

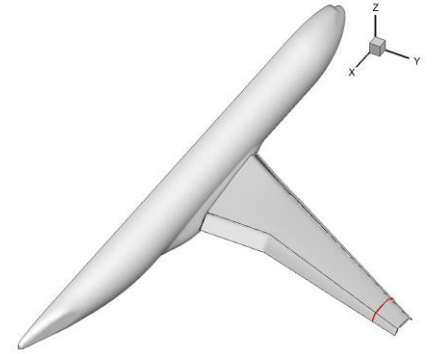
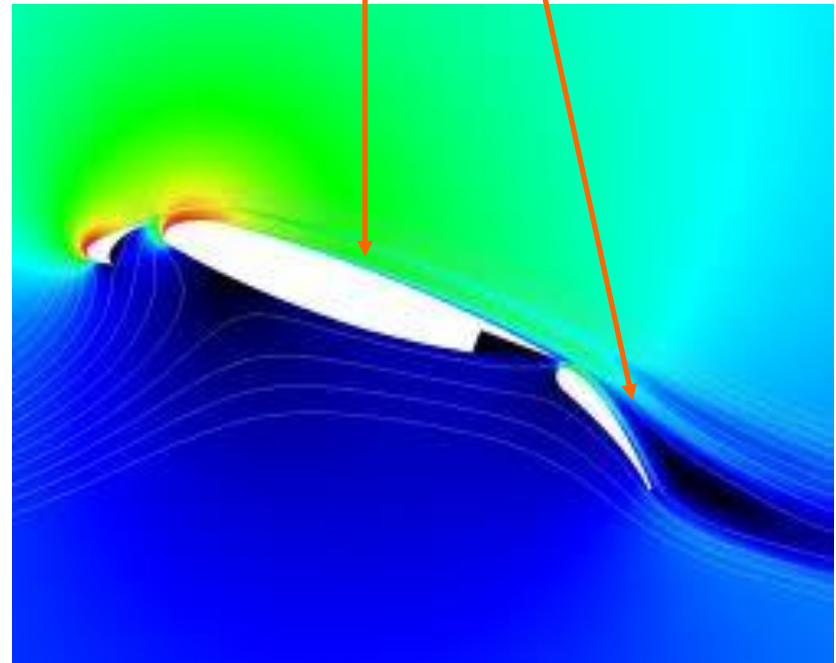
RANS-Turbulenzmodellierung für subsonische druckinduzierte Strömungsablösung

T. Knopp, A. Schröder, M. Novara, D. Schanz, C. Willert, A. Krumbein

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Goal: Improve RANS turbulence models to predict the onset of flow separation of low-speed flows

Significant adverse pressure gradient (APG) during take-off and landing



Outline

- Goal: Modification of the differential Reynolds stress model SSG/LRR- ω
- Method: Combination of theoretical work and experimental data
- Challenge (show stopper): Worldwide suitable test-cases and data are not available for high Re
=> VicToria experiment within the project VicToria



Strategy for RANS model improvement

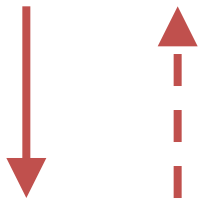
Physics-based improvement of RANS + RSM



Strategy for RANS model improvement

(Empirical) laws for turbulence statistics

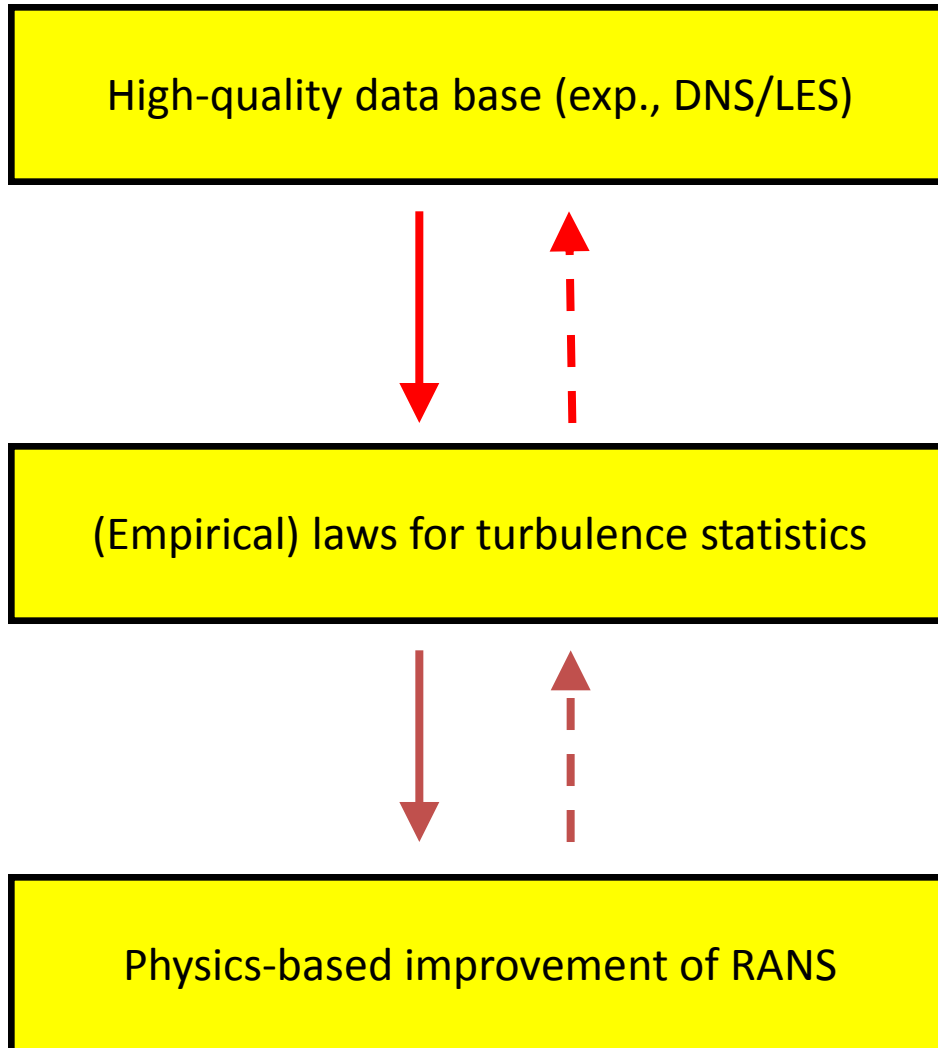
Extension of the log-law for adverse pressure gradients



Physics-based improvement of RANS



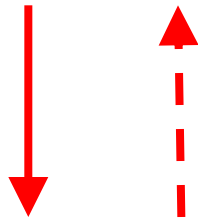
Strategy for RANS model improvement



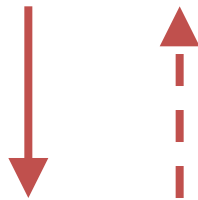
Strategy for RANS model improvement

High-quality data base (exp., DNS/LES)

At high Re: only by experiments



(Empirical) laws for turbulence statistics



Physics-based improvement of RANS



Part I:

The VicToria experiment.

Data base for turbulent boundary layers
at adverse pressure gradient with
incipient separation

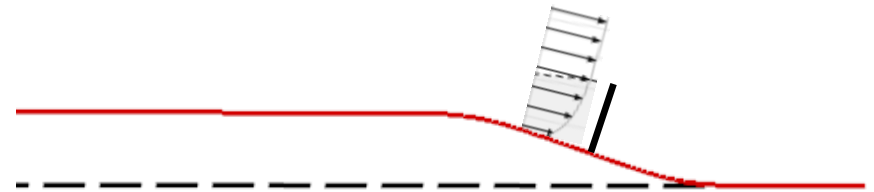


Design of the VicToria experiment



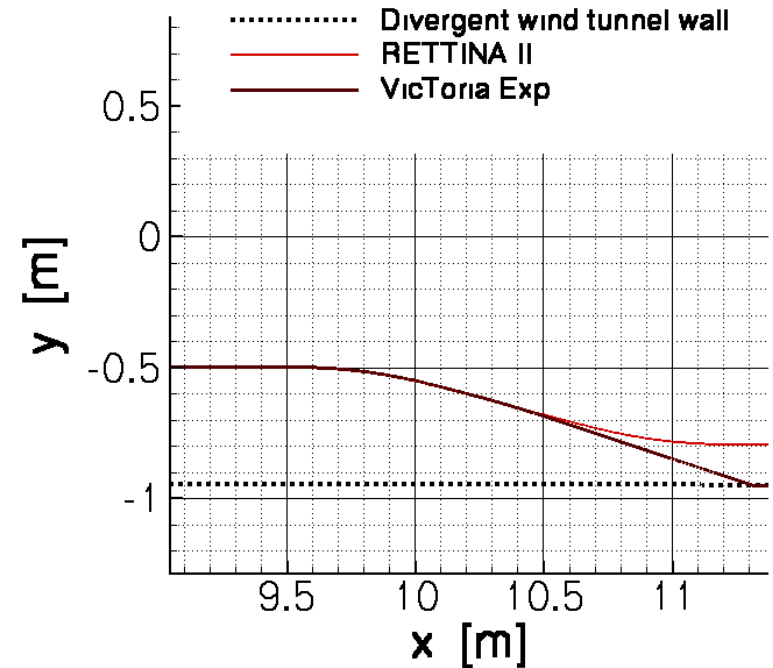
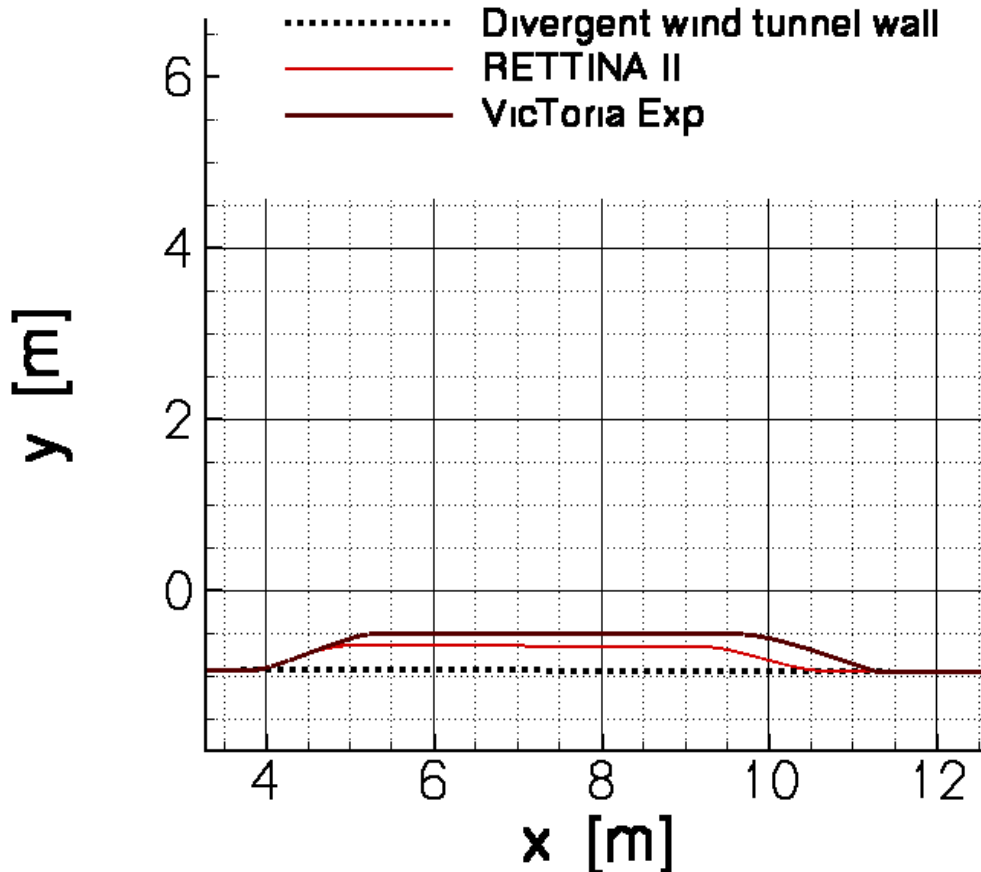
Design criteria for the VicToria experiment

- **Well defined and controlled flow conditions**
 - Use a generic contour mounted to wind tunnel wall instead of airfoil/wing at high incidence angle
- **Boundary layer characteristics similar to transport aircrafts at high-lift**
 - Large Reynolds numbers
 - Strong adverse pressure gradients leading to separation
 - Thin separation bubble
- **Highly resolved experimental data using particle-imaging/tracking methods**
 - Mean velocity, Reynolds stresses, wall-shear stress
 - ⇒ **Thick boundary layers** to enable measurement in the near-wall region



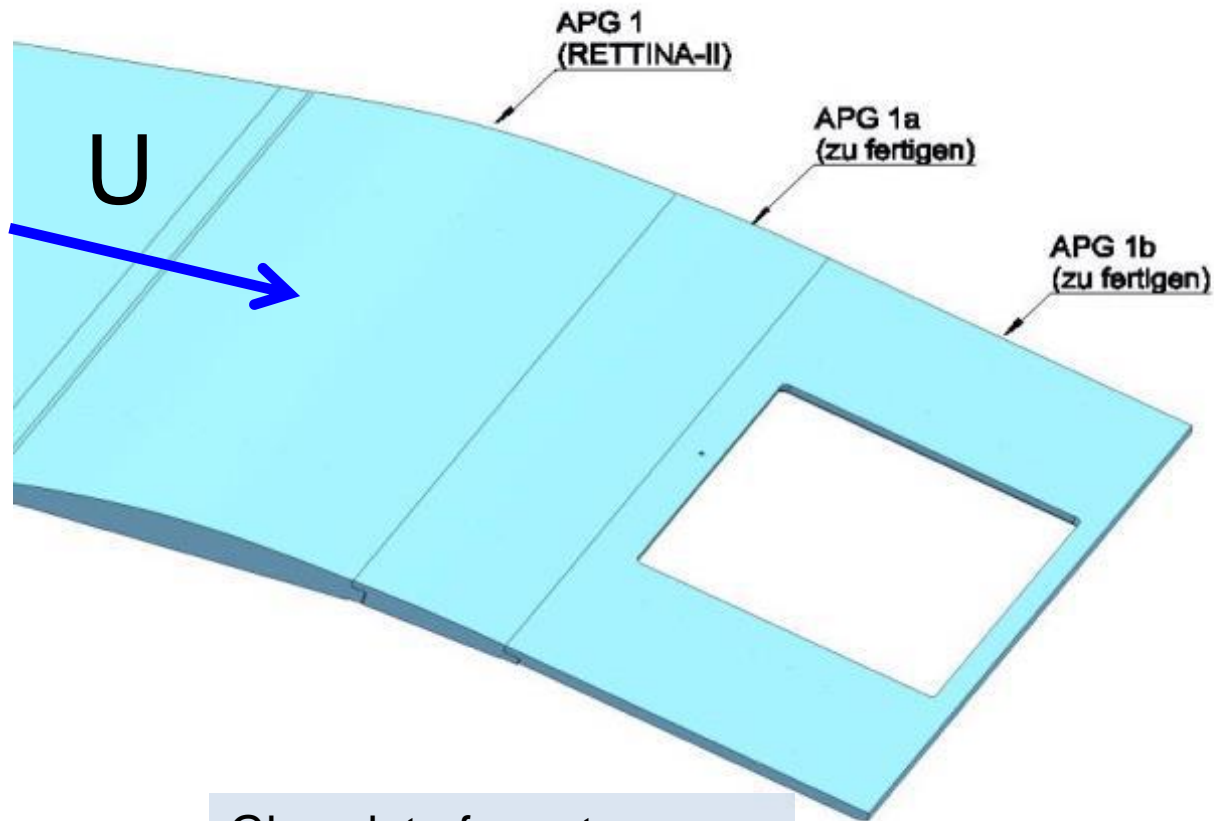
Design criteria for the VicToria experiment

- Re-use of parts of so-called RETTINA II geometry (precursor DFG/DLR exp.)
 - RETTINA II experiment: Moderate APG, flow remains attached
 - VicToria experiment: Strong APG leading to mild separation



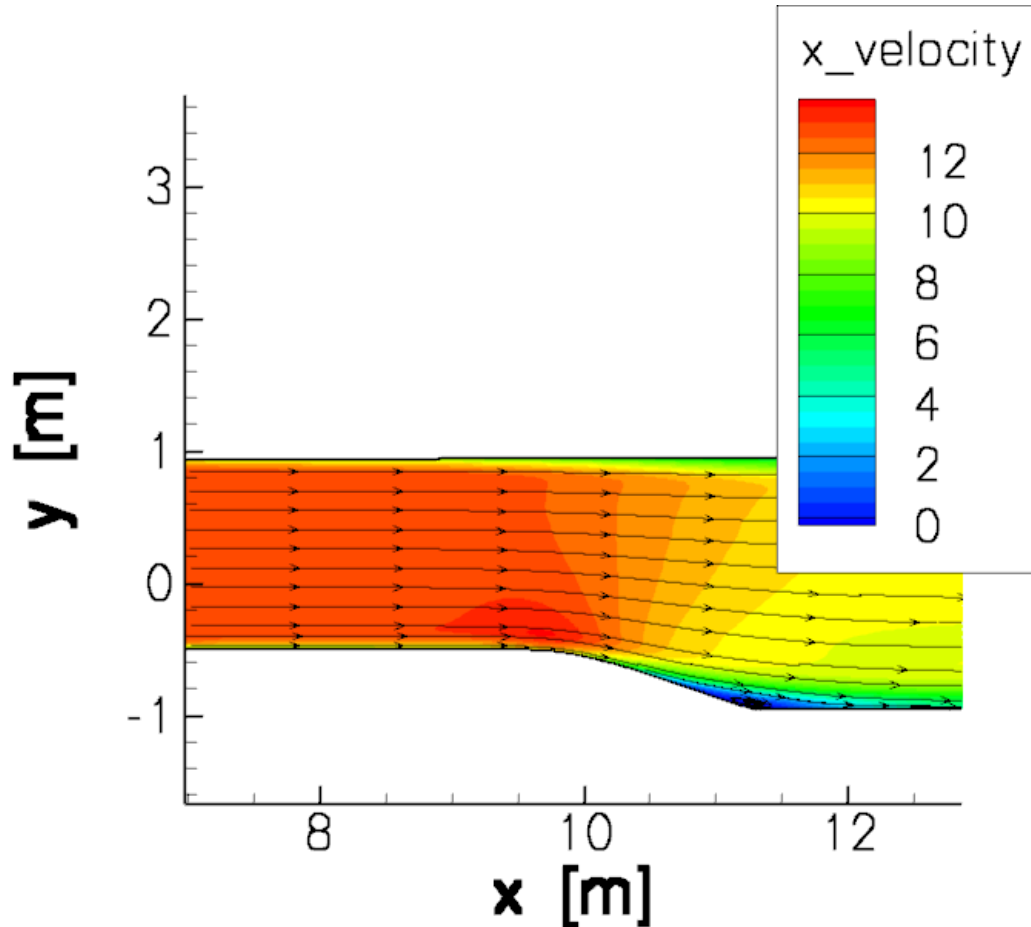
Design of the VicToria geometry model

- Requirement by measurement technique: onset of separation on an inclined flat plate
- This enables measurements through the geometry from behind



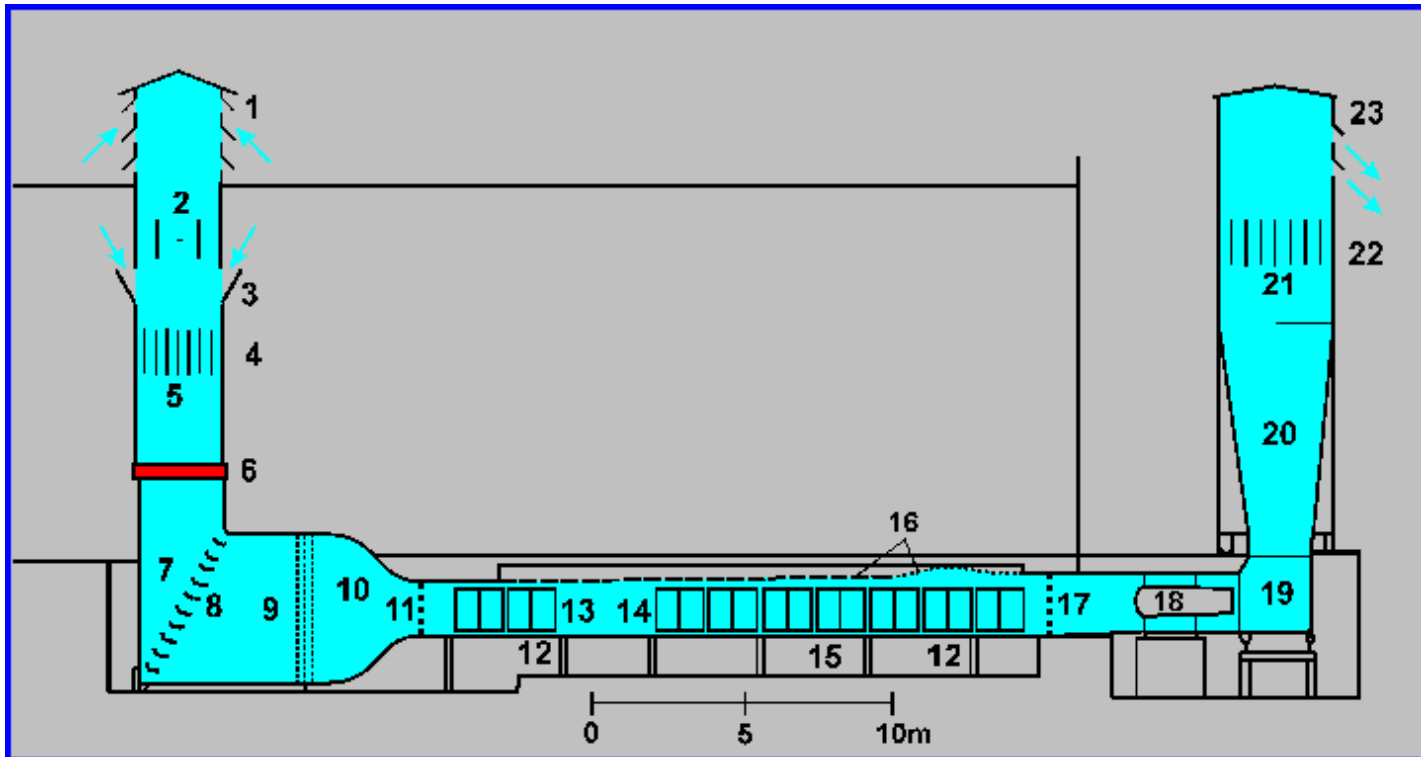
Design criteria for the VicToria experiment

Precursor RANS simulations for the design of the experiment



Atmospheric wind-tunnel AWM at UniBw München

- Experiments were performed in the AWM at UniBw München at the Institute of Fluid Mechanics and Aerodynamics headed by Prof. Christian Kähler

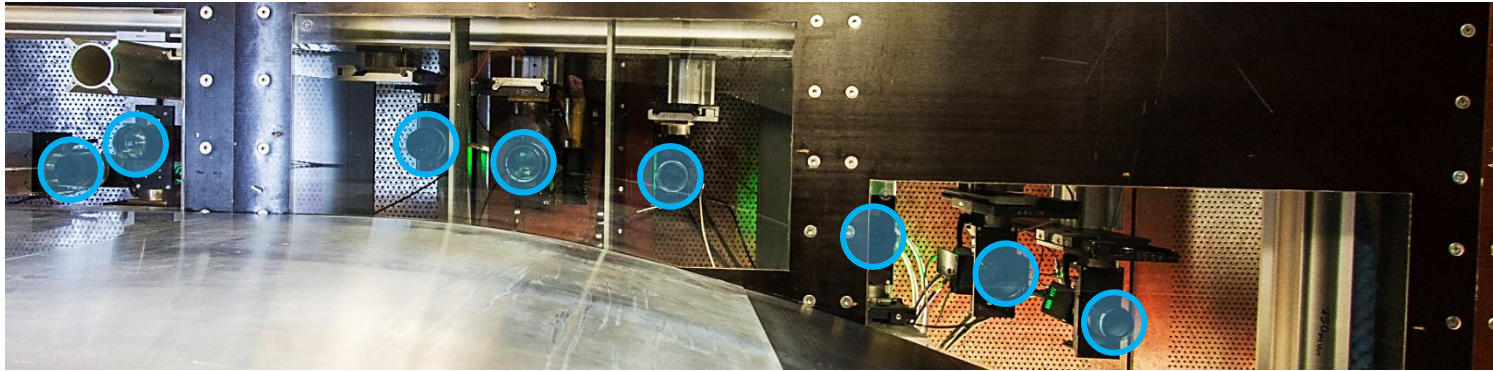


Measurement technique

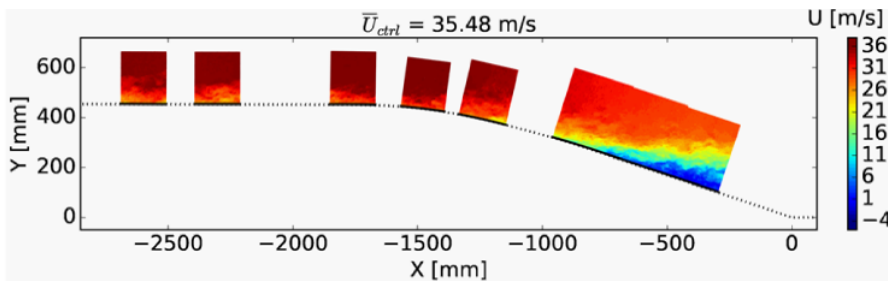


Large-scale overview measurement: 2D2C PIV

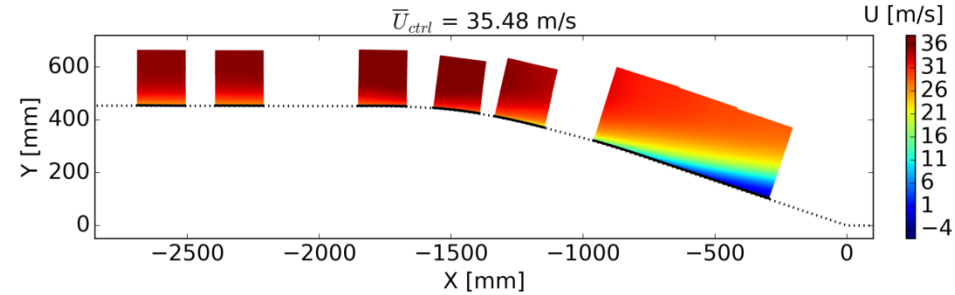
- High quality data for mean velocity from $y^+ \sim 150$ to the outer edge of boundary layer



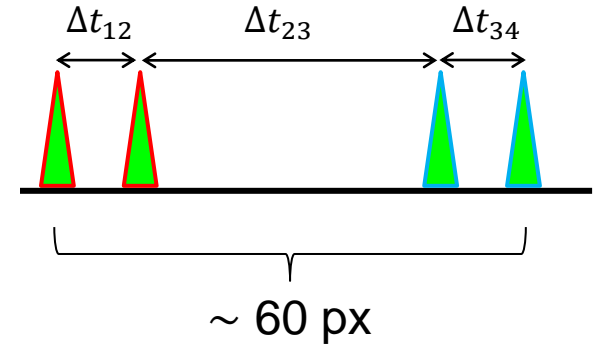
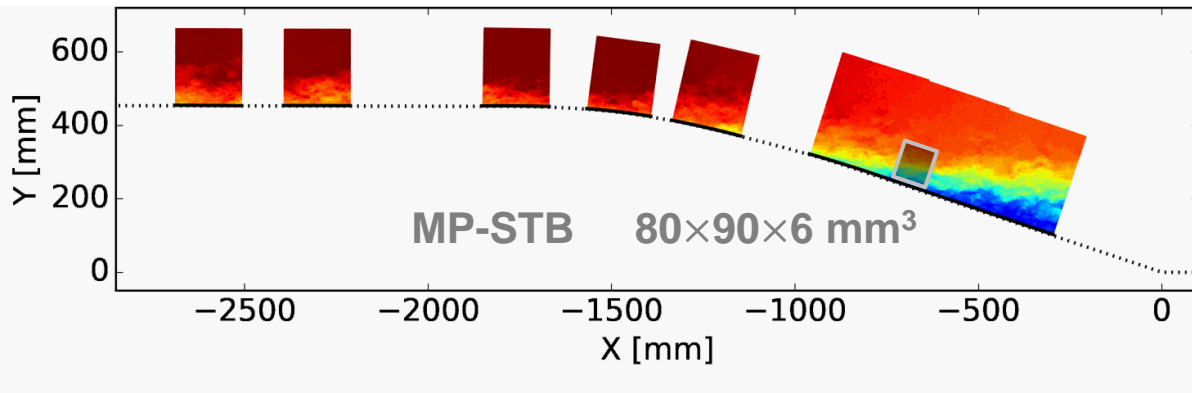
Instantaneous snapshot



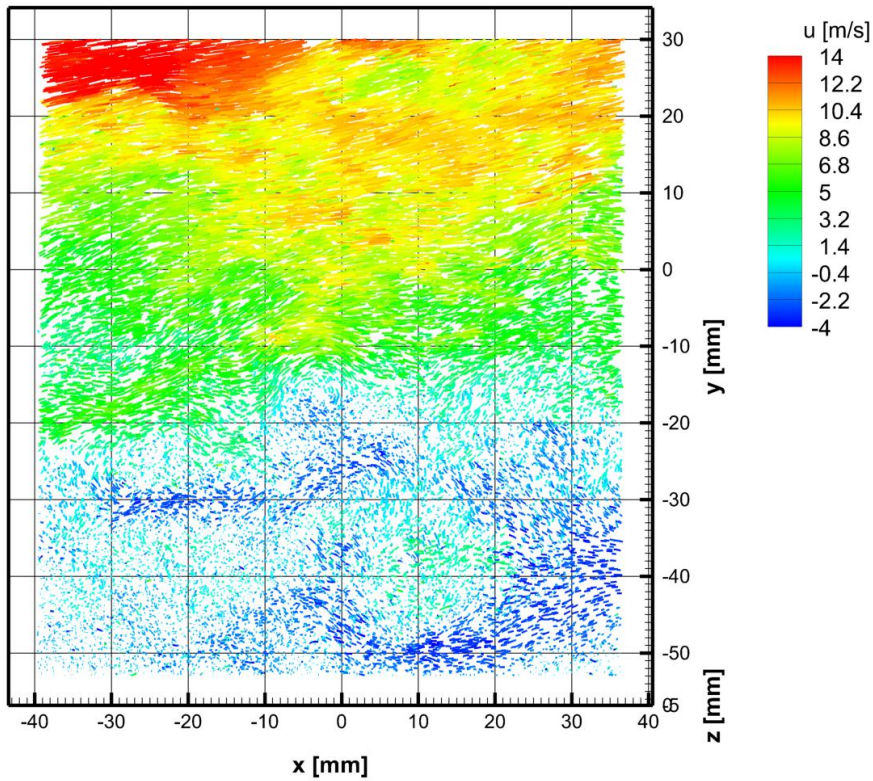
Statistically averaged flow field



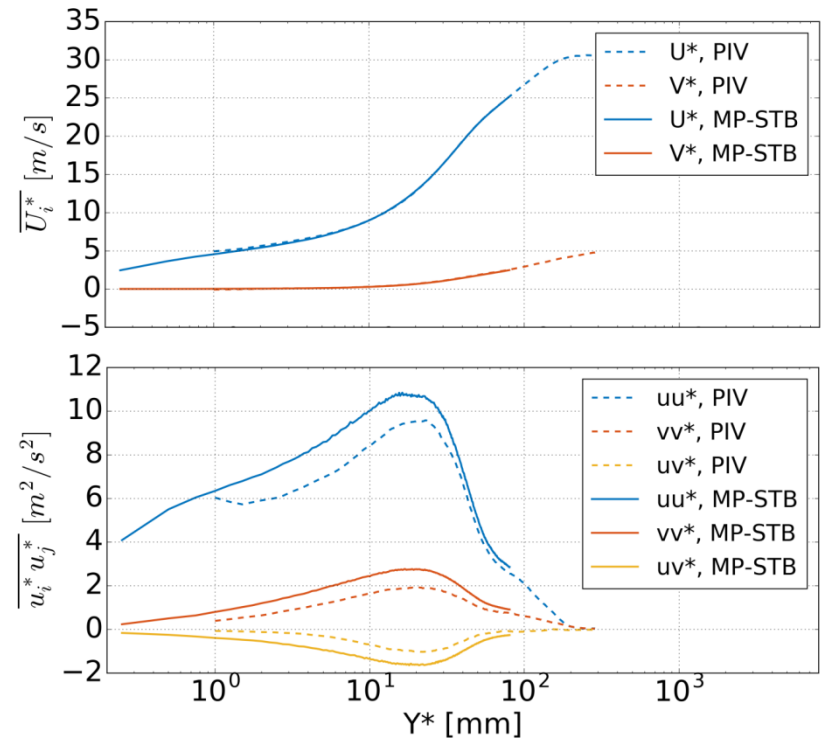
Detail measurement: 3D3C PTV STB (Multi-pulse)



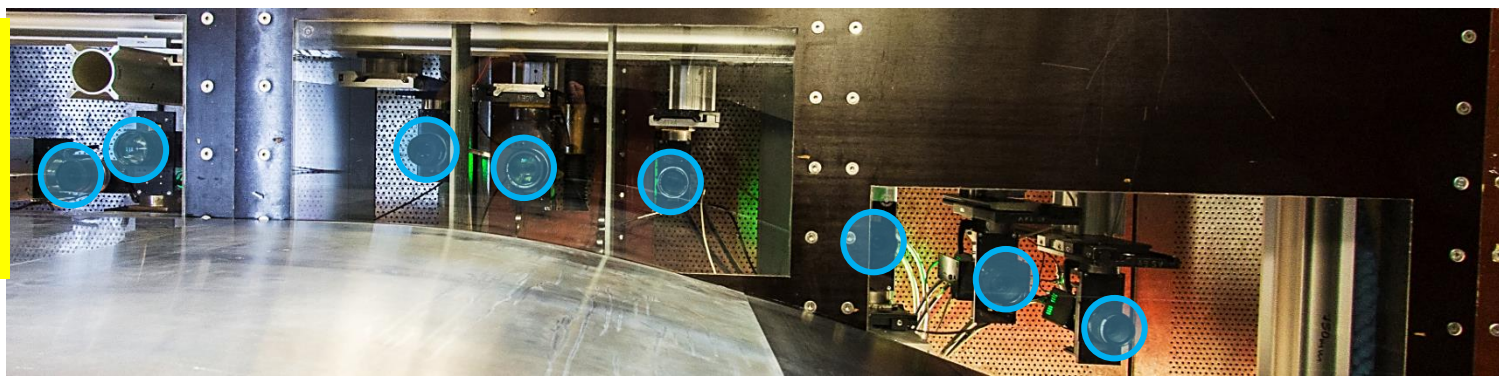
~ 20,000 instantaneous tracks



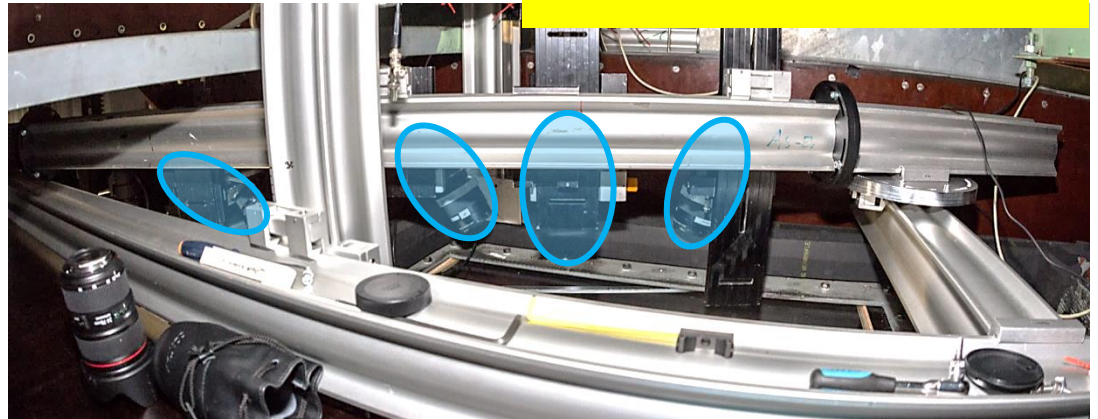
Ensemble average (bin size = 70 microns)



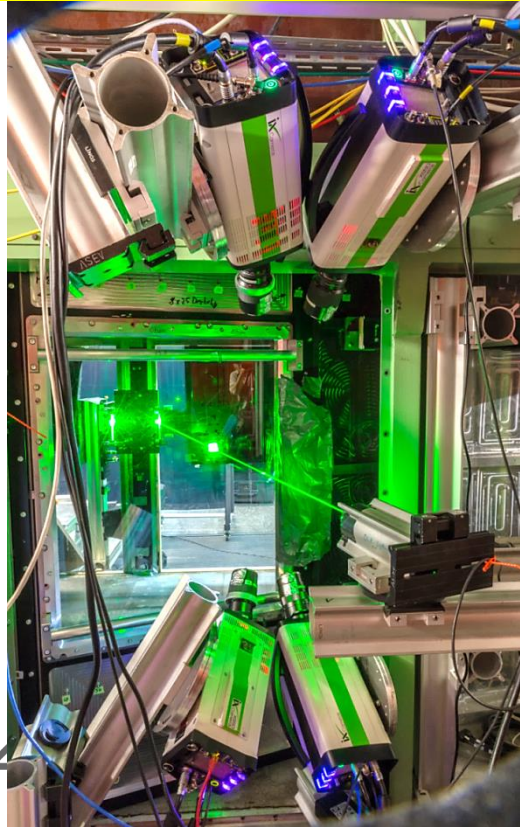
**Overview large-
scale
2D2C-PIV**



3D3C PTV MP-STB



Time resolved 3D3C PTV-STB



Measurement techniques and cameras

2D2C-PIV



8 PCO-Edge cameras

2D-2C overview measurement

2D2C-PTV



1 SA-X2 camera

high-resolution profiles with 2D-STB

3D3C PTV

TR-STB



4 IX cameras

time-resolved 3D STB

3D3C PTV

MP-STB



4 PCO Edge cameras

multi-pulse 3D-STB

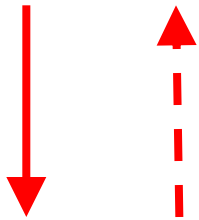


Part II:
Evaluation of the results
and
extension of the log-law for adverse
pressure gradients
when approaching separation



RANS model improvement

High-quality data base (VicToria exp.)



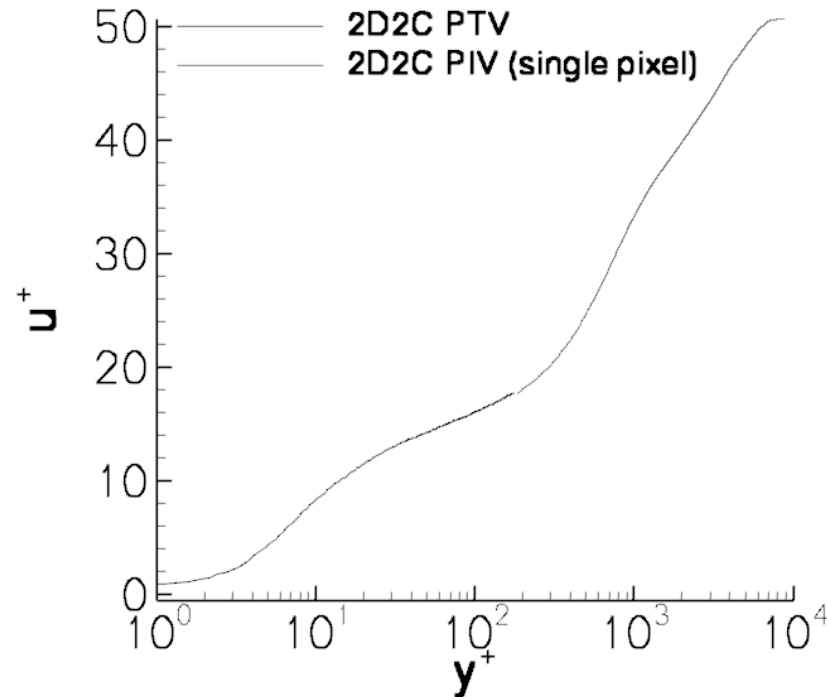
(Empirical) laws for turbulence statistics



Input for wall-law scaling: Wall-shear stress

- The wall-shear stress is the central quantity for the physically meaningful non-dimensionalization (“scaling”) of the data
 - scaling for the inner 15% of the boundary layer

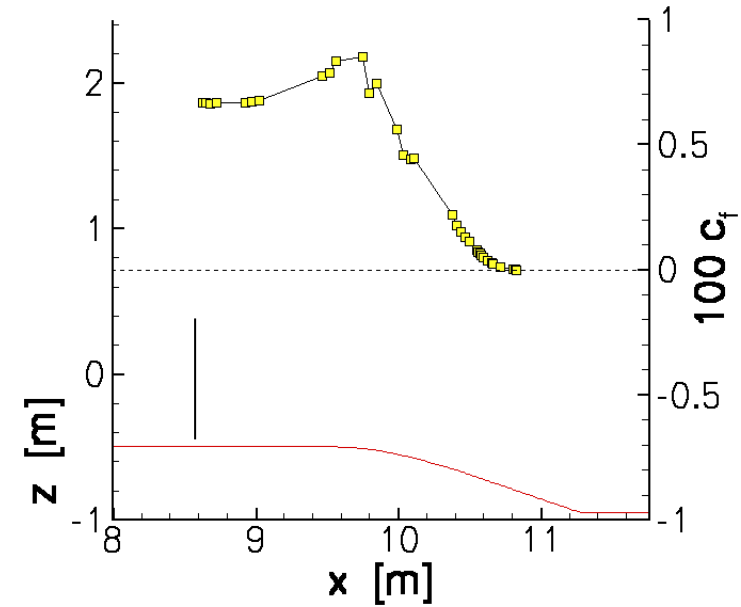
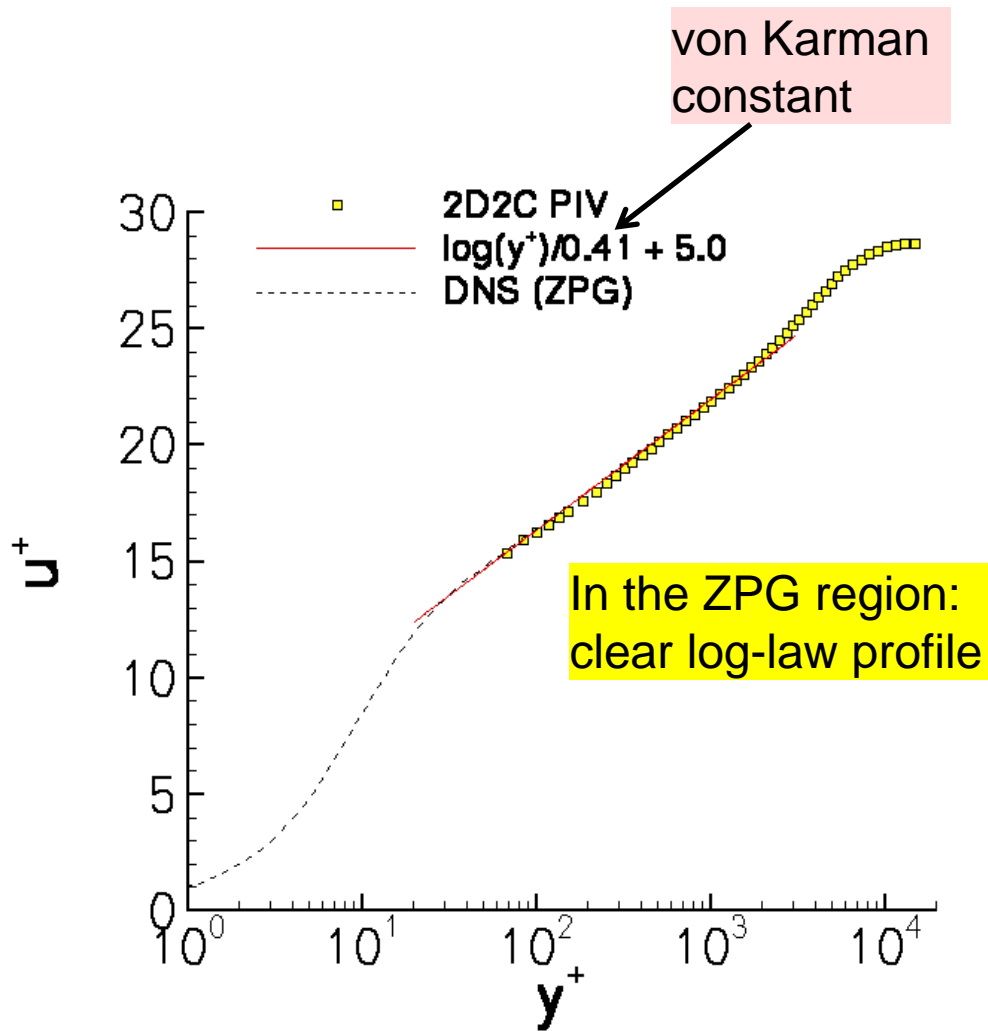
$$u^+ = \frac{U}{u_\tau}$$



$$y^+ = \frac{y u_\tau}{\nu}$$



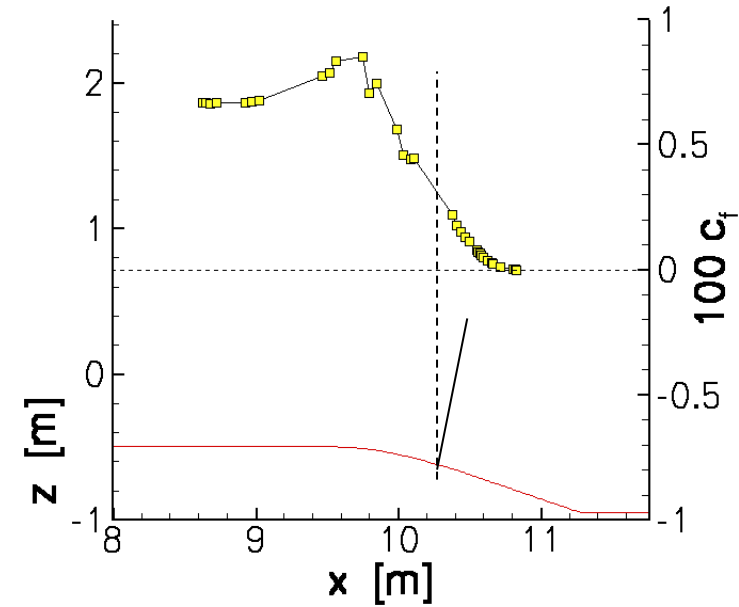
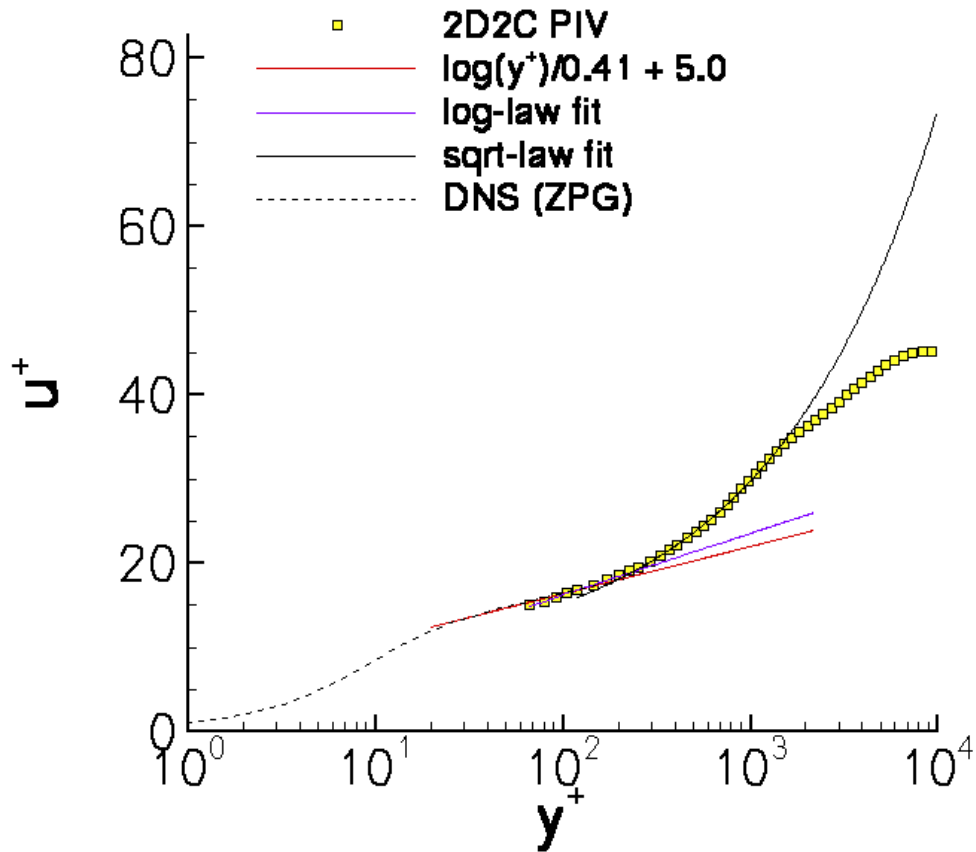
Mean velocity profiles



$$\Delta p_x^+ = dp^+/dx^+ = 0$$



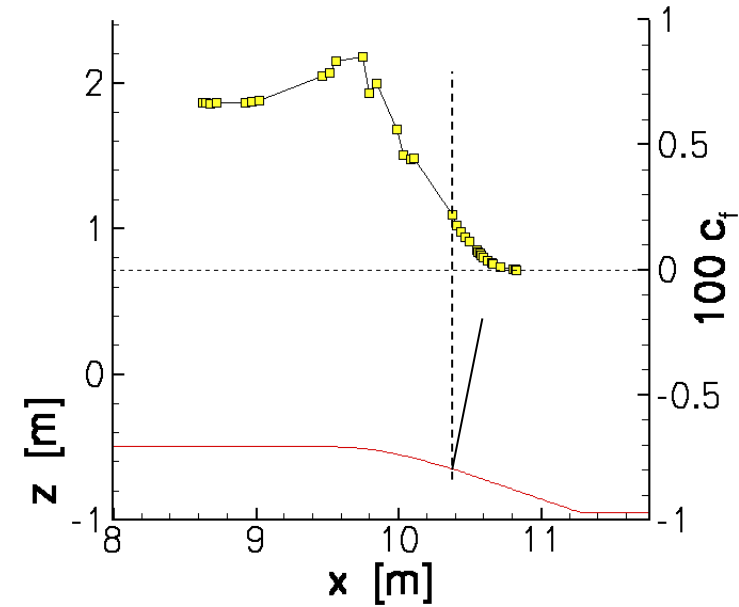
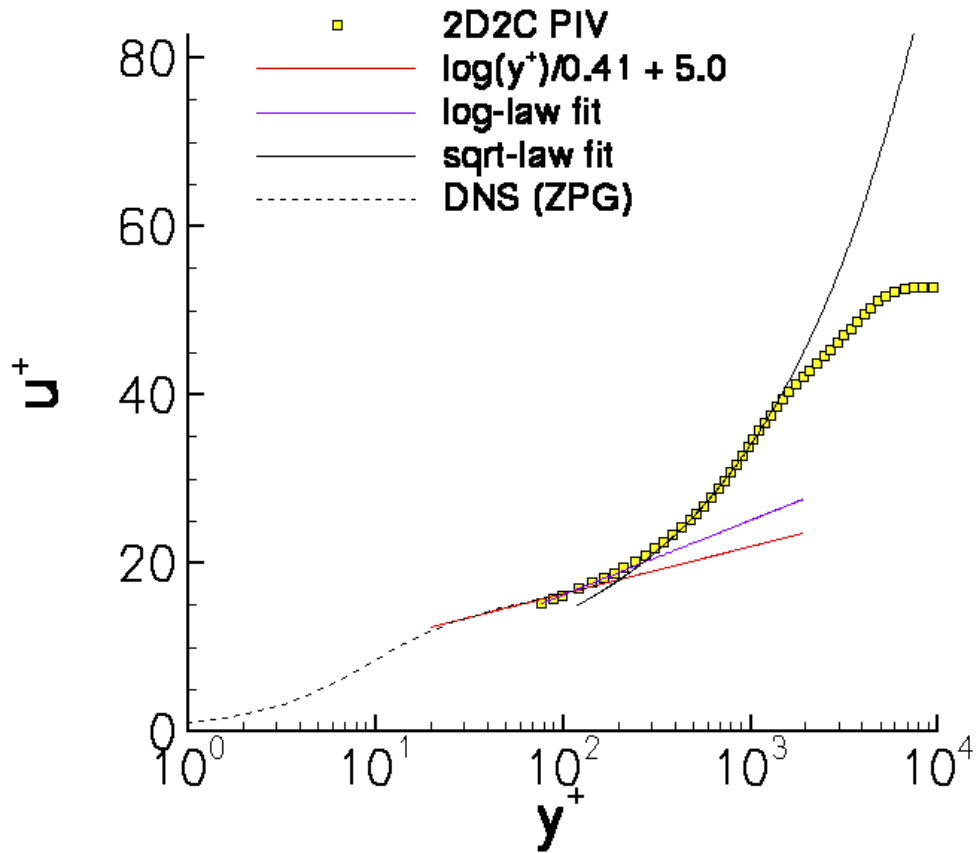
Mean velocity profiles



$$\Delta p_x^+ = dp^+/dx^+ = 0.039$$



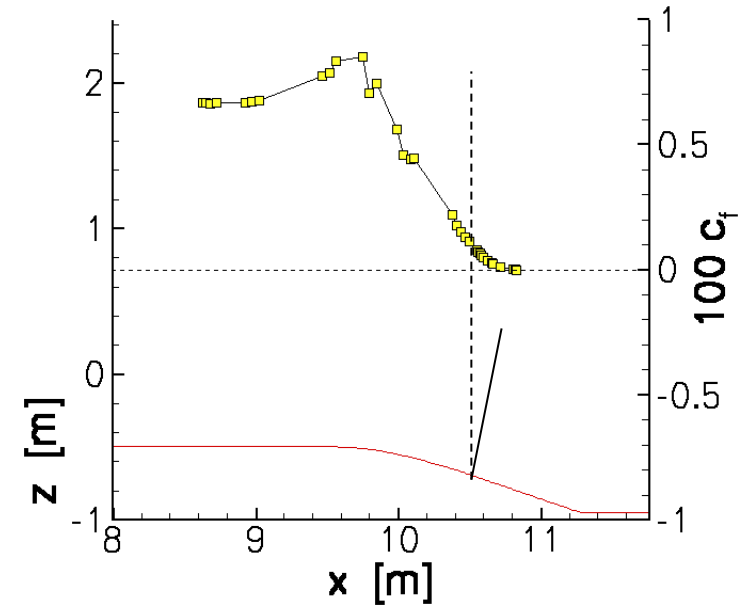
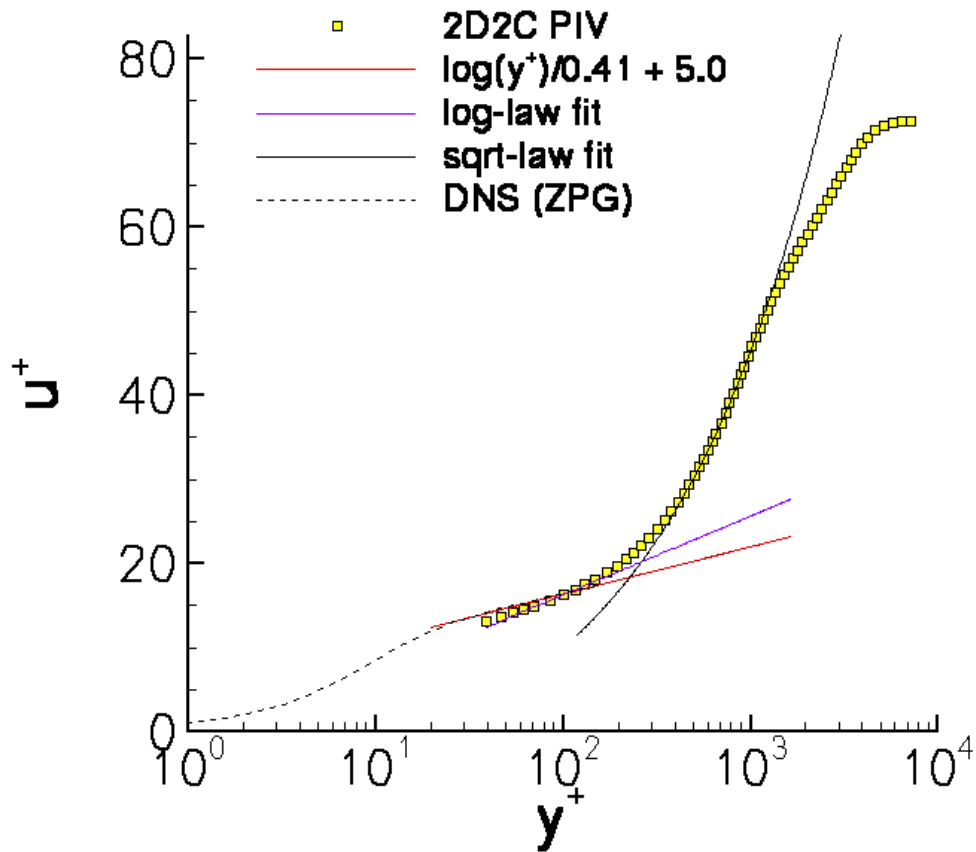
Mean velocity profiles



$$\Delta p_x^+ = dp^+/dx^+ = 0.064$$



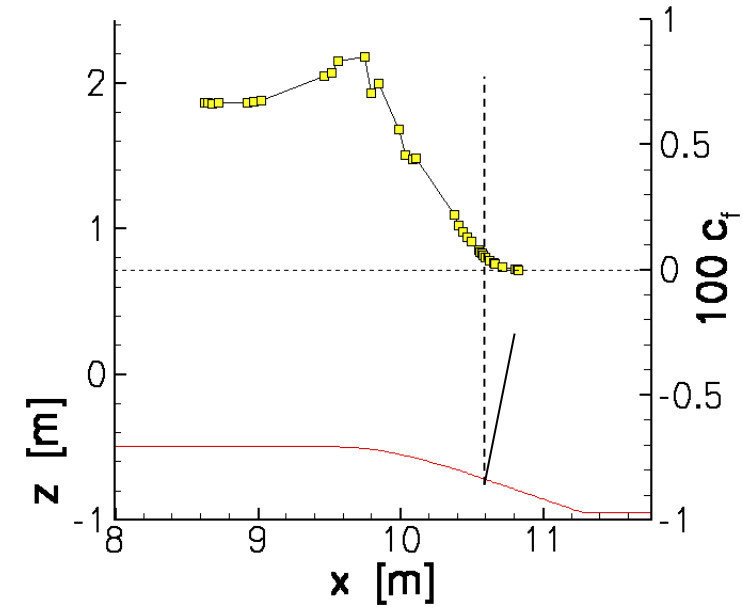
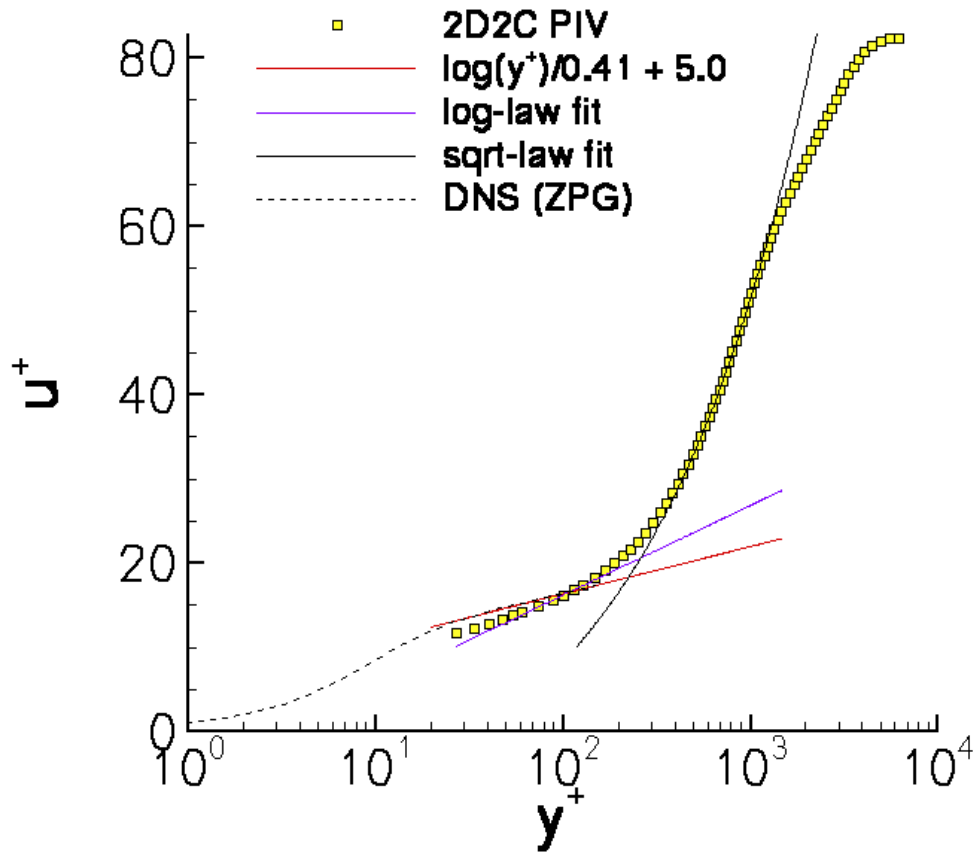
Mean velocity profiles



$$\Delta p_x^+ = dp^+/dx^+ = 0.140$$



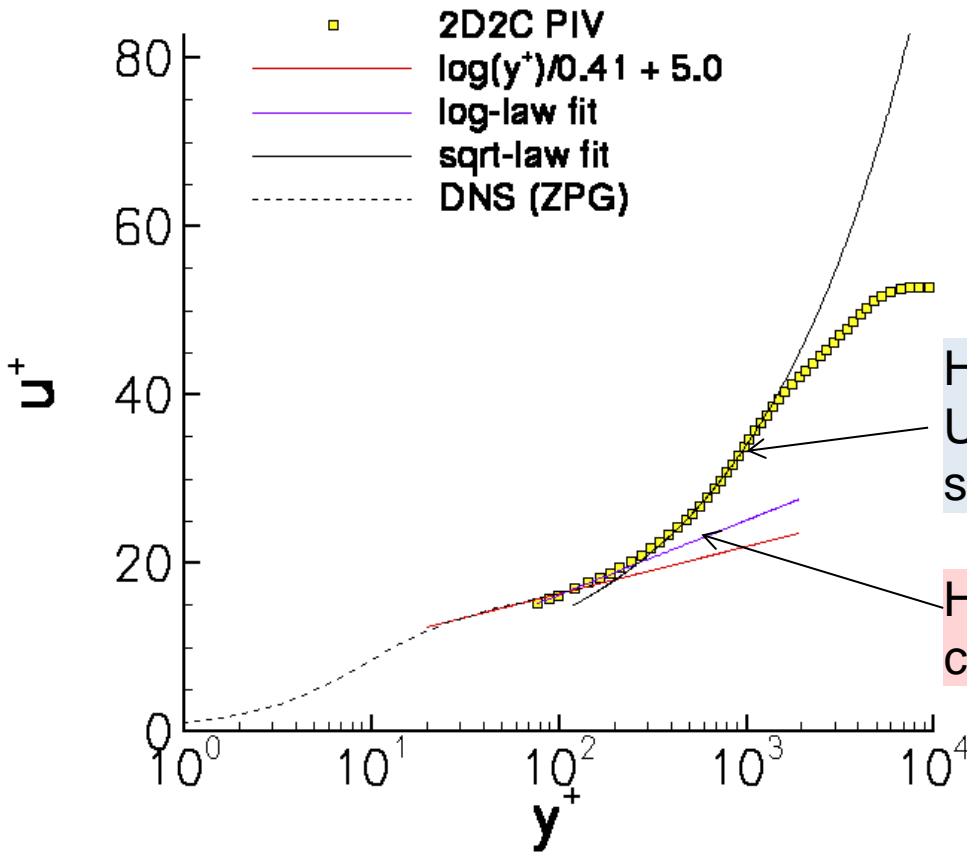
Mean velocity profiles



$$\Delta p_x^+ = dp^+/dx^+ = 0.180$$



Hypotheses for wall-law at adverse pressure gradients



Hypothesis #1:
Upward-turn of $U(y)$ above the log-law
sqrt-law $U \sim y^{1/2}$

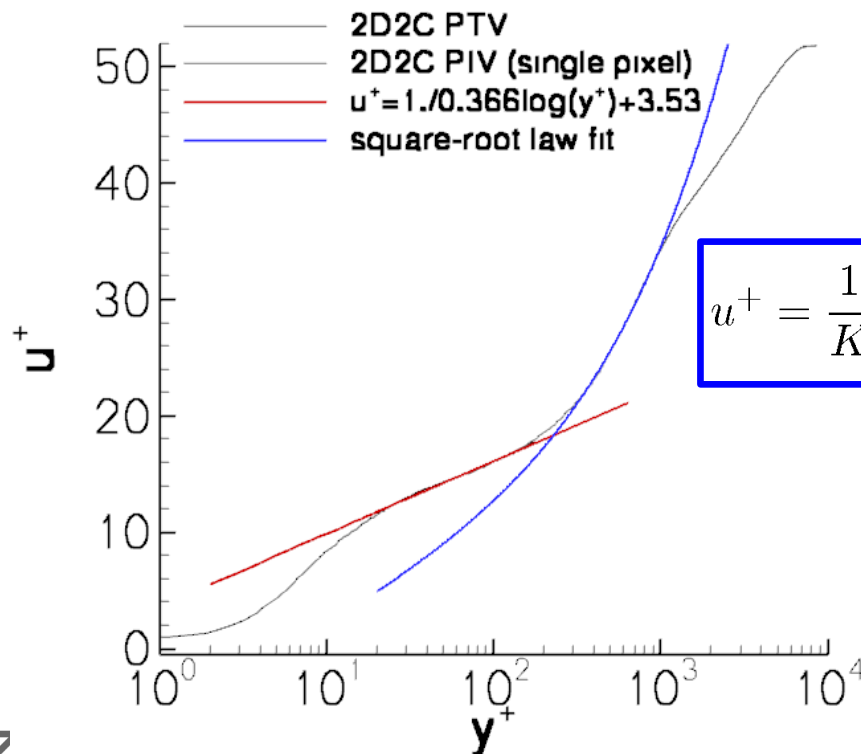
Hypothesis #2: Change of slope
coefficient of the log-law

$$\Delta p_x^+ = dp^+/dx^+ = 0.064$$



Hypothesis #1: Square-root law above the log-law

- Review of the literature of turbulent boundary layers at APG
- A square-root law is claimed by some authors in the literature
 - Szablewski (1952), Townsend (1960), Perry & Schofield (1973), van den Berg (1973), ...
- Sqrt-law was found in DFG RETTINA II experiment by DLR AS and UniBw München



$$u^+ = \frac{1}{K} \left[\log(y^+) + 2 \left(\sqrt{1 + \Delta p_x^+ y^+} - 1 \right) \right] + \tilde{B}$$

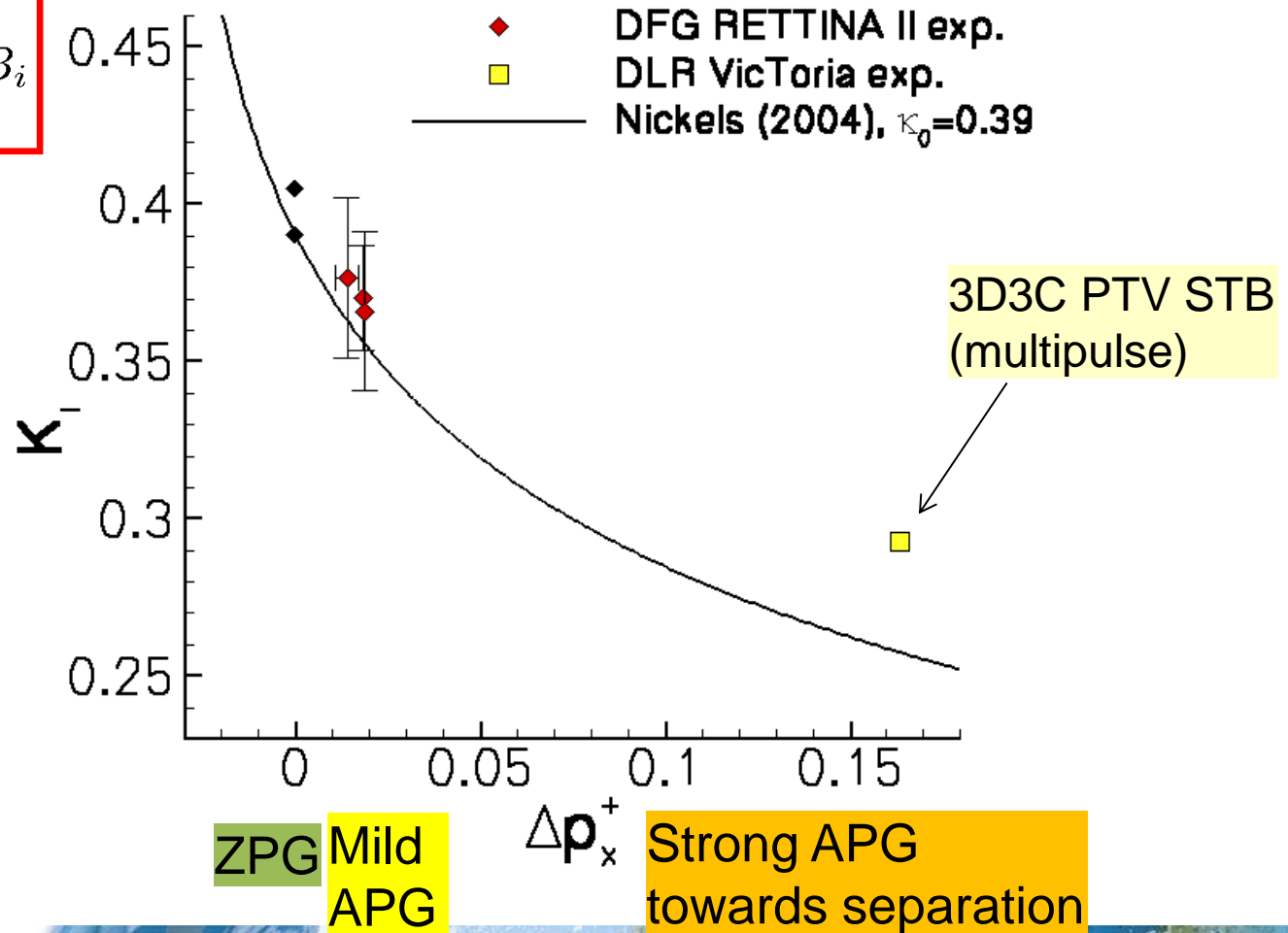
Dependent on dp/dx -parameter
Slope is increasing with increasing $(dp/dx)^+$



Hypothesis #2: Change of log-law slope coefficient

- Supported by data of DLR VicToria exp. and precursor RETTINA II experiment

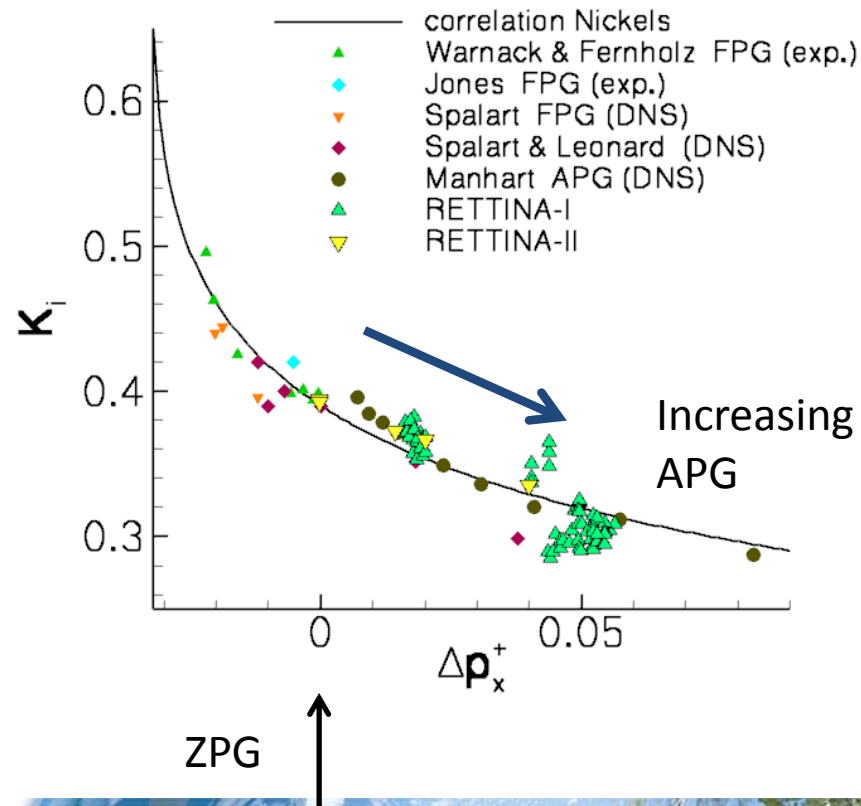
$$u_{\log}^+ = \frac{1}{K_i} \log(y^+) + B_i$$



Hypothesis #2: Change of log-law slope coefficient

- Slope coefficient K

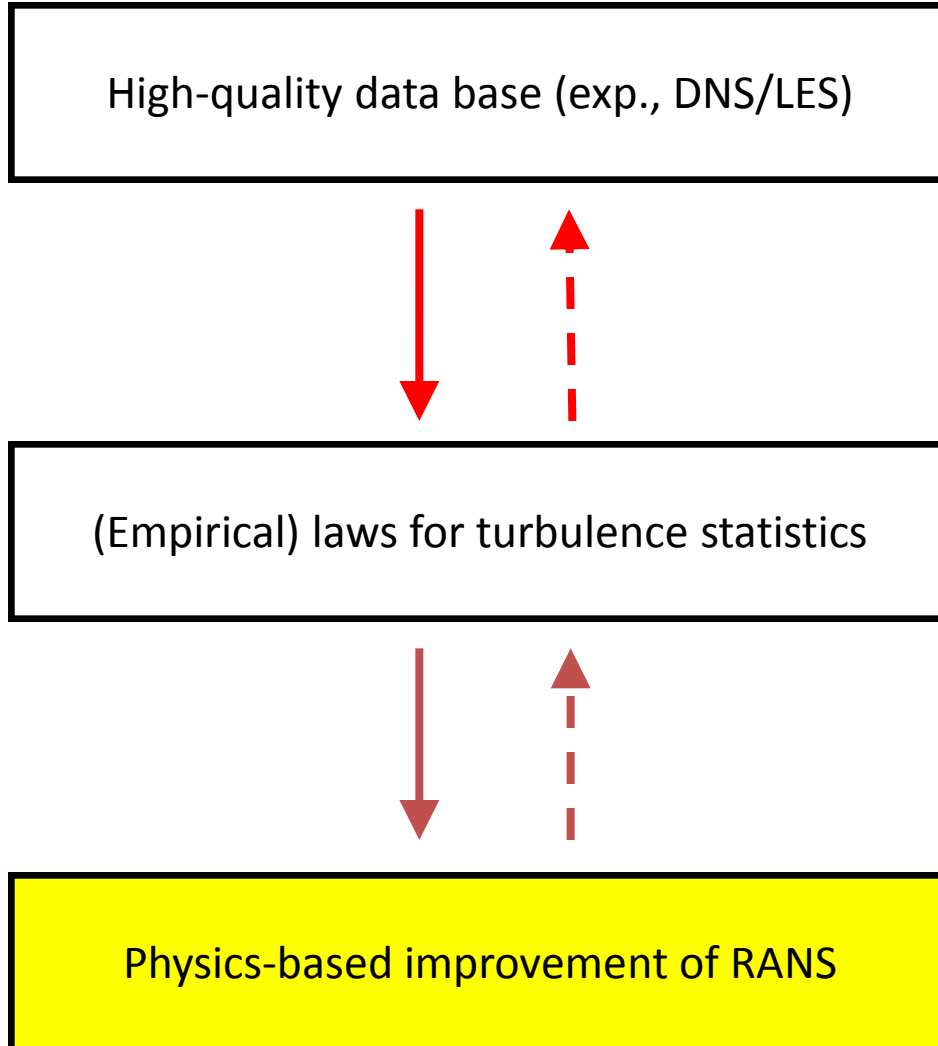
$$u_{\log}^+ = \frac{1}{K_i} \log(y^+) + B_i$$



Part III: Extension of RANS turbulence models for adverse pressure gradients



RANS model improvement



RANS model augmentation

- Transport equation for the mean velocity

$$\frac{\partial}{\partial x_j} (U_i U_j) + \frac{1}{\rho} \frac{\partial P}{\partial x_i} - \frac{\partial}{\partial x_j} \left(\nu \left(\frac{\partial U_i}{\partial x_j} + \frac{\partial U_j}{\partial x_i} \right) - \langle u'_i u'_j \rangle \right) = 0$$

- Transport equation for the Reynolds stress tensor

$$U_k \frac{\partial}{\partial x_k} \overline{u'_i u'_j} = \mathcal{P}_{ij} + D_{ij}^\nu + D_{ij}^t + D_{ij}^p + \Pi_{ij} - \epsilon_{ij}$$

- Transport equation for the dissipation rate ω

$$U_j \frac{\partial \omega}{\partial x_j} = P_\omega - \epsilon_\omega + D_\omega^\nu + D_\omega^t$$



RANS model augmentation

- Transport equation for the mean velocity

$$\frac{\partial}{\partial x_j} (U_i U_j) + \frac{1}{\rho} \frac{\partial P}{\partial x_i} - \frac{\partial}{\partial x_j} \left(\nu \left(\frac{\partial U_i}{\partial x_j} + \frac{\partial U_j}{\partial x_i} \right) - \langle u'_i u'_j \rangle \right) = 0$$

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- Transport equation for the dissipation rate ω

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RANS model augmentation

- Transport equation for the mean velocity

$$\frac{\partial}{\partial x_j} (U_i U_j) + \frac{1}{\rho} \frac{\partial P}{\partial x_i} - \frac{\partial}{\partial x_j} \left(\nu \left(\frac{\partial U_i}{\partial x_j} + \frac{\partial U_j}{\partial x_i} \right) - \langle u'_i u'_j \rangle \right) = 0$$

- Transport equation for the Reynolds stress tensor

$$U_k \frac{\partial}{\partial x_k} \overline{u'_i u'_j} = \mathcal{P}_{ij} + D_{ij}^\nu + D_{ij}^t + D_{ij}^p + \Pi_{ij} - \epsilon_{ij}$$

„Net effect“:
 The **sum** of all modelled terms determines $\langle u'_i u'_j \rangle$ and hence U

- Transport equation for the dissipation rate ω

$$U_j \frac{\partial \omega}{\partial x_j} = P_\omega - \epsilon_\omega + D_\omega^\nu + D_\omega^t$$



RANS model augmentation

- Transport equation for the mean velocity

$$\frac{\partial}{\partial x_j} (U_i U_j) + \frac{1}{\rho} \frac{\partial P}{\partial x_i} - \frac{\partial}{\partial x_j} \left(\nu \left(\frac{\partial U_i}{\partial x_j} + \frac{\partial U_j}{\partial x_i} \right) - \langle u'_i u'_j \rangle \right) = 0$$

- Transport equation for the Reynolds stress tensor

$$U_k \frac{\partial}{\partial x_k} \overline{u'_i u'_j} = \mathcal{P}_{ij} + D_{ij}^\nu + D_{ij}^t + D_{ij}^p + \Pi_{ij} - \epsilon_{ij}$$

The **sum** of all modelled terms determines $\langle u'_i u'_j \rangle$ and hence U

- Transport equation for the dissipation rate ω

$$U_j \frac{\partial \omega}{\partial x_j} = P_\omega - \epsilon_\omega + D_\omega^\nu + D_\omega^t$$



RANS model augmentation

- Transport equation for the mean velocity

$$\frac{\partial}{\partial x_j} (U_i U_j) + \frac{1}{\rho} \frac{\partial P}{\partial x_i} - \frac{\partial}{\partial x_j} \left(\nu \left(\frac{\partial U_i}{\partial x_j} + \frac{\partial U_j}{\partial x_i} \right) - \langle u'_i u'_j \rangle \right) = 0$$

- Transport equation for the Reynolds stress tensor

$$U_k \frac{\partial}{\partial x_k} \overline{u'_i u'_j} = \mathcal{P}_{ij} + D_{ij}^\nu + D_{ij}^t + D_{ij}^p + \Pi_{ij} - \epsilon_{ij}$$

- Transport equation for the dissipation rate ω

$$U_j \frac{\partial \omega}{\partial x_j} = P_\omega - \epsilon_\omega + D_\omega^\nu + D_\omega^t$$

Step #2: variation of kappa at APG

Step #1: sqrt-law for U(y) at APG



Step 1: Boundary layer approximation

Take into account only dominant terms and derivatives in wall-normal direction

$$U_j \frac{\partial \omega}{\partial x_j} = \gamma \left(\frac{\partial U_i}{\partial x_j} \right)^2 - \beta_\omega \omega^2 + \frac{\partial}{\partial x_j} \left[(\nu + \sigma_\omega \nu_t) \frac{\partial \omega}{\partial x_j} \right]$$

Non-dimensionalize (= scale) the equation to inner viscous units

$$-\frac{d}{dy^+} \left(\sigma_\omega \nu_t^+ \frac{d\omega^+}{dy^+} \right) = \gamma \left(\frac{du^+}{dy^+} \right)^2 - \beta_\omega (\omega^+)^2$$



Step 2: Substitute wall-law into the ω -equation

$$-\frac{d}{dy^+} \left(\sigma_\omega \nu_t^+ \frac{d\omega^+}{dy^+} \right) = \gamma \left(\frac{du^+}{dy^+} \right)^2 - \beta_\omega (\omega^+)^2$$

$$\Leftrightarrow \quad -D_{\omega,t}^+ = P_\omega^+ - \epsilon_\omega^+$$



Step 2: Substitute wall-law into the ω -equation

Following ideas by Rao & Hassan,
Catris & Aupoix

Part 2: Wall law for dU/dy and for turbulence statistics

$$-\frac{d}{dy^+} \left(\underbrace{\kappa y^+ \sqrt{1 + \alpha y^+}}_{\sigma_\omega \nu_t^+} \underbrace{\frac{\sqrt{1 + \alpha y^+}}{a_1 \kappa y^+}}_{\frac{du^+}{dy^+}} \right) = \gamma \left(\underbrace{\frac{\sqrt{1 + \alpha y^+}}{\kappa y^+}}_{\left(\frac{du^+}{dy^+}\right)^2} - \beta_\omega \underbrace{\frac{\sqrt{1 + \alpha y^+}}{a_1 \kappa y^+}}_{(\omega^+)^2} \right)$$

$$\Leftrightarrow -D_{\omega,t}^+ = P_\omega^+ - \epsilon_\omega^+$$



Step 2: Substitute wall-law into the ω -equation

$$\begin{array}{c}
 \boxed{\kappa y^+ \sqrt{1 + \alpha y^+}} \quad \boxed{\frac{\sqrt{1 + \alpha y^+}}{a_1 \kappa y^+}} \quad \boxed{\frac{\sqrt{1 + \alpha y^+}}{\kappa y^+}} \quad \boxed{\frac{\sqrt{1 + \alpha y^+}}{a_1 \kappa y^+}} \\
 \downarrow \quad \downarrow \quad \downarrow \quad \downarrow \\
 -\frac{d}{dy^+} \left(\sigma_\omega \nu_t^+ \frac{d\omega^+}{dy^+} \right) \neq \gamma \left(\frac{du^+}{dy^+} \right)^2 - \beta_\omega (\omega^+)^2
 \end{array}$$

$$\Leftrightarrow -D_{\omega,t}^+ \neq P_\omega^+ - \epsilon_\omega^+$$

$$\Leftrightarrow -\frac{\sigma_\omega}{a_1} \frac{1}{(y^+)^2} \neq \frac{1}{\kappa^2} \left(\gamma - \frac{\beta_\omega}{a_1^2} \right) \frac{1 + \alpha y^+}{(y^+)^2}$$



Step 3: Spatial discrepancy term

$$-\frac{d}{dy^+} \left(\boxed{\kappa y^+ \sqrt{1 + \alpha y^+}} \nu_t^+ \frac{d\omega^+}{dy^+} \right) = \gamma \left(\frac{du^+}{dy^+} \right)^2 - \beta_\omega (\omega^+)^2$$

$\frac{\sqrt{1 + \alpha y^+}}{a_1 \kappa y^+}$
 $\frac{\sqrt{1 + \alpha y^+}}{\kappa y^+}$
 $\frac{\sqrt{1 + \alpha y^+}}{a_1 \kappa y^+}$

$$\Leftrightarrow -D_{\omega,t}^+ = P_\omega^+ - \epsilon_\omega^+ + m^+(y^+, \Delta p_x^+)$$

$$\Leftrightarrow -\frac{\sigma_\omega}{a_1} \frac{1}{(y^+)^2} = \frac{1}{\kappa^2} \left(\gamma - \frac{\beta_\omega}{a_1^2} \right) \frac{1 + \alpha y^+}{(y^+)^2} + m^+(y^+, \Delta p_x^+)$$

This gives an analytical expression for m as a function of y^+ and the parameter $\alpha = \Delta p_x^+$

Spatial model discrepancy term m



Step 3: Spatial discrepancy term

Part 2: Wall law for dU/dy and for turbulence statistics

$$\begin{array}{c}
 \boxed{\kappa y^+ \sqrt{1 + \alpha y^+}} \quad \boxed{\frac{\sqrt{1 + \alpha y^+}}{a_1 \kappa y^+}} \quad \boxed{\frac{\sqrt{1 + \alpha y^+}}{\kappa y^+}} \quad \boxed{\frac{\sqrt{1 + \alpha y^+}}{a_1 \kappa y^+}} \\
 \swarrow \quad \searrow \quad \swarrow \quad \searrow \\
 -\frac{d}{dy^+} \left(\sigma_\omega \nu_t^+ \frac{d\omega^+}{dy^+} \right) = \gamma \left(\frac{du^+}{dy^+} \right)^2 - \beta_\omega (\omega^+)^2
 \end{array}$$

$$\Leftrightarrow -D_{\omega,t}^+ = P_\omega^+ - \epsilon_\omega^+ + m^+(y^+, \Delta p_x^+)$$

$$\Leftrightarrow -\frac{\sigma_\omega}{a_1} \frac{1}{(y^+)^2} = \frac{1}{\kappa^2} \left(\gamma - \frac{\beta_\omega}{a_1^2} \right) \frac{1 + \alpha y^+}{(y^+)^2} + m^+(y^+, \Delta p_x^+)$$

Inverse modelling: If we add the model discrepancy term m to the ω -equation, then the assumed wall-laws at APG solves the modified ω -equation



Step 4: Functional discrepancy term

- **Step 4: Express the discrepancy term as a function of admissible mean flow and turbulence quantities**

$$m^+(y^+) = \mathcal{M}^+ \left[\frac{du_{\text{law}}^+(y^+)}{dy^+}, \tau_{xy,\text{law}}^+(y^+), \omega_{\text{law}}^+(y^+); \Delta p_x^+ \right]$$

- For the turbulence model augmentation term to account for the sqrt-law at APG we choose the **pressure diffusion term by Rao & Hassan**

$$m = -D_{\omega,p} = -\frac{\omega}{k} \frac{\partial}{\partial y} \left[\sigma_{k,P} \nu_t \frac{-\overline{u'v'}}{k} \frac{1}{\rho} \frac{\partial P}{\partial x} \right]$$



RANS model augmentation. Summary of step #1

- Transport equation for the mean velocity

$$\frac{\partial}{\partial x_j} (U_i U_j) + \frac{1}{\rho} \frac{\partial P}{\partial x_i} - \frac{\partial}{\partial x_j} \left(\nu \left(\frac{\partial U_i}{\partial x_j} + \frac{\partial U_j}{\partial x_i} \right) - \langle u'_i u'_j \rangle \right) = 0$$

- Transport equation for the Reynolds stress tensor

$$U_k \frac{\partial}{\partial x_k} \overline{u'_i u'_j} = \mathcal{P}_{ij} + D_{ij}^\nu + D_{ij}^t + D_{ij}^p + \Pi_{ij} - \epsilon_{ij}$$

- Transport equation for the dissipation rate ω

$$U_j \frac{\partial \omega}{\partial x_j} = P_\omega - \epsilon_\omega + D_\omega^\nu + D_\omega^t + D_\omega^p$$

Modification #1 to account for sqrt-law at APG



Idea #2: RANS model coefficients for log-law slope sensitized to pressure gradient parameter Δp_x^+

$$U_j \frac{\partial \omega}{\partial x_j} = \gamma \left(\frac{\partial U_i}{\partial x_j} \right)^2 - \beta_\omega \omega^2 + \frac{\partial}{\partial x_j} \left[(\nu + \sigma_\omega \nu_t) \frac{\partial \omega}{\partial x_j} \right]$$

Coefficient γ controls the slope of the log-law

Standard calibration is for ZPG
 $\kappa=0.41 = \text{const}$

$$\gamma = \frac{\beta_\omega}{\beta_k} - \frac{\sigma_\omega \kappa^2}{\sqrt{\beta_k}}$$



Idea #2: RANS model coefficients for log-law slope sensitized to pressure gradient parameter Δp_x^+

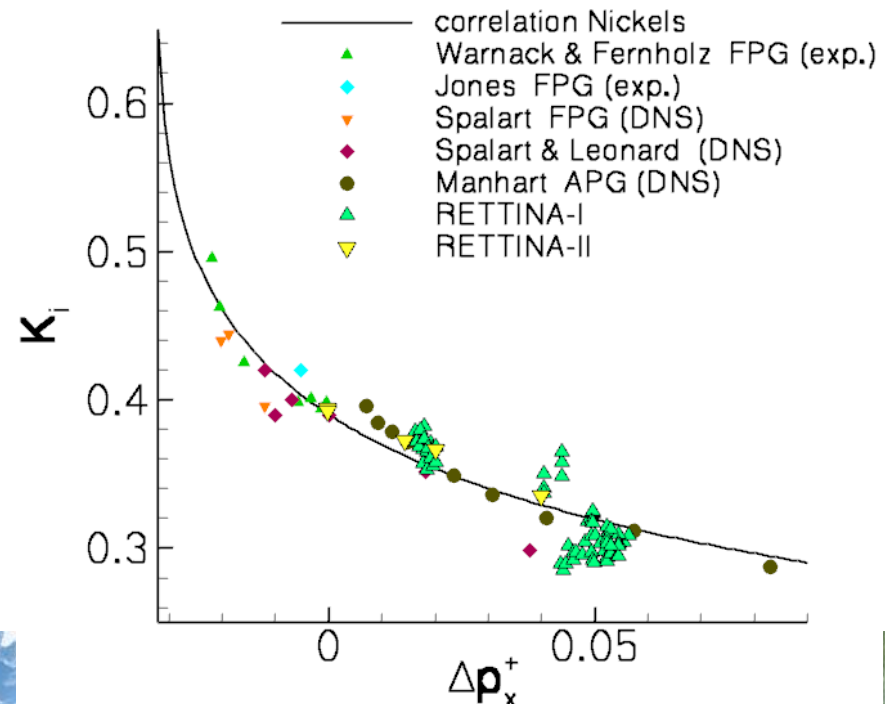
$$U_j \frac{\partial \omega}{\partial x_j} = \gamma \left(\frac{\partial U_i}{\partial x_j} \right)^2 - \beta_\omega \omega^2 + \frac{\partial}{\partial x_j} \left[(\nu + \sigma_\omega \nu_t) \frac{\partial \omega}{\partial x_j} \right]$$

Coefficient γ controls the slope of the log-law

Modification: $\kappa = \kappa(\Delta p_x^+)$

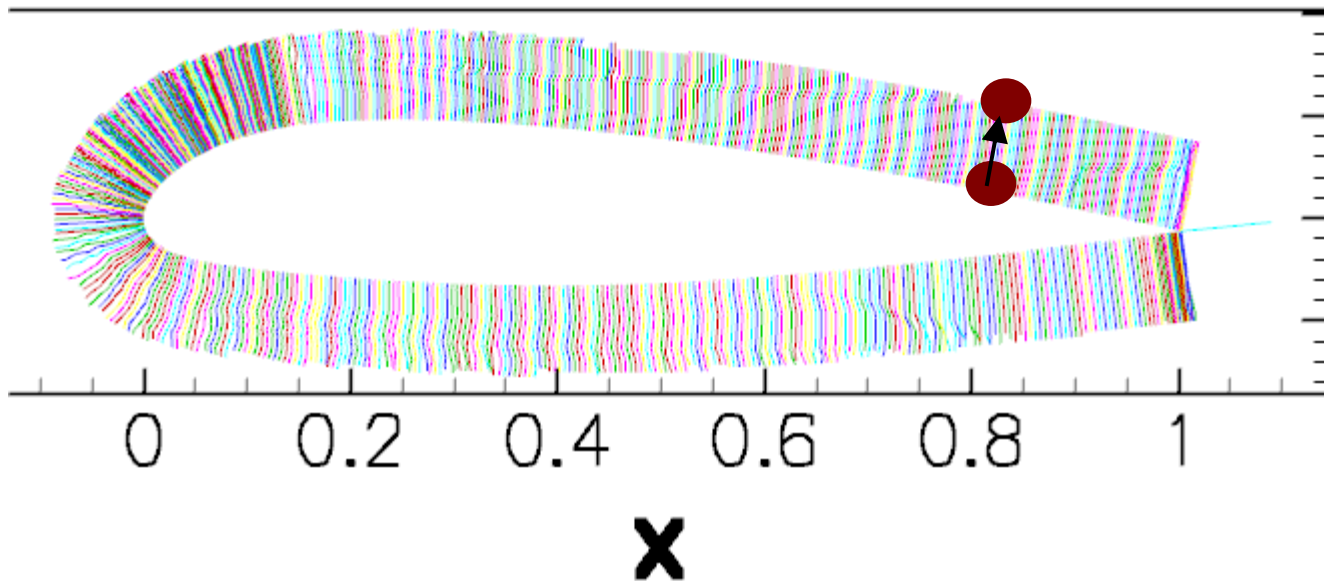
$$\gamma = \frac{\beta_\omega}{\beta_k} - \frac{\sigma_\omega \kappa^2}{\sqrt{\beta_k}}$$

Coefficients of the turbulence model become functions of the local flow conditions



Data structure of wall-normal lines for Δp_x^+

- Extension of unstructured flow solver DLR TAU code
 - Data structure for wall-normal lines
 - Method to determine δ_{99} , δ^* , θ , H_{12}



Field point



Surface point

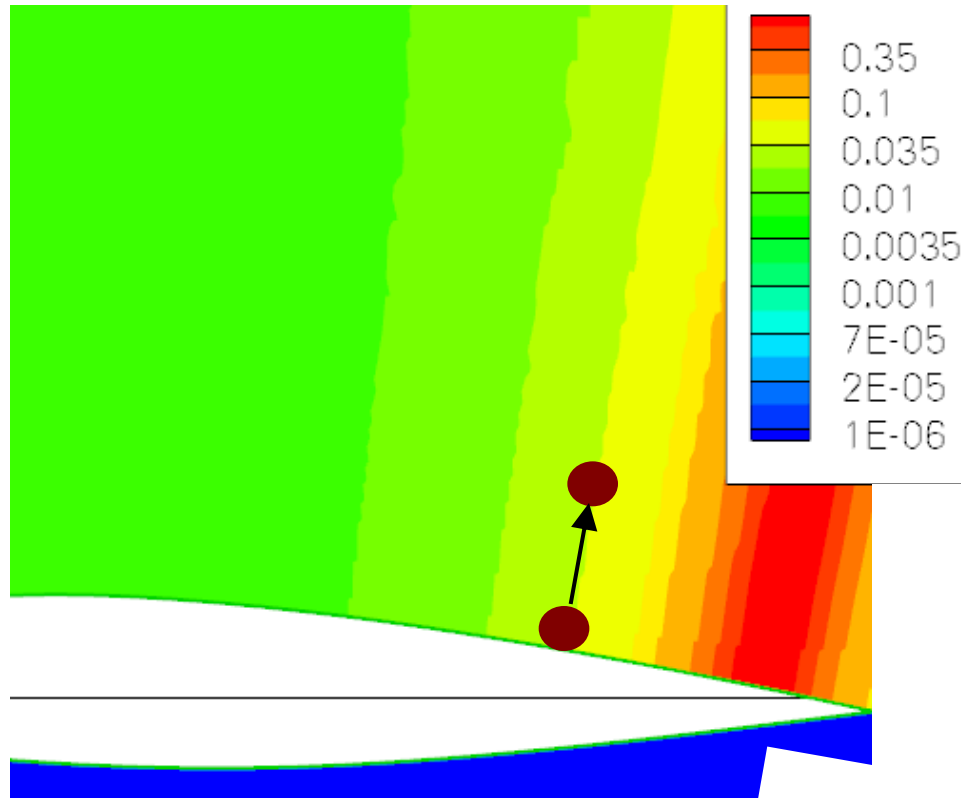
Δp_x^+ from dp/dx
and u_τ

δ_{99} , δ^* , θ , H_{12}



RANS model sensitized to pressure gradient Δp_x^+

Field distribution of Δp_x^+



Map to corresponding field points

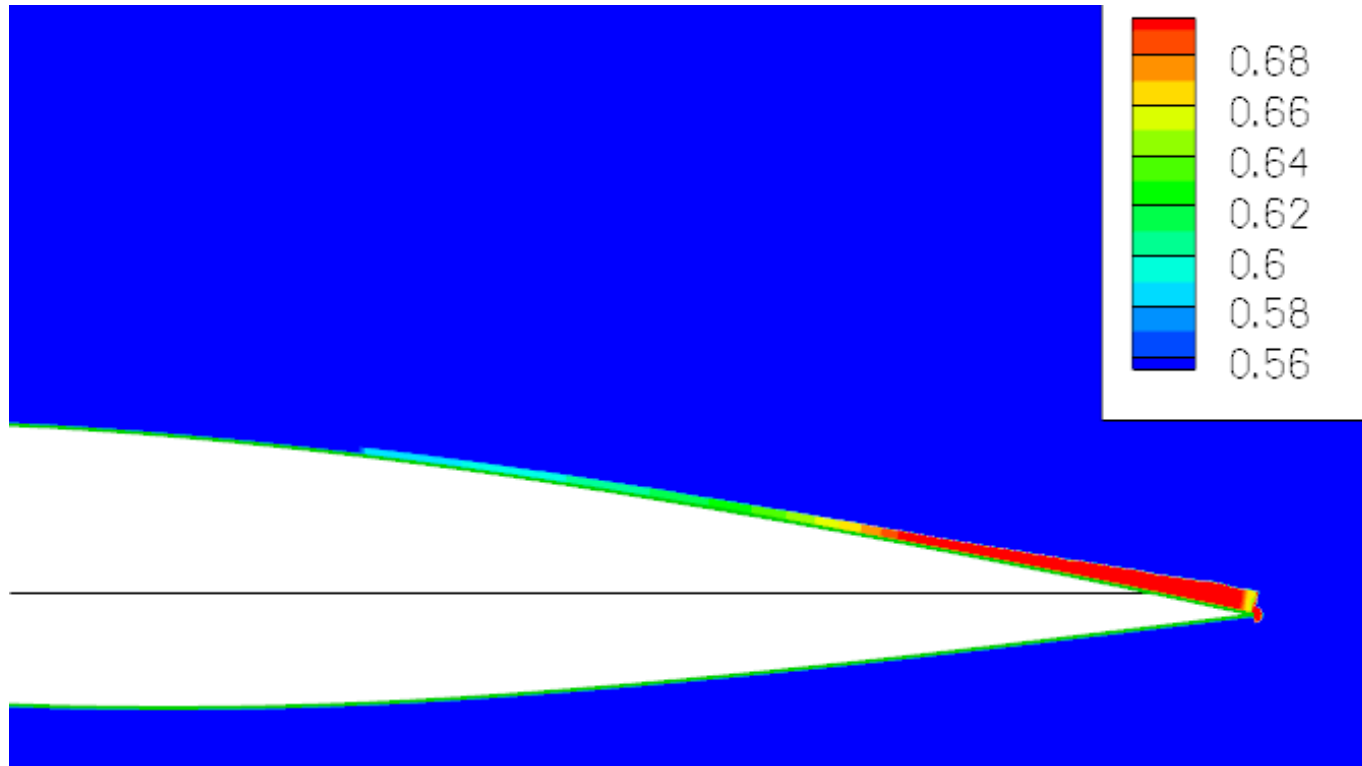


Surface quantities Δp_x^+
from dp/dx and u_τ

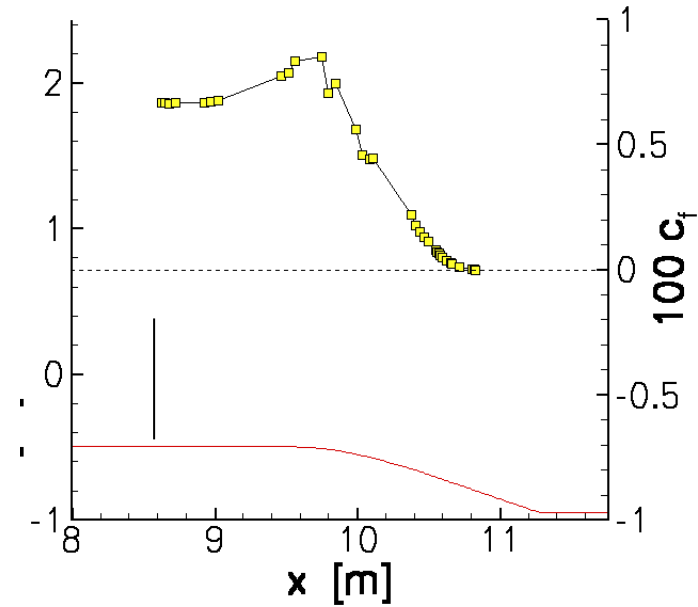
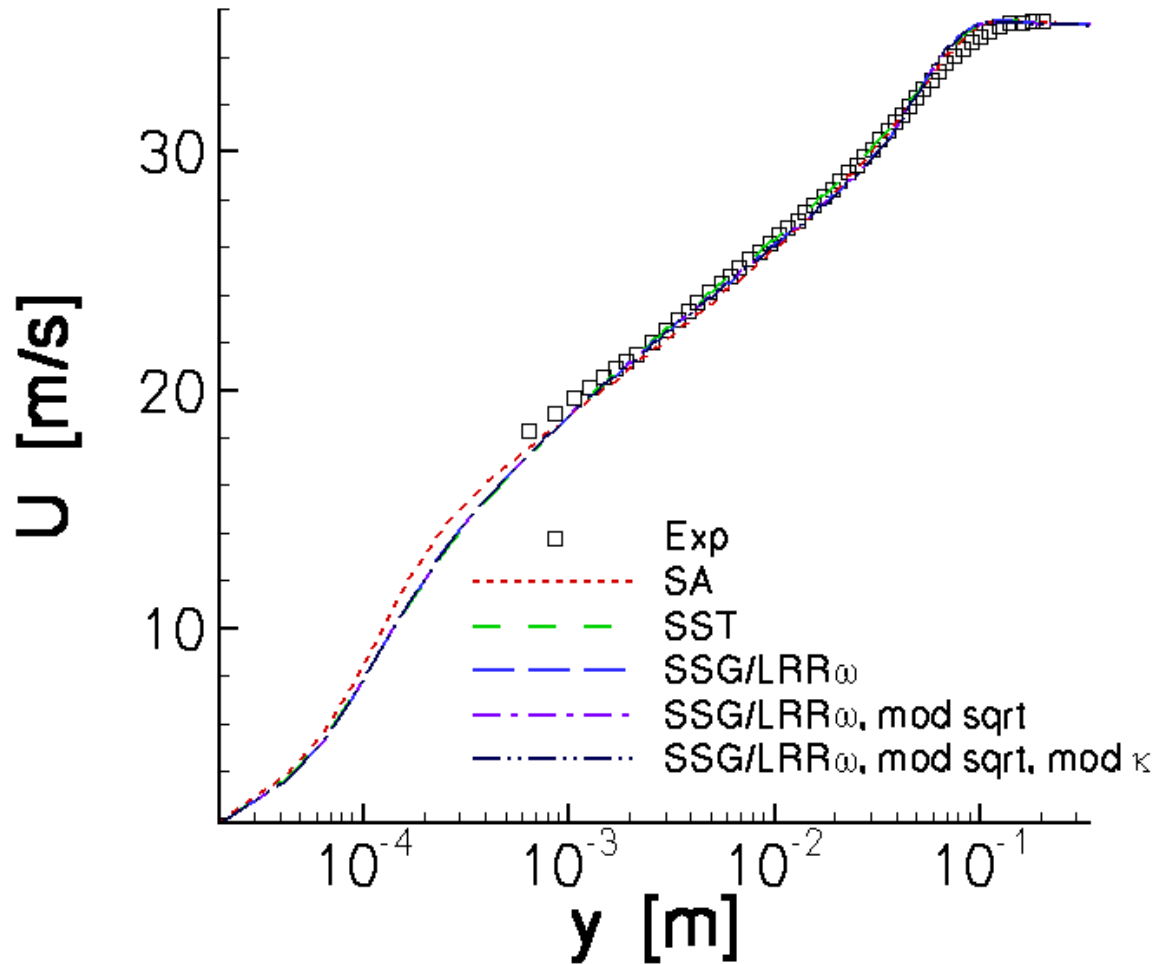


RANS model sensitized to pressure gradient Δp_x^+

RANS model coefficient γ
becomes a function of Δp_x^+



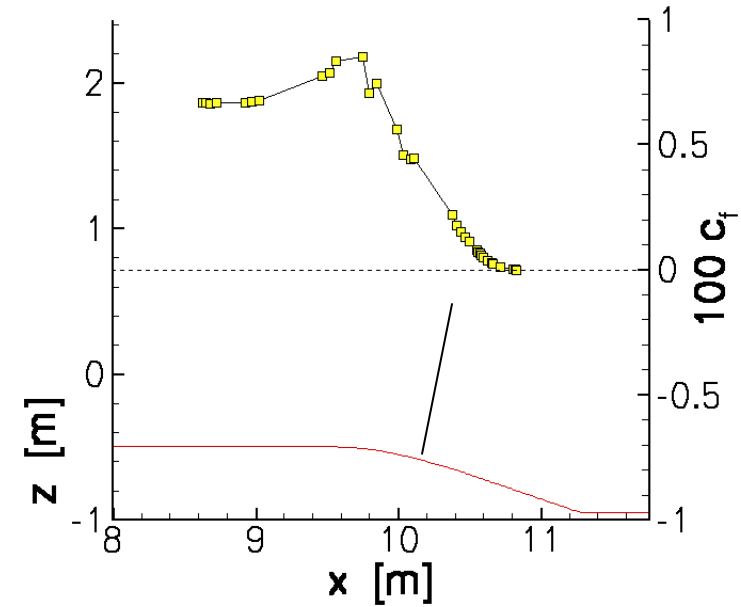
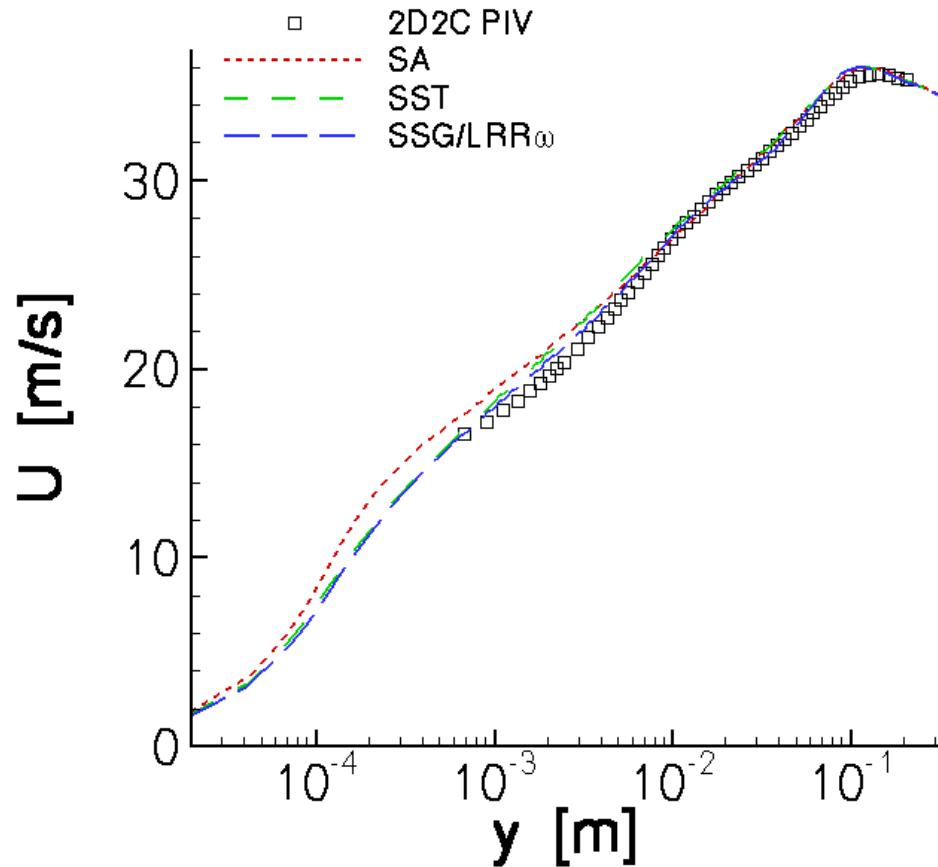
Calibration of RSM for VicToria experiment



$$\Delta p_x^+ = dp^+/dx^+ = 0$$



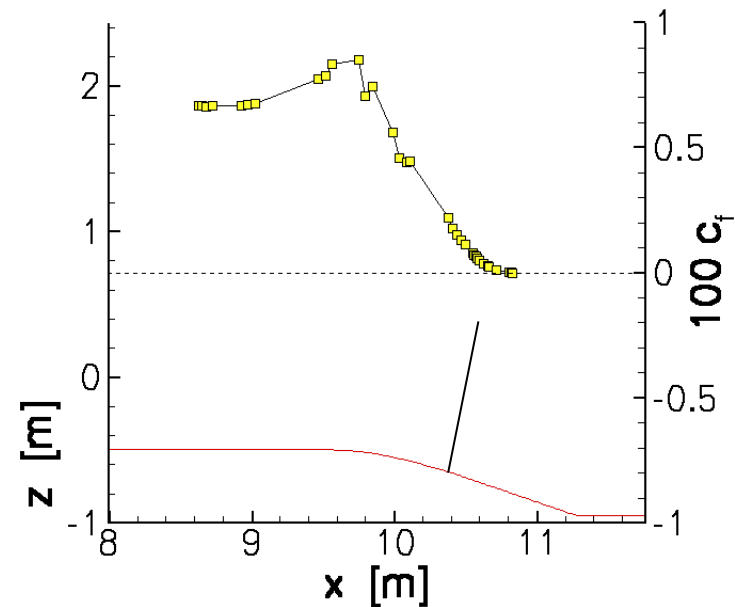
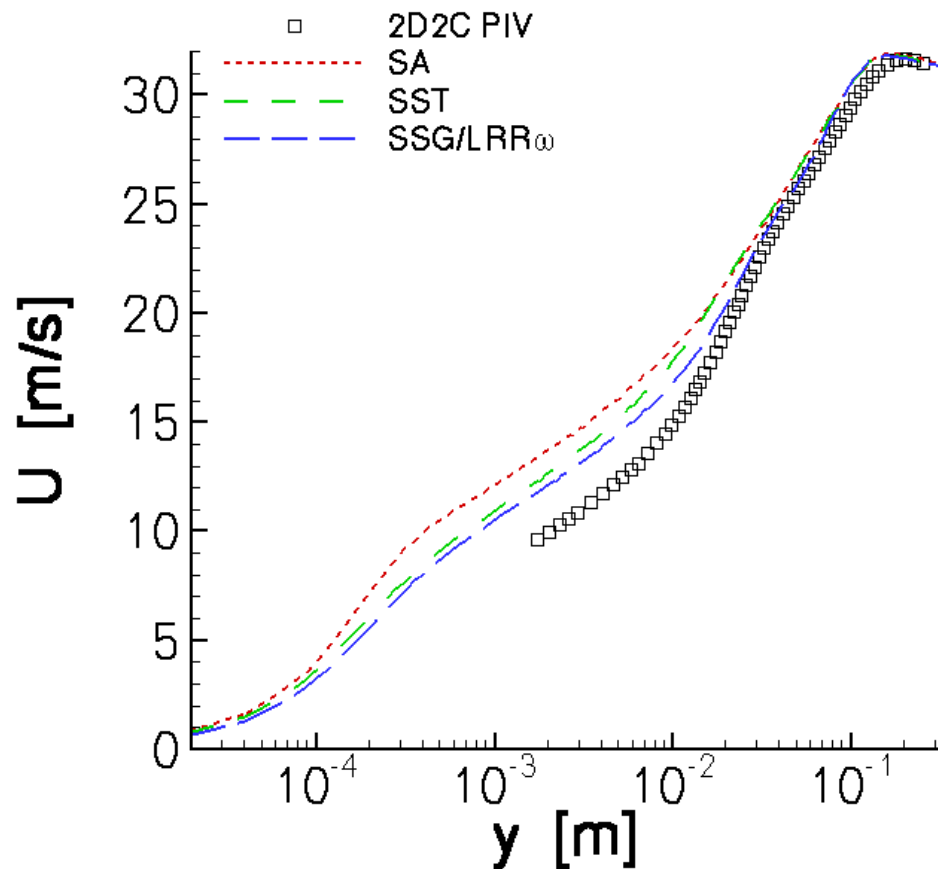
Calibration of RSM for VicToria experiment



$$\Delta p_x^+ = dp^+/dx^+ = 0.012$$



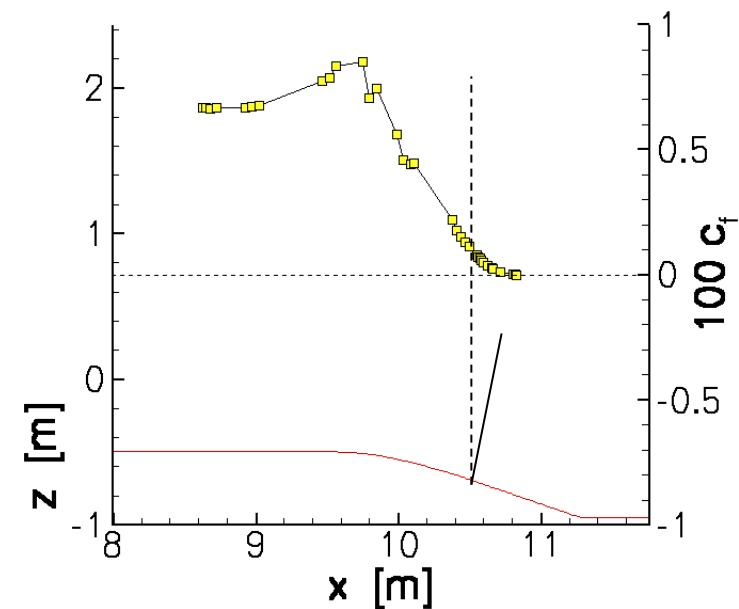
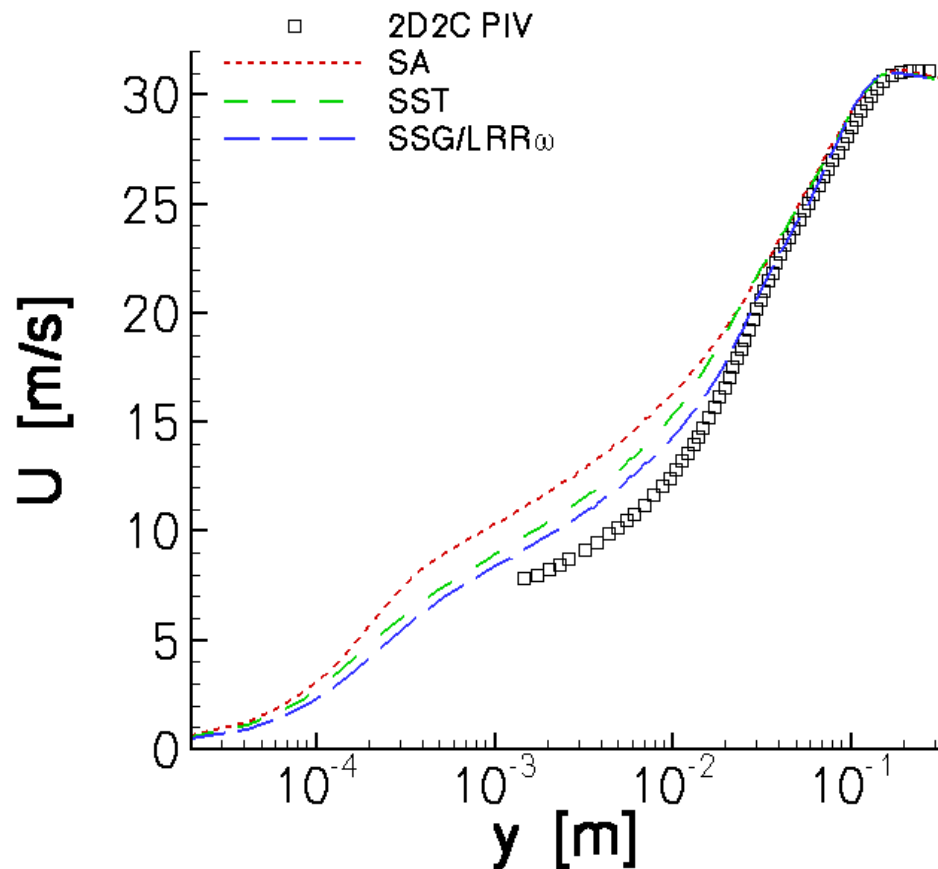
Calibration of RSM for VicToria experiment



$$\Delta p_x^+ = dp^+/dx^+ = 0.053$$



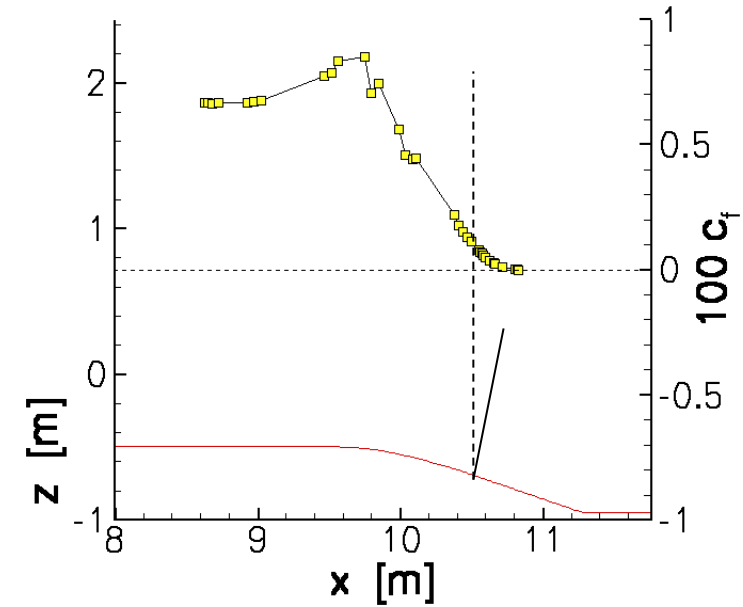
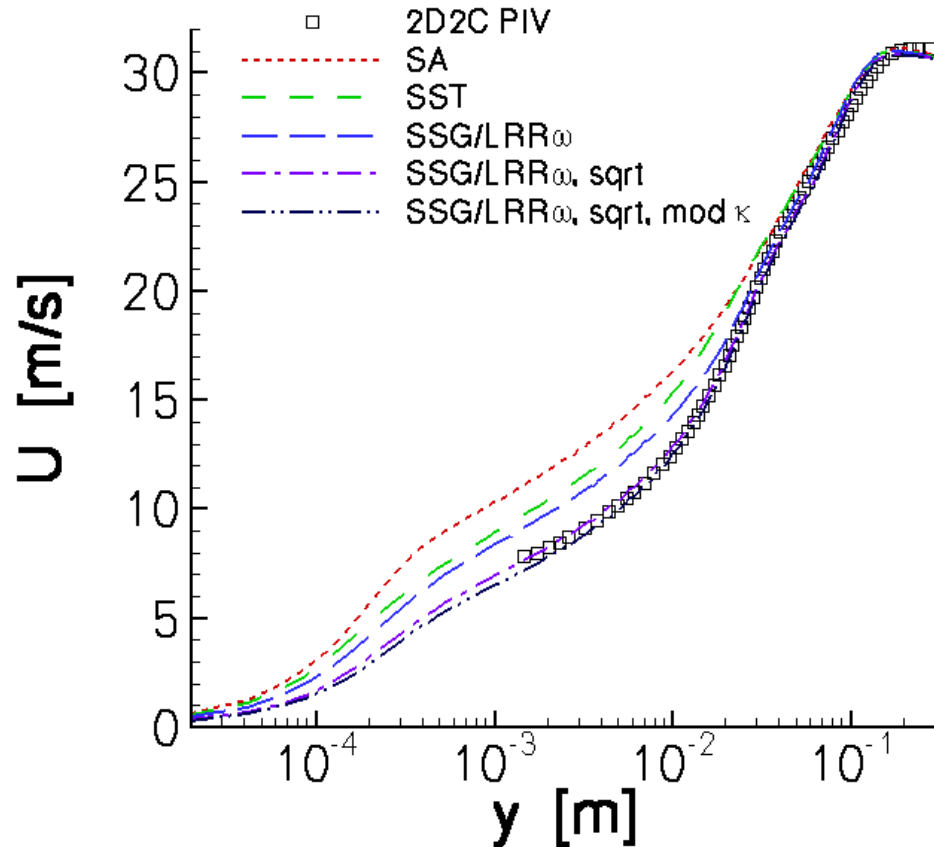
Calibration of RSM for VicToria experiment



$$\Delta p_x^+ = dp^+/dx^+ = 0.076$$



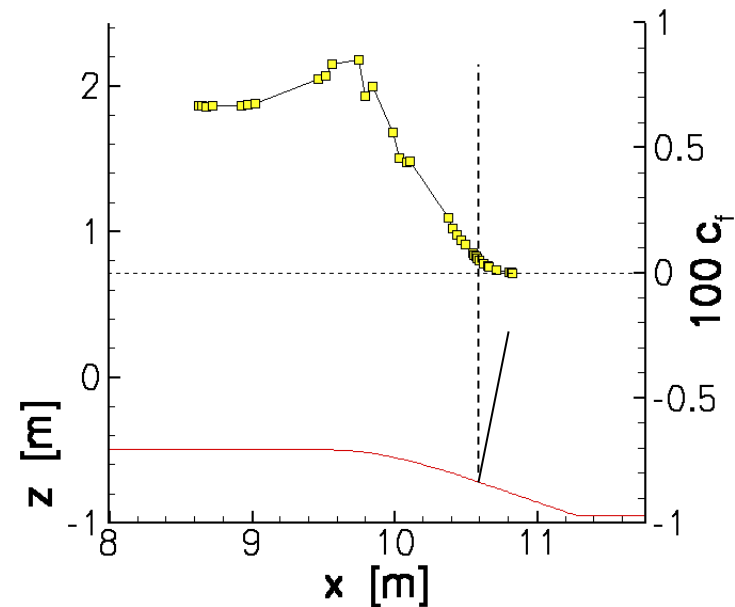
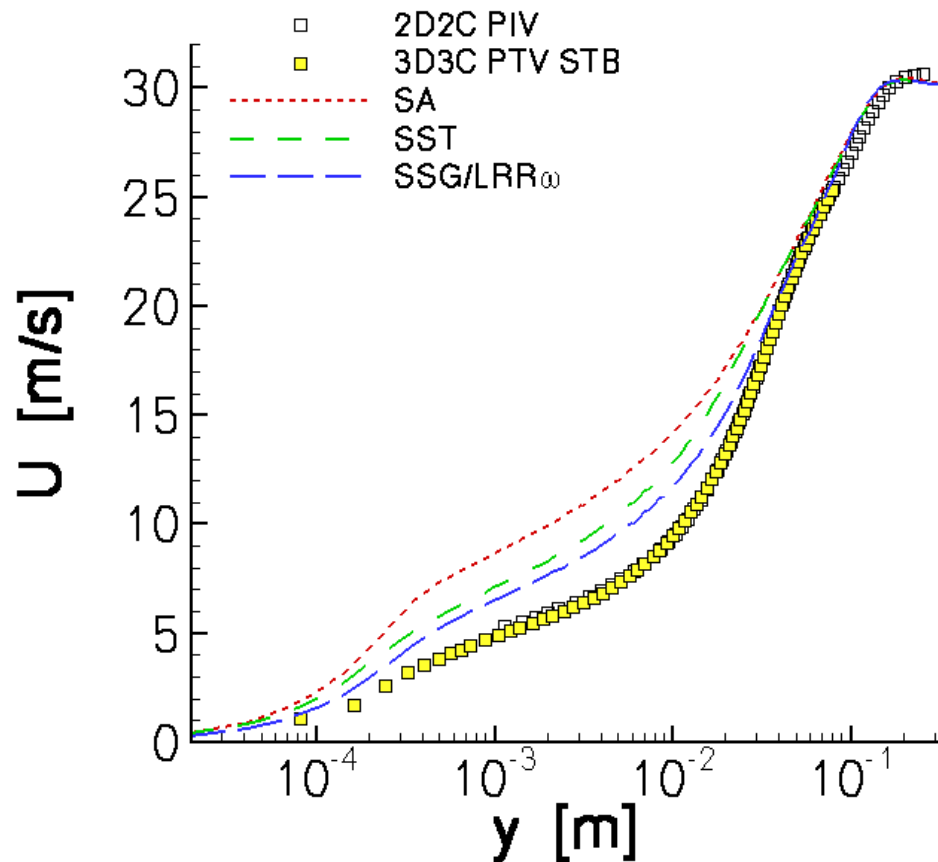
Calibration of RSM for VicToria experiment



$$\Delta p_x^+ = dp^+/dx^+ = 0.076$$



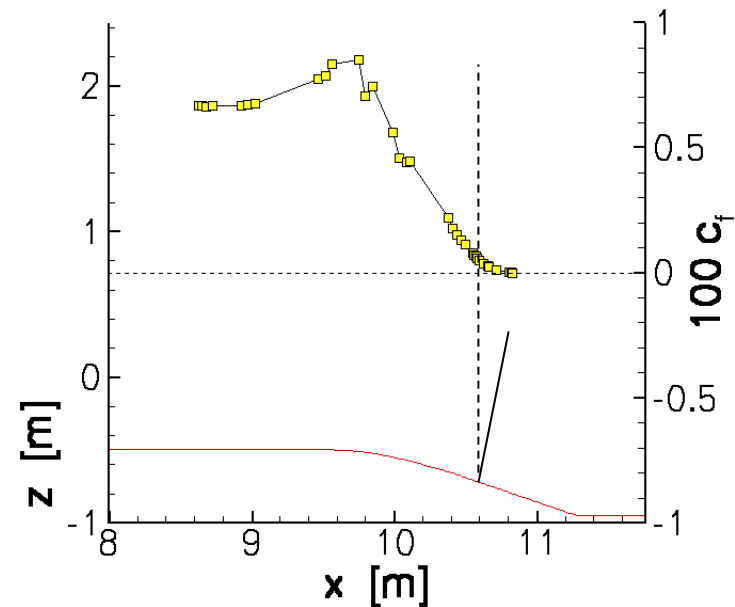
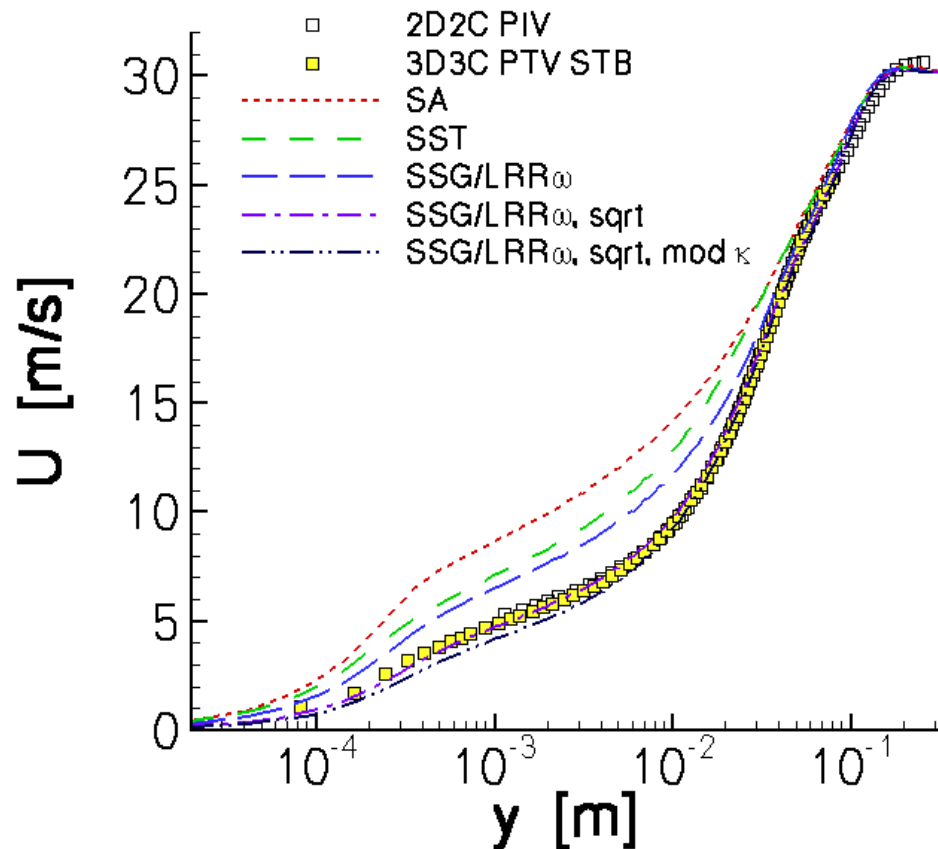
Calibration of RSM for VicToria experiment



$$\Delta p_x^+ = dp^+/dx^+ = 0.140$$



Calibration of RSM for VicToria experiment



$$\Delta p_x^+ = dp^+/dx^+ = 0.140$$



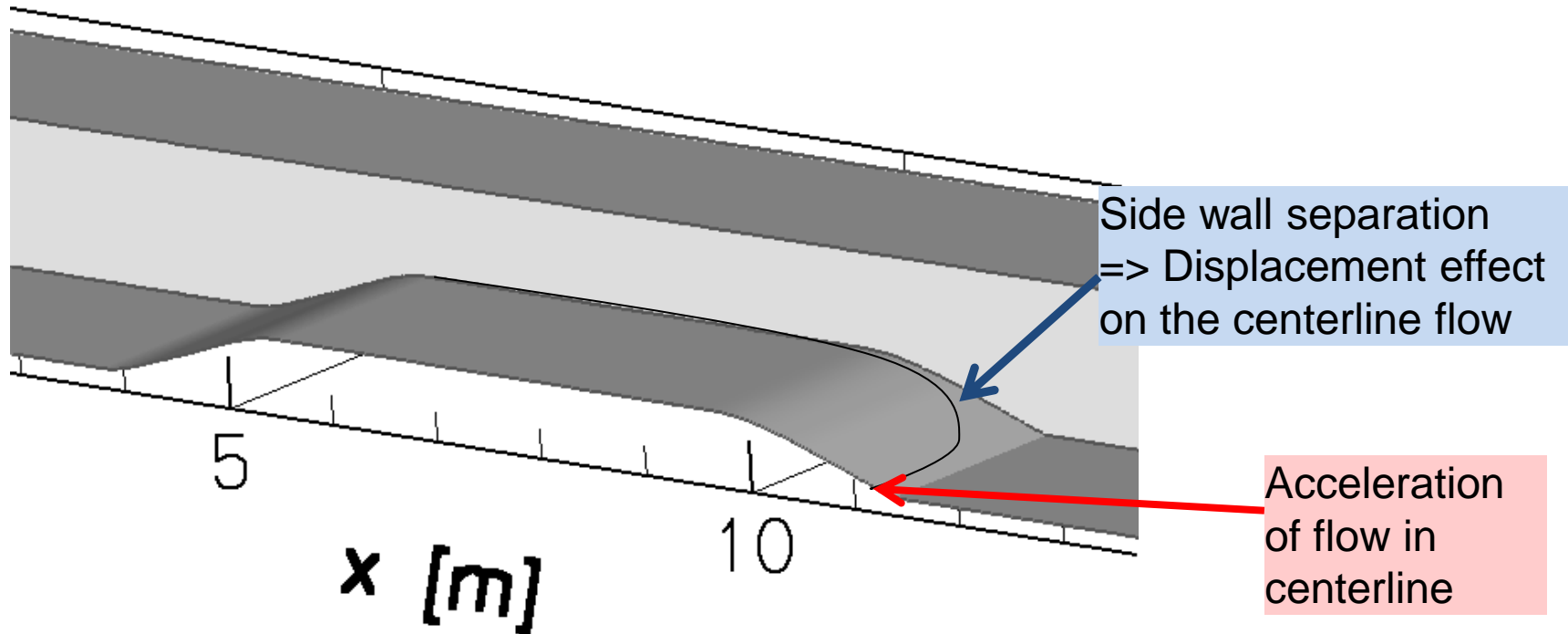
Outlook: Next steps #1

3D effects of side walls and their measurement



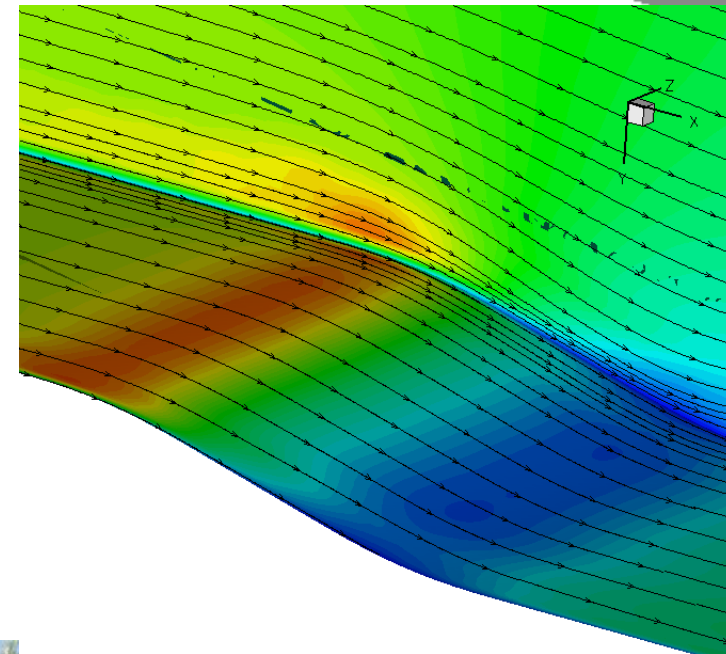
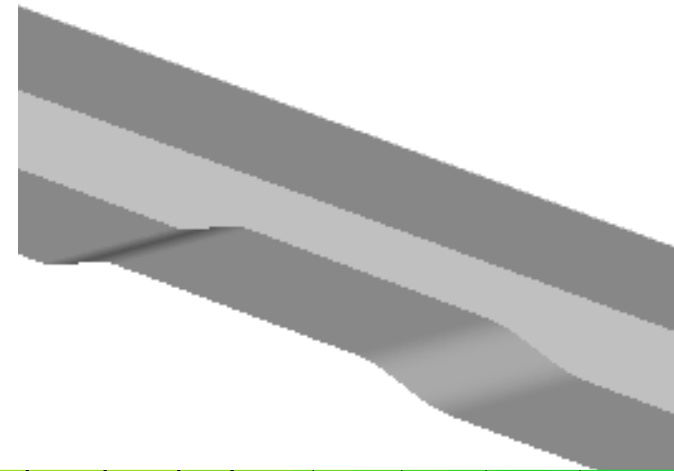
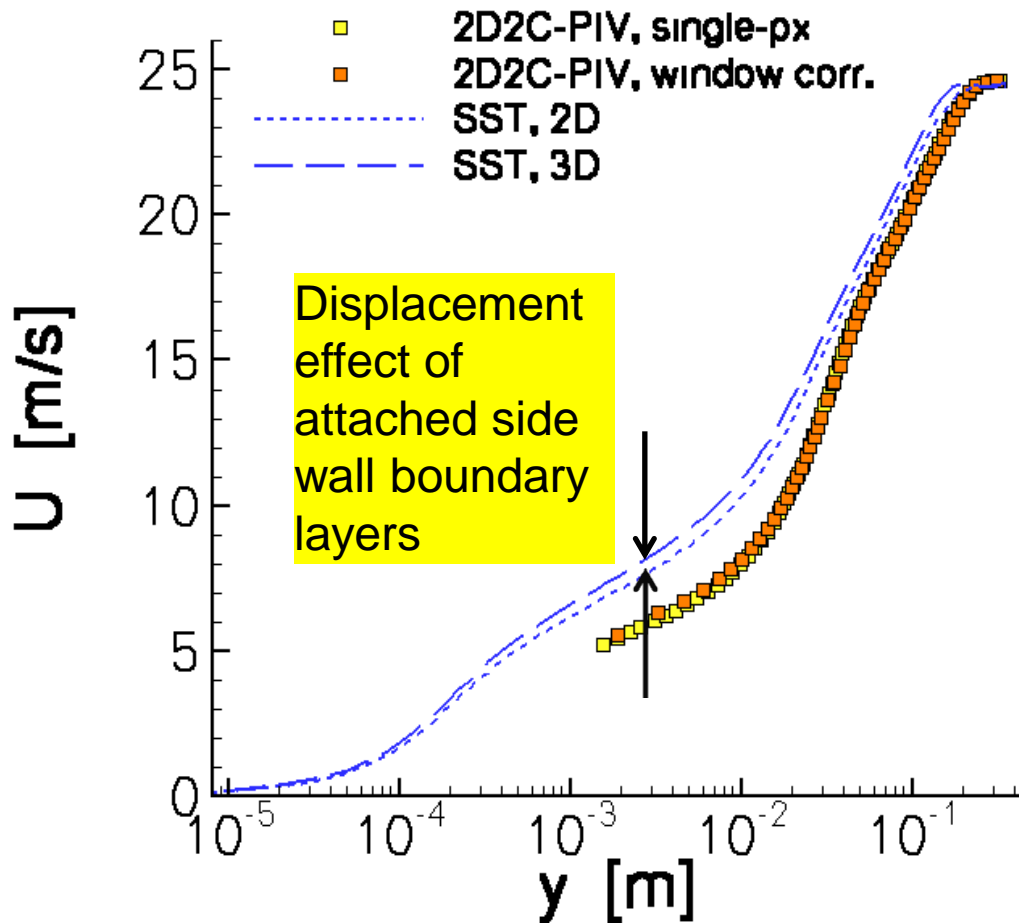
Need measurement of 3D effects (side wall separation)

- Need qualitative and quantitative information on 3D flow field
 - **Oil flow picture of surface streamlines over the entire span (E. Schülein from AS-HGK)**



Estimate of side wall effects from RETTINA II exp

- Centerline position at mild APG, albeit side wall flow remains attached (no corner flow separation)



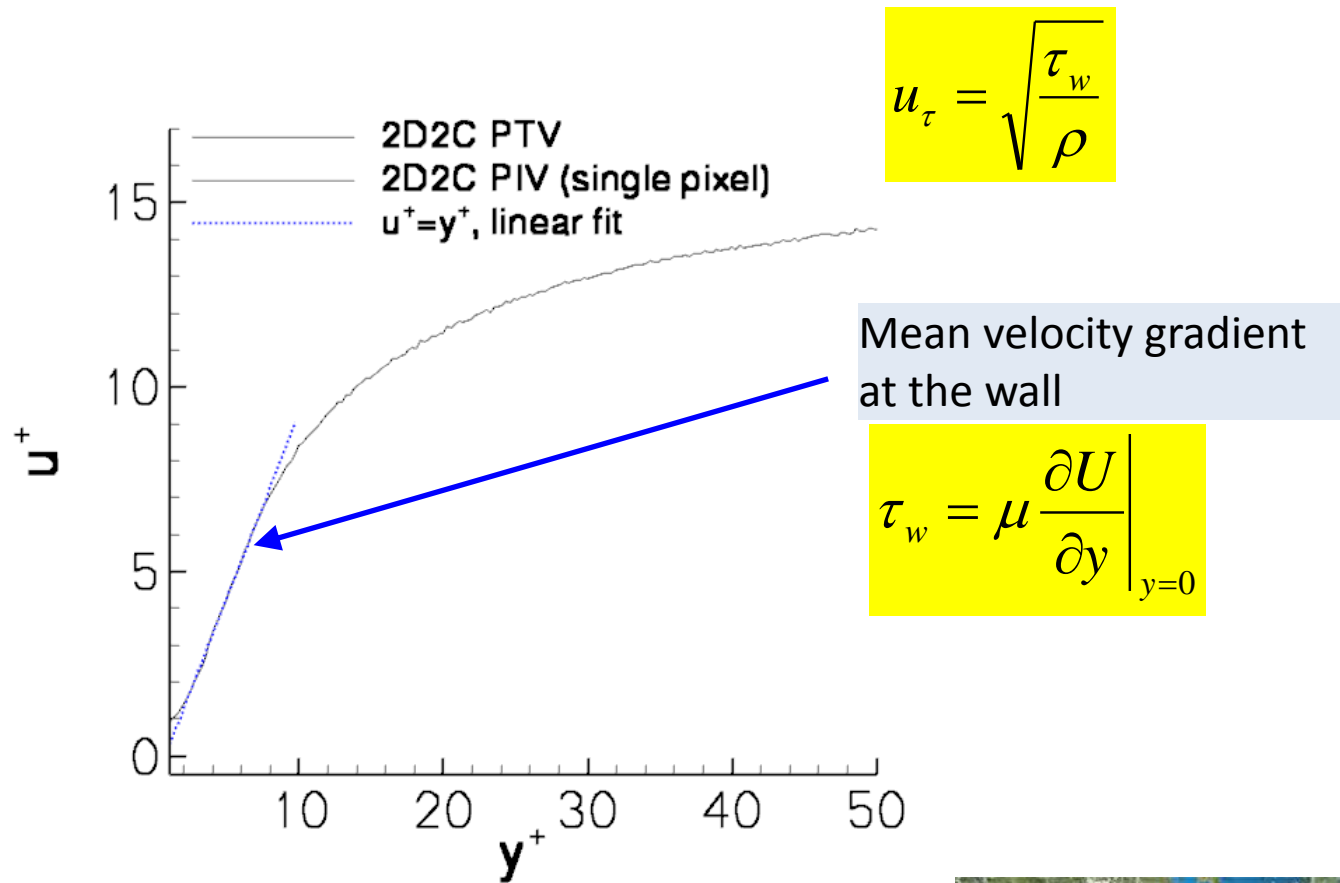
Outlook: Next steps #2

Measurement of wall shear stress

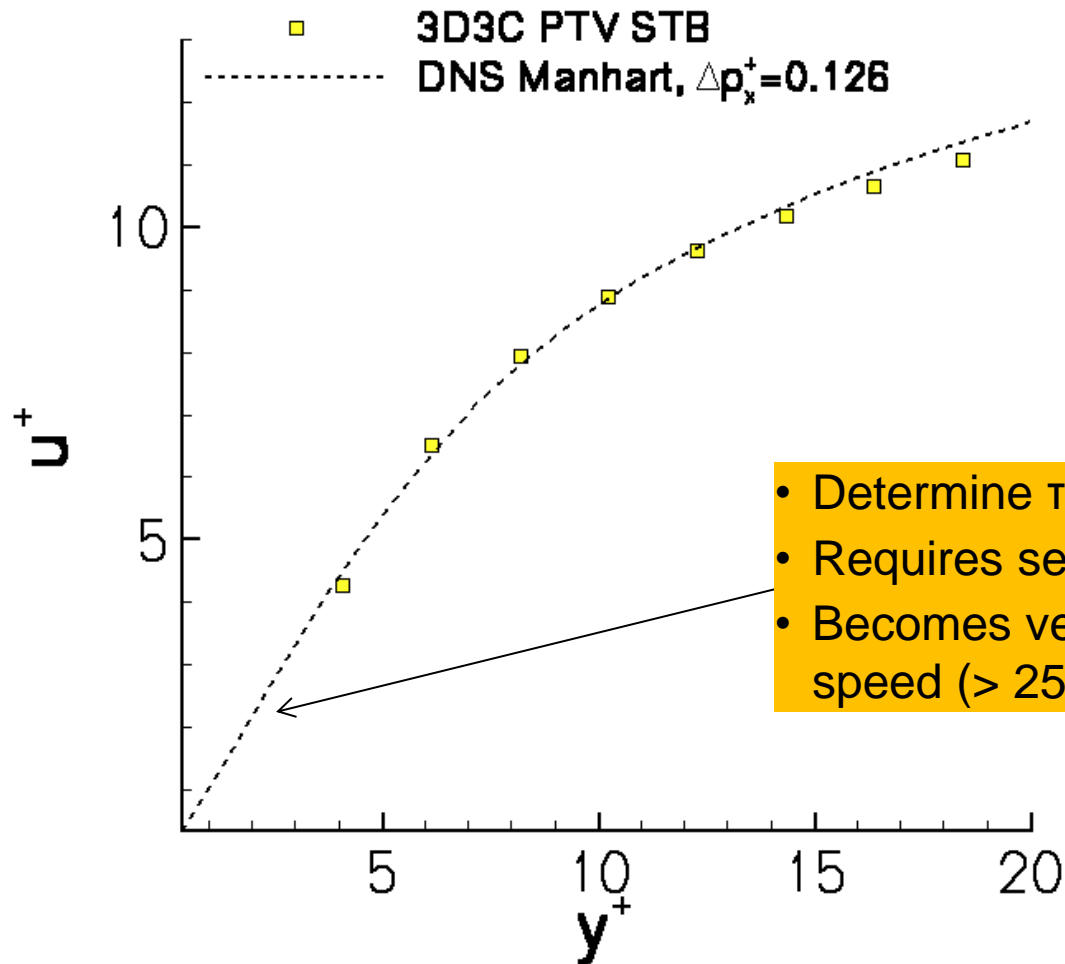


Input for wall-law scaling: Wall-shear stress

DFG RETTINA II experiment
 Microscopic PTV by N. Reuther (UniBw M)



Input for wall-law scaling: Wall-shear stress

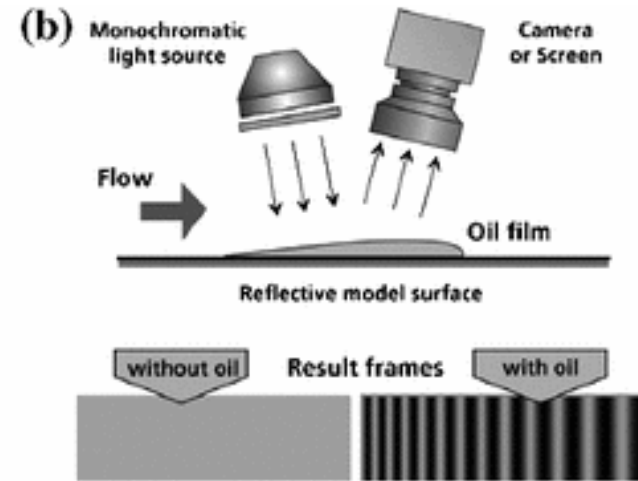
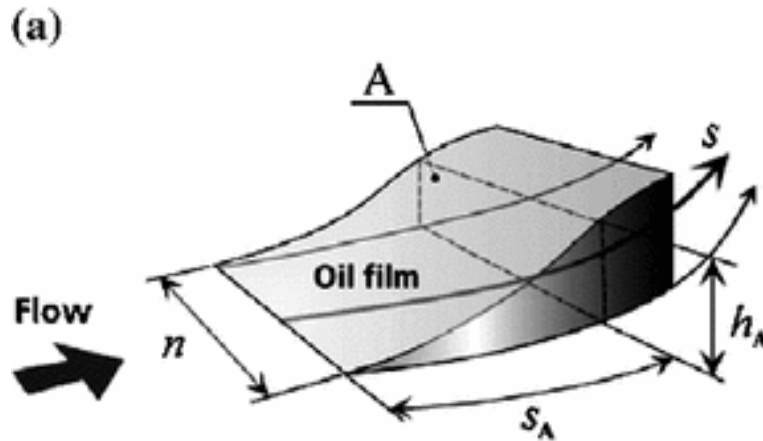


- Determine τ_w from the mean velocity profiles
- Requires several data points for $y^+ < 1.5$
- Becomes very complicated for high flow speed ($> 25\text{m/s}$)



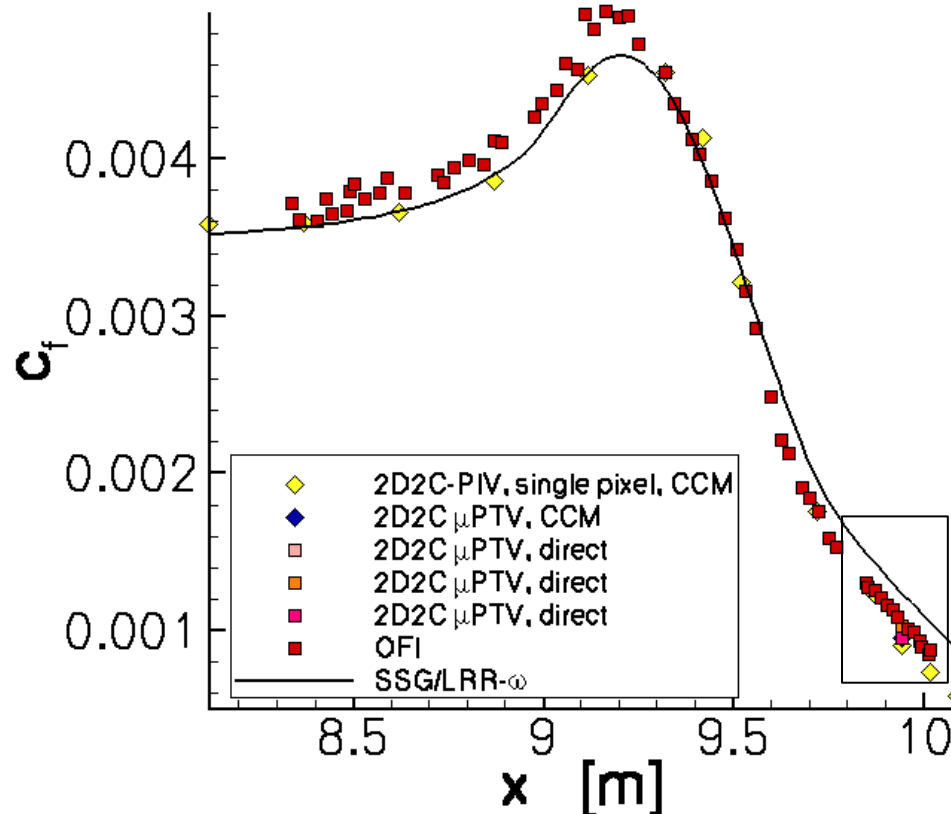
Need for additional (complementary) measurements

- Highly accurate measurement of wall shear stress τ_w
- Oil film interferometry
- Gave excellent data for RETTINA II experiment by Erich Schülein (DLR AS HGK)



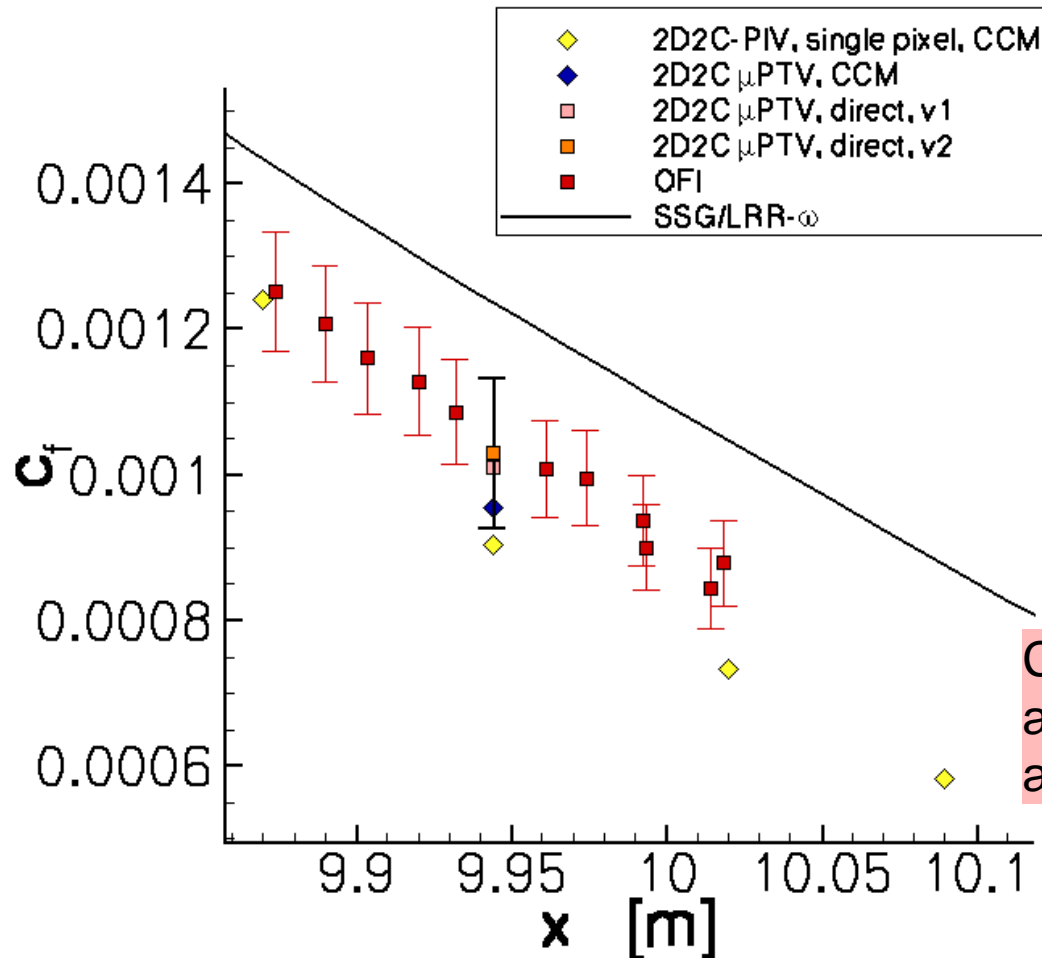
Comparison of PTV-direct versus Oil-film interferometry

- Evaluation of data for RETTINA II experiment was part of VicToria project
- Oil-film interferometry by Erich Schülein (DLR AS HGK), assisted by Nico Reuther (Uni Bw M)



Comparison of PTV-direct versus Oil-film interferometry

- Estimate of error bars for case $U=23\text{m/s}$



Summary & conclusion



Summary and conclusion

- We presented the work for the DLR VicToria experiment and the improvement of RANS turbulence models for adverse pressure gradients and the onset of separation
- Status of the work
 - ✓ Design of a high Re turbulent boundary layer exp with mild separation
 - ✓ Overview & detail PIV/PTV measurements performed and evaluated
 - ✓ Evaluation of a new wall law for adverse pressure gradient
 - ✓ Validation of modified SSG/LRR- ω RSM for the VicToria experiment
- A second measurement campaign is tentatively planned and would deliver important, missing complementary measurements
 - Information of 3D surface flow field and side wall separation (**oil film surface picture**)
 - **Oil film interferometry (OFI)** measurements for wall-shear stress
=> Needed for calibration of wall-law at APG towards separation
 - Measurement of details of the Reynolds stress transport equation (turbulent transport, dissipation) using recent improvements of the **3D3C PTV STB** method achieved during the VicToria project



Acknowledgement

- The experimental microscopic PTV data for the RETTINA II were measured by **Nico Reuther** and **Christian Kähler** (Uni Bw München)
- The OFI data for the RETTINA II experiment were measured by **Erich Schüle** (AS HGK) and assisted by Nico Reuther
- The funding of measurement campaign by **DFG** within „Investigation of turbulent boundary layers with pressure gradient at high Reynolds numbers with high resolution multi-camera techniques“ is gratefully acknowledged
- The funding of the geometry model of the RETTINA II experiment by **DLR AS-BS** is gratefully acknowledge
- Thanks to **Mike Zippert (DLR SHT)** for excellent cooperation in design and construction of the VicToria experiment



Thank you for your attention!

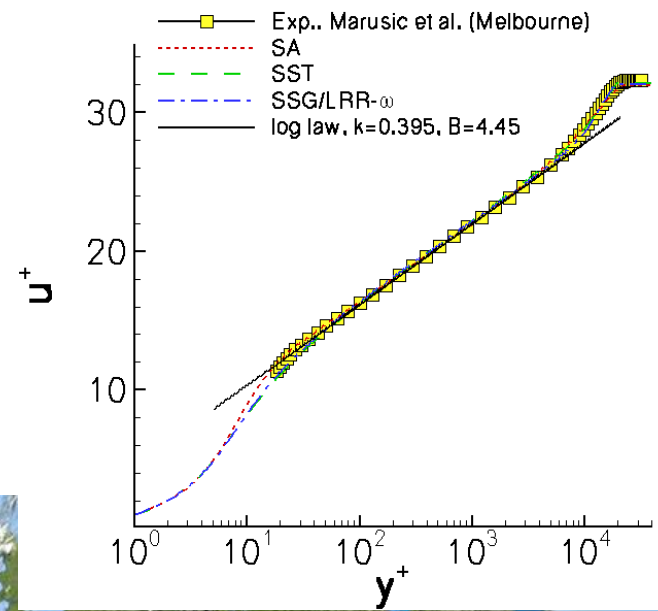
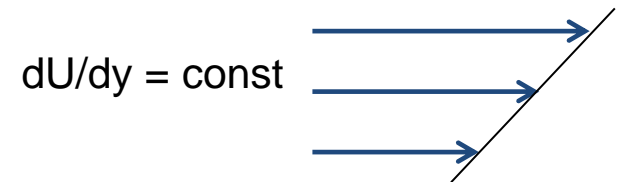
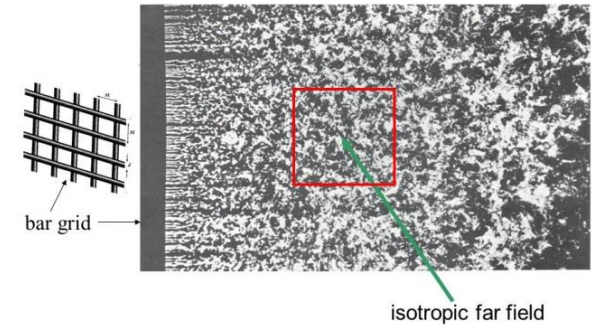
Questions ...?



State-of-the-art calibration of RANS models

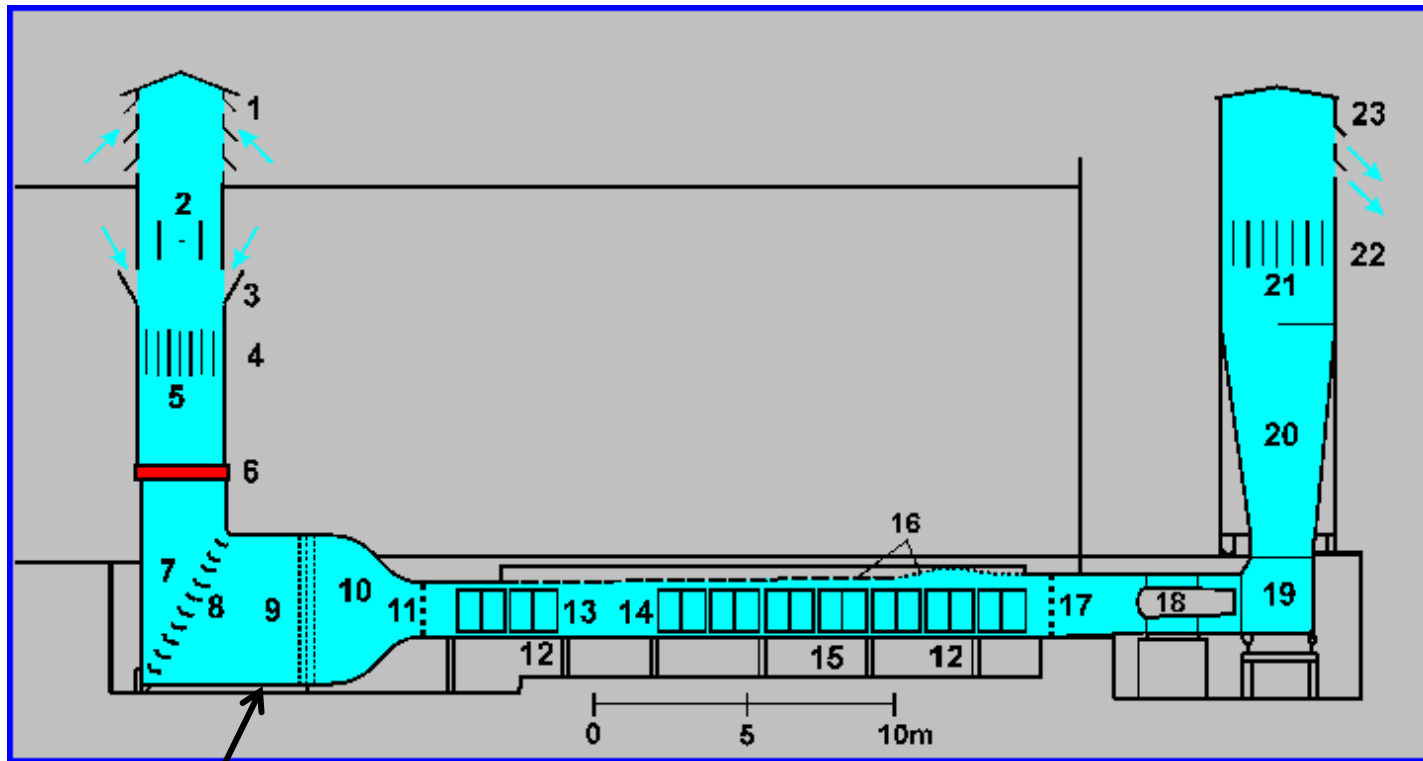
- Decaying isotropic turbulence (=turbulence downstream of a grid)
- Homogeneous shear flows (=flow with constant mean shear rate dU/dy remote from viscous walls)
- Turbulent boundary layer flow over a flat plate at zero pressure gradient: The log-law

Decaying isotropic turbulence behind a bar grid



Simulation of wind-tunnel characteristics of AWM

- Need correct boundary layer thickness in the test section
- Complicated flow history in open Eiffel wind tunnel

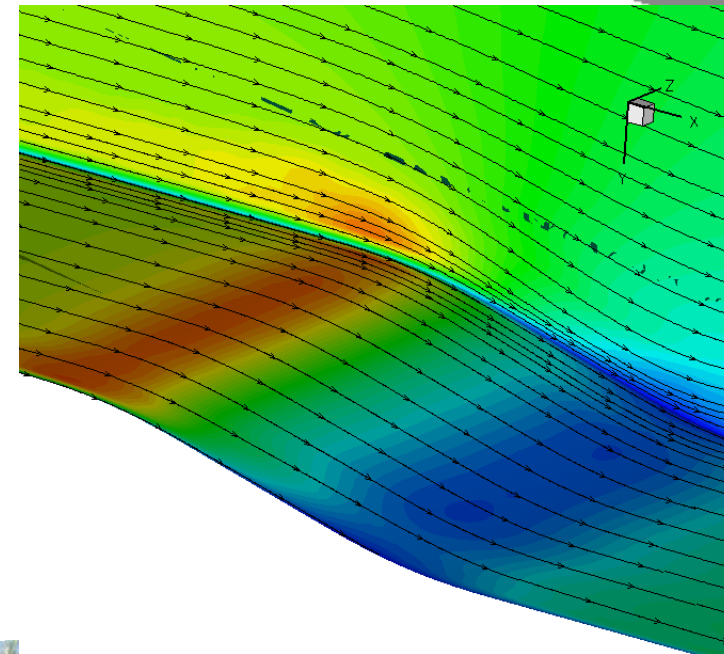
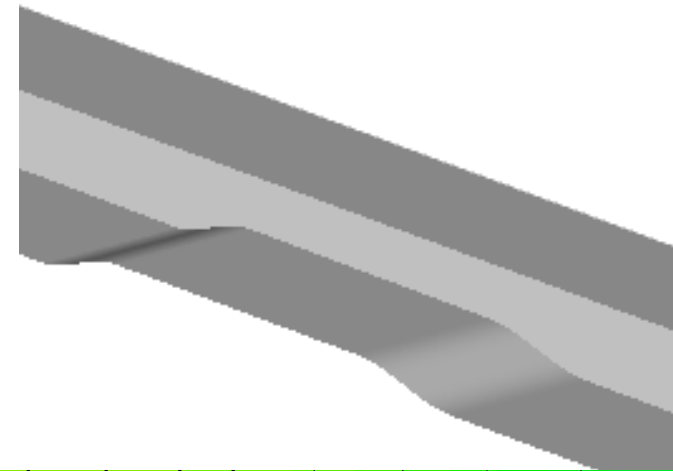
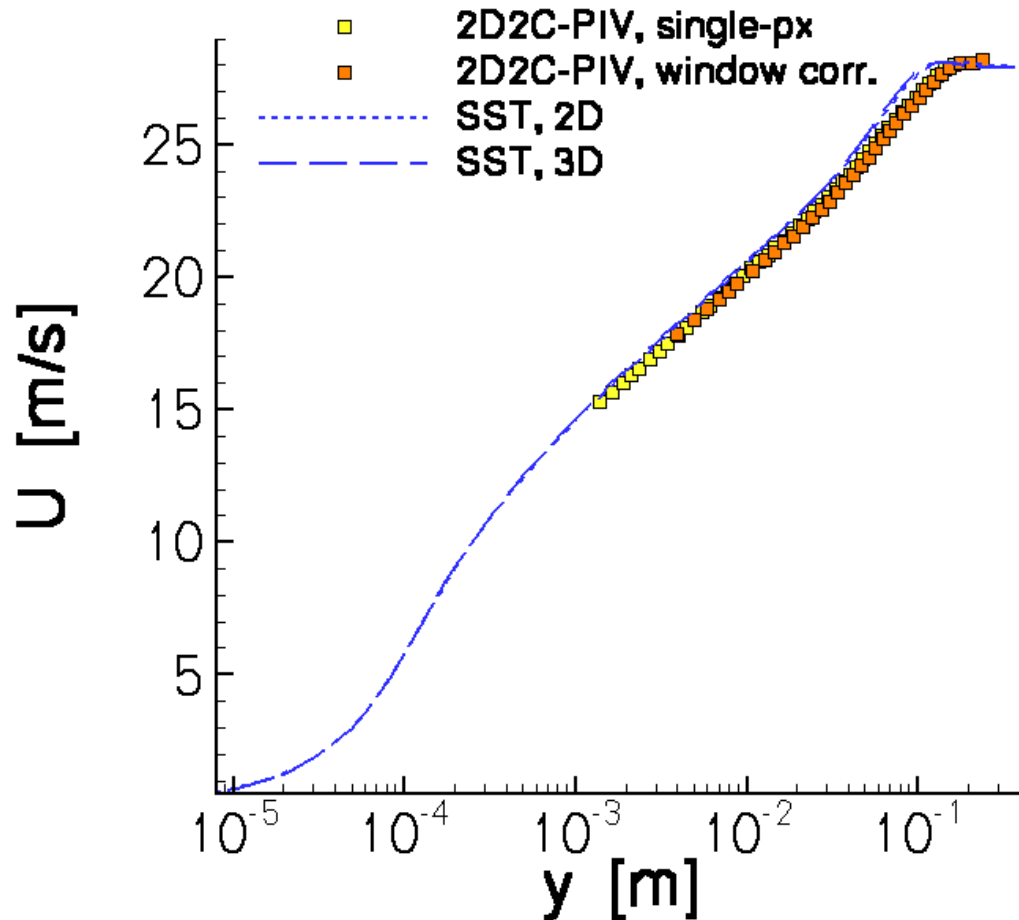


Complicated evolution of boundary layer thickness on wind tunnel walls



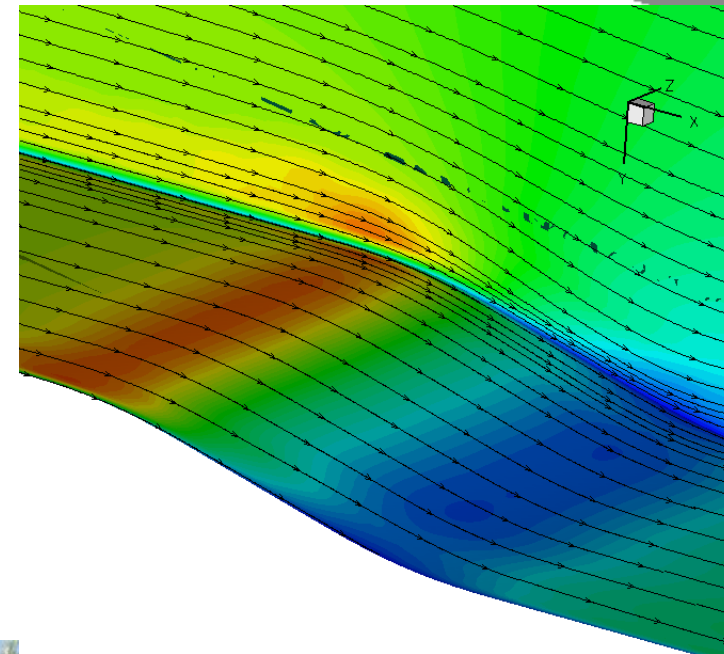
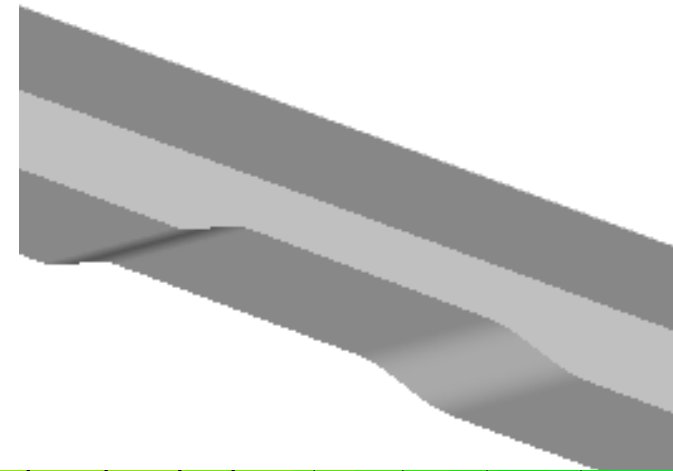
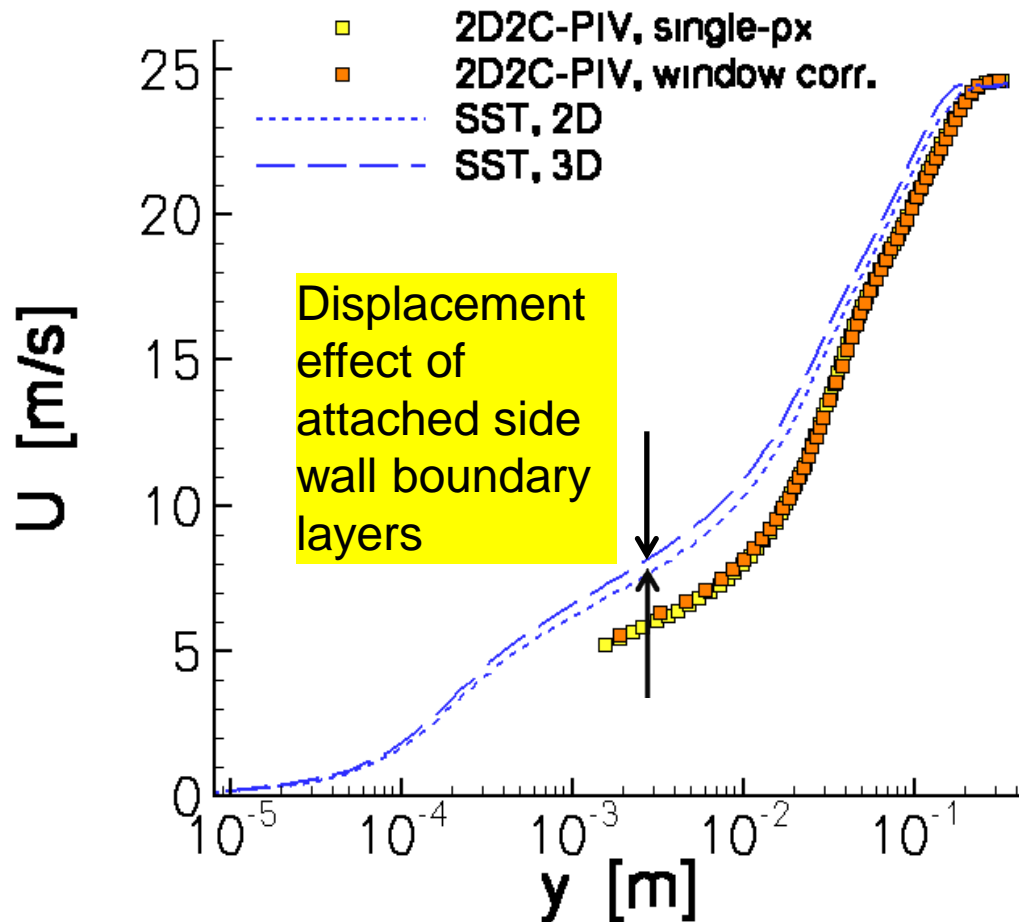
Estimate of side wall effects from RETTINA II exp

- Centerline position in ZPG region

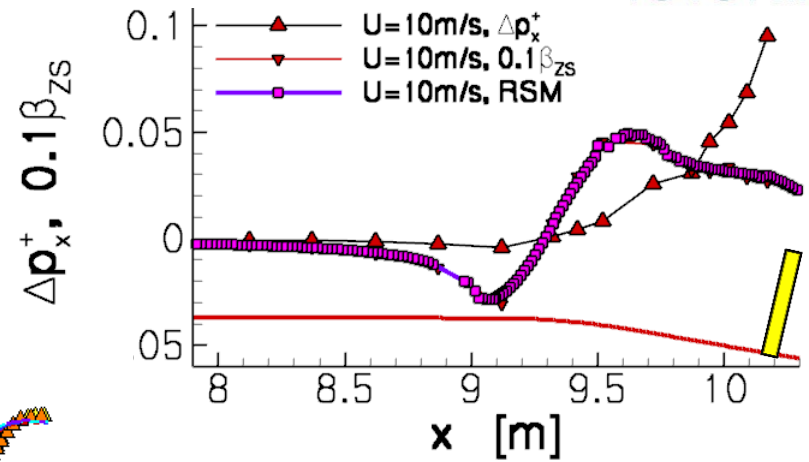
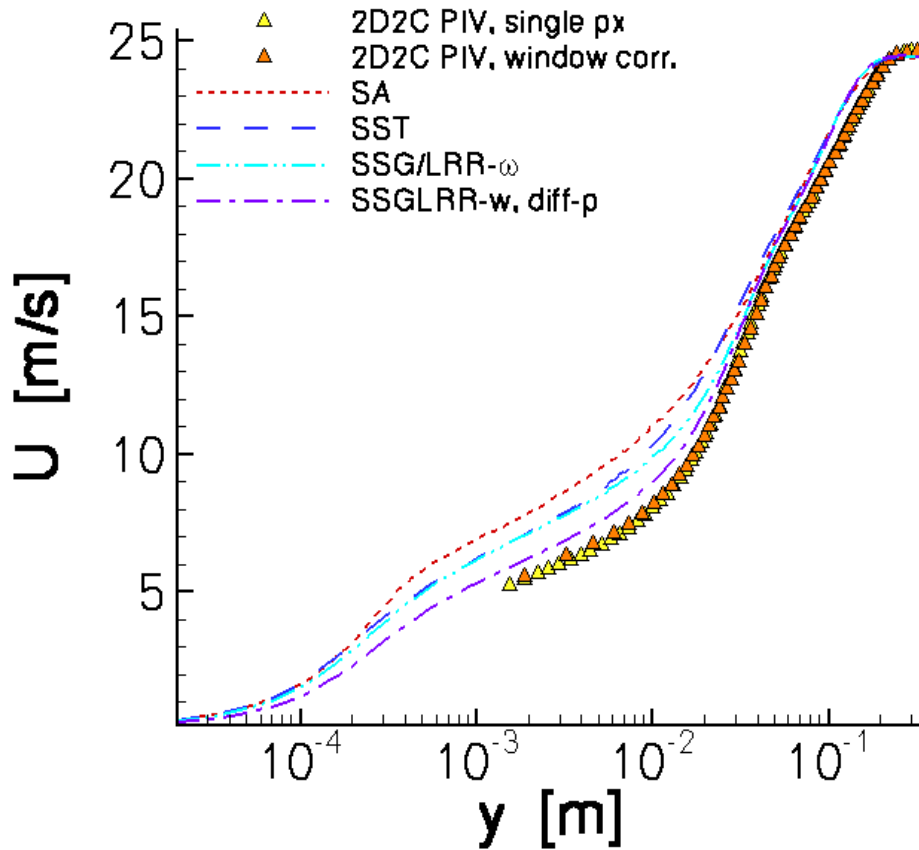


Estimate of side wall effects from RETTINA II exp

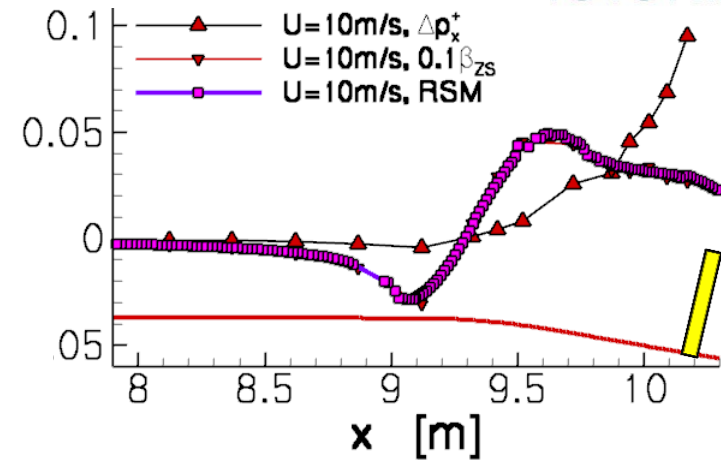
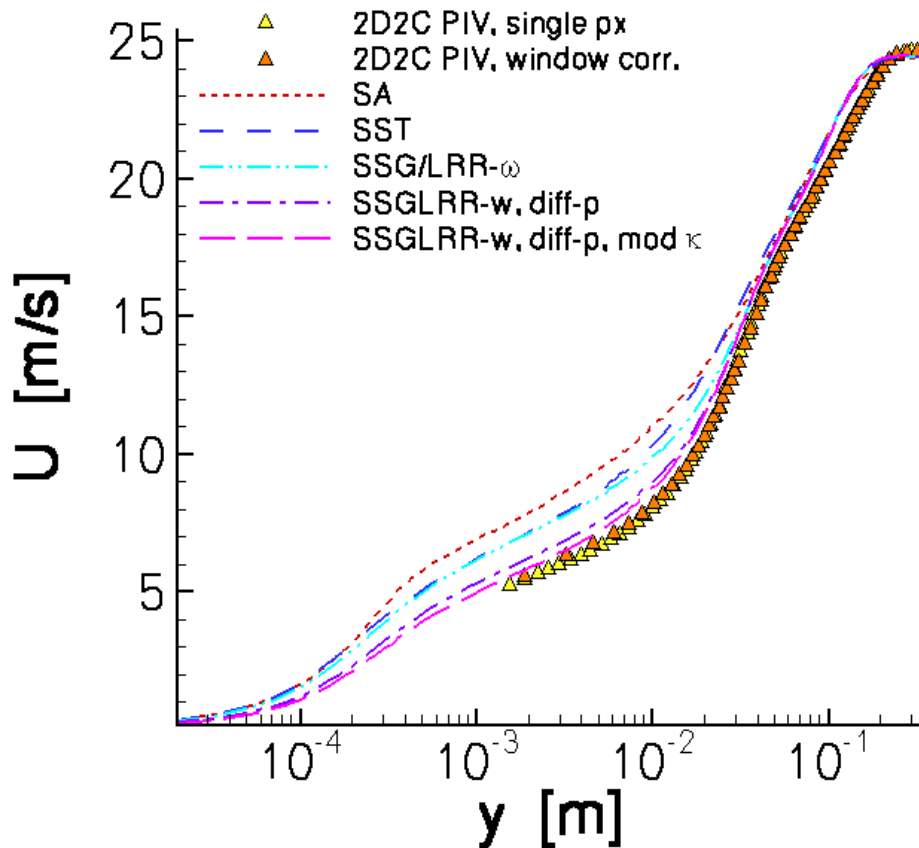
- Centerline position at mild APG, albeit side wall flow remains attached (no corner flow separation)



Results for RETTINA II experiment

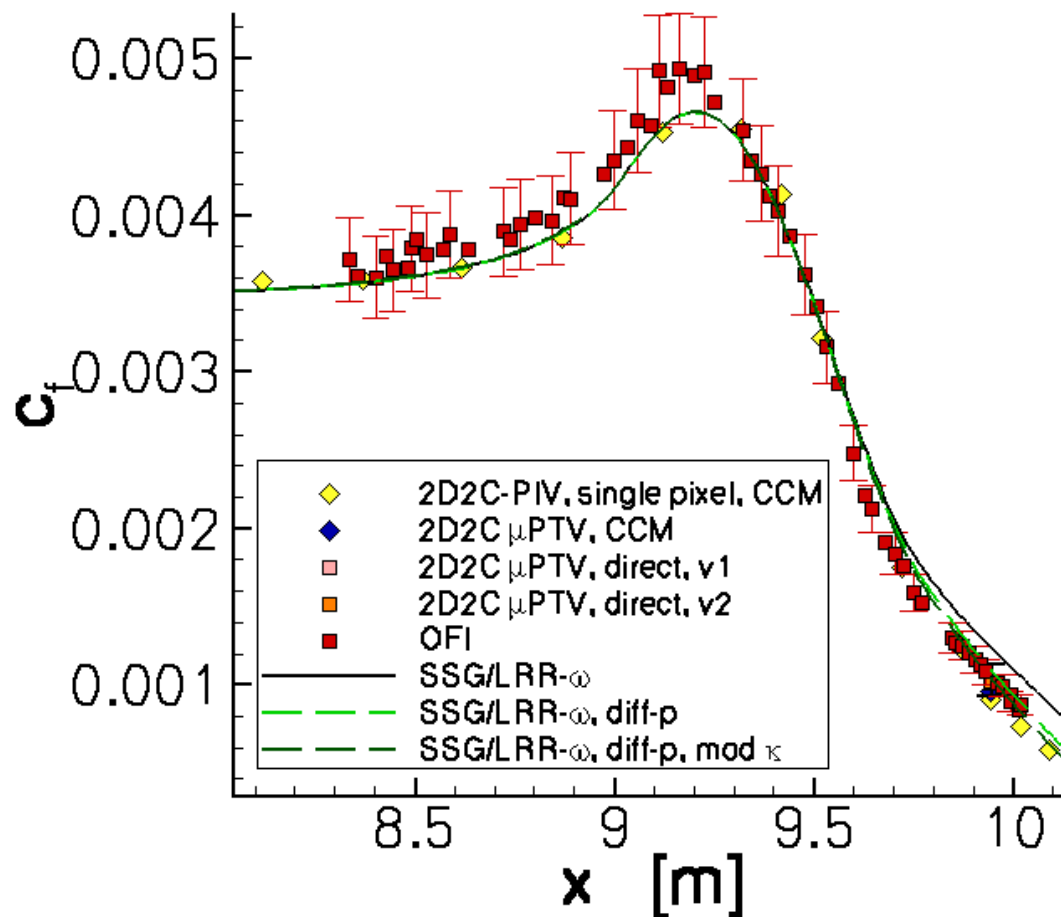


Results for RETTINA II experiment



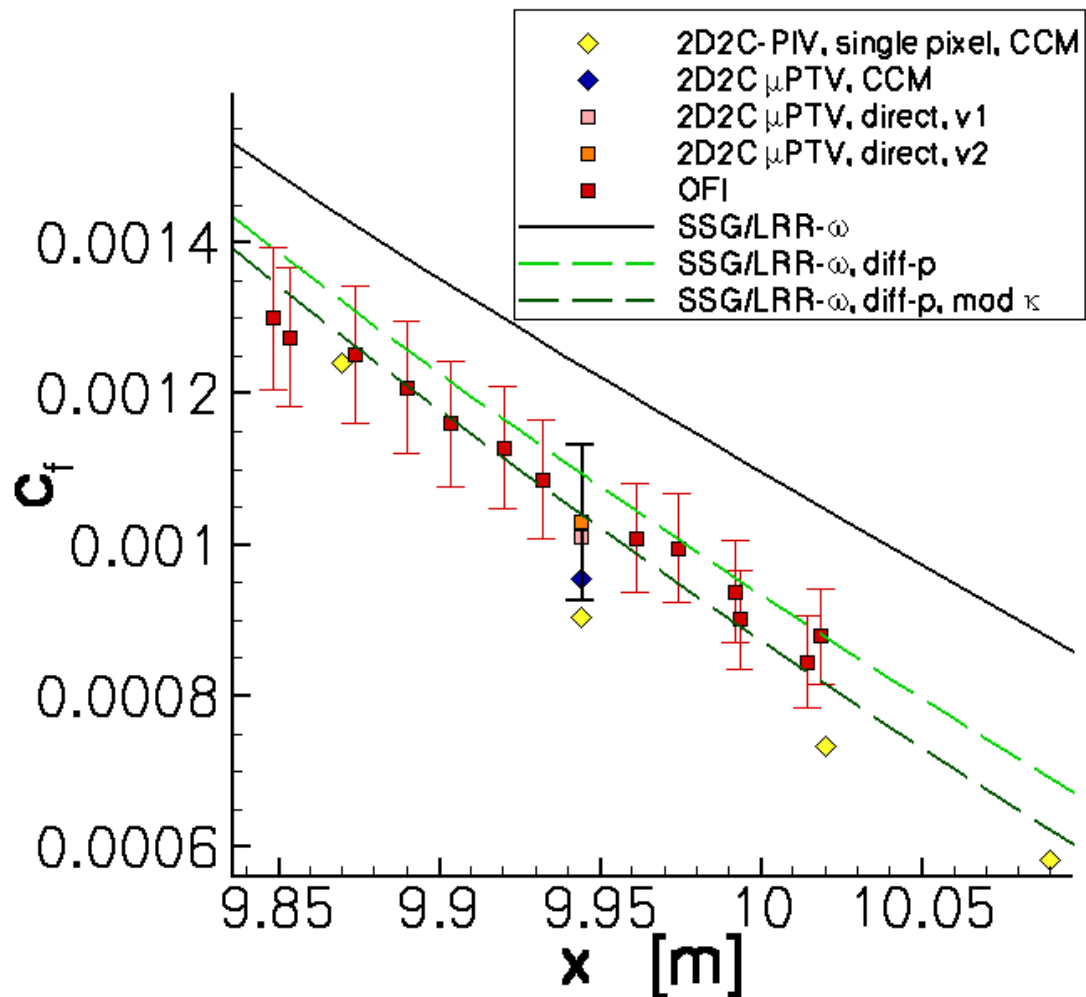
Results for RETTINA II experiment

- Case $U=23\text{m/s}$

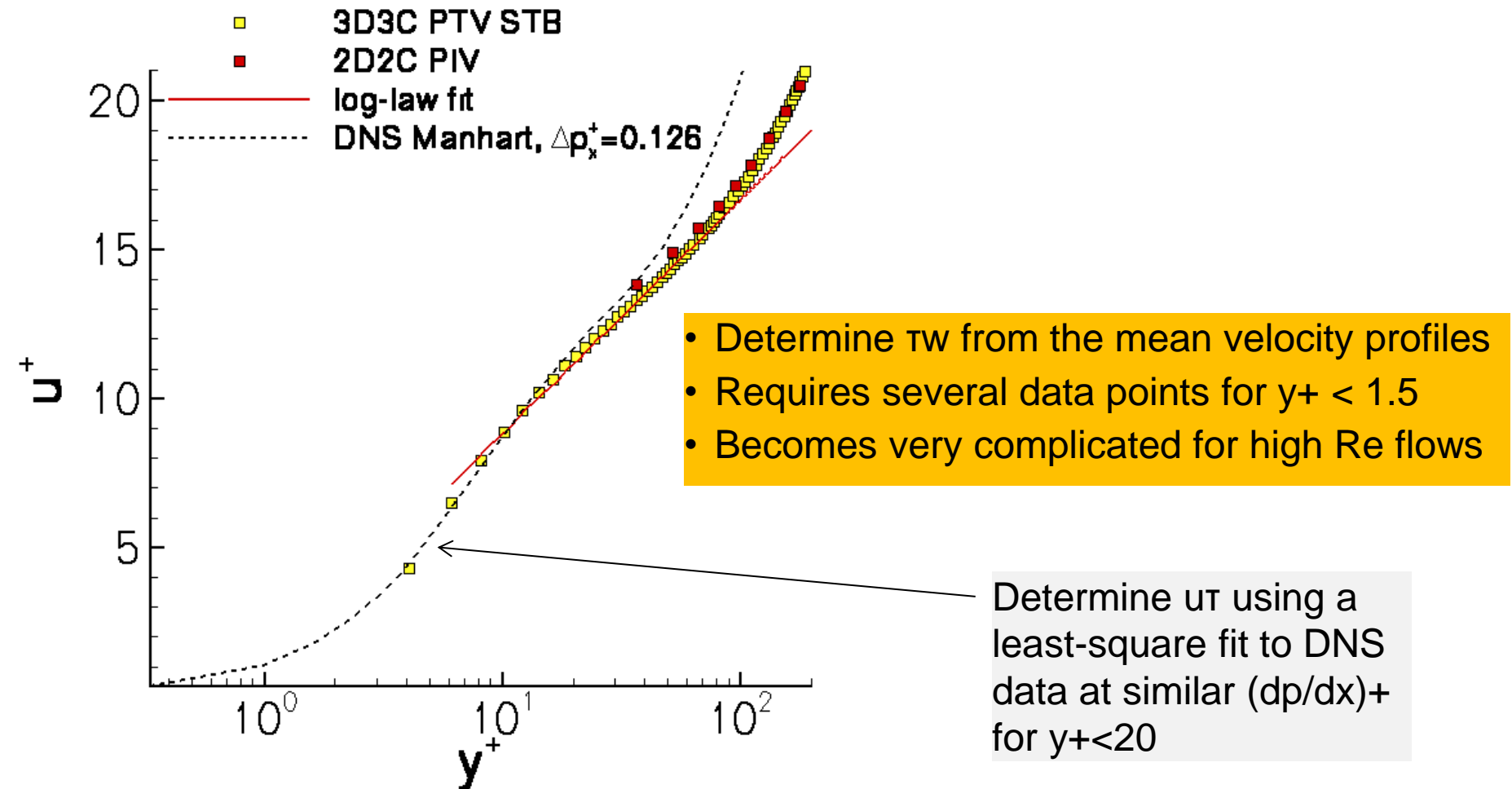


Results for RETTINA II experiment

- Case $U=23\text{m/s}$



Improved indirect method to determine wall-shear stress

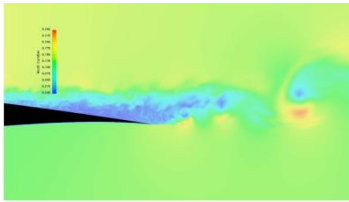


RANS turbulence modelling

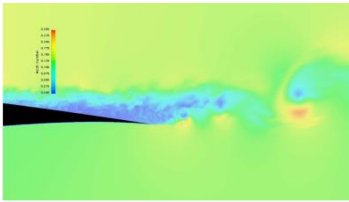
Laws of turbulence for statistically averaged data

Experiment number

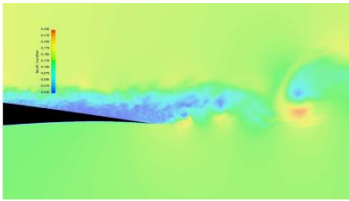
i=1



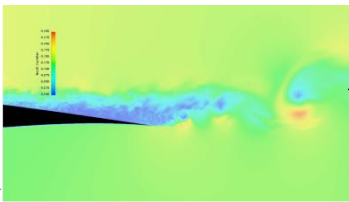
i=2



i=3



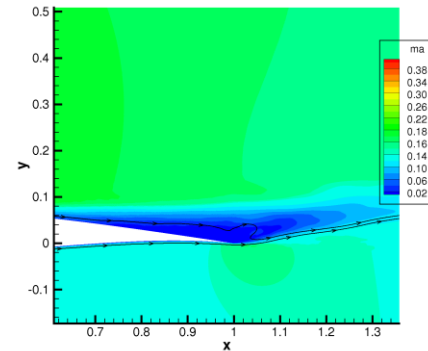
i=4



Average over an ensemble of N snapshots

$$\langle \vec{u}(\vec{x}, t) \rangle_N = \frac{1}{N} \sum_{i=1}^N \vec{u}^{(i)}(\vec{x}, t)$$

Averaged solution (=mean flow solution) looks smooth



Reynolds-averaged Navier-Stokes (RANS)

- Application of a statistical averaging operator to the Navier-Stokes equations gives the transport equation for the mean flow (RANS equations)

$$\frac{\partial}{\partial x_j} (U_i U_j) + \frac{1}{\rho} \frac{\partial P}{\partial x_i} - \frac{\partial}{\partial x_j} \left(\nu \left(\frac{\partial U_i}{\partial x_j} + \frac{\partial U_j}{\partial x_i} \right) - \langle u'_i u'_j \rangle \right) = 0$$



Reynolds-stress tensor

- averaged effect of velocity fluctuations



Summary: RANS equations

- Transport equation for the mean velocity

$$\frac{\partial}{\partial x_j} (U_i U_j) + \frac{1}{\rho} \frac{\partial P}{\partial x_i} - \frac{\partial}{\partial x_j} \left(\nu \left(\frac{\partial U_i}{\partial x_j} + \frac{\partial U_j}{\partial x_i} \right) - \langle u'_i u'_j \rangle \right) = 0$$

- Transport equation for the Reynolds stress tensor

$$U_k \frac{\partial}{\partial x_k} \overline{u'_i u'_j} = \mathcal{P}_{ij} + D_{ij}^\nu + \boxed{D_{ij}^t} + \boxed{D_{ij}^p} + \boxed{\Pi_{ij}} - \boxed{\epsilon_{ij}}$$

- Transport equation for the dissipation rate ω

$$U_j \frac{\partial \omega}{\partial x_j} = \boxed{P_\omega} - \boxed{\epsilon_\omega} + \boxed{D_\omega^\nu} + \boxed{D_\omega^t}$$

