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23 Findings from this study advance understanding of mineral recovery from reject brine and the  
24 capture and long-term storage of CO<sub>2</sub> in the form of HMCs.

25

26 **Keywords:** *Reject brine; Mg(OH)<sub>2</sub>; pH; hydrated magnesium carbonates (HMCs); carbon*  
27 *capture and storage*

28

## 29 **1. Introduction**

30 Fossil fuels have been the world's primary energy source, providing over 85% of the energy  
31 demands worldwide [1-6]. However, nearly 83% of the anthropogenic greenhouse gas (GHG)  
32 emissions are coming from combustion and non-fuel uses of fossil fuels [7]. CO<sub>2</sub>, which is the  
33 main GHG, has caused most of the global warming since it has the highest positive radiative  
34 forcing and far more abundant in the atmosphere than other heat-trapping gases [8, 9]. The  
35 concentration of CO<sub>2</sub> in the atmosphere has increased ~30% from 325 parts per million (ppm)  
36 at the beginning of the industrial era in 1970 to 409.7 ppm in May 2017 measured in Mauna  
37 Loa Observatory. Consequently, much attention has been drawn to the carbon management  
38 [10-12]. Carbon capture and storage (CCS) provides a feasible way to reduce the build-up of  
39 CO<sub>2</sub> in the atmosphere [13, 14]. CCS concept covers broad fields such as ocean, terrestrial,  
40 geological, biological and chemical approaches to store CO<sub>2</sub> gas in the long term [15-18],  
41 among which mineral carbonation via the reaction of CO<sub>2</sub> with saline aquifers is one of the  
42 most promising geologic CO<sub>2</sub> storage options [19-23]. Magnesium-based minerals have  
43 attracted great attentions worldwide as they show the potential to sequester anthropogenic  
44 CO<sub>2</sub> to counterpart the global warming [24-27]. Furthermore, reactive magnesia (MgO) cement  
45 has been studied as a potential alternative to the Portland cement due to its ability to sequester  
46 significant amount of carbon dioxide (CO<sub>2</sub>) and potential to be fully recycled [28-32].

47

48 Although the most thermodynamically stable carbonate for magnesium is in the anhydrous  
49 form, *i.e.*, magnesite ( $\text{MgCO}_3$ ) [33-35], formation of magnesite at the ambient condition is not  
50 common. Instead, formation of hydrated magnesium carbonates (HMCs) prevails as  $\text{Mg}^{2+}$  ions  
51 in the solution are highly hydrated [24]. HMCs are a class of magnesium compounds that form  
52 in  $\text{MgO-CO}_2\text{-H}_2\text{O}$  systems, where the carbonation of magnesium systems generate a variety of  
53 phases, including dypingite ( $\text{Mg}_5(\text{CO}_3)_4(\text{OH})_2 \cdot 5\text{H}_2\text{O}$ ) [36], hydromagnesite  
54 ( $\text{Mg}_5(\text{CO}_3)_4(\text{OH})_2 \cdot 4\text{H}_2\text{O}$ ) [37], and nesquehonite ( $\text{MgCO}_3 \cdot 3\text{H}_2\text{O}$ ) [18, 38]. It has been reported  
55 that inclusion of HMCs in reactive MgO cement enhances carbonation of the resulting binder  
56 [39].

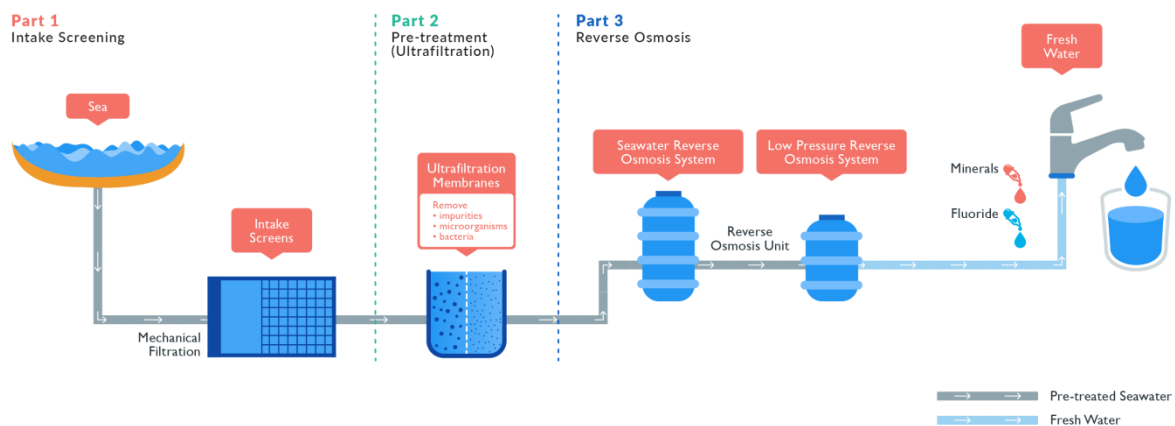
57  
58 Theoretically, the formation of different phases of HMCs with different morphologies is  
59 influenced by temperature, pH and  $\text{CO}_2$  partial pressure [24, 40, 41]. Recent experimental  
60 studies show that the precipitation of nesquehonite with needle-like morphology in an aqueous  
61 solution occurs commonly under ambient conditions [15, 18, 38]. As the reaction temperatures  
62 (333-368 K) and pH values increased, needle-like nesquehonite was replaced by  
63 hydromagnesite with sheet-like morphology since nesquehonite is widely known to transform  
64 to hydromagnesite at temperature above  $50^\circ\text{C}$  [40]. Hydromagnesite was reported to form at  
65  $120^\circ\text{C}$  and  $P_{\text{CO}_2}$  of 3 bar, which gradually transformed to magnesite within 5-15 hours.  
66 However, a further increase of  $P_{\text{CO}_2}$  to 100 bar at  $120^\circ\text{C}$  resulted in the direct precipitation of  
67 magnesite [24]. The thermal behavior of the synthesized HMCs (*e.g.*, nesquehonite) has been  
68 tested through real time in-situ X-ray diffraction (XRD), which indicated that nesquehonite and  
69 dypingite remained thermal and structural stable up to 373 K and 435 K, respectively [36, 42].  
70 Under the continued thermal treatment, nesquehonite transited into magnesite which was even  
71 thermally stable up to 600 K, while dypingite transited into hydromagnesite at around 570 K,  
72 assuring the long-term storage of  $\text{CO}_2$ . However, the influences of  $\text{Mg}(\text{OH})_2/\text{CO}_2$  molar ratios

73 and pH on the phases, morphology, and CCS efficiency of HMCs have yet been studied  
74 systematically.

75

76 Desalination is a process that removes minerals from saline water. In coastal regions such as  
77 Singapore where sources of fresh water are limited, desalination provides a feasible option to  
78 produce fresh water. However, a high salty waste stream (*i.e.*, reject brine) would be generated  
79 as much as the produced desalinated water at the end of the process [43]. Reject brine is a much  
80 more complex media because chemicals are often added into the intake seawater (*e.g.*, to  
81 precipitate the colloidal particles before running through the ultra-filtration) in the desalination  
82 process (Fig. 1). Although many studies have investigated mineral trapping of CO<sub>2</sub> into saline  
83 aquifers (*e.g.*, seawater, natural brine, or synthesized MgCl<sub>2</sub> solution) [18, 36, 42, 44-46], very  
84 few has reported the use of reject brine as the CO<sub>2</sub> reservoir [47] and no study has proposed to  
85 use reject brine as the Mg(OH)<sub>2</sub> source to synthesize HMCs.

86



87

88 Figure 1 Schematic illustration of the typical process in a reverse osmosis desalination plant

89

[48]

90

91 In this paper, influence of key parameters including  $\text{Mg}(\text{OH})_2:\text{CO}_2$  molar ratio, pH, and  
92  $\text{Mg}(\text{OH})_2$  source on HMCs synthesis were investigated. The resulting HMCs were  
93 characterized by means of XRD, scanning electron microscopy (SEM), and  
94 thermogravimetric/differential thermal analysis (TG/DTA) to reveal phases, morphology, and  
95 CCS efficiency of HMCs synthesized under different conditions. In the following sections,  
96 materials and methodologies are presented first, followed by results presentation and  
97 discussion.

98

## 99 **2. Materials and Methodology**

### 100 **2.1. Materials**

101 Reject brine sample was collected from a local desalination plant which generates 318,500 m<sup>3</sup>  
102 desalinated water per day. The sample was filtrated through a 45  $\mu\text{m}$  membrane filter to remove  
103 suspended solids before further analysis. An inductively coupled plasma-optical emission  
104 spectroscopy (ICP-OES) was used to analyze the chemical composition of reject brine in the  
105 current study (Table 1). Analytical grade  $\text{Mg}(\text{OH})_2$  (92% pure) and analytical grade sodium  
106 hydroxide (NaOH) with a purity of 97% were both purchased from VWR Pte Ltd in Singapore.  
107 Compressed  $\text{CO}_2$  was purchased from Leeden National Oxygen Ltd in Singapore.

108

109 Table 1 Chemical composition of reject brine

Element	Cl	Na	$\text{SO}_4$	Mg	K	Ca	Sr	B	Si	Li	P	Al
Concentration (ppm)	65593	13580	4323	1718	846	471	14.6	3.8	3.7	0.3	0.2	0.1

110

### 111 **2.2. Methodology**

112 In the first approach, 0.82 g commercially available analytical grade  $\text{Mg}(\text{OH})_2$  was dissolved  
113 into 200 ml ultra-pure water to prepare the  $\text{Mg}(\text{OH})_2$  slurry. To study the influences of

114  $\text{Mg(OH)}_2/\text{CO}_2$  molar ratios and pH on the microstructures of HMCs , three sets of experiments  
115 were designed at controlled conditions, *i.e.*,  $\text{Mg(OH)}_2:\text{CO}_2$  molar ratio (1:1-1:7) and pH (8-14).  
116  $\text{CO}_2$  was sparged into the slurry at a rate of 100 ml/min at room temperature under pre-  
117 determined conditions as follows,

118 a) pH = 8,  $\text{Mg(OH)}_2:\text{CO}_2$  molar ratio = 1:1 to 1:7

119 b) pH = 8 to 11,  $\text{Mg(OH)}_2:\text{CO}_2$  molar ratio = 1:1

120 c) pH = 8 to 11,  $\text{Mg(OH)}_2:\text{CO}_2$  molar ratio = 1:2

121

122 In the second approach,  $\text{Mg(OH)}_2$  was first synthesized from the reject brine via the addition  
123 of NaOH at an optimized condition (*i.e.*, NaOH/ $\text{Mg}^{2+}$  ratio of 2 at 25°C) determined from our  
124 previous work [49-51], which results high yield and high purity  $\text{Mg(OH)}_2$ . After which, 0.82 g  
125 of synthesized  $\text{Mg(OH)}_2$  was mixed with 200 ml ultra-pure water.  $\text{CO}_2$  was sparged into the  
126 slurry at a rate of 100 ml/min at room temperature under controlled condition (*i.e.*, pH = 8,  
127  $\text{Mg(OH)}_2:\text{CO}_2$  molar ratio = 1:1).

128

129 A pH/thermometer probe, inserted into reject brine, was used to continuously record the  
130 temperature and pH during the experiment. A  $\text{CO}_2$  flowmeter was used to monitor and record  
131 the volume of  $\text{CO}_2$  diffused into the slurry. Once the diffused  $\text{CO}_2$  reached the pre-determined  
132 value (*i.e.*, calculated based on the designed  $\text{Mg(OH)}_2:\text{CO}_2$  molar ratio), the reaction was  
133 terminated. 1M NaOH was added into the slurry continuously to maintain the pH to the  
134 designed value since sparging  $\text{CO}_2$  lowered the pH of slurry. HMCs were separated from the  
135 solution by a centrifuge and washed three times using ultra-pure water. The washed samples  
136 were fully dried in an oven at low temperature (*i.e.*, 40°C) to avoid any phase changes, before  
137 being ground into powder form. The prepared powder was finally passed through a 125  $\mu\text{m}$   
138 sieve for further microstructural analysis.

139

140 ICP-OES (PerkinElmer Optima DV2000) was employed to measure the chemical composition  
141 of the reject brine before and after the reactions. The XRD (Bruker D8 Advance) diffractograms  
142 of the synthesized HMCs were recorded from  $5^\circ$  to  $70^\circ$  at  $0.02^\circ/\text{step}$  with a  $\text{CuK}\alpha$  radiation at  
143 40 kV and 40 mA. The morphology of the synthesized HMCs was investigated by a field  
144 emission SEM (JSM-7600F). TG/DTA (PyrisDiamond 4000) of the synthesized HMCs was  
145 operated at a heating rate of  $10^\circ\text{C}/\text{min}$  under the air flow condition.

146

### 147 **3. Results and Discussion**

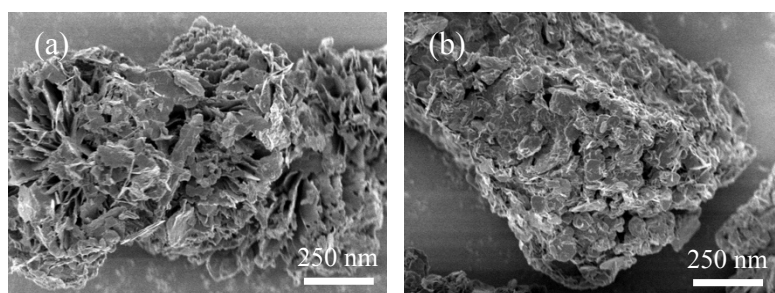
#### 148 **3.1. Characterization of HMCs synthesized from $\text{Mg}(\text{OH})_2$ slurry**

##### 149 **3.1.1. Effect of $\text{Mg}(\text{OH})_2/\text{CO}_2$ molar ratio**

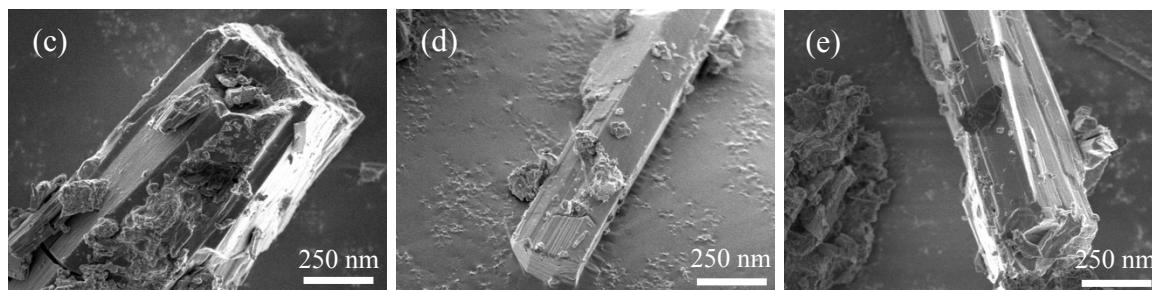
150 Figure 2 shows the FESEM images of all samples obtained under a constant pH of 8 while the  
151  $\text{Mg}(\text{OH})_2:\text{CO}_2$  molar ratio was varied between 1:1 and 1:7. The morphologies of the obtained  
152 HMCs dramatically changed with the  $\text{Mg}(\text{OH})_2:\text{CO}_2$  molar ratio. For instance, the rosette-like  
153 morphology observed when the  $\text{Mg}(\text{OH})_2:\text{CO}_2$  molar ratio was 1:1 (Fig. 2a), which was  
154 eventually replaced by rod-like structures with smooth surfaces when this ratio gradually  
155 increased to 1:6 (Figs. 2b-f). The boundaries of these rod-like carbonate phases became clearer  
156 with an increase in the  $\text{Mg}(\text{OH})_2:\text{CO}_2$  molar ratio. A further increase in the  $\text{Mg}(\text{OH})_2:\text{CO}_2$   
157 molar ratio to 1:7 revealed the formation of a layer of rosette-like flakes around the original  
158 rod-like morphology, producing a “house of cards” texture on the surface [52], as shown in  
159 Fig. 2g.

160

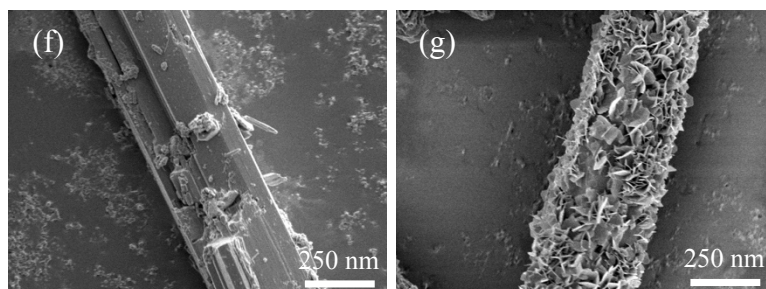




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162



163

164 Figure 2 FESEM images of HMCs obtained under a pH of 8 at different  $\text{Mg}(\text{OH})_2:\text{CO}_2$  molar  
 165 ratios of (a) 1:1, (b) 1:2, (c) 1:3, (d) 1:4, (e) 1:5, (f) 1:6 and (g) 1:7

166

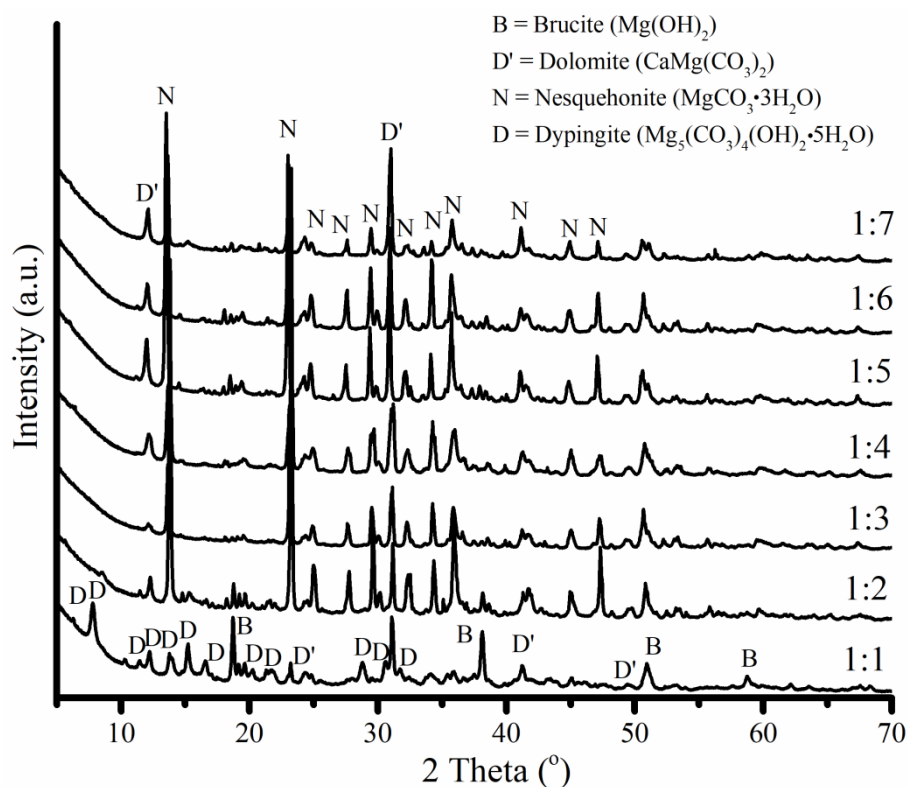
167 Fig. 3 indicates the XRD diffractograms of the same set of samples obtained under a pH of 8  
 168 at different  $\text{Mg}(\text{OH})_2:\text{CO}_2$  molar ratios. The XRD patterns confirmed that the rosette- and rod-  
 169 like particles observed in Fig. 2 could be attributed to dypingite and nesquehonite, respectively.  
 170 These morphological observations were in line with the previous literature [18, 36, 41], where  
 171 the distinct morphologies of dypingite and nesquehonite were reported. At the  $\text{Mg}(\text{OH})_2:\text{CO}_2$   
 172 molar ratio of 1:1, the precipitates consisted of dypingite, uncarbonated brucite and dolomite  
 173 that was present as an impurity within  $\text{Mg}(\text{OH})_2$ . An increase in the  $\text{Mg}(\text{OH})_2:\text{CO}_2$  molar ratio  
 174 to 1:2 revealed a reduction in the amount of uncarbonated brucite, resulting in the domination  
 175 of nesquehonite. These results corresponded well with the chemical composition of different

176 carbonate phases. Accordingly, the abundance of nesquehonite could be associated with the  
177 availability of higher amounts of CO<sub>2</sub> introduced into the mix under higher Mg(OH)<sub>2</sub>:CO<sub>2</sub>  
178 molar ratios. This is because nesquehonite (MgCO<sub>3</sub>·3H<sub>2</sub>O) requires a higher Mg:CO<sub>2</sub> molar  
179 ratio of 1:1 than dypingite (Mg<sub>5</sub>(CO<sub>3</sub>)<sub>4</sub>(OH)<sub>2</sub>·5(H<sub>2</sub>O)), which can theoretically form at a  
180 corresponding ratio of 1:0.8. Further increase of the Mg(OH)<sub>2</sub>:CO<sub>2</sub> molar ratio from 1:2 to 1:7  
181 did not lead to significant changes in the XRD patterns, where nesquehonite continued to be  
182 the dominate phase which is consistent with the SEM observation (Fig. 2).

183

184 The “house of cards” morphology is related to a dissolution-recrystallization self-assembly  
185 growth mechanism when the dissolution rate of nesquehonite was faster than the precipitation  
186 rate of hydromagnesite [52]. Thus, the formation of “house of cards” texture on the surface of  
187 HMCs synthesized at Mg(OH)<sub>2</sub>:CO<sub>2</sub> molar ratio of 1:7 (Fig. 2g) reveals that while  
188 nesquehonite is still the dominating phase of the main body (Fig. 3), nesquehonite on the  
189 surface was transformed into hydromagnesite phase due to elevated CO<sub>2</sub> concentration.

190



191

192 Figure 3 XRD diffractograms of HMCs obtained under a pH of 8 at different  $\text{Mg}(\text{OH})_2:\text{CO}_2$   
 193 molar ratios

194

195 **3.1.2. Effect of pH at  $\text{Mg}(\text{OH})_2$ -to- $\text{CO}_2$  molar ratio of 1**

196 Figure 4 illustrates the FESEM images of the samples obtained under different pH values  
 197 ranging between 8 and 11, at a constant  $\text{Mg}(\text{OH})_2:\text{CO}_2$  molar ratio of 1:1. At the lower pH  
 198 values of  $< 11$ , the obtained carbonates displayed rosette-like morphologies with an average  
 199 dimension of  $\sim 2 \mu\text{m}$ , as shown in Figures 4(a)-(c). These rosette-like formations were  
 200 confirmed to be dypingite, as shown by the XRD patterns presented in Figure 5. As the pH  
 201 increased from 8 to 10, the intensity of the uncarbonated brucite peak revealed a decrease  
 202 relative to the others, possibly indicating a reduction in the amount of brucite and an associated  
 203 higher degree of carbonation at elevated pH levels. This increase in the carbonation degree  
 204 could be associated with the higher  $\text{CO}_3^{2-}:\text{HCO}_3^-$  ratios in the prepared solutions at elevated  
 205 pH levels. An increase in the pH led to higher concentrations of  $\text{OH}^-$ , therefore enabling the

206 conversion of  $\text{HCO}_3^-$  to  $\text{CO}_3^{2-}$ , which then reacted with  $\text{Mg}^{2+}$ , leading to the precipitation of  
207 higher amounts of HMCs in the solution. Alternatively, a further increase in the pH from 11 to  
208 14 lowered the carbonation degree of brucite, which was observed with its flake-like  
209 morphology in Figure 4(d). These results were in line with the findings reported in previous  
210 studies, where the optimal pH for the carbonation of brucite was shown to be around 9 [53].

211

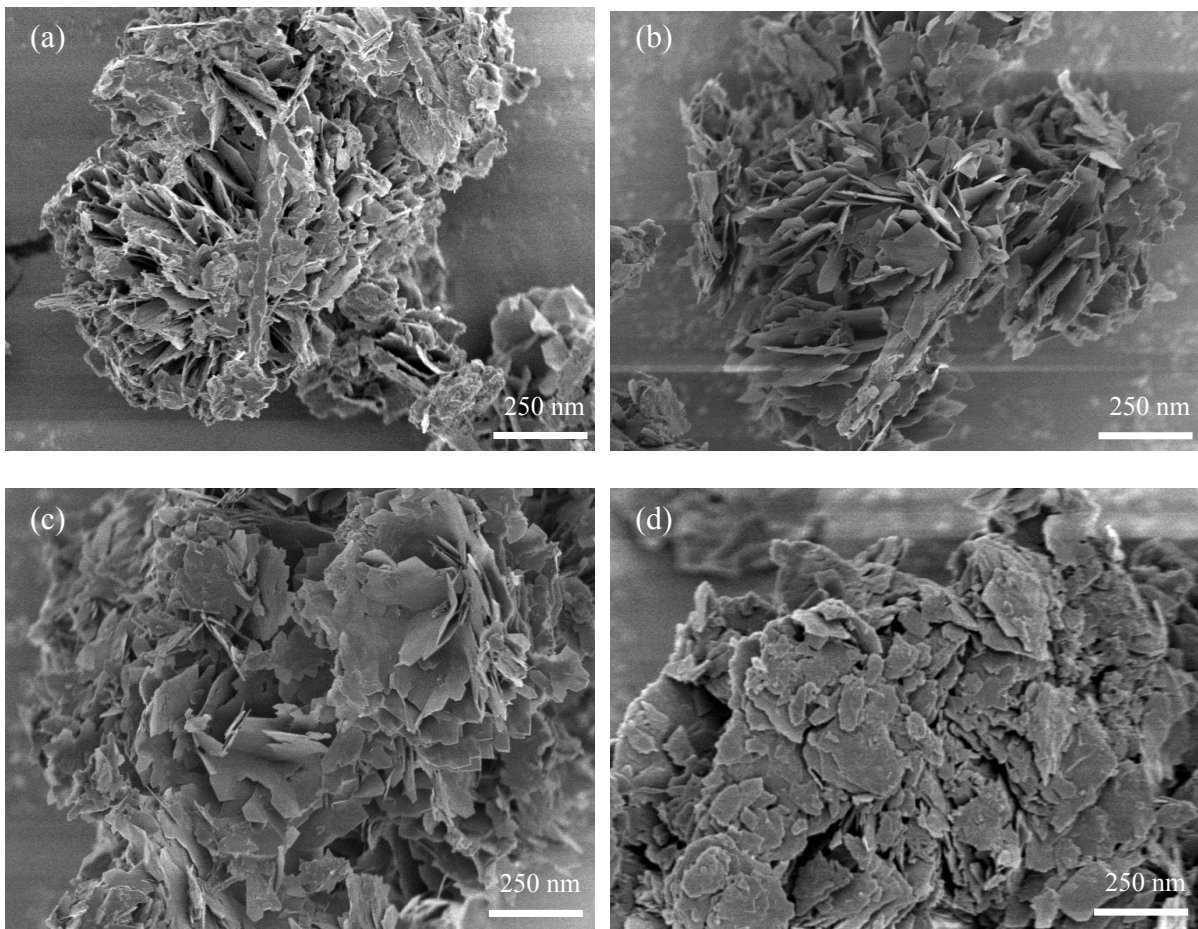
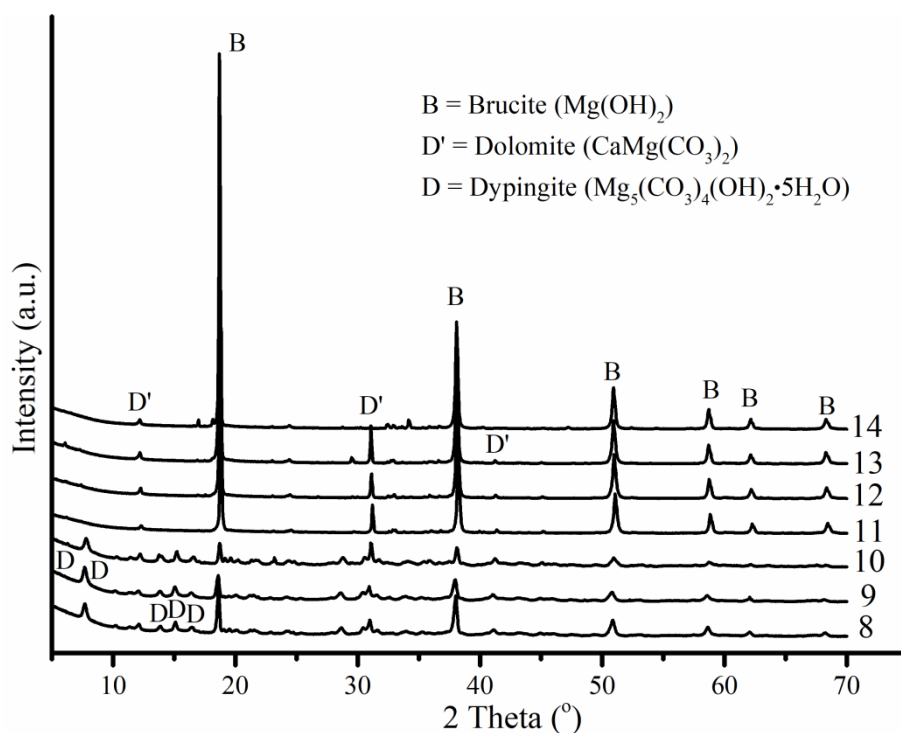


Figure 4 FESEM images of HMCs obtained at the  $\text{Mg}(\text{OH})_2:\text{CO}_2$  molar ratio of 1:1 under different pH values of (a) 8, (b) 9, (c) 10 and (d) 11



217

218 Figure 5 XRD diffractograms of HMCs obtained at the  $\text{Mg}(\text{OH})_2:\text{CO}_2$  molar ratio of 1:1

219 under different pH values

220

### 221 3.1.3 Effect of pH at $\text{Mg}(\text{OH})_2:\text{CO}_2$ molar ratio of 1:2

222 Figure 6 displays the morphologies of HMCs obtained under different pH values at the

223  $\text{Mg}(\text{OH})_2:\text{CO}_2$  molar ratio of 1:2. Different from HMCs obtained at the  $\text{Mg}(\text{OH})_2:\text{CO}_2$  molar

224 ratio of 1:1, where the presence of dypingite with a rosette-like morphology dominated

225 regardless of the pH value; HMCs obtained at the  $\text{Mg}(\text{OH})_2:\text{CO}_2$  molar ratio of 1:2 clearly

226 demonstrated a different morphology. Instead of the previously observed rosette-like plates, a

227 rod-like structure presenting the “house of cards” texture was seen in samples obtained under

228 pH values of 8 and 9 (Figs. 6a-b). An increase in the pH from 8 onwards resulted in the

229 distortion of the originally clear borders of the nesquehonite crystals, whose shape transformed

230 from the rod-like structure to a cluster of flakes forming on top. This change was mostly

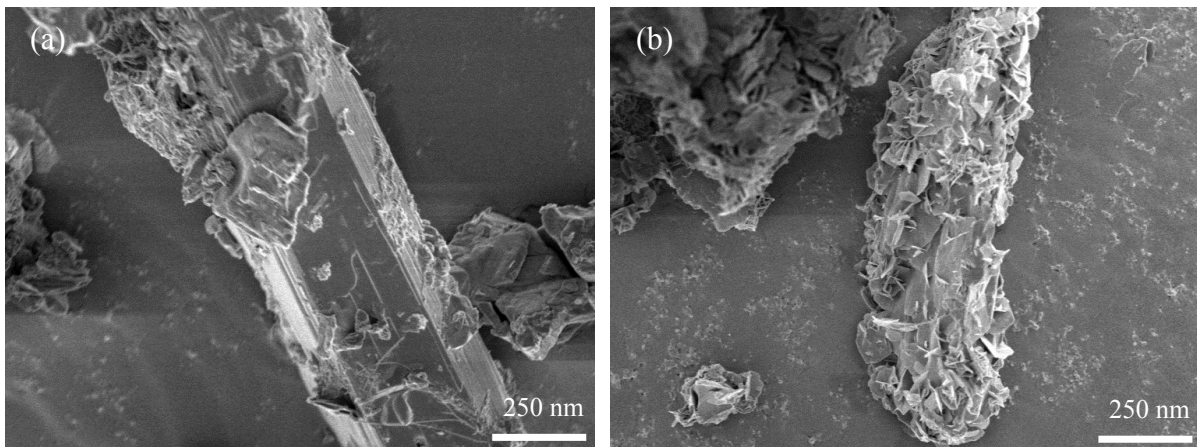
231 obvious at pH values of 10 and 11 (Figures 6(c) and (d)), which revealed the formation of flake-

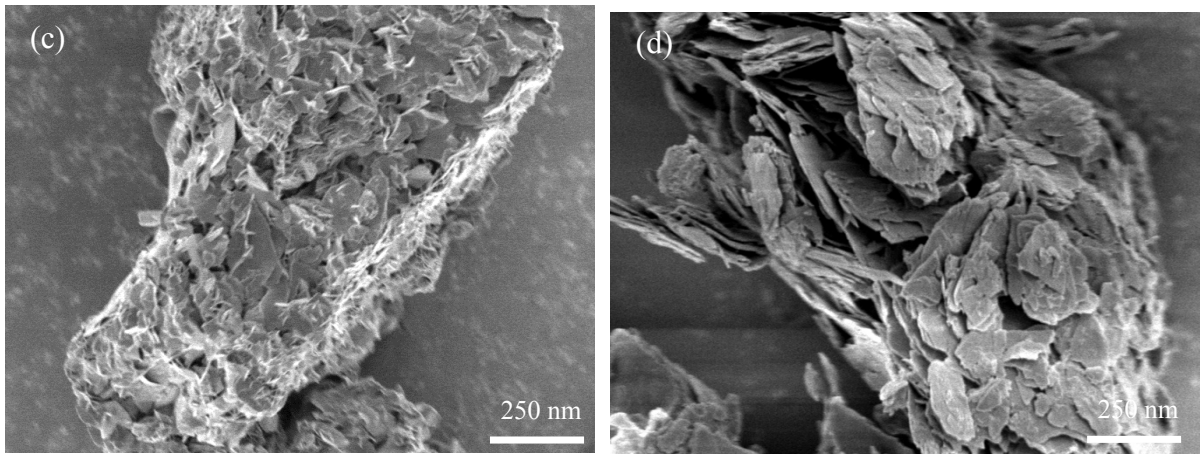
232 like clusters with clearly defined boundaries at a pH of 11.

233

234 The formation of nesquehonite under pH value of 11 was confirmed by the XRD patterns  
235 shown in Figure 7. In line with the findings obtained under the  $\text{Mg}(\text{OH})_2:\text{CO}_2$  molar ratio of  
236 1:1 as revealed in Figure 5, an increase in the pH to 10 and above resulted in the formation of  
237 uncarbonated brucite where a flake-like morphology was observed. This “house of cards”  
238 texture observed within the prepared samples was attributed to the dissolution-  
239 recrystallization-self-assembly growth mechanism as explained in the aforementioned text.  
240 The elevated pH used in the experiments conducted in this study increased the solubility of  
241  $\text{CO}_2$  in the solution. This has led to a dissolution of the surface of nesquehonite and served as  
242 the nucleation points for further hydromagnesite/dypingite plates growing with excessive  $\text{CO}_2$   
243 at the surface.

244





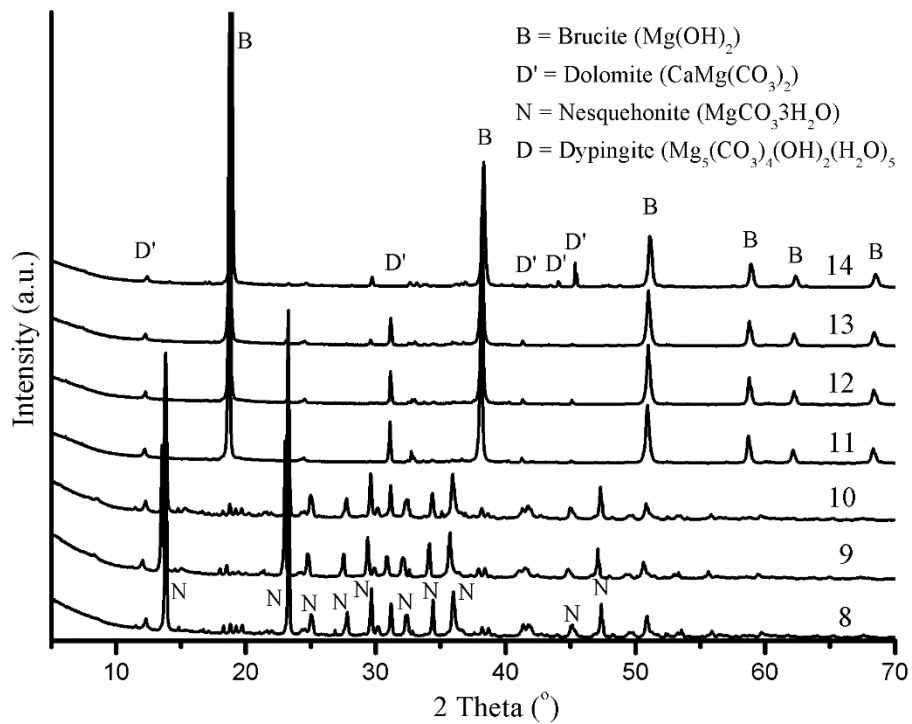
246

247 Figure 6 Typical FESEM images of HMCs obtained at a  $\text{Mg}(\text{OH})_2:\text{CO}_2$  molar ratio of 1:2

248

under different pH values of (a) 8, (b) 9, (c) 10 and (d) 11

249



250

251 Figure 7 XRD diffractograms of HMCs obtained at the  $\text{Mg}(\text{OH})_2:\text{CO}_2$  molar ratio of 1:2

252

under different pH values

253

### 254 3.2. Comparison of HMCs synthesized from different source

255 This section aims to provide a comparison of HMCs obtained via reject brine to those of

256 chemical Mg(OH)<sub>2</sub> slurry, whose detailed characterization was presented earlier in Section 3.1.  
257 The findings presented here aim to use reject brine for the long-term storage of anthropogenic  
258 CO<sub>2</sub>.

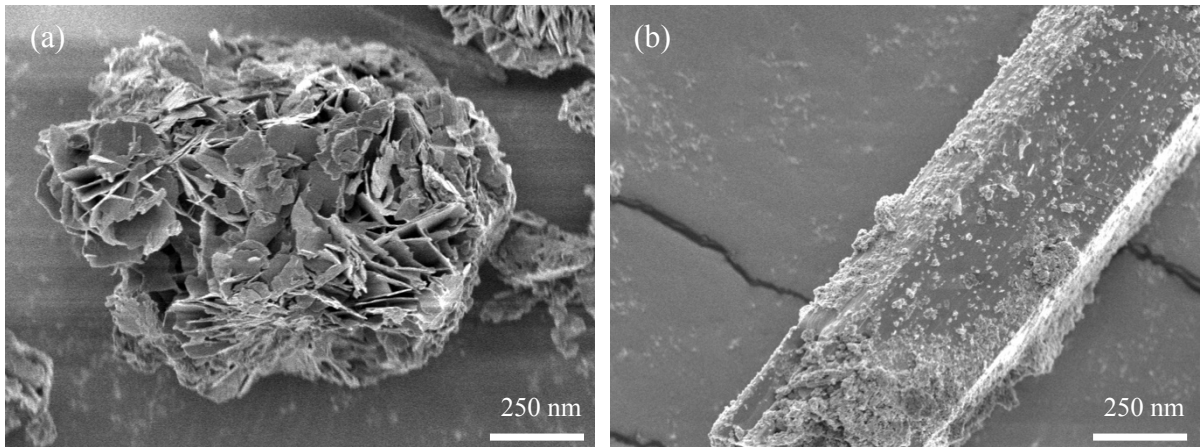
259

### 260 **3.2.1. Microstructure of HMCs**

261 Figure 8 provides a comparison of the morphologies of HMCs synthesized from Mg(OH)<sub>2</sub>  
262 slurry and reject brine under a constant pH and Mg(OH)<sub>2</sub>:CO<sub>2</sub> molar ratio of 8 and 1:1,  
263 respectively. As shown in Figure 8(a), the carbonate crystals obtained via the use of Mg(OH)<sub>2</sub>  
264 slurry led to a rosette-like morphology. Alternatively, the carbonation of reject brine led to the  
265 formation of a needle-like morphology with clear boundaries, as seen in Figure 8(b). The  
266 compositions of these rosette- and needle-like particles were confirmed to be nesquehonite and  
267 dypingite by XRD patterns revealed in Figure 9, respectively. The formation of different Mg-  
268 carbonate phases via the two sources could be associated with the relatively higher reactivity  
269 of Mg(OH)<sub>2</sub> prepared from reject brine when compared to that of Mg(OH)<sub>2</sub> slurry (i.e. with a  
270 specific surface area of 7.4 vs. 4.8 m<sup>2</sup>/g as tested by BET analysis). The carbonation of  
271 Mg(OH)<sub>2</sub> with a higher reactivity could have capture more CO<sub>2</sub> and enabled the formation of  
272 nesquehonite as opposed to dypingite since nesquehonite requires a higher Mg:CO<sub>2</sub> molar ratio  
273 as explained in the aforementioned text. This difference in the reactivity of the two samples  
274 was also reflected by the absence of the residual brucite peaks in reject brine, as opposed to the  
275 clearly defined uncarbonated brucite peaks observed in the Mg(OH)<sub>2</sub> slurry, as seen in Figure  
276 9.

277

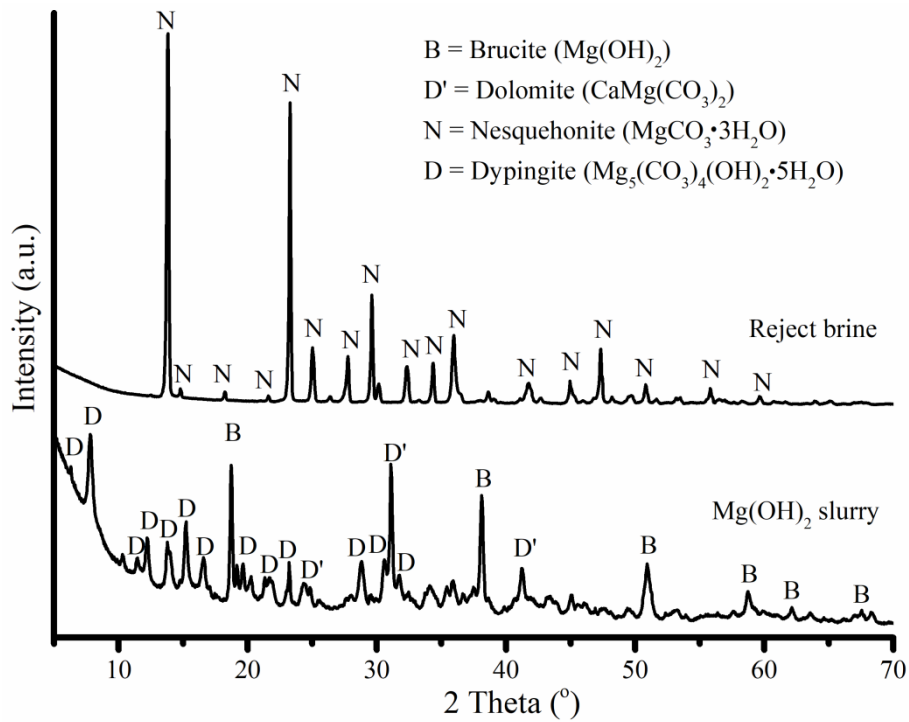




278

279 Figure 8 SEM images of HMCs obtained at the  $\text{Mg}(\text{OH})_2:\text{CO}_2$  molar ratio of 1:1 under a pH  
 280 of 8, showing (a)  $\text{Mg}(\text{OH})_2$  slurry and (b) reject brine

281



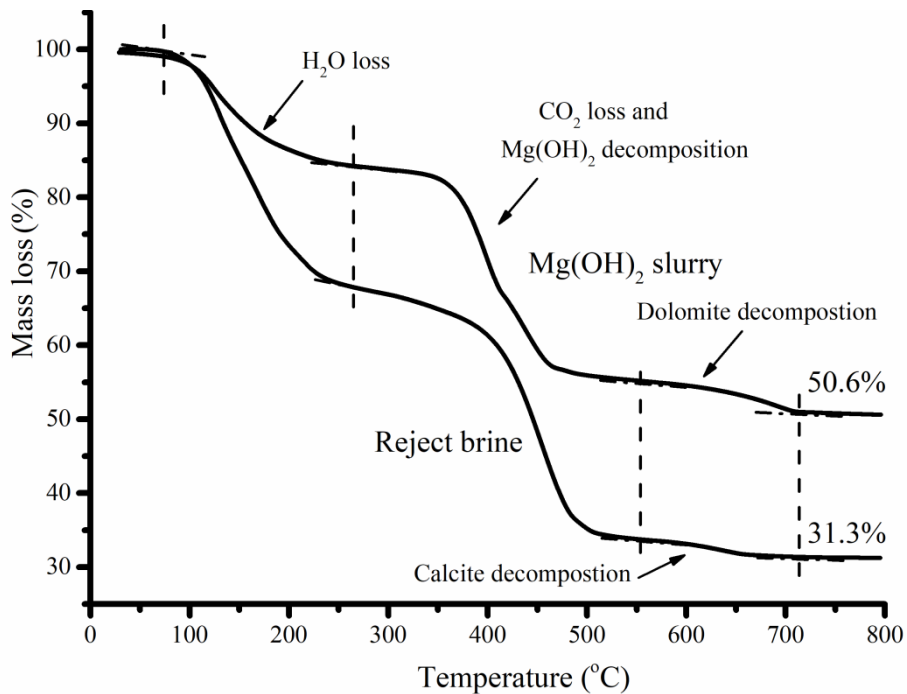
282

283 Figure 9 XRD diffractograms of HMCs obtained from  $\text{Mg}(\text{OH})_2$  slurry and reject brine at the  
 284  $\text{Mg}(\text{OH})_2:\text{CO}_2$  molar ratio of 1:1 under a pH of 8

285

286 **3.2.2.  $\text{CO}_2$  capture and storage**

287 The quantitative analysis of the chemical composition of HMCs and amount of CO<sub>2</sub> used in  
 288 their formation was carried out via TG/DTA and ICP-OES analyses. Figure 10 presents the  
 289 TG/DTA graphs of HMCs obtained from Mg(OH)<sub>2</sub> slurry and reject brine at the Mg(OH)<sub>2</sub>:CO<sub>2</sub>  
 290 molar ratio of 1:1 and under a pH 8. Both systems demonstrated a similar trend with three  
 291 stages of mass loss, which corresponded well with previous studies [36, 54, 55]. Firstly, the  
 292 dehydration of HMCs took place at ~100-250 °C, resulting in the loss of H<sub>2</sub>O. The second mass  
 293 loss occurred between 250 and 550 °C, which was because of the decomposition of  
 294 uncarbonated Mg(OH)<sub>2</sub> into MgO as well as the decarbonation of HMCs, resulting in a loss of  
 295 H<sub>2</sub>O and CO<sub>2</sub>. The final mass loss observed between 550 and 700 °C was due to the  
 296 decomposition of dolomite and calcite, respectively, which was present as an impurity in the  
 297 two systems (i.e. in the form of dolomite in Mg(OH)<sub>2</sub> slurry and calcite in reject brine).  
 298



299  
 300 Figure 10 Typical TG/DTA curves of HMCs obtained from Mg(OH)<sub>2</sub> slurry and reject brine  
 301 at the Mg(OH)<sub>2</sub>:CO<sub>2</sub> molar ratio of 1:1 under a pH of 8  
 302

303 The chemical composition of the final product was determined via a combination of the results  
 304 generated by TG/DTA and ICP-OES, where the recovery rate of  $Mg^{2+}$  was measured via ICP-  
 305 OES and TG/DTA was used to determine the quantity of each phase derived from XRD results.  
 306 Table 2 revealed the composition of the precipitate synthesized via the carbonation of  $Mg(OH)_2$   
 307 slurry to be composed of 62.1% dypingite and 30.5% uncarbonated brucite. On the other hand,  
 308 the carbonation of reject brine led to a precipitate composed of 93.1% nesquehonite and 3.7%  
 309 uncarbonated brucite, as detailed in Table 2. These results were used in the calculation of the  
 310 percentage of captured  $CO_2$ , which was derived by measuring the mass of  $CO_2$  in the HMCs  
 311 (i.e. dypingite/nesquehonite) divided by the initial input of  $CO_2$  degassed to the system at the  
 312  $Mg(OH)_2:CO_2$  molar ratio of 1:1. The outcome of these analyses indicated that 43.7%  $CO_2$   
 313 could be sequestered in the form of dypingite via the defusing  $CO_2$  into  $Mg(OH)_2$  slurry, while  
 314 the corresponding ratio of  $CO_2$  sequestered in reject brine was calculated to be 82.6%. The  
 315 higher efficiency of  $CO_2$  sequestration achieved via the use of reject brine was associated with  
 316 the increased reactivity of  $Mg(OH)_2$  synthesized from reject brine. Details of the chemical  
 317 composition and the percentage of captured  $CO_2$  were included in the Appendix section.

318

319 Table 2 Chemical composition of HMCs synthesized from  $Mg(OH)_2$  slurry and reject brine at  
 320 the  $Mg(OH)_2:CO_2$  molar ratio of 1:1 under a pH of 8

$Mg(OH)_2$ slurry	Mass (g)	Mass (%)	Reject brine	Mass (g)	Mass (%)
Dypingite	0.6	62.1	Nesquehonite	1.51	93.1
Brucite	0.07	30.5	Brucite	0.06	3.7
Dolomite	0.3	7.4	Calcite	0.05	3.2
$CO_2$ captured (%)	43.7		$CO_2$ captured (%)	82.6	

321

322 According to the Paris Agreement, it aims to reduce GHG emissions by 20% (i.e., 7 gigatonnes  
 323  $CO_2$  emission reduction as annual anthropogenic  $CO_2$  emissions is about 35 gigatonnes [56])  
 324 in order to hold the increase in the global average temperature to below  $2^\circ C$  above pre-

325 industrial levels [56]. According to the International Desalination Association, the global daily  
326 production of desalinated water generated by 18,426 desalination plants worldwide exceeds  
327 86.8 million m<sup>3</sup> [47]. It is estimated that an equivalent amount of reject brine is generated [47].  
328 The concentration of Mg<sup>2+</sup> in reject brine is around 1700 ppm, and thus around 54 million  
329 tonnes of Mg could be recovered every year. With a carbon capture and storage rate of 82.6%  
330 in the current study, around 45 million tonnes of CO<sub>2</sub> can be sequestered annually. The  
331 suggested methodology thus contributes to around 1% of the required CO<sub>2</sub> emission reduction  
332 (*i.e.*, 7 gigatonnes) aimed in the Paris Agreement.

333

#### 334 **4. Summary and Conclusions**

335 This study presented the influences of key parameters including the Mg(OH)<sub>2</sub>:CO<sub>2</sub> molar ratio,  
336 pH, and Mg(OH)<sub>2</sub> source on the synthesis of HMCs through the carbonation of Mg(OH)<sub>2</sub> slurry.  
337 The resulting HMCs were characterized via a combination of techniques including XRD,  
338 FESEM, and TG/DTA. Main conclusions drawn from this study are summarized below.

- 339 • The carbonation of Mg(OH)<sub>2</sub> slurry under the elevated of Mg(OH)<sub>2</sub>:CO<sub>2</sub> molar ratio  
340 resulted in the transformation of dypingite to nesquehonite.
- 341 • Increasing the pH from 8 to 10 was found to promote the carbonation process of  
342 Mg(OH)<sub>2</sub>, resulting in a higher carbonation degree.
- 343 • A specific “house of cards” texture, involving the formation of rosette-like dypingite  
344 flakes on the surface of nesquehonite needles, was discovered under elevated pH and  
345 Mg(OH)<sub>2</sub>:CO<sub>2</sub> ratios conditions. The formation of this structure was associated with to  
346 a dissolution-recrystallization-self-assembly growth mechanism as nesquehonite was  
347 seen as a precursor for the further nucleation and seeding of hydromagnesite/dypingite  
348 on the surface.

- 349       • Carbonation of Mg(OH)<sub>2</sub> slurry synthesized from reject brine led to high yield, high  
350           purity, and high carbonation degree (82.6%) HMCs. Reject brine shows high potential  
351           to be used for capture and long-term storage of CO<sub>2</sub> in the form of HMCs.

352

353   The use of compressed commercial CO<sub>2</sub> in the research was to provide a pure source to evaluate  
354   CO<sub>2</sub> sequestration rate of the synthesized Mg(OH)<sub>2</sub> from desalination reject brine, which  
355   served as a model case study. In the ‘real world’ case, different CO<sub>2</sub> sources and collecting  
356   methods such as CO<sub>2</sub> generated from factories, coal burning power plants, and municipal solid  
357   waste incineration plants, may be used. However, further study is necessary to evaluate CO<sub>2</sub>  
358   sequestration efficiency of the synthesized Mg(OH)<sub>2</sub> with different CO<sub>2</sub> sources and collecting  
359   methods. Furthermore, it is necessary to evaluate the mass, energy, reagents, wastes that  
360   come into play in the global process from the life cycle and life cycle cost viewpoint of HMCs  
361   synthesized from reject brine.

362

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364

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368

### 369   **References**

370   [1] International Energy Agency, Tracking industrial energy efficiency and CO<sub>2</sub> emissions,  
371       in, Organisation for Economic Co-operation and Development, 2007.

- 372 [2] V. Mashayekhizadeh, M.H. Ghazanfari, R. Kharrat, M. Dejam, Pore-level observation of  
373 free gravity drainage of oil in fractured porous media, *Transport in porous media*, 87  
374 (2011) 561-584.
- 375 [3] M. Dejam, M.H. Ghazanfari, V. Mashayekhizadeh, M. Kamyab, Factors affecting the  
376 gravity drainage mechanism from a single matrix block in naturally fractured reservoirs,  
377 *Special Topics & Reviews in Porous Media: An International Journal*, 2 (2011).
- 378 [4] M. Dejam, M.H. Ghazanfari, M. Kamyab, M. Masihi, The gas-oil gravity drainage model  
379 in a single matrix block: a new relationship between relative permeability and capillary  
380 pressure functions, *Journal of Porous Media*, 14 (2011).
- 381 [5] V. Mashayekhizadeh, R. Kharrat, M. Ghazanfari, M. Dejam, An experimental  
382 investigation of fracture tilt angle effects on frequency and stability of liquid bridges in  
383 fractured porous media, *Petroleum Science and Technology*, 30 (2012) 807-816.
- 384 [6] M. Dejam, H. Hassanzadeh, Z. Chen, Semi-analytical solutions for a partially penetrated  
385 well with wellbore storage and skin effects in a double-porosity system with a gas cap,  
386 *Transport in porous media*, 100 (2013) 159-192.
- 387 [7] J.D. Figueroa, T. Fout, S. Plasynski, H. McIlvried, R.D. Srivastava, Advances in CO<sub>2</sub>  
388 capture technology - the US department of energy's carbon sequestration program, *Int. J.*  
389 *Greenh. Gas Control*, 2 (2008) 9-20.
- 390 [8] T. Morita, J. Robinson, A. Adegbulugbe, J. Alcamo, D. Herbert, E.L. La Rovere, N.  
391 Nakicenovic, H. Pitcher, P. Raskin, K. Riahi, Greenhouse gas emission mitigation  
392 scenarios and implications, *Climate Change*, (2001) 115-166.
- 393 [9] P. Forster, V. Ramaswamy, P. Artaxo, T. Berntsen, R. Betts, D.W. Fahey, J. Haywood, J.  
394 Lean, D.C. Lowe, G. Myhre, Changes in atmospheric constituents and in radiative  
395 forcing. Chapter 2, *Climate Change 2007. The Physical Science Basis*, (2007).

- 396 [10] H. Arakawa, M. Aresta, J.N. Armor, M.A. Barteau, E.J. Beckman, A.T. Bell, J.E.  
397 Bercaw, C. Creutz, E. Dinjus, D.A. Dixon, K. Domen, D.L. DuBois, J. Eckert, E. Fujita,  
398 D.H. Gibson, W.A. Goddard, D.W. Goodman, J. Keller, G.J. Kubas, H.H. Kung, J.E.  
399 Lyons, L.E. Manzer, T.J. Marks, K. Morokuma, K.M. Nicholas, R. Periana, L. Que, J.  
400 Rostrup-Nielson, W.M.H. Sachtler, L.D. Schmidt, A. Sen, G.A. Somorjai, P.C. Stair,  
401 B.R. Stults, W. Tumas, Catalysis research of relevance to carbon management: Progress,  
402 challenges, and opportunities, *Chemical Reviews*, 101 (2001) 953-996.
- 403 [11] R. Lal, Soil carbon sequestration impacts on global climate change and food security,  
404 *Science*, 304 (2004) 1623-1627.
- 405 [12] R.S. Haszeldine, Carbon capture and storage: How green can black be?, *Science*, 325  
406 (2009) 1647-1652.
- 407 [13] A.B. Rao, E.S. Rubin, A technical, economic, and environmental assessment of amine-  
408 based CO<sub>2</sub> capture technology for power plant greenhouse gas control, *Environmental*  
409 *Science & Technology*, 36 (2002) 4467-4475.
- 410 [14] H.J. Herzog, CO<sub>2</sub> capture, reuse, and sequestration technologies for mitigating global  
411 climate change, in, USDOE Federal Energy Technology Center, Morgantown, WV  
412 (United States), 1998.
- 413 [15] A. Botha, C.A. Strydom, Preparation of a magnesium hydroxy carbonate from  
414 magnesium hydroxide, *Hydrometallurgy*, 62 (2001) 175-183.
- 415 [16] E. Rendek, G. Ducom, P. Germain, Carbon dioxide sequestration in municipal solid  
416 waste incinerator (MSWI) bottom ash, *Journal of Hazardous Materials*, 128 (2006) 73-  
417 79.
- 418 [17] J.T. Kloprogge, W.N. Martens, L. Nothdurft, L.V. Duong, G.E. Webb, Low temperature  
419 synthesis and characterization of nesquehonite, *J. Mater. Sci. Lett.*, 22 (2003) 825-829.

- 420 [18] V. Ferrini, C. De Vito, S. Mignardi, Synthesis of nesquehonite by reaction of gaseous  
421 CO<sub>2</sub> with Mg chloride solution: Its potential role in the sequestration of carbon dioxide,  
422 Journal of Hazardous Materials, 168 (2009) 832-837.
- 423 [19] E.H. Oelkers, S.R. Gislason, J. Matter, Mineral carbonation of CO<sub>2</sub>, Elements, 4 (2008)  
424 333-337.
- 425 [20] S.J. Gerdemann, W.K. O'Connor, D.C. Dahlin, L.R. Penner, H. Rush, Ex situ aqueous  
426 mineral carbonation, Environmental Science & Technology, 41 (2007) 2587-2593.
- 427 [21] W.J.J. Huijgen, G.J. Witkamp, R.N.J. Comans, Mineral CO<sub>2</sub> sequestration by steel slag  
428 carbonation, Environmental Science & Technology, 39 (2005) 9676-9682.
- 429 [22] M. Dejam, H. Hassanzadeh, The role of natural fractures of finite double-porosity  
430 aquifers on diffusive leakage of brine during geological storage of CO<sub>2</sub>, Int. J. Greenh.  
431 Gas Control, 78 (2018) 177-197.
- 432 [23] M. Dejam, H. Hassanzadeh, Diffusive leakage of brine from aquifers during CO<sub>2</sub>  
433 geological storage, Advances in Water Resources, 111 (2018) 36-57.
- 434 [24] M. Hanchen, V. Prigiobbe, R. Baciocchi, M. Mazzotti, Precipitation in the Mg-carbonate  
435 system - effects of temperature and CO<sub>2</sub> pressure, Chemical Engineering Science, 63  
436 (2008) 1012-1028.
- 437 [25] W.K. O'Connor, D.C. Dahlin, G.E. Rush, C.L. Dahlin, W.K. Collins, Carbon dioxide  
438 sequestration by direct mineral carbonation: process mineralogy of feed and products,  
439 Minerals & Metallurgical Processing, 19 (2002) 95-101.
- 440 [26] M.M. Maroto-Valer, D.J. Fauth, M.E. Kuchta, Y. Zhang, J.M. Andrésen, Activation of  
441 magnesium rich minerals as carbonation feedstock materials for CO<sub>2</sub> sequestration, Fuel  
442 Process. Technol., 86 (2005) 1627-1645.



- 443 [27] A. Sanna, M. Uibu, G. Caramanna, R. Kuusik, M.M. Maroto-Valer, A review of mineral  
444 carbonation technologies to sequester CO<sub>2</sub>, *Chemical Society Reviews*, 43 (2014) 8049-  
445 8080.
- 446 [28] C. Unluer, A. Al-Tabbaa, Enhancing the carbonation of MgO cement porous blocks  
447 through improved curing conditions, *Cement and Concrete Research*, 59 (2014) 55-65.
- 448 [29] C. Unluer, A. Al-Tabbaa, Impact of hydrated magnesium carbonate additives on the  
449 carbonation of reactive MgO cements, *Cement and Concrete Research*, 54 (2013) 87-97.
- 450 [30] M. Liska, A. Al-Tabbaa, K. Carter, J. Fifield, Scaled-up commercial production of  
451 reactive magnesia cement pressed masonry units. Part II: Performance, *Proceedings of  
452 the Institution of Civil Engineers-Construction Materials*, 165 (2012b) 225-243.
- 453 [31] M. Liska, A. Al-Tabbaa, K. Carter, J. Fifield, Scaled-up commercial production of  
454 reactive magnesium cement pressed masonry units. Part I: Production, *Proceedings of  
455 the Institution of Civil Engineers-Construction Materials*, 165 (2012a) 211-223.
- 456 [32] A. Al-Tabbaa, Reactive magnesia cement, *Eco-Efficient Concrete*, (2013) 523-543.
- 457 [33] T.J. Wolery, A software package for geochemical modeling of aqueous systems:  
458 package overview and installation guide (version 7.0), Lawrence Livermore National  
459 Laboratory Livermore, CA, 1992.
- 460 [34] C. Christ, P. Hostetler, Studies in the system MgO-SiO<sub>2</sub>-CO<sub>2</sub>-H<sub>2</sub>O (II); the activity-  
461 product constant of magnesite, *American Journal of Science*, 268 (1970) 439-453.
- 462 [35] J. Kittrick, F. Peryea, Determination of the Gibbs free energy of formation of magnesite  
463 by solubility methods, *Soil Science Society of America Journal*, 50 (1986) 243-247.
- 464 [36] P. Ballirano, C. De Vito, S. Mignardi, V. Ferrini, Phase transitions in the Mg-CO<sub>2</sub>-H<sub>2</sub>O  
465 system and the thermal decomposition of dypingite, Mg<sub>5</sub>(CO<sub>3</sub>)<sub>4</sub>(OH)<sub>2</sub>·5H<sub>2</sub>O:  
466 Implications for geosequestration of carbon dioxide, *Chemical Geology*, 340 (2013) 59-  
467 67.

- 468 [37] S. Teir, S. Eloneva, C.-J. Fogelholm, R. Zevenhoven, Fixation of carbon dioxide by  
469 producing hydromagnesite from serpentinite, *Applied Energy*, 86 (2009) 214-218.
- 470 [38] Y. Wang, Z. Li, G.P. Demopoulos, Controlled precipitation of nesquehonite  
471 ( $\text{MgCO}_3 \cdot 3\text{H}_2\text{O}$ ) by the reaction of  $\text{MgCl}_2$  with  $(\text{NH}_4)_2\text{CO}_3$ , *Journal of Crystal Growth*,  
472 310 (2008) 1220-1227.
- 473 [39] D.K. Panesar, L. Mo, Properties of binary and ternary reactive MgO mortar blends  
474 subjected to  $\text{CO}_2$  curing, *Cement and Concrete Composites*, 38 (2013) 40-49.
- 475 [40] Z. Zhang, Y. Zheng, Y. Ni, Z. Liu, J. Chen, X. Liang, Temperature-and pH-dependent  
476 morphology and FT-IR analysis of magnesium carbonate hydrates, *The Journal of*  
477 *Physical Chemistry B*, 110 (2006) 12969-12973.
- 478 [41] L. Hopkinson, P. Kristova, K. Rutt, G. Cressey, Phase transitions in the system MgO-  
479  $\text{CO}_2\text{-H}_2\text{O}$  during  $\text{CO}_2$  degassing of Mg-bearing solutions, *Geochimica Et*  
480 *Cosmochimica Acta*, 76 (2012) 1-13.
- 481 [42] P. Ballirano, C. De Vito, V. Ferrini, S. Mignardi, The thermal behaviour and structural  
482 stability of nesquehonite,  $\text{MgCO}_3 \cdot 3\text{H}_2\text{O}$ , evaluated by in situ laboratory parallel-beam  
483 X-ray powder diffraction: New constraints on  $\text{CO}_2$  sequestration within minerals,  
484 *Journal of Hazardous Materials*, 178 (2010) 522-528.
- 485 [43] S. Adham, A. Hussain, J.M. Matar, R. Dores, A. Janson, Application of Membrane  
486 Distillation for desalting brines from thermal desalination plants, *Desalination*, 314  
487 (2013) 101-108.
- 488 [44] S. Mignardi, C. De Vito, V. Ferrini, R.F. Martin, The efficiency of  $\text{CO}_2$  sequestration  
489 via carbonate mineralization with simulated wastewaters of high salinity, *Journal of*  
490 *Hazardous Materials*, 191 (2011) 49-55.

- 491 [45] Y. Soong, A.L. Goodman, J.R. McCarthy-Jones, J.P. Baltrus, Experimental and  
492 simulation studies on mineral trapping of CO<sub>2</sub> with brine, Energy Conversion and  
493 Management, 45 (2004) 1845-1859.
- 494 [46] Y. Soong, D.L. Fauth, B.H. Howard, J.R. Jones, D.K. Harrison, A.L. Goodman, M.L.  
495 Gray, E.A. Frommell, CO<sub>2</sub> sequestration with brine solution and fly ashes, Energy  
496 Conversion and Management, 47 (2006) 1676-1685.
- 497 [47] M.H. El-Naas, Reject brine management, Desalination, Trends and Technologies, (2011)  
498 237-252.
- 499 [48] PUB, Desalinated Water, [https:// www.pub.gov.sg /watersupply /fournationaltaps](https://www.pub.gov.sg/watersupply/fournationaltaps)  
500 /desalinatedwater.
- 501 [49] H. Dong, E.-H. Yang, C. Unluer, F. Jin, A. Al-Tabbaa, Investigation of the properties of  
502 MgO recovered from reject brine obtained from desalination plants, Journal of Cleaner  
503 Production, 196 (2018) 100-108.
- 504 [50] H. Dong, C. Unluer, E.-H. Yang, A. Al-Tabbaa, Recovery of reactive MgO from reject  
505 brine via the addition of NaOH, Desalination, 429 (2018) 88-95.
- 506 [51] H. Dong, C. Unluer, E.-H. Yang, A. Al-Tabbaa, Synthesis of reactive MgO from reject  
507 brine via the addition of NH<sub>4</sub>OH, Hydrometallurgy, 169 (2017) 165-172.
- 508 [52] Z.H. Hao, F.L. Du, Synthesis of basic magnesium carbonate microrods with a "house of  
509 cards" surface structure using rod-like particle template, Journal of Physics and  
510 Chemistry of Solids, 70 (2009) 401-404.
- 511 [53] D. Wu, B.J. Luo, W. Liu, L.C. Wang, Y. Yao, X.P. Huang, Study on the process  
512 optimization for intermediate Magnesium Carbonate Tri-hydrate, Advanced Materials  
513 Research, 960 (2014) 199-203.

514 [54] R. Dell, S. Weller, The thermal decomposition of nesquehonite  $\text{MgCO}_3 \cdot 3\text{H}_2\text{O}$  and  
515 magnesium ammonium carbonate  $\text{MgCO}_3 \cdot (\text{NH}_4)_2\text{CO}_3 \cdot 4\text{H}_2\text{O}$ , Transactions of the  
516 Faraday Society, 55 (1959) 2203-2220.

517 [55] J. Lanas, J.I. Alvarez, Dolomitic lime: thermal decomposition of nesquehonite,  
518 Thermochimica Acta, 421 (2004) 123-132.

519 [56] UNFCCC, The Paris Agreement Conference of the parties to the UNFCCC, (2015).

520

521

522

523 **Appendix – Chemical composition of HMCs and CO<sub>2</sub> captured percentage**

524

525 HMCs synthesized from Mg(OH)<sub>2</sub> slurry

526 Initially, 0.82 g Mg(OH)<sub>2</sub> is added into 200 ml distil water at a Mg(OH)<sub>2</sub>/CO<sub>2</sub> molar ratio of 1.

527 Assuming a purity of 92% for Mg(OH)<sub>2</sub>, the remaining 8% impurity is dolomite which does

528 not react or dissolve in the solution. The final precipitates consist of uncarbonated brucite,

529 dypingite and dolomite as supported by XRD results (Figures 5 and 7), which after calcination

530 decompose into MgO, MgO, and CaO·MgO, respectively. Let x and y denote the weights of

531 the uncarbonated brucite and dypingite, respectively. The weight of dolomite is 0.066 g

532 calculated based on 8% of the initial sample weight (i.e., 0.82 g). Residues after the TG/DTA

533 test is 50.6% (Figure 10). Based on the given information, the following equation can be

534 established.

535 
$$\frac{\frac{40}{58}x + \frac{40}{96.8}y + 0.82 \times 0.08 \times \frac{96}{184}}{x + y + 0.82 \times 0.08} = 0.506 \quad (A1)$$

536 Furthermore, the concentration of Mg<sup>2+</sup> in the residue was measured to be 308.4 ppm (0.308

537 g/L) as shown in Table 3. Thus,

538 
$$\frac{\frac{24}{58}x + \frac{24}{96.8}y}{0.2} = \frac{\frac{24}{58} \times 0.82 \times 0.92}{0.2} - 0.308$$

539 (A2)

540

541 By solving the two Eqns. (A1) and (A2), the weights of uncarbonated brucite and dypingite are

542 calculated to be 0.27 g and 0.55 g, respectively. The sum of the weights of uncarbonated brucite,

543 dolomite and dypingite was calculated to be 0.89 g, which was higher than 0.46 g of the

544 weighted precipitate as shown in Table 3. This was mainly due to the weight losses during the

545 process of separating the samples from the solution and grinding. The captured CO<sub>2</sub> percentage

546 was calculated by measuring the weight of CO<sub>2</sub> in the HMCs (dypingite) divided by the initial

547 input of CO<sub>2</sub> degassed to the system at the Mg(OH)<sub>2</sub>/CO<sub>2</sub> molar ratio of 1, which was calculated  
 548 to be 43.7% in consideration of 8% impurity.

549

550 Table A1 Concentration of Mg<sup>2+</sup> in the residue and final weight of HMCs obtained from

551 Mg(OH)<sub>2</sub> slurry and reject brine

	Mg <sup>2+</sup> in the residue solution (ppm)	Weight of solids (g)
Mg(OH) <sub>2</sub> slurry	309.9 ± 5.2	0.46 ± 0.20
Reject brine	161.5 ± 9.1	1.24 ± 0.14

552

553 HMCs synthesized from reject brine

554 The same principal applies to HMCs synthesized from the reject brine. The Mg(OH)<sub>2</sub> sample  
 555 precipitated from reject brine in the first step contains 6.3% calcite as the impurity which has  
 556 been detailed in [50]. The XRD result confirms that HMCs after carbonation of Mg(OH)<sub>2</sub>  
 557 consisted of nesquehonite, uncarbonated brucite and calcite, which after calcination decompose  
 558 into **MgO, MgO and CaO**, respectively. Let  $x$  and  $y$  denoted the weights of uncarbonated brucite  
 559 and nesquehonite, respectively. The weight of calcite is 0.052 g calculated based on 6.3% of  
 560 the initial sample weight (i.e., 0.82 g). Residues after the TG/DTA test is 31.3% (Figure 10).  
 561 Based on the given information, the following equation can be established.

$$562 \frac{\frac{40}{58}x + \frac{40}{138}y + 0.82 \times 0.063 \times \frac{56}{100}}{x + y + 0.82 \times 0.063} = 0.313 \quad (A3)$$

563 Furthermore, the concentration of Mg<sup>2+</sup> in the residue brine was measured to be 159.3 ppm  
 564 (0.159 g/L) as shown in Table 3. Thus,

$$565 \frac{\frac{24}{58}x + \frac{24}{138}y}{0.2} = \frac{\frac{24}{58} \times 0.82 \times 0.937}{0.2} - 0.159 \quad (A4)$$

566

567 By solving the two Eqns. (A1) and (A2), the weights of uncarbonated brucite and nesquehonite  
 568 are calculated to be 0.06 g and 1.51 g, respectively. The captured CO<sub>2</sub> percentage was  
 569 calculated by measuring the weight of CO<sub>2</sub> in the HMCs (nesquehonite) divided by the initial

570 input of CO<sub>2</sub> degassed to the system at the Mg(OH)<sub>2</sub>/CO<sub>2</sub> molar ratio of 1, which was calculated  
571 to be 82.6% in consideration of 6.3% impurity. A successful sequestration of CO<sub>2</sub> into reject  
572 brine as HMCs was therefore achieved to obtain an efficiency as high as 82.6%, which was  
573 significantly improved compared to the Mg(OH)<sub>2</sub> slurry.

574