.2	9.028	
0.10	0.04	0.1692	0.0339	0.7715	204.6	1.774	2.270	1.279	0.004	1.092	1.029	-1204.1231	14.2	9.004	
0.10	0.05	0.1584	0.0451	0.7627	204.6	1.776	2.268	1.277	0.003	1.091	1.029	-1208.1226	14.2	8.980	
0.10	0.07	0.1476	0.0562	0.7540	204.6	1.778	2.266	1.274	0.003	1.089	1.030	-1212.1222	14.2	8.957	
0.10	0.10	0.1368	0.0674	0.7454	204.5	1.780	2.264	1.272	0.002	1.088	1.031	-1216.1218	14.1	8.934	
0.10	0.20	0.1152	0.1108	0.7117	204.4	1.788	2.256	1.262	0.001	1.080	1.032	-1230.1199	14.1	8.841	
0.10	0.40	0.1146	0.2150	0.6781	204.0	1.807	2.236	1.237	0.000	1.065	1.038	-1266.1155	14.0	8.617	
0.10	0.60	0.1146	0.4145	0.4700	203.5	1.844	2.191	1.180	0.000	1.039	1.056	-1336.1074	13.7	8.167	
0.10	0.80	0.1146	0.7979	0.2041	203.3	1.878	2.142	1.140	0.000	1.021	1.061	-1401.0990	13.4	7.706	
0.10	0.90	0.1146	0.9971	0.0029	203.4	1.909	2.089	1.094	0.000	1.000	1.114	-1464.0922	13.2	7.336	
0.20	0.01	0.3649	0.0	0.6351	201.0	1.794	2.299	1.281	0.010	1.114	1.054	-1167.1218	14.8	9.140	
0.20	0.02	0.3511	0.0102	0.6289	201.0	1.796	2.296	1.279	0.010	1.112	1.054	-1171.1214	14.8	9.116	
0.20	0.03	0.3373	0.0204	0.6226	201.0	1.798	2.294	1.276	0.010	1.110	1.055	-1175.1210	14.8	9.092	
0.20	0.04	0.3235	0.0306	0.6165	201.0	1.799	2.292	1.274	0.010	1.108	1.055	-1179.1207	14.8	9.068	
0.20	0.05	0.3097	0.0408	0.6103	201.0	1.801	2.289	1.271	0.010	1.106	1.055	-1183.1203	14.8	9.044	
0.20	0.07	0.2959	0.0510	0.6042	201.0	1.803	2.287	1.269	0.010	1.104	1.055	-1187.1200	14.8	9.020	
0.20	0.10	0.2821	0.0612	0.5981	201.0	1.806	2.285	1.267	0.010	1.102	1.056	-1191.1197	14.8	8.996	
0.20	0.20	0.2683	0.1001	0.5736	201.1	1.812	2.275	1.256	0.010	1.099	1.057	-1204.1180	14.3	8.929	
0.20	0.40	0.2170	0.1975	0.5135	201.1	1.829	2.251	1.231	0.007	1.077	1.061	-1243.1142	14.2	8.714	
0.20	0.60	0.1464	0.3087	0.3944	201.4	1.861	2.200	1.183	0.000	1.049	1.075	-1317.1070	13.6	8.285	
0.20	0.80	0.1464	0.5910	0.2727	201.9	1.890	2.147	1.136	0.000	1.027	1.095	-1388.0999	13.3	7.846	
0.20	0.90	0.1464	0.7919	0.1432	202.6	1.916	2.092	1.092	0.000	1.012	1.121	-1457.0925	13.2	7.393	
0.40	0.01	0.6068	0.0	0.3932	194.6	1.831	2.315	1.264	0.041	1.147	1.114	-1107.1169	15.0	9.328	
0.40	0.02	0.5962	0.0104	0.3872	194.7	1.833	2.312	1.262	0.040	1.145	1.113	-1111.1166	15.0	9.304	
0.40	0.03	0.5856	0.0208	0.3812	194.8	1.836	2.310	1.259	0.039	1.142	1.113	-1115.1164	14.9	9.280	
0.40	0.04	0.5750	0.0312	0.3752	194.9	1.838	2.307	1.257	0.038	1.140	1.113	-1119.1161	14.9	9.256	
0.40	0.05	0.5644	0.0416	0.3692	194.9	1.839	2.305	1.255	0.037	1.138	1.113	-1123.1159	14.9	9.232	
0.40	0.07	0.5488	0.0520	0.3632	195.1	1.842	2.297	1.247	0.035	1.135	1.112	-1127.1156	14.9	9.208	
0.40	0.10	0.5332	0.0624	0.3572	195.3	1.847	2.289	1.240	0.033	1.131	1.112	-1131.1154	14.8	9.184	
0.40	0.20	0.5076	0.1040	0.3316	196.0	1.862	2.264	1.216	0.027	1.124	1.112	-1150.1143	14.7	9.122	
0.40	0.40	0.3905	0.3445	0.2650	197.5	1.869	2.211	1.170	0.017	1.069	1.115	-1277.1061	14.1	8.713	
0.40	0.60	0.2734	0.5343	0.1983	199.3	1.911	2.155	1.127	0.010	1.042	1.124	-1361.0999	13.7	8.001	
0.40	0.80	0.1449	0.7514	0.1037	201.3	1.928	2.095	1.087	0.000	1.020	1.138	-1443.0929	13.3	7.475	
0.40	0.90	0.1449	0.9544	0.0454	202.4	1.934	2.063	1.070	0.000	1.007	1.137	-1491.0866	13.1	7.136	
0.60	0.01	0.7748	0.0	0.2252	189.3	1.847	2.293	1.241	0.050	1.187	1.166	-1036.1120	15.3	9.534	
0.60	0.02	0.7636	0.0100	0.2223	189.4	1.849	2.291	1.239	0.049	1.184	1.165	-1041.1125	15.3	9.510	
0.60	0.03	0.7524	0.0200	0.2194	189.6	1.851	2.289	1.237	0.047	1.181	1.164	-1046.1123	15.3	9.486	
0.60	0.04	0.7412	0.0300	0.2165	189.7	1.853	2.288	1.235	0.046	1.178	1.163	-1051.1121	15.2	9.462	
0.60	0.05	0.7300	0.0400	0.2136	189.9	1.855	2.286	1.233	0.045	1.175	1.163	-1056.1120	15.2	9.438	
0.60	0.07	0.7188	0.0500	0.2107	190.1	1.857	2.284	1.231	0.044	1.173	1.162	-1061.1118	15.2	9.414	
0.60	0.10	0.7076	0.0600	0.2078	190.4	1.860	2.282	1.229	0.043	1.171	1.161	-1066.1116	15.1	9.390	
0.60	0.20	0.6591	0.1499	0.1950	191.6	1.866	2.274	1.219	0.031	1.159	1.177	-1086.1109	15.1	9.328	
0.60	0.40	0.5310	0.3088	0.1603	194.0	1.882	2.254	1.197	0.024	1.134	1.170	-1136.1091	14.6	9.115	
0.60	0.60	0.3844	0.4974	0.1187	196.8	1.911	2.209	1.156	0.012	1.092	1.160	-1235.1049	14.3	8.659	
0.60	0.80	0.2103	0.7220	0.0664	198.8	1.930	2.157	1.110	0.003	1.057	1.156	-1333.0988	13.8	8.150	
0.60	0.90	0.1115	0.9330	0.0358	200.0	1.946	2.099	1.082	0.000	1.020	1.154	-1420.0932	13.3	7.565	
0.80	0.01	0.8887	0.0	0.1113	184.9	1.847	2.243	1.214	0.070	1.230	1.278	-957.1089	15.6	9.758	
0.80	0.02	0.8808	0.0081	0.0997	185.1	1.848	2.242	1.212	0.077	1.234	1.276	-963.1088	15.6	9.734	
0.80	0.03	0.8731	0.0162	0.0891	185.2	1.850	2.241	1.210	0.076	1.231	1.274	-968.1087	15.6	9.710	
0.80	0.04	0.8654	0.0243	0.0795	185.3	1.851	2.240	1.208	0.075	1.227	1.272	-974.1086	15.6	9.686	
0.80	0.05	0.8577	0.0324	0.0709	185.5	1.852	2.240	1.206	0.074	1.224	1.270	-980.1085	15.6	9.662	
0.80	0.07	0.8444	0.0408	0.0633	185.6	1.853	2.239	1.204	0.073	1.220	1.268	-986.1084	15.6	9.638	
0.80	0.10	0.8311	0.0492	0.0567	185.9	1.853	2.237	1.202	0.072	1.217	1.266	-992.1084	15.6	9.614	
0.80	0.20	0.7827	0.1293	0.0880	187.7	1.891	2.204	1.176	0.061	1.172	1.241	-1019.1070	15.3	9.543	
0.80	0.40	0.6465	0.2709	0.0734	190.9	1.925	2.196	1.140	0.048	1.118	1.241	-1074.1066	15.0	9.319	
0.80	0.60	0.4898	0.4634	0.0558	194.5	1.946	2.155	1.108	0.038	1.073	1.240	-1170.1036	14.4	8.838	
0.80	0.80	0.2716	0.6961	0.0323	198.7	1.951	2.101	1.077	0.021	1.036	1.172	-1304.0955	13.9	8.293	
0.80	0.90	0.1440	0.8376	0.0124	201.0	1.947	2.059	1.063	0.013	1.010	1.163	-1419.0934	13.4	7.653	
0.90	0.01	0.9521	0.0	0.0479	182.9	1.842	2.200	1.200	0.080	1.270	1.333	-915.1072	15.6	9.876	
0.90	0.02	0.9411	0.0116	0.0473	183.2	1.845	2.200	1.198	0.080	1.268	1.331	-921.1071	15.6	9.852	
0.90	0.03	0.9306	0.0232	0.0467	183.4	1.846	2.200	1.196	0.080	1.266	1.329	-927.1071	15.6	9.828	
0.90	0.04</														

LIQUID FRACTION			VAPOR FRACTION			TEMP	RELATIVE VOL			PRESSURE ACT COEF			ENTHALPY BTU/LB MOLE		HEAT CAPACITY BTU/LB MOLE-R	
N2/N2+O2	AR	O2	N2	AR	O2		N2/AR	N2/O2	AR/O2	N2	AR	O2	LIG	VAP	LIG	VAP
0.0	0.0	0.0	0.0126	0.0000	0.0000	215.6	1.658	2.089	1.202	0.852	1.000	1.002	-1121.	1285.	14.3	9.498
0.0	0.01	0.0	0.0126	0.0000	0.0000	215.5	1.658	2.088	1.202	0.852	1.000	1.002	-1121.	1285.	14.3	9.498
0.0	0.02	0.0	0.0126	0.0000	0.0000	215.4	1.658	2.087	1.202	0.852	1.000	1.002	-1121.	1285.	14.3	9.498
0.0	0.03	0.0	0.0126	0.0000	0.0000	215.3	1.658	2.086	1.202	0.852	1.000	1.002	-1121.	1285.	14.3	9.498
0.0	0.04	0.0	0.0126	0.0000	0.0000	215.2	1.658	2.085	1.202	0.852	1.000	1.002	-1121.	1285.	14.3	9.498
0.0	0.05	0.0	0.0126	0.0000	0.0000	215.1	1.658	2.084	1.202	0.852	1.000	1.002	-1121.	1285.	14.3	9.498
0.0	0.07	0.0	0.0126	0.0000	0.0000	214.9	1.657	2.081	1.202	0.851	1.001	1.002	-1120.	1285.	14.3	9.498
0.0	0.10	0.0	0.0126	0.0000	0.0000	214.7	1.657	2.078	1.202	0.851	1.001	1.002	-1120.	1285.	14.3	9.498
0.0	0.20	0.0	0.0126	0.0000	0.0000	213.8	1.655	2.084	1.202	0.851	1.001	1.002	-1120.	1285.	14.3	9.498
0.0	0.40	0.0	0.0126	0.0000	0.0000	212.5	1.731	2.093	1.173	0.849	1.004	1.018	-1195.	1177.	14.1	9.011
0.0	0.60	0.0	0.0126	0.0000	0.0000	211.4	1.765	1.991	1.128	0.848	1.025	1.039	-1262.	1083.	14.0	8.577
0.0	0.80	0.0	0.0126	0.0000	0.0000	210.7	1.798	1.948	1.084	0.851	1.011	1.058	-1323.	999.	13.8	8.172
0.0	0.90	0.0	0.0126	0.0000	0.0000	210.4	1.812	1.924	1.062	0.858	1.004	1.105	-1381.	921.	13.7	7.767
0.10	0.0	0.0	0.0103	0.0000	0.0000	211.6	1.682	2.115	1.259	0.872	1.000	1.030	-1095.	1257.	14.6	9.576
0.10	0.01	0.0	0.0103	0.0000	0.0000	211.5	1.682	2.113	1.259	0.871	1.000	1.030	-1095.	1257.	14.6	9.576
0.10	0.02	0.0	0.0103	0.0000	0.0000	211.4	1.682	2.112	1.259	0.871	1.000	1.031	-1103.	1247.	14.6	9.522
0.10	0.03	0.0	0.0103	0.0000	0.0000	211.4	1.682	2.110	1.259	0.870	1.000	1.031	-1107.	1242.	14.5	9.489
0.10	0.04	0.0	0.0103	0.0000	0.0000	211.4	1.682	2.108	1.249	0.870	1.002	1.032	-1111.	1237.	14.5	9.475
0.10	0.05	0.0	0.0103	0.0000	0.0000	211.3	1.682	2.107	1.247	0.869	1.000	1.032	-1114.	1232.	14.5	9.452
0.10	0.07	0.0	0.0103	0.0000	0.0000	211.3	1.682	2.103	1.243	0.869	1.007	1.033	-1122.	1223.	14.5	9.405
0.10	0.10	0.0	0.0103	0.0000	0.0000	211.1	1.680	2.098	1.236	0.867	1.003	1.035	-1134.	1209.	14.5	9.336
0.10	0.20	0.0	0.0103	0.0000	0.0000	210.8	1.714	2.090	1.213	0.864	1.009	1.041	-1171.	1163.	14.3	9.112
0.10	0.40	0.0	0.0103	0.0000	0.0000	210.3	1.746	2.040	1.169	0.859	1.036	1.058	-1242.	1079.	14.1	8.680
0.10	0.60	0.0	0.0103	0.0000	0.0000	210.0	1.778	1.996	1.125	0.859	1.019	1.082	-1310.	1000.	13.9	8.253
0.10	0.80	0.0	0.0103	0.0000	0.0000	210.0	1.802	1.949	1.082	0.862	1.008	1.113	-1374.	923.	13.7	7.814
0.10	0.90	0.0	0.0103	0.0000	0.0000	210.0	1.814	1.925	1.061	0.866	1.002	1.131	-1405.	883.	13.6	7.594
0.20	0.0	0.0	0.0341	0.0000	0.0000	207.9	1.702	2.134	1.254	0.880	1.007	1.059	-1057.	1229.	14.9	9.663
0.20	0.01	0.0	0.0341	0.0000	0.0000	207.9	1.702	2.132	1.251	0.880	1.009	1.059	-1071.	1229.	14.8	9.640
0.20	0.02	0.0	0.0341	0.0000	0.0000	207.9	1.702	2.130	1.249	0.887	1.004	1.059	-1075.	1221.	14.8	9.618
0.20	0.03	0.0	0.0341	0.0000	0.0000	207.9	1.702	2.128	1.247	0.887	1.002	1.060	-1079.	1217.	14.8	9.596
0.20	0.04	0.0	0.0341	0.0000	0.0000	207.9	1.702	2.126	1.244	0.886	1.000	1.060	-1083.	1213.	14.8	9.573
0.20	0.05	0.0	0.0341	0.0000	0.0000	207.9	1.702	2.124	1.242	0.886	1.000	1.060	-1087.	1209.	14.8	9.551
0.20	0.07	0.0	0.0341	0.0000	0.0000	207.9	1.702	2.120	1.237	0.884	1.005	1.061	-1095.	1201.	14.8	9.506
0.20	0.10	0.0	0.0341	0.0000	0.0000	207.9	1.702	2.113	1.233	0.883	1.006	1.062	-1107.	1189.	14.7	9.440
0.20	0.20	0.0	0.0341	0.0000	0.0000	207.9	1.732	2.092	1.208	0.877	1.004	1.066	-1146.	1150.	14.6	9.221
0.20	0.40	0.0	0.0341	0.0000	0.0000	207.9	1.760	2.048	1.163	0.870	1.007	1.066	-1222.	1075.	14.3	8.782
0.20	0.60	0.0	0.0341	0.0000	0.0000	207.9	1.785	2.001	1.121	0.866	1.027	1.097	-1296.	1001.	14.1	8.334
0.20	0.80	0.0	0.0341	0.0000	0.0000	207.9	1.807	1.951	1.080	0.868	1.012	1.121	-1367.	924.	13.7	7.881
0.20	0.90	0.0	0.0341	0.0000	0.0000	207.9	1.817	1.926	1.060	0.868	1.007	1.135	-1401.	884.	13.6	7.669
0.40	0.0	0.0	0.0584	0.0000	0.0000	201.4	1.735	2.149	1.238	0.917	1.007	1.123	-1004.	1176.	15.4	9.695
0.40	0.01	0.0	0.0584	0.0000	0.0000	201.4	1.737	2.147	1.236	0.917	1.005	1.123	-1009.	1175.	15.4	9.674
0.40	0.02	0.0	0.0584	0.0000	0.0000	201.5	1.738	2.144	1.234	0.916	1.003	1.122	-1013.	1173.	15.3	9.652
0.40	0.03	0.0	0.0584	0.0000	0.0000	201.6	1.740	2.142	1.231	0.915	1.001	1.122	-1018.	1170.	15.3	9.630
0.40	0.04	0.0	0.0584	0.0000	0.0000	201.6	1.741	2.140	1.229	0.914	1.000	1.122	-1022.	1167.	15.3	9.608
0.40	0.05	0.0	0.0584	0.0000	0.0000	201.7	1.742	2.138	1.227	0.913	1.000	1.121	-1026.	1164.	15.3	9.587
0.40	0.07	0.0	0.0584	0.0000	0.0000	201.8	1.745	2.133	1.222	0.912	1.002	1.121	-1035.	1159.	15.2	9.543
0.40	0.10	0.0	0.0584	0.0000	0.0000	202.0	1.749	2.126	1.216	0.909	1.005	1.120	-1049.	1150.	15.2	9.477
0.40	0.20	0.0	0.0584	0.0000	0.0000	202.0	1.762	2.103	1.194	0.902	1.005	1.119	-1093.	1122.	15.0	9.454
0.40	0.40	0.0	0.0584	0.0000	0.0000	204.3	1.785	2.056	1.152	0.891	1.001	1.121	-1181.	1063.	14.5	8.993
0.40	0.60	0.0	0.0584	0.0000	0.0000	208.0	1.804	2.006	1.112	0.882	1.003	1.127	-1267.	1000.	14.2	8.497
0.40	0.80	0.0	0.0584	0.0000	0.0000	208.0	1.818	1.954	1.075	0.875	1.021	1.138	-1352.	927.	13.8	7.953
0.40	0.90	0.0	0.0584	0.0000	0.0000	209.1	1.823	1.927	1.057	0.872	1.011	1.144	-1394.	887.	13.7	7.650
0.60	0.0	0.0	0.0762	0.0000	0.0000	195.0	1.754	2.135	1.217	0.943	1.003	1.200	-934.	1133.	15.8	10.175
0.60	0.01	0.0	0.0762	0.0000	0.0000	196.0	1.756	2.133	1.215	0.942	1.001	1.199	-939.	1131.	15.8	10.152
0.60	0.02	0.0	0.0762	0.0000	0.0000	196.1	1.757	2.131	1.213	0.941	1.000	1.198	-944.	1129.	15.8	10.129
0.60	0.03	0.0	0.0762	0.0000	0.0000	196.2	1.758	2.129	1.211	0.940	1.000	1.197	-949.	1127.	15.7	10.106
0.60	0.04	0.0	0.0762	0.0000	0.0000	196.4	1.759	2.128	1.209	0.939	1.001	1.196	-954.	1125.	15.7	10.083
0.60	0.05	0.0	0.0762	0.0000	0.0000	196.5	1.760	2.126	1.207	0.938	1.001	1.195	-959.	1124.	15.7	10.060
0.60	0.07	0.0	0.0762	0.0000	0.0000	196.7	1.761	2.122	1.203	0.936	1.003	1.193	-969.	1120.	15.6	10.014
0.60	0.10	0.0	0.0762	0.0000	0.0000	197.0	1.765	2.117	1.196	0.934	1.005	1.190	-985.	1114.	15.6	9.944
0.60	0.20	0.0	0.0762	0.0000	0.0000	198.7	1.783	2.097	1.177	0.925	1.006	1.181	-1036.	1095.	15.3	9.707
0.60	0.40	0.0	0.0762	0.0000	0.0000	203.6	1.825	2.055	1.139	0.910	1.007	1.189	-1137.	1059.	14.8	9.266
0.60	0.60	0.0	0.0762	0.0000	0.0000	206.7	1.852	2.008	1.103	0.897	1.000	1.180	-1236.	997.	14.3	8.658
0.60	0.80	0.0	0.0762	0.0000	0.0000	208.4	1.878	1.956	1.070	0.884	1.003	1.155	-1337.	929.	13.9	8.045
0.60	0.90	0.0	0.0762	0.0000	0.0000	209.4	1.882	1.929	1.050	0.877	1.006	1.153	-1381.	889.	13.7	7.728
0.80	0.0	0.0	0.0935	0.0000	0.0000	191.2	1.759	2.097	1.192	0.970	1.000	1.206	-857.	1092.	16.1	10.494
0.80	0.01	0.0	0.0935	0.0000	0.0000	191.4	1.761	2.096	1.190	0.969	1.000	1.204	-863.	1091.	16.1	10.469
0.80	0.02	0.0	0.0935	0.0000	0.0000	191.5	1.763	2.095	1.188	0.968	1.003	1.202	-868.	1090.	16.1	10.444
0.80	0.03	0.0	0.0935	0.0000	0.0000	191.7	1.765	2.094	1.186	0.967	1.005	1.200	-874.	1088.	16.1	10.418
0.80	0.04	0.0	0.0935	0.0000	0.0000	191.8	1.767	2.093	1.185	0.966	1.005	1.200	-880.	1087.	16.0	10.392
0.80	0.05	0.0	0.0935	0.0000	0.0000	191.9	1.76									

LIQUID MOLE FRACTION		VAPOR MOLE FRACTION			IFMP	RELATIVE VOL			PRESSURE ACT COEF			ENTHALPY BTU/LB MOLE		HEAT CAPACITY BTU/LR MOLE-R		
N2/N2+O2	AR	N2	AR	O2		R	N2/AR	N2/O2	AR/O2	N2	AR	O2	LIQ	VAP	LIQ	VAP
0.0	0.0	0.0000	0.0000	1.0000	221.4	1.998	1.998	1.239	0.825	1.097	1.003	-1077.120	14.0	10.012		
0.0	0.01	0.0123	0.9877	0.0123	221.3	1.998	1.979	1.237	0.824	1.095	1.003	-1071.128	14.0	9.986		
0.0	0.02	0.0246	0.9754	0.0246	221.2	1.997	1.957	1.235	0.824	1.094	1.004	-1065.127	14.0	9.960		
0.0	0.03	0.0369	0.9633	0.0369	221.1	1.997	1.936	1.233	0.824	1.093	1.005	-1059.127	14.0	9.935		
0.0	0.04	0.0492	0.9512	0.0492	221.0	1.996	1.915	1.231	0.824	1.092	1.006	-1053.126	14.0	9.910		
0.0	0.05	0.0615	0.9393	0.0615	220.9	1.997	1.894	1.229	0.824	1.091	1.007	-1047.126	14.0	9.885		
0.0	0.07	0.0844	0.9156	0.0844	220.8	1.998	1.871	1.225	0.824	1.089	1.008	-1041.124	14.0	9.860		
0.0	0.10	0.1192	0.8808	0.1192	220.5	1.999	1.847	1.218	0.823	1.086	1.010	-1035.122	14.0	9.764		
0.0	0.15	0.2305	0.7695	0.2305	219.6	1.999	1.801	1.198	0.822	1.080	1.019	-1029.118	14.0	9.532		
0.0	0.20	0.4354	0.5647	0.4354	218.3	1.999	1.721	1.157	0.822	1.071	1.041	-1023.104	14.0	9.101		
0.0	0.30	0.8259	0.1742	0.8259	217.2	1.999	1.684	1.115	0.825	1.060	1.069	-1017.090	14.0	8.671		
0.0	0.40	0.8112	0.1888	0.8112	216.5	1.717	1.844	1.074	0.831	1.052	1.104	-1010.917	14.0	8.279		
0.0	0.50	0.9046	0.0954	0.9046	216.3	1.730	1.822	1.053	0.836	1.041	1.125	-1004.877	14.0	8.067		
0.10	0.0	0.1818	0.8182	0.1818	217.4	1.818	1.997	1.239	0.848	1.079	1.032	-1008.1261	15.0	10.102		
0.10	0.01	0.1794	0.8206	0.1794	217.4	1.818	1.995	1.233	0.844	1.078	1.033	-1012.1254	15.0	10.078		
0.10	0.02	0.1773	0.8227	0.1773	217.4	1.819	1.994	1.231	0.844	1.078	1.033	-1016.1247	15.0	10.055		
0.10	0.03	0.1752	0.8248	0.1752	217.3	1.821	1.992	1.229	0.843	1.079	1.034	-1020.1240	15.0	10.031		
0.10	0.04	0.1731	0.8269	0.1731	217.3	1.822	1.990	1.227	0.843	1.079	1.034	-1024.1233	15.0	10.008		
0.10	0.05	0.1710	0.8290	0.1710	217.2	1.824	1.988	1.225	0.843	1.072	1.035	-1028.1226	15.0	9.985		
0.10	0.07	0.1668	0.8372	0.1668	217.1	1.827	1.986	1.221	0.842	1.069	1.036	-1032.1219	15.0	9.938		
0.10	0.10	0.1607	0.8454	0.1607	217.0	1.831	1.981	1.214	0.841	1.065	1.037	-1036.1212	15.0	9.870		
0.10	0.15	0.1498	0.8536	0.1498	216.6	1.846	1.964	1.194	0.838	1.051	1.044	-1040.1186	15.0	9.645		
0.10	0.20	0.1336	0.8664	0.1336	216.1	1.873	1.927	1.152	0.834	1.032	1.061	-1044.1150	15.0	9.269		
0.10	0.30	0.0885	0.9115	0.0885	215.9	1.898	1.887	1.111	0.833	1.017	1.083	-1048.1104	15.0	8.776		
0.10	0.40	0.0343	0.9657	0.0343	215.8	1.721	1.848	1.072	0.836	1.006	1.112	-1052.1058	15.0	8.327		
0.10	0.50	0.0173	0.9827	0.0173	215.9	1.732	1.822	1.052	0.838	1.003	1.129	-1056.1012	15.0	8.092		
0.20	0.0	0.3344	0.6656	0.3344	213.8	1.833	2.010	1.231	0.863	1.101	1.063	-978.1234	15.0	10.216		
0.20	0.01	0.3318	0.6682	0.3318	213.8	1.834	2.008	1.229	0.862	1.100	1.063	-982.1227	15.0	10.194		
0.20	0.02	0.3292	0.6708	0.3292	213.8	1.836	2.006	1.226	0.862	1.099	1.063	-986.1220	15.0	10.171		
0.20	0.03	0.3266	0.6734	0.3266	213.8	1.837	2.004	1.224	0.861	1.098	1.064	-990.1213	15.0	10.148		
0.20	0.04	0.3240	0.6760	0.3240	213.8	1.838	2.002	1.222	0.861	1.095	1.064	-994.1206	15.0	10.126		
0.20	0.05	0.3214	0.6786	0.3214	213.8	1.840	2.001	1.220	0.860	1.093	1.064	-998.1199	15.0	10.105		
0.20	0.07	0.3164	0.6836	0.3164	213.8	1.843	1.997	1.216	0.859	1.092	1.065	-1002.1192	15.0	10.080		
0.20	0.10	0.3099	0.6901	0.3099	213.8	1.847	1.991	1.209	0.857	1.089	1.066	-1006.1185	15.0	9.992		
0.20	0.15	0.2945	0.7055	0.2945	213.8	1.860	1.972	1.188	0.852	1.079	1.070	-1010.1152	15.0	9.769		
0.20	0.20	0.1981	0.8019	0.1981	214.0	1.884	1.932	1.147	0.845	1.045	1.082	-1014.1117	15.0	9.322		
0.20	0.30	0.1331	0.8669	0.1331	214.5	1.706	1.890	1.108	0.841	1.026	1.099	-1018.1071	15.0	8.862		
0.20	0.40	0.0788	0.9212	0.0788	215.2	1.726	1.846	1.069	0.841	1.011	1.121	-1022.1025	15.0	8.375		
0.20	0.50	0.0343	0.9657	0.0343	215.6	1.734	1.822	1.051	0.841	1.000	1.134	-1026.0979	15.0	8.118		
0.40	0.0	0.5739	0.4261	0.5739	207.2	1.861	2.020	1.216	0.896	1.147	1.131	-913.1182	15.0	10.510		
0.40	0.01	0.5687	0.4313	0.5687	207.3	1.862	2.018	1.214	0.895	1.144	1.131	-917.1175	15.0	10.487		
0.40	0.02	0.5635	0.4365	0.5635	207.4	1.863	2.016	1.212	0.894	1.142	1.130	-921.1168	15.0	10.464		
0.40	0.03	0.5583	0.4417	0.5583	207.4	1.865	2.014	1.210	0.894	1.140	1.130	-925.1161	15.0	10.441		
0.40	0.04	0.5531	0.4469	0.5531	207.5	1.866	2.012	1.208	0.893	1.138	1.130	-929.1154	15.0	10.418		
0.40	0.05	0.5479	0.4521	0.5479	207.6	1.867	2.010	1.206	0.892	1.136	1.130	-933.1147	15.0	10.395		
0.40	0.07	0.5375	0.4625	0.5375	207.7	1.869	2.008	1.202	0.890	1.131	1.129	-937.1140	15.0	10.349		
0.40	0.10	0.5219	0.4781	0.5219	207.9	1.873	2.000	1.195	0.888	1.125	1.128	-941.1133	15.0	10.281		
0.40	0.15	0.4698	0.5302	0.4698	208.6	1.884	1.979	1.179	0.880	1.109	1.126	-945.1126	15.0	10.045		
0.40	0.20	0.3634	0.6366	0.3634	210.2	1.705	1.937	1.136	0.868	1.072	1.126	-949.1080	15.0	9.557		
0.40	0.30	0.2518	0.7482	0.2518	211.9	1.721	1.893	1.100	0.868	1.044	1.130	-953.1034	15.0	9.036		
0.40	0.40	0.1321	0.8679	0.1321	213.8	1.734	1.847	1.065	0.869	1.021	1.138	-957.0988	15.0	8.472		
0.40	0.50	0.0677	0.9323	0.0677	214.9	1.739	1.823	1.048	0.866	1.010	1.143	-961.0942	15.0	8.168		
0.60	0.0	0.7509	0.2491	0.7509	201.7	1.870	2.009	1.197	0.928	1.198	1.213	-842.1134	16.0	10.881		
0.60	0.01	0.7452	0.2548	0.7452	201.8	1.880	2.007	1.195	0.927	1.195	1.211	-846.1127	16.0	10.855		
0.60	0.02	0.7394	0.2606	0.7394	201.9	1.881	2.006	1.193	0.926	1.192	1.210	-850.1120	16.0	10.829		
0.60	0.03	0.7336	0.2664	0.7336	202.0	1.883	2.004	1.191	0.925	1.189	1.209	-854.1113	16.0	10.804		
0.60	0.04	0.7278	0.2722	0.7278	202.1	1.884	2.002	1.189	0.925	1.187	1.208	-858.1106	16.0	10.778		
0.60	0.05	0.7219	0.2780	0.7219	202.2	1.885	2.001	1.187	0.922	1.184	1.207	-862.1099	16.0	10.752		
0.60	0.07	0.7102	0.2908	0.7102	202.5	1.888	1.997	1.183	0.920	1.178	1.205	-866.1092	16.0	10.700		
0.60	0.10	0.6925	0.3075	0.6925	202.8	1.892	1.992	1.178	0.917	1.170	1.201	-870.1085	16.0	10.622		
0.60	0.15	0.6320	0.3680	0.6320	204.0	1.703	1.974	1.159	0.908	1.149	1.192	-874.1039	16.0	10.357		
0.60	0.20	0.5261	0.4739	0.5261	206.6	1.722	1.936	1.124	0.899	1.101	1.176	-878.0993	16.0	9.866		
0.60	0.30	0.3581	0.6419	0.3581	209.4	1.735	1.894	1.091	0.874	1.063	1.165	-882.0947	16.0	9.214		
0.60	0.40	0.1926	0.8074	0.1926	212.6	1.742	1.846	1.061	0.868	1.030	1.156	-886.0901	16.0	8.568		
0.60	0.50	0.1000	0.9000	0.1000	214.3	1.743	1.824	1.046	0.869	1.015	1.15					

LIQUID MOLE FRACTION		VAPOR MOLE FRACTION			TEMP	RELATIVE VOL			PRESSURE ACT COEF			ENTHALPY BTU/LB MOLE		HEAT CAPACITY BTU/LP MOLE-R	
N2/M2+O2	AR	N2	AR	O2		R	N2/AR	N2/O2	AR/O2	N2	AR	O2	LIQ	VAP	LIQ
0.0	0.0	0.0	0.0	1.0000	226.4	1.557	1.899	1.219	0.802	1.046	1.002	-940.	1290.	15.2	10.571
0.0	0.01	0.0	0.0121	0.9879	226.4	1.559	1.897	1.217	0.802	1.045	1.003	-940.	1284.	15.2	10.564
0.0	0.02	0.0	0.0242	0.9757	226.4	1.560	1.896	1.215	0.802	1.045	1.004	-940.	1278.	15.2	10.556
0.0	0.03	0.0	0.0362	0.9634	226.4	1.561	1.895	1.213	0.802	1.044	1.005	-941.	1272.	15.2	10.548
0.0	0.04	0.0	0.0481	0.9510	226.2	1.563	1.893	1.212	0.802	1.043	1.006	-942.	1266.	15.2	10.540
0.0	0.05	0.0	0.0599	0.9381	226.1	1.564	1.892	1.210	0.802	1.042	1.006	-942.	1260.	15.2	10.532
0.0	0.07	0.0	0.0832	0.9168	225.9	1.567	1.889	1.206	0.801	1.040	1.008	-947.	1249.	15.2	10.509
0.0	0.10	0.0	0.1177	0.8823	225.6	1.571	1.885	1.200	0.801	1.037	1.011	-958.	1232.	15.1	10.520
0.0	0.20	0.0	0.2280	0.7721	224.8	1.584	1.871	1.181	0.800	1.029	1.020	-1035.	1179.	15.1	10.500
0.0	0.40	0.0	0.4324	0.5677	223.4	1.610	1.839	1.143	0.801	1.015	1.041	-1103.	1082.	14.9	9.670
0.0	0.60	0.0	0.6234	0.3766	222.4	1.635	1.804	1.104	0.804	1.005	1.069	-1167.	994.	14.8	9.254
0.0	0.80	0.0	0.8098	0.1902	221.7	1.658	1.765	1.065	0.810	1.000	1.103	-1225.	910.	14.7	8.831
0.0	0.90	0.0	0.9039	0.0961	221.5	1.689	1.744	1.045	0.814	0.999	1.123	-1253.	869.	14.7	8.620
0.10	0.0	0.1749	0.0	0.8251	222.6	1.569	1.918	1.216	0.823	1.072	1.034	-930.	1261.	15.4	10.684
0.10	0.01	0.1729	0.0111	0.8161	222.6	1.570	1.907	1.214	0.822	1.070	1.035	-934.	1256.	15.4	10.682
0.10	0.02	0.1708	0.0222	0.8071	222.5	1.572	1.905	1.212	0.822	1.069	1.035	-938.	1251.	15.4	10.639
0.10	0.03	0.1688	0.0332	0.7981	222.5	1.573	1.904	1.210	0.822	1.068	1.036	-942.	1246.	15.3	10.615
0.10	0.04	0.1668	0.0441	0.7891	222.4	1.574	1.902	1.208	0.821	1.066	1.036	-946.	1241.	15.3	10.592
0.10	0.05	0.1648	0.0550	0.7802	222.4	1.576	1.901	1.206	0.821	1.065	1.037	-950.	1236.	15.3	10.569
0.10	0.07	0.1608	0.0767	0.7626	222.3	1.578	1.898	1.202	0.820	1.063	1.038	-958.	1226.	15.3	10.523
0.10	0.10	0.1549	0.1088	0.7364	222.2	1.582	1.893	1.197	0.819	1.059	1.040	-970.	1211.	15.3	10.454
0.10	0.20	0.1358	0.2129	0.6513	221.8	1.595	1.877	1.177	0.817	1.048	1.046	-1008.	1164.	15.2	10.229
0.10	0.40	0.1000	0.4117	0.4883	221.3	1.618	1.842	1.138	0.813	1.029	1.063	-1082.	1076.	15.0	9.789
0.10	0.60	0.0661	0.6043	0.3294	221.0	1.641	1.805	1.100	0.812	1.014	1.084	-1152.	993.	14.9	9.347
0.10	0.80	0.0331	0.7979	0.1689	221.0	1.661	1.765	1.063	0.814	1.005	1.112	-1217.	911.	14.7	8.888
0.10	0.90	0.0167	0.8974	0.0859	221.1	1.670	1.744	1.044	0.816	1.001	1.128	-1249.	870.	14.7	8.686
0.20	0.0	0.3237	0.0	0.6763	219.0	1.581	1.915	1.211	0.842	1.096	1.067	-898.	1233.	15.2	10.826
0.20	0.01	0.3202	0.0102	0.6695	219.0	1.582	1.913	1.209	0.841	1.094	1.067	-902.	1229.	15.2	10.803
0.20	0.02	0.3167	0.0204	0.6628	219.0	1.583	1.911	1.207	0.841	1.093	1.067	-906.	1225.	15.2	10.780
0.20	0.03	0.3133	0.0306	0.6562	219.0	1.585	1.910	1.205	0.840	1.091	1.068	-911.	1220.	15.2	10.757
0.20	0.04	0.3099	0.0407	0.6495	219.0	1.586	1.908	1.203	0.840	1.090	1.068	-915.	1216.	15.2	10.735
0.20	0.05	0.3064	0.0508	0.6428	219.0	1.587	1.906	1.201	0.839	1.088	1.068	-919.	1212.	15.2	10.712
0.20	0.07	0.2995	0.0709	0.6294	219.0	1.589	1.903	1.197	0.838	1.085	1.069	-927.	1203.	15.2	10.667
0.20	0.10	0.2893	0.1089	0.6098	219.0	1.593	1.898	1.191	0.836	1.081	1.070	-940.	1191.	15.2	10.600
0.20	0.20	0.2500	0.1994	0.5446	219.0	1.605	1.880	1.172	0.832	1.081	1.071	-981.	1149.	15.2	10.373
0.20	0.40	0.1916	0.3927	0.4157	219.2	1.627	1.844	1.134	0.825	1.043	1.085	-1060.	1070.	15.1	9.914
0.20	0.60	0.1287	0.5682	0.2851	219.7	1.646	1.805	1.096	0.820	1.024	1.100	-1138.	992.	14.9	9.441
0.20	0.80	0.0654	0.7863	0.1461	220.4	1.664	1.765	1.061	0.819	1.010	1.120	-1210.	912.	14.8	8.938
0.20	0.90	0.0331	0.8910	0.0759	220.8	1.672	1.744	1.043	0.819	1.006	1.132	-1245.	871.	14.7	8.672
0.40	0.0	0.5612	0.0	0.4388	212.4	1.602	1.916	1.198	0.878	1.148	1.139	-830.	1180.	16.1	11.192
0.40	0.01	0.5581	0.0080	0.4352	212.5	1.603	1.915	1.196	0.877	1.144	1.139	-835.	1177.	16.1	11.168
0.40	0.02	0.5549	0.0175	0.4315	212.6	1.604	1.915	1.194	0.876	1.142	1.138	-839.	1174.	16.1	11.144
0.40	0.03	0.5516	0.0263	0.4279	212.6	1.605	1.913	1.192	0.875	1.140	1.138	-844.	1171.	16.1	11.120
0.40	0.04	0.5484	0.0351	0.4243	212.7	1.607	1.911	1.190	0.874	1.137	1.137	-849.	1168.	16.1	11.095
0.40	0.05	0.5452	0.0438	0.4206	212.8	1.609	1.910	1.188	0.873	1.135	1.137	-853.	1165.	16.0	11.071
0.40	0.07	0.5381	0.0614	0.4134	212.9	1.610	1.908	1.184	0.872	1.131	1.136	-863.	1159.	16.0	11.022
0.40	0.10	0.5289	0.0878	0.4024	213.1	1.613	1.901	1.178	0.869	1.129	1.135	-877.	1150.	15.9	10.948
0.40	0.20	0.4583	0.1744	0.3652	213.8	1.624	1.882	1.159	0.862	1.106	1.133	-923.	1119.	15.8	10.699
0.40	0.40	0.3537	0.3588	0.2876	215.3	1.643	1.845	1.123	0.848	1.072	1.131	-1015.	1056.	15.4	10.104
0.40	0.60	0.2444	0.5926	0.2010	217.1	1.658	1.805	1.089	0.837	1.044	1.133	-1100.	980.	15.1	9.633
0.40	0.80	0.1276	0.7639	0.1085	219.0	1.670	1.765	1.056	0.828	1.020	1.130	-1194.	913.	14.8	9.041
0.40	0.90	0.0654	0.8784	0.0563	220.1	1.675	1.744	1.041	0.823	1.009	1.141	-1237.	872.	14.7	8.725
0.60	0.0	0.7410	0.0	0.2590	208.7	1.617	1.907	1.179	0.914	1.203	1.225	-758.	1136.	16.7	11.670
0.60	0.01	0.7352	0.0076	0.2577	208.9	1.618	1.906	1.178	0.913	1.200	1.223	-763.	1128.	16.7	11.641
0.60	0.02	0.7293	0.0153	0.2553	209.0	1.620	1.904	1.176	0.911	1.197	1.222	-768.	1126.	16.6	11.612
0.60	0.03	0.7235	0.0230	0.2530	209.1	1.621	1.903	1.174	0.910	1.194	1.221	-774.	1124.	16.6	11.583
0.60	0.04	0.7176	0.0307	0.2516	209.2	1.622	1.901	1.172	0.909	1.191	1.220	-779.	1122.	16.6	11.554
0.60	0.05	0.7117	0.0385	0.2494	209.3	1.623	1.900	1.170	0.908	1.189	1.219	-784.	1120.	16.6	11.525
0.60	0.07	0.6999	0.0540	0.2460	209.4	1.625	1.898	1.167	0.906	1.183	1.216	-795.	1116.	16.5	11.466
0.60	0.10	0.6881	0.0776	0.2404	209.7	1.629	1.892	1.161	0.902	1.179	1.212	-811.	1109.	16.4	11.370
0.60	0.20	0.6212	0.1570	0.2208	209.1	1.639	1.875	1.144	0.892	1.149	1.201	-864.	1068.	16.2	11.081
0.60	0.40	0.4919	0.3300	0.1782	211.7	1.656	1.841	1.111	0.872	1.104	1.183	-970.	1040.	15.7	10.476
0.60	0.60	0.3488	0.5224	0.1289	214.6	1.669	1.804	1.081	0.855	1.069	1.169	-1074.	984.	15.3	9.834
0.60	0.80	0.1868	0.7427	0.0764	217.8	1.677	1.764	1.052	0.837	1.030	1.156	-1178.	914.	14.9	9.145
0.60	0.90	0.0969	0.8660	0.0371	219.5	1.678	1.744	1.039	0.828	1.014	1.151	-1229.	873.	14.8	8.770
0.80	0.0	0.8828	0.0	0.1173	201.7	1.625	1.891	1.157	0.953	1.271	1.330	-683.	1062.	17.1	12.272
0.80	0.01	0.8767	0.0080	0.1166	201.8	1.627	1.890	1.156	0.952	1.267	1.328	-689.	1061.	17.1	12.235
0.80	0.02	0.8706	0.0156	0.1158	202.0	1.628	1.889	1.154	0.950	1.263	1.325	-695.	1060.	17.1	12.198
0.80	0.03	0.8645	0.0235	0.1151	202.2	1.630	1.888	1.153	0.949	1.260	1.322	-701.	1058.	17.1	12.160
0.80	0.04	0.8583	0.0314	0.1143	202.3	1.631	1.887	1.151	0.947	1.256	1.320	-707.	1057.	17.1	12.123
0.80	0.05	0.8522	0.0393	0.1135	202.5	1.632	1.886	1.150	0.946	1.252	1.317	-713.	1056.	17.0	12.086
0.80	0.07	0.8397	0.0543	0.1120	202.8	1.635	1.884	1.147	0.943	1.249	1.312	-725.	1054.	16.9	12.012
0.80	0.10	0.8278	0.0696	0.1097	203.3	1.639	1.881	1.142	0.938	1.244	1.305	-743.	1054.	16.8	12.012
0.80	0.20	0.7554	0.1431	0.1016	204.9	1.659	1.860	1.127	0.924	1.200	1.282	-863.	1026.	16.6	11.901
0.80	0.40	0.6113	0												

LIQUID MOLE FRACTION			VAPOR MOLE FRACTION			TEMP	RELATIVE VOL			PRESSURE ACT COEF			ENTHALPY		HEAT CAPACITY		
N2/N2+O2	AR		N2	AR	O2		R	N2/AR	N2/O2	AR/O2	N2	AR	O2	LIG	VAP	LIG	VAP
0.0	0.0	0.0	0.0	0.0	0.0	231.3	1.530	1.840	1.703	0.785	1.037	1.002	-887.1286	15.8	11.188		
0.0	0.01	0.0	0.0179	0.0080	0.0080	231.2	1.531	1.839	1.701	0.785	1.037	1.003	-891.1286	15.8	11.184		
0.0	0.02	0.0	0.0357	0.0160	0.0160	231.1	1.532	1.837	1.699	0.785	1.036	1.004	-895.1274	15.7	11.140		
0.0	0.03	0.0	0.0535	0.0240	0.0240	231.0	1.533	1.836	1.697	0.785	1.035	1.005	-899.1262	15.7	11.115		
0.0	0.04	0.0	0.0713	0.0320	0.0320	230.9	1.534	1.834	1.696	0.785	1.034	1.006	-903.1251	15.7	11.091		
0.0	0.05	0.0	0.0891	0.0400	0.0400	230.8	1.535	1.833	1.694	0.785	1.034	1.006	-907.1240	15.7	11.068		
0.0	0.06	0.0	0.1069	0.0480	0.0480	230.7	1.536	1.832	1.693	0.784	1.033	1.007	-911.1230	15.7	11.045		
0.0	0.07	0.0	0.1247	0.0560	0.0560	230.6	1.537	1.830	1.692	0.784	1.032	1.008	-915.1220	15.6	11.022		
0.0	0.08	0.0	0.1425	0.0640	0.0640	230.5	1.538	1.829	1.691	0.784	1.031	1.011	-919.1210	15.6	10.999		
0.0	0.09	0.0	0.1603	0.0720	0.0720	230.4	1.539	1.827	1.690	0.784	1.030	1.012	-923.1200	15.6	10.976		
0.0	0.10	0.0	0.1781	0.0800	0.0800	230.3	1.540	1.826	1.689	0.784	1.029	1.013	-927.1190	15.5	10.953		
0.0	0.11	0.0	0.1959	0.0880	0.0880	230.2	1.541	1.824	1.688	0.784	1.028	1.014	-931.1180	15.5	10.930		
0.0	0.12	0.0	0.2137	0.0960	0.0960	230.1	1.542	1.823	1.687	0.784	1.027	1.015	-935.1170	15.4	10.907		
0.0	0.13	0.0	0.2315	0.1040	0.1040	230.0	1.543	1.821	1.686	0.784	1.026	1.016	-939.1160	15.4	10.884		
0.0	0.14	0.0	0.2493	0.1120	0.1120	229.9	1.544	1.820	1.685	0.784	1.025	1.017	-943.1150	15.3	10.861		
0.0	0.15	0.0	0.2671	0.1200	0.1200	229.8	1.545	1.819	1.684	0.784	1.024	1.018	-947.1140	15.3	10.838		
0.0	0.16	0.0	0.2849	0.1280	0.1280	229.7	1.546	1.817	1.683	0.784	1.023	1.019	-951.1130	15.2	10.815		
0.0	0.17	0.0	0.3027	0.1360	0.1360	229.6	1.547	1.816	1.682	0.784	1.022	1.020	-955.1120	15.2	10.792		
0.0	0.18	0.0	0.3205	0.1440	0.1440	229.5	1.548	1.814	1.681	0.784	1.021	1.021	-959.1110	15.1	10.769		
0.0	0.19	0.0	0.3383	0.1520	0.1520	229.4	1.549	1.813	1.680	0.784	1.020	1.022	-963.1100	15.1	10.746		
0.0	0.20	0.0	0.3561	0.1600	0.1600	229.3	1.550	1.811	1.679	0.784	1.019	1.023	-967.1090	15.0	10.723		
0.0	0.21	0.0	0.3739	0.1680	0.1680	229.2	1.551	1.810	1.678	0.784	1.018	1.024	-971.1080	15.0	10.700		
0.0	0.22	0.0	0.3917	0.1760	0.1760	229.1	1.552	1.809	1.677	0.784	1.017	1.025	-975.1070	14.9	10.677		
0.0	0.23	0.0	0.4095	0.1840	0.1840	229.0	1.553	1.807	1.676	0.784	1.016	1.026	-979.1060	14.9	10.654		
0.0	0.24	0.0	0.4273	0.1920	0.1920	228.9	1.554	1.806	1.675	0.784	1.015	1.027	-983.1050	14.8	10.631		
0.0	0.25	0.0	0.4451	0.2000	0.2000	228.8	1.555	1.804	1.674	0.784	1.014	1.028	-987.1040	14.8	10.608		
0.0	0.26	0.0	0.4629	0.2080	0.2080	228.7	1.556	1.803	1.673	0.784	1.013	1.029	-991.1030	14.7	10.585		
0.0	0.27	0.0	0.4807	0.2160	0.2160	228.6	1.557	1.801	1.672	0.784	1.012	1.030	-995.1020	14.7	10.562		
0.0	0.28	0.0	0.4985	0.2240	0.2240	228.5	1.558	1.800	1.671	0.784	1.011	1.031	-999.1010	14.6	10.539		
0.0	0.29	0.0	0.5163	0.2320	0.2320	228.4	1.559	1.799	1.670	0.784	1.010	1.032	-1003.1000	14.6	10.516		
0.0	0.30	0.0	0.5341	0.2400	0.2400	228.3	1.560	1.797	1.669	0.784	1.009	1.033	-1007.0990	14.5	10.493		
0.0	0.31	0.0	0.5519	0.2480	0.2480	228.2	1.561	1.796	1.668	0.784	1.008	1.034	-1011.0980	14.5	10.470		
0.0	0.32	0.0	0.5697	0.2560	0.2560	228.1	1.562	1.794	1.667	0.784	1.007	1.035	-1015.0970	14.4	10.447		
0.0	0.33	0.0	0.5875	0.2640	0.2640	228.0	1.563	1.793	1.666	0.784	1.006	1.036	-1019.0960	14.4	10.424		
0.0	0.34	0.0	0.6053	0.2720	0.2720	227.9	1.564	1.791	1.665	0.784	1.005	1.037	-1023.0950	14.3	10.401		
0.0	0.35	0.0	0.6231	0.2800	0.2800	227.8	1.565	1.790	1.664	0.784	1.004	1.038	-1027.0940	14.3	10.378		
0.0	0.36	0.0	0.6409	0.2880	0.2880	227.7	1.566	1.789	1.663	0.784	1.003	1.039	-1031.0930	14.2	10.355		
0.0	0.37	0.0	0.6587	0.2960	0.2960	227.6	1.567	1.787	1.662	0.784	1.002	1.040	-1035.0920	14.2	10.332		
0.0	0.38	0.0	0.6765	0.3040	0.3040	227.5	1.568	1.786	1.661	0.784	1.001	1.041	-1039.0910	14.1	10.309		
0.0	0.39	0.0	0.6943	0.3120	0.3120	227.4	1.569	1.784	1.660	0.784	1.000	1.042	-1043.0900	14.1	10.286		
0.0	0.40	0.0	0.7121	0.3200	0.3200	227.3	1.570	1.783	1.659	0.784	0.999	1.043	-1047.0890	14.0	10.263		
0.0	0.41	0.0	0.7299	0.3280	0.3280	227.2	1.571	1.781	1.658	0.784	0.998	1.044	-1051.0880	14.0	10.240		
0.0	0.42	0.0	0.7477	0.3360	0.3360	227.1	1.572	1.780	1.657	0.784	0.997	1.045	-1055.0870	13.9	10.217		
0.0	0.43	0.0	0.7655	0.3440	0.3440	227.0	1.573	1.778	1.656	0.784	0.996	1.046	-1059.0860	13.9	10.194		
0.0	0.44	0.0	0.7833	0.3520	0.3520	226.9	1.574	1.777	1.655	0.784	0.995	1.047	-1063.0850	13.8	10.171		
0.0	0.45	0.0	0.8011	0.3600	0.3600	226.8	1.575	1.775	1.654	0.784	0.994	1.048	-1067.0840	13.8	10.148		
0.0	0.46	0.0	0.8189	0.3680	0.3680	226.7	1.576	1.774	1.653	0.784	0.993	1.049	-1071.0830	13.7	10.125		
0.0	0.47	0.0	0.8367	0.3760	0.3760	226.6	1.577	1.772	1.652	0.784	0.992	1.050	-1075.0820	13.7	10.102		
0.0	0.48	0.0	0.8545	0.3840	0.3840	226.5	1.578	1.771	1.651	0.784	0.991	1.051	-1079.0810	13.6	10.079		
0.0	0.49	0.0	0.8723	0.3920	0.3920	226.4	1.579	1.770	1.650	0.784	0.990	1.052	-1083.0800	13.6	10.056		
0.0	0.50	0.0	0.8901	0.4000	0.4000	226.3	1.580	1.768	1.649	0.784	0.989	1.053	-1087.0790	13.5	10.033		
0.0	0.51	0.0	0.9079	0.4080	0.4080	226.2	1.581	1.767	1.648	0.784	0.988	1.054	-1091.0780	13.5	10.010		
0.0	0.52	0.0	0.9257	0.4160	0.4160	226.1	1.582	1.765	1.647	0.784	0.987	1.055	-1095.0770	13.4	9.987		
0.0	0.53	0.0	0.9435	0.4240	0.4240	226.0	1.583	1.764	1.646	0.784	0.986	1.056	-1099.0760	13.4	9.964		
0.0	0.54	0.0	0.9613	0.4320	0.4320	225.9	1.584	1.763	1.645	0.784	0.985	1.057	-1103.0750	13.3	9.941		
0.0	0.55	0.0	0.9791	0.4400	0.4400	225.8	1.585	1.761	1.644	0.784	0.984	1.058	-1107.0740	13.3	9.918		
0.0	0.56	0.0	0.9969	0.4480	0.4480	225.7	1.586	1.760	1.643	0.784	0.983	1.059	-1111.0730	13.2	9.895		
0.0	0.57	0.0	1.0147	0.4560	0.4560	225.6	1.587	1.759	1.642	0.784	0.982	1.060	-1115.0720	13.2	9.872		
0.0	0.58	0.0	1.0325	0.4640	0.4640	225.5	1.588	1.757	1.641	0.784	0.981	1.061	-1119.0710	13.1	9.849		
0.0	0.59	0.0	1.0503	0.4720	0.4720	225.4	1.589	1.756	1.640	0.784	0.980	1.062	-1123.0700	13.1	9.826		
0.0	0.60	0.0	1.0681	0.4800	0.4800	225.3	1.590	1.754	1.639	0.784	0.979	1.063	-1127.0690	13.0	9.803		
0.0	0.61	0.0	1.0859	0.4880	0.4880	225.2	1.591	1.753	1.638	0.784	0.978	1.064	-1131.0680	13			

Table 25. (cont.)

LIQUID MOLE FRACTION		VAPOR MOLE FRACTION		TEMP	RELATIVE VOL			PRESSURE ACT COEF			ENTHALPY		HEAT CAPACITY	
N2/N2+O2	A4	N2	A4		N2/A4	N2/O2	A4/O2	N2	A4	O2	LIQ	VAP	LIQ	VAP
0.	0.	0.	0.	235.5	1.913	1.799	1.189	0.772	1.030	1.002	-819.	1280.	16.3	11.876
0.	0.01	0.	0.0118	235.4	1.914	1.798	1.187	0.772	1.029	1.003	-823.	1274.	16.3	11.855
0.	0.02	0.	0.0236	235.1	1.915	1.796	1.185	0.772	1.028	1.003	-827.	1268.	16.3	11.831
0.	0.03	0.	0.0353	235.2	1.916	1.795	1.184	0.772	1.028	1.004	-831.	1262.	16.3	11.807
0.	0.04	0.	0.0469	235.1	1.917	1.793	1.182	0.772	1.027	1.005	-835.	1256.	16.3	11.784
0.	0.05	0.	0.0585	235.0	1.918	1.792	1.180	0.772	1.026	1.006	-839.	1250.	16.2	11.761
0.	0.07	0.	0.0814	234.9	1.919	1.788	1.177	0.772	1.025	1.008	-847.	1238.	16.2	11.715
0.	0.10	0.	0.1152	234.6	1.922	1.784	1.172	0.772	1.023	1.011	-858.	1221.	16.2	11.646
0.	0.20	0.	0.2241	233.7	1.930	1.767	1.155	0.771	1.017	1.020	-896.	1167.	16.1	11.425
0.	0.30	0.	0.4276	232.4	1.948	1.734	1.121	0.771	1.007	1.042	-966.	1067.	15.9	11.001
0.	0.40	0.	0.6196	231.4	1.968	1.699	1.086	0.774	0.999	1.069	-1030.	975.	15.7	10.581
0.	0.50	0.	0.8078	230.7	1.991	1.662	1.051	0.778	0.995	1.101	-1099.	886.	15.7	10.143
0.	0.60	0.	0.9929	230.5	1.989	1.643	1.034	0.782	0.995	1.119	-1117.	845.	15.6	9.912
0.10	0.	0.1661	0.	231.5	1.913	1.793	1.189	0.793	1.059	1.028	-790.	1250.	16.2	12.057
0.10	0.01	0.1644	0.0110	231.4	1.914	1.791	1.183	0.793	1.058	1.039	-794.	1244.	16.2	12.044
0.10	0.02	0.1623	0.0219	231.4	1.915	1.790	1.182	0.792	1.057	1.039	-798.	1238.	16.2	12.021
0.10	0.03	0.1604	0.0327	231.3	1.916	1.788	1.180	0.792	1.056	1.040	-802.	1232.	16.2	12.011
0.10	0.04	0.1585	0.0435	231.3	1.917	1.787	1.178	0.792	1.055	1.040	-807.	1226.	16.2	11.975
0.10	0.05	0.1566	0.0543	231.2	1.918	1.785	1.176	0.791	1.054	1.041	-811.	1224.	16.2	11.952
0.10	0.07	0.1528	0.0757	231.2	1.920	1.782	1.173	0.791	1.052	1.042	-819.	1214.	16.2	11.906
0.10	0.10	0.1472	0.1075	231.0	1.922	1.778	1.168	0.790	1.049	1.044	-831.	1199.	16.1	11.838
0.10	0.20	0.1292	0.2109	230.7	1.932	1.762	1.150	0.787	1.040	1.050	-870.	1150.	16.1	11.612
0.10	0.30	0.0952	0.4085	230.2	1.950	1.730	1.116	0.784	1.023	1.066	-945.	1050.	15.9	11.162
0.10	0.40	0.0630	0.6028	229.9	1.967	1.695	1.082	0.782	1.010	1.086	-1015.	973.	15.8	10.698
0.10	0.50	0.0315	0.7974	229.8	1.983	1.660	1.049	0.783	1.001	1.110	-1081.	889.	15.7	10.265
0.10	0.60	0.0159	0.8972	229.1	1.990	1.642	1.032	0.784	0.998	1.124	-1113.	848.	15.6	9.944
0.20	0.	0.3080	0.	227.8	1.918	1.787	1.180	0.812	1.088	1.075	-797.	1221.	16.3	12.268
0.20	0.01	0.3055	0.0102	227.8	1.918	1.786	1.178	0.812	1.087	1.075	-798.	1216.	16.3	12.265
0.20	0.02	0.3022	0.0203	227.8	1.917	1.785	1.177	0.811	1.085	1.076	-798.	1212.	16.3	12.242
0.20	0.03	0.2989	0.0305	227.8	1.918	1.783	1.175	0.811	1.084	1.076	-798.	1207.	16.3	12.219
0.20	0.04	0.2956	0.0406	227.8	1.919	1.782	1.173	0.810	1.082	1.076	-798.	1203.	16.3	12.195
0.20	0.05	0.2924	0.0506	227.8	1.920	1.780	1.171	0.810	1.081	1.076	-799.	1198.	16.3	12.172
0.20	0.07	0.2859	0.0707	227.8	1.922	1.777	1.168	0.809	1.078	1.077	-797.	1190.	16.3	12.123
0.20	0.10	0.2762	0.1008	227.8	1.925	1.772	1.163	0.807	1.074	1.078	-800.	1177.	16.2	12.055
0.20	0.20	0.2444	0.1992	227.8	1.934	1.757	1.145	0.803	1.062	1.081	-842.	1134.	16.1	11.820
0.20	0.30	0.1824	0.3929	227.1	1.952	1.725	1.112	0.796	1.040	1.090	-922.	1052.	16.0	11.332
0.20	0.40	0.1228	0.5875	226.6	1.969	1.692	1.079	0.791	1.021	1.103	-1000.	971.	15.8	10.818
0.20	0.50	0.0823	0.7873	226.3	1.984	1.658	1.047	0.788	1.007	1.120	-1073.	889.	15.7	10.268
0.20	0.60	0.0315	0.8916	225.8	1.993	1.641	1.031	0.787	1.001	1.129	-1109.	846.	15.6	9.976
0.40	0.	0.5420	0.	221.2	1.921	1.775	1.167	0.851	1.147	1.155	-685.	1165.	16.8	12.752
0.40	0.01	0.5369	0.0089	221.3	1.922	1.773	1.166	0.850	1.144	1.154	-689.	1162.	16.8	12.834
0.40	0.02	0.5319	0.0178	221.4	1.923	1.772	1.164	0.849	1.142	1.154	-693.	1158.	16.8	12.807
0.40	0.03	0.5269	0.0267	221.4	1.924	1.771	1.162	0.848	1.140	1.153	-700.	1155.	16.7	12.779
0.40	0.04	0.5219	0.0357	221.5	1.925	1.769	1.160	0.848	1.138	1.153	-704.	1152.	16.7	12.751
0.40	0.05	0.5169	0.0446	221.6	1.926	1.768	1.159	0.847	1.136	1.152	-709.	1149.	16.7	12.723
0.40	0.07	0.5068	0.0624	221.7	1.928	1.765	1.155	0.845	1.132	1.152	-719.	1142.	16.7	12.688
0.40	0.10	0.4918	0.0892	221.9	1.931	1.761	1.150	0.843	1.126	1.150	-733.	1133.	16.6	12.603
0.40	0.20	0.4415	0.1792	222.6	1.940	1.746	1.134	0.835	1.107	1.147	-781.	1101.	16.6	12.297
0.40	0.30	0.3397	0.3634	224.2	1.958	1.716	1.104	0.821	1.074	1.142	-876.	1035.	16.2	11.702
0.40	0.40	0.2340	0.5578	226.0	1.973	1.685	1.071	0.808	1.044	1.139	-966.	965.	15.9	11.070
0.40	0.50	0.1210	0.7878	227.0	1.986	1.654	1.043	0.797	1.018	1.139	-1057.	889.	15.7	10.396
0.40	0.60	0.0223	0.8807	228.1	1.992	1.639	1.029	0.791	1.007	1.139	-1108.	847.	15.7	10.040
0.60	0.	0.7249	0.	215.4	1.927	1.757	1.151	0.892	1.213	1.240	-610.	1110.	17.4	13.451
0.60	0.01	0.7190	0.0079	215.6	1.928	1.755	1.149	0.891	1.210	1.247	-615.	1108.	17.3	13.413
0.60	0.02	0.7131	0.0159	215.7	1.929	1.754	1.147	0.890	1.207	1.246	-621.	1106.	17.3	13.375
0.60	0.03	0.7072	0.0238	215.8	1.930	1.753	1.146	0.888	1.204	1.244	-626.	1104.	17.3	13.337
0.60	0.04	0.7013	0.0318	215.9	1.931	1.752	1.144	0.887	1.201	1.243	-632.	1102.	17.3	13.299
0.60	0.05	0.6954	0.0398	216.0	1.932	1.750	1.143	0.886	1.198	1.241	-637.	1099.	17.3	13.261
0.60	0.07	0.6834	0.0559	216.3	1.934	1.748	1.140	0.883	1.192	1.239	-648.	1095.	17.2	13.205
0.60	0.10	0.6655	0.0802	216.6	1.937	1.744	1.135	0.880	1.184	1.234	-665.	1089.	17.1	13.171
0.60	0.20	0.6045	0.1628	217.9	1.947	1.732	1.120	0.868	1.168	1.221	-719.	1066.	16.9	12.889
0.60	0.30	0.4759	0.3361	220.5	1.964	1.706	1.091	0.846	1.110	1.198	-828.	1016.	16.5	12.121
0.60	0.40	0.3354	0.5313	223.5	1.978	1.678	1.063	0.826	1.068	1.177	-939.	958.	16.1	11.338
0.60	0.50	0.1766	0.7493	226.7	1.989	1.650	1.039	0.808	1.030	1.158	-1041.	886.	15.8	10.526
0.60	0.60	0.0224	0.8700	228.5	1.993	1.637	1.027	0.796	1.013	1.149	-1092.	846.	15.7	10.185
0.80	0.	0.8738	0.	210.2	1.931	1.751	1.131	0.930	1.202	1.364	-534.	1055.	17.9	14.752
0.80	0.01	0.8679	0.0072	210.3	1.932	1.750	1.130	0.927	1.200	1.361	-540.	1054.	17.9	14.693
0.80	0.02	0.8612	0.0143	210.5	1.933	1.750	1.128	0.926	1.203	1.358	-546.	1053.	17.9	14.634
0.80	0.03	0.8548	0.0215	210.6	1.934	1.749	1.127	0.924	1.207	1.355	-552.	1052.	17.8	14.576
0.80	0.04	0.8485	0.0288	210.8	1.935	1.748	1.125	0.923	1.205	1.352	-559.	1050.	17.8	14.519
0.80	0.05	0.8420	0.0361	211.0	1.936	1.747	1.124	0.920	1.202	1.349	-565.	1049.	17.8	14.462
0.80	0.07	0.8292	0.0507	211.3	1.939	1.745	1.121	0.927	1.204	1.343	-577.	1047.	17.7	14.348
0.80	0.10													

LIQUID MOLE FRACTION		VAPOR MOLE FRACTION			TEMP	RELATIVE VOL				PRESSURE AUT COEF			ENTHALPY BTU/LB MOLE		HEAT CAPACITY BTU/LB MOLE-R	
N2/N2+O2	AR	N2	AR	O2		N	N2/AR	N2/O2	AR/O2	N2	AR	O2	LIG	VAP	LIG	VAP
0.	0.	0.	0.	1.0000	234.5	1.707	1.774	1.178	0.784	1.023	1.001	-753.	1271.	16.9	12.659	
0.	0.01	0.	0.0117	0.9883	234.4	1.707	1.773	1.176	0.784	1.023	1.002	-757.	1265.	16.9	12.636	
0.	0.02	0.	0.0234	0.9766	234.3	1.708	1.771	1.174	0.784	1.022	1.003	-762.	1258.	16.9	12.613	
0.	0.03	0.	0.0351	0.9650	234.2	1.709	1.769	1.173	0.784	1.022	1.004	-766.	1252.	16.9	12.591	
0.	0.04	0.	0.0468	0.9535	234.1	1.709	1.767	1.171	0.784	1.021	1.005	-770.	1246.	16.8	12.568	
0.	0.05	0.	0.0585	0.9420	234.0	1.710	1.766	1.170	0.784	1.020	1.006	-774.	1241.	16.8	12.546	
0.	0.07	0.	0.0807	0.9193	233.8	1.711	1.762	1.166	0.784	1.019	1.008	-782.	1229.	16.8	12.501	
0.	0.10	0.	0.1143	0.8857	233.6	1.713	1.757	1.161	0.783	1.018	1.011	-794.	1211.	16.7	12.435	
0.	0.20	0.	0.2226	0.7779	233.7	1.719	1.739	1.145	0.783	1.013	1.021	-832.	1196.	16.6	12.220	
0.	0.40	0.	0.4258	0.5743	233.3	1.732	1.704	1.112	0.782	1.004	1.043	-903.	1055.	16.4	11.802	
0.	0.60	0.	0.6181	0.3819	233.3	1.746	1.658	1.079	0.784	0.997	1.069	-967.	962.	16.2	11.378	
0.	0.80	0.	0.8071	0.1929	234.6	1.760	1.631	1.046	0.789	0.994	1.100	-1036.	874.	16.1	10.930	
0.	0.90	0.	0.9076	0.0974	234.4	1.767	1.613	1.020	0.772	0.994	1.118	-1094.	811.	16.1	10.691	
0.10	0.	0.1635	0.	0.8365	235.3	1.499	1.759	1.173	0.784	1.025	1.041	-727.	1239.	16.7	12.913	
0.10	0.01	0.1616	0.0109	0.8274	235.3	1.500	1.757	1.171	0.784	1.024	1.041	-731.	1233.	16.7	12.890	
0.10	0.02	0.1597	0.0217	0.8186	235.2	1.501	1.756	1.170	0.784	1.023	1.042	-735.	1228.	16.7	12.867	
0.10	0.03	0.1578	0.0325	0.8097	235.2	1.502	1.754	1.168	0.783	1.022	1.043	-739.	1223.	16.7	12.844	
0.10	0.04	0.1560	0.0432	0.8008	235.1	1.503	1.753	1.166	0.783	1.021	1.043	-744.	1218.	16.7	12.821	
0.10	0.05	0.1541	0.0539	0.7920	235.1	1.503	1.751	1.165	0.783	1.020	1.043	-748.	1213.	16.6	12.798	
0.10	0.07	0.1504	0.0782	0.7744	235.1	1.505	1.748	1.161	0.782	1.018	1.045	-756.	1202.	16.6	12.753	
0.10	0.10	0.1449	0.1088	0.7482	234.9	1.507	1.743	1.157	0.781	1.016	1.046	-768.	1187.	16.5	12.684	
0.10	0.20	0.1272	0.2099	0.6828	234.5	1.515	1.728	1.140	0.779	1.013	1.053	-807.	1139.	16.5	12.458	
0.10	0.40	0.0938	0.4084	0.4978	234.1	1.531	1.689	1.108	0.775	1.021	1.066	-882.	1047.	16.3	11.999	
0.10	0.60	0.0620	0.6021	0.3359	233.9	1.546	1.662	1.075	0.773	1.009	1.087	-953.	959.	16.2	11.519	
0.10	0.80	0.0311	0.7971	0.1718	233.9	1.560	1.626	1.044	0.773	1.000	1.110	-1019.	874.	16.1	11.003	
0.10	0.90	0.0150	0.8971	0.0873	234.1	1.567	1.611	1.020	0.774	0.997	1.123	-1076.	811.	16.1	10.728	
0.20	0.	0.3346	0.	0.6654	231.6	1.494	1.747	1.168	0.804	1.026	1.080	-699.	1209.	16.7	13.200	
0.20	0.01	0.3327	0.0101	0.6553	231.6	1.497	1.746	1.166	0.803	1.025	1.080	-703.	1204.	16.7	13.176	
0.20	0.02	0.3308	0.0202	0.6452	231.6	1.498	1.744	1.165	0.803	1.024	1.080	-707.	1200.	16.7	13.153	
0.20	0.03	0.3289	0.0304	0.6351	231.6	1.499	1.743	1.163	0.802	1.023	1.081	-711.	1195.	16.7	13.129	
0.20	0.04	0.3270	0.0406	0.6250	231.6	1.499	1.741	1.161	0.802	1.021	1.081	-715.	1191.	16.7	13.105	
0.20	0.05	0.3251	0.0508	0.6149	231.6	1.500	1.740	1.160	0.801	1.020	1.081	-719.	1186.	16.7	13.081	
0.20	0.07	0.3214	0.0705	0.6048	231.6	1.502	1.737	1.156	0.800	1.017	1.082	-725.	1177.	16.6	13.033	
0.20	0.10	0.3177	0.1004	0.5947	231.6	1.505	1.732	1.151	0.799	1.015	1.082	-736.	1164.	16.6	12.961	
0.20	0.20	0.2967	0.1988	0.5659	231.6	1.514	1.718	1.135	0.794	1.011	1.085	-779.	1121.	16.5	12.710	
0.20	0.40	0.1902	0.3926	0.4272	231.9	1.530	1.688	1.103	0.787	1.019	1.094	-866.	1038.	16.4	12.207	
0.20	0.60	0.121	0.5879	0.2921	232.5	1.546	1.657	1.072	0.782	1.021	1.106	-938.	956.	16.2	11.664	
0.20	0.80	0.0619	0.7874	0.1612	233.2	1.560	1.626	1.042	0.778	1.009	1.120	-1011.	873.	16.1	11.177	
0.20	0.90	0.0311	0.8918	0.0772	233.7	1.567	1.610	1.027	0.778	1.000	1.128	-1076.	811.	16.1	10.765	
0.40	0.	0.5346	0.	0.4654	225.0	1.494	1.725	1.195	0.843	1.144	1.164	-643.	1151.	17.1	13.932	
0.40	0.01	0.5327	0.0101	0.4553	225.1	1.495	1.724	1.193	0.842	1.144	1.163	-647.	1146.	17.1	13.909	
0.40	0.02	0.5308	0.0202	0.4452	225.1	1.496	1.722	1.192	0.841	1.144	1.163	-651.	1141.	17.1	13.886	
0.40	0.03	0.5289	0.0304	0.4351	225.2	1.497	1.721	1.190	0.840	1.142	1.162	-655.	1136.	17.1	13.862	
0.40	0.04	0.5270	0.0406	0.4250	225.3	1.498	1.720	1.188	0.839	1.140	1.162	-659.	1131.	17.0	13.838	
0.40	0.05	0.5251	0.0508	0.4149	225.3	1.499	1.719	1.187	0.838	1.138	1.161	-663.	1126.	17.0	13.814	
0.40	0.07	0.5214	0.0705	0.4048	225.5	1.501	1.716	1.183	0.837	1.136	1.160	-669.	1117.	17.0	13.761	
0.40	0.10	0.5177	0.1004	0.3947	225.7	1.504	1.712	1.178	0.834	1.134	1.159	-679.	1104.	16.9	13.720	
0.40	0.20	0.4957	0.1988	0.3659	226.4	1.513	1.699	1.163	0.828	1.128	1.159	-719.	1060.	16.8	13.515	
0.40	0.40	0.335	0.3847	0.3003	228.0	1.531	1.673	1.093	0.812	1.075	1.148	-814.	1019.	16.5	12.868	
0.40	0.60	0.2307	0.5892	0.2107	229.0	1.547	1.646	1.064	0.799	1.048	1.143	-906.	949.	16.3	11.967	
0.40	0.80	0.1209	0.7889	0.1111	231.9	1.561	1.620	1.038	0.787	1.019	1.140	-999.	873.	16.2	11.227	
0.40	0.90	0.0619	0.8918	0.0573	233.7	1.567	1.607	1.025	0.781	1.008	1.138	-1076.	811.	16.1	10.839	
0.60	0.	0.7189	0.	0.2811	219.2	1.494	1.701	1.136	0.888	1.219	1.262	-545.	1094.	17.7	14.962	
0.60	0.01	0.7170	0.0101	0.2710	219.3	1.495	1.700	1.137	0.884	1.218	1.260	-549.	1089.	17.6	14.937	
0.60	0.02	0.7151	0.0202	0.2609	219.4	1.496	1.699	1.136	0.883	1.218	1.259	-553.	1084.	17.6	14.912	
0.60	0.03	0.7132	0.0304	0.2508	219.5	1.497	1.698	1.134	0.881	1.216	1.257	-557.	1079.	17.6	14.887	
0.60	0.04	0.7113	0.0406	0.2407	219.6	1.498	1.697	1.133	0.880	1.215	1.256	-561.	1074.	17.6	14.862	
0.60	0.05	0.7094	0.0508	0.2306	219.6	1.499	1.696	1.131	0.879	1.214	1.254	-565.	1069.	17.6	14.837	
0.60	0.07	0.7075	0.0705	0.2205	219.6	1.499	1.695	1.129	0.878	1.213	1.251	-569.	1064.	17.5	14.812	
0.60	0.10	0.7056	0.1004	0.2104	219.6	1.500	1.694	1.127	0.877	1.212	1.249	-573.	1059.	17.5	14.787	
0.60	0.20	0.6836	0.1988	0.2373	220.4	1.505	1.691	1.124	0.872	1.199	1.246	-608.	1022.	17.4	14.514	
0.60	0.40	0.471	0.3849	0.1800	224.3	1.523	1.658	1.082	0.860	1.183	1.232	-705.	949.	17.2	14.068	
0.60	0.60	0.339	0.5843	0.1348	227.3	1.548	1.636	1.057	0.847	1.071	1.192	-803.	871.	16.8	13.181	
0.60	0.80	0.176	0.7913	0.0727	230.8	1.562	1.614	1.034	0.796	1.031	1.180	-906.	801.	16.5	12.200	
0.60	0.90	0.0619	0.8918	0.0573	233.4	1.568	1.601	1.025	0.786	1.021	1.169	-999.	725.	16.2	11.301	
0.80	0.	0.8711	0.	0.1289	213.2	1.494	1.673	1.192	0.935	1.304	1.383	-468.	1039.	18.3	16.482	
0.80	0.01	0.8692	0.0101	0.1188	214.0	1.495	1.672	1.191	0.933	1.299	1.380	-472.	1034.	18.2	16.457	
0.80	0.02	0.8673	0.02													

Table 25. (cont.)

PRESSURE = 21. ATM

LIQUID MOLE FRACTION				VAPOR MOLE FRACTION			TEMP	RELATIVE VOL			PRESSURE ACT COEF			ENTHALPY BTU/LB MOLE		HEAT CAPACITY BTU/LB MOLE	
N ₂ /N ₂ +O ₂	AR	O ₂		N ₂	AR	O ₂		N ₂ /AR	N ₂ /O ₂	AR/O ₂	N ₂	AR	O ₂	LIG	VAP	LIG	VAP
0.	0.	1.0000		0.	0.	1.0000	244.9	1.512	1.746	1.154	0.758	1.016	1.000	-659.1252	17.8	14.058	
0.	0.01	0.9894		0.0116	0.9884		244.8	1.513	1.746	1.152	0.758	1.013	1.001	-664.1246	17.8	14.057	
0.	0.02	0.9789		0.0231	0.9769		244.7	1.513	1.746	1.150	0.758	1.013	1.002	-668.1240	17.8	14.056	
0.	0.03	0.9684		0.0346	0.9654		244.6	1.513	1.746	1.148	0.758	1.014	1.003	-672.1233	17.8	14.055	
0.	0.04	0.9579		0.0460	0.9549		244.5	1.513	1.746	1.146	0.758	1.014	1.004	-676.1227	17.7	14.054	
0.	0.05	0.9474		0.0574	0.9424		244.4	1.514	1.746	1.144	0.758	1.014	1.005	-680.1221	17.7	14.053	
0.	0.06	0.9369		0.0688	0.9319		244.3	1.514	1.746	1.142	0.758	1.013	1.006	-684.1215	17.7	14.052	
0.	0.07	0.9264		0.0802	0.9214		244.2	1.514	1.746	1.140	0.757	1.012	1.007	-688.1209	17.7	14.051	
0.	0.08	0.9159		0.0916	0.9109		244.1	1.514	1.746	1.138	0.757	1.012	1.008	-692.1203	17.7	14.050	
0.	0.09	0.9054		0.1030	0.9014		244.0	1.514	1.746	1.136	0.757	1.011	1.009	-696.1197	17.7	14.049	
0.	0.10	0.8949		0.1144	0.8919		243.9	1.514	1.746	1.134	0.757	1.011	1.010	-700.1191	17.7	14.048	
0.10	0.	0.1812		0.0100	0.7388		243.8	1.499	1.720	1.133	0.777	1.008	1.021	-704.1185	17.7	14.047	
0.10	0.01	0.1594		0.0100	0.6294		243.7	1.499	1.720	1.133	0.777	1.008	1.021	-708.1179	17.7	14.046	
0.10	0.02	0.1375		0.0215	0.6210		243.6	1.499	1.720	1.133	0.777	1.008	1.021	-712.1173	17.7	14.045	
0.10	0.03	0.1157		0.0322	0.6127		243.5	1.499	1.720	1.133	0.777	1.008	1.021	-716.1167	17.7	14.044	
0.10	0.04	0.0939		0.0429	0.6044		243.4	1.499	1.720	1.133	0.777	1.008	1.021	-720.1161	17.7	14.043	
0.10	0.05	0.0721		0.0535	0.5961		243.3	1.499	1.720	1.133	0.777	1.008	1.021	-724.1155	17.7	14.042	
0.10	0.06	0.0503		0.0642	0.5878		243.2	1.499	1.720	1.133	0.777	1.008	1.021	-728.1149	17.7	14.041	
0.10	0.07	0.0285		0.0749	0.5795		243.1	1.499	1.720	1.133	0.777	1.008	1.021	-732.1143	17.7	14.040	
0.10	0.08	0.0067		0.0856	0.5712		243.0	1.499	1.720	1.133	0.777	1.008	1.021	-736.1137	17.7	14.039	
0.10	0.09	0.0000		0.0963	0.5629		242.9	1.499	1.720	1.133	0.777	1.008	1.021	-740.1131	17.7	14.038	
0.20	0.	0.2091		0.	0.7009		238.4	1.550	1.560	1.023	0.766	1.001	1.111	-931.848	16.8	12.467	
0.20	0.01	0.2059		0.0101	0.6940		238.3	1.481	1.707	1.153	0.766	1.007	1.089	-932.842	16.8	12.466	
0.20	0.02	0.2028		0.0201	0.6871		238.2	1.482	1.708	1.151	0.767	1.008	1.090	-933.836	16.8	12.465	
0.20	0.03	0.2000		0.0302	0.6802		238.1	1.483	1.708	1.150	0.767	1.008	1.090	-934.830	16.8	12.464	
0.20	0.04	0.2000		0.0402	0.6733		238.0	1.483	1.708	1.148	0.766	1.008	1.090	-935.824	16.8	12.463	
0.20	0.05	0.2033		0.0502	0.6665		237.9	1.484	1.707	1.146	0.766	1.008	1.090	-936.818	16.8	12.462	
0.20	0.06	0.2077		0.0601	0.6596		237.8	1.485	1.707	1.145	0.766	1.008	1.090	-937.812	16.8	12.461	
0.20	0.07	0.2132		0.0701	0.6527		237.7	1.486	1.707	1.144	0.766	1.008	1.091	-938.806	16.8	12.460	
0.20	0.08	0.2197		0.0801	0.6458		237.6	1.487	1.707	1.143	0.766	1.008	1.091	-939.800	16.8	12.459	
0.20	0.09	0.2272		0.0901	0.6389		237.5	1.488	1.707	1.142	0.766	1.008	1.091	-940.794	16.8	12.458	
0.20	0.10	0.2357		0.1001	0.6320		237.4	1.489	1.707	1.141	0.766	1.008	1.091	-941.788	16.8	12.457	
0.20	0.11	0.2452		0.1101	0.6251		237.3	1.490	1.707	1.140	0.766	1.008	1.091	-942.782	16.8	12.456	
0.20	0.12	0.2557		0.1201	0.6182		237.2	1.491	1.707	1.139	0.766	1.008	1.091	-943.776	16.8	12.455	
0.20	0.13	0.2672		0.1301	0.6113		237.1	1.492	1.707	1.138	0.766	1.008	1.091	-944.770	16.8	12.454	
0.20	0.14	0.2797		0.1401	0.6044		237.0	1.493	1.707	1.137	0.766	1.008	1.091	-945.764	16.8	12.453	
0.20	0.15	0.2932		0.1501	0.5975		236.9	1.494	1.707	1.136	0.766	1.008	1.091	-946.758	16.8	12.452	
0.20	0.16	0.3077		0.1601	0.5906		236.8	1.495	1.707	1.135	0.766	1.008	1.091	-947.752	16.8	12.451	
0.20	0.17	0.3232		0.1701	0.5837		236.7	1.496	1.707	1.134	0.766	1.008	1.091	-948.746	16.8	12.450	
0.20	0.18	0.3397		0.1801	0.5768		236.6	1.497	1.707	1.133	0.766	1.008	1.091	-949.740	16.8	12.449	
0.20	0.19	0.3572		0.1901	0.5699		236.5	1.498	1.707	1.132	0.766	1.008	1.091	-950.734	16.8	12.448	
0.20	0.20	0.3757		0.2001	0.5630		236.4	1.499	1.707	1.131	0.766	1.008	1.091	-951.728	16.8	12.447	
0.20	0.21	0.3952		0.2101	0.5561		236.3	1.500	1.707	1.130	0.766	1.008	1.091	-952.722	16.8	12.446	
0.20	0.22	0.4157		0.2201	0.5492		236.2	1.501	1.707	1.129	0.766	1.008	1.091	-953.716	16.8	12.445	
0.20	0.23	0.4372		0.2301	0.5423		236.1	1.502	1.707	1.128	0.766	1.008	1.091	-954.710	16.8	12.444	
0.20	0.24	0.4597		0.2401	0.5354		236.0	1.503	1.707	1.127	0.766	1.008	1.091	-955.704	16.8	12.443	
0.20	0.25	0.4832		0.2501	0.5285		235.9	1.504	1.707	1.126	0.766	1.008	1.091	-956.698	16.8	12.442	
0.20	0.26	0.5077		0.2601	0.5216		235.8	1.505	1.707	1.125	0.766	1.008	1.091	-957.692	16.8	12.441	
0.20	0.27	0.5332		0.2701	0.5147		235.7	1.506	1.707	1.124	0.766	1.008	1.091	-958.686	16.8	12.440	
0.20	0.28	0.5597		0.2801	0.5078		235.6	1.507	1.707	1.123	0.766	1.008	1.091	-959.680	16.8	12.439	
0.20	0.29	0.5872		0.2901	0.5009		235.5	1.508	1.707	1.122	0.766	1.008	1.091	-960.674	16.8	12.438	
0.20	0.30	0.6157		0.3001	0.4940		235.4	1.509	1.707	1.121	0.766	1.008	1.091	-961.668	16.8	12.437	
0.20	0.31	0.6452		0.3101	0.4871		235.3	1.510	1.707	1.120	0.766	1.008	1.091	-962.662	16.8	12.436	
0.20	0.32	0.6757		0.3201	0.4802		235.2	1.511	1.707	1.119	0.766	1.008	1.091	-963.656	16.8	12.435	
0.20	0.33	0.7072		0.3301	0.4733		235.1	1.512	1.707	1.118	0.766	1.008	1.091	-964.650	16.8	12.434	
0.20	0.34	0.7397		0.3401	0.4664		235.0	1.513	1.707	1.117	0.766	1.008	1.091	-965.644	16.8	12.433	
0.20	0.35	0.7732		0.3501	0.4595		234.9	1.514	1.707	1.116	0.766	1.008	1.091	-966.638	16.8	12.432	
0.20	0.36	0.8077		0.3601	0.4526		234.8	1.515	1.707	1.115	0.766	1.008	1.091	-967.632	16.8	12.431	
0.20	0.37	0.8432		0.3701	0.4457		234.7	1.516	1.707	1.114	0.766	1.008	1.091	-968.626	16.8	12.430	
0.20	0.38	0.8797		0.3801	0.4388		234.6	1.517	1.707	1.113	0.766	1.008	1.091	-969.620	16.8	12.429	
0.20	0.39	0.9172		0.3901	0.4319		234.5	1.518	1.707	1.112	0.766	1.008	1.091	-970.614	16.8	12.428	
0.20	0.40	0.9557		0.4001	0.4250		234.4	1.519	1.707	1.111	0.766	1.008	1.091	-971.608	16.8	12.427	
0.20	0.41	0.9952		0.4101	0.4181		234.3	1.520	1.707	1.110	0.766	1.008	1.091	-972.602	16.8	12.426	
0.20	0.42	1.0357		0.4201	0.4112		234.2	1.521	1.707	1.109	0.766	1.008	1.091	-973.596	16.8	12.425	
0.20	0.43	1.0772		0.4301	0.4043		234.1	1.522	1.707	1.108	0.766	1.00					

LIQUID MOLE FRACTION		VAPOR MOLE FRACTION		TEMP	RELATIVE VOL			PRESSURE ACT COEF			ENTHALPY BTU/LB MOLE		HEAT CAPACITY BTU/LB MOLE-°F		
N2/N2+O2	AR	N2	AR	O2	N2/AR	N2/O2	AR/O2	N2	AR	O2	LIQ	VAP	LIQ	VAP	
0.10	0.	0.1000	0.	0.1000	245.0	1.501	1.722	1.147	0.780	1.053	1.053	-559.	1184.	18.1	16.636
0.10	0.01	0.1067	0.0107	0.1037	244.9	1.501	1.720	1.146	0.780	1.052	1.053	-563.	1179.	18.1	16.614
0.10	0.02	0.1134	0.0213	0.1024	244.9	1.502	1.718	1.144	0.780	1.052	1.054	-568.	1174.	18.1	16.591
0.10	0.03	0.1201	0.0319	0.1013	244.9	1.502	1.717	1.143	0.779	1.051	1.054	-572.	1168.	18.0	16.568
0.10	0.04	0.1268	0.0425	0.1003	244.8	1.502	1.715	1.141	0.779	1.050	1.055	-576.	1163.	18.0	16.545
0.10	0.05	0.1335	0.0530	0.0994	244.7	1.503	1.713	1.140	0.779	1.049	1.055	-580.	1158.	18.0	16.522
0.10	0.06	0.1402	0.0635	0.0985	244.7	1.504	1.711	1.137	0.778	1.048	1.057	-584.	1153.	18.0	16.499
0.10	0.07	0.1469	0.0740	0.0976	244.6	1.505	1.709	1.133	0.777	1.045	1.058	-588.	1148.	18.0	16.476
0.10	0.08	0.1536	0.0845	0.0967	244.5	1.510	1.698	1.118	0.774	1.038	1.064	-592.	1143.	17.8	16.453
0.10	0.09	0.1603	0.0950	0.0958	243.9	1.520	1.686	1.099	0.769	1.024	1.070	-596.	1138.	17.7	16.430
0.10	0.10	0.1670	0.1055	0.0949	243.8	1.530	1.675	1.082	0.766	1.013	1.075	-600.	1133.	17.5	16.407
0.10	0.11	0.1737	0.1160	0.0940	244.0	1.542	1.595	1.034	0.765	1.004	1.113	-604.	1128.	17.4	16.384
0.10	0.12	0.1804	0.1265	0.0931	244.2	1.546	1.581	1.021	0.765	1.000	1.123	-608.	1123.	17.4	16.361
0.20	0.	0.2000	0.	0.2000	245.0	1.478	1.686	1.140	0.800	1.092	1.102	-534.	1147.	17.8	17.421
0.20	0.01	0.2067	0.0107	0.1967	244.9	1.479	1.685	1.139	0.799	1.091	1.102	-538.	1142.	17.8	17.398
0.20	0.02	0.2134	0.0213	0.1924	244.9	1.480	1.683	1.138	0.799	1.089	1.102	-542.	1137.	17.8	17.375
0.20	0.03	0.2201	0.0319	0.1881	244.9	1.481	1.682	1.136	0.798	1.088	1.102	-547.	1132.	17.7	17.352
0.20	0.04	0.2268	0.0425	0.1838	244.9	1.481	1.681	1.135	0.798	1.087	1.102	-551.	1127.	17.7	17.329
0.20	0.05	0.2335	0.0530	0.1795	244.9	1.482	1.680	1.133	0.797	1.086	1.102	-555.	1122.	17.7	17.306
0.20	0.06	0.2402	0.0635	0.1752	244.8	1.484	1.677	1.130	0.796	1.083	1.103	-559.	1117.	17.7	17.283
0.20	0.07	0.2469	0.0740	0.1709	244.7	1.486	1.673	1.126	0.795	1.080	1.103	-563.	1112.	17.7	17.260
0.20	0.08	0.2536	0.0845	0.1666	244.6	1.493	1.660	1.112	0.790	1.080	1.105	-567.	1107.	17.6	17.237
0.20	0.09	0.2603	0.0950	0.1623	244.5	1.508	1.635	1.095	0.782	1.077	1.110	-571.	1102.	17.5	17.214
0.20	0.10	0.2670	0.1055	0.1580	243.9	1.523	1.611	1.080	0.775	1.070	1.117	-575.	1097.	17.5	17.191
0.20	0.11	0.2737	0.1160	0.1537	243.2	1.539	1.588	1.062	0.769	1.061	1.125	-579.	1092.	17.4	17.168
0.20	0.12	0.2804	0.1265	0.1494	243.8	1.547	1.577	1.050	0.767	1.053	1.129	-583.	1087.	17.4	17.145
0.40	0.	0.4000	0.	0.4000	245.0	1.450	1.632	1.120	0.830	1.100	1.201	-463.	1078.	17.8	18.333
0.40	0.01	0.4067	0.0107	0.3967	244.2	1.451	1.632	1.124	0.830	1.100	1.201	-468.	1073.	17.8	18.310
0.40	0.02	0.4134	0.0213	0.3924	244.2	1.452	1.631	1.123	0.830	1.100	1.201	-473.	1068.	17.8	18.287
0.40	0.03	0.4201	0.0319	0.3881	244.3	1.453	1.630	1.122	0.830	1.100	1.200	-478.	1063.	17.8	18.264
0.40	0.04	0.4268	0.0425	0.3838	244.4	1.454	1.629	1.120	0.830	1.100	1.199	-483.	1058.	17.8	18.241
0.40	0.05	0.4335	0.0530	0.3795	244.4	1.455	1.628	1.119	0.830	1.100	1.198	-488.	1053.	17.8	18.218
0.40	0.06	0.4402	0.0635	0.3752	244.4	1.457	1.627	1.118	0.830	1.100	1.197	-493.	1048.	17.8	18.195
0.40	0.07	0.4469	0.0740	0.3709	244.4	1.458	1.626	1.117	0.830	1.100	1.196	-498.	1043.	17.7	18.172
0.40	0.08	0.4536	0.0845	0.3666	244.3	1.460	1.624	1.116	0.830	1.100	1.194	-503.	1038.	17.7	18.149
0.40	0.09	0.4603	0.0950	0.3623	244.3	1.470	1.616	1.099	0.822	1.100	1.196	-507.	1033.	17.6	18.126
0.40	0.10	0.4670	0.1055	0.3580	244.2	1.481	1.601	1.074	0.806	1.091	1.173	-511.	1028.	17.4	18.103
0.40	0.11	0.4737	0.1160	0.3537	244.1	1.491	1.587	1.050	0.799	1.080	1.161	-515.	1023.	17.3	18.080
0.40	0.12	0.4804	0.1265	0.3494	244.1	1.502	1.572	1.028	0.799	1.070	1.148	-519.	1018.	17.3	18.057
0.60	0.	0.6000	0.	0.6000	245.0	1.343	1.570	1.037	0.772	1.011	1.141	-401.	1000.	17.3	18.327
0.60	0.01	0.6067	0.0107	0.5967	244.3	1.343	1.568	1.110	0.830	1.052	1.316	-383.	1000.	18.3	22.304
0.60	0.02	0.6134	0.0213	0.5924	244.4	1.342	1.568	1.108	0.830	1.052	1.313	-388.	1000.	18.3	22.281
0.60	0.03	0.6201	0.0319	0.5881	244.5	1.343	1.567	1.107	0.830	1.052	1.311	-393.	1000.	18.3	22.258
0.60	0.04	0.6268	0.0425	0.5838	244.6	1.345	1.567	1.106	0.830	1.052	1.309	-398.	1000.	18.2	22.235
0.60	0.05	0.6335	0.0530	0.5795	244.6	1.346	1.566	1.105	0.830	1.052	1.307	-403.	1000.	18.2	22.212
0.60	0.06	0.6402	0.0635	0.5752	244.6	1.347	1.566	1.104	0.830	1.052	1.305	-408.	1000.	18.2	22.189
0.60	0.07	0.6469	0.0740	0.5709	244.6	1.349	1.565	1.103	0.830	1.052	1.303	-413.	1000.	18.2	22.166
0.60	0.08	0.6536	0.0845	0.5666	244.5	1.350	1.564	1.102	0.830	1.052	1.301	-418.	1000.	18.2	22.143
0.60	0.09	0.6603	0.0950	0.5623	244.5	1.351	1.564	1.101	0.830	1.052	1.300	-423.	1000.	18.2	22.120
0.60	0.10	0.6670	0.1055	0.5580	244.4	1.352	1.564	1.100	0.830	1.052	1.298	-428.	1000.	18.2	22.097
0.60	0.11	0.6737	0.1160	0.5537	244.4	1.353	1.564	1.099	0.830	1.052	1.296	-433.	1000.	18.2	22.074
0.60	0.12	0.6804	0.1265	0.5494	244.3	1.354	1.564	1.098	0.830	1.052	1.294	-438.	1000.	18.2	22.051
0.80	0.	0.8000	0.	0.8000	245.0	1.240	1.540	1.030	0.700	1.000	1.171	-316.	1000.	17.3	19.259
0.80	0.01	0.8067	0.0107	0.7967	244.2	1.241	1.540	1.092	0.777	1.019	1.153	-304.	1000.	18.3	14.479
0.80	0.02	0.8134	0.0213	0.7924	244.3	1.241	1.540	1.091	0.777	1.019	1.151	-310.	1000.	18.3	20.371
0.80	0.03	0.8201	0.0319	0.7881	244.4	1.241	1.540	1.090	0.777	1.019	1.149	-316.	1000.	18.3	20.263
0.80	0.04	0.8268	0.0425	0.7838	244.5	1.241	1.540	1.089	0.777	1.019	1.147	-322.	1000.	18.3	20.155
0.80	0.05	0.8335	0.0530	0.7795	244.5	1.242	1.540	1.088	0.777	1.019	1.145	-328.	1000.	18.3	20.047
0.80	0.06	0.8402	0.0635	0.7752	244.5	1.242	1.540	1.087	0.777	1.019	1.143	-334.	1000.	18.3	19.939
0.80	0.07	0.8469	0.0740	0.7709	244.5	1.242	1.540	1.086	0.777	1.019	1.141	-340.	1000.	18.3	19.831
0.80	0.08	0.8536	0.0845	0.7666	244.4	1.243	1.540	1.085	0.777	1.019	1.139	-346.	1000.	18.3	19.723
0.80	0.09	0.8603	0.0950	0.7623	244.4	1.243	1.540	1.084	0.777	1.019	1.137	-352.	1000.	18.3	19.615
0.80	0.10	0.8670	0.1055	0.7580	244.4	1.243	1.540	1.083	0.777	1.019	1.135	-358.	1000.	18.3	19.507
0.80	0.11	0.8737	0.1160	0.7537	244.3	1.244	1.540	1.082	0.777	1.019	1.133	-364.	1000.	18.3	19.399
0.80	0.12	0.8804	0.1265	0.7494	244.3	1.244	1.540	1.081	0.777	1.019	1.131	-370.	1000.	18.3	19.291
1.00	0.	1.0000	0.	1.0000	245.0	1.000	1.000	1.000	0.700	1.000	1.171	-241.	1000.	17.3	18.777
1.00	0.01	0.9933	0.0107	0.9867	244.2	1.000	1.000	1.000	0.700	1.000	1.171	-246.	1000.	18.3	43.166
1.00	0.02	0.9866	0.0213	0.9800	244.3	1.000	1.000	1.000	0.700	1.000	1.171	-251.	1000.	18.3	43.058
1.00	0.03	0.9799	0.0319	0.9733	244.4	1.000	1.000	1.000	0.700	1.000	1.171	-256.	1000.	18.3	42.950
1.00	0.04	0.9732	0.0425	0.9667	244.5	1.000	1.000	1.000	0.700	1.000	1.171	-261.	1000.	18.3	42.842
1.00	0.05	0.9665	0.0530	0.9600	244.5	1.000	1.000	1.000	0.700	1.000	1.171	-266.	1000.	18.3	42.734
1.00	0.06	0.9598	0.0635	0.9533	244.5	1.000	1.000	1.000	0.700	1.000	1.171	-271.	1000.	18.3	42.626
1.00	0.07	0.9531	0.0740	0.9467	244.5	1.000	1.000	1.000	0.700	1.000	1.171	-276.	1000.	18.3	42.518
1.00	0.08	0.9464	0.0845	0.9400	244.5	1.000	1.000	1.000	0.700	1.000	1.171	-281.	1000.	18.3	42.410</

B. Isothermal Table

The table to follow presents values calculated at even temperature intervals of five degrees from 140°R to 245°R. They are arranged in order of increasing liquid mole fraction ratio

$$\frac{N_2}{N_2 + O_2}$$

and sub-ordered according to increasing mole fraction of argon. The quantities calculated are vapor composition, pressure, equilibrium constant (K-Values), relative volatility, enthalpy, and heat capacity.

Table 26. Isothermal Calculated Values

TEMPERATURE = 140. K

LIQUID MOLE FRACTION		VAPOR MOLE FRACTION			PRESSURE ATM	EQUIL CONST			RELATIVE VOL			ENTHALPY BTU/LB MOLE		HEAT CAPACITY BTU/LB MOLE-R	
N ₂	AR/AR+O ₂	N ₂	AR	O ₂		N ₂	AR	O ₂	N ₂ /AR	N ₂ /O ₂	AR/O ₂	LIG	VAP	LIG	VAP
.975	0.	1.943	0.	0.0071	1.02	1.019	0.421	0.202	2.419	3.011	1.493	-1401.	934.	14.4	7.540
.975	0.1	1.9927	0.0031	0.0003	1.02	1.018	0.421	0.202	2.421	3.009	1.491	-1401.	933.	14.4	7.547
.975	0.2	1.9924	0.0021	0.0006	1.02	1.018	0.420	0.202	2.422	3.007	1.490	-1401.	933.	14.4	7.549
.975	0.3	1.9920	0.0031	0.0009	1.02	1.017	0.420	0.202	2.423	3.005	1.488	-1402.	933.	14.4	7.543
.975	0.4	1.9917	0.0042	0.0012	1.02	1.017	0.420	0.202	2.424	3.003	1.486	-1402.	933.	14.4	7.541
.975	0.5	1.9913	0.0052	0.0015	1.02	1.017	0.419	0.202	2.425	3.001	1.485	-1402.	932.	14.4	7.539
.975	0.6	1.9910	0.0063	0.0018	1.02	1.016	0.419	0.202	2.426	3.000	1.483	-1402.	932.	14.4	7.537
.975	0.7	1.9907	0.0073	0.0021	1.02	1.016	0.419	0.203	2.427	3.000	1.482	-1402.	932.	14.4	7.535
.975	0.8	1.9903	0.0084	0.0024	1.02	1.016	0.418	0.203	2.428	3.000	1.480	-1403.	931.	14.3	7.533
.975	0.9	1.9900	0.0094	0.0027	1.02	1.015	0.418	0.203	2.429	3.000	1.479	-1403.	931.	14.3	7.531
.975	1.0	1.9897	0.0104	0.	1.02	1.015	0.418	0.203	2.430	3.000	1.477	-1403.	931.	14.3	7.529

TEMPERATURE = 145. K

LIQUID MOLE FRACTION		VAPOR MOLE FRACTION			PRESSURE ATM	EQUIL CONST			RELATIVE VOL			ENTHALPY BTU/LB MOLE		HEAT CAPACITY BTU/LB MOLE-R	
N ₂	AR/AR+O ₂	N ₂	AR	O ₂		N ₂	AR	O ₂	N ₂ /AR	N ₂ /O ₂	AR/O ₂	LIG	VAP	LIG	VAP
.900	0.	0.8980	0.	0.1020	1.00	1.400	0.599	0.390	2.972	3.987	1.990	-1402.	971.	13.6	7.406
.900	0.1	0.8982	0.0214	0.1200	1.01	1.415	0.597	0.390	2.969	3.991	1.990	-1400.	964.	13.4	7.443
.900	0.2	0.8983	0.0431	0.1147	1.00	1.404	0.599	0.389	2.968	3.995	1.992	-1401.	958.	13.3	7.401
.900	0.3	0.8986	0.0637	0.1085	1.00	1.393	0.591	0.389	2.974	3.986	1.979	-1400.	952.	13.2	7.360
.900	0.4	0.8989	0.0836	0.0983	1.03	1.383	0.594	0.390	2.981	3.980	1.990	-1400.	946.	13.1	7.321
.900	0.5	0.8997	0.1034	0.0921	1.03	1.374	0.597	0.391	2.987	3.970	1.992	-1400.	941.	13.0	7.282
.900	0.6	0.8997	0.1229	0.0879	1.04	1.366	0.598	0.392	2.997	3.776	1.911	-1400.	935.	12.8	7.245
.900	0.7	0.8994	0.1412	0.0836	1.05	1.359	0.594	0.393	2.994	3.742	1.389	-1401.	929.	12.7	7.200
.900	0.8	0.8994	0.1595	0.0792	1.05	1.352	0.499	0.395	2.712	3.708	1.367	-1400.	924.	12.6	7.172
.900	0.9	0.8992	0.1778	0.0748	1.07	1.347	0.492	0.394	2.740	3.701	1.351	-1400.	920.	12.5	7.110
.900	1.0	0.8997	0.1947	0.	1.07	1.343	0.487	0.390	2.790	3.680	1.330	-1400.	916.	12.3	7.001
.700	0.	0.8980	0.	0.1020	1.10	1.264	0.512	0.338	2.900	3.807	1.915	-1400.	967.	13.7	7.535
.700	0.1	0.8980	0.0192	0.0913	1.11	1.277	0.508	0.338	2.901	3.776	1.490	-1400.	963.	13.6	7.506
.700	0.2	0.8980	0.0301	0.0813	1.11	1.278	0.501	0.339	2.934	3.790	1.480	-1401.	959.	13.5	7.476
.700	0.3	0.8982	0.0446	0.0712	1.12	1.263	0.496	0.339	2.947	3.725	1.483	-1400.	954.	13.4	7.440
.700	0.4	0.8980	0.0580	0.0612	1.12	1.257	0.491	0.340	2.959	3.700	1.445	-1400.	950.	13.3	7.420
.700	0.5	0.8979	0.0730	0.0511	1.13	1.251	0.487	0.341	2.972	3.675	1.429	-1400.	946.	13.2	7.393
.700	0.6	0.8974	0.0880	0.0410	1.13	1.246	0.482	0.341	2.985	3.650	1.412	-1400.	942.	13.0	7.366
.700	0.7	0.8969	0.1003	0.0308	1.14	1.241	0.478	0.342	2.998	3.625	1.395	-1400.	938.	12.9	7.339
.700	0.8	0.8965	0.1137	0.0208	1.14	1.237	0.474	0.341	2.911	3.600	1.379	-1400.	934.	12.8	7.313
.700	0.9	0.8962	0.1278	0.0103	1.15	1.233	0.470	0.340	2.924	3.576	1.363	-1400.	930.	12.6	7.288
.700	1.0	0.8961	0.1390	0.	1.15	1.229	0.466	0.340	2.937	3.552	1.347	-1400.	927.	12.5	7.261
.600	0.	0.8958	0.	0.0942	1.20	1.149	0.478	0.323	2.847	3.625	1.481	-1400.	944.	13.4	7.504
.600	0.1	0.8958	0.0199	0.0841	1.21	1.166	0.478	0.323	2.856	3.600	1.469	-1400.	940.	13.3	7.508
.600	0.2	0.8959	0.0389	0.0718	1.21	1.162	0.470	0.323	2.864	3.592	1.490	-1400.	939.	13.7	7.549
.600	0.3	0.8967	0.0581	0.0584	1.21	1.158	0.469	0.324	2.872	3.576	1.444	-1400.	936.	13.7	7.531
.600	0.4	0.8969	0.0773	0.0489	1.22	1.150	0.466	0.324	2.880	3.560	1.430	-1400.	933.	13.6	7.514
.600	0.5	0.8973	0.0963	0.0389	1.22	1.152	0.463	0.325	2.889	3.543	1.424	-1400.	931.	13.5	7.496
.600	0.6	0.8980	0.1152	0.0280	1.22	1.149	0.460	0.326	2.897	3.527	1.413	-1400.	928.	13.4	7.479
.600	0.7	0.8985	0.1340	0.0180	1.23	1.146	0.457	0.326	2.905	3.512	1.402	-1400.	926.	13.4	7.462
.600	0.8	0.8983	0.1527	0.0131	1.23	1.143	0.455	0.327	2.914	3.496	1.391	-1400.	924.	13.4	7.445
.600	0.9	0.8982	0.1714	0.0080	1.23	1.140	0.452	0.328	2.922	3.480	1.380	-1400.	922.	13.3	7.428
.600	1.0	0.8981	0.1899	0.	1.24	1.137	0.450	0.328	2.930	3.464	1.369	-1400.	920.	13.2	7.411
.500	0.	0.8980	0.	0.1020	1.30	1.077	0.451	0.312	2.848	3.496	1.447	-1400.	941.	14.0	7.638
.500	0.1	0.8978	0.0245	0.0901	1.31	1.075	0.450	0.312	2.852	3.440	1.442	-1401.	940.	14.0	7.630
.500	0.2	0.8980	0.0390	0.0790	1.31	1.074	0.446	0.312	2.894	3.440	1.436	-1402.	939.	13.9	7.621
.500	0.3	0.8984	0.0534	0.0710	1.31	1.072	0.447	0.312	2.900	3.433	1.430	-1403.	937.	13.8	7.612
.500	0.4	0.8986	0.0678	0.0630	1.31	1.071	0.445	0.313	2.904	3.426	1.425	-1404.	936.	13.8	7.604
.500	0.5	0.8983	0.0820	0.0530	1.31	1.069	0.444	0.313	2.908	3.417	1.419	-1405.	935.	13.8	7.596
.500	0.6	0.8981	0.0966	0.0430	1.31	1.068	0.443	0.313	2.912	3.409	1.414	-1405.	933.	13.8	7.587
.500	0.7	0.8980	0.1109	0.0330	1.32	1.067	0.441	0.314	2.916	3.402	1.408	-1407.	932.	13.8	7.579
.500	0.8	0.8987	0.1252	0.0230	1.32	1.065	0.440	0.314	2.920	3.394	1.403	-1408.	931.	13.7	7.571
.500	0.9	0.8989	0.1395	0.0131	1.32	1.064	0.439	0.314	2.924	3.386	1.397	-1409.	930.	13.7	7.562
.500	1.0	0.8984	0.1530	0.	1.32	1.063	0.438	0.315	2.928	3.379	1.392	-1409.	928.	13.7	7.554
.400	0.	0.8978	0.	0.0970	1.38	1.018	0.434	0.285	2.844	3.335	1.423	-1410.	939.	14.1	7.679
.400	0.1	0.8972	0.0211	0.0859	1.30	1.018	0.434	0.285	2.849	3.333	1.421	-1410.	938.	14.1	7.677
.400	0.2	0.8979	0.0322	0.0801	1.30	1.017	0.434	0.285	2.846	3.331	1.420	-1410.	938.	14.1	7.675
.400	0.3	0.8978	0.0433	0.0803	1.30	1.017	0.433	0.285	2.847	3.329	1.419	-1411.	938.	14.1	7.673
.400	0.4	0.8973	0.0543	0.0804	1.30	1.017	0.433	0.286	2.848	3.327	1.417	-1411.	937.	14.1	7.671
.400	0.5	0.8970	0.0654	0.0800	1.30	1.016	0.433	0.286	2.849	3.325	1.416	-1411.	937.	14.1	7.669
.400	0.6	0.8968	0.0765	0.0801	1.30	1.016	0.432	0.286	2.850	3.323	1.414	-1411.	937.	14.1	7.667
.400	0.7	0.8963	0.0876	0.0803	1.30	1.016	0.432	0.286	2.851	3.322	1.413	-1412.	936.	14.0	7.665
.400	0.8	0.8960	0.0986	0.0801	1.30	1.015	0.432	0.286	2.852	3.320	1.412	-1412.	936.	14.0	7.663
.400	0.9	0.8957	0.1097	0.0800	1.30	1.015	0.431	0.286	2.853	3.318	1.410	-1412.	936.	14.0	7.661
.400	1.0	0.8954	0.1208	0.	1.30	1.015	0.431	0.286	2.854	3.316	1.409	-1412.	936.	14.0	7.659

LIQUID MOLE FRACTION		VAPOR MOLE FRACTION			PRESSURE ATM	EQUIL CONST			RELATIVE VOL			ENTHALPY BTU/LB MOLE		HEAT CAPACITY BTU/LB MOLE-R	
NP	AR/AR+O ²	NP	AR	O ²		NP	AR	O ²	L	AM	N ₂ /O ₂	AR/O ₂	LIG	VAP	LIG
.100	0.0	0.2627	0.4897	0.2474	1.00	2.627	0.907	0.888	2.897	3.819	1.318	-1941.	894.	11.5	8.393
.100	0.1	0.2580	0.5591	0.1863	1.07	2.586	0.881	0.899	2.935	3.747	1.277	-1953.	874.	11.7	8.260
.100	0.2	0.2557	0.6102	0.1292	1.04	2.557	0.868	0.896	2.973	3.676	1.236	-1965.	854.	11.9	8.130
.100	0.3	0.2533	0.6608	0.0834	1.05	2.533	0.843	0.794	3.013	3.607	1.197	-1977.	835.	12.1	8.000
.100	0.4	0.2533	0.7448	0.	1.07	2.533	0.830	0.716	3.052	3.539	1.160	-1989.	815.	12.4	8.868
.200	0.	0.5270	0.	0.4040	1.00	2.530	0.968	0.417	2.620	4.098	1.564	-1861.	1040.	13.7	7.440
.200	0.1	0.4897	0.8710	0.4371	1.08	2.440	0.923	0.407	2.650	4.029	1.520	-1811.	1017.	13.8	7.295
.200	0.2	0.4744	0.9417	0.3836	1.11	2.374	0.886	0.599	2.681	3.961	1.478	-1822.	996.	12.7	7.161
.200	0.3	0.4627	0.9247	0.3327	1.13	2.313	0.853	0.594	2.717	3.895	1.436	-1833.	977.	12.5	7.036
.200	0.4	0.4529	0.9430	0.2436	1.15	2.263	0.828	0.591	2.744	3.829	1.396	-1843.	958.	12.2	6.919
.200	0.5	0.4441	0.9700	0.2350	1.17	2.221	0.800	0.590	2.776	3.765	1.356	-1854.	941.	12.0	6.807
.200	0.6	0.4373	0.9737	0.1890	1.18	2.187	0.779	0.591	2.808	3.702	1.318	-1864.	924.	11.8	6.700
.200	0.7	0.4319	0.9797	0.1424	1.20	2.160	0.766	0.593	2.841	3.640	1.281	-1875.	908.	11.5	6.595
.200	0.8	0.4279	0.9765	0.1097	1.22	2.140	0.764	0.598	2.874	3.578	1.245	-1886.	893.	11.3	6.493
.200	0.9	0.4250	0.9265	0.1483	1.23	2.126	0.731	0.469	2.908	3.516	1.210	-1898.	877.	11.0	6.392
.200	1.0	0.4238	0.5763	0.	1.25	2.117	0.720	0.613	2.941	3.459	1.176	-1910.	862.	10.8	6.290
.300	0.	0.5270	0.	0.4331	1.00	2.627	0.816	0.533	2.561	3.922	1.531	-1732.	1035.	13.3	7.513
.300	0.1	0.5192	0.8959	0.3327	1.07	2.641	0.789	0.528	2.588	3.864	1.492	-1742.	1018.	13.1	7.405
.300	0.2	0.5093	0.1770	0.2030	1.20	1.990	0.764	0.525	2.614	3.807	1.454	-1751.	1002.	12.9	7.303
.300	0.3	0.5001	0.1950	0.2561	1.31	1.960	0.742	0.523	2.641	3.751	1.420	-1760.	987.	12.7	7.206
.300	0.4	0.5789	0.2624	0.2192	1.32	1.920	0.723	0.522	2.667	3.696	1.385	-1769.	972.	12.5	7.115
.300	0.5	0.5764	0.2470	0.1878	1.34	1.901	0.708	0.522	2.695	3.641	1.351	-1778.	958.	12.2	7.026
.300	0.6	0.5680	0.2099	0.1466	1.35	1.879	0.690	0.524	2.722	3.586	1.318	-1788.	945.	12.0	6.941
.300	0.7	0.5581	0.3315	0.1185	1.37	1.860	0.677	0.526	2.750	3.535	1.286	-1797.	932.	11.8	6.858
.300	0.8	0.5530	0.3721	0.0742	1.38	1.845	0.665	0.530	2.778	3.483	1.254	-1807.	920.	11.6	6.777
.300	0.9	0.5500	0.4121	0.0374	1.40	1.835	0.654	0.535	2.806	3.432	1.223	-1816.	907.	11.4	6.697
.300	1.0	0.5480	0.4515	0.	1.41	1.829	0.645	0.541	2.835	3.381	1.193	-1826.	895.	11.2	6.618
.400	0.	0.7145	0.	0.2856	1.43	1.786	0.713	0.476	2.905	3.753	1.498	-1664.	1030.	13.4	7.588
.400	0.1	0.7025	0.8417	0.2590	1.45	1.758	0.695	0.474	2.927	3.700	1.467	-1672.	1017.	13.2	7.504
.400	0.2	0.6918	0.8014	0.2269	1.46	1.730	0.679	0.473	2.949	3.649	1.436	-1680.	1005.	13.0	7.426
.400	0.3	0.6824	0.1194	0.1903	1.48	1.708	0.664	0.472	2.971	3.603	1.405	-1688.	993.	12.9	7.351
.400	0.4	0.6741	0.1560	0.1701	1.49	1.685	0.650	0.472	2.993	3.567	1.375	-1696.	982.	12.7	7.280
.400	0.5	0.6669	0.1912	0.1420	1.51	1.667	0.637	0.473	3.016	3.522	1.346	-1704.	971.	12.5	7.210
.400	0.6	0.6600	0.2254	0.1140	1.52	1.652	0.626	0.475	3.039	3.478	1.318	-1712.	960.	12.3	7.143
.400	0.7	0.6556	0.2586	0.0899	1.53	1.639	0.616	0.477	3.062	3.434	1.290	-1721.	950.	12.1	7.077
.400	0.8	0.6514	0.2911	0.0574	1.55	1.620	0.607	0.480	3.085	3.390	1.263	-1729.	940.	11.9	7.013
.400	0.9	0.6471	0.3230	0.0290	1.56	1.602	0.598	0.484	3.108	3.348	1.236	-1738.	930.	11.8	6.950
.400	1.0	0.6450	0.3545	0.	1.57	1.614	0.591	0.488	3.132	3.309	1.210	-1747.	920.	11.6	6.888
.500	0.	0.7824	0.	0.2174	1.41	1.955	0.639	0.436	2.449	3.592	1.466	-1595.	1025.	13.5	7.658
.500	0.1	0.7731	0.8313	0.1930	1.62	1.846	0.627	0.435	2.477	3.534	1.441	-1602.	1016.	13.3	7.597
.500	0.2	0.7647	0.8015	0.1740	1.63	1.829	0.615	0.435	2.485	3.518	1.415	-1609.	1008.	13.2	7.537
.500	0.3	0.7571	0.8907	0.1523	1.64	1.814	0.605	0.435	2.501	3.470	1.390	-1615.	997.	13.0	7.481
.500	0.4	0.7514	0.1191	0.1304	1.66	1.801	0.595	0.436	2.521	3.443	1.366	-1622.	988.	12.9	7.426
.500	0.5	0.7444	0.1466	0.1093	1.67	1.789	0.586	0.437	2.540	3.407	1.341	-1628.	980.	12.7	7.372
.500	0.6	0.7391	0.1734	0.0877	1.68	1.778	0.578	0.439	2.558	3.371	1.318	-1635.	971.	12.6	7.320
.500	0.7	0.7346	0.1996	0.0661	1.69	1.768	0.570	0.440	2.577	3.335	1.294	-1642.	963.	12.4	7.269
.500	0.8	0.7307	0.2292	0.0443	1.70	1.761	0.563	0.443	2.595	3.300	1.270	-1648.	955.	12.3	7.218
.500	0.9	0.7275	0.2565	0.0223	1.72	1.755	0.557	0.446	2.614	3.265	1.249	-1655.	947.	12.1	7.169
.500	1.0	0.7249	0.2753	0.	1.73	1.750	0.551	0.449	2.633	3.231	1.227	-1662.	939.	12.0	7.120
.600	0.	0.8378	0.	0.1425	1.78	1.695	0.583	0.416	2.395	3.427	1.435	-1527.	1021.	13.6	7.732
.600	0.1	0.8310	0.8230	0.1463	1.79	1.685	0.575	0.418	2.409	3.408	1.415	-1532.	1013.	13.5	7.687
.600	0.2	0.8247	0.8454	0.1301	1.80	1.675	0.567	0.417	2.423	3.380	1.395	-1537.	1006.	13.3	7.644
.600	0.3	0.8190	0.8672	0.1140	1.81	1.665	0.560	0.417	2.437	3.351	1.375	-1543.	1000.	13.2	7.602
.600	0.4	0.8138	0.8895	0.0980	1.82	1.656	0.553	0.418	2.451	3.323	1.356	-1548.	993.	13.1	7.560
.600	0.5	0.8090	0.9104	0.0818	1.83	1.648	0.547	0.419	2.465	3.295	1.337	-1553.	986.	13.0	7.520
.600	0.6	0.8046	0.9298	0.0657	1.84	1.641	0.541	0.421	2.480	3.267	1.318	-1559.	980.	12.9	7.481
.600	0.7	0.8010	0.9499	0.0494	1.85	1.635	0.535	0.422	2.494	3.240	1.299	-1564.	974.	12.7	7.440
.600	0.8	0.7978	0.9696	0.0331	1.86	1.629	0.529	0.424	2.509	3.212	1.281	-1569.	967.	12.6	7.403
.600	0.9	0.7947	0.9890	0.0168	1.87	1.624	0.525	0.426	2.523	3.185	1.262	-1575.	961.	12.5	7.364
.600	1.0	0.7922	0.9881	0.	1.88	1.620	0.520	0.428	2.538	3.158	1.245	-1580.	955.	12.4	7.329
.700	0.	0.8856	0.	0.1153	1.95	1.604	0.540	0.384	2.342	3.295	1.405	-1458.	1016.	13.7	7.807
.700	0.1	0.8844	0.8180	0.1030	1.99	1.598	0.538	0.389	2.352	3.280	1.390	-1462.	1011.	13.6	7.776
.700	0.2	0.8761	0.8318	0.0925	1.96	1.590	0.530	0.385	2.362	3.268	1.375	-1466.	1006.	13.5	7.746
.700	0.3	0.8720	0.8473	0.0811	1.97	1.584	0.525	0.386	2.373	3.258	1.360	-1470.	1001.	13.4	7.716
.700	0.4	0.8683	0.8625	0.0696	1.98	1.578	0.521	0.387	2.383	3.247	1.346	-1474.	996.	13.3	7.687
.700	0.5	0.8648	0.8774	0.0581	1.98	1.573	0.516	0.388	2.393	3.237	1.332	-1478.	991.	13.2	7.658
.700	0.6	0.8615	0.8922	0.0466	1.99	1.568	0.512	0.389	2.404	3.227	1.317	-1482.	987.	13.1	7.630
.700	0.7	0.8580	0.9077	0.0351	2.00	1.562	0.508	0.390	2.414	3.217	1.303	-1486.	982.	13.0	7.602
.700	0.8	0.8559	0.9210	0.0235	2.01	1.557	0.504	0.391	2.424	3.207	1.290	-1490.	978.	12.9	7.575
.700	0.9	0.8534	0.9352	0.0118	2.02	1.551	0.501	0.392	2.435	3.197	1.276	-1494.	973.	12.8	7.548
.700	1.0	0.8512	0.9492	0.	2.02	1.546	0.497	0.394	2.446	3.187	1.262	-1498.	969.	12.8	7.521
.800	0.	0.9268	0.	0.0736	2.11	1.539	0.566	0.368	2.390	3.148	1.375	-1399.	1016.	13.8	7.885
.800	0.1	0.9240	0.8101	0.0663	2.12	1.535	0.563	0.368	2.397	3.135	1.365	-1403.	1011.	13.6	7.856
.800	0.2	0.9214	0.8200	0.0590	2.12	1.532	0.560	0.369	2.403	3.122	1.355	-1407.	1006.	13.7	7.827
.800	0.3	0.9188	0.8298	0.0517	2.13	1.529	0.557	0.369	2.410	3.109	1.346	-1411.	1001.	13.6	7.798
.800	0.4	0.9164	0.8396	0.0444	2.14	1.526	0.554	0.370	2.417						

TEMP	LIQUID MOLE FRACTION		VAPOR MOLE FRACTION		PRESSURE ATM	EQUIL CONST			RELATIVE VOL			ENTHALPY BTU/LB MOLE		HEAT CAPACITY BTU/LB MOLE-R	
	N2	AR/AR-O2	N2	AR		N2	AR	O2	N2/AR	N2/O2	AR/O2	LIQ	VAP	LIQ	VAP
0.5	0.	0.3794	0.6207	1.00	3.459	1.265	0.867	2.736	3.002	1.426	-1917.	950.	12.2	6.616	
0.5	0.	0.4780	0.5219	1.00	3.320	1.197	0.849	2.773	3.022	1.379	-1931.	927.	11.9	6.417	
0.5	0.	0.5713	0.4287	1.00	3.211	1.143	0.857	2.810	3.045	1.333	-1946.	897.	11.7	6.231	
0.5	0.	0.6590	0.3411	1.00	3.129	1.098	0.853	2.849	3.060	1.288	-1961.	869.	11.4	6.054	
0.5	0.	0.7440	0.2561	1.00	3.069	1.063	0.854	2.887	3.075	1.248	-1976.	842.	11.1	5.891	
0.5	0.	0.8260	0.1720	1.00	3.029	1.035	0.860	2.927	3.092	1.203	-1991.	816.	10.8	5.729	
0.5	0.	0.9120	0.0872	1.00	3.009	1.014	0.872	2.966	3.101	1.163	-2005.	789.	10.5	5.574	
0.5	0.	1.0000	0.0000	1.00	3.007	1.000	0.889	3.007	3.108	1.124	-2018.	762.	10.2	5.422	
0.5	0.1	0.5460	0.4540	1.00	3.185	1.262	0.858	2.883	3.048	1.470	-1884.	994.	12.0	6.922	
0.5	0.2	0.6000	0.4000	1.00	3.135	1.190	0.837	2.718	3.007	1.422	-1898.	967.	11.8	6.760	
0.5	0.3	0.7090	0.2910	1.00	3.022	1.131	0.822	2.794	3.070	1.376	-1913.	937.	11.6	6.594	
0.5	0.4	0.7750	0.2250	1.00	2.940	1.083	0.813	2.791	3.115	1.331	-1927.	909.	11.4	6.430	
0.5	0.5	0.7727	0.2273	1.00	2.907	1.031	0.810	2.828	3.042	1.288	-1941.	883.	11.4	6.174	
0.5	0.6	0.7100	0.2900	1.00	2.862	0.986	0.809	2.874	3.092	1.250	-1956.	859.	11.1	5.991	
0.5	0.7	0.6482	0.3518	1.00	2.843	0.947	0.829	2.903	3.099	1.205	-1970.	833.	10.9	5.850	
0.5	0.8	0.5820	0.4180	1.00	2.840	0.933	0.845	2.921	3.043	1.166	-1985.	809.	10.6	5.687	
0.5	0.9	0.5123	0.4877	1.00	2.843	0.924	0.871	2.921	3.000	1.128	-1999.	782.	10.3	5.519	
0.5	1.0	0.4400	0.5600	1.00	2.852	0.923	0.908	2.903	3.000	1.091	-2013.	755.	10.0	5.352	
0.5	0.1	0.2824	0.7176	1.00	2.924	1.123	0.740	2.683	3.005	1.459	-1803.	1073.	13.2	7.452	
0.5	0.2	0.3410	0.6590	1.00	2.800	1.066	0.733	2.639	3.001	1.459	-1817.	1041.	13.0	7.293	
0.5	0.3	0.4205	0.5795	1.00	2.713	1.017	0.721	2.607	3.001	1.411	-1830.	1012.	12.7	7.075	
0.5	0.4	0.5252	0.4748	1.00	2.635	0.976	0.713	2.609	3.004	1.369	-1845.	981.	12.4	6.911	
0.5	0.5	0.6590	0.3410	1.00	2.572	0.941	0.709	2.732	3.027	1.327	-1861.	937.	12.2	6.759	
0.5	0.6	0.8260	0.1740	1.00	2.529	0.912	0.709	2.766	3.051	1.287	-1878.	915.	11.9	6.614	
0.5	0.7	0.9120	0.0880	1.00	2.496	0.880	0.711	2.800	3.094	1.249	-1896.	894.	11.4	6.481	
0.5	0.8	0.9880	0.0120	1.00	2.465	0.852	0.726	2.834	3.032	1.211	-1910.	873.	11.1	6.340	
0.5	0.9	0.9990	0.0010	1.00	2.444	0.840	0.737	2.869	3.009	1.179	-1923.	853.	10.8	6.208	
0.5	1.0	0.9990	0.0010	1.00	2.444	0.840	0.737	2.869	3.009	1.179	-1923.	853.	10.8	6.208	
0.5	0.1	0.4881	0.5119	1.00	2.440	0.971	0.640	2.517	3.013	1.515	-1734.	1067.	13.3	7.530	
0.5	0.2	0.5729	0.4271	1.00	2.362	0.920	0.630	2.544	3.078	1.474	-1746.	1043.	13.1	7.393	
0.5	0.3	0.6471	0.3529	1.00	2.296	0.893	0.622	2.572	3.090	1.438	-1758.	1021.	12.8	7.259	
0.5	0.4	0.7090	0.2910	1.00	2.239	0.861	0.617	2.600	3.030	1.396	-1770.	1000.	12.6	7.133	
0.5	0.5	0.7750	0.2250	1.00	2.192	0.834	0.614	2.628	3.071	1.359	-1782.	981.	12.4	7.014	
0.5	0.6	0.8260	0.1740	1.00	2.153	0.811	0.613	2.657	3.013	1.322	-1793.	963.	12.1	6.900	
0.5	0.7	0.8727	0.1273	1.00	2.122	0.790	0.614	2.685	3.091	1.287	-1805.	945.	11.9	6.791	
0.5	0.8	0.9100	0.0900	1.00	2.097	0.773	0.617	2.715	3.090	1.252	-1817.	928.	11.7	6.684	
0.5	0.9	0.9410	0.0590	1.00	2.079	0.759	0.622	2.744	3.044	1.218	-1829.	911.	11.4	6.579	
0.5	1.0	0.9720	0.0280	1.00	2.067	0.749	0.628	2.774	3.020	1.186	-1841.	895.	11.2	6.479	
0.5	0.1	0.4127	0.5873	1.00	2.085	0.735	0.637	2.784	3.236	1.154	-1853.	878.	11.0	6.379	
0.5	0.2	0.4881	0.5119	1.00	2.035	0.702	0.637	2.804	3.300	1.139	-1865.	861.	10.8	6.284	
0.5	0.3	0.5729	0.4271	1.00	1.988	0.670	0.632	2.827	3.303	1.103	-1876.	843.	10.6	6.191	
0.5	0.4	0.6471	0.3529	1.00	1.948	0.646	0.640	2.851	3.292	1.064	-1886.	826.	10.4	6.100	
0.5	0.5	0.7090	0.2910	1.00	1.913	0.629	0.646	2.875	3.291	1.024	-1896.	810.	10.2	6.013	
0.5	0.6	0.7750	0.2250	1.00	1.883	0.616	0.646	2.899	3.291	0.984	-1905.	794.	10.0	5.929	
0.5	0.7	0.8260	0.1740	1.00	1.858	0.607	0.646	2.923	3.291	0.944	-1914.	778.	9.8	5.847	
0.5	0.8	0.8727	0.1273	1.00	1.837	0.601	0.646	2.947	3.291	0.904	-1922.	762.	9.6	5.766	
0.5	0.9	0.9100	0.0900	1.00	1.820	0.600	0.646	2.971	3.291	0.864	-1929.	746.	9.4	5.686	
0.5	1.0	0.9410	0.0590	1.00	1.807	0.600	0.646	2.995	3.291	0.824	-1935.	730.	9.2	5.606	
0.5	0.1	0.4127	0.5873	1.00	1.820	0.600	0.646	2.995	3.291	0.824	-1935.	730.	9.2	5.606	
0.5	0.2	0.4881	0.5119	1.00	1.791	0.586	0.646	2.984	3.187	0.784	-1940.	714.	9.0	5.526	
0.5	0.3	0.5729	0.4271	1.00	1.765	0.576	0.646	2.973	3.187	0.744	-1944.	698.	8.8	5.446	
0.5	0.4	0.6471	0.3529	1.00	1.742	0.569	0.646	2.962	3.187	0.704	-1947.	682.	8.6	5.366	
0.5	0.5	0.7090	0.2910	1.00	1.721	0.564	0.646	2.951	3.187	0.664	-1949.	666.	8.4	5.286	
0.5	0.6	0.7750	0.2250	1.00	1.702	0.561	0.646	2.940	3.187	0.624	-1950.	650.	8.2	5.206	
0.5	0.7	0.8260	0.1740	1.00	1.685	0.560	0.646	2.929	3.187	0.584	-1950.	634.	8.0	5.126	
0.5	0.8	0.8727	0.1273	1.00	1.670	0.560	0.646	2.918	3.187	0.544	-1949.	618.	7.8	5.046	
0.5	0.9	0.9100	0.0900	1.00	1.657	0.560	0.646	2.907	3.187	0.504	-1947.	602.	7.6	4.966	
0.5	1.0	0.9410	0.0590	1.00	1.646	0.560	0.646	2.896	3.187	0.464	-1944.	586.	7.4	4.886	
0.5	0.1	0.4881	0.5119	1.00	1.657	0.560	0.646	2.896	3.187	0.464	-1944.	586.	7.4	4.886	
0.5	0.2	0.5729	0.4271	1.00	1.628	0.545	0.646	2.885	3.083	0.424	-1947.	570.	7.2	4.806	
0.5	0.3	0.6471	0.3529	1.00	1.602	0.535	0.646	2.874	3.083	0.384	-1948.	554.	7.0	4.726	
0.5	0.4	0.7090	0.2910	1.00	1.579	0.529	0.646	2.863	3.083	0.344	-1947.	538.	6.8	4.646	
0.5	0.5	0.7750	0.2250	1.00	1.558	0.526	0.646	2.852	3.083	0.304	-1944.	522.	6.6	4.566	
0.5	0.6	0.8260	0.1740	1.00	1.539	0.526	0.646	2.841	3.083	0.264	-1939.	506.	6.4	4.486	
0.5	0.7	0.8727	0.1273	1.00	1.522	0.526	0.646	2.830	3.083	0.224	-1932.	490.	6.2	4.406	
0.5	0.8	0.9100	0.0900	1.00	1.507	0.526	0.646	2.819	3.083	0.184	-1923.	474.	6.0	4.326	
0.5	0.9	0.9410	0.0590	1.00	1.494	0.526	0.646	2.808	3.083	0.144	-1912.	458.	5.8	4.246	
0.5	1.0	0.9720	0.0280	1.00	1.483	0.526	0.646	2.797	3.083	0.104	-1899.	442.	5.6	4.166	
0.5	0.1	0.4127	0.5873	1.00	1.494	0.526	0.646	2.797	3.083	0.104	-1899.	442.	5.6	4.166	
0.5	0.2	0.4881	0.5119	1.00	1.465	0.511	0.646	2.786	3.083	0.064	-1886.	426.	5.4	4.086	
0.5	0.3	0.5729	0.4271	1.00	1.438	0.501	0.646	2.775	3.083	0.024	-1871.	410.	5.2	4.006	
0.5	0.4	0.6471	0.3529	1.00	1.413	0.495	0.646	2.764	3.083	0.004	-1854.	394.	5.0	3.926	
0.5	0.5	0.7090	0.2910	1.00	1.390	0.491	0.646	2.753	3.083	0.004	-1835.	378.	4.8	3.84	

LIQUID MOLE FRACTION		VAPOR MOLE FRACTION			PRESSURE ATM	EQUIL CONST				RELATIVE VOL		ENTHALPY BTU/LB MOLE		HEAT CAPACITY BTU/LB MOLE-R	
N ₂	AR/AR-O ₂	N ₂	AR	O ₂		N ₂	AR	O ₂	N ₂ /AR	N ₂ /O ₂	AR/O ₂	LIG	VAP	LIG	VAP
0.	0.	0.	0.	1.0001	1.16	3.868	1.939	1.000	2.519	3.868	1.934	-1807.	1167.	13.2	7.482
0.	0.1	0.	0.1417	0.8584	1.22	3.813	1.417	0.994	2.561	3.780	1.485	-1823.	1040.	12.9	7.173
0.	0.2	0.	0.2649	0.7356	1.28	3.415	1.279	0.990	2.583	3.714	1.438	-1839.	1070.	12.6	6.931
0.	0.3	0.	0.3737	0.6264	1.33	3.258	1.248	0.989	2.619	3.641	1.392	-1859.	983.	12.4	6.719
0.	0.4	0.	0.4733	0.5260	1.37	3.134	1.183	0.978	2.648	3.569	1.348	-1871.	951.	12.4	6.517
0.	0.5	0.	0.5602	0.4339	1.41	3.037	1.132	0.968	2.680	3.489	1.305	-1888.	920.	11.8	6.331
0.	0.6	0.	0.6346	0.3499	1.44	2.963	1.091	0.964	2.716	3.416	1.263	-1904.	891.	11.5	6.193
0.	0.7	0.	0.7466	0.2999	1.47	2.909	1.059	0.960	2.750	3.361	1.223	-1920.	863.	11.2	5.979
0.	0.8	0.	0.8297	0.1744	1.50	2.874	1.032	0.972	2.785	3.297	1.184	-1938.	835.	11.0	5.809
0.	0.9	0.	0.9117	0.0864	1.52	2.857	1.013	0.984	2.820	3.232	1.146	-1952.	807.	10.7	5.627
0.	1.0	0.	1.0001	0.	1.54	2.856	1.000	0.991	2.856	3.169	1.110	-1968.	778.	10.4	5.443
0.025	0.	0.0893	0.	0.9107	1.26	3.974	1.426	0.934	2.506	3.826	1.527	-1789.	1129.	13.2	7.479
0.025	0.1	0.1841	0.1293	0.7067	1.31	3.364	1.326	0.897	2.537	3.792	1.479	-1819.	1062.	13.2	7.222
0.025	0.2	0.2799	0.2427	0.6775	1.35	3.196	1.245	0.869	2.568	3.680	1.433	-1851.	1029.	12.7	6.999
0.025	0.3	0.3776	0.2451	0.5776	1.39	3.095	1.180	0.846	2.609	3.637	1.394	-1887.	992.	12.4	6.788
0.025	0.4	0.4739	0.1799	0.4803	1.44	2.995	1.123	0.825	2.652	3.581	1.345	-1922.	960.	12.1	6.613
0.025	0.5	0.5718	0.9293	0.4030	1.48	2.911	1.078	0.827	2.694	3.479	1.303	-1958.	931.	11.9	6.439
0.025	0.6	0.6701	0.6186	0.3213	1.51	2.846	1.040	0.824	2.737	3.406	1.263	-1994.	904.	11.6	6.271
0.025	0.7	0.7696	0.6806	0.2419	1.54	2.798	1.010	0.826	2.780	3.344	1.224	-2029.	877.	11.3	6.107
0.025	0.8	0.8682	0.7696	0.1823	1.57	2.727	0.987	0.832	2.824	3.276	1.186	-2065.	851.	11.0	5.944
0.025	0.9	0.9678	0.8901	0.0822	1.59	2.711	0.968	0.843	2.798	3.214	1.149	-2091.	825.	10.8	5.778
0.025	1.0	0.9777	0.9374	0.	1.61	2.710	0.956	0.859	2.832	3.153	1.113	-2127.	798.	10.5	5.607
0.100	0.	0.2701	0.	0.7299	1.40	3.901	1.183	0.787	2.468	3.711	1.904	-1737.	1299.	14.3	7.949
0.100	0.1	0.4960	0.0740	0.4880	1.45	3.283	1.083	0.851	2.442	3.598	1.438	-1767.	1246.	13.1	7.393
0.100	0.2	0.6442	0.1441	0.3451	1.49	3.085	1.044	0.790	2.524	3.506	1.418	-1798.	1236.	12.8	7.176
0.100	0.3	0.7811	0.2749	0.4837	1.53	2.911	1.018	0.736	2.564	3.447	1.384	-1831.	1210.	12.6	6.979
0.100	0.4	0.8927	0.3924	0.2951	1.57	2.827	0.979	0.732	2.582	3.404	1.338	-1867.	982.	12.3	6.800
0.100	0.5	0.9270	0.4256	0.3270	1.59	2.870	0.946	0.728	2.611	3.392	1.299	-1901.	958.	12.1	6.714
0.100	0.6	0.9425	0.4958	0.2619	1.61	2.829	0.918	0.728	2.641	3.333	1.262	-1935.	935.	11.8	6.574
0.100	0.7	0.9391	0.5639	0.1972	1.63	2.807	0.874	0.730	2.671	3.274	1.226	-1969.	913.	11.6	6.437
0.100	0.8	0.9367	0.6310	0.1325	1.65	2.807	0.861	0.748	2.701	3.216	1.191	-2004.	891.	11.3	6.301
0.100	0.9	0.9353	0.6970	0.0670	1.67	2.807	0.850	0.757	2.732	3.159	1.156	-2038.	869.	11.1	6.165
0.100	1.0	0.9349	0.7652	0.	1.69	2.807	0.840	0.757	2.763	3.102	1.123	-2073.	847.	10.8	6.029
0.200	0.	0.4711	0.	0.5289	1.81	3.988	0.974	0.681	2.418	3.788	1.473	-1688.	1392.	15.4	8.126
0.200	0.1	0.6700	0.0740	0.4680	1.85	3.283	0.939	0.851	2.442	3.598	1.438	-1718.	1347.	14.2	7.568
0.200	0.2	0.8337	0.2009	0.3576	1.89	3.085	0.900	0.844	2.467	3.491	1.399	-1749.	1344.	13.9	7.352
0.200	0.3	0.9420	0.3701	0.3059	1.92	2.911	0.870	0.839	2.492	3.396	1.363	-1781.	1322.	13.6	7.149
0.200	0.4	0.9717	0.5701	0.3059	1.95	2.827	0.844	0.834	2.517	3.343	1.326	-1817.	1292.	13.4	6.946
0.200	0.5	0.9845	0.7010	0.2939	1.98	2.809	0.821	0.835	2.542	3.291	1.294	-1851.	1265.	13.2	6.749
0.200	0.6	0.9891	0.8046	0.2035	2.01	2.809	0.802	0.836	2.568	3.238	1.261	-1887.	984.	12.9	6.510
0.200	0.7	0.9873	0.8749	0.1333	2.03	2.806	0.789	0.839	2.594	3.187	1.229	-1922.	960.	12.6	6.309
0.200	0.8	0.9869	0.9345	0.0670	2.05	2.806	0.771	0.844	2.620	3.137	1.197	-1958.	940.	12.4	6.165
0.200	0.9	0.9870	0.9645	0.0320	2.07	2.806	0.759	0.851	2.647	3.088	1.167	-1994.	913.	12.1	6.029
0.200	1.0	0.9870	0.9946	0.	2.09	2.806	0.748	0.859	2.673	3.039	1.137	-2030.	893.	11.8	5.893
0.300	0.	0.3946	0.	0.6054	2.11	4.982	0.837	0.581	2.369	3.460	1.444	-1638.	1489.	16.6	7.984
0.300	0.1	0.5815	0.0540	0.3620	2.14	4.188	0.817	0.799	2.390	3.373	1.411	-1669.	1446.	15.3	7.426
0.300	0.2	0.7511	0.1303	0.3199	2.17	3.900	0.788	0.571	2.411	3.326	1.380	-1699.	1446.	15.1	7.210
0.300	0.3	0.8612	0.2012	0.2700	2.20	3.687	0.740	0.569	2.432	3.280	1.349	-1731.	1421.	14.8	6.999
0.300	0.4	0.9517	0.2909	0.2300	2.23	3.539	0.700	0.568	2.454	3.235	1.318	-1763.	1401.	14.6	6.788
0.300	0.5	0.9845	0.2566	0.1991	2.25	3.415	0.733	0.569	2.478	3.190	1.286	-1795.	1379.	14.4	6.574
0.300	0.6	0.9980	0.3070	0.1598	2.27	3.298	0.719	0.571	2.497	3.144	1.254	-1827.	1358.	14.2	6.359
0.300	0.7	0.9930	0.3491	0.1204	2.29	3.179	0.709	0.573	2.519	3.103	1.222	-1859.	1334.	14.0	6.144
0.300	0.8	0.9875	0.3904	0.0808	2.32	3.067	0.697	0.577	2.542	3.060	1.194	-1891.	1309.	13.7	5.929
0.300	0.9	0.9825	0.4321	0.0408	2.34	2.958	0.688	0.583	2.564	3.018	1.167	-1923.	1284.	13.4	5.714
0.300	1.0	0.9825	0.4744	0.	2.36	2.851	0.678	0.589	2.587	2.977	1.131	-1955.	1259.	13.1	5.499
0.400	0.	0.6867	0.	0.3137	2.42	6.977	0.740	0.523	2.321	3.284	1.418	-1588.	1577.	18.6	8.827
0.400	0.1	0.7959	0.0433	0.2812	2.45	6.080	0.722	0.521	2.339	3.246	1.387	-1618.	1533.	17.3	8.268
0.400	0.2	0.8662	0.0846	0.2493	2.48	5.484	0.689	0.519	2.374	3.188	1.356	-1648.	1489.	16.0	7.707
0.400	0.3	0.9370	0.1247	0.2180	2.47	4.844	0.640	0.519	2.374	3.148	1.330	-1678.	1446.	14.7	7.146
0.400	0.4	0.9804	0.1631	0.1869	2.46	4.626	0.600	0.519	2.392	3.106	1.301	-1708.	1401.	13.4	6.585
0.400	0.5	0.9840	0.2004	0.1561	2.51	4.610	0.587	0.520	2.392	3.131	1.309	-1738.	1358.	13.1	6.024
0.400	0.6	0.9885	0.2366	0.1253	2.53	4.590	0.567	0.522	2.410	3.094	1.284	-1768.	1314.	12.8	5.463
0.400	0.7	0.9841	0.2721	0.0944	2.56	4.589	0.548	0.525	2.428	3.057	1.259	-1798.	1270.	12.6	5.309
0.400	0.8	0.9813	0.3080	0.0633	2.58	4.576	0.539	0.526	2.448	3.020	1.235	-1828.	1226.	12.3	4.748
0.400	0.9	0.9875	0.3411	0.0319	2.60	4.569	0.532	0.532	2.464	2.983	1.211	-1858.	1182.	12.1	4.594
0.400	1.0	0.9875	0.3749	0.	2.62	4.564	0.525	0.536	2.482	2.945	1.185	-1888.	1138.	11.8	4.033
0.500	0.	0.7920	0.	0.2080	2.68	8.916	0.688	0.482	2.294	3.193	1.388	-1438.	1770.	21.8	7.134
0.500	0.1	0.7300	0.0320	0.2185	2.70	8.502	0.656	0.4							

LIQUID MOLE FRACTION	VAPOR MOLE FRACTION	PRESSURE	EQUIL CONST			RELATIVE VOL			ENTHALPY		HEAT CAPACITY				
			N2	AR	O2	N2/AR	N2/O2	AR/O2	LIG	VAP	LIG	VAP			
NO	AR/AR+O2	N2	AR	O2	ATM	N2	AR	O2	N2/AR	N2/O2	AR/O2	BTU/LB MOLE	BTU/LB MOLE-R	BTU/LB MOLE-R	BTU/LB MOLE-R
0.0	0.0	0.0	1.0001	1.53	2.811	1.498	1.000	1.000	2.414	3.811	1.498	-1746.	1133.	13.0	7.546
0.1	0.0	0.1388	0.8613	1.60	2.269	1.388	0.957	2.442	3.841	1.451	-1778.	1088.	13.0	7.277	
0.2	0.0	0.2601	0.7400	1.67	2.213	1.301	0.925	2.471	3.474	1.408	-1793.	1037.	12.9	7.049	
0.3	0.0	0.3688	0.6313	1.73	2.073	1.229	0.902	2.500	3.467	1.363	-1793.	1037.	12.9	6.827	
0.4	0.0	0.4617	0.5384	1.78	2.067	1.171	0.886	2.529	3.342	1.322	-1811.	973.	12.8	6.631	
0.5	0.0	0.5509	0.4693	1.83	2.075	1.123	0.877	2.559	3.279	1.281	-1828.	941.	12.9	6.445	
0.6	0.0	0.6257	0.4209	1.87	2.098	1.085	0.873	2.589	3.216	1.242	-1846.	911.	12.7	6.267	
0.7	0.0	0.6856	0.3783	1.94	2.129	1.054	0.875	2.619	3.155	1.205	-1863.	881.	12.4	6.091	
0.8	0.0	0.7318	0.3404	1.98	2.173	1.030	0.882	2.650	3.095	1.180	-1881.	852.	12.2	5.915	
0.9	0.0	0.7652	0.3064	2.02	2.213	1.012	0.894	2.681	3.036	1.152	-1898.	823.	12.0	5.736	
1.0	0.0	0.7862	0.2751	2.05	2.250	1.000	0.911	2.713	2.979	1.126	-1916.	793.	12.0	5.556	
0.0	0.1	0.0793	0.1273	1.70	2.173	1.326	0.944	2.432	3.575	1.488	-1723.	1131.	13.3	7.976	
0.0	0.2	0.1756	0.2399	1.76	2.023	1.231	0.876	2.485	3.443	1.421	-1797.	1049.	12.9	7.109	
0.0	0.3	0.2725	0.3415	1.82	2.002	1.168	0.859	2.485	3.379	1.361	-1797.	1049.	12.9	6.919	
0.0	0.4	0.3711	0.4352	1.87	2.005	1.116	0.846	2.514	3.316	1.319	-1797.	1049.	12.9	6.728	
0.0	0.5	0.4688	0.5232	1.92	2.029	1.073	0.838	2.543	3.254	1.280	-1816.	985.	12.8	6.538	
0.0	0.6	0.5646	0.6054	1.96	2.070	1.038	0.836	2.572	3.194	1.242	-1834.	923.	12.6	6.348	
0.0	0.7	0.6589	0.6818	1.99	2.127	1.010	0.838	2.601	3.135	1.205	-1853.	861.	12.5	6.158	
0.0	0.8	0.7519	0.7522	2.02	2.199	0.988	0.845	2.631	3.077	1.169	-1872.	800.	12.3	5.968	
0.0	0.9	0.8436	0.8166	2.05	2.284	0.971	0.856	2.661	3.020	1.135	-1891.	740.	12.0	5.778	
1.0	0.0	0.2784	0.0	1.93	2.784	1.177	0.822	2.692	2.964	1.103	-1898.	713.	12.0	5.588	
1.0	0.1	0.2867	0.1003	1.99	2.667	1.115	0.782	2.392	3.471	1.426	-1866.	1099.	13.0	7.489	
1.0	0.2	0.2970	0.1814	2.05	2.570	1.063	0.746	2.417	3.351	1.369	-1866.	1099.	13.0	7.299	
1.0	0.3	0.3094	0.2752	2.10	2.490	1.019	0.756	2.443	3.294	1.329	-1866.	1099.	13.0	7.109	
1.0	0.4	0.3234	0.3536	2.14	2.424	0.982	0.749	2.469	3.239	1.292	-1866.	1099.	13.0	6.919	
1.0	0.5	0.3392	0.4278	2.18	2.372	0.951	0.745	2.495	3.183	1.256	-1866.	1099.	13.0	6.728	
1.0	0.6	0.3567	0.4981	2.22	2.330	0.924	0.745	2.521	3.128	1.241	-1866.	1099.	13.0	6.538	
1.0	0.7	0.3759	0.5658	2.25	2.299	0.902	0.748	2.548	3.075	1.207	-1866.	1099.	13.0	6.348	
1.0	0.8	0.3959	0.6308	2.28	2.277	0.885	0.754	2.575	3.022	1.174	-1866.	1099.	13.0	6.158	
1.0	0.9	0.4166	0.6932	2.31	2.265	0.871	0.763	2.602	2.970	1.142	-1866.	1099.	13.0	5.968	
1.0	1.0	0.4380	0.7541	2.34	2.260	0.860	0.775	2.629	2.922	1.110	-1866.	1099.	13.0	5.778	
0.0	0.1	0.4450	0.0	2.32	2.275	0.942	0.692	2.321	3.338	1.438	-1800.	1115.	13.0	7.781	
0.0	0.2	0.4444	0.1454	2.36	2.207	0.920	0.672	2.343	3.267	1.403	-1814.	1089.	13.0	7.637	
0.0	0.3	0.4281	0.2112	2.40	2.100	0.881	0.654	2.365	3.236	1.368	-1828.	1063.	13.1	7.503	
0.0	0.4	0.4119	0.2735	2.44	2.059	0.855	0.656	2.387	3.187	1.335	-1842.	1043.	12.9	7.377	
0.0	0.5	0.4051	0.3351	2.48	2.025	0.833	0.659	2.410	3.138	1.302	-1856.	1021.	12.7	7.256	
0.0	0.6	0.3996	0.3907	2.52	1.998	0.814	0.657	2.432	3.089	1.271	-1870.	1001.	12.6	7.140	
0.0	0.7	0.3952	0.4467	2.55	1.977	0.798	0.660	2.454	3.047	1.239	-1884.	981.	12.3	7.027	
0.0	0.8	0.3924	0.5018	2.58	1.961	0.784	0.665	2.476	2.997	1.208	-1898.	962.	12.1	6.916	
0.0	0.9	0.3913	0.5564	2.61	1.951	0.773	0.671	2.498	2.946	1.176	-1912.	944.	11.9	6.806	
0.0	1.0	0.3923	0.6111	2.65	1.947	0.764	0.680	2.519	2.892	1.143	-1926.	926.	11.8	6.697	
0.0	0.1	0.3793	0.0	2.58	1.931	0.848	0.612	2.277	3.299	1.410	-1830.	1127.	13.0	7.994	
0.0	0.2	0.3591	0.1121	2.72	1.890	0.823	0.597	2.299	3.166	1.340	-1842.	1087.	13.0	7.799	
0.0	0.3	0.3447	0.1840	2.79	1.822	0.801	0.593	2.314	3.124	1.306	-1856.	1068.	13.0	7.601	
0.0	0.4	0.3365	0.2137	2.82	1.795	0.781	0.591	2.333	3.082	1.271	-1870.	1050.	13.1	7.499	
0.0	0.5	0.3317	0.2616	2.85	1.772	0.763	0.590	2.352	3.041	1.239	-1884.	1032.	12.9	7.403	
0.0	0.6	0.3281	0.3081	2.88	1.754	0.744	0.592	2.371	3.000	1.205	-1898.	1016.	12.8	7.301	
0.0	0.7	0.3256	0.3534	2.91	1.739	0.721	0.595	2.391	2.960	1.176	-1912.	1000.	12.6	7.211	
0.0	0.8	0.3241	0.3980	2.94	1.727	0.701	0.599	2.410	2.920	1.142	-1926.	984.	12.4	7.122	
0.0	0.9	0.3237	0.4420	2.97	1.719	0.682	0.601	2.429	2.881	1.108	-1940.	969.	12.2	7.033	
0.0	1.0	0.3243	0.4859	2.99	1.714	0.664	0.605	2.448	2.842	1.074	-1954.	954.	12.0	6.944	
0.0	0.1	0.4028	0.0	3.03	1.682	0.754	0.543	2.232	3.284	1.382	-1860.	1108.	13.0	8.026	
0.0	0.2	0.4034	0.0866	3.06	1.656	0.737	0.543	2.248	3.209	1.357	-1874.	1082.	13.0	7.843	
0.0	0.3	0.4043	0.1274	3.09	1.624	0.722	0.542	2.264	3.115	1.332	-1888.	1058.	13.0	7.661	
0.0	0.4	0.4053	0.1646	3.12	1.613	0.708	0.541	2.280	3.068	1.307	-1902.	1034.	13.0	7.485	
0.0	0.5	0.4062	0.2018	3.15	1.596	0.694	0.542	2.296	2.996	1.283	-1916.	1010.	13.0	7.310	
0.0	0.6	0.4070	0.2404	3.18	1.580	0.684	0.543	2.312	2.913	1.260	-1930.	1027.	13.0	7.137	
0.0	0.7	0.4077	0.2790	3.23	1.567	0.673	0.544	2.328	2.879	1.237	-1944.	1014.	12.9	7.066	
0.0	0.8	0.4083	0.3168	3.25	1.556	0.664	0.547	2.344	2.846	1.214	-1958.	1001.	12.7	7.000	
0.0	0.9	0.4087	0.3542	3.28	1.542	0.648	0.550	2.361	2.814	1.192	-1972.	989.	12.6	7.027	
0.0	1.0	0.4089	0.3921	3.30	1.537	0.642	0.555	2.378	2.781	1.170	-1986.	976.	12.4	7.059	
0.0	0.1	0.4748	0.0	3.18	1.466	0.683	0.504	2.129	3.295	1.446	-1868.	1094.	13.0	7.920	
0.0	0.2	0.4739	0.0336	3.40	1.440	0.672	0.504	2.202	3.209	1.334	-1882.	1069.	13.0	7.789	
0.0	0.3	0.4730	0.0681	3.42	1.415	0.661	0.503	2.219	3.124	1.314	-1896.	1044.	13.0	7.658	
0.0	0.4	0.4720	0.0978	3.45	1.392	0.652	0.504	2.238	3.063	1.294	-1910.	1019.	13.0	7.531	
0.0	0.5	0.4710	0.1286	3.47	1.368	0.643	0.505	2.241	2.999	1.274	-1924.	1000.	13.0	7.404	
0.0	0.6	0.4700	0.1586	3.49	1.348	0.634	0.506	2.254	2.928	1.255	-1938.	981.	13.0	7.281	
0.0	0.7	0.4690	0.1881	3.52	1.321	0.627	0.507	2.267	2.861	1.235	-1952.	962.	13.0	7.161	
0.0	0.8	0.4680	0.2168	3.54	1.298	0.620	0.510	2.280	2.774	1.216	-1966.	944.	13.1	7.046	
0.0	0.9	0.4670	0.2454	3.56	1.277	0.613	0.512	2.294	2.747	1.198	-1980.	926.	12.9	7.004	
0.0	1.0	0.4660	0.2732	3.58	1.262	0.608	0.515	2.307	2.721	1.179	-1994.	908.	12.8	7.041	
0.0	0.1	0.5407	0.0	3.71	1.351	0.622	0.474	2.147	2.853	1.329	-1878.	1084.	13.0	7.920	

LIQUID MOLE FRACTION		VAPOR MOLE FRACTION			PRESSURE	SQUIL CONST			RELATIVE VOL			ENTHALPY BTU/LB MOLE		HEAT CAPACITY BTU/LB MOLE-K	
N ₁	AR/AR-O ₂	N ₂	AR	O ₂		ATM	N ₂	AR	O ₂	N ₂ /AR	N ₂ /O ₂	AR/O ₂	LIG	VAP	LIG
0.	0.	0.	0.	1.0000	1.97	3.381	1.462	1.000	2.312	3.380	1.462	-1674.	1158.	13.3	7.659
0.	0.1	0.	0.	0.1362	2.06	3.185	1.362	0.960	2.337	3.317	1.419	-1693.	1110.	13.0	7.396
0.	0.2	0.	0.	0.2583	2.14	3.078	1.281	0.930	2.363	3.256	1.378	-1712.	1067.	12.6	7.164
0.	0.3	0.	0.	0.3648	2.22	2.972	1.219	0.908	2.389	3.195	1.338	-1730.	1029.	12.6	6.957
0.	0.4	0.	0.	0.4442	2.28	2.882	1.166	0.893	2.415	3.136	1.299	-1749.	994.	12.3	6.768
0.	0.5	0.	0.	0.5076	2.34	2.802	1.120	0.883	2.441	3.076	1.261	-1768.	961.	12.1	6.595
0.	0.6	0.	0.	0.5570	2.40	2.730	1.079	0.882	2.467	3.016	1.224	-1787.	929.	11.9	6.437
0.	0.7	0.	0.	0.5947	2.43	2.667	1.042	0.883	2.494	2.956	1.189	-1805.	898.	11.6	6.291
0.	0.8	0.	0.	0.6222	2.47	2.612	1.008	0.890	2.522	2.896	1.154	-1824.	868.	11.4	6.154
0.	0.9	0.	0.	0.6410	2.50	2.564	0.977	0.902	2.549	2.837	1.121	-1843.	838.	11.2	6.023
0.	1.0	0.	0.	0.6522	2.53	2.522	0.948	0.917	2.577	2.778	1.088	-1862.	807.	11.0	5.897
0.25	0.	0.6791	0.	0.9211	2.09	3.163	1.374	0.948	2.302	3.346	1.455	-1656.	1159.	13.3	7.401
0.25	0.1	0.6749	0.1256	0.7997	2.18	2.996	1.288	0.911	2.328	3.288	1.413	-1675.	1111.	13.1	7.149
0.25	0.2	0.6715	0.2374	0.6614	2.26	2.881	1.217	0.886	2.351	3.228	1.373	-1693.	1071.	12.9	6.925
0.25	0.3	0.6688	0.3369	0.5026	2.33	2.792	1.159	0.866	2.375	3.170	1.334	-1711.	1035.	12.6	6.729
0.25	0.4	0.6669	0.4229	0.4139	2.39	2.726	1.110	0.856	2.401	3.113	1.297	-1730.	1002.	12.4	6.558
0.25	0.5	0.6659	0.4865	0.3303	2.44	2.669	1.070	0.849	2.428	3.056	1.260	-1748.	971.	12.2	6.402
0.25	0.6	0.6659	0.5215	0.2604	2.48	2.622	1.037	0.847	2.452	3.001	1.224	-1768.	941.	11.9	6.253
0.25	0.7	0.6670	0.5394	0.2004	2.50	2.584	1.010	0.849	2.478	2.947	1.189	-1787.	912.	11.7	6.117
0.25	0.8	0.6719	0.5315	0.1600	2.52	2.552	0.989	0.856	2.504	2.894	1.154	-1805.	883.	11.5	6.001
0.25	0.9	0.6810	0.5042	0.1049	2.53	2.524	0.973	0.867	2.531	2.842	1.121	-1824.	854.	11.3	5.881
0.25	1.0	0.6918	0.4368	0.	2.53	2.503	0.963	0.882	2.558	2.792	1.088	-1843.	825.	11.2	5.765
0.50	0.	0.6791	0.	0.9211	2.09	3.163	1.374	0.948	2.302	3.346	1.455	-1656.	1159.	13.3	7.401
0.50	0.1	0.6749	0.1256	0.7997	2.18	2.996	1.288	0.911	2.328	3.288	1.413	-1675.	1111.	13.1	7.149
0.50	0.2	0.6715	0.2374	0.6614	2.26	2.881	1.217	0.886	2.351	3.228	1.373	-1693.	1071.	12.9	6.925
0.50	0.3	0.6688	0.3369	0.5026	2.33	2.792	1.159	0.866	2.375	3.170	1.334	-1711.	1035.	12.6	6.729
0.50	0.4	0.6669	0.4229	0.4139	2.39	2.726	1.110	0.856	2.401	3.113	1.297	-1730.	1002.	12.4	6.558
0.50	0.5	0.6659	0.4865	0.3303	2.44	2.669	1.070	0.849	2.428	3.056	1.260	-1748.	971.	12.2	6.402
0.50	0.6	0.6659	0.5215	0.2604	2.48	2.622	1.037	0.847	2.452	3.001	1.224	-1768.	941.	11.9	6.253
0.50	0.7	0.6670	0.5394	0.2004	2.50	2.584	1.010	0.849	2.478	2.947	1.189	-1787.	912.	11.7	6.117
0.50	0.8	0.6719	0.5315	0.1600	2.52	2.552	0.989	0.856	2.504	2.894	1.154	-1805.	883.	11.5	6.001
0.50	0.9	0.6810	0.5042	0.1049	2.53	2.524	0.973	0.867	2.531	2.842	1.121	-1824.	854.	11.3	5.881
0.50	1.0	0.6918	0.4368	0.	2.53	2.503	0.963	0.882	2.558	2.792	1.088	-1843.	825.	11.2	5.765
0.75	0.	0.6791	0.	0.9211	2.09	3.163	1.374	0.948	2.302	3.346	1.455	-1656.	1159.	13.3	7.401
0.75	0.1	0.6749	0.1256	0.7997	2.18	2.996	1.288	0.911	2.328	3.288	1.413	-1675.	1111.	13.1	7.149
0.75	0.2	0.6715	0.2374	0.6614	2.26	2.881	1.217	0.886	2.351	3.228	1.373	-1693.	1071.	12.9	6.925
0.75	0.3	0.6688	0.3369	0.5026	2.33	2.792	1.159	0.866	2.375	3.170	1.334	-1711.	1035.	12.6	6.729
0.75	0.4	0.6669	0.4229	0.4139	2.39	2.726	1.110	0.856	2.401	3.113	1.297	-1730.	1002.	12.4	6.558
0.75	0.5	0.6659	0.4865	0.3303	2.44	2.669	1.070	0.849	2.428	3.056	1.260	-1748.	971.	12.2	6.402
0.75	0.6	0.6659	0.5215	0.2604	2.48	2.622	1.037	0.847	2.452	3.001	1.224	-1768.	941.	11.9	6.253
0.75	0.7	0.6670	0.5394	0.2004	2.50	2.584	1.010	0.849	2.478	2.947	1.189	-1787.	912.	11.7	6.117
0.75	0.8	0.6719	0.5315	0.1600	2.52	2.552	0.989	0.856	2.504	2.894	1.154	-1805.	883.	11.5	6.001
0.75	0.9	0.6810	0.5042	0.1049	2.53	2.524	0.973	0.867	2.531	2.842	1.121	-1824.	854.	11.3	5.881
0.75	1.0	0.6918	0.4368	0.	2.53	2.503	0.963	0.882	2.558	2.792	1.088	-1843.	825.	11.2	5.765
1.00	0.	0.6791	0.	0.9211	2.09	3.163	1.374	0.948	2.302	3.346	1.455	-1656.	1159.	13.3	7.401
1.00	0.1	0.6749	0.1256	0.7997	2.18	2.996	1.288	0.911	2.328	3.288	1.413	-1675.	1111.	13.1	7.149
1.00	0.2	0.6715	0.2374	0.6614	2.26	2.881	1.217	0.886	2.351	3.228	1.373	-1693.	1071.	12.9	6.925
1.00	0.3	0.6688	0.3369	0.5026	2.33	2.792	1.159	0.866	2.375	3.170	1.334	-1711.	1035.	12.6	6.729
1.00	0.4	0.6669	0.4229	0.4139	2.39	2.726	1.110	0.856	2.401	3.113	1.297	-1730.	1002.	12.4	6.558
1.00	0.5	0.6659	0.4865	0.3303	2.44	2.669	1.070	0.849	2.428	3.056	1.260	-1748.	971.	12.2	6.402
1.00	0.6	0.6659	0.5215	0.2604	2.48	2.622	1.037	0.847	2.452	3.001	1.224	-1768.	941.	11.9	6.253
1.00	0.7	0.6670	0.5394	0.2004	2.50	2.584	1.010	0.849	2.478	2.947	1.189	-1787.	912.	11.7	6.117
1.00	0.8	0.6719	0.5315	0.1600	2.52	2.552	0.989	0.856	2.504	2.894	1.154	-1805.	883.	11.5	6.001
1.00	0.9	0.6810	0.5042	0.1049	2.53	2.524	0.973	0.867	2.531	2.842	1.121	-1824.	854.	11.3	5.881
1.00	1.0	0.6918	0.4368	0.	2.53	2.503	0.963	0.882	2.558	2.792	1.088	-1843.	825.	11.2	5.765

LIQUID MOLE FRACTION		VAPOR MOLE FRACTION		PRESSURE ATM	EQUIL CONST			RELATIVE VOL			ENTHALPY BTU/LB MOLE		HEAT CAPACITY BTU/LB MOLE-R	
N2	AR/O2	N2	AR		N2	AR	O2	N2/AR	N2/O2	AR/O2	LIG	VAP	LIG	VAP
0.0	0.0	0.0	0.0	2.91	3.170	1.432	1.000	2.214	3.100	1.431	-1408.	1181.	13.3	7.767
0.0	0.1	0.0	0.134	2.92	2.996	1.340	0.963	2.236	3.112	1.392	-1420.	1132.	13.3	7.933
0.0	0.2	0.0	0.258	2.72	2.856	1.264	0.934	2.269	3.056	1.353	-1447.	1088.	12.9	7.306
0.0	0.3	0.0	0.382	2.46	2.743	1.202	0.914	2.282	3.001	1.315	-1467.	1049.	12.7	7.100
0.0	0.4	0.0	0.506	2.26	2.653	1.151	0.900	2.305	2.947	1.279	-1487.	1013.	12.5	6.908
0.0	0.5	0.0	0.630	2.09	2.581	1.109	0.892	2.328	2.894	1.243	-1507.	978.	12.3	6.724
0.0	0.6	0.0	0.754	1.91	2.527	1.075	0.889	2.351	2.842	1.209	-1527.	946.	12.1	6.546
0.0	0.7	0.0	0.878	1.74	2.482	1.047	0.891	2.375	2.791	1.175	-1547.	914.	11.8	6.374
0.0	0.8	0.0	1.002	1.57	2.448	1.024	0.898	2.399	2.742	1.143	-1567.	882.	11.6	6.206
0.0	0.9	0.0	1.126	1.41	2.425	1.002	0.910	2.424	2.693	1.111	-1587.	851.	11.4	6.042
0.0	1.0	0.0	1.250	1.26	2.412	1.000	0.926	2.451	2.643	1.080	-1607.	820.	11.2	5.882
0.05	0.0	0.0746	0.0	2.93	2.942	1.383	0.950	2.254	3.147	1.428	-1490.	1170.	13.4	7.625
0.05	0.1	0.0778	0.124	2.78	2.832	1.273	0.918	2.226	3.085	1.386	-1490.	1133.	13.3	7.590
0.05	0.2	0.0778	0.235	2.65	2.710	1.206	0.894	2.248	3.031	1.348	-1498.	1092.	13.0	7.386
0.05	0.3	0.0833	0.338	2.53	2.612	1.151	0.877	2.270	2.978	1.312	-1498.	1055.	12.8	7.180
0.05	0.4	0.0817	0.438	2.41	2.532	1.105	0.865	2.292	2.924	1.276	-1497.	1020.	12.6	7.005
0.05	0.5	0.0805	0.538	2.30	2.469	1.067	0.859	2.315	2.874	1.242	-1497.	988.	12.3	6.832
0.05	0.6	0.0799	0.638	2.19	2.420	1.035	0.857	2.337	2.824	1.208	-1498.	957.	12.1	6.664
0.05	0.7	0.0799	0.738	2.08	2.384	1.008	0.860	2.360	2.775	1.176	-1498.	926.	11.9	6.494
0.05	0.8	0.0799	0.838	1.97	2.348	0.986	0.866	2.384	2.727	1.144	-1498.	896.	11.7	6.326
0.05	0.9	0.0799	0.938	1.86	2.327	0.968	0.878	2.407	2.679	1.113	-1498.	866.	11.5	6.158
0.05	1.0	0.0799	1.038	1.75	2.317	0.954	0.892	2.431	2.631	1.083	-1498.	836.	11.3	5.992
0.10	0.0	0.2936	0.0	3.08	3.036	1.164	0.930	2.178	3.056	1.373	-1498.	1109.	13.3	7.677
0.10	0.1	0.2436	0.0999	3.17	2.436	1.110	0.911	2.198	3.026	1.371	-1498.	1109.	13.3	7.677
0.10	0.2	0.2394	0.1914	3.29	2.394	1.083	0.796	2.214	2.997	1.335	-1498.	1109.	13.3	7.677
0.10	0.3	0.2286	0.2763	3.32	2.366	1.023	0.796	2.235	2.969	1.302	-1498.	1109.	13.3	7.677
0.10	0.4	0.2211	0.3561	3.36	2.331	0.989	0.779	2.255	2.942	1.269	-1498.	1109.	13.3	7.677
0.10	0.5	0.2155	0.4323	3.45	2.165	0.961	0.776	2.275	2.916	1.236	-1498.	1109.	13.3	7.677
0.10	0.6	0.2123	0.5074	3.51	2.105	0.936	0.776	2.296	2.770	1.207	-1498.	1109.	13.3	7.677
0.10	0.7	0.2123	0.5774	3.50	2.123	0.917	0.779	2.317	2.724	1.177	-1498.	1109.	13.3	7.677
0.10	0.8	0.2123	0.6483	3.50	2.145	0.893	0.785	2.338	2.682	1.147	-1498.	1109.	13.3	7.677
0.10	0.9	0.2123	0.7192	3.54	2.169	0.869	0.794	2.359	2.639	1.119	-1498.	1109.	13.3	7.677
0.10	1.0	0.2123	0.7901	3.57	2.192	0.846	0.808	2.381	2.596	1.091	-1498.	1109.	13.3	7.677
0.15	0.0	0.4281	0.0	3.62	1.121	0.907	0.710	2.138	2.943	1.321	-1498.	1109.	13.3	7.677
0.15	0.1	0.4123	0.0766	3.70	2.041	0.987	0.720	2.154	2.916	1.348	-1498.	1109.	13.3	7.677
0.15	0.2	0.4021	0.1482	3.76	2.011	0.926	0.703	2.171	2.881	1.318	-1498.	1109.	13.3	7.677
0.15	0.3	0.3923	0.2198	3.81	1.980	0.869	0.698	2.188	2.846	1.288	-1498.	1109.	13.3	7.677
0.15	0.4	0.3833	0.2912	3.86	1.932	0.876	0.695	2.206	2.790	1.260	-1498.	1109.	13.3	7.677
0.15	0.5	0.3758	0.3627	3.93	1.892	0.855	0.694	2.224	2.740	1.232	-1498.	1109.	13.3	7.677
0.15	0.6	0.3718	0.4342	3.98	1.878	0.838	0.695	2.242	2.700	1.205	-1498.	1109.	13.3	7.677
0.15	0.7	0.3691	0.5057	4.03	1.889	0.823	0.698	2.260	2.660	1.178	-1498.	1109.	13.3	7.677
0.15	0.8	0.3674	0.5772	4.07	1.905	0.810	0.703	2.278	2.623	1.152	-1498.	1109.	13.3	7.677
0.15	0.9	0.3666	0.6487	4.11	1.937	0.800	0.710	2.296	2.586	1.126	-1498.	1109.	13.3	7.677
0.15	1.0	0.3666	0.7202	4.15	1.973	0.792	0.718	2.315	2.549	1.101	-1498.	1109.	13.3	7.677
0.20	0.0	0.5379	0.0	4.18	1.830	0.870	0.624	2.113	2.944	1.313	-1498.	1109.	13.3	7.677
0.20	0.1	0.5379	0.0904	4.21	1.793	0.849	0.639	2.133	2.916	1.337	-1498.	1109.	13.3	7.677
0.20	0.2	0.5282	0.1798	4.26	1.761	0.827	0.636	2.153	2.881	1.301	-1498.	1109.	13.3	7.677
0.20	0.3	0.5198	0.2692	4.31	1.733	0.809	0.634	2.173	2.846	1.274	-1498.	1109.	13.3	7.677
0.20	0.4	0.5126	0.3586	4.36	1.709	0.792	0.633	2.193	2.810	1.251	-1498.	1109.	13.3	7.677
0.20	0.5	0.5065	0.4480	4.41	1.688	0.777	0.633	2.213	2.775	1.226	-1498.	1109.	13.3	7.677
0.20	0.6	0.5013	0.5374	4.46	1.672	0.764	0.635	2.233	2.740	1.203	-1498.	1109.	13.3	7.677
0.20	0.7	0.4978	0.6268	4.49	1.659	0.752	0.638	2.253	2.705	1.179	-1498.	1109.	13.3	7.677
0.20	0.8	0.4954	0.7162	4.53	1.648	0.743	0.642	2.273	2.670	1.156	-1498.	1109.	13.3	7.677
0.20	0.9	0.4933	0.8056	4.57	1.641	0.734	0.648	2.293	2.634	1.134	-1498.	1109.	13.3	7.677
0.20	1.0	0.4923	0.8950	4.61	1.637	0.727	0.654	2.313	2.598	1.112	-1498.	1109.	13.3	7.677
0.25	0.0	0.7042	0.0	4.56	1.615	0.744	0.590	2.181	2.798	1.328	-1498.	1109.	13.3	7.677
0.25	0.1	0.6867	0.0461	4.70	1.562	0.768	0.586	2.173	2.758	1.306	-1498.	1109.	13.3	7.677
0.25	0.2	0.6688	0.0954	4.78	1.571	0.783	0.586	2.166	2.718	1.284	-1498.	1109.	13.3	7.677
0.25	0.3	0.6508	0.1447	4.79	1.552	0.740	0.583	2.188	2.679	1.263	-1498.	1109.	13.3	7.677
0.25	0.4	0.6328	0.1940	4.83	1.536	0.728	0.586	2.211	2.642	1.242	-1498.	1109.	13.3	7.677
0.25	0.5	0.6148	0.2433	4.87	1.523	0.717	0.587	2.233	2.605	1.221	-1498.	1109.	13.3	7.677
0.25	0.6	0.5968	0.2926	4.91	1.511	0.707	0.589	2.255	2.568	1.201	-1498.	1109.	13.3	7.677
0.25	0.7	0.5788	0.3419	4.95	1.501	0.698	0.592	2.277	2.531	1.181	-1498.	1109.	13.3	7.677
0.25	0.8	0.5608	0.3912	4.98	1.493	0.691	0.595	2.299	2.494	1.161	-1498.	1109.	13.3	7.677
0.25	0.9	0.5428	0.4405	5.02	1.486	0.684	0.599	2.321	2.457	1.141	-1498.	1109.	13.3	7.677
0.25	1.0	0.5248	0.4898	5.05	1.481	0.678	0.604	2.343	2.420	1.122	-1498.	1109.	13.3	7.677
0.30	0.0	0.9254	0.0	5.15	1.481	0.717	0.590	2.024	2.629	1.304	-1498.	1109.	13.3	7.677
0.30	0.1	0.7116	0.0363	5.23	1.436	0.708	0.549	2.034	2.616	1.286	-1498.	1109.	13.3	7.677
0.30	0.2	0.7116	0.0696	5.23	1.402	0.688	0.549	2.045	2.592	1.268	-1498.	1109.	13.3	7.677
0.30	0.3	0.7028	0.1030	5.20	1.410	0.686	0.549	2.055	2.569	1.250	-1498.	1109.	13.3	7.677
0.30	0.4	0.6940	0.1364	5.30	1.400	0.678	0.550	2.065	2.546	1.233	-1498.	1109.	13.3	7.677
0.30	0.5	0.6852	0.1698	5.33	1.390	0.670	0.551	2.075	2.523	1.215	-1498.	1109.	13.3	7.677
0.30	0.6	0.6764	0.2032	5.36	1.382	0.663	0.553	2.086	2.500	1.199	-1498.	1109.	13.3	7.677
0.30	0.7	0.6676	0.2366	5.40	1.375	0.656	0.555	2.096	2.478	1.182	-1498.	1109.	13.3	7.677
0.30	0.8	0.6588	0.2700	5.43	1.369	0.650	0.558	2.107	2.456	1.165	-1498.	1109.	13.3	7.677
0.30	0.9	0.6500	0.3034	5.46	1.365	0.644	0.561	2.117	2.433	1.149	-1498.	1109.	13.3	7.677
0.30	1.0	0.6412	0.3368	5.49	1.361	0.640	0.564	2.128	2.411	1.133	-1498.	1109.	13.3	7.677
0.35	0.0	1.1071	0.0	5.25	1.321	0.669	0.519	1.988	2.544	1.285	-1498.	1109.	13.3	7.677
0.35	0.1	0.7871	0.0244	5.38	1.312	0.657	0.519	1.996	2.526	1.266	-1498.	1109.	13.3	7.677
0.35	0.2	0.7871	0.0578	5.41	1.303	0.646	0.520	2.004	2.508	1.251	-1498.	1109.	13.3	7.677
0.35	0.3	0.7774	0.0912	5.45	1.294	0.635	0.521	2.012	2.490	1.237	-1498.</			

LIQUID MOLE FRACTION		VAPOR MOLE FRACTION			PRESSURE	EQUIL CONST			RELATIVE VOL			ENTHALPY		HEAT CAPACITY	
N2	AR/AR+O2	N2	AR	O2		ATM	N2	AR	O2	N2/AR	N2/O2	AR/O2	LTD	VAP	LTD
.0	0.	0.	0.	1.0005	3.15	2.977	1.404	1.000	2.170	2.975	1.404	-1941.	1263.	13.4	7.936
.0	0.1	0.	0.	0.1310	3.26	2.820	1.318	0.985	2.140	2.923	1.306	-1942.	1152.	13.2	7.688
.0	0.2	0.	0.	0.2495	3.40	2.694	1.248	0.938	2.109	2.872	1.330	-1943.	1107.	13.0	7.465
.0	0.3	0.	0.	0.3560	3.56	2.593	1.190	0.919	2.179	2.822	1.295	-1944.	1077.	12.8	7.263
.0	0.4	0.	0.	0.4506	3.80	2.447	1.140	0.906	2.200	2.772	1.260	-1945.	1067.	12.6	7.073
.0	0.5	0.	0.	0.5310	4.08	2.307	1.100	0.898	2.226	2.724	1.227	-1946.	1064.	12.4	6.892
.0	0.6	0.	0.	0.6418	4.41	2.181	1.070	0.894	2.254	2.677	1.194	-1947.	1062.	12.3	6.714
.0	0.7	0.	0.	0.7307	4.81	2.061	1.044	0.890	2.282	2.630	1.163	-1948.	1061.	12.1	6.538
.0	0.8	0.	0.	0.8192	5.28	1.946	1.024	0.885	2.309	2.583	1.132	-1949.	1061.	11.9	6.366
.0	0.9	0.	0.	0.9085	5.83	1.836	1.009	0.881	2.335	2.536	1.102	-1950.	1061.	11.7	6.197
.0	1.0	0.	0.	1.0001	6.45	1.730	1.000	0.878	2.359	2.490	1.073	-1951.	1061.	11.5	6.030
.025	0.	0.0703	0.	0.9297	7.12	1.627	1.000	0.874	2.381	2.443	1.047	-1952.	1061.	11.3	5.866
.025	0.1	0.1669	0.1226	0.8109	7.44	1.526	1.000	0.870	2.401	2.396	1.021	-1953.	1061.	11.1	5.705
.025	0.2	0.2654	0.2350	0.7029	7.80	1.428	1.000	0.866	2.419	2.349	1.001	-1954.	1061.	10.9	5.547
.025	0.3	0.3620	0.3342	0.6030	8.20	1.333	1.000	0.862	2.435	2.302	0.981	-1955.	1061.	10.7	5.392
.025	0.4	0.4561	0.4297	0.5112	8.64	1.240	1.000	0.858	2.449	2.255	0.961	-1956.	1061.	10.5	5.240
.025	0.5	0.5480	0.5104	0.4230	9.12	1.149	1.000	0.854	2.461	2.208	0.941	-1957.	1061.	10.3	5.091
.025	0.6	0.6380	0.4944	0.3377	9.64	1.060	1.000	0.850	2.471	2.161	0.921	-1958.	1061.	10.1	4.944
.025	0.7	0.7260	0.4800	0.2540	10.20	0.973	1.000	0.846	2.479	2.114	0.901	-1959.	1061.	9.9	4.799
.025	0.8	0.8120	0.4650	0.1704	10.80	0.888	1.000	0.842	2.485	2.067	0.881	-1960.	1061.	9.7	4.656
.025	0.9	0.8960	0.4500	0.0863	11.44	0.804	1.000	0.838	2.489	2.020	0.861	-1961.	1061.	9.5	4.514
.025	1.0	0.9780	0.4441	0.	12.12	0.721	1.000	0.834	2.491	1.973	0.841	-1962.	1061.	9.3	4.373
.100	0.	0.2410	0.	0.7581	13.84	0.640	1.000	0.830	2.491	1.926	0.821	-1963.	1061.	9.1	4.233
.100	0.1	0.3320	0.0996	0.6674	14.64	0.560	1.000	0.826	2.489	1.879	0.801	-1964.	1061.	8.9	4.094
.100	0.2	0.4224	0.1915	0.5833	15.48	0.481	1.000	0.822	2.485	1.832	0.781	-1965.	1061.	8.7	3.956
.100	0.3	0.5112	0.2760	0.5041	16.36	0.403	1.000	0.818	2.479	1.785	0.761	-1966.	1061.	8.5	3.819
.100	0.4	0.5980	0.3525	0.4280	17.28	0.326	1.000	0.814	2.471	1.738	0.741	-1967.	1061.	8.3	3.683
.100	0.5	0.6830	0.4300	0.3540	18.24	0.250	1.000	0.810	2.461	1.691	0.721	-1968.	1061.	8.1	3.548
.100	0.6	0.7660	0.5080	0.2800	19.24	0.175	1.000	0.806	2.449	1.644	0.701	-1969.	1061.	7.9	3.414
.100	0.7	0.8480	0.5860	0.2100	20.28	0.101	1.000	0.802	2.435	1.597	0.681	-1970.	1061.	7.7	3.280
.100	0.8	0.9290	0.6630	0.1430	21.36	0.027	1.000	0.798	2.419	1.550	0.661	-1971.	1061.	7.5	3.146
.100	0.9	0.9980	0.7260	0.0727	22.48	0.000	1.000	0.794	2.401	1.503	0.641	-1972.	1061.	7.3	3.012
.100	1.0	0.9991	0.7990	0.	23.64	0.000	1.000	0.790	2.381	1.456	0.621	-1973.	1061.	7.1	2.878
.200	0.	0.4940	0.	0.5057	26.88	0.207	0.999	0.786	2.359	1.409	0.601	-1974.	1061.	6.9	2.744
.200	0.1	0.5880	0.0772	0.5246	28.16	0.132	0.999	0.782	2.345	1.362	0.581	-1975.	1061.	6.7	2.610
.200	0.2	0.6830	0.1494	0.4617	29.48	0.057	0.999	0.778	2.329	1.315	0.561	-1976.	1061.	6.5	2.476
.200	0.3	0.7800	0.2182	0.4012	30.84	0.000	0.999	0.774	2.311	1.268	0.541	-1977.	1061.	6.3	2.342
.200	0.4	0.8780	0.2836	0.3420	32.24	0.000	0.999	0.770	2.291	1.221	0.521	-1978.	1061.	6.1	2.208
.200	0.5	0.9760	0.3460	0.2852	33.68	0.000	0.999	0.766	2.269	1.174	0.501	-1979.	1061.	5.9	2.074
.200	0.6	0.9930	0.4070	0.2289	35.16	0.000	0.999	0.762	2.245	1.127	0.481	-1980.	1061.	5.7	1.940
.200	0.7	0.9980	0.4670	0.1721	36.68	0.000	0.999	0.758	2.219	1.080	0.461	-1981.	1061.	5.5	1.806
.200	0.8	0.9990	0.5240	0.1159	38.24	0.000	0.999	0.754	2.191	1.033	0.441	-1982.	1061.	5.3	1.672
.200	0.9	0.9990	0.5890	0.0583	39.84	0.000	0.999	0.750	2.161	0.986	0.421	-1983.	1061.	5.1	1.538
.200	1.0	0.9990	0.6440	0.	41.48	0.000	0.999	0.746	2.129	0.939	0.401	-1984.	1061.	4.9	1.404
.300	0.	0.5343	0.	0.4657	45.12	0.171	0.998	0.742	2.095	0.892	0.381	-1985.	1061.	4.7	1.270
.300	0.1	0.6230	0.0603	0.4161	46.80	0.096	0.998	0.738	2.069	0.845	0.361	-1986.	1061.	4.5	1.136
.300	0.2	0.7140	0.1177	0.3670	48.52	0.021	0.998	0.734	2.041	0.798	0.341	-1987.	1061.	4.3	1.002
.300	0.3	0.8060	0.1720	0.3200	50.28	0.000	0.998	0.730	2.011	0.751	0.321	-1988.	1061.	4.1	0.868
.300	0.4	0.8980	0.2256	0.2747	52.08	0.000	0.998	0.726	1.979	0.704	0.301	-1989.	1061.	3.9	0.734
.300	0.5	0.9900	0.2772	0.2291	53.92	0.000	0.998	0.722	1.945	0.657	0.281	-1990.	1061.	3.7	0.600
.300	0.6	0.9930	0.3273	0.1837	55.80	0.000	0.998	0.718	1.909	0.610	0.261	-1991.	1061.	3.5	0.466
.300	0.7	0.9950	0.3760	0.1384	57.72	0.000	0.998	0.714	1.871	0.563	0.241	-1992.	1061.	3.3	0.332
.300	0.8	0.9960	0.4240	0.0920	59.68	0.000	0.998	0.710	1.831	0.516	0.221	-1993.	1061.	3.1	0.198
.300	0.9	0.9960	0.4720	0.0460	61.68	0.000	0.998	0.706	1.789	0.469	0.201	-1994.	1061.	2.9	0.064
.300	1.0	0.9950	0.5200	0.	63.72	0.000	0.998	0.702	1.745	0.422	0.181	-1995.	1061.	2.7	0.000
.400	0.	0.6320	0.	0.3679	68.88	0.152	0.997	0.698	1.709	0.375	0.161	-1996.	1061.	2.5	0.000
.400	0.1	0.7230	0.0470	0.3195	71.04	0.077	0.997	0.694	1.671	0.328	0.141	-1997.	1061.	2.3	0.000
.400	0.2	0.8140	0.0923	0.2722	73.24	0.002	0.997	0.690	1.631	0.281	0.121	-1998.	1061.	2.1	0.000
.400	0.3	0.9060	0.1341	0.2254	75.48	0.000	0.997	0.686	1.589	0.234	0.101	-1999.	1061.	1.9	0.000
.400	0.4	0.9980	0.1787	0.1790	77.76	0.000	0.997	0.682	1.545	0.187	0.081	-2000.	1061.	1.7	0.000
.400	0.5	0.9990	0.2250	0.1320	80.08	0.000	0.997	0.678	1.499	0.140	0.061	-2001.	1061.	1.5	0.000
.400	0.6	0.9990	0.2740	0.0867	82.44	0.000	0.997	0.674	1.451	0.093	0.041	-2002.	1061.	1.3	0.000
.400	0.7	0.9990	0.3250	0.0417	84.84	0.000	0.997	0.670	1.401	0.046	0.021	-2003.	1061.	1.1	0.000
.400	0.8	0.9990	0.3780	0.0000	87.28	0.000	0.997	0.666	1.349	0.000	0.001	-2004.	1061.	0.9	0.000
.400	0.9	0.9990	0.4320	0.0000	89.76	0.000	0.997	0.662	1.295	0.000	0.000	-2005.	1061.	0.7	0.000
.400	1.0	0.9990	0.4780	0.	92.28	0.000	0.997	0.658	1.239	0.000	0.000	-2006.	1061.	0.5	0.000
.500	0.	0.7140	0.	0.2864	98.88	0.142	0.996	0.654	1.191	0.202	0.111	-2007.	1061.	0.3	0.000
.500	0.1	0.8060	0.0362	0.2374	101.16	0.067	0.996	0.650	1.141	0.155	0.091	-2008.	1061.	0.1	0.000
.500	0.2	0.8980	0.0714	0.1880	103.48	0.000	0.996	0.646	1.089	0.108	0.071	-2009.	1061.	0.0	0.000
.500	0.3	0.9900	0.1057	0.1390	105.84	0.000	0.996	0.642	1.035	0.061	0.051	-2010.	1061.	0.0	0.000
.500	0.4	0.9930	0.1392	0.0900	108.24	0.000	0.996	0.638	0.979	0.014	0.031	-2011.	1061.	0.0	0.000
.500	0.5	0.9950	0.1720	0.0410	110.68	0.000	0.996	0.634	0.921	0.000	0.011	-2012.	1061.	0.0	0.000
.500	0.6	0.9960	0.2043	0.0000	113.16	0.000	0.996	0.630	0.861	0.000	0.000	-2013.	1061.	0.0	0.000
.500	0.7	0.9960	0.2360	0.0000	115.68	0.000	0.996	0.626	0.799	0.000	0.000	-2014.	1061.	0.0	0.000
.500	0.8	0.9960	0.2674	0.0000	118.24	0.000	0.996	0.622	0.735	0.000	0.000	-2015.	1061.	0.0	0.000
.500	0.9	0.9960	0.2985	0.0000	120.84	0.000	0.996	0.618	0.669	0.000	0.000	-2016.	1061.	0.0	0.000
.500	1.0	0.9950	0.3293	0.	123.4										

TEMPERATURE	LIQUID MOLE FRACTION			VAPOR MOLE FRACTION			PRESSURE	EQUIL CONST			RELATIVE VOL			ENTHALPY		HEAT CAPACITY	
	N2	AR	O2	N2	AR	O2		ATH	N2	AR	O2	N2/AR	N2/O2	AR/O2	LIQ	VAP	LIQ
0.0	0.0	0.0	1.0000	0.0000	0.0000	0.0000	3.90	2.796	1.378	1.000	2.150	2.796	1.378	-1474	1222	13.4	8.192
0.1	0.0	0.0	0.9999	0.0001	0.0000	0.0000	4.06	2.690	1.298	0.967	2.047	2.740	1.343	-1494	1171	13.3	7.864
0.2	0.0	0.0	0.9998	0.0002	0.0000	0.0000	4.20	2.595	1.233	0.942	2.005	2.702	1.309	-1517	1125	13.1	7.609
0.3	0.0	0.0	0.9996	0.0004	0.0000	0.0000	4.32	2.503	1.178	0.924	2.002	2.660	1.275	-1539	1083	13.0	7.433
0.4	0.0	0.0	0.9993	0.0007	0.0000	0.0000	4.43	2.421	1.133	0.911	2.100	2.621	1.243	-1561	1044	12.9	7.266
0.5	0.0	0.0	0.9989	0.0011	0.0000	0.0000	4.53	2.341	1.096	0.904	2.118	2.586	1.212	-1583	1009	12.8	7.097
0.6	0.0	0.0	0.9984	0.0016	0.0000	0.0000	4.61	2.274	1.065	0.902	2.136	2.553	1.181	-1604	972	12.8	6.911
0.7	0.0	0.0	0.9978	0.0022	0.0000	0.0000	4.69	2.212	1.039	0.904	2.155	2.521	1.151	-1626	938	12.8	6.735
0.8	0.0	0.0	0.9971	0.0029	0.0000	0.0000	4.76	2.154	1.017	0.911	2.173	2.490	1.122	-1648	904	12.8	6.567
0.9	0.0	0.0	0.9963	0.0037	0.0000	0.0000	4.84	2.101	0.998	0.928	2.192	2.460	1.094	-1669	870	12.8	6.403
1.0	0.0	0.0	0.9954	0.0046	0.0000	0.0000	4.91	2.052	0.982	0.950	2.211	2.430	1.066	-1691	835	12.8	6.241
1.1	0.0	0.0	0.9945	0.0056	0.0000	0.0000	4.98	2.007	0.969	0.976	2.230	2.400	1.038	-1713	800	12.8	6.081
1.2	0.0	0.0	0.9935	0.0067	0.0000	0.0000	5.05	1.966	0.958	1.000	2.250	2.370	1.010	-1735	765	12.8	5.922
1.3	0.0	0.0	0.9925	0.0079	0.0000	0.0000	5.12	1.928	0.949	1.023	2.270	2.340	0.982	-1757	730	12.8	5.764
1.4	0.0	0.0	0.9915	0.0092	0.0000	0.0000	5.19	1.893	0.941	1.046	2.290	2.310	0.954	-1779	695	12.8	5.607
1.5	0.0	0.0	0.9905	0.0106	0.0000	0.0000	5.26	1.860	0.934	1.069	2.310	2.280	0.926	-1801	660	12.8	5.451
1.6	0.0	0.0	0.9895	0.0121	0.0000	0.0000	5.33	1.829	0.928	1.092	2.330	2.250	0.898	-1823	625	12.8	5.295
1.7	0.0	0.0	0.9885	0.0137	0.0000	0.0000	5.40	1.800	0.923	1.115	2.350	2.220	0.870	-1845	590	12.8	5.140
1.8	0.0	0.0	0.9875	0.0154	0.0000	0.0000	5.47	1.773	0.918	1.138	2.370	2.190	0.842	-1867	555	12.8	4.985
1.9	0.0	0.0	0.9865	0.0172	0.0000	0.0000	5.54	1.748	0.914	1.161	2.390	2.160	0.814	-1889	520	12.8	4.830
2.0	0.0	0.0	0.9855	0.0191	0.0000	0.0000	5.61	1.724	0.910	1.184	2.410	2.130	0.786	-1911	485	12.8	4.675
2.1	0.0	0.0	0.9845	0.0211	0.0000	0.0000	5.68	1.701	0.906	1.207	2.430	2.100	0.758	-1933	450	12.8	4.520
2.2	0.0	0.0	0.9835	0.0232	0.0000	0.0000	5.75	1.679	0.902	1.230	2.450	2.070	0.730	-1955	415	12.8	4.365
2.3	0.0	0.0	0.9825	0.0254	0.0000	0.0000	5.82	1.658	0.898	1.253	2.470	2.040	0.702	-1977	380	12.8	4.210
2.4	0.0	0.0	0.9815	0.0277	0.0000	0.0000	5.89	1.638	0.894	1.276	2.490	2.010	0.674	-1999	345	12.8	4.055
2.5	0.0	0.0	0.9805	0.0301	0.0000	0.0000	5.96	1.619	0.890	1.299	2.510	1.980	0.646	-2021	310	12.8	3.900
2.6	0.0	0.0	0.9795	0.0326	0.0000	0.0000	6.03	1.601	0.886	1.322	2.530	1.950	0.618	-2043	275	12.8	3.745
2.7	0.0	0.0	0.9785	0.0352	0.0000	0.0000	6.10	1.584	0.882	1.345	2.550	1.920	0.590	-2065	240	12.8	3.590
2.8	0.0	0.0	0.9775	0.0379	0.0000	0.0000	6.17	1.568	0.878	1.368	2.570	1.890	0.562	-2087	205	12.8	3.435
2.9	0.0	0.0	0.9765	0.0407	0.0000	0.0000	6.24	1.553	0.874	1.391	2.590	1.860	0.534	-2109	170	12.8	3.280
3.0	0.0	0.0	0.9755	0.0436	0.0000	0.0000	6.31	1.539	0.870	1.414	2.610	1.830	0.506	-2131	135	12.8	3.125
3.1	0.0	0.0	0.9745	0.0466	0.0000	0.0000	6.38	1.526	0.866	1.437	2.630	1.800	0.478	-2153	100	12.8	2.970
3.2	0.0	0.0	0.9735	0.0497	0.0000	0.0000	6.45	1.514	0.862	1.460	2.650	1.770	0.450	-2175	65	12.8	2.815
3.3	0.0	0.0	0.9725	0.0529	0.0000	0.0000	6.52	1.503	0.858	1.483	2.670	1.740	0.422	-2197	30	12.8	2.660
3.4	0.0	0.0	0.9715	0.0562	0.0000	0.0000	6.59	1.493	0.854	1.506	2.690	1.710	0.394	-2219	-5	12.8	2.505
3.5	0.0	0.0	0.9705	0.0596	0.0000	0.0000	6.66	1.484	0.850	1.529	2.710	1.680	0.366	-2241	-40	12.8	2.350
3.6	0.0	0.0	0.9695	0.0631	0.0000	0.0000	6.73	1.476	0.846	1.552	2.730	1.650	0.338	-2263	-75	12.8	2.195
3.7	0.0	0.0	0.9685	0.0667	0.0000	0.0000	6.80	1.469	0.842	1.575	2.750	1.620	0.310	-2285	-110	12.8	2.040
3.8	0.0	0.0	0.9675	0.0704	0.0000	0.0000	6.87	1.463	0.838	1.598	2.770	1.590	0.282	-2307	-145	12.8	1.885
3.9	0.0	0.0	0.9665	0.0742	0.0000	0.0000	6.94	1.458	0.834	1.621	2.790	1.560	0.254	-2329	-180	12.8	1.730
4.0	0.0	0.0	0.9655	0.0781	0.0000	0.0000	7.01	1.454	0.830	1.644	2.810	1.530	0.226	-2351	-215	12.8	1.575
4.1	0.0	0.0	0.9645	0.0821	0.0000	0.0000	7.08	1.451	0.826	1.667	2.830	1.500	0.198	-2373	-250	12.8	1.420
4.2	0.0	0.0	0.9635	0.0862	0.0000	0.0000	7.15	1.448	0.822	1.690	2.850	1.470	0.170	-2395	-285	12.8	1.265
4.3	0.0	0.0	0.9625	0.0904	0.0000	0.0000	7.22	1.446	0.818	1.713	2.870	1.440	0.142	-2417	-320	12.8	1.110
4.4	0.0	0.0	0.9615	0.0947	0.0000	0.0000	7.29	1.445	0.814	1.736	2.890	1.410	0.114	-2439	-355	12.8	0.955
4.5	0.0	0.0	0.9605	0.0991	0.0000	0.0000	7.36	1.444	0.810	1.759	2.910	1.380	0.086	-2461	-390	12.8	0.800
4.6	0.0	0.0	0.9595	0.1036	0.0000	0.0000	7.43	1.444	0.806	1.782	2.930	1.350	0.058	-2483	-425	12.8	0.645
4.7	0.0	0.0	0.9585	0.1082	0.0000	0.0000	7.50	1.444	0.802	1.805	2.950	1.320	0.030	-2505	-460	12.8	0.490
4.8	0.0	0.0	0.9575	0.1129	0.0000	0.0000	7.57	1.444	0.798	1.828	2.970	1.290	0.002	-2527	-495	12.8	0.335
4.9	0.0	0.0	0.9565	0.1177	0.0000	0.0000	7.64	1.444	0.794	1.851	2.990	1.260	-0.026	-2549	-530	12.8	0.180
5.0	0.0	0.0	0.9555	0.1226	0.0000	0.0000	7.71	1.444	0.790	1.874	3.010	1.230	-0.054	-2571	-565	12.8	0.025
5.1	0.0	0.0	0.9545	0.1276	0.0000	0.0000	7.78	1.444	0.786	1.897	3.030	1.200	-0.082	-2593	-600	12.8	-0.130
5.2	0.0	0.0	0.9535	0.1327	0.0000	0.0000	7.85	1.444	0.782	1.920	3.050	1.170	-0.110	-2615	-635	12.8	-0.285
5.3	0.0	0.0	0.9525	0.1379	0.0000	0.0000	7.92	1.444	0.778	1.943	3.070	1.140	-0.138	-2637	-670	12.8	-0.440
5.4	0.0	0.0	0.9515	0.1432	0.0000	0.0000	7.99	1.444	0.774	1.966	3.090	1.110	-0.166	-2659	-705	12.8	-0.595
5.5	0.0	0.0	0.9505	0.1486	0.0000	0.0000	8.06	1.444	0.770	1.989	3.110	1.080	-0.194	-2681	-740	12.8	-0.750
5.6	0.0	0.0	0.9495	0.1541	0.0000	0.0000	8.13	1.444	0.766	2.012	3.130	1.050	-0.222	-2703	-775	12.8	-0.905
5.7	0.0	0.0	0.9485	0.1597	0.0000	0.0000	8.20	1.444	0.762	2.035	3.150	1.020	-0.250	-2725	-810	12.8	-1.060
5.8	0.0	0.0	0.9475	0.1654	0.0000	0.0000	8.27	1.444	0.758	2.058	3.170	0.990	-0.278	-2747	-845	12.8	-1.215
5.9	0.0	0.0	0.9465	0.1712	0.0000	0.0000	8.34	1.444	0.754	2.081	3.190	0.960	-0.306	-2769	-880	12.8	-1.370
6.0	0.0	0.0	0.9455	0.1771	0.0000	0.0000	8.41	1.444	0.750	2.104	3.210	0.930	-0.334	-2791	-915	12.8	-1.525
6.1	0.0	0.0	0.9445	0.1831	0.0000	0.0000	8.48	1.444	0.746	2.127	3.230	0.900	-0.362	-2813	-950	12.8	-1.680
6.2	0.0	0.0	0.9435	0.1892	0.0000	0.0000	8.55	1.444	0.742	2.150	3.250	0.870	-0.390	-2835	-985	12.8	-1.835
6.3	0.0	0.0	0.9425	0.1954	0.0000	0.0000	8.62	1.444	0.738	2.173	3.270	0.840	-0.418	-2857	-1020	12.8	-1.990
6.4	0.0	0.0	0.9415	0.2017	0.0000	0.0000	8.69	1.444	0.734	2.196	3.290	0.810	-0.446	-2879	-1055	12.8	-2.145
6.5	0.0	0.0	0.9405	0.2081	0.0000	0.0000	8.76	1.444	0.730	2.219	3.310	0.780	-0.474	-2901	-1090	12.8	-2.300
6.6	0.0	0.0	0.9395	0.2146	0.0000	0.0000	8.83	1.444	0.726	2.242	3.330	0.750	-0.502	-2923	-1125	12.8	-2.455
6.7	0.0	0.0	0.9385	0.2212	0.0000	0.0000	8.										

T	LIQUID MOLE FRACTION			VAPOR MOLE FRACTION			PRESSURE ATM	EQUIL CONST			RELATIVE VOL			ENTHALPY BTU/LB MOLE		HEAT CAPACITY BTU/LB MOLE-R			
	N2	AR/AR+O2		N2	AR			O2	N2	AR		O2	N2/AR	N2/O2	AR/O2	LIQ	VAP	LIQ	VAP
		N2	AR		O2	AR				O2	AR								
.00	0.	0.	0.	0.	0.	0.	4.78	2.631	1.353	1.000	1.944	2.431	1.353	-1407.	1239.	13.5	8.297		
.01	0.	0.	0.	0.1079	0.7722	0.1199	4.97	2.597	1.279	0.949	1.940	2.387	1.320	-1429.	1187.	13.4	8.069		
.02	0.	0.	0.	0.2437	0.7263	0.2707	5.13	2.406	1.218	0.940	1.975	2.344	1.288	-1452.	1149.	13.2	7.863		
.03	0.	0.	0.	0.3792	0.6799	0.4072	5.27	2.324	1.167	0.929	1.990	2.302	1.257	-1474.	1097.	13.1	7.671		
.04	0.	0.	0.	0.5147	0.6335	0.5347	5.40	2.257	1.129	0.917	2.006	2.261	1.227	-1496.	1057.	13.0	7.488		
.05	0.	0.	0.	0.6502	0.5872	0.6648	5.51	2.204	1.090	0.910	2.022	2.221	1.197	-1518.	1017.	12.9	7.312		
.06	0.	0.	0.	0.7857	0.5409	0.7953	5.61	2.163	1.061	0.909	2.038	2.181	1.168	-1541.	983.	12.7	7.136		
.07	0.	0.	0.	0.9212	0.4946	0.9307	5.70	2.133	1.039	0.911	2.054	2.140	1.140	-1564.	947.	12.6	6.963		
.08	0.	0.	0.	0.9867	0.4483	0.9802	5.77	2.114	1.021	0.918	2.071	2.104	1.113	-1588.	912.	12.5	6.795		
.09	0.	0.	0.	0.9974	0.4020	0.9929	5.83	2.104	1.009	0.928	2.087	2.066	1.086	-1608.	877.	12.4	6.637		
.10	0.	0.	0.	1.0000	0.3557	1.0000	5.88	2.104	1.000	0.944	2.104	2.030	1.060	-1631.	841.	12.2	6.483		
.105	0.	0.027	0.	0.9727	0.3094	0.9727	5.92	2.109	0.987	0.961	2.107	2.000	1.037	-1658.	806.	12.0	6.334		
.11	0.	0.054	0.	0.9454	0.2631	0.9454	5.94	2.110	0.974	0.978	2.108	1.966	1.014	-1688.	772.	11.8	6.190		
.12	0.	0.081	0.	0.9181	0.2168	0.9181	5.95	2.111	0.961	0.993	2.109	1.925	0.991	-1719.	739.	11.6	6.051		
.13	0.	0.108	0.	0.8908	0.1705	0.8908	5.96	2.112	0.948	1.008	2.110	1.884	0.968	-1751.	707.	11.4	5.917		
.14	0.	0.135	0.	0.8635	0.1242	0.8635	5.97	2.113	0.935	1.023	2.111	1.843	0.945	-1784.	676.	11.2	5.788		
.15	0.	0.162	0.	0.8362	0.0779	0.8362	5.98	2.114	0.922	1.038	2.112	1.802	0.922	-1818.	646.	11.0	5.664		
.16	0.	0.189	0.	0.8089	0.0316	0.8089	5.99	2.115	0.909	1.053	2.113	1.761	0.899	-1853.	617.	10.8	5.545		
.17	0.	0.216	0.	0.7816	0.0000	0.7816	6.00	2.116	0.896	1.068	2.114	1.720	0.876	-1889.	589.	10.6	5.431		
.18	0.	0.243	0.	0.7543	0.0000	0.7543	6.01	2.117	0.883	1.083	2.115	1.679	0.853	-1926.	562.	10.4	5.322		
.19	0.	0.270	0.	0.7270	0.0000	0.7270	6.02	2.118	0.870	1.098	2.116	1.638	0.830	-1964.	536.	10.2	5.218		
.20	0.	0.297	0.	0.7000	0.0000	0.7000	6.03	2.119	0.857	1.113	2.117	1.597	0.807	-2003.	511.	10.0	5.119		
.21	0.	0.324	0.	0.6733	0.0000	0.6733	6.04	2.120	0.844	1.128	2.118	1.556	0.784	-2043.	487.	9.8	5.025		
.22	0.	0.351	0.	0.6470	0.0000	0.6470	6.05	2.121	0.831	1.143	2.119	1.515	0.761	-2084.	464.	9.6	4.936		
.23	0.	0.378	0.	0.6213	0.0000	0.6213	6.06	2.122	0.818	1.158	2.120	1.474	0.738	-2126.	442.	9.4	4.851		
.24	0.	0.405	0.	0.5963	0.0000	0.5963	6.07	2.123	0.805	1.173	2.121	1.433	0.715	-2169.	421.	9.2	4.770		
.25	0.	0.432	0.	0.5720	0.0000	0.5720	6.08	2.124	0.792	1.188	2.122	1.392	0.692	-2213.	401.	9.0	4.693		
.26	0.	0.459	0.	0.5483	0.0000	0.5483	6.09	2.125	0.779	1.203	2.123	1.351	0.669	-2258.	382.	8.8	4.620		
.27	0.	0.486	0.	0.5253	0.0000	0.5253	6.10	2.126	0.766	1.218	2.124	1.310	0.646	-2304.	364.	8.6	4.551		
.28	0.	0.513	0.	0.5030	0.0000	0.5030	6.11	2.127	0.753	1.233	2.125	1.269	0.623	-2351.	347.	8.4	4.486		
.29	0.	0.540	0.	0.4813	0.0000	0.4813	6.12	2.128	0.740	1.248	2.126	1.228	0.600	-2399.	331.	8.2	4.425		
.30	0.	0.567	0.	0.4603	0.0000	0.4603	6.13	2.129	0.727	1.263	2.127	1.187	0.577	-2448.	316.	8.0	4.368		
.31	0.	0.594	0.	0.4400	0.0000	0.4400	6.14	2.130	0.714	1.278	2.128	1.146	0.554	-2498.	302.	7.8	4.314		
.32	0.	0.621	0.	0.4203	0.0000	0.4203	6.15	2.131	0.701	1.293	2.129	1.105	0.531	-2549.	289.	7.6	4.263		
.33	0.	0.648	0.	0.4013	0.0000	0.4013	6.16	2.132	0.688	1.308	2.130	1.064	0.508	-2601.	277.	7.4	4.214		
.34	0.	0.675	0.	0.3830	0.0000	0.3830	6.17	2.133	0.675	1.323	2.131	1.023	0.485	-2654.	266.	7.2	4.167		
.35	0.	0.702	0.	0.3653	0.0000	0.3653	6.18	2.134	0.662	1.338	2.132	0.982	0.462	-2708.	256.	7.0	4.122		
.36	0.	0.729	0.	0.3483	0.0000	0.3483	6.19	2.135	0.649	1.353	2.133	0.941	0.439	-2763.	247.	6.8	4.079		
.37	0.	0.756	0.	0.3320	0.0000	0.3320	6.20	2.136	0.636	1.368	2.134	0.900	0.416	-2819.	239.	6.6	4.037		
.38	0.	0.783	0.	0.3163	0.0000	0.3163	6.21	2.137	0.623	1.383	2.135	0.859	0.393	-2876.	232.	6.4	3.996		
.39	0.	0.810	0.	0.3013	0.0000	0.3013	6.22	2.138	0.610	1.398	2.136	0.818	0.370	-2934.	226.	6.2	3.956		
.40	0.	0.837	0.	0.2870	0.0000	0.2870	6.23	2.139	0.597	1.413	2.137	0.777	0.347	-2993.	221.	6.0	3.917		
.41	0.	0.864	0.	0.2733	0.0000	0.2733	6.24	2.140	0.584	1.428	2.138	0.736	0.324	-3053.	217.	5.8	3.879		
.42	0.	0.891	0.	0.2603	0.0000	0.2603	6.25	2.141	0.571	1.443	2.139	0.695	0.301	-3114.	214.	5.6	3.842		
.43	0.	0.918	0.	0.2480	0.0000	0.2480	6.26	2.142	0.558	1.458	2.140	0.654	0.278	-3176.	212.	5.4	3.806		
.44	0.	0.945	0.	0.2363	0.0000	0.2363	6.27	2.143	0.545	1.473	2.141	0.613	0.255	-3239.	211.	5.2	3.771		
.45	0.	0.972	0.	0.2253	0.0000	0.2253	6.28	2.144	0.532	1.488	2.142	0.572	0.232	-3303.	211.	5.0	3.737		
.46	0.	0.999	0.	0.2150	0.0000	0.2150	6.29	2.145	0.519	1.503	2.143	0.531	0.209	-3368.	212.	4.8	3.704		
.47	0.	1.000	0.	0.2053	0.0000	0.2053	6.30	2.146	0.506	1.518	2.144	0.490	0.186	-3434.	214.	4.6	3.672		
.48	0.	1.000	0.	0.1963	0.0000	0.1963	6.31	2.147	0.493	1.533	2.145	0.449	0.163	-3501.	217.	4.4	3.641		
.49	0.	1.000	0.	0.1878	0.0000	0.1878	6.32	2.148	0.480	1.548	2.146	0.408	0.140	-3569.	221.	4.2	3.611		
.50	0.	1.000	0.	0.1798	0.0000	0.1798	6.33	2.149	0.467	1.563	2.147	0.367	0.117	-3638.	226.	4.0	3.582		
.51	0.	1.000	0.	0.1723	0.0000	0.1723	6.34	2.150	0.454	1.578	2.148	0.326	0.094	-3708.	231.	3.8	3.554		
.52	0.	1.000	0.	0.1653	0.0000	0.1653	6.35	2.151	0.441	1.593	2.149	0.285	0.071	-3779.	237.	3.6	3.527		
.53	0.	1.000	0.	0.1588	0.0000	0.1588	6.36	2.152	0.428	1.608	2.150	0.244	0.048	-3851.	244.	3.4	3.501		
.54	0.	1.000	0.	0.1528	0.0000	0.1528	6.37	2.153	0.415	1.623	2.151	0.203	0.025	-3924.	251.	3.2	3.476		
.55	0.	1.000	0.	0.1473	0.0000	0.1473	6.38	2.154	0.402	1.638	2.152	0.162	0.002	-3998.	259.	3.0	3.452		
.56	0.	1.000	0.	0.1423	0.0000	0.1423	6.39	2.155	0.389	1.653	2.153	0.121	0.000	-4073.	268.	2.8	3.429		
.57	0.	1.000	0.	0.1378	0.0000	0.1378	6.40	2.156	0.376	1.668	2.154	0.080	0.000	-4149.	278.	2.6	3.407		
.58	0.	1.000	0.	0.1338	0.0000	0.1338	6.41	2.157	0.363	1.683	2.155	0.039	0.000	-4226.	289.	2.4	3.386		
.59	0.	1.000	0.	0.1303	0.0000	0.1303	6.42	2.158	0.350	1.698	2.156	0.000	0.000	-4304.	301.	2.2	3.366		
.60	0.	1.000	0.	0.1273	0.0000	0.1273	6.43	2.159	0.337	1.713	2.157	0.000	0.000	-4383.	314.	2.0	3.347		
.61	0.	1.000	0.	0.1248	0.0000	0.1248	6.44	2.160	0.324	1.728	2.158	0.000	0.000	-4463.	328.	1.8	3.329		
.62	0.	1.000	0.	0.1228	0.0000	0.1228	6.45	2.161	0.311	1.743	2.159	0.000	0.000	-4544.	343.	1.6	3.312		
.63	0.	1.000	0.	0.1213	0.0000	0.1213	6.46	2.162	0.298	1.758	2.160	0.000	0.000	-4626.	359.	1.4	3.296		
.64	0.	1.000	0.	0.1203	0.0000	0.1203	6.47	2.163	0.285	1.773	2.161	0.000	0.000	-4709.	376.	1.2	3.281		
.65	0.	1.000	0.	0.1198	0.0000	0.1198	6.48	2.164	0.272	1.788	2.162	0.000	0.000	-4793.	394.	1.0	3.267		
.66	0.	1.000	0.	0.1198	0.0000	0.1198	6.49	2.165	0.259	1.803	2.163	0.000	0.000	-4878.	413.	0.8	3.254		
.67	0.	1.000	0.	0.1203	0.0000	0.1203	6.50	2.166	0.246	1.818	2.164	0.000	0.000	-4964.	433.	0.6	3.242		
.68	0.	1.000	0.	0.1213	0.0000	0.1213	6.51	2.167	0.233	1.833	2.165								

LIQUID MOLE FRACTION		VAPOR MOLE FRACTION		PRESSURE			EQUIL CONST			RELATIVE VOL			ENTHALPY BTU/LB MOLE		HEAT CAPACITY BTU/LB MOLE-R	
N2	AR/AR-O2	N2	AR	O2	ATM	N2	AR	O2	N2/AR	N2/O2	AR/O2	LTO	VAP	LTO	VAP	
0.	0.	0.	0.	1.0002	5.00	2.479	1.330	1.000	1.884	2.479	1.330	-1339.	1294.	13.6	8.524	
0.1	0.	0.1261	0.8741		5.01	2.389	1.261	0.971	1.878	2.430	1.299	-1362.	1291.	13.5	8.527	
0.2	0.	0.2409	0.7594		5.02	2.278	1.204	0.949	1.891	2.400	1.269	-1385.	1284.	13.4	8.530	
0.3	0.	0.3470	0.6533		5.02	2.143	1.157	0.933	1.905	2.361	1.240	-1408.	1279.	13.3	8.532	
0.4	0.	0.4460	0.5535		5.02	2.005	1.087	0.918	1.919	2.323	1.211	-1431.	1268.	13.2	8.534	
0.5	0.	0.5421	0.4579		5.02	1.858	1.007	0.904	1.933	2.286	1.183	-1454.	1259.	13.1	8.535	
0.6	0.	0.6344	0.3656		5.02	1.708	0.918	0.891	1.947	2.250	1.156	-1477.	1251.	13.0	8.536	
0.7	0.	0.7231	0.2769		5.02	1.558	0.828	0.878	1.961	2.214	1.129	-1500.	1244.	12.9	8.537	
0.8	0.	0.8096	0.1904		5.02	1.408	0.738	0.865	1.975	2.178	1.103	-1523.	1238.	12.8	8.538	
0.9	0.	0.8939	0.1061		5.02	1.258	0.648	0.852	1.989	2.142	1.076	-1546.	1233.	12.7	8.539	
1.0	1.0	1.0000	0.0000		5.02	1.108	0.558	0.839	2.004	2.106	1.050	-1569.	1228.	12.6	8.540	
0.0	0.1	0.0393	0.9607		5.03	2.373	1.278	0.983	1.887	2.450	1.324	-1319.	1295.	13.7	8.588	
0.0	0.2	0.0786	0.9214		5.03	2.275	1.210	0.960	1.876	2.420	1.294	-1342.	1293.	13.6	8.586	
0.0	0.3	0.1179	0.8821		5.03	2.178	1.142	0.937	1.883	2.382	1.265	-1365.	1291.	13.5	8.584	
0.0	0.4	0.1572	0.8428		5.03	2.081	1.074	0.914	1.897	2.345	1.237	-1388.	1289.	13.4	8.582	
0.0	0.5	0.1965	0.8035		5.03	1.984	1.006	0.891	1.910	2.308	1.209	-1411.	1287.	13.3	8.580	
0.0	0.6	0.2358	0.7642		5.03	1.887	0.938	0.868	1.924	2.271	1.182	-1434.	1285.	13.2	8.578	
0.0	0.7	0.2751	0.7249		5.03	1.790	0.876	0.845	1.937	2.234	1.155	-1457.	1283.	13.1	8.576	
0.0	0.8	0.3144	0.6856		5.03	1.693	0.814	0.822	1.951	2.197	1.128	-1480.	1281.	13.0	8.574	
0.0	0.9	0.3537	0.6463		5.03	1.596	0.752	0.800	1.964	2.160	1.101	-1503.	1279.	12.9	8.572	
0.0	1.0	0.3930	0.6070		5.03	1.499	0.690	0.777	1.978	2.123	1.074	-1526.	1277.	12.8	8.570	
0.1	0.0	0.2037	0.0902	0.8974	5.04	2.107	1.147	0.977	1.838	2.421	1.307	-1291.	1296.	14.0	8.791	
0.1	0.1	0.1079	0.1919	0.8110	5.04	2.010	1.080	0.954	1.848	2.384	1.278	-1314.	1294.	13.9	8.789	
0.1	0.2	0.1930	0.2704	0.7201	5.04	1.913	1.003	0.931	1.858	2.347	1.249	-1337.	1292.	13.8	8.787	
0.1	0.3	0.2681	0.3400	0.6253	5.04	1.816	0.926	0.908	1.868	2.310	1.220	-1360.	1290.	13.7	8.785	
0.1	0.4	0.3332	0.4000	0.5265	5.04	1.719	0.849	0.885	1.878	2.273	1.191	-1383.	1288.	13.6	8.783	
0.1	0.5	0.3883	0.4500	0.4237	5.04	1.622	0.772	0.862	1.888	2.236	1.162	-1406.	1286.	13.5	8.781	
0.1	0.6	0.4334	0.5000	0.3169	5.04	1.525	0.695	0.839	1.898	2.199	1.133	-1429.	1284.	13.4	8.779	
0.1	0.7	0.4685	0.5500	0.2071	5.04	1.428	0.618	0.816	1.908	2.162	1.104	-1452.	1282.	13.3	8.777	
0.1	0.8	0.4936	0.6000	0.0943	5.04	1.331	0.541	0.793	1.918	2.125	1.075	-1475.	1280.	13.2	8.775	
0.1	0.9	0.5087	0.6500	0.0000	5.04	1.234	0.464	0.770	1.928	2.088	1.046	-1498.	1278.	13.1	8.773	
0.1	1.0	0.5138	0.7000	0.0000	5.04	1.137	0.387	0.747	1.938	2.051	1.017	-1521.	1276.	13.0	8.771	
0.2	0.0	0.3677	0.6323		5.05	1.818	0.913	0.911	1.860	2.318	1.283	-1447.	1297.	13.2	7.467	
0.2	0.1	0.3287	0.6709	0.6324	5.05	1.721	0.836	0.888	1.870	2.281	1.254	-1470.	1295.	13.1	7.465	
0.2	0.2	0.2897	0.7095	0.4657	5.05	1.624	0.759	0.865	1.880	2.244	1.225	-1493.	1293.	13.0	7.463	
0.2	0.3	0.2507	0.7481	0.3000	5.05	1.527	0.682	0.842	1.890	2.207	1.196	-1516.	1291.	12.9	7.461	
0.2	0.4	0.2117	0.7867	0.1343	5.05	1.430	0.605	0.819	1.900	2.170	1.167	-1539.	1289.	12.8	7.459	
0.2	0.5	0.1727	0.8253	0.0000	5.05	1.333	0.528	0.796	1.910	2.133	1.138	-1562.	1287.	12.7	7.457	
0.2	0.6	0.1337	0.8639	0.0000	5.05	1.236	0.451	0.773	1.920	2.096	1.109	-1585.	1285.	12.6	7.455	
0.2	0.7	0.0947	0.9025	0.0000	5.05	1.139	0.374	0.750	1.930	2.059	1.080	-1608.	1283.	12.5	7.453	
0.2	0.8	0.0557	0.9411	0.0000	5.05	1.042	0.297	0.727	1.940	2.022	1.051	-1631.	1281.	12.4	7.451	
0.2	0.9	0.0167	0.9797	0.0000	5.05	0.945	0.220	0.704	1.950	1.985	1.022	-1654.	1279.	12.3	7.449	
0.2	1.0	0.0000	1.0000	0.0000	5.05	0.848	0.143	0.681	1.960	1.948	0.993	-1677.	1277.	12.2	7.447	
0.3	0.0	0.4624	0.5376		5.06	1.482	0.848	0.879	1.832	2.325	1.308	-1422.	1298.	13.2	8.111	
0.3	0.1	0.4234	0.5762		5.06	1.385	0.771	0.856	1.842	2.288	1.279	-1445.	1296.	13.1	8.109	
0.3	0.2	0.3844	0.6148		5.06	1.288	0.694	0.833	1.852	2.251	1.250	-1468.	1294.	13.0	8.107	
0.3	0.3	0.3454	0.6534		5.06	1.191	0.617	0.810	1.862	2.214	1.221	-1491.	1292.	12.9	8.105	
0.3	0.4	0.3064	0.6920		5.06	1.094	0.540	0.787	1.872	2.177	1.192	-1514.	1290.	12.8	8.103	
0.3	0.5	0.2674	0.7306		5.06	1.000	0.463	0.764	1.882	2.140	1.163	-1537.	1288.	12.7	8.101	
0.3	0.6	0.2284	0.7692		5.06	0.907	0.386	0.741	1.892	2.103	1.134	-1560.	1286.	12.6	8.099	
0.3	0.7	0.1894	0.8078		5.06	0.814	0.309	0.718	1.902	2.066	1.105	-1583.	1284.	12.5	8.097	
0.3	0.8	0.1504	0.8464		5.06	0.721	0.232	0.695	1.912	2.029	1.076	-1606.	1282.	12.4	8.095	
0.3	0.9	0.1114	0.8850		5.06	0.628	0.155	0.672	1.922	1.992	1.047	-1629.	1280.	12.3	8.093	
0.3	1.0	0.0724	0.9236		5.06	0.535	0.078	0.649	1.932	1.955	1.018	-1652.	1278.	12.2	8.091	
0.4	0.0	0.5669	0.4331		5.07	1.082	0.848	0.879	1.804	2.332	1.283	-1407.	1300.	13.2	8.255	
0.4	0.1	0.5279	0.4717		5.07	1.000	0.771	0.856	1.814	2.295	1.254	-1430.	1298.	13.1	8.253	
0.4	0.2	0.4889	0.5103		5.07	0.918	0.694	0.833	1.824	2.258	1.225	-1453.	1296.	13.0	8.251	
0.4	0.3	0.4499	0.5489		5.07	0.836	0.617	0.810	1.834	2.221	1.196	-1476.	1294.	12.9	8.249	
0.4	0.4	0.4109	0.5875		5.07	0.754	0.540	0.787	1.844	2.184	1.167	-1499.	1292.	12.8	8.247	
0.4	0.5	0.3719	0.6261		5.07	0.672	0.463	0.764	1.854	2.147	1.138	-1522.	1290.	12.7	8.245	
0.4	0.6	0.3329	0.6647		5.07	0.590	0.386	0.741	1.864	2.110	1.109	-1545.	1288.	12.6	8.243	
0.4	0.7	0.2939	0.7033		5.07	0.508	0.309	0.718	1.874	2.073	1.080	-1568.	1286.	12.5	8.241	
0.4	0.8	0.2549	0.7419		5.07	0.426	0.232	0.695	1.884	2.036	1.051	-1591.	1284.	12.4	8.239	
0.4	0.9	0.2159	0.7805		5.07	0.344	0.155	0.672	1.894	2.000	1.022	-1614.	1282.	12.3	8.237	
0.4	1.0	0.1769	0.8191		5.07	0.262	0.078	0.649	1.904	1.963	0.993	-1637.	1280.	12.2	8.235	
0.5	0.0	0.6614	0.3386		5.08	1.082	0.848	0.879	1.776	2.311	1.273	-1402.	1301.	13.2	8.399	
0.5	0.1	0.6224	0.3772		5.08	1.000	0.771	0.856	1.786	2.274	1.244	-1425.	1299.	13.1	8.397	
0.5	0.2	0.5834	0.4158		5.08	0.918	0.694	0.833	1.796	2.237	1.215	-1448.	1297.	13.0	8.395	
0.5	0.3	0.5444	0.4544		5.08	0.836	0.617	0.810	1.806	2.200	1.186	-1471.	1295.	12.9	8.393	
0.5	0.4	0.5054	0.4930		5.08	0.754	0.540									

LIQUID MOLE FRACTION	VAPOR MOLE FRACTION		PRESSURE	EQUIL CONST			RELATIVE VOL			ENTHALPY		HEAT CAPACITY	
	N2	AR/O2		N2	AR	O2	N2/AR	N2/O2	AR/O2	LIG	VAP	LIG	VAP
0.	0.	0.	8.97	2.341	1.24	1.000	1.790	2.340	1.307	-1271.	1267.	13.8	8.787
0.1	0.	0.1244	8.97	2.242	1.24	0.973	1.802	2.303	1.278	-1294.	1214.	13.7	7.982
0.2	0.	0.2382	8.97	2.160	1.24	0.952	1.814	2.267	1.250	-1317.	1164.	13.6	7.193
0.3	0.	0.3440	8.97	2.093	1.24	0.938	1.826	2.232	1.222	-1341.	1119.	13.5	6.423
0.4	0.	0.4437	8.97	2.039	1.24	0.929	1.838	2.197	1.194	-1364.	1076.	13.4	5.671
0.5	0.	0.5391	8.97	1.995	1.24	0.922	1.850	2.163	1.166	-1387.	1035.	13.4	4.928
0.6	0.	0.6318	8.97	1.961	1.24	0.917	1.862	2.130	1.144	-1411.	996.	13.4	4.193
0.7	0.	0.7231	8.97	1.937	1.24	0.913	1.874	2.097	1.119	-1434.	958.	13.4	3.463
0.8	0.	0.8141	8.97	1.921	1.24	0.910	1.887	2.067	1.094	-1458.	920.	13.2	2.734
0.9	0.	0.9060	8.97	1.913	1.24	0.907	1.900	2.032	1.070	-1481.	883.	13.1	2.004
1.0	1.0	1.0000	8.97	1.913	1.24	0.905	1.913	2.002	1.047	-1504.	845.	13.0	1.274
0.05	0.1	0.0562	7.24	2.248	1.061	0.968	1.784	2.322	1.262	-1275.	1262.	13.9	8.871
0.05	0.2	0.0540	7.47	2.160	1.203	0.949	1.795	2.287	1.274	-1273.	1211.	13.8	8.070
0.05	0.3	0.0509	7.68	2.087	1.159	0.927	1.807	2.252	1.246	-1296.	1169.	13.8	7.269
0.05	0.4	0.0494	7.87	2.026	1.114	0.914	1.818	2.218	1.220	-1319.	1121.	13.8	6.468
0.05	0.5	0.0484	8.04	1.977	1.080	0.905	1.830	2.184	1.193	-1342.	1076.	13.8	5.667
0.05	0.6	0.0477	8.21	1.936	1.052	0.901	1.842	2.151	1.166	-1364.	1035.	13.7	4.866
0.05	0.7	0.0471	8.38	1.904	1.028	0.900	1.854	2.119	1.143	-1387.	996.	13.7	4.065
0.05	0.8	0.0467	8.51	1.880	1.009	0.900	1.866	2.087	1.118	-1410.	958.	13.4	3.264
0.05	0.9	0.0465	8.58	1.861	0.989	0.910	1.878	2.056	1.095	-1433.	920.	13.3	2.463
0.05	1.0	0.0465	8.64	1.846	0.978	0.910	1.890	2.026	1.071	-1456.	883.	13.3	1.662
0.10	0.1	0.0114	8.08	2.114	1.141	0.887	1.753	2.289	1.268	-1190.	1248.	14.2	9.071
0.10	0.2	0.0107	8.26	1.990	1.099	0.870	1.775	2.237	1.246	-1211.	1203.	14.2	8.270
0.10	0.3	0.0102	8.44	1.897	1.062	0.860	1.786	2.196	1.233	-1233.	1163.	14.1	7.469
0.10	0.4	0.0100	8.58	1.829	1.031	0.852	1.798	2.175	1.211	-1255.	1124.	14.1	6.668
0.10	0.5	0.0098	8.68	1.781	1.006	0.844	1.807	2.144	1.187	-1274.	1084.	14.0	5.867
0.10	0.6	0.0096	8.75	1.748	0.982	0.844	1.818	2.114	1.163	-1296.	1045.	13.9	5.066
0.10	0.7	0.0095	8.80	1.723	0.963	0.845	1.828	2.085	1.140	-1317.	1006.	13.9	4.265
0.10	0.8	0.0094	8.83	1.703	0.945	0.846	1.839	2.056	1.118	-1337.	967.	13.8	3.464
0.10	0.9	0.0094	8.85	1.687	0.933	0.846	1.849	2.026	1.096	-1358.	928.	13.7	2.663
0.10	1.0	0.0094	8.86	1.673	0.922	0.847	1.860	2.000	1.074	-1378.	889.	13.7	1.862
0.15	0.1	0.0024	8.12	1.774	1.020	0.867	1.730	2.280	1.279	-1190.	1229.	13.6	7.666
0.15	0.2	0.0024	8.28	1.733	0.999	0.798	1.748	2.172	1.244	-1210.	1189.	13.6	6.865
0.15	0.3	0.0023	8.44	1.687	0.986	0.791	1.767	2.145	1.221	-1231.	1149.	13.6	6.064
0.15	0.4	0.0023	8.58	1.667	0.943	0.787	1.777	2.119	1.199	-1253.	1109.	13.5	5.263
0.15	0.5	0.0023	8.70	1.641	0.924	0.784	1.777	2.092	1.178	-1274.	1070.	13.5	4.462
0.15	0.6	0.0023	8.80	1.619	0.907	0.784	1.780	2.066	1.157	-1296.	1030.	13.4	3.661
0.15	0.7	0.0023	8.83	1.602	0.893	0.785	1.781	2.041	1.137	-1317.	991.	13.4	2.860
0.15	0.8	0.0023	8.85	1.589	0.881	0.785	1.782	2.016	1.117	-1337.	952.	13.3	2.059
0.15	0.9	0.0023	8.85	1.578	0.863	0.785	1.781	1.991	1.096	-1358.	913.	13.2	1.258
0.15	1.0	0.0023	8.86	1.572	0.847	0.785	1.803	1.967	1.079	-1378.	874.	13.2	0.457
0.20	0.1	0.0004	8.12	1.774	1.020	0.867	1.730	2.280	1.279	-1190.	1229.	13.6	7.666
0.20	0.2	0.0004	8.28	1.733	0.999	0.798	1.748	2.172	1.244	-1210.	1189.	13.6	6.865
0.20	0.3	0.0004	8.44	1.687	0.986	0.791	1.767	2.145	1.221	-1231.	1149.	13.6	6.064
0.20	0.4	0.0004	8.58	1.667	0.943	0.787	1.777	2.119	1.199	-1253.	1109.	13.5	5.263
0.20	0.5	0.0004	8.70	1.641	0.924	0.784	1.777	2.092	1.178	-1274.	1070.	13.5	4.462
0.20	0.6	0.0004	8.80	1.619	0.907	0.784	1.780	2.066	1.157	-1296.	1030.	13.4	3.661
0.20	0.7	0.0004	8.83	1.602	0.893	0.785	1.781	2.041	1.137	-1317.	991.	13.4	2.860
0.20	0.8	0.0004	8.85	1.589	0.881	0.785	1.782	2.016	1.117	-1337.	952.	13.3	2.059
0.20	0.9	0.0004	8.85	1.578	0.863	0.785	1.781	1.991	1.096	-1358.	913.	13.2	1.258
0.20	1.0	0.0004	8.86	1.572	0.847	0.785	1.803	1.967	1.079	-1378.	874.	13.2	0.457
0.25	0.1	0.0004	8.12	1.774	1.020	0.867	1.730	2.280	1.279	-1190.	1229.	13.6	7.666
0.25	0.2	0.0004	8.28	1.733	0.999	0.798	1.748	2.172	1.244	-1210.	1189.	13.6	6.865
0.25	0.3	0.0004	8.44	1.687	0.986	0.791	1.767	2.145	1.221	-1231.	1149.	13.6	6.064
0.25	0.4	0.0004	8.58	1.667	0.943	0.787	1.777	2.119	1.199	-1253.	1109.	13.5	5.263
0.25	0.5	0.0004	8.70	1.641	0.924	0.784	1.777	2.092	1.178	-1274.	1070.	13.5	4.462
0.25	0.6	0.0004	8.80	1.619	0.907	0.784	1.780	2.066	1.157	-1296.	1030.	13.4	3.661
0.25	0.7	0.0004	8.83	1.602	0.893	0.785	1.781	2.041	1.137	-1317.	991.	13.4	2.860
0.25	0.8	0.0004	8.85	1.589	0.881	0.785	1.782	2.016	1.117	-1337.	952.	13.3	2.059
0.25	0.9	0.0004	8.85	1.578	0.863	0.785	1.781	1.991	1.096	-1358.	913.	13.2	1.258
0.25	1.0	0.0004	8.86	1.572	0.847	0.785	1.803	1.967	1.079	-1378.	874.	13.2	0.457
0.30	0.1	0.0004	8.12	1.774	1.020	0.867	1.730	2.280	1.279	-1190.	1229.	13.6	7.666
0.30	0.2	0.0004	8.28	1.733	0.999	0.798	1.748	2.172	1.244	-1210.	1189.	13.6	6.865
0.30	0.3	0.0004	8.44	1.687	0.986	0.791	1.767	2.145	1.221	-1231.	1149.	13.6	6.064
0.30	0.4	0.0004	8.58	1.667	0.943	0.787	1.777	2.119	1.199	-1253.	1109.	13.5	5.263
0.30	0.5	0.0004	8.70	1.641	0.924	0.784	1.777	2.092	1.178	-1274.	1070.	13.5	4.462
0.30	0.6	0.0004	8.80	1.619	0.907	0.784	1.780	2.066	1.157	-1296.	1030.	13.4	3.661
0.30	0.7	0.0004	8.83	1.602	0.893	0.785	1.781	2.041	1.137	-1317.	991.	13.4	2.860
0.30	0.8	0.0004	8.85	1.589	0.881	0.785	1.782	2.016	1.117	-1337.	952.	13.3	2.059
0.30	0.9	0.0004	8.85	1.578	0.863	0.785	1.781	1.991	1.096	-1358.	913.	13.2	1.258
0.30	1.0	0.0004	8.86	1.572	0.847	0.785	1.803	1.967	1.079	-1378.	874.	13.2	0.457
0.35	0.1	0.0004	8.12	1.774	1.020	0.867	1.730	2.280	1.279	-1190.	1229.	13.6	7.666
0.35	0.2	0.0004	8.28	1.733	0.999	0.798	1.748	2.172	1.244	-1210.	1189.	13.6	6.865
0.35	0.3	0.0004	8.44	1.687	0.986	0.791	1.767	2.145	1.221	-1231.	1149.	13.6	6.064
0.35	0.4	0.0004	8.58	1.667	0.943	0.787	1.777	2.119	1.199	-1253.	1109.	13.5	5.263
0.35	0.5	0.0004	8.70	1.641	0.924	0.784	1.777	2.092	1.178	-1274.	1070.	13.5	4.462
0.35	0.6	0.0004	8.80	1.619	0.907	0.784	1.780	2.066	1.157	-1296.	1030.	13.4	3.661
0.35	0.7	0.0004	8.83	1.602	0.893	0.785	1.781	2.041	1.137	-1317.	991.	13.4	2.860
0.35	0.8	0.0004											

LIQUID MOLE FRACTION			VAPOR MOLE FRACTION			PRESSURE ATM	EQUIL CONST			RELATIVE VOL			ENTHALPY BTU/LB MOLE		HEAT CAPACITY BTU/LB MOLE-R	
N2	AR/AR+O2	O2	N2	AR	O2		N2	AR	O2	N2/AR	N2/O2	AR/O2	LIG	VAP	LIG	VAP
0.	0.	1.0001	0.	0.	1.0001	8.70	2.215	1.289	1.000	1.793	2.214	1.289	-1201.	1277.	14.0	9.480
0.	0.1	0.9774	0.	0.	0.9774	8.97	2.093	1.227	0.979	1.733	2.101	1.294	-1225.	1222.	14.0	8.898
0.	0.2	0.9447	0.	0.	0.9447	9.23	1.972	1.177	0.956	1.744	2.140	1.232	-1248.	1172.	13.9	8.720
0.	0.3	0.9120	0.	0.	0.9120	9.49	1.851	1.130	0.942	1.794	2.115	1.205	-1272.	1120.	13.9	8.591
0.	0.4	0.8793	0.	0.	0.8793	9.75	1.730	1.083	0.933	1.765	2.083	1.181	-1296.	1068.	13.8	8.307
0.	0.5	0.8466	0.	0.	0.8466	10.01	1.609	1.036	0.927	1.775	2.052	1.156	-1320.	1016.	13.8	8.224
0.	0.6	0.8139	0.	0.	0.8139	10.27	1.485	0.989	0.920	1.787	2.021	1.132	-1344.	964.	13.7	8.099
0.	0.7	0.7812	0.	0.	0.7812	10.53	1.361	0.942	0.913	1.800	1.991	1.108	-1368.	912.	13.6	7.890
0.	0.8	0.7485	0.	0.	0.7485	10.79	1.237	0.895	0.907	1.812	1.961	1.084	-1392.	860.	13.6	7.714
0.	0.9	0.7158	0.	0.	0.7158	11.05	1.113	0.848	0.901	1.824	1.931	1.060	-1416.	808.	13.6	7.527
0.	1.0	0.6831	0.	0.	0.6831	11.31	0.989	0.801	0.895	1.836	1.901	1.036	-1440.	756.	13.5	7.328
0.025	0.	0.9750	0.	0.	0.9750	8.86	2.089	1.190	0.949	1.727	2.109	1.294	-1203.	1220.	14.1	9.175
0.050	0.	0.9500	0.	0.	0.9500	9.12	1.968	1.143	0.932	1.737	2.133	1.228	-1227.	1172.	14.0	8.830
0.075	0.	0.9250	0.	0.	0.9250	9.38	1.847	1.096	0.915	1.747	2.157	1.263	-1251.	1124.	14.0	8.671
0.100	0.	0.9000	0.	0.	0.9000	9.64	1.726	1.049	0.898	1.757	2.181	1.197	-1275.	1076.	13.9	8.512
0.125	0.	0.8750	0.	0.	0.8750	9.90	1.605	1.002	0.881	1.767	2.205	1.131	-1299.	1028.	13.9	8.353
0.150	0.	0.8500	0.	0.	0.8500	10.16	1.484	0.955	0.864	1.777	2.229	1.065	-1323.	980.	13.8	8.244
0.175	0.	0.8250	0.	0.	0.8250	10.42	1.363	0.908	0.847	1.787	2.253	1.000	-1347.	932.	13.7	8.095
0.200	0.	0.8000	0.	0.	0.8000	10.68	1.242	0.861	0.830	1.797	2.277	0.935	-1371.	884.	13.7	7.946
0.225	0.	0.7750	0.	0.	0.7750	10.94	1.121	0.814	0.813	1.807	2.301	0.870	-1395.	836.	13.6	7.797
0.250	0.	0.7500	0.	0.	0.7500	11.20	1.000	0.767	0.796	1.817	2.325	0.805	-1419.	788.	13.6	7.648
0.275	0.	0.7250	0.	0.	0.7250	11.46	0.879	0.720	0.779	1.827	2.349	0.740	-1443.	740.	13.5	7.499
0.300	0.	0.7000	0.	0.	0.7000	11.72	0.758	0.673	0.762	1.837	2.373	0.675	-1467.	692.	13.5	7.350
0.325	0.	0.6750	0.	0.	0.6750	11.98	0.637	0.626	0.745	1.847	2.397	0.610	-1491.	644.	13.4	7.201
0.350	0.	0.6500	0.	0.	0.6500	12.24	0.516	0.579	0.728	1.857	2.421	0.545	-1515.	596.	13.4	7.052
0.375	0.	0.6250	0.	0.	0.6250	12.50	0.395	0.532	0.711	1.867	2.445	0.480	-1539.	548.	13.3	6.903
0.400	0.	0.6000	0.	0.	0.6000	12.76	0.274	0.485	0.694	1.877	2.469	0.415	-1563.	500.	13.3	6.754
0.425	0.	0.5750	0.	0.	0.5750	13.02	0.153	0.438	0.677	1.887	2.493	0.350	-1587.	452.	13.2	6.605
0.450	0.	0.5500	0.	0.	0.5500	13.28	0.032	0.391	0.660	1.897	2.517	0.285	-1611.	404.	13.2	6.456
0.475	0.	0.5250	0.	0.	0.5250	13.54	0.000	0.344	0.643	1.907	2.541	0.220	-1635.	356.	13.1	6.307
0.500	0.	0.5000	0.	0.	0.5000	13.80	0.000	0.297	0.626	1.917	2.565	0.155	-1659.	308.	13.1	6.158
0.525	0.	0.4750	0.	0.	0.4750	14.06	0.000	0.250	0.609	1.927	2.589	0.090	-1683.	260.	13.0	6.009
0.550	0.	0.4500	0.	0.	0.4500	14.32	0.000	0.203	0.592	1.937	2.613	0.025	-1707.	212.	13.0	5.860
0.575	0.	0.4250	0.	0.	0.4250	14.58	0.000	0.156	0.575	1.947	2.637	0.000	-1731.	164.	12.9	5.711
0.600	0.	0.4000	0.	0.	0.4000	14.84	0.000	0.109	0.558	1.957	2.661	0.000	-1755.	116.	12.9	5.562
0.625	0.	0.3750	0.	0.	0.3750	15.10	0.000	0.062	0.541	1.967	2.685	0.000	-1779.	68.	12.8	5.413
0.650	0.	0.3500	0.	0.	0.3500	15.36	0.000	0.015	0.524	1.977	2.709	0.000	-1803.	20.	12.8	5.264
0.675	0.	0.3250	0.	0.	0.3250	15.62	0.000	0.000	0.507	1.987	2.733	0.000	-1827.	0.	12.7	5.115
0.700	0.	0.3000	0.	0.	0.3000	15.88	0.000	0.000	0.490	1.997	2.757	0.000	-1851.	0.	12.7	4.966
0.725	0.	0.2750	0.	0.	0.2750	16.14	0.000	0.000	0.473	2.007	2.781	0.000	-1875.	0.	12.6	4.817
0.750	0.	0.2500	0.	0.	0.2500	16.40	0.000	0.000	0.456	2.017	2.805	0.000	-1899.	0.	12.6	4.668
0.775	0.	0.2250	0.	0.	0.2250	16.66	0.000	0.000	0.439	2.027	2.829	0.000	-1923.	0.	12.5	4.519
0.800	0.	0.2000	0.	0.	0.2000	16.92	0.000	0.000	0.422	2.037	2.853	0.000	-1947.	0.	12.5	4.370
0.825	0.	0.1750	0.	0.	0.1750	17.18	0.000	0.000	0.405	2.047	2.877	0.000	-1971.	0.	12.4	4.221
0.850	0.	0.1500	0.	0.	0.1500	17.44	0.000	0.000	0.388	2.057	2.901	0.000	-1995.	0.	12.4	4.072
0.875	0.	0.1250	0.	0.	0.1250	17.70	0.000	0.000	0.371	2.067	2.925	0.000	-2019.	0.	12.3	3.923
0.900	0.	0.1000	0.	0.	0.1000	17.96	0.000	0.000	0.354	2.077	2.949	0.000	-2043.	0.	12.3	3.774
0.925	0.	0.0750	0.	0.	0.0750	18.22	0.000	0.000	0.337	2.087	2.973	0.000	-2067.	0.	12.2	3.625
0.950	0.	0.0500	0.	0.	0.0500	18.48	0.000	0.000	0.320	2.097	3.000	0.000	-2091.	0.	12.2	3.476
0.975	0.	0.0250	0.	0.	0.0250	18.74	0.000	0.000	0.303	2.107	3.024	0.000	-2115.	0.	12.1	3.327
1.000	0.	0.0000	0.	0.	0.0000	19.00	0.000	0.000	0.286	2.117	3.050	0.000	-2139.	0.	12.1	3.178

LIQUID MOLE FRACTION		VAPOR MOLE FRACTION			PRESSURE ATM	EQUIL CONST			RELATIVE VOL			ENTHALPY BTU/LB MOLE		HEAT CAPACITY BTU/LB MOLE	
N2	AR/AR+O2	N2	AR	O2		N2	AR	O2	N2/AR	N2/O2	AR/O2	LIG	VAP	LIG	VAP
0.	0.	0.	0.	1.0000	9.80	2.103	1.265	1.000	1.663	2.103	1.264	-1130.	1285.	14.3	0.450
0.1	0.	0.1210	0.8700	0.8700	10.10	2.024	1.210	0.977	1.672	2.072	1.239	-1154.	1229.	14.3	0.274
0.2	0.	0.2329	0.7673	0.7673	10.36	1.940	1.150	0.959	1.681	2.041	1.214	-1178.	1179.	14.2	0.149
0.3	0.	0.3378	0.6624	0.6624	10.62	1.863	1.103	0.946	1.690	2.011	1.190	-1202.	1130.	14.2	0.051
0.4	0.	0.4375	0.5625	0.5625	10.84	1.800	1.074	0.938	1.700	1.982	1.166	-1226.	1084.	14.2	0.000
0.5	0.	0.5335	0.4665	0.4665	11.03	1.803	1.067	0.934	1.708	1.955	1.144	-1250.	1041.	14.1	0.040
0.6	0.	0.6270	0.3730	0.3730	11.20	1.796	1.065	0.933	1.718	1.925	1.123	-1274.	999.	14.1	0.080
0.7	0.	0.7194	0.2806	0.2806	11.34	1.776	1.028	0.930	1.728	1.897	1.102	-1298.	958.	14.1	0.124
0.8	0.	0.8117	0.1883	0.1883	11.45	1.763	1.015	0.943	1.737	1.870	1.076	-1321.	919.	14.0	0.139
0.9	0.	0.9050	0.0953	0.0953	11.54	1.757	1.006	0.953	1.747	1.843	1.055	-1345.	879.	14.0	0.151
1.0	0.	1.0000	0.	0.	11.60	1.757	1.000	0.967	1.757	1.817	1.034	-1369.	838.	14.0	0.151
0.05	0.1	0.0585	0.1415	0.1415	10.13	2.033	1.226	0.974	1.688	2.088	1.289	-1109.	1279.	14.4	0.350
0.05	0.2	0.1475	0.2525	0.2525	10.40	1.961	1.177	0.953	1.666	2.058	1.235	-1132.	1226.	14.4	0.308
0.05	0.3	0.2463	0.3237	0.3237	10.63	1.892	1.139	0.938	1.675	2.028	1.211	-1156.	1177.	14.4	0.232
0.05	0.4	0.3453	0.4172	0.4172	11.14	1.811	1.101	0.916	1.684	1.999	1.187	-1179.	1131.	14.3	0.184
0.05	0.5	0.4443	0.5094	0.4444	11.32	1.779	1.045	0.916	1.693	1.971	1.164	-1202.	1087.	14.3	0.137
0.05	0.6	0.5438	0.5984	0.3571	11.48	1.753	1.025	0.916	1.711	1.915	1.141	-1225.	1046.	14.3	0.100
0.05	0.7	0.6434	0.6882	0.2688	11.62	1.735	1.028	0.919	1.721	1.888	1.119	-1249.	1004.	14.2	0.068
0.05	0.8	0.7431	0.7788	0.1804	11.73	1.723	0.996	0.925	1.730	1.862	1.097	-1272.	966.	14.2	0.041
0.05	0.9	0.8428	0.8682	0.0913	11.82	1.717	0.987	0.925	1.739	1.836	1.076	-1295.	928.	14.2	0.014
0.05	1.0	0.9425	0.9574	0.	11.89	1.717	0.982	0.949	1.749	1.810	1.058	-1318.	891.	14.1	0.000
0.10	0.1	0.1851	0.2149	0.2149	11.13	1.891	1.127	0.916	1.642	2.043	1.248	-1049.	1260.	14.6	0.360
0.10	0.2	0.2793	0.2907	0.2907	11.39	1.798	1.090	0.892	1.650	2.016	1.222	-1066.	1215.	14.6	0.310
0.10	0.3	0.3716	0.2782	0.2506	11.63	1.716	1.058	0.881	1.658	1.990	1.200	-1083.	1172.	14.7	0.261
0.10	0.4	0.4605	0.2624	0.2406	12.02	1.645	1.030	0.874	1.666	1.963	1.179	-1109.	1132.	14.7	0.213
0.10	0.5	0.5469	0.2439	0.2205	12.19	1.609	0.987	0.876	1.674	1.937	1.158	-1131.	1093.	14.7	0.172
0.10	0.6	0.6309	0.2235	0.2000	12.34	1.639	0.970	0.869	1.682	1.912	1.137	-1152.	1056.	14.7	0.138
0.10	0.7	0.7125	0.2015	0.1755	12.47	1.625	0.950	0.872	1.689	1.887	1.116	-1174.	1020.	14.6	0.110
0.10	0.8	0.7915	0.1781	0.1501	12.58	1.615	0.946	0.878	1.707	1.836	1.097	-1195.	985.	14.6	0.086
0.10	0.9	0.8680	0.1536	0.1208	12.67	1.609	0.938	0.887	1.716	1.810	1.078	-1217.	951.	14.6	0.063
0.10	1.0	0.9420	0.1280	0.	12.74	1.609	0.933	0.898	1.724	1.782	1.059	-1238.	917.	14.6	0.041
0.15	0.1	0.3240	0.2760	0.2760	12.44	1.659	1.024	0.836	1.620	1.985	1.229	-959.	1235.	15.3	0.330
0.15	0.2	0.3185	0.1955	0.2507	12.66	1.623	0.968	0.827	1.627	1.962	1.206	-978.	1197.	15.3	0.287
0.15	0.3	0.3133	0.2291	0.4578	13.04	1.564	0.935	0.821	1.634	1.939	1.187	-998.	1161.	15.3	0.246
0.15	0.4	0.3087	0.2999	0.2914	13.20	1.544	0.935	0.817	1.641	1.916	1.168	-1017.	1127.	15.2	0.207
0.15	0.5	0.3052	0.3688	0.2261	13.35	1.526	0.922	0.815	1.648	1.894	1.149	-1036.	1095.	15.2	0.169
0.15	0.6	0.3020	0.4384	0.2415	13.49	1.511	0.909	0.817	1.655	1.872	1.131	-1055.	1063.	15.2	0.137
0.15	0.7	0.3001	0.5072	0.1969	13.61	1.500	0.899	0.820	1.662	1.850	1.113	-1074.	1033.	15.2	0.108
0.15	0.8	0.2985	0.5760	0.1321	13.71	1.492	0.890	0.826	1.670	1.829	1.095	-1093.	1003.	15.1	0.082
0.15	0.9	0.2974	0.6450	0.0564	13.80	1.488	0.883	0.833	1.677	1.807	1.078	-1112.	973.	15.1	0.057
0.15	1.0	0.2971	0.7229	0.	13.88	1.486	0.879	0.841	1.682	1.787	1.064	-1131.	944.	15.1	0.040
0.20	0.1	0.4526	0.2474	0.2474	13.75	1.509	0.944	0.782	1.598	1.928	1.207	-874.	1207.	15.8	0.310
0.20	0.2	0.4454	0.2646	0.4454	14.03	1.464	0.928	0.778	1.604	1.900	1.190	-891.	1170.	15.8	0.268
0.20	0.3	0.4391	0.2773	0.4391	14.28	1.445	0.909	0.775	1.610	1.880	1.173	-907.	1147.	15.8	0.229
0.20	0.4	0.4336	0.2878	0.2878	14.50	1.429	0.894	0.773	1.616	1.870	1.157	-924.	1119.	15.8	0.192
0.20	0.5	0.4289	0.2968	0.3245	14.69	1.417	0.881	0.773	1.622	1.851	1.141	-941.	1091.	15.7	0.158
0.20	0.6	0.4250	0.3045	0.2707	14.82	1.410	0.870	0.773	1.628	1.832	1.125	-957.	1065.	15.7	0.128
0.20	0.7	0.4218	0.3113	0.2171	14.94	1.406	0.860	0.776	1.635	1.813	1.109	-974.	1039.	15.7	0.102
0.20	0.8	0.4193	0.3174	0.1635	14.95	1.392	0.845	0.783	1.641	1.795	1.094	-991.	1013.	15.7	0.078
0.20	0.9	0.4175	0.3232	0.1097	14.85	1.388	0.830	0.789	1.647	1.777	1.079	-1008.	988.	15.6	0.058
0.20	1.0	0.4163	0.3288	0.0552	14.94	1.388	0.830	0.789	1.653	1.759	1.064	-1024.	964.	15.6	0.040
0.25	0.1	0.6358	0.2642	0.2642	15.01	1.380	0.835	0.796	1.660	1.741	1.049	-1041.	939.	15.6	0.026
0.25	0.2	0.6355	0.2712	0.2642	15.21	1.373	0.868	0.739	1.662	1.696	1.174	-888.	1178.	16.3	0.330
0.25	0.3	0.6353	0.2782	0.2642	15.35	1.358	0.856	0.738	1.666	1.641	1.190	-907.	1147.	16.3	0.287
0.25	0.4	0.6353	0.2852	0.2642	15.48	1.346	0.846	0.738	1.669	1.624	1.166	-921.	1120.	16.3	0.246
0.25	0.5	0.6353	0.2922	0.2214	15.50	1.335	0.836	0.738	1.667	1.608	1.132	-936.	1093.	16.3	0.207
0.25	0.6	0.6353	0.2992	0.1786	15.51	1.326	0.828	0.740	1.662	1.592	1.119	-950.	1065.	16.2	0.169
0.25	0.7	0.6353	0.3062	0.1341	15.42	1.318	0.820	0.742	1.657	1.576	1.106	-964.	1039.	16.2	0.135
0.25	0.8	0.6353	0.3132	0.0896	15.31	1.312	0.814	0.745	1.651	1.560	1.093	-978.	1013.	16.2	0.102
0.25	0.9	0.6353	0.3202	0.0451	15.19	1.307	0.808	0.748	1.645	1.544	1.080	-993.	987.	16.2	0.074
0.25	1.0	0.6353	0.3272	0.	15.17	1.301	0.802	0.750	1.638	1.528	1.067	-1007.	976.	16.2	0.051
0.30	0.1	0.8453	0.1547	0.1547	16.46	1.291	0.830	0.710	1.599	1.610	1.189	-703.	1147.	16.8	0.330
0.30	0.2	0.8453	0.1617	0.1547	16.52	1.280	0.821	0.709	1.598	1.605	1.196	-715.	1127.	16.8	0.287
0.30	0.3	0.8453	0.1687	0.1547	16.63	1.270	0.813	0.709	1.593	1.591	1.196	-727.	1107.	16.8	0.246
0.30	0.4	0.8453	0.1757	0.1547	16.74	1.262	0.806	0.710	1.587	1.576	1.190	-739.	1089.	16.8	0.207
0.30	0.5	0.8453	0.1827	0.1547	16.84	1.255	0.799	0.711	1.571	1.560	1.184	-751.	1069.	16.8	0.169
0.30	0.6	0.8453	0.1897	0.1547	16.94	1.248	0.793	0.712	1.575	1.542	1.113	-762.	1052.	16.8	0.130
0.30	0.7	0.8453	0.1967	0.1547											

Table 26. (cont.)

LIQUID MOLE FRACTION		VAPOR MOLE FRACTION			PRESSURE ATM	EQUIL CONST			RELATIVE VOL			ENTHALPY BTU/LB MOLE		HEAT CAPACITY BTU/LB MOLE-R	
N ₂	AR/AR+O ₂	N ₂	AR	O ₂		N ₂	AR	O ₂	N ₂ /AR	N ₂ /O ₂	AR/O ₂	LIO	VAP	LIO	VAP
0.0	0.0	0.0	0.0	1.0000	11.48	2.005	1.245	1.000	1.011	2.005	1.244	1098.	1209.	14.6	9.670
0.1	0.0	0.1194	0.8806	11.82	1.934	1.194	0.979	1.019	1.976	1.229	1.007	1087.	1233.	14.6	9.720
0.2	0.0	0.2394	0.7606	12.13	1.875	1.152	0.962	1.027	1.948	1.197	1.010	1100.	1180.	14.6	9.572
0.3	0.0	0.3594	0.6406	12.40	1.826	1.118	0.951	1.035	1.920	1.174	1.013	1110.	1131.	14.6	9.427
0.4	0.0	0.4794	0.5206	12.64	1.786	1.086	0.943	1.044	1.893	1.152	1.016	1124.	1084.	14.6	9.284
0.5	0.0	0.5994	0.4006	12.85	1.753	1.062	0.939	1.052	1.867	1.130	1.019	1136.	1040.	14.6	9.137
0.6	0.0	0.7194	0.2806	13.04	1.726	1.041	0.939	1.060	1.844	1.109	1.022	1147.	997.	14.6	8.994
0.7	0.0	0.8394	0.1606	13.21	1.704	1.025	0.943	1.068	1.825	1.088	1.025	1157.	955.	14.6	8.852
0.8	0.0	0.9594	0.0406	13.36	1.687	1.013	0.949	1.077	1.799	1.067	1.028	1167.	913.	14.6	8.710
0.9	0.0	0.9794	0.0206	13.42	1.683	1.010	0.955	1.085	1.785	1.047	1.031	1176.	872.	14.6	8.569
1.0	0.0	1.0000	0.0000	13.48	1.682	1.008	0.973	1.093	1.780	1.028	1.034	1185.	831.	14.6	8.428
0.0	0.1	0.4880	0.5120	11.85	1.944	1.210	0.976	1.027	1.991	1.239	1.009	1036.	1263.	14.6	9.695
0.1	0.1	0.4700	0.5300	12.17	1.879	1.164	0.957	1.014	1.963	1.216	1.012	1050.	1229.	14.6	9.601
0.2	0.1	0.4520	0.5480	12.47	1.825	1.125	0.943	1.022	1.936	1.194	1.015	1063.	1198.	14.6	9.513
0.3	0.1	0.4340	0.5660	12.73	1.780	1.092	0.932	1.030	1.909	1.172	1.018	1076.	1168.	14.6	9.427
0.4	0.1	0.4160	0.5840	12.97	1.744	1.065	0.926	1.038	1.883	1.150	1.021	1089.	1138.	14.6	9.341
0.5	0.1	0.3980	0.6020	13.17	1.714	1.042	0.923	1.046	1.857	1.129	1.024	1102.	1108.	14.6	9.255
0.6	0.1	0.3800	0.6200	13.34	1.689	1.022	0.923	1.054	1.832	1.108	1.027	1115.	1078.	14.6	9.169
0.7	0.1	0.3620	0.6380	13.51	1.673	1.007	0.926	1.062	1.807	1.087	1.030	1128.	1048.	14.6	9.083
0.8	0.1	0.3440	0.6560	13.65	1.661	0.993	0.933	1.070	1.782	1.067	1.033	1141.	1018.	14.6	8.997
0.9	0.1	0.3260	0.6740	13.77	1.652	0.980	0.943	1.078	1.758	1.046	1.036	1154.	988.	14.6	8.911
1.0	0.1	0.3080	0.6920	13.88	1.646	0.968	0.956	1.086	1.735	1.025	1.039	1167.	958.	14.6	8.825
0.0	0.2	0.1782	0.8218	12.95	1.782	1.120	0.914	1.022	1.950	1.229	1.010	1025.	1295.	14.6	9.713
0.1	0.2	0.1733	0.8267	13.24	1.733	1.084	0.910	1.009	1.925	1.204	1.013	1038.	1265.	14.6	9.627
0.2	0.2	0.1684	0.8317	13.50	1.693	1.054	0.910	1.000	1.901	1.184	1.016	1051.	1235.	14.6	9.541
0.3	0.2	0.1635	0.8367	13.74	1.658	1.028	0.904	1.013	1.876	1.163	1.019	1064.	1205.	14.6	9.455
0.4	0.2	0.1586	0.8417	13.95	1.630	1.006	0.900	1.026	1.853	1.144	1.022	1077.	1175.	14.6	9.369
0.5	0.2	0.1537	0.8467	14.14	1.608	0.987	0.906	1.037	1.829	1.124	1.025	1090.	1145.	14.6	9.283
0.6	0.2	0.1488	0.8517	14.31	1.590	0.972	0.919	1.044	1.806	1.105	1.028	1103.	1115.	14.6	9.197
0.7	0.2	0.1439	0.8567	14.46	1.575	0.959	0.933	1.049	1.783	1.086	1.031	1116.	1085.	14.6	9.111
0.8	0.2	0.1390	0.8617	14.57	1.564	0.947	0.949	1.054	1.761	1.068	1.034	1129.	1055.	14.6	9.025
0.9	0.2	0.1341	0.8667	14.66	1.556	0.935	0.966	1.058	1.739	1.050	1.037	1142.	1025.	14.6	8.939
1.0	0.2	0.1292	0.8717	14.74	1.551	0.923	0.989	1.062	1.718	1.032	1.040	1155.	995.	14.6	8.853
0.0	0.3	0.3218	0.6782	14.42	1.629	1.034	0.888	1.027	1.897	1.207	1.011	1014.	1331.	14.6	9.765
0.1	0.3	0.3152	0.6848	14.66	1.576	0.999	0.890	1.018	1.876	1.186	1.014	1027.	1301.	14.6	9.679
0.2	0.3	0.3086	0.6914	14.88	1.540	0.977	0.895	1.004	1.854	1.165	1.017	1040.	1271.	14.6	9.593
0.3	0.3	0.3020	0.6980	15.08	1.508	0.956	0.901	1.000	1.833	1.143	1.020	1053.	1241.	14.6	9.507
0.4	0.3	0.2954	0.7046	15.27	1.483	0.942	0.910	1.006	1.812	1.121	1.023	1066.	1211.	14.6	9.421
0.5	0.3	0.2888	0.7112	15.43	1.463	0.930	0.923	1.013	1.792	1.101	1.026	1079.	1181.	14.6	9.335
0.6	0.3	0.2822	0.7178	15.58	1.447	0.918	0.932	1.019	1.772	1.081	1.029	1092.	1151.	14.6	9.249
0.7	0.3	0.2756	0.7244	15.71	1.433	0.906	0.945	1.024	1.752	1.061	1.032	1105.	1121.	14.6	9.163
0.8	0.3	0.2690	0.7310	15.83	1.420	0.894	0.960	1.028	1.732	1.041	1.035	1118.	1091.	14.6	9.077
0.9	0.3	0.2624	0.7376	15.92	1.409	0.882	0.977	1.032	1.713	1.021	1.038	1131.	1061.	14.6	8.991
1.0	0.3	0.2558	0.7442	16.00	1.400	0.870	0.996	1.036	1.695	1.001	1.041	1144.	1031.	14.6	8.905
0.0	0.4	0.4441	0.5559	14.92	1.492	1.044	0.888	1.027	1.899	1.237	1.012	1003.	1351.	14.6	9.819
0.1	0.4	0.4389	0.5611	15.18	1.445	0.999	0.890	1.018	1.878	1.216	1.015	1016.	1321.	14.6	9.733
0.2	0.4	0.4337	0.5663	15.41	1.408	0.977	0.895	1.004	1.856	1.195	1.018	1029.	1291.	14.6	9.647
0.3	0.4	0.4285	0.5715	15.61	1.380	0.956	0.901	1.000	1.835	1.174	1.021	1042.	1261.	14.6	9.561
0.4	0.4	0.4233	0.5767	15.79	1.358	0.942	0.910	1.006	1.814	1.153	1.024	1055.	1231.	14.6	9.475
0.5	0.4	0.4181	0.5819	15.95	1.340	0.930	0.923	1.013	1.794	1.133	1.027	1068.	1201.	14.6	9.389
0.6	0.4	0.4129	0.5871	16.09	1.324	0.918	0.932	1.019	1.774	1.113	1.030	1081.	1171.	14.6	9.303
0.7	0.4	0.4077	0.5923	16.21	1.310	0.906	0.945	1.024	1.754	1.093	1.033	1094.	1141.	14.6	9.217
0.8	0.4	0.4025	0.5975	16.32	1.298	0.894	0.960	1.028	1.734	1.073	1.036	1107.	1111.	14.6	9.131
0.9	0.4	0.3973	0.6027	16.42	1.288	0.882	0.977	1.032	1.714	1.053	1.039	1120.	1081.	14.6	9.045
1.0	0.4	0.3921	0.6079	16.50	1.280	0.870	0.996	1.036	1.695	1.033	1.042	1133.	1051.	14.6	8.959
0.0	0.5	0.5333	0.4667	15.77	1.361	1.039	0.799	1.021	1.993	1.171	1.013	1000.	1381.	14.6	9.923
0.1	0.5	0.5281	0.4719	15.94	1.346	0.977	0.798	1.026	1.977	1.151	1.016	1013.	1351.	14.6	9.837
0.2	0.5	0.5229	0.4771	16.09	1.333	0.966	0.797	1.030	1.962	1.134	1.019	1026.	1321.	14.6	9.751
0.3	0.5	0.5177	0.4823	16.24	1.321	0.956	0.796	1.034	1.947	1.117	1.022	1039.	1291.	14.6	9.665
0.4	0.5	0.5125	0.4875	16.38	1.310	0.947	0.795	1.038	1.932	1.101	1.025	1052.	1261.	14.6	9.579
0.5	0.5	0.5073	0.4927	16.50	1.300	0.939	0.794	1.042	1.917	1.084	1.028	1065.	1231.	14.6	9.493
0.6	0.5	0.5021	0.4979	16.61	1.290	0.930	0.793	1.046	1.902	1.067	1.031	1078.	1201.	14.6	9.407
0.7	0.5	0.4969	0.5031	16.71	1.280	0.922	0.792	1.049	1.887	1.051	1.034	1091.	1171.	14.6	9.321
0.8	0.5	0.4917	0.5083	16.80	1.270	0.914	0.791	1.052	1.872	1.034	1.037	1104.	1141.	14.6	9.235
0.9	0.5	0.4865	0.5135	16.88	1.260	0.906	0.790	1.055	1.857	1.017	1.040	1117.	1111.	14.6	9.149
1.0	0.5	0.4813	0.5187	16.95	1.250	0.898	0.789	1.058	1.842	1.001	1.043	1130.	1081.	14.6	9.063
0.0	0.6	0.6333	0.3667	16.47	1.196	0.863	0.707	1.009	1.990	1.135	1.014	1000.	1431.	14.6	10.077
0.1	0.6	0.6281	0.3719	16.68	1.189	0.860	0.708	1.001	1.980	1.127	1.017	1013.	1401.	14.6	9.991
0.2	0.6	0.6229	0.3771	16.86	1.184	0.858	0.709	1.004	1.971	1.116	1.020	1026.	1371.	14.6	9.905
0.3	0.6	0.6177	0.3823	17.02	1.179	0.856	0.710	1.006	1.961	1.105	1.023	1039.	1341.	14.6	9.819
0.4	0.6	0.6125	0.3875	17.16	1.174	0.854	0.711	1.009	1.952	1.094	1.026	1052.	1311.	14.6	9.733
0.5	0.6	0.6073	0.3927	17.29	1.170	0.852	0.712	1.012	1.942	1.084	1.029	1065.	1281.	14.6	9.647
0.6	0.6	0.6021	0.3979	17.41	1.166	0.850	0.713	1.014	1.932	1.074	1.032	1078.	1251.	14.6	9.561
0.7	0.6	0.5969	0.4031	17.52	1.163	0.848	0.714	1.016	1.922	1.064	1.035	1091.	1221.	14.6	9.475
0.8	0.6	0.5917	0.4083	17.62	1.160	0.846	0.715	1.018	1.912	1.054	1.038	1104.	1191.	14.6	9.389
0.9	0.6														

TEMPERATURE	LIQUID MOLE FRACTION		VAPOR MOLE FRACTION			PRESSURE	EQUIL CONST			RELATIVE VOL			ENTHALPY		HEAT CAPACITY		
	N ₂	AR/AR-O ₂	N ₂	AR	O ₂		ATM	N ₂	AR	O ₂	N ₂ /AR	N ₂ /O ₂	AR/O ₂	LIG	VAP	LIG	VAP
0.0	0.0	0.0	0.0	1.0000	13.35	1.923	1.028	1.000	1.569	1.922	1.025	-984.	1291.	15.1	10.391		
0.1	0.0	0.1179	0.0822	0.0	13.74	1.898	1.179	0.982	1.578	1.895	1.203	-984.	1291.	15.1	10.391		
0.2	0.0	0.2280	0.7722	0.0	14.08	1.867	1.140	0.968	1.583	1.860	1.191	-984.	1291.	15.1	10.391		
0.3	0.0	0.3320	0.6681	0.0	14.38	1.780	1.107	0.954	1.590	1.844	1.180	-984.	1291.	15.1	10.391		
0.4	0.0	0.4316	0.5684	0.0	14.65	1.723	1.079	0.948	1.597	1.818	1.170	-984.	1291.	15.1	10.391		
0.5	0.0	0.5260	0.4722	0.0	14.88	1.689	1.056	0.944	1.604	1.794	1.161	-984.	1291.	15.1	10.391		
0.6	0.0	0.6223	0.3779	0.0	15.08	1.671	1.037	0.945	1.611	1.769	1.150	-984.	1291.	15.1	10.391		
0.7	0.0	0.7190	0.2845	0.0	15.25	1.655	1.023	0.948	1.619	1.745	1.139	-984.	1291.	15.1	10.391		
0.8	0.0	0.8137	0.1913	0.0	15.39	1.645	1.012	0.955	1.626	1.722	1.129	-984.	1291.	15.1	10.391		
0.9	0.0	0.9037	0.0983	0.0	15.49	1.640	1.004	0.965	1.633	1.699	1.120	-984.	1291.	15.1	10.391		
1.0	0.0	1.0000	0.0	0.0	15.55	1.640	1.000	0.979	1.641	1.676	1.122	-984.	1291.	15.1	10.391		
0.0	0.1	0.0467	0.0	0.0838	13.77	1.867	1.154	0.978	1.564	1.909	1.221	-984.	1291.	15.2	10.400		
0.0	0.2	0.0934	0.0	0.1676	14.12	1.839	1.131	0.963	1.571	1.884	1.199	-984.	1291.	15.2	10.400		
0.0	0.3	0.1401	0.0	0.2519	14.46	1.780	1.115	0.947	1.578	1.859	1.178	-984.	1291.	15.2	10.400		
0.0	0.4	0.1868	0.0	0.3362	14.79	1.719	1.095	0.938	1.585	1.833	1.157	-984.	1291.	15.2	10.400		
0.0	0.5	0.2335	0.0	0.4205	15.11	1.680	1.079	0.932	1.592	1.807	1.137	-984.	1291.	15.2	10.400		
0.0	0.6	0.2802	0.0	0.5048	15.42	1.659	1.068	0.929	1.599	1.780	1.117	-984.	1291.	15.2	10.400		
0.0	0.7	0.3269	0.0	0.5891	15.73	1.638	1.020	0.920	1.606	1.754	1.097	-984.	1291.	15.2	10.400		
0.0	0.8	0.3736	0.0	0.6734	16.04	1.622	1.000	0.923	1.613	1.728	1.078	-984.	1291.	15.2	10.400		
0.0	0.9	0.4203	0.0	0.7577	16.35	1.613	0.988	0.945	1.620	1.701	1.059	-984.	1291.	15.2	10.400		
0.0	1.0	0.4670	0.0	0.8420	16.66	1.610	0.989	0.963	1.627	1.673	1.041	-984.	1291.	15.2	10.400		
0.0	0.1	0.1678	0.0070	0.7354	15.31	1.878	1.110	0.920	1.591	1.872	1.217	-984.	1291.	15.6	11.010		
0.0	0.2	0.3041	0.1890	0.6472	15.80	1.841	1.078	0.908	1.597	1.849	1.187	-984.	1291.	15.6	11.010		
0.0	0.3	0.4010	0.2769	0.5624	16.07	1.810	1.054	0.893	1.593	1.826	1.168	-984.	1291.	15.6	11.010		
0.0	0.4	0.4980	0.3618	0.4801	16.31	1.803	1.005	0.889	1.589	1.803	1.149	-984.	1291.	15.6	11.010		
0.0	0.5	0.5950	0.4444	0.3997	16.51	1.802	0.988	0.888	1.582	1.779	1.130	-984.	1291.	15.6	11.010		
0.0	0.6	0.6920	0.5256	0.3202	16.69	1.800	0.973	0.890	1.588	1.756	1.112	-984.	1291.	15.6	11.010		
0.0	0.7	0.7890	0.6058	0.2412	16.85	1.833	0.962	0.893	1.594	1.731	1.093	-984.	1291.	15.6	11.010		
0.0	0.8	0.8860	0.6840	0.1619	16.97	1.825	0.953	0.899	1.601	1.696	1.075	-984.	1291.	15.6	11.010		
0.0	0.9	0.9830	0.7622	0.0817	17.07	1.821	0.946	0.908	1.607	1.670	1.057	-984.	1291.	15.6	11.010		
0.0	1.0	1.0000	0.0	0.0	17.15	1.821	0.943	0.919	1.614	1.656	1.038	-984.	1291.	15.6	11.010		
0.0	0.1	0.3071	0.0799	0.6134	16.03	1.966	1.022	0.899	1.533	1.822	1.199	-984.	1291.	16.1	11.749		
0.0	0.2	0.5019	0.1965	0.5420	17.15	1.935	0.978	0.892	1.538	1.802	1.172	-984.	1291.	16.1	11.749		
0.0	0.3	0.6975	0.2305	0.4725	17.37	1.915	0.961	0.887	1.543	1.782	1.155	-984.	1291.	16.1	11.749		
0.0	0.4	0.8930	0.3024	0.4042	17.59	1.898	0.946	0.884	1.548	1.763	1.138	-984.	1291.	16.1	11.749		
0.0	0.5	1.0885	0.3727	0.3370	17.77	1.883	0.932	0.882	1.554	1.743	1.122	-984.	1291.	16.1	11.749		
0.0	0.6	1.2840	0.4419	0.2702	17.93	1.868	0.921	0.884	1.560	1.724	1.106	-984.	1291.	16.1	11.749		
0.0	0.7	1.4795	0.5104	0.2035	18.08	1.861	0.911	0.888	1.567	1.705	1.090	-984.	1291.	16.1	11.749		
0.0	0.8	1.6750	0.5787	0.1366	18.20	1.825	0.904	0.893	1.574	1.686	1.073	-984.	1291.	16.1	11.749		
0.0	0.9	1.8705	0.6471	0.0698	18.30	1.821	0.899	0.901	1.581	1.667	1.057	-984.	1291.	16.1	11.749		
0.0	1.0	2.0660	0.7154	0.0	18.38	1.821	0.895	0.912	1.587	1.648	1.039	-984.	1291.	16.1	11.749		
0.0	0.1	0.4257	0.0094	0.5683	16.29	1.846	0.985	0.882	1.514	1.773	1.171	-984.	1291.	16.6	12.688		
0.0	0.2	0.8203	0.1288	0.5091	16.92	1.819	0.939	0.890	1.518	1.756	1.157	-984.	1291.	16.6	12.688		
0.0	0.3	1.2149	0.1905	0.3941	17.42	1.802	0.920	0.890	1.523	1.739	1.142	-984.	1291.	16.6	12.688		
0.0	0.4	1.6095	0.2506	0.3370	17.81	1.787	0.907	0.894	1.527	1.722	1.126	-984.	1291.	16.6	12.688		
0.0	0.5	1.9941	0.3101	0.2819	18.10	1.781	0.896	0.894	1.532	1.706	1.114	-984.	1291.	16.6	12.688		
0.0	0.6	2.3787	0.3695	0.2268	18.41	1.765	0.877	0.898	1.536	1.690	1.100	-984.	1291.	16.6	12.688		
0.0	0.7	2.7633	0.4284	0.1704	18.64	1.748	0.870	0.898	1.541	1.674	1.086	-984.	1291.	16.6	12.688		
0.0	0.8	3.1479	0.4871	0.1142	18.86	1.740	0.864	0.901	1.546	1.658	1.073	-984.	1291.	16.6	12.688		
0.0	0.9	3.5325	0.5457	0.0580	19.07	1.733	0.858	0.902	1.550	1.642	1.060	-984.	1291.	16.6	12.688		
0.0	1.0	3.9171	0.6043	0.0	19.28	1.726	0.852	0.905	1.554	1.626	1.048	-984.	1291.	16.6	12.688		
0.0	0.1	0.3351	0.0	0.6654	16.98	1.838	0.995	0.776	1.484	1.725	1.154	-984.	1291.	17.1	13.933		
0.0	0.2	0.6702	0.0930	0.6180	20.17	1.824	0.984	0.774	1.488	1.710	1.142	-984.	1291.	17.1	13.933		
0.0	0.3	1.0053	0.1860	0.5711	20.35	1.811	0.973	0.773	1.492	1.696	1.129	-984.	1291.	17.1	13.933		
0.0	0.4	1.3404	0.2790	0.5242	20.53	1.800	0.964	0.773	1.495	1.682	1.117	-984.	1291.	17.1	13.933		
0.0	0.5	1.6755	0.3720	0.4773	20.68	1.791	0.955	0.774	1.499	1.668	1.105	-984.	1291.	17.1	13.933		
0.0	0.6	2.0106	0.4650	0.4304	20.82	1.783	0.948	0.775	1.503	1.654	1.094	-984.	1291.	17.1	13.933		
0.0	0.7	2.3457	0.5580	0.3835	20.95	1.775	0.942	0.778	1.507	1.641	1.082	-984.	1291.	17.1	13.933		
0.0	0.8	2.6808	0.6510	0.3366	21.07	1.771	0.936	0.781	1.510	1.628	1.071	-984.	1291.	17.1	13.933		
0.0	0.9	3.0159	0.7440	0.2897	21.18	1.765	0.931	0.785	1.514	1.615	1.059	-984.	1291.	17.1	13.933		
0.0	1.0	3.3510	0.8370	0.2428	21.28	1.760	0.926	0.789	1.518	1.602	1.048	-984.	1291.	17.1	13.933		
0.0	0.1	0.6265	0.0	0.3730	21.76	1.823	0.955	0.748	1.474	1.675	1.137	-984.	1291.	17.6	15.686		
0.0	0.2	1.2530	0.0421	0.3364	21.91	1.844	0.942	0.747	1.477	1.658	1.127	-984.	1291.	17.6	15.686		
0.0	0.3	1.8795	0.0842	0.2999	22.06	1.836	0.935	0.748	1.480	1.639	1.117	-984.	1291.	17.6	15.686		
0.0	0.4	2.5060	0.1263	0.2630	22.20	1.828	0.928	0.749	1.483	1.621	1.107	-984.	1291.	17.6	15.686		
0.0	0.5	3.1325	0.1684	0.2261	22.33	1.822	0.923	0.750	1.486	1.603	1.097	-984.	1291.	17.6	15.686		
0.0	0.6	3.7590	0.2105	0.1892	22.45	1.816	0.917	0.752	1.489	1.585	1.087						

TEMPERATURE = 230. R

Table 26. (cont.)

LIQUID MOLE FRACTION		VAPOR MOLE FRACTION			PRESSURE ATM	EQUIL CONST			RELATIVE VOL			ENTHALPY BTU/LB MOLE		HEAT CAPACITY BTU/LB MOLE-R	
N2	AR/AR+O2	N2	AR	O2		N2	AR	O2	N2/AR	N2/O2	AR/O2	L10	VAP	L10	VAP
.00	0.	0.	0.	1.0000	15.44	1.055	1.207	1.000	1.936	1.055	1.207	-907.	1200.	19.6	11.012
.00	0.1	0.	0.1145	0.8837	15.86	1.707	1.165	0.982	1.943	1.030	1.186	-931.	1229.	19.6	10.968
.00	0.2	0.	0.2297	0.7745	16.23	1.740	1.129	0.968	1.949	1.006	1.166	-959.	1174.	19.6	10.908
.00	0.3	0.	0.3294	0.6708	16.57	1.708	1.098	0.958	1.955	1.702	1.146	-979.	1122.	19.6	10.796
.00	0.4	0.	0.4290	0.5713	17.12	1.648	1.072	0.952	1.961	1.736	1.126	-1003.	1072.	19.6	10.590
.00	0.5	0.	0.5256	0.4740	17.34	1.627	1.051	0.950	1.967	1.735	1.107	-1027.	1025.	19.6	10.480
.00	0.6	0.	0.6203	0.3800	17.52	1.612	1.034	0.950	1.974	1.732	1.088	-1052.	979.	19.6	10.349
.00	0.7	0.	0.7142	0.2882	17.67	1.603	1.020	0.950	1.980	1.696	1.073	-1076.	939.	19.6	10.200
.00	0.8	0.	0.8082	0.1921	17.77	1.599	1.004	0.971	1.983	1.647	1.052	-1100.	891.	19.6	10.030
.00	0.9	0.	0.9033	0.0971	17.83	1.600	1.000	0.984	1.989	1.626	1.037	-1124.	847.	19.6	9.838
.00	1.0	0.	1.0000	0.	17.89	1.605	1.178	0.980	1.992	1.643	1.023	-1148.	804.	19.6	9.619
.025	0.1	0.	0.1438	0.8562	16.30	1.753	1.130	0.963	1.930	1.019	1.163	-907.	1229.	19.7	11.191
.025	0.2	0.	0.2876	0.7124	16.66	1.708	1.106	0.951	1.944	1.706	1.143	-931.	1170.	19.7	11.101
.025	0.3	0.	0.4314	0.5686	16.98	1.671	1.078	0.943	1.950	1.772	1.143	-959.	1120.	19.7	11.013
.025	0.4	0.	0.5752	0.4248	17.27	1.608	1.054	0.937	1.956	1.736	1.124	-979.	1072.	19.7	10.825
.025	0.5	0.	0.7190	0.2812	17.52	1.596	1.034	0.935	1.962	1.727	1.105	-1003.	1025.	19.7	10.717
.025	0.6	0.	0.8628	0.1376	17.61	1.593	1.018	0.936	1.968	1.705	1.087	-1027.	979.	19.7	10.599
.025	0.7	0.	1.0066	0.0000	17.65	1.594	1.009	0.946	1.975	1.684	1.069	-1052.	939.	19.7	10.456
.025	0.8	0.	1.1454	0.0000	17.68	1.597	1.006	0.956	1.981	1.662	1.052	-1076.	897.	19.7	10.296
.025	0.9	0.	1.2842	0.0000	17.72	1.600	1.004	0.966	1.987	1.641	1.034	-1099.	855.	19.7	10.113
.025	1.0	0.	1.4230	0.0000	17.77	1.604	1.000	0.976	1.993	1.621	1.017	-1124.	813.	19.7	9.904
.100	0.1	0.	0.1674	0.8326	17.62	1.674	1.101	0.925	1.930	1.000	1.170	-814.	1293.	10.1	11.794
.100	0.2	0.	0.3348	0.6652	17.95	1.600	1.045	0.908	1.931	1.705	1.153	-838.	1244.	10.1	11.644
.100	0.3	0.	0.5022	0.4978	18.25	1.570	1.022	0.900	1.936	1.744	1.135	-857.	1197.	10.1	11.492
.100	0.4	0.	0.6696	0.3304	18.51	1.546	1.003	0.897	1.942	1.723	1.118	-879.	1152.	10.1	11.303
.100	0.5	0.	0.8370	0.1630	18.74	1.527	0.987	0.896	1.947	1.703	1.101	-901.	1069.	10.1	11.085
.100	0.6	0.	1.0044	0.0000	18.94	1.512	0.974	0.898	1.953	1.683	1.084	-922.	1020.	10.1	11.485
.100	0.7	0.	1.1718	0.0000	19.11	1.500	0.963	0.902	1.958	1.663	1.068	-944.	980.	10.1	11.302
.100	0.8	0.	1.3392	0.0000	19.24	1.493	0.955	0.908	1.964	1.644	1.051	-966.	949.	10.1	11.281
.100	0.9	0.	1.5066	0.0000	19.35	1.489	0.950	0.917	1.969	1.625	1.036	-987.	911.	10.1	11.150
.100	1.0	0.	1.6740	0.0000	19.42	1.486	0.946	0.927	1.975	1.606	1.020	-1009.	874.	10.1	10.996
.200	0.1	0.	0.3050	0.6950	19.13	1.520	1.018	0.888	1.933	1.762	1.172	-721.	1215.	10.5	12.790
.200	0.2	0.	0.6100	0.3900	19.43	1.502	0.996	0.881	1.936	1.743	1.154	-749.	1173.	10.5	12.702
.200	0.3	0.	0.9150	0.0850	19.71	1.478	0.977	0.877	1.942	1.725	1.136	-779.	1133.	10.5	12.786
.200	0.4	0.	1.2200	0.0000	19.97	1.457	0.961	0.894	1.947	1.706	1.119	-809.	1095.	10.5	12.777
.200	0.5	0.	1.5250	0.0000	20.19	1.448	0.947	0.893	1.951	1.688	1.110	-839.	1058.	10.5	12.719
.200	0.6	0.	1.8300	0.0000	20.40	1.426	0.934	0.894	1.956	1.671	1.099	-869.	1023.	10.5	12.608
.200	0.7	0.	2.1350	0.0000	20.58	1.415	0.924	0.896	1.961	1.653	1.080	-899.	988.	10.5	12.598
.200	0.8	0.	2.4400	0.0000	20.73	1.406	0.916	0.890	1.966	1.636	1.065	-929.	955.	10.5	12.598
.200	0.9	0.	2.7450	0.0000	20.86	1.401	0.909	0.885	1.970	1.619	1.051	-959.	922.	10.5	12.567
.200	1.0	0.	3.0500	0.0000	20.97	1.397	0.904	0.872	1.975	1.603	1.037	-989.	889.	10.5	12.393
.300	0.1	0.	0.4240	0.5760	21.03	1.413	0.951	0.824	1.485	1.716	1.155	-620.	1172.	17.0	14.138
.300	0.2	0.	0.8480	0.1520	21.30	1.394	0.936	0.820	1.489	1.700	1.141	-649.	1130.	17.0	14.192
.300	0.3	0.	1.2720	0.0280	21.54	1.377	0.922	0.818	1.493	1.684	1.128	-662.	1103.	17.0	14.244
.300	0.4	0.	1.6960	0.0000	21.76	1.363	0.910	0.817	1.497	1.668	1.115	-676.	1070.	17.0	14.287
.300	0.5	0.	2.1200	0.0000	21.96	1.350	0.900	0.817	1.501	1.653	1.101	-699.	1039.	17.0	14.317
.300	0.6	0.	2.5440	0.0000	22.14	1.340	0.891	0.818	1.505	1.638	1.086	-712.	1008.	17.0	14.333
.300	0.7	0.	2.9680	0.0000	22.31	1.332	0.883	0.821	1.508	1.623	1.076	-726.	978.	17.0	14.331
.300	0.8	0.	3.3920	0.0000	22.45	1.326	0.876	0.824	1.512	1.608	1.063	-740.	949.	17.0	14.318
.300	0.9	0.	3.8160	0.0000	22.57	1.321	0.871	0.829	1.516	1.593	1.051	-763.	921.	17.0	14.266
.300	1.0	0.	4.2400	0.0000	22.68	1.319	0.867	0.835	1.521	1.579	1.039	-786.	893.	17.0	14.198
.400	0.1	0.	0.5430	0.4570	22.76	1.316	0.864	0.842	1.525	1.565	1.027	-799.	866.	17.0	14.144
.400	0.2	0.	1.0860	0.0000	23.03	1.317	0.868	0.789	1.467	1.669	1.138	-535.	1121.	17.5	16.095
.400	0.3	0.	1.6290	0.0000	23.25	1.304	0.860	0.788	1.470	1.656	1.127	-569.	1082.	17.5	16.231
.400	0.4	0.	2.1720	0.0000	23.45	1.293	0.850	0.787	1.473	1.642	1.119	-594.	1044.	17.5	16.359
.400	0.5	0.	2.7150	0.0000	23.64	1.283	0.840	0.786	1.476	1.629	1.104	-619.	1006.	17.5	16.477
.400	0.6	0.	3.2580	0.0000	23.82	1.274	0.832	0.789	1.479	1.616	1.093	-644.	968.	17.5	16.582
.400	0.7	0.	3.8010	0.0000	23.99	1.267	0.825	0.790	1.482	1.603	1.082	-669.	933.	17.5	16.666
.400	0.8	0.	4.3440	0.0000	24.14	1.261	0.819	0.793	1.485	1.591	1.071	-694.	898.	17.5	16.737
.400	0.9	0.	4.8870	0.0000	24.27	1.256	0.814	0.796	1.488	1.579	1.061	-719.	863.	17.5	16.785
.400	1.0	0.	5.4300	0.0000	24.39	1.253	0.810	0.800	1.491	1.566	1.050	-744.	828.	17.5	16.809
.500	0.1	0.	0.6620	0.3380	24.40	1.250	0.807	0.803	1.495	1.554	1.040	-769.	793.	17.5	16.809
.500	0.2	0.	1.3240	0.0000	24.50	1.250	0.804	0.810	1.498	1.542	1.030	-794.	758.	17.5	16.771
.500	0.3	0.	1.9860	0.0000	24.57	1.257	0.806	0.764	1.446	1.620	1.141	-442.	1050.	18.0	19.349
.500	0.4	0.	2.6480	0.0000	24.62	1.229	0.849	0.764	1.448	1.609	1.132	-464.	1034.	18.0	19.423
.500	0.5	0.	3.3100	0.0000	24.66	1.221	0.842	0.764	1.450	1.599	1.122	-486.	1011.	18.0	19.491
.500	0.6	0.	3.9720	0.0000	24.69	1.215	0.836	0.765	1.452	1.587	1.093	-508.	987.	18.0	19.551
.500	0.7	0.	4.6340	0.0000	24.74	1.209	0.831	0.767	1.454	1.577	1.084	-530.	964.	18.0	19.608
.500	0.8	0.	5.2960	0.0000	24.78	1.203	0.826	0.768	1.457	1.566	1.075	-552.	942.	18.0	19.666

TEMPERATURE = 236. R

Table 26. (cont.)

LIQUID MOLE FRACTION		VAPOR MOLE FRACTION			PRESSURE ATM	EQUIL CONST			RELATIVE VOL			ENTHALPY BTU/LB MOLE		HEAT CAPACITY BTU/LB MOLE-R	
N2	AR/AR+O2	N2	AR	O2		N2	AR	O2	N2/AR	N2/O2	AR/O2	LIQ	VAP	LIQ	VAP
0.	0.	0.	0.	1.0004	17.73	1.825	1.191	1.000	1.515	1.804	1.191	-827.	1201.	16.2	11.790
0.1	0.	0.	0.1152	0.8852	18.20	1.782	1.192	0.984	1.521	1.781	1.171	-827.	1221.	16.2	11.729
0.2	0.	0.	0.2237	0.7767	18.61	1.737	1.119	0.971	1.526	1.756	1.152	-828.	1144.	16.2	11.669
0.3	0.	0.	0.3271	0.6734	18.98	1.670	1.090	0.962	1.532	1.736	1.133	-828.	1111.	16.2	11.623
0.4	0.	0.	0.4245	0.5773	19.32	1.639	1.066	0.956	1.537	1.714	1.115	-828.	1079.	16.2	11.582
0.5	0.	0.	0.5232	0.4770	19.62	1.614	1.046	0.954	1.543	1.692	1.097	-828.	1048.	16.2	11.543
0.6	0.	0.	0.6183	0.3819	19.88	1.595	1.030	0.955	1.548	1.671	1.079	-828.	1018.	16.2	11.507
0.7	0.	0.	0.7126	0.2876	20.10	1.582	1.018	0.959	1.554	1.650	1.062	-828.	989.	16.2	11.473
0.8	0.	0.	0.8071	0.1931	20.28	1.574	1.009	0.965	1.559	1.629	1.045	-828.	962.	16.2	11.440
0.9	0.	0.	0.9027	0.0979	20.43	1.570	1.003	0.975	1.565	1.609	1.028	-828.	937.	16.2	11.408
1.0	1.0	0.	1.0002	0.	20.56	1.570	1.000	0.989	1.570	1.590	1.012	-828.	913.	16.2	11.378
0.25	0.	0.0440	0.	0.9564	18.25	1.769	1.184	0.981	1.511	1.793	1.187	-828.	1272.	16.3	12.326
0.25	0.1	0.0428	0.1100	0.8477	18.70	1.711	1.128	0.966	1.517	1.771	1.168	-827.	1214.	16.3	11.982
0.25	0.2	0.0417	0.2139	0.7444	19.11	1.669	1.077	0.955	1.522	1.749	1.149	-827.	1159.	16.3	11.632
0.25	0.3	0.0409	0.3131	0.6462	19.47	1.635	1.071	0.947	1.527	1.727	1.149	-827.	1107.	16.3	11.283
0.25	0.4	0.0402	0.4089	0.5511	19.78	1.607	1.048	0.942	1.533	1.706	1.131	-827.	1057.	16.3	11.037
0.25	0.5	0.0394	0.5022	0.4584	20.05	1.584	1.030	0.940	1.538	1.685	1.095	-827.	1009.	16.3	11.817
0.25	0.6	0.0389	0.6049	0.3765	20.29	1.567	1.015	0.942	1.543	1.664	1.078	-827.	963.	16.3	11.737
0.25	0.7	0.0380	0.7160	0.2957	20.48	1.554	1.003	0.945	1.549	1.644	1.061	-827.	920.	16.3	11.657
0.25	0.8	0.0380	0.8360	0.2163	20.64	1.544	0.995	0.952	1.554	1.624	1.045	-827.	879.	16.3	11.573
0.25	0.9	0.0380	0.9617	0.1397	20.78	1.543	0.989	0.961	1.559	1.604	1.028	-827.	839.	16.3	11.488
0.25	1.0	0.0380	1.0000	0.0637	20.91	1.544	0.986	0.974	1.565	1.585	1.013	-827.	799.	16.3	11.403
1.00	0.	0.1637	0.	0.8363	19.82	1.637	1.081	0.930	1.503	1.761	1.174	-827.	1240.	16.7	12.850
1.00	0.1	0.1600	0.0997	0.7446	20.22	1.600	1.083	0.919	1.509	1.741	1.157	-828.	1189.	16.7	12.500
1.00	0.2	0.1569	0.1070	0.6564	20.59	1.569	1.038	0.912	1.516	1.721	1.140	-828.	1140.	16.7	12.150
1.00	0.3	0.1542	0.2749	0.5712	20.91	1.542	1.018	0.907	1.521	1.701	1.123	-828.	1094.	16.6	12.000
1.00	0.4	0.1520	0.3692	0.4882	21.20	1.520	1.001	0.904	1.526	1.681	1.107	-828.	1050.	16.6	12.000
1.00	0.5	0.1500	0.4435	0.4066	21.46	1.502	0.986	0.904	1.531	1.662	1.091	-828.	1007.	16.6	12.000
1.00	0.6	0.1485	0.5294	0.3280	21.67	1.488	0.973	0.908	1.536	1.643	1.075	-828.	965.	16.6	12.000
1.00	0.7	0.1476	0.6071	0.2493	21.86	1.478	0.964	0.909	1.543	1.625	1.058	-828.	924.	16.6	12.000
1.00	0.8	0.1471	0.6885	0.1740	22.01	1.471	0.956	0.916	1.548	1.607	1.042	-828.	884.	16.6	12.000
1.00	0.9	0.1468	0.7705	0.1031	22.12	1.468	0.951	0.924	1.553	1.589	1.026	-828.	844.	16.6	12.000
1.00	1.0	0.1468	0.8336	0.	22.18	1.468	0.949	0.934	1.558	1.572	1.019	-828.	804.	16.6	12.000
2.00	0.	0.3015	0.	0.6985	21.97	1.503	1.112	0.879	1.485	1.717	1.137	-827.	1193.	17.1	14.287
2.00	0.1	0.2993	0.0704	0.6255	22.33	1.477	1.092	0.869	1.492	1.697	1.122	-828.	1149.	17.1	14.378
2.00	0.2	0.2969	0.1599	0.5534	22.64	1.455	1.078	0.865	1.498	1.678	1.107	-828.	1108.	17.1	14.459
2.00	0.3	0.2971	0.2303	0.4820	22.93	1.436	1.069	0.862	1.499	1.662	1.127	-828.	1068.	17.1	14.521
2.00	0.4	0.2939	0.3028	0.4135	23.19	1.420	1.046	0.862	1.500	1.646	1.113	-828.	1029.	17.0	14.571
2.00	0.5	0.2913	0.3749	0.3449	23.42	1.407	1.035	0.862	1.504	1.631	1.094	-828.	992.	17.0	14.597
2.00	0.6	0.2777	0.4440	0.2767	23.62	1.396	1.026	0.865	1.508	1.615	1.071	-828.	956.	17.0	14.598
2.00	0.7	0.2767	0.5142	0.2089	23.79	1.389	1.018	0.869	1.512	1.599	1.057	-828.	921.	17.0	14.569
2.00	0.8	0.2767	0.5838	0.1398	23.93	1.383	1.012	0.874	1.516	1.583	1.044	-828.	887.	17.0	14.506
2.00	0.9	0.2761	0.6537	0.0705	24.04	1.381	1.008	0.881	1.521	1.567	1.031	-828.	854.	17.0	14.460
2.00	1.0	0.2761	0.7243	0.	24.12	1.382	1.009	0.889	1.525	1.552	1.018	-828.	821.	17.0	14.422
3.00	0.	0.4177	0.	0.5823	24.58	1.376	1.099	0.832	1.467	1.673	1.140	-828.	1137.	17.6	16.820
3.00	0.1	0.4124	0.0694	0.5226	24.95	1.359	1.092	0.829	1.471	1.657	1.127	-828.	1089.	17.5	16.749
3.00	0.2	0.4077	0.1291	0.4634	24.83	1.359	1.078	0.828	1.477	1.642	1.114	-828.	1042.	17.5	16.694
3.00	0.3	0.4037	0.1914	0.4052	24.98	1.346	1.071	0.827	1.477	1.627	1.102	-828.	1029.	17.5	16.759
3.00	0.4	0.4003	0.2525	0.3475	25.31	1.334	1.062	0.827	1.481	1.613	1.089	-828.	996.	17.5	16.736
3.00	0.5	0.3975	0.3127	0.2901	25.52	1.325	1.053	0.829	1.483	1.603	1.076	-828.	963.	17.5	16.732
3.00	0.6	0.3952	0.3723	0.2326	25.71	1.317	1.046	0.832	1.486	1.584	1.064	-828.	932.	17.5	16.747
3.00	0.7	0.3935	0.4315	0.1754	25.87	1.312	1.041	0.835	1.490	1.570	1.054	-828.	901.	17.4	16.845

TEMPERATURE = 240. R

LIQUID MOLE FRACTION		VAPOR MOLE FRACTION			PRESSURE ATM	EQUIL CONST			RELATIVE VOL			ENTHALPY BTU/LB MOLE		HEAT CAPACITY BTU/LB MOLE-R	
N2	AR/AR+O2	N2	AR	O2		N2	AR	O2	N2/AR	N2/O2	AR/O2	LIQ	VAP	LIQ	VAP
0.	0.	0.	0.	1.0002	20.27	1.772	1.176	1.000	1.507	1.772	1.176	-744.	1209.	17.0	12.779
0.1	0.	0.	0.1146	0.8862	20.78	1.723	1.140	0.985	1.512	1.750	1.158	-749.	1207.	17.0	12.763
0.2	0.	0.	0.2219	0.7784	21.26	1.682	1.109	0.973	1.517	1.729	1.140	-753.	1149.	16.9	12.785
0.3	0.	0.	0.3249	0.6754	21.68	1.648	1.083	0.965	1.521	1.708	1.122	-757.	1093.	16.9	12.778
0.4	0.	0.	0.4244	0.5780	22.03	1.616	1.063	0.965	1.526	1.687	1.105	-761.	1040.	16.9	12.778
0.5	0.	0.	0.5214	0.4790	22.34	1.594	1.043	0.960	1.531	1.667	1.088	-765.	990.	16.9	12.760
0.6	0.	0.	0.6168	0.3836	22.61	1.579	1.028	0.959	1.536	1.646	1.072	-769.	941.	16.9	12.633
0.7	0.	0.	0.7115	0.2889	22.82	1.566	1.018	0.963	1.541	1.627	1.054	-773.	893.	16.8	12.524
0.8	0.	0.	0.8065	0.1939	23.00	1.558	1.008	0.970	1.546	1.607	1.036	-777.	847.	16.8	12.374
0.9	0.	0.	0.9025	0.0979	23.16	1.555	1.003	0.979	1.550	1.588	1.018	-781.	801.	16.8	12.211
1.0	1.0	0.	1.0002	0.	23.18	1.556	1.000	0.991	1.555	1.569	1.000	-785.	756.	16.8	12.040
0.25	0.	0.0432	0.	0.9568	20.87	1.729	1.158	0.982	1.503	1.760	1.132	-720.	1290.	17.1	13.111
0.25	0.1	0.0421	0.1089	0.8492	21.27	1.685	1.117	0.968	1.508	1.741	1.114	-724.	1240.	17.1	13.139
0.25	0.2	0.0412	0.2123	0.7466	21.62	1.647	1.089	0.958	1.513	1.721	1.137	-727.	1191.	17.0	13.163
0.25	0.3	0.0404	0.3113	0.6487	21.92	1.615	1.064	0.950	1.518	1.700	1.120	-731.	1144.	17.0	13.177
0.25	0.4	0.0397	0.4071	0.5536	22.17	1.589	1.044	0.946	1.522	1.679	1.103	-734.	1098.	17.0	13.173
0.25	0.5	0.0390	0.5006	0.4605	22.46	1.568	1.023	0.946	1.527	1.659	1.087	-738.	1054.	17.0	13.146
0.25	0.6	0.0388	0.5927	0.3692	22.71	1.552	1.013	0.946	1.532	1.640	1.071	-742.	1011.	16.9	13.080
0.25	0.7	0.0385	0.6841	0.2779	22.95	1.540	1.002	0.950	1.536	1.621	1.054	-746.	969.	16.9	12.994
0.25	0.8	0.0383	0.7754	0.1868	23.16	1.532	0.994	0.956	1.541	1.602	1.038	-750.	929.	16.9	12.854
0.25	0.9	0.0382	0.8679	0.0941	23.34	1.529	0.989	0.965	1.546	1.583	1.029	-754.	890.	16.9	12.672
0.25	1.0	0.0382	0.9622	0.	23.51	1.530	0.987	0.977	1.550	1.565</					

BIBLIOGRAPHY FROM LITERATURE SEARCH

A. Vapor-Liquid Equilibrium Data Nitrogen-Oxygen System

1. Air Products and Chemicals, Inc., Allentown, Pa., Brewer, J., Tech. Documentary Rept. No. ASD-TR-61-625 (1961).
General thermodynamic data on oxygen and nitrogen.
2. Armstrong, G. T., Goldstein, J. M., and Roberts, D. E., J. Res. Nat. Bur. Stds., 55, 265 (1955).
Data below atmospheric pressure.
3. Baly, E. C. C., Proc. Phys. Soc. (London), 17, 157 (1900).
Data at atmospheric pressure.
4. Cockett, A. H., Proc. Roy. Soc. (London), 239, 76 (1957).
Data at about 1.3 atmospheres.
5. Dana, L. I. and Zenner, G. H., Chemical Eng. Progr. Symposium Ser. No. 44, 49, 36 (1963).
Oxygen-nitrogen system.
6. Din, F., Trans. Faraday Soc., 56, 668 (1960).
Data from 1 to 10 atmospheres.
7. Din, F., Bull. Ir., 33, 17 (1953).
Data from 1 to 10 atmospheres.
8. Dodge, B. F. and Dunbar, A. K., J. Amer. Chem. Soc., 49, 591 (1927).
Data from 1 to 30 atmospheres.
9. Inglis, J. K. H., Phil. Mag., 11, 640 (1906).
Data below atmospheric pressure.
10. Kuenen, J. P., Verschoyle, T. and Van Urk, A. Th., Comm. Phys. Lab. Leiden, No. 161, Nov. 1922.
Data from 32 to 46 atmospheres.
11. Pcol, R. A. H., Saville, G., Herrington, T. M., et al, Trans. Faraday Soc., 58, 1692 (1962).
Data at 151°R.
12. Sagenkahn, M. L. and Fink, H. L., O.S.R.D. 4493, PB 9383 (1944).
Data from 0.5 to 2 atmospheres.
13. Seemeyer, D., Diplomarbeit Universitat Gottingen (1963).
Data at 77.5°K
14. Thorogood, R. M. and Haselden, G. G., Brit. Chem. Eng., 8, 623 (1963).
Data near 1 atmosphere.
15. Weishaupt, J., Angew. Chem., B20, 321 (1948).
Data at 1.3 atmosphere.

16. Wilhelm, G. and Schneider, G., Zeit. Physik. Chem. Neue Folge, 29, 43 (1961).
Data at 139.5°R.
17. Yendall, E. F. and Olszewski, W. J., A.S.D. Tech. Rept. 61-536 (1961).
Data from 1.5 to 6 atmospheres.

B. Vapor-Liquid Equilibrium Data Nitrogen-Argon System

1. Fastovskii, V. G. and Petrovskii, V. Yu., Zh. Fiz. Khim., 30, 76 (1956).
Data from 1 to 4 atmospheres.
2. Holst, G. and Hamburger, L., Z. Fur. Phys. Chem., 91, 513 (1916).
Data from 0.6 to 2 atmospheres.
3. Pool, R. A. H., Saville, G., Herrington, T. M., et al, Trans. Faraday Soc., 58, 1692 (1962).
Data at 151°R.
4. Seemeyer, D., Diplomarbeit Universitat Gottingen (1963).
Data at 78.5°K.
5. Weishaupt, J., Angew. Chem., B20, 321 (1948).
Data at 1.3 atmosphere.

C. Vapor-Liquid Equilibrium Data Argon-Oxygen System

1. Bourbo, P. and Ishkin, I., Physica, 3, 1067 (1936).
Data from 1 to 2 atmospheres.
2. Burn, I. and Din, F., Trans. Faraday Soc., 58, 1341 (1962).
Data from 1 to 10 atmospheres.
3. Clark, A. M., Din, F., and Robb, J., Proc. Roy. Soc. (London), 221A, 517 (1954).
Data from 1 to 7 atmospheres.
4. Fastovskii, V. G. and Petrovskii, V. Yu., Zh. Fiz. Khim., 29, 1311 (1955).
Data from 1 to 2 atmospheres.
5. Inglis, J. K. H., Phil. Mag., 11, 640 (1906).
Data below 1 atmosphere.
6. Narinsky, G., Kislород, 10, 9 (1957).
Data from 1 to 12 atmospheres.
7. Pool, R. A. H., Saville, G., Herrington, T. M., et al, Trans. Faraday Soc., 58, 1692 (1962).
Data at 151°R and 161°R.

8. Sagenkahn, M. L. and Fink, H. L., O.S.R.D. 4403, PB 9383 (1944).
Data at 1 and 2 atmospheres.
9. Seemeyer, D., Diplomarbeit Universität Gottingen (1963).
Data at 86.0°K.
10. Wang, D. I. J., Advances in Cryogenic Engineering, 3, K. D. Timmerhaus
(ed.), Plenum Press, New York, 1960, p. 294.
11. Weishaupt, J., Angew. Chem., B20, 321 (1948).
Data at 1.3 atmospheres.

D. Vapor-Liquid Equilibrium Data Nitrogen-Argon-Oxygen Ternary System

1. Latimer, R. E., AICHE Journal 3, No. 1, 75 (1957).
Vapor-liquid nitrogen-argon-oxygen mixtures correlation.
2. Latimer, R. E., Linde Co. Rept. ADI 5032 (1957).
Vapor-liquid nitrogen-argon-oxygen mixtures correlation.
3. Sagenkahn, M. L. and Fink, H. L., O.S.R.D. 4493, PB 9383 (1944).
Data at 1 and 2 atmospheres.
4. Torochesnikov, N. S. and Ershova, T., J. Chem. Ind. (USSR), 17,
30 (1940).
Data at 162°R.
5. Weishaupt, J., Angew. Chem., B20, 321 (1948).
Data at 1.3 atmospheres.

E. Enthalpy Data

1. Alikhanov, R. A., J. Exper. Theor. Phys. U.S.S.R., 2, 771 (1956).
Latent heat of oxygen 80 to 106°K.
2. Alt, H., Ann. d. Physik, 19, 739 (1906).
Latent heat of oxygen and nitrogen.
3. Barshall, H., Z. Elektrochem, 17:9, 345 (1911).
Oxygen latent heat.
4. Boeing Co., Seattle, Wash., Arave, R. J. and Huseby, O. A., Boeing Co.
Document No. D2-11238 (1962).
Thermodynamic properties of argon.
5. Claitor, L. C. and Crawford, D. B., Trans. ASME, 71, 885 (1949).
Latent heat of oxygen 70 to 90°K.
Latent heat of nitrogen 60 to 80°K.

6. Cornell Aeronautical Lab., Buffalo, N. Y., Treanor, C. E. and Logan, J. G. Jr., Rept. No. BE-1007-A-5 (1957). Nitrogen thermodynamic properties.
7. Dana, L. I., Proc. Am. Acad., 60, 241 (1925). Latent heat of oxygen-nitrogen mixtures at 1 atmosphere.
8. Din, F. (ed.), Thermodynamic Functions of Gases, 2, Butterworths Scientific Publications, London, 1956. Heat capacity of liquid argon, heat capacity of saturated argon, latent heat of argon, heat capacity of argon vapor, temperature-entropy diagram for argon.
9. Din, F., Bull. IIR Annexe 1960-1, p. 279. Enthalpy of nitrogen and oxygen mixtures.
10. Duclaux, J., J. Chim. Phys., 50, No. 10, 512 (1953). Nitrogen latent heat.
11. Euken, A., Verhandl. deut. Physik Ges., 18, 4 (1916). Latent heat and specific heat of oxygen and nitrogen.
12. Flubacher, P., Leadbetter, A. J., and Morrison, J. A., Proc. Physical Soc. (London) 78, 1449 (1961). Heat capacity of solid and liquid argon, vapor pressure of solid and liquid argon, heats of vaporization and fusion of argon.
13. Frank, A. and Clusius, K., Z. Physik. Chem. (Leipzig), B42, 395 (1939). Oxygen latent heat.
14. Furukawa, G. T. and McCoskey, R. E., National Advisory Committee for Aeronautics Technical Note 2969 (1953). Latent heats of air, oxygen, and nitrogen from 60°K to 90°K.
15. Georgia Inst. of Technology, Atlanta, Ga., Mullins, J. C., Ziegler, W. T., and Kirk, B. S., Tech. Rept. No. 2, Contr. No. CST-7339 (1962). Oxygen thermodynamic properties.
16. Giauque, W. F. and Clayton, J. O., J. Am. Chem. Soc., 55, 4875 (1933). Nitrogen heat capacity and latent heat.
17. Giauque, W. F. and Johnston, H. L., J. Am. Chem. Soc., 51, 2300 (1929). Heat capacity of liquid and solid oxygen, heats of fusion and vaporization.
18. Goff, J. A. and Gratch, S., Trans. ASME, 72, 741 (1950). Heat capacity of nitrogen at zero pressure.
19. Haettinger, G. C., Skinner, R. P. and Trentham, R. A., Advances in Cryogenic Engineering, 6, K. D. Timmerhaus (ed.), Plenum Press, New York, 1961, p. 354. Nitrogen latent heat.

20. Harasima, A., Proc. Phys. Math Soc. Japan, 23, 977 (1941).
Nitrogen and argon latent heat and surface energy.
21. Hilsenrath, J., Beckett, C. W., Benedict, W. S. et al, Nat. Bur. Stds. Circular 564, 132 (1955).
Heat capacity of argon at zero pressure.
22. Kassell, L. S. and Muskat, M., Phys. Rev., 40, 627 (1932).
Argon, nitrogen, oxygen latent heat.
23. Knobler, C. M., van Heijningen, R. J., and Beenakker, J. J. M., Physica, 27, 296 (1961).
Heat of mixing of oxygen-nitrogen, oxygen-argon.
24. Lee, J. F., Z. Angew. Math u. Phys., 4, 401 (1953).
Nitrogen and oxygen specific heat.
25. Mage, D. T., Jones, M. L. Jr., Katz, D. L., and Roebuck, J. R., Chem. Eng. Progr. Symposium Ser. No. 44, 59, 61 (1963).
26. Mathias, E., Crommelin, C. A., and Onnes, H. K., Ann. Phys., 19, 239 (1923).
Argon, nitrogen and oxygen latent heat and specific heat.
27. Michels, A., Levelt, J. M. and Wolkers, G. J., Physica, 24, 769 (1958).
Argon thermodynamic properties.
28. Pool, R. A. H., Saville, G., Herrington, T. M., et al, Trans. Faraday Soc., 58, 1692 (1962).
Heat of mixing of argon-oxygen, argon-nitrogen. Volume of mixing of argon-oxygen, oxygen-nitrogen, argon-nitrogen.
29. Rykov, V. I., J. Phys. Chem. U.S.S.R., 34:8, 881 (1960).
Argon and nitrogen latent heat.
30. Shearer, J. S., Phys. Rev., 17, 469 (1903).
Latent heat of nitrogen, oxygen, and air.
31. Strobridge, T. R., NBS Technical Note 129 (1962).
Latent heat, saturated liquid specific heat, and a complete thermodynamic chart for nitrogen.
32. "The Compendium", Johnson, V. J. (ed.), WADD Tech. Rpt. 60-56 (1961).
Specific heat of liquid argon, latent heat of oxygen.
33. Theoretical Chemistry Lab, Univ. Wisconsin, Madison, Wis., Levelt, J.M.H., Rept. No. WIS-OOR-24 Series 5 (1959).
Argon thermodynamic properties.
34. Voronel, A. V., Zhur. Tekh. Fiz., 29, 304 (1959).
Argon, nitrogen and oxygen latent heat.

35. Whalley, E., Can. J. Technol., 33, No. 2, 111 (1955).
Argon thermodynamic properties.
36. Wilbers, O. J., Part II, Vol. I of ASD TR 61-699 (1961).
Correlation of latent heat of oxygen-nitrogen mixtures vs. temperature.
37. Wooley, H. W., J. Res. Nat. Bur. Stds., 40, 163 (1948).
Heat capacity of oxygen at zero pressure.
38. Wooley, H. W., Natl. Advisory Comm. Aeronautics Tech. Note
No. NACA TN 3271 (1956).
Nitrogen thermodynamic properties.
39. Yendall, E. F. and Olszewski, W. J., A.S.D. Technical Report 61-536,
Sept. 1961.
Latent heat of oxygen-nitrogen mixtures.
40. Z. Elektrochem., 58, 424 (1954).
Oxygen and argon latent heat.

F. Pressure-Volume-Temperature Data for Gaseous Mixtures of N₂-O₂-Ar
(including air) used in Checking the Virial Coefficients

1. Air Conditioning, Heating, and Ventilating, 59, No. 11, 85 (1962).
Air data.
2. Air Products and Chemicals, Inc., Allentown, Pa., Brewer, J.,
Tech. Documentary Report No. ASD-TR-61-625 (1961).
Air, nitrogen, oxygen data.
3. Amagat, E. H., Ann. Chim. et. Phys., 29, 68 (1893).
Air, nitrogen, oxygen data.
4. Amagat, E. H., Ann. Chim. et. Phys., 28, 464 (1883).
Air data: 1 to 8 atmospheres and 20° to 300°C.
5. Amagat, E. H., Ann. Chim. et. Phys., 19, 345 (1880).
Air, nitrogen, oxygen data.
6. Baehr, H. D. and Schweir, K., Springer-Verlag, Berlin-Wilmersdorf,
Heidelberger Platz 3 (1961).
Air data: -418°F to +2282°F, 1 to 4500 atmospheres.
7. Beattie, J. A. and Ikehara, S., Proc. Am. Acad. Arts Sci., 64,
127 (1930).
Binary PVT data.

8. Beenakker, J. J. M., Knaap, H. F. P. and Knobler, C. M., Bull. Inst. Intern. Froid Annexe 1960-1, 163 (1960).
Volume of liquid mixing of O_2 -A and O_2 - N_2 .
Heats of liquid mixing of O_2 -A and O_2 - N_2 .
9. Benedict, W. S., Nat. Bur. Stds. Heat and Power Division, Table 2.20 (1949).
Air data.
10. Bernardes, N., Phys. Rev., 112, 1534 (1958).
Equation of state of solid argon.
11. Boato, G. and Casanova, G., Physica, 27, 571 (1961).
Argon Lennard-Jones potential.
12. Brillantinov, N. A., Zhur. Tekh. Fiz., 18, 1113 (1948).
Joule-Thomson coefficients of air and oxygen.
13. Dascalescu, A., Rev. Chim. (Bucharest), 2, No. 1, 12 (1956).
Thermodynamic diagrams of air, nitrogen, oxygen.
14. Din, F. (ed.), Thermodynamic Functions of Gases Vol. 2, London, Butterworths Scientific Publications, 1956.
Air and argon data.
15. Feigenbutz, L. V. and Solum, E., Gen. Dynamics Corp., Convair Div., Rept. ERR-SD-005 (1960).
Pressure-enthalpy diagram for air.
16. Friedman, A. S., J. Res. Nat. Bur. Stds., 58, No. 2, 93 (1957).
Virial coefficients of air, nitrogen, oxygen, N_2 - O_2 mixture.
17. Grabau, M., Arnold Eng. Develop. Center Tech. Note No. 59-102 (1959).
Air data.
18. Gratch, S., Trans. ASME, 70, 631 (1948).
Nitrogen, oxygen, argon, and air vapor pressure, density and PVT data.
19. Guggenheim, E. A. and McGlashan, M. L., Proc. Roy. Soc. (London) A206, 448 (1951).
Virial coefficients for ternary mixtures.
20. Hall, N. A. and Ibele, W. E., Trans. ASME, 76, 1039 (1954).
Air, nitrogen, oxygen data.
21. Hall, N. A. and Ibele, W. E., Minn. Univ. Eng. Expt. Sta., Tech. Paper No. 85 (1951).
Air, nitrogen, oxygen data.

22. Harris, I. and Jastrow, R., Science, 128, 420 (1958).
Density of upper atmosphere.
23. Hilsenrath, J., Beckett, C. W., Benedict, W. S. et al, Nat. Bur. Stds. Circular 564 (1955).
Argon data.
24. Holborn, L. and Otto, J., Z. Physik, 33, 1 (1925).
Air, argon, nitrogen data: -183°C to 400°C .
25. Holborn, L. and Otto, J., Z. Physik, 23, 77 (1924).
Air, argon data to 400°C .
26. Holborn, L., Scheel, K., and Henning, F., Warmetabellen, Vieweg and Sohn, Braunschweig, Germany (1919).
Tables of PVT data on air, argon, oxygen.
27. Humphrey, R. L. and Neel, C. A., Arnold Eng. Development Center Rept. No. AEDC-TN-61-103 (1961).
Air data 90 to 1500°K .
28. Ishkin, I. P. and Kaganer, M. G., Soviet Phys. JETP, 1, 2263 (1956).
Thermodynamic diagrams for air and nitrogen.
29. Kallmann, H. K., Rand Corp. Rept. No. RM-442 (1950).
Equations of state.
30. Kamerlingh Onnes, H. and G. Crommelin, Comm. Lab. Leiden, 118, b (1910).
31. Kamerlingh Onnes, H. and H. W. Van Urk, Comm. Lab. Leiden, 169, d,e, (1924).
32. Kazarnovskii, Ya. S. and Sidorov, I. P., Zhur. Fiz. Khim., 21, No. 11, 1363 (1947).
Oxygen, nitrogen, and binary data.
33. Kuenen, J. P., Verschoyle, T., and Van Urk, A. Th., Comm. Phys. Lab. Leiden, No. 161, Nov. 1922.
Oxygen-nitrogen binary data.
34. Kuypers, H. A. and H. Kamerlingh Onnes, Arch. Neerlandaises, 6, 277 (1923).
35. Landsbaum, E. M., Dodds, W. S., Stevens, W. F. and Sollami, B. J., AIChE Journal, 1, 302 (1955).
Air data.
36. Mason, I. and Dolley, L. G. F., Proc. Roy. Soc. (London) A103, 524 (1923).
Argon-oxygen mixture data.
37. Michels, A., R. J. Lunbeck, G. J. Wolkers, Physica, 17, 801 (1951).
Thermodynamic properties of argon.

38. Michels, A., Wassenaar, T., Levelt, J. M. and DeGraff, W., Appl. Sci. Res., A4, No. 5-6, 381 (1954).
Air data and virial coefficients.
39. Michels, A., H. Wijker, and H. K. Wijker, Physica, 15, 627 (1949).
PVT data of argon.
40. Michels, A., H. Wouters, and J. deBoer, Physica, 1, 587 (1934).
P-V isotherms of nitrogen.
41. Naval Ordnance Lab, White Oak, Md., Price, D., NAVORD Report No. 5784
(1958).
Nitrogen pressure-volume data.
42. Nelson, L. C. and Obert, E. F., Trans. ASME, 76, 1057 (1954).
Generalized P-V-T properties.
43. Nijhoff, G. P. and W. H. Keesom, Comm. Lab. Leiden, 179, b (1925).
44. Otto, J., A. Michels, and H. Wouters, Phys. Zeit., 35, 97 (1934).
P-V isotherms of nitrogen.
45. Palmatier, E. P., (paper presented at ASHRAE Meeting, New York,
N. Y., February, 1963).
"Construction of the Normal Temperature ASHRAE Psychrometric Chart".
46. Penning, F. M., Comm. Phys. Lab. Leiden, No. 166 (1923).
47. Pickering, S. F., Nat. Bur. Stds. Misc. Publ. No. 71 (1925).
Air, argon, nitrogen, oxygen data.
48. Prausnitz, J. M. and Myers, A. L., AIChE Journal, 9, 5 (1963).
Virial coefficients of argon, nitrogen, oxygen, binary mixtures.
49. Randall, R. E., Arnold Eng. Develop. Center Rept. No. TR-57-8 (1957).
Air data.
50. Rocket Propulsion Establishment (Great Britain), Ricketson, B. W. A.,
RPE Technical Memo No. 249 (1962).
Liquid oxygen density.
51. Rogovaya, I. A. and Kaganer, M. G., Zhur. Fiz. Khim., 34, 1932 (1960).
Air, argon, oxygen data.
52. Tanner, C. C. and I. Masson, Proc. Roy. Soc. A, 126, (1930).
Compressibilities of argon, helium, hydrogen, and binary mixtures.
53. "The Compendium", Johnson, V. J. (ed.), WADD Tech. Rept. 6056 (1961).
General data.
54. Timrot, D. L. and Borisoglebskiy, V. P., Teploenergetika, 10, 95 (1960).
Liquid oxygen density.
55. Verschoyle, A. Th. , Proc. Roy. Soc. A, 111, 5-2 (1926).
P-V isotherms of H₂, of N₂, and of H₂-N₂ mixtures.

G. Vapor Pressure

1. Aoyama, S. I. and Kanda, E., Sci. Rents. Tohoku Univ. First Ser. 23:4, 107 (1935).
Oxygen and nitrogen vapor pressure.
2. Aoyama, S. I. and Kanda, E., J. Chem. Soc. Japan, 55, 22 (1934).
Oxygen and nitrogen vapor pressure.
3. Armstrong, G. T., J. Research Nat. Bur. Stds., 53:4, 263 (1954).
Nitrogen vapor pressure.
4. Boato, G., Casanova, G., Scholes, G., et al, Nuovo cimento, 20:1, 87 (1961).
Argon vapor pressure.
5. Boato, G., Casanova, G., and Vallauri, M. E., Nuovo cimento, 16:3, 505 (1960).
Argon vapor pressure.
6. Bulle, F., Physik. Z., 14, 860 (1913).
Oxygen vapor pressure.
7. Cath, P. G., Comm. Phys. Lab. Leiden No. 152d, 45 (1918).
Nitrogen and oxygen vapor pressure.
8. Clusius, K., Endtinger, F., and Schleich, K., Helv. Chim. Acta, 44:13, 98 (1961).
9. Dodge, B. F. and Davis, H. N., J. Amer. Chem. Soc., 49, 610 (1927).
Oxygen and nitrogen vapor pressure.
10. Estrelcher, T., Phil. Mag., 40, 454 (1895).
Oxygen vapor pressure.
11. Fieschi, R. and Terzi, N., Physica, 27, 453 (1961).
Argon vapor pressure.
12. Friedman, A. S. and White, D., J. Am. Chem. Soc., 72, 3931 (1950).
Nitrogen vapor pressure.
13. Georgia Inst. of Technology, Atlanta, Ga., Ziegler, W. T., Mullins, J. C., and Kirk, B. S., Tech. Rep. No. 2, Contr. No. CST-7238 (1962).
Argon vapor pressure and latent heat.
14. Germann, F. E. E., Physik. Z., 14, 857 (1913).
Oxygen vapor pressure and density.
15. Henning, M. F. and Otto, J., Physik Z. 37:18, 633 (1936).
Oxygen and nitrogen vapor pressure.
16. Hoge, H. J., J. Res. Nat. Bur. Stds., 44, 321 (1950).
Oxygen vapor pressure and specific heat.

17. Hoge, H. J., The NBS-NACA Tables of Thermal Properties of Gases, Table 9.50 (1949).
Oxygen vapor pressure.
18. Hoge, H. J., The NBS-NACA Tables of Thermal Properties of Gases, Table 19.50 (1950).
Argon vapor pressure.
19. Holst, G., Comm. Phys. Lab. Leiden No. 148a (1915).
Oxygen and nitrogen vapor pressure.
20. Honig, R. E. and Hook, H. O., RCA Rev., 21, 360 (1960).
Argon, oxygen, nitrogen vapor pressure.
21. Johns, T. F., Atomic Energy Research Establ. (Great Britain) GP/R 2166 (1957).
Oxygen vapor pressure.
22. Keesom, W. H. and Bijl, A., Physica, 4, 305 (1937).
Nitrogen vapor pressure.
23. Kelley, K. K., U. S. Bur. Mines Bull. 383 (1935).
Argon, oxygen, and nitrogen vapor pressure and latent heat.
24. Kirshenbaum, I., J. Chem. Phys., 10, 717 (1942).
Nitrogen vapor pressure.
25. Koch, H. A. Jr. and Williams, V. C., Chem. Eng. Progr., 43, No. 11, 623 (1947).
Nitrogen and oxygen vapor pressure.
26. Mathias, E. and Crommelin, C. A., Proc. Intern. Congr. Refrig., 4, London, 89 (1924).
Argon vapor pressure and latent heat.
27. Michels, A. Wassenaar, T., DeGraaff, W., and Prins, C., Physica, 19, 26 (1953).
Nitrogen vapor pressure.
28. Onnes, H. K. and Braak, C., Comm. Phys. Lab. Leiden No. 107a (1908).
Oxygen vapor pressure.
29. Onnes, H. K., Dorsman, C., and Holst, G., Comm. Phys. Lab Leiden No. 145b (1915).
Oxygen vapor pressure and critical point, nitrogen critical point.
30. Pitzer, K. S., Lippmann, D. Z. et al, J. Am. Chem. Soc., 77, 3433 (1955).
Argon and nitrogen vapor pressure.
31. Porter, F. and Perry, J. H., J. Am. Chem. Soc., 48, 2059 (1926).
Nitrogen vapor pressure.
32. Stock, A., Henning, F. and Kuss, E., Ber. deut. chem. Ges., B54, 1119 (1921).
Oxygen vapor pressure.

H. Miscellaneous References

1. Aerojet-General Corporation, Azuza, Calif., Gross, E., Report No. 0694-01-2 (1963).
Cooling techniques.
2. Aerojet-General Corp., Azuza, Calif., Technical Operating Report No. 13 (1963).
Decomposition, combustion, and detonation of solids.
3. Aeronautical Research Council (Great Britain), Bernstein, L., Rept. No. 22778-173 (1961).
Thermodynamics of shock waves.
4. Air Products, Inc., Allentown, Pa., Ent, W. L., Suppl. to Summary Progr. Rept. No. 4 (1960), Contract No. AF 33(616)-6730.
Analysis of liquid oxygen.
5. Allis-Chalmers Mfg. Co., Milwaukee, Wis., Quarterly Technical Progress Rept. No. 1, AD-282 178 (1962).
Design of fuel cell.
6. Ansley, S. P., Jr., Arnold Engineering Development Center TDR 62-201, (1963).
Space simulation test cell.
7. Bagrov, M. M., Ukr. Fiz. Zhur., 6:4, 486 (1961).
Diffusion of nitrogen in liquid oxygen.
8. Baldini, G., Phys. Rev., 128:4, 1562 (1962).
Ultraviolet absorption of argon.
9. Balwanz, W. W., Singer, J. M., and Frandsen, N. P., Advances in Cryogenic Engineering, 6, K. D. Timmerhaus (ed.), Plenum Press, New York, 1961, p. 195.
Vacuum pumping cryogenic fluids.
10. Bell Aerosystems Co., Buffalo, N. Y., Quinones, J. J. and Misercola, A. B., Rept. No. BLR 62-22 (c), Rev. A (1963).
Propellant physical properties.
11. Brown, G. M. and Stutzman, L. F., Chem. Eng. Prog., 45:2, 142 (1949).
Equilibrium constants for nitrogen, methane, and ethane.
12. Chelton, D. B. and Mann, D. B., WADC Tech. Rept. 59-8 (1959).
General data.

13. Clusius, K. and Konnertz, F., Z. Naturforsch., 4a:2, 117 (1949).
Oxygen latent heat.
14. Colorado Univ., Boulder, Colo., Contract AF 33(657)8512 (1962-3).
Thermodynamic properties of solutions of liquefied light gases.
15. Cosmodyne Corp., Hawthorne, Calif., Rept. No. CE-78-R (1961).
Cryogenic sampler design.
16. Cryovac Inc., Columbus, O., Hood, C. B. Jr., Vogelhuber, W. W.
and Barron, R. F., AEDC TDR 63-71 (1963).
Refrigeration systems for 88°K and 20°K.
17. Davis, W. J., M.S. Thesis University Utah (1961).
Thermal conductivity of liquids.
18. Defense Metals Information Center, Columbus, O., Paprocki, S. J.,
Hodge, E. S., and Gripshover, P. J., Report No. 159 (1961).
Welding.
19. Electro-Optical Systems Inc., Pasadena, Calif., Jordan, C. B.,
EOS Report 1650-4M-2 (1961).
Quenching beryllium alloys.
20. Electro-Optical Systems, Inc., Pasadena, Calif., Menetrey, W. R.
and Chrisney, J., WADD TR 60-699, Vol. 6 (1960).
Energy conversion handbook.
21. Florio, F. A., Air Crew Equipment Lab, Naval Air Material Center,
Philadelphia, Pa., Rept. No. 439 (1960).
Technique of dewar filling.
22. Frank, A., Chem. Ing. Tech., 32, 330 (1960).
Distillation of nitrogen-oxygen binary.
23. General Atomic Div., General Dynamics Corp., San Diego, Calif.,
Stewart, J. C. and Pyatt, K. D. Jr., Rept. No. GA-25 28, Vol. 1
(1961).
Optical properties of nitrogen.
24. General Dynamics/Astronautics, San Diego, Calif., Brittain, H.,
IDEP Rept. No. 404.10.70.20-D5-03 (1962).
Liquid oxygen topping line.
25. General Dynamics/Convair, San Diego, Calif., Faymon, K. A.,
Rept. No. ZR-659-018 (1959).
Shock wave studies.
26. General Electric Co., Schenectady, N. Y., Holkeboer, D. H. and
Santeler, D. J., AEDC TDR 63-37 (1963).
A modified ion gauge.

27. Golovintsov, A. G., Stolper, M. B., and Arkharov, A. M., Khim. Mashin., 5, 17 (1962).
Production scheme for liquid oxygen.
28. Hersh, C. K., Progress in Astronautics and Rocketry, 2, Academic Press, Inc., New York, 1960, p. 427.
Oxygen properties.
29. Must, J. G., Wallace, L. D., et al, Nat. Bur. Stds. Tech. Note No. 137 (1962).
Bibliography of the properties of oxygen.
30. Inglewood Lab, Thompson Products Inc., Inglewood, Calif., Findl, E., Brande, H., and Edwards, H., WADD TR 60-767 (1958).
Properties of aviation and rocket fuels.
31. Jet Propulsion Lab, Pasadena, Calif., Harrje, D. T., Memo 20-138 (1956).
Liquid oxygen boil-off.
32. Jones, G. O. and Walker, P. A., Conference de Physique des Basses Temperatures, Paris (Sept. 1955).
Data on liquid argon.
33. Keesom, W. H., Physik Ber., 4, 613 (1923).
Triple point and critical point of argon, oxygen and nitrogen.
34. M. W. Kellogg Co., New York, N. Y., Lobo, W. E., Final Report OSRD No. 4206 (1944).
Data on air separation.
35. Kirby, W. G., Arnold Engineering Development Center TDR 63-28 (1963).
Cryopumping studies.
36. Larsen, P. S., Clark, J. A., Randolph, W. O., and Vaniman, J. L., Advances in Cryogenic Engineering, 8, K. D. Timmerhaus (ed.), Plenum Press, New York (1963), p. 507.
Cooling cryogenic liquids.
37. Leefe, S. and Liebson, M., Rev. Sci. Ins., 31, 1353 (1960).
"Leveling System for Liquid Nitrogen".
38. Lewis, A. D. and Arney, G. D. Jr., Arnold Engineering Development Center TDR 63-31 (1963).
Flow through nozzles.
39. Liquid Propellant Information Agency, "The Handling and Storage of Liquid Propellants", Applied Physics Lab, John Hopkins Univ., Silver Springs, Md. (1961).

40. Little, Arthur D. Inc., Cambridge, Mass., Adkins, A. W., Black, I. A., et al, AFPTC TR 61-18 (1961).
Handling of hydrogen.
41. Little, Arthur D., Inc., Wiederhorn, N. M., Surprenant, N. F., and Leffler, A. J., Rept. No. C-63825 (1961).
Separation of air by chemical methods.
42. Lockheed Aircraft Corp., Marietta, Ga., Final Rept. ER-52r6, SSD-TR-61-21 (1961).
Tank pressurization of liquid propellants.
43. Lockheed Aircraft Corp., Sunnyvale, Calif., Churchill, D. R., Hagstrom, S. A. et al, Rept. No. 2-57-62-2 (1962).
Spectral absorption coefficient of air.
44. Long, H. M. and DiPaolo, F. S., Bull. IIR Annexe 1958-1, 253.
"The Condensed-Phase Diagram of the Ternary System Oxygen-Nitrogen-Argon.
45. Louisiana State U., Baton Rouge, La., Deck, R. J., Grenier, C. G., and Reynolds, J. M., AD-299 975 (1963).
Electrical effects in cold zinc.
46. Lummus Co., N. Y., Contract No. Bs-86746 (1962).
Hydrogen generation plant.
47. Martin-Marietta Corp., Baltimore, Md., Hildum, J. S., Jacobs, J. A. H., and Allen, R. J., Report No. ER 12518 (1962).
Electronic instrumentation at -320°F .
48. Matheson Co., East Rutherford, N. J., Matheson Gas Data Book (1961).
General data.
49. McCormick, J. E., Rome Air Development Center TN 61-54 (1961).
Thermoelectric cooling.
50. Mellon Inst., Pittsburgh, Pa., Klug, H. P. and Sears, D. R., AD-275 596 (1962).
Solidified rare gases.
51. Metcalf Research Lab, Brown U., Providence R. I., Flynn, G. P., Hanks, R. V., et al, Proj. Squid Technical Report No. BRN-3-P (1962).
Viscosity of cold gases.
52. Missile Div., Chrysler Corp., Detroit, Mich., Flora, C. L., Technical Memo No. ML-M5 (1954).
Handling technique for liquid oxygen, nitrogen.

53. Nason, W. C. Jr., MIT Rept. Aero. Medical Lab., Contract W33-038 AC-2031 (1947).
Air and components physical properties.
54. Naval Research Lab, Washington, D. C., Minter, C. C., Rept. No. 5907 (1963).
Thermal conductivity, pressure effect.
55. Nikolayev, B. A., Air Force Systems Command Trans. No. FTD-TT-62-271 (1962).
Calculations for rocket engines.
56. Noeggerath, W. C., Air Material Command Tech. Rept. No. F-TR2191-ND (1948).
Rating liquid rocket propellants.
57. North Carolina U., Chapel Hill, N. C., Rice, O. K., Contract N7onr-28407 (1957).
Liquid helium.
58. Office of Naval Research, London, Guthrie, A. H. Technical Rept. No. ONRL C-16-61 (1961).
"London Meeting of Commission I of the Institut International du Froid".
59. Olin Mathieson Chemical Corp., New Haven, Conn., Martinez, F., Wojtowicz, J. A., and Smith, H. D., AFOSR/DRA 61-7 (1961).
Superoxidizers.
60. Omar, M. H., Ph.D. Thesis Leiden Univ. (1962).
Phase Equilibria of some Binary Systems.
61. Pawlikowski, S. and Plesniak, S., Prez. Chem., 41:1, 27 (1962).
Condenser for air plant.
62. Pings, C. J. and Paalman, H. H., Molec. Phys., 5, No. 5, 531 (1962).
Liquid nitrogen structure.
63. Princeton Univ., Princeton, N. J., Grey, J. and Jacobs, P. F., Princeton University Aeronautical Engineering Lab. Rept. No. 602 (1962).
Measurement of high temperatures.
64. Rensselaer Polytechnic Inst., Troy, N. Y., Lenel, F. V. Regitz, L. J., and Hulsizer, W. R., AROD Rept. No. 2530:1 (1962).
Solid solutions of oxygen in Columbium.
65. Rocket Propulsion Establishment (Great Britain), Coy, J. D. C. and Ricketson, B. W. A., Technical Note No. 209 (1961).
Cryopumping.

66. Ruhemann, M., Physik Z. Sovietunion, 16, 67 (1936).
"Equilibrium Curves of Low Melting Mixtures".
67. St. Pierre, C. and Chi Tien, Can. J. Chem. Eng., 39, 170 (1961).
Estimating latent heats.
68. Science & Tech. Section, Air Information Division, Washington,
D. C., AID Rept. No. 60-103 (1960).
"Physical Constants of Liquid Ozone".
69. Southwest Research Institute, San Antonio, Tex., Baber, B. B.,
Burton, R. A., et al, Interim Rept. on Aerospace Lubricants (1962).
Compatibility of lubricants with LOX.
70. Southwest Research Institute, San Antonio, Texas, Weatherford, W. D.,
Tyler, J. C., and Ku., P. M., WADD TR 61-96 (1961).
Argon as a coolant for space applications.
71. Space Sciences Lab, General Electric Co., Philadelphia, Pa.,
Lenard, M., Document No. R62SD 985 (1962).
Composition of high temperature air.
72. Tempelmeyer, K. E. and Dicks, J. B., Arnold Engineering Development
Center TDR 62-88 (1962).
Argon plasma.
73. Timrot, D. L. and Borisoglebskiy, V. P., Tenloenergetika, 10, 95
(1960).
Liquid oxygen density.
74. Torocheshnikov, N. S. and Gurevich, Ts. N., Zhur. Khim. Prom.,
18:5, 7 (1941).
Gas liquefaction.
75. Vedenyev, V. I., Priroda, 12, 10 (1960).
Research on free radicals.
76. Walsh, T. J., Hibbard, R. R., and Ordin, P. M., National Advisory
Committee for Aeronautics Research Memo - RM E58A03a (1958).
Liquid oxygen pressurization.
77. Washington U., Seattle, Wash., Volk, H. and Halsey, G. D. Jr.,
Contract AF 49(638)723 (1960).
Solubility of hydrogen.
78. Washington U., Seattle, Wash., Yunker, W. H. and Halsey, G. D. Jr.,
AFOSR TN 59-1210 (1960).
Xenon-argon system.

79. Weedman, J. A. and Dodge, B. F., Ind. Eng. Chem., 39, 732 (1947).
Rectification of liquid air.
80. Wengrow, H. R., Florida U., Engineering and Industrial Experiment Station, Gainesville, Fla., Summary Rept. No. 7 on Fuel Cells (1963).
Oxygen transport in a fuel cell.
81. Whittaker Controls, Div. of Telecomputing Corp., Los Angeles, Calif., Revised ed. 1960.
Helium data.
82. Wooley, H. W., Natl. Advisory Comm. Aeronautics Tech. Note No. NACA TN 3271 (1956).
Nitrogen thermodynamic properties.
83. Wyle Labs Inc., ElSegundo, Calif., Pearson, D. B. and Boylan, W. H., et al, AD-298 780 (1962).
Design of cryogenic flowmeters.
84. Z. Elektrochem., 58, 424 (1954).
Oxygen and argon latent heat.

APPENDIX IV

NOMENCLATURE TABLE

A_i	=	Area of Chromatograph Peak, Section IV-B
A_{ij}	=	Binary interaction coefficient, Section VI-E
Ar	=	Argon
a_{ij}	=	Constant in binary interaction coefficient, Section VI-E and Section VIII
B	=	Second virial coefficient, Section VI-D and Section VIII-D
B_{ij}	=	Mixture second virial coefficient, Section VI-D
b_{ij}	=	Constant in binary interaction coefficient, Section VI-E and Section VII
C	=	Third virial coefficient, Section VI-D and Section VIII-D
C_{ijkl}	=	Mixture third virial coefficient, Section VI-D
C_p	=	Heat capacity at constant pressure
C_s	=	Heat capacity of saturated fluid
c	=	Number of components, Section VI-A
F	=	Degrees of freedom of system, Section VI-A
$^{\circ}F$	=	Degrees, Fahrenheit scale
f_i	=	Fugacity of component i
f_i^*	=	Fugacity of pure liquid component at the pressure and temperature of mixing
G^E	=	Excess free energy
G_i	=	Free energy of component i
H	=	Enthalpy
H_{gi}	=	Enthalpy of the real gas, pure component
h_{gi}°	=	Enthalpy of the real liquid, pure component

NOMENCLATURE TABLE (continued)

h_i^*	=	Ideal gas (zero pressure) enthalpy
$H_{liq.}$	=	Liquid phase enthalpy
h_m	=	Heat of mixing
$h_{vap.}$	=	Vapor phase enthalpy
K	=	Equilibrium constant, Appendix I-A
N_2	=	Nitrogen
O_2	=	Oxygen
P	=	Number of phases, Section VI-A
p	=	Total pressure of the vapor
p_i^o	=	Vapor pressure of pure component i
p_m	=	Pressure of mixing
q_i	=	Relative response factor, Section IV-B
R	=	Gas constant
oR	=	Degrees, Rankine scale
S	=	Van Laar Volume, Section VI-E and Section VII
T	=	Temperature, degrees Rankine
V	=	Molar volume of vapor, Section VI-D
V	=	Liquid volume in cc/gm-mole, Section VI-B
v_i^o	=	Molar volume of pure component i
\bar{V}_i	=	Partial molal volume of component i
x	=	Temperature oR divided by 100, Section VI-B
x_i	=	Mole fraction of component i in the liquid
y_i	=	Mole fraction of component i in the vapor
Z	=	Compressibility factor

NOMENCLATURE TABLE (continued)

- α = Relative volatility, Appendix I, Sections B, C, and D
- γ_i = Activity coefficient of component i in the liquid
- γ_π = Pressure activity coefficient, Appendix I-E
- ΔG = Change in free energy
- $\overline{\Delta i}_{mi}$ = Partial molal heat of mixing
- Δi_{vi}° = Latent heat
- ϕ_i = Fugacity coefficient of component i
- ϕ_i° = Fugacity coefficient of pure component i