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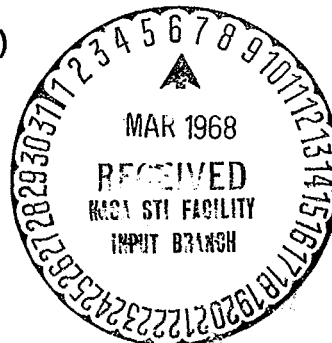
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Report No. 1111-2

COMPUTER PROGRAM FOR THE ANALYSIS
OF ANNULAR COMBUSTORS

VOLUME 11: OPERATING MANUAL

Prepared for the
National Aeronautics and Space Administration
Air Breathing Engine Division
Lewis Research Center
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NORTHERN RESEARCH AND ENGINEERING CORPORATION
219 Vassar Street
Cambridge, Massachusetts 02139

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Dr. A. D. Carmichael, Professor A. H. Lefebvre, I. N. Momtchiloff, and Professor D. B. Spalding contributed in a consulting capacity.

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SUMMARY

This is the second of two volumes devoted to a computer program for predicting the performance of an annular combustor. It is intended to form a self-contained operating manual allowing the program to be operated without reference to Volume I.

INTRODUCTION

In this volume the computer program, which incorporates the methods discussed in Volume I, is described and presented.

Arrangement of Report

First, there is a brief description of each of the subroutines, and the complete set of flow charts is presented. Then the procedures for setting up the program input are described, and samples of input data-- for library data and for the overall test case described in Volume I - are shown. The output format is illustrated by the computer printout for the same test case.

The Fortran listing of the program, a compilation of program messages, and a guide to the Fortran nomenclature, are presented as appendices.

A copy of the program can be obtained by anyone interested in using it by writing to Mr. Jack S. Grobman, NASA-Lewis Research Center, 21000 Brookpark Road, Cleveland, Ohio 44135.

PROGRAM DESCRIPTION

This section shows how the calculation methods described in Volume I are fitted into the program.

As explained in Volume I, the program consists of four independent subprograms, each of which contains a family of subroutines. A brief discussion of the purpose and content of each subroutine is given here, together with a set of flow charts. Numerical techniques used in the program are also discussed. A complete Fortran listing of the program is given in Appendix IV, and the Fortran nomenclature is defined in Appendix VI.

Control Subprogram

The control subprogram sets up starting values for the whole calculation. The action taken depends on the values of the indices NCASE and INPUT. NCASE is the number of cases to be considered in the run; if $NCASE > 1$ the control subprogram prepares starting values for the second case at the conclusion of the first. INPUT indicates which variables are to be altered from one case to the next.

If $NCASE = 0$, the input data are read in and written out, but none of the main calculations are carried out.

The main program and subroutines will now be described in turn.

Program CLARE

This is the main program. It calls subroutines INPUT1 and INPUT2 and the control subroutines for each of the subprograms. The flow chart is shown on Figure 1.

Subroutine INPUT1

In this subroutine, all run data (i.e. data that do not change from one case to the next) are read in. Units are converted where necessary, subroutine TAPE is called to obtain the data required from the library tape, and subroutine GEOM is called to set up geometric parameters required later in the program. The data are then written out in a convenient format. INPUT1 is only called once in each run, at the beginning of the first case.

The flow chart for subroutine INPUT1 is shown on Figure 2.

Subroutine INPUT2

This subroutine is called by CLARE at the beginning of each case of a run. It reads in the case data (i.e. the data that alter from one case of a run to the next) and writes them out.

The flow chart for Subroutine INPUT2 is shown on Figure 3.

Subroutine TAPE

Subroutine TAPE selects from the library tape the data that are required for use in the program. The library tape is designated KTAPE in the program, and Subroutine TAPE is the only subroutine that refers to it.

The discharge-coefficient and initial-jet-angle data are taken from the library tape as follows. The first set of hole data is read into core storage. Then the set of indices denoting hole types in the flame tube is searched to see whether hole type "1" is required. If so, these data are preserved in core storage; otherwise,

the data are overwritten by the set of data for the next hole type on the library tape. In this way, a "short list" of data for the hole types that are to be used in the combustor is assembled.

The generalized empirical diffuser data and the flame-emissivity data are treated in a similar way. The flow chart is given on Figure 4.

Subroutine GEOM

This subroutine calculates various geometric quantities, such as reference area, total hole areas, and cross-sectional areas, that are of interest or required elsewhere in the program. It also fixes the axial locations of the calculation points as follows:

1. One calculation point for each axial position at which holes are located. There may be more than one row of holes at a given axial position; the calculation point for all these hole rows is located at the upstream edge of the holes in the first row specified on the input data.
2. Calculation points at specified intervals downstream of all cooling slots (up to a maximum of five per cooling slot).
3. Calculation points as specified in the input. (These are specified as rows of holes with hole type zero).
4. A calculation point at the very end of the combustor.

Linear or parabolic interpolation is used to provide the values of quantities that are required at each calculation point. (Input quantities are provided at each geometric input point or at each hole-row centerline).

The flow chart for subroutine GEOM is shown on Figure 5.

Subroutine BLOCKDATA

This subroutine consists of a series of data statements providing recommended starting values for a number of variables, including "optional" input quantities.

Diffuser Subprogram

The diffuser subprogram calculates the flow properties in the diffuser from the compressor outlet to the first calculation point in each annulus. Subroutine DIFLOW contains the entry points to the diffuser subprogram, and organizes the internal calculation procedure. The methods of calculation used are:

1. The streamtube method
2. The empirical-data method
3. The mixing-equation method

The streamtube method is organized in subroutines TUBCTS, TUBSTA, and TUBSA1, and the analysis is carried out in subroutine TUBFW1, TUBEIN, TUBANL, and NEWRAD. The empirical-data method is organized in subroutines EMPTCS and EMPSTA, and the analysis is carried out in EMPANL and PROFL. The mixing-equation method is contained in subroutine DIFLOW. The diffuser subprogram also calls subroutines DCUTPT, GASTBL, SLOPE, IIAPI, and INTPL8.

An overall flow chart for the diffuser subprogram is shown on Figure 6. The function of each subroutine will now be discussed in more detail.

Subroutine DIFLOW

Subroutine DIFLOW has three main functions:

1. To organize the calculation procedure used in the diffuser subprogram depending on the input variable NDIFF
2. To calculate the flow properties in the two annuli between the snout and the outer casing if the mixing equation is being used
3. To calculate the flow properties beyond Station 2 if the diffuser does not have a snout

Station numbers for the diffuser are defined on pages 14-16 of Volume 1.

The subroutine has three entry points splitting the program into three separate parts. The three parts perform the following functions:

1. The first part organizes the calculation procedure between Stations 1 and 2. If the mixing equation is to be used between Stations 2 and 4, a corrective term for the curvature of the passages is calculated.
2. Following Entry DIFLW the calculation procedure between Stations 2 and 4 is organized. If the diffuser does not have a snout, or if the mixing equation is being used between Stations 2 and 4, the flow properties at Station 4 are calculated.
3. The third part, following Entry DIFLW2, calculates the flow in the diffuser with a given mass-flow split using the streamtube method throughout.

A flow chart for subroutine DIFLOW is shown on Figure 7.

Subroutine TUBCTS

Subroutine TUBCTS is called by DIFLOW if the streamtube method is to be used between Stations 1 and 2. The subroutine:

1. Calls subroutine TUBEIN to calculate the inlet static pressure and the inlet streamtube properties
2. Calculates the reference velocity, Mach number, and dynamic head
3. Sets up an iteration loop calling TUBANL and NEWRAD to calculate the flow properties and the boundary-layer characteristics
4. Calculates the outlet velocity profile and the diffuser performance
5. Calls DOUTPT to print out the diffuser performance, and NEWRAD to print out the boundary-layer characteristics

A flow chart for subroutine TUBCTS is shown on Figure 8.

Subroutine TUBSTA

Subroutine TUBSTA is called by DIFLOW if the streamtube method is to be used between Stations 2 and 3. This subroutine is called before the iteration on the mass flow commences, and its function is to set up the geometric data in a form that can be used by subroutine TUBSA1.

The flow chart for subroutine TUBSTA is shown on Figure 9.

Subroutine TUBSA1

Subroutine TUBSA1 is called by DIFLOW to perform a streamtube

calculation between Stations 2 and 4. The subroutine is organized as a large DO loop for the two annular passages, with the following steps:

1. Call subroutine TUBEIN to calculate the streamtube properties
2. Set up an iteration loop calling TUBANL and NEWRAD to calculate the flow properties and the boundary-layer characteristics
3. Calculate the flow properties and diffuser performance up to Station 3
4. Calculate flow properties and diffuser performance up to Station 4, assuming the flow mixes between Stations 3 and 4
5. Call DOUTPT to print out the diffuser performance, and NEWRAD to print out the boundary-layer characteristics

The flow chart for subroutine TUBSA1 is shown on Figure 10.

Subroutine TUBFW1

Subroutine DIFLOW calls TUBFW1 during the iteration on the mass-flow split if the streamtube method is used between Stations 1 and

2. For a given flow split at Station 2, TUBFW1 calculates:
 1. The geometric positions of the flow split
 2. The area-mean velocity and weight-mean velocity for the flow streams into each annulus and the snout

The flow chart for subroutine TUBFW1 is shown on Figure 11.

Subroutine TUBEIN

Subroutine TUBEIN is called by TUBCTS and TUBSA1 to calculate the input quantities for the streamtube calculation. In TUBEIN the following calculations are performed:

1. If the static pressure is not given (i.e. if TUBEIN is called by TUBCTS), calculate the static pressure
2. Split the flow into a number of streamtubes and calculate the total pressure for each streamtube
3. Calculate the flow area for each streamtube when the flow is accelerated isentropically to Mach 1

The flow chart for subroutine TUBEIN is shown on Figure 12.

Subroutine TUBANL

Subroutine TUBANL is called by TUBCTS and TUBSA1, to calculate:

1. The pressure at each calculation point in the diffuser
2. The velocity and density of the wall streamtubes at each calculation point
3. The outlet velocity profile

TUBANL calculates the above properties by performing a one-dimensional analysis for each streamtube, and satisfying the continuity equation for the section at each calculation point. Its flow chart is shown on Figure 13.

Subroutine NEWRAD

Subroutine NEWRAD is called by TUBCTS and TUBSA1 to perform

a boundary-layer calculation for each wall of the diffuser.

Subroutine NEWRAD also:

1. Calculates the position of separation, if it occurs
2. Checks the solution for convergence
3. Calculates a new guess for the boundary-layer displacement thickness
4. Following Entry NEWRI, prints out the boundary-layer properties

The flow chart for subroutine NEWRAD is shown on Figure 14.

Subroutine EMPCTS

Subroutine EMPCTS is called by DIFLOW if the empirical-data method is to be used between Stations 1 and 2. The subroutine is divided into two parts. The first part:

1. Calculates the static pressure at inlet
2. Calculates the reference velocity, Mach number, and dynamic head
3. Calls EMPANL to calculate the diffuser performance from empirical data
4. Calls PROFL to calculate the outlet velocity profile
5. Calls DOUTPT to print out the results

The second part following Entry EMPDTI is called during the iteration on the mass-flow split, to:

1. Call PROFL to calculate the geometric position of the

flow split

2. Calculate the weight-mean, and area-mean velocities for the flow streams into each annulus and the snout

The flow chart for subroutine EMPCTS is shown on Figure 15.

Subroutine EMPSTA

Subroutine EMPSTA is called by DIFLOW to calculate the diffuser performance between Stations 2 and 3 using empirical data.

The calculation is performed in the following steps:

1. Set up a DO loop for the two annular passages
2. Call EMPANL to calculate the diffuser performance between Stations 2 and 3
3. Call PROFL to calculate the flow properties at Station 3
4. Calculate the flow properties at Station 4 assuming the flow mixes between Stations 3 and 4
5. Call DOUTPT to print out the diffuser performance

The flow chart for subroutine EMPSTA is shown on Figure 16.

Subroutine EMPANL

Subroutine EMPANL is called by subroutines EMPCTS and EMPSTA to calculate the diffuser performance from empirical data. EMPANL calls INTPL8 to perform Lagrangian interpolation from a table of data of diffuser effectiveness at various values of area ratio and a nondimensional length at a fixed value of inlet blockage. A correction

is made to allow for variations in inlet blockage. The flow chart for subroutine EMPANL is shown on Figure 17.

Subroutine PROFL

Subroutine PROFL is called by EMPCTS and EMPSTA and it is in two parts. The subroutine assumes that the velocity distribution at any section is given by a top-hat profile, and the first section calculates this velocity. The second section, following Entry PROFL1, calculates for a given flow split:

1. The geometric positions of the flow split
2. The area-mean velocity, and weight-mean velocity for the flow stream into each annulus and the snout

The flow chart for subroutine PROFL is shown on Figure 18.

Subroutine DOUTPT

DOUTPT is called by EMPCTS, EMPSTA, DIFLOW, TUBCTS, and TUBSA1 to print out the diffuser performance for the various diffusing passages.

Subroutine GASTBL

Subroutine GASTBL is a general subroutine which calculates:

1. The Mach number
2. The ratio of static temperature to stagnation temperature
3. The ratio of static pressure to stagnation pressure
4. The ratio of flow area to flow area for the same mass flow expanded isentropically to Mach 1

Either of the last two ratios may be given. It is assumed in this subroutine that the flow behaves as a perfect gas with constant specific heats; the specific heat ratio, γ , is taken to be 1.4.

Subroutine SLOPE

From a tabulated set of variable x against y , subroutine SLOPE calculates the gradient dy/dx from the equation:

$$\left(\frac{dy}{dx}\right)_i = \frac{1}{2} \left(\frac{y_{i+1} - y_i}{x_{i+1} - x_i} + \frac{y_i - y_{i-1}}{x_i - x_{i-1}} \right)$$

Subroutine IIAPI

Subroutine IIAPI performs parabolic interpolation for a single tabulated function.

Subroutine INTPL8

Subroutine INTPL8 is used to perform Lagrangian interpolation from a two-dimensional table of y tabulated against x and z . INTPL8 also calls upon its own subroutines, UNS, LAGRAN, and DISSER.

Air-Flow Subprogram

The air-flow subprogram calculates the flow properties in the flame tube and annuli from the first calculation point (which corresponds to the first hole row on the wall, as distinct from the dome) to the end of the combustor. It also organizes the mass-flow-split iteration.

The overall flow chart for the air-flow subprogram is shown on Figure 19. Each subroutine will now be described in turn.

Subroutine AIRFLO

This subroutine controls the air-flow calculation. It carries out the following operations:

1. An initial estimate of the mass-flow split is based on the

total hole areas in the dome and on each annulus .

2. Subroutine DIFLOW is called to obtain initial conditions on the dome and at the start of each annulus .
3. From the discharge characteristics of the holes in the dome, the primary-zone pressure is obtained .
4. The annulus equations are solved (Subroutine EQUAN) at each calculation point along the inner annulus to the secondary holes; then along the outer annulus to the secondary holes .
5. Subroutine PRTEMP is called to obtain the primary-zone temperature and initial conditions for the flame-tube calculations .
6. At each calculation point from the secondary holes to the end of the combustor:
 - a. The annulus equations are solved for the inner annulus .
 - b. The annulus equations are solved for the outer annulus .
 - c. The flame-tube equations are solved (Subroutine EQUFT).
7. If the air mass flows remaining in the annuli are of opposite sign, the initial mass-flow split between the two annuli is adjusted and Steps 2 to 6 are repeated.
8. If the air mass flows remaining in the annuli are not approximately zero, the initial mass-flow split between dome holes and annuli is adjusted and Steps 2 to 7 are repeated .

The flow chart for Subroutine AIRFLO is shown on Figure 20. To avoid overflowing the computer memory, this subroutine has been divided into two sections (AIRFLO and BIRFLO) as noted on the flow chart.

Subroutine DISJET

Subroutine DISJET determines jet discharge parameters:

1. Jet information to be used by Subroutine JETMIX:
 - a. Initial jet-air mass flow rate
 - b. Jet angle of discharge
 - c. Jet discharge coefficient
2. Jet information to be used by Subroutines EQUAN and EQUFT:
 - a. Initial jet-air mass flow rate
 - b. Initial jet momentum
 - c. Initial axial jet momentum
 - d. Initial jet enthalpy

This subroutine uses discharge-coefficient and jet-angle data that have been selected from the library tape and set up in COMMON by Subroutine TAPE.

Another function performed by this subroutine is to sense when unrealistic conditions are occurring in the combustor (due to an incorrect mass-flow-split estimate), and to set the residual annulus flows so as to ensure that the next estimate of mass-flow split is adjusted in the right direction. This is done in the following way:

1. When the flame-tube static pressure is higher than the annulus static pressure (or, in the case of scoops, the annulus total pressure), the annulus equations are not solved in the normal way. Instead, increments of mass

flow proportional to the local hole area are added to the annulus flow at all subsequent calculation points down to the end of the combustor. The positive mass flow at the end of the annulus ensures that in subsequent flow-split estimates the flow through the dome will be increased and the flame-tube pressure lowered.

2. When the pressure drop from annulus to flame tube is such that the required flow through the hole exceeds that available in the annulus, the annulus equations are not solved in the normal way. Instead, increments of mass flow proportional to the local hole area are subtracted from the annulus flow at all subsequent calculation points down to the end of the combustor. The negative mass flow at the end of the annulus ensures that in subsequent flow-split estimates the flow through the dome will be decreased and the flame-tube pressure increased.

An overall flow chart for Subroutine DISJET is shown on Figure 21.

Subroutine PRTEMP

This subroutine calculates conditions within the primary zone by solution of a simplified form of the flame-tube equations, assuming the primary zone acts as a stirred reactor. Flame-tube conditions are thus set up for the secondary-hole calculation point, so that from then on the flame-tube equations can be solved in the normal way.

This subroutine also calculates the fraction of air entering the secondary holes which recirculates upstream, if this fraction is not specified as input.

The flow chart is shown on Figure 22.

Subroutine EQUAN

This subroutine solves the equations for flow in the annuli. The main equation is a quadratic in $u_{an,2}$. The rest of the subroutine is concerned with evaluating the constants in this equation. The following effects are included:

1. A total-pressure loss due to expansion of the annulus air as it passes across the hole
2. The loss of air bled from the annulus for cooling purposes
3. The loss of air due to transpiration cooling, as well as air passing through penetration holes and cooling slots

The flow chart for subroutine EQUAN is shown on Figure 23.

Subroutine EQUFT

This subroutine solves the equations for flow in the flame tube downstream of the primary zone. As explained in Volume 1, the solution follows an iterative procedure. For convenience, this procedure is summarized again here. Calculations are performed for a control volume bounded by two adjacent calculation stations (defined as Station 1 and 2 for this discussion).

1. Initial values are assumed for $u_{ft,2}$, c_{p2} , and \dot{q} based on conditions at the upstream station (Station 1).
2. The energy equation is solved for $T_{ft,2}$.
3. Using this estimate of $T_{ft,2}$, improved estimates of c_{p2}

and \dot{q} are obtained.

4. Steps 2 and 3 are repeated until the change in $T_{ft,2}$ between successive cycles is smaller than FIENTH (which is supplied as data).
5. The momentum, continuity, and state equations are solved for an improved estimate of $u_{ft,2}$.
6. Steps 2 to 5 are repeated until the changes in $u_{ft,2}$ and $T_{ft,2}$ between successive $u_{ft,2}$ -cycles are smaller than $u_{ft,2} \cdot FIPHI$ and FIENTH respectively.

The flow chart for subroutine EQUFT is shown on Figure 24.

Subroutine HEATAD

This subroutine provides EQUFT with the heat-addition term in the energy equation. It makes use of:

1. The fuel-burning rate, supplied as input to the program.
2. The effective fuel calorific value, including a correction for dissociation.
3. Correlations for the specific heat of air and of a mixture of stoichiometric combustion products.

The flow chart is shown on Figure 25.

Subroutine JETMIX

This subroutine provides EQUFT with the characteristics of the residual jets (entering the flame tube through holes upstream of the

point under consideration). Mixing is calculated using one of three models, according to the value of the index NEF:

1. Mass-loss model
2. Equivalent-entrainment model
3. Profile-substitution model
4. Instantaneous-mixing model

Wall jets and penetration jets are calculated separately using the same model but different values of the mixing constant. In each case, the calculation proceeds stepwise along the jet from the hole to the axial position of the current calculation point.

The flow chart for this subroutine is shown on Figure 26.

Heat-Transfer Subprogram

An overall flow chart for the heat-transfer subprogram is shown on Figure 27.

Subroutine HEAT1

This subroutine carries out a noniterative heat-transfer calculation. The route through the subroutine is controlled by the index NHT1, which takes the following values:

- 1 for one-dimensional radiation, uncooled wall
- 2 for one-dimensional radiation, cooled wall
- 3 for two-dimensional radiation, uncooled wall
- 4 for two-dimensional radiation, cooled wall

The coefficients in the heat-balance equation are evaluated, using subroutines EEFT, COOL, and PROP, and the results are put in a form suitable for output.

The flow chart for this subroutine is shown on Figure 28.

Subroutine HEAT2

This subroutine carries out an iterative heat-transfer calculation. The route through the subroutine is controlled by the index NHT2, which takes the following values:

- 2 for longitudinal wall conduction
- 3 for radiation interchange between walls
- 4 for longitudinal conduction and radiation interchange
- 1 if none of these options required

The subroutine also writes out the results for the heat-transfer subprogram (whether the calculation is iterative or noniterative). The flow chart is shown on Figure 29.

Subroutine TWALL

This subroutine uses Newton's approximation to solve the heat-balance equation, which is of the following form:

$$D_1 T_w^4 + D_2 T_w^{2.5} + D_3 T_w + D_4 = 0$$

The flow chart is shown on Figure 30.

Subroutine EEFT

This subroutine calculates the emissivity of the flame in one of six ways, according to the value of the index NLUM:

- 1 Non-luminous correlation for distillate fuels
- 2 Non-luminous correlation for residual fuels
- 3 Lefebvre correlation for luminous flames

- 4 NREC 1964 correlation for luminous flames
- 5 NREC 1966 correlation for luminous flames
- 6 Interpolation from a table of experimental data

Subroutine PROP

This subroutine obtains average values for the specific heat, thermal conductivity, and the dynamic viscosity of a gas mixture containing oxygen, nitrogen, carbon dioxide, and water vapor. The flow chart for this subroutine is shown on Figure 31.

Subroutine COOL

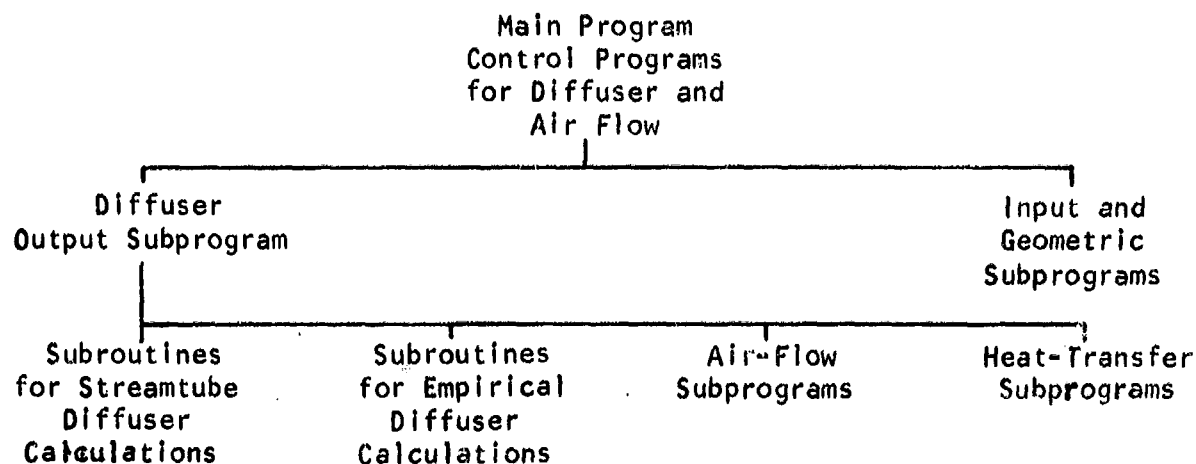
This subroutine calculates wall cooling parameters according to the value of the index NCOOL:

- 1 Film cooling
- 2 Transpiration cooling

The flow chart for this subroutine is shown on Figure 32.

Overlay Structure

In order to fit the whole program into the storage space available on the 7094, the program has been split into several links, which overwrite each other as the calculation proceeds. The sketch on the next page shows the overall arrangement, and the correct position for each subroutine is shown on Figure 33.



Numerical Techniques

The numerical techniques used in this program are quite simple, and need not be described in great detail. Most of them have been covered adequately in Volume I; only the iteration scheme on the overall mass-flow split will be discussed here.

Normal Iteration Procedure

As mentioned in Volume I, the iteration proceeds in two stages:

1. If the annulus flows at the end of the combustor, AFSTA and AFSTB, are of opposite sign, the mass flow through the dome is held constant and the ratio of the flows entering the two annuli is adjusted. The following ratio is used:

$$AFC = \frac{AFA}{AFA + AFB} \quad (2)$$

where AFA = flow entering inner annulus

AFB = flow entering outer annulus

A running check is kept on AFCL, the highest value of AFC for which AFSTA is negative and AFSTB is positive, and AFCU, the

lowest value of AFC for which AFSTA is positive and AFSTB is negative. At each step, the new value of AFC is taken to be $(AFCL + AFCU)/2$. At the start, values of AFCL and AFCU well outside the realistic range are chosen and the step size is limited to 1 per cent of AFC. In using this procedure it is assumed that the AFC corresponding to the converged solution will not lead to residual annulus flows of opposite sign at other values of AFS, the flow through the dome.

2. If AFSTA and AFSTB are of the same sign, AFS is adjusted in the following way. A running check is kept on AFSL, the highest value of AFS for which the residual flows are positive, and AFSU, the lowest value of AFS for which the residual flows are negative. At each step, the new value of AFS is taken to be $(AFSL + AFSU)/2$ and the change in AFS is split equally between AFA and AFB. At the start, values of AFSL and AFSU well outside the realistic range are chosen and the maximum step size is limited to 30 per cent of AFS.

Starting values of AFCL, AFCU, AFSL, and AFSU may be assigned as input; by judicious choice of these values the number of flow-split iterations may be substantially reduced. Likewise, starting values of AFS, AFA, and AFB may be assigned by supplying the input quantities DAFA and DAFB (fractions of total flow passing through inner and outer annuli, respectively). If no input values are supplied, starting values are assigned in Subroutines GEOM and INPUT2 on the basis of the total hole areas in the dome and the flame-tube walls.

Characteristics of the Method

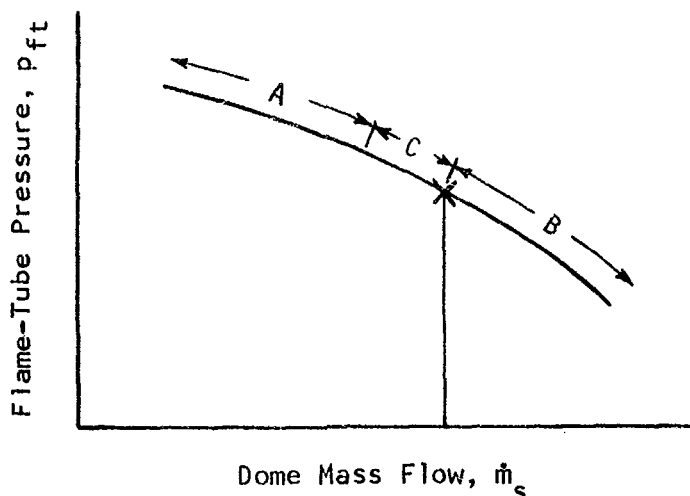
In a well-designed combustor (that is, one in which there is no flow out of the flame tube at the converged solution), the number of cycles to convergence depends on the accuracy required and the number of hole rows. To reduce AFSTA and AFSTB to 1 per cent of AF2 (the total mass flow) typically requires about 18 cycles. The number of cycles increases with the number of hole rows because the effect of small changes in upstream pressure builds up cumulatively down the combustor.

If the limit on the number of cycles permitted (LCANIL) is set too low, the program will print out an error message, "Increase LCANIL" when convergence fails to occur. However, there is no point in increasing LCANIL beyond about 50 because by that time the limit of accuracy of the machine has been reached - effectively:

AFSL = AFS = AFSU
and/or
AFCL = AFC = AFCU

If there is no convergence at 50 cycles and pressure reversal across the flame tube is still occurring, the program will print out an error message "Combustor poorly designed". This case will now be discussed more fully.

The relationship between the pressure at any point in the flame tube and the mass flow through the dome is of the form shown in the sketch.



By contrast, the pressures in the annuli are relatively unaffected by changes in the dome mass flow.

At low dome mass flows there will be a region (marked A in the sketch) in which pressure reversal across flame tube holes occurs. At high flows (B) the flame-tube pressure will be lowered, the hole pressure drop will be so high that more air will be called for than there is in the annulus, and the residual annulus flow will be negative.

Between A and B there will be a region C in which the residual flow is positive but no pressure reversal occurs.

In a badly designed combustor, region A may include the convergence point; there will then be no region C and the program will attempt to converge on the interface between A and B. Convergence will not be detected since the residual flows will not be near zero.

Decreasing the dome hole area will increase the flow resistance through the dome and may rectify the pressure reversal. Alternatively, the hole distribution along the flame-tube wall may be adjusted; the critical holes can easily be recognized since their discharge coefficients are zero when pressure reversal is just about to occur.

INPUT AND OUTPUT

This section contains the procedure for preparing the input data for program CLARE and a description of the types of output. Input and output sheets for the sample case discussed in Volume 1 of this report are shown.

Data required by the program are fed in via two input tapes, designated ITAPE and KTAPE. ITAPE refers to the normal input tape. KTAPE contains the library data which will only occasionally be altered between one run and the next; a deck of library data is supplied with the program.

Library Data

The library data consist of:

1. Hole-discharge-coefficient and jet-angle information. The data provided cover 100 different hole types, including all those mentioned in Reference 1 ; any number of additional hole types may be added. A key to these hole types is given in Table 1.
2. Diffuser-performance data for all straight-walled-annular and two-dimensional diffuser types shown in Figures 9 and 23 of Volume 1. Space is available for further data (such as curved-wall-diffuser data) to be added as they become available.
3. Flame-emissivity data for particular combustor configurations. Initially, no data are provided for this table, but the option is available for inserting a set of values of

emissivity at various pressures and temperatures and using an emissivity obtained from this table in the heat-transfer calculation.

The method used to prepare the data-input sheet for this group is described below.

<u>Line</u>	<u>Location</u>	<u>Input Item</u>	<u>Type of Number*</u>	<u>Fortran Name</u>	<u>Description</u>
1	1-10		I	NMXTYP	Number of hole types for which discharge-coefficient data are to be given. There is no limit on this quantity.
2	1-10		I	NHTYP	Identification number indicating hole type. These numbers should run from 1 through NMXTYP. A key to the hole type numbers is given in Table 1.
2	11-20		R	DXH	Hole radius or distance from hole center-line to upstream edge, inches. For continuous cooling slots, this quantity should be zero.
2	21-30		R	HAA	Hole area, square inches. For continuous cooling slots this is the face area per inch width, i.e. the slot height, inches.
2	31-35		I	NSC00Q	Index. 1 in tens position indicates that no initial-jet-angle data are available. 0 in units position indicates that the discharge coefficient is based on flush hole area, 1 indicates that it is based on hole face area, and 2 indicates that the hole type is a continuous cooling scoop.

* R refers to real numbers. These should be written with decimal points; they may appear anywhere within their allotted fields. I refers to integers. These are written without decimal points on the right side of their fields.

<u>Line</u>	<u>Location</u>	<u>Input Item</u>	<u>Type of Number</u>	<u>Fortran Name</u>	<u>Description</u>
2	36-40		I	NSPA	Number of values of pressure-loss factor at which discharge coefficient is to be given (maximum value 15).
2	41-50	$1 + \frac{\Delta P_h}{q_{an}}$	R	DPHSA	First value of pressure-loss factor
2	51-60	C_d	R	CDSA	First value of corrected discharge coefficient.
2	61-70	ξ	R	GXISA	First value of initial jet angle
3	11-20	$1 + \frac{\Delta P_h}{q_{an}}$	R	DPHSA	Second value of pressure-loss factor
3	21-30	C_d	R	CDSA	Second value of corrected discharge coefficient
3	31-40	ξ	R	GXISA	Second value of initial jet angle
3	41-50	$1 + \frac{\Delta P_h}{q_{an}}$	R	DPHSA	Third value of pressure-loss factor
3	51-60	C_d	R	CDSA	Third value of corrected discharge coefficient
3	61-70	ξ	R	GXISA	Third value of initial jet angle

The remaining values of $1 + \frac{\Delta P_h}{q_{an}}$, C_d , and ξ are listed on subsequent lines in the same format as Line 3 until all NSPA of the sets of values for this hole type have been given. The last set is on line N.

Lines 2 through N are repeated until all NMXTYP hole types have been covered. The last values are on line N_A .

<u>Line</u>	<u>Location</u>	<u>Input Item</u>	<u>Type of Number</u>	<u>Fortran Name</u>	<u>Description</u>
N_A+1	72		1	INDEX	The program expects to find a 1 here, indicating that the correct number of hole-data cards have been read.
N_A+2	1-10		1	NWALMX	Number of diffuser types for which performance data are to be given. There is no limit on this quantity. ¹
N_A+3	1-10		1	NCARD(1)	Number of lines used for data for first diffuser type.
N_A+3	11-20		1	NCARD(2)	Number of lines used for data for second diffuser type.
					The remaining values of NCARD are entered on this line (and, if necessary, subsequent lines up to N_B) in the usual 7-column integer format until all NWALMX values are listed.
					The following lines N_B+1 through N_C relate to the first diffuser type.
N_B+1	1-10		1	NWALL	Identification number indicating diffuser type. These numbers should run from 1 through NWALMX.
N_B+1	11-20		1	NXDIFD	Number of values of ARDTA (area ratio A_2/A_1) that are to be given (maximum value 200).
N_B+1	21-30		1	NYDIFA	Number of values of EFDTA (diffuser effectiveness) that are to be given (maximum value 200).
N_B+1	31-40		1	NZDIFA	Number of values of XLNDTA (nondimensional length) that are to be given (maximum value 20).
N_B+1	41-50		1	NCDIFA	Index. Sign indicates the form in which the data are tabulated: positive sign

¹ If NWALMX \geq 10, the dimension of NCARD should be increased.

<u>Line</u>	<u>Location</u>	<u>Input Item</u>	<u>Type of Number</u>	<u>Fortran Name</u>	<u>Description</u>
					indicates that NXDIFD = NYDIFA/NZDIFA; negative sign indicates that NXDIFD = NYDIFA. Hundreds position should always contain 1. Number in tens position indicates degree of Lagrangian interpolation in X direction that is to be used with these data. Number in units position indicates degree of interpolation in Z direction.
N_B+1	51-60	E_1	R	E1DTAA	Value of (1-inlet blockage) at which this set of data was taken.
N_B+2	1-10	ξ	R	EFDTA(1)	First value of diffuser effectiveness.
N_B+2	11-20	ξ	R	EFDTA(2)	Second value of diffuser effectiveness.
					The remaining values of diffuser effectiveness are entered on this and subsequent lines in the usual 7-column real format. The first set of values of EFDTA are for the first value of XLNDTA, the next set of values of EFDTA are for the second value of XLNDTA, and so on.
					Immediately following (not necessarily on a new card), the NXDIFD values of area ratio, ARDTA are listed, then the NZDIFA values of nondimensional length, XLNDTA. The last value is on line $N_C = N_B + \text{NCARD}(1)$.
					Data for the second diffuser type (NWALL = 2) are presented in the same way as for type 1, on line N_C+1 through line $N_C + \text{NCARD}(2)$.

<u>Line</u>	<u>Location</u>	<u>Input Item</u>	<u>Type of Number</u>	<u>Fortran Name</u>	<u>Description</u>
					Data for the remaining diffuser types are entered in the same way. The last data for diffuser type NWALMX are on line N_D .
N_D+1	72		I	INDEX	The program expects to find a 1 here, indicating that the correct number of diffuser-data cards have been read.
N_D+2	1-10		I	NTFT	Number of points at which flame temperature is to be specified in table of empirical flame-emissivity data.
N_D+2	11-20		I	NEFT	Number of points at which emissivity is to be given in table of empirical flame-emissivity data. Normally $NEFT = NTFT \times NPFT$.
N_D+2	21-30		I	NPFT	Number of points at which pressure is to be given in table of empirical flame-emissivity data.
N_D+2	31-40		I	NFORM	Index. This refers to the way in which data are presented and interpolated; rules for assigning values to it were given above in connection with NCDIFA. It normally takes the value 133.
N_D+3	1-10		R	TABTFT(1)	First value of flame temperature (deg F) in table of empirical flame-emissivity data. Subsequent values of flame temperature are entered in the usual 7-column format, immediately followed by values of pressure, TABPFT (lbf/ft ²) and emissivity, TABEFT. The last value is on line N_E .
N_E+1	72		I	INDEX	The program expects to find a 1 here, indicating that the correct

<u>Line</u>	<u>Location</u>	<u>Input Item</u>	<u>Type of Number</u>	<u>Fortran Name</u>	<u>Description</u>
					number of emissivity-data cards have been read.

This completes the library data.

Normal Input Data

The procedure used for setting up the normal input data is described below. There are a number of quantities that the user will only occasionally wish to specify; these are treated in the following way. Recommended values are automatically supplied to the program via a BLOCK DATA subroutine; any quantities that the user wishes to vary are then overwritten via the READ statement. In the list below, the word "optional" is given with these quantities, and the recommended values are shown in parentheses.

Run Identification

Line 1 of the normal input data contains a run identification message in columns 1-72. This message is later written out at the head of the output sheet.

Fixed Data - Integer

The first group of data is fed in via the namelist FIXED1, using the normal format¹. The variables in FIXED1 are as follows:

<u>Name</u>	<u>Description</u>
NCASE	No. of cases to be considered. If zero, major sub-routines are not entered. Optional (0).

¹\$FIXED1 beginning in column 2 of the first card, followed by the names of the variables and their input values in pairs, separated by commas, on this card and columns 2 to 80 of succeeding cards. The end of the list is marked by a \$.

<u>Name</u>	<u>Description</u>
NRECT	Index. 1 for annular combustors, 2 for combustors of rectangular cross-section. Optional (1).
NG	No. of geometric input points. Maximum value 120.
NH	No. of hole rows. Maximum value 50.
NWH	No. of first hole row on the flame-tube wall (as distinct from the dome).
NSH	No. of hole row that marks the end of the primary zone. If there are hole rows on both annuli at this location, NSH must equal the hole row number on the inner annulus.
NSNOUT	Index. 1 if there is a snout. 0 otherwise.
NWALL1 NWALL2	Indices designating empirical diffuser data to be used in sections 1-2 and 2-4 respectively. Optional (1 for annular combustors, 2 for two-dimensional).
INPUT	Index. 0 if input flow conditions varied between cases. 1 if program routing varied. Optional (0).
K4	Index. 1 if flow split at secondary holes is specified. Otherwise 0. Optional (0).
K6	Index. 0 for no swirler 1 for specified swirler 2 for unspecified swirler Optional (0).
NCOOL	Index. 1 for film cooling 2 for transpiration cooling Optional (1).
NUMSW	Number of swirlers. Optional (0). NUMSW must be supplied if K6 = 1 or 2.
NBLADE	Number of swirler blades. Optional (8)
IPRINT	Index. 1 if intermediate results are to be printed! 0 otherwise. Optional (0).

Combustor Geometry

The next set of cards contains the combustor geometry. The first and last cards define the beginning and end of the combustor. There should

¹This option is only available if output is on tape unit 6.

be NG cards in this group, each containing the following:

<u>Location</u>	<u>Type of Number</u>	<u>Fortran Name</u>	<u>Description</u>
1-10	R	XINCH	Axial location, measured from compressor discharge, inches. The XINCH values should increase monotonically; no two should be equal. It is advisable to specify the geometry at points a small distance downstream of each stepped cooling slot.
11-20	R	CA	Inner casing diameter, inches.
21-30	R	SA	Inner snout diameter, ¹ inches. This field should be left blank if there is no snout at this location.
31-40	R	FTA	Inner flame-tube diameter, ¹ inches. If XINCH coincides with the location of a cooling slot, the larger of the two FTA values should be given.
41-50	R	FTB	Outer flame-tube diameter, ¹ inches. If there is a cooling slot at this point, the smaller of the two FTB values should be given.
51-60	R	SB	Outer snout diameter, ¹ inches. If there is no snout at this location, the field should be left blank.
61-70	R	CB	Outer casing diameter, ¹ inches.

The diffuser section should not occupy more than 50 geometric input points, and at least one geometric input point should lie upstream of the snout lip.

Hole and Miscellaneous Data

The next set of cards contains the hole data and fuel-burning-rate distribution. The casing temperature may also be specified on these cards. There should be NH cards in this group, each containing the following:

<u>Location</u>	<u>Type of Number</u>	<u>Fortran Name</u>	<u>Description</u>
1-10	R	XH	Axial location of hole-row center-

¹ If the combustor is of rectangular cross section, "diameter" is replaced by "dimension from arbitrary datum".

<u>Location</u>	<u>Type of Number</u>	<u>Fortran Name</u>	<u>Description</u>
			line, inches. These values should lie between the first value of XINCH for which flame tube coordinates are given, and the last value of XINCH. Values of XH should generally increase, but there may be up to six rows of holes (i.e. six cards) corresponding to a single value of XH. For splash-ring cooling slots, the location specified should be that of the slot exit.
11-20	R	HAB	Hole area, square inches. In the case of continuous cooling slots, this is the height of the slot in inches. This field may be left blank if the hole area is the same as that used in the experiments on which the hole data are based (see Table I).
21-30	R	TCATA	Inner casing temperature, deg F.
31-40	R	TCATB	Outer casing temperature, deg F. These fields should be left blank if the casing temperature is not specified. To specify the casing temperature, it is only necessary to give a value on the first of each group of cards corresponding to a distinct value of XH.
41-50	R	FFB	Fraction of fuel burned up to this hole row. These values should increase from 0 to 1; it is only necessary to give a value on the first of each group of cards corresponding to a distinct XH.
51-55	I	NAB	Index indicating whether the hole row is on the inner or the outer wall. 1 for inner wall. 2 for outer wall.
56-60	I	NHH	Number of holes in this row. For continuous cooling slots this quantity should be made equal to 1.
61-65	I	NHTU	Index designating hole type. (Used to locate discharge-coefficient and jet-angle data on library tape). A zero indicates that calculations are to be performed at this point, although there are no holes. If NHTU = 0,

<u>Location</u>	<u>Type of Number</u>	<u>Fortran Name</u>	<u>Description</u>
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the following columns may be left blank: HAB, NAB, NHH. It is not permissible to set NHTU = 0 for the first hole row.

Fixed Data - Real

The next group of data is fed in via the namelist FIXEDR. The variables are as follows:

<u>Name</u>	<u>Description</u>
XINT	Interval downstream of cooling slot at which wall temperatures required, inches. Optional (100).
THIKFT	Flame-tube wall thickness, inches. Optional (a very small value).
FLCV	Fuel lower heating value, Btu per lbm. Optional (18540)
FHCR	Fuel hydrogen-carbon ratio. Optional (0.17).
SHAFST	Fraction of secondary air recirculating upstream. Optional (0.5).
AF23A	Fraction of inlet air bled from inner annulus. Optional (0). Up to three values may be provided, using the format shown in the example: AF23A = 0.02, 0.05, 0.03.
AF23B	Fraction of inlet air bled from outer annulus. Optional (0). Up to three values may be provided.
XAF23A	Axial location, inches, at which bleed air is removed from inner annulus. Optional (0). One value should be provided for each value of AF23A; it is not possible to bleed air from the diffuser.
XAF23B	Axial location, inches, at which bleed air is removed from outer annulus. Optional (0).
BETA	Swirler blade angle, degrees. Optional (50).
DSWLOU	Outer diameter of swirler, inches.

<u>Name</u>	<u>Description</u>
DSWLIN	Inner diameter of swirler, inches. DSWLOU and DSWLIN must be supplied if K6 = 1.
ABSW	Absorptivity of flame-tube wall. Optional (0.85)
EMW	Emissivity of wall. Optional (0.85).
EMC	Emissivity of casing. Optional (0.8).
CONDFT	Conductivity of flame-tube wall material, Btu per ft hr deg F. Optional (15.0).
XFILMZ	Constant in film-cooling correlation (X_0 in Equation 3-22 of Volume I). Optional (3.5).
DOMLOS	Number of velocity-heads of pressure lost inside the snout. Optional (0).
PERCO	Permeability coefficient of porous wall, sq ft. Optional (0).
WIDTH1	Width, inches, of rectangular-cross-section combustor. Optional (12).

Limits and Tolerances

The next group of data is fed in via the namelist LIMITS. The variables are as follows:

<u>Name</u>	<u>Description</u>
NXDIF	No. of geometric input point corresponding to station "2" (just upstream of snout) in diffuser analysis. Optional (if this value is not specified, NXDIF will be taken as the last geometric input point before the snout).
NXDIF1, NXDIF2	Nos. of geometric input points corresponding to Station 3 in inner and outer annulus respectively. These values must be specified if NDIFF = 11, 12, or 22. The annulus areas at Stations 3 and 4 (upstream edge of hole row NWH) must be equal.
LCANIL	Loop counter limit in the mass-flow-split iteration. Optional (50).

<u>Name</u>	<u>Description</u>
STEP	Step size in jet-mixing calculation, inches. Optional (0.25).

This completes the data that are unchanged from case to case within a run.

Case Data

The set of cards required for the first case is described below. These continue straight on from the library-data cards, the last of which is on line L_A .

<u>Line</u>	<u>Location</u>	<u>Type of Number</u>	<u>Fortran Name</u>	<u>Description</u>
L_A+1	1-10	R	STAGT	Total temperature at compressor discharge, deg F.
L_A+1	11-20	R	STPREF	Weight-mean total pressure at compressor discharge, lbf per sq in
L_A+1	21-30	R	AF2	Air mass flow rate at compressor discharge, lbm per sec.
L_A+1	31-40	R	FAR	Overall fuel-air ratio based on air-flow rate at compressor discharge.
L_A+1	41-50	R	ABLOCK	Fraction of inlet boundary-layer blockage that is on inner wall.
L_A+1	51-60	R	SHAPE ¹	Initial boundary-layer shape factor on inner wall. Optional (1.4) ¹ .
L_A+1	61-70	R	SHAPE ¹	Initial shape factor on outer wall. Optional (1.4) ¹ .
L_A+2	1-10	R	BLOCK(1)	Boundary-layer blockage at inlet. First estimates of the blockage at downstream geometric input points are given in the usual format (7 columns of 10) on this and subsequent lines. There should be NXDIF such values, including the first. The last value is on line L_B .

¹A method of calculating the initial shape factor more accurately is given on page 134 of Volume 1.

<u>Line</u>	<u>Location</u>	<u>Type of Number</u>	<u>Fortran Name</u>	<u>Description</u>
$L_B + 1$	1-10	R	DAFA	Estimated fraction of total flow passing through inner annulus. ¹
$L_B + 1$	11-20	R	DAFB	Estimated fraction of total flow passing through outer annulus. ¹
$L_B + 1$	21-30	R	AFCL	Lower bound on the ratio of the flow through the inner annulus to the flow through both annuli. ¹
$L_B + 1$	31-40	R	AFCU	Upper bound on the ratio of the flow through the inner annulus to the flow through both annuli. ¹
$L_B + 1$	41-50	R	AFSL	Lower bound on the flow through the snout. ¹
$L_B + 1$	51-60	R	AFSU	Upper bound on the flow through the snout. ¹
$L_B + 2$	1-10	I	NTUBE	Number of streamtubes considered in diffuser calculation. Maximum value 15.
$L_B + 2$	11-20	I	NUPR	Number of points at which inlet velocity profile specified. Minimum value 2, maximum value 15.
$L_B + 3$	1-10	R	VPDATA	First value of velocity.
$L_B + 3$	11-20	R	RDATA	First value of annulus height.
				The other points on the velocity profile are entered on subsequent lines up to $L_C = L_B + NUPR + 2$. RDATA should be made dimensionless so that all values lie between 0 (for the inner wall) and 1 (for the outer wall). VPDATA may consist of any set of numbers proportional to the velocity.
$L_C + 1$	1-10	I	NDIFF	Index for diffuser calculations. Tens position indicates method for Stations 1-2: 1 For streamtube analysis 2 For empirical data and units position for Stations 2-4:

¹ These quantities can be estimated from information obtained from previous runs. If such information is not available, the quantities should all be set equal to 0.0 in which case they will be estimated within the program.

<u>Line</u>	<u>Location</u>	<u>Type of Number</u>	<u>Fortran Name</u>	<u>Description</u>
				1 For streamtube analysis 2 For empirical data 3 For mixing equation Note, however, that 1 in the units position cannot be specified with 2 in the tens position. 1 in hundreds position implies streamtube method to be carried out after empirical data method; negative sign implies no diffuser calculation; fixed effectivenesses supplied as input.
$L_c + 1$	11-20	1	NEF	Index indicating entrainment correlation to be used. 1 For mass-loss method 2 For equivalent-entrainment method 3 For profile-substitution method 4 For instantaneous mixing
$L_c + 1$	21-30	1	NLUM	Index indicating correlation to be used for flame emissivity. 1 For nonluminous flames, distillate fuels 2 For nonluminous flames, residual fuels 3 For Lefebvre correlation 4 For NREC 1964 correlation 5 For NREC 1966 correlation 6 For emissivity from table of experimental data
$L_c + 1$	31-40	1	LANHET	Index. 0 If heat transfer to annulus air ignored 1 If heat transfer to annulus air considered 2 If no heat transfer calculation required
$L_c + 1$	41-50	1	NHTI	Index indicating route through non-iterative heat-transfer calculation. 1 For uncooled wall, 1-dimensional radiation 2 For cooled wall, 1-dimensional radiation 3 For uncooled wall, 2-dimensional radiation 4 For cooled wall, 2-dimensional radiation

<u>Line</u>	<u>Location</u>	<u>Type of Number</u>	<u>Fortran Name</u>	<u>Description</u>
L_C+1	51-60	I	NHT2	Index indicating route through iterative heat-transfer calculation. 2 For longitudinal conduction 3 For radiation interchange between walls 4 For longitudinal conduction and radiation interchange 1 Otherwise
L_C+2	1-10	R	EFC(1)	Constant used to specify rate of mixing of penetration jets.
L_C+2	11-20	R	EFC(2)	Constant used to specify rate of mixing of wall jets.
L_C+2	21-30	R	EFDT(1)	Effectiveness of diffuser between Stations 1 and 2 (i.e. between geometric input points no. 1 and NXDIF).
L_C+2	31-40	R	EFDT(2)	Effectiveness of inner diffusing passage between Stations 2 and 4.
L_C+2	41-50	R	EFDT(3)	Effectiveness of outer diffusing passage between Stations 2 and 4.

The three values of EFDT are required for the model in which no diffuser calculation is required, but experimental data for a diffuser of similar geometry operating under similar flow conditions are specified as input. For this case, NDIFF takes a value of -22. If this option is not required, the last three columns may be left blank.

This completes the data for the first case. Subsequent cases are specified in one of two ways:

1. Input Flow Conditions Varied

If INPUT = 0, only the first part of the case data (lines L_A+1 to L_C) is given for subsequent cases.

2. Program Routing and Correlations Varied

If INPUT = 1, only the second part of the case data (lines L_C+1 and L_C+2) is given for subsequent cases.

Sample Input Data

Appendix I contains samples to illustrate the preparation of library data input. In Appendix II the input data for Overall Test Case 3 are listed. Appendix II illustrates the instructions given above for the preparation of input data and also shows where the library data should be placed if ITAPE = KTAPE.

Output Data

The format for the computer output is self-explanatory and need not be discussed here. If problems arise, intermediate results may be printed out by setting IPRINT = 1. (This option is only available when output is on tape unit No. 6.) The format for these intermediate results is rudimentary, and the program user must refer to the individual WRITE statement for details. Condensed output is obtained on tape unit JTAPE (JTAPE = 8 in the present BLOCKDATA) by setting IPRINT = 0. With IPRINT = 1 under the present arrangement, intermediate results are written on tape unit 6 and condensed results on unit JTAPE (8).

Appendix III contains the condensed computer output from Test Case 3, and illustrates the format for this output.

Output of computer test-case input only may be obtained by setting NCASE = 0.

Program Messages

A number of messages are printed out by the program, either as part of the normal output or as indications of errors in program operation. A list of these program messages is included as Appendix V, with explanatory notes.

1. Dittrich, R. T. and Graves, C. C., Discharge Coefficients for Combustor-Liner Air-Entry Holes, I - Circular Holes (NACA TN 3663), National Advisory Committee for Aeronautics, 1965.
2. Kaddah, K. Sh., Discharge Coefficient and Jet Deflection Studies for Combustor-Liner Air-Entry Holes, Thesis No. 17/10, College of Aeronautics, Cranfield, England, June, 1964.
3. Venneman, W. F., Flow Coefficients and Jet Deflection Angles for Combustor-Liner Air-Entry Holes, Part I, General Electric Company, Schenectady, New York, 1959.
4. Dittrich, R. T., Discharge Coefficients for Combustor-Liner Air-Entry Holes, II - Flush Rectangular Holes, Step Louvers, and Scoops (NACA TN 3924), National Advisory Committee for Aeronautics, 1958.
5. Marshall, L. A., Aerodynamic Characteristics of Combustor-Liner Air-Entry Passages (Rep. R58 AGT 558), Aircraft Gas Turbine Division, General Electric Company, Cincinnati, 1958.
6. Venneman, W. F., Flow Coefficients and Jet Deflection Angles for Combustor-Liner Air-Entry Holes, Part II, General Electric Company, Schenectady, New York, 1960.

TABLES

TABLE 1 - KEY TO HOLE-DISCHARGE-COEFFICIENT AND JET-ANGLE DATA

Number	Hole Description	Reference	Figure	Curve
Flush Circular Holes				
1	Flush hole 0.125 in dia	1	6(a)	
2	Flush hole 0.25 in dia	1	6(b)	
3	Flush hole 0.328 in dia	2	42	
4	Flush hole 0.472 in dia	2	43	
5	Flush hole 0.75 in dia with 45 degree bevel	3	7	
6	Flush hole 0.75 in dia	1	6(e)	
7	Flush hole 0.75 in dia	4	14	E-1
8	Flush hole 0.75 in dia	5	3	
9	Flush hole 0.759 in dia	3	6	
10	Flush hole 0.807 in dia	2	44	
11	Flush hole 0.985 in dia	2	45	
12	Flush hole 1.5 in dia	1	6(k)	
13	Flush hole 1.59 in dia	2	46	
14	Flush hole 1.809 in dia	3	13	
Flush Rectangular Holes				
15	Flush hole 0.5 in square	4	14	A-1
16	Flush hole 0.708 in square	2	90	
17	Flush hole 0.412 in long and 0.206 in wide	2	83	

TABLE I (CONTINUED) - KEY TO HOLE-DISCHARGE-COEFFICIENT AND JET-ANGLE DATA

Number	Hole Description	Reference	Figure	Curve
18	Flush hole 0.436 in long and 0.218 in wide with semi-circular ends	2	60	
19	Flush hole 0.591 in long and 0.295 in wide	2	84	
20	Flush hole 0.624 in long and 0.312 in wide with semicircular ends	2	61	
21	Flush hole 1.0 in long and 0.5 in wide	2	85	
22	Flush hole 1.0 in long and 0.5 in wide	4	14	A-2
23	Flush hole 1.062 in long and 0.531 in wide with semicircular ends	2	62	
24	Flush hole 1.24 in long and 0.62 in wide	2	86	
25	Flush hole 1.312 in long and 0.656 in wide with semicircular ends	2	63	
26	Flush hole 2.0 in long and 1.0 in wide	2	87	
27	Flush hole 2.0 in long and 1.0 in wide	4	14	A-4
28	Flush hole 2.124 in long and 1.062 in wide	2	64	
29	Flush hole 1.42 in long and 0.355 in wide	2	91	
30	Flush hole 1.497 in long and 0.375 in wide with semi-circular ends	2	67	
31	Flush hole 4.0 in long and 0.5 in wide	4	14	A-3
32	Flush hole 2.0 in long and 0.25 in wide	2	92	

TABLE I (CONTINUED) - KEY TO HOLE-DISCHARGE COEFFICIENT AND JET-ANGLE DATA

Number	Hole Description	Reference	Figure	Curve
33	Flush hole 2.1 in long and 0.25 in wide with semi-circular ends	2	68	
34	Flush hole 4.0 in long and 0.25 in wide	4	14	A-5
Thimbled (Plunged) Holes without Scoops				
35	Thimbled hole 0.475 in dia with tapered skirt	5	4	
36	Thimbled hole 0.625 in dia with tapered skirt	5	5	
37	Thimbled hole 0.792 in dia with tapered skirt	5	6	
38	Thimbled hole 1.286 in dia with full tapered skirt	3	9	
39	Thimbled hole 1.82 in dia with tapered skirt	3	10	
40	Thimbled hole 1.828 in dia with full skirt	3	3	
41	Thimbled hole 1.832 in dia with half tapered skirt	3	11	
42	Thimbled hole 2.281 in long and 1.281 in wide with semicircular ends and full skirt	3	8	
Step Louvers (For continuous cooling films)				
43	Step louver 0.095 in high with overlap	4	16(a)	B-4
44	Step louver 0.095 in high with wiggle strip	4	16(a)	B-6
45	Step louver 0.104 in high	4	15	B-1

TABLE 1 (CONTINUED) - KEY TO HOLE-DISCHARGE-COEFFICIENT AND JET-ANGLE DATA

Number	Hole Description	Reference	Figure	Curve
46	Step louver 0.168 in high	4	15	B-10
47	Step louver 0.25 in high with overlap	4	16(b)	B-5
48	Step louver 0.25 in high with wiggle strip	4	16(b)	B-7
49	Step louver 0.255 in high (without sidewall extension)	4	17	B-2
50	Step louver 0.26 in high	4	15	B-3
51	Step louver 0.38 in high	4	15	B-9
52	Step louver 0.623 in high	4	15	B-8
	Holes with Scoops			
53	Thimbled hole 1.843 in dia with scoop 0.31 in high and 2.5 in wide	3	2	
54	Hole 2.0 in long and 1.63 in wide with scoop 0.5 in high and projecting 0.43 in into flame tube	3	4	
55	Hole 2.0 in long and 2.87 in wide tapering to 1.5 in wide at rear with scoop 0.437 in high and projecting 0.375 in into flame tube	3	5	
56	Half thimbled hole 1.286 in dia with scoop 0.437 in high and 2.83 in wide	3	12	
57	Triangular hole assumed 2.0 in long and 2.87 in wide with scoop assumed 0.437 in high and 2.87 in wide	3	16	
58	Hole 2.3 in long and 1.3 in wide with semicircular ends, scoop, and turning vane	6	8	

TABLE 1 (CONTINUED) - KEY TO HOLE-DISCHARGE-COEFFICIENT AND JET-ANGLE DATA

Number	Hole Description	Reference	Figure	Curve
59	Thimbled hole 1.05 in square with 0.3 in radius at leading edge corners, trailing edge raised 0.112 in, and tapered skirt	6	10	
60	Thimbled hole 1.05 in square with 0.3 in radius at leading edge corners, trailing edge raised 0.112 in, scoop projecting into flame tube, and tapered skirt	6	11	
61	Thimbled hole 1.05 in square with 0.3 in radius at leading edge corners, trailing edge raised 0.112 in, 90 degree vane projecting into flame tube, and tapered skirt	6	12	
62	Thimbled hole 1.05 in square with 0.3 in radius at leading edge corners, trailing edge raised 0.075 in, vane projecting into flame tube, and tapered skirt	6	13	
63	Hole assumed 0.75 in long and 0.65 in wide with 0.26 in radius at leading edge corners and raised trailing edge	6	14	
64	Hole assumed 0.75 in long and 0.65 in wide with 0.26 in radius at leading edge corners, raised trailing edge, and vane projecting into flame tube	6	16	
65	Hole assumed 0.75 in long and 0.65 in wide with 0.26 in radius at leading edge corners, raised trailing edge, and 50 degree vane projecting into annulus and flame tube	6	18	

TABLE 1 (CONTINUED) - KEY TO HOLE-DISCHARGE-COEFFICIENT AND JET-ANGLE DATA

Number	Hole Description	Reference	Figure	Curve
66	Hole assumed 0.75 in long and 0.65 in wide with 0.26 in radius at leading edge corners, raised trailing edge, and 70 degree vane projecting into annulus and flame tube	6	19	
67	Hole 2.3 in long and 1.3 in wide with semicircular ends, scoop, and turning vane	6	20	
68	Hole 2.3 in long and 1.3 in wide with semicircular ends, scoop raised 0.125 in, and turning vane	6	21	
69	Hole 2.3 in long and 1.3 in wide with semicircular ends, scoop raised 0.25 in, and turning vane	6	22	
70	Hole 2.3 in long and 1.3 in wide with semicircular ends, scoop, and turning vane with rounded corners	6	23	
71	Hole 2.3 in long and 1.3 in wide with semicircular ends, scoop with leading edge raised 0.125 in, and turning vane	6	24	
72	Semicircular hole assumed 0.295 in radius with thumbnail scoop 0.15 in high	4	18	C-1
73	Semicircular hole assumed 0.373 in radius with thumbnail scoop 0.265 in high	4	18	C-2
74	Hole 0.75 in dia with scoop 0.75 in wide and 0.427 in high	4	19	D-1
75	Hole 0.75 in dia with scoop 0.75 in wide and 0.636 in high	4	19	D-2

TABLE 1 (CONTINUED) - KEY TO HOLE-DISCHARGE-COEFFICIENT AND JET-ANGLE DATA

Number	Hole Description	Reference	Figure	Curve
76	Hole 0.75 in dia with scoop 0.753 in wide and 0.891 in high	4	19	D-3
77	Hole 0.75 in dia with scoop 1.461 in wide and 0.585 in high	4	19	D-4
78	Thimbled hole 2.155 in long and 1.27 in wide with semi-circular leading end, trailing edge raised 0.19 in, and tapered skirt	6	9	
79	Thimbled hole 2.155 in long and 1.27 in wide with semi-circular leading end, trailing edge raised 0.19 in, scoop 0.7 in behind leading edge, and tapered skirt	6	9	
80	Thimbled hole 2.155 in long and 1.27 in wide with semi-circular leading end, trailing edge raised 0.19 in, scoop 0.32 in behind leading edge, and tapered skirt	6	9	
81	Thimbled hole 0.815 in dia with scoop 0.312 in high and full skirt	5	7	
82	Hole 1.0 in dia with scoop 0.312 in high and long tube in place of skirt	5	10	
83	Thimbled hole 0.8 in dia with scoop 0.312 in high	5	11	
84	Thimbled hole 0.815 in dia with scoop 0.312 in high placed at 20 degrees to annulus flow direction and full skirt	5	12	

TABLE 1 (CONTINUED) - KEY TO HOLE-DISCHARGE-COEFFICIENT AND JET-ANGLE DATA

Number	Hole Description	Reference	Figure	Curve
85	Hole 0.49 in long and 1.012 in wide with scoop 0.21 in high and turning vane	5	13	"Rear Hole Closed"
86	Hole 0.7 in long and 1.012 in wide with scoop 0.21 in high and turning vane	5	13	"Rear Hole Open"
87	Hole 0.123 in wide with scoop 0.47 in high	5	15	
88	Thimbled hole 0.75 in long and 0.745 in wide with scoop 0.506 in high and 0.765 in wide and full skirt	5	16	4a
89	Thimbled hole 0.48 in long and 0.745 in wide with scoop 0.506 in high and 0.765 in wide and full skirt	5	16	4b
90	Thimbled hole 0.24 in long and 0.745 in wide with scoop 0.506 in high and 0.765 in wide and full skirt	5	16	4c
91	Thimbled hole 0.57 in long and 0.51 in wide with scoop 0.5 in high and 0.555 in wide and full skirt	5	17	
92	Thimbled hole 0.325 in long and 0.74 in wide with scoop 0.53 in high and 0.76 in wide and full skirt	5	18	"Based on Exit Area"
93	Thimbled hole 0.325 in long and 0.74 in wide with scoop 0.53 in high and 0.76 in wide and full skirt	5	18	"Based on Inlet Area"
94	Hole 0.75 in long and 0.765 in wide with scoop 0.545 in high placed 0.75 in in front of hole leading edge	5	19	

TABLE I (CONTINUED) - KEY TO HOLE-DISCHARGE-COEFFICIENT AND JET-ANGLE DATA

Number	Hole Description	Reference	Figure	Curve
95	Thimble hole 0.875 in long and 0.8 in wide with scoop 0.507 in high and 0.76 in wide and half skirt	5	20	
96	Hole 0.375 in dia fitted with elbow scoop 0.385 in dia with entrance centre-line 0.528 in from wall	5	22	
97	Hole 0.68 in long and 0.65 in wide with scoop 0.165 in high and 0.63 in wide projecting into flame tube	5	22	
98	Hole 0.69 in long and 0.65 in wide with scoop 0.205 in high and 0.63 in wide projecting into flame tube	5	23	
99	Hole 0.69 in long and 0.65 in wide with scoop 0.305 in high and 0.642 in wide projecting into flame tube	5	24	
100	Hole 0.92 in long and 0.89 in wide with scoop 0.273 in high and 1.02 in wide projecting into flame tube	5	25	

FIGURES

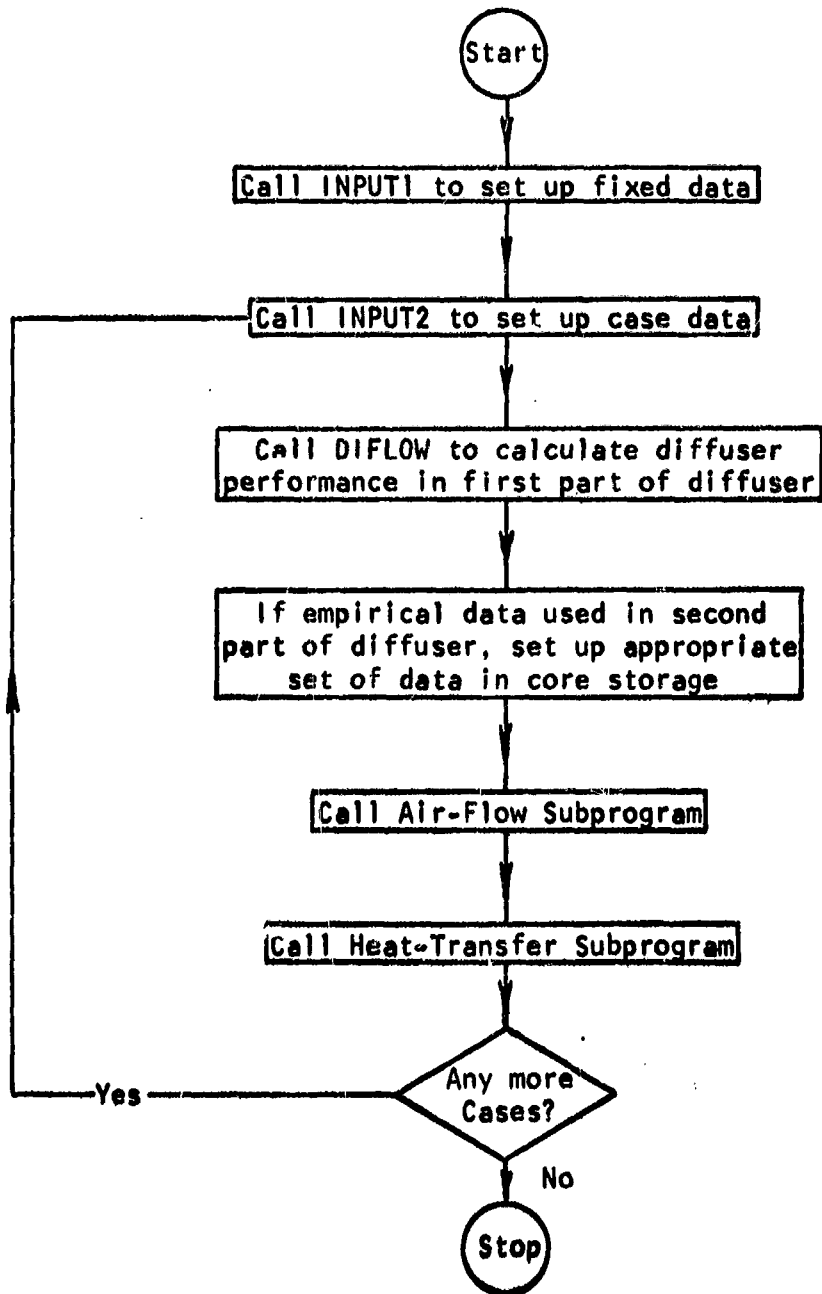


FIGURE 1 - FLOW CHART FOR MAIN PROGRAM CLARE

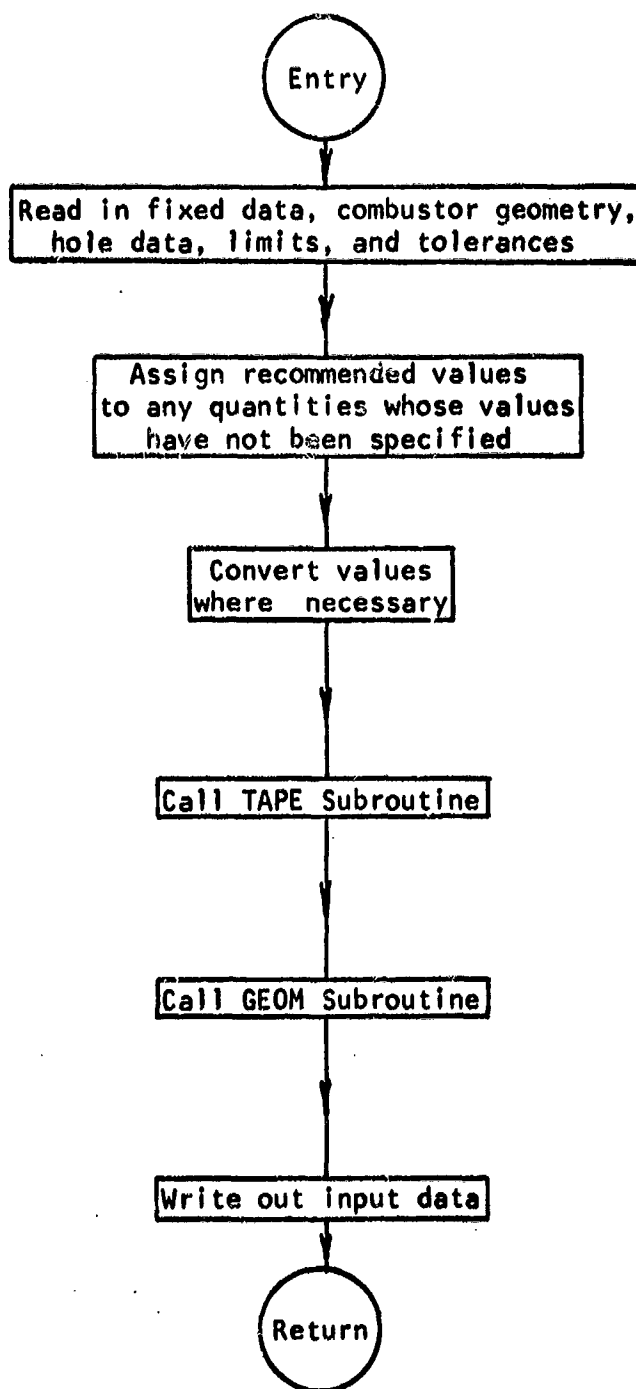


FIGURE 2 - FLOW CHART FOR SUBROUTINE INPUT

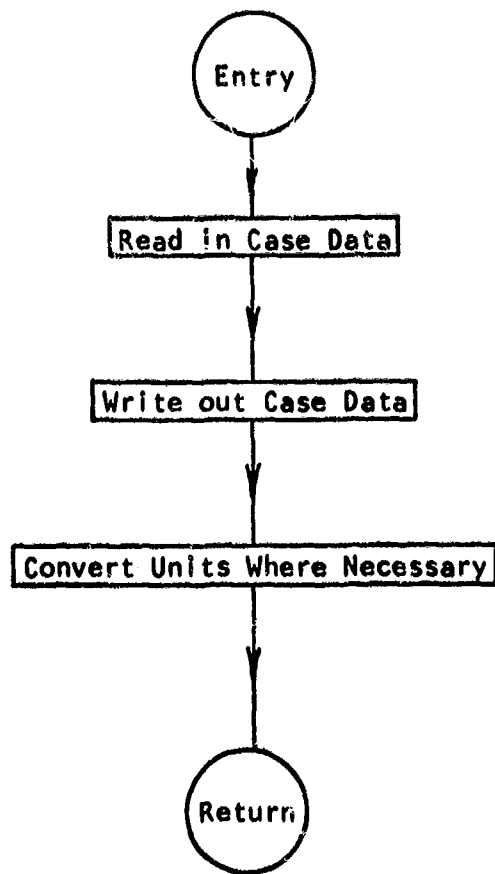


FIGURE 3 - FLOW CHART FOR SUBROUTINE INPUT2

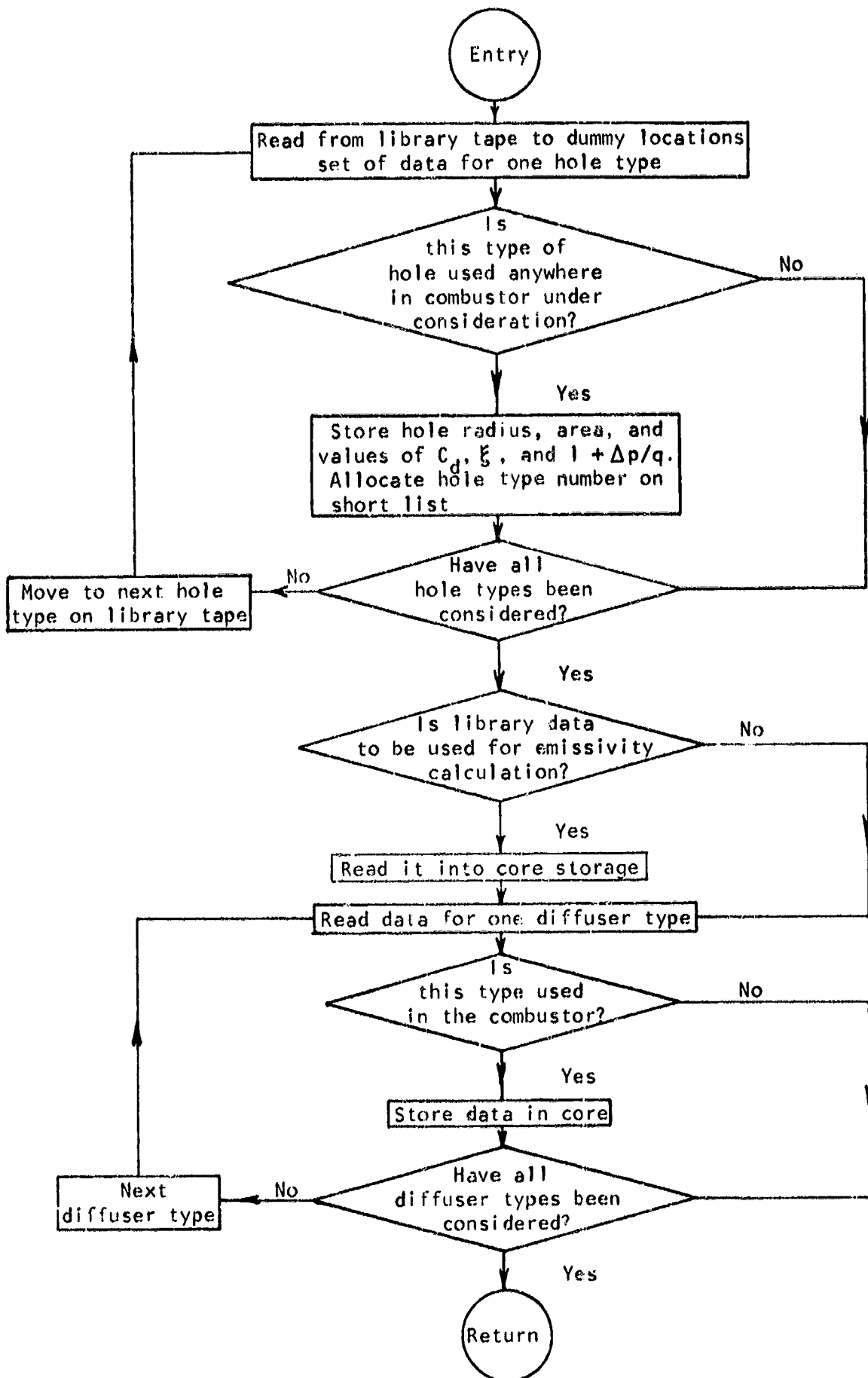


FIGURE 4 - FLOW CHART FOR SUBROUTINE TAPE

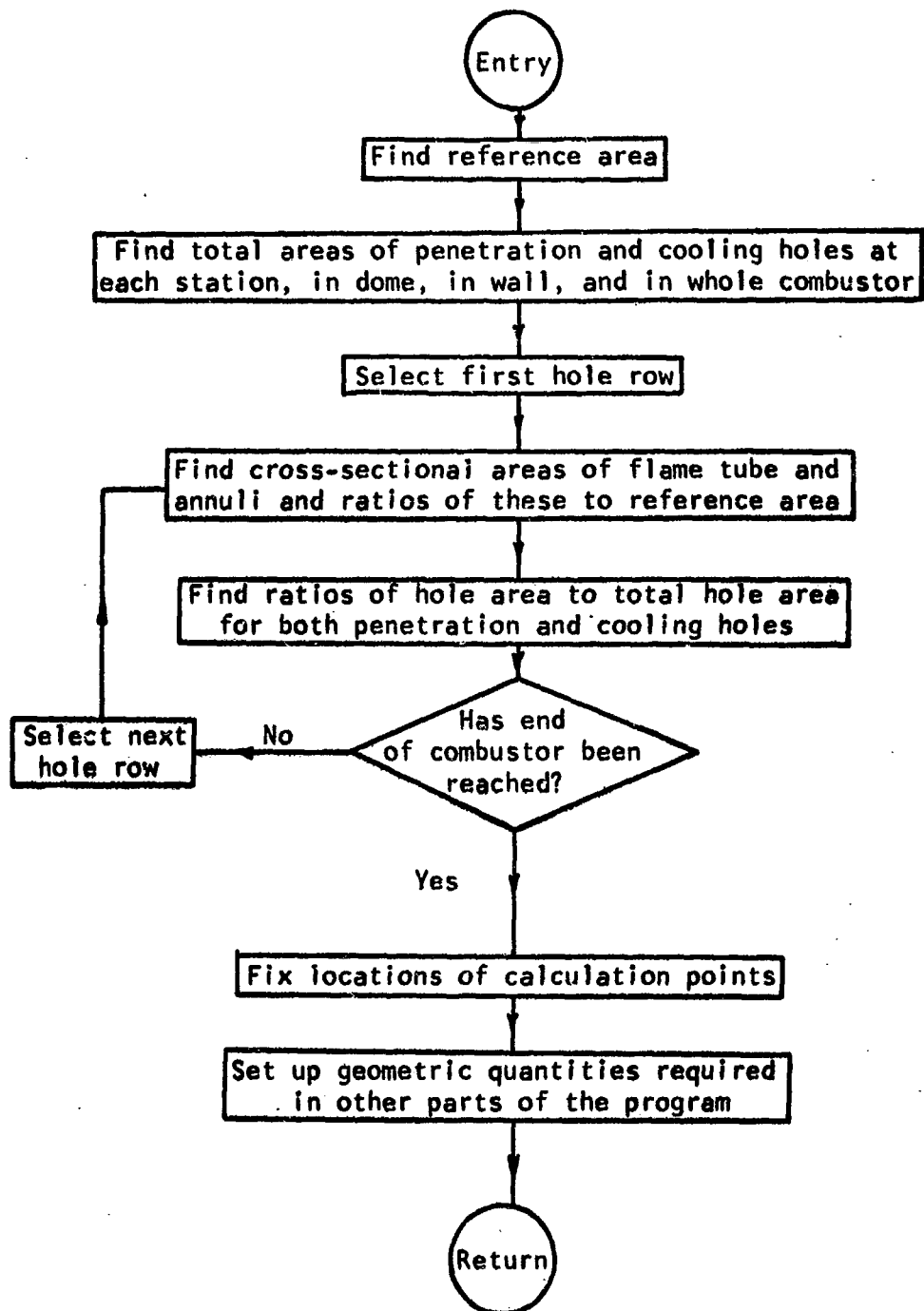


FIGURE 5 - FLOW CHART FOR SUBROUTINE GEOM

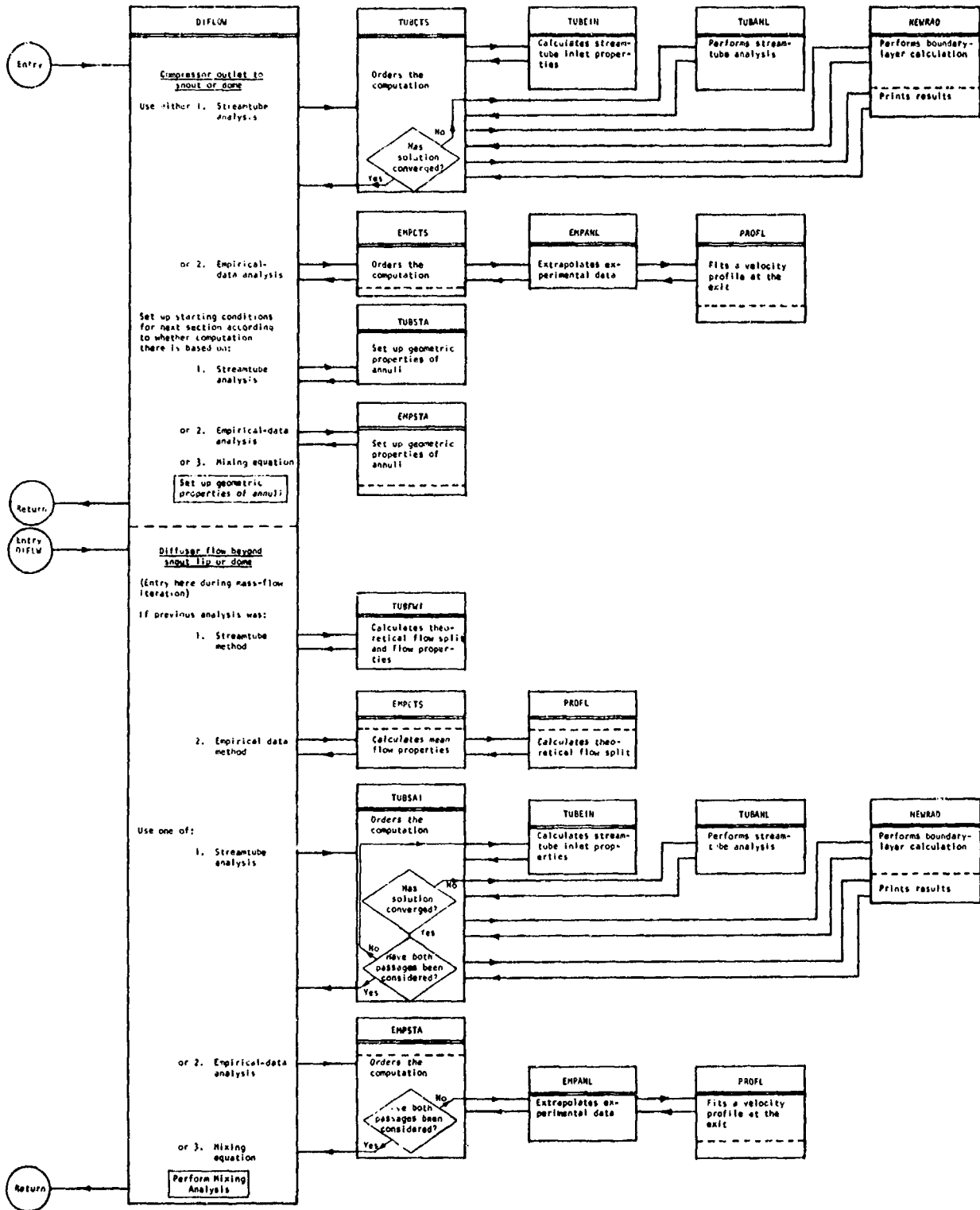


FIGURE 6 - OVERALL FLOW CHART FOR DIFFUSER SUBPROGRAM

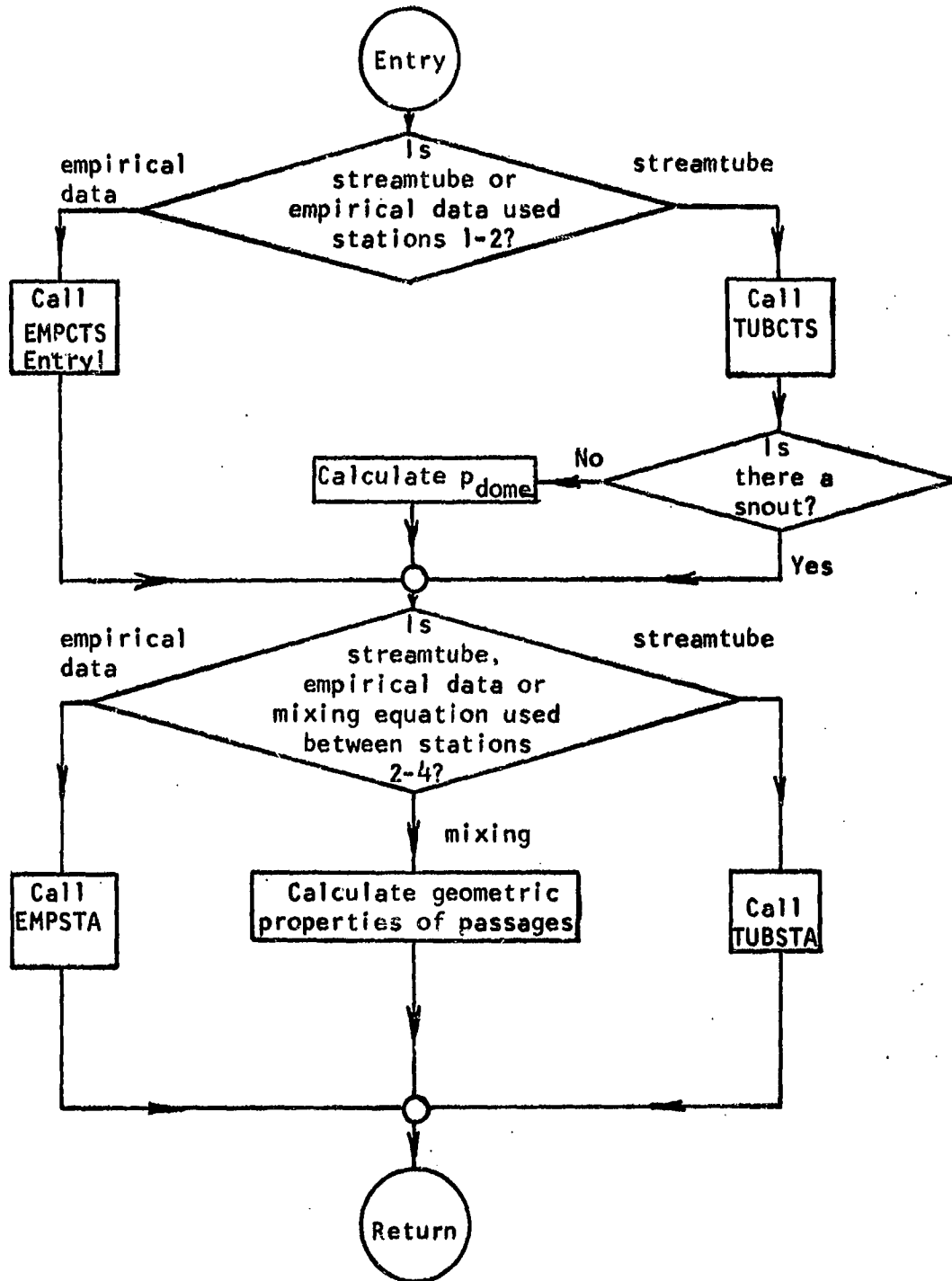


FIGURE 7 - FLOW CHART FOR SUBROUTINE DIFLOW

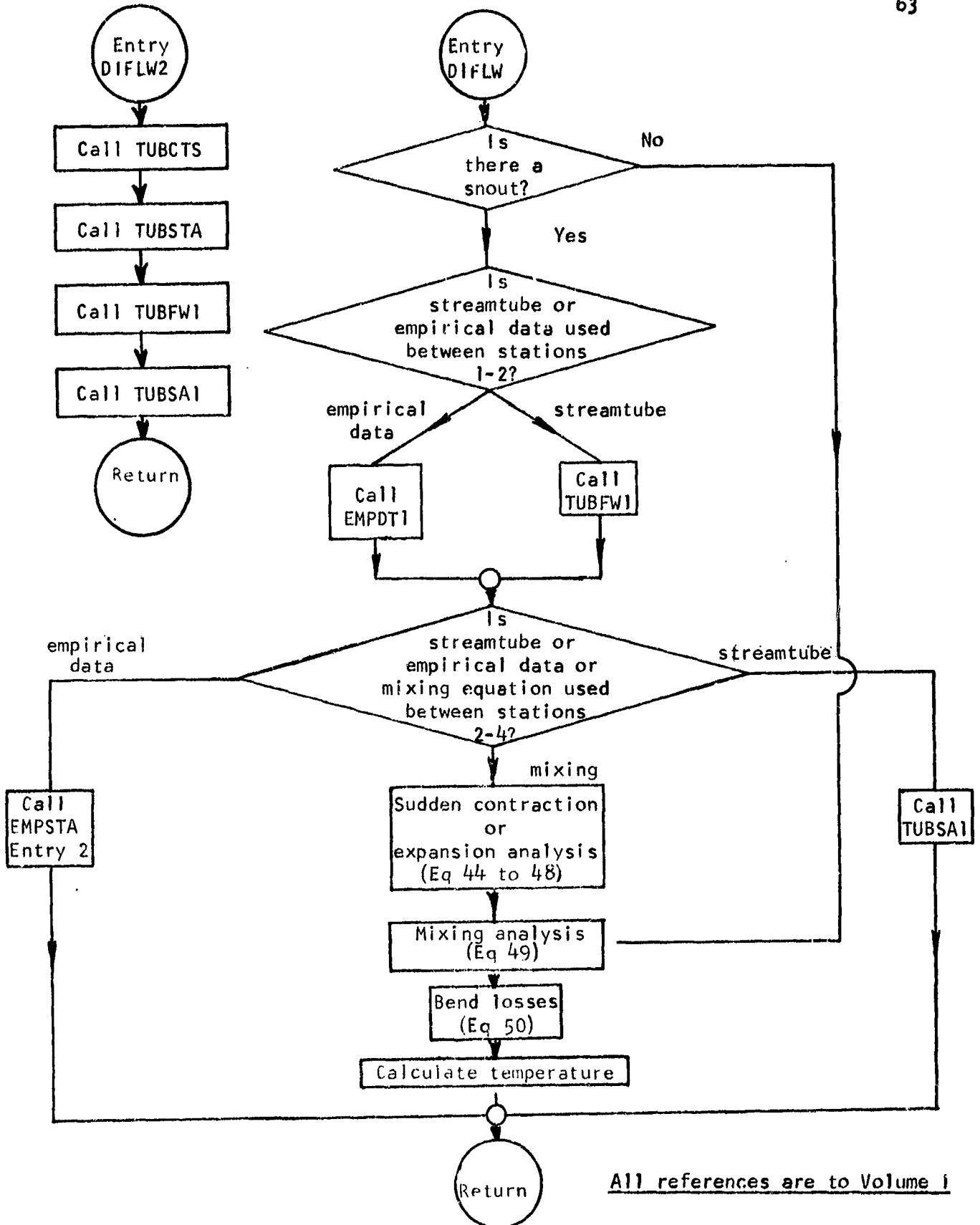
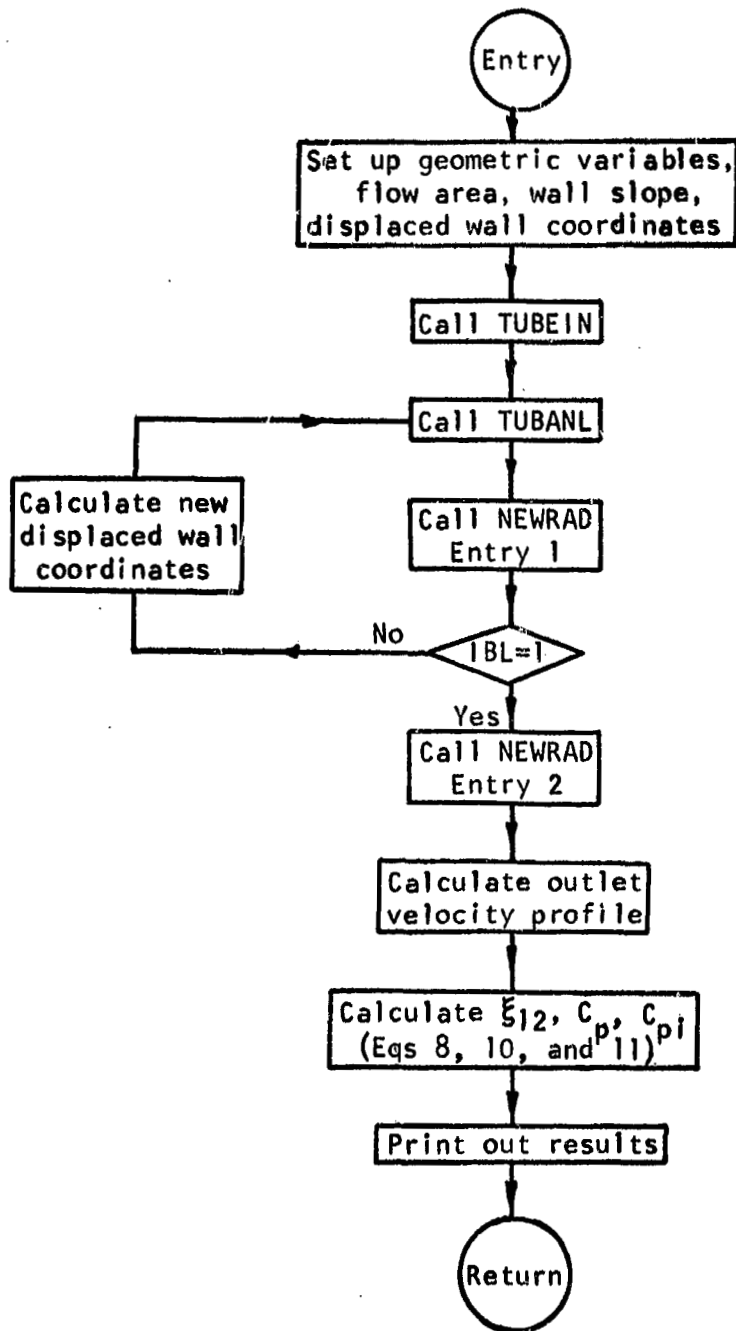


FIGURE 7 (CONTINUED) - FLOW CHART FOR SUBROUTINE DIFLOW



All references are to Volume 1

FIGURE 8 - FLOW CHART FOR SUBROUTINE TUBCTS

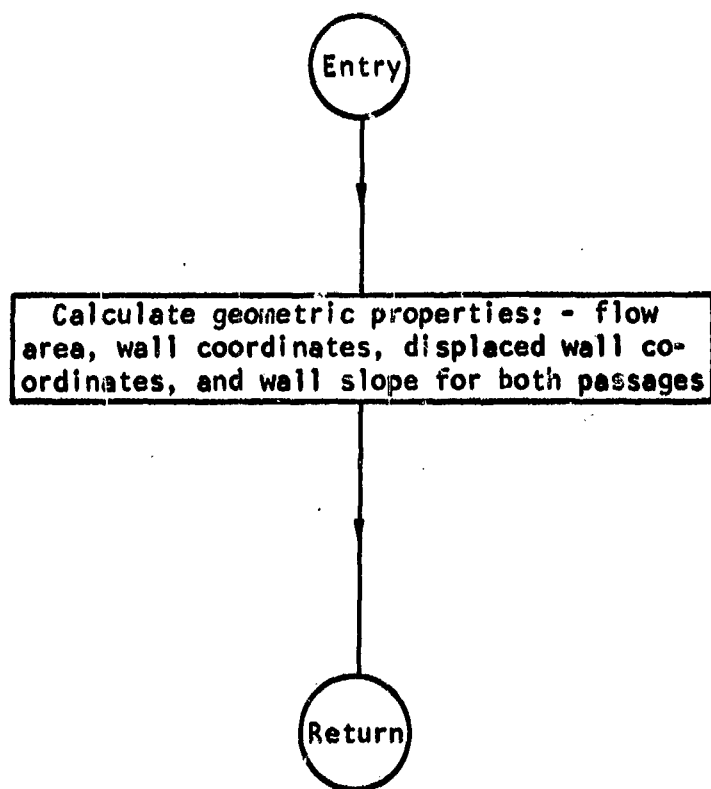
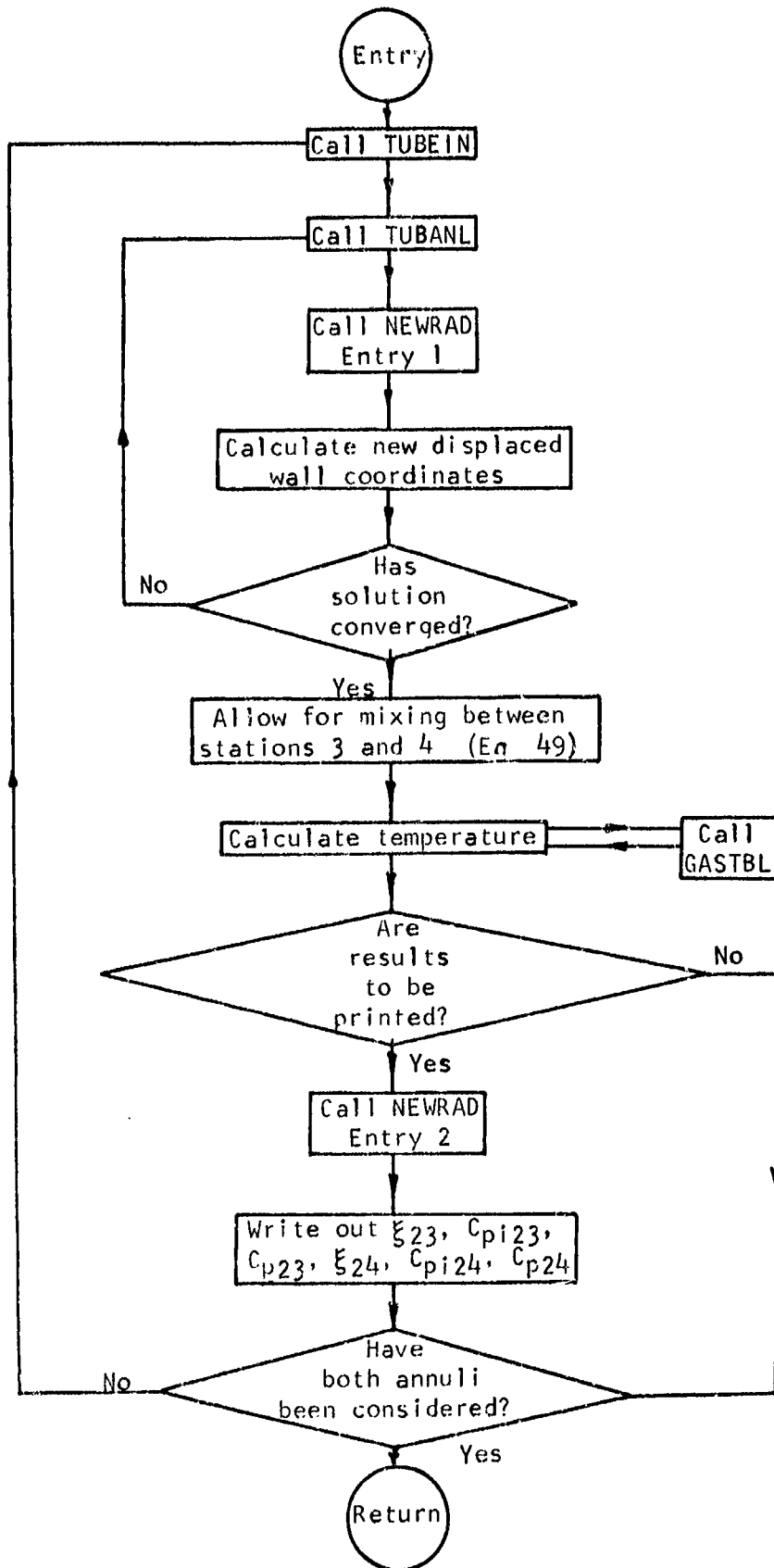


FIGURE 9 - FLOW CHART FOR SUBROUTINE TUBSTA



All references are to Volume 1

FIGURE 10 - FLOW CHART FOR SUBROUTINE TUBSA1

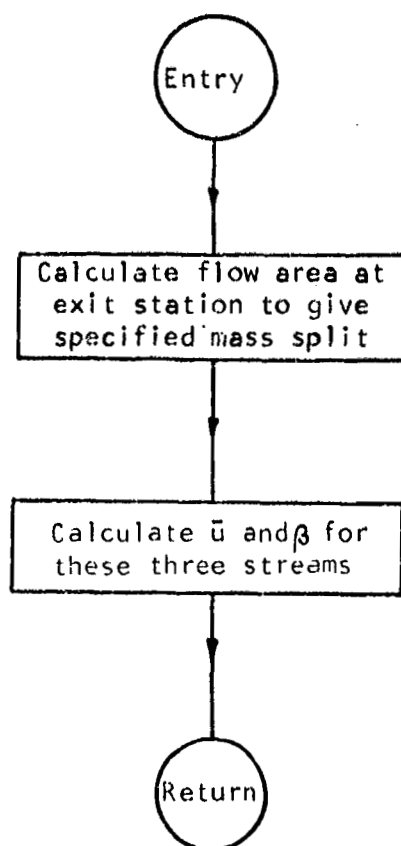
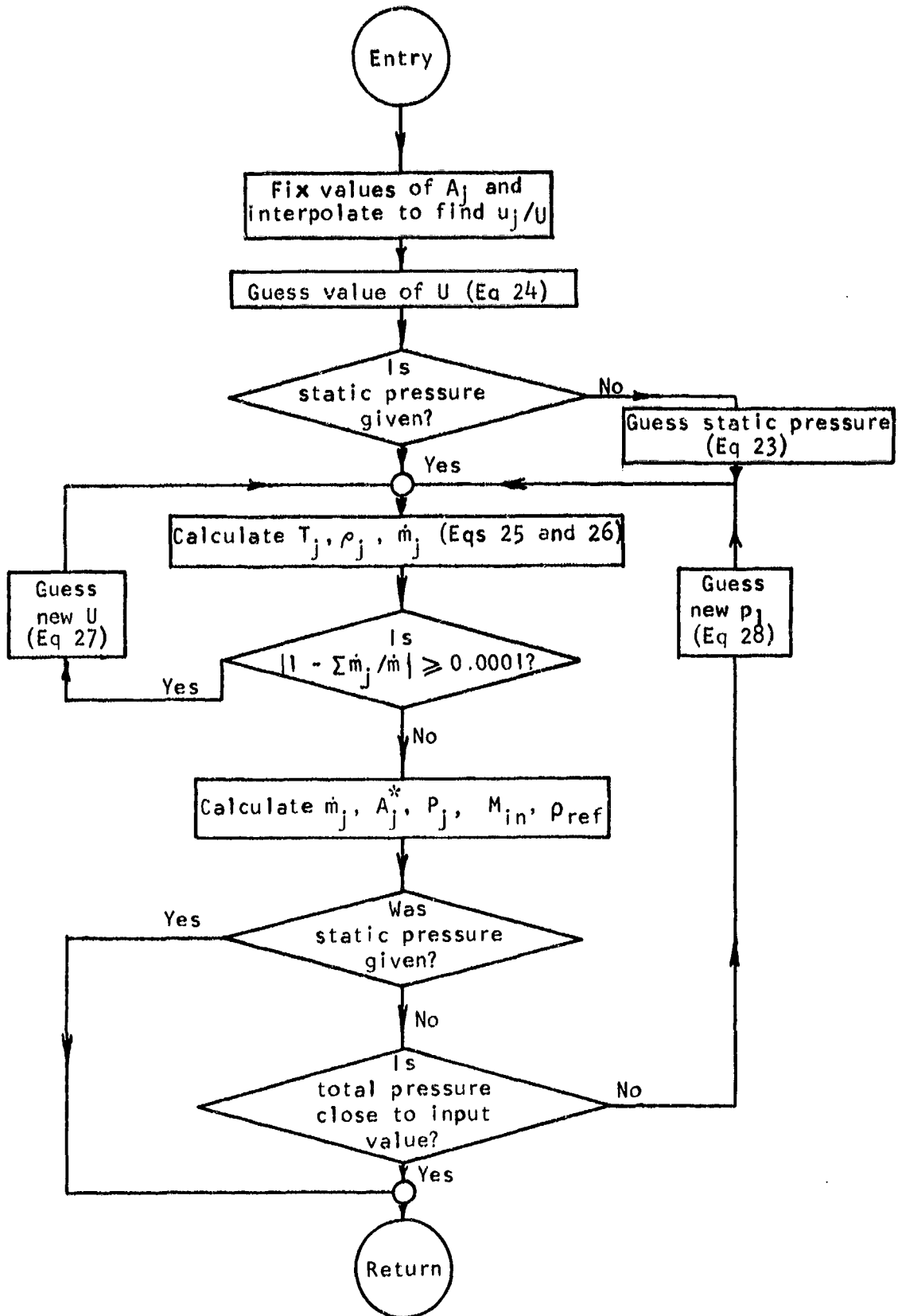
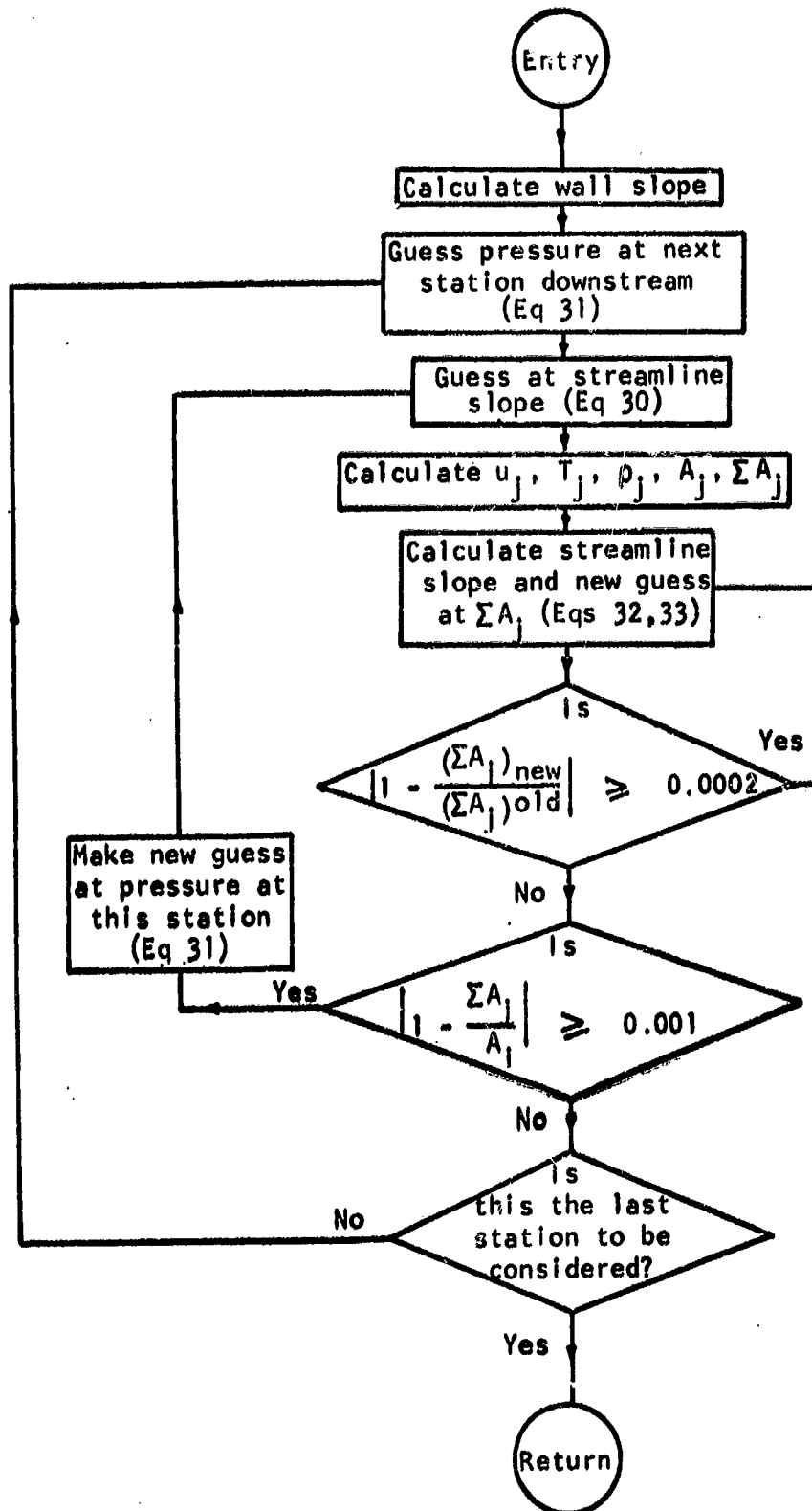


FIGURE 11 - FLOW CHART FOR SUBROUTINE TUBFW1



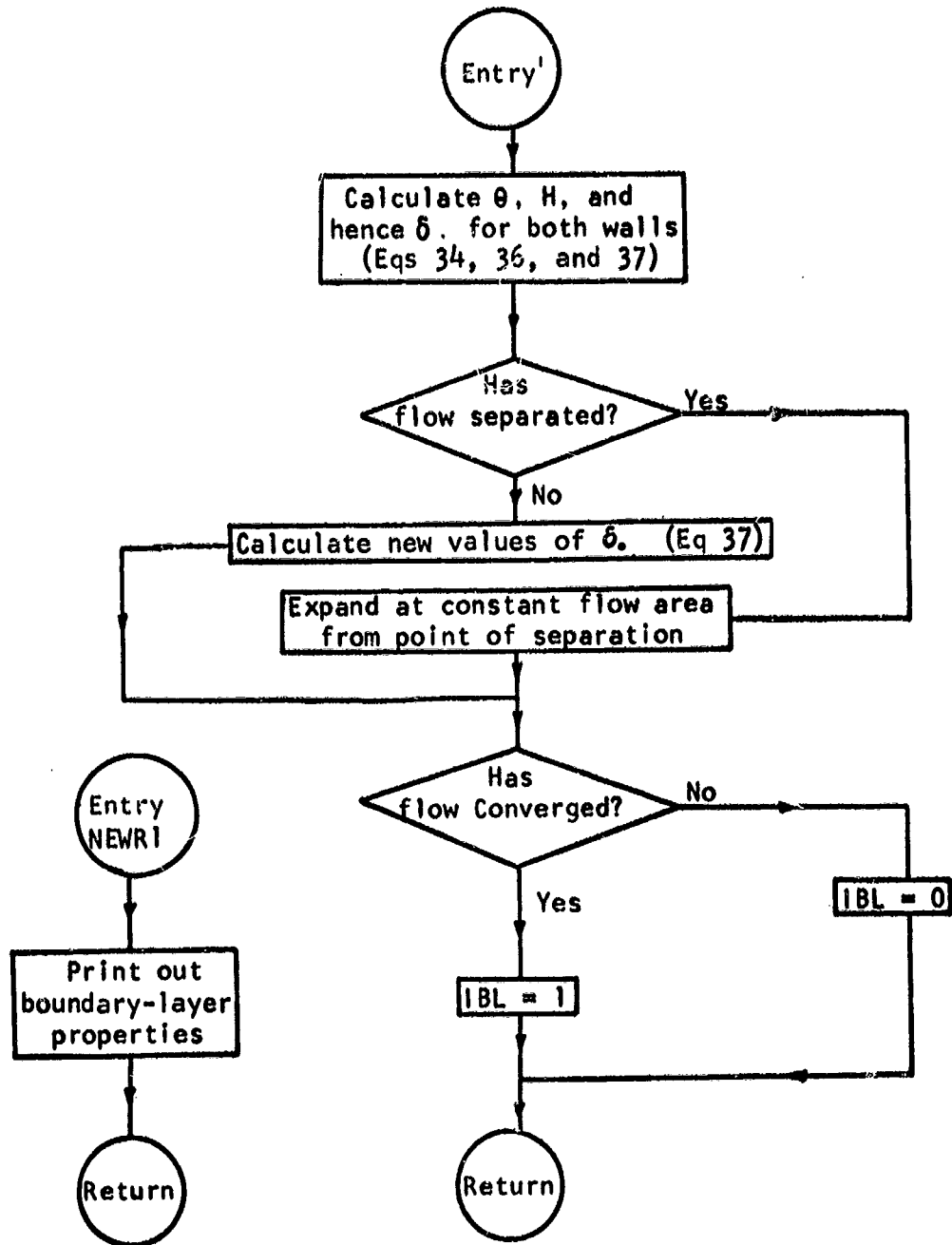
All references are to Volume 1

FIGURE 12 - FLOW CHART FOR SUBROUTINE TUBEIN



All references are to Volume I

FIGURE 13 - FLOW CHART FOR SUBROUTINE TUBANL



All references are to Volume I

FIGURE 14 - FLOW CHART FOR SUBROUTINE NEWRAD

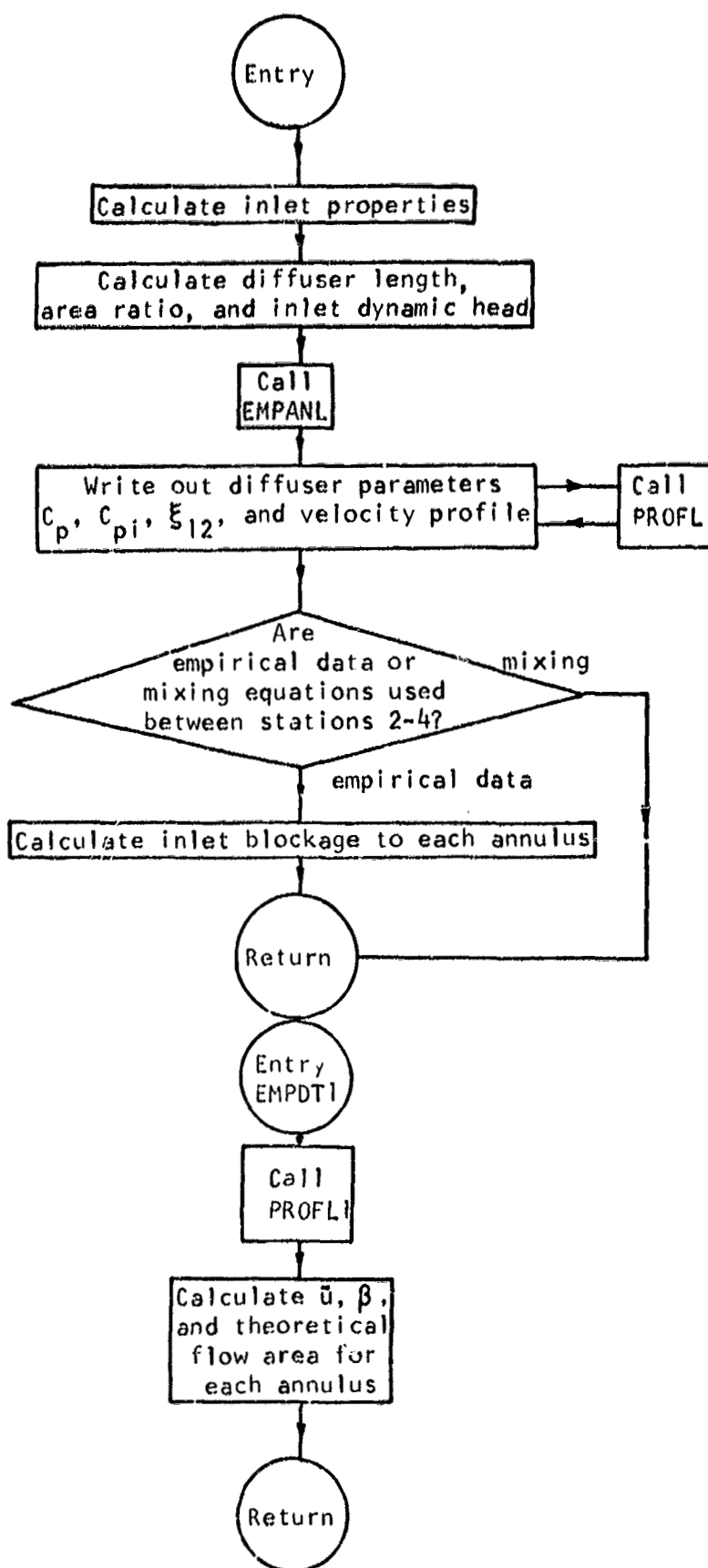
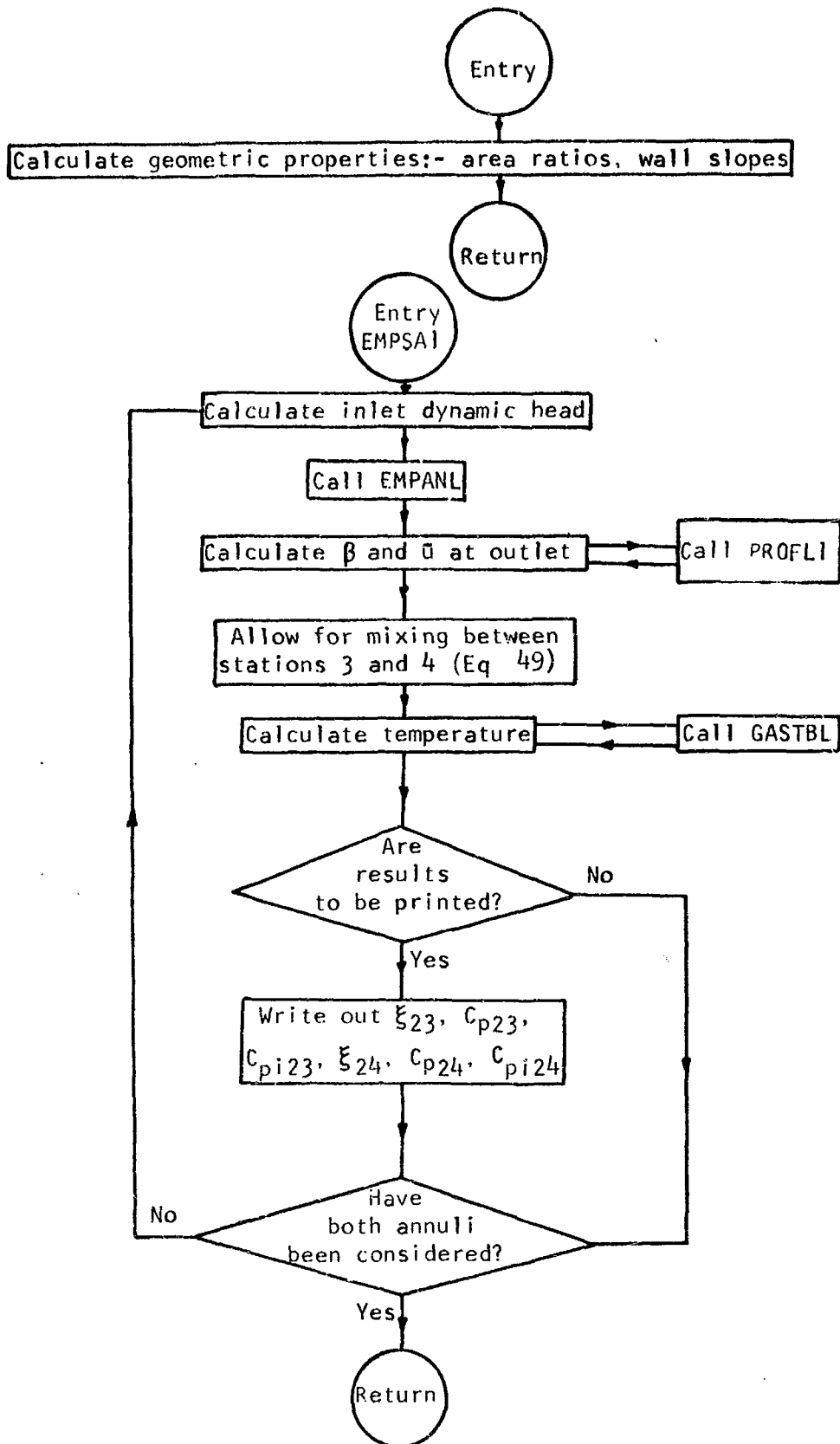
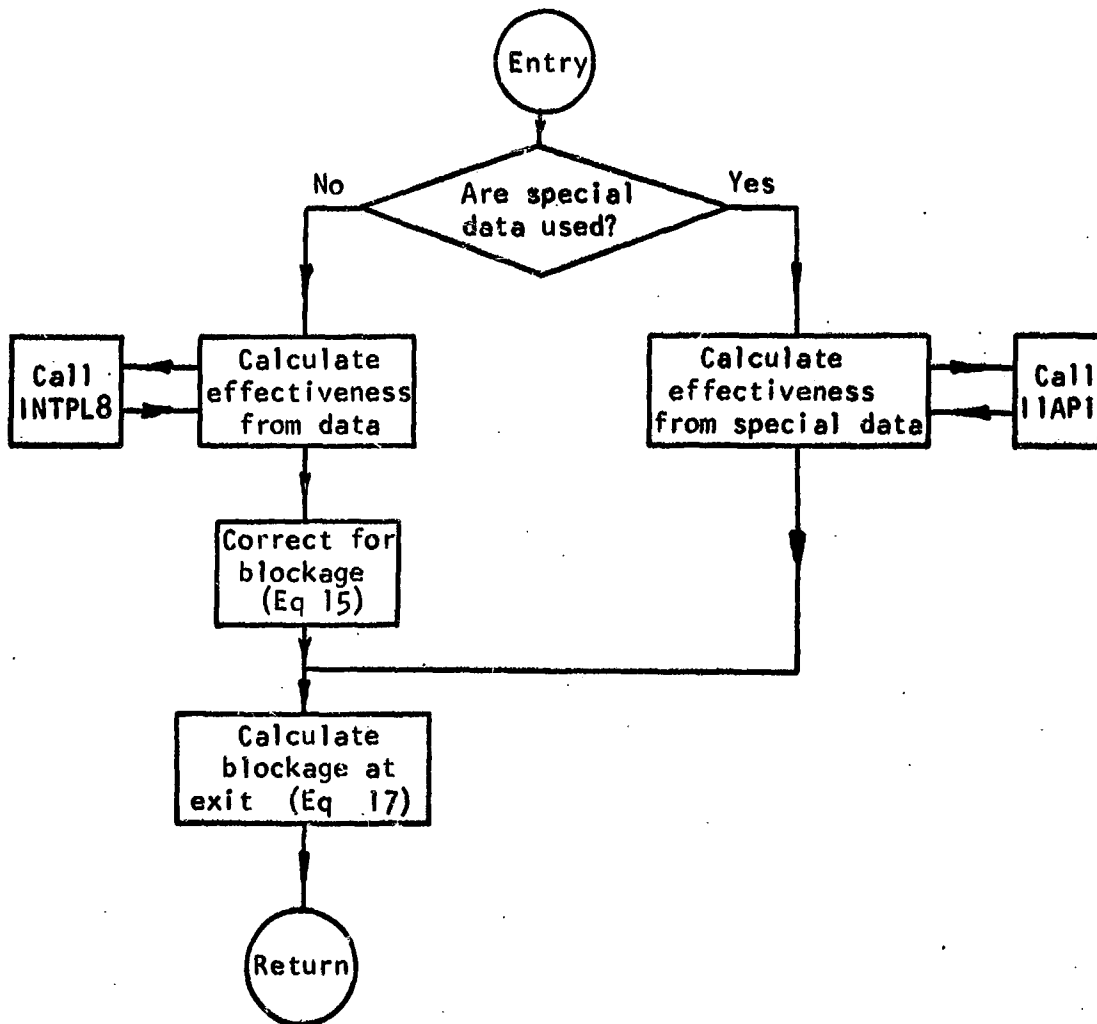


FIGURE 15 - FLOW CHART FOR SUBROUTINE EMPCTS



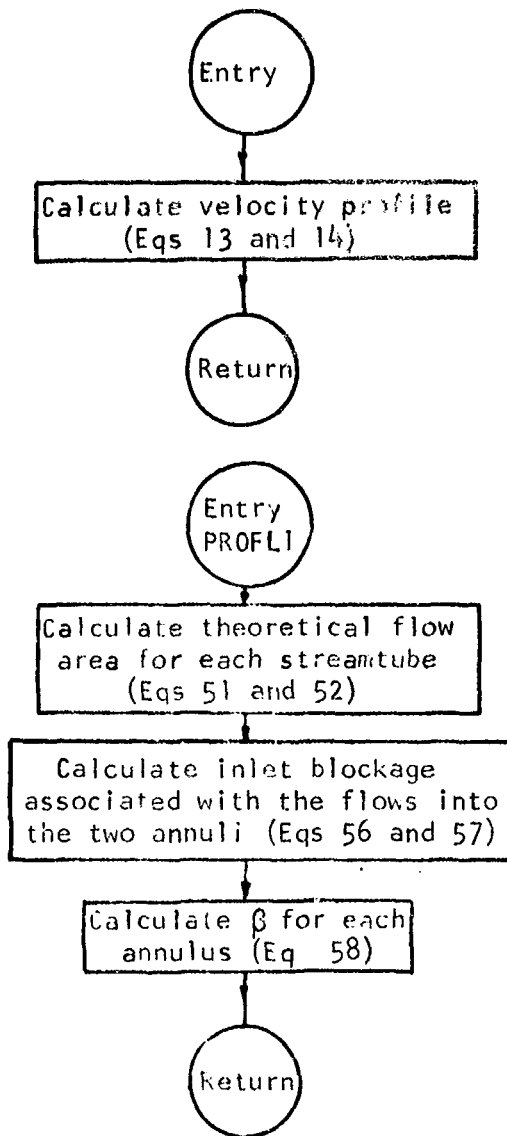
All references are to Volume I

FIGURE 16 - FLOW CHART FOR SUBROUTINE EMPSTA



All references are to Volume I

FIGURE 17 - FLOW CHART FOR SUBROUTINE EMPANL



All references are to Volume I

FIGURE 18 - FLOW CHART FOR SUBROUTINE PROFL

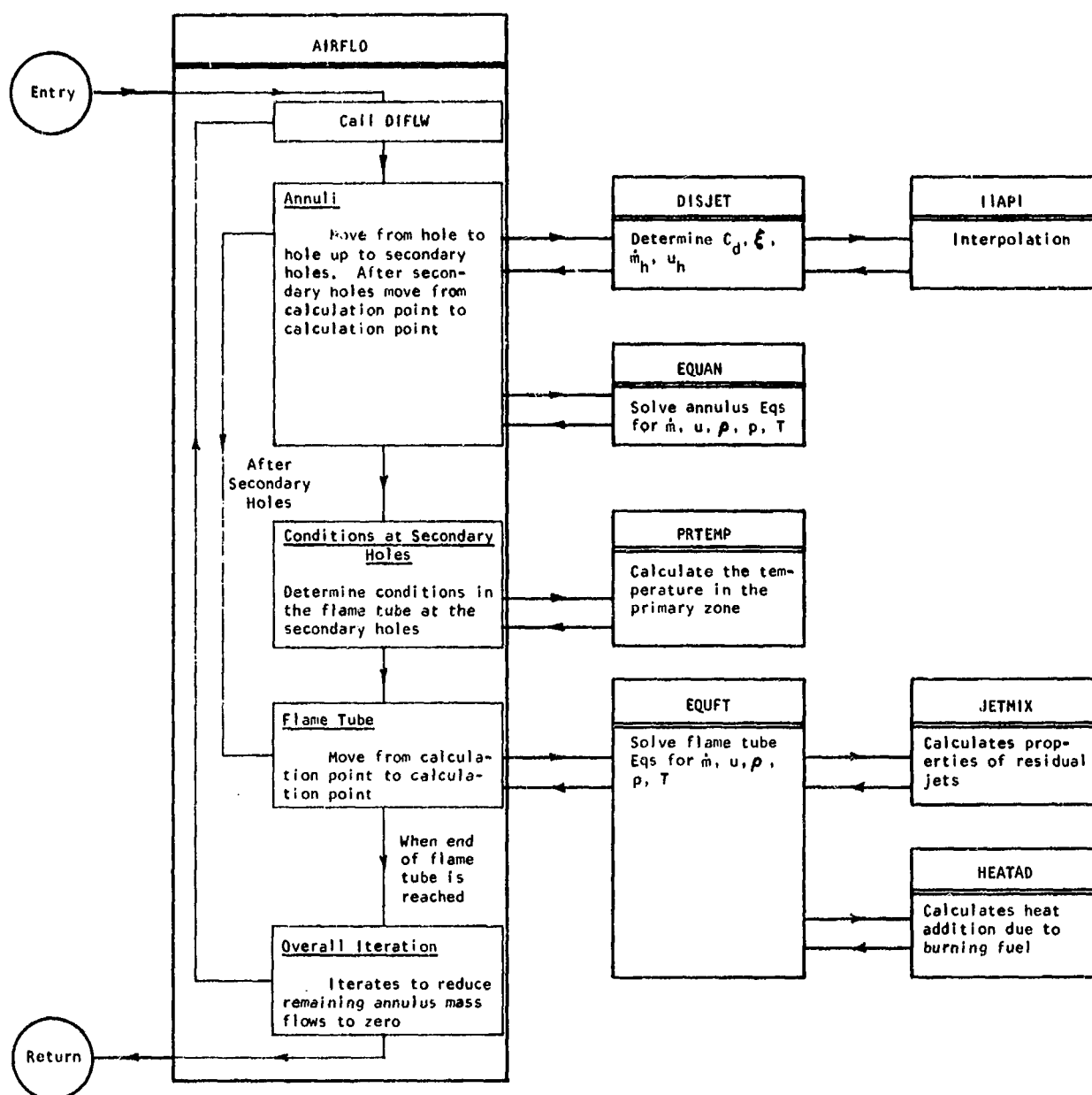


FIGURE 19 - OVERALL FLOW CHART FOR AIR-FLOW SUBPROGRAM

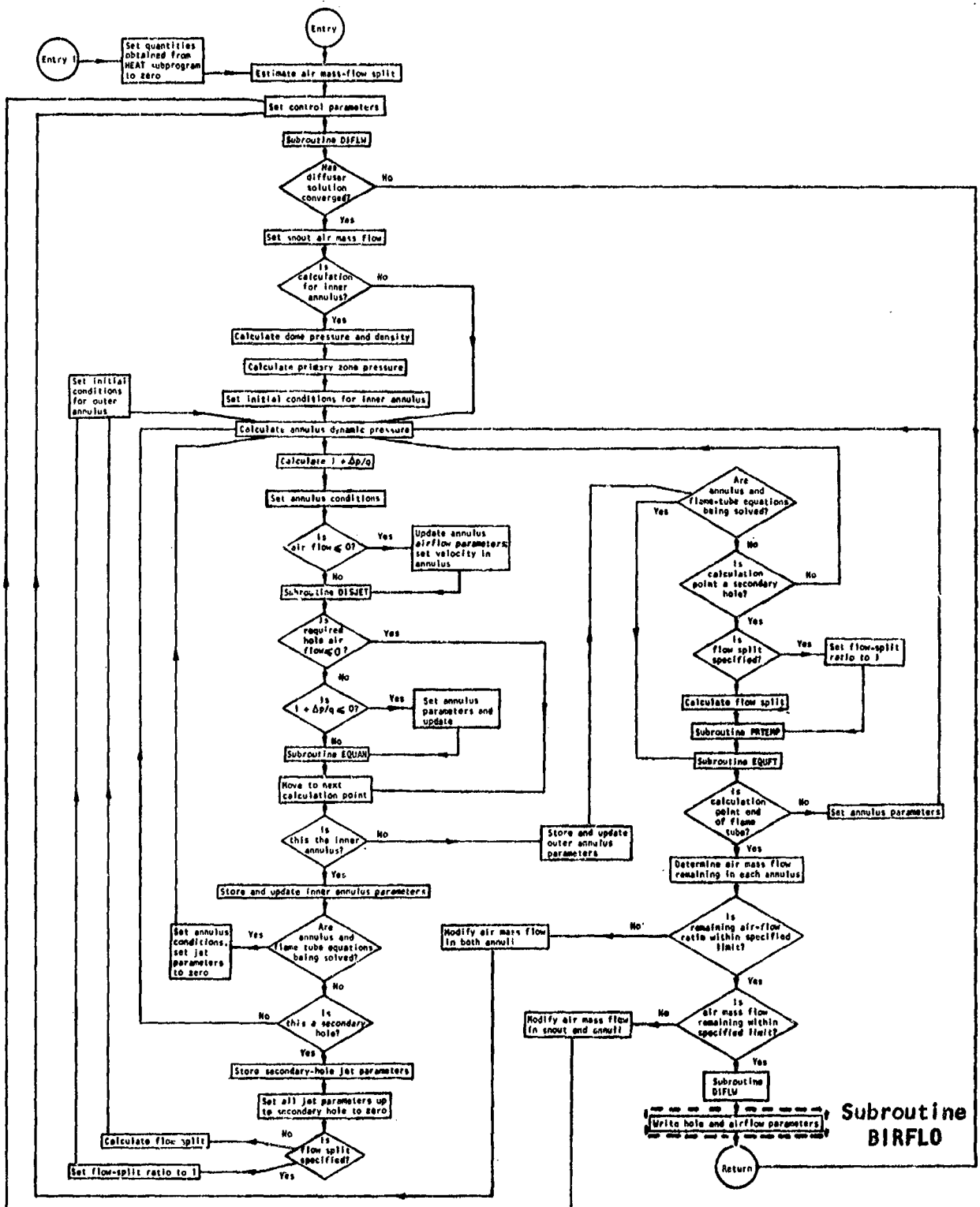


FIGURE 20 - FLOW CHART FOR SUBROUTINE AIRFLO

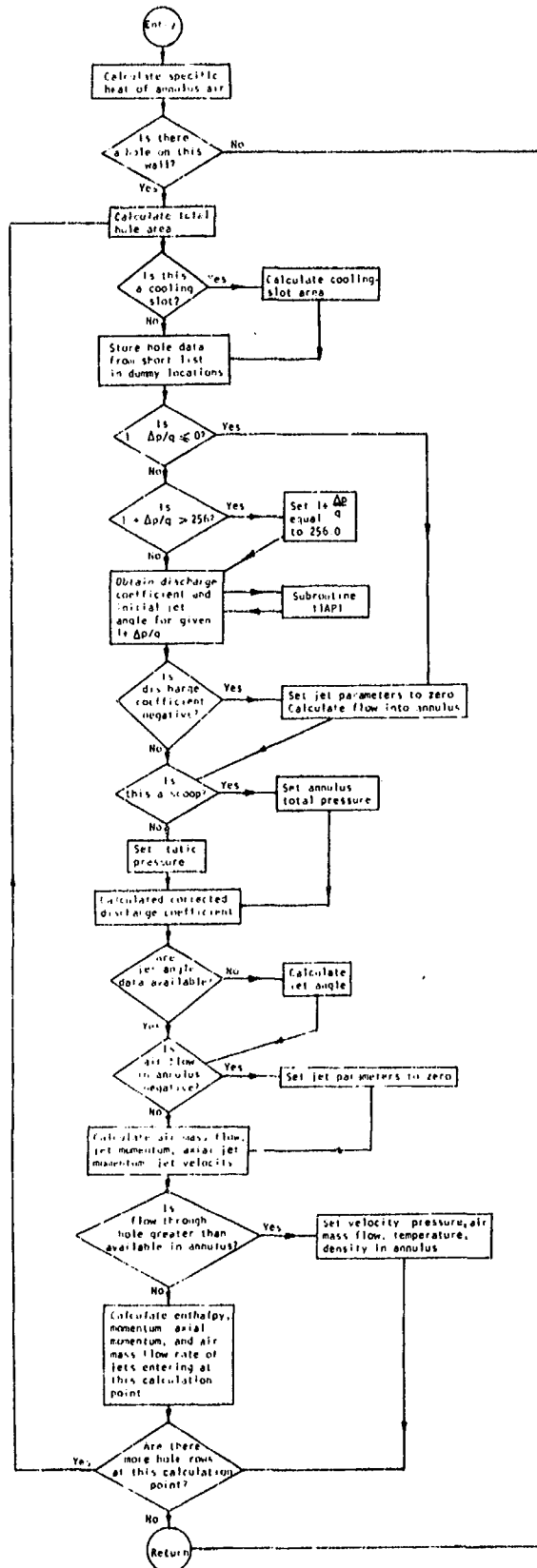


FIGURE 21 - FLOW CHART FOR SUBROUTINE DISJET

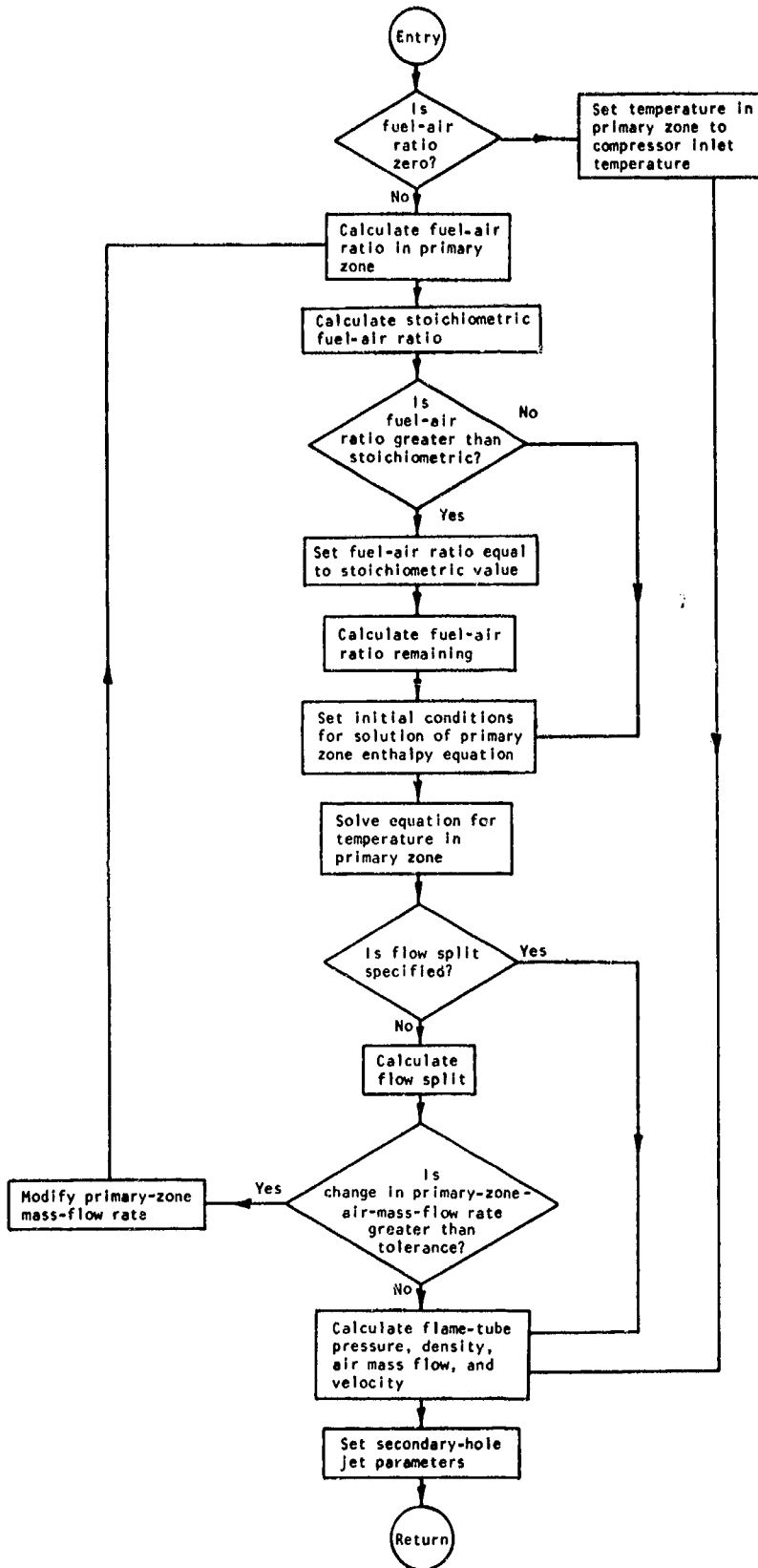


FIGURE 22 - FLOW CHART FOR SUBROUTINE PRTEMP

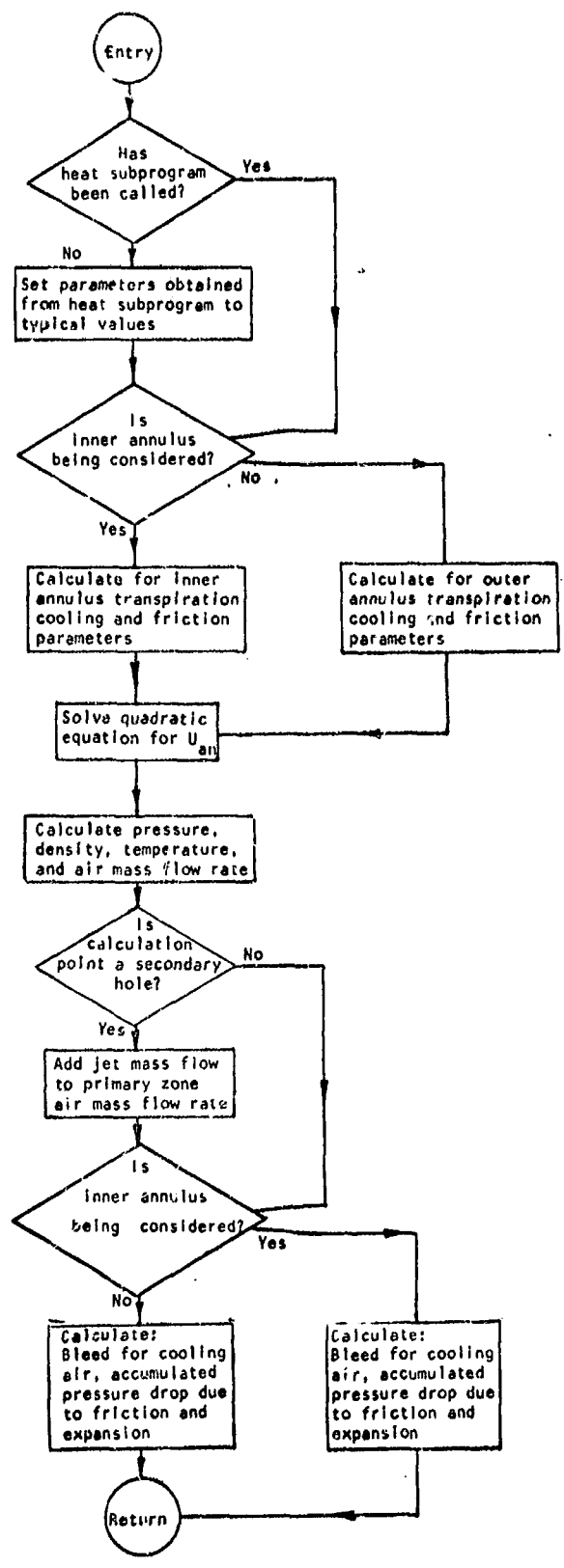


FIGURE 23 - FLOW CHART FOR SUBROUTINE EQUAN

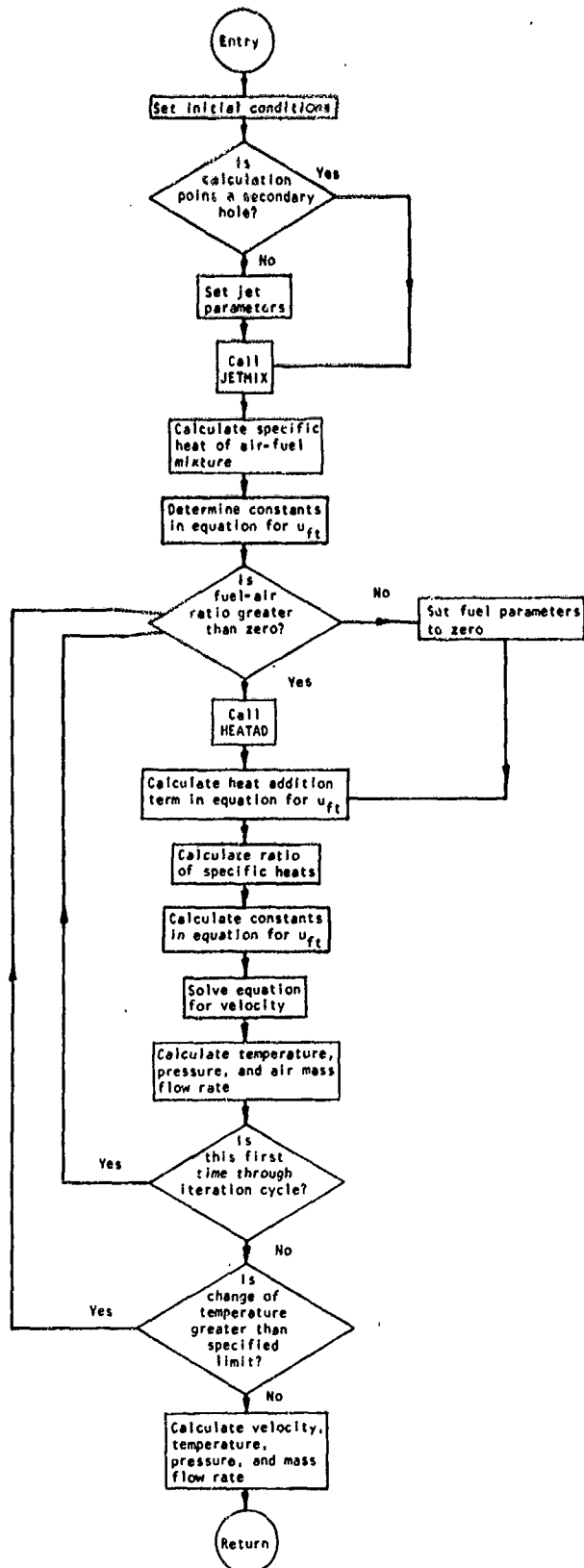
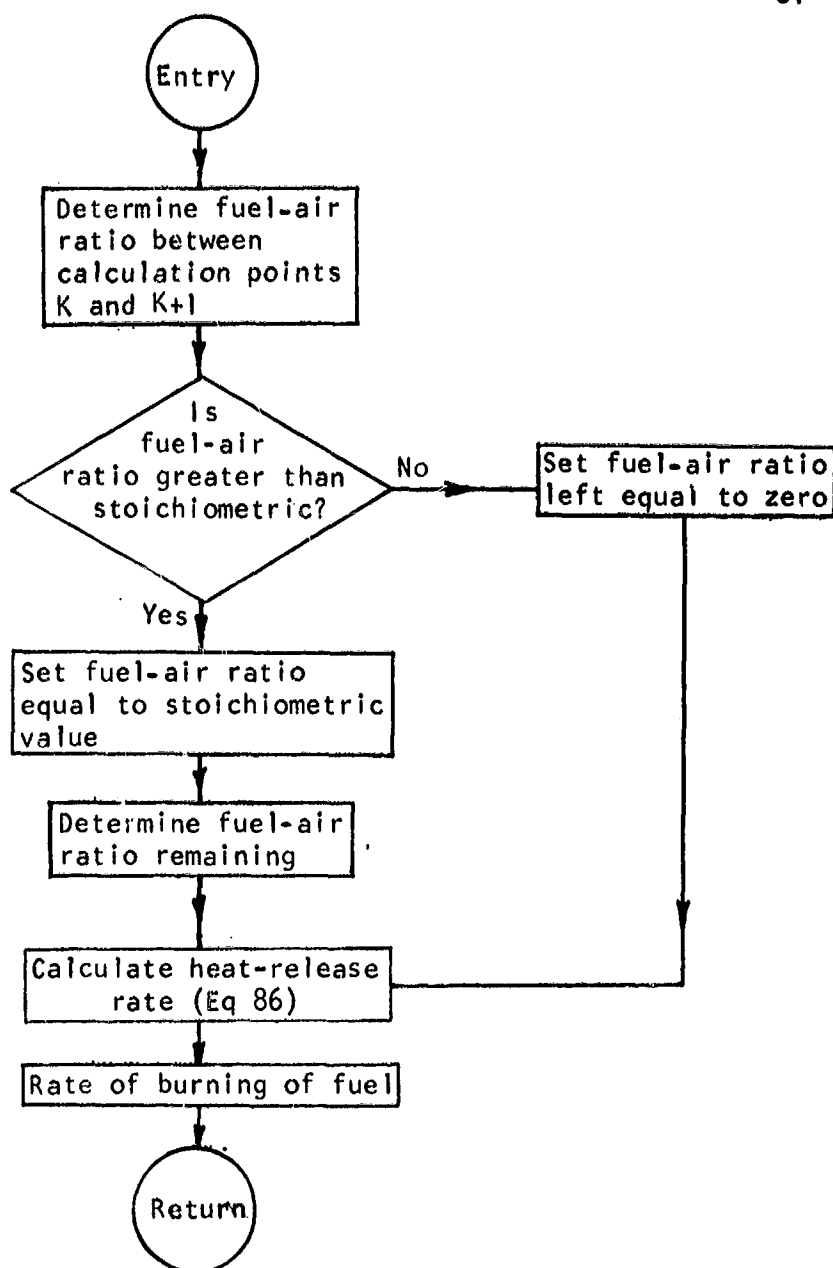
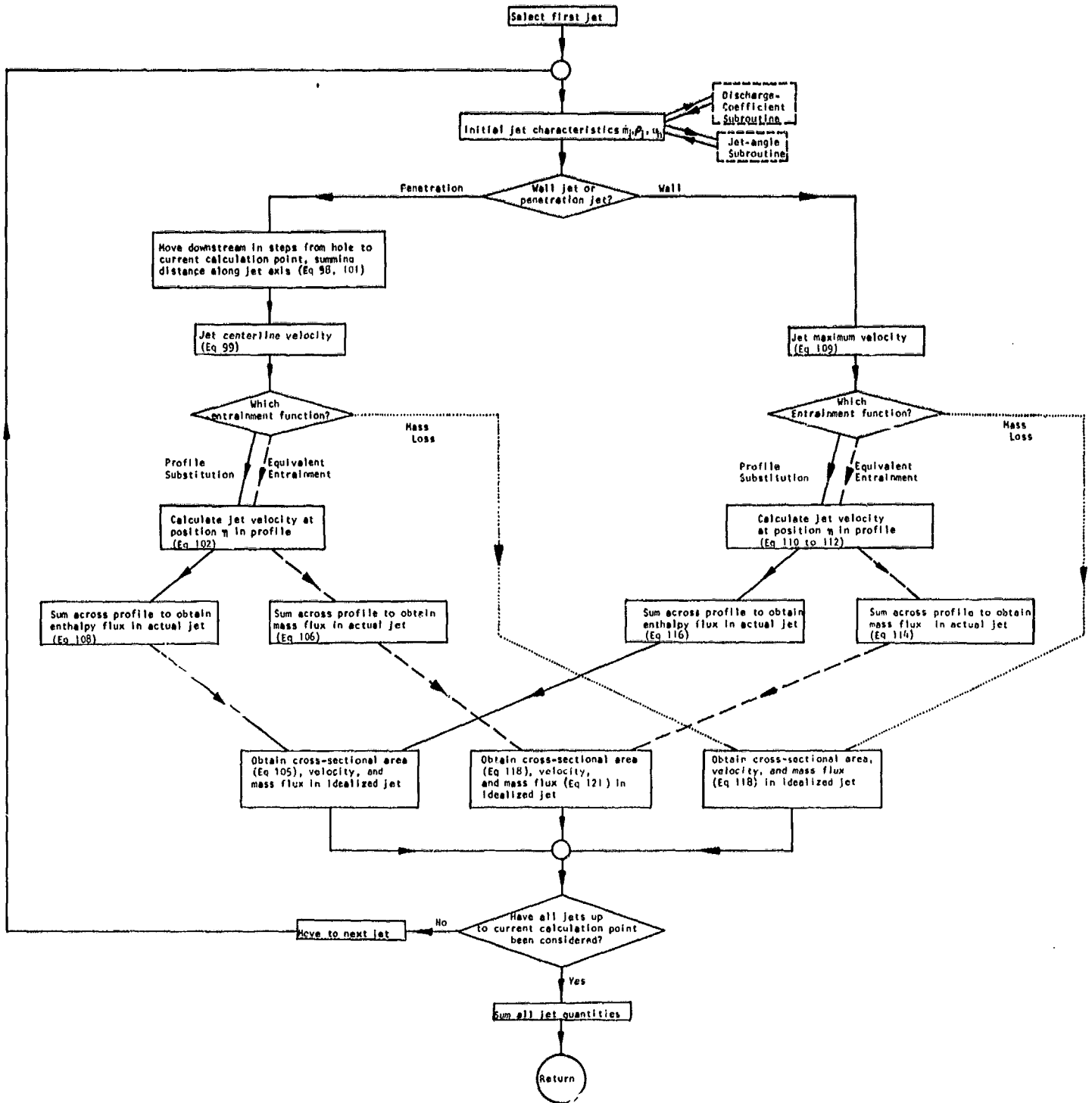


FIGURE 24 - FLOW CHART FOR SUBROUTINE EQUFT



Reference is to Volume I

FIGURE 25 - FLOW CHART FOR SUBROUTINE HEATAD



All References Are to Volume I

FIGURE 26 - FLOW CHART FOR SUBROUTINE JETMIX

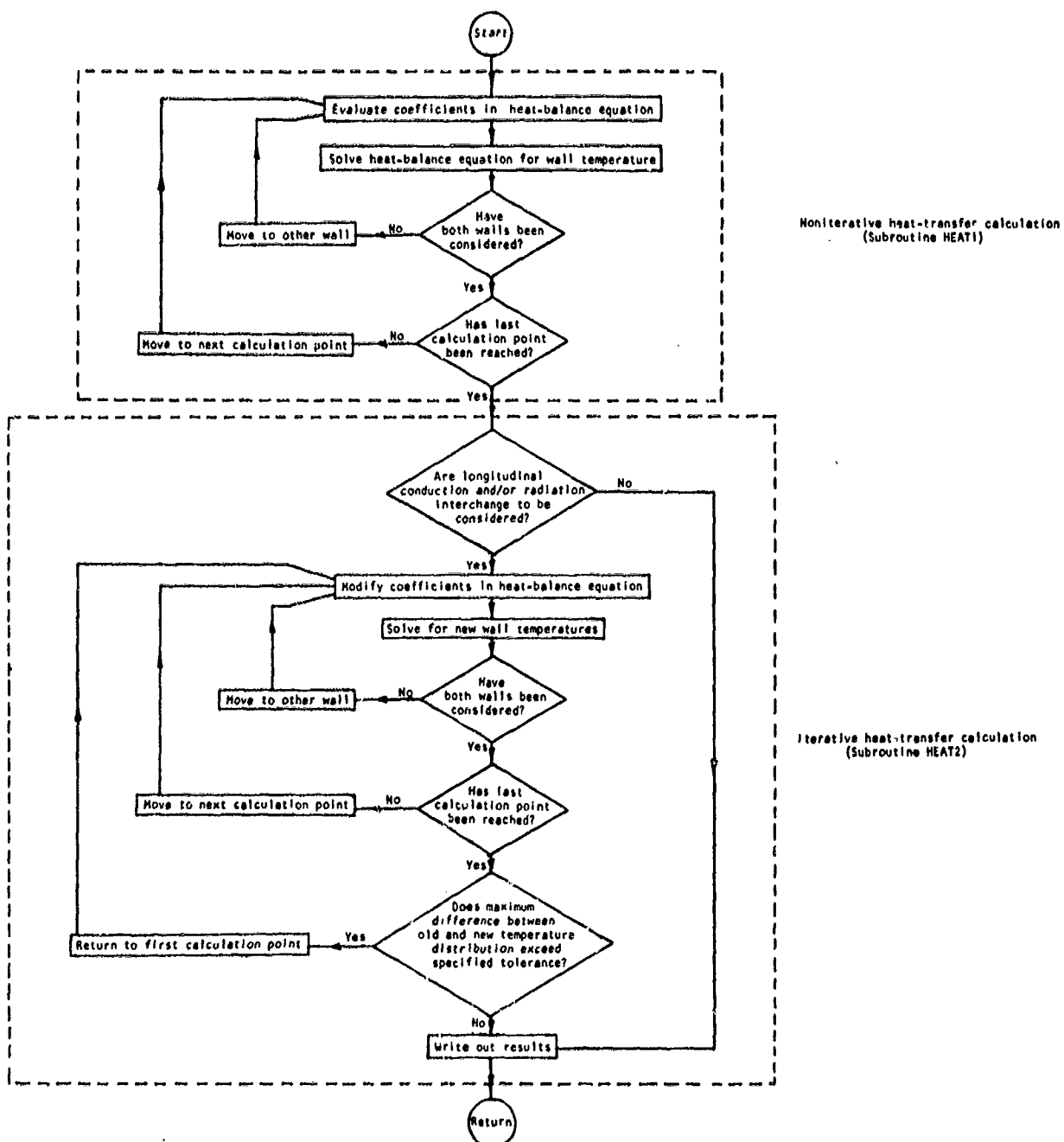
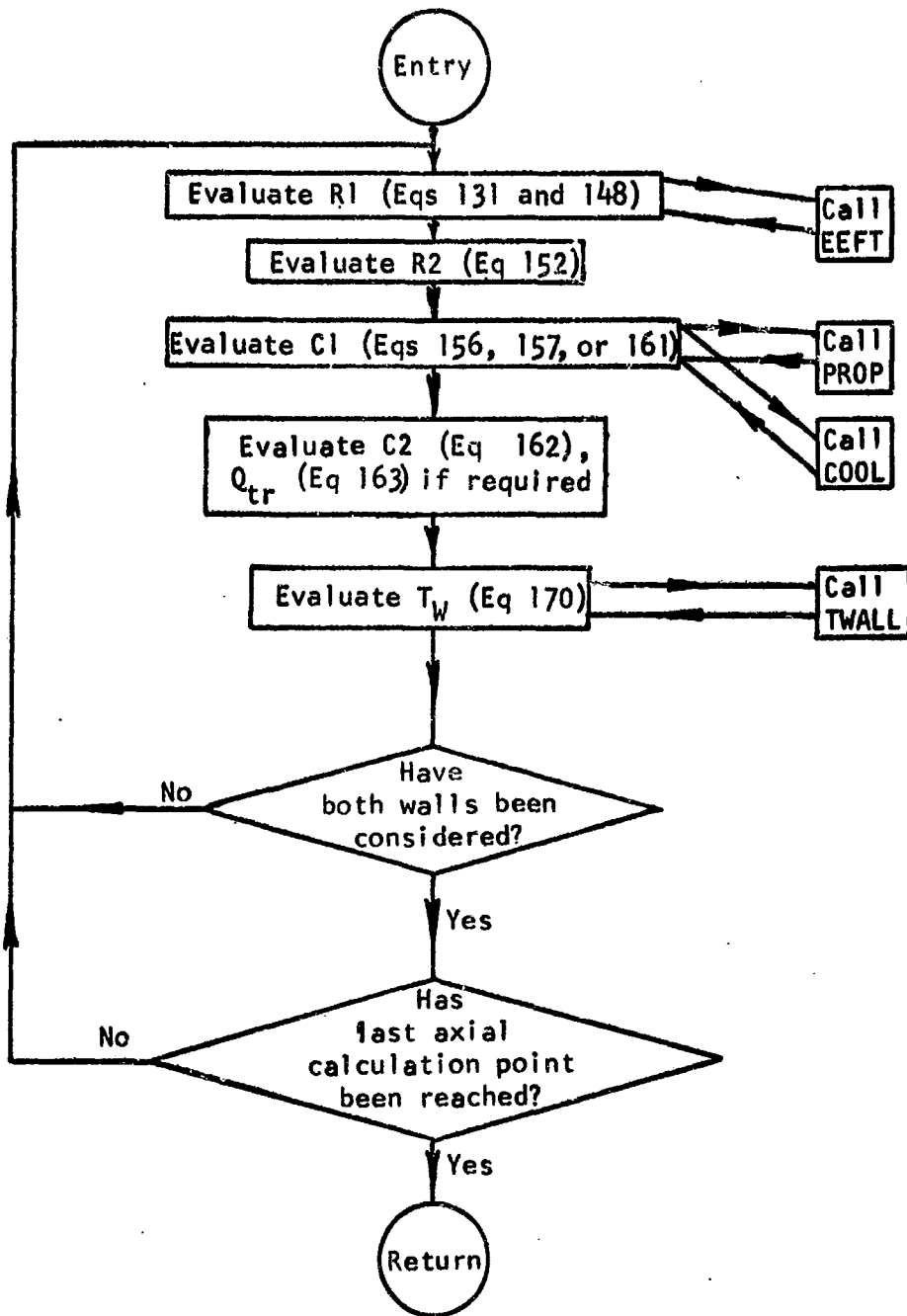
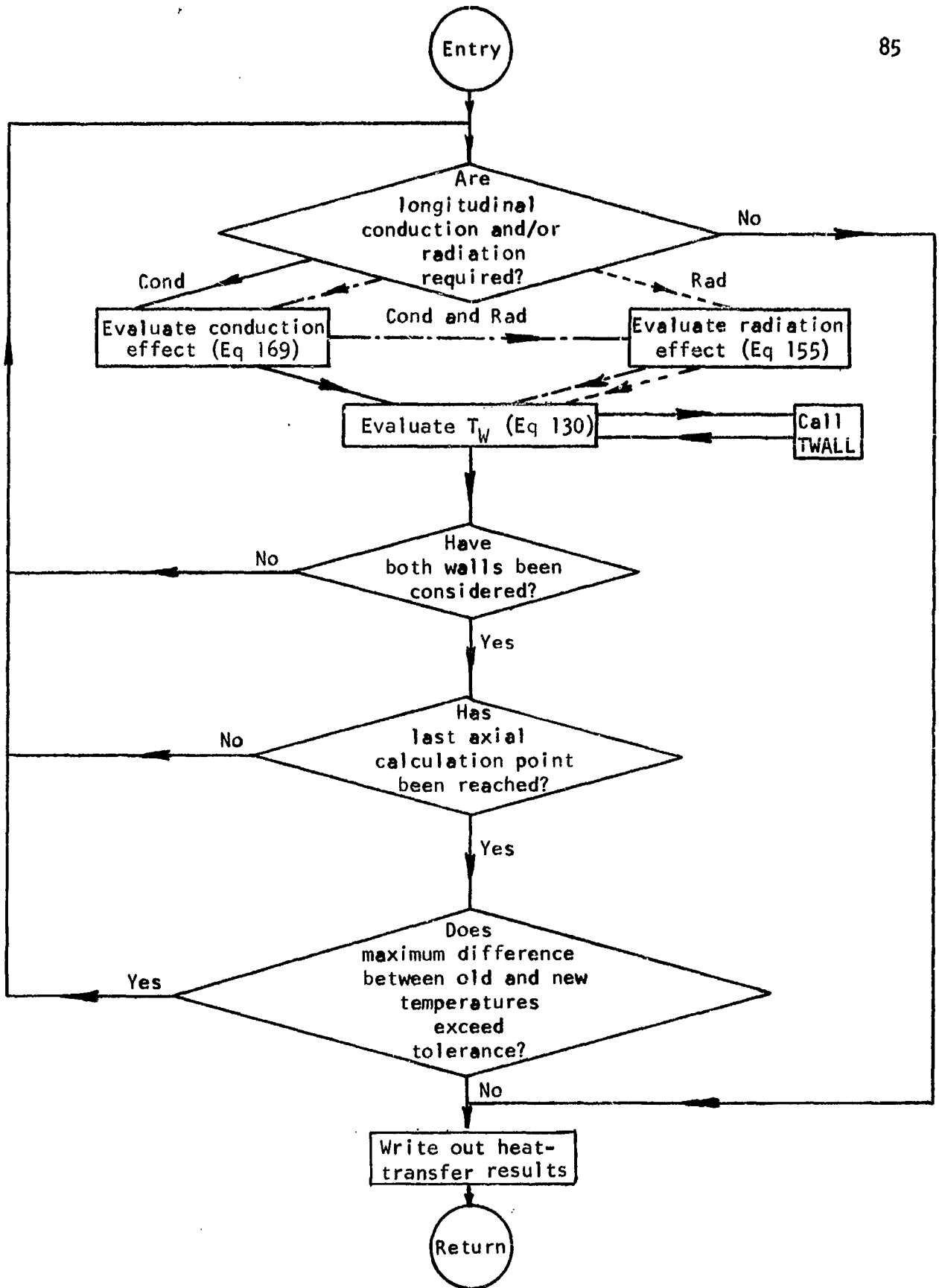


FIGURE 27 - OVERALL FLOW CHART FOR HEAT-TRANSFER SUBPROGRAM



All references are to Volume 1

FIGURE 28 - FLOW CHART FOR SUBROUTINE HEAT1



All references are to Volume I

FIGURE 29 - FLOW CHART FOR SUBROUTINE HEAT2

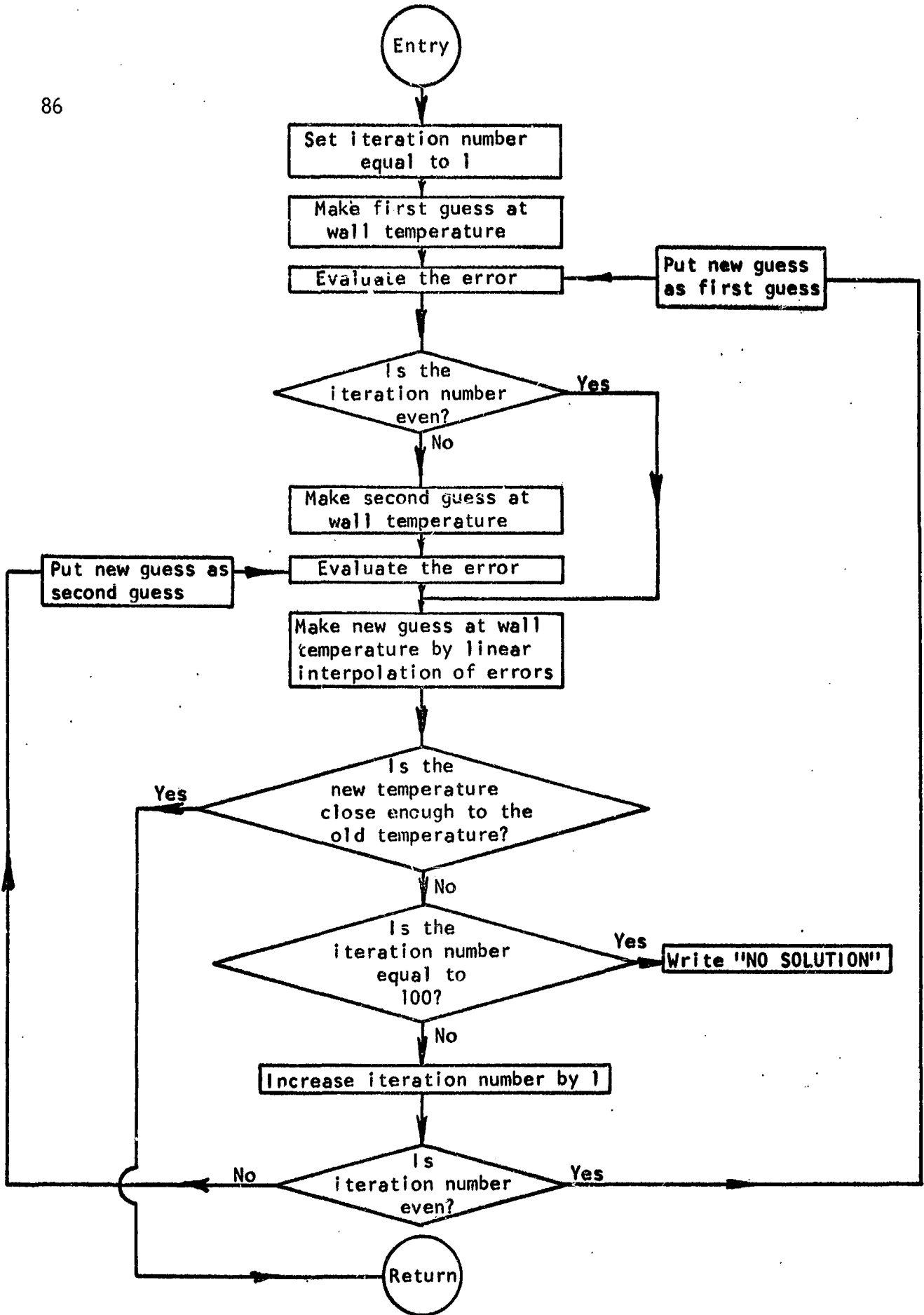
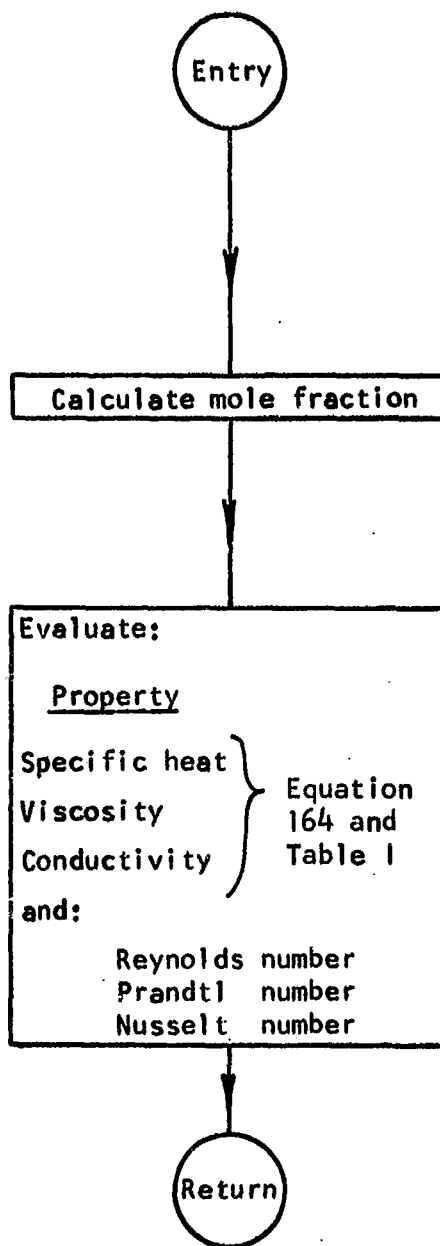
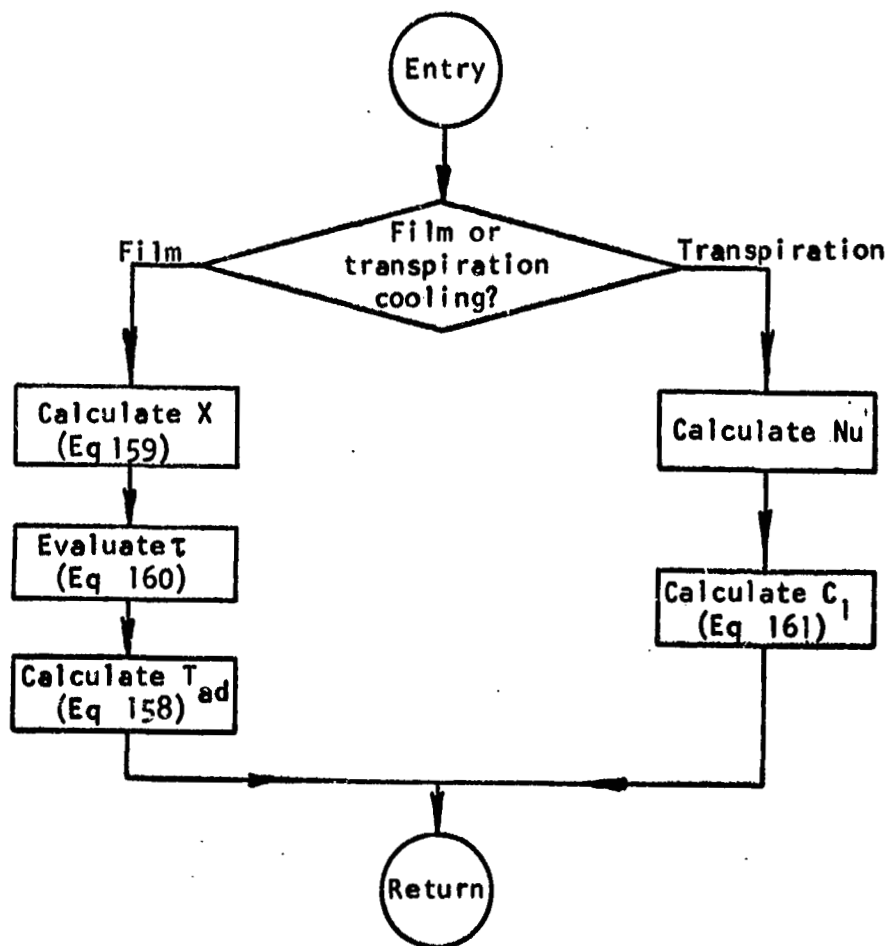


FIGURE 30 - FLOW CHART FOR SUBROUTINE TWALL



All references are to Volume I

FIGURE 31 - FLOW CHART FOR SUBROUTINE PROP



All references are to Volume I

FIGURE 32 - FLOW CHART FOR SUBROUTINE COOL

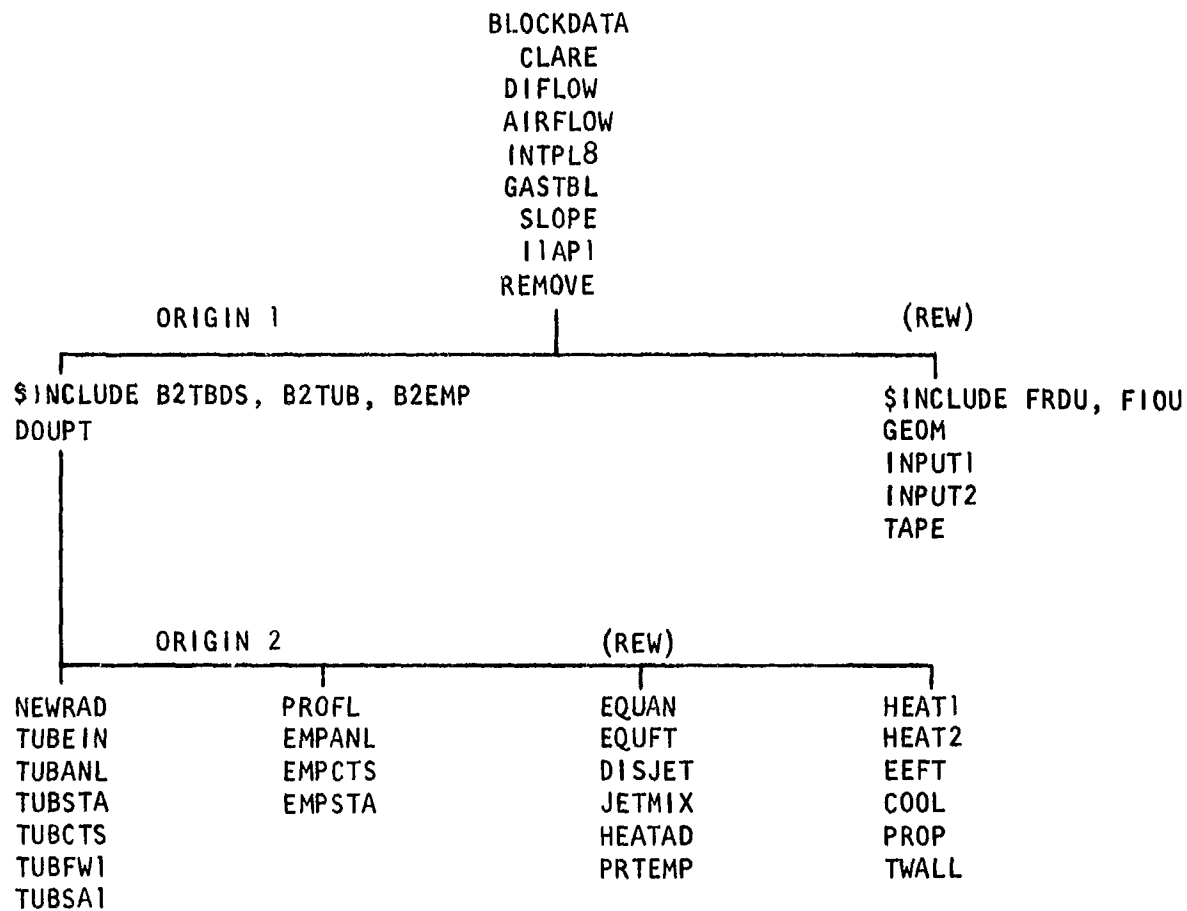


FIGURE 33 - OVERLAY STRUCTURE OF THE PROGRAM

APPENDICES

APPENDIX ISAMPLE LIBRARY-DATA INPUT

The following three sample input-data sheets illustrate the computer card format used for the library data. The numbers at the tops of the input data sheets correspond to the 80 columns in a computer card; each line of data represents the content of one computer card. Beneath each input data sheet is a tabulated version of the data. For a verbal description of the library data-format the reader should refer to pages 27 to 33 of this volume.

Flame Emissivity

1	-	1011	-	2021	-	3031	-	4041	-	5051	-	6061	-	7071	-	80
		4		12		3		133								
540.		1540.		2540.		3540.		4230.		846.		211.5				
.17		.185		.16		.092		.11		.13		.085				
.054		.07		.076		.05		.03								
																1

Data* Employed in Above Example

Pressure lbf/ft ²	Temperature deg F	Flame Emissivity
4230	540	.17
	1540	.185
	2540	.16
	3540	.092
846	540	.11
	1540	.13
	2540	.085
	3540	.054
211.5	540	.07
	1540	.076
	2540	.05
	3540	.03

*Purely Illustrative

Diffuser Effectiveness of Two Diffuser Types

1	1011	2021	3031	4041	5051	6061	7071	80
2								
5	4							
1	14	14	2	-133	0.98			
0.85	0.75	0.3	0.2	0.2	0.2	0.2		
0.73	0.85	0.85	0.78	0.6	0.4	0.2		
1.1	1.2	1.3	1.4	1.5	1.6	1.7		
1.1	1.2	1.3	1.4	1.52	1.62	1.75		
1.0	2.0							
2	8	16	2	133	0.98			
0.9	0.9	0.88	0.87	0.86	0.8	0.67		
0.58	0.88	0.9	0.9	0.88	0.86	0.85		
0.8	0.7	1.1	1.2	1.3	1.4	1.5		
1.6	1.7	1.8	1.0	2.0				
								1

Data Employed in the Above Example

Dimensionless Length	Area Ratio	Diffuser Effectiveness
1.0	1.1	0.85
	1.2	0.75
	1.3	0.3
	1.4	0.2
	1.5	0.2
	1.6	0.2
	1.7	0.2
2.0	1.1	0.73
	1.2	0.85
	1.3	0.85
	1.4	0.78
	1.52	0.6
	1.62	0.4
	1.75	0.2

Dimensionless Length	Area Ratio	Diffuser Effectiveness
1.0	1.1	0.9
	1.2	0.9
	1.3	0.88
	1.4	0.87
	1.5	0.86
	1.6	0.8
	1.7	0.67
	1.8	0.58
2.0	1.1	0.88
	1.2	0.9
	1.3	0.9
	1.4	0.88
	1.5	0.86
	1.6	0.85
	1.7	0.8
	1.8	0.7

Discharge Coefficient and Initial Jet Angle

1	1011	2021	3031	4041	5051	6061	7071	80
2								
10.0625	0.01227		10	91.	0.	0.		
2.	0.33			4.	0.477			
8.	0.555			16.	0.597			
32.	0.623			64.	0.642			
128.	0.65			256.	0.656			
20.164	0.0845		0	71.	0.	0.		
2.	0.475	62.		4.	0.525	66.		
8.	0.565	69.		16.	0.602	72.		
32.	0.635	75.		64.	0.655	77.		
								1

Data Employed in the Above Example

Hole Number	Radius Inches	Area Square Inches	Pressure Loss Factor	Discharge Coefficient	Initial Jet Angle Deg.
1	0.0625	0.01227	1	0	0
			2	0.33	-
			4	0.477	-
			8	0.555	-
			16	0.597	-
			32	0.623	-
			64	0.642	-
			128	0.65	-
2	0.164	0.0845	1	0	0
			2	0.475	62
			4	0.525	66
			8	0.565	69
			16	0.602	72
			32	0.635	75
			64	0.655	77

APPENDIX II

SAMPLE INPUT DATA (OVERALL TEST CASE NUMBER 3)

1	1011	2021	3031	4041	5051	6061	7071	80
SDATA								
TEST CASE NO. 3								
\$FIXED NCASE=1, NG=29, NH=19, NWH=1, NSH=3, NSNOUT=1, K6=1, NUMSW=24\$								
0.	32.5					35.7		
0.5	32.3					35.9		
1.	32.					36.2		
1.5	31.8					36.4		
2.	31.5					36.7		
2.5	31.3					36.9		
2.8	31.1	33.1			35.1	37.1		
3.	31.	33.			35.2	37.2		
4.	30.5	32.5			35.7	37.7		
5.	30.1	32.1			36.1	38.1		
6.	29.6	31.6			36.6	38.6		
7.	29.1	31.1	34.1	34.1	37.1	39.1		
8.	28.6	30.6	31.1	37.1	37.6	39.6		
8.8	28.2	30.2	30.2	38.	38.	40.		
9.	28.2	30.2	30.2	38.	38.	40.		
9.1	28.2	29.9	29.9	38.3	38.3	40.		
14.	28.2	29.9	29.9	38.3	38.3	40.		
15.	28.2	29.9	29.9	38.3	38.3	40.		
15.1	28.2	29.6	29.6	38.6	38.6	40.		
20.	28.2	29.6	29.6	38.6	38.6	40.		
21.	28.2	29.6	29.6	38.6	38.6	40.		
21.1	28.2	29.3	29.3	38.9	38.9	40.		
26.	28.2	29.3	29.3	38.9	38.9	40.		
27.	28.2	29.3	29.3	38.9	38.9	40.		
27.1	28.2	29.	29.	39.2	39.2	40.		
29.	28.2	29.	29.	39.2	39.2	40.		
30.	28.2	29.	29.	38.2	38.2	40.		
31.	28.2	29.	29.	37.2	37.2	40.		
32.8	28.2	29.	29.	37.2	37.2	40.		

APPENDIX III

SAMPLE COMPUTER OUTPUT

(RESULTS OF OVERALL TEST CASE NO. 3)

ANALYSIS OF AN ANNULAR COMBUSTOR

TEST CASE NO. 3

***** INPUT DATA *****

GEOMETRIC CONFIGURATION OF COMBUSTOR

 THE GEOMETRY IS DEFINED AT 29 GEOMETRIC INPUT POINTS

AXIAL POSITION FROM COMPRESSOR DISCHARGE INCHES	----- DIAMETER INCHES -----						GEOMETRIC INPUT POINT NUMBER
	INNER CASING	INNER SNOUT	INNER DOME OR FLAME TUBE WALL	CLTER DOME OR FLAME TUBE WALL	OUTER SNOUT	CLTER CASING	
0.	32.500	-0.	-0.	-0.	-0.	35.700	1
0.500	32.300	-0.	-0.	-0.	-0.	35.900	2
1.000	32.000	-0.	-0.	-0.	-0.	36.200	3
1.500	31.800	-0.	-0.	-0.	-0.	36.400	4
2.000	31.500	-0.	-0.	-0.	-0.	36.700	5
2.500	31.300	-0.	-0.	-0.	-0.	36.900	6
2.800	31.100	33.100	-0.	-0.	35.100	37.100	7
3.000	31.000	33.000	-0.	-0.	35.200	37.200	8
4.000	30.500	32.500	-0.	-0.	35.700	37.700	9
5.000	30.100	32.100	-0.	-0.	36.100	38.100	10
6.000	29.600	31.600	-0.	-0.	36.600	38.600	11
7.000	29.100	31.100	34.100	34.100	37.100	39.100	12
8.000	28.600	30.600	31.100	37.100	37.600	39.600	13
8.800	28.200	30.200	30.200	38.000	38.000	40.000	14
9.000	28.200	30.200	30.200	38.000	38.000	40.000	15
9.100	28.200	29.900	29.900	38.300	38.300	40.000	16
14.000	28.200	29.900	29.900	38.300	38.300	40.000	17
15.000	28.200	29.900	29.900	38.300	38.300	40.000	18
15.100	28.200	29.600	29.600	38.600	38.600	40.000	19
20.000	28.200	29.600	29.600	38.600	38.600	40.000	20
21.000	28.200	29.600	29.600	38.600	38.600	40.000	21
21.100	28.200	29.300	29.300	38.900	38.900	40.000	22
26.000	28.200	29.300	29.300	38.900	38.900	40.000	23
27.000	28.200	29.300	29.300	38.900	38.900	40.000	24
27.100	28.200	29.000	29.000	39.200	39.200	40.000	25
29.000	28.200	29.000	29.000	39.200	39.200	40.000	26
30.000	28.200	29.000	29.000	39.200	39.200	40.000	27
31.000	28.200	29.000	29.000	37.200	37.200	40.000	28
32.800	28.200	29.000	29.000	37.200	37.200	40.000	29

SWIRLER DESIGN

(SPECIFIED AS INPUT)

NUMBER OF SWIRLERS = 24
 NUMBER OF BLADES = 4
 BLADE STAGGER ANGLE = 45.00 DEGREES
 INNER DIAMETER = 1.00 INCHES
 OUTER DIAMETER = 1.50 INCHES
 AREA PER SWIRLER = 0.94 SQUARE INCHES (IGNORING BLOCKAGE DUE TO VANES)

DETAILS OF AIR ENTRY PORTS AND GEOMETRY AT EACH HOLE ROW

THERE ARE 19 HOLE ROWS

HOLE ROW NUMBER	AXIAL POSITION OF HOLE CENTER-LINE INCHES	HOLE TYPE	INNER OR OUTER WALL	NUMBER OF HOLES IN THIS ROW	TOTAL PORT AREA AT THIS HOLE ROW SQUARE FEET	RATIO TOTAL PORT AREA THIS ROW TO GRAND TOTAL	CUMULATIVE SUM OF AREA RATIO (LAST COLUMN)	RATIO FLAME TUBE C S AREA TO REF AREA	RATIO INNER ANALLUS C S AREA TO REF AREA	RATIO OUTER ANVILLUS C S AREA TO REF AREA
-----------------	---	-----------	---------------------	-----------------------------	--	---	--	---------------------------------------	--	---

TOTAL COOLING AIR ENTRY PORT AREA IN THE DOME = 0. SC FT
 TOTAL PENETRATION AIR ENTRY PORT AREA IN THE DOME = 0.164 SQ FT (INCLUDING TOTAL SWIRLER AREA)

					FLAME TUBE WALL								
1	9.000	44	INNER	1	0.	0.063	0.	0.111	0.045	0.111	0.651	0.145	0.194
2	9.000	44	OUTER	1	0.	0.079	0.	0.139	0.045	0.250	0.661	0.145	0.194
3	12.000	75	INNER	50	0.153	0.	0.042	0.	0.087	0.250	0.712	0.123	0.165
4	12.000	75	OUTER	50	0.153	0.	0.042	0.	0.128	0.250	0.712	0.123	0.165
5	15.500	0		-0	0.	0.	0.	0.	0.128	0.250	0.712	0.123	0.165
6	15.000	44	INNER	1	0.	0.062	0.	0.110	0.128	0.360	0.712	0.123	0.165
7	15.000	44	OUTER	1	0.	0.079	0.	0.140	0.128	0.500	0.712	0.123	0.165
8	16.500	0		-0	0.	0.	0.	0.	0.128	0.500	0.763	0.101	0.137
9	18.000	27	INNER	40	0.556	0.	0.152	0.	0.280	0.500	0.763	0.101	0.137
10	18.000	27	OUTER	40	0.556	0.	0.152	0.	0.432	0.500	0.763	0.101	0.137
11	19.500	0		-0	0.	0.	0.	0.	0.432	0.500	0.763	0.101	0.137
12	21.000	44	INNER	1	0.	0.061	0.	0.105	0.432	0.609	0.763	0.101	0.137
13	21.000	44	OUTER	1	0.	0.080	0.	0.141	0.432	0.750	0.763	0.101	0.137
14	22.500	0		-0	0.	0.	0.	0.	0.432	0.750	0.814	0.079	0.108
15	24.000	27	INNER	75	1.042	0.	0.284	0.	0.716	0.750	0.814	0.079	0.108
16	24.000	27	OUTER	75	1.042	0.	0.284	0.	1.000	0.750	0.814	0.079	0.108
17	27.000	44	INNER	1	0.	0.061	0.	0.107	1.000	0.857	0.814	0.079	0.108
18	27.000	44	OUTER	1	0.	0.081	0.	0.143	1.000	1.000	0.814	0.079	0.108
19	32.700	0		-0	0.	0.	0.	0.	1.000	1.000	0.675	0.057	0.269

TOTAL COOLING PORT AREA IN THE FLAME-TUBE WALL = 0.565 SQ FT
 TOTAL PENETRATION PORT AREA IN THE FLAME-TUBE WALL = 3.501 SQ FT

RATIO OF TOTAL HOLE AREA (INCLUDING SHT LIP, COME HOLES,
COOLING SLOTS, AND PENETRATION HOLES) TO REFERENCE AREA = 0.964

THERE ARE NO JET-ANGLE DATA FOR HOLE TYPE NO. 75. THE INITIAL JET-ANGLE ESTIMATE USED IN THE PROGRAM IS NOT AT ALL
ACCURATE FOR SCRAMS.

100

MISCELLANEOUS DATA - DIFFUSER SECTION

THE DIFFUSER SECTION CONTAINS A SNOOT
INPUT POINT 7 IS THE LAST STATION BEFORE THE SNOOT
DIFFUSION IS CONSIDERED TO END AT INPUT POINT NUMBER 14 IN THE INNER ANNULUS
DIFFUSION IS CONSIDERED TO END AT INPUT POINT NUMBER 14 IN THE OUTER ANNULUS
THE EMPIRICAL DATA TO BE USED BEFORE THE SNOOT IS SET NUMBER 1
THE EMPIRICAL DATA TO BE USED AFTER THE SNOOT IS SET NUMBER 1

MISCELLANEOUS DATA - AIRFLOW SECTION

HOLE ROW NUMBER 1 IS THE FIRST HOLE ROW IN THE FLAME-TUBE WALL, AS DISTINCT FROM THE COME
HOLE ROW NUMBER 3 IS CONSIDERED TO MARK THE END OF THE PRIMARY ZONE (WHICH IS CONSIDERED AS A STIRRED REACTOR)
THE FRACTION OF AIR FLOWING THROUGH THE SECONDARY HOLES THAT RECIRCULATES
INTO THE PRIMARY ZONE IS WORKED OUT IN THE PROGRAM
THE FLOW RESISTANCE IN THE SNOOT IS 0. VELOCITY HEADS (BASED ON CONDITIONS IN THE SNOOT LIP)
FRACTION OF INLET AIR BYPASSING COMBUSTOR

INNER ANNULUS 0.010
OUTER ANNULUS 0.030

AXIAL POSITION AT WHICH THIS OCCURS

INNER ANNULUS 32.800 IN
OUTER ANNULUS 32.800 IN

FUEL DATA

LOWER HEATING VALUE* 18560.0 BTU PER LBM
HYDROGEN/CARBON RATIO 0.170

MISCELLANEOUS DATA - HEAT TRANSFER SECTION

FLAME TUBE WALL THICKNESS..... 0.060 IN
THERMAL CONDUCTIVITY OF WALL MATERIAL... 15.00 BTU PER FT HR DEG F
ABSORPTIVITY OF FLAME TUBE WALL..... 0.350
EMISSIVITY OF FLAME TUBE WALL..... 0.850
EMISSIVITY OF OUTER CASING..... 0.800
THE CASING TEMPERATURE IS NOT SPECIFIED
FILM COOLING CAN BE USED
TRANSPIRATION COOLING IS NOT USED

CASES CONSIDERED IN THIS PLAN

1 CASES ARE TO BE CONSIDERED
PROGRAM ROUTING IS ALTERED FROM CASE TO CASE

INLET FLOW CONDITIONS

TOTAL TEMPERATURE AT COMPRESSOR DISCHARGE = 1150.000 DEG F
 TOTAL PRESSURE AT COMPRESSOR DISCHARGE = 96.000 PSIA
 AIR FLOW RATE AT COMPRESSOR DISCHARGE = 96.000 LBM PER SEC
 OVERALL FUEL-AIR RATIO = 0.014

DIFFUSER INPUT DATA

INLET SHAPE FACTORS
 INNER WALL = 1.400
 OUTER WALL = 1.400
 INLET BOUNDARY LAYER BLOCKAGE = 0.006
 FRACTION OF INLET BLOCKAGE ON INNER WALL = 0.500
 NUMBER OF STREAM TUBES TO BE CONSIDERED = 7

FIRST ESTIMATE OF BLOCKAGE AT DOWNSTREAM POINTS

AXIAL DISTANCE INCHES	BLOCKAGE
0.	0.006
0.400	0.010
1.000	0.010
1.500	0.010
2.000	0.010
2.500	0.010
2.800	0.010

INLET VELOCITY PROFILE

FRACTIONAL DISTANCE ACROSS INLET PLANE (MEASURED FROM INNER WALL)	VELOCITY NONDIMENSIONALIZED WITH AN ARBITRARY VELOCITY
0.100	0.850
0.200	0.900
0.300	1.000
0.400	0.900
0.500	0.900
0.600	0.900
0.700	0.850

FUEL BURNING RATE AND CASING TEMPERATURE AT CALCULATION POINTS

CALCULATION POINT NUMBER	AXIAL POSITION IN	CUMULATIVE FRACTION FUEL BURNED	FUEL BURNING RATE LBM PER SEC	CASING TEMPERATURE DEG F	
				INNER	OUTER
1	9.000	0.100	0.173	1150.0	1150.0
2	9.500	0.123	0.144	1150.0	1150.0
3	10.000	0.247	0.144	1150.0	1150.0
4	10.500	0.350	0.144	1150.0	1150.0
5	11.000	0.433	0.144	1150.0	1150.0
6	11.625	0.537	0.140	1150.0	1150.0
7	13.500	0.700	0.281	1150.0	1150.0
8	15.000	0.800	0.173	1150.0	1150.0
9	15.500	0.817	0.027	1150.0	1150.0
10	16.000	0.833	0.027	1150.0	1150.0
11	16.500	0.850	0.027	1150.0	1150.0
12	17.000	0.867	0.027	1150.0	1150.0
13	19.500	0.950	0.144	1150.0	1150.0
14	21.000	0.950	0.	1150.0	1150.0
15	21.500	0.950	0.	1150.0	1150.0
16	22.000	0.950	0.	1150.0	1150.0
17	22.500	0.950	0.	1150.0	1150.0
18	23.000	0.950	0.	1150.0	1150.0
19	27.000	0.950	0.	1150.0	1150.0
20	27.500	0.950	0.	1150.0	1150.0
21	28.000	0.950	0.	1150.0	1150.0
22	28.500	0.950	0.	1150.0	1150.0
23	29.000	0.950	0.	1150.0	1150.0
24	32.700	0.950	0.	1150.0	1150.0
25	32.800	0.950	0.	1150.0	1150.0

ROUTING THROUGH THE PROGRAM

THE EQUIVALENT ENTRAINMENT MODEL IS USED TO REPRESENT JET MIXING WITH A CONSTANT OF 1.000 FOR PENETRATION JETS AND 0.200 FOR WALL JETS
 HEAT TRANSFER TO ANNULUS AIR IS NOT CONSIDERED
 THE FLAME IS ASSUMED TO BE LUMINOUS. THE LEFFERVRE CORRELATION IS USED
 THE BASIC HEAT TRANSFER CALCULATION SOLVES FOR A MODEL WITH COOLED FLAME-TUBE WALLS AND 1-DIMENSIONAL RADIATION TRANSFER FROM THE FLAME
 NO CORRECTIONS ARE MADE TO THE BASIC HEAT TRANSFER CALCULATION
 THE STREAPTURE METHOD IS USED TO CALCULATE DIFFUSER PERFORMANCE FROM THE DIFFUSER INLET TO THE SNOUT
 THE MIXING EQUATION METHOD IS USED TO CALCULATE THE DIFFUSER PERFORMANCE IN THE PASSAGES BETWEEN SNOUT AND OUTER CASING
 IF EMPIRICAL DATA ARE USED TO CALCULATE THE DIFFUSER EFFECTIVENESS, THESE DATA ARE TAKEN FROM THE LIBRARY FILE

REFERENCE CONDITIONS

REFERENCE AREA = 4.389 SQ FT
 REFERENCE VELOCITY = 145.2 FT PER SEC
 INLET MACH NUMBER = 0.287
 REFERENCE MACH NUMBER = 0.074
 REFERENCE DYNAMIC PRESSURE = 0.34 PSI

DIFFUSER PARAMETERS - COMPRESSOR OUTLET TO THE LIP OF THE SACUT

IN THIS PART OF THE DIFFUSER A SIMPSON ANALYSIS IS USED

DIFFUSER PERFORMANCE

NO MIXING AT OUTLET
 IDEAL PRESSURE RECOVERY COEFF. = 0.716
 PRESSURE RECOVERY COEFF. = 0.540
 DIFFUSER EFFECTIVENESS = 0.755
 FRACTIONAL TOTAL PRESSURE LOSS = 0.000

VELOCITY PROFILE AT EXIT OF DIFFUSER

FRACTIONAL ANNULUS HEIGHT.....	0.114	0.191	0.278	0.345	0.423	0.500	0.577	0.655	0.732	0.809	0.886
HEIGHT ALLOWING FOR BLOCKAGE...	0.	0.100	0.200	0.300	0.400	0.500	0.600	0.700	0.800	0.900	1.000
VELOCITY, FT PER SEC.....	294.40	328.59	373.06	429.31	472.42	375.84	380.03	342.61	380.20	376.13	285.03

BOUNDARY LAYER PROPERTIES - SOLUTION HAS CONVERGED

STATION NUMBER	X(1) IN	PRESSURE PSIA	INNER WALL			OUTER WALL			ANN. AREA SQ IN	FRACTIONAL BLOCKAGE	STATION NUMBER
			DELTA IN	TETA IN	H	DELTA IN	TETA IN	H			
1	0.	84.902	0.005	0.004	1.400	0.005	0.003	1.400	171.475	0.0062	1
2	0.500	85.994	0.012	0.008	1.567	0.011	0.007	1.575	152.831	0.0174	2
3	1.000	87.006	0.029	0.016	1.812	0.027	0.015	1.775	224.969	0.0256	3
4	1.500	87.413	0.042	0.024	1.780	0.040	0.023	1.769	246.355	0.0342	4
5	2.000	87.440	** 0.083	0.039	2.151**	** 0.080	0.038	2.137**	278.513	0.0605	5
6	2.500	87.531	0.253	0.030	3.500	0.252	0.029	3.500	299.955	0.1734	6
7	2.800	87.545	0.358	0.030	3.400	0.357	0.029	3.500	321.395	0.2274	7

SEPARATION IF IT OCCURS IS INDICATED BY **.....**

DIFFUSER PARAMETERS - INNER DIFFUSING PASSAGE BETWEEN SNOUT AND CASING

IN THIS PART OF THE DIFFUSER THE PERFORMANCE IS CALCULATED USING THE MIXING EQUATION

DIFFUSER PERFORMANCE

FLOW ALLOWED TO MIX AT OUTLET

IDEAL PRESSURE RECOVERY COEFF. = -0.130 (INCLUDING MIXING EFFECTS)

PRESSURE RECOVERY COEFF. = -0.275

DIFFUSER EFFECTIVENESS = 1.445

FRACTIONAL TOTAL PRESSURE LOSS = 0.007 (BASED ON MEAN CONDITIONS AT COMPRESSOR OUTLET)

THIS SECTION HAS AN AREA RATIO LESS THAN ONE AND ACTS AS A NOZZLE AND NOT AS A DIFFUSER
 THE VALUE PRINTED OUT AS THE DIFFUSER EFFECTIVENESS IS NOT AN INDICATION OF HOW WELL THE SECTION PERFORMS
 MISMATCH AT THE SNOUT IS CHARACTERISED BY THE RATIO -
 (TOTAL STREAMTUBE AREA JUST BEFORE THE SNOUT)/(FLOW AREA JUST INSIDE THE SNOUT). THIS RATIO IS 1.356
 AS THIS RATIO IS OUTSIDE THE RANGE 0.85-1.15 THE FLOW SPLIT ON THE SNOUT IS NOT WELL MATCHED

DIFFUSER PARAMETERS - OUTER DIFFUSING PASSAGE BETWEEN SNOUT AND CASING

IN THIS PART OF THE DIFFUSER THE PERFORMANCE IS CALCULATED USING THE MIXING EQUATION

DIFFUSER PERFORMANCE

FLOW ALLOWED TO MIX AT OUTLET

IDEAL PRESSURE RECOVERY COEFF. = -0.114 (INCLUDING MIXING EFFECTS)

PRESSURE RECOVERY COEFF. = -0.264

DIFFUSER EFFECTIVENESS = 3.191

FRACTIONAL TOTAL PRESSURE LOSS = 0.015 (BASED ON MEAN CONDITIONS AT COMPRESSOR OUTLET)

THIS SECTION HAS AN AREA RATIO LESS THAN ONE AND ACTS AS A NOZZLE AND NOT AS A DIFFUSER
 THE VALUE PRINTED OUT AS THE DIFFUSER EFFECTIVENESS IS NOT AN INDICATION OF HOW WELL THE SECTION PERFORMS
 MISMATCH AT THE SNOUT IS CHARACTERISED BY THE RATIO -
 (TOTAL STREAMTUBE AREA JUST BEFORE THE SNOUT)/(FLOW AREA JUST INSIDE THE SNOUT). THIS RATIO IS 1.496
 AS THIS RATIO IS OUTSIDE THE RANGE 0.85-1.15 THE FLOW SPLIT ON THE SNOUT IS NOT WELL MATCHED

AERODYNAMIC PARAMETERS AT EACH CALCULATION POINT

AXIAL POSITION FROM COMPRESSOR IN	TOTAL TEMPERATURE	TOTAL PRESSURE PSIA		STATIC PRESSURE PSIA		BLK VELOCITY FT PER SEC		MACH NUMBER		ACCUMULATED PRESSURE LOSS IN ANNULE PSI	
		ANNULE	FLANG	ANNULE	FLANG	ANNULE	FLAPE	ANNULE	FLAPE	OLE TO	OUT TC

DISCHARGE INCHES	FLAPE TUBE DEC F STATIC TEMP IN ANNULUS DEC F INNER CUTER	INNER	OUTER	TUBE	INNER	OUTER	TUBE	INNER	OUTER	TUBE	INNER	OUTER	TUBE	INNER	OUTER	FRICITION HEAT	ACCITION INNER CUTER	EXPANSION INNER CUTER
9.000	3758.7 1133.6 1137.1	89.36	88.66	85.56	86.23	86.21	85.49	443.1	392.8	111.7	0.227	C.201	0.036	0.	0.	0.	0.	
9.500	3758.7 1133.1 1136.8	89.35	88.65	85.56	86.12	86.15	85.49	445.7	396.9	111.7	C.230	C.203	C.036	0.01	0.01	0.	0.	
10.000	3758.7 1132.6 1136.6	89.31	88.64	85.56	86.01	86.08	85.49	456.3	401.1	111.7	0.233	C.205	C.036	0.03	0.02	0.	0.	
10.500	3758.7 1132.2 1136.3	89.32	88.63	85.56	85.90	86.02	85.49	462.9	405.3	111.7	C.237	C.207	C.036	0.04	0.03	0.	0.	
11.000	3758.7 1131.7 1136.1	89.31	88.62	85.56	85.80	85.96	85.49	469.5	409.4	111.7	0.240	C.209	0.036	0.05	0.04	0.	0.	
11.625	3758.6 1131.2 1135.8	89.30	88.61	85.56	85.66	85.88	85.49	477.7	414.6	111.7	C.244	C.212	C.036	0.06	0.05	0.	0.	
13.500	4027.3 1136.8 1139.1	89.15	88.52	85.38	86.58	86.42	85.27	401.5	363.8	139.9	C.205	C.186	C.064	0.12	0.10	0.09	C.04	
15.000	3852.3 1136.8 1139.1	89.11	88.48	85.49	86.51	86.38	85.34	401.7	363.9	162.6	C.205	0.186	C.052	0.16	0.13	0.09	0.04	
15.500	3861.4 1134.5 1137.7	89.12	88.49	85.50	86.07	86.09	85.36	437.4	389.0	155.5	C.224	C.199	C.051	0.15	0.13	0.09	C.04	
16.000	3898.4 1134.5 1137.6	89.09	88.47	85.50	86.05	86.07	85.35	437.5	389.0	161.7	C.224	C.199	C.051	0.17	0.15	0.09	C.04	
16.500	3934.3 1134.5 1137.4	89.07	88.45	85.50	86.03	86.05	85.35	437.6	389.1	163.4	0.224	C.199	0.057	0.20	0.16	0.09	0.04	
17.000	3994.3 1134.5 1137.6	89.05	88.44	85.50	86.00	86.04	85.34	437.7	389.2	164.4	C.224	C.199	C.052	0.22	0.18	0.09	C.04	
19.500	3984.4 1140.2 1141.9	86.85	88.30	85.50	86.89	86.71	85.30	351.6	316.5	188.5	C.175	C.161	0.059	C.28	0.24	0.21	C.12	
21.000	3649.1 1140.2 1141.9	88.87	88.26	85.61	86.85	86.67	85.37	351.7	316.6	195.8	C.179	C.161	C.065	0.33	0.27	0.21	0.12	
21.500	3366.4 1138.4 1140.8	88.83	88.27	85.72	86.48	86.45	85.45	384.2	338.4	203.9	0.156	C.173	C.069	C.32	0.27	0.21	C.12	
22.000	3343.1 1138.4 1140.8	88.81	88.25	85.73	86.46	86.43	85.46	384.3	338.5	206.4	C.196	0.173	C.069	0.34	0.29	0.21	0.12	
22.500	3335.3 1138.4 1140.8	88.79	88.23	85.74	86.44	86.42	85.46	384.4	338.4	204.7	C.156	C.173	C.070	0.36	0.30	0.21	0.12	
23.000	3333.9 1138.4 1140.8	88.77	88.21	85.74	86.42	86.40	85.46	384.5	338.7	204.8	0.196	0.173	C.070	0.38	0.32	0.21	0.12	
27.000	2662.1 1150.3 1149.7	87.20	87.24	85.91	87.12	87.11	85.32	71.3	92.7	277.8	0.036	C.047	C.107	0.39	0.33	1.78	1.09	
27.500	2387.3 1150.5 1150.0	87.17	87.22	86.13	87.19	87.16	85.44	35.2	61.0	275.4	0.018	0.031	C.110	0.41	0.35	1.79	1.09	
28.000	2367.0 1150.5 1150.0	87.17	87.22	86.15	87.15	87.16	85.45	35.2	61.0	280.7	C.018	C.031	C.111	0.41	0.36	1.79	1.09	
28.500	2364.2 1150.6 1150.0	87.17	87.22	86.15	87.15	87.16	85.45	35.2	61.0	280.9	0.018	C.031	C.111	0.41	0.36	1.78	1.09	
29.000	2362.9 1150.6 1150.0	87.17	87.21	86.15	87.15	87.16	85.45	35.2	61.0	281.0	C.018	C.031	C.111	0.42	0.36	1.78	1.09	
32.700	2321.6 1150.6 1150.3	87.16	87.21	86.22	87.15	87.20	85.00	35.2	17.5	368.9	C.018	C.009	C.147	0.42	0.36	1.78	1.09	
32.800	2311.1 1150.7 1173.9	87.15	86.22	87.15	87.21	85.00	8.9	1.2	368.8	C.065	0.001	0.147	0.43	0.37	1.78	1.09		

COMBUSTOR TOTAL-PRESSURE LOSS COEFFICIENT FOR INNER ANNULUS = 5.1507 (RELATIVE TO REFERENCE DYNAMIC PRESSURE)
 COMBUSTOR TOTAL-PRESSURE LOSS COEFFICIENT FOR OUTER ANNULUS = 7.1072
 TOTAL-PRESSURE LOSS FACTOR FOR COMPLETE DIFFUSER AND COMBUSTOR = 0.0420 (RELATIVE TO COMPRESSOR DELIVERY PRESSURE)
 COMBUSTOR TOTAL-PRESSURE LOSS FACTOR FOR INNER ANNULUS = 0.0349
 COMBUSTOR TOTAL-PRESSURE LOSS FACTOR FOR OUTER ANNULUS = 0.0271
 EXPANSION TOTAL-PRESSURE LOSS FACTOR FOR INNER ANNULUS = 0.0190
 EXPANSION TOTAL-PRESSURE LOSS FACTOR FOR OUTER ANNULUS = 0.0121
 PRESSURE-LOSS FACTOR DUE TO FRICTION AND HEAT ADDITION FOR INNER ANNULUS = 0.0041
 PRESSURE-LOSS FACTOR DUE TO FRICTION AND HEAT ADDITION FOR OUTER ANNULUS = 0.0041

MISCELLANEOUS QUANTITIES

AXIAL POSITION FROM COMPRESSOR DISCHARGE INCHES	RATE OF BURNING OF FUEL LBM PER SFC PER FT AXIAL DISTANCE	FRICTION FACTOR IN ANNULI	
		INNER	OUTER
9.000	3.456	0.00466	0.00472
9.500	3.456	0.00466	0.00472
10.000	3.456	0.00466	0.00472
10.500	3.456	0.00466	0.00472
11.000	3.456	0.00466	0.00472
11.475	1.797	0.00470	0.00476
12.500	1.382	0.00479	0.00485
13.000	0.691	0.00479	0.00485
13.500	0.691	0.00485	0.00492
14.000	0.691	0.00485	0.00492
14.500	0.691	0.00485	0.00492
15.000	0.691	0.00491	0.00492
15.500	0.	0.00491	0.00505
16.000	0.	0.00491	0.00505
16.500	0.	0.00500	0.00517
17.000	0.	0.00500	0.00517
17.500	0.	0.00500	0.00517
18.000	0.	0.00500	0.00517
18.500	0.	0.00500	0.00517
19.000	0.	0.00500	0.00517
19.500	0.	0.00500	0.00517
20.000	0.	0.00500	0.00517
20.500	0.	0.00500	0.00517
21.000	0.	0.00500	0.00517
21.500	0.	0.00500	0.00517
22.000	0.	0.00500	0.00517
22.500	0.	0.00500	0.00517
23.000	0.	0.00500	0.00517
23.500	0.	0.00500	0.00517
24.000	0.	0.00500	0.00517
24.500	0.	0.00500	0.00517
25.000	0.	0.00500	0.00517
25.500	0.	0.00500	0.00517
26.000	0.	0.00500	0.00517
26.500	0.	0.00500	0.00517
27.000	0.	0.00500	0.00517
27.500	0.	0.00500	0.00517
28.000	0.	0.00500	0.00517
28.500	0.	0.00500	0.00517
29.000	0.	0.00500	0.00517
29.500	0.	0.00500	0.00517
30.000	0.	0.00500	0.00517
30.500	0.	0.00500	0.00517
31.000	0.	0.00500	0.00517
31.500	0.	0.00500	0.00517
32.000	0.	0.00500	0.00517

QUANTITIES RELATED TO FLOW THROUGH HOLES

HOLE ROW NUMBER	AXIAL POSITION FROM COMPRESSOR DISCHARGE INCHES	HOLE TYPE	INNER CUTER WALL	NUMBER IN THIS HOLE ROW	HOLE PRESSURE LOSS FACTOR	DISCHARGE COEFFICIENTS			EFFECTIVE HOLE AREA SQ FT	INITIAL JET ANGLE DEGREES	INITIAL JET VELOCITY FT PER SEC	FRACTION OF CURRENT ANNULLS AIR FLOW THROUGH HOLES	ACCUMULATED FRACTION OF INLET AIR IN FLAME TUBE
						CORRECTED	RATIO OF ACTUAL TO CORRECTED	ACTUAL					
1	9.000	44	1	1	1.25	0.921	1.002	0.923	0.575	-0.	486.22	0.093	0.102
2	9.000	44	2	1	1.25	0.932	1.002	0.934	0.581	-0.	439.73	0.107	0.154
3	12.000	75	1	50	1.11	0.534	1.000	0.534	0.092	90.00	487.19	0.154	0.714
4	12.000	75	2	50	1.11	0.535	1.001	0.536	0.082	90.00	436.09	0.117	0.268
5	13.500	0	-0	-0	0.	0.	-0.	-0.000	0.	-0.	0.	-0.000	0.268
6	15.000	44	1	1	1.53	0.836	1.004	0.835	0.521	0.	477.75	0.111	0.305
7	15.000	44	2	1	1.53	0.836	1.003	0.839	0.521	0.	459.90	0.119	0.152
8	16.500	0	-0	-0	0.	0.	-0.	-0.000	0.	-0.	0.	-0.000	0.353
9	18.000	27	1	40	1.29	0.136	1.011	0.138	0.077	28.27	442.75	0.171	0.405
10	18.000	27	2	40	1.29	0.172	1.009	0.174	0.057	32.18	441.72	0.183	0.473
11	19.500	0	-0	-0	0.	0.	-0.	-0.000	0.	-0.	0.	-0.000	0.473
12	21.000	44	1	1	1.87	0.836	1.005	0.840	0.521	0.	457.67	0.149	0.505
13	21.000	44	2	1	1.87	0.836	1.004	0.840	0.520	0.	465.00	0.158	0.555
14	22.500	0	-0	-0	0.	0.	-0.	-0.000	0.	-0.	0.	-0.000	0.555
15	24.000	27	1	75	1.52	0.275	1.010	0.277	0.277	37.48	456.43	0.914	0.719
16	24.000	27	2	75	1.52	0.265	1.008	0.268	0.279	41.36	417.28	0.726	0.496
17	27.000	44	1	1	13.14	0.812	1.005	0.816	0.505	-0.	322.33	0.643	0.920
18	27.000	44	2	1	13.14	0.814	1.005	0.818	0.506	0.	361.23	0.519	0.954
19	32.700	0	-0	-0	0.	0.	-0.	-0.000	0.	-0.	0.	-0.000	0.954

SECONDARY HOLE FLOW SPLIT

FRACTION OF SECONDARY HOLE AIR RECIRCULATING UPSTREAM FOR INNER WALL = .8071
 FRACTION OF SECONDARY HOLE AIR RECIRCULATING UPSTREAM FOR OUTER WALL = .8075

AIR MASS FLOW SPLIT

FRACTION OF INLET AIR PASSING THROUGH SNOUT AND/OR DOME = 0.06231
 FRACTION OF INLET AIR PASSING INTO INNER ANNULUS = 0.42994
 FRACTION OF INLET AIR PASSING INTO OUTER ANNULUS = 0.50775

DIMENSIONLESS GROUPS ASSOCIATED WITH HEAT TRANSFER

AXIAL POSITION FROM COMPRESSOR DISCHARGE INCHES	REYNOLDS NUMBER				PRANDTL NUMBER			NUSSELT NUMBER		
	ANNUL I		FLAME TUBE		ANNUL I		FLAME TUBE	ANNUL I		FLAME TUBE
	INNER	OUTER	INNER	OUTER	INNER	OUTER	INNER	OUTER	INNER	OUTER
0.000	0.413E 06	0.365E 06	0.206E 06	0.206E 06	0.691	0.691	0.689	617.11	558.45	353.82
0.500	0.418E 06	0.363E 06	0.206E 06	0.206E 06	0.691	0.691	0.689	619.73	557.02	353.82
10.000	0.415E 06	0.361E 06	0.206E 06	0.206E 06	0.691	0.691	0.689	619.41	557.06	353.82
10.500	0.425E 06	0.364E 06	0.206E 06	0.206E 06	0.691	0.691	0.689	619.85	557.10	353.82
11.000	0.410E 06	0.364E 06	0.206E 06	0.206E 06	0.691	0.691	0.689	619.57	557.14	353.82
11.625	0.377E 06	0.327E 06	0.206E 06	0.206E 06	0.691	0.691	0.689	573.54	511.30	353.82
13.500	0.318E 06	0.287E 06	0.118E 06	0.118E 06	0.691	0.691	0.685	501.08	461.56	226.20
15.000	0.318E 06	0.287E 06	0.122E 06	0.122E 06	0.691	0.691	0.688	501.08	461.56	231.60
15.500	0.285E 06	0.252E 06	0.160E 06	0.160E 06	0.691	0.691	0.684	458.11	416.11	287.92
16.000	0.285E 06	0.252E 06	0.159E 06	0.159E 06	0.691	0.691	0.687	458.11	416.11	286.48
16.500	0.285E 06	0.252E 06	0.158E 06	0.158E 06	0.691	0.691	0.686	458.11	416.11	285.10
17.00	0.284E 06	0.252E 06	0.146E 06	0.146E 06	0.691	0.691	0.685	458.11	416.11	282.81
18.5	0.230E 06	0.204E 06	0.280E 06	0.280E 06	0.691	0.691	0.685	385.88	353.64	398.90
21.000	0.193E 06	0.170E 06	0.280E 06	0.280E 06	0.691	0.691	0.691	385.88	353.64	375.29
21.500	0.197E 06	0.173E 06	0.280E 06	0.280E 06	0.691	0.691	0.694	340.71	307.22	443.28
22.000	0.197E 06	0.173E 06	0.280E 06	0.280E 06	0.691	0.691	0.694	340.75	307.22	444.77
22.500	0.197E 06	0.173E 06	0.280E 06	0.280E 06	0.691	0.691	0.694	340.79	307.22	445.77
23.000	0.197E 06	0.173E 06	0.280E 06	0.280E 06	0.691	0.691	0.694	340.75	307.22	445.36
27.000	0.169E 05	0.147E 05	0.560E 06	0.560E 06	0.691	0.691	0.699	88.76	108.92	724.19
27.500	0.130E 05	0.110E 05	0.560E 06	0.560E 06	0.691	0.691	0.700	38.89	60.45	797.51
28.000	0.130E 05	0.110E 05	0.560E 06	0.560E 06	0.691	0.691	0.700	38.89	60.45	800.29
28.500	0.130E 05	0.110E 05	0.560E 06	0.560E 06	0.691	0.691	0.700	38.89	60.45	800.67
29.000	0.130E 05	0.110E 05	0.560E 06	0.560E 06	0.691	0.691	0.700	38.89	60.45	800.45
33.700	0.130E 05	0.110E 05	0.560E 06	0.560E 06	0.691	0.691	0.700	38.89	61.69	826.56
38.000	0.129E 04	0.110E 04	0.560E 06	0.560E 06	0.691	0.692	0.700	12.92	7.01	828.06

HEAT TRANSFER RATES

AXIAL POSITION FROM COMPRESSOR DISCHARGE INCHES	HEAT TRANSFER RATE FROM FLAME TO WALL BTU PER SQ FT SEC				HEAT TRANSFER RATE FROM WALL TO ANNUL I BTU PER SQ FT SEC				RADIATION INTERCHANGE FROM OPPOSITE WALL BTU PER SQ FT SEC		HEAT TRANSFERRED TO TRANSPARATION AIR IN THE WALL BTU PER SEC PER SQ FT WALL SURFACE	
	RADIATION		CONVECTION		RADIATION		CONVECTION		INNER	OUTER	INNER	OUTER
	INNER	OUTER	INNER	OUTER	INNER	OUTER	INNER	OUTER	INNER	OUTER	INNER	OUTER
0.000	36.086	35.461	19.200	18.476	15.264	16.493	40.306	37.551	0.	0.	0.	0.
0.500	42.241	41.779	-1.766	-2.314	7.922	8.681	32.777	31.031	0.	0.	0.	0.
10.000	41.962	41.478	-0.213	-0.767	8.285	9.082	33.653	31.822	0.	0.	0.	0.
10.500	41.697	41.198	1.248	0.724	8.632	9.475	34.547	32.702	0.	0.	0.	0.
11.000	41.291	40.711	3.689	3.152	9.229	10.131	35.960	34.015	0.	0.	0.	0.
11.625	40.414	39.913	5.314	4.750	10.379	11.401	35.832	33.419	0.	0.	0.	0.
13.500	49.317	48.920	5.637	5.340	15.937	17.016	39.940	37.475	0.	0.	0.	0.
15.000	42.545	42.170	6.551	6.274	13.465	14.426	35.912	34.305	0.	0.	0.	0.
15.500	46.529	46.146	-2.644	-3.039	10.155	11.020	34.048	32.347	0.	0.	0.	0.

16.000	47.727	47.302	-1.409	-1.419	10.974	11.927	15.604	33.831	C.	0.	0.	0.
16.500	49.011	48.564	-0.755	-1.170	11.669	12.675	16.861	35.006	0.	0.	0.	0.
17.000	51.031	50.525	1.143	0.750	13.120	14.250	19.350	37.334	0.	0.	0.	0.
17.500	47.872	47.473	6.829	6.420	17.013	18.195	38.077	36.072	0.	0.	0.	0.
21.000	35.657	35.414	8.043	7.684	17.217	13.118	31.746	30.245	C.	0.	0.	0.
21.500	30.259	30.152	-1.958	-2.402	5.770	6.313	22.709	21.632	0.	0.	0.	0.
22.000	29.322	29.207	-0.507	-0.943	5.915	6.474	23.078	21.584	C.	0.	0.	0.
22.500	28.958	28.836	0.267	-0.166	6.033	6.604	23.373	22.263	0.	0.	0.	0.
23.000	28.667	28.545	1.545	1.109	6.124	6.922	24.089	22.935	C.	0.	0.	0.
27.000	10.035	10.564	4.316	4.073	7.586	7.240	6.914	8.290	0.	0.	0.	0.
27.500	8.494	8.981	-4.041	-4.050	2.571	2.259	1.968	2.770	0.	0.	0.	0.
28.000	7.942	8.428	-2.944	-2.858	2.920	2.593	2.168	3.083	C.	0.	0.	0.
28.500	7.749	8.218	-2.390	-2.253	3.154	2.815	2.297	3.282	C.	0.	0.	0.
29.000	7.623	8.115	-2.013	-1.841	3.318	2.971	2.385	3.418	0.	0.	0.	0.
32.700	6.074	6.371	0.834	-0.706	4.710	4.429	2.830	1.330	0.	0.	0.	0.
32.800	5.636	6.027	0.069	-1.158	4.775	4.812	1.027	0.155	C.	0.	0.	0.

HEAT TRANSFER PARAMETERS

AXIAL POSITION FROM COMPRESSOR DISCHARGE INCHES	EMISSIVITY OF FLAME	FLAME INTENSITY BTU PER SQ FT SEC	FILM-COOLING EFFECTIVENESS		WALL TEMPERATURES DEG F			
			INNER WALL	OUTER WALL	ADIABATIC		ACTUAL	
					INNER	OUTER	INNER	OUTER
9.000	0.379	57.506	0.	0.	3761.6	3765.2	2226.6	2272.7
9.500	0.390	59.186	0.789	0.788	1733.6	1725.0	1885.6	1828.2
10.000	0.390	59.186	0.729	0.728	1887.9	1883.7	1906.3	1949.8
10.500	0.390	59.186	0.672	0.671	2033.0	2032.7	1925.5	1970.4
11.000	0.390	59.186	0.578	0.577	2275.1	2275.0	1957.5	2003.6
11.625	0.390	59.186	0.501	0.500	2473.4	2473.5	2015.9	2064.5
13.500	0.381	74.144	0.377	0.376	2961.5	2963.5	2252.0	2291.4
15.000	0.387	64.064	0.323	0.323	2996.3	2999.8	2154.8	2193.9
15.500	0.397	66.122	0.801	0.802	1712.8	1711.0	2004.8	2046.7
16.000	0.396	68.443	0.741	0.740	1829.7	1808.5	2044.6	2088.4
16.500	0.395	70.547	0.706	0.706	1994.1	1992.3	2076.7	2121.4
17.000	0.393	74.167	0.616	0.615	2264.7	2268.4	2140.4	2186.9
17.500	0.393	73.509	0.397	0.396	2878.7	2884.7	2271.3	2337.5
21.000	0.403	55.067	0.339	0.338	2820.6	2827.7	2101.1	2140.3
21.500	0.423	43.391	0.816	0.816	1580.2	1578.0	1750.4	1786.9
22.000	0.424	42.424	0.752	0.752	1716.1	1715.1	1780.4	1797.4
22.500	0.424	42.101	0.716	0.716	1751.6	1791.2	1768.3	1805.7
23.000	0.424	42.042	0.656	0.656	1922.5	1922.6	1787.6	1825.8
27.000	0.446	20.217	0.355	0.355	2145.3	2157.2	1866.1	1945.3
27.500	0.464	14.532	0.951	0.978	1213.2	1180.3	1486.8	1454.5
28.000	0.464	14.137	0.863	0.886	1321.1	1294.5	1521.0	1489.0
28.500	0.465	14.078	0.814	0.836	1380.6	1357.9	1543.0	1510.9
29.000	0.465	14.051	0.781	0.801	1421.2	1400.8	1558.0	1525.9
32.700	0.429	12.153	0.561	0.628	1679.0	1613.8	1634.2	1651.7
32.800	0.429	11.974	0.554	0.620	1682.3	1615.2	1678.6	1681.4

APPENDIX IV

PROGRAM LISTING

SIBFTC	CLAR	LIST	
C			CLAR0010
C		PROGRAM FOR THE ANALYSIS OF AN	CLAR0020
C		ANNULAR COMBUSTOR	CLAR0030
C			CLAR0040
C		PROGRAM CLARE. THIS IS THE MAIN PROGRAM. IT READS IN DATA, WORKS OUT	CLAR0050
C		REFERENCE QUANTITIES, AND DIRECTS CONTROL THROUGH THE SUBROUTINES	CLAR0060
C		IN THE APPROPRIATE SEQUENCE.	CLAR0070
C			CLAR0080
C		THIS PROGRAM CONTAINS THE FOLLOWING COMMON BLOCKS	CLAR0090
C		B3, B12, B13, B126, B168, B178, B12678	CLAR0100
		COMMON/B3/M, NCASE, INPUT, ITAPE, FGIZ(45)	CLAR0110
		COMMON/B12/ X(120), CA(120), CB(120), SA(50), SB(50),	CLAR0120
		1 NRECT, NXDIF, NDIFF, NSNOUT, NXDIF1, NXDIF2, NXDIFA, NXDIFB, NTUBE,	CLAR0130
		2 PRESIN, BLOCK(50), ABLOCK, SHAPEH(2, 50),	CLAR0140
		3 VPDATA(15), RDATA(15), NUPR, ARDTA(200), XLNDDTA(20), EFDTA(200), NCOF,	CLAR0150
		4 NYDF, NZDF, E1DTA, NXDF, AREF, WIDTH1,	CLAR0160
		5 XMACH, RHOREF, EFD(3)	CLAR0170
		COMMON/B13/ AREA1, NXDIFC, NYDIFB, NZDIFB, NCDIFB, E1DTAB	CLAR0180
		1, XLNDDTB(20), EFDTAB(200), ARDTAB(200) ,	CLAR0190
		1 NWALL1, NWALL2	CLAR0200
		COMMON/B16/CDS(20, 15), DPHS(20, 15), FLCV, IH, NABX(45)	CLAR0210
		1, NSP(20), GXIS(20, 15), K4, K6, FIT, FIPHI, FIPSI, FIA, FITAU, FID, FIENH	CLAR0220
		2, SHAFST, FIFTPR, LCMFL, LCMFL	CLAR0230
		3, LCMFL, LCFTL, LCFTL, LCPRTL, BETA, ASW, FFIZ(45), AHDOME, NSCOOP(20)	CLAR0240
		4, LCPTAL, PAFRZ, NHTU(50)	CLAR0250
		5, AF23A(3), AF23B(3), XAF23A(3), XAF23B(3)	CLAR0260
		COMMON/B126/AF2, TAN1A, TAN1B, PAN1A, PAN1B, AFA, AFB, PREDM, STAGT	CLAR0270
		1, IBL, STPREF, PNRTA, PNRTB, DPHSNT, DOMLOS	CLAR0280
		COMMON/B168/AANA(45), AANB(45), CCA(45), CCB(45), FHCR, NLAST	CLAR0290
		1, KANHET, LANHET, PERCO, THIKFT	CLAR0300
		2, DANA(45), DANB(45)	CLAR0310
		COMMON/B178/DFT(45)	CLAR0320
		COMMON/B12678/JTAPE, IPRINT	CLAR0330
			CLAR0340
			CLAR0350
C		FORMAT STATEMENTS	CLAR0360
			CLAR0370
		1 FORMAT(2X7E10.3)	CLAR0380
			CLAR0390
		M=1	CLAR0400
		CALL INPUT1	CLAR0410
		CALL INPUT2	CLAR0420
		ICHNGE=0	CLAR0430
		IDFLOW=1	CLAR0440
		NDIFF=NDIFF-100	CLAR0450
		IF(NDIFF.GE.0) GO TO 200	CLAR0460
		IDFLOW=0	CLAR0470
		NDIFF=NDIFF+100	CLAR0480
		200 IPRINU=IPRINT	CLAR0490
		CALL DIFLOW	CLAR0500
		IPRINT=IPRINU	CLAR0510
		IF(IBL.EQ.0) GO TO 500	CLAR0520
C		EMPIRICAL DATA REQUIRED TO CALCULATE DIFFUSER PERFORMANCE STATIONS 2-4	CLAR0530
		IF(MOD(NDIFF,10).NE.2.OR.NWALL1.EQ.NWALL2)GOTO105	CLAR0540
		I=NXDIFC	CLAR0550
		IF(NXDF.GE.I) I=NXDF	CLAR0560
		DUM=NXDF	CLAR0570
		NXDF=NXDIFC	CLAR0580
		NXDIFC=DUM	CLAR0590


```

DO 106 J=1,I
DUM=ARCTA(J)
ARDTA(J)=ARDTAB(J)
106 ARDTAB(J)=DUM
I=NYDIFB
IF(NYDF.GE.1) I=NYDF
DUM=NYCF
NYDF=NYDIFB
NYDIFB=DUM
DO 107 J=1,I
DUM=EFDTA(J)
EFDTA(J)=EFDTAB(J)
107 EFDTAB(J)=DUM
I=NZDIFB
IF(NZDF.GE.1) I=NZDF
DUM=NZCF
NZDF=NZDIFB
NZDIFB=DUM
DO 108 J=1,I
DUM=XLNDA(J)
XLNDA(J)=XLNDB(J)
108 XLNDB(J)=DUM
DUM=NCDF
NCDF=NCDIFB
NCDIFB=DUM
ICHNGE=1
105 KANHET=0
LCMFL=0
CALL AIR1
FITAU=.05
IF(IBL.EQ.0) GO TO 500
IF(LANHET.EQ.2) GO TO 400
CALLHEAT1

LANHET = 1 IF HEAT TRANSFER TO ANNULUS AIR IS TO BE CONSIDERED

IF(LANHET.NE.1)GOTO112
CALLAIRFLO
IF(IBL.EQ.0) GO TO 500
CALLHEAT1
112 CALLHEAT2
400 IF(IDFLOW.EQ.1) CALL DIFLW2
500 IF(M.EC.NCASE) STOP
M=M+1
IF(ICHNGE.EQ.0) GO TO 600
I=NXDIFC
IF(NXDF.GE.1) I=NXDF
DUM=NXDF
NXDF=NXDIFC
NXDIFC=DUM
DO 606 J=1,I
DUM=ARCTA(J)
AROTA(J)=AROTAB(J)
606 AROTAB(J)=DUM
I=NYDIFB
IF(NYDF.GE.1) I=NYDF
DUM=NYCF
NYDF=NYDIFB
NYDIFB=DUM
DO 607 J=1,I
DUM=EFDTA(J)

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CLAR0600
CLAR0610
CLAR0620
CLAR0630
CLAR0640
CLAR0650
CLAR0660
CLAR0670
CLAR0680
CLAR0690
CLAR0700
CLAR0710
CLAR0720
CLAR0730
CLAR0740
CLAR0750
CLAR0760
CLAR0770
CLAR0780
CLAR0790
CLAR0800
CLAR0810
CLAR0820
CLAR0830
CLAR0840
CLAR0850
CLAR0860
CLAR0870
CLAR0880
CLAR0890
CLAR0900
CLAR0910
CLAR0920
CLAR0930
CLAR0940
CLAR0950
CLAR0960
CLAR0970
CLAR0980
CLAR0990
CLAR1000
CLAR1010
CLAR1020
CLAR1030
CLAR1040
CLAR1050
CLAR1060
CLAR1070
CLAR1080
CLAR1090
CLAR1100
CLAR1110
CLAR1120
CLAR1130
CLAR1140
CLAR1150
CLAR1160
CLAR1170
CLAR1180
CLAR1190
CLAR1200

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114

```
EFDTA(J)=EFDTAB(J)
607 EFDTAB(J)=DUM
I=NZDIFB
IF(NZDF.GE.I) I=NZDF
DUM=NZCF
NZDF=NZDIFB
NZDIFB=DUM
DD 608 J=1,I
DUM=XLNDA(J)
XLNDA(J)=XLNDB(J)
608 XLNDB(J)=DUM
DUM=NCDF
NCDF=NCDIFB
NCDIFB=DUM
ICHNGE=0
600 CONTINUE
CALL INPUT2
GO TO 200
END
```

```
CLAR1210
CLAR1220
CLAR1230
CLAR1240
CLAR1250
CLAR1260
CLAR1270
CLAR1280
CLAR1290
CLAR1300
CLAR1310
CLAR1320
CLAR1330
CLAR1340
CLAR1350
CLAR1360
CLAR1370
CLAR1380
CLAR1390
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```

SIBFTC BKDA LIST
BLOCK DATA
C SUBROUTINE BLOCK DATA
C
C THIS SUBROUTINE FILLS IN RECOMMENDED STARTING VALUES FOR A
C NUMBER OF VARIABLES. SOME OF THESE MAY BE OVER-WRITTEN,
C IF DESIRED, VIA NAMELIST INPUTS.
C
C THIS SUBROUTINE USES COMMON BLOCKS B1,B3,B12,B16,B17,B18,B68,B167,
C B168,B1678,B12678
C COMMON STATEMENTS
COMMON/B18/ABSW,EMW,EMC,NLUM, NHT1,NHT2
1, X1FCA(45),X1FCB(45),CONDFT,TCASA(45),TCASB(45),TOLTW1,TOLTBKDA0001
2W2,XFILMZ, TABTFT(10),TABEFT(100),TABPFT(10),NEFT,NPFT,NFORMBKDA0002
3, NCOOL, NUMAX1,NUMAX2 BKDA0003
COMMON/B08/AFANA(45),AFANB(45),AFFT(45),AFPRZ,C2A(45),C2B(45) BKDA0004
2,AFSYP,FARFT(45),DENANA(45),DENANB(45) BKDA0005
3,SAFTRA(45),SAFTRB(45),QTRA(45),QTRB(45),REAN(45),REBAN(45) BKDA0006
4,TWA(45),TWB(45) BKDA0007
COMMON/B168/AANA(45),AANB(45),CCA(45),CCB(45),FHCR,NLAST BKDA0008
1,KANHET,LANHET,PERCO,THIKFT BKDA0009
2,DANA(45),DANB(45) BKDA0010
COMMON/B12678/JTAPE,IPRINT BKDA0011
COMMON/B1/KTAPE, XINT,PI4,NWH,NG,FFB(50),FTA(120) BKDA0012
1,FTB(120),NBLADE,NUMSW, DSWLOU,DSWLIN, BKDA0013
1TCATA(50),TCATB(50),HAB(50) BKDA0014
COMMON/B67/DENFT(45),EK17,EK19,EK20, EK16 BKDA0015
1, C(50),GXIA(50),K,WUJ(50) BKDA0016
COMMON/B2/ RAD(16),DELTA(2,50),EE1(2),UJ(15),THA,THB,THS,PRES(50), BKDA0017
1NGO,NWAY,ZZR,ZZGAMA,BETA1,BETA2,XMVA,XMVB,XMVS, ZZCP,IDIF BKDA0018
1,HSEP,FLAREA(50),AREA(50) BKDA0019
COMMON/B13/ AREA1,NXDIFC,NXDIFB,NZDIFB,NCDIFB,E1DTAB BKDA0020
1,XLNDTB(20),EFDTAB(200),ARDTAB(200), BKDA0021
1NWALL1,NWALL2 BKDA0022
COMMON/B3/M,NCASE,INPUT,ITAPE,FGIZ(45) BKDA0023
COMMON/B12/ X(120),CA(120),CB(120),SA(50),SB(50), BKDA0024
1NRECT,NXDIF,NDIFF,NSNOUT,NXDIF1,NXDIF2,NXDIFA,NXDIFB,NTUBE, BKDA0025
2PRESIN, BLOCK(50),ABLOCK,SHAPEH(2,50), BKDA0026
3VPDATA(15),RDATA(15),NUPR,ARDTA(200),XLNDTA(20),EFDTA(200),NCDF, BKDA0027
4NYDF,NZDF,E1DTA, NXDF,AREF,WIDTH1, BKDA0028
5XMACH,RHOREF,EFDT(3) BKDA0029
COMMON/B16/CDS(20,15),DPHS(20,15),FLCV,IH, NABX(45) BKDA0030
1,NSP(20),GXIS(20,15),K4,K6,FIT,FIPHI,FIPSI,FIA,FITAU,FID,FIENH BKDA0031
2,SHAFST, FIFTPR, LCMFL,LCANIL BKDA0032
3,LCANL,LCFTEL,LCFTL,LCPRTL,BETA,ASW,FFIZ(45),AHDOME,NSCOOP(20) BKDA0033
4,LCPTAL,PAFRZ,NHTU(50) BKDA0034
5,AF23A(3),AF23B(3),XAF23A(3),XAF23B(3) BKDA0035
COMMON/B17/ XHU(50),DXHU(50),EFC(2), NEF,STEP,JKSN(50),NSH BKDA0036
COMMON/B167/GASC,GRAVC,GJoule,IHJ(50),XH(50),NH BKDA0037
COMMON/B1678/NSHCP,XCP(45),AFT(45),PI BKDA0038
1,NKH(50),KJSN(45,6),HAU(50),CFTA(45),CFTB(45),NAB(50),NCODEA(45) BKDA0039
2,NCODEB(45),TZ BKDA0040
COMMON/B126/AF2,TAN1A,TAN1B,PAN1A,PAN1B, AFA,AFB,PREDM,STAGTBKDA0041
1,IBL,STPREF,PNRTA,PNRTB,DPHSNT,DOMLOS BKDA0042
C DATA STATEMENTS BKDA0043
DATA ITAPE,JTAPE,KTAPE,PI,PI4,GASC,GRAVC,GJoule,TZ/5,8,5,3,14159, BKDA0044
10.7854,53.3,32.18,778.,459.7/ BKDA0045
DATA K4,K6,NCASE,NCOOL,NG,NH,NLUM,NRECT,NSH,NSNOUT,NWALL1,NWALL2, BKDA0046
1NWH,NXDIF,INPUT/3*0,1,3*0,1,7*0/ BKDA0047
DATA ABSW, CONDFT,EMC,EMW,FHCR,FLCV,SHAFST,STEP,THIKFT,BKDA0048
BKDA0049
BKDA0050
BKDA0051
BKDA0052
BKDA0053
BKDA0054
BKDA0055
BKDA0056
BKDA0057
BKDA0058
BKDA0059

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1 TOLTW1, TOLTW2, XFILMZ, XINT/.85,	15., .8, .85, .17, 18540., .5, .25,	BKDA0060
2.1E-6, 1., 1., 3.5, 100./		BKDA0061
DATA SHAPEH(1,1), SHAPEH(2,1)/1.4, 1.4/, (BLOCK(I), I=2,50)/49*0./		BKDA0062
DATA (TWA(I), TWB(I), I=1,45)/90*2500./		BKDA0063
DATA NUMAX1, NUMAX2, LCANIL, LCFTL, FID, FIA, FITAU, LCPTAL, LCPRTL, FIT,		BKDA0064
1 LCFTL, FIENH, LCANL, FIPSI, FIFTPR/		BKDA0065
1 20, 20, 50, 50, .01, .5, .3, 5, 25, .01,	25, 1., 100, .01, 1./	BKDA0066
1, LCMFL/0/		BKDA0067
1, FIPHI/.01/		BKDA0068
DATA KANHET/0/	, (NAB(J), J=1,50)/50*0/,	BKDA0069
1 BETA, ASW/50., 0./, AREF/0./,		BKDA0070
DATA IDIF/0/		BKDA0071
DATA ((KJSN(K, IX), IX=1,6), K=1,45)/270*0/		BKDA0072
DATA (NCODEA(K), NCODEB(K), K=1,45)/90*0/, (NHH(J), J=1,50)/50*1/		BKDA0073
1, NSHCP/0/		BKDA0074
DATA (C(K), K=1,50)/50*0./		BKDA0075
DATA (QTRA(K), QTRB(K), K=1,45)/90*0./		BKDA0076
DATA (SAFTRA(K), SAFTRB(K), K=1,45)/90*0./		BKDA0077
DATA (AF23A(I), AF23B(I), XAF23A(I), XAF23B(I), I=1,3)/12*0./		BKDA0078
DATA (HAB(J), J=1,50)/50*0./		BKDA0079
DATA EK16, WIDTH1, STAGT/0., 12., 1./		BKDA0080
DATA (EFDT(J), J=1,3)/3*1./		BKDA0081
DATA NUMSW, NBLADE, DOMLOS, PERCO/0, 8, 0., 0./		BKDA0082
DATA HSEP/1.9/		BKDA0083
DATA PAFRZ/.1/		BKDA0084
DATA AF2/1./		BKDA0085
DATA IBL/1/		BKDA0086
1, IPRINT/0/		BKDA0087
END		BKDA0088

SIBMAP	REMOV			
	ENTRY	.UN01.		REM 0001
	ENTRY	.UN02.		REM 0002
	ENTRY	.UN03.		REM 0003
	ENTRY	.UN04.		REM 0004
	ENTRY	.UN07.		REM 0005
	ENTRY	.UN09.		REM 0007
	ENTRY	.UN10.		REM 0008
	ENTRY	.UN11.		REM 0009
	ENTRY	.UN12.		REM 0010
	ENTRY	.UN13.		REM 0011
	ENTRY	.UN14.		REM 0012
	ENTRY	.UN19.		REM 0013
	ENTRY	.UN20.		REM 0014
	ENTRY	.UN21.		REM 0015
	ENTRY	.UN22.		REM 0016
	ENTRY	.UN23.		REM 0017
	ENTRY	.UN24.		REM 0018
.UN01.	PZE	0		REM 0019
.UN02.	PZE	0		REM 0020
.UN03.	PZE	0		REM 0021
.UN04.	PZE	0		REM 0022
.UN07.	PZE	0		REM 0023
.UN09.	PZE	0		REM 0025
.UN10.	PZE	0		REM 0026
.UN11.	PZE	0		REM 0027
.UN12.	PZE	0		REM 0028
.UN13.	PZE	0		REM 0029
.UN14.	PZE	0		REM 0030
.UN19.	PZE	0		REM 0031
.UN20.	PZE	0		REM 0032
.UN21.	PZE	0		REM 0033
.UN22.	PZE	0		REM 0034
.UN23.	PZE	0		REM 0035
.UN24.	PZE	0		REM 0036
	END			REM 0037

SIBFTC INP1 LIST

SUBROUTINE INPUT1

SUBROUTINE INPUT1

THIS SUBROUTINE READS AND WRITES OUT THE FIXED RUN DATA

THIS SUBROUTINE USES THE FOLLOWING COMMON BLOCKS

B1,B12,B13,B16,B17,B18,B126,B167,B168,B178,B1678,B12678
ALSO B3 (SHARED WITH CLARE)

```

COMMON/B1/KTAPE, XINT,PI4,NWH,NG,FFB(50),FTA(120)
1,FTB(120),NBLADE,NUMSW, DSWLOU,DSWLIN,
1TCATA(50),TCATB(50),HAB(50)
COMMON/B3/M,NCASE,INPUT,ITAPE,FGIZ(45)
COMMON/B12/ X(120),CA(120),CB(120),SA(50),SB(50),
1NRECT,NXDIF,NDIFF,NSNOUT,NXDIF1,NXDIF2,NXDIFA,NXDIFB,NTUBE,
2PRESIN, BLOCK(50),ABLOCK,SHAPEH(2,50),
3VPDATA(15),RDATA(15),NUPR,ARDTA(200),XLNDA(20),EFDTA(200),NCDF,
4NYDF,NZDF,E1DTA,NXDF,AREF,WIDTH1,
5XMACH,RHOREF,EFD(3)
COMMON/B13/ AREAL,NXDIFC,NXDIFB,NZDIFB,NCDFB,E1DTAB
1,XLNDA(20),EFDTAB(200),ARDTAB(200),
1NWALL1,NWALL2
COMMON/B16/CDS(20,15),DPHS(20,15),FLCV,IH, NABX(45)
1,NSP(20),GXIS(20,15),K4,K6,FIT,FIPHI,FIPSI,FIA,FITAU,FID,FIENH
2,SHAFST, FIFTPR, LCMFL,LCANIL
3,LCANL,LCFTEL,LCFTL,LCPTL,BETA,ASH,FFIZ(45),AHDOME,NSCOOP(20)
4,LCPTAL,PAFRZ,NHTU(50)
5,AF23A(3),AF23B(3),XAF23A(3),XAF23B(3)
COMMON/B17/ XHU(50),DXHU(50),EFC(2), NEF,STEP,JKSN(50),NSH
COMMON/B18/ABSW,EMW,EMC,NLUM, NHT1,NHT2
1, X1FCA(45),X1FCB(45),CONDF,TCASA(45),TCASB(45),TOLTM1,TOLTM2
2W2,XFILMZ, TABTFT(10),TABEFT(100),TABPFT(10),NEFT,NPFT,NFORMIN
3,NCOOL, NUMAX1,NUMAX2
COMMON/B126/AF2,TAN1A,TAN1B,PAN1A,PAN1B, AFA,AFB,PREDM,STAGT
1,IBL,STPREF,PARTA,PNRTB,DPHSNT,DOMLOS
COMMON/B167/GASC,GRAVC,GJOLE,IHJ(50),XH(50),NH
COMMON/B168/AANA(45),AANB(45),CCA(45),CCB(45),FHCR,NLAST
1,KANHET,LANHET,PERCO,THIKFT
2,DANA(45),CAND(45)
COMMON/B178.DFT(45)
COMMON/B1678/NSHCP,XCP(45),AFT(45),PI
1,NHJ(50),KJSN(45,6),HAU(50),CFTA(45),CFTB(45),NAB(50),NCODEA(45)
2,NCODEB(45),TZ
COMMON/B12678/JTAPE,IPRINT

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DIMENSION CA(60),DC(20),XINCH(120)

NAMELIST DECLARATIONS

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NAMELIST/FIXED/NCASE,NRECT,NG,NH,NWH,NSH,NSNOUT,NWALL1,NWALL2
1,INPUT,K4,K6,NUMSW,NBLADE
1,IPRINT,NCCOL
NAMELIST/FIXEDR/XINT,THIKFT,FLCV,FHCR,SHAFST,AF23A,AF23B,XAF23A,XAF23B,ABSW,EMW,EMC,
1F23B,DOMLOS,CONDF,XFILMZ,PERCO
1,WIDTH1,EFD
2,DSWLOU,DSWLIN,BETA
NAMELIST/LIMITS/ LCANIL,STEP,NXDIF1,NXDIF2,NXDIF

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INP10001
INP10002
INP10003
INP10004
INP10005
INP10006
INP10007
INP10008
INP10009
INP10010
INP10011
INP10012
INP10013
INP10014
INP10015
INP10016
INP10017
INP10018
INP10019
INP10020
INP10021
INP10022
INP10023
INP10024
INP10025
INP10026
INP10027
INP10028
INP10029
INP10030
INP10031
INP10032
INP10033
INP10034
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INP10036
INP10037
INP10038
INP10039
INP10040
INP10041
INP10042
INP10043
INP10044
INP10045
INP10046
INP10047
INP10048
INP10049
INP10050
INP10051
INP10052
INP10053
INP10054
INP10055
INP10056
INP10057
INP10058
INP10059

C	FORMAT STATEMENTS	INP10060
		INP10061
		INP10062
	1 FORMAT(7E10.3)	INP10063
	4 FORMAT(12A6)	INP10064
	5 FORMAT(1X,12A6////////)	INP10065
	8 FORMAT(5E10.3,3I5)	INP10066
	14 FORMAT(29X13(2H*),10HINPUT DATA13(2H *)////////37H0GEOINP10067	INP10068
	2METRIC CONFIGURATION OF COMBUSTOR/1X36(1H-))	INP10069
	16 FORMAT(1H125X69HANA L Y S I S O F A R E C T A N G U L A R INP10069	INP10070
	1 C O M B U S T O R////////)	INP10071
	17 FORMAT(1H128X63HANA L Y S I S O F A N A N N U L A R C O INP10071	INP10072
	1 M B U S T O R////////)	INP10073
	18 FORMAT(8HO AXIAL9X13(2H-),15HDIAMETER INCHES13(2H -))	INP10074
	19 FORMAT(8HO AXIAL9X7(2H-),37HDIMENSION FROM ARBITRARY DATUM INCHEINP10074	INP10075
	1S7(2H -))	INP10076
	20 FORMAT(11H POSITION/7H FROM,81X9HGEOMETRIC/	INP10077
	1 13H COMPRESSOR4X5HINNER7X5HINNERINP10077	INP10078
	15X22HINNER DOME OUTER DOME4X5HOUTER7X5HOUTER, 6X5HINPUT/	INP10079
	1 12H DISCHARGE5X6HCINP10079	INP10080
	2ASING6X5HSNOUT2X2(3X9HOR FLAME),5X5HSNOUT7X6HCASING,5X,5HPOINT/	INP10081
	1 9H INCHES27INP10081	INP10082
	3X2(3X9HTUBE WALL),28X,6HNUMBER//)	INP10083
	21 FORMAT(1XF10.3,6F12.3,6X,I3)	INP10084
	25 FORMAT(39HOTHE COMBUSTOR HAS A CONSTANT WIDTH OF ,F7.3,3H IN)	INP10085
	27 FORMAT(////////19HOMISCELLANEOUS DATA/1X18(1H-)//16H HOLE ROW NUMBER INP10085	INP10086
	1I3,90H IS CONSIDERED TO MARK THE END OF THE PRIMARY ZONE (WHICH ISINP10086	INP10087
	2 TREATED AS A STIRRED REACTOR)/54H THE FIRST HOLES ON THE FLAME-TUINP10087	INP10088
	3BE WALL ARE IN ROW NO.I3/10H FUEL DATA/11X19HLOWER HEATING VALUE9XINP10088	INP10089
	41H=F10.3,12H BTU PER LBM/11X21HHYDROGEN-CARBON RATIO7X1H=F10.3/46HINP10089	INP10090
	5 FRACTION OF INLET AIRFLOW BYPASSING COMBUSTOR/11X13HINNER ANNULUSINP10090	INP10091
	616XF10.3/11X13HOUTER ANNULUS16XF10.3/36H AXIAL POSITION AT WHICH TINP10091	INP10092
	7THIS OCCURS/11X13HINNER ANNULUS16XF10.3,7H INCHES/11X13HOUTER ANNULINP10092	INP10093
	8US16XF10.3,7H INCHES/26H FLAME-TUBE WALL THICKNESS13X1H=F10.3,7H IINP10093	INP10094
	9NCHES/40H THERMAL CONDUCTIVITY OF WALL MATERIAL =F10.3,20H BTU PERINP10094	INP10095
	1 FT HR DEG F/21H ABSORPTIVITY OF WALL18X1H=F10.3/19H EMISSIVITY OFINP10095	INP10096
	2 WALL20X1H=F10.3/27H EMISSIVITY OF OUTER CASING12X1H=F10.3)	INP10097
	37 FORMAT(63H SINCE NCASE IS ZERO, NONE OF THE MAJOR SUBROUTINES ARE INP10097	INP10098
	1 ENTERED)	INP10099
	50 FORMAT(1X////////29H CASES CONSIDERED IN THIS RUN/1X, 29(1H-))	INP10100
	51 FORMAT(1X////////38H MISCELLANEOUS DATA - DIFFUSER SECTION/	INP10101
	11X,38(1H-))	INP10102
	52 FORMAT(1X////////37H MISCELLANEOUS DATA - AIRFLOW SECTION//	INP10103
	11X,37(1H-))	INP10104
	53 FORMAT(1X////////43H MISCELLANEOUS DATA - HEAT TRANSFER SECTION/	INP10105
	11X,43(1H-))	INP10106
	61 FORMAT(1X,I2,27H CASES ARE TO BE CONSIDERED)	INP10107
	62 FORMAT(1X,26HTHE GEOMETRY IS DEFINED AT,I3	INP10108
	1,23H GEOMETRIC INPUT POINTS)	INP10109
	64 FORMAT(1X,3A6,A1,26H ALTERED FROM CASE TO CASE)	INP10110
	65 FORMAT(38H THE DIFFUSER SECTION CONTAINS A SNOOT)	INP10111
	66 FORMAT(46H THE DIFFUSER SECTION DOES NOT CONTAIN A SNOOT)	INP10112
	67 FORMAT(12H INPUT POINT, I3,32H IS THE LAST STATION BEFORE THE ,A5INP10112	INP10113
	1)	INP10114
	68 FORMAT(53H DIFFUSION IS CONSIDERED TO END AT INPUT POINT NUMBER,	INP10115
	1I3,	INP10116
	18H IN THE ,A5, 8H ANNULUS)	INP10117
	69 FORMAT(19H INPUT POINT NUMBER, I3,47H MARKS THE END OF THE DIFFUSINP10117	INP10118
	1ING SECTION IN THE ,A5,8H ANNULUS)	INP10119
	70 FORMAT(31H THE EMPIRICAL DATA TO BE USED ,A6,5H THE , A5,14H IS SEINP10119	INP10120
	1T NUMBER,I3)	INP10120

71 FORMAT(16H HOLE ROW NUMBER,I3,72H IS THE FIRST HOLE ROW IN THE FLAINP10121
 1ME-TUBE WALL, AS DISTINCT FROM THE DOME) INP10122

72 FORMAT(16H HOLE ROW NUMBER,I3,93H IS CONSIDERED TO MARK THE END OFINP10123
 1 THE PRIMARY ZONE (WHICH IS CONSIDERED AS A STIRRED REACTOR)) INP10124

73 FORMAT(81H THE FRACTION OF AIR FLOWING THROUGH THE SECONDARY HOLESINP10125
 1 INTO THE PRIMARY ZONE IS, F7.3) INP10126

74 FORMAT(36H THE FLOW RESISTANCE IN THE SNOOT IS, F7.3,54H VELOCITY INP10127
 1HEADS (BASED ON CONDITIONS IN THE SNOOT LIP)) INP10128

75 FORMAT (42H FRACTION OF INLET AIR BYPASSING COMBUSTOR, INP10129
 1 1X/ 36X, 13HINNER INP10130
 1ANNULUS,F7.3/36X,13HOUTER ANNULUS,F7.3/36H AXIAL POSITION AT WHICHINP10131
 2 THIS OCCURS/35X,14H INNER ANNULUS,F7.3, 5H IN / 35X,14H OUTER ANINP10132
 3NULUS,F7.3, 5H IN /) INP10133

76 FORMAT(10H FUEL DATA/10X,20H LOWER HEATING VALUE,3X,F8.1,12H BTU PINP10134
 1ER LBM/10X,23H HYDROGEN/CARBON RATIO ,F8.3) INP10135

77 FORMAT(41H FLAME TUBE WALL THICKNESS.....,F7.3,5H IN / INP10136
 1 41H THERMAL CONDUCTIVITY OF WALL MATERIAL...,F7.2,20H BTU PER FT INP10137
 2HR DEG F/ 41H ABSORPTIVITY OF FLAMETUBE WALL.....,F7.3/ INP10138
 3 41H EMISSIVITY OF FLAMETUBE WALL.....,F7.3/ INP10139
 4 41H EMISSIVITY OF OUTER CASING.....,F7.3) INP10140

78 FORMAT(24H THE CASIN/ TEMPERATURE ,A6, 10H SPECIFIED) INP10141

79 FORMAT(14H FILM COOLING ,A6, 5H USED) INP10142

80 FORMAT(23H TRANSPIRATION COOLING ,A6, 5H USED) INP10143

81 FORMAT(51H THE PERMEABILITY COEFFICIENT OF THE POROUS WALL IS, INP10144
 1E10.3, 6H SQ FT) INP10145

87 FORMAT(74H THE FRACTION OF AIR FLOWING THROUGH THE SECONDARY HOLESINP10146
 1 THAT RECIRCULATES/51H INTO THE PRIMARY ZONE IS WORKED OUT IN THE INP10147
 2PROGRAM) INP10148

90 FORMAT(19H1*** ERROR MESSAGE/38H0X(I) WAS FOUND TO BE LESS THAN XINP10149
 1(I-1), INP10150
 1 F7.3,50H INCHES ALONG THE COMBUSTOR. THIS IS NOT ALLOWED.) INP10151

97 FORMAT(46H1IF THERE IS NO SNOOT, NXDIF MUST BE SPECIFIED) INP10152

98 FORMAT(43H1NG, NH, NWH, AND NSH MUST ALL BE SPECIFIED) INP10153

: DATA DECLARATION INP10154
 : INP10155
 : INP10156

DATA DC(I),DC(5) /19HPROGRAM ROUTING IS ,19HFLOW CONDITIONS ARE/ INP10157
 DATA (CA(I),I=7,8)/5HSNOOT,5HDOME / INP10158
 DATA (CA(I),I=9,10)/5HOUTER,5HINNER/ INP10159
 DATA (CA(I),I=11,12)/6HBEFORE,6H AFTER/ INP10160
 DATA (CA(I),I=13,15)/6H IS ,6HIS NOT,6HCAN BE/ INP10161
 DATA NTEMP/0/ INP10162

: INP10163
 : INP10164
 : INP10165
 : INP10166
 : INP10167

READ RUN IDENTIFICATION CARD

READ(ITAPE,4) (DC(I),I=9,20)

: INP10168
 : INP10169
 : INP10170

READ IN FIXED DATA, COMBUSTOR GEOMETRY, HOLE SPECIFICATIONS, LIMITS,
 AND TOLERANCES

READ(ITAPE,FIXEDI) INP10171
 IF(NG*NH*NWH*NSH .EQ.0)GOTO198 INP10172
 IF(NWALL1.EQ.0)NWALL1=NRECT INP10173
 IF(NWALL2.EQ.0)NWALL2=NRECT INP10174
 READ(ITAPE,1)(XINCH(I),CA(I),SA(I),FTA(I),FTB(I),SB(I),CB(I),I=1,NINP10175
 1G) INP10176
 READ(ITAPE,8)(XH(J),HAB(J),TCATA(J),TCATB(J),FFB(J),NAB(J),NHH(J),INP10177
 1NHTU(J),J=1,NH) INP10178
 IF(TCATA(1).NE.0.) NTEMP=1 INP10179
 READ(ITAPE,FIXEDR) INP10180
 READ(ITAPE,LIMITS) INP10181

		INP10246
		INP10247
		INP10248
		INP10249
	WRITE(JTAPE,51)	INP10250
	IF(NSNCUT.EQ.1) WRITE(JTAPE,65)	INP10251
	IF(NSNCUT.NE.1) WRITE(JTAPE,66)	INP10252
	IF(NSNCUT.EQ.1) WRITE(JTAPE,67) NXDIF,DA(7)	INP10253
	IF(NSNCUT.NE.1) WRITE(JTAPE,67) NXDIF,DA(8)	INP10254
	IF(NSNCUT.EQ.1) WRITE(JTAPE,68) NXDIF1,DA(10)	INP10255
	IF(NSNCUT.EQ.1) WRITE(JTAPE,68) NXDIF2,DA(9)	INP10256
	IF(NSNCUT.NE.1) GO TO 990	INP10257
	WRITE(JTAPE,70) DA(11),DA(7),NWALL1	INP10258
	WRITE(JTAPE,70) DA(12),DA(7),NWALL2	INP10259
	GO TO 991	INP10260
990	WRITE(JTAPE,70) DA(11),DA(8),NWALL1	INP10261
991	CONTINUE	INP10262
		INP10263
	WRITE(JTAPE,52)	INP10264
	WRITE(JTAPE,71) NWH	INP10265
	WRITE(JTAPE,72) NSH	INP10266
	IF(K4.EQ.0)WRITE(JTAPE,87)	INP10267
	IF(K4.EQ.1)WRITE(JTAPE,73)SHAFST	INP10268
	WRITE(JTAPE,74) DOMLOS	INP10269
	DO 1995 JL=1,3	INP10270
		INP10271
	IF(AF23A(JL)*AF23B(JL).GT.0.)WRITE(JTAPE,75)AF23A(JL),AF23B(JL),	INP1 272
	1XAF23A(JL),XAF23B(JL)	INP1 273
	XAF23A(JL)=XAF23A(JL)/12.	INP10274
1995	XAF23B(JL)=XAF23B(JL)/12.	INP10275
	WRITE(JTAPE,76) FLCV,FHCR	INP10276
		INP10277
	WRITE(JTAPE,53)	INP10278
	THIKFT=THIKFT*12.	INP10279
	WRITE(JTAPE,77) THIKFT,CONDFT,ABSW,EMW,EMC	INP10280
	THIKFT=THIKFT/12.	INP10281
	IF(NTEMP.EQ.1) GO TO 992	INP10282
	WRITE(JTAPE,78) DA(14)	INP10283
	GO TO 993	INP10284
992	WRITE(JTAPE,78) DA(13)	INP10285
993	IF(NCCCL.EQ.1) GO TO 1990	INP10286
	WRITE(JTAPE,79) DA(14)	INP10287
	GO TO 1991	INP10288
1990	WRITE(JTAPE,79) DA(15)	INP10289
1991	IF(NCOCL.EQ.2) GO TO 1992	INP10290
	WRITE(JTAPE,80) DA(14)	INP10291
	GO TO 1993	INP10292
1992	WRITE(JTAPE,80) DA(15)	INP10293
	WRITE(JTAPE,81) PERCO	INP10294
1993	CONTINUE	INP10295
		INP10296
	IF(IPRINT.EQ.1)	INP10297
	1WRITE(6,FIXEDI)	INP10298
	IF(IPRINT.EQ.1)	INP10299
	1WRITE(6,FIXEDR)	INP10300
	IF(IPRINT.EQ.1)	INP10301
	1WRITE(JTAPE,LIMITS)	INP10302
	WRITE(JTAPE,50)	INP10303
	WRITE(JTAPE,61) NCASE	INP10304
	IF(NCASE.EQ.0) WRITE(JTAPE,37)	INP10305
	IF(INPUT.EQ.1) WRITE(JTAPE,64) (LC(I),I=1,4)	INP10306

123

IF(INPUT.EQ.0) WRITE(JTAPE,64) (DC(I),I=5,8)

RETURN

190 WRITE(JTAPE,90)X(I)

STOP

198 WRITE(JTAPE,98)

199 STOP

END

INP10307
INP10308
INP10309
INP10310
INP10311
INP10312
INP10313
INP1 314

IBFTC INP2 LIST

SUBROUTINE INPUT2

0010 INP20020

SUBROUTINE INPUT2

INP20030

THIS SUBROUTINE READS AND WRITES OUT THE CASE DATA

INP20040

COMMON STATEMENTS

INP20050

THIS SUBROUTINE USES COMMON BLOCKS WHOSE NAMES CONTAIN THE NUMBER 1
P1,P12,B13,B16,P17,P18,B126,B167,B168,B178,B1678,B12678
ALSO B3 (SHARED WITH CLARE)

INP20060

INP20070

INP20080

INP20090

INP20100

INP20110

INP20120

INP20130

INP20140

INP20150

INP20160

INP20170

INP20180

INP20190

INP20200

INP20210

INP20220

INP20230

INP20240

INP20250

INP20260

INP20270

INP20280

INP20290

INP20300

INP20310

INP20320

INP20330

INP20340

INP20350

INP20360

INP20370

INP20380

INP20390

INP20400

INP20410

INP20420

INP20430

INP20440

INP20450

INP20460

INP20470

INP20480

INP20490

INP20500

INP20510

INP20520

INP20530

INP20540

INP20550

INP20560

INP20570

INP20580

INP20590

DIMENSION STATEMENT

DIMENSION DA(60),CB(40),DUMF(46),WORD(2),HORE(6,5),XINCH(120)

FORMAT STATEMENTS

- 1 FCRMAT(7E10.3)
- 2 FORMAT(7I10)
- 3 FCRMAT(2E10.3)

1H TABULATED EMISSIVITY DATA
2QUAL TO 4)

/30H NLUM HAS BEEN SET EY

DATA STATEMENTS

DATA (DA(1),I=7,8)/5H SNOUT,5H COME / INP21200
 DATA DA(20),DA(22) /8H UNCOOLED,8H COOLED /,DA(24),DA(25)/1H1,1H2/ INP21210
 DATA DA(26),DA(32),DA(38)/35H LONGITUDINAL WALL CONDUCTION , INP21220
 1 35H RADIATION INTERCHANGE BETWEEN WALLS,5H AND / INP21230
 DATA DA(50),DA(53),CA(56)/15H EMPIRICAL DATA,15H STREAMTUBE , INP21240
 115H MIXING EQUATION/ INP21250
 DATA DB(6),DB(1),DB(11),DB(16)/ 26H THE EQUIVALENT ENTRAINMENT, INP21260
 126H THE MASS LOSS ,26H THE PROFILE SUBSTITUTION , INP21270
 226H THE INSTANTANEOUS MIXING / INP21280
 DATA DB(21),DB(24),DB(28),DB(29)/ 18H WITH A CONSTANT OF,21H FOR PE INP21290
 1 NETRICATION JETS, 3HAND,14K FOR WALL JETS/ INP21300
 DATA (WCRD(I),I=1,2)/12H IS IS NOT/,(HORE(I,J),I=1,6),J=1,5)/18C INP21310
 1H NONLUMINOUS. REEVES DISTILLATE-FUEL NONLUMINOUS. REEVES RESIDU INP21320
 2AL-FUEL LUMINOUS. THE LEFEBVRE LUMINOUS. INP21330
 3THE NREC 1964 LUMINOUS. THE NREC 1966/ INP21340

DC 1313 I=1,NG

1313 XINCH(I)=X(I)*12.

1314 WRITE(JTAPE,34)M

IF(M.NE.1.AND.INPUT.EQ.1)GOTO110

CHANGE UNITS IF INPUT=0

IF(M.EQ.1)AF2=1.0

AFA=AFA/AF2

AFB=AFB/AF2

DC 136 JL=1,3

AF23A(JL)=AF23A(JL)/AF2

136 AF23B(JL)=AF23B(JL)/AF2

IF(TCASA(1).EQ.STAGT) TCASA(1)=0.

** THERE ARE NO CARDS INP21560, 1570, AND 1580 **

1354 CONTINUE

READ NEW CASE DATA TO CHANGE FLOW VARIABLES

DUM1=SHAPEH(1,1)

DUM2=SHAPEH(2,1)

READ(ITAPE,1)STAGT,STPREF,AF2,FAR,ABLOCK,SHAPEH(1,1),SHAPEH(2,1),

1(BLOCK(I),I=1,NXDIF)

READ(ITAPE,1)DAFA,CAFB,AFCL,AFCU,AFSL,AFSU

IF(DAFA.GT.0.)AFA=CAFA

IF(CAFB.GT.0.)AFB=CAFB

IF(AFCL.LE.0.)AFCL=0.1

IF(AFCU.LE.0.)AFCU=0.9

IF(AFSU.LE.0.)AFSU=AF2

IF(AFSL.LE.0.)AFSL=0.0

IF(SHAPEH(1,1).EQ.0.) SHAPEH(1,1)=DUM1

IF(SHAPEH(2,1).EQ.0.) SHAPEH(2,1)=DUM2

READ(ITAPE,2)NTUBE,NUPR

READ(ITAPE,3)(VPDATA(15),RDATA(15),15=1,NUPR)

AFA=AFA*AF2

AFB=AFB*AF2

FFPRZ=FAR*AF2

DC 132 JL=1,3

AF23A(JL)=AF23A(JL)*AF2

INP21210
 INP21220
 INP21230
 INP21240
 INP21250
 INP21260
 INP21270
 INP21280
 INP21290
 INP21300
 INP21310
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 INP21770
 INP21780
 INP21790
 INP21800
 INP21810
 INP21820


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WRITE(JTAPE,86) INP22370
NLUM=4 INP22380
1104 CCNTINUE INP2239C
IF(NLUM.NE.6)WRITE(JTAPE,33)(WORE(IB,NLUM),IB=1,6) INP22400
IF(LAMHT.EC.4)GO TO 1107 INP22410
IF(NHT1.EC.1)WRITE(JTAPE,40)DA(20),CA(21),DA(24) INP22420
IF(NHT1.EQ.2)WRITE(JTAPE,40)DA(22),CA(23),DA(24) INP22430
IF(NHT1.EC.3)WRITE(JTAPE,40)DA(20),DA(21),DA(25) INP22440
IF(NHT1.EC.4)WRITE(JTAPE,40)DA(22),DA(23),DA(25) INP22450
IF(NHT2.EC.1)WRITE(JTAPE,43) INP22460
IF(NHT2.EC.2)WRITE(JTAPE,41)(DA(JL),JL=26,31) INP22470
IF(NHT2.EQ.3)WRITE(JTAPE,41)(DA(JL),JL=32,37) INP22480
IF(NHT2.EC.4)WRITE(JTAPE,42)(DA(JL),JL=32,37),DA(38),(DA(JL),
1JL=26,31) INP22500
1107 CCNTINUE INP22510
NDIF=1 INP22520
NDIG=0 INP22530
IF(NDIFF.GE.0)GO TO 1109 INP22540
NDIF=-1 INP2255C
NDIFF=-NDIFF INP22560
1109 IF(NDIFF.LE.100)GO TO 1110 INP22570
NDIFF=NDIFF-100 INP22580
NDIG=1 INP22590
1110 CCNTINUE INP22600
NWAY=NDIFF/10 INP22610
NGO=NDIFF-NWAY*10 INP22620
NDIFF=(NDIFF+100*NDIG)*NDIF INP22630
IF(NSNOUT.EC.1)IJ=7 INP22640
IF(NSNCUT.EC.0)IJ=8 INP22650
IF(NWAY.EC.1)WRITE(JTAPE,45)(DA(JK),JK=53,55),DA(IJ) INP22660
IF(NWAY.EC.2)WRITE(JTAPE,45)(DA(JK),JK=50,52),CA(IJ) INP22670
IF(NGC.EC.1)WRITE(JTAPE,46)(DA(JK),JK=53,55),DA(IJ) INP22680
IF(NGC.EC.2)WRITE(JTAPE,46)(DA(JK),JK=50,52),DA(IJ) INP22690
IF(NGO.EC.3)WRITE(JTAPE,46)(DA(JK),JK=56,58),DA(IJ) INP22700
IF(NDIF.EC.1)WRITE(JTAPE,38) INP22710
IF(NDIF.EQ.-1)WRITE(JTAPE,39) INP22720
IF(NDIG.EC.1)WRITE(JTAPE,47) INP22730
111 MN=1 INP22740
IF(M.NE.1)WRITE(JTAPE,36) MN INP22750
IF(NCASE.EQ.0)GOTO 1315 INP22760
RETURN INP22770
1315 M=M+1 INP22780
GO TO 1314 INP22790
END INP22800

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..........*.....*.....*.....*.....*.....*.....*.....*

\$IBFTC TAP
C TAPE0001

C SUBROUTINETAPE TAPE0002

C READS DATA FROM LIBRARY TAPE AND ASSEMBLES SHORT LIST OF RELEVANT TAPE0003
C DATA IN CCRE TAPE0004

C COMMON STATEMENTS TAPE0005
C TAPE0006

C THIS SUBROUTINE USES COMMON BLOCKS WHOSE NAMES CONTAIN THE NUMBER 1 TAPE0007
C VIZ- B1,B12,B13,B15,B17,B18,B167,B168,B178,B1234,B1678,B12346 TAPE0008

C TAPE0009
C TAPE0010

C COMMON/B1/KTAPE, XINT,PI4,NWH,NG,FFB(50),FTA(120) TAPE0011
C 1,FTB(120),NBLADE,NUMSW, CSWLOU,DSWLIN, TAPE0012

C 1TCATA(50),TCATB(50),HAB(50) TAPE0013
C COMMON/B12/ X(120),CA(120),CB(120),SA(50),SB(50), TAPE0014

C 1NRECT,NXDIF,NCIFF,NSNGUT,NXCIF1,NXCIF2,NXCIFA,NXDIFB,NTUBE, TAPE0015
C 2PRESIN, BLOCK(50),ABLCCK,SHAPEH(2,50), TAPE0016

C 3VPDATA(15),RDATA(15),NUPR,ARDTA(200),XLNDTA(20),EFDTA(200),NCDF, TAPE0017
C 4NYCF,NZDF,E1DTA, NXCF,AREF,WIDTH1, TAPE0018

C 5XMACH,RMOREF,EFACT(3) TAPE0019
C COMMON/B16/CDS(20,15),DPHS(20,15),FLCV, IH, NABX(45) TAPE0020

C 1,NSP(20),GXIS(20,15),K4,K6,FIT,FIPHI,FIPSI,FIA,FITAU,FID,FIENH TAPE0021
C 2,SHAFST, FIFTPR, LCMFL,LCANIL TAPE0022

C 3,LCANL,LCFTEL,LCFTL,LCPTL,BETA,ASH,FFIZ(45),AHDCME,NSCOCP(20) TAPE0023
C 4,LCPTAL,PAFRZ,NHTU(50) TAPE0024

C 5,AF23A(3),AF23B(3),XAF23A(3),XAF23B(3) TAPE0025
C COMMON/B13/ AREA1,NXDIFC,NXDIFB,NZDIFB,NCDFB,E1DTAB TAPE0026

C 1,XLNDTB(20),EFDTAB(200),ARDTAB(200) , TAPE0027
C 1NwALL1,NwALL2 TAPE0028

C COMMON/B17/ XHU(50),DXHU(50),EFC(2), NEF,STEP,JKSN(50),NSH TAPE0029
C COMMON/B18/ABSW,EMW,EMC,NLUM, NHT1,NHT2 TAPE0030

C 1, X1FCA(45),X1FCB(45),CCNDFT,TCASA(45),TCASB(45),TCLTW1,TOLIT TAPE0031
C 2W2,XFILMZ, TABTFT(10),TABEFT(100),TABPFT(10),NEFT,NPF1,NFORMTAPE0032

C 3,NCool, NUPAX1,NUMAX2 TAPE0033
C COMMON/B126/AF2,TAN1A,TAN1B,PAN1A,PAN1B, AFA,AFB,PREDH,STAGT TAPE0034

C 1,IBL,STPREF,PARTA,PNRTB,DPHSNT,DOMLOS TAPE0035
C COMMON/B167/GASC,GRAVC,GJOLLE,IPJ(50),XH(50),NH TAPE0036

C COMMON/B168/AANA(45),AANB(45),CCA(45),CCB(45),FCR,NLAST TAPE0037
C 1,KANHET,LANHET,PERCO,THIKFT TAPE0038

C 2,DANA(45),DANE(45) TAPE0039
C COMMON/B178/DFT(45) TAPE0040

C COMMON/B1678/NSHCP,XCP(45),AFT(45),PI TAPE0041
C 1,NHH(50),KJSN(45,6),HAU(50),CFTA(45),CFTB(45),NAB(50),NCODEA(45) TAPE0042

C 2,NCODEB(45),TZ TAPE0043
C COMMON/B12678/JTAPE ,IPRINT TAPE0044

C DIMENSION STATEMENTS TAPE0045
C DIMENSIONCDSA(25),DPHSA(25),GXISA(25), NCARD(10),IDX(60) TAPE0046

C FORMAT STATEMENTS TAPE0047
C TAPE0048

C 1 FORMAT(7E10.3) TAPE0049
C 2 FCRMAT(7I10) TAPE0050

C 5 FCRMAT(5I10,E10.3) TAPE0051
C 6 FCRMAT(7OXI2) TAPE0052

C 7 FCRMAT(I10,2E10.3,2I5,3E10.3/(10X6E10.3)) TAPE0053
C 96 FCRMAT(65H EMPIRICAL FLAME-EMISSIVITY DATA INCORRECTLY WRITTEN ON TAPE0054

C 1DATA TAP2) TAPE0055
C TAPE0056
C TAPE0057
C TAPE0058
C TAPE0059

```

.....*.....*.....*.....*.....*.....*.....*.....*.....*.....*
97 FCRMAT(47H DIFFUSER DATA INCORRECTLY WRITTEN ON DATA TAPE) TAPE0060
98 FORMAT(65H HOLE DISCHARGE COEFFICIENT DATA INCORRECTLY WRITTEN ON TAPE0061
  1DATA TAPE) TAPE0062
99 FCRMAT(/////37H0*** ERROR MESSAGE - PROGRAM STOPPED) TAPE0063

```

```
DC110J=1,NH TAPE0064
```

```
110 IHJ(J)=0 TAPE0065
```

```

C C C HOLE DISCHARGE COEFFICIENT AND JET ANGLE DATA TAPE0066

```

```
IH=1 TAPE0067
```

```
READ(KTAPE,2)NMXTYP TAPE0068
```

```
102 READ(KTAPE,7)NHTYP,DXH,HAA,NSCOOQ,NSPA,(DPHSA(I),CDSA(I),GXISA(I), TAPE0069
```

```
  1I=1,NSPA) TAPE0070
```

```
NEND=0 TAPE0071
```

```
DC101J=1,NH TAPE0072
```

```
IF(NHTYP.NE.NHTU(J))GOTO101 TAPE0073
```

```
IF(HAB(J).NE.0.) HAA=HAB(J) TAPE0074
```

```
DXHU(J)=DXH/12. TAPE0075
```

```
HAU(J)=HAA/144. TAPE0076
```

```
IF(MOC(NSCOOQ,10).NE.2)GOTO1025 TAPE0077
```

```
HAU(J)=HAA/12. TAPE0078
```

```
NHH(J)=1 TAPE0079
```

```
1025 IHJ(J)=IH TAPE0080
```

```
IF(NEND.NE.0)GOTO101 TAPE0081
```

```
NEND=1 TAPE0082
```

```
DO103I4=1,NSPA TAPE0083
```

```
DPHS(IH,I4)=ALOG(DPHSA(I4)) TAPE0084
```

```
CDS(IH,I4)=CDSA(I4) TAPE0085
```

```
103 GXIS(IH,I4)=GXISA(I4)*PI/180. TAPE0086
```

```
NSP(IH)=NSPA TAPE0087
```

```
NSCOOP(IH)=NSCOOQ TAPE0088
```

```
101 CCNTINUE TAPE0089
```

```
IF(NEND.EQ.1)IH=IH+1 TAPE0090
```

```
109 CCNTINUE TAPE0091
```

```
IF(NHTYP.LT.NMXTYP)GOTO102 TAPE0092
```

```
READ(KTAPE,6)INDEX TAPE0093
```

```
IF(INDEX.NE.1)GOTO198 TAPE0094
```

```
INDEX=0 TAPE0095
```

```

C C C

```

```
EMPIRICAL GENERALIZED DIFFUSER DATA TAPE0096
```

```
READ(KTAPE,2)NWALMX TAPE0097
```

```
READ(KTAPE,?) (NCARC(I7),I7=1,NWALMX) TAPE0098
```

```
DC105I7=1,NWALMX TAPE0099
```

```
104 READ(KTAPE,5)NWALL,NXDIFD,NYDIFA,NZDIFA,NCDIFA,E1DTAA TAPE0100
```

```
IF(NWALL.NE.NWALL1)GOTO100 TAPE0101
```

```
NXDF=NXDIFD TAPE0102
```

```
NYDF=NYDIFA TAPE0103
```

```
NZDF=NZDIFA TAPE0104
```

```
NCDF=NCDIFA TAPE0105
```

```
E1DTA=E1DTAA TAPE0106
```

```
READ(KTAPE,1)(EFDTA(I),I=1,NYDF),(ARDTA(I),I=1,NXDF),(XLNDTA(I),I= TAPE0107
```

```
  11,NZDF) TAPE0108
```

```
GOTO105 TAPE0109
```

```
100 IF(NWALL.NE.NWALL2)GOTO106 TAPE0110
```

```
NXDIFB=NXDIFD TAPE0111
```

```
NYDIFB=NYDIFA TAPE0112
```

```
NZDIFB=NZDIFA TAPE0113
```

```
NCDIFB=NCDIFA TAPE0114
```

```
TAPE0115
```

```
TAPE0116
```

```
TAPE0117
```

```
TAPE0118
```

```
TAPE0119
```

```

.....*.....*.....*.....*.....*.....*.....*.....*.....*.....*
E1DTAB=E1DTAA
READ(KTAPE,1)(E1DTAB(I),I=1,NYDIFB),(AROTAB(I),I=1,NXDIFC),
1(XLNDTB(I),I=1,NZDIFB)
GOTO105
106 ACRO=NCARD(NWALL)
READ(KTAPE,6)(ICX(I11),I11=1,NCRD)
105 CONTINUE
READ(KTAPE,6)INDEX
IF(INDEX.NE.1)GOTO197
INDEX=0
C
C EMPIRICAL FLAME-EMISSIVITY DATA
C
C WHEN THIS TABLE IS SET UP ON THE DATA TAPE, NLUM IN BLOCK DATA
C SHOULD BE CHANGED TO 6.

IF(NLUM.NE.6)GOTO107
READ(KTAPE,2) NTFT,NEFT,NPFT,NFORM
READ(KTAPE,1) (TABTFT(I2),I2=1,NTFT),(TABPFT(I2),I2=1,NPFT),
1(TABEFT(I2),I2=1,NEFT)
DC 1055 I2=1,NTFT
1055 TABTFT(I2)=TABTFT(I2)+TZ
READ(KTAPE,6)INDEX
IF(INDEX.NE.1)GOTO196
INDEX=0
107 RETURN
196 WRITE(JTAPE,99)
WRITE(JTAPE,96)
STCP
197 WRITE(JTAPE,99)
WRITE(JTAPE,97)
STOP
198 WRITE(JTAPE,99)
WRITE(JTAPE,98)
STOP
END

```

TAPE0120
TAPE0121
TAPE0122
TAPE0123
TAPE0124
TAPE0125
TAPE0126
TAPE0127
TAPE0128
TAPE0129
TAPE0130
TAPE0131
TAPE0132
TAPE0133
TAPE0134
TAPE0135
TAPE0136
TAPE0137
TAPE0138
TAPE0139
TAPE0140
TAPE0141
TAPE0142
TAPE0143
TAPE0144
TAPE0145
TAPE0146
TAPE0147
TAPE0148
TAPE0149
TAPE0150
TAPE0151
TAPE0152
TAPE0153
TAPE0154
TAPE0155

..........*.....*.....*.....*.....*.....*.....*.....*

SIBFTC GEC LIST

SUBROUTINEGEOM

OC1C
GECM0020
GECM0030
GECM0040
GECM0050
GECM0060
GECM0070
GECM0080
GECM0090
GECM0100
GECM0110
GECM0120
GECM0130
GECM0140
GECM0150
GECM0160
GECM017C
GECM018C
GECM0190
GECM0200
GECM0210
GECM022C
GECM0230
GECM0240
GECM0250
GECM0260
GECM0270
GECM028C
GECM0290
GECM0300
GECM0310
GECM0320
GECM033C
GECM034C
GECM0350
GECM0360
GECM037C
GECM038C
GECM0390
GECM0400
GECM0410
GECM0420
GECM0430
GECM0440
GECM0450
GECM0460
GECM0470
GECM0480
GECM0490
GECM0500
GECM0510
GECM0520
GECM0530
GECM0540
GECM0550
GECM0560
GECM0570
GECM0580
GECM0590

C
C CALCULATES GEOMETRIC QUANTITIES AND FIXES LOCATIONS OF CALCULATION
C PCINTS

C
C COMMON STATEMENTS

C THIS SUBROUTINE USES COMMON BLOCKS WHOSE NAMES CONTAIN THE NUMBER 1
C VIZ- B1,B12,B13,B16,B17,B18,B167,B168,B17E,B1234,B1E7E,B12346

COMMON/B1/KTAPE, XINT,PI4,NWH,NG,FFB(50),FTA(120)
1,FTB(120),NBLADE,NUMSW, DSWLOU,DSWLIN,
1TCATA(50),TCATB(50),FAB(50)
COMMON/B12/ X(120),CA(120),CB(120),SA(50),SB(50),
1NRECT,NXDIF,NCIFF,NSNCUT,NXDIF1,NXCIF2,NXDIFA,NXDIFB,NTUBE,
2PRESIN, BLOCK(50),ABLOCK,SHAPEH(2,50),
3Vpdata(15),RDATA(15),NUPR,ARDTA(200),XLNDDTA(20),EFDTA(200),NCDF,
4NYDF,NZDF,E1DTA, NXDF,AREF,WIDTH1,
5XMACH,RHGREF,EFDT(3)

COMMON/B16/CDS(20,15),DPHS(20,15),FLCV,IH, NABX(45)
1,NSP(20),GXIS(20,15),K4,K6,FIT,FIPFI,FIPSI,FIA,FITAL,FID,FIENH
2,SHAFST, FIFTPR, LCMFL,LCANIL
3,LCANL,LCFTEL,LCFTL,LCPRTL,BETA,ASW,FFIZ(45),AHDOME,NSCOOP(20)
4,LCPTAL,PAFRZ,NHTU(50)

5,AF23A(3),AF23B(3),XAF23A(3),XAF23B(3)
COMMON/B13/ AREA1,NXDIFC,NYDIFB,NZDIFB,NCDFB,E1DTAB
1,XLNDDTB(20),EFDTAB(200),ARDTAB(200),
1NWALL1,NWALL2

COMMON/B17/ XHU(50),DXHU(50),EFC(2), NEF,STEP,JKSN(50),NSH
COMMON/B167/GASC,GRAVC,GJCULE,IMJ(50),XH(50),NH
COMMON/B178/DFT(45)

COMMON/B1678/NSHCP,XCP(45),AFT(45),PI
1,NHH(50),KJSN(45,6),HAU(50),CFTA(45),CFTB(45),NAB(50),NCODEA(45)
2,NCODEB(45),TZ

COMMON/B12678/JTAPE,IPRINT
COMMON/B18/ABSW,EMW,EMC,NLUM,

1, X1FCA(45),X1FCB(45),CONDFT,TCASA(45),TCASB(45),TOLTH1,TOLTGEOM038C
2W2,XFILMZ, TABTFT(10),TABEFT(100),TABPFT(10),NEFT,NPFT,NFORMGEOM0390
3,NCool, NUMAX1,NUMAX2

COMMON/B126/AF2,TAN1A,TAN1B,PAN1A,PAN1B, AFA,AFB,PREDM,STAGTGEOM0410
1,IBL,STPREF,PNRTA,PNRTB,DPHSNT,DOMLOS

COMMON/B168/AANA(45),AANB(45),CCA(45),CCB(45),FHCR,NLAST
1,KANHET,LANHET,PERCO,THIKFT
2,DANA(45),DANB(45)

C DIMENSION STATEMENTS

DIMENSION HAT(50),XFC(51,5),AR(2),NAME(3)

C FUNCTION DEFINITIONS

FINTRP(X,X1,X2,X3,Y1,Y2,Y3)=Y1*(X-X2)*(X-X3)/((X1-X2)*(X1-X3))+Y2*GECM0530
1*(X-X1)*(X-X3)/((X2-X1)*(X2-X3))+Y3*(X-X1)*(X-X2)/((X3-X1)*(X3-X2))GECM0540
FINTL(X,X1,X2,Y1,Y2)=Y1+(X-X1)*(Y2-Y1)/(X2-X1)

C DATA DECLARATION

DATA NAME(1)/18H INNER OUTER /


```

*.....*.....*.....*.....*.....*.....*.....*.....*.....*
J=NWH-1
JLAST=J
K2=0
NSHCP=0
JA=NH
JB=NH
112 K=K+1
IX=1
IF(K.GT.KMAX)GOTC199
IF(JA.EQ.JB.AND.NAB(JA).EQ.1.AND.JA.LE.NH) JB=JA+1
IF(JA.EQ.JB.AND.NAB(JA).EQ.2.AND.JA.LE.NH) JA=JB+1
XCP(K)=AMIN1(XFC(JA,LA),XFC(JB,LB),XFC(J+1,1))
IF(ABS(XCP(K)-XFC(J+1,1))/XCP(K).LE.0.00001) XCP(K)=XFC(J+1,1)
IF(XCP(K).EQ.XFC(J+1,1))GOTC125
IF(XCP(K).EQ.XFC(JA,LA))GOTO152
154 IF(DXHU(J).NE.0..OR.LB.NE.1)GOTO109
NCCDER(K)=1
NABX(K)=2
109 L=LB
LB=LB+1
IF(K2.EQ.1)LA=LB
IF(LB.LE.5)GOTO153
LB=1
JB=NH+1
GOTO153
125 J=J+1
IF(J.EQ.NH+1) GC TO 150
IF(J.EQ.NSH)NSHCP=K
JKSN(J)=K
IF(NHTU(J).EQ.0) GC TO 1250
IF(NAB(J).NE.1)GOTC128
IF(DXHU(J).EQ.0.)NCODEA(K)=1
JA=J
LA=2
128 IF(NAB(J).NE.2)GOTO130
IF(DXHU(J).EQ.0.)NCODEB(K)=1
JE=J
LE=2
130 L=1
NABX(K)=NAB(J)
K2=0
GCTC153
1250 IF(ABS(XH(J)-XFC(JA,LA))/XH(J).LE.0.00001) LA=LA+1
IF(ABS(XH(J)-XFC(JB,LB))/XH(J).LE.0.00001) LB=LB+1
NABX(K)=4
KJSN(K,1)=J
IF(LA.LE.5) GC TO 1251
LA=1
JA=NH+1
1251 IF(LB.LE.5) GO TO 153
LB=1
JB=NH+1
GO TO 153
150 NLAST=K
XCP(K)=X(NG)
FFIZ(K)=0.
FTACPI=FTA(NG)
FTBCPI=FTB(NG)
CACPI=CA(NG)
CBCPI=CB(NG)
GEOF2950
GEOF2960
GEOF2970
GEOF2980
GEOF2990
GEOF3000
GEOF3010
GEOF3020
GEOF3030
GEOF3040
GEOF3050
GEOF3060
GEOF3070
GEOF3080
GEOF3090
GEOF3100
GEOF3110
GEOF3120
GEOF3130
GEOF3140
GEOF315C
GEOF3160
GEOF3170
GEOF3180
GEOF3190
GEOF320C
GEOF3210
GEOF3220
GEOF3230
GEOF3240
GEOF3250
GEOF3260
GEOF3270
GEOF328C
GEOF3290
GEOF3300
GEOF3310
GEOF3320
GEOF3330
GEOF3340
GEOF3350
GEOF3360
GEOF3370
GEOF3380
GEOF3390
GEOF3400
GEOF3410
GEOF3420
GEOF3430
GEOF3440
GEOF3450
GEOF3460
GEOF3470
GEOF3480
GEOF3490
GEOF3500
GEOF3510
GEOF3520
GEOF3530
GEOF3540

```


140

```
*.....*.....*.....*.....*.....*.....*.....*.....*.....*
C --- FIRST RCW ON INNER WALL
139 NXDIFA=I-1
143 K=K+1
    IF(NABX(K).NE.2.AND.NABX(K).NE.3)GO TO 143
145 IF(X(I).GT.XCP(K))GC TO 144
    I=I+1
    GO TO 145
141 NXDIFA=I-1
144 NXDIFR=I-1
    GC TO 146
C --- FIRST RCW ON OUTER WALL
140 NXDIFR=I-1
148 K=K+1
    IF(NABX(K).NE.1.AND.NABX(K).NE.3)GO TO 148
159 IF(X(I).GT.XCP(K))GC TO 160
    I=I+1
    GC TO 159
160 NXDIFA=I-1
146 CCNTINUE
    RETURN
193 WRITE(JTAPE,93)J
    GCTO200
199 WRITE(JTAPE,95)J
    GC TO 200
142 WRITE(JTAPE,91)
200 STCP
C
    END
YOUR CARD TOTAL IS ---
```

GECM4750
GECM4760
GECM4770
GECM4780
GECM4790
GECM4800
GECM4810
GECM4820
GECM4830
GECM4840
GECM4850
GECM4860
GECM4870
GECM4880
GECM4890
GECM4900
GECM4910
GECM4920
GECM4930
GECM4940
GECM4950
GECM4960
GECM4970
GECM4980
GECM4990
GECM5000
GECM5010
GECM5020
GECM5030
GECM5040

```

$IBFTC DIFL
SUBROUTINE DIFLOW
C
C THIS SUBROUTINE CONTROLS THE DIFFUSER CALCULATION
C
C NDIFF CONTROLS THE METHOD OF CALCULATING THE DIFFUSER
C PERFORMANCE
C 1 IN TEN POSITION = USE STREAMTUBE ANALYSIS UP TO SNOOT
C 2 IN TEN POSITION = USE EMPIRICAL DATA UP TO SNOOT
C 1 IN UNIT POSITION = USE STREAMTUBE ANALYSIS AFTER SNOOT LIP
C 2 IN UNIT POSITION = USE EMPIRICAL DATA AFTER SNOOT LIP
C 3 IN UNIT POSITION = USE MIXING EQUATION AFTER SNOOT LIP
C POSITIVE SIGN = USE EFFECTIVENESS PLOT
C NEGATIVE SIGN = USE SPECIFIC DIFFUSER DATA
C
COMMON/B2/ RAD(16),DELTA(2,50),EE1(2),UJ(15),THA,THB,THS,PRES(50),
1NGO,NWAY,ZZR,ZZGAMA,BETA1,BETA2,XMVA,XMVB,XMVS, ZZCP, IDIF
2,HSEP ,FLAREA(50),AREA(50)
COMMON/B12/ X(120),CA(120),CB(120),SA(50),SB(50),
1NRECT,NXDIF,NDIFF,NSNOOT,NXDIF1,NXDIF2,NXDIFA,NXDIFB,NTUBE,
2PRESIN, BLOCK(50),ABLOCK,SHAPEH(2,50),
3VPDATA(15),RDATA(15),NUPR,ARDTA(200),XLNDDTA(20),EFDTA(200),NCDF,
4NYDF,NZDF,EIDTA, NXDF,AREF,WIDTH1,
5XMACH,RHOREF,EFD(3)
COMMON/B126/AF2,TANIA,TANIB,PANIA,PANIB, AFA,AFB,PREDM,STAGT
1,IBL,STPREF,PNRTA,PNRTB,DPHSNT,DOMLOS
COMMON/B12678/JTAPE ,IPRINT
COMMON/BZERO/ALPHA1(50),ALPHA2(50),ALPHA3(50),ALPHA4(50),DMY(400)
COMMON/BPLOS/PLOSS(2)
DIMENSION ASTAR(2),ARAT(3),AFUN(3),DPT(3),AR(2),CPID(2),CPAC(2),
1AF(2),PDLS(3)
C
8765 FORMAT(7HODIFLCW10F11.3/(7X10F11.3))
C
C CALCULATE GAS PROPERTIES AND CHOOSE ROUTING THROUGH DIFFUSER
C SUBPROGRAM
C
IBL=1
IDIF=0
IF(NRECT.EQ.2) AF2=AF2/WIDTH1
CALL GASTBL(D1,D2,D3,D4,-1,D6,ZZR,ZZGAMA)
ZZCP=ZZR*ZZGAMA/(ZZGAMA-1.)
IF(NDIFF) 90,99,98
90 IDIF=1
NDIFF=-NDIFF
GO TO 99
98 IDIF=0
99 NWAY=NDIFF/10
NGO =NDIFF - NWAY*10
IF(IDIF.EQ.1) NDIFF=-NDIFF
C
C CALCULATE DIFFUSER PERFORMANCE FROM COMPRESSOR EXIT TO THE LIP OF
C SNOOT OR TO THE DOME
C
GO TO (100,140),NWAY
100 CALL TUBCIS
IF(IBL) 140,140,1401
140 NWAY=2
IF(NGO) 1400,141,1400
DIFL0010
DIFL0020
DIFL0030
DIFL0040
DIFL0050
DIFL0060
DIFL0070
DIFL0080
DIFL0090
DIFL0100
DIFL0110
DIFL0120
DIFL0130
DIFL0140
DIFL0150
DIFL0160
DIFL0170
DIFL0180
DIFL0190
DIFL0200
DIFL0210
DIFL0220
DIFL0230
DIFL0240
DIFL0250
DIFL0260
DIFL0270
DIFL0280
DIFL0290
DIFL0300
DIFL0310
DIFL0320
DIFL0330
DIFL0340
DIFL0350
DIFL0360
DIFL0370
DIFL0380
DIFL0390
DIFL0400
DIFL0410
DIFL0420
DIFL0430
DIFL0440
DIFL0450
DIFL0460
DIFL0470
DIFL0480
DIFL0490
DIFL0500
DIFL0510
DIFL0520
DIFL0530
DIFL0540
DIFL0550
DIFL0560
DIFL0570
DIFL0580
DIFL0590

```

141	NGO=2	DIFL0600
	IBL=1	DIFL0610
1400	CALL EMPCTS	DIFL0620
	IF (IBL) 1401,900,1401	DIFL0630
1401	IF(NSNCUT.EQ.1) GO TO 150	DIFL0640
102	PREDM=PRES(NXDIF)	DIFL0650
111	A1=0.	DIFL0660
	B1=0.	DIFL0670
	GO TO (1570,1580),NRECT	DIFL0680
C		DIFL0690
C	CALCULATE VARICUS GEOMETRIC PROPERTIES OF THE ANNULUS DIFFUSER	DIFL0700
C		DIFL0710
150	CALL SLOPE(X,CA,NXDIF ,NXDIFA,ALPHA1,NXDIFA+1)	DIFL0720
	CALL SLOPE(X,SA,NXDIF+2,NXDIFA,ALPHA2,NXDIFA+1)	DIFL0730
	CALL SLOPE(X,CB,NXDIF ,NXDIFB,ALPHA3,NXDIFB+1)	DIFL0740
	CALL SLOPE(X,SB,NXDIF+2,NXDIFB,ALPHA4,NXDIFB+1)	DIFL0750
	NXDf1=NXDIF+1	DIFL0760
	NXDf2=NXDIF+2	DIFL0770
	NXDFA1=NXDIFA-1	DIFL0780
	NXDfB1=NXDIFB-1	DIFL0790
	DO 1500 I=NXDIF,NXDf1	DIFL0800
	ALPHA2(I)=ALPHA1(I)	DIFL0810
1500	ALPHA4(I)=ALPHA3(I)	DIFL0820
	DO 151 I=NXDIF,NXDIFA	DIFL0830
	DD=1.	DIFL0840
	DE=1.	DIFL0850
	IF(ALPHA1(I).LT.0.) DD=-1.	DIFL0860
	IF(ALPHA2(I).LT.0.) DE=-1.	DIFL0870
	ALPHA1(I)=DD*ATAN(DD*ALPHA1(I))	DIFL0880
151	ALPHA2(I)=DE*ATAN(DE*ALPHA2(I))	DIFL0890
	DO 152 I=NXDIF,NXDIFB	DIFL0900
	DD=1.	DIFL0910
	DE=1.	DIFL0920
	IF(ALPHA3(I).LT.0.) DD=-1	DIFL0930
	IF(ALPHA4(I).LT.0.) DE=-1.	DIFL0940
	ALPHA3(I)=DD*ATAN(DD*ALPHA3(I))	DIFL0950
152	ALPHA4(I)=DE*ATAN(DE*ALPHA4(I))	DIFL0960
156	A=(ALPHA1(NXDIF+1)+ALPHA2(NXDIF+1))/2.	DIFL0970
	B=(ALPHA3(NXDIF+1)+ALPHA4(NXDIF+1))/2.	DIFL0980
	A1=(ALPHA1(NXDIFA)+ALPHA2(NXDIFA))/2.	DIFL0990
	B1=(ALPHA3(NXDIFB)+ALPHA4(NXDIFB))/2.	DIFL1000
	GO TO (157,158),NRECT	DIFL1010
157	THA1=(SA(NXDIF+1)**2-CA(NXDIF+1)**2)*3.141593 *COS(A)	DIFL1020
	THB1=(CB(NXDIF+1)**2-SB(NXDIF+1)**2)*3.141593 *COS(B)	DIFL1030
	THS1=(SB(NXDIF+1)**2-SA(NXDIF+1)**2)*3.141593	DIFL1040
1570	SUMA=(SA(NXDIFA)**2-CA(NXDIFA)**2)*3.141593	DIFL1050
	SUMB=(CB(NXDIFB)**2- SB(NXDIFB)**2)*3.141593	DIFL1060
	GO TO 159	DIFL1070
158	THA1=(SA(NXDIF+1)-CA(NXDIF+1))*COS(A)	DIFL1080
	THB1=(CB(NXDIF+1)-SB(NXDIF+1))*COS(B)	DIFL1090
	THS1=SB(NXDIF+1)-SA(NXDIF+1)	DIFL1100
1580	SUMA=(SA(NXDIFA)-CA(NXDIFA))	DIFL1110
	SUMB=(CB(NXDIFB)- SB(NXDIFB))	DIFL1120
159	CONTINUE	DIFL1130
	GO TO (1590,1591,1592),NGO	DIFL1140
1590	CALL TUBSTA	DIFL1150
	GO TO 1600	DIFL1160
1591	CALL EMPSTA	DIFL1170
	GO TO 1600	DIFL1180
1592	COR1=0.	DIFL1190
	COR2=0.	DIFL1200

```

DO 240 I=NXDF2,NXDFA1
TURN=ABS(ALPHA1(I)-ALPHA1(I-1)+ALPHA2(I)-ALPHA2(I-1))/2.
RADC=(X(I)-X(I-1))/COS((ALPHA1(I)+ALPHA2(I))/2.)/TURN
C=(SA(I)-CA(I))*COS((ALPHA1(I)+ALPHA2(I))/2.)
DHY=1. /32./2.*((SA(NXDIF+1)-CA(NXDIF+1))*COS(A )/C)**2
240 COR1 =COR1 +DHY*(0.124+3.1*SQRT(C/2./RADC))*TURN/3.14159
DO 241 I=NXDF2,NXDFA1
TURN=ABS(ALPHA3(I)-ALPHA3(I-1)+ALPHA4(I)-ALPHA4(I-1))/2.
RADC=(X(I)-X(I-1))/COS((ALPHA3(I)+ALPHA4(I))/2.)/TURN
C=(CB(I)-SB(I))*COS((ALPHA3(I)+ALPHA4(I))/2.)
DHY=1. /32./2.*((CB(NXDIF+1)-SB(NXDIF+1))*COS(B )/C)**2
241 COR2 =COR2 +DHY*(0.124+3.1*SQRT(C/2./RADC))*TURN/3.14159
1600 IF(NRECT.EQ.2) AF2=AF2*WIDTH1
DPHSNT=STPREF-PREDM
AG=A
BG=B
RETURN
C
C DIFFUSER CALCULATION ENTERED HERE DURING MASS FLOW ITERATION
C
ENTRY DIFLW
IF(NRECT.EQ.2) AF2=AF2/WIDTH1
AF(1)=AFA
AF(2)=AFB
IF(NSNCUT.EQ.1) GO TO 200
C
C PRESSURE DOWN STREAM OF DIFFUSER CALCULATED AS AN ISENTROPIC
C EXPANSION FROM PRESSURE(DOME) AND TSTAG.
C
165 PREM=STPREF-DOMLOS*(STPREF-PREDM)
PNRTA=STPREF-DOMLOS*DPHSNT
PNRTB=PNRTA
ASTAR(1)=AFA*SQRT(ZZCP*STAGT*((ZZGAMA-1.)*32.)*(1.+(ZZGAMA-1.)/2.)
1*((ZZGAMA+1.)/(ZZGAMA-1.)/2.)/(PREM *32.)/(ZZGAMA)
ASTAR(2)=ASTAR(1)*AFB/AFA
AAS=SUMA/ASTAR(1)
CALL GASTBL(AAS,TTO,Z,D4,1,IBL,D7,D8)
IF(IBL) 900,500,166
166 PAN1A=Z*PREM
TAN1A=TTO*STAGT
AAS=SUMB/ASTAR(2)
CALL GASTBL(AAS,TTO,Z,D4,1,IBL,D7,D8)
IF(IBL) 900,900,169
169 PAN1B=Z*PREM
TAN1B=TTO*STAGT
DP=(STPREF-PREM )/STPREF
IF(IPRINT)190,190,170
170 CALL DCUTP1(NSNOUT,PREM ,PAN1A,D4,D5,D6,D7,3,1,D8,DP)
CALL DCUTP1(NSNOUT,PREM ,PAN1B,D4,D5,D6,D7,3,2,D8,DP)
190 GO TO 900
200 GO TO (210,220),NWAY
C
C USE STREAM TUBE ANALYSIS
C
210 CALL TUBFW1
GO TO 230
C
C USE EMPIRICAL DATA
C
220 CALL EMPDT1

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DIFL1210
DIFL1220
DIFL1230
DIFL1240
DIFL1250
DIFL1260
DIFL1270
DIFL1280
DIFL1290
DIFL1300
DIFL1310
DIFL1320
DIFL1330
DIFL1340
DIFL1350
DIFL1360
DIFL1370
DIFL1380
DIFL1390
DIFL1400
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DIFL1420
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DIFL1440
DIFL1450
DIFL1460
DIFL1470
DIFL1480
DIFL1490
DIFL1500
DIFL1510
DIFL1520
DIFL1530
DIFL1540
DIFL1550
DIFL1560
DIFL1570
DIFL1580
DIFL1590
DIFL1600
DIFL1610
DIFL1620
DIFL1630
DIFL1640
DIFL1650
DIFL1660
DIFL1670
DIFL1680
DIFL1690
DIFL1700
DIFL1710
DIFL1720
DIFL1730
DIFL1740
DIFL1750
DIFL1760
DIFL1770
DIFL1780
DIFL1790
DIFL1800
DIFL1810

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MIXING EQUATION USED IN DIFFUSING PASSAGE BEYOND THE SNOUT LIP
USE SUDDEN EXPANSION OR CONTRACTION ANALYSIS

230 THA=THA* \cos (AG)
 THB=THE* \cos (BG)
 BETAS=1.
 ARAT(1)=THA/THA1
 ARAT(2)=THB/THB1
 ARAT(3)=THS/THS1
 DO 235 I=1,3
 IF(ARAT(I)-1.)232,232,231
 231 AFUN(I)=(3.*ARAT(I)**2.-2.-ARAT(I))/4.
 HDLS(I)=0.5*(1.-1./ARAT(I))
 GO TO 235
 232 AFUN(I)=ARAT(I)**2-ARAT(I)
 HDLS(I)=(1.-ARAT(I))**2
 235 CONTINUE
 RHA =AFA/THA/XMVA
 RHB =AFB/THB/XMVB
 RHS =(AF2-AFA-AFB)/THS/XMVS
 XV2S=(BETAS*XMVS)**2
 XV2A=(BETA1*XMVA)**2
 XV2B=(BETA2*XMVB)**2
 PANDA=PRES(NXDIF)-RHA*XV2A*AFUN(1)/32.
 PANDB=PRES(NXDIF)-RHB*XV2B*AFUN(2)/32.
 PREDM=PRES(NXDIF)-RHS*XV2S*AFUN(3)/32.
 A=(AFA*ZZR/PANCA/THA1)**2/(2.*32.18*ZZCP)
 TSTAT=(-1.+SQRT(1.+4.*A*STAGT))/2./A
 PLOSS(1)=HDLS(1)*RHA*XV2A/64.36
 RH2PA=PANCA/ZZR/TSTAT
 V2PRA=AFA/THA1/RH2PA
 A=(AFB*ZZR/PANDB/THB1)**2/(2.*32.18*ZZCP)
 TSTAT=(-1.+SQRT(1.+4.*A*STAGT))/2./A
 PLOSS(2)=HDLS(2)*RHB*XV2B/64.36
 RH2PB=PANDB/ZZR/TSTAT
 V2PRB=AFB/THB1/RH2PB
 THA=THA/CCS(AG)
 THB=THE/COS(BG)
 DPHSNT=RHS*(XMVS*ARAT(3))**2/2./32.
 GO TO (300,310,2300),NGO

MIXING EQUATION IS USED TO GIVE PRESSURE IN ANNULUS

2300 THA=THA*CCS(AG)
 THB=THE* \cos (BG)
 ARAT(1)=SUMA/THA1
 ARAT(2)=SUMB/THB1
 BLN=0.
 PAN1A=PANDA+(1.+1./ARAT(1))*(BETA1-1./ARAT(1))*RH2PA*V2PRA**2/64.4
 PAN1B=PANDB+(1.+1./ARAT(2))*(BETA2-1./ARAT(2))*RH2PB*V2PRB**2/64.4
 ALLOW FOR LOSSES DUE TO BENDS
 PAN1A=PAN1A-COR1*RHA*XV2A*(THA/THA1)**2
 PAN1B=PAN1B-COR2*RHB*XV2B*(THB/THB1)**2
 CALCULATE TEMPERATURE AND TOTAL PRESSURE LOSS
 B=1.
 C=-STAGT

DIFL1820
 DIFL1830
 DIFL1840
 DIFL1850
 DIFL1860
 DIFL1870
 DIFL1880
 DIFL1890
 DIFL1900
 DIFL1910
 DIFL1920
 DIFL1930
 DIFL1940
 DIFL1950
 DIFL1960
 DIFL1970
 DIFL1980
 DIFL1990
 DIFL2000
 DIFL2010
 DIFL2020
 DIFL2030
 DIFL2040
 DIFL2050
 DIFL2060
 DIFL2070
 DIFL2080
 DIFL2090
 DIFL2100
 DIFL2110
 DIFL2120
 DIFL2130
 DIFL2140
 DIFL2150
 DIFL2160
 DIFL2170
 DIFL2180
 DIFL2190
 DIFL2200
 DIFL2210
 DIFL2220
 DIFL2230
 DIFL2240
 DIFL2250
 DIFL2260
 DIFL2270
 DIFL2280
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 DIFL2350
 DIFL2360
 DIFL2370
 DIFL2380
 DIFL2390
 DIFL2400
 DIFL2410
 DIFL2420


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A=(AF(1)*ZZR/SUMA/PAN1A)**2/(2.*ZZCP*32.)
TAN1A=(-B+SQRT(B*B-4.*A*C))/2./A
PNRTA=PAN1A*(STAGT/TAN1A)**(ZZGAMA/(ZZGAMA-1.))
DPT(1)=(STPREF-PNRTA)/STPREF
A=(AF(2)*ZZR/SUMB/PAN1B)**2/(2.*ZZCP*32.)
TAN1B=(-B+SQRT(B*B-4.*A*C))/2./A
PNRTB=PAN1B*(STAGT/TAN1B)**(ZZGAMA/(ZZGAMA-1.))
DPT(2)=(STPREF-PNRTB)/STPREF
C
C PRINT CUT RESULTS
C
IF(IPRINT) 900,900,250
250 AR(1)=THA/THA1
AR(2)=THB/THB1
ARZ=(SUMA/THA)**2
CPID(1)=(2.*(BETA1-1.)+1.-1./ARZ)/BETA1**2
ARZ=(SUMB/THB)**2
CPID(2)=(2.*(BETA2-1.)+1.-1./ARZ)/BETA2**2
CPAC(1)=(PAN1A-PRES(NXDIF))/(RHA*XV2A/2./32.)
1/BETA1**2
CPAC(2)=(PAN1B-PRES(NXDIF))/(RHB*XV2B/2./32.)
1/BETA2**2
DO 255 K=1,2
CALL DCUTP1(NSNOUT,D2,D3,D4,CPID(K),CPAC(K),CPAC(K)/CPID(K),3,K,
1AR(K),CPT(K))
255 CONTINUE
GO TO 900
C
C USE STREAMTUBE ANALYSIS IN DIFFUSING PASSAGES BEYOND THE SNOOT LIP
C
300 CALL TUBSA1
GO TO 900
C
C USE EMPIRICAL DATA IN THE DIFFUSING PASSAGES BEYOND THE SNOOT LIP
C
310 CALL EMPSA1
900 IF(NRECT.EQ.2) AF2=AF2*WIDTH1
RETURN
C
ENTRY DIFLW2
IF(NRECT.EQ.2) AF2=AF2/WIDTH1
IPN=IPRINT
IPRINT=3
CALL TUBCTS
IF(IBL) 1000,1000,910
910 CALL TUBSTA
CALL TUBFW1
IF(IBL) 1000,1000,920
920 CALL TUBSA1
1000 IPRINT=IPN
GO TO 900
END
DIFL2430
DIFL2440
DIFL2450
DIFL2460
DIFL2470
DIFL2480
DIFL2490
DIFL2500
DIFL2510
DIFL2520
DIFL2530
DIFL2540
DIFL2550
DIFL2560
DIFL2570
DIFL2580
DIFL2590
DIFL2600
DIFL2610
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DIFL2770
DIFL2780
DIFL2790
DIFL2800
DIFL2810
DIFL2820
DIFL2830
DIFL2840
DIFL2850
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DIFL2870
DIFL2880
DIFL2890
DIFL2900
DIFL2910
DIFL2920
DIFL2930
DIFL2940

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$IBFTC TBCT LIST
SUBROUTINE TUBCTS
C
C THIS SUBROUTINE PERFORMS A STREAMTUBE ANALYSIS OF THE DIFFUSING
C SECTION IMMEDIATELY FOLLOWING THE COMPRESSOR CUTLET
C
COMMON/B2/ RAC(16),DELTA(2,50),EE1(2),UJ(15),THA,THB,THS,PRES(50),
1NGC,AKAY,ZZR,ZZGAMA,BETA1,BETA2,XMVA,XMVB,XMVS, ZZCP, IDIF
2,HSEP ,FLAREA(50),AREA(50)
COMMON/B4/DPREF
COMMON/B12/ X(120),CA(120),CB(120),SA(50),SB(50),
1NRECT,NXDIF,NDIFF,NSNCUT,NXDIF1,NXDIF2,NXDIFA,NXDIFB,NTUBE,
2PRESIN, BLOCK(50),ABLOCK,SHAPEH(2,50),
3VPDATA(15),RDATA(15),NUPR,ARDTA(200),XLNDDTA(20),EFDTA(200),NCDF,
4NYDF,NZDF,EIDTA, NXDF,AREF,WIDT+1,
5XMACH,RHOREF,EFD(3)
COMMON/B126/AF2,TAN1A,TAN1B,PAN1A,PAN1B, AFA,AFB,PREDM,STAGT
1,IBL,STPREF,PARTA,PNRTB,DPHSNT,COMLOS
COMMON/B12678/JTAPE ,IPRINT
COMMON/BZERO/ ALFA(50),ALFB(50),ALFC(50),VEL(2,50),RO(2,50),
1ALFC(50),ASTAR(15),STAGP(15),RHO(15),Y(11),YY(11),UJY(11),AR(2),
2DUMMY(70),ALFG(50)
COMMON/B2TBCS/SHP(2),THET(2),ROJ(2),VELJ(2),SUMXJ(4)
COMMON/B2TUB/ XMTB(15),ATUBE(15),ALPHA(15),CAL(15),CBL(15)
C
2 FORMAT(91H SOLUTION FAILED TO CONVERGE IN SUBROUTINE TUBEIN. SOLUT
2ICN CONTINUED USING EMPIRICAL DATA.)
3 FORMAT(91H SOLUTION FAILED TO CONVERGE IN SUBROUTINE TUBANL. SOLUT
1ICN CONTINUED USING EMPIRICAL DATA.)
7 FORMAT(86H SOLUTION FAILED TO CONVERGE AFTER 40 CYCLES. SOLUTION C
1CNTINUED USING EMPIRICAL DATA./54H THE LAST CALCULATED BOUNCARY LAT
2YER PARAMETERS ARE....)
10 FORMAT(18H1*** ERROR MESSAGE)
11 FORMAT(1X/////18H *** ERROR MESSAGE)
21 FORMAT(1H149X3(2H- ),7HRESULTS3(2H -)/////21HREFERENCE CCADITION
1S/1X20(1H-)/15HREFERENCE AREA13X1H=F10.3,6H SQ FT/19H REFERENCE V
2ELOCITY9X1H=F10.1,11H FT PER SEC/18H INLET MACH NUMBER10X1H=F10.3/
322H REFERENCE MACH NUMBER6X1H=F10.3/29H REFERENCE DYNAMIC PRESSURE
4 =F10.2,4H PSI)
22 FORMAT(115H0THE DIFFUSER TREATMENT USED IN THIS PROGRAM BECOMES INT
1CREASINGLY INACCURATE AT INLET MACH NUMBERS GREATER THAN 0.7)
C
C SET UP GEOMETRIC VARIABLES
C
LN=1
IHLC=1
GC TO (101,103),NRECT
101 DO 102 I=1,NXDIF
AREA(I)=3.14159*(CB(I)**2-CA(I)**2)
B=(1.-ABLOCK)*BLOCK(I)
DELTA(2,I)=CB(I)*(1.-SQRT(1.-B*(1.-(CA(I)/CB(I))**2)))
102 DELTA(1,I)=CA(I)*(-1.+SQRT(1.+(BLOCK(I)-B)*((CB(I)/CA(I))**2-1.)))
AR(1)=3.14159*(SA(NXDIF+1)**2-CA(NXDIF+1)**2)
AR(2)=3.14159*(CB(NXDIF+1)**2-SB(NXDIF+1)**2)
GC TO 106
103 DO 104 I=1,NXDIF
AREA(I)=CB(I)-CA(I)
DELTA(2,I)=AREA(I)*BLOCK(I)*(1.-ABLOCK)
104 DELTA(1,I)=AREA(I)*BLOCK(I)*ABLOCK
AR(1)=SA(NXDIF+1)-CA(NXDIF+1)

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TCTC01C
TCTC0020
TBCT003C
TBCT0040
TBCT0050
TBCT0060
TBCT0070
TBCT0080
TCTC0090
TCTC0100
TCTC0110
TBCT012C
TBCT0130
TCTC0140
TCTC015C
TBCT0160
TCTC0170
TBCT0180
TBCT0190
TCTC020C
TBCT021C
TCTC0220
TBCT0230
TBCT0240
TBCT025C
TBCT0260
TCTC0270
TBCT0280
TCTC029C
TCTC0300
TBCT0310
TBCT032C
TBCT0330
TBCT0340
TBCT0350
TBCT0360
TBCT037C
TCTC0380
TCTC0390
TBCT0400
TBCT041C
TCTC0420
TCTC0430
TCTC0440
TBCT0450
TCTC0460
TCTC0470
TCTC0480
TCTC049C
TCTC050C
TCTC0510
TCTC0520
TCTC053C
TCTC0540
TCTC0550
TCTC0560
TCTC0570
TCTC0580
TCTC0590

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AR(2)=CB(NXDIF+1)-SB(NXDIF+1)
106 DC 108 I=1,NXDIF
ALFG(I)=0.
FLAREA(I)=AREA(I)*(1.-BLOCK(I))
CAL(I)=CA(I)+DELTA(1,I)
108 CBL(I)=CB(I)-DELTA(2,I)
CALL SLCPE(X,CA,1,NXDIF,ALFC,NXDIF+1)
CALL SLCPE(X,CB,1,NXDIF,ALFD,NXDIF+1)
DC 1080 I=2,NXDIF
DC=1
DE=1
IF(ALFC(I).LE.0.) DC=-1
IF(ALFD(I).LE.0.) DE=-1
ALFC(I)=DD*ATAN(CC*ALFC(I))
1080 ALFD(I)=DE*ATAN(DE*ALFD(I))
C
C CALCULATE INLET PROPERTIES
C
DC 1060 J=1,NUPR
1060 RDATA(J)=(RDATA(J)*(CBL(1)-CA(1))+CA(1)-CAL(1))/(CBL(1)-CAL(1))
CALL TUBEIN( IBL,NRECT,FLAREA(1),CAL(1),CPL(1),NTUBE,AF2,PRESIN,STAT
1GT,VPDATA,RDATA,NUPR,UJ,ASTAR,STAGP,RHO,XMTB,STPREF,1)
PRES(1)=PRESIN
IF( IBL) 1081,1082,1081
1082 WRITE(JTAPE,11)
WRITE(JTAPE,2)
RETURN
1081 DYHD=0.
RH=0.
DC 1084 J=1,NTUBE
DYHD=DYHD+XMTB(J)/AF2*UJ(J)
1084 RH=RH+XMTB(J)/AF2*RHO(J)
DYHD=DYHD**2*RH/2./32.
VEL(2,1)=UJ(NTUBE)
VEL(1,1)=UJ(1)
RC(2,1) = RHO(NTUBE)
RC(1,1) = RHO(1)
ALFA(1)=0.
ALFB(1)=0.
DC 1085 J=1,2
SUMXJ(J)=0.
SHP(J)=SHAPEH(J,1)
THET(J)=DELTA(J,1)/SHAPEH(J,1)
RCJ(J)=RC(J,1)
1085 VELJ(J)=VEL(J,1)
C
C CALCULATE REFERENCE PROPERTIES
C
ASS=FLAREA(1)*0.532*STPREF/AF2/SQRT(STAGT)
CALL GASTBL(ASS,TSS,PSS,YMACH,1,IBL,ZZR,ZZGAMA)
ASS=AREF*ASS/FLAREA(1)
IF(NRECT.EQ.2) ASS=ASS/WIDTH1
CALL GASTBL(ASS,TSS,PSS,XMACH,1,IBL,ZZK,ZZGAMA)
DPREF=STPREF*(1.0-PSS)/144.
UREF=XMACH*SQRT(ZZGAMA*ZZR*32.2*STAGT*TSS)
IF(IPRINT.EQ.3) GO TO 1083
WRITE OUT REFERENCE CONDITIONS
C
C
WRITE(JTAPE,21)AREF,UREF,YMACH,XMACH,DPREF
IF(YMACH.GE..7)WRITE(JTAPC,22)

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TBCT0600
TBCT0610
TBCT0620
TBCT0630
TBCT0640
TBCT0650
TBCT0660
TBCT0670
TBCT0680
TBCT0690
TBCT0700
TBCT0710
TBCT0720
TBCT0730
TBCT0740
TBCT0750
TBCT0760
TBCT0770
TBCT0780
TBCT0790
TBCT0800
TBCT0810
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TBCT0980
TBCT0990
TBCT1000
TBCT1010
TBCT1020
TBCT1030
TBCT1040
TBCT1050
TBCT1060
TBCT1070
TBCT1080
TBCT1090
TBCT1100
TBCT1110
TBCT1120
TBCT1130
TBCT1140
TBCT1150
TBCT1160
TBCT1170
TBCT1180
TBCT1190

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*.....*.....*.....*.....*.....*.....*.....*.....*.....*
1083 DPREF=CPREF*144.
C
    IF(NXDIF-1) 5000,5000,109
C
    ITERATION LOOP STARTS HERE
C
109 ALFA(1)=0.
    ALFB(1)=0.
    DC 110 I=2,NXDIF
    ALFA(I)=(CAL(I)-CAL(I-1))/(X(I)-X(I-1))
    ALFB(I)=(CBL(I)-CBL(I-1))/(X(I)-X(I-1))
    DD=1
    DE=1
    IF(ALFA(I).LE.0.) DD=-1
    IF(ALFB(I).LE.0.) DE=-1
    ALFA(I)=DD*ATAN(CC*ALFA(I))
110 ALFB(I)=DE*ATAN(DE*ALFB(I))
115 CALL TUBANL(IPL, LN, ALFA, ALFB, IHLD, NXDIF, PRES, ASTAR, RHO,
    1STAGP, UJ, VEL, RO, FLAREA, ATUBE, STAGT, ALPHA, NTUBE)
    IF(1BL) 120,120,130
120 WRITE(JTAPE,11)
    WRITE(JTAPE,3)
    RETURN
130 CALL NEWRAD (IBL,X,VEL,RO,DELTA,SPAPEN,1,NXDIF,IHLD,CB,CA,
    1ALFC,ALFD,HSEP,NRECT,ALFG)
    IF(1BL) 135,135,5000
135 LA=LN+1
    IF(LN=40) 140,140,137
137 WRITE(JTAPE,10)
    WRITE(JTAPE,7)
    GC TO 200
140 DC 145 I=2,NXDIF
    CAL(I)=CA(I)+DELTA(1,I)*CCS(ALFC(I))
    CBL(I)=CB(I)-DELTA(2,I)*COS(ALFD(I))
    GC TO (141,144),NRECT
141 BLOCK(I)=1.-((CBL(I)**2-CAL(I)**2)/(CB(I)**2-CA(I)**2))
    GC TO 145
144 BLOCK(I)=1.-((CBL(I)-CAL(I))/(CB(I)-CA(I)))
145 FLAREA(I)=AREA(I)*(1.-BLOCK(I))
    GC TO 109
C
C    CALCULATE OUTLET VELOCITY PROFILE
C
5000 RAD(1)=CAL(NXDIF)
    GC TO (510,515),NRECT
510 DO 512 J=1,NTUBE
512 RAD(J+1)=SQRT(RAD(J)**2.+ATUBE(J)*COS(ALPHA(J))/3.14159)
    GC TO 518
515 DC 517 J=1,NTUBE
517 RAD(J+1)=RAD(J)+ATUBE(J)*COS(ALPHA(J))
518 DC 520 J=1,NTUBE
520 RAD(J)=(RAD(J)+RAD(J+1))/2.
    Y(1)=CAL(NXDIF)
    DC 525 I=2,11
525 Y(I)=CAL(NXDIF)+(CBL(NXDIF)-CAL(NXDIF))*0.1*(FLCAT(I)-1.)
    DC 530 I=1,11
    YI=Y(I)
    CALL I1AP1(YI,ANS,RAD,UJ,NTUBE)
    UJY(I)=ANS
    YY(I)=(Y(I)-CA(NXDIF))/(CB(NXDIF)-CA(NXDIF))

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TBCT1200
TBCT1210
TBCT1220
TBCT1230
TBCT1240
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TBCT1280
TBCT1290
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TBCT1310
TBCT1320
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TBCT1380
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TBCT1480
TBCT1490
TBCT1500
TBCT1510
TBCT1520
TBCT1530
TBCT1540
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TBCT1560
TBCT1570
TBCT1580
TBCT1590
TBCT1600
TBCT1610
TBCT1620
TBCT1630
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TBCT1680
TBCT1690
TBCT1700
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TBCT1760
TBCT1770
TBCT1780
TBCT1790

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..........*.....*.....*.....*.....*.....*.....*.....*

\$IBFTC TBST
SUBROUTINE TUBSTAC
C
C
C

THIS SUBROUTINE PREPARES DATA FOR SUBROUTINE TUBSTA

TBSTCC01
TBST0002
TBSTCC03
TBST0004
TBST0005
TBST0006
TBST0007
TBST0008
TBST0009
TBST0010
TBST0011
TBST0012
TBST0013
TBST0014
TBST0015
TBST0016
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TBST0018
TBST0019
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TBST0021
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TBST0024
TBST0025
TBST0026
TBST0027
TBST0028
TBST0029
TBST0030
TBST0031
TBST0032
TBST0033
TBST0034
TBST0035
TBSTCC36
TBST0037
TBST0038
TBST0039
TBSTCC40
TBST0041
TBST0042
TBST0043
TBST0044
TBST0045
TBST0046
TBST0047
TBST0048
TBST0049
TBST0050
TBST0051
TBST0052
TBST0053
TBST0054
TBST0055
TBST0056
TBSTCC57
TBST0058
TBST0059

CCMCON/R2/ RAD(16), DELTA(2,50), EE1(2), UJ(15), THA, THB, THS, PRES(50),
 1NGC, NWAY, ZZR, ZZGAMA, BETA1, BETA2, XMVA, XMVB, XMVS, ZZCP, IDIF
 2, HSEP, FLAREA(50), AREA(50)
 CCMCON/R12/ X(120), CA(120), CB(120), SA(50), SB(50),
 1NRECT, NXDIF, NDIFF, NSNGUT, NXDIF1, NXDIF2, NXCIFA, NXDIFB, NTUBE,
 2PRESIN, ELCK(50), ABLCK, SHAPEH(2,50),
 3VFDATA(15), RDATA(15), NUPR, ARCTA(200), XLNDA(20), EFDTA(200), NCDF,
 4NYDF, NZDF, EIDTA, NXDF, AREF, WIDTH-1,
 5XMACH, RHCREF, EFCT(3)
 CCMCON/BZERO/ ALPA(50), ALPB(50), ALPC(50), ALPD(50), DUMMY(400)
 CCMCON/R2TBDS/ ALFA(2,50), AL(2,2,50), WIL(2,50), WCL(2,50), WI(2,50),
 1WC(2,50), ARR(2,50), DELT(2,2), SHAPH(2,2), NX(2), NXDD(2), ARF(2,50),
 1SHPP(2,2), THETT(2,2), SUMXJJ(2,2), ROJJ(2), VELJJ(2)
 CCMCON/R2TBDS/SHP(2), THET(2), ROJ(2), VELJ(2), SUMXJ(4)

C
C
C

CALCULATE GEOMETRIC VARIABLES AND INPUT PARAMETERS

NX(1)=NXDIF1
 NX(2)=NXDIF2
 NXDD(1)=NXCIFA
 NXDD(2)=NXDIFB
 DELT(1,1)=DELTA(1,NXDIF)
 DELT(1,2)=0.
 DELT(2,1)=0.
 DELT(2,2)=DELTA(2,NXDIF)
 SHAPH(1,1)=SHAPEH(1,NXDIF)
 SHAPH(1,2)=1.4
 SHAPF(2,1)=1.4
 SHAPH(2,2)=SHAPEH(2,NXDIF)
 SHPP(1,1)=SHAPEH(1,1)
 SHPP(1,2)=1.4
 SHPP(2,1)=1.4
 SHPP(2,2)=SHAPEF(2,1)
 THETT(1,1)=DELTA(1,1)/SHAPEF(1,1)
 THETT(1,2)=0.
 THETT(2,1)=0.
 THETT(2,2)=DELTA(2,1)/SHAPEH(2,1)
 SUMXJJ(1,1)=SUMXJ(3)
 SUMXJJ(1,2)=0.
 SUMXJJ(2,1)=0.
 SUMXJJ(2,2)=SUMXJ(4)
 RCJJ(1)=RCJ(1)
 RCJJ(2)=RCJ(2)
 VELJJ(1)=VELJ(1)
 VELJJ(2)=VELJ(2)
 CALL SLCPE(X,CA,NXDIF,NXDIFA,ALPA,NXDIFA+1)
 CALL SLOPE(X,CB,NXDIF,NXDIFB,ALPB,NXDIFB+1)
 CALL SLOPE(X,SA,NXDIF+2,NXDIFA,ALPC,NXDIFA+1)
 CALL SLOPE(X,SB,NXDIF+2,NXDIFB,ALPD,NXDIFB+1)
 NXDF1=NXDIF+1
 DO 119 I=NXCIF,NXDF1
 ALPC(I)=ALPA(I)
 119 ALPD(I)=ALPB(I)
 SA(NXDIF)=CA(NXDIF)+SA(NXCIF+1)-CA(NXCIF+1)

```

SB(NXDIF)=SB(NXCIF+1)-CB(NXDIF+1)+CB(NXDIF)
DC 120 I=NXCIF,NXCIFA
DD=1
DE=1
IF(ALPA(I).LE.0.) DD=-1
IF(ALPC(I).LE.0.) DE=-1
ALFA(1,I)=(CD*ATAN(CD*ALPA(I))+DE*ATAN(CE*ALPC(I)))/2.
WI(1,I)=CA(I)
WC(1,I)=SA(I)
WIL(1,I)=WI(1,I)+DELTA(1,NXCIF)/COS(ALFA(1,I))
WOL(1,I)=WC(1,I)
AL(1,1,I)=CD*ATAN(CD*ALPA(I))-ALFA(1,I)
120 AL(1,2,I)=DE*ATAN(CE*ALPC(I))-ALFA(1,I)
DO 121 I=NXCIF,NXDIFB
DD=1
DE=1
IF(ALPB(I).LE.0.) CD=-1
IF(ALPD(I).LE.0.) DE=-1
ALFA(2,I)=(DD*ATAN(DD*ALPB(I))+DE*ATAN(DE*ALPD(I)))/2.
WI(2,I)=SB(I)
WC(2,I)=CB(I)
WIL(2,I)=WI(2,I)
WOL(2,I)=WC(2,I)-DELTA(2,NXCIF)/COS(ALFA(2,I))
AL(2,2,I)=DD*ATAN(DD*ALPB(I))-ALFA(2,I)
121 AL(2,1,I)=DE*ATAN(CE*ALPD(I))-ALFA(2,I)
DC 130 K=1,2
NXD=NXDD(K)
DC 130 I=NXCIF,NXD
GC TO (125,127),NRECT
125 ARR(K,I)=3.14159*(WC(K,I)**2-WI(K,I)**2)*COS(ALFA(K,I))
ARF(K,I)=3.14159*(WOL(K,I)**2-WIL(K,I)**2)*COS(ALFA(K,I))
GO TC 130
127 ARR(K,I)=(WO(K,I)-WI(K,I))*COS(ALFA(K,I))
ARF(K,I)=(WOL(K,I)-WIL(K,I))*COS(ALFA(K,I))
130 CONTINUE
GC TO (131,132),NRECT
131 ARR(1,NXDIFA)=3.14159*(SA(NXDIFA)**2-CA(NXDIFA)**2)
ARR(2,NXDIFB)=3.14159*(CB(NXDIFB)**2-SB(NXDIFB)**2)
GC TC 133
132 ARR(1,NXDIFA)=SA(NXDIFA)-CA(NXDIFA)
ARR(2,NXDIFB)=CB(NXDIFB)-SB(NXDIFB)
133 CONTINUE
RETURN
END

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TBST0C60
TBST0061
TBST0062
TBST0063
TBST0C64
TBST0065
TBST0066
TBST0067
TBST0C68
TBST0069
TBST0070
TBST0071
TBST0C72
TBST0073
TBST0074
TBST0075
TBST0C76
TBST0077
TBST0078
TBST0079
TBST0C80
TBST0081
TBST0082
TBST0083
TBST0084
TBST0085
TBST0086
TBST0087
TBST0088
TBST0089
TBST0C90
TBST0091
TBST0092
TBST0C93
TBST0094
TBST0095
TBST0096
TBST0097
TBST0098
TBST0099
TBST0100
TBST0101
TBST0102
TBST0103


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*.....*.....*.....*.....*.....*.....*.....*.....*.....*
GC TC 200 TBA10600
1971 ARF(1,NXDIF)=(WOL(1,NXDIF)-WIL(1,NXDIF))*COS(ALFA(1,NXDIF)) TBA10610
      ARF(2,NXDIF)=(WCL(2,NXDIF)-WIL(2,NXDIF))*COS(ALFA(2,NXDIF)) TBA10620
C TBA10630
C START OF CC LCOP FOR TWO ANNULI TBA10640
C TBA10650
200 DC 500 K=1,2 TBA10660
      IHLD=NXDIF TBA10670
      NXX=NX(K) TBA10680
      NXD=NXCC(K) TBA10690
      DC 2000 I=NXDIF,NXX TBA10700
      X(I+1)=XX(I)+(X(I+1)-X(I))/CCS(ALFA(K,I)) TBA10710
      DELTA(1,I)=DELTA(K,1) TBA10720
      DELTA(2,I)=DELTA(K,2) TBA10730
2000 CCNTINUE TBA10740
      SHAPEH(1,NXDIF)=SHAPH(K,1) TBA10750
      SHAPEH(2,NXDIF)=SHAPH(K,2) TBA10760
      WILX=WIL(K,NXDIF)*COS(ALFA(K,NXDIF)) TBA10770
      WOLX=WCL(K,NXDIF)*COS(ALFA(K,NXDIF)) TBA10780
      LN=1 TBA10790
      DC 210 J=1,NTUBE TBA10800
      RD(J)=RAD(J)*CCS(ALFA(K,NXDIF)) TBA10810
210 RD(J)=(RD(J)-WILX)/(WCLX-WILX) TBA10820
      CALL TUBEIN(1BL,NRECT,ARF(K,NXDIF),WILX,WOLX,NTUBE
      1,AF(K),PRES(NXDIF),STAGT,UJ,RC,NTUBE,UJK,ASTAR,STAGP,RHO,XMTB,
      2PRES(NXDIF),0) TBA10830
      IF(1BL) 215,215,220 TBA10840
215 WRITE(JTAPE,10) TBA10850
      WRITE(JTAPE,1) TBA10860
      RETURN TBA10870
220 DC 225 I=NXDIF,NXX TBA10880
      ARK(I)=ARF(K,I) TBA10890
      ALA(I)=AL(K,1,I) TBA10900
225 ALB(I)=AL(K,2,I) TBA10910
      VFL(1,NXDIF)=UJK(1) TBA10920
      VFL(2,NXDIF)=UJK(NTUBE) TBA10930
      RC(1,NXDIF)=RHO(1) TBA10940
      RC(2,NXDIF)=RHO(NTUBE) TBA10950
      IF(K.EQ.2) GO TO 2250 TBA10960
      RCJ(1)=ROJJ(1) TBA10970
      RCJ(2)=RHO(NTUBE) TBA10980
      VELJ(1)=VELJJ(1) TBA10990
      VELJ(2)=UJ(NTUBE) TBA11000
      GC TC 2251 TBA11010
2250 RCJ(1)=RHC(1) TBA11020
      RCJ(2)=ROJJ(2) TBA11030
      VELJ(1)=UJ(1) TBA11040
      VFLJ(2)=VELJJ(2) TBA11050
2251 DC 2252 J=1,2 TBA11060
      SUMXJ(J)=SUMXJJ(K,J) TBA11070
      SHP(J)=SHPP(K,J) TBA11080
2252 THET(J)=THETT(K,J) TBA11090
      SUP=0. TBA11100
      SUMA=0. TBA11110
      DO 226 J=1,NTUBE TBA11120
      SUP=SUP+XMTB(J)/RHC(J) TBA11130
226 SUMA=SUMA+XMTB(J)*UJK(J)/RHO(J) TBA11140
      RHR=AF(K)/SUM TBA11150
      BTA=SUMA*ARR(K,NXDIF)/SUM**2 TBA11160
      DYHD=(SUMA/SUM)**2*RHR/32./2. TBA11170
      TBA11180
      TBA11190

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*.....*.....*.....*.....*.....*.....*.....*.....*.....*
C
C   START OF ITERATION LOOP
C
227 CALL TUBANL(IPL, LN, ALA, ALB, IHLD, NXX, PRES, ASTAR, RHC,
  1STAGP, UJK, VEL, RC, ARK, ATUBE, STAGT, ALPHA, NTUBE)
  IF(IPL) 228, 228, 230
228 WRITE(JTAPE, 10)
  WRITE(JTAPE, 2)
  RETURN
230 DC 2300 I=NXDIF, NXX
  ALA(I)=AL(K, 1, I)
  ALB(I)=AL(K, 2, I)
  ARK(I)=ALFA(K, I)
  YAL(I)=WI(K, I)*COS(ALFA(K, I))
2300 YBL(I)=WC(K, I)*COS(ALFA(K, I))
  CALL NEWRAD(IPL, XX, VEL, RO, CELTA, SHAPEF, NXDIF, NXX, IHLD, YBL, YAL,
  1ALA, ALB, HSEP, NRECT, ARK)
  IF(IPL) 250, 250, 320
250 IF(LN-40) 255, 270, 270
255 LN=LN+1
257 DC 260 I=NXDF1, NXX
  WIL(K, I)=WI(K, I)+DELTA(1, I)*CCS(AL(K, 1, I))/COS(ALFA(K, I))
260 WOL(K, I)=WC(K, I)-DELTA(2, I)*COS(AL(K, 2, I))/COS(ALFA(K, I))
  GO TO (261, 263), NRECT
261 DC 262 I=NXDIF, NXX
  ARK(I)=3.14159*(WOL(K, I)**2-WIL(K, I)**2)*COS(ALFA(K, I))
262 BLOCK(I)=1.-ARK(I)/ARR(K, I)
  GO TO 265
263 DC 264 I=NXDIF, NXX
  ARK(I)=(WOL(K, I)-WIL(K, I))*COS(ALFA(K, I))
264 BLOCK(I)=1.-ARK(I)/ARR(K, I)
265 DC 266 I=NXDIF, NXX
  YAL(I)=WIL(K, I)
266 YBL(I)=WOL(K, I)
  CALL SLOPE(XX, YAL, NXDIF+1, NXX, ALA, NXX)
  CALL SLCPE(XX, YBL, NXDIF+1, NXX, ALB, NXX)
  DC 267 I=NXDF1, NXX
  DD=1
  DE=1
  IF(ALA(I).LE.0.) DC=-1
  IF(ALB(I).LE.0.) DE=-1
  ALA(I)=DD*ATAN(CD*ALA(I))-ALFA(K, I)
267 ALB(I)=DE*ATAN(CE*ALB(I))-ALFA(K, I)
  GO TO 227
270 WRITE(JTAPE, 10)
  WRITE(JTAPE, 7)
  GO TO 450
C
C   CALCULATE OUTLET PROPERTIES
C
320 RHM=0.
  XMV2=0.
  XAV=0.
  DC 321 J=1, NTUBE
  XMV2=XMV2+UJK(J)**2*ATUBE(J)*COS(ALPHA(J))
321 XAV=XAV+UJK(J)*ATUBE(J)*COS(ALPHA(J))
  XMV2=XMV2/ARR(K, NXX)
  XAV=XAV/ARR(K, NXX)
  BT =XMV2/XAV**2
  RHM=AF(K)/XAV/ARR(K, NXX)

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TBA11200
TBA11210
TBA11220
TBA11230
TBA11240
TBA11250
TBA11260
TBA11270
TBA11280
TBA11290
TBA11300
TBA11310
TBA11320
TBA11330
TBA11340
TBA11350
TBA11360
TBA11370
TBA11380
TBA11390
TBA11400
TBA11410
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TBA11670
TBA11680
TBA11690
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TBA11780
TBA11790

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*.....*.....*.....*.....*.....*.....*.....*.....*.....*
  ARAT= ARR(K,NXD)/ARR(K,NXX)
  PRES(NXD) = PRES(NXX)+ (1.+1./ARAT)*(BT-1./ARAT)*RHM*XAV**2/
164.4
C
C   CALCULATE TEMPERATURE AT INLET TO ANNULI AND TOTAL PRESSURE LOSS
C
  B=1.
  C=-STAGT
  A=(AF(K)*ZZR/ARR(K,NXD)/PRES(NXD))**2/(2.*ZZCP*32.)
  TANA=(-B+SQRT(B*B-4.*A*C))/2./A
  PNRT=PRES(NXD)*(STAGT/TANA)**(ZZGAMA/(ZZGAMA-1.))
  PNRT=PNRT-PLOSS(K)
  ASS=AF(K)*SQRT(STAGT)/(0.532*PNRT)
  ASS=ARR(K,NXD)/ASS
  CALL GASTBL(ASS,RAT,RAP,XMACH,1,IBL,ZZR,ZZGAMA)
  PRES(NXD)=RAP*PNRT
  TANA=STAGT*RAT
  DELTP=(STPREF-PNRT)/STPREF
C
  GO TO (323,324),K
323 PAN1A=PRES(NXD)
  TAN1A=TANA
  PNRTA=PNRT
  GO TO 400
324 PAN1B=PRES(NXD)
  TAN1B=TANA
  PNRTB=PNRT
400 IF(IPRINT) 500,500,410
C
C   CALCULATE DIFFUSER PERFORMANCE
C
410 CPACT=(PRES(NXX)-PRES(NXDIF))/DYHD
  AR=ARR(K,NXX)/ARR(K,NXDIF)
  IF(AR-1.) 4100,4101,4100
4101 CPIDL=0.
  EFECTN=1.
  GO TO 420
4100 CPIDL=1.-1./AR/AR
  EFECTN=CPACT/CPIDL
C
C   CALCULATE DIFFUSER PERFORMANCE ALLOWING FOR MIXING
C
420 CPCT=(PRES(NXC)-PRES(NXDIF))/CYHD
  AR=ARR(K,NXC)/ARR(K,NXDIF)
  BT=BTA
4200 CPID=(2.*(BT-1.)+1.-1./AR**2)/BT**2
  EFECT=CPCT/CPID
430 CONTINUE
C
C   PRINT OUT RESULTS
C
  CALL DOUTP1(NSNOUT,CPIDL,CPACT,EFECTN,CPID,CPCT,EFECT,1,K,
  IARR(K,NXDIF)/ARR(K,NXDIF+1),DELTP)
450 DO 460 I=NXDIF,NXX
  WID=1.
  IF(NRECT.EQ.2) WID=WICHTH1
460 ARRK(I)=ARR(K,I)*WID
490 CALL NEWRI(PRES,ARRK,BLOCK)
  IF(IBL) 500,900,500
500 CCNTINUE

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TBA11800
TBA11810
TBA11820
TBA11830
TBA11840
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TBA11880
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TBA11930
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TBA11960
TBA11970
TBA11980
TBA11990
TBA12000
TBA12010
TBA12020
TBA12030
TBA12040
TBA12050
TBA12060
TBA12070
TBA12080
TBA12090
TBA12100
TBA12110
TBA12120
TBA12130
TBA12140
TBA12150
TBA12160
TBA12170
TBA12180
TBA12190
TBA12200
TBA12210
TBA12220
TBA12230
TBA12240
TBA12250
TBA12260
TBA12270
TBA12280
TBA12290
TBA12300
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TBA12320
TBA12330
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TBA12360
TBA12370
TBA12380
TBA12390

156

C

900 RETURN
END

TBA12400
TBA12410
TEA12420

YOUR CARD TCTAL IS ---

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$IBFTC TBFW
SUBROUTINE TUBFW1
THIS SUBROUTINE CALCULATES THEORETICAL FLOW SPLITS
USING DATA FROM SUBROUTINE TURCTS.
COMMON/B2/ RAD(16), DELTA(2,50), EE1(2), UJ(15), THA, THB, THS, PRES(50),
1NGO, NWAY, ZZR, ZZGAMA, BETA1, BETA2, XMVA, XMVB, XMVS, ZZCP, IDIF
2, HSEP, FLAREA(50), AREA(50)
COMMON/B12/ X(120), CA(120), CB(120), SA(50), SB(50),
1NRECT, NXDIF, NDIFF, NSNGUT, NXDIF1, NXDIF2, NXDIFA, NXDIFB, NTUBE,
2PRESIN, BLOCK(50), ABLOCK, SHAPEH(2,50),
3VPDATA(15), RDATA(15), NUPR, ARDTA(200), XLNDDTA(20), EFDTA(200), NCDF,
4NYDF, NZDF, E1DTA, NXDF, AREF, WIDTH1,
5XMACH, RHOREF, EFDT(3)
COMMON/B126/AF2, TAN1A, TAN1B, PAN1A, PAN1B, AFA, AFB, PREDM, STAGT
1, IBL, STPREF, PNRTA, PNRTB, DPHSNT, DOMLOS
COMMON/B12678/JTAPE, IPRINT
COMMON/B2TUB/ XMTB(15), ATUBE(15), ALPHA(15), CAL(15), CBL(15)
4 FORMAT(96H SOLUTION FAILED TO CALCULATE THEORETICAL FLOW AREAS FOR
1A GIVEN FLCW SPLIT. SOLUTION TERMINATED.)
10 FORMAT(18H1*** ERROR MESSAGE)
THA=0.
THB=0.
BETA1=0.
BETA2=0.
XMVA=0.
XMVB=0.
XMVS=0.
SUM=0.
INNER ANNULUS
DO 600 J=1, NTUBE
THA=THA+ATUBE(J)*COS(ALPHA(J))
BETA1=BETA1+ATUBE(J)*UJ(J)*UJ(J)*COS(ALPHA(J))
XMVA=XMVA+UJ(J)*ATUBE(J)*COS(ALPHA(J))
SUM=SUM+XMTB(J)
JK=J
IF(SUM-AFA) 600, 610, 604
600 CONTINUE
WRITE(JTAPE, 10)
WRITE(JTAPE, 4)
STOP
604 J=JK
THA=THA-((SUM-AFA)/XMTB(J))*ATUBE(J)*COS(ALPHA(J))
BETA1=BETA1-((SUM-AFA)/XMTB(J))*ATUBE(J)*UJ(J)*UJ(J)*COS(ALPHA(J))
XMVA=XMVA-((SUM-AFA)/XMTB(J))*ATUBE(J)*UJ(J)*COS(ALPHA(J))
OUTER ANNULUS
610 SUM=0.
DO 620 J=1, NTUBE
JJ=NTUBE+1-J
THB=THB+ATUBE(JJ)*COS(ALPHA(JJ))
BETA2=BETA2+ATUBE(JJ)*UJ(JJ)*UJ(JJ)*COS(ALPHA(JJ))
XMVB=XMVB+UJ(JJ)*ATUBE(JJ)*COS(ALPHA(JJ))
SUM=SUM+XMTB(JJ)

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TBFW0001
TBFW0002
TBFW0003
TBFW0004
TBFW0005
TBFW0006
TBFW0007
TBFW0008
TBFW0009
TBFW0010
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TBFW0012
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TBFW0047
TBFW0048
TBFW0049
TBFW0050
TBFW0051
TBFW0052
TBFW0053
TBFW0054
TBFW0055
TBFW0056
TBFW0057
TBFW0058
TBFW0059

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	IF(SUM-AFB) 620,630,625	TBFW0060
620	CONTINUE	TBFW0061
	WRITE(JTAPE,10)	TBFW0062
	WRITE(JTAPE,4)	TBFW0063
	STOP	TBFW0064
C		TBFW0065
625	THB=THE-(SUM-AFB)/XMTB(JJ)*ATUBE(JJ)*COS(ALPHA(JJ))	TBFW0066
	BETA2=BETA2-(SUM-AFB)/XMTB(JJ)*ATUBE(JJ)*UJ(JJ)*UJ(JJ)*COS(ALPHA(JJ))	TBFW0067
	1 J)	TBFW0068
	XMVB=XMVB-(SUM-AFB)/XMTB(JJ)*ATUBE(JJ)*COS(ALPHA(JJ))*UJ(JJ)	TBFW0069
C		TBFW0070
C	FLOW INTO THE SNOOT	TBFW0071
C		TBFW0072
630	THS=FLAREA(NXDIF)-THB-THA	TBFW0073
	IF(THS)635,635,640	TBFW0074
635	THS=0.000001	TBFW0075
640	CONTINUE	TBFW0076
C		TBFW0077
C	ALLOW FOR BOUNDARY LAYER BLOCKAGE	TBFW0078
C		TBFW0079
	GO TO (650,660),NRECT	TBFW0080
650	THA=THA+(CAL(NXDIF)**2.-CA(NXDIF)**2.)*3.14159	TBFW0081
	THB=THB+(CB(NXDIF)**2.-CBL(NXDIF)**2.)*3.14159	TBFW0082
	GO TO 680	TBFW0083
660	THA=THA+ CAL(NXDIF)-CA(NXDIF)	TBFW0084
	THB=THB+ CB(NXDIF)-CBL(NXDIF)	TBFW0085
680	CONTINUE	TBFW0086
	XMVA=XMVA/THA	TBFW0087
	XMVB=XMVB/THB	TBFW0088
	BETA1=BETA1/THA/XMVA**2	TBFW0089
	BETA2=BETA2/THB/XMVB**2	TBFW0090
	DO 685 J=1,NTUBE	TBFW0091
685	XMVS=XMVS+UJ(J)*ATUBE(J)*COS(ALPHA(J))	TBFW0092
	XMVS=(XMVS-XMVA*THA-XMVB*THB)/THS	TBFW0093
900	RETURN	TBFW0094
	END	TBFW0095

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$IBFTC TBIN
SUBROUTINE TUBEIN( IBL, NRECT, AREA, YA, YB, NTUBE, XMDOOT, PRES, STAGT,
1 Vpdata, RDATA, NUPR, UJ, ASTAR, STAGP, RHO, XMTB, STP, N)
C
C THIS SUBROUTINE CALCULATES THE INPUT STREAMTUBE PROPERTIES
C FOR THE STREAMTUBE CALCULATION
C
COMMON/ B12678/ JTAPE, IPRINT
DIMENSION VPR(15), Vpdata(15), RDATA(15), UJ(15), ASTAR(15), STAGP(15)
1), ATUBE(15), RAD(16), RHO(15), TJ(15), XMTB(15), ATB(15)
C
1 FORMAT(99H1SOLUTION FAILED TO FIND A CONVERGED VALUE OF U. PROBLEMT
1 TERMINATED. THE LAST TWO VALVES OF U WERE..)
2 FORMAT (1X,6(E12.5))
10 FORMAT(1X/////18H *** ERROR MESSAGE)
11 FORMAT(66H SOLUTION FAILED TO CALCULATE STATIC PRESSURE AT COMPRES
1SOR OUTLET)
C
C CALL GASTBL(D1,D2,D3,D4,-1,D6,ZZR,ZZGAMA)
ZZCP=ZZR*ZZGAMA/(ZZGAMA-1.)
IBL=1
C
C CALCULATE AREA OF EACH STREANTUBE AND NONDIMENSIONAL VELOCITY
C
SUMA=0.
RAD(1)=YA
GO TO (103,106),NRECT
103 AR=3.14159*(YB**2-YA**2)
DO 104 J=1,NTUBE
ATB(J)=AR/FLOAT(NTUBE)
ATUBE(J)=AREA/FLOAT(NTUBE)
SUMA=SUMA+ATB(J)
104 RAD(J+1)=SQRT(SUMA/3.14159+YA**2)
GO TO 110
106 AR=YB-YA
DO 108 J=1,NTUBE
ATB(J)=AR/FLOAT(NTUBE)
ATUBE(J)=AREA/FLOAT(NTUBE)
108 RAD(J+1)=RAD(J)+ATB(J)
110 DO 115 J=1,NTUBE
115 RAD(J)=((RAD(J)+RAD(J+1))/2.-YA)/(YB-YA)
DO 120 J=1,NTUBE
120 CALL I1AP1(RAD(J),VPR(J),RDATA,Vpdata,NUPR)
RHOR=STP/ZZR/STAGT
SUM=0.
DO 121 J=1,NTUBE
121 SUM=SUM+VPR(J)*RHOR*ATUBE(J)
U=XMDOOT/SUM
LC=0
C
C IS STAGNATION PRESSURE GIVEN (N=1) OR STATIC PRESSURE (N=0)
C IF TOTAL PRESSURE GIVEN (N=1) GUESS STATIC PRESSURE
C
IF(N.EQ.0) GO TO 1210
PRES=STP-U*U*RHOR/32./2.
LD=0
1210 SUM=0.
C
C CALCULATE VELOCITY TEMPERATURE AND DENSITY FOR EACH STREAMTUBE

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TBIN0001
TBIN0002
TBIN0003
TBIN0004
TBIN0005
TBIN0006
TBIN0007
TBIN0008
TBIN0009
TBIN0010
TBIN0011
TBIN0012
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TBIN0014
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TBIN0046
TBIN0047
TBIN0048
TBIN0049
TBIN0050
TBIN0051
TBIN0052
TBIN0053
TBIN0054
TBIN0055
TBIN0056
TBIN0057
TBIN0058
TBIN0059

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DO 122 J=1,NTUBE
UJ(J)=VPR(J)*U
TJ(J)=STAGT-UJ(J)**2/(2.*ZZCP*32.)
RHO(J)=PRES/ZZR/TJ(J)
122 SUM=SUM+VPR(J)*RHO(J)*ATUBE(J)
UU=XMDCT/SUM

IS GUESS AT VELOCITY GOOD ENOUGH

IF(ABS((UU-U)/U)-0.00001) 130,130,123
123 U=UU
LC=LC+1
IF(LC-40)1210,1210,124
124 WRITE(JTAPE,1)
WRITE(JTAPE,2)UU,U
IBL=0
RETURN

CALCULATE TOTAL PROPERTIES FOR EACH STREAMTUBE

130 SUM=0.
DO 135 J=1,NTUBE
STAGP(J)=PRES*(STAGT/TJ(J))*(ZZGAMA/(ZZGAMA-1.))
CALL GASTBL(AAS,D2,PRES/STAGP(J),D4,0,IBL,D7,D8)
IF(IBL)900,900,133
133 XMTB(J)=RHO(J)*ATUBE(J)*UJ(J)
135 ASTAR(J)=ATUBE(J)/AAS
IF(N.EC.0) GO TO 900
STPP=0.

CALCULATE WEIGHT MEAN TOTAL PRESSURE

DO 140 J=1,NTUBE
140 STPP=STPP+STAGP(J)*XMTB(J)/XMDOT

IS TOTAL PRESSURE NEAR ENOUGH TO INPUT VALUE

IF(ABS(STPP/STP-1.)-0.0001) 200,200,150

GUESS NEW VALUE OF STATIC PRESSURE

150 PRES=PRES/STPP*STP
LD=LD+1
IF(LD-40)1210,1210,160
160 WRITE(JTAPE,10)
WRITE(JTAPE,11)
IBL=0
RETURN
200 STP=STPP
900 RETURN
END
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TBIN0060
TBIN0061
TBIN0062
TBIN0063
TBIN0064
TBIN0065
TBIN0066
TBIN0067
TBIN0068
TBIN0069
TBIN0070
TBIN0071
TBIN0072
TBIN0073
TBIN0074
TBIN0075
TBIN0076
TBIN0077
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TBIN0080
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TBIN0100
TBIN0101
TBIN0102
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TBIN0105
TBIN0106
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TBIN0108
TBIN0109
TBIN0110
TBIN0111


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SIBFTC TBAN
SUBROUTINE TUBANL( IBL, LN, ALPHA1, ALPHA2, N, NX, PRES, ASTAR, RHO,
1 STAGP, UJ, VEL, RO, AREA, ATUBE, STAGT, ALPHA, NTUBE)
COMMON/812678/ JTAPE, IPRINT
C
C THIS SUBROUTINE PERFORMS A STREAM TUBE ANALYSIS FROM GIVEN
C STARTING CONDITIONS
C
DIMENSION ALPHA1(50), ALPHA2(50), PRES(50), ASTAR(15),
1 RHO(15), STAGP(15), VEL(2, 50), RO(2, 50), AREA(50), ATUBE(15), UJ(15),
2 TJ(15), ALPHA(15), C1(15), C2(15), XMTB(15)
C
2 FORMAT(1X, 9(E12.5, 1X))
3 FORMAT(34H1 ITERATION ON ALPHA AT STATION NO., I3, 10H CYCLE NO., I3, 5T
15H HAS NOT CONVERGED. THE LATEST VALUES OF ALPHA ARE.....)
5 FORMAT(33H ITERATION ON AREA AT STATION NO., I3, 10H CYCLE NO., I3, 67T
1H HAS NOT CONVERGED. THE LATEST VALUES OF GUESSED AREA AND FLOW ART
2EA)
6 FORMAT(11H ARE....., 2(E12.5, 2X))
10 FORMAT(1X///// 18H *** ERROR MESSAGE)
C
CALL GASTBL(D1, D2, D3, D4, -1, D6, ZZR, ZZGAMA)
ZZCP=ZZR*ZZGAMA/(ZZGAMA-1.)
IBL=1
DO 125 J=1, NTUBE
Z= PRES(N)/STAGP(J)
CALL GASTBL(AAS, D2, Z, D4, 0, IBL, D7, D8)
IF( IBL) 900, 900, 121
121 ATUBE(J)=AAS*ASTAR(J)
TJ(J)=STAGT*D2
RHO(J)=PRES(N)/ZZR/TJ(J)
UJ(J)=SQRT(32.*ZZCP*(STAGT-TJ(J))*2.)
XMTB(J)=ATUBE(J)*UJ(J)*RHO(J)
125 ALPHA(J)=ALPHA1(N+1)+(ALPHA2(N+1)-ALPHA1(N+1))*FLOAT(J)/FLOAT(NTUBE
1E)
C
C GUESS PRESSURE AT NEXT STATION DOWN STREAM
C
N1=N+1
DO 300 I=N1, NX
150 PRR= PRES(I-1)
LR=0
2000 DP=10.*10.
DO 201 J=1, NTUBE
C1(J)=RHO(J)*(UJ(J)*ATUBE(J))*2/2./32.
C2(J)=C1(J)/ATUBE(J)**2
201 IF(DP.GE.C2(J)) DP=C2(J)
R=0.
DO 202 J=1, NTUBE
202 R=R+SQRT(C1(J)/C2(J))*COS(ALPHA(J))
R=R-AREA(I)
IF (R) 2020, 2021, 2022
2021 PRES(I)=PRR
GOTO 300
2022 DP=-10.*DP
2020 SUM=ABS(DP/4. )
DP=DP/2.
DO 206 KK=1, 30
R=0.
DO 203 J=1, NTUBE

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203	R=R+SQRT(C1(J)/(C2(J)-DP))*COS(ALPHA(J))	TBAN0060
	R=R-AREA(I)	TBAN0061
	IF (ABS(R/AREA(I))-0.00001)207,207,2040	TBAN0062
2040	IF(R) 204,207,205	TBAN0063
204	DP=DP+SUM	TBAN0064
	GO TO 206	TBAN0065
205	DP=DP-SUM	TBAN0066
206	SUM=SUM/2.	TBAN0067
207	PRES(I)=PRR+DP	TBAN0068
	DO 212 J=1,NTUBE	TBAN0069
	Z=PRES(I)/STAGP(J)	TBAN0070
	CALL GASTBL(AAS,TTO,Z,D4,0,IBL,D7,D8)	TBAN0071
	IF (IBL)900,900,211	TBAN0072
211	ATUBE(J)=AAS*ASTAR(J)	TBAN0073
	TJ(J)=TTO*STAGT	TBAN0074
	RHO(J)=PRES(I)/ZZR/TJ(J)	TBAN0075
212	UJ(J)=SQRT(2.*ZZCP*32.*(STAGT-TJ(J)))	TBAN0076
C		TBAN0077
C	CALCULATE STREAM-TUBE SLOPE	TBAN0078
C		TBAN0079
	LC=0	TBAN0080
	SUMA=0.	TBAN0081
	DO 215 J=1,NTUBE	TBAN0082
215	SUMA=SUMA+ATUBE(J)*COS(ALPHA(J))	TBAN0083
2150	SUMB=0.	TBAN0084
	DO 2151 J=1,NTUBE	TBAN0085
	SUMB=SUMB+ATUBE(J)*COS(ALPHA(J))	TBAN0086
2151	ALPHA(J)=ALPHA1(I)+(ALPHA2(I)-ALPHA1(I))*((SUMB-ATUBE(J)*COS(ALPHA(J)))/SUMA)	TBAN0087
	SUMC=0.	TBAN0088
	DO 218 J=1,NTUBE	TBAN0089
218	SUMC=SUMC+ATUBE(J)*COS(ALPHA(J))	TBAN0090
	IF (ABS((SUMA-SUMC)/SUMA)-0.000005)225,225,220	TBAN0091
220	LC=LC+1	TBAN0092
	SUMA=SUMC	TBAN0093
	IF (LC-40)2150,2150,221	TBAN0094
221	WRITE(JTAPE,10)	TBAN0095
	WRITE(JTAPE,3) I, LN	TBAN0096
	WRITE(JTAPE,2) (ALPHA(J),J=1,NTUBE)	TBAN0097
	IBL=0	TBAN0098
	RETURN	TBAN0099
C		TBAN0100
C	COMPARE COMPUTED FLOW AREA AT THIS GUESSED PRESSURE TO ACTUAL FLOW	TBAN0101
C	AREA AT THIS STATION NUMBER	TBAN0102
C		TBAN0103
225	IF (ABS((AREA(I)-SUMC)/AREA(I))-0.0001) 290,290,230	TBAN0104
230	LR=LR+1	TBAN0105
	IF (LR-40)240,240,235	TBAN0106
235	WRITE(JTAPE,10)	TBAN0107
	WRITE(JTAPE,5) I, LN	TBAN0108
	SUMB=AREA(I)	TBAN0109
	WRITE(JTAPE,6) SUMA,SUMB	TBAN0110
	IBL=0	TBAN0111
	RETURN	TBAN0112
240	PRR=PRES(I)	TBAN0113
	GO TO 2000	TBAN0114
290	VEL(1,I)=UJ(1)	TBAN0115
	VEL(2,I)=UJ(NTUBE)	TBAN0116
	RO(1,I)=RHO(1)	TBAN0117
	RO(2,I)=RHO(NTUBE)	TBAN0118
300	CONTINUE	TBAN0119
		TBAN0120

900 RETURN
END

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TBAN0121
TBAN0122

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$IBFTC NEWR LIST
SUBROUTINE NEWRAD (IBL,X,VEL,RO,DELTB,SHAPEH,N,NX,IHLD,CB,CA,
1 ALFA,ALFB,HSEP,NRECT,ALFC) NEWROC01
NEWROC02
NEWROC03
C THIS SUBROUTINE CALCULATES THE BOUNDARY LAYER DISPLACEMENT NEWROC04
C THICKNESS FOR A GIVEN VELOCITY DISTRIBUTION NEWROC05
C NEWROC06
COMMON/B12678/ JTAPE,IPRINT NEWROC07
COMMON/B2TBCS/SHP(2),THET(2),ROJ(2),VELJ(2),SUMXJ(4) NEWROC08
DIMENSION VEL(2,50), RO(2,50), SHAPEH(2,50), NEWROC09
1X( 1),CA( 1),CB( 1),ISEP(2),DELTB(2,50), NEWROC10
2 DELTA(2,50),THETA(2,50),E(4),F(2),G(2),DT(2), NEWROC11
3ALFA(1),ALFB(1) NEWROC12
4,ALFC(1) NEWROC13
DATA A,C/2H**,2H NEWROC14
NEWROC15
C 1 FORMAT(1X/// 35X,50HBOUNDARY LAYER PROPERTIES - SOLUTION HAS CONV NEWROC16
1 ERGED) NEWROC17
2 FORMAT(1X/// NEWROC18
3 FORMAT(1X/// 35X,54HBOUNDARY LAYER PROPERTIES - SOLUTION HAS NOT NEWROC19
1 CONVERGED) NEWROC20
4 FORMAT(76H INNER WALL NEWROC21
1 OUTER WALL) NEWROC22
5 FORMAT(116H STATION X(I) PRESSURE DELTA THETA H NEWROC23
1 DELTA THETA H AN. AREA FRACTIONAL STATION) NEWROC24
6 FORMAT(115H NUMBER IN PSIA IN IN NEWROC25
1 IN IN SQ IN BLOCKAGE NUMBER) NEWROC26
7 FORMAT( 2X,I4,2X,F9.3,F9.3,3X,A2,3F7.3,A2,3X,A2, NEWROC27
13F7.3, A2,2X,F9.3,F11.4,5X,I4) NEWROC28
8 FORMAT(51H SEPARATION IF IT OCCURS IS INDICATED BY **.....**) NEWROC29
12 FORMAT(1X/) NEWROC30
IBL=1 NEWROC31
THETA(1,N)=DELTB(1,N)/SHAPEH(1,N) NEWROC32
THETA(2,N)=DELTB(2,N)/SHAPEH(2,N) NEWROC33
DELTA(1,N)=DELTB(1,N) NEWROC34
DELTA(2,N)=DELTB(2,N) NEWROC35
NEWROC36
CALCULATE THETA AND SHAPE FACTOR H FOR BOTH WALLS NEWROC37
NEWROC38
N1=N+1 NEWROC39
DO 140 J=1,2 NEWROC40
ISEP(J)=N +1 NEWROC41
SUMX=SUMXJ(J) NEWROC42
DO 1050 I=N1,NX NEWROC43
II=I-1 NEWROC44
SUMX=SUMX+(VEL(J,I)**4*RO(J,I)**(7./6.))+VEL(J,II)**4*RO(J,II)**(7. NEWROC45
1/6.))/2.*(X(I)-X(II)) NEWROC46
1050 THETA(J,I)=(THET(J)**(7./6.)*(VELJ(J)/VEL(J,I))**((25./6.)*(ROJ(J)/ NEWROC47
1RO(J,I))**((7./6.))+SUMX*.0076*.23/VEL(J,I)**((25./6.)/RO(J,I)** NEWROC48
2(7./6.))**((6./7.)) NEWROC49
SUMXJ(J+2)=SUMX NEWROC50
DO 140 I=N1,NX NEWROC51
TA =(THETA(J,I)-THETA(J,I-1))/(X(I)-X(I-1)) NEWROC52
SHAPEH(J,I)=SHP(J)+70.*(SHP(J)-1.05)*TA NEWROC53
IF(SHAPEH(J,I).LE.1.1) SHAPEH(J,I)=1.1 NEWROC54
IF(SHAPEH(J,I).GE.3.5) SHAPEH(J,I)=3.5 NEWROC55
106 IF(SHAPEH(J,I)-HSEP) 108,108,110 NEWROC56
108 ISEP(J)=ISEP(J)+1 NEWROC57
IF(ISEP(J).LE.I) ISEP(J)=ISEP(J)-1 NEWROC58
NEWROC59

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110 DELTA(J,I)=THETA(J,I)*SHAPEH(J,I)
140 CONTINUE
C
C CALCULATE NEW VALUES OF THE DISPLACEMENT THICKNESS FROM THE
C PREVIOUS VALUES AND THE PREDICTED VALUES AT THE PREVIOUS BLOCKAGE
C
ISP=NX+1
JH=1
IF(ISEP(1).GT.ISEP(2) ) JH=2
IF(ISEP(JH).EQ.NX+1) GO TO 145
ISP=ISEP(JH)
JK=1
IF(JH.EQ.1) JK=2
145 DT(1)=0.
DT(2)=0.
E(3)=DELTB(1,N)
E(4)=DELTB(2,N)
DO 2000 I=N1,NX
IF(I.GT.ISP) GO TO 250
DO 2001 J=1,2
D=240.*(SHP(J)-1.05)/SHAPEH(J,I)*THETA(J,I)/(X(I)-X(I-1))+3.3
IF(SHAPEH(J,I)-3.5) 1501,1503,1501
1501 IF(SHAPEH(J,I)-1.1) 1500,1503,1500
1503 D=3.3
DT(J)=0.
1500 CONTINUE
E(J)=DELTA(J,I)*(1.+D/(CB(I)-CA(I))*(DELTB(1,I)+DELTB(2,I)))
1-70.*DT(J)*(SHP(J)-1.05)/SHAPEH(J,I)/(X(I)-X(I-1))
2*DELTA(J,I)
F(J)=DELTA(J,I)*D/(CB(I)-CA(I))
2001 G(J)=F(J)
F(1)=F(1)+1.
G(2)=G(2)+1.
G(1)=G(1)/F(1)
E(1)=E(1)/F(1)
E(2)=E(2)-E(1)*F(2)
G(2)=G(2)-G(1)*F(2)
E(2)=E(2)/G(2)
E(1)=F(1)-E(2)*G(1)
AB1=DELTB(1,I)
AB2=DELTB(2,I)
DO 2004 J=1,2
IF(E(J).LE.0.) E(J)=0.
IF(E(J).GT.0.5*(CB(I)-CA(I))) E(J)=0.5*(CB(I)-CA(I))
IF(DELTB(J,I).LE.0.02*(CB(I)-CA(I))) GO TO 2002
IF(ABS(E(J)-DELTB(J,I))/DELTB(J,I).LE.0.4) GO TO 2002
DELTB(J,I)=DELTB(J,I)*(1.+0.2*SIGN(1.,E(J)/DELTB(J,I)-1.))
GO TO 2004
2002 DELTB(J,I)=(E(J)+DELTB(J,I))/2.
2004 CONTINUE
DO 2006 J=1,2
2006 DT(J)=-3.3*THETA(J,I)*(E(1)+E(2)-AB1-AB2)/(CB(I)-CA(I))
E(3)=E(1)
E(4)=E(2)
GO TO 220
C
C IF FLOW HAS SEPERATED EXPAND AT CONSTANT PRESSURE I.E. CONSTANT
C FLOW AREA
C
250 RT=(SHAPEH(JH,ISP)-HSEP)/(SHAPEH(JH,ISP)-SHAPEH(JH,ISP-1))
IF(ISP.EQ.N1) RT=1.
NEWRO060
NEWRO061
NEWRO062
NEWRO063
NEWRO064
NEWRO065
NEWRO066
NEWRO067
NEWRO068
NEWRO069
NEWRO070
NEWRO071
NEWRO072
NEWRO073
NEWRO074
NEWRO075
NEWRO076
NEWRO077
NEWRO078
NEWRO079
NEWRO080
NEWRO081
NEWRO082
NEWRO083
NEWRO084
NEWRO085
NEWRO086
NEWRO087
NEWRO088
NEWRO089
NEWRO090
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NEWRO092
NEWRO093
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NEWRO101
NEWRO102
NEWRO103
NEWRO104
NEWRO105
NEWRO106
NEWRO107
NEWRO108
NEWRO109
NEWRO110
NEWRO111
NEWRO112
NEWRO113
NEWRO114
NEWRO115
NEWRO116
NEWRO117
NEWRO118
NEWRO119
NEWRO120

```

```

IF(RT.GT.1.)RT=1.
ALF=(ABS(ALFA(ISP))+ABS(ALFB(ISP)))/4.
IF(NRECT.EQ.1)GO TO 350
FL1=CB(ISP)-CA(ISP)-DELTB(1,ISP)*COS(ALFA(ISP))-DELTB(2,ISP)*
1COS(ALFB(ISP))
FL2=CB(ISP-1)-CA(ISP-1)-DELTB(1,ISP-1)*COS(ALFA(ISP-1))-DELTB(2,
1ISP-1)*COS(ALFB(ISP-1))
FL=FL1*(1.-RT)+FL2*RT
FL=FL/COS(ALF)
AL1=COS(ALFA(I))
AL2=COS(ALFB(I))
IF(ISEP(1).EQ.ISEP(2)) GO TO 270
IF(JH.EQ.2) AL1=AL2
IF(JH.EQ.2) AL2=COS(ALFA(I))
E(JK)=DELTA(JK,I)
E(JH)=(CB(I)-CA(I)-FL-DELTA(JK,I)*AL2)/AL1.
SHAPEH(JH,I)=3.5
GO TO 2509
270 E(1)=(CB(I)-CA(I)-FL)/AL1* E(3)/(E(3)+E(4))
E(2)=(CB(I)-CA(I)-FL)/AL2* E(4)/(E(3)+E(4))
DO 251 J=1,2
251 SHAPEH(J,I)=3.5
GO TO 2509
350 DO 351 K=1,2
IS=ISP+1-K
AA=3.141593*((CB(IS)-DELTB(2,IS)*COS(ALFB(IS)))*2-(CA(IS)+DELTB(1
1,IS)*COS(ALFA(IS)))*2)/COS(ALFC(IS))
IF(K.EQ.1) FL1=AA
351 IF(K.EQ.2) FL2=AA
FL=FL1*(1.-RT)+FL2*RT
FL=FL/COS(ALF)
360 AL1=COS(ALFA(I))
AL2=COS(ALFB(I))
IF(ISEP(1).EQ.ISEP(2)) GO TO 370
E(JK)=DELTA(JK,I)
IF(JH.EQ.1) E(JH)=(SQRT((CB(I)-DELTB(2,I)*AL2
)*2-FL*COS(ALFC
1(I)))/3.141593)-CA(I))/AL1
IF(JH.EQ.2) E(JH)=(CB(I)-SQRT(FL*COS(ALFC(I))/3.141593+(CA(I)+DELT
1B(1,I)*AL1)*2))/AL2
SHAPEH(JH,I)=3.5
GO TO 2509
370 E(1)=(CB(I)*2-CA(I)*2-FL*COS(ALFC(I))/3.141593)/2./(CB(I) +
1CA(I) )/AL1
E(2)=E(1)/AL2*AL1
SHAPEH(1,I)=3.5
SHAPEH(2,I)=3.5
2509 DO 2511 J=1,2
2511 DELTB(J,I)=(DELTB(J,I)+E(J))/2.
C
C FIND IF SOLUTION HAS CONVERGED (IBL=1) OR NOT (IBL=0)
C
220 IF(IBL) 2008,2000,2008
2008 IF(ABS(DELTB(1,I)/E(1)-1.)-0.01 ) 200,200,210
200 IF(ABS(DELTB(2,I)/E(2)-1.)-0.01 ) 205,205,210
205 CONTINUE
IFL=1
GO TO 2000
210 IBL=0
IHL=I-2
IF(IHL.LE.N) IHL=N
2000 CONTINUE

```

NEWRO121
NEWRO122
NEWRO123
NEWRO124
NEWRO125
NEWRO126
NEWRO127
NEWRO128
NEWRO129
NEWRO130
NEWRO131
NEWRO132
NEWRO133
NEWRO134
NEWRO135
NEWRO136
NEWRO137
NEWRO138
NEWRO139
NEWRO140
NEWRO141
NEWRO142
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NEWRO148
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NEWRO162
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NEWRO164
NEWRO165
NEWRO166
NEWRO167
NEWRO168
NEWRO169
NEWRO170
NEWRO171
NEWRO172
NEWRO173
NEWRO174
NEWRO175
NEWRO176
NEWRO177
NEWRO178
NEWRO179
NEWRO180
NEWRO181

	RETURN	NEWRO182
	WRITE CUT BOUNDARY LAYER PARAMETERS	NEWRO183
C	ENTRY NEWR1(PRES,AREA,BLOCK)	NEWRO184
C	DIMENSION PRES(50),BLOCK(50),AREA(50)	NEWRO185
C	WRITE(JTAPE,12)	NEWRO186
	IF(IBL) 490,490,491	NEWRO187
490	WRITE(JTAPE,3)	NEWRO188
	GO TO 500	NEWRO189
491	WRITE(JTAPE,1)	NEWRO190
500	DO 510 I=N,NX	NEWRO191
	PRES(I)=PRES(I)/144.	NEWRO192
	X(I)=X(I)*12.	NEWRO193
	DELTA(1,I)=DELTB(1,I)*12.	NEWRO194
	DELTA(2,I)=DELTB(2,I)*12.	NEWRO195
	THETA(1,I)=THETA(1,I)*12.	NEWRO196
	THETA(2,I)=THETA(2,I)*12.	NEWRO197
510	AREA(I)=AREA(I)*144.	NEWRO198
	WRITE(JTAPE,2)	NEWRO199
	WRITE(JTAPE,4)	NEWRO200
	WRITE(JTAPE,5)	NEWRO201
	WRITE(JTAPE,6)	NEWRO202
	WRITE(JTAPE,12)	NEWRO203
	DO 600 I=N,NX	NEWRO204
	IF(ISEP(1)-I) 560,565,560	NEWRO205
560	IF(ISEP(2)-I) 570,575,570	NEWRO206
565	IF(ISEP(2)-I) 580,585,580	NEWRO207
570	WRITE(JTAPE,7)	NEWRO208
	1 I,X(I),PRES(I),C,DELTA(1,I),THETA(1,I),SHAPEH(1,I),C,C,	NEWRO209
	1DELTA(2,I),THETA(2,I),SHAPEH(2,I),C,AREA(I),BLOCK(I),I	NEWRO210
	GO TO 600	NEWRO211
575	WRITE(JTAPE,7)	NEWRO212
	1 I,X(I),PRES(I),C,DELTA(1,I),THETA(1,I),SHAPEH(1,I),C,A,	NEWRO213
	1DELTA(2,I),THETA(2,I),SHAPEH(2,I),A,AREA(I),BLOCK(I),I	NEWRO214
	GO TO 600	NEWRO215
580	WRITE(JTAPE,7)	NEWRO216
	1 I,X(I),PRES(I),A,DELTA(1,I),THETA(1,I),SHAPEH(1,I),A,C,	NEWRO217
	1DELTA(2,I),THETA(2,I),SHAPEH(2,I),C,AREA(I),BLOCK(I),I	NEWRO218
	GO TO 600	NEWRO219
585	WRITE(JTAPE,7)	NEWRO220
	1 I,X(I),PRES(I),A,DELTA(1,I),THETA(1,I),SHAPEH(1,I),A,A,	NEWRO221
	1DELTA(2,I),THETA(2,I),SHAPEH(2,I),A,AREA(I),BLOCK(I),I	NEWRO222
600	CONTINUE	NEWRO223
	WRITE(JTAPE,8)	NEWRO224
	DO 610 I=N,NX	NEWRO225
	PRES(I)=PRES(I)*144.	NEWRO226
	X(I)=X(I)/12.	NEWRO227
	THETA(1,I)=THETA(1,I)/12.	NEWRO228
	THETA(2,I)=THETA(2,I)/12.	NEWRO229
610	AREA(I)=AREA(I)/144.	NEWRO230
	RETURN	NEWRO231
	END	NEWRO232
		NEWRO233
		NEWRO234

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$IBFTC EMPC LIST
SUBROUTINE EMPCTS
C
C
C THIS SUBROUTINE USES EMPIRICAL DATA TO CALCULATE THE DIFFUSER
C PERFORMANCE FROM THE COMPRESSOR OUTLET TO THE SNOUT LIP OR
C TO THE DOME
C
COMMON/B2/ RAD(16),DELTA(2,50),EE1(2),UJ(15),THA,THB,THS,PRES(50),
1NGO,NWAY,ZZR,ZZGAMA,BETA1,BETA2,XMVA,XMVB,XMVS, ZZCP,IDIF
2,HSEP,FLAREA(50),AREA(50)
COMMON/B4/DPREF
COMMON/B12/ X(120),CA(120),CB(120),SA(50),SB(50),
1NRECT,NXDIF,NDIFF,NSNOUT,NXDIF1,NXDIF2,NXDIFA,NXDIFB,NTUBE,
2PRESIN,BLOCK(50),ABLOCK,SHAPEH(2,50),
3VPDATA(15),RDATA(15),NUPR,ARDTA(200),XLNDDTA(20),EFDTA(200),NCDF,
4NYDF,NZDF,E1DTA,NXDF,AREF,WIDTH1,
5XMACH,RHOREF,EFD(3)
COMMON/B126/AF2,TAN1A,TAN1B,PAN1A,PAN1B, AFA,AFB,PREDM,STAGTEMPCO190
1,IBL,STPREF,PNRTA,PNRTB,DPHSNT,DOMLOS
COMMON/B12678/JTAPE,IPRINT
COMMON/BZERO/ UJY(11),YY(11),F(2),D9(11),DUMMY(565)
COMMON/B2EMP/ DUMMIE(135),UCL2
1,ZCTS
C
1 FORMAT(1X////////18H *** ERROR MESSAGE/64H SOLUTION FAILED TO CALCULEMPCO260
1ATE STATIC PRESSURE AT COMPRESSOR EXIT) EMPCO270
21 FORMAT(1H149X3(2H-),7HRESULTS3(2H-)//21HOREFERENCE CONDITIONEMPCO280
1S/1X20(1H-)/15HOREFERENCE AREA13X1H=F10.3,6H SQ FT/19H REFERENCE VEMPCO290
2ELOCITY9X1H=F10.1,11H FT PER SEC/18H INLET MACH NUMBER10X1H=F10.3/EMP0300
322H REFERENCE MACH NUMBER6X1H=F10.3/29H REFERENCE DYNAMIC PRESSUREEMP0310
4 =F10.2,4H PSI) EMP0320
22 FORMAT(115HOTHEDIFFUSER TREATMENT USED IN THIS PROGRAM BECOMES INEMP0330
1CREASINGLY INACCURATE AT INLET MACH NUMBERS GREATER THAN 0.7) EMP0340
8765 FORMAT(7H0EMPCTS10F11.3/(7X10F11.3)) EMP0350
C
NXDF1=NXDIF-1
GO TO (100,104),NRECT
100 DO 102 I=1,NXDIF,NXDF1
102 AREA(I)=(CB(I)**2-CA(I)**2)*3.141593
GO TO 1505
104 DO 105 I=1,NXDIF,NXDF1
105 AREA(I)=CB(I)-CA(I)
C
C CALCULATE STATIC PRESSURE AT INLET
C
1505 LG=0
106 FLAREA(1)=AREA(1)*(1.-BLOCK(1))
PRESIN=STPREF
A=1./(2.*ZZCP*32.)
C=-STAGT
1500 B=FLAREA(1)*PRESIN/(AF2*ZZR)
U=(-B+SQRT(B*B-4.*A*C))/2./A
TEMP=STAGT-U*U*A
PRS=STPREF*(TEMP/STAGT)**(ZZGAMA/(ZZGAMA-1.))
IF(ABS(PRS/PRESIN-1.)-0.0001) 1504,1504,1501
1501 LG=LG+1
PRESIN=PRS
IF(LG-40) 1500,1500,1502
EMP0360
EMP0370
EMP0380
EMP0390
EMP0400
EMP0410
EMP0420
EMP0430
EMP0440
EMP0450
EMP0460
EMP0470
EMP0480
EMP0490
EMP0500
EMP0510
EMP0520
EMP0530
EMP0540
EMP0550
EMP0560
EMP0570
EMP0580
EMP0590

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1502 WRITE (JTape,1)
      IBL=0.
      RETURN
1504 PRESIN=PRS
C
C   CALCULATE INLET AND REFERENCE PROPERTIES
C
      ASS=FLAREA(1)*0.532*STPREF/AF2/SQRT(STAGT)
      CALL GASTBL(ASS,TSS,PSS,YMACH,1,IBL,ZZR,ZZGAMA)
      ASS=AREF*ASS/FLAREA(1)
      IF(NRECT.EQ.2) ASS=ASS/WIDTH1
      CALL GASTBL(ASS,TSS,PSS,XMACH,1,IBL,ZZK,ZZGAMA)
      DPREF=STPREF*(1.0-PSS)/144.
      UREF=XMACH*SQRT(ZZGAMA*ZZR*32.2*STAGT*TSS)
      IF(IPRINT.EQ.3) GO TO 107
C
C   WRITE OUT REFERENCE CONDITIONS
C
      WRITE (JTape,21)AREF,UREF,YMACH,XMACH,DPREF
      IF(YMACH.GE..7)WRITE (JTape,22)
107  DPREF=DPREF*144.
C
C   CALCULATE DIFFUSER PERFORMANCE
C
      AR=AREA(NXDIF)/AREA(1)
      B=B*AREA(1)/FLAREA(1)
      U=(-B+SQRT(B*B-4.*A*C))/2./A
      RH=PRESIN/ZZR/(STAGT-U*U*A)
      DYHD=RH*U*U/2./32.
      CPIDL=1.-1./AR/AR
      XLNGTH=(X(NXDIF)-X(1))/(CB(1)-CA(1))
      E1=FLAREA(1)/AREA(1)
      CALL EMPANL(AR,XLNGTH,ARDTA,XLNDTA,EFDTA,NCDF,NYDF,NZDF,E1,E1DTA,
1E2,EFFECTN,IDIF,EFDT,1)
      CPACT=CPIDL*EFFECTN
      PRES(NXDIF)=PRESIN+DYHD*CPACT
      B=E2*AREA(NXDIF)*PRES(NXDIF)/AF2/ZZR
      U=(-B+SQRT(B*B-4.*A*C))/2./A
      TEMP=STAGT-U*U*A
      RHO2=PRES(NXDIF)/ZZR/TEMP
      UCL2=AF2/E2/AR*AREA(NXDIF)/RHO2
      SUM=0.
      CALL PROFL(E2,UJY,ZCTS)
      DO 120 J=1,11
      UJY(J)=UJY(J)*UCL2
      YY(J)=SUM
120  SUM=SUM+0.1
C
C   PRINT OUT SOLUTION
C
      CALL DCUTPT(PSOUT,CPIDL,CPACT,EFFECTN,UJY,YY,D9,2)
C
      GO TO (150,1200,150),NGO
1200 GO TO (121,130),NRECT
121  F(1)=(SA(NXDIF+1)**2-CA(NXDIF+1)**2)/(CB(NXDIF+1)**2-CA(NXDIF+1)**
12)
      F(2)=(SB(NXDIF+1)**2-SB(NXDIF+1)**2)/(CB(NXDIF+1)**2-CA(NXDIF+1)**
12)
      GO TO 101
130  F(2)=(CB(NXDIF+1)-SB(NXDIF+1))/(CB(NXDIF+1)-CA(NXDIF+1))
      F(1)=(SA(NXDIF+1)-CA(NXDIF+1))/(CB(NXDIF+1)-CA(NXDIF+1))
131  EE1(1)=1.-(1.-E2)/2./F(1)

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EMPC0600
EMPC0610
EMPC0620
EMPC0630
EMPC0640
EMPC0650
EMPC0660
EMPC0670
EMPC0680
EMPC0690
EMPC0700
EMPC0710
EMPC0720
EMPC0730
EMPC0740
EMPC0750
EMPC0760
EMPC0770
EMPC0780
EMPC0790
EMPC0800
EMPC0810
EMPC0820
EMPC0830
EMPC0840
EMPC0850
EMPC0860
EMPC0870
EMPC0880
EMPC0890
EMPC0900
EMPC0910
EMPC0920
EMPC0930
EMPC0940
EMPC0950
EMPC0960
EMPC0970
EMPC0980
EMPC0990
EMPC1000
EMPC1010
EMPC1020
EMPC1030
EMPC1040
EMPC1050
EMPC1060
EMPC1070
EMPC1080
EMPC1090
EMPC1100
EMPC1110
EMPC1120
EMPC1130
EMPC1140
EMPC1150
EMPC1160
EMPC1170
EMPC1180
EMPC1190
EMPC1200

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	170	EE1(2)=1.-(1.-E2)/2./F(2)	EMPC1210
150		RETURN	EMPC1220
C			EMPC1230
C		ENTRY HERE DURING MASS FLOW ITERATION WITH MIXING EQUATION BEING	EMPC1240
C		USED IN THE PASSAGE BETWEEN SNOOT AND OUTER CASING	EMPC1250
			EMPC1260
		ENTRY EMPDT1	EMPC1270
		XMA=AF1/AF2	EMPC1280
		XMB=AFB/AF2	EMPC1290
		CALL PROFL1(XMA,XMB,YA,YB,EA,EB,ES,BETA1,BETA2,ZCTS)	EMPC1300
		THA=AREA(NXDIF)*YA	EMPC1310
		THB=AREA(NXDIF)*(1.-YB)	EMPC1320
		THS=AREA(NXDIF)-THA-THB	EMPC1330
		XMVA=EA*UCL2	EMPC1340
		XMVB=EB*UCL2	EMPC1350
		XMVS=ES*UCL2	EMPC1360
		BETA1=BETA1	EMPC1370
		BETA2=BETA2	EMPC1380
900		RETURN	EMPC1390
		END	EMPC1400

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SUBROUTINE EMPSTA
C
C THIS SUBROUTINE CALCULATES THE FLOW PROPERTIES IN THE TWO ANULI
C USING EMPIRICAL DATA
C
COMMON/B2/ RAD(16),DELTA(2,50),EE1(2),UJ(15),THA,THB,THS,PRES(50),
INGO,NWAY,ZZR,ZZGAMA,BETA1,BETA2,XMVA, XMVB, XMVS, ZZCP, IDIF
2,HSEP ,FLAREA(50),AREA(50)
COMMON/B12/ X(120),CA(120),CB(120),SA(50),SB(50),
1ARECT,NXDIF,NCIFF,NSNOUT,NXDIF1,NXDIF2,NXDIFA,NXDIFB,NTUBE,
2PRESIN, BLCK(50),ABLCK,SHAPEH(2,50),
3VPDATA(15),RDATA(15),NUPR,ARDTA(20C),XLNTA(20),EFDTA(20C),NCDF,
4NYDF,NZCF,E1DTA, NXCF,AREF,WICHT1,
5XMACH,RHOREF,EFCT(3)
COMMON/B126/AF2,TAN1A,TAN1B,PAN1A,PAN1B, AFA,AFB,PREDH,STAGT
1,IBL,STPREF,PNRTA,PNRTB,DPHSNT,DOMLOS
COMMON/B12678/JTAPE ,IPRINT
COMMON/BZERO/ ALPB(50),ALPC(50),ALPD(50),
1CUMMY(400),ALPA(50)
COMMON/B2EMP/ NXC(2),AR(3,2),TH(2),R(2),T(2),ASTR(2),AF(2),
1UJY(11),XX(2),DYD(2) ,ALFA(2,50),NX(2),UCL2
1,ZCTS
COMMON/BPLOS/PLCSS(2)
C
8765 FORMAT(7HOEMPSTA10F11.3/(7X10F11.3))
C
C SET UP VALUES NEEDED IN THE DC LOOP
C
NXDF1=NXCIF-1
NX(1)=NXDIF1
NX(2)=NXDIF2
NXD(1)=NXDIFA
NXD(2)=NXDIFB
CALL SLOPE(X,CA,NXCIF,NXDIFA,ALPA,NXDIFA+1)
CALL SLOPE(X,CB,NXDIF,NXDIFB,ALPB,NXDIFB+1)
CALL SLOPE(X,SA,NXCIF+2,NXCIFA,ALPC,NXDIFA+1)
CALL SLOPE(X,SB,NXDIF+2,NXDIFB,ALPD,NXDIFB+1)
NXDF2=NXDIF+1
DC 119 I=NXDIF,NXCF2
ALPC(I)=ALPA(I)
119 ALPD(I)=ALPB(I)
DO 120 I=NXDIF,NXCIFA
DC=1
DE=1
IF(ALPA(I).LE.0.) DD=-1
IF(ALPC(I).LE.0.) DE=-1
120 ALFA(1,I)=(DD*ATAN(DD*ALPA(I))+DE*ATAN(DE*ALPC(I)))/2.
CC 121 I=NXDIF,NXDIFB
DD=1
DE=1
IF(ALPB(I).LE.0.) CC=-1
IF(ALPD(I).LE.0.) DE=-1
121 ALFA(2,I)=(DD*ATAN(DD*ALPB(I))+DE*ATAN(DE*ALPC(I)))/2.
DC 130 K=1,2
XX(K)=0.
NXX=NX(K)-1
DC 130 I=NXCIF,NXX
130 XX(K)=XX(K)+(X(I+1)-X(I))/COS((ALFA(K,I)+ALFA(K,I+1))/2.)
GO TO (140,145),NRECT
EMPSC010
EMPSC020
EMPSC030
EMPSC040
EMPSC050
EMPSC060
EMPSC070
EMPSC080
EMPSC090
EMPSC100
EMPSC110
EMPSC120
EMPSC130
EMPSC140
EMPSC150
EMPSC160
EMPSC170
EMPSC180
EMPSC190
EMPSC200
EMPSC210
EMPSC220
EMPSC230
EMPSC240
EMPSC250
EMPSC260
EMPSC270
EMPSC280
EMPSC290
EMPSC300
EMPSC310
EMPSC320
EMPSC330
EMPSC340
EMPSC350
EMPSC360
EMPSC370
EMPSC380
EMPSC390
EMPSC400
EMPSC410
EMPSC420
EMPSC430
EMPSC440
EMPSC450
EMPSC460
EMPSC470
EMPSC480
EMPSC490
EMPSC500
EMPSC510
EMPSC520
EMPSC530
EMPSC540
EMPSC550
EMPSC560
EMPSC570
EMPSC580
EMPSC590

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*.....*.....*.....*.....*.....*.....*.....*.....*.....*
140 AR(2,1)=3.14159*(SA(NXDIF1)**2-CA(NXDIF1)**2)*COS(ALFA(1,NXDIF1)) EMP S0600
    AR(3,1)=3.14159*(SA(NXDIFA)**2-CA(NXDIFA)**2) EMP S0610
    AR(2,2)=3.14159*(CB(NXDIF2)**2-SB(NXDIF2)**2)*COS(ALFA(2,NXDIF2)) EMP S062C
    AR(3,2)=3.14159*(CB(NXDIFB)**2-SB(NXDIFB)**2) EMP S0630
    AR(1,1)=3.14159*(SA(NXDIF+1)**2-CA(NXDIF+1)**2) EMP S0640
1*CCS(ALFA(1,NXDIF+1)) EMP S0650
    AR(1,2)=3.14159*(CB(NXDIF+1)**2-SB(NXDIF+1)**2) EMP S066C
1*COS(ALFA(2,NXDIF+1)) EMP S0670
GC TC 147 EMP S0680
145 AR(2,1)=(SA(NXDIF1)-CA(NXDIF1))*COS(ALFA(1,NXDIF1)) EMP S0690
    AR(3,1)=(SA(NXDIFA)-CA(NXDIFA)) EMP S070C
    AR(2,2)=(CB(NXDIF2)-SB(NXDIF2))*COS(ALFA(2,NXDIF2)) EMP S071C
    AR(3,2)=(CB(NXDIFB)-SB(NXDIFB)) EMP S0720
    AR(1,1)=(SA(NXDIF+1)-CA(NXDIF+1))*COS(ALFA(1,NXDIF+1)) EMP S0730
    AR(1,2)=(CB(NXDIF+1)-SB(NXDIF+1))*COS(ALFA(2,NXDIF+1)) EMP S0740
147 R(1)=(SA(NXDIF+1)-CA(NXDIF+1))*COS(ALFA(1,NXDIF+1)) EMP S075C
    R(2)=(CB(NXDIF+1)-SB(NXDIF+1))*COS(ALFA(2,NXDIF+1)) EMP S0760
RETURN EMP S0770
C EMP S0780
C ENTRY HERE DURING INTERATION CN MASS SPLIT EMP S0790
C EMP S0800
C ENTRY EMPSA1 EMP S0810
C EMP S082C
C CALCULATE DIFFUSER PERFORMANCE EMP S0830
C EMP S0840
C AF(1)=AFA EMP S0850
C AF(2)=AFB EMP S0860
C TH(1)=THA*COS(ALFA(1,NXDIF1)) EMP S0870
C TH(2)=THB*COS(ALFA(2,NXDIF2)) EMP S0880
C DYD(1)=XMVA**2 EMP S0890
C DYD(2)=XMVB**2 EMP S0900
C CC 500 K=1,2 EMP S0910
C IF(K.EQ.1) BT=BETA1 EMP S0920
C IF(K.EQ.2) BT=BETA2 EMP S0930
C ARR=AR(2,K)/TH(K) EMP S094C
200 E1=1.-(1.-E1(K))*AR(1,K)/TH(K) EMP S0950
C RHC=AF(K)/TH(K)/SCRT(DYD(K)) EMP S0960
C DYHD=RHC*DYD(K)/2./32.*BT**2 EMP S0970
C CPIDL=1.-1./ARR/ARR EMP S098C
C XLN=XX(K)/R(K) EMP S099C
C IF(ARR-1.) 223,223,222 EMP S100C
222 CALL EMPANL(ARR,XLN,ARDTA,XLNCTA,EFDTA,NCCF,NYDF,NZDF,E1,E1DTA, EMP S1010
1E2,EFECTN,IDIF,EFDT, K+1) EMP S1020
GC TO 224 EMP S1030
C EMP S104C
C ASSUME THAT FLOW MAINTAINS A SIMILAR PROFILE IF PASSAGE ACTS EMP S105C
C AS A NOZZLE EMP S1060
C EMP S1070
223 EFECTN=1. EMP S1080
C F2=E1 EMP S1090
224 CPACT=CPICL*EFECTN EMP S1100
C PRSCUT=PRC(NXDIF)+CPACT*DYHD EMP S1110
C A=1./((ZZCP*2.*32.)) EMP S1120
C B=E2*AR(2,K)*PRSCUT/(AF2*ZZR) EMP S1130
C C=-STAGT EMP S1140
C UM=(-B+SCRT(B*B-4.*A*C))/2./A EMP S1150
C RHC=PRSCUT/ZZR/(STAGT-UM*UM*A) EMP S1160
C UCL3=AF(K)/E2/AR(2,K)/RHO EMP S1170
C EMP S1180
C CALCULATE DIFFUSER PERFORMANCE ALLOWING FOR MIXING EMP S1190

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.....*.....*.....*.....*.....*.....*.....*.....*.....*
C      CALL PRCFL(E2,UJY,ZAN)                                EMPS1200
      CALL PRCFL1(1.,C.,C3,C4,C5,C6,C7,BT,C8,ZAN)           EMPS1210
      ARR=AR(3,K)/AR(2,K)                                    EMPS1220
      DYH=RHC*UCL3**2/32./2.                                EMPS1230
      BTA=1./E2                                              EMPS1240
      PRR=PRSCUT+(1.+1./ARR)*(BTA-1./ARR)*DYH              EMPS1250
1/BTA**2                                                    EMPS1260
      AZ =1.-1./(AR(3,K)/TH(K))**2                          EMPS1270
      CPID=(2.*(BT-1.)+AZ)/BT**2                            EMPS1280
C      CALCULATE TEMPERATURE AT INLET TO ANNULI AND TOTAL PRESSURE LOSS EMPS1290
C      B=1.                                                  EMPS1300
C      C=-STAGT                                             EMPS131C
      A=(AF(K)*ZZR/AR(3,K)/PRR)**2/(2.*ZZCP*32.)           EMPS1320
      TANA=(-B+SQRT(B*B-4.*A*C))/2./A                       EMPS1330
      PNRT=PRR*(STAGT/TANA)**(ZZGAMA/(ZZGAMA-1.))          EMPS1340
      PNRT=PNRT-PLOSS(K)                                    EMPS1350
      ASS=AF(K)*SQRT(STAGT)/(0.532*PNRT)                   EMPS1360
      ASS=AR(3,K)/ASS                                       EMPS1370
      CALL GASTBL(ASS,RAT,RAP,XMACH,1,IBL,ZZR,ZZGAMA)       EMPS1380
      PRR=RAP*PNRT                                           EMPS1390
      TANA=STAGT*RAT                                         EMPS1400
      CPCT=(PRR-PRES(NXDIF))/DYHD                           EMPS1410
      EFECT=CPCT/CPID                                        EMPS1420
      DELTP=(STPREF-PNRT)/STPREF                            EMPS1430
      IF(IPRINT)300,300,250                                  EMPS1440
C      PRINT CUT RESULTS                                     EMPS1450
C      250 CALL CCUTP1(NSNCUT,CPIDL,CPACT,EFECTN,CPID,CPCT,EFECT,2,K,TH(K)/AREMPS1460
      1(1,K),DELTP)                                         EMPS1470
C      300 GO TO (323,324),K                                EMPS1480
      323 PANIA=PRR                                          EMPS1490
      IF(DELTP.LT.0.)PANIA=PANIA*(1.+DELTP)                 EMPS1500
      TANIA=TANA                                             EMPS1510
      PNRTA=PNRT                                             EMPS1520
      GO TO 500                                              EMPS1530
      324 PANIB=PRR                                          EMPS1540
      IF(DELTP.LT.0.)PANIB=PANIB*(1.+DELTP)                 EMPS1550
      TANIB=TANA                                             EMPS1560
      PNRTB=PNRT                                             EMPS1570
      GO TO 500                                              EMPS1580
      500 CCNTINUE                                          EMPS1590
      900 RETURN                                             EMPS1600
      END                                                    EMPS1610
EMPS1620
EMPS1630
EMPS1640
EMPS1650
EMPS1660

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YOUR CARD TCTAL IS ---

168

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SIBFIC EMPA
  SUBROUTINE EMPANL (AR,XLNGTH,ARDTA,XLNDTA,EFDTA,NCDF,NYDF,NZDF,E1,EMPA0001
1E1DTA,E2,EFECTN,IDIF,EFDT,NUDF)      EMPA0002
  DIMENSION ARDTA(1),XLNDTA(1),EFDTA(1)  EMPA0003
1,EFDT(1)                                EMPA0004
C                                          EMPA0005
  IF(IDIF)200,100,200                    EMPA0006
100 CALL INTPL8( AR,XLNGTH,ARDTA,EFDTA,XLNDTA,NCDF,NYDF,NZDF,EFECT)  EMPA0007
101 SUM=0.25                               EMPA0008
  EFB=0.5                                   EMPA0009
  DO 120 J=1,14                             EMPA0010
  R=2./0.15*(0.85-E1DTA)**2*COS(3.141593*(EFB-0.5))+EFB-EFECT  EMPA0011
  IF(R) 110,130,117                          EMPA0012
117 EFB=EFB-SUM                              EMPA0013
  GO TO 120                                   EMPA0014
110 EFB=EFB+SUM                              EMPA0015
120 SUM=SUM/2.                                EMPA0016
130 EFECTN=EFB+2./0.15*(0.85-E1)**2*COS(3.141593*(EFB-0.5))  EMPA0017
135 E2=1./SQRT(AR**2*(1./E1**2-EFECTN*(1.-1./AR**2)))  EMPA0018
  CPIDL=1.-1./AR**2                          EMPA0019
  GO TO 900                                   EMPA0020
200 EFECTN=EFDT(NUDF)                        EMPA0021
  GO TO 135                                   EMPA0022
900 RETURN                                    EMPA0023
  END                                          EMPA0024

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.....*.....*.....*.....*.....*.....*.....*.....*.....*
GO TO 102
101 WRITE(JTAPE,21)
102 GO TO (103,104,120),N
103 WRITE(JTAPE,2)
GO TO 110
104 WRITE(JTAPE,3)
110 WRITE(JTAPE,53)
WRITE(JTAPE,24)
WRITE(JTAPE,52)
WRITE(JTAPE,26)
WRITE(JTAPE,14) CPIDL,CPACT,EFFECT
WRITE(JTAPE,53)
GO TO (111,112,120),N
111 WRITE(JTAPE,8)
WRITE(JTAPE,52)
WRITE(JTAPE,9) (Y(I),I=1,11)
WRITE(JTAPE,10)(YY(I),I=1,11)
WRITE(JTAPE,11)(UJ(I),I=1,11)
GO TO 120
112 WRITE(JTAPE,8)
WRITE(JTAPE,52)
WRITE(JTAPE,9) (Y(I),I=1,11)
WRITE(JTAPE,11)(UJ(I),I=1,11)
120 RETURN

C
C
C
C
ENTRY HERE TO PRINT OUT PERFORMANCE OF FLOW IN ANNULI
ENTRY DOUTP1(NSNOUT,CPIDL,CPACT,EFFECT,CPID,CPAC,EFEC,N,K,AR,DP)
DATA A,B,C,D/SHINNER,SHOUTER,SHSNOUT,SHOOME /
GO TO (301,302),K
301 WW=A
GO TO 303
302 WW=B
303 IF(NSNOUT-1)600,310,600
310 WRITE(JTAPE,22)WW,C
GO TO(311,312,313),N
311 WRITE(JTAPE,2)
GO TO 320
312 WRITE(JTAPE,3)
GO TO 320
313 WRITE(JTAPE,4)
GO TO 350
320 WRITE(JTAPE,53)
WRITE(JTAPE,24)
WRITE(JTAPE,52)
WRITE(JTAPE,26)
WRITE(JTAPE,14) CPIDL,CPACT,EFFECT
WRITE(JTAPE,25)
WRITE(JTAPE,15)CPID,CPAC,EFEC,DP
GO TO 500
350 WRITE(JTAPE,53)
WRITE(JTAPE,24)
WRITE(JTAPE,52)
WRITE(JTAPE,25)
WRITE(JTAPE,15) CPID,CPAC,EFEC,DP
500 IF(CPID.LE.0.0.OR.CPIDL.LE.0.0) WRITE(JTAPE,43)
IA=1
IB=3
IF(ABS(1.-IR).LE.0.15) GO TO 501
DOPT0060
DOPT0061
DCPT0062
DCPT0063
DCPT0064
DOPT0065
DCPT0066
DCPT0067
DCPT0068
DCPT0069
DOPT0070
DCPT0071
DCPT0072
DOPT0073
DOPT0074
DCPT0075
DCPT0076
DCPT0077
DOPT0078
DCPT0079
DCPT0080
DCPT0081
DOPT0082
DCPT0083
DCPT0084
DOPT0085
DOPT0086
DCPT0087
DCPT0088
DCPT0089
DOPT0090
DCPT0091
DCPT0092
DCPT0093
DCPT0094
DCPT0095
DCPT0096
DCPT0097
DOPT0098
DCPT0099
DCPT0100
DCPT0101
DOPT0102
DOPT0103
DCPT0104
DCPT0105
DOPT0106
DOPT0107
DCPT0108
DCPT0109
DCPT0110
DOPT0111
DCPT0112
DCPT0113
DOPT0114
DOPT0115
DOPT0116
DCPT0117
DOPT0118
DOPT0119

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*.....*.....*.....*.....*.....*.....*.....*.....*.....*
IA=2
IB=4
501 WRITE(JTAPE,40) AR,DA(IA),DA(IB)
RETURN
C
600 WRITE(JTAPE,22)WW,D
WRITE(JTAPE,4)
WRITE(JTAPE,53)
CPIDL=CPIDL/144.
CPACT=CPACT/144.
WRITE(JTAPE,41)CPIDL,CPACT
WRITE(JTAPE,42)DP
CPIDL=CPIDL*144.
CPACT=CPACT*144.
RETURN
END
YOUR CARD TOTAL IS ---          136
DCPT0120
DCPT0121
DCPT0122
DCPT0123
DCPT0124
DCPT0125
DCPT0126
DCPT0127
DCPT0128
DCPT0129
DCPT0130
DCPT0131
DCPT0132
DCPT0133
DCPT0134
DCPT0135

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SIBFTC GAST
SUBROUTINE GASTBL(X,Y,Z,XMACH,N,IBL,ZZR ,ZZGAMA)
C
C X=AREA(1)/AREA(MACH NO = 1.)
C Y=TEMP(1)/STAGT
C Z=PRES(1)/STAGP
C XMACH=MACH NUMBER
C N=0 SUBROUTINE ACCEPTS A VALUE Z TO GIVE X,Y,AND XMACH
C N=1 SUBROUTINE ACCEPTS A VALUE X TO GIVE Y,Z,AND XMACH
C N=-1 SUBROUTINE RETURN THE VALUE OF R AND GAMMA
C IN THIS SUBROUTINE GAMMA=1.4 AND R=53.3 LBF FT SEC
C
COMMON/B12678/ JTAPE,IPRINT
1 FORMAT(42H NEGATIVE VALUE CALCULATED FOR MACH NUMBER/ZOH SOLUTION
1 TERMINATED)
2 FORMAT(49H MACH NUMBER GREATER THAN ONE. SOLUTION CONTINUED)
11 FORMAT(18H *** ERROR MESSAGE)
12 FORMAT(1X////////)
C
IF(N)50,100,200
50 ZZGAMA=1.4
ZZR=53.3
RETURN
100 Y=Z**(2./7.)
IF(Z.LE.0..OR.Z.GT.1.) GO TO 101
XMACH=SQRT(5.*((1./Z)**(2./7.)-1.))
IBL=1
IF(XMACH)101,101,102
101 WRITE(JTAPE,12)
WRITE(JTAPE,11)
WRITE(JTAPE,1)
IBL=0
RETURN
102 IF(XMACH-1.)104,104,103
103 WRITE(JTAPE,12)
WRITE(JTAPE,11)
WRITE(JTAPE,2)
104 ASTAR=1.2**3.
A =((1.+0.2*XMACH**2.)**3.)/XMACH
X=A/ASTAR
RETURN
200 XMACH=1./X
IF(X.LT.1.) GO TO 101
DC 210 J=1,20
R=(1.+0.2*XMACH**2.)**3./((1.2**3.*XMACH)-R
DRDM=(1.2*(1.+0.2*XMACH**2)**2-(1.+0.2*XMACH**2)**3)/X/1.2**3
1*3
DM=-R/DRDM
IF(ABS(DM/XMACH)-0.0001)220,205,205
205 XMACH=XMACH+DM
210 CONTINUE
IBL=0
RETURN
220 Z=1./((1.+0.2*XMACH**2.)**3.5
Y=Z**(2./7.)
900 RETURN
END
GASTOC01
GASTO002
GASTO003
GASTO004
GASTO005
GASTO006
GASTO007
GASTO008
GASTO009
GASTOC10
GASTO011
GASTOC12
GASTOC13
GASTO014
GASTO015
GASTO016
GASTO017
GASTOC18
GASTO019
GASTOC20
GASTO021
GASTO022
GASTO023
GASTOC24
GASTO025
GASTO026
GASTO027
GASTOC28
GASTOC29
GASTO030
GASTO031
GASTOC32
GASTO033
GASTOC34
GASTOC35
GASTOC36
GASTO037
GASTO038
GASTO039
GASTO040
GASTO041
GASTO042
GASTO043
GASTOC44
GASTO045
GASTO046
GASTOC47
GASTO048
GASTO049
GASTO050
GASTO051
GASTO052
GASTO053
GASTO054
GASTO055
GASTO056

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\$IBFTC SLOP	
SUBROUTINE SLOPE(X,Y,LS,LE,DYDX,NX)	SLOP0001
	SLOPC002
DIMENSION X(1),Y(1),DYDX(1)	SLOPC003
	SLOPC004
NIS=0	SLOP0005
IS=LS	SLOPC006
IE=LE	SLOPC007
IF(IS-1) 4,4,3	SLOPC008
3 IS=IS-1	SLOPC009
NIS=1	SLOP0010
HLD=DYDX(IS)	SLOP0011
4 NIE=0	SLOP0012
IF(NX-IE) 45,45,40	SLOP0013
40 IE=IE+1	SLOP0014
NIE=1	SLOPC015
HLE=DYDX(IE)	SLOP0016
45 CONTINUE	SLOPC017
IF(IS-IE) 8,5,8	SLOPC018
5 DYDX(IS)=0.0	SLOPC019
GO TO 60	SLOP0020
8 DO 50 I=IS,IE	SLOP0021
IF(I-IS) 10,10,20	SLOP0022
10 DX1=X(IS+1)-X(IS)	SLOPC023
DY1=Y(IS+1)-Y(IS)	SLOP0024
DYDX(IS)=DY1/DX1	SLOP0025
GO TO 50	SLOPC026
20 IF(I-IE) 30,41,60	SLOPC027
30 DYDX(I)=((Y(I+1)-Y(I))/(X(I+1)-X(I))+(Y(I)-Y(I-1))/(X(I)-X(I-1)))/	SLOP0028
12.0	SLOP0029
GO TO 50	SLOPC030
41 DXIE=X(IE)-X(IE-1)	SLOP0031
DYIE=Y(IE)-Y(IE-1)	SLOP0032
DYDX(IE)=DYIE/DXIE	SLOPC033
50 CONTINUE	SLOPC034
51 IF(NIS-1) 53,52,52	SLOPC035
52 DYDX(IS)=HLD	SLOP0036
53 IF(NIE-1) 55,54,54	SLOP0037
54 DYDX(IE)=HLE	SLOP0038
55 CONTINUE	SLOP0039
60 RETURN	SLOP0040
END	SLOP0041

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$IBFTC I1AP
      SUBROUTINE I1AP1(X,Y,ARGX,ARGY,IMX)
C
C SUBROUTINE FOR THE PARABOLIC INTERPOLATION OF A FUNCTION OF ONE
C ARGUMENT
      DIMENSION ARGX(1),ARGY(1)
      DIMENSION DI(2)
C
      IF (IMX-2)5,7,6
5 Y=ARGY(1)
  GO TO 95
C LINEAR EXTRAPOLATIONS ARE PERFORMED
6 IF(X-ARGX(1))7,7,8
7 IE=1
  NE=2
  GO TO 10
8 IF(X-ARGX(IMX))15,9,9
9 IE=IMX
  NE=IMX-1
10 Y=ARGY(IE)+(ARGY(NE)-ARGY(IE))*(X-ARGX(IE))/(ARGX(NE)-ARGX(IE))
  GO TO 95
15 IM1=IMX-1
  IREF=2
  DI(2)=ABS(ARGX(2)-X)
  DO 30 I=2,IM1
  DI(1)=ABS(ARGX(I)-X)
  IF(DI(1)-DI(2))20,30,30
20 IREF=I
  DI(2)=DI(1)
30 CONTINUE
  I=IREF
40 X1=ARGX(I+1)
  X2=ARGX(I)
  X3=ARGX(I-1)
  Y1=ARGY(I+1)
  Y2=ARGY(I)
  Y3=ARGY(I-1)
70 A=((Y1-Y2)*(X2-X3)-(Y2-Y3)*(X1-X2))/((X1**2-X2**2)*(X2-X3)
  1 -(X2**2-X3**2)*(X1-X2))
  B=((Y2-Y3)-A*(X2**2-X3**2))/(X2-X3)
  Y=A*(X**2-X2**2)+B*(X-X2)+Y2
95 RETURN
  END
I1AP0001
I1AP0002
I1AP0003
I1AP0004
I1AP0005
I1AP0006
I1AP0007
I1AP0008
I1AP0009
I1AP0010
I1AP0011
I1AP0012
I1AP0013
I1AP0014
I1AP0015
I1AP0016
I1AP0017
I1AP0018
I1AP0019
I1AP0020
I1AP0021
I1AP0022
I1AP0023
I1AP0024
I1AP0025
I1AP0026
I1AP0027
I1AP0028
I1AP0029
I1AP0030
I1AP0031
I1AP0032
I1AP0033
I1AP0034
I1AP0035
I1AP0036
I1AP0037
I1AP0038
I1AP0039
I1AP0040
I1AP0041
I1AP0042

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SUBROUTINE INTPL8 (XA,ZA,TABX,TABY,TABZ,NC,NY,NZ,ANS)	INT80001
COMMON/B12678/ JTAPE,IPRINT	INT80002
DIMENSION TABX(1),TABY(1),TABZ(1),NRX(8),NPY(8),YY(8),TABXN(8),	INT80003
1 TABYN(8),TABZN(8)	INT80004
IN=1	INT80005
CALL UNS (NC,IA,IDX,IDZ,IMS)	INT80006
IF (NZ-1) 5,5,10	INT80007
5 IF(XA.GT.TABX(NZ).OR.XA.LT.TABX(1)) IN=IN+2	INT80008
IF(XA.GT. TABX(NZ)) XA=TABX(NZ)	INT80009
IF(XA.LT.TABX(1)) XA=TABX(1)	INT80010
CALL DISSER(XA,TABX,1,NY,IDX,NN)	INT80011
NN=IDX+1	INT80012
NNM=NN-1	INT80013
DO 7 K=1,NNN	INT80014
NNMK=NAM+K	INT80015
TABXN(K)=TABX(NNMK)	INT80016
7 TABYN(K)=TABY(NNMK)	INT80017
CALL LAGRAN (XA,TABXN,TABYN,NNN,ANS)	INT80018
GO TO 615	INT80019
10 ZARG=ZA	INT80020
IP1X=IDX+1	INT80021
IP1Z=IDZ+1	INT80022
15 IF(ZARG.GT.TABZ(NZ).OR.ZARG.LT.TABZ(1)) IN=IN+1	INT80023
IF(ZARG.GT.TABZ(NZ)) ZARG=TABZ(NZ)	INT80024
IF(ZARG.LT.TABZ(1)) ZARG=TABZ(1)	INT80025
25 CALL DISSER (ZARG,TABZ,1,NZ,IDZ,NPZ)	INT80026
NX=NY/NZ	INT80027
NPZL=NPZ+IDZ	INT80028
I=1	INT80029
IF (IMS) 30,30,40	INT80030
30 CALL DISSER (XA,TABX,1,NX,IDX,NPX)	INT80031
DO 35 JJ=NPZ,NPZL	INT80032
NPY(I)=(JJ-1)*NX+NPX	INT80033
NRX(I)=NPX	INT80034
35 I=I+1	INT80035
GOTO 50	INT80036
40 DO 45 JJ=NPZ,NPZL	INT80037
IS=(JJ-1)*NX+1	INT80038
CALL DISSER (XA,TABX,IS,NX,IDX,NPX)	INT80039
NPY(I)=NPX	INT80040
NRX(I)=NPX	INT80041
45 I=I+1	INT80042
50 INN=0	INT80043
DO 55 I=1,IP1Z	INT80044
XH=XA	INT80045
NLOC =NRX(I)-1	INT80046
NLOCY=NPY(I)-1	INT80047
DO 53 K=1,IP1X	INT80048
NLOCK=NLOC+K	INT80049
NLOCYK=NLOCY+K	INT80050
TABXN(K)=TABX(NLOCK)	INT80051
53 TABYN(K)=TABY(NLOCYK)	INT80052
IF(XA.GT.TABX(NLOCK).OR.XA.LT.TABX(NLOC+1)) INN=INN+1	INT80053
IF(XA.GT.TABX(NLOCK)) XH=TABX(NLOCK)	INT80054
IF(XA.LT.TABX(NLOC+1)) XH=TABX(NLOC+1)	INT80055
CALL LAGRAN(XH,TABXN,TABYN,IP1X,AN)	INT80056
55 YY(I)=AN	INT80057
IF(INN.GT.0) IN=IN+2	INT80058
NPZN=NPZ-1	INT80059
DO 60 K=1,IP1Z	INT80060

NPZNK=NPZN+K	INT80061
60 TABZN(K)=TABZ(NPZNK)	INT80062
CALL LAGRAN (ZARG,TABZN,YY,IP1Z,ANS)	INT80063
615 IF(IN.EQ.1) GO TO 70	INT80064
WRITE(JTAPE,4)	INT80065
GO TO (70,620,621,622),IN	INT80066
620 WRITE(JTAPE,1)	INT80067
RETURN	INT80068
621 WRITE(JTAPE,2)	INT80069
RETURN	INT80070
622 WRITE(JTAPE,3)	INT80071
1 FORMAT(33H DATA EXTRAPOLATED IN Z DIRECTION)	INT80072
2 FORMAT(33H DATA EXTRAPOLATED IN X DIRECTION)	INT80073
3 FORMAT(37H DATA EXTRAPOLATED IN BOTH DIRECTIONS)	INT80074
4 FORMAT(1X////////18H *** ERROR MESSAGE)	INT80075
70 RETURN	INT80076
END	INT80077
\$IBFTC UN	
SUBROUTINE UNS (IC,IA,IDX,IDZ,IMS)	INT80078
IF (IC) 5,5,10	INT80079
5 IMS=1	INT80080
NC=-IC	INT80081
GOTO 15	INT80082
10 IMS=0	INT80083
NC=IC	INT80084
15 IF (NC-100) 20,25,25	INT80085
20 IA=0	INT80086
GOTO 30	INT80087
25 IA=1	INT80088
NC=NC-100	INT80089
30 IDX=NC/10	INT80090
IDZ=NC-IDX*10	INT80091
RETURN	INT80092
END	INT80093
\$IBFTC LAGR	
SUBROUTINE LAGRAN (XA,X,Y,N,ANS)	INT80094
DIMENSION X(1),Y(1)	INT80095
SUM=0.0	INT80096
DC 3 I=1,N	INT80097
PROD=Y(I)	INT80098
DC 2 J=1,N	INT80099
A=X(I)-X(J)	INT80100
IF (A) 1,2,1	INT80101
1 B=(XA-X(J))/A	INT80102
PROD=PROD*B	INT80103
2 CONTINUE	INT80104
3 SUM=SUM+PROJ	INT80105
ANS=SUM	INT80106
RETURN	INT80107
END	INT80108
\$IBFTC DISS	
SUBROUTINE DISSER (XA,TAB,I,NX,IO,NPX)	INT80109
DIMENSION TAB(1)	INT80110
NPT=IO+1	INT80111
NPB=NPT/2	INT80112
NPU=NPT-NPB	INT80113
IF (NX-NPT) 10,5,10	INT80114
5 NPX=I	INT80115
RETURN	INT80116
10 NLOW=I+NPB	INT80117
	INT80118

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```
NUPP=I+NX-(NPU+1)
DO 15 II=NLOW,NUPP
NLOC=II
IF (TAB(II)-XA) 15,20,20
15 CONTINUE
NPX=NUPP-NPB+1
RETURN
20 NL=NLOC-NPB
NU=NL+ID
DO 25 JJ=NL,NU
NDIS=JJ
IF (TAB(JJ)-TAB(JJ+1)) 25,30,25
25 CONTINUE
NPX=NL
RETURN
30 IF (TAB(NDIS)-XA) 40,35,35
35 NPX=NDIS-ID
RETURN
40 NPX=NDIS+1
RETURN
END
```

```
INT80119
INT80120
INT80121
INT80122
INT80123
INT80124
INT80125
INT80126
INT80127
INT80128
INT80129
INT80130
INT80131
INT80132
INT80133
INT80134
INT80135
INT80136
INT80137
INT80138
INT80139
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 \$IBFTC AIRF LIST
 SUBROUTINE AIRFLO

S U B R O U T I N E A I R F L O

THIS SUBROUTINE CALCULATES AIRFLOW CONDITIONS IN THE
 FLAME TUBE AND ANNULUS OF A COMBUSTION CHAMBER.

FOUR SUBROUTINES ARE CALLED BY AIRFLO

1. EQUAN - SOLUTION TO ANNULUS EQUATIONS
2. DISJET - JET PARAMETERS RELATING TO FLOW
THROUGH HOLES IN THE FLAME TUBE
3. EQUFT - SOLUTION TO FLAME TUBE EQUATIONS
4. PRTEMP - CALCULATION OF PRIMARY ZONE TEMP.

ONE SUBROUTINE CALLS AIRFLO

1. CLARE

COMMON STATEMENTS

C THIS SUBROUTINE USES COMMON BLOCKS WHOSE NAMES CONTAIN THE NUMBER 6
 C VIZ- B6, B16, B67, B68, B126, B167, B168, B678, B1678, B12678
 C ALSO B4 (SHARED WITH EMPCTS AND TUBCTS)
 C BZERO IS A DUMMY BLOCK, USED INSTEAD OF A DIMENSION STATEMENT

COMMON/B4/DPREF

COMMON/B16/CDS(20,15),DPHS(20,15),FLCV,IH, NABX(45)

1,NSP(20),GXIS(20,15),K4,K6,FIT,FIPHI,FIPSI,FIA,FITAU,FID,FIENTH

2,SHAFST, FIFTPR, LCMFL,LCANIL

3,LCANL,LCFTEL,LCFTL,LCPRTL,BETA,ASW,FFIZ(45),AHDOME,NSCOOP(20)

4,LCPTAL,PAFRZ,NHTU(50),AF23A(3),AF23B(3),XAF23A(3),XAF23B(3)

COMMON/B68/AFANA(45),AFANB(45),AFFT(45),AFPRZ,C2A(45),C2B(45)

2,AFSYP,FARFT(45),DENANA(45),DENANB(45)

3,SAFTRA(45),SAFTRB(45),QTRA(45),QTRB(45),REAN(45),REBAN(45)

4,TWA(45),TWB(45)

COMMON/B168/AANA(45),AANB(45),CCA(45),CCB(45),FPCR,NLAST

1,KANHET,LANHET,PERCO,THIKFT

2,DANA(45),DANB(45)

COMMON/B67/DENFT(45),EK17,EK19,EK20, EK16

1 ,C(50),GXIA(50),K,WUJ(50)

COMMON/B167/GASC,GRAVC,GJCULE,IHJ(50),XH(50),NH

COMMON/B678/PREFT(45),PREANA(45),PREANB(45),TFT(45),TANANA(45),TANA

IANB(45),AFJ1(50),UFT(45)

COMMON/B1678/NSHCP,XCP(45),AFT(45),PI

1,NHH(50),KJSN(45,6),HAU(50),CFTA(45),CFTB(45),NAB(50),NCODEA(45)

2,NCODEB(45),TZ

COMMON/B12678/JTAPE,IPRINT

COMMON/B126/AF2,TAN1A,TAN1B,PAN1A,PAN1B

1, AFA,AFB,PREDM,STAGT,IBL,STPREF,PNTRA,PNTRB,DPHSNT,DOMLOS

COMMON/B6/PREAN1,PREAN2,DENAN1,DENAN2,TAN1,TAN2,AAN1,AAN2,AFAN1,

1AFAN2,UAN1,UAN2,ZAJM(45),ZMH(45),ZZCP,K1,K11,J,KSH,LANB(45),

2FARL,FAR,ZSTOC,AFFT1,AFFT1,TFT1,TFT2,HRRATE,

3ZMJUJ(45),ZMJET(45),CD,GXI,DPH1, PREFT1,PREFT2,

4DENFT1,DENFT2,AFT1,AFT2,AFFT2,UFT1,UFT2,FARFT1,

5FARFT2,ENTHAL,LCMF,LCANI,LCAN,LCFTE,LCFT,K7,K13,K12,

6AFSYP,AFSYPB,AFSYIA,AFSYIB,LCPRT,LCPTA

7,C2(45), UANA(45), ZMHA(2),GXIA,GX1B

8,DPH(50),WCD(50),WFFIZ(45),DPAFS,DPBFS,DPAES,DPBES

9,RC(50),A,B,D,E,K30,K40,K50,K60

AIRF0010
 AIRF0020
 AIRF0030
 AIRF0040
 AIRF0050
 AIRF0060
 AIRF0070
 AIRF0080
 AIRF0090
 AIRF0100
 AIRF0110
 AIRF0120
 AIRF0130
 AIRF0140
 AIRF0150
 AIRF0160
 AIRF0170
 AIRF0180
 AIRF0190
 AIRF0200
 AIRF0210
 AIRF0220
 AIRF0230
 AIRF0240
 AIRF0250
 AIRF0260
 AIRF0270
 AIRF0280
 AIRF0290
 AIRF0300
 AIRF0310
 AIRF0320
 AIRF0330
 AIRF0340
 AIRF0350
 AIRF0360
 AIRF0370
 AIRF0380
 AIRF0390
 AIRF0400
 AIRF0410
 AIRF0420
 AIRF0430
 AIRF0440
 AIRF0450
 AIRF0460
 AIRF0470
 AIRF0480
 AIRF0490
 AIRF0500
 AIRF0510
 AIRF0520
 AIRF0530
 AIRF0540
 AIRF0550
 AIRF0560
 AIRF0570
 AIRF0580
 AIRF0590

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COMMON/B5867/XFSA,XFSB AIRF0600
COMMON/B126E/AF1,AF3,AF4,AFS,N,NSH,KK1 AIRF0610
COMMON/BZERO/DFFT(50),FRICFA(45),FRICFB(45),HAW(50),AFJZ(50), AIRF0620
IDUM(360) AIRF0630
COMMON/BUNIK/DUMAE(45),DUMBE(45) AIRF0640
COMMON/B126D/AFCL,AFCU,AFSL,AFSU AIRF0650
DIMENSION DOOM(4),Q(9) AIRF0660
AIRF0670
AIRF0680
AIRF0690
AIRF0700

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C FORMAT STATEMENTS

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1 FORMAT(8HOREACHEDI3) AIRF0710
20 FORMAT(/////49HOAERODYNAMIC PARAMETERS AT EACH CALCULATION POINT/1AIRF0710
1X48(1H-)/6HOAXIAL6X23HTOTAL TOTAL PRESSURE7X15HSTATIC PRESSURE6AIRF0720
2X55HBULK VELOCITY MACH NUMBER ACCUMULATED PRESSURE/18H POAIRF0730
3SITION TEMPER2(8X4HPSIA9X), 4X10HFT PER SEC25X18HLOSS IN ANNULI AIRF0740
4PSI/5H FROM7X6H-ATURE/14H COMPRESSOR IN6X2(8H ANNULI5X5HFLAME3X),AIRF0750
52(18H ANNULI FLAME ),7H DUE TO6X6HDUE TO/17H DISCHARGE FLAME2AIRF0760
6(16X5HTUBE ),2(14X4HTUBE),24H FRICTION AND EXPANSION/16H INCHES AIRF0770
7 TUBE2(15H INNER OUTER6X),2(3X11HINNER OUTER4X),2X13HHEAT ADDAIRF0780
8ITION/12X5HDEG F79X2(12H INNER OUTER)/12X6HSTATIC/12X7HTEMP IN/12XAIRF0790
97HANNULUS/12X5HDEG F/9X11HINNER OUTER//) AIRF0795
C **INCLUDE CARDS AIRF0795 AND 0805 ** AIRF0800
21 FORMAT(58HOCOMBUSTOR TOTAL-PRESSURE LOSS COEFFT FOR INNER ANNULUS AIRF0800
1 =F7.4/41H (RELATIVE TO REFERENCE DYNAMIC PRESSURE)/58HOCOMBUSTOR AIRF0810
2TOTAL-PRESSURE LOSS COEFFT FOR OUTER ANNULUS =F7.4/66HOTOTAL-PRESAIRF0820
3SURE LOSS FACTOR FOR COMBINED DIFFUSER AND COMBUSTOR =F7.4/43H (RAIRF0830
4RELATIVE TO COMPRESSOR DELIVERY PRESSURE)/58HOCOMBUSTOR TOTAL-PRESSAIRF0840
5SURE LOSS FACTOR FOR INNER ANNULUS =F7.4/58HOCOMBUSTOR TCTAL-PRESSAIRF0850
6SURE LOSS FACTOR FOR OUTER ANNULUS =F7.4/58HOEXPANSION TOTAL-PRESSAIRF0860
7SURE LOSS FACTOR FOR INNER ANNULUS =F7.4/58HOEXPANSION TOTAL-PRESSAIRF0870
8SURE LOSS FACTOR FOR OUTER ANNULUS =F7.4/76HOPRESSURE-LOSS FACTOR AIRF0880
9DUE TO FRICTION AND HEAT ADDITION FOR INNER ANNULUS =F7.4/76HOPREAIRF0890
XSSURE-LOSS FACTOR DUE TO FRICTION AND HEAT ADDITION FOR OUTER ANNUAIRF0900
XLUS =F7.4) AIRF0910
C ** THERE ARE NO CARDS AIRF 0930,0940,0950,0960 ** AIRF0920
38 FORMAT(/////20HOAIR MASS FLOW SPLIT/1X19(1H-)/58HCFRACTION OF INLEAIRF0970
1T AIR PASSING THROUGH SNOUT AND/OR DOME =F8.5/49H FRACTION OF INLEAIRF0980
2T AIR PASSING INTO INNER ANNULUS8X1H=F8.5/49H FRACTION OF INLET AIAIRF0990
3R PASSING INTO OUTER ANNULUS8X1H=F8.5) AIRF1000
42 FORMAT(1XF8.3,F9.1,0F7.2,3F6.1,3F6.3,4F6.2) AIRF1010
67 FORMAT(1XF13.1,F7.1) AIRF1020
C ** THERE ARE NO CARDS AIRF 1040 THROUGH 1120 * AIRF1030
1000 FORMAT(40H PROGRAMME STOPPED IN SUBROUTINE AIRFLO.,/31H LOOP COUNTAIRF1130
1ER *LCANL* EXCEEDED.,/31H MAX CALL FOR *EQUAN* EXCEEDED.) AIRF1140
1001 FORMAT(40H PROGRAMME STOPPED IN SUBROUTINE AIRFLO.,/31H LOOP COUNTAIRF1150
1ER *LCFTL* EXCEEDED.,/31H MAX CALL FOR *EQUFT* EXCEEDED.) AIRF1160
1002 FORMAT(90H IN SUBROUTINE AIRFLO THE MAXIMUM NUMBER OF ITERATIONS OAIRF1170
IN THE AIR FLOW SPLIT WAS EXCEEDED.) AIRF1180
1003 FORMAT(59H INCREASE ITERATION CYCLE LIMIT *LCANIL* OR TOLERANCE *FAIRF1190
110*) AIRF1200
1004 FORMAT(88H THE COMBUSTOR IS BADLY DESIGNED - NEGATIVE PRESSURE DROAIRF1210
IP IS OCCURRING ACROSS THE HOLES./80H TO REMEDY - 1. IF ANNULUS VELAIRF1220
CITIES GREATER THAN 300 FPS, OPEN UP THE ANNULUS./13X31H2. INCREAAIRF1230
3SE SIZE OF WALL HOLES./13X25H3. REDUCE DOME HOLE AREA./13X35H4. USAIRF1240
4E MORE SCOOPS OVER WALL HOLES.) AIRF1250
1005 FORMAT(54H AIR FLOW RESULTS FOR THE LAST ITERATION CYCLE FOLLOW.) AIRF1260
3000 FORMAT(1X,/////19H *** ERROR MESSAGE) AIRF1270
8761 FORMAT(1H03F11.3) AIRF1280
8762 FORMAT(1H04I10) AIRF1290
8763 FORMAT(1H03I10,10X6I10) AIRF1300

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8764 FORMAT(7H0AIRCON3F9.1,7F11.7,I10)
8765 FORMAT(1H010F11.3)
C    AIR FLOW PROGRAM
      GC TC 7
      ENTRY AIR1
      LD=IPRINT
      LDD=0
      IF(KANHET.NE.0)GOTC9999
C    QUANTITIES OBTAINED FROM SUBROUTINE HEAT,SET TO ZERO IF HEAT HAS
C    NCT BEEN CALLED
      DC9998K=1,NLAST
      C2A(K)=0.
      C2B(K)=0.
      WFFIZ(K)=0.
      REAAN(K)=1.E4
      REBAN(K)=1.E4
      QTRA(K)=0.0
      QTRB(K)=0.0
9998 CCNTINUE
9999 CONTINUE
      DO 2012 J=1,NH
2012 AFJ1(J)=0.
      IF(IPRINT.NE.1)GOTC8760
      WRITE(6,8765)(HAU(J),XH(J),J=1,20)
      WRITE(6,8765)FLCV,BETA,ASW,AHDOME
      WRITE(6,8762)(NFH(J),NHTU(J),NAB(J),IHJ(J),J=1,20)
      WRITE(6,8765)(FFIZ(K),CFTA(K),CFTB(K),AANA(K),AANB(K),CCA(K),CCB(K),
1),DANA(K),DANB(K),AFT(K),K=1,26)
      WRITE(6,8763)(NABX(K),NCODEA(K),NCODEB(K),(KJSN(K,I),I=1,6),K=1,26)
1)
      WRITE(6,8765)
1
2
3IH=1,3)
      WRITE(6,8763)NLAST,MSHCP
8760 CONTINUE
C    SETTING OF CONTROL PARAMETERS.
7    CONTINUE
      NSTOP=0
      LCANI=0
      LCANJ=0
      FITAV=FITAU/2.
      DCOM(1)=AFCU
      DCOM(2)=AFCL
      DCOM(3)=AFSL
      DCOM(4)=AFSU
C    ITERATION LCOP COUNTERS SET TO ZERO
97  LCAN=0
      LCFT=0
C    K1=0  INNER ANNULUS.
C    K1=1  OUTER ANNULUS.

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AIRF1310
AIRF1320
AIRF1330
AIRF1340
AIRF1350
AIRF1360
AIRF1370
AIRF1380
AIRF1390
AIRF1400
AIRF1410
AIRF1420
AIRF1430
AIRF1440
AIRF1450
AIRF1460
AIRF1470
AIRF1480
AIRF1490
AIRF1500
AIRF1510
AIRF1520
AIRF1530
AIRF1540
AIRF1550
AIRF1560
AIRF1570
AIRF1580
AIRF1590
AIRF1600
AIRF1610
AIRF1620
AIRF1630
AIRF1640
AIRF1650
AIRF1660
AIRF1670
AIRF1680
AIRF1690
AIRF1700
AIRF1710
AIRF1720
AIRF1730
AIRF1740
AIRF1750
AIRF1760
AIRF1770
AIRF1780
AIRF1790
AIRF1800
AIRF1810
AIRF1820
AIRF1830
AIRF1840
AIRF1850
AIRF1860
AIRF1870
AIRF1880
AIRF1890
AIRF1900

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*.....*
C   K2=0  ANNULUS EQUATIONS ONLY. AIRF1910
C   K2=1  ANNULUS AND FLAMETUBE EQUATIONS. AIRF1920
C   K3=0  FOR FIRST SECONDARY HOLE. AIRF1930
C   K3=1  FOR SECONDARY HOLE. AIRF1940
C   K5=0  FOR ANNULUS A. AIRF1950
C   K5=1  FOR ANNULUS B. AIRF1960
C   K10=0 FIRST TIME THROUGH EACH ANNULUS AIRF1970
C   K20=0 FIRST TIME THROUGH EACH ANNULUS WITH FLAME TUBE EQUATIONS AIRF1980
C   BEING SOLVED AIRF1990
AIRF2000
K1=0 AIRF2010
K2=0 AIRF2020
K3=0 AIRF2030
K5=0 AIRF2040
K10=0 AIRF2050
K20=0 AIRF2060
AIRF2070
C   SET JET PARAMETERS OBTAINED IN SUBROUTINE DISJET TO ZERO AIRF2080
AIRF2090
EK16=0.0 AIRF2100
EK17=0.0 AIRF2110
EK19=0.0 AIRF2120
EK20=0.0 AIRF2130
AIRF2140
C   PRESSURE LOSS DUE TO EXPANSION AND FRICTIONAL EFFECTS IN ANNULI AIRF2150
C   USED ONLY FOR PRINTING OUT RESULTS AIRF2160
AIRF2170
DPAES=0.0 AIRF2180
DPAFS=0.0 AIRF2190
DPBFS=0.0 AIRF2200
DPBES=0.0 AIRF2210
AIRF2220
C   INTEGERS USED IN SUBROUTINE DISJET TO FIX PRESSURE REVERSAL OR AIRF2230
C   NEGATIVE AIR MASS FLOW IN THE ANNULI FOR THE WHOLE COMBUSTOR AIRF2240
AIRF2250
K30=0 AIRF2260
K40=0 AIRF2270
K50=0 AIRF2280
K60=0 AIRF2290
AIRF2300
C   CCNSTANT IN SWIRLER PRESSURE LOSS EQUATION AIRF2310
AIRF2320
ZZKSW=1.3 AIRF2330
AIRF2340
C   CLEARING SUMMARY ON LOCATIONS. AIRF2350
AIRF2360
DO 99 K=1,NLAST AIRF2370
ZMJET(K)=0.0 AIRF2380
ZAJM(K)=0.0 AIRF2390
ZMJUJ(K)=0.0 AIRF2400
ZMH(K)=0.0 AIRF2410
99 CONTINUE AIRF2420
AIRF2430
C   AIR MASS FLOW IN PRIMARY ZONE AIRF2440
AIRF2450
AFPRZ=0.0 AIRF2460
AIRF2470
C   AIR FLOW IN SNOOT. AIRF2480
AIRF2490
IF(LC=FL.NE.1)CALLDIFLW AIRF2500

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*.....*.....*.....*.....*.....*.....*.....*.....*.....*
IF(IPRINT.NE.1)GOTO8759
WRITE(6,8765)AF2,TAN1A,TAN1B,PAN1A,PAN1B,AFA,AFB,PREDM,STAGT,STPRE
IF,PNTA,PNTRB,DPHSNT,COMLOS
8759 CONTINUE
IF(IPRINT.GE.1.CR.LCMFL.EG.1)WRITE(JTAPE,20)
C TEST CONVERGENCE INDEX, SET IN SUBROUTINE DIFLW
IF(1BL)100,900,100
C AIR MASS FLOW THROUGH DOME
100 AFS=AF2-AFA-AFB
AFPRZ=AFS
C PRESSURE IN THE PRIMARY ZONE.
K=1
J=K
GO TO 124
145 K10=1
IF(K1)90,90,105
C PRESSURE IN THE DOME
90 PREDM=PREDM-DCMLOS*DPHSNT
IF(PREDM.LE.0.)NSTOP=1
DENDM=PREDM/(GASC*STAGT)
C TEST K6=0 NO SWIRLER.
C K6=1 SWIRLER.
80 IF(K6)102,102,101
C PRESSURE IN PRIMARY ZONE BEFORE COMBUSTION
101 PREFT(K)=PREDM-0.5*AFS**2/(GRAVC*DENDM*(0.6*AHDCME+ASH*AFT(K)/
1SCRT(ZZKSW*((AFT(K)/COS(BETA))**2-ASH**2))**2)
IF(PREFT(K).LT..2*PREDM)PREFT(K)=.2*PREDM
PREFT1=PREFT(K)
GO TO 103
102 PREFT(K)=PREDM-AFS**2/(DENDM*.36*AHDDOME**2*GRAVC)*0.5
IF(PREFT(K).LT..2*PREDM)PREFT(K)=.2*PREDM
PREFT1=PREFT(K)
C INITIAL CONDITIONS FOR ANNULUS A.
103 IF(NSHCP.EG.1)GOTO1031
DO1030I=1,NSHCP
1030 PREFT(I)=PREFT(1)
1031 AFAN1=AFA
DENAN1=PAN1A/(GASC*TAN1A)
TAN1=TAN1A
UAN1=AFAN1/(DENAN1*AANA(K))
PREAN1=PAN1A
K1=0
DENANA(1)=DENAN1
AFANA(1)=AFAN1
PREANA(1)=PREAN1
UANA(1)=UAN1
AIRF2510
AIRF2520
AIRF2530
AIRF2540
AIRF2550
AIRF2560
AIRF2570
AIRF2580
AIRF2590
AIRF2600
AIRF2610
AIRF2620
AIRF2630
AIRF2640
AIRF2650
AIRF2660
AIRF2670
AIRF2680
AIRF2690
AIRF2700
AIRF2710
AIRF2720
AIRF2730
AIRF2740
AIRF2750
AIRF2760
AIRF2770
AIRF2780
AIRF2790
AIRF2800
AIRF2810
AIRF2820
AIRF2830
AIRF2840
AIRF2850
AIRF2860
AIRF2870
AIRF2880
AIRF2890
AIRF2900
AIRF2910
AIRF2920
AIRF2930
AIRF2940
AIRF2950
AIRF2960
AIRF2970
AIRF2980
AIRF2990
AIRF3000
AIRF3010
AIRF3020
AIRF3030
AIRF3040
AIRF3050
AIRF3060
AIRF3070
AIRF3080
AIRF3090
AIRF3100

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TANANA(1)=TAN1
GO TO 105

AIRF3110
AIRF3120
AIRF3130
AIRF314C
AIRF3150
AIRF3160
AIRF3170
AIRF3180
AIRF3190
AIRF3200
AIRF3210
AIRF3220
AIRF3230
AIRF3240
AIRF3250
AIRF3260
AIRF3270
AIRF3280
AIRF3290
AIRF3300
AIRF3310
AIRF3320
AIRF3330
AIRF3340
AIRF3350
AIRF3360
AIRF3370
AIRF3380
AIRF3390
AIRF3400
AIRF3410
AIRF3420
AIRF3430
AIRF3440
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AIRF3470
AIRF3480
AIRF3490
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AIRF3520
AIRF3530
AIRF3540
AIRF3550
AIRF3560
AIRF3570
AIRF3580
AIRF3590
AIRF3600
AIRF3610
AIRF3620
AIRF3630
AIRF3640
AIRF3650
AIRF3660
AIRF3670
AIRF3680
AIRF3690
AIRF3700

C INITIAL CONDITIONS FOR ANNULUS B.

104 AFAN1=AFB
DENAN1=PAN1B/(GASC+TAN1B)
TAN1=TAN1B
K=1
UAN1=AFAN1/(DENAN1+AANB(K))
PREAN1=PAN1B
DENANB(1)=DENAN1
TANANB(1)=TAN1
UANB(1)=UAN1
PREANB(1)=PREAN1
AFANB(1)=AFAN1
K20=1
K1=1
J=K

C TEST FOR ANNULUS AND FLAME-TUBE EQUATIONS.

GO TO 124
851 K20=0

C DYNAMIC PRESSURE IN ANNULUS.

105 DYPAN1=0.5*DENAN1*UAN1**2/GRAVC
DPH1=1.0+(PREAN1-PREFT1)/DYPAN1

C LCCP CCOUNTER INDEXED AND TESTED FOR ANNULUS EQUATION SOLUTIONS.

LCAN=LCAN+1
IF(LCANL-LCAN)404,404,405
404 CCNTINUE
WRITE(JTAPE,3000)
WRITE(JTAPE,1000)
RETURN

C TEST FOR INNER OR OUTER ANNULUS

405 IF(K1)106,106,107

C SET ANNULUS AREAS AND HEAT CONVECTION INNER ANNULUS

106 AAN1=AANA(K)
AAN2=AANA(J)
C2(K)=C2A(K)
GO TO 108

C SET ANNULUS AREAS AND HEAT CONVECTION, OUTER ANNULUS

107 AAN1=AANB(K)
AAN2=AANB(J)
C2(K)=C2B(K)
108 CCNTINUE

C TEST ANNULUS AIR MASS FLOW, IF NEGATIVE SET ANNULUS PARAMETERS AND
C DO NOT CALL SUBROUTINE EQUAN

```

*.....*.....*.....*.....*.....*.....*.....*.....*.....*
  IF(AFANI)60,60,53
60  PREAN2=PREAN1
    DENAN2=DENAN1
    TAN2=TAN1
    UAN2=0.01
53  CALL DISJET
C   IF PRESSURE REVERSAL OCCURS OR AIR MASS FLOW IS NEGATIVE DO NOT CALL
C   SUBROUTINE EQUAN
  IF(ZMH(K)-AFANI)59,56,56
59  IF(DPH1.LE.0.0)GO TO 56
    CALL ECUAN
    GO TO 52
C   SET ANNULUS PARAMETERS
56  AFAN2=AFAN1
    PREAN2=PREAN1
    TAN2=TAN1
    UAN2=UAN1
    DENAN2=DENAN1
52  KSH=K
C   TEST FOR SECONDARY HOLES
  IF(KSH.EQ.NSHCP)GOTO1325
  K=J
C   TEST IF ANNULUS AND FLAME TUBE EQUATIONS ARE BEING SOLVED.
701 IF(K2)124,124,95
95  J=K+1
    GO TO 134
C   TEST FOR HOLE AT NEXT CALCULATION POINT.
C   NABX(K)=1 HOLES ON INNER WALL ONLY.
C   NABX(K)=2 HOLES ON OUTER WALL ONLY.
C   NABX(K)=3 HOLES ON BOTH WALLS.
C   NABX(K)=4 NO HOLES.
124 IF(NLAST-J+1)134,6,6
   6 IF(J.EQ.NSHCP .OR.NABX(J+1).LE.3)GOTO126
125 J=J+1
    GO TO 124
126 IF(NABX(J+1)-2)127,127,133
127 IF(K1)128,128,131
128 IF(NABX(J+1)-1)132,133,132
131 IF(NABX(J+1)-1)132,132,133
132 J=J+1
    GO TO 124
1325 K=KSH+1
     J=K
133 J=J+1
C   IS THIS THE FIRST TIME ANNULUS EQUATIONS HAVE BEEN SOLVED
C   TOGETHER WITH FLAME TUBE EQUATIONS FOR THE CURRENT ANNULUS
  IF(K20)850,850,851

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```

AIRF3710
AIRF3720
AIRF3730
AIRF3740
AIRF3750
AIRF3760
AIRF3770
AIRF3780
AIRF3790
AIRF3800
AIRF3810
AIRF3820
AIRF3830
AIRF3840
AIRF3850
AIRF3860
AIRF3870
AIRF3880
AIRF3890
AIRF3900
AIRF3910
AIRF3920
AIRF3930
AIRF3940
AIRF3950
AIRF3960
AIRF3970
AIRF3980
AIRF3990
AIRF4000
AIRF4010
AIRF4020
AIRF4030
AIRF4040
AIRF4050
AIRF4060
AIRF4070
AIRF4080
AIRF4090
AIRF4100
AIRF4110
AIRF4120
AIRF4130
AIRF4140
AIRF4150
AIRF4160
AIRF4170
AIRF4180
AIRF4190
AIRF4200
AIRF4210
AIRF4220
AIRF4230
AIRF4240
AIRF4250
AIRF4260
AIRF4270
AIRF4280
AIRF4290
AIRF4300

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*.....*.....*.....*.....*.....*.....*.....*.....*.....*
LAN1=UAN2
PREAN1=PREAN2
DENAN1=DENAN2
TAN1=TAN2
AFAN1=AFAN2
GX1B=GX1
C TEST IF ANNULUS AND FLAMETUBE EQUATIONS ARE BEING SOLVED.
IF(K2)138,138,151
C TEST FOR SECONDARY HOLES.
138 IF(KSH-NSHCP)105,139,105
C TEST FOR SPECIFICATION OF FLOW SPLIT
139 IF(K4)147,147,142
C SPECIFICATION OF FLOW SPLIT.
C FLOW SPLIT FOR A SECONDARY HOLES.
141 AFSYPA=ZMHAS*SHAFST
AFSYIA=ZMHAS-AFSYPA
AFPRZ=AFPRZ+AFSYPA
GO TO 104
C FLOW SPLIT FOR B SECONDARY HOLES.
142 AFSYPB=ZMH(KSH)*SHAFST
AFSYIB=ZMH(KSH)-AFSYPB
AFPRZ=AFPRZ+AFSYPB
CALL PRTEMP
GO TO 151
C SET FLOW SPLIT =0.5 FIRST ITERATION A ANNULUS
94 AFSYIA=0.5*ZMHAS
AFSYPA=AFSYIA
AFPRZ=AFPRZ+AFSYPA
ZMHA(1)=ZMHAS
GO TO 104
C SET FLOW SPLIT =0.5 FIRST ITERATION B ANNULUS
147 AFSYIB=0.5*ZMH(K-1)
AFSYPB=AFSYIB
AFPRZ=AFPRZ+AFSYPB
ZMHA(2)=ZMH(KSH)
CALL PRTEMP
GO TO 151
C SOLUTION OF FLAME TUBE EQUATIONS.
150 K2=1
K1=1
J=J-1
K=K-1
C SET ANNULUS PARAMETERS FOR USE IN SUBROUTINE EQUAN

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```

AIRF4910
AIRF4920
AIRF4930
AIRF4940
AIRF4950
AIRF4960
AIRF4970
AIRF4980
AIRF4990
AIRF5000
AIRF5010
AIRF5020
AIRF5030
AIRF5040
AIRF5050
AIRF5060
AIRF5070
AIRF5080
AIRF5090
AIRF5100
AIRF5110
AIRF5120
AIRF5130
AIRF5140
AIRF5150
AIRF5160
AIRF5170
AIRF5180
AIRF5190
AIRF5200
AIRF5210
AIRF5220
AIRF5230
AIRF5240
AIRF5250
AIRF5260
AIRF5270
AIRF5280
AIRF5290
AIRF5300
AIRF5310
AIRF5320
AIRF5330
AIRF5340
AIRF5350
AIRF5360
AIRF5370
AIRF5380
AIRF5390
AIRF5400
AIRF5410
AIRF5420
AIRF5430
AIRF5440
AIRF5450
AIRF5460
AIRF5470
AIRF5480
AIRF5490
AIRF5500

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*.....*.....*.....*.....*.....*.....*.....*.....*.....*
C      MACH NUMBER IN ANLLUS AND FLAME TUBE
      AA=UANA(K)/((SQRT(1.40*TANANA(K)*GASC*GRAVC)))
      AB=UANB(K)/((SQRT(1.40*TANANB(K)*GASC *GRAVC))
      AF=UFT(K)/((SQRT(1.33*TFT(K)*GASC *GRAVC))
AIRF6110
AIRF6120
AIRF6130
AIRF6140
AIRF6150
AIRF6160
AIRF6170
AIRF6180
AIRF6190
AIRF6200
AIRF6210
AIRF6220
AIRF6230
AIRF6233
AIRF6237
AIRF6240
AIRF6250
AIRF6260
AIRF6270
AIRF6280
AIRF6290
AIRF6300
AIRF6310
AIRF6320
AIRF6330
AIRF6340
AIRF6350
AIRF6360
AIRF6370
AIRF6380
AIRF6385
AIRF6390
AIRF6400
AIRF6410
AIRF6413
AIRF6417
AIRF6420
AIRF6430
AIRF6440
AIRF6450
AIRF6460
AIRF6470
AIRF6480
AIRF6490
AIRF6500
AIRF6510
AIRF6520
AIRF6530
AIRF6540
AIRF6550
AIRF6560
AIRF6570
AIRF6580
AIRF6590
AIRF6600
AIRF6610
AIRF6620
AIRF6630
AIRF6640
AIRF6650

C      TCTAL TEMPERATURE IN FLAME TUBE
      TFTTOT=TFT(K)+0.5*UFT(K)**2/(GRAVC+ZZCP*GJCULE)-459.7
AIRF6220
AIRF6230
AIRF6233
AIRF6237
AIRF6240
AIRF6250
AIRF6260
AIRF6270
AIRF6280
AIRF6290
AIRF6300
AIRF6310
AIRF6320
AIRF6330
AIRF6340
AIRF6350
AIRF6360
AIRF6370
AIRF6380
AIRF6385
AIRF6390
AIRF6400
AIRF6410
AIRF6413
AIRF6417
AIRF6420
AIRF6430
AIRF6440
AIRF6450
AIRF6460
AIRF6470
AIRF6480
AIRF6490
AIRF6500
AIRF6510
AIRF6520
AIRF6530
AIRF6540
AIRF6550
AIRF6560
AIRF6570
AIRF6580
AIRF6590
AIRF6600
AIRF6610
AIRF6620
AIRF6630
AIRF6640
AIRF6650

C      UNITS CONVERSION
C      ** INCLUDE CARDS AIRF6233 AND 6237 **
      TANANA(K)=TANANA(K)-459.7
      TANANB(K)=TANANB(K)-459.7
      XCP(K)=XCP(K)*12.
      PREANA(K)=PREANA(K)/144.
      PREANB(K)=PREANB(K)/144.
      PREFT(K)=PREFT(K)/144.
      PSA=PSA/144.
      PSB=PSB/144.
      PSF=PSF/144.
      IF(K.NE.1)GCTC 980
      PSAIN=PSA
      PSBIN=PSB
980    DPARS=PSAIN-PSA-DUMAE(K)
      DPBRB=PSBIN-PSB-DUMBE(K)
      WRITE(JTAPE,42)XCP(K),TFTTOT,PSA,PSB,PSF,PREANA(K),PREANB(K),
1    PREFT(K),UANA(K),UANB(K),UFT(K),AA,AB,AF,DPARS,DPBRB,
2    DUMAE(K),DUMBE(K)
      WRITE(JTAPE,67)TANANA(K),TANANB(K)
C      ** INCLUDE CARD AIRF6385 **
C      UNITS CONVERSION
C      ** INCLUDE CARDS AIRF6413 AND 6417 **
      TANANA(K)=TANANA(K)+459.7
      TANANB(K)=TANANB(K)+459.7
      PREANA(K)=PREANA(K)*144.
      PREANB(K)=PREANB(K)*144.
      PREFT(K)=PREFT(K)*144.
      IF(!PRINT,NE.1)GOTO8758
      WRITE(6,8765)XCP(K),UANA(K),TANANA(K),AFANA(K),AFANB(K),
1    PREAN1,PREFT1,ZZCP,GASC,GRAVC
8758  CCNTINUE
      IF(NSTCP.EQ.1)STOP
      XCP(K)=XCP(K)/12.
      IF(K.GE.NSHCP)GCTO906
      K=K+1
      GOTO9070
906   CCNTINUE
C      TEST FOR END OF FLAMETUBE.
      IF(K+1-NLAST)157,9060,138
CC     INDEX TO NEXT CALCULATION POINT
9060  K=NLAST
      GCTO908
157   K=K+1
      J=K+1

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.....*

SET ANNULUS PARAMETERS FOR SUBROUTINE EQUAN

UAN)=UANA(K)
 PREANI=PREANA(K)
 DENANI=DEANA(K)
 TANI=TANANA(K)
 AFANI=AFANA(K)
 GC TO 105

ITERATION CONTROL TO ADJUST MASS FLOWS.
 AIR MASS FLOW REMAINING IN EACH ANNULUS

	AIRF6660
	AIRF6670
	AIRF6680
	AIRF6690
	AIRF6700
	AIRF6710
	AIRF6720
	AIRF6730
	AIRF6740
	AIRF6750
	AIRF6760
	AIRF6770
	AIRF6780
	AIRF6790
158	AIRF6800
	AIRF6810
	AIRF6820
	AIRF6830
	AIRF6840
	AIRF6850
	AIRF6860
	AIRF6870
	AIRF6880
	AIRF6890
	AIRF6900
	AIRF6910
	AIRF6920
	AIRF6930
	AIRF6940
	AIRF6950
	AIRF6960
	AIRF6970
	AIRF6980
	6990
	AIRF7000
	AIRF7010
	AIRF7020
	AIRF7030
	AIRF7040
	AIRF7050
	AIRF7060
	AIRF7070
	AIRF7080
	AIRF7090
	AIRF7100
	AIRF7110
	AIRF7120
	AIRF7130
	AIRF7140
	AIRF7150
	AIRF7160
	AIRF7170
	AIRF7180
	AIRF7190
	AIRF7200
	AIRF7210
	AIRF7220
	AIRF7230
	AIRF7240
	AIRF7250

8750 IF (PSF.GT.1.E10) PSF=1.E10
 STREFF=STREF/144.
 Q(1)=(PSAIN-PSF)/DPREF*144.
 Q(2)=(PSBIN-PSF)/DPREF*144.
 Q(3)=(STREFF-PSF)/STREFF
 Q(4)=(PSAIN-PSF)/STREFF
 Q(5)=(PSBIN-PSF)/STREFF
 Q(6)=DUMAE(NLAST)/STREFF
 Q(7)=DUMBE(NLAST)/STREFF
 Q(8)=DPAES/STREFF
 Q(9)=DPERE/STREFF
 IF (IPRINT.GE.1.OR.LCMFL.EQ.1)
 1WRITE (JTAPE,21)(Q(K),K=1,9)
 AF1=AFS/AF2
 AF3=AFA/AF2
 AF4=AFB/AF2
 IF (IPRINT.GE.1)
 1WRITE (JTAPE,38) AF1, AF3, AF4
 ZAFB=AFB
 AFSS=AFS

LCOP COUNTER INDEXED AND TESTED FOR MA*/MAMB*/MB ITERATION.

LCANI=LCANI+1
 IF (K30+K40.GE.1) LCANJ=LCANI
 IF (LCMFL.EQ.1) GOTO 163
 IF (LCANI.LE.LCANIL) GOTO 403
 WRITE (JTAPE,3000)
 WRITE (JTAPE,1002)
 IF (LCANIL.LE.45) WRITE (JTAPE,1003)
 IF (LCANJ.GE.35) WRITE (JTAPE,1004)
 WRITE (JTAPE,1005)
 LANHET=2
 GO TO 163

TEST IF MA* IS APPROX. 0.

403 IF (AFSTA*AFSTB.LT.0.) GOTO 160

```

*.....*.....*.....*.....*.....*.....*.....*.....*.....*
IF(ABS(AFSTA+AFSTB)/2./AF2.LE.FID)GOTO163
C      MODIFICATION OF MA AND MB.
      IF((AFSTA+AFSTB).GT.0.)GOTO1615
      IF(AFS.LT.AFSU)AFSU=AFS
      AFS=AMAX1(AFS*(1.-FITAU),(AFSL+AFSU)/2.)
      GOTO1616
1615  IF(AFS.GT.AFSL)AFSL=AFS
      AFS=AMIN1(AFS*(1.+FITAU),(AFSL+AFSU)/2.)
C      NEW AIR MASS FLOW IN INNER ANNULUS
1616  AFA=AFA-(AFS-AFSS)/2.
C      NEW AIR MASS FLOW IN OUTER ANNULUS
      AFB=AF2-AFA-AFS
      GC TO 97
C      MODIFICATION OF MA AND MB.
160  AFD=AFA+AFB
      AFC=AFA/AFD
      IF(AFSTA.GE.0.)GOTO159
      IF(AFC.GT.AFCL)AFCL=AFC
      AFC=AMIN1(AFC*(1.+FITAV),(AFCL+AFCU)/2.)
      GOTO1590
159  IF(AFC.LT.AFCU)AFCU=AFC
      AFC=AMAX1(AFC*(1.-FITAV),(AFCL+AFCU)/2.)
C      NEW AIR MASS FLOW IN INNER ANNULUS
1590  AFA=AFC+AFD
      AFB=AFD-AFA
      IF(AFB.LE.0.0)STOP
      GO TO 97
163  IF(LDD.EQ.1)GOTO911
      IF(KANHET.NE.0)GOTO909
      IF(LANHET.EQ.1)GOTO9000
909  LDD=1
      LD=1
      LCMFL=1
      IPN=IPRINT
      IPRINT=1
      CALL CIFLW
      IPRINT=IPN
      GOTO97
911  CCNTINUE
      CALL BIRFLO
779  CCNTINUE
900  RETURN
9000  AFCU=DCCM(1)
      AFCL=DCCM(2)
      AFSL=DCCM(3)
      AFSU=DCCM(4)
      GOTO 900
      END
AIRF7260
AIRF7270
AIRF7280
AIRF7290
AIRF7300
AIRF7310
AIRF7320
AIRF7330
AIRF7340
AIRF7350
AIRF7360
AIRF7370
AIRF7380
AIRF7390
AIRF7400
AIRF7410
AIRF7420
AIRF7430
AIRF7440
AIRF7450
AIRF7460
AIRF7470
AIRF7480
AIRF7490
AIRF7500
AIRF7510
AIRF7520
AIRF7530
AIRF7540
AIRF7550
AIRF7560
AIRF7570
AIRF7580
AIRF7590
AIRF7600
AIRF7610
AIRF7620
AIRF7630
AIRF7640
AIRF7650
AIRF7660
AIRF7670
AIRF7680
AIRF7690
AIRF7700
AIRF7710
AIRF7720
AIRF7730
AIRF7740
AIRF7750
AIRF7760
AIRF7770
AIRF7780
AIRF7790
AIRF7800
AIRF7810
AIRF7820
AIRF7830

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BFTC BIRF LIST
SUBROUTINE BIRFLO

S U B R O U T I N E B I R F L O

THIS SUBROUTINE IS A CONTINUATION OF SUBROUTINE AIRFLO

NC SUBROUTINES ARE CALLED BY AIRFLO

CNE SUBROUTINE CALLS BIRFLC

1. AIRFLO

THIS SUBROUTINE USES COMMON BLOCKS WHOSE NAMES CONTAIN THE NUMBER 6.
BZERO IS A DUMMY BLOCK, USED INSTEAD OF A DIMENSION STATEMENT

COMMON/B4/DPREF

COMMON/B16/CDS(20,15),DPHS(20,15),FLCV,IH, NABX(45)
1,NSP(20),GXIS(20,15),K4,K6,FIT,FIPFI,FIPSI,FIA,FITAL,FID,FIETH
2,SHAFST, FIFTPR, LCPFL,LCANIL
3,LCANL,LCFTEL,LCFTL,LCPRTL,BETA,ASH,FFI2(45),AHCOME,NSCOOP(20)
4,LCPTAL,PAFRZ,NHTU(50),AF23A(3),AF23B(3),XAF23A(3),XAF23B(3)
COMMON/B68/AFANA(45),AFANB(45),AFFT(45),AFPRZ,C2A(45),C2B(45)
2,AFSYP,FARFT(45),DENANA(45),DENANB(45)
3,SAFTRA(45),SAFTRB(45),QTRA(45),QTRB(45),REAN(45),REBAN(45)
4,TWA(45),TWB(45)

COMMON/B168/AANA(45),AANB(45),CCA(45),CCB(45),FHCR,NLAST

1,KANHET,LANHET,PERCC,THIKFT

2,DANA(45),DANB(45)

COMMON/B67/DENFT(45),EK17,EK19,EK20, EK16

1,C(50),GXIA(50),K,WUJ(50)

COMMON/B167/GASC,GRAVC,GJOLE,IHJ(50),XH(50),NH

COMMON/B678/PREFT(45),PREANA(45),PREANB(45),TFT(45),TANANA(45),TANB

1ANB(45),AFJ1(50),UFT(45)

COMMON/B1678/NSHCP,XCP(45),AFT(45),PI

1,NHH(50),KJSN(45,6),HAU(50),CFTA(45),CFTB(45),NAB(50),NCODEA(45)

2,NCODEB(45),TZ

COMMON/B12678/JTAPE,IPRINT

COMMON/B126/AF2,TAN1A,TAN1B,PAN1A,PAN1B

1,AFA,AFB,PREDM,STAGT,IBL,STPREF,PNTA,PNTRB,DPHSNT,DOPLS

COMMON/B6/PREAN1,PREAN2,DENAN1,DENAN2,TAN1,TAN2,AAN1,AAN2,AFAN1,

1AFAN2,UAN1,UAN2,ZAJM(45),ZMH(45),ZZCP,K1,K11,J,KSH,UANB(45),

2FARL,FAR,ZSTOC,AFFT1,AFFT2,TFT1,TFT2,RRATE,

3ZMJUJ(45),ZMJET(45),CD,GXI,DPH1,

PREFT1,PREFT2,

4DENFT1,DENFT2,AFT1,AFT2,AFFT2,UFT1,UFT2,FARFT1,

5FARFT2,ENTHAL,LCMF,LCANI,LCAN,LCFTE,LCPT,K7,K13,K12,

6AFBYP,AFBYPB,AFBYIA,AFBYIB,LCPT,LCPTA

7,C2(45), UANA(45), ZMHA(2),GX1A,GX1B

8,DPH(50),hCC(50),HFFI2(45),DPAPS,DPBPS,DPARS,DPBES

9,RC(50)

1,A,B,D,E

2,K30,K40,K50,K60

COMMON/BZERO/CFFT(50),FRICFA(45),FRICFB(45),HAM(50),AFJZ(50),

1DUP(360)

COMMON/BUNIK/DUMAE(45),DUMBE(45)

COMMON/B126D/AFCL,AFCU,AFSL,AFSU

COMMON/B5867/XFSA,XFSB

COMMON/B126E/AF1,AF3,AF4,AFS,N,NSH,KK1

25 FORMAT(/////25NONISCELLANEOUS QUANTITIES/1X24(1H-)/56H0 AXIAL POSBIRF0057

1ITION RATE OF BURNING FRICTION FACTOR/10H FRCH COMPRESSORBIRF0058

20X7HOF FUEL11X9MIN ANNULI/6X9HDISCHARGE7X15MLBM PER SEC PER/7X6MINBIRF0059

- BIRFOCC1
- BIRFO002
- BIRFO003
- BIRFO004
- BIRFO005
- BIRFO006
- BIRFO007
- BIRFO008
- BIRFO009
- BIRFO010
- BIRFO011
- BIRFOCC12
- BIRFO013
- BIRFO014
- BIRFO015
- BIRFO016
- BIRFO017
- BIRFO018
- BIRFO019
- BIRFO020
- BIRFO021
- BIRFO022
- BIRFO023
- BIRFO024
- BIRFO025
- BIRFO026
- BIRFO027
- BIRFO028
- BIRFO029
- BIRFO030
- BIRFO031
- BIRFO032
- BIRFO033
- BIRFO034
- BIRFO035
- BIRFO036
- BIRFO037
- BIRFO038
- BIRFO039
- BIRFO040
- BIRFO041
- BIRFO042
- BIRFO043
- BIRFO044
- BIRFO045
- BIRFO046
- BIRFO047
- BIRFO048
- BIRFO049
- BIRFO050
- BIRFO051
- BIRFO052
- BIRFO053
- BIRFO054
- BIRFO055
- BIRFO056
- BIRFO057
- BIRFO058
- BIRFO059

```

*.....*.....*.....*.....*.....*.....*.....*.....*.....*
3 CHES8X35HFT AXIAL DISTANCE INNER OUTER// (5XF8.3,11XF8.3,7X2FBIRF0060
49.5) BIRF0061
38 FORMAT(/////20HOAIR MASS FLOW SPLIT/1X19(1H-)/5EFCFRACTION OF INLETBIRF0062
1T AIR PASSING THROUGH SNOUT AND/OR DCME =F8.5/49H FRACTION OF INLETBIRF0063
2T AIR PASSING INTO INNER ANNULUS8X1H=F8.5/49H FRACTION OF INLET AIRBIRF0064
3R PASSING INTO OUTER ANNULUS8X1H=F8.5) BIRF0065
54 FORMAT(/////41HOQUANTITIES RELATED TO FLOW THROUGH HOLES/1X40(1H-)BIRF0066
1/16HOLE ROW AXIAL6X95HOLE INNER NUMBER HOLE DISCHARGE COEFFBIRF0067
2EFFICIENTS EFFECT INITIAL INITIAL FRACTION ACCUM-/37H NUMBER BIRF0068
3 POSITION TYPE OR IN6X5HPRESS27X11H-IVE JET6X11HJET VEBIRF0069
4L OF8X6HULATED/11X8HFROM COM9X91FCUTER THIS -URE CORRECT REBIRF0070
5ATIO ACTUAL HOLE ANGLE -OCITY CURRENT FRACTION/11X8H-BIRF0071
6PRESSOR9X33HWALL HOLE LOSS -ED OF14X44HAREA DEGREESBIRF0072
7 FT PER ANNULUS OF INLET/11X9HDISCHARGE15X14FCW FACTOR1CBIRF0073
8X7HACTUAL 9X5HSC FT12X3HSEC6X16HAIR FLOW AIR IN/11X6HINCHES42X6HTBIRF0074
9C COR36X15HTHROUGH FLAME/59X6HRECTED36X5HHOLES5X4HTUBE //(1X15,F1BIRF0075
12.3,17,15,19,F10.2,4F8.3,F8.2,F10.2,F8.3,F10.3)) BIRF0076
73 FORMAT(/////26HSECONDARY HOLE FLOW SPLIT/1X24(1H-)/71HOFRACTION CBIRF0077
1F SECONDARY HOLE AIR RECIRCULATING UPSTREAM FOR INNER WALL =F5.4/7BIRF0078
21HOFRACTION OF SECONDARY HOLE AIR RECIRCULATING UPSTREAM FOR OUTERBIRF0079
3 WALL =F5.4) BIRF0080
DC 2 K=1,NLAST BIRF0081
XCP(K)=XCP(K)*12. BIRF0082
BIRF0083
C FRICTION FACTOR BIRF0084
FRICFA(K)=.0035+.264*REAN(K)**(-.42) BIRF0086
FRICFB(K)=.0035+.264*REBAN(K)**(-.42) BIRF0087
2 CCNTINUE BIRF0088
WRITE(JTAPE,25)(XCP(K),WFFIZ(K),FRICFA(K),FRICFB(K),K=1,NLAST) BIRF0089
DO 3 K=1,NLAST BIRF0090
XCP(K)=XCP(K)/12. BIRF0091
3 CCNTINUE BIRF0092
NSH=KJSN(1,1) BIRF0093
DC 901 K=1,NLAST BIRF0094
DO 902 I=1,6 BIRF0095
IF(KJSN(K,I))902,902,903 BIRF0096
903 KK1=KJSN(K,I) BIRF0097
IF(NHTU(KK1).GE.1)CCT057 BIRF0098
AFJ1(KK1)=0. BIRF0099
DPH(KK1)=0. BIRF0100
WCD(KK1)=0. BIRF0101
HAU(KK1)=0. BIRF0102
BIRF0103
C RATIO OF ACTUAL TO CORRECTED DISCHARGE COEFFICIENT EFF HOLE AREA BIRF0104
57 RC(KK1)=C(KK1)/WCD(KK1) BIRF0105
HAW(KK1)=HAU(KK1)*C(KK1)*FLOAT(NHH(KK1)) BIRF0108
IF(CXHU(KK1).NE.0.0) GO TO 631 BIRF0109
IF(NAB(KK1).EQ.1) HAW(KK1)=HAW(KK1)*CFTA(K) BIRF0110
IF(NAB(KK1).EQ.2) HAW(KK1)=HAW(KK1)*CFTB(K) BIRF0111
BIRF0112
C ACCUMULATED FRACTION OF INLET AIR IN FLAME TUBE BIRF0113
631 IF(KK1.EQ.NSH)DFFT(KK1)=AF1 +AFJ1(KK1)/AF2 BIRF0115
IF(KK1.NE.NSH)DFFT(KK1)=DFFT(KK1-1)+AFJ1(KK1 )/AF2 BIRF0116
BIRF0117
C FRACTION OF ANNULUS AIR FLOW THROUGH HOLES BIRF0118
BIRF0119

```

200

```
.....*.....*.....*.....*.....*.....*.....*.....*.....*
IF(NAB(KK1).EQ.1)AFJZ(KK1)=AFJ1(KK1)/AFANA(K)      BIRF0120
IF(NAB(KK1).EQ.2)AFJZ(KK1)=AFJ1(KK1)/AFANB(K)      BIRF0121
902 CONTINUE                                         BIRF0122
K1=(KJSN(K,1)-1)                                    BIRF0123
IF(K1.LT.1)K1=KK1                                   BIRF0124
IF(K.EQ.1)AFFT(K)=A+S                               BIRF0125
901 IF(K.NE.1)AFFT(K)=CFFT(K1)*AF2                 BIRF0126
DO 4 KK1=NSH,NH                                     BIRF0127
                                                    BIRF0128
C INITIAL JET ANGLE                                 BIRF0129
C UNITS CONVERSION                                  BIRF0130
                                                    BIRF0131
GXIA(KK1)=GXIA(KK1)*180./PI                         BIRF0132
XH(KK1)=XH(KK1)*12.                                 BIRF0133
4 CONTINUE                                           BIRF0134
WRITE(JTAPE,54)(KK1,XH(KK1),NHTU(KK1),NAB(KK1),NHH(KK1),DPH(KK1),WBIRF0135
ICD(KK1),RC(KK1),C(KK1),HAW(KK1),GXIA(KK1),WUJ(KK1),AFJZ(KK1),DFFT(BIRF0136
2KK1),KK1=NSH,NH)                                  BIRF0137
DO 5 KK1=NSH,NH                                     BIRF0138
C UNITS CONVERSION                                  BIRF0139
GXIA(KK1)=GXIA(KK1)*PI/180.                         BIRF0140
XH(KK1)=XH(KK1)/12.                                 BIRF0141
5 CONTINUE                                           BIRF0142
346 XFSAQ=1.0-XFSA                                   BIRF0143
XFSBQ=1.0-XFSB                                       BIRF0144
WRITE(JTAPE,73)XFSAQ,XFSBQ                           BIRF0145
WRITE(JTAPE,38)AF1,AF3,AF4                           BIRF0146
IF(NSHCP.EQ.1)GOTO779                                BIRF0147
N=NSHCP-1                                             BIRF0148
DO778K=1,N                                           BIRF0149
778 FARFT(K)=FARFT(NSHCP)                            BIRF0150
779 CONTINUE                                         BIRF0151
900 RETURN                                           BIRF0152
END                                                    BIRF0153
```

YOUR CARD TOTAL IS ---

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```

*.....*.....*.....*.....*.....*.....*.....*.....*.....*
      8765 FCRMAT(7HODISJET3I11,7F11.3/(7X10F11.3))
C      DISCHARGE CCEFFICIENT AND JET ANGLE
      F=NLAST
C      SET HOLE AREA TO ZERO
      THA=0.0
C      SPECIFIC HEAT AT CONSTANT PRESSURE
      TA1=TAN1
      ZCPT=.2419*TA1-.8181E-5*TA1**2/2.+17.91E-9*TA1**3/3.-2.742E-12*
1     TA1**4/4.-102.42
      CC 116 I=1,6
C      ARE THERE ANY MORE HOLES AT THIS CALCULATION POINT
      IF(KJSN(K,I))117,117,109
109   KK1=KJSN(K,I)
      DPH(KK1)=CPH1
      IF(K1)110,110,111
C      ARE HOLES ON THE CURRENT ANNULUS
111   IF(NAB(KK1)-2)116,112,116
110   IF(NAB(KK1).NE.1)GOTO116
112   KKK=KK1
      HNHH=NHH(KKK)
      IH=IHJ(KK1)
      THA=HNHH*HAU(KKK)
      NSPN=NSP(IH)
      IF(MCD(NSCCCP(IH),10).NE.2)GOTO1125
C      HOLE AREA FOR COOLING SLOTS
      IF(NAB(KKK).EQ.1)THA=HAU(KKK)*CCA(K)
      IF(NAB(KKK).EQ.2)THA=HAU(KKK)*CCB(K)
C      HAS PRESSURE REVERSAL OCCURRED PREVIOUSLY
1125  IF(NAB(KK1).EQ.1.AND.K30.EQ.1)GOTO150
      IF(NAB(KK1).EQ.2.AND.K40.EQ.1) GOTO150
C      HAS ANNULUS AIR FLOW BEEN NEGATIVE PREVIOUSLY
      IF(NAB(KK1).EQ.1.AND.K50.EQ.1) GOTO500
      IF(NAB(KK1).EQ.2.AND.K50.EQ.1) GOTO500
C      TRANSFER HOLE DATA TO DUMMY STORE
      CC 113 I3 = 1,NSPN
      DUMDPH(I3)=DPHS(IH,I3)
      DUMCD(I3)=CDS(IH,I3)
      DUMGXI(I3)=GXIS(IH,I3)
113   CCNTINUE
      IF(DPH1.LE.0.)GO TO 150
      DUMNSP=NSP(IH)
      DPHILG=ALOG(DPH1)
DISJ0600
DISJ0610
DISJ0620
DISJ0630
DISJ0640
DISJ0650
DISJ0660
DISJ0670
DISJ0680
DISJ0690
DISJ0700
DISJ0710
DISJ0720
DISJ0730
DISJ0740
DISJ0750
DISJ0760
DISJ0770
DISJ0780
DISJ0790
DISJ0800
DISJ0810
DISJ0820
DISJ0830
DISJ0840
DISJ0850
DISJ0860
DISJ0870
DISJ0880
DISJ0890
DISJ0900
DISJ0910
DISJ0920
DISJ0930
DISJ0940
DISJ0950
DISJ0960
DISJ0970
DISJ0980
DISJ0990
DISJ1000
DISJ1010
DISJ1020
DISJ1030
DISJ1040
DISJ1050
DISJ1060
DISJ1070
DISJ1080
DISJ1090
DISJ1100
DISJ1110
DISJ1120
DISJ1130
DISJ1140
DISJ1150
DISJ1160
DISJ1170
DISJ1180
DISJ1190

```



```
.....*.....*.....*.....*.....*.....*.....*.....*.....*
IF(CDC.GT.1.5*CD)CDC=1.5*CD
```

```
TEST FOR NO JET ANGLE DATA.
```

```
IF(NSCCCP(IH).NE.10.AND.NSGOOP(IH).NE.11)GOTO19C
```

```
191 DMAXL=ALOG(256.0)
```

```
CALLI1AP1(DMAXL,CC,DUMDPH,DUMCD,NS?N)
```

```
CDINF=CC
```

```
CDINFC=CDINF*(0.25*CP/PREFT1+0.75)
```

```
AA=CDC/CDINFC
```

```
IF(AA.GT.1.0)AA=1.0
```

```
GXI=AR SIN(SQRT(AA))
```

```
190 CD=CDC
```

```
TEST ANNULUS AIR FLOW
```

```
IF(AFAN1.LE.0.0)GO TO 500
```

```
GC TO 115
```

```
SET JET PARAMETERS
```

```
500 ZAJM(K)=0.0
```

```
ZMJET(K)=0.0
```

```
ZMF(K)=0.0
```

```
ZMJUJ(K)=0.0
```

```
AFJ(KK1)=0.0
```

```
GXIA(KK1)=0.0
```

```
C(KK1)=0.0
```

```
UH(KK1)=0.0
```

```
SET AIR FLOW PARAMETERS
```

```
AFHH=ABS(.6*THA*AFAN1*SQRT(ABS(DPH1))/AAN1)
```

```
IF(AFHH.GT.AF2/F/4.)AFHH=AF2/F/4.
```

```
CCONTINUE
```

```
AFAN1=AFAN1-AFHH
```

```
AFAN2=AFAN1
```

```
PREAN2=PREAN1
```

```
TAN2=TAN1
```

```
UAN2=LAN1
```

```
DENAN2=DENAN1
```

```
IF(NAB(KK1).EQ.1)K50=1
```

```
IF(NAB(KK1).EQ.2)K60=1
```

```
GC TO 116
```

```
C CALCULATE JET AIR MASS FLOW RATE
```

```
115 AFJ(KK1)=CD*AFAN1*THA*DPH1**0.5/AAN1
```

```
C(KK1)=CD
```

```
GXIA(KK1)=GXI
```

```
AFJ1(KK1)=AFJ(KK1)
```

```
JET VELOCITY.
```

```
AAA=2.*(PREAN1+.5*DENAN1*UAN1**2/GRAVC-PREFT1)*GRAVC/DENAN1
```

```
IF(AAA.LE.0.0)AAA=0.0
```

```
UH(KK1)=SQRT(AAA)
```

```
WUJ(KK1)=UH(KK1)
```

```
AXIAL JET MOMENTUM.
```

```
DISJ1800
```

```
DISJ181C
```

```
DISJ1820
```

```
DISJ1830
```

```
DISJ184C
```

```
DISJ1850
```

```
DISJ1860
```

```
DISJ1870
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```
DISJ1880
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```
DISJ1890
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```
DISJ1900
```

```
DISJ1910
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```
DISJ1920
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```
DISJ1930
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```
DISJ1940
```

```
DISJ1950
```

```
DISJ1960
```

```
DISJ1970
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```
DISJ1980
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```
DISJ1990
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```
DISJ2000
```

```
DISJ2010
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```
DISJ2020
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```
DISJ2030
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```
DISJ2040
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```
DISJ2050
```

```
DISJ2060
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```
DISJ2070
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```
DISJ2080
```

```
DISJ2090
```

```
DISJ2100
```

```
DISJ2110
```

```
DISJ2120
```

```
DISJ2130
```

```
DISJ214C
```

```
DISJ2150
```

```
DISJ2160
```

```
DISJ2170
```

```
DISJ2180
```

```
DISJ2190
```

```
DISJ2200
```

```
DISJ221C
```

```
DISJ222C
```

```
DISJ2230
```

```
DISJ2240
```

```
DISJ2250
```

```
DISJ226C
```

```
DISJ227C
```

```
DISJ2280
```

```
DISJ2290
```

```
DISJ230C
```

```
DISJ2310
```

```
DISJ2320
```

```
DISJ2330
```

```
DISJ2340
```

```
DISJ2350
```

```
DISJ2360
```

```
DISJ2370
```

```
DISJ2380
```

```
DISJ2390
```

```

*.....*.....*.....*.....*.....*.....*.....*.....*.....*
AJM=AFJ(KK1)*UH(KK1)*COS(GXI)
C  SUMMATION OF JET AIR FLOW.
ZPH(K)=ZPH(K)+AFJ(KK1)
C  IS THE NET REMAINING ANNULUS FLOW NEGATIVE
IF(IPRINT.GE.1)
1WRITE(6,8765)K,K1,KK1,DPH(KK1),C(KK1),AFJ(KK1),ZMH(K)
305 IF(ZMH(K)-AFAN1)300,300,301
301 IF(K.LT.NSHCP)AFPRZ=AFPRZ+ABS(AFAN1)
AFAN1=-AF2/F
AFAN2=AFAN1
AFJ(KK1)=0.0
ZPH(K)=0.0
ZMJUJ(K)=0.0
ZMJET(K)=0.0
ZAJM(K)=0.0
DENAN2=DENAN1
TAN2=TAN1
UAN1=0.01
PREAN2=PREAN1
IF(NAB(KK1).EQ.1)K50=1
IF(NAB(KK1).EQ.2)K60=1
IF(K.LT.NSHCP)AFPRZ=AF2
GCTO116
C  SUMMATION OF JET ENTHALPY.
300 ZMJET(K)=AFJ(KK1)* ( ZCPT *GRAVC*GJOULE+UH(KK1)**2/2.)+
1ZMJET(K)
C  SUMMATION OF AXIAL JET MOMENTUM
ZAJM(K)=ZAJM(K)+AJM
C  SUMMATION OF JET MOMENTUM.
ZMJUJ(K)=AFJ(KK1)*UH(KK1)+ZMJUJ(K)
116 CONTINUE
117 RETURN
END

```

```

DISJ2400
DISJ2410
DISJ2420
DISJ2430
DISJ2440
DISJ2450
DISJ2460
DISJ2470
DISJ2480
DISJ2490
DISJ2500
DISJ2510
DISJ2520
DISJ2530
DISJ2540
DISJ2550
DISJ2560
DISJ2570
DISJ2580
DISJ2590
DISJ2600
DISJ2610
DISJ2620
DISJ2630
DISJ2640
DISJ2650
DISJ2660
DISJ2670
DISJ2680
DISJ2690
DISJ2700
DISJ2710
DISJ2720
DISJ2730
DISJ2740
DISJ2750
DISJ2760
DISJ2770
DISJ2780
DISJ2790
DISJ2800
DISJ2810
DISJ2820
DISJ2830

```

YOUR CARD TOTAL IS ---

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	COMMON/B5867/XFSA,XFSB	PRT 0600
		PRT 0610
C	DATA STATEMENT	PRT 0620
	DATA NTOTP,PLIMIT/20,.1/	PRT 0630
		PRT 0640
C	FORMAT STATEMENTS	PRT 0650
	1 FORMAT(7H PRTEMP10F11.3)	PRT 0660
	100 FORMAT(40H PROGRAMME STOPPED IN SUBROUTINE PRTEMP.,/35H ITERATION	PRT 0670
	1LIMIT *LCPRTL* EXCEEDED.)	PRT 0680
	101 FORMAT(40H PROGRAMME STOPPED IN SUBROUTINE PRTEMP.,/35H ITERATION	PRT 0690
	1LIMIT *LCPTAL* EXCEEDED.)	PRT 0700
	3000 FORMAT(1X,////////19H *** ERROR MESSAGE)	PRT 0710
	3001 FORMAT(68H ITERATION LIMIT ON TOTAL PRESSURE LOSS DUE TO HEAT RELE	PRT 0720
	1ASE EXCEEDED)	PRT 0730
		PRT 0740
		PRT 0750
		PRT 0760
C	CALCULATION OF FLAME TUBE TEMPERATURE AT SECONDARY HOLES.	PRT 0770
C	SET LOCP COUNTER TO ZERO FOR FLOW SPLIT ITERATION	PRT 0780
		PRT 0790
	LCPTA=0	PRT 0800
		PRT 0810
C	FUEL AIR RATIO IN THE PRIMARY ZONE.	PRT 0820
		PRT 0830
	3005 FARPRZ=FFIZ(1)/AFPRZ	PRT 0840
	IF(NSHCP.EQ.1)GOTO3007	PRT 0850
	NSHCP1=NSHCP-1	PRT 0860
	DO3006K=1,NSHCP1	PRT 0870
	WFFIZ(K)=FFIZ(K+1)/(XCP(K+1)-XCP(K))	PRT 0880
	3006 FARPRZ=FARPRZ+FFIZ(K+1)/AFPRZ	PRT 0890
		PRT 0900
C	TEST IF FUEL IS AVAILABLE	PRT 0910
		PRT 0920
	3007 ZSTOC=C.0867*(1.+FHCR)/(1.+3.*FHCR)	PRT 0930
	IF(FARPRZ.GT.0.) GO TO 300	PRT 0940
	TFT1=STAGT	PRT 0950
	FARPRZ=0.0	PRT 0960
	FARL=0.0	PRT 0970
	GO TO 310	PRT 0980
		PRT 0990
C	STOICHIOMETRIC FUEL AIR RATIO.	PRT 1000
		PRT 1010
	300 CONTINUE	PRT 1020
		PRT 1030
C	TEST FOR FUEL AIR RATIO GREATER THAN STOICHIOMETRIC.	PRT 1040
C	YES PUT EQUAL TO STOICHIOMETRIC	PRT 1050
C	NO CONTINUE.	PRT 1060
		PRT 1070
	IF(ZSTCC-FARPRZ)301,302,302	PRT 1080
		PRT 1090
C	CALCULATE FUEL AIR RATIO REMAINING.	PRT 1100
		PRT 1110
	301 FARL=AMAX1(0.,FARPRZ-ZSTOC)	PRT 1120
	FARPRZ=ZSTOC	PRT 1130
	AFRPRZ=1.0/FARPRZ	PRT 1140
	GO TO 400	PRT 1150
	302 FARL=0.0	PRT 1160
	AFRPRZ=1.0/FARPRZ	PRT 1170
	400 TFT1=STAGT	PRT 1180
	FARFT(NSHCP)=FARPRZ	PRT 1190
C		PRT 1200

C	TEST LCOP COUNTER	PRT 1820
		PRT 1830
	IF(LCPTA-LCPTAL)350,350,351	PRT 1840
351	CONTINUE	PRT 1850
	WRITE(JTAPE,3000)	PRT 1860
	WRITE(JTAPE,101)	PRT 1870
	GO TO 310	PRT 1880
250	AFPRZ=AFPRZ-AFSYPA-AFSYPB	PRT 1890
	AFSYPA=ZMHA(1)*0.5*SIN(GX1A)*SQRT(TANANA(NSHCP)/TFT11)	PRT 1900
	AFSYIA=ZMHA(1)-AFSYPA	PRT 1910
	AFSYPB=ZMHA(2)*0.5*SIN(GX1B)*SQRT(TANANB(NSHCP)/TFT11)	PRT 1920
	AFSYIB=ZMHA(2)-AFSYPB	PRT 1930
	AFPRZ=AFPRZ+AFSYPA+AFSYPB	PRT 1940
		PRT 1950
C	TEST CHANGE IN FLOW SPLIT THROUGH SECONDARY HOLES	PRT 1960
		PRT 1970
	IF(ABS(AFPRZZ-AFPRZ)/AFPRZZ*100.0-PAFRZ)310,310,3005	PRT 1980
		PRT 1990
C	TOTAL PRESSURE LOSS DUE TO HEAT RELEASE IN THE PRIMARY ZONE	PRT 2000
		PRT 2010
310	DENFT(1)=PREFT(1)/STAGT/GASC	PRT 2020
	UFT(1)=AFPRZ/AFT(NSHCP)/DENFT(1)	PRT 2030
	PREFT(2)=PREFT(1)	PRT 2040
	PLAST=PREFT(2)	PRT 2050
	DO3105 I=1,NTOTP	PRT 2060
	DENFT(2)=PREFT(2)/(TFT11*(53.32+1.725*FARPRZ-1.49*FARPRZ**2))	PRT 2070
	UFT(2)=AFPRZ/AFT(NSHCP)/DENFT(2)	PRT 2080
	1*(1.+FARPRZ)	PRT 2090
	PREFT(2)=PREFT(1)+AFRPRZ/AFT(NSHCP)/32.*(UFT(1)-UFT(2)*(1.+FARPRZ)	PRT 2100
	1)	PRT 2110
	IF(ABS(PREFT(2)-PLAST).LT.PLIMIT)GOTO3106	PRT 2120
	PLAST=PREFT(2)	PRT 2130
	IF(IPRINT.EQ.1)WRITE(6,1)PREFT(2)	PRT 2140
3105	CONTINUE	PRT 2150
	WRITE(JTAPE,3000)	PRT 2160
	WRITE(JTAPE,3001)	PRT 2170
3106	CONTINUE	PRT 2180
		PRT 2190
C	FLOW PARAMETERS AT THE SECONDARY HOLES	PRT 2200
C	SET FLOW PARAMETERS UP TO THE SECONDARY HOLES TO THE SAME VALUES	PRT 2210
		PRT 2220
	DO 20 I=1,NSHCP	PRT 2230
	DENFT(I)=DENFT(2)	PRT 2240
	UFT(I)=UFT(2)	PRT 2250
	AFFT(I)=AFPRZ*(1.+FARFT(NSHCP))	PRT 2260
	TFT(I)=TFT11	PRT 2270
	PREFT(I)=PREFT(2)	PRT 2280
20	CONTINUE	PRT 2290
502	TFT2=TFT11	PRT 2300
		PRT 2310
C	PROPORTION JET PARAMETERS ACCORDING TO FLOW SPLIT	PRT 2320
		PRT 2330
	X=AFSYIB/(AFSYIB+AFSYPB)	PRT 2340
	Y=AFSYIA/(AFSYIA+AFSYPA)	PRT 2350
		PRT 2360
C	SET FLOW-SPLIT INDEX	PRT 2370
C		PRT 2380
	IF(K4)5001,5001,5002	PRT 2390
5001	XFSA=Y	PRT 2400
	XFSB=X	PRT 2410
	GO TO 5003	PRT 2420

002	XFSA=1.-SHAFST	PRT 2430
	XFSA=1.-SHAFST	PRT 2440
003	CONTINUE	PRT 2450
	ZMH(NSHCP)=AFSYIA+AFSYIB	PRT 2460
	ZMJET(NSHCP)=A*Y+X*ZMJET(NSHCP)	PRT 2470
	ZAJM(NSHCP)=E*Y+X*ZAJM(NSHCP)	PRT 2480
	ZMJUJ(NSHCP)=B*Y+ZMJUJ(NSHCP)*X	PRT 2490
	IF(IPRINT.GE.1)WRITE(6,1)AFPRZ,FARPRZ,ZSTOC,FARL,(FFIZ(K),K=1,NSHCP	PRT 2500
	1P),(WFFIZ(K),K=1,NSHCP)	PRT 2510
	RETURN	PRT 2520
	END	PRT 2530


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*.....*.....*.....*.....*.....*.....*.....*.....*.....*
C          SOLUTION OF ANNULI EQUATIONS.          ECAN0600
C          AA23=0.0                                ECAN0610
C          TEST KANHET TO SEE IF HEAT SUBPROGRAM HAS BEEN CALLED ECAN0620
C          IF IT HAS NOT, SET HEAT PARAMETERS TO EITHER TYPICAL VALUES OR ZERO ECAN0630
C          IF (KANHET.NE.0)GOTC600                ECAN0640
C          TRAN=0.0                                ECAN0650
C          PERCO=0.0                                ECAN0660
C          V=3.057E-3+8.607E-5*TAN1-2.279E-8*TAN1**2+2.908E-12*TAN1**3 ECAN0670
C          IF (K1.EQ.0)REAN(K)=3600.*DANA(K)*AFANA(K)/V/AANA(K) ECAN0680
C          IF (K1.EC.1)REBAN(K)=3600.*DANB(K)*AFANB(K)/V/AANB(K) ECAN0690
C          C2(K)=0.0                                ECAN0700
C          TWA(K)=0.0                                ECAN0710
C          TWB(K)=0.0                                ECAN0720
C          QTRA(K)=0.0                               ECAN0730
C          QTRB(K)=0.0                               ECAN0740
C          AAN3=(AAN1+AAN2)/2.                      ECAN0750
600 CCNTINUE                                       ECAN0760
C          TEST INNER OUTER ANNULUS.              ECAN0770
C          IF (K1)118,118,119                      ECAN0780
C          INNER ANNULUS                           ECAN0790
C          118 CIR=CCA(K)+CFTA(K)                   ECAN0800
C          CIRFT=CFTA(K)                            ECAN0810
C          FRICTION FACTOR                          ECAN0820
C          FRICF=.0035+.264*REAN(K)**(-.42)        ECAN0830
C          FRICFA(K)=FRICF                          ECAN0840
C          TRANSPIRATION COOLING                   ECAN0850
C          SAFTRA(K)=(PREANA(K)**2-PREFT(K)**2)*PERCO*3600./3.32/THIKFT/TWA(K) ECAN0860
C          ** INCLUDE CARDS EQAN0991 AND 0995 **    ECAN0870
C          1)/(3.057E-3+8.607E-5*TWA(K)-2.279E-8*TWA(K)**2+2.908E-12*TWA(K) ECAN0880
C          2**3)                                     ECAN0890
C          TRAN=SAFTRA(K)*CFTA(K)*(XCP(J)-XCP(K))   ECAN0900
C          GO TO 200                                 ECAN0910
C          OUTER ANNULUS                            ECAN0920
C          119 CIR=CCB(K)+CFTB(K)                   ECAN0930
C          CIRFT=CFTB(K)                            ECAN0940
C          FRICTION FACTOR                          ECAN0950
C          FRICF=.0035+.264*REBAN(K)**(-.42)        ECAN0960
C          FRICFB(K)=FRICF                          ECAN0970
C          TRANSPIRATION COOLING                   ECAN0980
C          SAFTRB(K)=(PREANB(K)**2-PREFT(K)**2)*PERCO*3600./3.32/THIKFT/TWB(K) ECAN0990
C          ** INCLUDE CARDS EQAN1161 AND 1165 **    ECAN0991
C          1)/(3.057E-3+8.607E-5*TWB(K)-2.279E-8*TWB(K)**2+2.908E-12*TWB(K) ECAN0995
C          ECAN1000
C          ECAN1010
C          ECAN1020
C          ECAN1030
C          ECAN1040
C          ECAN1050
C          ECAN1060
C          ECAN1070
C          ECAN1080
C          ECAN1090
C          ECAN1100
C          ECAN1110
C          ECAN1120
C          ECAN1130
C          ECAN1140
C          ECAN1150
C          ECAN1160
C          ECAN1161

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*.....*.....*.....*.....*.....*.....*.....*.....*.....*
2**3)
TRAN=SAFTRB(K)*CFTE(K)*(XCP(J)-XCP(K))
GC TC 201
200 DO 202 I=1,3
C BLEED AIR FOR INNER ANNULUS
IF(XAF23A(I).GT.XCP(K).AND.XAF23A(I).LE.XCP(J)+1.E-3)AA23=AA23+AF2
13A(I)
202 CONTINUE
GCTC203
201 DC 204 I=1,3
C BLEED AIR FOR OUTER ANNULUS
IF(XAF23B(I).GT.XCP(K).AND.XAF23B(I).LE.XCP(J)+1.E-3)AA23=AA23+AF2
13B(I)
204 CCNTINUE
203 CCNTINUE
F=NLAST
C TEST TGTAL FLOW FROM ANNULUS
120 IF(AA23+TRAN+ZPH(K)-AFAN1)124,124,125
C IF TOTAL FLOW IS NEGATIVE, SET ANNULUS PARAMETERS AT NEXT
125 AFAN1=-AF2/F
AFAN2=AFAN1
DENAN2=DENAN1
TAN2=TAN1
UAN2=0.001
PREAN2=PREAN1
CCNTINUE
GC TC 82
C TOTAL-PRESSURE LOSS DUE TO SUDDEN EXPANSION OF ANNULUS AIR AS IT
C PASSES ACROSS AIR ENTRY HOLE
124 DPE=0.
IF(K1.EQ.0.AND.NCODEA(K).EQ.1)GOTO1242
IF(K1.EQ.1.AND.NCODEB(K).EQ.1)GOTO1242
AA1=UAN1/SCRT(1.4*TAN1*GASC*GRAVC)
IF(AA1.GT..85)AA1=.85
DPEXP=1.85*(ZMH(K)/AFAN1/1.36)**(1./(1.5+.242*AA1**2.22))
IF(DPEXP.GT.1.2)DPEXP=1.2
DPE=DENAN1*UAN1**2/2./GRAVC*DPEXP
DPEXQ=CPE-DENAN1*UAN1**2/2./GRAVC*(1.-(1.-ZMH(K)/AFAN1)**2)
IF(IPRINT.NE.1)GOTO8755
WRITE(6,8765)PREAN1,AA1,DPEXP,DPAE,DPEXQ
8755 CCNTINUE
C
C CALCULATE GAS PROPERTIES DOWN-STREAM OF THE EXPANSION
C
ZZCP=0.2121+5.06E-5*TAN1-13.1E-9*TAN1**2+2.1E-12*TAN1**3
AFZ=AFAN1-ZPH(K)
DQ=53.3*1.4/0.4*GRAVC
TNRT=TAN1+UAN1**2/2./DQ
PNRT=PREAN1*(TNRT/TAN1)**(1.4/0.4)
PNRT=PNRT-DPE

```

ECAN1165
 ECAN1170
 EQAN1180
 ECAN1190
 ECAN1200
 ECAN1210
 ECAN1220
 ECAN1230
 EQAN1240
 ECAN1250
 ECAN1260
 EQAN1270
 EQAN1280
 ECAN1290
 ECAN1300
 ECAN1310
 ECAN1320
 ECAN1330
 ECAN1340
 EQAN1350
 ECAN1360
 ECAN1370
 ECAN1380
 ECAN1390
 ECAN1400
 ECAN1410
 EQAN1420
 ECAN1430
 ECAN1440
 EQAN1450
 ECAN1460
 EQAN1470
 ECAN1480
 ECAN1490
 ECAN1500
 ECAN1510
 EQAN1520
 EQAN1530
 ECAN1540
 ECAN1550
 EQAN1560
 EQAN1570
 ECAN1580
 ECAN1590
 ECAN1600
 EQAN1610
 ECAN1620
 ECAN1630
 EQAN1640
 ECAN1650
 ECAN1660
 ECAN1670
 EQAN1680
 ECAN1690
 EQAN1700
 EQAN1710
 ECAN1720
 EQAN1730
 EQAN1740
 ECAN1750

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.....*.....*.....*.....*.....*.....*.....*.....*.....*
ASTAR=AFZ*SCRT(DQ*TNRT*0.4)*1.2**3/PNRT/GRAVC/1.4          ECAN1760
AAS=AAN1/ASTAR                                              ECAN1770
CALL GASTBL(AAS,TTC,PPO,MNZ,1,IBL,MNX,MNV)                  ECAN1780
PREAN1=PPO*PNRT                                             ECAN1790
TAN1=TTC*TNRT                                              EQAN1800
DENAN1=PREAN1/GASC/TAN1                                    EQAN1810
UAN1=AFZ/DENAN1/AAN1                                       ECAN1820
1242 IF(K1.NE.0)GOTO1243                                    EQAN1830
CPAE=DPE/144.                                              ECAN1840
DUMAE(K)=DPAES                                             EQAN1850
DPAES=DPAES+DPAE                                           ECAN1860
GCTC1245                                                  EQAN1870
1243 DPBE=DPE/144.                                         ECAN1880
DUMBE(K)=DPBES                                             ECAN1890
DPBES=DPBES+DPBE                                          ECAN1900
                                                           ECAN191C
CALCULATION OF CONSTANTS FOR ANNULUS EQUATIONS.          ECAN192C
                                                           ECAN1930
1245 AFAN2=AFAN1-ZPH(K)-TRAN-AA23                          ECAN1940
EK2=AFAN2                                                  ECAN195C
ARQ=AAN2/AAN1                                              ECAN1960
ZZCP=0.2121+5.06E-5*TAN1-13.1E-9*TAN1**2+2.1E-12*TAN1**3 EQAN1970
EK3=(TAN1*ZZCP*GRAVC*GJCULE+0.5*UAN1**2)*EK2             ECAN198C
1+C2(K)*CIRFT*GRAVC*GJOULE*(XCP(J)-XCP(K))              ECAN1990
AAN4=2.*AAN2/(ARQ+1.)                                     EQAN2000
EK1=PREAN1*GRAVC*AAN4+UAN1*EK2                            EQAN2010
EK4=PREAN1/(DENAN1*TAN1)*GRAVC                           ECAN2020
D1=(FRICF*0.5*CIR*DENAN1*(XCP(J)-XCP(K))*                GRAVC*GJOULE*ZZCP)/(ECAN2030
1EK2*EK4*1.) *UAN1**2*(ARQ+1.)/2.                       EQAN2040
C2=.5-ZZCP*GRAVC*GJOULE /EK4*(ARQ+1.)/2.               ECAN2050
D3=ZZCP*GRAVC*GJOULE* EK1/( EK2*EK4)*(ARQ+1.)/2.-D1    ECAN2060
D4=EK3/EK2                                                EQAN2070
                                                           ECAN2080
ANNULUS VELOCITY AT NEXT CALCULATION POINT                ECAN2090
                                                           ECAN2100
IF((D3**2+4.*D2*D4).LT.0.)UAN2=UAN1                       ECAN2110
IF((D3**2+4.*D2*D4).GE.0.)                                ECAN2120
1UAN2=(-D3+SQRT(C3**2+4.*D2*D4))/(2.*D2)                  ECAN2130
                                                           ECAN2140
CALCULATE PRESSURE,DENSITY,TEMPERATURE AND AIRFLOW.      ECAN2150
                                                           ECAN216C
123 PREAN2=(EK1-UAN2*EK2-FRICF*.5*CIR*DENAN1*(XCP(J)-XCP(K))*UAN1**2)/ECAN2170
1GRAVC/AAN4                                                ECAN2180
DENAN2=AFAN2/(AAN2*UAN2)                                   ECAN2190
TAN2=PREAN2*GRAVC/(DENAN2*EK4)                             ECAN2200
IF(IPRINT.EQ.1)                                            ECAN2210
1WRITE(6,8765)UAN1,PREAN1,DENAN1,AAN1,AAN2,AFAN1,ZPH(K),TRAN, ECAN2220
1AA23,TAN1,FRICF,CIR,ZZCP,C2(K),EK1,EK2,EK4,D1,D2,D3,D4  ECAN2230
2 ,UAN2,PREAN2,AFAN2,DENAN2,TAN2                          EQAN224C
DUMBE(K+1)=DPBES                                           EQAN2250
IF(K1.EQ.1) GO TO 3654                                     EQAN2260
DUMAE(K+1)=DPAES                                           ECAN2270
                                                           ECAN2280
CALCULATION OF ANNULUS PARAMETERS AT CALCULATION POINTS HAVING NO EQAN2290
HOLES                                                       ECAN2300
                                                           ECAN2310
3654 IF(K-NSHCP.GT.0)GCTC501                               EQAN232C
N=K+1                                                       ECAN2330
DC502I=N,J                                                 EQAN2340
X1=(XCP(I)-XCP(K))/(XCP(J)-XCP(K))                       EQAN2350

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SIBFTC EQFT LIST
SUBROUTINE EQFT

S U B R C U T I N E E Q U F T .

THIS SUBROUTINE SOLVES THE EQUATIONS OF MOMENTUM, CONTINUITY,
STATE, AND ENTHALPY FOR A COMBUSTOR FLAME TUBE.

TWO SUBROUTINES ARE CALLED BY EQFT.

1. JETMIX - FOR JET PARAMETERS
2. HEATAD - FOR ENTHALPY ADDED TO FLAME
TUBE AIR BY BURNING FUEL.

ONE SUBROUTINE CALLS EQFT

1. AIRFLO

THIS SUBROUTINE USES COMMON BLOCKS WHOSE NAMES CONTAIN THE NUMBER 6
VIZ- B6, B16, B67, B68, B126, B167, B168, B678, B1678, B12678

COMMON/B16/CDS(20,15),DPHS(20,15),FLCV,IH, NABX(45)
1,NSP(20),GXIS(20,15),K4,K6,FIT,FIPHI,FIPSI,FIA,FITAU,FID,FIENTH
2,SHAFST, FIFTPR, LCMFL,LCANIL
3,LCANL,LCFTEL,LCFTL,LCPRTL,BETA,ASH,FFIZ(45),AHDOME,NSCOCP(20)
4,LCPTAL,PAFRZ,NFTU(50),AF23A(3),AF23B(3),XAF23A(3),XAF23B(3)
COMMON/B68/AFANA(45),AFANB(45),AFFT(45),AFPRZ,C2A(45),C2B(45)
2,AFSYP,FARFT(45),DENANA(45),DENANB(45)
3,SAFTRA(45),SAFTRB(45),QTRA(45),QTRB(45),REAN(45),REBAN(45)
4,TWA(45),TWB(45)
COMMON/B168/AANA(45),AANB(45),CCA(45),CCB(45),FHCR,NLAST
1,KANHET,LANHET,PERCC,THIKFT
2,DANA(45),DANB(45)
COMMON/B67/DENFT(45),EK17,EK19,EK20, EK16
1 ,C(50),GXIA(50),K,WUJ(50)
COMMON/B167/GASC,GRAVC,GJOLE,IHJ(50),XH(50),NH
COMMON/B678/PREFT(45),PREANA(45),PREANB(45),TFT(45),TANANA(45),TANANB(45),AFJ1(50),UFT(45)
1ANB(45),AFJ1(50),UFT(45)
COMMON/B1678/NSHCP,XCP(45),AFT(45),PI
1,NHH(50),KJSN(45,6),HAU(50),CFTA(45),CFTB(45),NAB(50),NCODEA(45)
2,NCCDEB(45),TZ
COMMON/B12678/JTAPE,IPRINT
COMMON/B126/AF2,TANIA,TAN1B,PANIA,PAN1B
1,AFB,AFR,PREDP,STAGT,IBL,STPREF,PNTA,PNTB,DPHSNT,COMLOS
COMMON/B6/PREAN1,PREAN2,DENAN1,DENAN2,TAN1,TAN2,AAN1,AAN2,AFAN1,
1AFAN2,UAN1,UAN2,ZAJM(45),ZMH(45),ZZCP,K1,K11,J,KSH,LANB(45),
2FARL,FAR,ZSTOC,AFFT1,AFFT1,TFT1,TFT2,HRRATE,
3ZMJUJ(45),ZMJET(45),CD,GXI,DPH1, PREFT1,PREFT2,
4DENFT1,DENFT2,AFT1,AFT2,AFFT2,UFT1,UFT2,FARFT1,
5FARFT2,ENTHAL,LCMF,LCANI,LCAN,LCFTE,LCFT,K7,K13,K12,
6AFSYPA,AFSYPB,AFSYIA,AFSYIB,LCPRT,LCPTA
7,C2(45), UANA(45), ZMHA(2),GXIA,GXIB
8,DPH(50),WCD(50),WFFIZ(45),DPAFS,DPBFS,DPAES,DPBES
9,RC(50)
1,A,B,D,E
2,K30,K40,K50,K60

EQFT0010
EQFT0020
EQFT0030
EQFT0040
EQFT0050
EQFT0060
EQFT0070
EQFT0080
EQFT0090
EQFT0100
EQFT0110
EQFT0120
EQFT0130
EQFT0140
EQFT0150
EQFT0160
EQFT0170
EQFT0180
EQFT0190
EQFT0200
EQFT0210
EQFT0220
EQFT0230
EQFT0240
EQFT0250
EQFT0260
EQFT0270
EQFT0280
EQFT0290
EQFT0300
EQFT0310
EQFT0320
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EQFT0340
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EQFT0370
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EQFT0580
EQFT0590

2 FORMAT(6H EQFT ,9E12.3/(6X,9E12.3))

3 FORMAT(1H05F12.3)

4 FORMAT(1H0I10,2F12.3)

3000 FORMAT(1X,//////19H *** ERROR MESSAGE)

4000 FORMAT(38H TEMPERATURE IN *EQFT* LESS THAN ZERO)


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.....*.....*.....*.....*.....*.....*.....*.....*.....*
TFT2=.4*TFT2+.6*TFT1
D7=TFT2
GC TO 10
11 CONTINUE
TFT2=.45*TFT2+.55*D6
D7=TFT2
C TEST CHANGE IN TEMPERATURE AGAINST SPECIFIED LIMIT
IF (ABS(D7-D6)-FIENTH)155,155,10
155 X=EK13*TFT2*(AFT2-EK14)
Y=EK11**2/(AFT2-EK17)
IF(4.*X*Y.GE.EK10**2)GOTO1555
DENFT2=(EK10+SQRT(EK10**2-4.*X*Y))/(2.*X)
GCTO1556
1555 DENFT2=EK10/2./X
1556 CCNTINUE
C FLAME TUBE PRESSURE VELOCITY AND AIR MASS FLOW RATE
PREFT2=EK13*DENFT2*TFT2/GPAVC
UFT2=AFFTT1/(DENFT2*(AFT2-EK17))
AFFT2=AFFTT1
D9=D10
IF(K8.EQ.1)GO TO 12
K8=1
D11=TFT2
D10=UFT2
GC TO 10
12 CONTINUE
D12=D11
D10=UFT2
D11=TFT2
C IS THE CHANGE IN VELOCITY LESS THAN ONE PERCENT OF PREVIOUS VELOCITY
IF (ABS(D9-D10).LE.UFT2*FIPHI.AND.ABS(D11-D12).LE.FIENTH)GCTO156
10 IF (IPRINT.GE.1)WRITE(6,2)AFFTT1,AFFT1,FAR,FARL,AFR,HRRATE,FARFT2,
1EK11,EK12,ENTHAL,TFT1,TFT2
GC TO 156
60 WRITE(JTAPE,3000)
WRITE(JTAPE,4000)
TFT2=100.
C STORE FLAME TUBE PARAMETERS
156 UFT(K+1)=UFT2
PREFT(K+1)=PREFT2
DENFT(K+1)=DENFT2
TFT(K+1)=TFT2
AFFT(K+1)=AFFT2
FARFT(K+1)=FARFT2
C
C SET UNBURNT-FUEL TO GAS RATIO
C
FARL=FARR/AFFTT1
RETURN
END

```

IBFTC HTAD LIST
SUBROUTINE HEATAD

SUBROUTINE HEATAD

THIS SUBROUTINE CALCULATES THE HEAT PRODUCED BY
THE BURNING OF FUEL IN THE COMBUSTOR FLAME TUBE.

NO SUBROUTINE IS CALLED BY HEATAD

ONE SUBROUTINE CALLS HEATAD
1. EQUFT

HTAD0010
HTAD0020
HTAD0030
HTAD0040
HTAD0050
HTAD0060
HTAD0070
HTAD0080
HTAD0090
HTAD0100
HTAD0110
HTAD0120
HTAD0130
HTAD0140
HTAD0150
HTAD0160
HTAD0170
HTAD0180
HTAD0190
HTAD0200
HTAD0210
HTAD0220
HTAD0230
HTAD0240
HTAD0250
HTAD0260
HTAD0270
HTAD0280
HTAD0290
HTAD0300
HTAD0310
HTAD0320
HTAD0330
HTAD0340
HTAD0350
HTAD0360
HTAD0370
HTAD0380
HTAD0390
HTAD0400
HTAD0410
HTAD0420
HTAD0430
HTAD0440
HTAD0450
HTAD0460
HTAD0470
HTAD0480
HTAD0490
HTAD0500
HTAD0510
HTAD0520
HTAD0530
HTAD0540
HTAD0550
HTAD0560
HTAD0570
HTAD0580
HTAD0590

THIS SUBROUTINE USES COMMON BLOCKS WHOSE NAMES CONTAIN THE NUMBER 6
VIZ- B6, B16, B67, B68, B126, B167, B168, B678, B1678, B12678

COMMON/B16/CDS(20,15),DPHS(20,15),FLCV,IH, NABX(45)
1,NSP(20),GXIS(20,15),K4,K6,FIT,FIPHI,FIPSI,FIA,FITAU,FID,FIENTH
2,SHAFST, FIFTPR, LCMFL,LCANIL
3,LCANL,LCFTEL,LCFTL,LCPRTL,BETA,ASW,FFIZ(45),AHDOME,NSCOOP(20)
4,LCPTAL,PAFRZ,NHTU(50),AF23A(3),AF23B(3),XAF23A(3),XAF23B(3)
COMMON/B68/AFANA(45),AFANB(45),AFFT(45),AFPRZ,C2A(45),C2B(45)
2,AFSYP,FARFT(45),DENANA(45),DENANB(45)
3,SAFTRA(45),SAFTRB(45),QTRA(45),QTRB(45),REAN(45),REBAN(45)
4,TWA(45),TWB(45)
COMMON/B168/AANA(45),AANB(45),CCA(45),CCB(45),FHCR,NLAST
1,KANHET,LANHET,PERCO,THIKFT
2,DANA(45),DANB(45)
COMMON/B67/DENFT(45),EK17,EK19,EK20, EK16
1,C(50),GXIA(50),K,WUJ(50)
COMMON/B167/GASC,GRAVC,GJOULE,IHJ(50),XH(50),NH
COMMON/B678/PREFT(45),PREANA(45),PREANB(45),TFT(45),TANANA(45),TANANB(45)
1ANB(45),AFJ1(50),UFT(45)
COMMON/B1678/NSHCP,XCP(45),AFT(45),PI
1,NHH(50),KJSN(45,6),HAU(50),CFTA(45),CFTB(45),NAB(50),NCODEA(45)
2,NCODEB(45),TZ
COMMON/B12678/JTAPE,IPRINT
COMMON/B126/AF2,TAN1A,TAN1B,PAN1A,PAN1B
1,AFA,AFB,PREDM,STAGT,IBL,STPREF,PNTRA,PNTRB,DPHSNT,DOMLOS
COMMON/B6/PREAN1,PREAN2,DENAN1,DENAN2,TAN1,TAN2,AAN1,AAN2,AFAN1,
1AFAN2,UAN1,UAN2,ZAJH(45),ZMH(45),ZZCP,K1,k11,J,KSH,UANB(45),
2FARL,FAR,ZSTOC,AFFT1,AFFT1,TFT1,TFT2,HRRATE,
3ZMJUJ(45),ZMJET(45),CD,GXI,DPH1, PREFT1,PREFT2,
4DENFT1,DENFT2,AFT1,AFT2,AFFT2,UFT1,UFT2,FARFT1,
5FARFT2,ENTHAL,LCMF,LCANI,LCAN,LCFTE,LCFT,K7,K13,K12,
6AFSYP,AFSYPB,AFSYIA,AFSYIB,LCPRT,LCPTA
7,C2(45), UANA(45), ZMHA(2),GX1A,GX1B
8,DPH(50),WCD(50),WFFIZ(45),DPAFS,DPBFS,DPAES,DPBES
9,RC(50)
1,A,B,D,E
2,K30,K40,K50,K60

CALCULATION OF FLAME TUBE HEAT ADDITION

CALCULATE MASS OF FUEL BURNT BETWEEN CALCULATION POINTS K AND K+1

FARZ=FARL

IF (FARFT2.LE.ZSTOC) GO TO 200	HTAD0600
FAL=FARFT2-ZSTOC	HTAD0610
FGL=FAL/(1.+FARFT2)	HTAD0620
FARZ=FARL-FGL*AFFT1/AFFT1	HTAD0630
IF (FARZ.LE.0.) FARZ=0.	HTAD0640
200 CONTINUE	HTAD0650
MRRATE=PLGV*FARZ*AFFT1+(3.0*1.0-26)*(TPT1**7.0*AFFT1/(1.+FARFT(K))	HTAD0660
1-TPT2**7.5*AFFT1/(1.+FARFT2))	HTAD0670
WFFIZ(K)=FARZ*AFFT1/(XCP(K+1)-XCP(K))	HTAD0680
RETURN	HTAD0690
END	HTAD0700

IBFTC JETM LIST

SUBROUTINE JETMIX

SUBROUTINE JETMIX

THIS SUBROUTINE CALCULATES RESIDUAL JET PARAMETERS
THE METHOD OF CALCULATION IS GOVERNED BY THE VALUE OF THE
VARIABLE - NEF

NEF=1 MASS LOSS
NEF=2 EQUIVALENT ENTRAINMENT
NEF=3 PROFILE SUBSTITUTION
NEF=4 INSTANTANEOUS MIXING

THIS SUBROUTINE USES COMMON BLOCKS WHOSE NAMES CONTAIN THE NUMBER 7
VIZ- B17, B67, B167, B178, B678, B1678, B12678

COMMON/BZERO/ A(430),EFCL(40),TJETA(40),UJCL(50),UJETA(40)
COMMON/B17/ XHU(50),DXHU(50),EFC(2), NEF,STEP,JKSN(50),NSH
COMMON/B67/DENFT(45),EK17,EK19,EK20, EK16
1 ,C(50),GXIA(50),K,WUJ(50)
COMMON/B167/GASC,GRAVC,GJoule,INHJ(50),XNI(50),NH
COMMON/B178/DFT(45)
COMMON/B678/PREFT(45),PREANA(45),PREANB(45),TFT(45),TANANA(45),TAN
1ANB(45),AFJ1(50),UFT(45)
COMMON/B1678/NSHCP,XCP(45),AFT(45),PI
1,NHH(50),KJSN(45,6),HAU(50),CFTA(45),CFTB(45),NAB(50),NCODEA(45)
2,ACODEB(45),TZ
COMMON/B12678/JTAPE ,IPRINT
COMMON/B5867/XFSA,XFSB

DIMENSION STATEMENTS

DIMENSION NDIS(50)

FORMAT STATEMENT

1 FCRMAT(1X/////18H *** ERROR MESSAGE) JETM0010
2 FCRMAT(7H JETMIX317, 9F10.3) JETM0020
10 FCRMAT(1X /120H J NDIS(J) EK17 EK19 EK16 JETM0030
1 EK20 AJET FLUXH FLUXM DENSJ S JETM0040
2 UJ/2(5X,15),10(E10.3)/ 40H DJ UJCL(J) EFCLZ ET JETM0050
3AH/4(E10.3)) JETM0060
11 FORMAT(5X,15,3(E10.3),5X,15,4(E10.3),5X,15) JETM0070
12 FCRMAT(5X,15,2(E10.3),5X,15,5(E10.3)) JETM0080
13 FCRMAT(1X/ 50H IX S X UJCL(J) EFCLZ/JETM0090
15X,15,4(E10.3)) JETM0100
14 FORMAT(1X/ 30H IX Y S/5X,15,2(E10.3)) JETM0110
21 FORMAT(1X / 90H J2 ETA AJET EFCL(J2) J3 JETM0120
1 TJET FLUXU FLUXH FLUXM,10H K2) JETM0130
22 FORMAT(1X/ 90H J2 AJET EFCL(J2) J3 TJETA(J2) JETM0140
1 FLUXU FLUXH FLUXM ETA) JETM0150
23 FCRMAT(26H SUBROUTINE JETMIX ENTERED) JETM0160
24 FCRMAT(25H SUBROUTINE JETMIX EXITED) JETM0170
91 FCRMAT(41H WHEN SUBROUTINE JETMIX WAS CALLED, K WAS 13,20H, LESS TH, JETM0180
1AN NSHCP+1.) JETM0190
92 FCRMAT(21H PECULIAR JET PROFILE/11H IN JET NO.13,10H,EFCL(40)=F6.3 JETM0200


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*.....*.....*.....*.....*.....*.....*.....*.....*.....*
C
113 ETAH=AMAX1(.215*S,DJ)
    IF (NEF.EQ.1) GO TO 143
    ETA=0.0
C
C --- WCRK ACROSS JET PROFILE, SUMMING HEAT OR MASS FLUX
C
    ETAINC=.1*ETAH
    IF(IPRINT.EQ.1)
1WRITE(6,22)
    DO114J2=1,40
    ETA=ETA+ETAINC
    IF(ETA.GT.ETAH)GOTC116
    UJETA(J2)=UFT(K)+(0.5*(COS(0.5*PI*ETA/ETAH))+C.5)*(UJCL(J)-UFT(K))
    GOTC117
116 UJETA(J2)=UFT(K)+1.74*EXP(-1.25*ETA/ETAH)*(UJCL(J)-UFT(K))
117 EFCL(J2)=(UJETA(J2)-UFT(K))/(UJ-UFT(K))
    J3=.5+FLOAT(J2)/1.4
    IF(NEF.EQ.2) GO TO 1119
    IF(4.8/6.5*EFCL(J3).GE.EFD) GO TO 1119
    IF(J2.GT.1) GO TO 143
    GC TO 1430
1119 TJETA(J2)=TFT(K)+(TAN-TFT(K))*EFCL(J3) *4.8/6.5
    FLUXM=FLUXM+CCNT /TJETA(J2)*UJETA(J2)*.12*1.8*ETA**.8*ETAINC
    IF(NEF.EQ.2) GO TO 114
    AJET=.12*ETA**1.8/COSETA
    FLUXU=FLUXU+CONT /TJETA(J2)*UJETA(J2)**2*.12*1.8*ETA**.8*ETAINC
1 *CCSETA
    ZZCP1=.2419-.8181E-5*TJETA(J2)/2.+17.91E-9*TJETA(J2)**2/3.
1 -2.742E-12*TJETA(J2)**3/4.-102.42/TJETA(J2)
    CCNST=CONS*ZZCP1
    FLUXH=FLUXH+(CONST+CONT/TJETA(J2)*0.5*UJETA(J2)**2)*UJETA(J2)*
1.12*1.8*ETA**.8*ETAINC
114 IF(IPRINT.EC.1)
1WRITE(6,12) J2, AJET,EFCL(J2),J3,TJETA(J2),FLUXU ,FLUXH,FLUXM,
1ETA
    GO TO 143
C
C --- WALL JETS
C
100 DJ=HAU(J)*C(J)
    COSETA = 1.0
    K2=K
    K22=K
    K=K1
    EFD=EFC(2)
    IF(NAB(J).EQ.2)GOTC132
    CFT=CFTA(K)
    GOTC133
132 CFT=CFTB(K)
133 UJ=AFJ1(J)/(DENSJ*DJ*CFT)
    WUJ(J)=UJ
    UJCL(J)=UJ
C
C --- FIND DISTANCE PARAMETER ALONG WALL
C
    DO122IX=1,100
    AI=IX
    XL=XCP(K2+1)-XCP(K22)
    X=AI*STEP

```

JETM1800
 JETM1810
 JETM1820
 JETM1830
 JETM1840
 JETM1850
 JETM1860
 JETM1870
 JETM1880
 JETM1890
 JETM1900
 JETM1910
 JETM1920
 JETM1930
 JETM1940
 JETM1950
 JETM1960
 JETM1970
 JETM1980
 JETM1990
 JETM2000
 JETM2010
 JETM2020
 JETM2030
 JETM2040
 JETM2050
 JETM2060
 JETM2070
 JETM2080
 JETM2090
 JETM2100
 JETM2110
 JETM2120
 JETM2130
 JETM2140
 JETM2150
 JETM2160
 JETM2170
 JETM2180
 JETM2190
 JETM2200
 JETM2210
 JETM2220
 JETM2230
 JETM2240
 JETM2250
 JETM2260
 JETM2270
 JETM2280
 JETM2290
 JETM2300
 JETM2310
 JETM2320
 JETM2330
 JETM2340
 JETM2350
 JETM2360
 JETM2370
 JETM2380
 JETM2390

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.....*.....*.....*.....*.....*.....*.....*.....*.....*
IF(X.LT.(XHDUM -XH(J)))GOTO135
X=XHDUM -XH(J)
INE=1
135 IF(X.GE.XL) K2=K2+1
S=S+ABS(1.-UFT(K2)/UJCL(J))*(X-XLAST)
IF(S.LE.0.)UJCL(J)=UJ
IF(ABS(1.-UFT(K2)/UJ ) .LT. .012) GO TO 3135
IF(S.GT.0.)
1UJCL(J)=UFT(K2)+0.0287*DJ*(UJ-UFT(K2))*DENSJ/(VISJ*(S*12.)
2*((1.06/ABS(1.-UFT(K2)/UJ))-5))
IF((UJCL(J).GE.UJ).AND.(UJCL(J).LE.UFT(K2))) .OR.
1 ((UJCL(J).LE.UJ).AND.(UJCL(J).GE.UFT(K2)))) GO TO 148
UJCL(J)=UJ
GC TC 148
3135 UJCL(J)=UFT(K2)
148 IF(INE.EQ.1)GCTC118
134 XLAST=X
122 IF(IPRINT.EQ.1)
1WRITE(6,13) IX,S,X,UJCL(J),EFCLZ
--- WORK ACROSS JET PROFILE, SUMMING HEAT OR MASS FLUX
118 IF(NEF.EQ.1)GOTO143
EFCLZ=(UJCL(J)-UFT(K))/(UJ-UFT(K))
IF(NEF.EQ.3.AND.4.8/6.5*EFCLZ.LE.EFD) GO TO 143C
ETAH=AMAX1(.065*S,CJ)
DELTA1=0.0109*S
ETA=-0.6
TJCL=TFT(K)+(TAN-TFT(K))*EFCLZ *4.8/6.5
ZZCP1=.2419-.8181E-5*TJCL /2.+17.91E-9*TJCL **2/3.
1 -2.742E-12*TJCL **3/4.-102.42/TJCL
CONST=CONS*ZZCP1
FLUXH=(CONST+CONT/TJCL*0.5*UJCL(J)**2+0.95 )*UJCL(J)
1*CFT*DELTA1*0.95
FLUXM=CONT /TJCL*UJCL(J)*CFT*DELTA1
FLUXU=CONT /TJCL*UJCL(J)**2*CFT*DELTA1*0.95
AJET=DELTA1*CFT
IF(IPRINT.EC.1)
1WRITE(6,21)
DO112J2=1,40
ETA=ETA+.12
UJETA(J2)=UFT(K)+(UJCL(J)-UFT(K))*EXP(-0.693*ETA*ETA)
EFCL(J2)=(UJETA(J2)-UFT(K))/(UJ-UFT(K))
J3=.5+FLOAT(J2)/1.4
TJET =TFT(K)+(TAN-TFT(K))*EFCL(J3)*4.8/6.5
ZZCP1=.2419-.8181E-5*TJET /2.+17.91E-9*TJET **2/3.
1 -2.742E-12*TJET **3/4.-102.42/TJET
CCNST=CONS*ZZCP1
FLUXH=FLUXH+(CONST+CONT/TJET*0.5*UJETA(J2)**2)*.1*ETAH*CFT*UJETA(J2)
1 2)
FLUXM=FLUXM+CONT/TJET*.1*ETAH*CFT*UJETA(J2)
FLUXU=CONT/TJET*.1*ETAH*CFT*UJETA(J2)**2 + FLUXU
AJET=AJET+.1*ETAH*CFT
GO TO (143,112,140),NEF
140 IF(4.8/6.5*EFCL(J3).LE.EFD) GO TO 143
112 IF(IPRINT.EQ.1)
1WRITE(6,11) J2,ETA, AJET,EFCL(J2),J3,TJET,FLUXU ,FLUXH,FLUXM
1,K2
--- AREA OF IDEALIZED JET

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JETM2400
 JETM2410
 JETM2420
 JETM2430
 JETM2440
 JETM2450
 JETM2460
 JETM2470
 JETM2480
 JETM2490
 JETM2500
 JETM2510
 JETM2520
 JETM2530
 JETM254C
 JETM2550
 JETM2560
 JETM2570
 JETM2580
 JETM2590
 JETM2600
 JETM2610
 JETM262C
 JETM2630
 JETM264C
 JETM2650
 JETM2660
 JETM2670
 JETM2680
 JETM2690
 JETM270C
 JETM2710
 JETM2720
 JETM2730
 JETM274C
 JETM2750
 JETM2760
 JETM2770
 JETM2780
 JETM2790
 JETM2800
 JETM2810
 JETM282C
 JETM2830
 JETM2840
 JETM2850
 JETM2860
 JETM2870
 JETM2880
 JETM2890
 JETM2900
 JETM291C
 JETM2920
 JETM2930
 JETM2940
 JETM2950
 JETM2960
 JETM2970
 JETM2980
 JETM2990

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*.....*.....*.....*.....*.....*.....*.....*.....*.....*
C
143 IF(IPRINT.GE.0)WRITE(6,2)K1,J,NDIS(J),UJ,UFT(K),UJCL(J),EFCL(J),
  1FLUXM,AFJ1(J)
  IF(NEF.EQ.1.AND.DXHU(J).EQ.0.0) GO TO 2111
  GC TO (111,125,2130),NEF
111 FLUXM=AFJ1(J)*(1.-EFD*S/(2.*DXHU(J)))
  GC TO 126
2111 FLUXM = AFJ1(J)*(1.-EFD*S/HAU(J))
  GC TO 126
125 FLUXM=AMIN1*(AFJ1(J)*(1.+EFD)-EFD*FLUXM),FLUXM)
126 IF(FLUXM.GT.0.) GO TO 2126
  AJET=0.
  FLUXU=0.
  FLUXH=0.
1131 FLUXM=0.
1430 NDIS(J) = 1
  GO TO 1030
2126 AJET=FLUXM/UJ/DENSJ /COSETA
  FLUXU=FLUXM*UJ *COSETA
  ZXCPT=.2419*TAN-.8181E-5*TAN**2/2.+17.91E-9*TAN**3/3.-2.742E-12*
  1 TAN**4/4.-102.42
  FLUXH=FLUXM*( ZXCPT *GRAVC*GJDULE+0.5*UJ**2)
2130 IF(DXHU(J).EQ.0.0) GO TO 2131
  130 BB=4.*ETAH*OFT(K1)/2.
  IF(AJET.GT.BB) AJET=BB
  CC=FLOAT(NHH(J))
  GC TO 2199
2131 CC=1.
2199 IF(AJET.LE.0.25*AFT(K1)/CC) GO TO 131
  199 IF(IPRINT.LT.0.AND.LCMFL.NE.1)GOTO1030
  WRITE(JTAPE,1)
  WRITE(JTAPE,99) J
  GC TO 1030
  198 IF(IPRINT.LT.0.AND.LCMFL.NE.1)GOTO1030
  WRITE(JTAPE,1)
  WRITE(JTAPE,98) DENSJ,DENFT(K),UJ,UFT(K),X,DJA
  GOTO1030
  131 EK16=EK16+FLUXU*CC
  EK17=EK17+AJET*CC
  EK19=EK19+FLUXM*CC
  EK20=EK20+FLUXH*CC
C
C IF THIS IS A SECONDARY HOLE, RESET AFJ1(J)
C
1030 IF(JKSN(J).EQ.NSHCP) AFJ1(J)=AFJ1(J)/SPL
1031 IF(IPRINT.GE.0)
  1WRITE(6,10) J,NDIS(J),EK17,EK19,EK16,EK20,AJET,FLUXH,FLUXM,DENSJ,
  IS,UJ,DJ,UJCL(J),EFCLZ,ETAH
  K=K1
  GC TO 900
191 WRITE(JTAPE,1)
  WRITE(JTAPE,91)K
900 DC 901 J=1,NH
901 AFJ1(J)=AFJ1(J)*FLOAT(NHH(J))
  IF(IPRINT.EQ.1) WRITE(6,24)
  IPRINT=IPRINT+1
  RETURN
  END

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JETM3000
 JETM3010
 JETM3020
 JETM3030
 JETM3040
 JETM3050
 JETM3060
 JETM3070
 JETM3080
 JETM3090
 JETM3100
 JETM3110
 JETM3120
 JETM3130
 JETM3140
 JETM3150
 JETM3160
 JETM3170
 JETM3180
 JETM3190
 JETM3200
 JETM3210
 JETM3220
 JETM3230
 JETM3240
 JETM3250
 JETM3260
 JETM3270
 JETM3280
 JETM3290
 JETM3300
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 JETM3480
 JETM3490
 JETM3500
 JETM3510
 JETM3520
 JETM3530
 JETM3540
 JETM3550
 JETM3560
 JETM3570

\$IBFTC HT1 LIST

		HT1 0010
	SUBROUTINE HEAT1	HT1 0020
C		HT1 0030
C	SUBROUTINE HEAT1	HT1 0040
C		HT1 0050
C	THIS SUBROUTINE CARRIES OUT A NONITERATIVE HEAT TRANSFER	HT1 0060
C	CALCULATION.	HT1 0070
C		HT1 0080
C	THIS SUBROUTINE CALLS FOR FOUR SUBROUTINES	HT1 0090
C	1. EEFT	HT1 0100
C	2. PROP	HT1 0110
C	3. COOL	HT1 0120
C	4. TWSOLN	HT1 0130
C		HT1 0140
C	THIS SUBROUTINE IS USED BY THE MAIN PROGRAM CLARE	HT1 0150
C		HT1 0160
C	THE ROUTE THROUGH THIS PART OF THE PROGRAM IS CONTROLLED BY	HT1 0170
C	THE INDEX NHT1	HT1 0180
C		HT1 0190
C	NHT1 = 1 FOR 1-DIMENSIONAL RADIATION, UNCOOLED WALL	HT1 0200
C	NHT1 = 2 FOR 1-DIMENSIONAL RADIATION, COOLED WALL	HT1 0210
C	NHT1 = 3 FOR 2-DIMENSIONAL RADIATION, UNCOOLED WALL	HT1 0220
C	NHT1 = 4 FOR 2-DIMENSIONAL RADIATION, COOLED WALL	HT1 0230
C		HT1 0240
C	THIS SUBROUTINE USES COMMON BLOCKS WHOSE NAMES CONTAIN THE NUMBER 8	HT1 0250
C	VIZ- B8, B18, B68, B168, B178, B678, B1678, B12678	HT1 0260
C		HT1 0270
C	COMMON STATEMENTS	HT1 0280
C		HT1 0290
C	COMMON/B8/D1A(45),D2A(45),D3A(45),D4A(45),D1B(45),D2B(45),D3B(45)	HT1 0300
C	1,D4B(45),FMOCO2(45),FMOH2O(45),C1A(45),C1B(45),R1A(45),R1B(45),R2	HT1 0310
C	2A(45),R2B(45),R3A(45),R3B(45),TNUAAN(45),TNUBAN(45),TNUFT(45),	HT1 0320
C	3TWADA(45),TWADB(45),	HT1 0330
C	4EMFT(45),FILMFA(45),FILMFB(45),PRAAN(45),PRBAN(45),PRFT(45),REFT(4	HT1 0340
C	55),FINT(45),TCFA(45),TCFB(45),UFTA(45),UFTB(45),UJ1A(45),UJ1B(45),	HT1 0350
C	6AFJA(45),AFJB(45),YCFA(45),YCFB(45)	HT1 0360
C	COMMON/B18/ABSW,EMW,EMC,NLUM, NHT1,NHT2	HT1 0370
C	1, X1FCA(45),X1FCB(45),CONDFT,TCASA(45),TCASB(45),TOLTW1,TOLTH1	HT1 0380
C	2W2,XFILMZ, TABTFT(10),TABEFT(100),TABPFT(10),NEFT,NPFT,NFORMHT1	HT1 0390
C	3,NCOODL, NUMAX1,NUMAX2	HT1 0400
C	COMMON/B68/AFANA(45),AFANB(45),AFFT(45),AFPRZ,C2A(45),C2B(45)	HT1 0410
C	1, AFSYP,FARFT(45),DENANA(45),DENANB(45)	HT1 0420
C	3,SAFTRA(45),SAFTRB(45),QTRA(45),QTRB(45),REAN(45),REBAN(45)	HT1 0430
C	4,TWA(45),TWB(45)	HT1 0440
C	COMMON/B168/AANA(45),AANB(45),CCA(45),CCB(45),FHCR,NLAST	HT1 0450
C	1,KANHET,LANHET,PERCO,THIKFT	HT1 0460
C	2,DANA(45),DANB(45)	HT1 0470
C	COMMON/B178/DFT(45)	HT1 0480
C	COMMON/B678/PREFT(45),PREANA(45),PREANB(45),TFT(45),TANANA(45),TANHT1	HT1 0490
C	1ANB(45),AFJ1(50),UFT(45)	HT1 0500
C	COMMON/B1678/NSHCP,XCP(45),AFT(45),PI	HT1 0510
C	1,NHH(50),KJSN(45,6),HAU(50),CFTA(45),CFTB(45),NAB(50),NCODEA(45)	HT1 0520
C	2,NCODEB(45),TZ	HT1 0530
C	COMMON/B12678/JTAPE ,IPRINT	HT1 0540
C		HT1 0550
C	DATA STATEMENT	HT1 0560
C		HT1 0570
C	DATA YA,YB/2=0./	HT1 0580
C		HT1 0590

C	FORMAT STATEMENTS	HT1 0600
C		HT1 0610
	1 FORMAT(6HOHEAT11OF11.3/(6X10F11.3))	HT1 0620
	2 FORMAT(1H010I5)	HT1 0630
	3 FORMAT(6HOHEAT11OF11.6/(6X10F11.6))	HT1 0640
C		HT1 0650
C	QUANTITIES REQUIRED FOR FILM-COOLING CALCULATION	HT1 0660
C		HT1 0670
	DO201K=1,NLAST	HT1 0680
	TWADA(K)=0.	HT1 0690
	TWADB(K)=0.	HT1 0700
	R3A(K)=0.	HT1 0710
	R3B(K)=0.	HT1 0720
	FILMFA(K)=0.	HT1 0730
	FILMFB(K)=0.	HT1 0740
	IF(K.NE.1)GO TO 2004	HT1 0750
	X1FCA(K) = 100.	HT1 0760
	X1FCB(K) = 100.	HT1 0770
	GO TO 2005	HT1 0780
2004	XCPDIF = XCP(K) - XCP(K-1)	HT1 0790
	IF(NCDEA(K-1).EQ.1) X1FCA(K) = XCPDIF	HT1 0800
	IF(NCDEA(K-1).NE.1) X1FCA(K) = XCPDIF + X1FCA(K-1)	HT1 0810
	IF(NCDEB(K-1).EQ.1) X1FCB(K) = XCPDIF	HT1 0820
	IF(NCDEB(K-1).NE.1) X1FCB(K) = XCPDIF + X1FCB(K-1)	HT1 0830
2005	AFJA(K)=FJA	HT1 0840
	AFJB(K)=FJB	HT1 0850
	TCFA(K)=TA	HT1 0860
	TCFB(K)=TB	HT1 0870
	UFTA(K)=UA	HT1 0880
	UFTB(K)=UB	HT1 0890
	UJ1A(K)=UJA	HT1 0900
	UJ1B(K)=UJB	HT1 0910
	YCFA(K)=YA	HT1 0920
	YCFB(K)=YB	HT1 0930
	IF(NCDEA(K).NE.1) GO TO 202	HT1 0940
	DO2001 L = 1,6	HT1 0950
	J = KJSN(K,L)	HT1 0960
	IF(NAB(J).NE.1) GO TO 2001	HT1 0970
	YA=HAU(J)	HT1 0980
	FJA=AFJ1(J)	HT1 0990
	UA=UFT(K)	HT1 1000
	UJA=FJA/(YA*CFTA(K)*DENANA(K))	HT1 1010
	UAN=AFANA(K)/DENANA(K)/AANA(K)	HT1 1020
	TA=TANANA(K) +UAN**2/(2.*32.2*53.35)	HT1 1030
	GO TO 202	HT1 1040
2001	CONTINUE	HT1 1050
202	IF(NCDEB(K).NE.1)GOTO201	HT1 1060
	DO2002 L = 1,6	HT1 1070
	J = KJSN(K,L)	HT1 1080
	IF(NAB(J).NE.2) GO TO 2002	HT1 1090
	YB=HAU(J)	HT1 1100
	FJB=AFJ1(J)	HT1 1110
	UB=UFT(K)	HT1 1120
	UJB=FJB/(YB*CFTB(K)*DENANB(K))	HT1 1130
	UAN=AFANB(K)/DENANB(K)/AANB(K)	HT1 1140
	TB=TANANB(K) +UAN**2/(2.*32.2*53.35)	HT1 1150
	GO TO 201	HT1 1160
2002	CONTINUE	HT1 1170
201	CONTINUE	HT1 1180
	IF(IPRINT.NE.1)GOTO8765	HT1 1190
	WRITE(6,1)(TFT(K),TANANA(K),TANANB(K),TCFA(K),TCFB(K),UFTA(K),	HT1 1200

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1UFTB(K),UJ1A(K),UJ1B(K),DFT(K),K=1,NLAST) HT1 1210
WRITE(6,3)(AFT(K),DANA(K),AANA(K),AANB(K),DANB(K),CCA(K),CCB(K), HT1 1220
1X1FCA(K),X1FCB(K),YCFA(K),K=1,NLAST) HT1 1230
WRITE(6,1)(YCFB(K),AFJA(K),AFJB(K),PREFT(K),PREANA(K),PREANB(K), HT1 1240
1FARFT(K),TCASA(K),TCASB(K),XCP(K),K=1,NLAST) HT1 1250
WRITE(6,1)AFPRZ,AFSYP,ABSW,EMC,PI,CONDFT,THIKFT,XFILMZ,PERCO, HT1 1260
1FHCR,(AFANA(K),K=1,NLAST),(AFANB(K),K=1,NLAST),(AFFT(K),K=1,NLAST) HT1 1270
8765 CONTINUE HT1 1280
C HT1 1290
KANHET=KANHET+1 HT1 1300
K=1 HT1 1310
5 CALL EEFT(K) HT1 1320
FINT(K)=4.8E-13*EMFT(K)*TFT(K)**4 HT1 1330
C HT1 1340
C*****CALCULATE THE INTERNAL DIRECT RADIATION COEFFICIENT, A HT1 1350
C HT1 1360
A=2.4E-13*(1.+ABSW)*EMFT(K)*TFT(K)**1.5 HT1 1370
C HT1 1380
C*****CALCULATE THE EXTERNAL RADIATION COEFFICIENT, B HT1 1390
C HT1 1400
B=4.8E-13*(EMW*EMC)/(EMC+EMW*(1.-EMC)) HT1 1410
CALL PROP(K,CNDAV,FHCO2,FMH2O) HT1 1420
C HT1 1430
C*****CALCULATE THE INTERNAL CONVECTION COEFFICIENT, CFT HT1 1440
C HT1 1450
CFT=TNUFT(K)*CNDAV/DFT(K) /3600. HT1 1460
C HT1 1470
C*****CALCULATE GAS PROPERTIES IN THE ANNULUS HT1 1480
C*****SET CALCULATION TO INNER ANNULUS HT1 1490
C HT1 1500
INXAN=1 HT1 1510
AAN =AANA(K) HT1 1520
AFAN=AFANA(K) HT1 1530
DAN=DANA(K) HT1 1540
TAN=TANANA(K) HT1 1550
TCAS=TCASA(K) HT1 1560
10 CNDAN=-0.2853E-3+3.268E-5*TAN-0.825E-8*TAN**2+1.239E-12*TAN**3 HT1 1570
VISAN=3.057E-3+8.607E-5*TAN-2.279E-8*TAN**2+2.908E-12*TAN**3 HT1 1580
CPAN =0.2419-0.8181E-5*TAN+1.791E-8*TAN**2-0.2743E-11*TAN**3 HT1 1590
REAN=3600.*DAN*AFAN/VISAN/AAN HT1 1600
IF(REAN.LT.1.)REAN=1. HT1 1610
PRAN=CPAN*VISAN/CNDAN HT1 1620
IF(PRAN.LT..01)PRAN=.01 HT1 1630
TNUAN=.023*REAN**0.8*PRAN**0.4 HT1 1640
C HT1 1650
C*****CALCULATE CONVECTION COEFFICIENT IN ANNULUS HT1 1660
C HT1 1670
CAN = TNUAN*CNDAN/DAN/3600. HT1 1680
GO TO (50,40,20,20),NHT1 HT1 1690
C HT1 1700
C*****INCLUDE TOTAL RADIATION FROM FLAME HT1 1710
C HT1 1720
20 GO TO(30,30,31,32,33),NLUM HT1 1730
NLUM=1,2 NON LUMINOUS HT1 1740
30 DUMLUM=1. HT1 1750
GO TO 35 HT1 1760
C HT1 1770
C NLUM=3 LEVEBVE CORRELATION FOR LUMINOSITY HT1 1780
C HT1 1790
31 DUMLUM =7.53*(1./FHCR-5.5)**0.85 HT1 1800
GO TO 35 HT1 1810

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C NLUM=4 NREC 1964 HT1 1820
32 DUMLUM=EXP((1.-4.4*FHCR)/(2.3*FHCR)) HT1 1830
   GO TO 35 HT1 1840
C NLUM=5 NREC 1966 HT1 1850
33 DUMLUM=((1.-FHCR*5.)/(FHCR*0.16))**0.74 HT1 1860
35 S1=0. HT1 1870
   S2=0. HT1 1880
   DO 1400 KK=1,NLAST HT1 1890
C HT1 1900
   DUMR3=(XCP(K)-XCP(KK)) HT1 1910
   IF(INXAN.EQ.1) GO TO 1000 HT1 1920
   DUMR1=((CCA(K)-CCA(KK))/PI+DANA(K)-DANA(KK)+DFT(K))/2. HT1 1930
   DUMR2=DUMR1-DFT(KK)/2. HT1 1940
   GO TO 1020 HT1 1950
1000 DUMR1=((CCA(KK)-CCA(K))/PI+DANA(KK)-DANA(K)+DFT(KK))/2. HT1 1960
   DUMR2=DUMR1-DFT(KK)/2. HT1 1970
1020 TRANSM=0. HT1 1980
   DO37I=1,20 HT1 1990
37 TRANSM=TRANSM+14.82/20./((14.82+(FMCO2+FMH20)*PREFT(KK)*SQRT
1 (DUMR3**2+(DUMR1-(FLOAT(I)/20.-.025)*(DUMR1-DUMR2))**2)) HT1 2000
   HT1 2010
C HT1 2020
C VIEW FACTOR PER UNIT LENGTH OF RECEIVING SECTION HT1 2030
C HT1 2040
C IF(DUMR2.LE.0.0001)GO TO 1040 HT1 2050
   VU=0.25/DUMR1*(1.-DUMR3/SQRT(DUMR3**2+DUMR1**2)) HT1 2060
1 +0.25/DUMR2*(1.-DUMR3/SQRT(DUMR3**2+DUMR2**2)) HT1 2070
   GO TO 1060 HT1 2080
1040 VU=0.25/DUMR1*(1.-DUMR3/SQRT(DUMR3**2+DUMR1**2)) HT1 2090
C HT1 2100
C EVALULATE WIDTH OF RADIATING SECTION HT1 2110
C HT1 2120
C 1060 IF(KK.EQ.1) GO TO 1080 HT1 2130
   IF(KK.EQ.NLAST) GO TO 1100 HT1 2140
   WIDTH=(XCP(KK+1)-XCP(KK-1))/2. HT1 2150
   GO TO 1200 HT1 2160
1080 WIDTH=(XCP(KK+1)-XCP(KK)) HT1 2170
   GO TO 1200 HT1 2180
1100 WIDTH=(XCP(KK)-XCP(KK-1)) HT1 2190
C HT1 2200
C EVALULATE FLAME CROSS-SECTIONAL AREA HT1 2210
C HT1 2220
1200 FLAR=PI*((CCA(KK)/2./PI+DANA(KK)/2.+ HT1 2230
1 DFT(KK)/2.))**2-(CCA(KK)/2./PI+DANA(KK)/2.))**2) HT1 2240
   S1=S1+4.*4.8E-13*PREFT(KK)*(FMCO2+FMH20) HT1 2250
1 *3.6/TFT(KK)*WIDTH*FLAR*VU*TRANSM*DUMLUM HT1 2260
2 *(1.0+ABSW)/2.0*TFT(KK)**4 HT1 2270
   S2=S2+4.*4.8E-13*PREFT(KK)*(FMCO2+FMH20) HT1 2280
1 *3.6/TFT(KK)*WIDTH*FLAR*VU*TRANSM*(1.+ABSW)/2.*DUMLUM HT1 2290
1400 IF(IPRINT.EQ.1) WRITE(6,1) TRANSM,VU,FLAR,S1,S2,DUMR1,DUMR2,DUMR3 HT1 2300
C HT1 2310
C FORM EQUIVALENT FLAME TEMPERATURE HT1 2320
C HT1 2330
   TSTAR1=S1/S2 HT1 2340
1700 IF(INXAN.EQ.1)GO TO 1800 HT1 2350
C HT1 2360
C FORM TOTAL RADIATION COMPONENT, AA HT1 2370
C HT1 2380
   AA=S2/((CCB(K)-DANB(K)*PI)) HT1 2390
   GO TO 1900 HT1 2400
1800 AA=S2/((CCA(K)+DANA(K)*PI)) HT1 2410
1900 IF(NHT1.EQ.3)GO TO 50 HT1 2420

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40	CALL CCOL(K,INXAN,CNDAV,TRNSCO,CFTTRN)	HT1 2430
C		HT1 2440
C	***** FCRM COEFFICIENTS IN HEAT BALANCE EQUATION *****	HT1 2450
C		HT1 2460
	IF(INXAN.EQ.2)GO TO 45	HT1 2470
	TWAD=TWADA(K)	HT1 2480
	GO TO 50	HT1 2490
45	TWAD=TWADB(K)	HT1 2500
50	D1=B	HT1 2510
	D2=A	HT1 2520
	D3=CFT+CAN	HT1 2530
	D4=B*TCAS**4+A*TFT(K)**2.5+CFT*TFT(K)+CAN*TAN	HT1 2540
	GO TO (110,60,80,90),NHT1	HT1 2550
60	IF(NCOCL.EQ.2)GO TO 70	HT1 2560
	D4=D4+CFT*(TWAD-TFT(K))	HT1 2570
	GO TO 110	HT1 2580
70	D3=D3+CFTTRN+TRNSCO-CFT	HT1 2590
	D4=D4+(CFTTRN-CFT)*TFT(K)+TRNSCO*TAN	HT1 2600
	GO TO 110	HT1 2610
80	D1=D1+AA	HT1 2620
	D2=0.	HT1 2630
	D4=D4+AA*TSTAR1 -A*TFT(K)**2.5	HT1 2640
	GO TO 110	HT1 2650
90	IF(NCOCL.EQ.2)GO TO 100	HT1 2660
	D1=D1+AA	HT1 2670
	D2= 0.	HT1 2680
	D4=D4+AA*TSTAR1+CFT*(TWAD-TFT(K)) -A*TFT(K)**2.5	HT1 2690
	GO TO 110	HT1 2700
100	D1=D1+AA	HT1 2710
	D2=0.	HT1 2720
	D3=D3+CFTTRN+TRNSCO-CFT	HT1 2730
	D4=D4+(CFTTRN-CFT)*TFT(K)+TRNSCO*TAN+AA*TSTAR1 -A*TFT(K)**2.5	HT1 2740
110	IF(IPRINT.EQ.1)WRITE(6,2)NCOOL,K,NHT1,INXAN	HT1 2750
	IF(D4.LE.0.)GOTO290	HT1 2760
	CALL TWSOLN(K,D1,D2,D3,D4,DTW1)	HT1 2770
	IF(INXAN.EQ.2)GO TO 200	HT1 2780
C		HT1 2790
C		HT1 2800
C	STORE REQUIRED VARIABLES	HT1 2810
		HT1 2820
	TWA(K)=DTW1	HT1 2830
	C2A(K)=CAN*(TWA(K)-TAN)	HT1 2840
	IF(KANHET.EQ.1.AND.LANHET.EQ.1)GO TO 190	HT1 2850
	GO TO (120,120,130,130),NHT1	HT1 2860
120	RIA(K)=A*(TFT(K)**2.5-TWA(K)**2.5)	HT1 2870
	GO TO 140	HT1 2880
130	RIA(K)=AA*(TSTAR1-TWA(K)**4)	HT1 2890
140	GO TO (170,150,170,150),NHT1	HT1 2900
150	IF(NCOCL.EQ.2)GO TO 160	HT1 2910
	C1A(K)=CFT*(TWADA(K)-TWA(K))	HT1 2920
	GO TO 180	HT1 2930
160	C1A(K)=CFTTRN*(TFT(K)-TWA(K))	HT1 2940
	OTRA(K)=TRNSCO*(TWA(K)-TAN)	HT1 2950
	GO TO 180	HT1 2960
170	C1A(K)=CFT*(TFT(K)-TWA(K))	HT1 2970
180	REAN(K)=REAN	HT1 2980
	PRAAN(K)=PRAN	HT1 2990
	TNUAN(K)=TNUAN	HT1 3000
	R2A(K)=B*(TWA(K)**4-TCAS**4)	HT1 3010
	TANANA(K)=TAN	HT1 3020
	D1A(K)=D1	HT1 3030
	D2A(K)=D2	

	D3A(K)=D3	HT1 3040
	D4A(K)=D4	HT1 3050
C		HT1 3060
C	SET CALCULATION TO OUTER ANNULUS	HT1 3070
C		HT1 3080
190	INXAN=2	HT1 3090
	AAN = AANB(K)	HT1 3100
	AFAN=AFANB(K)	HT1 3110
	DAN=DANB(K)	HT1 3120
	TAN=TANANB(K)	HT1 3130
	TCAS=TCASB(K)	HT1 3140
	GO TO 10	HT1 3150
C		HT1 3160
C	STORE REQUIRED VARIABLES	HT1 3170
C		HT1 3180
200	TWB(K)=DTW1	HT1 3190
	C2B(K)=CAN*(TWB(K)-TAN)	HT1 3200
	IF(KANHET.EQ.1.AND.LANHET.EQ.1)GO TO 280	HT1 3210
	GO TO(210,210,220,220),NHT1	HT1 3220
210	R1B(K)=A*(TFT(K)**2.5-TWB(K)**2.5)	HT1 3230
	GO TO 230	HT1 3240
220	R1B(K)=AA*(TSTAR1-TWB(K)**4)	HT1 3250
230	GO TO(260,240,260,240),NHT1	HT1 3260
240	IF(NCOOL.EQ.2)GO TO 250	HT1 3270
	C1B(K)=CFT*(TWADB(K)-TWB(K))	HT1 3280
	GO TO 270	HT1 3290
250	C1B(K)=CFTTRN*(TFT(K)-TWB(K))	HT1 3300
	QTRB(K)=TRNSCO*(TWB(K)-TAN)	HT1 3310
	GO TO 270	HT1 3320
260	C1B(K)=CFT*(TFT(K)-TWB(K))	HT1 3330
270	REBAN(K)=REAN	HT1 3340
	PRBAN(K)=PRAN	HT1 3350
	TNUBAN(K)=TNUAN	HT1 3360
	R2B(K)=B*(TWB(K)**4-TCAS**4)	HT1 3370
	TANANB(K)=TAN	HT1 3380
	D1B(K)=D1	HT1 3390
	D2B(K)=D2	HT1 3400
	D3B(K)=D3	HT1 3410
	D4B(K)=D4	HT1 3420
	FMCO2(K)=FMCO2	HT1 3430
	FMOH2O(K)=FMOH2O	HT1 3440
280	IF(K.EQ.NLAST)GO TO 290	HT1 3450
	K=K+1	HT1 3460
	GO TO 5	HT1 3470
290	RETURN	HT1 3480
	END	HT1 3490

\$IBFTC HT2 LIST

SUBROUTINE HEAT2

S U B R O U T I N E H E A T 2

THIS SUBROUTINE CARRIES OUT AN ITERATIVE HEAT-TRANSFER CALC.

THIS SUBROUTINE CALLS FOR ONE SUBROUTINE
1. TWSOLN

THIS SUBROUTINE IS USED BY THE MAIN PROGRAM CLARE

THE ROUTE THROUGH THIS PART OF THE PROGRAM IS CONTROLLED BY
THE INDEX NHT2

NHT2 = 2 FOR LONGITUDINAL WALL CONDUCTION
NHT2 = 3 FOR RADIATION INTERCHANGE BETWEEN WALLS
NHT2 = 4 FOR LONGITUDINAL CONDUCTION AND RADIATION
INTERCHANGE
NHT2 = 1 IF NONE OF THESE OPTIONS ARE REQUIRED

THIS SUBROUTINE USES COMMON BLOCKS WHOSE NAMES CONTAIN THE NUMBER 8
VIZ- B8, B18, B68, B168, B178, B678, B1678, B12678

COMMON/BZERO/TWAX(45),TWBX(45),REST(51C)

COMMON/B8/D1A(45),D2A(45),D3A(45),D4A(45),D1B(45),D2B(45),D3B(45)

1,D4B(45),FMOC02(45),FMOH20(45),C1A(45),C1B(45),R1A(45),R1B(45),R2

2A(45),R2B(45),R3A(45),R3B(45),TNUAAN(45),TNUBAN(45),TNUFT(45),

3TWADA(45),TWADB(45),

4EMFT(45),FILMFA(45),FILMFB(45),PRAAN(45),PRBAN(45),PRFT(45),REFT(4

55),FINT(45),TCFA(45),TCFB(45),UFTA(45),UFTB(45),UJ1A(45),UJ1B(45),

6AFJA(45),AFJB(45),YCFA(45),YCFB(45)

COMMON/B18/ABSW,EMW,EMC,NLUM,

1, X1FCA(45),X1FCB(45),CONDFT,TCASA(45),TCASB(45),TOLTW1,TOLTHT

2W2,XFILMZ, TABTFT(10),TABEFT(100),TABPFT(10),NEFT,NPFT,NFORMHT

3,NC00L, NUMAX1,NUMAX2

COMMON/B68/AFANA(45),AFANB(45),AFFT(45),AFPRZ,C2A(45),C2B(45)

1, AFSYP,FARFT(45),DENANA(45),DENANB(45)

3,SAFTRA(45),SAFTRB(45),QTRA(45),QTRB(45),REAN(45),REBAN(45)

4,TWA(45),TH9(45)

COMMON/B168/AANA(45),AANB(45),CCA(45),CCB(45),FHCR,NLAST

1,KANHET,LANHET,PERCO,THIKFT

2,DANA(45),DANB(45)

COMMON/B178/DFT(45)

COMMON/B678/PREFT(45),PREANA(45),PREANB(45),TFT(45),TANANA(45),TANHT

1ANB(45),AFJ1(50),UFT(45)

COMMON/B1678/NSHCP,XCP(45),AFT(45),PI

1,NHH(50),KJSN(45,6),HAU(50),CFTA(45),CFTB(45),NAB(50),NCODEA(45)

2,NCODEB(45),TZ

COMMON/B12678/JTAPE,IPRI/IT

DIMENSION NAME(2)

DATA(NAME(I),I=1,2)/12H INNER OUTER/

1 FORMAT(6H AFTER14,30H TRIALS, ERROR IS GREATER THAN,F9.2,6H DEG R)HT2 0560

2 FORMAT(2I5,5X,4E12.4) HT2 0570

39 FORMAT(/////51HODIMENSIONLESS GROUPS ASSOCIATED WITH HEAT TRANSFERHT2 0580

1/1X50(1H-)/6H0AXIAL16X35HREYNOLDS NUMBER15X14HPRANDTL NUMBER12X14HHT2 0590

HT2 0010
HT2 0020
HT2 0030
HT2 0040
HT2 0050
HT2 0060
HT2 0070
HT2 0080
HT2 0090
HT2 0100
HT2 0110
HT2 0120
HT2 0130
HT2 0140
HT2 0150
HT2 0160
HT2 0170
HT2 0180
HT2 0190
HT2 0200
HT2 0210
HT2 0220
HT2 0230
HT2 0240
HT2 0250
HT2 0260
HT2 0270
HT2 0280
HT2 0290
HT2 0300
HT2 0310
HT2 0320
HT2 0330
HT2 0340
HT2 0350
HT2 0360
HT2 0370
HT2 0380
HT2 0390
HT2 0400
HT2 0410
HT2 0420
HT2 0430
HT2 0440
HT2 0450
HT2 0460
HT2 0470
HT2 0480
HT2 0490
HT2 0500
HT2 0510
HT2 0520
HT2 0530
HT2 0540
HT2 0550
HT2 0560
HT2 0570
HT2 0580
HT2 0590

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2 NUSSELT NUMBER/9H POSITION/5H FROM16X6HANNULI11X5HFLAME1X2(9X16HANHT2 0600
3 NULL FLAME)/11H COMPRESSOR27X4HTUBE2X 2(20X5HTUBE )/10H DISCHT2 0610
4 LARGE6X5HINNER 6X5HOUTER16X2(14H INNER OUTER11X)/7H INCHES//(1X HT2 0620
5 F8.3,3X3E11.3,3X3F7.3,4X3F7.2)) HT2 0630
4 FORMAT(/////20HOHEAT TRANSFER RATES/1X19(1H-)/6HOAXIAL12X2(20H HEHT2 0640
1 AT TRANSFER RATE12X),9HRADIATION6X16HEAT TRANSFERRED/9H POSITION1HT2 0650
2 1X18HFROM FLAME TO WALL14X19HFROM WALL TO ANNULI10X11HINTERCHANGE5HT2 0660
3 X16HTC TRANSPIRATION/5H FROM11X2(21H BTU PER SQ FT SEC11X),13HFHT2 0670
4 ROM OPPOSITE4X15HAIR IN THE WALL/11H COMPRESSOR69X12HWALL BTU PER5HT2 0680
5 X15HBTU PER SEC PER/10H DISCHARGE2(7X23HRADIATION CONVECTION2X)HT2 0690
6 ,8X9HSQ FT SEC5X18HSQ FT WALL SURFACE/7H INCHES/14XA6,1XA6,2XA6,1XHT2 0700
7 A6,4XA6,1XA6,2XA6,1XA6,5XA6,1XA6,6XA6,1XA6//(1XF8.3,1X2(F10.3,F7.3HT2 0710
8 ,F8.3,F7.3),2(F11.3,F7.3))) HT2 0720
41 FORMAT(/////25HOHEAT TRANSFER PARAMETERS/1X24(1H-)/6HOAXIAL8X18HEMHT2 0730
1 ISSIVITY FLAME12X12HFILM-COOLING17X17HWALL TEMPERATURES/36H POSIHT2 0740
2 TION OF FLAME INTENSITY8X13HEFFECTIVENESS22X5HDEG F/5H FROHT2 0750
3 M22X7HBTU PER/11H COMPRESSOR16X9HSQ FT SEC33X9HADIABATIC9X6HACTUALHT2 0760
4 /10H DISCHARGE/7H INCHES32X24HINNER WALL OUTER WALL 2(17H INNHT2 0770
5 ER OUTER)//(1XF8.3,F12.3,F13.3,2F12.3,5X2(F9.1,F8.1))) HT2 0780
C HT2 0790
NUM=1 HT2 0800
20 K=1 HT2 0810
C HT2 0820
C SET LARGEST ERROR SO FAR TO ZERO HT2 0830
C HT2 0840
BIGDIF=0. HT2 0850
C HT2 0860
C SET CALCULATION TO INNER ANNULUS HT2 0870
C HT2 0880
30 INXAN=1 HT2 0890
40 IF(K.EC.1)GO TO 300 HT2 0900
C HT2 0910
C*****CALCULATE LONGITUDINAL CONDUCTION EFFECT HT2 0920
C HT2 0930
IF(K.EC.NLAST)GO TO 400 HT2 0940
GO TO (450,50,90,50),NHT2 HT2 0950
50 IF(INXAN.EQ.2)GO TO 70 HT2 0960
DELTW1=TWA(K-1)-TWA(K) HT2 0970
DELTW2=TWA(K)-TWA(K+1) HT2 0980
GO TO 80 HT2 0990
70 DELTW1=TWB(K-1)-TWB(K) HT2 1000
DELTW2=TWB(K)-TWB(K+1) HT2 1010
80 DELX1=XCP(K)-XCP(K-1) HT2 1020
DELX2=XCP(K+1)-XCP(K) HT2 1030
DELK=2.*CONDFT*THIKFT*(DELTW1/DELX1/(DELX1+DELX2)-DELTW2/DELX2/ HT2 1040
1(DELX1+DELX2)) /3600. HT2 1050
IF(NHT2.EQ.2)GO TO 130 HT2 1060
C HT2 1070
C*****CALCULATE TOTAL RADIATION INTERCHANGE EFFECT HT2 1080
C HT2 1090
90 S1=0 HT2 1100
S2=0 HT2 1110
NN=NLAST-1 HT2 1120
DO 120 KK=2,NN HT2 1130
X1=(XCP(KK+1)-XCP(KK-1))/2. HT2 1140
IF(INXAN.EQ.2)GO TO 100 HT2 1150
DUMR4=(CCA(KK)/PI+DANA(KK)+DFT(KK))/2. HT2 1160
DUMR5=(CCA(K)/PI+DANA(K))/2. HT2 1170
X3=TWB(KK)**4 HT2 1180
GO TO 110 HT2 1190
100 DUMR4=(CCA(KK)/PI+DANA(KK))/2. HT2 1200

```

	DUMR5=(CCA(K)/PI+DANA(K)+DFT(K))/2.	HT2 1210
	X3=TWA(KK)**4	HT2 1220
110	DUMR6=DUMR4-DUMR5	HT2 1230
	X4=(DUMR6**2+(XCP(K)-XCP(KK))**2)**1.5	HT2 1240
	X2=14.82/(14.82+(FMOCO2(K)+FMOH2O(K))*SQRT(DUMR6**2+(XCP(K)-XCP	HT2 1250
	1(KK))**2)*PREFT(K))	HT2 1260
	S1=S1+X1*X2*X3*DUMR4/X4/DUMR5	HT2 1270
	S2=S2+X1*X2*DUMR4/X4/DUMR5	HT2 1280
120	CONTINUE	HT2 1290
C		HT2 1300
C	FORM CORRECTED OPPOSITE WALL TEMPERATURE	HT2 1310
C		HT2 1320
	TSTAR2=S1/S2	HT2 1330
C		HT2 1340
C	*****CALCULATE TOTAL RADIATION COEFFICIENT FROM OPPOSITE WALL,AAA	HT2 1350
C		HT2 1360
	AAA=2.4E-13*EMW**2*DFT(K)**2*S2	HT2 1370
	IF(INXAN.EQ.2)GO TO 125	HT2 1380
	DELK=AAA*(TSTAR2-TWA(K)**4)	HT2 1390
	GO TO 130	HT2 1400
125	DELK=AAA*(TSTAR2-TWB(K)**4)	HT2 1410
130	IF(NHT2.EQ.1)GO TO 450	HT2 1420
C		HT2 1430
C	MODIFY COEFFICIENTS IN HEAT BALANCE EQUATION	HT2 1440
C		HT2 1450
	IF(INXAN.EQ.2)GO TO 170	HT2 1460
	D1=D1A(K)	HT2 1470
	D2=D2A(K)	HT2 1480
	D3=D3A(K)	HT2 1490
	GO TO(450,140,150,160),NHT2	HT2 1500
140	IF(ABS(DELK).GT.(0.05*D4A(K)))GO TO 145	HT2 1510
	D4=D4A(K)+DELK	HT2 1520
	GO TO 200	HT2 1530
145	D4=D4A(K)+DELK*0.05*D4A(K)/ABS(DELK)	HT2 1540
	GO TO 200	HT2 1550
150	IF(ABS(DELK).GT.(0.05*D4A(K)))GO TO 155	HT2 1560
	D4=D4A(K)+DELK	HT2 1570
	GO TO 200	HT2 1580
155	D4=D4A(K)+DELK*0.05*D4A(K)/ABS(DELK)	HT2 1590
	GO TO 200	HT2 1600
160	IF(ABS(DELK+DELK).GT.(0.05*D4A(K)))GO TO 165	HT2 1610
	D4=D4A(K)+DELK+DELK	HT2 1620
	GO TO 200	HT2 1630
165	D4=D4A(K)+(DELK+DELK)*0.05*D4A(K)/ABS(DELK+DELK)	HT2 1640
	GO TO 200	HT2 1650
170	D1=D1B(K)	HT2 1660
	D2=D2B(K)	HT2 1670
	D3=D3B(K)	HT2 1680
	GO TO(450,171,180,190),NHT2	HT2 1690
171	IF(ABS(DELK).GT.(0.05*D4B(K)))GO TO 175	HT2 1700
	D4=D4B(K)+DELK	HT2 1710
	GO TO 200	HT2 1720
175	D4=D4B(K)+DELK*0.05*D4B(K)/ABS(DELK)	HT2 1730
	GO TO 200	HT2 1740
180	IF(ABS(DELK).GT.(0.05*D4B(K)))GO TO 185	HT2 1750
	D4=D4B(K)+DELK	HT2 1760
	GO TO 200	HT2 1770
185	D4=D4B(K)+DELK*0.05*D4B(K)/ABS(DELK)	HT2 1780
	GO TO 200	HT2 1790
190	IF(ABS(DELK+DELK).GT.(0.05*D4B(K)))GO TO 195	HT2 1800
	D4=D4B(K)+DELK+DELK	HT2 1810

	GO TO 200	HT2 1820
195	D4=D4B(K)+(DELR+DELK)*0.05*D4B(K)/ABS(DELR+DELK)	HT2 1830
200	IF(D4.LE.0.)GOTO490	HT2 1840
	CALL TWSOLN(K,D1,D2,D3,D4,DTW1)	HT2 1850
	IF(INXAN.EQ.2)GO TO 230	HT2 1860
	TWAX(K)=(TWA(K)+DTW1)/2.	HT2 1870
	R3A(K)=AAA*(TSTAR2-TWAX(K)**4)	HT2 1880
	INXAN=2	HT2 1890
	GO TO 40	HT2 1900
230	TWBX(K)=(TWB(K)+DTW1)/2.	HT2 1910
	R3B(K)=AAA*(TSTAR2-TWBX(K)**4)	HT2 1920
300	K=K+1	HT2 1930
	GO TO 30	HT2 1940
C		HT2 1950
C	CALCULATE FIRST AND LAST CALCULATION POINT TEMPERATURES BY LINEAR	HT2 1960
C	EXTRAPCLATION	HT2 1970
C		HT2 1980
400	TWAX(1)=(TWAX(2)-TWAX(3))*(XCP(2)-XCP(1))/(XCP(3)-XCP(2))+TWAX(2)	HT2 1990
	TWBX(1)=(TWBX(2)-TWBX(3))*(XCP(2)-XCP(1))/(XCP(3)-XCP(2))+TWBX(2)	HT2 2000
	TWAX(NLAST)=(TWAX(NLAST-1)-TWAX(NLAST-2))*(XCP(NLAST)-XCP(NLAST-1)	HT2 2010
	1)/(XCP(NLAST-1)-XCP(NLAST-2))+TWAX(NLAST-1)	HT2 2020
	TWBX(NLAST)=(TWBX(NLAST-1)-TWBX(NLAST-2))*(XCP(NLAST)-XCP(NLAST-1)	HT2 2030
	1)/(XCP(NLAST-1)-XCP(NLAST-2))+TWBX(NLAST-1)	HT2 2040
	DO 430 NN=1,NLAST	HT2 2050
C		HT2 2060
C	COMPARE EACH ERROR WITH THE LARGEST ERROR AND STORE THE LARGEST	HT2 2070
C		HT2 2080
	DIFF=ABS(TWA(NN)-TWAX(NN))	HT2 2090
	IF(DIFF.LE.BIGDIF)GO TO 410	HT2 2100
	BIGDIF=DIFF	HT2 2110
410	DIFF=ABS(TWB(NN)-TWBX(NN))	HT2 2120
	IF(DIFF.LE.BIGDIF)GO TO 420	HT2 2130
	BIGDIF=DIFF	HT2 2140
C		HT2 2150
C	SUBSTITUTE PREVIOUS TEMPERATURE DISTRIBUTION BY CURRENT TEMPERATURE	HT2 2160
C	DISTRIBUTION	HT2 2170
C		HT2 2180
420	TWA(NN)=TWAX(NN)	HT2 2190
	TWB(NN)=TWBX(NN)	HT2 2200
430	CONTINUE	HT2 2210
C		HT2 2220
C	COMPARE LARGEST ERROR WITH TOLERANCE	HT2 2230
C		HT2 2240
	IF(BIGDIF.LE.TOLTW2)GO TO 450	HT2 2250
C		HT2 2260
C	CHECK THAT LOOP COUNTER HAS NOT BEEN EXCEEDED	HT2 2270
C		HT2 2280
	IF(NUM.LT.NUMAX2)GO TO 440	HT2 2290
	WRITE(6,1)NUMAX2,TOLTW2	HT2 2300
	GO TO 450	HT2 2310
440	NUM=NUM+1	HT2 2320
	GO TO 20	HT2 2330
450	DO 460 KK=1,NLAST	HT2 2340
	XCP(KK)=XCP(KK)*12.	HT2 2350
	IF(TWADA(KK).NE.0.)TWADA(KK)=TWADA(KK)-TZ	HT2 2360
	IF(TWADB(KK).NE.0.)TWADB(KK)=TWADB(KK)-TZ	HT2 2370
	TWA(KK)=TWA(KK)-TZ	HT2 2380
460	TWB(KK)=TWB(KK)-TZ	HT2 2390
C		HT2 2400
C	WRITE OUT ALL REQUIRED OUTPUT	HT2 2410
C		HT2 2420

```
WRITE(JTAPE,39)(XCP(K),REAN(K),REBAN(K),REFT(K),PRAAN(K),PRBAN(K)HT2 2430
1,PRFT(K),TNUAAN(K),TNUBAN(K),TNUFT(K),K=1,NLAST) HT2 2440
WRITE(JTAPE,4)((NAME(I),I=1,2),J=1,6),(XCP(K),R1A(K),R1B(K),C1A(K) HT2 2450
1),C1B(K),R2A(K),R2B(K),C2A(K),C2B(K),R3A(K),R3B(K),QTRA(K),QTRB(K)HT2 2460
2,K=1,NLAST) HT2 2470
WRITE(JTAPE,41)(XCP(K),EMFT(K),FINT(K),FILMFA(K),FILMFB(K),TWADA(K)HT2 2480
1),TWADB(K),TWA(K),TWB(K),K=1,NLAST) HT2 2490
DO 480 KK=1,NLAST HT2 2500
XCP(KK)=XCP(KK)/12. HT2 2510
TWA(KK)=TWA(KK)+TZ HT2 2520
480 TWB(KK)=TWB(KK)+TZ HT2 2530
490 RETURN HT2 2540
END HT2 2550
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\$IBFTC TWAL

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SUBROUTINE TWSOLN(K,D1,D2,D3,D4,DTW1)
C
C
C
SUBROUTINE TWSOLN
THIS SUBROUTINE USES NEWTONS METHOD TO SOLVE THE HEAT BALANCE EQUATION
D1 * TW**4 + D2 * TW**2.5 + D3 * TW = D4
THIS SUBROUTINE IS CALLED FOR BY TWO SUBROUTINES
1. HEAT1
2. HEAT2
IS SUBROUTINE USES COMMON BLOCKS WHOSE NAMES CONTAIN THE NUMBER 8
VIZ- B8, B18, B68, B168, B178, B678, B1678, B12678
COMMON/B8/D1A(45),D2A(45),D3A(45),D4A(45),D1B(45),D2B(45),D3B(45)
1,D4B(45),FMOCO2(45),FMOH2O(45),C1A(45),C1B(45),R1A(45),R1B(45),R2
2A(45),R2B(45),R3A(45),R3B(45),TNUAAN(45),TNUBAN(45),TNUFT(45),
3TWADA(45),TWADB(45),
4EMFT(45),FILMFA(45),FILMFB(45),PRAAN(45),PRBAN(45),PRFT(45),REFT(4
55),FINT(45),TCFA(45),TCFB(45),UFTA(45),UFTB(45),UJ1A(45),UJ1B(45),
6AFJA(45),AFJB(45),YCFA(45),YCFB(45)
COMMON/B18/ABSW,EMW,EMC,NLUM, NHT1,NHT2
1, X1FCA(45),X1FCB(45),CONDFT,TCASA(45),TCASB(45),TOLTW1,TOLTTW
2W2,XFILMZ, TABTFT(10),TABEFT(100),TABPFT(10),NEFT,NPFT,NFORMT
3, NCOOL, NUMAX1,NUMAX2
COMMON/B68/AFANA(45),AFANB(45),AFFT(45),AFPRZ,C2A(45),C2B(45)
1, AFSYP,FARFT(45),DENANA(45),DENANB(45)
3,SAFTRA(45),SAFTRB(45),QTRA(45),QTRB(45),REAN(45),REBAN(45)
4,TWA(45),TWB(45)
COMMON/B168/AANA(45),AANB(45),CCA(45),CCB(45),FHCR,NLAST
1,KANHET,LANHET,PERCO,THIKFT
2,DANA(45),DANB(45)
COMMON/B178/DFT(45)
COMMON/B678/PREFT(45),PREANA(45),PREANB(45),TFT(45),TANANA(45),TANT
1ANB(45),AFJ1(50),UFT(45)
COMMON/B1678/NSHCP,XCP(45),AFT(45),PI
1,NHH(50),KJSN(45,6),HAU(50),CFTA(45),CFTB(45),NAB(50),NCODEA(45)
2,NCODEB(45),TZ
COMMON/B12678/JTAPE ,IPRINT
1 FORMAT(6H AFTER I4,30H TRIALS, ERROR IS GREATER THAN,F9.2,6H DEG R)
2 FORMAT(38H CHECK INPUT DATA TO SUBROUTINE TWSOLN)
*** CONVERT THE COEFFICIENTS TO A MORE MANAGABLE SIZE *****
DEE1=D1*10.**12
DEE2=D2*3.11*10.**7
DEE3=D3*10.**3
*** MAKE FIRST GUESSES AT THE SOLUTION AND CHOOSE THE ONE WHICH
GIVES THE SMALLEST POSITIVE ERROR *****
DTW1=(D4/DEE1)**0.25
DUMER1=DEE1*DTW1**4+DEE2*DTW1**2.5+DEE3*DTW1-D4
DTW2=(D4/DEE2)**0.4
DUMER2=DEE1*DTW2**4+DEE2*DTW2**2.5+DEE3*DTW2-D4
DTW3=D4/DEE3
DUMER3=DEE1*DTW3**4+DEE2*DTW3**2.5+DEE3*DTW3-D4

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DTW4=TFT(K)/1000.	TWAL0060
DUMER4=DEE1*DTW4**4+DEE2*DTW4**2.5+DEE3*DTW4-D4	TWAL0061
IF(DTW1.LE.DTW2.AND.DUMER1.GE.0.)GO TO 10	TWAL0062
DTW1=DTW2	TWAL0063
10 IF(DTW1.LE.DTW3.AND.DUMER2.GE.0.)GO TO 20	TWAL0064
DTW1=DTW3	TWAL0065
20 IF(DTW1.LE.DTW4.AND.DUMER3.GE.0.)GO TO 30	TWAL0066
DTW1=DTW4	TWAL0067
IF(DUMER4.GE.0.)GO TO 30	TWAL0068
WRITE(6,2)	TWAL0069
30 NUM=1	TWAL0070
	TWAL0071
C***** CALCULATE A NEW VALUE USING NEWTONS METHOD	TWAL0072
	TWAL0073
40 DTW1=DTW1-(DEE1*DTW1**4+DEE2*DTW1**2.5+DEE3*DTW1-D4)/(4.*DEE1*DTW1	TWAL0074
1**3+2.5*DEE2*DTW1**1.5+DEE3)	TWAL0075
DUMER1=DEE1*DTW1**4+DEE2*DTW1**2.5+DEE3*DTW1-D4	TWAL0076
IF(D4*DEE2.LT.0.)DTW2=0.	TWAL0077
IF(D4*DEE2.GT.0.)DTW2=(D4/DEE2)**.4	TWAL0078
IF(DEE2*(DTW1-TOLTW1/1000.).GE.0.)	TWAL0079
1DUMER2=DEE1*(DTW1-TOLTW1/1000.)**4+DEE2*(DTW1-TOLTW1/1000.)**2.5+	TWAL0080
1DEE3*(DTW1-TOLTW1/1000.)-D4	TWAL0081
DUMER3=DEE1*(DTW1+TOLTW1/1000.)**4+DEE2*(DTW1+TOLTW1/1000.)**2.5+	TWAL0082
1DEE3*(DTW1+TOLTW1/1000.)-D4	TWAL0083
IF((DUMER1.GE.0..AND.DUMER2.LE.0.).OR.(DUMER1.LE.0..AND.DUMER3.GE.	TWAL0084
10.))GO TO 50	TWAL0085
NUM=NUM+1	TWAL0086
IF(NUM.LE.NUMAX1)GO TO 40	TWAL0087
WRITE(JTAPE,1)NUMAX1,TOLTW1	TWAL0088
50 DTW1=DTW1*1000.	TWAL0089
RETURN	TWAL0090
END	TWAL0091

\$IBFTC EEF LIST

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SUBROUTINE EEFT(K)
C
C          S U B R O U T I N E   E E F T
C
C          THIS SUBROUTINE EVALUATES THE FLAME EMMISIVITY FROM ANY ONE
C          OF FIVE CORRELATIONS, OR FROM TABULATED DATA.
C
C          SUBROUTINE EEFT IS CALLED FOR BY ONE SUBROUTINE
C          1. HEAT1
C THIS SUBROUTINE USES COMMON BLOCKS WHOSE NAMES CONTAIN THE NUMBER 8
C          VIZ- B8, B18, B68, B168, B178, B678, B1678, B12678
C
COMMON/B8/D1A(45),D2A(45),D3A(45),D4A(45),D1B(45),D2B(45),D3B(45)
1,D4B(45),FMOC2(45),FMOH20(45),C1A(45),C1B(45),R1A(45),R1B(45),R2
2A(45),R2B(45),R3A(45),R3B(45),TNUAAN(45),TNUBAN(45),TNUFT(45),
3TWADA(45),TWADB(45),
4EMFT(45),FILMFA(45),FILMFB(45),PRAAN(45),PRBAN(45),PRFT(45),REFT(4
55),FINT(45),TCFA(45),TCFB(45),UFTA(45),UFTB(45),UJ1A(45),UJ1B(45),
6AFJA(45),AFJB(45),YCFA(45),YCFB(45)
COMMON/B18/ABSW,EMW,EMC,NLUM,
1,
X1FCA(45),X1FCB(45),CONDF,TCASA(45),TCASB(45),TOLTW1,TOLTEEFT0220
2W2,XFILMZ,
TABTFT(10),TABEFT(100),TABPFT(10),NEFT,NPFT,NFORMEEFT0230
3,NCOOL,
NUMAX1,NUMAX2
COMMON/B68/AFANA(45),AFANB(45),AFFT(45),AFPRZ,C2A(45),C2B(45)
1
,
AFSYP,FARFT(45),DENANA(45),DENANB(45)
3,SAFTRA(45),SAFTRB(45),QTRA(45),QTRB(45),REAN(45),REBAN(45)
4,TWA(45),TWB(45)
COMMON/B168/AANA(45),AANB(45),CCA(45),CCB(45),FHCR,NLAST
1,KANHET,LANHET,PERCO,THIKFT
2,DANA(45),DANB(45)
COMMON/B178/DFT(45)
COMMON/B678/PREFT(45),PREANA(45),PREANB(45),TFT(45),TANANA(45),TANE
1ANB(45),AFJ1(50),UFT(45)
COMMON/B1678/NSHCP,XCP(45),AFT(45),PI
1,NHH(50),KJSN(45,6),HAU(50),CFTA(45),CFTB(45),NAB(50),NCODEA(45)
2,NCODEB(45),TZ
COMMON/B12678/JTAPE , IPRINT
C
2 FORMAT(5H EEFT,10X,5(E12.5,2X),I5)
IF(IPRINT.EQ.1)
1WRITE(6
,2) TFT(K),FARFT(K),PREFT(K),FHCR,DFT(K),NLUM
IF(FARFT(K).LE.0.)FARFT(K)=1.E-4
IF(NLUM.EQ.6)GO TO 70
DUMCOR=-((10.**4*(.9*DFT(K)*FARFT(K))**.5*TFT(K)**(-1.5))
GO TO(10,20,30,50,60,70),NLUM
C
NLUM=1 NON-LUMINOUS CORRELATION FOR DISTILLATE FUELS
10 EMFT(K)=1.-EXP(0.00184*PREFT(K)*DUMCOR)
RETURN
C
NLUM=2 NON-LUMINOUS CORRELATION FOR RESIDUAL FUELS
20 EMFT(K)=1.-EXP(0.01530*PREFT(K)**0.75*DUMCOR)
RETURN
C
NLUM=3 LEFEBVRE CORRELATION FOR LUMINOUS FLAMES

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EEFT0010
EEFT0C20
EEFT0030
EEFT0040
EEFT0050
EEFT0C60
EEFT0070
EEFT0C80
EEFT0090
EEFT0100
EEFT0110
EEFT0120
EEFT0130
EEFT0140
EEFT0150
EEFT0160
EEFT0170
EEFT0180
EEFT0190
EEFT0200
EEFT0210
EEFT0220
EEFT0230
EEFT0240
EEFT0250
EEFT0260
EEFT0270
EEFT0280
EEFT0290
EEFT0300
EEFT0310
EEFT0320
EEFT0330
EEFT0340
EEFT0350
EEFT0360
EEFT0370
EEFT0380
EEFT0390
EEFT0400
EEFT0410
EEFT0420
EEFT0430
EEFT0440
EEFT0450
EEFT0460
EEFT0470
EEFT0480
EEFT0490
EEFT0500
EEFT0510
EEFT0520
EEFT0530
EEFT0540
EEFT0550
EEFT0560
EEFT0570
EEFT0580
EEFT0590

30	DUMLUM=7.53*(1./FHCR-5.5)**0.85	EEFT0600
40	EMFT(K)=1.-EXP(0.00184*DUMLUM*PREFT(K)*DUMCOR)	EEFT0610
	RETURN	EEFT0620
	NLUM=4 NREC 1964 CORRELATION FOR LUMINOUS FLAMES	EEFT0630
		EEFT0640
50	DUMLUM=EXP((1.-4.4*FHCR)/(2.3*FHCR))	EEFT0650
	GO TO 40	EEFT0660
		EEFT0670
	NLUM=5 NREC 1966 CORRELATION FOR LUMINOUS FLAMES	EEFT0680
		EEFT0690
60	DUMLUM=((1.-FHCR*5.)/(FHCR*0.16))**0.74	EEFT0700
	EMFT(K)=1.-EXP(0.0000474*PREFT(K)**1.3*DUMCOR*DUMLUM)	EEFT0710
	RETURN	EEFT0720
		EEFT0730
	NLUM=6 VALUE INTERPOLATED FROM DATA	EEFT0740
		EEFT0750
70	DUMT=TFT(K)	EEFT0760
	DUMYP=PREFT(K)	EEFT0770
	CALLINTPL8(DUMT,DUMYP,TABTFT,TABEFT,TABPFT,NFORM,NEFT,NPFT,	EEFT0780
	1 DUMEFT)	EEFT0790
	EMFT(K)=DUMEFT	EEFT0800
80	RETURN	EEFT0810
	END	EEFT0820
		EEFT0830

\$IBFTC PROP LIST

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SUBROUTINE PROP(K,CNDAV,FMCO2,FMH2O)
C
C      S U B R O U T I N E   P R O P
C
C      THIS SUBROUTINE EVALUATES THE THERMAL CONDUCTIVITY, DYNAMIC
C      VISCOSITY, SPECIFIC HEAT, REYNOLDS NUMBER, PRANDTL NUMBER,
C      AND NUSSELT NUMBER FOR THE GAS MIXTURE IN THE FLAME TUBE.
C
C      THIS SUBROUTINE CALLS FOR ONE SUBROUTINE
C      1. INTPL8
C
C      SUBROUTINE PROP IS CALLED FOR BY ONE SUBROUTINE
C      1. HEAT1
C
C THIS SUBROUTINE USES COMMON BLOCKS WHOSE NAMES CONTAIN THE NUMBER 8
C VIZ- B8, B18, B68, B168, B178, B678, B1678, B12678
C
COMMON/B8/D1A(45),D2A(45),D3A(45),D4A(45),D1B(45),D2B(45),D3B(45)
1,D4B(45),FMCO2(45),FMH2O(45),C1A(45),C1B(45),R1A(45),R1B(45),R2
2A(45),R2B(45),R3A(45),R3B(45),TNUAAN(45),TNUBAN(45),TNUFT(45),
3TWADA(45),TWADB(45),
4EMFT(45),FILMFA(45),FILMFB(45),PRAAN(45),PRBAN(45),PRFT(45),REFT(4
55),FINT(45),TCFA(45),TCFB(45),UFTA(45),UFTB(45),UJ1A(45),UJ1B(45),
6AFJA(45),AFJB(45),YCFA(45),YCFB(45)
COMMON/B18/ABSW,EMW,EMC,NLUM,
1,
X1FCA(45),X1FCB(45),CONDFT,TCASA(45),TCASB(45),TOLTW1,TOLTP
2WZ,XFILMZ,
TABTFT(10),TABEFT(100),TABPFT(10),NEFT,NPFT,NFORM
3,NCool,
NUMAX1,NUMAX2
COMMON/B68/AFANA(45),AFANB(45),AFFT(45),AFPRZ,C2A(45),C2B(45)
1,
AFSYP,FARFT(45),DENANA(45),DENANB(45)
3,SAFTRA(45),SAFTRB(45),QTRA(45),QTRB(45),REAN(45),REBAN(45)
4,TWA(45),TWB(45)
COMMON/B168/AANA(45),AANB(45),CCA(45),CCB(45),FHCR,NLAST
1,KANHET,LANHET,PERCO,THIKFT
2,DANA(45),DANB(45)
COMMON/B178/DFT(45)
COMMON/B678/PREFT(45),PREANA(45),PREANB(45),TFT(45),TANANA(45),TAN
1ANB(45),AFJ1(50),UFT(45)
COMMON/B1678/NSHCP,XCP(45),AFT(45),PI
1,NHH(50),KJSN(45,6),HAU(50),CFTA(45),CFTB(45),NAB(50),NCODEA(45)
2,NCODEB(45),TZ
COMMON/B12678/JTAPE,IPRINT
C*****
C*****COMPARE THE CURRENT FUEL-AIR RATIO TO THE STOICHIOMETRIC FUEL-AIR
C*****RATIO AND CALCULATE THE MOLE FRACTIONS OF CO2,H2O,N2, AND O2
C*****
FARSTO=0.0862*(1.+FHCR)/(1.+3.*FHCR)
IF(FARFT(K).GT.FARSTO)GOTO 10
DUMOLE=25.*FHCR+3.45*(1.+FHCR)/FARFT(K)
FMO2=(0.72*(1.+FHCR)/FARFT(K)-8.33-25.*FHCR)/DUMOLE
FMN2=2.75*(1.+FHCR)/FARFT(K)/DUMOLE
FMCO2=8.33/DUMOLE
FMH2O=50.*FHCR/DUMOLE
GOTO 20
10 FMO2=0.021
FMN2=0.748
FMCO2=0.1
PROP0010
PROP0C20
PROP0C30
PROP0040
PROP0C5C
PROP0C60
PROP0070
PROP0080
PROP0090
PROP0100
PROP0110
PROP0120
PROP0130
PROP0140
PROP0150
PROP0160
PROP017C
PRCPC180
PRCPC190
PROP020C
PROP0210
PROP0220
PROP0230
PROP0240
PROP0250
PROP0260
PROP0270
PROP0280
PROP0290
PROP0300
PROP0310
PROP0320
PROP0330
PROP0340
PROP0350
PROP0360
PROP0370
PROP0380
PROP0390
PROP0400
PROP0410
PROP0420
PROP0430
PROP0440
PROP0450
PROP0460
PROP0470
PROP0480
PROP0490
PROP0500
PROP0510
PROP0520
PROP0530
PROP0540
PROP0550
PROP0560
PROP0570
PROP0580
PROP0590

```

```

FMH2O=0.131
20 T1=TFT(K)*1.E-3
T2=TFT(K)**2*1.E-6
C***** EVALUATE THE THERMAL CONDUCTIVITY OF THE MIXTURE *****
CND02 = .0155 + .0157*T1
CNDN2 = .01352+ .01401*T1
CNDCO2= .0111 + .0156*T1
CNDH2O=-.0145 + .0456*T1
CNDAV=(CND02*FM02*3.18+CNDN2*FMN2*3.04+CNDCO2*FMCO2*3.53+CNDH2O*
1FMH2O*2.62)/(FM02*3.18+FMN2*3.04+FMCO2*3.53+FMH2O*2.62)
C***** EVALUATE THE DYNAMIC VISCOSITY OF THE MIXTURE *****
VIS02 = .0550 + .0345*T1
VISN2=.0479+.0277*T1
VISCO2=.0423+.0296*T1
VISH2O=.0174+.039*T1
VISAV=(VIS02*FM02*5.65+VISN2*FMN2*5.29+VISCO2*FMCO2*6.62+VISH2O*
1FMH2O*4.24)/(FM02*5.65+FMN2*5.29+FMCO2*6.62+FMH2O*4.24)
C***** EVALUATE THE SPECIFIC HEAT OF THE MIXTURE *****
CPO2=.242+.01057*T1
CPN2=.232+.0313*T1-.00293*T2
CPCO2=.228+.0454*T1-.00489*T2
CPH2O=.334+.141*T1-.0124*T2
CPAV=(CPO2*FM02*32.+CPN2*FMN2*28.+CPCO2*FMCO2*44.+CPH2O*FMH2O*18.0
1)/(FM02*32.+FMN2*28.+FMCO2*44.+FMH2O*18.)
C*****IF CALCULATION POINT IS IN THE PRIMARY ZONE ALLOW FOR
C*****RECIRCULATION WHEN CALCULATING REYNOLDS NUMBER IN THE FLAME TUBE
IF(K.GT.NSHCP) GOTO 30
REFT(K)=7200.*DFT(K)*(AFPRZ+AFSYP)/(VISAV*AFT(K))
GOTO 40
30 REFT(K)=DFT(K)*3600.*AFFT(K)/VISAV/AFT(K)
C*****CALCULATE PRANDTL NUMBER IN THE FLAME-TUBE
40 PRFT(K)=CPAV*VISAV/CNDAV
IF(REFT(K).LT.1.)REFT(K)=1.
IF(PRFT(K).LT..01)PRFT(K)=.01
C*****CALCULATE NUSSOLT NUMBER IN THE FLAME-TUBE
TNUFT(K)=0.023*REFT(K)**0.8*PRFT(K)**0.4
RETURN
END

```

PROP0600
PROP0610
PROP0620
PROP0630
PROP0640
PROP0650
PROP0660
PROP0670
PROP0680
PROP0690
PROP0700
PROP0710
PROP0720
PROP0730
PROP0740
PROP0750
PROP0760
PROP0770
PROP0780
PROP0790
PROP0800
PROP0810
PROP0820
PROP0830
PROP0840
PROP0850
PROP0860
PROP0870
PROP0880
PROP0890
PROP0900
PROP0910
PROP0920
PROP0930
PROP0940
PROP0950
PROP0960
PROP0970
PROP0980
PROP0990
PROP1000
PROP1010
PROP1020
PROP1030
PROP1040
PROP1050
PROP1060
PROP1070
PROP1080
PROP1090

```

$IBFTC COO LIST
SUBROUTINE COOL(K, INXAN, CNDAV, TRNSCO, CFTRN)
C
C SUBROUTINE COOL
C
C THIS SUBROUTINE EVALUATES FILM COOLING OR TRANSPIRATION
C COOLING PARAMETERS
C
C SUBROUTINE COOL IS CALLED FOR BY ONE SUBROUTINE
C 1. HEAT1
C THIS SUBROUTINE USES COMMON BLOCKS WHOSE NAMES CONTAIN THE NUMBER 8
C VIZ- B8, B18, B68, B168, B178, B678, B1678, B12678
COMMON/B8/D1A(45),D2A(45),D3A(45),D4A(45),D1B(45),D2B(45),D3B(45)
1,D4B(45),FMOCO2(45),FMOH2O(45),C1A(45),C1B(45),R1A(45),R1B(45),R2
2A(45),R2B(45),R3A(45),R3B(45),TNUAAN(45),TNUBAN(45),TNUFT(45),
3TWADA(45),TWADB(45),
4EMFT(45),FILMFA(45),FILMFB(45),PRAAN(45),PRBAN(45),PRFT(45),REFT(45)
55),FINT(45),TCFA(45),TCFB(45),UFTA(45),UFTB(45),UJ1A(45),UJ1B(45),
6AFJA(45),AFJB(45),YCFA(45),YCFB(45)
COMMON/B18/ABSW,EMW,EMC,NLUM, NHT1,NHT2
1, X1FCA(45),X1FCB(45),CONDFT,TCASA(45),TCASB(45),TDLTW1,TDLT
2W2,XFILMZ, TABTFT(10),TABEFT(100),TABPFT(10),NEFT,NPFT,NFORMC
3, NCOOL, NUMAX1,NUMAX2
COMMON/B68/AFANA(45),AFANB(45),AFFT(45),AFPRZ,C2A(45),C2B(45)
1, AFSYP,FARFT(45),DENANA(45),DENANB(45)
3,SAFTRA(45),SAFTRB(45),QTRA(45),QTRB(45),REAN(45),REBAN(45)
4,TWA(45),TWB(45)
COMMON/B168/AANA(45),AANB(45),CCA(45),CCB(45),FHCR,NLAST
1,KANHET,LANHET,PERCO,THIKFT
2,DANA(45),DANB(45)
COMMON/B178/DFT(45)
COMMON/B678/PREFT(45),PREANA(45),PREANB(45),TFT(45),TANANA(45),TAN
1ANB(45),AFJ1(50),UFT(45)
COMMON/B1678/NSHCP,XCP(45),AFT(45),PI
1,NHH(50),KJSN(45,6),HAU(50),CFTA(45),CFTB(45),NAB(50),NCODEA(45)
2,NCODEB(45),TZ
COMMON/B12678/JTAPE,IPRINT
2 FORMAT(5H COOL,I5,7(E12.5,2X))
IF(NCOOL.EQ.2) GO TO 60
C***** FILM COOLING CALCULATION *****
C***** SET UP DUMMY FILM-COOLING VARIABLES *****
TFTDYN=UFT(K)*2/(2.*32.2*53.35)
TFT(K)=TFT(K)+TFTDYN
IF(INXAN.EQ.2) GO TO 10
IF(YCFA(K).EQ.0.0.OR.UJ1A(K).LT.0.001) GO TO 45
UFQ =UFTA(K)
UJ1 =UJ1A(K)
X1FC=X1FCA(K)
YCF =YCFA(K)
AFJ =AFJA(K)
TCF =TCFA(K)
PVZ=PREANA(K)
GO TO 20
10 IF(YCFB(K).EQ.0.0.OR.UJ1B(K).LT.0.001) GO TO 55
UFQ =UFTB(K)
UJ1 =UJ1B(K)
X1FC=X1FCB(K)
YCF =YCFB(K)

```

```

AFJ = AFJB(K)
TCF = TCFB(K)
PVZ = PREANB(K)
C***** FORM EXPRESSION FOR FILM-COOLING CORRELATION *****
20 AVZ = PVZ * YCF * 3600. / TCF / 53.3
XFILM = 0.91 * (UFQ / UJ1 * X1FC / YCF) ** 0.8 * (UJ1 * AVZ / (3.057E-3 + 8.607E-5 * TCF))
1-2.279E-8 * TCF ** 2 + 2.908E-12 * TCF ** 3) ** (-0.2) + 1.41 * (X1FC / YCF * ABS(1. -
2UFQ / UJ1)) ** 0.5
IF (IPRINT.EQ.1)
WRITE(6,2) K, XFILM, UFQ, UJ1, X1FC, YCF, AFJ, TCF
IF (XFILM.GE.XFILMZ * 1.43) GO TO 30
IF (XFILM.LT.(XFILMZ / 3.5)) GOTO 25
FILMEF = (XFILMZ / 3.5 / XFILM) ** 0.22
GO TO 40
25 FILMEF = 1.0
GO TO 40
30 FILMEF = XFILMZ / XFILM
40 TWAD = TFT(K) - FILMEF * (TFT(K) - TCF)
IF (INXAN.EQ.2) GO TO 50
FILMFA(K) = FILMEF
TWADA(K) = TWAD
GO TO 120
45 FILMFA(K) = 0.
TWADA(K) = TFT(K)
GO TO 120
50 FILMFB(K) = FILMEF
TWADB(K) = TWAD
GO TO 120
55 FILMFB(K) = 0.
TWADB(K) = TFT(K)
GO TO 120
C***** TRANSPIRATION COOLING *****
60 IF (INXAN.EQ.2) GO TO 80
IF (K.EQ.1.AND.KANHET.EQ.1) GO TO 70
IF (KANHET.EQ.1) GO TO 75
TWALL = TWA(K)
GO TO 100
70 TWALL = (TFT(K) + TANANA(K)) / 2.
GO TO 100
75 TWALL = TWA(K-1)
GO TO 100
80 IF (K.EQ.1.AND.KANHET.EQ.1) GO TO 90
IF (KANHET.EQ.1) GO TO 95
TWALL = TWB(K)
GO TO 110
90 TWALL = (TFT(K) + TANANB(K)) / 2.
GO TO 110
95 TWALL = TWB(K-1)
GO TO 110
100 TRNSCO = SAFTRA(K) * (0.2419 - 0.8181E-5 * TWALL + 1.791E-8 * TWALL ** 2 - 0.2743E-11 * TWALL ** 3)
CFTRN = CNDAV * 0.002 * REFT(K) / DFT(K) / 3600.
GO TO 120
110 TRNSCO = SAFTRB(K) * (0.2419 - 0.8181E-5 * TWALL + 1.791E-8 * TWALL ** 2 - 0.2743E-11 * TWALL ** 3)
CFTRN = CNDAV * 0.002 * REFT(K) / DFT(K) / 3600.
TFT(K) = TFT(K) - TFTDYN
120 RETURN
END

```

COOL0600
CCOL0610
CCOL0620
CCOL0630
CCOL0640
CCOL0650
CCOL0660
CCOL0670
CCOL0680
CCOL0690
CCOL0700
CCOL0710
CCOL0720
CCOL0730
CCOL0740
CCOL0750
CCOL0760
CCOL0770
CCOL0780
CCOL0790
CCOL0800
CCOL0810
CCOL0820
CCOL0830
CCOL0840
CCOL0850
CCOL0860
CCOL0870
CCOL0880
CCOL0890
CCOL0900
CCOL0910
CCOL0920
CCOL0930
CCOL0940
CCOL0950
CCOL0960
CCOL0970
CCOL0980
CCOL0990
CCOL1000
CCOL1010
CCOL1020
CCOL1030
CCOL1040
CCOL1050
CCOL1060
CCOL1070
CCOL1080
CCOL1090
CCOL1100
CCOL1110
CCOL1120
CCOL1130
CCOL1140
CCOL1150
CCOL1160
CCOL1170
CCOL1180

APPENDIX V
PROGRAM MESSAGES

Many of the subroutines contain format statements which are written out in the printout whenever the program wants to convey a particular message, generally as a result of an error which has arisen. A list of these statements is presented below; each statement is accompanied by an interpretation of the message and, where appropriate, an indication of what course of action should be taken. The statements are arranged with the first letters of the messages in alphabetic order to provide easy reference.

1. AFTER (NUMAX2) TRIALS, ERROR IS GREATER THAN (TOLTW2) DEG R
(Subroutine HEAT2, Heat-Transfer Subprogram). The iterative solution of the heat-balance equation has not converged to within the tolerance, TOLTW2, on the wall temperature after NUMAX2 attempts. If a solution is obtainable for the case where longitudinal conduction and radiation interchange are ignored, then check the input data relating to these two effects; if the input is correct, increase the values in Subroutine BLOCKDATA of either NUMAX2 or TOLTW2 or both.
2. AFTER (NUMAX1) TRIALS, ERROR IS GREATER THAN (TOLTW1) DEG R.
CHECK INPUT DATA TO SUBROUTINE TWSOLN (Subroutine TWSOLN, Heat-Transfer Subprogram). The solution of the heat-balance equation, using Newton's method, has not converged to within the tolerance, TOLTW2, on the wall temperature after NUMAX1 attempts. If the input appears to be correct, increase the values in Subroutine BLOCKDATA of either NUMAX1 or TOLTW1 or both.

3. DIFFUSER DATA INCORRECTLY WRITTEN ON DATA TAPE (Subroutine TAPE).
The diffuser-effectiveness data supplied as input through the library tape have been incorrectly specified. Check with the library-data input description.
4. EMPIRICAL FLAME-EMISSIVITY DATA INCORRECTLY WRITTEN ON DATA TAPE (Subroutine TAPE). See Message Number 3.
5. HOLE DISCHARGE COEFFICIENT DATA INCORRECTLY WRITTEN ON DATA TAPE (Subroutine TAPE). See Message Number 3.
6. IF THERE IS NO SNOUT, NXDIF MUST BE SPECIFIED (Subroutine INPUT).
NXDIF is a program input quantity.
7. INCREASE ITERATION CYCLE LIMIT * LCNIL * OR TOLERANCE * FID * (Subroutine AIRFLO, Air-Flow Subprogram). This message is always preceded by Message Number 8. LCNIL is specified in the program input and FID is set in Subroutine BLOCKDATA.
8. IN SUBROUTINE AIRFLO THE MAXIMUM NUMBER OF ITERATIONS ON THE AIR FLOW SPLIT WAS EXCEEDED (Subroutine AIRFLO, Air-Flow Subprogram).
This message is followed by either Message Number 7 or Message Number 31. The average of the fractions of the total air mass flow left at the end of the two annuli is not within the tolerance FID after the specified number of iterations, LCNIL.
9. ITERATION ON ALPHA AT STATION NO. (I), CYCLE NO. (LN) HAS NOT CONVERGED. THE LATEST VALUES OF ALPHA ARE (ALPHA(J), J=1, NTUBE) (Subroutine TUBANL, Diffuser Subprogram). The iteration to determine the streamtube slope at the axial Station I has failed to converge after LN cycles. The cycle number refers to the number

of streamtube-boundary-layer iterations which have been made. The solution is continued using the empirical-data method if the portion of the diffuser upstream of the snout is being treated; otherwise the solution is terminated. This difficulty is not expected to occur in reasonably shaped diffusers.

10. ITERATION LIMIT ON TOTAL PRESSURE LOSS DUE TO HEAT RELEASE EXCEEDED (Subroutine PRTEMP, Air-Flow Subprogram). In the iterative calculation of the total pressure at the end of the primary zone, the change in pressure between the last iteration (number NTOTP) and the preceding one was greater than the limit, PLIMIT. The two quantities NTOTP and PLIMIT are set in a data statement in Subroutine PRTEMP.
11. ITERATION ON AREA AT STATION NO.(I), CYCLE NO.(LN) HAS NOT CONVERGED. THE LATEST VALUES OF GUESSED AREA AND FLOW AREA ARE (SUMA, SUMB). (Subroutine TUBAML, Diffuser Subprogram). The iteration in the streamtube method to determine the static pressure at the axial station I, has failed to converge after LN cycles. The cycle number refers to the number of streamtube-boundary-layer iterations which have been made. The solution is continued using the empirical-data method if the portion of the diffuser upstream of the snout is being treated; otherwise the solution is terminated. This difficulty is not expected to occur in reasonably shaped diffusers.
12. IX HAS EXCEEDED ITS LIMIT IN HOLE ROW NO.(J) (Subroutine GEOM). In the Jth hole row position, more than 6 hole rows have been specified at the same axial location; this is not permitted.

This is a program input error.

13. K HAS EXCEEDED ITS LIMIT IN HOLE ROW NO.(J) (Subroutine GEOM).
In the Jth hole row position, the number of calculation points, K has exceeded the maximum permissible number, KMAX. The value of KMAX is set in a data statement in Subroutine GEOM.
14. MACH NUMBER GREATER THAN ONE. SOLUTION CONTINUED (Subroutine GASTBL, Diffuser Subprogram). The Mach number determined by a low value of static-to-total pressure ratio exceeds unity. The solution proceeds in this case, but the results are invalid if the final iteration on mass-flow split retains this difficulty. This is indicative of an error in the diffuser geometry specified as input, or an excessively large mass-flow rate specified as input.
15. MISMATCH AT THE SNOOT IS CHARACTERIZED BY THE RATIO (TOTAL STREAMTUBE AREA JUST BEFORE THE SNOOT)/(FLOW AREA JUST INSIDE THE SNOOT). THIS RATIO IS (AR). AS THIS RATIO IS (IN/OUT)SIDE THE RANGE 0.85-1.15 THE FLOW SPLIT ON THE SNOOT (IS/IS NOT) WELL MATCHED (Subroutine DOUTPT, Diffuser Subprogram). This message is self-explanatory.
16. NABX(1)=4 NOT ALLOWED (Subroutine GEOM). The first hole row specified in the program input must not be a dummy hole, that is, NHTU must not be zero.
17. NEGATIVE QUANTITY IN EXPRESSION FOR JET PENETRATION (Subroutine JETMIX, Air-Flow Subprogram). Following this message, the variables forming the expression for jet penetration are printed out; these are:

DENSJ (density of air in jet)

DENFT(K) (density of flame-tube gases at Calculation Station K)

UJ (initial jet velocity)

UFT(K) (velocity of flame-tube gases at calculation Station K)

X (axial distance downstream from jet origin)

DJA (longitudinal length of hole).

One of these quantities will be found to be negative, indicating the direction in which to search for the source of the error.

After encountering this error, the program moves to the next hole row and proceeds with the solution. The above message is not printed out if the air-flow-split iteration is in its first cycle or if a condensed printout has been requested (IPRINT=0).

18. NEGATIVE VALUE CALCULATED FOR MACH NUMBER. SOLUTION TERMINATED (Subroutine GASTBL, Diffuser Subprogram). An attempt has been made to calculate the Mach number from the usual compressible-flow relations with any of the following:

- a. A negative static-to-total pressure ratio
- b. A static-to-total pressure ratio in excess of unity
- c. A flow area smaller than the critical area

The third case is of most frequent occurrence, and is indicative of an error in the diffuser geometry supplied as input (resulting in a too small passage area), a specification of an excessively large mass-flow rate, or an intermediate value of the mass-flow split which is extreme.

19. `NC, NH, NWH, AND NSH MUST ALL BE SPECIFIED (Subroutine INPUT1).`
All of the above quantities are to be supplied in the program input. The appearance of this error message means that one or more of the quantities were omitted.
20. `PROGRAM STOPPED IN SUBROUTINE AIRFLO. LOOP COUNTER * LKANL * EXCEEDED. MAX CALL FOR * EQUAN * EXCEEDED (Subroutine AIRFLO, Air-Flow Subprogram).` The number of times Subroutine AIRFLO calls Subroutine EQUAN is counted. If this number exceeds the limit, LKANL, which is set in Subroutine BLOCKDATA, the program is returned to the Main Subprogram CLARE.
21. `PROGRAM STOPPED IN SUBROUTINE AIRFLO. LOOP COUNTER * LCFTL * EXCEEDED. MAX CALL FOR * EQUFT * EXCEEDED (Subroutine AIRFLO, Air-Flow Subprogram).` The number of times Subroutine AIRFLO calls Subroutine EQUFT is counted. If this number exceeds the limit, LCFTL, which is set in Subroutine BLOCKDATA, the program is returned to the Main Subroutine CLARE.
22. `PROGRAM STOPPED IN SUBROUTINE PRTEMP. ITERATION LIMIT * LCPTAL * EXCEEDED (Subroutine PRTEMP, Air-Flow Subprogram).` The number of iterations to determine the secondary-hole mass-flow split in Subroutine PRTEMP is counted. If this number exceeds the limit, LCPTAL, which is set in Subroutine BLOCKDATA, the iterations are stopped and the solution proceeds with the last calculated value of the secondary-hole flow split.
23. `PROGRAM STOPPED IN SUBROUTINE PRTEMP. ITERATION LIMIT * LCPRTL * EXCEEDED (Subroutine PRTEMP, Air-Flow Subprogram).` The number of iterations to determine the primary-zone temperature in Subroutine PRTEMP is counted. If this number exceeds the limit, LCPRTL, which

is set in Subroutine BLOCKDATA, the iterations are stopped and the solution proceeds with the last calculated value of primary-zone temperature.

24. SOLUTION FAILED TO CALCULATE STATIC PRESSURE AT COMPRESSOR EXIT (Subroutines EMPCTS and TUBEIN, Diffuser Subprogram). The iteration to determine the static pressure at the compressor exit from a specified mass-average total pressure and velocity profile failed to converge after 40 cycles. If the streamtube method is being used, it is replaced by the empirical-data method. The only time this is expected to occur is if the required solution is highly supersonic; hence this message indicates a mass-flow rate which is too large for the specified areas.
25. SOLUTION FAILED TO CALCULATE THEORETICAL FLOW AREAS FOR A GIVEN FLOW SPLIT. SOLUTION TERMINATED (Subroutine TUBFWI, Diffuser Subprogram). This only occurs if the mass flow to either of the two annuli, obtained from the air-flow subprogram, exceeds the total mass flow. This should never occur if the program input has been prepared properly.
26. SOLUTION FAILED TO CONVERGE AFTER 40 CYCLES. SOLUTION CONTINUED USING EMPIRICAL DATA. THE LAST CALCULATED BOUNDARY LAYER PARAMETERS ARE (Subroutine TUBCTS, Diffuser Subprogram). In using the streamtube method between the compressor exit and the snout, the iteration on the boundary-layer displacement thickness failed to converge. In general, this will only occur in a badly separated diffuser. The solution continues by employing the empirical-data

method in this portion of the diffuser; if the streamtube method is specified to be used in the subsequent portions of the diffuser, the empirical-data method is also used there.

27. SOLUTION FAILED TO CONVERGE IN SUBROUTINE TUBANL. SOLUTION CONTINUED USING EMPIRICAL DATA (Subroutine TUBCTS, Diffuser Subprogram). This message is always preceded by either Message Number 9 or 11. It is an indication that the streamtube method has failed to converge on either streamtube area or slope and that the empirical-data method is used in its place.
28. SOLUTION FAILED TO CONVERGE IN SUBROUTINE TUBANL. SOLUTION TERMINATED (Subroutine TUBSA1, Diffuser Subprogram). This message is always preceded by either Message Number 9 or 11. It is an indication that the streamtube method has failed to converge on either streamtube area or slope and that the solution is terminated.
29. SOLUTION FAILED TO CONVERGE IN SUBROUTINE TUBEIN. SOLUTION CONTINUED USING EMPIRICAL DATA (Subroutine TUBCTS, Diffuser Subprogram). This message is always preceded by either Message Number 24 or 31. It is indicative of a failure in the calculation in the streamtube method to determine the streamtube properties at the inlet to the first part of the diffuser. The solution is continued using the empirical-data method.
30. SOLUTION FAILED TO CONVERGE IN SUBROUTINE TUBEIN. SOLUTION TERMINATED (Subroutine TUBSA1, Diffuser Subprogram). This message is always preceded by either Message Number 24 or 31. It is indicative of a failure in the calculation in the streamtube method to determine the streamtube properties at the inlet to

the second half of the diffuser (after the snout). The solution is terminated.

31. SOLUTION FAILED TO FIND A CONVERGED VALUE OF U. PROBLEM TERMINATED. THE LAST TWO VALUES OF U WERE . . . (Subroutine TUBEIN, Diffuser Subprogram). The iteration in the streamtube method to determine the appropriate value of the normalization velocity U at the inlet to a diffusing passage has failed to converge after 40 cycles. The solution is continued with the empirical-data method if the first portion of the diffuser is being treated, while the solution is terminated if the portions of the diffuser downstream of the snout are being treated. The latter is the more likely occurrence, and is indicative of a mass-flow rate which is too high for the area of the passage.
32. TEMPERATURE IN * EQUFT * LESS THAN ZERO (Subroutine EQUFT, Air-Flow Subprogram). In the iterative solution for the flame-tube temperature, TFT2, in Subroutine EQUFT, a negative value has been calculated for TFT2. This will normally only appear in the first cycle of the air-flow-split iteration when the flow through the snout is close to zero. It is due to neglecting the enthalpy of the fuel in the flame-tube energy equation. When the program encounters this situation, TFT2 is given a value of 100 and the solution leaves the temperature iteration cycle; this value of TFT2 will, however, be reset in subsequent cycles in the air-flow-split iteration.

33. THE COMBUSTER IS BADLY DESIGNED--NEGATIVE PRESSURE DROP IS OCCURRING ACROSS THE HOLES. TO REMEDY:

1. IF ANNULUS VELOCITIES GREATER THAN 300 FPS, OPEN UP THE ANNULUS
2. INCREASE SIZE OF WALL HOLES
3. REDUCE DOME HOLE AREA
4. USE MORE SCOOPS OVER WALL HOLES

(Subroutine AIRFLO, Air-Flow Subprogram). This message is always preceded by Message Number 8. It indicates that the flow resistances through the annuli are too large compared with the flow resistance through the snout and flame tube such that an air-mass flow split cannot be found to satisfy the two conditions:

- a. Zero flow at the downstream end of the annuli
- b. Positive flow from the annuli into the flame tube at all hole rows.

The message itself indicates various methods for overcoming this problem.

34. THE STREAMTUBE ANALYSIS IN THE DIFFUSING PASSAGES BETWEEN SNOUT AND OUTER CASING HAS FAILED TO CONVERGE. SOLUTION TERMINATED. THE LAST CALCULATED BOUNDARY LAYER PARAMETERS ARE . . . (Subroutine TUBSA1, Diffuser Subprogram). This indicates that the iteration on boundary-layer displacement thickness has failed to converge after 40 cycles. It is expected to occur only in diffusers which are badly separated.

35. THE DIFFUSER TREATMENT USED IN THIS PROGRAM BECOMES INCREASINGLY INACCURATE AT INLET MACH NUMBERS GREATER THAN 0.7 (Subroutines TUBCTS and EMPCTS, Diffuser Subprogram). This is merely an

indication that the Mach number of the flow at the compressor exit is in excess of 0.7.

36. THE JET FROM HOLE ROW NO. (J) IS SPREADING TOO FAR. INCREASE EFC (Subroutine JETMIX, Air-Flow Subprogram). At each calculation station, the program compares the area of each jet with the cross-sectional area of the flame tube. If the total area of all jets from a particular hole row (J) occupies more than one quarter of the flame-tube area, the above message is printed out and the solution continues. It is suggested that the jet entrainment constant, EFC, be increased in such cases.
37. THE TWO-DIMENSIONAL-RADIATION OPTION CANNOT BE USED IN A COMBUSTOR OF RECTANGULAR CROSS SECTION. THE FLAME RADIATION WILL BE CALCULATED ONE-DimensionALLY (Subroutine INPUT2). The program input has been incorrectly specified; the solution proceeds using the one-dimensional-radiation option.
38. THE TWO-DIMENSIONAL-RADIATION OPTION CANNOT BE USED WITH TABULATED EMISSIVITY DATA. NLUM HAS BEEN SET EQUAL TO 4 (Subroutine INPUT2). The program input has been incorrectly specified, the solution proceeds using the NREC 1964 correlation for flame emissivity.
39. THERE ARE NO JET-ANGLE DATA FOR HOLE TYPE NO. (NHTU) THE INITIAL JET-ANGLE ESTIMATE USED IN THE PROGRAM IS NOT AT ALL ACCURATE FOR SCOOPS (Subroutine GEOM). This is an informative message printed out when noncontinuous scoops have been specified for which there are no jet-angle data.

40. THIS SECTION HAS AN AREA RATIO LESS THAN ONE AND ACTS AS A NOZZLE AND NOT AS A DIFFUSER. THE VALUE PRINTED OUT AS THE DIFFUSER EFFECTIVENESS IS NOT AN INDICATION OF HOW WELL THE SECTION PERFORMS (Subroutine DOUPT, Diffuser Subprogram). This indicates that the area at diffuser Station 2 occupied by the flow passing through either annulus is greater than the exit area of the respective diffuser passage. In this case, the empirical-data and streamtube-analysis methods yield essentially no losses due to diffusion, and the values of effectiveness obtained are generally not meaningful since the ideal pressure-recovery coefficients are negative.
41. WHEN SUBROUTINE JETMIX WAS CALLED, K WAS (K), LESS THAN NSHCP+1 (Subroutine JETMIX, Air-Flow Subprogram). JETMIX should not be called for calculation stations in the primary zone. This indicates an error in subroutine EQUFT, from which JETMIX is called.
42. X(I) WAS FOUND TO BE LESS THAN X(I-1) (X(I)) INCHES ALONG THE COMBUSTOR. THIS IS NOT ALLOWED (Subroutine INPUT1). The program input quantity XINCH must increase monotonically with no two values equal.

APPENDIX VI
FORTRAN NOMENCLATURE

This appendix gives the Fortran nomenclature for program CLARE and its subroutines. Only the variables contained in COMMON blocks are included; the others are mainly dummy variables which appear exclusively in a particular subroutine. (The COMMON block BZERO also contains only dummy variables which are not listed here).

In many parts of the program, different quantities apply to the inner (closest to shaft) and outer walls of the combustor; these have generally been given names which are identical except that A is used for the inner wall, B for the outer wall. To avoid extensive duplication of these names, the following shorthand notation has been adopted. When A in a name is underlined, there exists a corresponding quantity with A replaced by B and with "inner" in the definition replaced by "outer". For example,

CA Diameter of inner wall

indicates that there is, in addition to CA, a quantity:

CB Diameter of outer wall.

Variables having names beginning with the letters I, J, K, L, M, and N are integers. All other variables are real.

Units

In some cases, the units used in the program differ from those used for input and output. For example, lengths and diameters are given in inches on input and output, whereas feet units are consistently used in the program. In such cases, the units given in this list are those

used in the program.

Subscripts

In this list, the subscripts I, J, and K are used with variables that are defined at each geometric input point, each hole row, and each calculation point respectively. I runs from 1 to NG, J from 1 to NH, and K from 1 to NLAST. The subscripts L and N are used with other variables, as defined below.

<u>Fortran Name</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
A		Enthalpy flow rate with jet from secondary holes on inner wall	lbm ft ² per sec ³
AAN1	$A_{an,1}$	Cross-sectional area of annulus at previous calculation point	sq ft
AAN2	$A_{an,2}$	Cross-sectional area of annulus at current calculation point	sq ft
AANA(K)	A_{an}	Cross-sectional area of inner annulus	sq ft
ABLOCK		Fraction of boundary-layer blockage at inlet that is on the inner wall	-
ABSW	α_w	Absorptivity of flame-tube wall	-
AF(L)		Air mass flow rate in diffuser annulus. L=1 for inner, 2 for outer	lbm per sec
AF2	\dot{m}	Air mass flow rate at combustor inlet	lbm per sec
AF23A(L)		Fraction of inlet air that is bled from the annulus for turbine cooling or other auxiliary purposes	-
AFA	\dot{m}_{an}	Air mass flow rate in inner annulus used in the diffuser calculation	lbm per sec
AFAN1	$\dot{m}_{an,1}$	Air mass flow rate in annulus at previous calculation point	lbm per sec

<u>Fortran Name</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
AFAN2	$\dot{m}_{an,2}$	Air mass flow rate in annulus at current calculation point	lbm per sec
AFANA(K)	\dot{m}_{an}	Air mass flow rate in inner annulus	lbm per sec
AFCL		Lower bound on ratio of flow through inner annulus to flow through both annuli	-
AFCU		Upper bound on ratio of flow through inner annulus to flow through both annuli	-
AFFT(K)	\dot{m}_{ft}	Gas mass flow rate inside flame tube	lbm per sec
AFFT1	$\dot{m}_{ft,1}$	Gas mass flow rate in flame tube at previous calculation point	lbm per sec
AFFTT1		Gas mass flow rate in flame tube at next calculation point	lbm per sec
AFFT2	$\dot{m}_{ft,2}$	Gas mass flow rate in flame tube at current calculation point	lbm per sec
AFJ(J), AFJI(J)	\dot{m}_h	Initial mass flow in jets in Jth hole row	lbm per sec
AFJA(K)		Mass flow through previous cooling slot in inner wall	lbm per sec
AFJZ(J)		Fraction of annulus air flowing through Jth hole row	-
AFPRZ	\dot{m}_p	Total mass flow in primary zone	lbm per sec
AFSL		Lower bound on flow through snout	lbm per sec
AFSU		Upper bound on flow through snout	lbm per sec
AFSYIA		Air mass flow rate into intermediate zone, from secondary holes in inner annulus	lbm per sec
AFSYP	$\dot{m}_{sy,p}$	Mass flow rate through secondary holes into primary zone	lbm per sec
AFSYPA		Air mass flow rate into primary zone, from secondary holes in inner annulus	lbm per sec

<u>Fortran</u> <u>Name</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
AFT(K)	A_{ft}	Cross-section area of flame tube	sq ft
AFT1	$A_{ft,1}$	Cross-section area of flame tube at previous calculation point	sq ft
AFT2	$A_{ft,2}$	Cross-section area of flame tube at current calculation point	sq ft
AHDOME	$A_{hT,dome}$	Total hole area in the dome	sq ft
AL(L,N,I)		Difference in angle between mean angle of diffusing passage and angle of passage wall. L=1 for inner passage, 2 for outer; N=1 for inner wall, 2 for outer	radians
ALFA(L,I)		Mean angle of diffuser annulus between stations 2' and 4. L=1 for inner, 2 for outer	radians
ALFC(I), ALFD(I)		Angle of inner, outer casing at the diffuser snout	radians
ALPHA1, ALPA		Angle of inner casing	radians
ALPHA2, ALPB		Angle of inner wall of snout	radians
ALPHA3, ALPC		Angle of outer wall of snout	radians
ALPHA4, ALPD		Angle of outer casing	radians
AR(I,N)		Flow area at diffuser station I for annulus N	sq ft
ARF(L,I)		Area of diffusing passage normal to flow direction, allowing for boundary-layer displacement thickness. L=1 for inner passage, 2 for outer	sq ft
ARDTA(L) AR		Area ratio for point L in table of empirical diffuser data	-
ARR(L,I)		Area of diffusing passage normal to flow direction. L=1 for inner passage, 2 for outer	sq ft

<u>Fortran</u> <u>Name</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
ARTAB(L)	AR	Area ratio for point L in table of empirical diffuser data for an alternative set of data	-
AREA(I)		Diffuser cross-section area	sq ft
AREA1		Diffuser cross-section area at entry	sq ft
AREF	A_{ref}	Combustor reference cross-section area	sq ft
ASTAR (N)		Critical flow area for stream-tube N	sq ft
ASW	A_{sw}	Swirler area (ignoring blockage due to blades)	sq ft
B		Axial momentum of jet from secondary hole on inner wall	ft lbm per sec ²
BETA	β	Swirler blade stagger angle	radians
BETA1	β	Profile parameter at inlet to inner annulus	-
BETA2	β	Profile parameter at inlet to outer annulus	-
BLOCK(I)		Boundary-layer blockage in the diffuser	-
C(J)	C_d	Discharge coefficient in Jth hole row	-
C1A(K)	C_1	Rate of heat transfer by convection from flame (or cooling film) to inner wall	Btu per sq ft sec
C2A(K)	C_2	Heat transfer rate from wall to air in inner annulus by convection	Btu per sq ft sec
CA(I)		Inner casing diameter	ft

<u>Fortran</u> <u>Name</u>	<u>Symbol</u>	<u>Description</u>	<u>Unit</u>
CAL(I)		Effective radius of inner diffuser wall between stations 1 and 2, accounting for boundary-layer displacement thickness	ft
CCA(K)		Inner casing circumference	ft
CD	C_d	Discharge coefficient uncorrected for velocity	-
CDC(L,N)	C_d^1	Discharge coefficient corrected for velocity	-
CDS(L,N), DUMCD(N)		Discharge coefficient, library value	-
CFTA(K)		Circumference of flame-tube inner wall	ft
CONDFT	K_w	Thermal conductivity of flame-tube wall material	Btu per ft hr deg F
D		Mass flow in jets from secondary hole on inner wall	lbm per sec
D1A(K)		Coefficient of T_w^4 in heat-balance equation on inner wall	deg R ⁻⁴
D2A(K)		Coefficient of $T_w^{2.5}$ in heat-balance equation on inner wall	deg R ^{-2.5}
D3A(K)		Coefficient of T_w in heat-balance equation on inner wall	deg R ⁻¹
D4A(K)		Constant in heat-balance equation on inner wall	
DANA(K)	D_{an}^1	Hydraulic diameter of inner annulus	ft
DELT(L,1)		Boundary-layer displacement thickness at the diffuser wall. L=1 for inner passage, 2 for outer; l=1 for inner wall, 2 for outer	ft
DELTA(L,1)	δ	Displacement thickness at point l. L=1 for inner wall, 2 for outer wall	ft
DENANI	$\rho_{an,1}$	Air density in annulus at previous calculation point	lbm per ft ³

<u>Fortran</u> <u>Name</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
DENAN2	$\rho_{an,2}$	Air density in annulus at current calculation point	lbm per ft ³
DENANA(K)	ρ_{an}	Air density in inner annulus	lbm per ft ³
DENFT(K)	ρ_{ft}	Gas density in flame tube	lbm per ft ³
DENFTi	$\rho_{ft,1}$	Gas density in flame tube at previous calculation point	lbm per ft ³
DENFT2	$\rho_{ft,2}$	Gas density in flame tube at current calculation point	lbm per ft ³
DFFT(J)		Accumulated fraction of inlet air in flame tube after J th hole row	-
DFT(K)	D_{ft}^1	Hydraulic diameter of flame tube	ft
DOMLOS		Number of velocity heads (based on velocity at snout entrance) lost between snout entry and dome if the diffuser has a snout. If the diffuser has no snout DOMLOS = no. of velocity heads lost at calculation point NXDIF due to mixing on the dome	-
DPH(J)	$1 + \frac{\Delta p_h}{q_{an}}$	Pressure-loss factor for Jth hole row	-
DPHI	$1 + \frac{\Delta p_h}{q_{an}}$	Current value of pressure-loss value	-
DPHS(L,N), DUMPH(N)	$1 + \frac{\Delta p_h}{q_{an}}$	Library value of pressure-loss value	-
DPHSNT		Dynamic pressure at snout inlet	lbf per sq ft
DPREF	q_{ref}	Reference dynamic pressure	lbf per sq ft
DSWLIN		Inside diameter of swirler	in
DSWLOU		Outside diameter of swirler	in
DUMAE(K)		Accumulated pressure loss in inner annulus due to expansion	lbf per sq ft

<u>Fortran</u> <u>Name</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
DXHU(J)		Hole radius (for noncircular holes, half the axial length)	ft
DYD		Square of mean velocity into inner annulus from first part of diffuser (Station 2)	ft ² per sec ²
D9(N)		Fractional distance across velocity profile at diffuser Station 2, allowing for blockage	-
E		Momentum of jets from secondary holes on inner wall	ft lbm per sec ²
EIDTA	E_1	(1 - boundary-layer blockage) at inlet for table of empirical diffuser data	-
EIDTAB	E_1	(1 - boundary-layer blockage) at inlet for an alternative table of empirical diffuser data	-
EE1(L)		Parameter used in calculating boundary-layer blockage at entrance to second stage of diffusion (Station 2)	-
EFC(1)		Constant used to denote rate of mixing of penetration jets	-
EFC(2)		Constant used to denote rate of mixing of wall jets	-
EFCL(N)	$\frac{u_{j,} - u_{ft}}{u_{j,0} - u_{ft}}$	Local velocity ratio in residual-jet velocity profile	-
EFDT(L)	ξ	Diffuser effectiveness. L = 1 for diffuser inlet to station NXDIF L = 2,3 for two annular passages	-
EFDTA(L)	ξ	Effectiveness for point L in table of empirical diffuser data	-
EFDTAB(L)	ξ	Effectiveness for point L in an alternative table of empirical diffuser data	-

<u>ortran</u> <u>Name</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
EK16	M_{jo}	Total axial jet momentum flow rate of entering jets.	ft lbm per sec ²
EK17	A_{jo}	Total cross-sectional area of entering jets	sq ft
EK19	\dot{m}_{jo}	Total air mass-flow rate of entering jets	lbm per sec
EK20		Total jet enthalpy flow rate of entering jets.	lbm ft ² per sec ³
EMC	ϵ_c	Emissivity of casing	-
EMFT(K)	ϵ_{ft}	Flame emissivity	-
EMW	ϵ_w	Emissivity of flame tube wall	-
ENTHAL		Ratio of mean specific heat at TFT2 to that at TFT1	-
F(i)		Ratio of inner or outer annulus area to total combustor area at diffuser Station 2'	-
FAR		Fuel-air ratio	-
FARFT(K)		Fuel-air ratio in flame tube	-
FARFT1		Fuel-air ratio in flame tube at previous calculation point	-
FARFT2		Fuel-air ratio in flame tube at current calculation point	-
FARL		Fuel air ratio left at the current calculation point	-
FFB(J)		Cumulative fraction of fuel burned up to Jth hole row	-
FFIZ(K)		Mass of fuel available for burning in flame tube between previous calculation point and current one	lbm
FHCR		Fuel hydrogen-carbon ratio	-
FIA		Constant used in deriving new mass flow split	-

<u>Fortran</u> <u>Name</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
FID		Maximum value of \dot{m}_A^{**} in air mass flow iteration cycle	lbm per sec
FIENTH		Maximum allowable change in temperature in solution of flame-tube equations	deg F
FIFTPR		Maximum allowable error in enthalpy equation to determine primary zone temperature	-
FILMFA(K)	τ	Film-cooling effectiveness	-
FINT(K)		Flame intensity at calculation point K	Btu per sq ft sec
FIPHI		Tolerance on velocity in solving flame-tube equations, expressed as a fraction	-
FIT		Velocity percentage accuracy required in solution of annulus equations	-
FITAU		Constant used in deriving new mass-flow split	-
FLAREA(I)		Flow area in diffuser	sq ft
FLCV		Fuel lower calorific value	Btu per lbm
FMOC02(K)		Mole fraction of carbon dioxide in burning gas	-
FMOH20(K)		Mole fraction of water vapor in burning gas	-
FRICFA(K)	f	Friction factor (Fanning) in annulus	-
FTA(!)		Diameter of inner flame-tube wall	ft
GASC	R	Gas constant for air	ft lbf per lbm deg R
GJCOLE	J	Mechanical equivalent of heat	ft lbf per Bt
GRAVC	g_0	Gravitational constant	ft lbm per lbf sec ²
GX1A	ξ	Jet angle for secondary-hole jets on inner annulus	radians

<u>Fortran</u> <u>Name</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
GXI	ξ	Initial jet angle	radians
GXIA(J)	ξ	Jet angle in Jth hole row	radians
GXIS(L,N)	ξ	Initial jet angle, library value	radians
HAB(J)		Input value of hole area	sq ft
HAU(J)	A_h	Cross sectional area of each hole in Jth row	sq ft
HAW(J)		Effective total area of Jth hole row	
HRRATE		Effective lower calorific value of fuel times the fuel air ratio	Btu per lbm
IBL		Index. 1 When diffuser calculation has converged 0 Otherwise	-
IDIF		Index. 0 For empirical data from generalized tabulation 1 For empirical data from table for particular geometry	-
IH		Number of hole type on short list	-
IHJ(J)		Hole type number on short list for the Jth hole row	-
INPUT		Index. 0 If input flow conditions varied between cases 1 If program routing varied between cases	-
IPRINT		Index. 1 If intermediate results are to be printed 0 Otherwise	-
ITAPE		Number of computer input device	-
JKSN(J)		Number of calculation point corresponding to Jth hole row	-

<u>Fortran Name</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
JTAPE		Number of computer output device	-
K		index denoting calculation point	-
K1		Index. 0 For inner annulus 1 For outer annulus	-
K4		Index. 0 For secondary-hole flow split not specified 1 For secondary-hole flow split specified	-
K6		Index. 0 For no swirler 1 For swirler specified 2 For swirler unspecified	-
K30, K40, K50, K60		Integers used in subroutine DISJET to fix pressure reversal or negative air mass flow in the annuli for the whole combustor	-
KANHET		Number of times the heat transfer subprogram has been entered	-
KJSN(K, L)		Hole row number of Lth hole row at calculation point no. K	-
KTAPE		Number of computer input device used for library data	-
LANHET		Index. 0 If heat transfer to annulus air is neglected 1 If heat transfer to annulus air is to be con- sidered 2 If no heat transfer cal- culation is to be done	-
LCAN		Loop counter in AIRFLO; check on number of times EQUAN is called	-
LCANL		Loop counter limit in AIRFLO; check on number of times EQUAN is called	-

<u>Fortran</u> <u>Name</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
LCANI		Loop counter in AIRFLO; iteration on mass-flow split	-
LCANIL		Loop counter limit in AIRFLO; iteration on mass-flow split	-
LCFT		Loop counter in AIRFLO; check on number of times EQUFT is called	-
LCFTE		Loop counter in EQUFT; iteration on flame-tube temperature	-
LCFTEL		Loop counter limit in EQUFT; iteration on flame-tube temp- erature	-
LCFTL		Loop counter limit in AIRFLO; check on number of times EQUFT is called	-
LCMF		Loop counter in EQUAN; iteration on annulus velocity	-
LCMFL		Loop counter limit in EQUAN, iteration on annulus velocity	-
LCPRT		Loop counter in PRTEMP; iteration on primary-zone temperature	-
LCPRTL		Loop counter limit in PRTEMP, iteration on primary-zone temperature	-
LCPTA		Loop counter in PRTEMP; iteration on secondary-hole-mass-flow split	-
LCPTAL		Loop counter limit in PRTEMP; iteration on secondary-hole-mass flow-split	-
M		Number of current case	-
NAB(J)		Index indicating hole position; 1. For inner wall 2. For outer wall	-

<u>Fortran</u> <u>Name</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
NABX(K)		Index. 1 For hole on inner wall 2 For hole on outer wall 3 For holes on both walls 4 For no holes on either wall	-
NBLADE		Number of swirler blades	-
NCASE		Number of cases to be considered NCASE = 0 if only a check on the input data is required, and none of the major subroutines are to be entered	-
NCDF		Index indicating form of empirical diffuser data and degree of interpolation used. See page 30 for details (NCDF = NCDIFA)	-
NCDFB		Index indicating form of empirical diffuser data and degree of interpolation used for an alternative set of data	-
NCODEA(K)		Index. 1 If there is a cooling slot on inner wall at this calculating point 0 Otherwise	-
NCOOL		Index. 1 For film cooling 2 For transpiration cooling	-
NDIFF		Index indicating route through diffuser subprogram. Tens position indicates calculation method in first part of diffuser (Stations 1-2), units position indicates method for second part (Stations 2-4). Can take values 11, 12, 13, 22, 23. See page 40 for details	-
NEF		Index indicating entrainment correlation-to be used. 1 For mass-loss method 2 For equivalent-entrainment method 3 For profile-substitution method 4 For instantaneous mixing	-

<u>Fortran</u> <u>Name</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
NDIS(J)		Index indicating state of residual jets from Jth hole row. 0 If jets have not disappeared 1 If jets have disappeared	
NEFT		Number of emissivity values in table of empirical flame-emissivity data	-
NG		Number of geometric input points	-
NGO		Index. 1 For streamtube method 2 For empirical-data method	-
NH		Number of hole rows	-
NHH(J)		Number of holes in hole row J	-
NHT1		Index indicating route through basic heat-transfer calculation. 1 For uncooled wall, 1-dimensional radiation 2 For cooled wall, 1-dimensional radiation 3 For uncooled wall, 2-dimensional radiation 4 For cooled wall, 2-dimensional radiation	-
NHT2		Index indicating the corrections applied to the basic heat-transfer calculation 2 For longitudinal conduction 3 For radiation interchange between walls 4 For longitudinal conduction and radiation interchange 1 No corrections used	-
NHTU		Hole type used in Jth hole row	-
NLAST		Number of calculation points	-
NLUM		Index indicating correlation to be used for flame emissivity. 1 For Reeves correlation for distillate fuels 2 For Reeves correlation for residual fuels 3 For Lefebvre correlation	-

<u>Fortran</u> <u>Name</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
		4 For NREC 1964 Correlation 5 For NREC 1966 correlation 6 For emissivity from table of experimental data	
NPFT		Number of values of pressure in table of empirical flame- emissivity data	-
NRECT		Index. 1 For annular combustor 2 for rectangular com- bustor	-
NSCOOP(L)		Index. 1 In units position for non-continuous scoop 2 In units position for continuous film-cooling slot 0 In units position other- wise 1 in tens position if jet- angle data not available	-
NSH		Hole-row number corresponding to secondary holes	-
NSHCP		Number of calculation point corresponding to secondary holes	-
NSNOUT		Index. 1 If there is a snout 0 Otherwise	-
NSP(L)		Number of points at which dis- charge-coefficient data given for Lth hole type on short list	
NTUBE		Number of streamtubes in diffuser theoretical calculation	-
NUMAX1		Permissible number of iterations in solving heat-balance equation for noniterative heat-transfer calculation	
NUMAX2		Permissible number of iterations in solving heat balance equation for iterative heat transfer	
NUMSW		Number of swirlers	
NUMPR		Number of points across velocity profile in diffuser inlet plane	-

<u>Fortran</u> <u>Name</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
NWALL1		Index indicating set of empirical data to be used in first part of diffuser (Stations 1-2)	-
NWALL2		Index indicating set of empirical data to be used in second part of diffuser (Stations 2-4)	-
NWAY		Index. 1 For streamtube method 2 For empirical-data method 3 For mixing-equation method	-
NWH		Number of first hole row on flame-tube wall, as distinct from dome	-
NXDIF		Number of geometric-input point corresponding to diffuser Station 2 (just before snout)	-
NXDIF1		Number of geometric-input point corresponding to diffuser Station 3 in inner annulus	-
NXDIF2		Number of geometric-input point corresponding to diffuser Station 3 in outer annulus	-
NXDIFA,NXD(1)		Number of geometric-input point corresponding to diffuser Station 4 in inner annulus	-
NXDIFC		Number of area-ratio points in table of empirical diffuser data for an alternative set of data	-
NYDF		Number of effectiveness points in table of empirical diffuser data	-
NYDIFB		Number of effectiveness points in table of empirical diffuser data for an alternative set of data	-
NZDF		Number of nondimensional-length points in table of empirical diffuser data	-

<u>Fortran</u> <u>Name</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
NZDIFB		Number of nondimensional-length points in table of empirical diffuser data for an alternative set of data	-
PAN1A		Static pressure in inner annulus at diffuser exit (Station 4)	lbf per sq ft
PERCO	$1/\alpha$	Permeability coefficient of porous wall	sq ft
PI	π	3.14159	-
PI4	$\pi/4$	3.14159/4	-
PLOSS(I)		Total-pressure loss in the diffuser due to expansion or contraction at the snout	lbf per sq ft
PRAAN(K)	Pr	Prandtl number in inner annulus	-
PREAN1	$p_{an,1}$	Static pressure at previous calculation point in annulus	lbf per sq ft
PREAN2	$p_{an,2}$	Static pressure at current calculation point in annulus	lbf per sq ft
PREANA(K)	p_{an}	Static pressure in inner annulus	lbf per sq ft
PREDM	p_{dome}	Static pressure on dome	lbf per sq ft
PREFT(K)	p_{ft}	Static pressure in flame tube	lbf per sq ft
PREFT1	$p_{ft,1}$	Static pressure at previous calculation point in the flame tube	lbf per sq ft
PREFT2	$p_{ft,2}$	Static pressure at current calculation point in the flame tube	lbf per sq ft
PRES(I)		Diffuser static pressure at point I	lbf per sq ft
PRESIN	p_2	Static pressure at inlet	lbf per sq ft
PRFT(K)	Pr	Prandtl number in flame tube	-
QTRA(X)		Rate of enthalpy added to flame-tube gas due to transpiration cooling through inner annulus wall	Btu per ft ² sec

<u>Fortran Name</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
R		Distance across annulus, normal to mean flow direction, at diffuser Station 2'	Btu per sq ft sec
RIA(K)	R_1	Rate of heat transfer by radiation from flame to inner wall	Btu per sq ft sec
R2A(K)	R_2	Rate of heat transfer by radiation from flame tube wall to inner casing	Btu per sq ft sec
R3A(K)	R_3	Net rate of heat received by inner wall due to radiation interchange with opposite wall	Btu per sq ft sec
RAD(L)		Mid-point coordinate of stream-tube	-
RC(J)		Ratio of corrected to actual discharge coefficient in Jth hole row	-
RDATA(L)		Nondimensional distance across diffuser inlet plane at point L	-
REAN(K)	Re	Reynolds number in the inner annulus	-
REFT(K)	Re	Reynolds number in the flame	-
RHOREF	ρ_2	Density at diffuser inlet	lbm per ft ³
RO(L,N)		Density in streamtube adjacent to station N in diffuser. L=1 for inner wall, 2 for outer	lbm per ft ³
SA(I)		Inner snout diameter	ft
SAFTRA(K)		Air mass flow rate transpiring through the inner annulus walls between current calculation point and the previous one	lbm per sq ft sec
SHAFST		Fraction of air flowing through secondary holes that recirculates upstream	-
SHAPEH(L,I) H		Shape factor on wall. L=1 for inner wall, 2 for outer wall	-
SHP(L)		Shape factor of boundary layer on wall at diffuser inlet. L=1 for inner wall, 2 for outer	-

<u>Fortran</u> <u>Name</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
STAGP(N)		Stagnation pressure of Nth streamtube in diffuser	lbf per ft ²
STAGT	T ₂	Total temperature of air at compressor outlet	deg R
STEP		Step size used in jet mixing calculations	ft
STPREF	P ₂	Mass-averaged total pressure at compressor outlet	lbf per sq ft
TABEFT(L)	E _{ft}	Table of experimental flame emissivities	-
TABPFT(L)	p _{ft}	Gas pressure in table of experimental flame emissivities	lbf per sq ft
TABTFT(L)	T _{ft}	Gas temperature in table of experimental flame emissivities	deg R
TANI	T _{an,1}	Static temperature of annulus air at previous calculation point	deg R
TANIA		Static temperature in inner annulus at diffuser exit (Station 4)	deg R
TAN2	T _{an,2}	Static temperature of annulus air at current calculation point	deg R
TANANA(K)	T _{an}	Static temperature of air in inner annulus	deg R
TCASA(K)	T _c	Temperature of inner casing	deg R
TCATA(K)	T _c	Temperature of inner casing	deg F
TCFA(K)		Temperature of air entering previous cooling slot on inner wall	deg R
TFT(K)	T _{ft}	Total temperature of gas in flame tube	deg R
TFT1	T _{ft,1}	Total temperature of gas in flame tube at previous calculation point	deg R
TFT2	T _{ft,2}	Total temperature of gas in flame tube at current calculation point	deg R

<u>Fortran Name</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
THA		Theoretical inlet area for inner annulus	sq ft
THET(L)		Momentum thickness on diffuser wall L=1 for inner wall, 2 for outer	ft
THETT(L,I)		Momentum thickness of the boundary layer in the plane of the snout. L=1 for inner passage, 2 for outer; I=1 for inner wall, 2 for outer.	ft
THIKFT	t_w	Flame-tube wall thickness	ft
THS		Theoretical inlet area for snout	sq ft
TNUAAN(K)	Nu	Nusselt number in inner annulus	-
TNUFT(K)	Nu	Nusselt number in flame tube	-
TOLTW1		Accuracy to which solution of noniterative heat balance required	deg F
TOLTW2		Accuracy to which solution of iterative heat balance required	deg F
TWA(K)	T_w	Flame-tube wall temperature	deg R
TWADA(K)	T_{ad}	Adiabatic-wall temperature on inner wall	deg R
TZ		Zero Fahrenheit expressed in deg R	deg R
UAN1	$U_{an,1}$	Velocity of air in annulus at previous calculation point	ft per sec
UAN2	$U_{an,2}$	Velocity of air in annulus at current calculation point	ft per sec
UANA(K)	U_{an}	Velocity of air in inner annulus	ft per sec
UFT(K)	U_{ft}	Velocity of gas in the flame tube	ft per sec
UFT1	$U_{ft,1}$	Velocity of gas at previous calculation point	ft per sec

<u>Fortran Name</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
UFT2	$U_{ft,2}$	Velocity of gas at current calculation point	ft per sec
UFTA(K)		Velocity of gas in flame tube at previous cooling slot on inner wall	ft per sec
UH	u_j	Initial jet velocity	ft per sec
UJ(L)		Velocity of Lth streamtube	ft per sec
UJCL(J)	u_j	Centerline velocity of residual jet from Jth hole row	ft per sec
UJETA(N)	u_j	Local velocity at station N in residual-jet transverse velocity profile	ft per sec
UJY(N)		Local velocity at station 2 of diffuser	ft per sec
UJIA(K)		Velocity of air entering previous cooling slot on inner wall	ft per sec
VEL(L,N)		Velocity in streamtube adjacent to diffuser wall at station N. L=1 for inner wall, 2 for outer	ft per sec
VELJ(L)		Velocity in streamtube adjacent to diffuser wall at inlet. L=1 for inner wall, 2 for outer	ft per sec
VPDATA(L)		Nondimensional velocity at point L across diffuser inlet profile	-
WCD(J)	C_d	Discharge coefficients of holes in Jth row	-
WFFIZ(K)		Rate of fuel burning as a function of axial length	lbm per sec per ft
WI(1,1), WI(2,1)		Diameter of inner casing, outer snout	ft
WIDTH1		Width of rectangular combustor	ft
WIL(1,1), WIL(2,1)		Diameter of inner casing, outer snout, allowing for boundary-layer displacement thickness	ft

<u>Fortran</u> <u>Name</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
WO(1,1), WO(2,1)		Diameter of inner snout, outer casing	ft
WOL(1,1), WOL(2,1)		Diameter of inner snout, outer casing allowing for boundary-layer displacement thickness	ft
WUJ(J)	u_j	Initial jet velocity for Jth hole row	ft per sec
X(I)		Axial location of geometric input point	ft
XIFCA(K)		Axial distance from previous cooling slot on inner wall	ft
XAF23A(L)		Axial location at which cooling is bled from annulus	ft
XCP(K)		Axial location of Kth calculation point	ft
XFILMZ	x_o	Constant in film-cooling correlation	-
XFSA		Fraction of secondary air flowing downstream from secondary holes in the inner annulus	-
XH(J)		Axial location of centerline of Jth hole row	ft
XHU(J)		Axial location of upstream edge of Jth hole row	ft
XINT		Interval downstream of cooling slots at which calculation points required	ft
XLNDA(L)		Nondimensional length for point L in table of empirical diffuser data	-
XLNDB(L)		Nondimensional length of point L in table of empirical diffuser data for an alternate set of data	-
XMACH	M_2	Mach number at diffuser inlet	-
XMTB(J)		Mass flow in streamtube J	lbm per sec

<u>Fortran</u> <u>Name</u>	<u>Symbol</u>	<u>Description</u>	<u>Units</u>
XMVA		Mean velocity into inner annulus from first part of diffuser (Station 2)	ft per sec
XMVS		Mean velocity into snout from first part of diffuser (Station 2)	ft per sec
YCFA(K)	Y_{cf}	Height of previous cooling slot on inner wall	ft
Y(N)		Fractional distance across velocity profile at diffuser station 2, allowing for blockage	-
YY		Fractional distance across annulus at diffuser station 2	-
ZAJH(K)		Summation of axial jet momentum for hole rows at current calculation point	lbm ft per sec ²
ZMH(K)	$\sum \dot{m}_j$	Summation of jet air mass flow for hole rows at current calculation point	lbm per sec
ZMHA(L)	\dot{m}_{sy}	Mass flow through secondary holes. L=1 for inner annulus, 2 for outer annulus	lbm per sec
ZHJJ(K)		Summation of jet momentum for hole rows at current calculation point	lbm ft per sec
ZMJET(K)		Summation of flow rates of enthalpy with jets for hole rows at current calculation point	ft ² lbm per sec ³
ZSTOC		Stoichiometric fuel air ratio	-
ZZCP	C_p	Specific heat	Btu per lbm deg F
ZZGAMA	γ	Ratio of specific heat	-
ZZR	R	Gas constant	ft lbf per lbm deg R

APPENDIX VII

LISTING OF LIBRARY DATA

2.	.345	50.	4.	.513	63.	DATA0061
8.	.588	72.	16.	.617	78.	DATA0062
32.	.625.	80.				DATA0063
17.206	.0849	0	71.	0.	0.	DATA0064
2.	.48	53.	4.	.535	63.	DATA0065
8.	.585	69.	16.	.62	74.	DATA0066
32.	.645	76.	64.	.655	78.	DATA0067
18.218	.0848	0	71.	0.	0.	DATA0068
2.	.4	52.	4.	.51	61.	DATA0069
8.	.585	68.	16.	.625	72.	DATA0070
32.	.645	75.	64.	.65	77.	DATA0071
19.2955	.1743	0	71.	0.	0.	DATA0072
2.	.316	48.	4.	.48	58.	DATA0073
8.	.565	66.	16.	.61	71.	DATA0074
32.	.62	75.	64.	.627	78.	DATA0075
20.312	.1738	0	71.	0.	0.	DATA0076
2.	.325	51.	4.	.51	60.	DATA0077
8.	.585	66.	16.	.615	71.	DATA0078
32.	.63	75.	64.	.64	78.	DATA0079
21.5	.5743	0	71.	0.	0.	DATA0080
2.	.377	48.	4.	.52	62.	DATA0081
8.	.587	71.	16.	.617.	77.	DATA0082
32.	.626	81.	64.	.63	84.	DATA0083
22.5	.5	10	71.	0.		DATA0084
2.	.38		4.	.508		DATA0085
8.	.561		16.	.584		DATA0086
32.	.594		64.	.6		DATA0087
23.531	.5035	0	71.	0.	0.	DATA0088
2.	.385	49.	4.	.503	62.	DATA0089
8.	.552	72.	16.	.575	78.	DATA0090
32.	.58	81.	64.	.585	83.	DATA0091
24.62	.7688	0	51.	0.	0.	DATA0092
2.	.39	47.	4.	.504	64.	DATA0093
8.	.564	73.	16.	.59	79.	DATA0094
25.656	.7685	0	61.	0.	0.	DATA0095
2.	.412	51.	4.	.537	66.	DATA0096
8.	.575	74.	16.	.595	79.	DATA0097
32.	.595	81.				DATA0098
261.	2.688	0	51.	0.	0.	DATA0099
2.	.44	56.	4.	.538	70.	DATA0100
8.	.567	76.	16.	.575	77.	DATA0101
271.	2.	10	71.	0.		DATA0102
2.	.388		4.	.511		DATA0103
8.	.563		16.	.587		DATA0104
32.	.596		64.	.6		DATA0105
281.067	2.0139	0	41.	0.	0.	DATA0106
2.	.44	57.	4.	.55	70.	DATA0107
8.	.59	76.				DATA0108
29.71	.5041	0	61.	0.	0.	DATA0109
2.	.413	42.	4.	.525	60.	DATA0110
8.	.585	71.	16.	.611	78.	DATA0111
32.	.62	83.				DATA0112
30.7485	.53128	0	61.	0.	0.	DATA0113
2.	.45	49.	4.	.565	64.	DATA0114
8.	.62	73.	16.	.645	80.	DATA0115
32.	.65	84.				DATA0116
312.	2.	10	71.	0.		DATA0117
2.	.425		4.	.537		DATA0118
8.	.576		16.	.592		DATA0119
32.	.597		64.	.6		DATA0120

321.	.5041	0	61.	0.	0.	DATA0121
2.	.458	46.	4.	.565	66.	DATA0122
8.	.605	74.	16.	.62	79.	DATA0123
32.	.63	82.				DATA0124
331.05	.9534	0	61.	0.	0.	DATA0125
2.	.435	55.	4.	.56	63.	DATA0126
8.	.605	69.	16.	.625	74.	DATA0127
32.	.635	78.				DATA0128
342.	1.	10	71.	0.		DADATA0129
2.	.417		4.	.532		DATA0130
8.	.584		16.	.6		DATA0131
32.	.611		64.	.613		DATA0132
35.2375	.1772	10	61.	0.		DADATA0133
2.	.43		4.	.57		DATA0134
8.	.65		16.	.683		DATA0135
32.	.7					DATA0136
36.3125	.3068	10	61.	0.		DADATA0137
2.	.47		4.	.58		DATA0138
8.	.64		16.	.67		DATA0139
32.	.705					DATA0140
37.396	.4927	10	61.	0.		DADATA0141
2.	.38		4.	.506		DATA0142
8.	.58		16.	.633		DATA0143
32.	.65					DATA0144
38.643	1.299	0	51.	0.	90.	DADATA0145
2.	.4	65.	4.	.585	68.	DATA0146
8.	.687	75.	16.	.735	75.	DATA0147
39 1	2.602	0	51.	C.	86.	DADATA0148
2.	.425	65.	4.	.59	70.	DATA0149
8.	.665	77.	16.	.75	84.	DATA0150
40.914	2.624	0	51.	0.	87.	DADATA0151
2.	.44	63.	4.	.62	68.	DATA0152
8.	.73	73.	16.	.8	80.	DATA0153
41.916	2.636	0	51.	0.	84.	DADATA0154
2.	.35	65.	4.	.51	71.	DATA0155
8.	.594	74.	16.	.63	76.	DATA0156
421.1405	2.57	0	51.	C.	56.	DADATA0157
2.	.5	54.	4.	.685	62.	DATA0158
8.	.76	70.	16.	.765	80.	DATA0159
430.	.095	12	8.519	0.		DADATA0160
1.	.855		2.	.85		DATA0161
4.	.832		8.	.817		DATA0162
16.	.804		32.	.798		DATA0163
64.	.79					DATA0164
440.	.095	12	8.515	0.		DADATA0165
1.	.832		2.	.836		DATA0166
4.	.827		8.	.817		DATA0167
16.	.813		32.	.812		DATA0168
64.	.812					DATA0169
450.	.104	12	8.531	0.		DADATA0170
1.	.924		2.	.895		DATA0171
4.	.842		8.	.805		DATA0172
16.	.784		32.	.763		DATA0173
64.	.75					DATA0174
460.	.168	12	8.531	0.		DATA0175
1.	.947		2.	.905		DATA0176
4.	.842		8.	.795		DATA0177
16.	.768		32.	.747		DATA0178
64.	.737					DATA0179
470.	.25	12	9.43	C.		DADATA0180

.5	.858		1.	.922		DATA0181
2.	.89		4.	.856		DATA0182
8.	.83		16.	.813		DATA0183
32.	.8		64.	.79		DATA0184
480.	.25	12	9.43	0.		DADATA0185
.5	.917		1.	.878		DATA0186
2.	.852		4.	.83		DATA0187
8.	.813		16.	.8		DATA0188
32.	.787		64.	.78		DATA0189
490.	.255	12	9.465	0.		DADATA0190
.5	.6		1.	.976		DATA0191
2.	.896		4.	.853		DATA0192
8.	.781		16.	.751		DATA0193
32.	.73		64.	.717		DATA0194
500.	.26	12	9.44	0.		DADATA0195
.5	.665		1.	.958		DATA0196
2.	.905		4.	.816		DATA0197
8.	.79		16.	.758		DATA0198
32.	.737		64.	.721		DATA0199
510.	.38	12	9.4	0.		DATA0200
.5	.77		1.	.958		DATA0201
2.	.915		4.	.833		DATA0202
8.	.768		16.	.735		DATA0203
32.	.71		64.	.69		DATA0204
520.	.623	12	10.219	0.		DADATA0205
.25	.215		.5	.85		DATA0206
1.	.974		2.	.926		DATA0207
4.	.833		8.	.773		DATA0208
16.	.716		32.	.667		DATA0209
64.	.666					DATA0210
53.9215	2.668	1	6.66	0.	0.	DADATA0211
1.	.36	48.	2.	.49	33.	DATA0212
4.	.51	32.	8.	.495	35.	DATA0213
16.	.44	38.				DATA0214
541.	1.3097	1	6.82	0.	0.	DADATA0215
1.	.22	60.	2.	.62	78.	DATA0216
4.	.62	85.	8.	.62	84.	DATA0217
16.	.62	84.				DATA0218
551.	2.28	1	6.56	0.	0.	DADATA0219
1.	.66	48.	2.	.835	48.	DATA0220
4.	.85	49.	8.	.81	50.	DATA0221
16.	.7	50.				DATA0222
56.643	.958	1	7.28	0.	85.	DADATA0223
.5	.32	85.	1.	.67	73.	DATA0224
2.	.74	70.	4.	.73	68.	DATA0225
8.	.71	67.	16.	.71	67.	DATA0226
571.	1.679	1	6.58	0.	58.	DADATA0227
1.	.52	58.	2.	.63	38.	DATA0228
4.	.66	35.	8.	.66	35.	DATA0229
16.	.66	35.				DATA0230
581.15	1.3	1	6.8	0.	50.	DADATA0231
1.	.64	45.	2.	.86	38.	DATA0232
4.	.913	38.	8.	.915	38.	DATA0233
16.	.91	38.				DATA0234
59.525	.99	0	6.96	0.		DADATA0235
1.	.12	0.	2.	.66	46.	DATA0236
4.	.84	56.	8.	.915	65.	DATA0237
16.	.94	72.				DATA0238
60.525	.99	1	6.92	0.	80.	DADATA0239
1.	.14	80.	2.	.55	80.	DATA0240

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4.	.64	55.	8.	.68	60.	DATA0241
16.	.68	78.				CATA0242
61.525	.99	0	6.92	0.	80.	DADATA0243
1.	.18	80.	2.	.58	80.	DATA0244
4.	.67	58.	8.	.69	66.	DATA0245
16.	.7	90.				DATA0246
62.525	.99	0	6.94	0.	80.	DADATA0247
1.	.12	80.	2.	.55	80.	DATA0248
4.	.65	63.	8.	.685	68.	DATA0249
16.	.7	80.				DATA0250
63.395	.4582	0	6.96	0.	0.	DADATA0251
1.	.2	10.	2.	.75	50.	DATA0252
4.	.87	62.	8.	.95	70.	DATA0253
16.	.98	72.				DATA0254
64.395	.4582	0	6.8	0.	82.	DADATA0255
1.	.24	82.	2.	.72	78.	DATA0256
4.	.87	74.	8.	.9	74.	DATA0257
16.	.91	70.				DATA0258
65.395	.4582	1	6.86	0.	90.	DADATA0259
1.	.18	90.	2.	.68	90.	DATA0260
4.	.775	75.	8.	.6	75.	CATA0261
16.	.8	75.				DATA0262
66.395	.4582	1	6.84	0.	90.	DADATA0263
1.	.32	90.	2.	.73	65.	DATA0264
4.	.79	65.	8.	.75	65.	DATA0265
16.	.75	65.				DATA0266
671.15	1.3	1	6.52	C.	90.	DADATA0267
1.	.64	62.	2.	.765	51.	DATA0268
4.	.79	51.	8.	.79	52.	DATA0269
16.	.79	52.				DATA0270
681.15	1.561	1	7.4	C.	55.	DADATA0271
.5	.14	55.	1.	.56	55.	DATA0272
2.	.72	55.	4.	.72	55.	DATA0273
8.	.72	55.	16.	.72	55.	DATA0274
691.15	1.822	1	7.43	0.	48.	DADATAC275
.5	.12	48.	1.	.48	48.	DATA0276
2.	.57	44.	4.	.57	45.	DATA0277
8.	.56	45.	16.	.54	45.	DATA0278
701.15	1.3	1	6.54	C.	58.	DATA0279
1.	.63	58.	2.	.77	60.	DATA0280
4.	.8	57.	8.	.6	56.	DATA0281
16.	.8	55.				DATA0282
711.15	2.598	1	7.48	C.	57.	DADATAC283
.5	.04	57.	1.	.6	57.	DATA0284
2.	.72	58.	4.	.7	58.	DATA0285
8.	.69	60.	16.	.69	60.	DATA0286
720.01	.1367	11	8.521	C.		DADATA0287
1.	.885		2.	.637		DATA0288
4.	.8		8.	.772		DATA0289
16.	.757		32.	.747		CATA0290
64.	.741					DATA0291
730.01	.2186	11	9.476	0.		DADATA0292
.5	.2		1.	.677		DATA0293
2.	.882		4.	.853		CATA0294
8.	.807		16.	.772		DATA0295
32.	.747		64.	.73		DATAC296
74.375	.4418	11	10.216	C.		DADATA0297
.25	.1		.5	.37		DATA0298
1.	.437		2.	.434		DATA0299
4.	.415		8.	.4		DATAC300

16.	.39		32.	.38	DATA0301
64.	.37				DATA0302
75.375	.4418	11	11.088	0.	DADATA0303
.125	.38		.25	.46	DATA0304
.5	.515		1.	.534	DATA0305
2.	.535		4.	.53	DATA0306
8.	.524		16.	.517	DATA0307
32.	.51		64.	.502	DATA0308
76.375	.4418	11	13.022	0.	DADATA0309
.03125	.17		.0625	.86	DATA0310
.125	.67		.25	.585	DATA0311
.5	.6		1.	.605	DATA0312
2.	.6		4.	.597	CATA0313
8.	.59		16.	.586	DATA0314
32.	.585		64.	.583	DATA0315
77.01	.4418	11	9.286	0.	DADATA0316
.5	.46		1.	.57	DATA0317
2.	.576		4.	.566	DATA0318
8.	.55		16.	.536	DATA0319
32.	.525		64.	.516	DATA0320
781.5775	2.616	10	6.96	0.	DADATA0321
1.	.055		2.	.560	DATA0322
4.	.710		8.	.786	DATA0323
16.	.78				DATA0324
791.5775	1.876	11	6.63	0.	DADATA0325
1.	.35		2.	.75	DATA0326
4.	.805		8.	.81	DATA0327
16.	.81				DATA0328
801.5775	1.659	11	6.7	0.	DADATA0329
1.	.31		2.	.89	DATA0330
4.	.96		8.	.965	DATA0331
16.	.94				DATA0332
81.4075	.2543	11	9.36	0.	DADATA0333
.5	.65		1.	.83	DATA0334
2.	.815		4.	.72	DATA0335
8.	.656		16.	.612	DATA0336
32.	.6		64.	.6	DATA0337
82.4075	.2543	11	9.345	0.	DADATA0338
.5	.72		1.	.858	DATA0339
2.	.85		4.	.79	DATA0340
8.	.736		16.	.687	DATA0341
32.	.65		64.	.64	DATA0342
83.4	.2543	11	9.36	0.	DADATA0343
.5	.6		1.	.92	DATA0344
2.	.915		4.	.843	DATA0345
8.	.745		16.	.7	DATA0346
32.	.675		64.	.665	DATA0347
84.4075	.2543	11	9.42	0.	DADATA0348
.5	.37		1.	.725	DATA0349
2.	.74		4.	.704	DATA0350
8.	.666		16.	.63	DATA0351
32.	.61		64.	.58	DATA0352
85.35	.2125	11	6.4	0.	DATA0353
.5	.68		1.	.73	DATA0354
2.	.7		4.	.676	DATA0355
8.	.66				DATA0356
86.35	.425	11	5.5	0.	DADATA0357
1.	.28		2.	.608	DATA0358
4.	.65		8.	.632	DATA0359
87.23	.578	11	13.011	0.	DADATA0360

Value	Value	Value	Value	Value	Label
.03125	.4	.C625	.5		DATA0361
.125	.6	.25	.665		DATA0362
.5	.684	1.	.69		DATA0363
2.	.68	4.	.674		DATA0364
8.	.67	16.	.664		DATA0365
32.	.66	64.	.66		DATA0366
88.075	.3871	11	8.17	0.	DADATA0367
.25	.578		.5	.74	DATA0368
1.	.79		2.	.775	DATA0369
4.	.72		8.	.67	DATA0370
16.	.636				DATA0371
89.24	.3871	11	8.17	0.	DADATA0372
.25	.507		.5	.55	DATA0373
1.	.52		2.	.52	DATA0374
4.	.508		8.	.51	DATA0375
16.	.515				DATA0376
90.12	.3871	11	8.17	0.	DADATA0377
.25	.185		.5	.27	DATA0378
1.	.29		2.	.28	DATA0379
4.	.29		8.	.295	DATA0380
16.	.313				DATA0381
91.285	.2775	11	10.125	.69	DADATA0382
.25	.88		.5	.917	DATA0383
1.	.9		2.	.86	DATA0384
4.	.8		8.	.75	DATA0385
16.	.725		32.	.715	DATA0386
64.	.705				DATA0387
92.1625	.2405	11	10.15	0.	DADATA0388
.25	.65		.5	.88	DATA0389
1.	.945		2.	.92	DATA0390
4.	.88		8.	.87	DATA0391
16.	.835		32.	.82	DATA0392
64.	.825				DATA0393
93.1625	.4028	11	10.15	0.	DADATA0394
.25	.35		.5	.52	DATA0395
1.	.58		2.	.54	DATA0396
4.	.52		8.	.505	DATA0397
16.	.5		32.	.5	DATA0398
64.	.495				DATA0399
94.375	.4169	11	11.12	0.	DADATA0400
.125	.045		.25	.772	DATA0401
.5	.8		1.	.754	DATA0402
2.	.684		4.	.61	DATA0403
8.	.57		16.	.558	DATA0404
32.	.552		64.	.55	DATA0405
95.4375	.3853	11	9.33	0.	DADATA0406
.5	.55		1.	.82	DATA0407
2.	.83		4.	.8	DATA0408
8.	.75		16.	.71	DATA0409
32.	.67		64.	.653	DATA0410
96.1875	.1134	11	8.5	.8	DADATA0411
1.	.836		2.	.826	DATA0412
4.	.79		8.	.75	DATA0413
16.	.72		32.	.69	DATA0414
64.	.68				DATA0415
97.34	.104	11	8.565	0.	DADATA0416
1.	.817		2.	.822	DATA0417
4.	.78		8.	.742	DATA0418
16.	.717		32.	.69	DATA0419
64.	.66				DATA0420

98.345	.1291	11	8.52	0.	DADATA0421
1.	.82		2.	.83	DATA0422
4.	.82		8.	.773	DATA0423
16.	.73		32.	.69	DATA0424
64.	.66				DATA0425
99.345	.1958	11	9.39	0.	DADATA0426
.5	.66		1.	.832	DATA0427
2.	.827		4.	.77	DATA0428
8.	.71		16.	.66	DATA0429
32.	.635		64.	.643	DATA0430
100.46	.4423	11	9.39	0.	DADATA0431
.5	.74		1.	.86	DATA0432
2.	.86		4.	.81	DATA0433
8.	.74		16.	.67	DATA0434
32.	.64		64.	.65	DATA0435

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0.98

0.85	0.75	0.3	0.2	0.2	0.2	0.2	0.2	DIFF0001
0.2	0.2	0.2	0.2	0.2	0.2	0.2	0.2	DIFF0002
0.73	0.85	0.85	0.78	0.6	0.4	C.2	C.2	DIFF0003
0.2	0.2	0.2	0.2	0.2	0.2	0.2	0.2	DIFF0004
0.67	0.8	0.85	0.85	C.83	0.8	C.7	C.7	DIFF0005
0.6	0.4	0.2	0.2	0.2	0.2	0.2	0.2	DIFF0006
0.63	0.76	0.81	C.83	0.85	0.83	C.8	C.8	DIFF0007
0.7	0.6	0.4	0.2	0.2	0.2	0.2	0.2	DIFF0008
0.58	0.72	0.78	0.81	0.83	0.83	0.8	0.8	DIFF0009
0.7	0.6	0.4	0.2	0.2	C.2	0.2	0.2	DIFF0010
0.5	0.69	0.76	0.79	0.83	0.83	C.8	C.8	DIFF0011
0.7	0.6	0.4	0.2	0.2	0.2	0.2	0.2	DIFF0012
0.5	0.66	0.74	0.77	0.79	0.80	0.83	0.83	DIFF0013
0.83	0.8	0.7	0.6	0.4	C.2	C.2	C.2	DIFF0014
0.5	0.63	0.72	0.76	0.78	0.8	C.83	C.83	DIFF0015
0.83	0.8	0.7	0.6	0.4	0.2	0.2	0.2	DIFF0016
0.5	0.62	0.71	0.75	0.77	0.80	0.83	0.83	DIFF0017
0.83	0.8	0.7	0.6	0.4	C.2	C.2	C.2	DIFF0018
0.5	0.61	0.69	0.74	0.77	0.8	C.83	C.83	DIFF0019
0.83	0.8	0.7	0.6	0.4	0.2	0.2	0.2	DIFF0020
0.5	0.58	0.62	0.71	0.74	0.75	C.8	C.8	DIFF0021
0.83	0.83	0.8	0.7	0.6	C.4	C.2	C.2	DIFF0022
0.5	0.55	0.58	0.65	0.72	0.75	C.8	C.8	DIFF0023
0.83	0.83	0.8	C.7	0.6	0.4	0.2	0.2	DIFF0024
1.1	1.2	1.3	1.4	1.5	1.6	1.7	1.7	DIFF0025
1.8	1.9	2.0	2.1	2.2	2.3	2.4	2.4	DIFF0026
1.1	1.2	1.3	1.4	1.52	1.62	1.75	1.75	DIFF0027
1.8	1.9	2.0	2.1	2.2	2.3	2.4	2.4	DIFF0028
1.1	1.2	1.3	1.4	1.51	1.6	1.74	1.74	DIFF0029
1.83	2.0	2.27	2.4	2.5	3.0	3.5	3.5	DIFF0030
1.1	1.2	1.3	1.4	1.5	1.69	1.84	1.84	DIFF0031
2.05	2.16	2.45	2.9	3.1	3.3	3.5	3.5	DIFF0032
1.1	1.2	1.3	1.4	1.56	1.78	2.09	2.09	DIFF0033
2.36	2.5	2.95	3.6	3.7	3.8	3.9	3.9	DIFF0034
1.1	1.2	1.3	1.4	1.67	2.08	2.32	2.32	DIFF0035
2.68	2.86	3.5	4.4	4.6	4.8	5.0	5.0	DIFF0036
1.1	1.2	1.3	1.4	1.5	1.54	1.8	1.8	DIFF0037
2.3	2.6	3.0	3.25	4.12	5.5	5.6	5.6	DIFF0038
1.1	1.2	1.3	1.4	1.5	1.6	1.91	1.91	DIFF0039
2.53	2.84	3.36	3.67	4.83	6.5	6.6	6.6	DIFF0040
1.1	1.2	1.3	1.4	1.5	1.69	2.03	2.03	DIFF0041

DIFF0001
DIFF0002
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DIFF0038
DIFF0039
DIFF0040
DIFF0041
DIFF0042
DIFF0043
DIFF0044

2.77	3.15	3.75	4.15	5.6	7.6	7.8	DIFF0045
1.1	1.2	1.3	1.4	1.5	1.78	2.14	DIFF0046
3.05	3.45	4.2	4.65	6.5	8.9	9.0	DIFF0047
1.1	1.2	1.3	1.4	1.5	1.56	1.96	DIFF0048
2.36	3.68	4.17	5.17	5.85	8.4	11.0	DIFF0049
1.1	1.2	1.3	1.4	1.5	1.72	2.21	DIFF0050
2.68	4.8	5.4	7.0	8.0	10.0	15.0	DIFF0051
1.0	2.0	3.0	4.0	5.0	6.0	7.0	DIFF0052
8.0	9.0	10.0	12.0	15.0			DIFF0053
	2	168	168	12	-133	0.98	DIFF0054
0.9	0.9	0.88	0.87	0.86	0.8	0.67	DIFF0055
0.58	0.47	0.4	0.3	0.3	0.3	0.3	DIFF0056
0.88	0.9	0.9	0.88	0.86	0.85	0.8	DIFF0057
0.7	0.6	0.4	0.3	0.3	0.3	0.3	DIFF0058
0.87	0.9	0.9	0.9	0.88	0.875	0.85	DIFF0059
0.8	0.7	0.6	0.4	0.3	0.3	0.3	DIFF0060
0.85	0.88	0.9	0.9	0.9	0.9	0.875	DIFF0061
0.85	0.8	0.7	0.6	0.4	0.3	0.3	DIFF0062
0.82	0.875	0.9	0.9	0.91	0.9	0.875	DIFF0063
0.85	0.8	0.7	0.6	0.4	0.3	0.3	DIFF0064
0.77	0.86	0.875	0.89	0.91	0.91	0.9	DIFF0065
0.875	0.85	0.8	0.7	0.6	0.4	0.3	DIFF0066
0.74	0.85	0.87	0.88	0.91	0.91	0.9	DIFF0067
0.875	0.85	0.8	0.7	0.6	0.4	0.3	DIFF0068
0.875	0.85	0.8	0.7	0.6	0.4	0.3	DIFF0069
0.7	0.84	0.86	0.88	0.9	0.91	0.9	DIFF0070
0.6	0.82	0.85	0.88	0.9	0.9	0.9	DIFF0071
0.875	0.85	0.8	0.7	0.6	0.4	0.3	DIFF0072
0.5	0.8	0.85	0.87	0.875	0.9	0.9	DIFF0073
0.875	0.85	0.8	0.7	0.6	0.4	0.3	DIFF0074
0.5	0.7	0.8	0.86	0.875	0.89	0.89	DIFF0075
0.875	0.85	0.8	0.75	0.7	0.6	0.5	DIFF0076
0.5	0.6	0.7	0.8	0.85	0.875	0.885	DIFF0077
0.875	0.85	0.8	0.75	0.7	0.6	0.5	DIFF0078
1.1	1.2	1.3	1.4	1.5	1.6	1.7	DIFF0079
1.8	1.9	2.0	2.1	2.2	2.3	2.4	DIFF0080
1.1	1.2	1.3	1.4	1.5	1.62	1.7	DIFF0081
1.84	2.0	2.3	2.6	2.9	3.0	3.1	DIFF0082
1.1	1.2	1.3	1.4	1.5	1.55	1.7	DIFF0083
1.84	2.07	2.26	2.7	3.0	3.3	3.6	DIFF0084
1.1	1.2	1.3	1.4	1.5	1.55	1.66	DIFF0085
1.8	2.0	2.31	2.53	3.2	3.5	3.7	DIFF0086
1.1	1.2	1.3	1.4	1.5	1.67	1.77	DIFF0087
1.93	2.2	2.57	2.83	3.65	4.0	4.2	DIFF0088
1.1	1.2	1.3	1.4	1.5	1.65	1.76	DIFF0089
1.9	2.07	2.4	2.8	3.17	4.1	4.6	DIFF0090
1.1	1.2	1.3	1.4	1.5	1.7	1.9	DIFF0091
2.04	2.25	2.6	3.08	3.48	4.7	5.0	DIFF0092
1.1	1.2	1.3	1.4	1.48	1.7	2.04	DIFF0093
2.18	2.45	2.8	3.32	3.8	5.2	6.0	DIFF0094
1.1	1.2	1.3	1.4	1.53	1.7	2.08	DIFF0095
2.32	2.6	3.0	3.6	4.1	5.6	6.5	DIFF0096
1.1	1.2	1.3	1.4	1.42	1.6	2.07	DIFF0097
2.43	2.75	3.2	3.9	4.5	6.3	7.0	DIFF0098
1.1	1.2	1.3	1.4	1.52	1.7	2.1	DIFF0099
2.55	3.05	3.55	4.0	4.5	5.2	6.0	DIFF0100
1.1	1.2	1.3	1.4	1.5	1.74	2.3	DIFF0101
2.8	3.55	4.0	4.8	5.4	6.5	7.5	DIFF0102
1.0	2.0	3.0	4.0	5.0	6.0	7.0	DIFF0103
8.0	9.0	10.0	12.0	15.0			DIFF0104

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YOUR CARD TOTAL IS ---

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